

# **Internal Repair of Gas Pipelines Survey of Operator Experience and Industry Needs Report**

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Measurement Units -- SI Metric System of Units are the primary units of measure for this report followed by their U.S. Customary Equivalents in parentheses ( ).

Note: SI is an abbreviation for Le Systeme International d'Unites."

## ABSTRACT

A repair method that can be applied from the inside of a gas transmission pipeline (i.e., a trenchless repair) is an attractive alternative to conventional repair methods since the need to excavate the pipeline is precluded. This is particularly true for pipelines in environmentally sensitive and highly populated areas.

The objectives of the project are to evaluate, develop, demonstrate, and validate internal repair methods for pipelines; develop a functional specification for an internal pipeline repair system; and prepare a recommended practice for internal repair of pipelines. The purpose of this survey is to better understand the needs and performance requirements of the natural gas transmission industry regarding internal repair.

A total of fifty-six surveys were sent to pipeline operators. A total of twenty completed surveys were returned, representing a 36% response rate, which is considered very good given the fact that tailored surveys are known in the marketing industry to seldom attract more than a 10% response rate.

The twenty survey responses produced the following principal conclusions:

1. Use of internal weld repair is most attractive for river crossings, under other bodies of water (e.g., lakes and swamps) in difficult soil conditions, under highways, under congested intersections, and under railway crossings. All these areas tend to be very difficult and very costly if, and where, conventional excavated repairs may be currently used.
2. Internal pipe repair offers a strong potential advantage to the high cost of horizontal direct drilling (HDD) when a new bore must be created to solve a leak or other problem in a water/river crossing.
3. The typical travel distances required can be divided into three distinct groups: up to 305 m (1,000 ft.); between 305 m and 610 m (1,000 ft. and 2,000 ft.); and beyond 914 m (3,000 ft.). In concept, these groups require pig-based systems; despoiled umbilical systems could be considered for the first two groups. For the last group a self-propelled system with an onboard self-contained power and welding system is required.
4. Pipe size range requirements range from 50.8 mm (2 in.) through 1,219.2 mm (48 in.) in diameter. The most common size range for 80% to 90% of operators surveyed is 508 mm to 762 mm (20 in. to 30 in.) diameter, with 95% using 558.8 mm (22 in.) diameter pipe.

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## 1.0 INTRODUCTION

A repair method that can be applied from the inside of a gas transmission pipeline (i.e., a trenchless repair) is an attractive alternative to conventional repair methods since the need to excavate the pipeline is precluded. This is particularly true for pipelines in environmentally sensitive and highly populated areas. Several repair methods that are commonly applied from the outside of the pipeline are, in theory, directly applicable from the inside. However, issues such as development of the required equipment to perform repairs remotely and mobilization of equipment through the pipeline to areas that require repair need to be addressed. Several additional repair methods that are commonly applied to other types of pipelines (e.g. gas distribution lines, water lines, etc.) also have potential applicability for internal repair of gas transmission pipelines. Many of these require further development to meet the requirements for repair of gas transmission pipelines. The objectives of the project are to evaluate, develop, demonstrate, and validate internal repair methods for pipelines; develop a functional specification for an internal pipeline repair system; and prepare a recommended practice for internal repair of pipelines. The purpose of this survey was to better understand the needs and performance requirements of the natural gas transmission industry regarding internal repair.

## 2.0 EXECUTIVE SUMMARY

A repair method that can be applied from the inside of a gas transmission pipeline (i.e., a trenchless repair) is an attractive alternative to conventional repair methods since the need to excavate the pipeline is precluded. This is particularly true for pipelines in environmentally sensitive and highly populated areas.

The objectives of the project are to evaluate, develop, demonstrate, and validate internal repair methods for pipelines; develop a functional specification for an internal pipeline repair system; and prepare a recommended practice for internal repair of pipelines. The purpose of this survey was to better understand the needs and performance requirements of the natural gas transmission industry regarding internal repair.

A total of fifty-six surveys were sent to pipeline operators. A total of twenty completed surveys were returned, representing a 36% response rate, which is considered very good given the fact that tailored surveys are known in the marketing industry to seldom attract more than a 10% response rate.

The twenty survey responses produced the following conclusions:

1. Use of internal weld repair is most attractive for river crossings, under other bodies of water such as lakes and swamps, in difficult soil conditions, under highways and in congested intersections, and under railway crossings. All these areas tend to be very difficult and very costly, if, and where conventional excavated repairs may be currently used.
2. Internal pipe repair offers a strong potential advantage to the high cost of HDD when a new bore must be created to solve a leak or other problem in a water/river crossing.
3. The typical travel distances required can be divided into three distinct groups: up to 305 m (1,000 ft.); between 305 m and 610 m (1,000 ft. and 2,000 ft.); and beyond 914 m (3,000 ft.). In concept, all these systems would be pig-based. Systems with despooled umbilicals could be considered for the first two groups. For the last group a self-propelled system with an onboard self-contained power and welding system is required.
4. Pipe size range requirements range from 51 mm (2 in.) through 1,219 mm (48 in.) in diameter. The most common size range for 80% to 90% of operators surveyed is 508 mm to 762 mm (20 in. to 30 in.) diameter, with 95% using 559 mm (22 in.) diameter pipe.
5. Based on the frequency of expected use by many operators, the issue of acceptable system cost for a deployable solution could best be tackled through selling such technology as an additional service through existing "smart pig" vendors/operators.
6. There has been almost no use of internal repair to date and the concept is currently fairly alien to pipeline operators. Even the potential for internal repair of external damage using such a system needs further promotion/education within the industry as a whole.
7. Most operators were open to the economic potential an internal repair system may offer in terms of reducing interruption to product flow, particularly if they did not have looped lines.
8. The top three items of concern for selecting a repair method were cost, availability of the repair method (time/cost), and the position of the defect(s).
9. A wide range of pipe coatings were cited as being deployed in the field. The top three mentioned were fusion bonded epoxy (FBE), coal tar, and concrete/POWERCRETE®.
10. The majority of operators considered the ability for the pipeline to remain in service while the repair was conducted to be very important.
11. Radiographic testing (RT) is by far the most accepted method for pipeline nondestructive evaluation (NDE). Ultrasonic testing (UT) was the second most common process cited.

## **3.0 EXPERIMENTAL**

This part of the project was a survey and so did not involve an experimental procedure or equipment in the conventional sense.

### **Survey Development**

The survey (Appendix A) was sent to a wide range of gas transmission companies, both member companies of the Pipeline Research Council International (PRCI), and also to other companies within the industry (Appendix B). The list of contacts was built up from the PRCI Materials Committee Roster, a list of other gas companies from the <http://www.ferc.gov/gas> companies/pipelines web site, and a web-based list of gas company executives, in addition to personal contacts within the industry. An extensive series of phone calls were made to establish the most appropriate person or persons at each company to whom to send the survey, and to establish whether a central point of contact (POC) or multiple recipients was preferred. In most cases, the appropriate staff member at parent companies with several pipeline subsidiaries preferred to be a central POC, gathering this and sending the feedback to EWI through one survey for their company.

Email addresses were gathered for all the survey recipients such that the survey could be sent, completed, and returned, electronically.

## **4.0 RESULTS AND DISCUSSION**

A total of fifty-six surveys were sent out mostly to the single main identified POC at each company. In two cases, three surveys were sent to individuals within a single company. A total of twenty completed surveys were returned, representing a 36% response rate. Four additional companies responded that they did not plan to complete the survey, due to construction or other time pressures. The response rate of 36% is considered very good given the fact that tailored surveys are known in the marketing industry to seldom attract more than a 10% response rate.

The following companies responded to the survey:

CenterPoint Energy	Texas Eastern Transmission Corporation
- Mississippi River Transmission System	Maritime & Northeast Pipeline LLC
Reliant Energy Gas Transmission System	Dynergy Midstream Pipeline, Inc.
EI Paso Corporation	- Venice Gathering System, LLC
- ANR Pipeline Company	ExxonMobil Pipeline Company
ANR Storage Company	Foothills Pipe Lines Ltd
- Blue Lake Gas Storage Company	Gasunie, Netherlands
- Colorado Interstate Gas Company	Great Lakes Gas Transmission Company
EI Paso Natural Gas Company	Iroquois Gas Transmission System, LP
EI Paso Field Services	Keyspan Energy
EPGT Texas Pipeline, LP	Nisource
- Gulf States Transmission Company	- Columbia Gas Transmission Corp. Co.
- High Island Offshore System	- Columbia Gulf Transmission Co.
- Mojave Pipeline Company	- Crossroads Pipeline Company
- Petal Gas Storage Company	- Granite State Gas Transmission, Inc.
- Southern Natural Gas Company	Oncor Group
- Tennessee Gas Pipeline Company	- Oncor Gas
- Wyoming Interstate Company, Ltd.	- TXU Gas/TXU Lone Star Pipeline
Young Gas Storage Company, Ltd.	Ozark Gas Transmission System
Dominion Transmission, Inc.	Pacific Gas and Electric Gas Transmission–Northwest Corporation
Duke Energy Gas Transmission	Sempra Energy Utilities/Southern California Gas Company
- Algonquin Gas Transmission Company	Southwest Gas Corporation
Algonquin LNG, Inc.	TransGas
East Tennessee Natural Gas Company	
Egan Hub Partners, LP	

In the following sections, the survey responses are summarized in categories that correspond to the sections and questions asked in the survey itself. The questions are repeated (and presented in bold type to distinguish them) within each section to avoid the need to continually refer to Appendix A. In most instances, the data collected is presented in the form of a bar chart for easy interpretation.

Most respondents answered all the survey questions, but this was not always the case. As such, in many cases there were twenty responses to a particular question, in others there were less, and in some cases, such as the types of coatings used on pipelines, there were many more, since most companies have used several coating types over the years.

## **Survey Responses**

### **Part 1 – Currently-Used Repair Methods**

#### **1. Describe the corrective actions your company has taken due to degradation (corrosion, cracking, etc.) of transmission pipelines, especially repair or replacement actions.**

Figure 1 summarizes the responses received. The most common type of repair is a welded external steel sleeve which was mentioned fourteen times, followed closely by "cut-out and replace" which was listed thirteen times. ClockSpring®, grind-out repairs, and composite wraps were all mentioned eight times.

One response summarized the company's perspective in the following fashion: cut-out and replace cylinder (seldom), full encirclement steel sleeves (most common), direct deposition of weld metal (seldom, but frequency may increase), grinding to remove gouges (common), and welding a plugged fitting like a Threadolet over the damage.

After the degradation is detected by whatever means, repair protocols are used. For general corrosion these include steel sleeves or composite sleeves. For stress corrosion cracking (SCC), gouges, and sharp corrosion profiles, grinding is often used. Typically gouges are ground until the cold worked material has been removed and are sleeved where necessary. For cracks, much of the time these are cut out, however, there are times that cracks are ground out using in-house protocols. Repair of dents is carried out with steel reinforcement sleeves. All respondents indicated that excavations and repairs involve the replacement of the existing coating with liquid applied epoxy coating.

One reply indicated that the first step was evaluation to ASME B31G. For repairs needed in lines that can be taken out of service, the solution is to either replace the damaged section as a "cylinder" or attach a sleeve. In the past, sleeves were exclusively steel, as technology has evolved, fiberglass wraps have been used. For low pressure lines leak clamps are used where appropriate.

In the case of internal corrosion, on-stream cleaning, chemical treatment, in-situ coating and in-situ polyethylene (PE) sleeve repairs have been applied. Recently, an internal repair approach of a 914 m (3,000 ft.) long, 607 mm (24 in.) diameter, river crossing was considered (<http://www.unisert.com>) using an internal fiberglass sleeve supported by a grouted annulus. Ultimately, a new HDD river crossing option was selected because of loss of cover in the river bottom.

Another respondent stated that a variety of repair methods are used, with the selection of the method dependent on several factors including class location, type of damage, operating pressure, and operational considerations.

Corrosion is repairable by a variety of repair methods dependent upon the conditions. Options include band clamp, mechanical sleeve, weld-on sleeve, ClockSpring®, and replacement. External repair methods used by one company include sleeves (reinforcing, pressure containment), grinding (cracks) and pipe replacement. Another company indicated that they normally use ClockSpring® to re-enforce external corrosion areas, whereas cracks that exceed code limitations require an automatic cut-out (which is the last option to consider). Yet another company uses external repair techniques that include a simple blast and recoat, grind and recoat, ClockSpring® repair, welded sleeve repair or pipe replacement.

**2. Have you used methods other than external sleeving or pipe replacement to repair different types of degradation?**

The responses to this question were split 50% "no" and 50% "yes." The "yes" responses typically gave examples which are summarized as follows:

- Grinding is used to remove gouges (common), cracks, SCC, and sharp anomalies.
- Plugs are fitted and welded over the damage, e.g. a Threadolet.
- Composite wraps are used.
- ClockSpring® is used.
- Direct deposition welding has been used to repair wall loss

- “Encapsulating” a malfunctioning or defective area has been used.
- Taps have been used for small defects.
- Leak clamps have also been used.

Seven of the responses mentioned grinding of one type of defect or another and was the most common other type of repair. Three examples of different types of welding solution were cited, of which only one involved direct deposition of weld metal on the outside of the pipe.

#### **4. What criteria (including ease of pipe access) affect choice of the specific repair method to be used?**

The compiled answers to this question are represented in Figure 2 and show twelve responses, of which cost and the availability of the repair method were those most frequently cited. The next important consideration is the position of the defect, and whether the line had to be out-of-service as the next most frequently mentioned criteria.

One respondent summarized the evaluated criteria as follows:

- Consequence of failure
- Position of defect (on bend, weld, top/bottom, etc.)
- Impact of a pressure restriction
- Cost of repair
- Type of defect
- Availability of repair method, crews, expertise, etc.

Another response listed the following criteria:

- Maximum allowable operating pressure (MAOP) and possible future increases
- Maximum operating pressure (MOP) at time of repair
- Pipeline specified minimum yield strength (SMYS)
- Downstream demand
- Ability to remove the pipeline from service
- Cost
- Projected life of the pipeline

The size of flaw (surface area), the ability to shut in and replace the damaged section, the ratio of estimated failure pressure to MAOP, and the ability to stop additional degradation (in the case of internal corrosion) were stated as important criteria by another respondent.

