

Final Report: Pilot-scale Cross-flow Filtration Test - Envelope A + Entrained Solids

by

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**Final Report: Pilot-scale Cross-flow Ultrafiltration Test Using a Hanford Site Tank
241-AN-105 Waste Simulant – Envelope A + Entrained Solids**

February 23, 2000

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SUMMARY

This report discusses the results of the operation of a cross-flow filter in a pilot-scale experimental facility that was designed, built, and run by the Experimental Thermal Fluids Laboratory of the Savannah River Technology Center of the Westinghouse Savannah River Company. This filter technology was evaluated for its inclusion in the pretreatment section of the nuclear waste stabilization plant being designed by BNFL, Inc. The plant will be built at the U.S. Department of Energy's Hanford Site as part of the River Protection Project.

The filter element under study was recommended by BNFL, Inc. and it was manufactured by the Mott Metallurgical Corporation in Connecticut. The filter unit contained seven 316 stainless steel sintered metal tubes. Each tube had an inside diameter of 0.375 inch, an outside diameter of 0.5 inch, a porous length of 40 inches, and a filter pore size that is classified as a nominal rated 0.1 micron. These dimensions give an active filter surface area of 2.29 ft². At the time of this task these aforementioned dimensions were given as prototypic, therefore each filter tube was considered full size to the filter, which would be built for the plant. Only the number of tubes was expected to change.

The filter was tested with a simulated nuclear waste of Tank 241-AN-105, which is referred to as envelope A waste. The recipe for the simulant was developed by Waste Process Technology section of SRTC and the simulant was made by TFL personnel specifically for this task. The supernatant portion of the simulant was non-organic, alkaline, pH > 14, and had molarities of sodium, nitrates, and nitrites, of approximately 5 M, 1.4 M, and 1.2 M, respectively. To the supernatant insoluble solids were added to simulate those in the real waste. The solids loading began at 0.5 wt% and then was eventually raised to about 16 wt% during the test. The particle sizes ranged from 0.5 to 5 microns by design. At 25°C, and a solids loading of 0.5 wt%, this slurry had a density of approximately 1.23 g/mL, a viscosity of 3 cP, and Newtonian rheological characteristics. However, as the solids loading increased a yield stress was present, but it dropped very fast to revert to a Newtonian fluid while in motion. The flow conditions for the test varied: Axial slurry velocities ranged from 3 ft/s to 15 ft/s (1 m/s to 4.6 m/s) and transmembrane pressures ranged from 15 psid to 70 psid (100 kPa to 480 kPa) at a temperature of 25°C.

The results showed a good filtrate flux and separation. Under the optimum flow conditions of a slurry velocity of 12.4 ft/s and a transmembrane pressure of 42 psid (3.8 m/s and 300 kPa), the observed filtrate flux was consistently greater than 0.10 gpm/ft² (4.1 lpm/m²), even without backpulsing for more than 7 hours. However, a backpulse frequency of 30 minutes would increase the flux to 0.16 gpm/ft² (6.5 lpm/m²). A filtrate flux could be maintained above 0.10 gpm/ft² as the insoluble solids loading increased to 16 wt% and at no time did the filter plug from a slurry cake build up. To free the filter surface of the slurry cake, a volume of only 0.036 gal/ft² (1.17 liters/m²) was needed. This backpulse volume leads to a lost flux of 0.0012 gpm/ft² (0.05 lpm/m²) for a backpulse frequency of 30 minutes. Finally, for all test runs the measurable amount of insoluble solids was insignificant in the filtrate.

ACKNOWLEDGMENTS

The author would like to thank all that were involved in this task. Andy Foreman's care and dedication in running this experiment allowed it to be successfully completed. Support from the other Experimental Thermal Fluids Laboratory personnel: Mike Armstrong, Vern Bush, Jimmy Mills, and Jerry Corbett was instrumental in keeping the experiment on track and maintaining the test rig ready, from instrumental calibration to last minute changes that were needed due to unforeseen difficulties. The Lab supervisor, Susan Hatcher, is to be commended for keeping us safe, even when things seemed to be the most hectic. A special thanks is in order to all those individuals just mentioned for the long hours they invested in the experiment, which at times disrupted their family life. I would also like to thank Charles Nash and John Steimke for their help in planning the test from their expertise and past work in filtration. The management of both Dan Burns and Martha Ebra made this task's successful completion a sure thing. Thanks to Hector Guerrero who had the unenviable task of reviewing this report, and to Gwen Watts, who would probably want to forget all the cutting and pasting. Finally, I would like to thank both my SRS customer, Steve Wach, and my BNFL customers, Paul Townson and Mike Johnson, for their support and insight, which made this work possible.

NOMENCLATURE

BNFL	BNFL, Inc.
DIF	Deionized and Filtered (0.2 micron) Water
i.d.	Inside Diameter
LAW	Low Activity Waste
nominal	The word "nominal" for a filter rating is a vague term because its meaning is manufacturer depend. Further, a "nominal" rating does not give an exact size to a filter medium; but rather an approximation to the expected performance of a filter. In the case of Mott, a nominal rated 0.1- μ m filter means that approximately 95% of particles greater than 0.1 μ m will not pass the filter.
RPP	River Protection Project
o.d.	Outside Diameter
SRTC	Savannah River Technology Center
TMP	Transmembrane Pressure (the average pressure drop across the thickness of the filter medium – perpendicular to the slurry flow.)
TR	Test Rig
TTR	Technical Task Request
V	Velocity of the slurry flow along the length of the filter tubes
WPT	Waste Processing Technology
WSRC	Westinghouse Savannah River Company
XF	Cross-flow Filter

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INTRODUCTION

BNFL, Inc. (BNFL) has been contracted by the Department of Energy to design a facility to stabilize liquid radioactive waste that is stored at the Hanford Site. Because of its experience with radioactive waste stabilization, the Savannah River Technology Center (SRTC) of the Westinghouse Savannah River Company is working with BNFL to help design and test certain parts of the waste treatment facility. One part of the process is the separation of radioactive solids from the liquid wastes by cross-flow filtration. This task tested a cross-flow filter with a simulated radioactive waste, made to prototypically represent the waste chemical and physical characteristics.