Other responses follow:

- Must make repairs without taking the line out of service since it is not looped.
- Need to have the line out-of-service or at less pressure during repair work
- Can the pipeline be taken out-of-service, gas loss?
- Leak history
- Corrosion records
- ILI (in-line inspection) logs
- Cost (access, out-of-service time, mobilization time, etc.)
- Reliability (how reliable is the repair method to fix the problem, permanent repair, temp. repair)
- Safety issues
- Operator qualification
- Type and depth
- Material properties and type of pipes, e.g. electric resistance welded (ERW), seamless, etc.
- Coating
- Location (proximity to housing or public facilities)
- Operational timing (ability to take line out-of-service, i.e. impacts to customers and system)
- Type or severity of defect, access to site, time constraints in regards to length of line outage or restriction, soil conditions (e.g. swamp, rock, etc.), environmental issues (wetlands, streams, etc.).
- Pressure, Department of Transportation (DOT) status (we operate many rural gathering lines), contents of line, risk to public
- Location, pipe condition, operating pressure/SMYS, pipe geometry (e.g. straight, over-bend, sag, etc.)

## 5. Comments pertaining to currently used repair methods.

Not unexpectedly, comments ranged from:

- Most of our line has easy access
- The use of sleeves for the repair of external flaws has been satisfactory to date
- Most existing methods have been effective
- The ClockSpring® has been a very useful repair method in the last few years
- Many are very difficult in swamp or underwater locations

Cut-out repair is considered the last resort due to flow disruption and overall cost. External faults are more readily repaired using sleeves than internal anomalies. Internal damage requiring repair in bends equate to a pipe replacement. The threshold for pipe replacement versus repair decreases once the first replacement in a section is justified.

Live repair methods require a reduction in operating pressure. Normally the excavation trench requires tight sheeting and shoring, a certified welder, and qualified maintenance welding procedure with low hydrogen procedures (e.g. E7018 low hydrogen electrodes).

## Part 2 – Use/Potential Use of Internal Repair

### 1. Has your company attempted repair of a transmission line from inside the pipe?

Of the nineteen responses to this question, only one was "yes." Another company indicated that they considered the use of the Pacific Gas & Electric (PG&E) tool for weld repair on the internal diameter, but the expense was said to be large and the diameter range was limited. Other companies raised the question of how to ensure the quality of the repair.

#### If so, describe the repair(s)

Plastic tight liners were used and for lower pressure lines (less than 100 psig MAOP) slip lined plastic liners have been used. Both of these methods require the line to be out of service when repair is made.

**2. There are many factors that affect the decision to repair or replace pipe. What circumstances would favor performing a repair from inside the pipe using only one or two excavations rather than excavating the entire length of pipe?**

Figure 3 shows the primary factor for choice of an internal repair method is road and river crossings. Confidence in repair method, presence of numerous but localized areas of damage, inability to excavate large areas because of environmental permitting issues, economics/cost and availability of a proven, industry (and regulator) accepted internal method were also factors mentioned.

Specific comments follow:

- Depending on the depth of burial and the presence of over-bends, sag bends or side-bends or road/river crossings etc., then an internal repair may be much more preferable than cutting out the piece of affected pipe. Single barrel pipelines (versus looped lines) are more difficult to remove from service (customer interruption).
- Factors, such as, class location, environmentally sensitive areas, in crossings, under waterways or rugged terrain would be some of the major factors influencing this decision; an anomaly found inside a casing might be (a factor), under a road, irrigation canal, or railroad tracks; difficult to excavate locations (e.g. rocky conditions, caliche soils, etc.); and cost would be another factor influencing the decision. This potential technology would also be useful for locating and repairing internal wall loss identified by ILI inspections without excavation of the entire pipeline and numerous cuts to the line.
- Property damages, contractor costs, inaccessible right-of-way, lack of temporary workspace, road, railroad, and stream crossings sometimes must be replaced just because indicated damage cannot be directly measured highway crossings, railroad crossings, and heavy traffic intersections.
- Highly congested areas that impact risk to other pipelines or utilities and proximity to structures.
- Possibly a pipeline under water or a permanent structure where the pipeline is not easily accessible
- Where the pipe repair is located under a road or body of water where access is limited.
- Pipelines that are under paved areas, or in narrow or confined rights-of-way where space is limited. Crossings at roads, railroads, lakes, and rivers, and water cover, such as, marsh or swamp.

- If the cost of an internal repair plus the outage restriction was less than the cost of an external repair. For example, if the defect was in the middle of a major water crossing or swamp which would normally require ice road construction for access.
  - High traffic areas
  - Federal, state, city or county roadway restoration requirements
  - Environmental concerns
  - Railway crossings

3. **If the technology were available to perform a repair from the inside, would your company consider using the technology?**

One "no" response was received. The other seventeen responses were "yes" and some were qualified with additional comments as follows:

- We would want to review testing and possibly witness a demonstration
- Only if proven
- If cost is reasonable
- Particularly if DOT compatible
- Depending on the site-specific conditions

One response indicated that the company transports non-corrosive natural gas, so the probability of an internal flaw is highly unlikely. While this may be true for many companies in terms of internal corrosion, it misses the point that the internal repair can be used for repair of external damage.

**If so, for what application(s) – e.g., specific geographic locations and special situations?**

Figure 4 summarizes the answers to this question. River crossings and populated areas with highway crossings were most frequently cited. Use for repair of flaws found by pigging, included internal or external corrosion pitting, gouges, seam or weld flaws (if detectable by pigging).

Seven responses mentioned river crossings and this was the most common response to this question. Others cited pipelines that are under paved areas, or in narrow or confined rights-of-way where space is limited, crossings at roads, railroads, lakes, swamp areas, and difficult access due to physical barriers inherent to high population density and congested areas (e.g., numerous utilities, building, streets, etc.).

One response mentioned concerns regarding the use of internal repair on a direction bored crossing of a freeway, because of unknown future cathodic protection (CP) effectiveness after welding.

Another response referred to applications where it is not cost effective to repair or replace the pipe conventionally, provided the internal repair is an equivalent repair. Probably the best application in this case would be offshore.

4. **At least one excavation will be required to insert the internal repair device into the pipe. From this excavation, the repair device could travel in each direction from the excavation. About how far from the insertion point should the repair device be able to travel?**

Answers ranged from 15 m (50 ft.) to 113 km (70 miles); the latter for offshore operation, with most answers being in the 305 m to 915 m (1,000 ft. to 3,000 ft.) range. The array of responses is summarized in Figure 5, showing that there are discrete lengths of 305 m (1,000 ft.) and 610 m (2,000 ft.) "umbilicals" (or travel distances) for certain categories of repairs or related requirements. The typical travel distances required are divided into three groups; up to 305 m (1,000 ft.); between 305 m to 610 m (1,000 ft. and 2,000 ft.); and beyond 915 m (3,000 ft.), and are indicated by the dotted lines in Figure 5. In concept, all these systems would be pig-based. Systems with despoiled umbilicals could be considered for the first two groups, while the last group would be better served with a self propelled system with self-contained onboard power and welding system.

152 m (500 ft.) appears to be adequate to cross most interstate highway crossings and 610 m (2,000 ft.) for all river crossings. A major river crossing would require the device to travel up to 610 m (2,000 ft.). In one case it was stated that the longest section of pipe which is not accessible (directional bore) is approximately 1,219 m (4,000 ft.), so the need would be to access the pipe a distance of approximately 610 m (2,000 ft.) from either end.

Longer distances, probably from 915 m (3,000 ft.) to several miles or more would require the technology to travel in a similar way as an inspection pig. Realistically, such a system would have to be based on an onboard propulsion device using gas line pressure as the motive force. A self-contained, inverter-based welding power source and welding system would also be required.

#### **In what range of pipe diameters should the repair device be capable of operation?**

A wide range of pipe sizes were cited, both within a particular company, and between various companies. The results are summarized in Figure 6 show that pipe size range

requirements run from 51 mm (2 in.) through 1,219 mm (48 in.) diameter. The common size range for 80% to 90% of operators surveyed is 508 mm to 762 mm (20 in. to 30 in.) diameter, with 95% using 559 mm (22 in.) diameter pipe.

**5. What potential obstructions such as elbows, bends, branches, and taps should the repair system be able to negotiate?**

The answers to this question were quite varied and are summarized in Figure 7. Pipe bends of various radii were most commonly mentioned including 1.5 times the diameter (1.5D), 3 times the diameter (3D), and 6 times the diameter (6D), with 3D pipe bends being the most commonly used. Elbows were mentioned in three responses. It is interesting to note that the answer "all" was given four times.

**6. For the situations described in Question #3, at what approximate cost would an internal repair method become competitive with existing repair options?**

Statements and cost figures varied widely from \$25,000 to \$1,000,000 depending on the perspective of the survey respondent and the terrain that their pipeline systems crossed (see Figure 8).

One reply indicated that internal repair probably would not be competitive with external repair/replacement except in river crossings. Anything cheaper than a new HDD and tie-in would be economical in that case.

One company indicated that the cost is related directly to the amount of time the pipeline would be out of service. For major river/road crossings the technology would be competing with HDD @ \$1,000/305 m (\$1,000/ft.). On land, if one can dig up the area and cut out the affected piece of pipe faster than repairing it, then this is what companies would do since the cost of the pipe and a couple of field welds is inconsequential compared with the cost of having the pipeline out of service. The potential cost option could be the reconstruction of a river crossing or other directionally bored crossing.

One respondent indicated that pipe repairs without external access are typically expensive, thus limiting the types of repairs to critical service lines. Repair costs, if the repair can be quickly mobilized (i.e. leaking system) and be confidently applied, can approach \$1,000,000. Therefore the repair would have to serve as a permanent repair.

Another company noted that existing external methods are relatively inexpensive. Repairs required in an area that is inaccessible to current external repair methods can be very expensive and vary by the pipe size, length, and situation. The advantage will be to repair multiple locations or hard to reach locations with minimal excavation. Quite reasonably,

several respondents answered that this would have to be examined on a case-by-case basis.

Yet another response indicated that an internal repair tool would be valuable where the pipe is inaccessible. Replacing a road crossing/directional bore could range from \$50,000 to \$1,000,000 depending on the size of pipe/distance. Other quantitative replies were within the wide range of about \$30,000 to \$60,000 per repair site in one case; for repairs other than in crossings, about \$25,000 per site total including excavation, recoating and backfill; and another reply mentioned about \$200,000, while a another response indicated that an internal repair would have to be 50% to 75% of the cost for a conventional repair/replacement to be competitive.

**7. Have new regulatory requirements created a need to improve the fitness for service of existing transmission lines via localized repair or removal of conditions that are acceptable under previous criteria?**

Responses to this question were varied, with six "no" responses and nine "yes" responses. Specific remarks are listed below:

- Not in Canada – new requirements only change documentation effort.
- Regulations will require companies to prove the fitness for purpose of their pipelines rather than improve. There maybe circumstances with HCA's where repairs are now required.
- Some, but I see this as having little impact on the use of this technology. The newly proposed pipeline integrity regulation will make us more aware more quickly to the extent of repair required.
- Under the current Texas Railroad Commission Integrity Rule, and the pending DOT integrity rule, operators are in-line inspecting more pipe than has been done in the past. More repairs may be necessary as a result of more inspections.
- Upcoming inspection requirements may result in the discovery of defects requiring repairs that would not otherwise have been discovered. Increased cost of excavation restoration has been imposed by various municipalities.

**8. What is the estimated number of repairs per year which could potentially be performed by internal repair in your company for the reasons discussed in Questions #3 and #7?**

Responses varied from "none," through "1 repair in 5 years," and in one case "10-75 repairs per site." These answers are summarized in Figure 9 which shows that answers

from "1 repair in 5 years," up to "5 repairs per year" were by far the most common response. This indicates a limited expected requirement for such a system, particularly based on expected relative cost to purchase and operate. This supports the suggestion that pigging operators would be the best source to supply and operate such equipment on a contracted basis.

#### **9. Comments pertaining to the use/potential use of internal repair.**

Significant individual responses follow:

- Internal methods would be hard to accept as it would be difficult for QA/QC and direct inspection.
- It would have to provide a permanent repair and be piggable to be worthwhile.
- Reinforcing weld joints internally for the in-service pipelines built using welding process, which produced joints with incomplete penetration and lack of fusions.
- Any internal repair sites would have to still be capable of passing an ILI tool and be visible to that tool.
- Internal repair could not impede the ability to pig lines and still be a viable option.
- The major concern would be not to obstruct subsequent ability to assess the pipeline's integrity through internal inspection schemes.
- It is a good to have, whenever necessary.
- A method of inspection of the repaired area may need to be devised.
- It would seem that internal repair methods would have minimal use unless long distances need repaired in congested locations.
- Offshore or underwater (e.g. river crossings, swamps, etc.) offer best economics.
- It would be a valuable tool to have; however, I see no advantage to the process for pipe which is accessible. The only value would be where pipe is inaccessible in a road/stream.
- The use of an internal repair would probably be driven by the discovery of unacceptable corrosion in an inaccessible location. We are currently unaware of this situation in our system.

#### **Part 3 – Need for *In-Service* Internal Repair**

**1. How important is the ability to perform a repair from the inside the pipe while the pipeline remains in service?**

The majority of survey respondents considered the ability for the pipeline to remain in service while the repair was conducted to be very important (Figure 10), especially if their system was not looped. Companies with looped pipeline systems presumably account for the respondents that considered this to be only somewhat important.

Significant individual responses:

- If the pipeline could remain in service the probability of using the tool would be very greatly increased.
- The ability to keep a pipeline in service during repair work would be an important factor when considering internal repair as a possible option.
- Very important for the economics of a large diameter transmission line. Keeping the line in-service is a distinct advantage over cut-out.
- For us it would be important because we are not looped.
- Because this may compete with external sleeving, I think that this is real important.
- This repair method would save gas that would normally be lost and would allow service to be uninterrupted. It is very important.
- Minimizing business disruptions to key customers is important. This ability would make such a repair method very important.
- For those pipelines where service cannot be interrupted and where welding is impractical, it is very important.

**2. Would internal repair remain attractive if it was necessary to completely shut down the pipeline (depressurized and evacuated) during the repair?**

The answers summarized in Figure 11 include six "yes" and three "no," with a variety of other responses in between.

Twelve respondents collectively indicated that this depends on a number of other criteria. It would remain attractive if:

- It could eliminate the need to build an ice road in the swamp or dam and flume a river
- in highly congested areas it could be attractive
- Could be where it is too hard to get to the defect location directly like under a river, lake, for offshore and underwater.
- For offshore environments, shut-in is possible, blow-down probably an extra \$100k minimum dependant upon gas prices.
- To depressurize and evacuate the gas adds cost that would affect how attractive this type of repair would be.

**Depressurized but not evacuated?**

Responses are presented in Figure 12: there were eight "yes" responses and two "no" responses.

Individual responses:

- Depressurized but still flowing is better.
- Depressurized and not flowing is poor; usually the cost of excavation is minor compared to the outage.
- It is typically not possible to depressurize without a blow down and would not be as attractive.
- There could still possibly be applications but would then be much more a function of the cost of the internal repair versus the cost of external repair or replacement.

### **Out-of-service (no flow), but remain pressurized?**

Responses are summarized in Figure 13: there were eleven "yes" responses and two "no" responses. If the pipeline must be out-of-service, the amount of pressure remaining and whether or not it is evacuated are probably far lesser considerations.

Specific responses:

- This is more attractive than the previous two.
- It would be an attractive repair technology under these conditions.
- Leaving the line pressurized would reduce the gas lost, and reduce the potential cost of the repair.

### **3. Comments pertaining to the need for in-service internal repair.**

One response commented that hopefully internal repair would only be required for operators who transport wet or corrosive products. This comment refers to their lack of internal corrosion damage, but also indicates a lack of understanding that the internal repair could be used to repair external corrosion damage. An internal repair appears to be attractive if it reduces the potential for gas lost from blowing down a pipeline, and reduces cost, and/or reduces out-of-service time. Obviously, as the price of gas increases each of the above options will have more impact.

## **Part 4 – Applicable Types of Damage**

### **1. What types of external coatings would be found on transmission lines owned by your company?**

A wide variety of coatings were cited ranging from none (bare steel pipe) through a wide range of bitumastic, coal tar, wax; plastic and composite tapes and wraps; to POWERCRETE® and concrete. The number of responses indicating the use of each coating type is summarized in Figure 14. The top three coating types mentioned were fusion bonded epoxy (FBE), coal tar, and concrete/POWERCRETE®.

**2. If a repair involving welding from the inside was performed, how important is it to preserve the integrity of the coating?**

The ten responses are summarized in Figure 15. There were ten responses to this question. One company indicated a level of importance of "important," six companies listed the level as "very important," and three indicated a level of "critical/essential." Five respondents commented that preserving the coating integrity was not very important, as the CP system was considered capable of taking care of local degradation in these instances.

Individual responses:

- It is of utmost importance.
- If the existing coating cannot be maintained, then additional excavations will be necessary and the coating repaired.
- It is very important for large damaged areas since access to site to repair the coating may be difficult.
- It is necessary to try to preserve as much coating as possible since the repair may be applied to an area of external corrosion and we would not be able to assess the root cause of the corrosion or know if it is mitigated.
- An offshore pipeline operator suggested that perhaps considering attaching an anode if necessary, but then again, reasonable access would be required. In offshore applications, a small amount of coating damage is not too much of a problem.

**3. Is your cathodic protection system capable of compensating for relatively small breaches in the coating?**

The results here are shown in Figure 16. All respondents said that the CP system is capable of compensating for relatively small breaches in the coating: there were thirteen "yes" responses and five qualified "yes" responses.

Comments received:

- Preservation of external coating must be a major consideration.
- Not for disbonded coating.
- It would not meet DOT code requirements under 192/195.
- We do not want any breaches or holidays in their coatings. Coating damage would reduce the attractiveness of this repair system.

One company stated that the CP system can normally compensate, but that one would have to consider that if you had an external corrosion anomaly at the repair site, you may repair it and still have an active external corrosion site. The internal repair would have to be fully pressure containing. Also, if the weld damages good coating, and there is some localized issues with CP protection, that may set-up an active corrosion site at the weld sites (especially if damaged coating is left disbonded and shielded from CP).

#### **4. Comments pertaining to applicable types of damage.**

The following three comments were received:

- I would not want to trade a known likelihood of external coating damage in order to permit an internal repair.
- I do not think the industry or the regulators would accept a repair method that damages the coating and leaves it in worse shape than originally found
- If the coating is damaged and CP shielding occurs, then problems would be great. It may be possible to install a Magnesium (Mg) anode at the repair location to spot protect damage to the coating.

### **Part 5 – Operational and Performance Requirements for Internal Repairs**

#### **1. Two general categories of repairs are being considered, (1) using weld metal to restore a surface and (2) installing an internal sleeve, either metallic or nonmetallic, to provide structural reinforcement of leak tightness. Is it important that the line remain inspectable by pigging after repair?**

The responses are summarized in Figure 17, which shows the unanimous response was "yes."

The five "yes" responses contained the following comments:

- Maybe not for a temporary repair. One scenario that comes to mind is in the mountains where there is too much snow to access. A temporary repair could be made and not worry about ILI restriction. Would perform cut-out in the summer.
- Yes, if original line was piggable.
- DOT code 49 CFR 192.150 states that all new lines, or line repaired, will be able to accommodate the passage of an ILI device. Additionally, with the new integrity

management rules requiring regular pigging of pipelines, any internal repair would have to allow the passage of a pig.

- Under existing DOT codes it would seem that being able to inspect the line is required. New pipeline integrity regulations may allow for alternative methods.
- For some lines, being "smart- piggable" after repair would be mandatory.

**About how far could the repair protrude into the pipe before it would interfere with pigging?**

The responses are summarized in Figure 18. Six responses gave a range in the region of 5% to 10% of nominal pipe diameter. Even for relatively small diameter pipe this amount of protrusion could be quite large.

Seeking guidance from pigging vendors was suggested by seven of the responses. An amount of 1% of diameter was considered a good number as a rule of thumb in one case. In another, about 1.5 mm (0.6 in.) for a 914 mm (36 in.) pipe (2% of diameter) was mentioned. Several responses mentioned that the type of pig is an important consideration when considering an answer to this question. A "smart pig" was said to be able to accommodate a 10% reduction in diameter.

One response stated that the acceptable protrusion varies depending on the type of pig, pipe size, geometry, and longitudinal length of the restriction. Another response stated that this is dependent upon the type of pigging utilized (e.g., traditional versus smart).

**2. What NDE would your utility require for a repair to an existing longitudinal or circumferential weld?**

Thirteen survey respondents included radiographic testing (RT) or indicated that only radiographic inspection was used or allowed; five indicated that ultrasonic testing (UT) is also permitted; and two responses indicated that magnetic particle inspection (MPI) is also allowed (see Figure 19).

UT or RT acceptability is judged to code acceptance criteria; specifically ASME B31.8 or B31.4, and CSA Z662 codes were mentioned. In one case it was noted that all welds below 40% SMYS are repaired with a reinforcement sleeve/canopy or removed from the system. In another, it was stated that inspection must comply with Part 192 NDE requirements.

**What NDE would your utility require for a welded repair to base metal (e.g. corrosion pitting)?**

Figure 20 summarizes the NDE requirements for weld repair to base metal: seven responses include or only use/allow RT, three responses include UT as an acceptable alternative to RT, and three responses include MPI. UT or RT acceptability to code acceptance criteria ASME B31.8 or ASME B31.4 were also mentioned. In one case, it was noted that, at a minimum, all weld repairs are visually inspected and soap tested. Another response indicated that all welds must meet the acceptability standards of the currently referenced edition of the API 1104.

**Could a visual or magnetic particle examination be substituted for radiography in these special circumstances?**

The answers to the question were evenly distributed. There were three "yes" only responses, three qualified "yes" answers, three "MPI not visual," three "maybe," three "no," and three "don't know."

Specific comments:

- On fillet welds to the base metal, yes. For the long seam repair, probably not.
- Below 40% SMYS repairs utilizing pre-qualified components with a manufacturer established MAOP require both a visual and a soap test.
- I am not sure how the MPI would be done remotely, but it would have value.

**3. Would the use of internal repair be attractive even if it were considered a temporary repair?**

The answers to this question were mixed, as summarized in Figure 21: eight were "no" responses, three were "yes" only, and eight were qualified "yes" responses.

Individual comments:

- In some circumstances, especially in seasonal climates (Canada, mountains, muskeg).
- Yes, if it could be done at relatively low cost (competing with an external sleeve, which is permanent) and with little to no interruption in service.
- Only if the cost was very low.
- If we were using this as a repair, we would rather have a permanent solution.

- Only in a very limited number of cases.
- It could be to allow for scheduling repairs and avoid a shut down during critical times.
- Yes – if it could be accomplished without purging the pipeline.
- Possibly, dependent upon the situation.

#### **4. Comments pertaining to operational and performance requirements for internal repairs.**

Specific responses:

- Repairs would need to be as good as the original pipe; one wouldn't want to create local corrosion cells if the weld filler metal was more/less active than the base metal. This would only be attractive if shutdown is not required and no excavation is required to find the defect.
- The internal repair should provide for a smooth internal surface. The weld repair would not leave an area subject to long term cracking. CP would not be compromised. Repair will not interfere with future inspections.

#### **Part 6 - General Comments**

**Please provide any general comments that you may have. For example, comments on an acceptable range of commercial pricing for such a system would be useful (as distinct from a repair cost in Question#6 of Part 2).**

Individual responses follow:

- This would not be a piece of equipment that our company would use often enough to justify us owning it. The most effective management of this system may be through a smart pigging company that could offer this as a follow-on service after inspection.
- The internal repair should return pipe to its original serviceability and safety factor. Pricing would determine selection if the repair was appropriate and proven for the type of defect. The costs are going to be weighed against the cost of excavation and the need to purge the line. Quite often, corrosion damage and even some dents can be repaired with steel sleeves using hot tap procedures so the pipeline does not have to be shut down. In swamp conditions, excavation is very expensive due to special equipment and the need to construct isolation dams to keep out the

water and use pumps to dry the hole. Of course, offshore repairs require divers and habitats. The internal repair method would have the best economics for underwater repair locations. Some urban areas may have the same type of economics.

- Having an internal welding tool option would be very advantageous for a given situation. That situation is a totally inaccessible location such as a directional bore. For a busy intersection or street alignment where the pipeline can be accessed by conventional method at a high cost, accessing the pipeline externally would be preferred. The repair method would have to be approved by DOT prior to being used.
- The cost depends mainly on the requirements of the repair as in pipe size, length, customer outages, etc. I would say that it has to be considerably less than the standard repair methods to make the new repair method accepted by industry. Because it is internal and the integrity of the repair has to be assessed through some form of NDE, the actual repair strength will be hard to sell.

## 5.0 CONCLUSIONS

The twenty survey responses produced the following principal conclusions:

1. Use of internal weld repair is most attractive for river crossings, under other bodies of water such as lakes and swamps, in difficult soil conditions, under highways and in congested intersections, and under railway crossings. All these areas tend to be very difficult and very costly, if, and where conventional excavated repairs may be currently used.
2. Internal pipe repair offers a strong potential advantage to the high cost of HDD when a new bore must be created to solve a leak or other problem in a water/river crossing.
3. The typical travel distances required can be divided into three groups: up to 305 m (1,000 ft.); between 305 m and 610 m (1,000 ft. and 2,000 ft.); and beyond 914 m (3,000 ft.). In concept, all appropriate systems would be pig-based. Systems with despoiled umbilicals could be considered for the first two groups, with a self propelled system with self-contained onboard power and welding system for the third.
4. Pipe size range requirements run from 50.8 mm (2 in.) through 1,219.2 mm (48 in.) in diameter. Of the survey respondents, a common size range for 80% to 90% of operators is 508 mm to 762 mm (20 in. to 30 in.) in diameter, with 95% using 558.8 mm (22 in.) diameter pipe.
5. Based on the frequency of expected use by many operators, the issue of acceptable system cost for a deployable solution could best be tackled through selling such technology as an additional service through existing "smart pig" vendors/operators.
6. There has been almost no use of internal repair to date and the concept is currently fairly alien to pipeline operators. Even the potential for internal repair of external damage using such a system needs further promotion/education within the industry as a whole.
7. Most operators were open to the economic potential an internal repair system may offer in terms of reducing interruption to product flow, particularly if they did not have looped lines.
8. The top three items of concern for selecting a repair method were cost, availability of the repair method (time/cost), and the position of the defect(s).
9. A wide range of pipe coatings were cited as being deployed in the field. The top three mentioned were FBE, coal tar, and concrete/POWERCRETE®.
10. The majority of operators considered the ability for the pipeline to remain in service while the repair was conducted to be very important.
11. RT is by far the most accepted method for pipeline NDE. UT was the second most common process cited.

## 6.0 REFERENCES

Not applicable, as the contents of this report are based on direct contact with fifty-four companies who provided twenty responses to the survey.

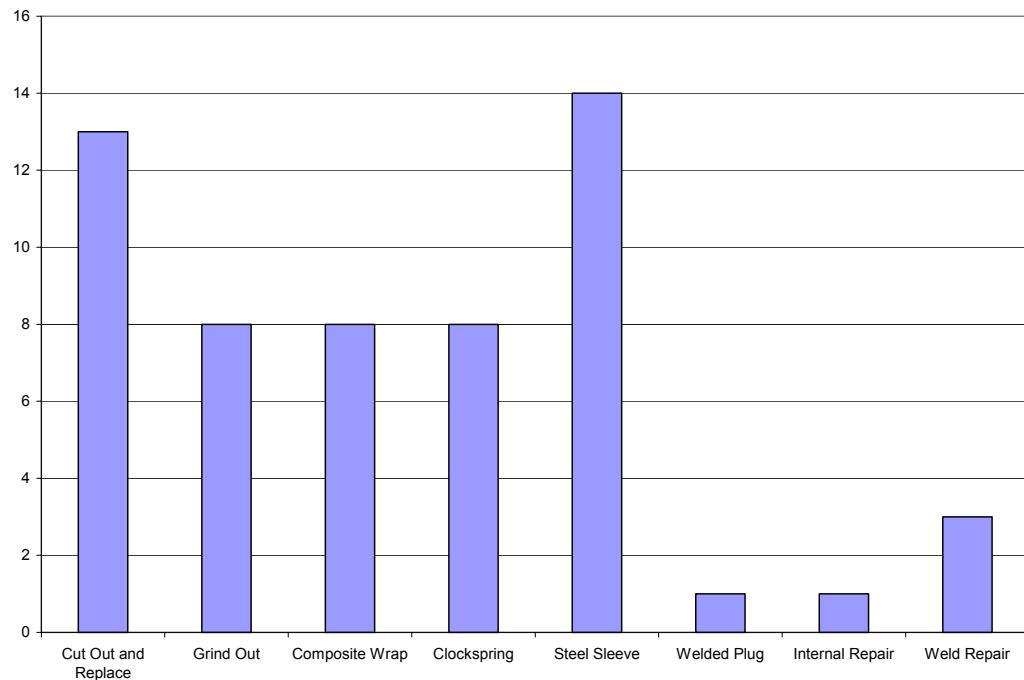
## 7.0 BIBLIOGRAPHY

Not applicable, as the contents of this report are based on direct contact with fifty-four companies who provided twenty responses to the survey.