This technical baseline research and development work was initiated by a Technical Task Request (TTR) (1) that was issued in October of 1998. This TTR came about from the BNFL specifications (2, 3) to design and test a pilot scale cross-flow filtration system. With initial documentation in place (4, 5, 6) the task began by defining a slurry to be filtered. A recipe for a low activity waste (LAW) slurry simulant, which would contain entrained solids, was developed by the Waste Process Technology section of SRTC to represent the waste in Hanford Tank 241-AN-105 (7, 8). This waste is referred to as Envelope A waste. At the beginning of this task the exact composition of the complex slurry was not completely defined, however, enough information did exist to begin work by modifying an existing test rig and getting the appropriate approvals to insure its safe operation (9, 10, 11). Previous work (12, 13, 14) assisted in guiding the plan of this task.

Envelope A simulant was the first in a series of two that would be used in this task. This report deals solely with this first simulant to evaluate a cross-flow filter. The chosen filter was manufactured by the Mott Metallurgical Corporation to meet the required specification (2, 3):

- 7 filter tubes with each having an inside diameter of 0.375 inch
- 40-inch porous length for each filter tube and made of stainless steel
- Nominal rated 0.1 micron filter element (the Nomenclature explains 'nominal')

and the test rig was modified to meet the required specification (2, 3):

- Maximum recirculation flow of 5 m/s (16 ft/s)
- Maximum transmembrane pressure (TMP) of 80 psid
- Maximum recirculation flow to be achievable at the maximum TMP
- Instrumentation to monitor the recirculation flow rate, the filtrate flow rate, the TMP, and the slurry temperature
- All materials to be compatible with 1 M nitric acid solution

All specifications were met or exceeded. A short history of task activities is:

- Arrival of the filter from Mott - February 19, 1999
- Shakedown activities began - March 1, 1999
- Envelope A simulant was defined - March 2, 1999
- Simulant was made - April 16, 1999
- Permission was received from BNFL to begin testing - May 12, 1999
- Test was completed - July 26, 1999
- Preliminary data were sent to BNFL on November 9, 1999 (15)

EXPERIMENTAL

Equipment

In general, the equipment assembled for this task was done to conform to the Test Specification (2, 3). To facilitate understanding of the experimental equipment an explanation of the salient features follows.

Test Rig

Figure 1 is a schematic of the entire Test Rig (TR) and Fig. 2 is a photograph of the same. It stood approximately 25-feet tall and was serviced by a two-level mezzanine. The TR was much taller than the 3-foot tall filter element because it originally was used to test a 10-foot tall filter in 1994 (12). Several modifications were made in order to install the meter-long cross-flow filter. The entire TR was made of 300 series stainless steel with the majority being of 304 stainless steel.

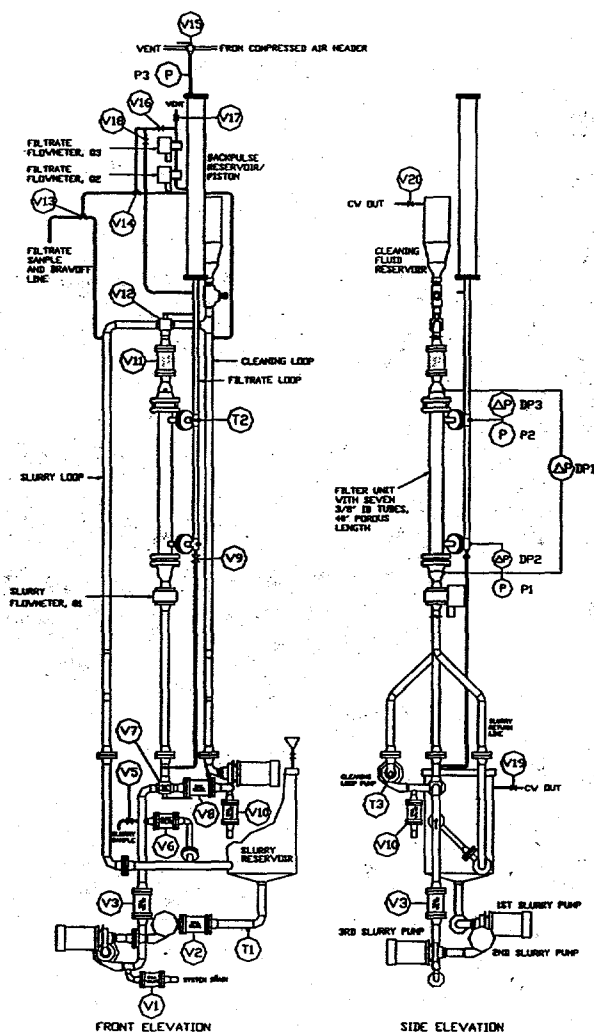


Figure 1. Schematic of the Pilot-scale Cross Flow Ultrafiltration Test Facility



Figure 2. Pilot-scale Cross Flow Ultrafiltration Test Facility

The TR is made up of three basic flow loops:

1. Slurry loop, which contains the filter and its housing and serves as the primary flow path for circulating slurries. This loop has an internal volume of approximately 20 liters, excluding the reservoir tank.
2. Filtrate loop, which begins at the filter housing and allows the separated filtrate liquid to flow up through the backpulse piston before returning to the top of the slurry loop to close the circuit. This loop has an internal volume of approximately 6 liters.
3. Cleaning loop, which enables cleaning of the filter in place without having to remove the slurry from the test rig by correctly orienting two 3-way valves. This loop has an internal volume of approximately 15 liters.

Two other flow circuits that are subsections of the other loops are the backpulse and the recirculations loops:

1. The backpulse loop is part of the filtrate loop and stands ready to reverse the flow of filtrate. A pulse forces filtrate back through the seven filter elements in order to knock off built-up slurry cake on the inside diameter of the porous tubes. [The backpulse piston assembly controls the amount of filtrate used for a backpulse. The maximum piston travel was 2 inches, but it was initially set at $\frac{3}{4}$ inch to inject 0.041 gallon back through the filter (the piston housing inside diameter is 4.026 inches) to attain a 0.018 gal/ft² (the filter inside surface area was 2.29 ft²), as was found in a previous filtration test (12). However, starting with test run 2.09 on 5/20/99 the injection volume was doubled to 0.036 gal/ft² because it showed a considerable improvement in the filtrate flux recovery. Even with this volume, a backpulse frequency of 30 minutes would cause an insignificant reduction in the mean filtrate flux of 0.0012 gpm/ft².]
2. The recirculation loop is part of the slurry loop (by using valve V6). This loop is used to: better control the slurry flow, increase mixing, and keeps the slurry well-mixed when the flow through the filter needs to be stopped.

The TR is controlled through a series of valves, which are described below:

- V1: Drains slurry from the test rig
- V2: Isolates the slurry reservoir from the pumps
- V3: Controls the slurry (cleaning fluid) flow upstream of the filter and isolates the slurry loop from the pump
- V4: Allows liquid to be introduced to the slurry reservoir
- V5: Allows slurry to be samples (not used for this test)
- V6: Recirculates slurry to the reservoir
- V7: Directs either slurry (cleaning fluid) to the filter; 3-way valve
- V8: Used for the same functions as V3 but for the cleaning loop
- V9: Drains the filtrate loop
- V10: Drains the cleaning loop
- V11: Controls the slurry (cleaning fluid) flow downstream of the filter
- V12: Directs either slurry (cleaning fluid) from the filter; 3-way valve

- V13: Directs filtrate to the sample port or back to the slurry loop; 3-way valve
 V14: Directs filtrate to the to the slurry loop or to the cleaning loop; 3-way valve
 V15: Allows air to pressurize the backpulse piston
 V16: Shuts filtrate flow from the backpulse piston
 V13: Directs either filtrate to the sample port or back to the slurry loop; 3-way valve
 V17: Vents the test rig
 V18: Allows filtrate to bypass the backpulse piston
 V19: Allows coolant flow to the cooling coil in the slurry reservoir
 V20: Allows coolant flow through the cooling coil in the cleaning fluid reservoir

To circulate slurries and liquids the test rig and mixing tank were serviced by five TEEL stainless steel centrifugal pumps:

Location	Model hp	Housing	Materials			Seals
			Shaft	Impeller	Sleeve	
1.Slurry Loop	2P392 3	304SS	304SS	303SS		Graphite/Ceramic/Viton
2.Slurry Loop	2P392 3	304SS	304SS	303SS		Graphite/Ceramic/Viton
3.Slurry Loop	2P392 3	304SS	304SS	303SS		Graphite/Ceramic/Viton
4.CleaningLoop	2P392 3	304SS	304SS	303SS		Graphite/Ceramic/Viton
5.Mixing Tank	1P701B ¾	304SS	304SS	416SS		Graphite/Ceramic/Viton

Three 3 hp pumps were used in series on the slurry loop to attain the head of 80 psig at 40 gpm (~5 m/s) since one pump is able to produce about 28 psi at 40 gpm with water.

Cross Flow Filter

The heart of this entire experimental task was the cross-flow filter element that was to be tested to define its operational characteristics under required flow conditions. There were several candidates that could have been used for this test but due to availability and past experience in robust designs a Mott Filter was chosen. The specifications for the filter unit were:

Material:	316 stainless steel (sintered metal)
Porosity:	nominal rated 0.1 micron
Length:	40 inches
Diameter:	3/8-inch I.D., 1/2-inch O.D.
Number:	7 tubes

The unit which was received from Mott met the requirements, see Figs. 3, 4, and 5. The 40-inch length was made from two 20-inch lengths that were welded together at the center. [When subtracting the weldments at the end and middle of the tubes, the actual active porous length was 39 3/4 inches (1.01 meter)]. The 7 tubes were welded together with the tube sheets and extra support was made with a central stabilizing plate and supporting solid metal 1/4-inch rods which ran the length of the tube bundle, Fig. 3c. From the figures it is possible to see that some of the porous surfaces were slightly marred. Because of the large surface area this marring was not expected to affect results and no effects were notice during testing. The tube housing, Figs. 4 and 5, was made

from a 3-inch schedule 10 pipe with two pipes connected at either end to remove filtrate. For this test the filter unit was oriented vertically in the test rig, see Figs. 1, 2, and 5. The tube bundle sat in the housing such that the large tube sheet (right side of Fig. 3a) was secured to the top flange of the housing; this tube sheet also supported the weight of the assembly. The smaller, lower, tube sheet (foreground in Fig. 3b) was able to pass through the housing and separated the slurry side of the flow channel from the filtrate side with an "O" ring between the outer perimeter of the lower tube sheet and the inside diameter of the filter housing.

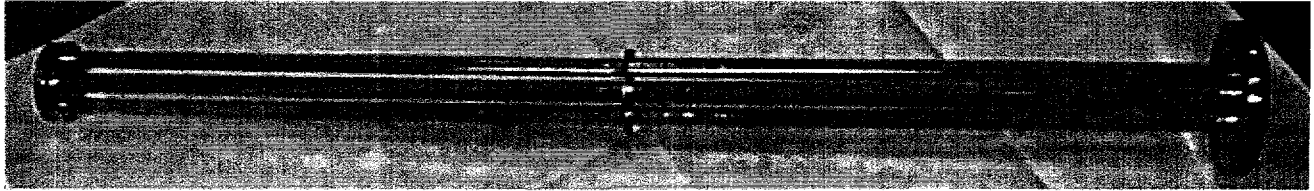


Figure 3a. 7-tube bundle of nominal rated 0.1 micron filter, 3/8" i.d., 1/2" o.d., 40" long