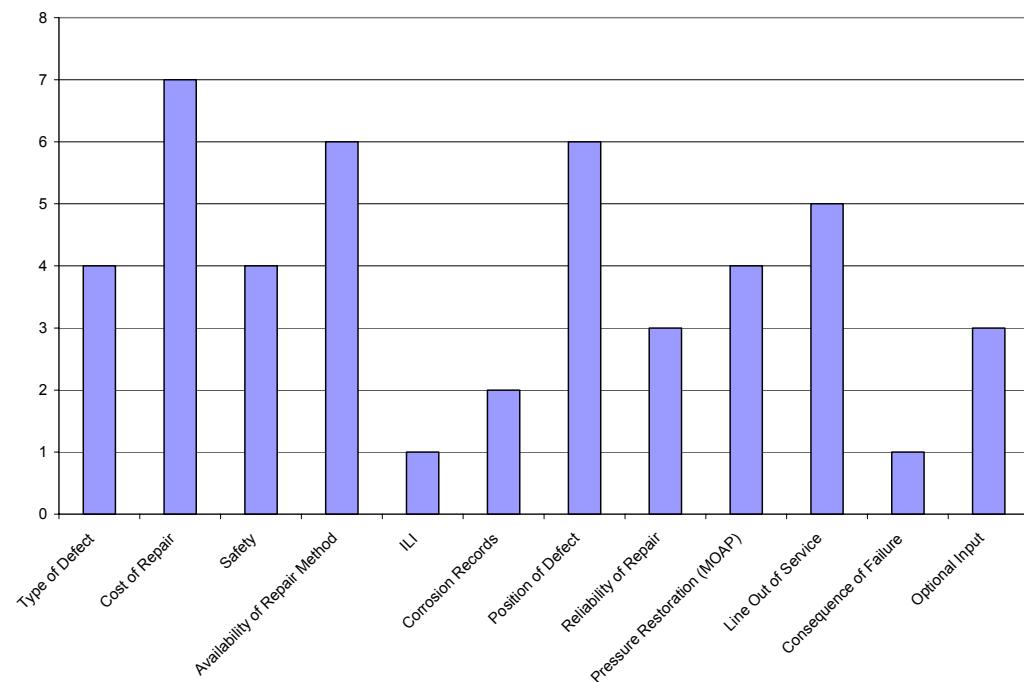
## 8.0 LIST OF ACRONYMS

<b>Acronym</b>	<b>Definition</b>
API	American Petroleum Institute
ASME	American Society of Mechanical Engineers
CP	Cathodic Protection
CSA	Canadian Standards Association
DOT	Department of Transportation
ERW	Electric Resistance Welded
FBE	Fusion Bonded Epoxy
HDD	Horizontal Direct Drilling
ILI	In-Line Inspection
MAOP	Maximum Allowable Operating Pressure
MOP	Maximum Operating Pressure
MPI	Magnetic Particle Inspection
NDE	Nondestructive Examination
PE	Polyethylene
PG&E	Pacific Gas & Electric Co.
PRCI	Pipeline Research Council International
QA	Quality Assurance
QC	Quality Control
RT	Radiographic Testing
SCC	Stress Corrosion Cracking
SMYS	Specified Minimum Yield Strength
UT	Ultrasonic Testing

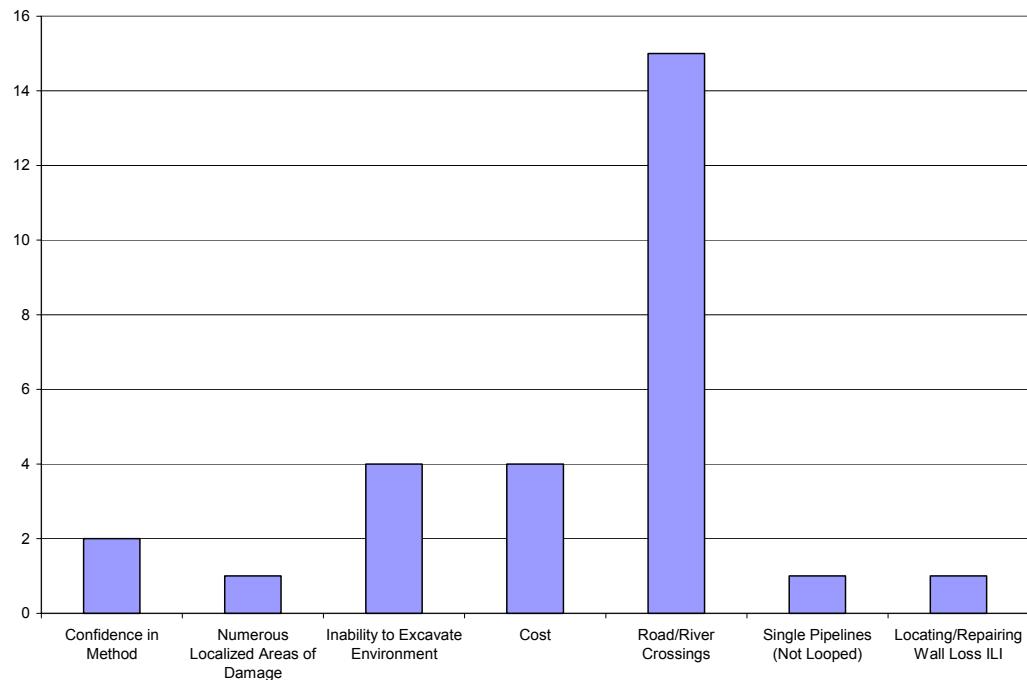
**Figure 1 - Currently Used Repair Methods**



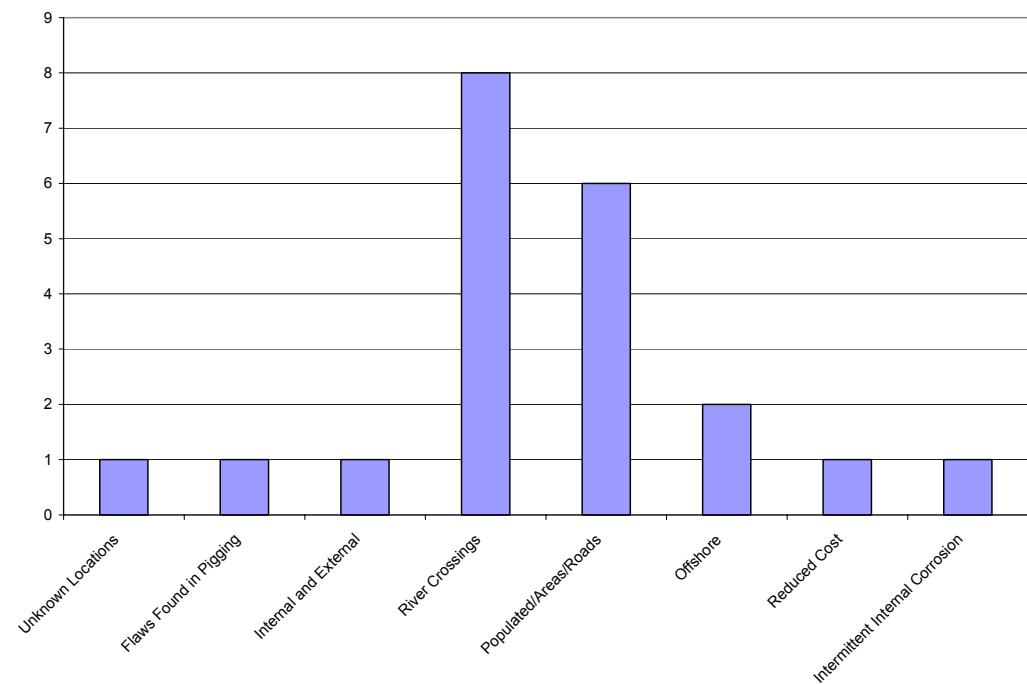
**Figure 2 - Criteria Affecting Choice of Repair Method**



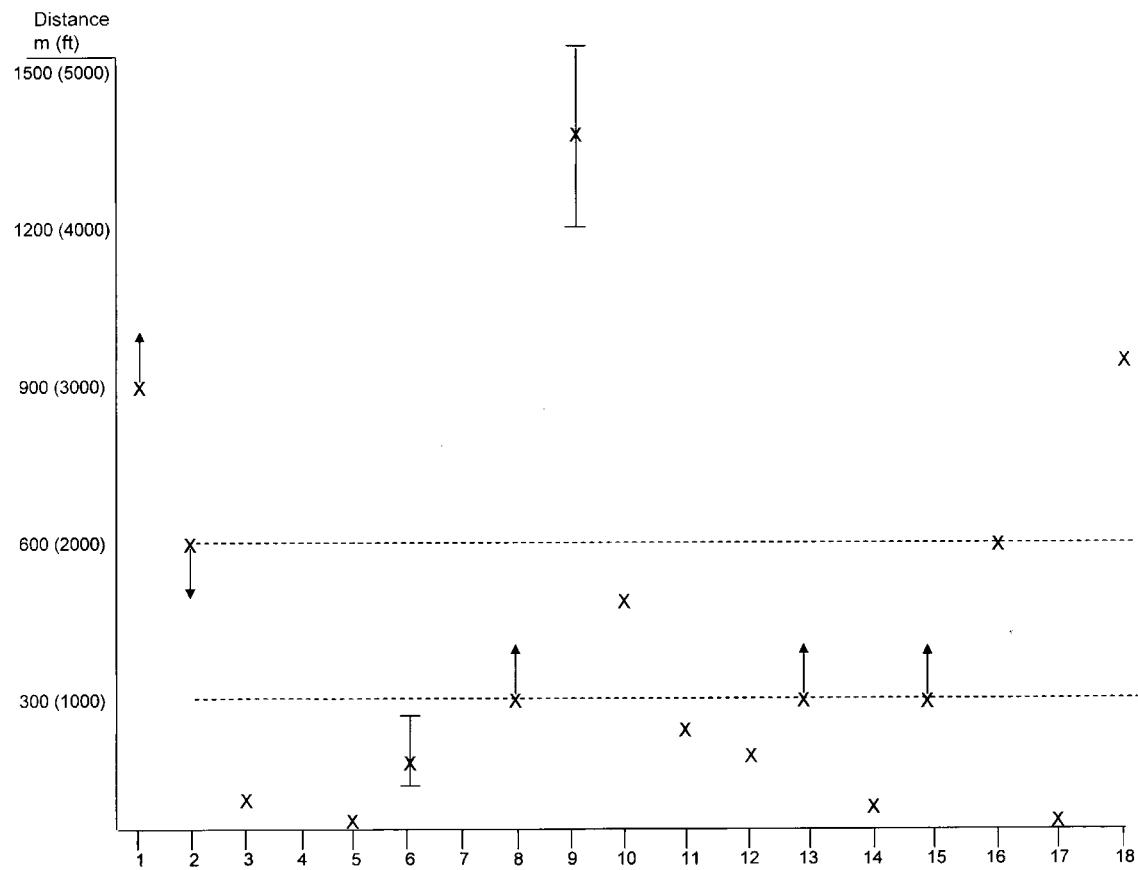
**Figure 3 - Decision Factors for Internal Pipe Repair**



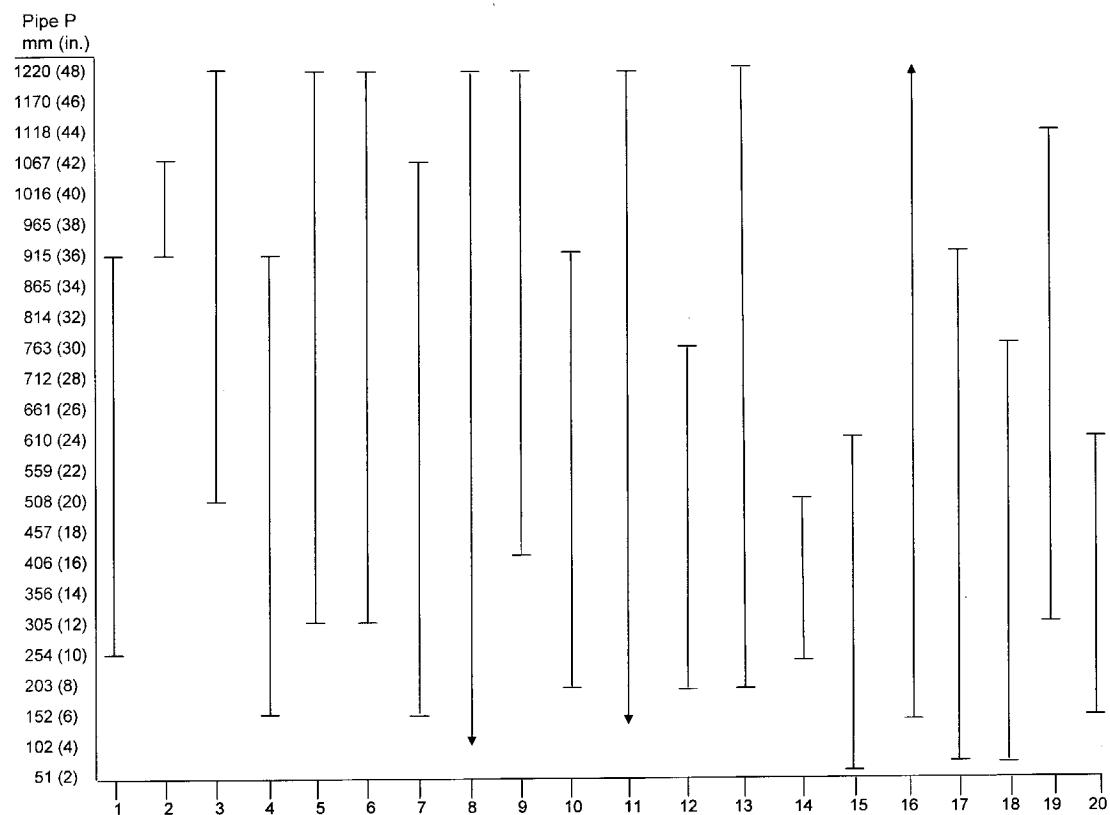
**Figure 4 - Specific Geographic Locations and Special Situations**