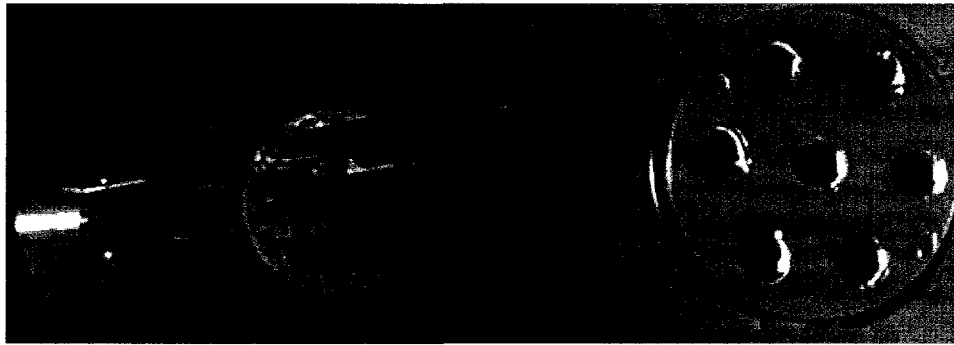


Figure 3b. Upstream view of the seven-tube bundle

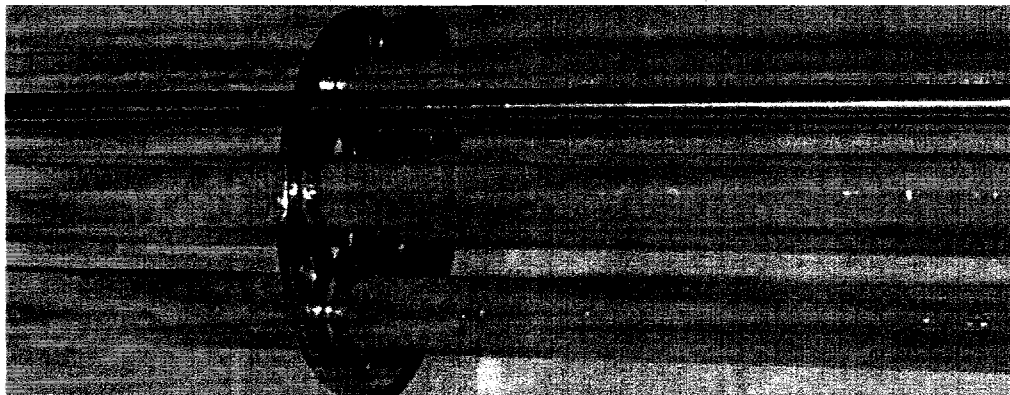


Figure 3c. Support plate at the mid-section of the seven-tube bundle

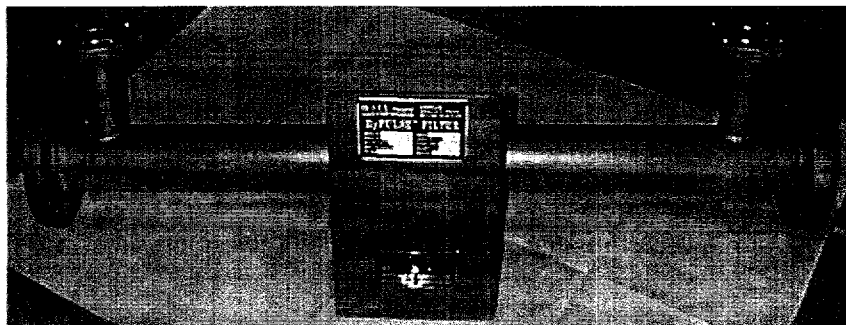


Figure 4. Cross-flow Filter Housing

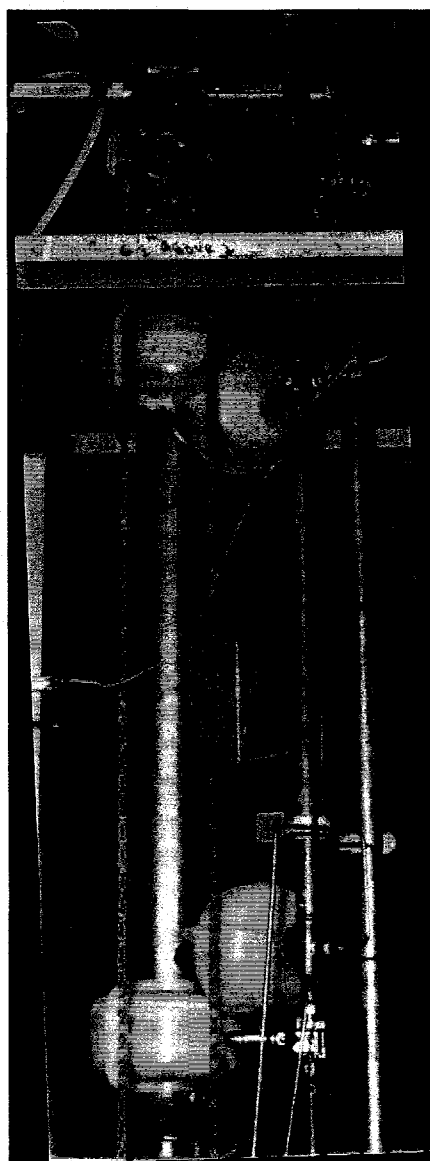


Figure 5. Cross-flow Filter in Test Rig

Mixing Tanks

There were two main tanks used for mixing and preparing the slurry solutions:

1. The slurry reservoir was a 110-liter plastic tank that primarily served as the Test Rig reservoir. It was also used (along with the recirculation loop) as a mixing tank when solids had to be added to the slurry and was the location from where slurry samples were taken. Mixing was accomplished with the recirculation loop by using valve V6. [The slurry reservoir is shown in Fig. 1 and is the large white tank in the foreground of Fig. 2.]
2. The mixing tank (MT) was a separate 110-liter plastic tank. It served to make the 75-liter batch of simulant supernate before the solids were added to complete the slurry. Since it was hard-piped to the slurry reservoir it was also used to make the cleaning fluid (1 M nitric acid) as well as the cleaning solution used to clean the entire test rig during shakedown activities (1% Alconox solution – phosphate). Mixing was accomplished with the recirculation loop by using valve V23. [Figure 6 is a schematic of this tank and can be found in Fig. 2 as the lower white tank behind the vertical I-beam at the lower right side of the photograph.]

The MT is controlled through a series of valves, which are described below:

- V21: Controls the flow to the pump
- V22: Drains the MT
- V23: Recirculates the contents of the MT
- V24: Allows the mixed contents to enter the slurry reservoir
- V25: Allows liquid to be introduced into the MT

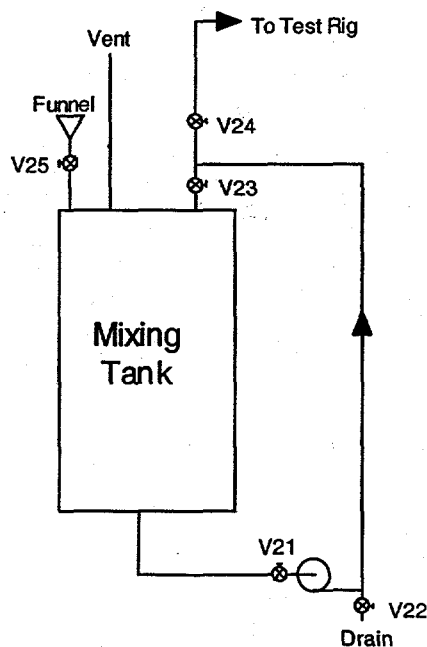


Figure 6. Main Mixing Tank for the Experiment

Instrumentation

The measurement equipment used for this experiment was:

- 5 Type E thermocouples with accuracies from* 1.0 to 1.5°C,
- 6 Variable capacitance pressure transducers with accuracies from* 0.02 to 0.38 psi, and
- 3 Magnetic flow meters with accuracies from* 0.005 to 0.19 gpm.

*accuracies are a function of the instrument and calibration. The uncertainty introduced through the use of the 16-bit data acquisition system was insignificant (<0.1% reading) and was not included in the values above.

Figure F1, Appendix F, shows two tables which list all the instruments and data acquisition system (DAS) channels for each of the non-thermocouple instruments. The thermocouples had their own dedicated computer card to interface and convert the temperatures properly. The calibration of the DAS was checked and that information can also be found in Fig. F1, which includes tables and graphs that show the results and the transfer functions used for each channel.

Two instrument changes were made during this task:

1. On 3/24/99, the pressure transducer used for dP2 (No. TR-00532). was recalibrated to reduce the calibrated pressure range so that the measurement uncertainty was reduced to 0.13 psid from 0.42 psid. Even though the actual experiment did not begin until May of 1999, the pre-3/24/99 calibration was used in obtaining certain shakedown data for water and thus it is included for completeness.
2. On 7/14/99, another filtrate flowmeter was added (Q3; No. TR-03562). By this date the experiment was complete, except for the final water run 2.22. This new flow meter increased the measurable range for filtrate flow from a maximum of 1.2 gpm to 5 gpm, or the flux from 0.52 gpm/ft² to 2.18 gpm/ft², respectively. However, the measurement uncertainty for the larger filtrate flow rate was larger by a factor of four. This new meter was only necessary for the water runs, since with slurry, the filtrate fluxes were always below 0.5 gpm/ft².

From Figs. 1, F1, and F2 the location and the usage of each instrument can be determined, however the following list will better describe the placement and usage of all the measurement instruments:

- T1 – A thermocouple located in the exit pipe of the slurry reservoir to measure the slurry temperature on its way to the filter.
- T2 – A thermocouple located in the filtrate line at the end of the upper filter housing filtrate exit pipe to measure the filtrate temperature as it leaves the filter housing.
- T3 – A thermocouple located in the cleaning loop at the exit of the cleaning loop pump.
- T4 – A thermocouple located at the top of the test rig near valve V13 to measure ambient temperature.
- T5 – A thermocouple located at the bottom of the test rig near valve V5 to measure ambient temperature.

For the 6 pressure transducers also refer to Fig. F2, which indicates, pressure-line locations as well as their heights.

P1 – A gauge pressure transducer located at the beginning of the filter housing to measure the pressure of the slurry just before entering the filter tubes.

P2 – A gauge pressure transducer located in the filtrate line at the end of the upper filter housing filtrate exit pipe to measure the pressure of the filtrate as it leaves the filter housing.

P3 – A gauge pressure transducer located at the air side of the backpulse piston to measure the pressure applied to produce a backpulse.

dP1 – A differential pressure transducer located across the slurry side of the filter to measure the drop in pressure along the filter tubes.

dP2 – A differential pressure transducer located across filter and housing at the filter entrance to measure the transmembrane pressure at the beginning of the filter.

dP3 – A differential pressure transducer located across filter and housing at the filter exit to measure the transmembrane pressure at the end of the filter.

[The transmembrane pressure is determined from the average of dP2 and dP3.]

Q1 – A magnetic flowmeter located at the entrance of the filter to measure the slurry flowrate.

Q2 – A magnetic flowmeter located at the filtrate line between the exit of the backpulse piston and valve V16 to measure the filtrate flowrate.

Q3 – A magnetic flowmeter located at the filtrate line between the exit of the backpulse piston and valve V16 to measure the filtrate flowrate.

Measurement Uncertainty

Appendix F has all the pertinent information on the uncertainties. The measurement uncertainties (at a 95% confidence level) for the important calculated quantities are:

Slurry Velocity in a Filter Tube	=	V	± 8.16 %
Transmembrane Pressure	=	TMP	± 1.07 %
Temperature Corrected Filtrate Flux	=	Fc	± 6.72 %
Permeability	=	P	± 6.80 %

These numbers are based on pre- and post-test calibrations of the instruments.