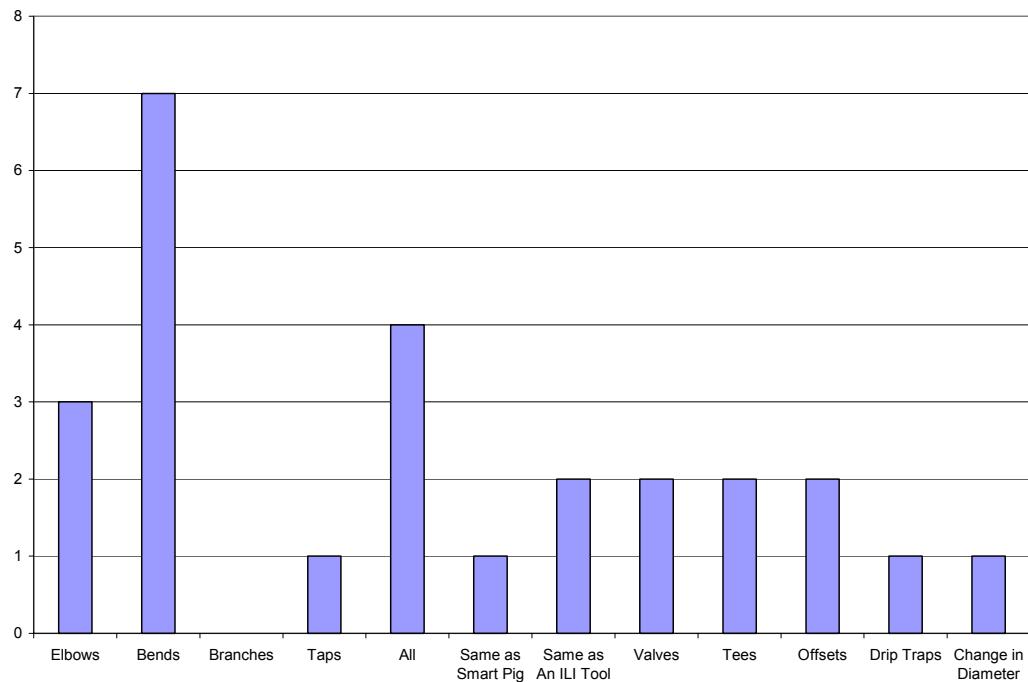
**Figure 5 - Distance Repair System Required to Travel Down Pipe**



**Figure 6 - Range of Pipe Diameters Used**



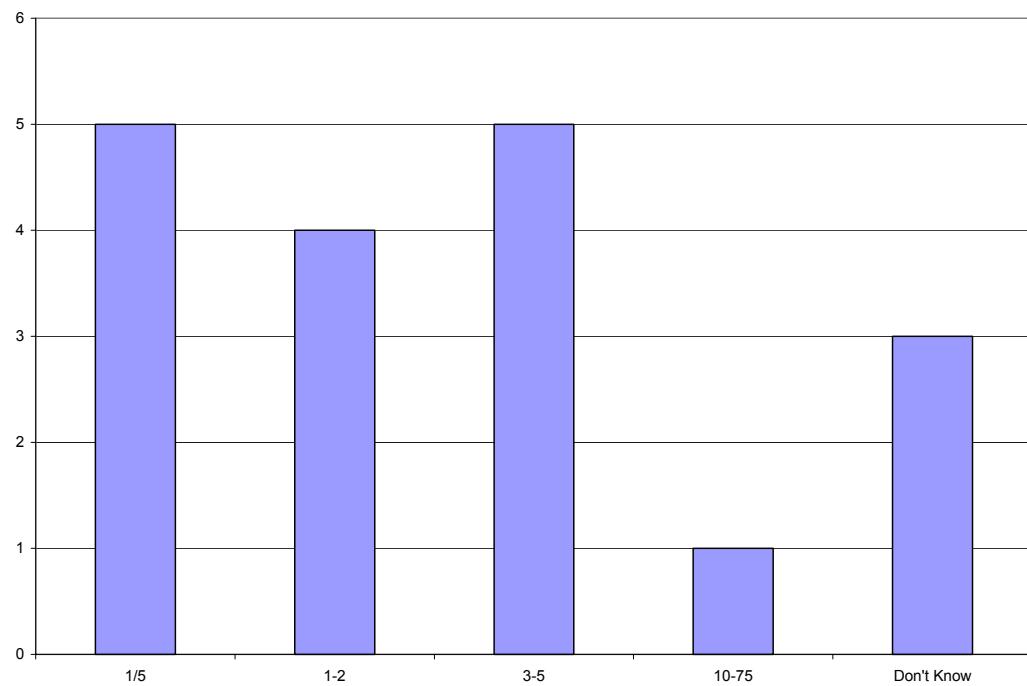
**Figure 7 - Potential Obstructions to be Negotiated**



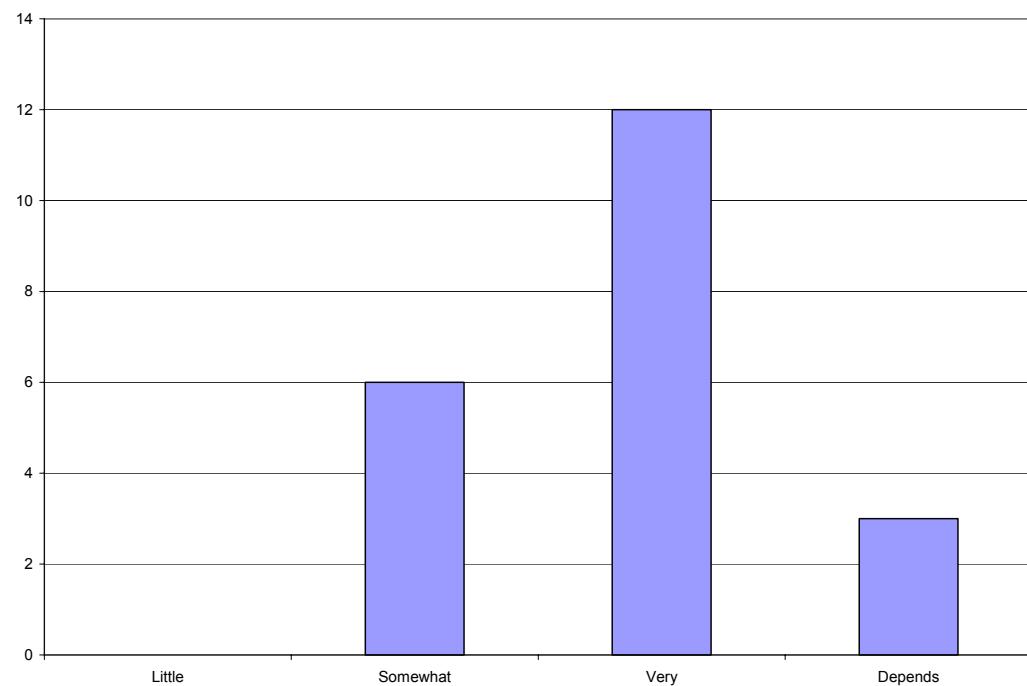
**Figure 8 - Cost Comparative Breakpoint for Internal Repair**

- Case by case basis
- \$1,000/0.3 m (\$1,000/ft.) is the benchmark for internal repair as this is the cost for HDD
- Road crossing/HDD cost is \$50,000 to \$1,000,000 depending on pipe size & distance
- \$25,000 per repair site
- \$30,000 - \$60,000 per repair site
- \$50,000 - \$70,000 per repair site
- \$200,000 per repair site
- Permanent repair less up to \$1,000,000
- Twice the cost of conventional repair
- Half the cost of conventional repair

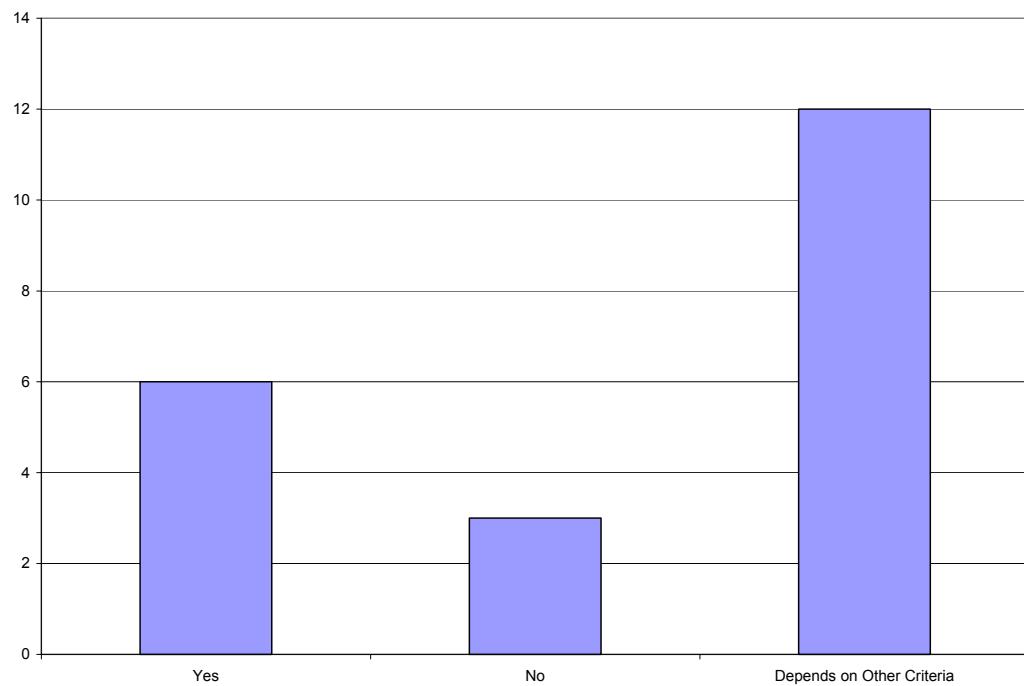
**Figure 9 - Estimated Number of Internal Repairs Required Per Year**



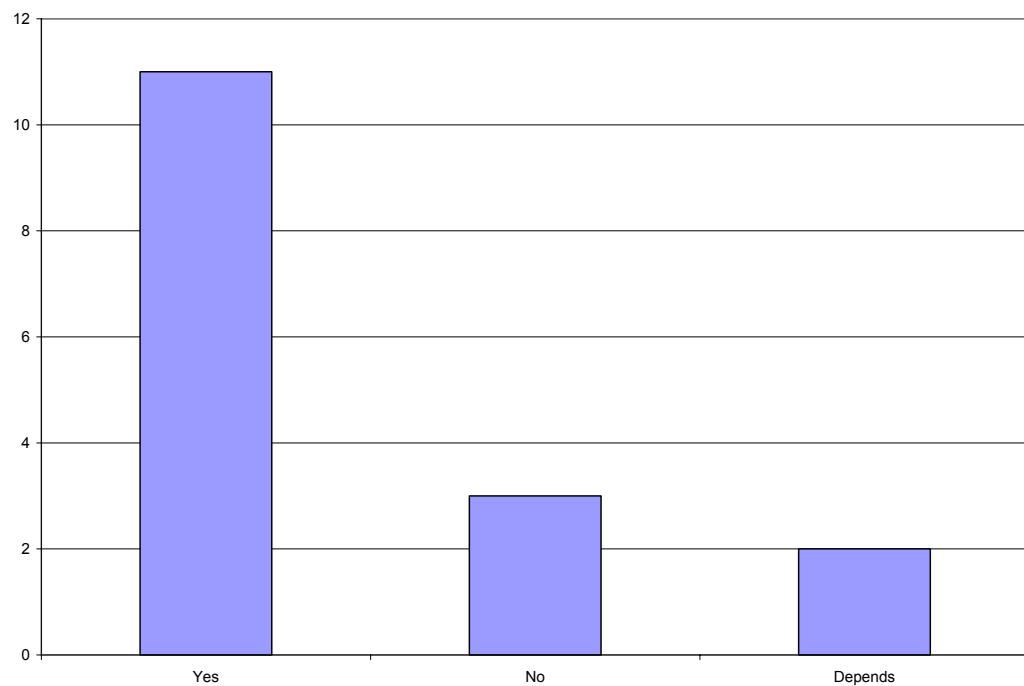
**Figure 10 - Importance of Repair While Pipeline Remains In Service**



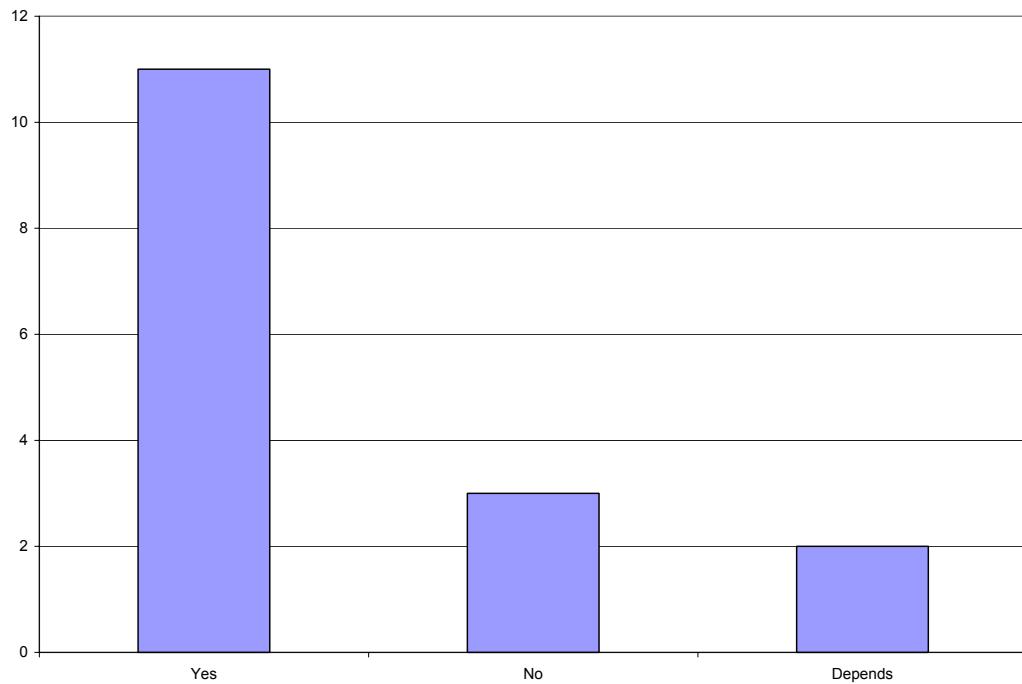
**Figure 11 - Still Attractive if Pipeline Must be Shut Down (Depressurized and Evacuated)**