Simulated Waste Slurry

Beside the cross-flow filter, the most important aspect of this experiment was the slurry used to simulate a Hanford Site waste. The waste that was simulated is referred to as Envelope A + ES. The Envelope A components include soluble radioactive wastes in tank 241-AN-105 from the Hanford Site and the ES refers to the insoluble Entrained Solids from that tank. The simulant used for this task was cold (non-radioactive), but made chemically equivalent to actual waste. The actual simulant development is beyond the scope of this task and not elaborated here. A recipe for the simulant supernate, Fig. 7,

Complete Envelope A Recipe at 5.5 Molar Na
(valid as of 4/13/99)

Volume of Feed 1000 mL

Needed
grams

Fill the container with water 200

Transition Metals and Complexing agents

Compounds	Formula	Conc., PPM	M	grams
Boric Acid	H3BO3	126	2.43E-03	0.150
Calcium Nitrate	Ca(NO3)2.4H2O	102	5.13E-04	0.121
Cesium Nitrate	CsNO3	10	6.27E-05	0.012
Magnesium Nitrate	Mg(NO3)2.6H2O	25	1.14E-04	0.029
Potassium Nitrate	KNO3	8302	9.77E-02	9.880
Zinc Nitrate	Zn(NO3)2.6H2O	20	7.94E-05	0.024
Glycolic Acid	HOCH2COOH, 70 wt%	719	7.88E-03	0.856
Sodium Chloride	NaCl	6472	1.32E-01	7.702
Sodium Fluoride	NaF	181	5.14E-03	0.216
Sodium Sulfate	Na2SO4	492	4.13E-03	0.586
Potassium Molybdate	K2MoO4	88	4.39E-04	0.105
Ammonium Acetate	CH3COONH4	221	3.42E-03	0.264

In a separate container mix the following

grams

Fill the container with water 300

Compounds	Formula	Conc., PPM	M	grams
Aluminum Trihydroxide	Al(OH)3	49574	7.56E-01	58.993
Sodium Hydroxide	NaOH	84956	2.53E+00	101.098
Sodium meta-silicate	Na2SiO3.9H2O	922	3.86E-03	1.097
Sodium Acetate	NaCH3COO.3H2O	1670	1.46E-02	1.987
Sodium Formate	HCOONa	1879	3.29E-02	2.236
Sodium Oxalate	Na2C2O4	401	3.56E-03	0.477
Sodium Phosphate	Na3PO4.12H2O	985	3.09E-03	1.173

Mix thoroughly. Then add this solution to the first solution. Then

Add	Formula	Conc., PPM	M	grams
Sodium Carbonate	Na2CO3	9567	1.07E-01	11.385

Mix thoroughly. Then

Add	Formula	Conc., PPM	M	grams
Sodium Nitrate	NaNO3	90607	1.27E+00	107.822
Sodium Nitrite	NaNO2	71911	1.24E+00	85.574

Mix thoroughly and dilute to the mark.

The final addition of water would be, needed = 298.2 grams
based upon a density of 1.25 g/mL

Final Weight	Needed grams
	1250

Figure 7. Envelope A Simulant: Supernate Only

and one for the simulant solids, Fig. 8, were obtained from the WSRC Waste Processing Technology group.

Envelope A Entrained Solids

Approximate Supernate Volume	1000.0	mL
Approximate Supernate Density	1.25	g/mL
Approximate Supernate Mass	1250.0	grams
At 0.5 wt% solids loading	6.28	grams
Total Mass Supernate + Solids	1256.3	grams

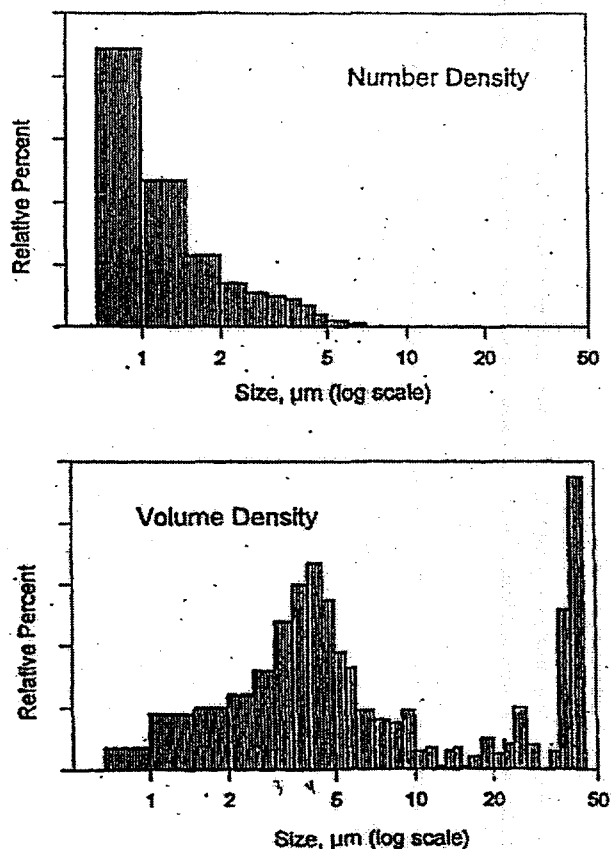
Compound*	Compound	Concentration	Needed
Name	Formula	g/100g solids	grams
Alumina	Al ₂ O ₃	9.20%	0.58
Calcium Oxalate	CaC ₂ O ₄	5.00%	0.31
Chromium Oxide	Cr ₂ O ₃	26.00%	1.63
Ferric Oxide	Fe ₂ O ₃	1.10%	0.07
Manganese Oxide	MnO ₂	0.30%	0.02
Sodium Oxalate	Na ₂ C ₂ O ₄	52.40%	3.29
Nickel Oxide	NiO	0.50%	0.03
Silicon Oxide	SiO ₂	5.40%	0.34
	Total	99.90%	6.28