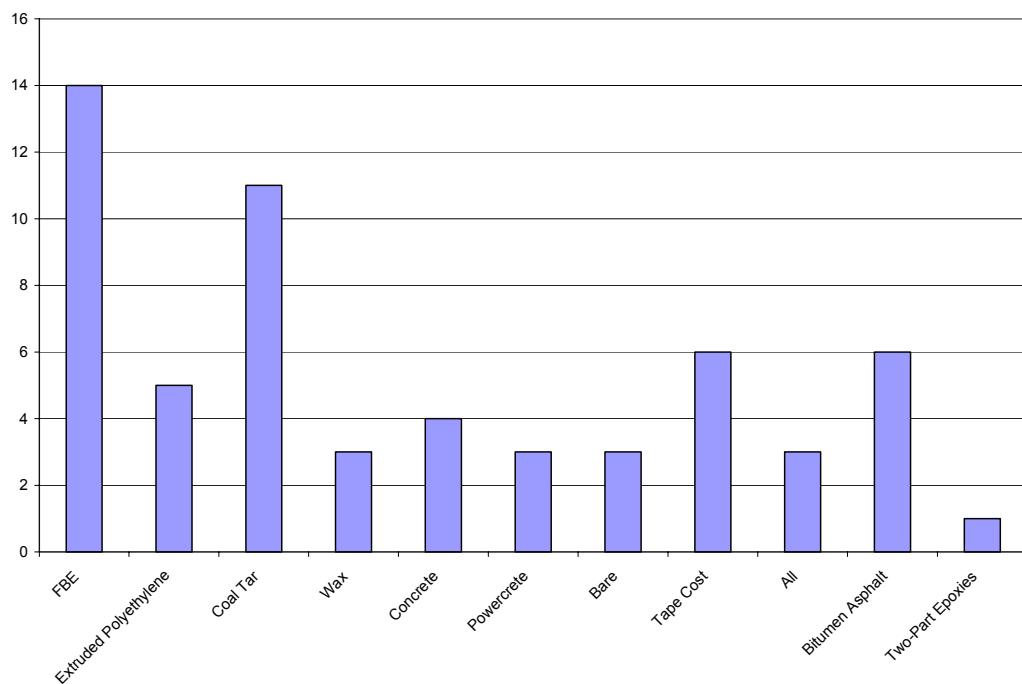
**Figure 12 - Still Attractive if Pipeline Must be Depressurized but Not Evacuated**



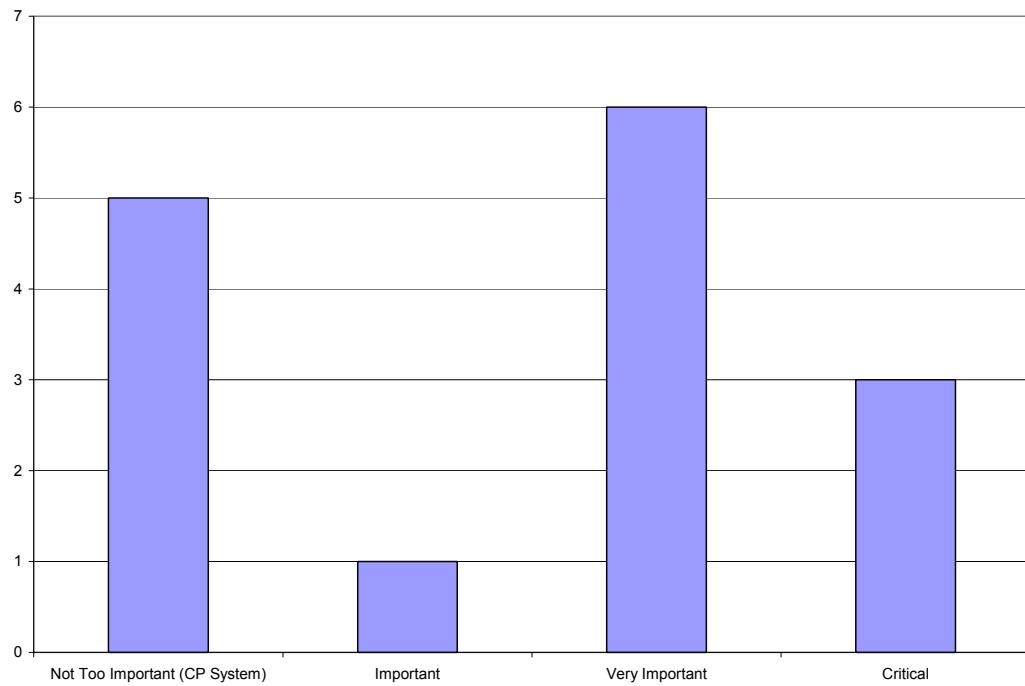
**Figure 13 - Still Attractive if Pipeline Must be Out of Service but Pressurized**



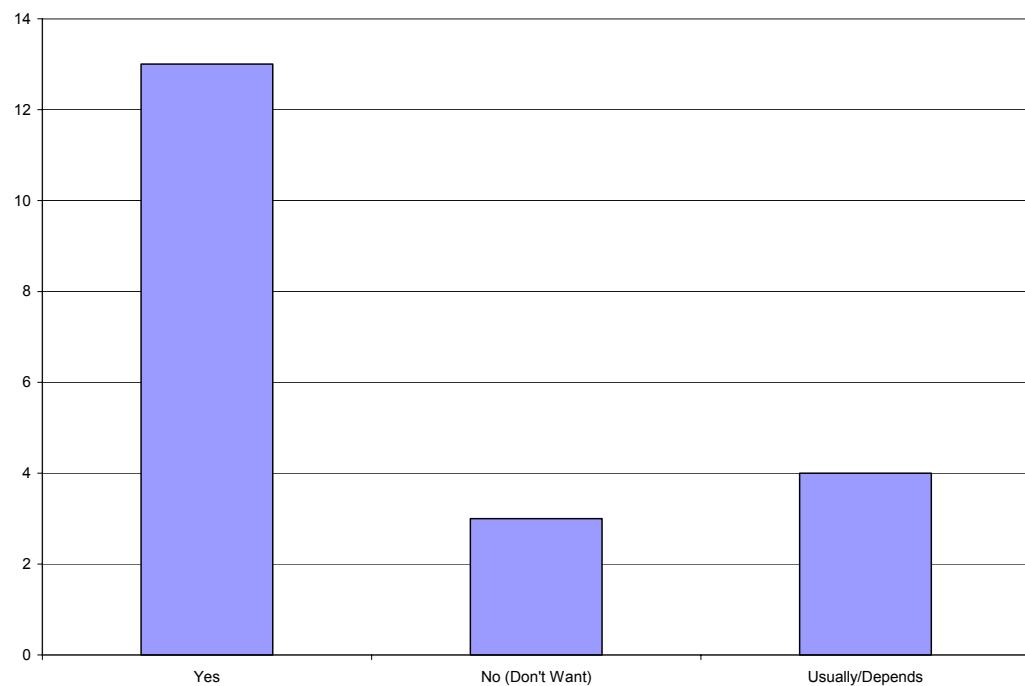
**Figure 14 - External Coatings Used**



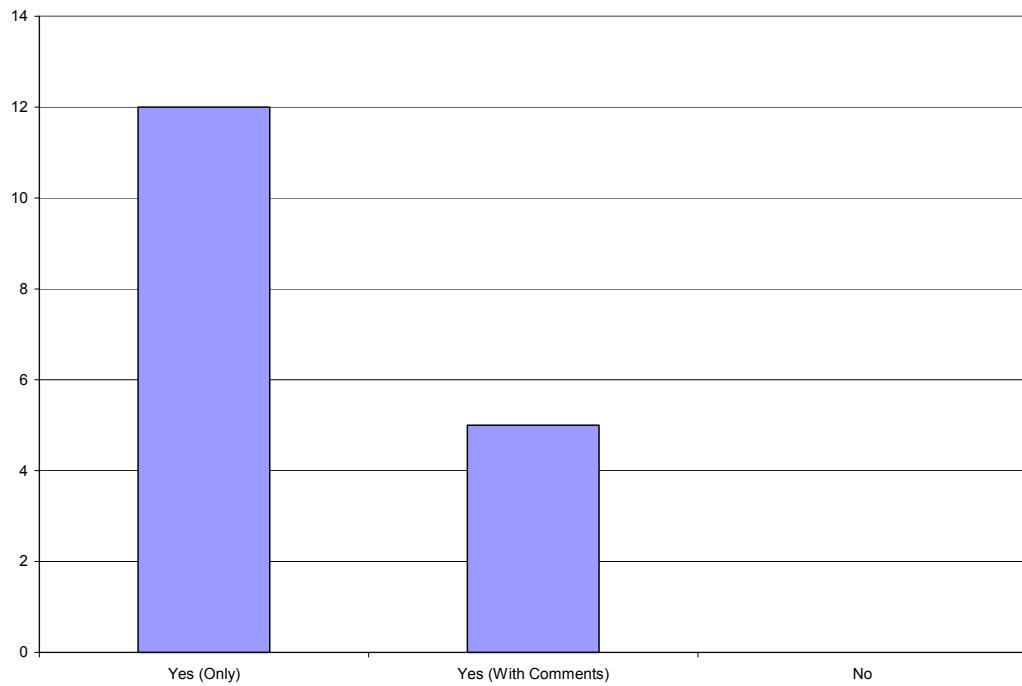
**Figure 15 - Maintenance on Coating Integrity**



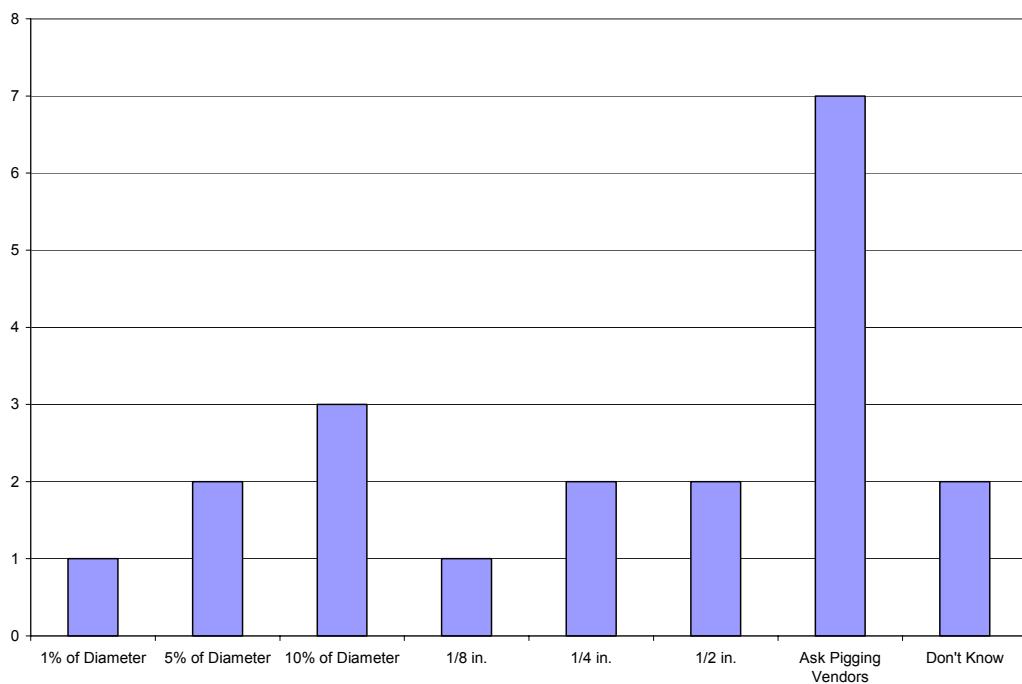
**Figure 16 - Is CP System Capable of Compensating for Small Coating Breaches**



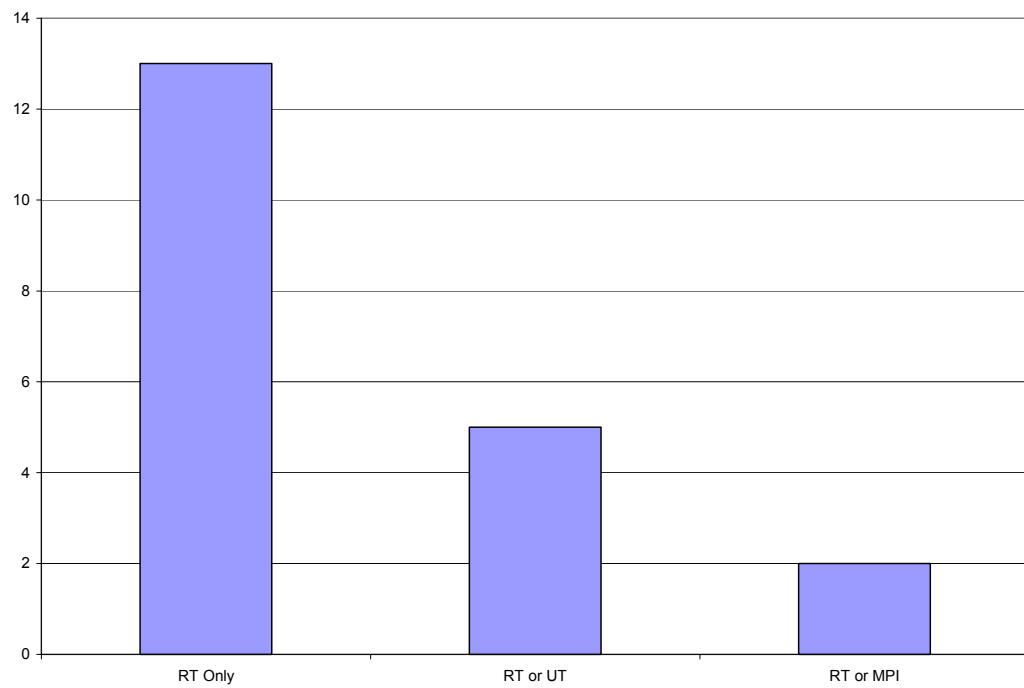
**Figure 17 - Inspectable by Pigging**



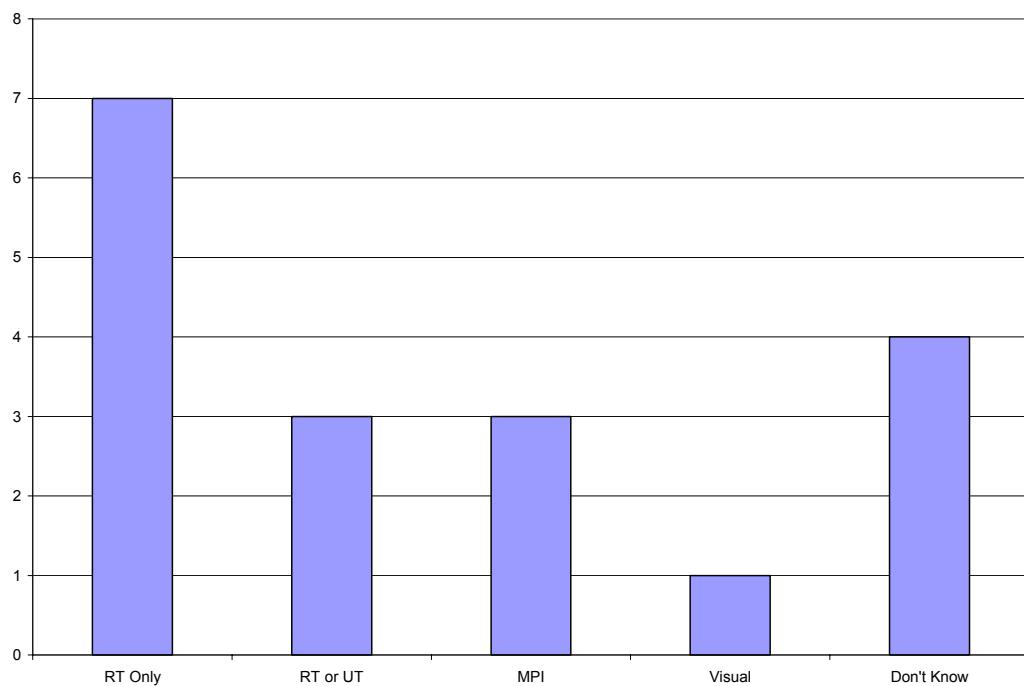
**Figure 18 - How Far Could the Repair Protrude Into Pipe Before Interference**