* All compounds should be sized between 0.5 and 5 microns

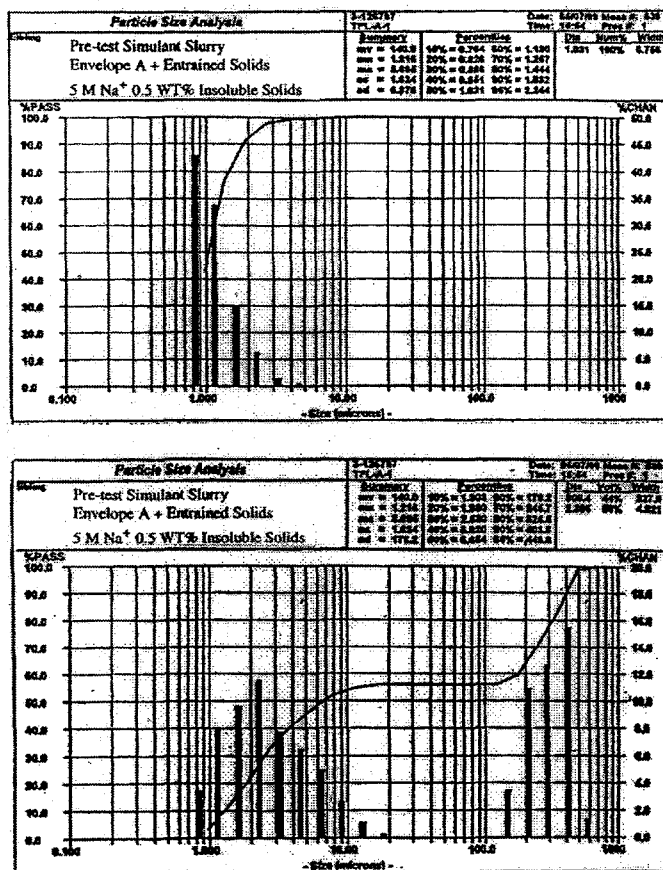
Figure 8. Envelope A Simulant: Solids Only – 0.5 wt%

Each recipe is shown on a per-liter basis. The test required a batch of 75 liters, therefore the quantities shown in both recipes were increased accordingly. (A volume of 75 liters was chosen to fill the slurry reservoir to the half-way mark, since the test rig proper held approximately 25 liters and the reservoir tank held 110 liters. The extra space was needed for foaming if it had occurred.) Along with the recipe for the solids, Fig. 8, the particle size distribution was specified: all particle should be between 0.5 and 5 microns based on the actual waste sampling, Fig. 9a. Therefore, all the solids indicated in Fig. 8 were purchased to that specification. Before adding the solids to the 75 liters of supernate the customer requested to evaluate the actual solids distribution. It was important to know if the purchased solids were of the correct size, as well as, what the distribution would be after the simulant was prepared. On 4/16/99 the 75 liters of supernate was made. On 4/19/99 a sample of 250 mL of the supernate was taken and

enough solids were added to obtain 0.5 wt%. Then the sample was submitted to determine the solids distribution. The distribution was obtained by Microtrac, Fig. 9b, on 5/12/99 and sent to the customer by facsimile transmission. On the same day the approval to begin testing was obtained. Both the actual waste and the simulant show a relatively small number of particles greater than 20 microns. In fact, for the simulant the large particles (thought to be soft sodium oxalate) eventually were broken up and do not show up in later distributions. Run 2.00 (water) began the following day and the simulant was finalized.



(a) Solids Distribution in Actual Waste Sample



(b) Solids Distribution in Waste Simulant

Figure 9. Insoluble Solids Distribution

Specifics about the simulant can be found in Appendix E: Analytical Data, but some general properties at 25°C were:

Slurry Density: ~1.23 g/mL at 0.5 wt% insoluble solids and 30 wt% total solids

Slurry Density: ~1.28 g/mL at 8 wt% insoluble solids and 36 wt% total solids

Slurry Viscosity: ~3 cP at 0.5 wt% insoluble solids and 30 wt% total solids

Slurry Viscosity (washed): ~2 cP at 12 wt% insoluble solids and 14 wt% total solids

Slurry Rheology ~Newtonian (at high insoluble solids loadings Bingham plastic characteristics are present, i.e., yield stress. See Figs, E2 and E3)
Supernate Density: ~1.21 g/mL at 36 wt% soluble solids
Supernate Viscosity: ~1.8 cP at 36 wt% soluble solids
Sodium [Na⁺] Conc: ~5 M

Test Procedure/Matrix

Details of the test matrix and test execution can be found in the Test Procedure (16) and the accompanying Operational Instructions (17), which are also listed in the task notebook (4). However, to facilitate understanding of the test's general operation, the procedural steps are summarized below:

Daily pre-test activities –

1. Equipment is turned on to warm up if not already on.
2. The equipment was checked for functionality and after each of the four liquid-filled pressure sensing lines (see Fig. F2; Appendix F) were purged with 5 ml of distilled and filtered water, the transducers were checked at their zeroes for drift. The zeroes are recorded for 2 to 3 minutes by the DAS. Those data are included in each day's data sheets.

Daily testing activities for constant solids runs (low and high concentrations) –

3. Begin circulating the slurry in the recirculation loop until the temperature reached 25°C.
4. Turn on the reservoir cooling coil.
5. Allow the slurry to flow through the cross-flow filter.
6. Set the appropriate flow conditions as per the test procedure by iterating between valves V3 and V1.
7. When the slurry and filtrate loops establish steady flows adjust the backpulse piston pressure to at least 30 psi over the slurry pressure in the filter.
8. Set the DAS to read every minute.
9. Backpulse the filter, hold the piston down for 10 seconds, then allow the filtrate flow to return. (At times this step had to be repeated so that the flow parameters could be set correctly. Also, because the filtrate had to refill the backpulse piston plenum, the filtrate-flow return-time was a function of the filtrate flux. As mentioned in "backpulse loop" description of the *Test Rig* section, the volume of the plenum was 0.036 gallon/ft², therefore the recovery time at 0.5 gpm/ft² was approximately 0.036 / 0.53 x 60 = 4 seconds. A flux of 0.53 gpm/ft² was taken because that was close to the filtrate flux right after a backpulse, Fig. 10.)