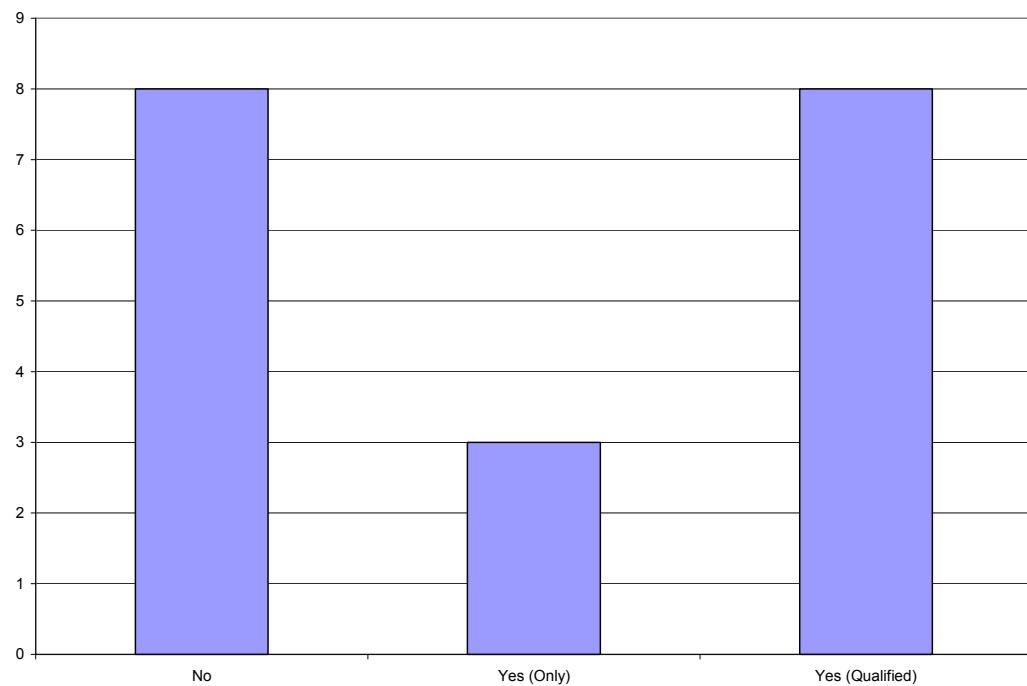
**Figure 19 - NDE Required for Repair to an Existing Weld**



**Figure 20 - NDE Required for Base Metal Repair**



**Figure 21 - Would Internal Repair be Attractive Even as a Temporary Repair?**



## **9.0 APPENDICES**

## **APPENDIX A**

### **Survey and Cover Letter**

June 10, 2003

<<<FIELD 1>>>

**EWI Project No. 46211GTH, "Internal Repair of Gas Transmission Pipelines – Survey of Operator Experience and Industry Needs"**

Dear <<<FIELD 2>>>:

Enclosed is a survey of operator experience and industry needs pertaining to internal repair of gas transmission pipelines.

EWI is conducting this survey as part of a project being funded by the National Energy Technology Laboratory. The objectives of the project are to evaluate, develop, demonstrate, and validate internal repair methods for pipelines; develop a functional specification for an internal pipeline repair system; and prepare a recommended practice for internal repair of pipelines.

One of the initial tasks of this project, co-funded by Pipeline Research Council International, involves conducting a survey to determine the repair needs and performance requirements for internal pipeline repairs. The purpose of this survey is to better understand the needs of the natural gas transmission industry regarding internal repair.

Please complete this survey at your earliest convenience.<sup>1</sup> Your participation is greatly appreciated. If you have questions or require additional information, please contact me at 614-688-5059 or [bill\\_bruce@ewi.org](mailto:bill_bruce@ewi.org)

Sincerely,

Ian D. Harris and William A. Bruce, P.E.  
Principal Engineers  
Arc Welding, Automation and Materials

Enclosure

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<sup>1</sup> A copy of this survey was also sent to <<<FIELD 3>>> at your company. You may want to coordinate your response.

Project No. 46211GTH

on

**Internal Repair of Gas Transmission Pipelines – Survey of  
Operator Experience and Industry Needs**

for

**National Energy Technology Laboratory**  
Morgantown, WV

June 10, 2003

**EWI**  
1250 Arthur E. Adams Drive  
Columbus, OH 43221

# **Internal Repair of Gas Transmission Pipelines – Survey of Operator Experience and Industry Needs**

## **1.0 Introduction**

A repair method that can be applied from the inside of a gas transmission pipeline (i.e., a trenchless repair) is an attractive alternative to conventional repair methods since the need to excavate the pipeline is precluded. This is particularly true for pipelines in environmentally sensitive and highly populated areas. Several repair methods that are commonly applied from the outside of the pipeline are, in theory, directly applicable from the inside. However, issues such as development of the required equipment to perform repairs remotely and mobilization of equipment through the pipeline to areas that require repair need to be addressed. Several additional repair methods that are commonly applied to other types of pipelines (gas distribution lines, water lines, etc.) also have potential applicability for internal repair of gas transmission pipelines. Many of these require further development to meet the requirements for repair of gas transmission pipelines. The purpose of this survey is to better understand the needs of the natural gas transmission industry regarding internal repair.

## **2.0 Instructions**

Please respond as completely as possible to as many questions as possible. Space is also provided for any comments that you may have.

## **3.0 Survey**

### **Part 1 – Currently-Used Repair Methods**

1. Has your company experienced degradation (corrosion, cracking, etc) of a transmission line?

If so, describe the corrective actions your company has taken due to degradation of transmission pipelines, especially repair or replacement actions?

2. What specific repair methods would typically be used to repair different types of degradation?
3. What criteria (including ease of pipe access) affect choice of the specific repair method to be used?

Comments pertaining to currently-used repair methods –

## **Part 2 – Use/Potential Use of Internal Repair**

1. Has your company attempted repair of a transmission line from inside the pipe?

If so, describe the repair(s)

2. There are many factors that affect the decision to repair or replace pipe. What circumstances would favor performing a repair from inside the pipe using only one or two excavations rather than excavating the entire length of pipe?
3. If the technology were available to perform a repair from the inside, would your company consider using the technology?

If so, for what application(s) – e.g., specific geographic locations and special situations?

4. At least one excavation will be required to insert the internal repair device into the pipe. From this excavation, the repair device could travel in each direction from the excavation. About how far from the insertion point should the repair device be able to travel?

In what range of pipe diameters should the repair device be capable of operation?

5. What potential obstructions such as elbows, bends, branches, and taps should the repair system be able to negotiate?
6. For the situations described in Question #3, at what approximate cost would an internal repair method become competitive with existing repair options?
7. Have new regulatory requirements created a need to improve the fitness for service of existing transmission lines via localized repair or removal of conditions which are acceptable under previous criteria?
8. What is the estimated number of repairs per year which could potentially be performed by internal repair in your company for the reasons discussed in Questions #3 and 7?

Comments pertaining to the use/potential use of internal repair –

### **Part 3 – Need for In-Service Internal Repair**

1. How important is the ability to perform a repair from the inside the pipe while the pipeline remains in service?
2. Would internal repair remain attractive if it was necessary to completely shut down the pipeline (depressurized and evacuated) during the repair?

Depressurized but not evacuated?

Out of service (no flow) but remain pressurized?

Comments pertaining to the need for in-service internal repair –

### **Part 4 – Applicable Types of Damage**

1. What types of external coatings would be found on transmission lines owned by your company?
2. If a repair involving welding from the inside was performed, how important is it to preserve the integrity of the coating?

Is your cathodic protection system capable of compensating for relatively small breaches in the coating?

Comments pertaining to applicable types of damage –

### **Part 5 – Operational and Performance requirements for Internal Repairs**

1. Two general categories of repairs are being considered, (1) using weld metal to restore a surface and (2) installing an internal sleeve, either metallic or nonmetallic, to provide structural reinforcement of leak tightness. Is it important that the line remain inspectable by pigging after repair?

About how far could the repair protrude into the pipe before it would interfere with pigging?

2. What NDE would your utility require for a repair to an existing longitudinal or circumferential weld?

Could a visual or magnetic particle examination be substituted for radiography in these special circumstances?

What NDE would your utility require for a welded repair to base metal (e.g. corrosion pitting)?

3. Would the use of internal repair be attractive even if it were considered a temporary repair

Comments pertaining to operational and performance requirements for internal repairs –

#### **Part 6 - General Comments**

Please provide any general comments that you may have. For example, comments on a acceptable range of commercial pricing for such a system would be useful (as distinct from a repair cost in question 6 of Part 2.)

## **APPENDIX B**

**Lists of PRCI Member and Other Gas Transmission Companies  
Including Contact Name, Email, and Telephone Contact Information  
Generated for the Survey**

## Members of the Pipeline Research Council International Email Contacts for Survey

(As of 7/9/03 Email of main POC {when determined} for multiple listings, or single listings on Materials Committee)

Organization	POC Email Address
Advantica Technologies Ltd	bob.andrews@advanticatech.com
BP	moskowlh@bp.com, moredh@bp.com hammondj3@bp.com,
Buckeye Pipe Line Company	wshea@buckeye.com
Chevron Texaco Pipeline Company	GBKO@ChevronTexaco.com
CMS Panhandle Companies	smgallagher@cmsenergy.com
Colonial Pipeline Company	jgodfrey@colpipe.com
Columbia Gas Transmission Co.	jswatzel@nisource.com
ConocoPhillips	dave.ysebaert@conocophillips.com
Consumers Energy	rswelsh@cmsenergy.com
Dominion Transmission	brian_c_sheppard@dom.com
Duke Energy Gas Transmission	scrapp@duke-energy.com
El Paso Corporation	bennie.barnes@elpaso.com
Enbridge Pipelines	scott.ironside@enbridge.com
Enron Transportation Services Corp.	mcrump@enron.com
Explorer Pipeline Company	jwenzell@expl.com
ExxonMobil Pipeline Company	don.e.drake@exxonmobil.com
Foothills Pipe Lines Ltd	jack.beattie@foothillspipe.com
Gassco A.S. (Norway)	eh@gassco.no
Gasum Oy (Finland)	ilkka.taka-aho@gasum.fi
Gaz de France	gerard.jammes@gazdefrance.com
Gulf South Pipeline	scott.williams@gulfsouthpl.com
Marathon Ashland Pipe Line LLC	tlshaw@mapllc.com
N.V. Nederlandse Gasunie/Gastransport Services (The Netherlands)	w.sloterdijk@gasunie.nl
National Fuel Gas Supply Corporation	pustulkaj@natfuel.com
Saudi Aramco	shuler.cox@aramco.com
Sempra Energy Utilities/Southern California Gas Company	bamend@semprautilities.com
Shell Pipeline Company LP	janiemeyer@shellopus.com
Southern Natural Gas Company	george.benoit@elpaso.com
TEPPCO	lwmallett@teppco.com
TransCanada PipeLines Limited	david_dorling@transcanada.com
Transco (UK)	jeremy.bending@uktransco.com
TransGas	btorgunrud@transgas.com
Williams Gas Pipeline	Thomas.R.Odom@Williams.com

## Members of the Pipeline Research Council International Contact Names and Phone Numbers

(As of 7/9/03)

Organization	POC Name	Phone Number
Advantica Technologies Ltd	Bob Andrews	011 44 1509 282749
BP	John Hammond	011 44 1932 775909
BP	David Moore	907 564 4190
BP	Larry Moskowitz	281 366 2924
Buckeye Pipe Line Company	William Shea	610 254 4650
Chevron Texaco Pipeline Company	George Kohut	510 242 3245
CMS Panhandle Companies	Scott Gallagher	713 989 7444
Colonial Pipeline Company	John Godfrey	678 762 2217
Columbia Gas Transmission Co.	Jim Swatzel	304 357 2797
ConocoPhillips	Dave Ysebaert	281 293 2969
Consumers Energy	Robert Welsh	517 788 1928
Dominion Transmission	Brian Sheppard	304 627 3733
Duke Energy Gas Transmission	Steve Rapp	713 627 6394
EI Paso Corporation	Bennie Barnes	719 520 4677
Enbridge Pipelines	Scott Ironside	780 420 5267
Enron Transportation Services Corp.	Michael Crump	713 345 1623
Explorer Pipeline Company	Jeff Wenzell	918 493 5140
ExxonMobil Pipeline Company	Don Drake	713 656 2288
Foothills Pipe Lines Ltd	Jack Beattie	403 294 4143
Gassco A.S. (Norway)	Egil Hurloe	011 47 52812500
Gasum Oy (Finland)	Ilkka Taka-Aho	011 358 20 44 78653
Gaz de France	Gerard Jammes	011 33 49 22 54 19
Gulf South Pipeline	Scott Williams	713 544 5220
Marathon Ashland Pipe Line LLC	Thomas Shaw	419 421 4002
N.V. Nederlandse Gasunie/Gastransport	Wytze Sloterdijk	011 31 50 521 2674
National Fuel Gas Supply Corporation	John Pustulka	716 857 7909
Saudi Aramco	Shuler Cox	011 966 3 874 6664
Sempra Energy Utilities/Southern Cal Gas	Bill Amend	213 244 5277
Shell Pipeline Company LP	John Niemeyer	713 241 1856
Southern Natural Gas Company	George Benoit	832 528 4244
TEPPCO	Leonard Mallett	713 759 3615
TransCanada PipeLines Limited	David Dorling	403 948 8147
Transco (UK)	Jeremy Bending	011 44 1689 881479
TransGas	Brian Torgunrud	306 777 9357
Williams Gas Pipeline	Thomas Odom	270 688 6964

## Other Natural Gas Pipeline Operating Companies – Email Contacts

(As of 7/9/03)

Organization	Location	Email Address
Algonquin Gas Transmission Co.	Duke Energy	scrapp@duke-energy.com
Algonquin LNG, Inc.	Duke Energy	scrapp@duke-energy.com
Alliance Pipeline Ltd.		arti.bhatia@alliance-pipeline.com
ANR Pipeline Co.	El Paso	george.benoit@elpaso.com
ANR Storage Co.	El Paso	george.benoit@elpaso.com
Black Marlin Pipeline Co.	Williams	Thomas.R.Odom@Williams.com
Blue Lake Gas Storage Co.	El Paso	robert.white@elpaso.com
Canyon Creek Compression Co.	K. Morgan (KM)	mark_mayworn@kindermorgan.com
Carnegie Interstate Pipeline Co.	Equitrans	amurphy@eqt.com
Chandeleur Pipe Line Co.	ChevronTexaco	GBKO@ChevronTexaco.com
Colorado Interstate Gas Co.	El Paso	bennie.barnes@elpaso.com
Columbia Gas Transmission Corp.	Columbia	jswatzel@nisource.com
Columbia Gulf Transmission Co.	Columbia	jswatzel@nisource.com
Cove Point LNG, L.P.	Dominion	brian_c_sheppard@dom.com
Crossroads Pipeline Co.	Columbia	jswatzel@nisource.com
Discovery Gas Transmission LLC	Williams	Thomas.R.Odom@Williams.com
Dynegy Midstream Pipeline, Inc.		rich.a.mueller@dynegy.com
East Tennessee Natural Gas Co.	Duke Energy	scrapp@duke-energy.com
Egan Hub Partners, L.P.	Duke Energy	scrapp@duke-energy.com
El Paso Natural Gas Co.	El Paso	bennie.barnes@elpaso.com
El Paso Field Services	El Paso	pat.davis@elpaso.com
Energy East		spmartin@energyearth.com
EPGT Texas Pipeline, L.P.	El Paso	pat.davis@elpaso.com
Equitrans, Inc.		amurphy@eqt.com
Florida Gas Transmission Co.	Enron	mcrump@enron.com
Granite State Gas Transmission, Inc.	Columbia	jswatzel@nisource.com
Great Lakes Gas Transmission, L.P.		rgrondin@glgt.com
Gulf South Pipeline		scott.williams@gulfsouthpl.com
Gulf States Transmission Corp.	El Paso	george.benoit@elpaso.com
High Island Offshore System	El Paso	george.benoit@elpaso.com
Iroquois Gas Transmission System		ben_gross@iroquois.com
Kansas Pipeline Co.	Midcoast Energy Enbridge	scott.ironside@enbridge.com
Kentucky West Virginia Gas Co.	Equitrans	amurphy@eqt.com
Kern River Gas Transmission Co.	Williams	Thomas.R.Odom@Williams.com
Keyspan Energy		psheth@keyspanenergy.com
KM Interstate Gas Transmission Co.	KM	mark_mayworn@kindermorgan.com
KN Wattenberg Transmission	KM	mark_mayworn@kindermorgan.com
Maritimes & Northeast Pipeline L.L.C.	Duke Energy	scrapp@duke-energy.com
Michigan Gas Storage Co.	Consumers Energy	rswelsh@cmsenergy.com
Midwestern Gas Transmission Co.	Enron	mcrump@enron.com

Organization	Location	Email Address
MIGC, Inc.	Western Gas	jcurtis@westerngas.com
Mississippi River Transmission Corp.	CenterPoint Energy	scott.mundy@centerpointenergy.com
Mojave Pipeline Co.	El Paso	bennie.barnes@elpaso.com
National Fuel Gas Supply Corp.		pustulkaj@natfuel.com
Natural Gas Pipeline Co. of America	KM	mark_mayworn@kindermorgan.com
Nora Transmission Co.	Equitrans	amurphy@eqt.com
North Carolina Natural Gas	Carolina Power & Light	Theodore.hodges@cplc.com
Northern Border Pipeline Co.	Enron	mcrump@enron.com
Northern Natural Gas Co.	Midamerican Energy	paul.fuhrer@nngco.com
Northwest Pipeline Corp.	Williams	Thomas.R.Odom@Williams.com
Overthrust Pipeline Co.	Questar	ronji@questar.com
Oncor Gas		mrothba1@oncorgroup.com
Ozark Gas Transmission System		strawnlw@oge.com
Paiute Pipeline Co.	Southwest Gas	jerry.schmitz@swgas.com
Panhandle Eastern Pipe Line Co.	CMS	smgallagher@cmsenergy.com
Petal Gas Storage Co.	El Paso	bennie.barnes@elpaso.com
PG&E Gas Transmission-Northwest Corp.	PG&E	WJH7@pge.com
PG&E Gas Transmission-Northwest Corp.	PG&E	ADE1@pge.com
Questar Pipeline Co.	Questar	ronji@questar.com
Reliant Energy Gas Transmission Co.	CenterPoint Energy	scott.mundy@centerpointenergy.com
Sabine Pipe Line Co.	ChevronTexaco	GBKO@ChevronTexaco.com
Sea Robin Pipeline Co.	CMS	smgallagher@cmsenergy.com
Shell Offshore Pipelines	Shell	janiemeyer@shellopus.com
Southern Natural Gas Co.	El Paso	george.benoit@elpaso.com
Southwest Gas Corp.		jerry.Schmitz@swgas.com
Southwest Gas Storage Co.	CMS	smgallagher@cmsenergy.com
Steuben Gas Storage Co.	ANR/Arlington	george.benoit@elpaso.com
Tennessee Gas Pipeline Co.	El Paso	george.benoit@elpaso.com
Texas Eastern Transmission Corp.	Duke Energy	scrapp@duke-energy.com
Texas Gas Transmission Corp.	Williams	Thomas.R.Odom@Williams.com
Total Peaking LLC	Energy East	spmartin@energyearth.com
Trailblazer Pipeline Co.	KM	mark_mayworn@kindermorgan.com
TransColorado Gas Transmission Co.	KM	mark_mayworn@kindermorgan.com
Transcontinental Gas Pipe Line Corp.	Williams	Thomas.R.Odom@Williams.com
Transwestern Pipeline Co.	Enron	mcrump@enron.com
Trunkline Gas Co.	CMS	smgallagher@cmsenergy.com
Trunkline LNG Co.	CMS	smgallagher@cmsenergy.com
Tuscarora Gas Transmission Co.		lcherwenuk@tuscaroragas.com
TXU Gas/TXU Lone Star Pipeline	TXU Gas	mrothba1@oncorgroup.com
Vector Pipeline	Enbridge	scott.ironside@enbridge.com
Venice Gathering System, L.L.C.	Dynergy	rich.a.mueller@dynegy.com

Organization	Location	Email Address
Viking Gas Transmission Co.	Northern Border (Enron)	mcrump@enron.com
Williams Gas Pipelines Central, Inc.	Williams	Thomas.R.Odom@Williams.com
Williston Basin Interstate Pipeline Co.		keith.seifert@wbip.com
Wyoming Interstate Co., Ltd.	El Paso	bennie.barnes@elpaso.com
Young Gas Storage Co., Ltd.	El Paso	bennie.barnes@elpaso.com

## Other Natural Gas Pipeline Operating Companies Contact Names and Phone Numbers

(As of 7/9/03)

Organization	POC Name	Phone Number
Algonquin Gas Transmission Co.	Steve Rapp	713 627 6394
Algonquin LNG, Inc.	Steve Rapp	713 627 6394
Alliance Pipeline Ltd.	Arti Bhatia	403 517 7727
ANR Pipeline Co.	George Benoit	832 528 4244
ANR Storage Co.	George.Benoit	832 528 4244
Black Marlin Pipeline Co.	Thomas Odom	270 688 6964
Blue Lake Gas Storage Co.	Robert White	248 994 4046
Canyon Creek Compression Co. K. Morgan	Mark Mayworn	713 369 9347
Carnegie Interstate Pipeline Co.	Andy Murphy	412 231 4888
Chandeleur Pipe Line Co.	George Kohut	510 242 3245
Colorado Interstate Gas Co.	Bennie Barnes	719 520 4677
Columbia Gas Transmission Corp.	Jim Swatzel	304 357 2797
Columbia Gulf Transmission Co.	Jim Swatzel	304 357 2797
Cove Point LNG Limited Partnership	Brian Sheppard	304 627 3733
Crossroads Pipeline Co.	Jim Swatzel	304 357 2797
Discovery Gas Transmission LLC	Thomas Odom	270 688 6964
Dynegy Midstream Pipeline, Inc.	Rich Mueller	713 507 3992
East Tennessee Natural Gas Co.	Steve Rapp	713 627 6394
Egan Hub Partners, L.P.	Steve Rapp	713 627 6394
El Paso Field Services	Pat Davis	210 528 4244
El Paso Natural Gas Co.	Bennie Barnes	719 520 4677
Energy East	Scott Martin	607 347 2561
EPGT Texas Pipeline, L.P.	Pat Davis	210 528 4244
Equitrans, Inc.	Andy Murphy	412 231 4888
Florida Gas Transmission Co.	Michael Crump	713 345 1623
Granite State Gas Transmission, Inc.	Jim Swatzel	304 357 2797
Great Lakes Gas Transmission L.P.	Ryan Grondin	321 439 1777
Gulf South Pipeline	Scott Williams	713 544 5220
Gulf States Transmission Corp.	George Benoit	832 528 4244
High Island Offshore System	George.Benoit	832 528 4244
Iroquois Gas Transmission System, L.P.	Ben Gross	203 925 7257
Kansas Pipeline Company	Scott Ironside	780 420 5267
Kentucky West Virginia Gas Co.	Andy Murphy	412 231 4888
Kern River Gas Transmission Co.	Thomas Odom	270 688 6964
Keyspan Energy	Perry Sheth	516 545 3844
KM Interstate Gas Transmission Co.	Mark Mayworn	713 369 9347
KN Wattenberg Transmission	Mark Mayworn	713 369 9347
Maritimes & Northeast Pipeline L.L.C.	Steve Rapp	713 627 6394
Michigan Gas Storage Co.	Robert Welsh	517 788 1928
Midwestern Gas Transmission Co.	Michael Crump	713 345 1623
MIGC, Inc.	John Curtis	

Organization	POC Name	Phone Number
Mississippi River Transmission Corp.	Scott Mundy	318 429 3943
Mojave Pipeline Co.	Bennie Barnes	719 520 4677
National Fuel Gas Supply Corp.	John Pustulka	716 857 7909
Natural Gas Pipeline Co. of America	Mark Mayworn	713 369 9347
Nora Transmission Co.	Andy Murphy	412 231 4888
North Carolina Natural Gas	Ted Hodges	919 546 6369
Northern Border Pipeline Co.	Michael Crump	713 345 1623
Northern Natural Gas Co.	Paul Fuhrer	402 398 7733
Northwest Pipeline Corp.	Thomas Odom	270 688 6964
Oncor Gas	Mark Rothbauer	214 875 5574
Overthrust Pipeline Co.	Questar	ronji@questar.com
Ozark Gas Transmission System	Larry Strawn	405 557 5271
Paiute Pipeline Co.	Jerry Schmitz	702 365 2204
Panhandle Eastern Pipe Line Co.	Scott Gallagher	713 989 7444
Petal Gas Storage Co.	Bennie Barnes	719 520 4677
PG&E Gas Transmission-Northwest Corp.	Bill Harris	925 974 4030
PG&E Gas Transmission-Northwest Corp.	Alan Eastman	925 974 4312
Questar Pipeline Co.	Questar	ronji@questar.com
Reliant Energy Gas Transmission Co.	Scott Mundy	318 429 3943
Sabine Pipe Line Co.	George Kohut	510 242 3245
Sea Robin Pipeline Co.	Scott Gallagher	713 989 7444
Shell Offshore Pipelines	John Niemeyer	713 241 1856
Southern Natural Gas Co.	George Benoit	832 528 4244
Southwest Gas Corp.	Jerry Schmitz	702 365 2204
Southwest Gas Storage Co.	Scott Gallagher	713 989 7444
Steuben Gas Storage Co.	George Benoit	832 528 4244
Tennessee Gas Pipeline Co.	George Benoit	832 528 4244
Texas Eastern Transmission Corp.	Steve Rapp	713 627 6394
Texas Gas Transmission Corp.	Thomas Odom	270 688 6964
Total Peaking LLC	Scott Martin	607 347 2561
Trailblazer Pipeline Co.	Mark Mayworn	713 369 9347
TransColorado Gas Transmission Co.	Mark Mayworn	713 369 9347
Transcontinental Gas Pipe Line Corp.	Thomas Odom	270 688 6964
Transwestern Pipeline Co.	Michael Crump	713 345 1623
Trunkline Gas Co.	Scott Gallagher	713 989 7444
Trunkline LNG Co.	Scott Gallagher	713 989 7444
Tuscarora Gas Transmission Co.	Les Cherwenuk	775 834 3674
TXU Gas/TXU Lone Star Pipeline	Mark Rothbauer	214 875 5574
Vector Pipeline	Scott Ironside	780 420 5267
Venice Gathering System, L.L.C.	Rich Mueller	318 429 3943
Viking Gas Transmission Co.	Michael Crump	713 345 1623
Williams Gas Pipelines Central, Inc.	Thomas Odom	270 688 6964
Williston Basin Interstate Pipeline Co.	Keith Seifert	406 359 7223
Wyoming Interstate Company, Ltd.	Bennie Barnes	719 520 4677
Young Gas Storage Company, Ltd.	Bennie Barnes	719 520 4677