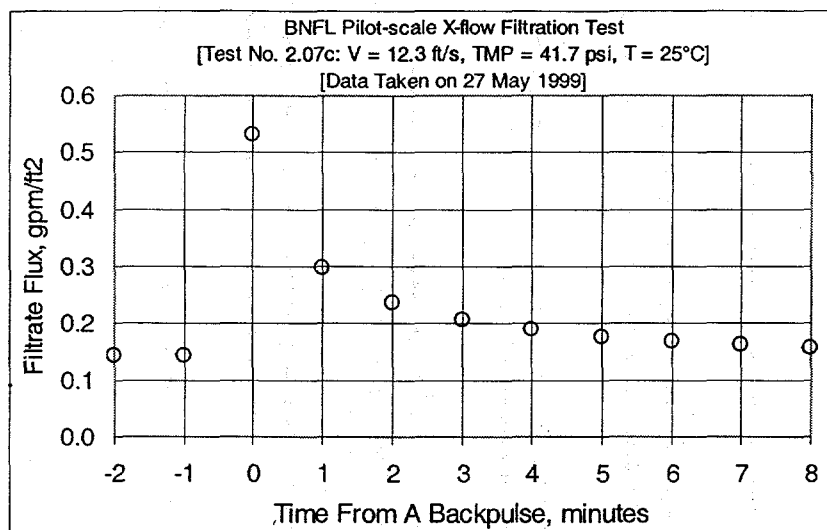


Figure 10. Filtrate flux immediately following a backpulse

10. Allow the test rig to run for approximately 2 hours.
11. Backpulse the filter once again.
12. Repeat from Step 6 for next set of flow conditions or shut down the test rig, if near the end of the work day.
13. End the test run.

Daily testing activities for wash test runs –

[Do Steps 3 to 9 from above, but just before Step 6 pour in a volume of distilled and filtered water equal to the volume of slurry in the test rig (~50 liters).]

10. Switch valve V13 to the open-loop position so that the filtrate is not returned to the slurry loop, but is collected outside the test rig.
11. Allow the test rig to run until a volume of filtrate is removed that is equal to the volume of water that was put in. (Slightly more mass is taken out than was put in because of the filtrate's higher density.)
12. Switch valve V13 to the close-loop position.
13. Backpulse the filter once again.
14. Repeat from Step 6 for each wash run until finished with all wash runs.
15. End the test run.

Daily testing activities for post-wash dewatering/plugging test run –

[Do Steps 3 to 9 from above.]

10. Switch valve V13 to the open-loop position so that the filtrate is not returned to the slurry loop, but is collected outside the test rig.
11. Continue run until either the filter or pumps do not allow further operation.
12. End the test run.

Shakedown

Before beginning test runs with water to evaluate the filter's hydraulic characteristics, the test rig (TR) was cleaned to remove any foreign contamination that may have been left inside the system from past testing or that could have been introduced when modifications were made. In March of 1999, before the new seven-tube filter unit was installed, the entire TR was cleaned with 1 wt% solution of Alconox in distilled and filtered (0.2 micron) water (referred to as DIF water). Fifty liters of this phosphate based solution was circulated in the TR for several hours at 35°C. This was followed with several DIF water rinses, until the water returned crystal clear. During the cleaning and rinsing the filter tubes were soaked in water for 4 days. With the TR clean and the filter installed, the slurry reservoir was filled with 75 liters of DIF water. Several runs were done with water to characterize the Mott filter.

A cross-flow filter (XF) is significantly different from a dead-end filter in that the main slurry flow is not forced through the filter medium. Instead, the slurry flows parallel to the filter substrate while allowing the filtrate to be removed perpendicularly, as a result of the transmembrane pressure (TMP). In this way the XF is basically self cleaning as the turbulent slurry flow tend to shear solids away from the filter wall as they try to adhere. However, because of this cross flowing stream, there is an added degree of freedom. For instance, an increase in slurry velocity may, but not necessarily, lead to an increase in filtrate flux. This is because the slurry system pressure can be made to decrease. That is, the slurry system pressure can be controlled independently from the slurry axial velocity and both of these quantities will affect the rate of filtrate flow. With this in mind, the following figures are shown to illustrate the character of the XF with DIF water, which contains no solids.

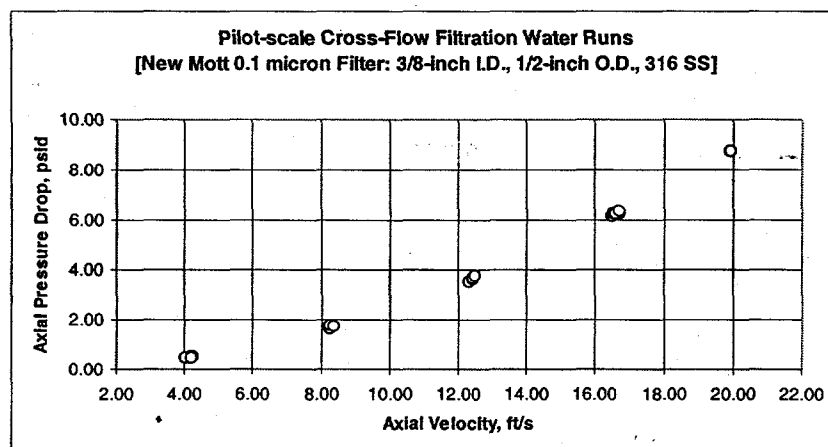


Figure 11. Axial pressure drop vs. axial velocity of water in the cross-flow filter

Figure 11 is the axial pressure drop versus the axial velocity. Those velocities came from the TR flow settings of 10, 20, 30, 40, and 50 gpm. These obtained results were expected because a pre-test calculation indicated that the pressure drop at 12.6 ft/s should be close to 4 psid, and it is. The calculation was not straight forward because to determine an

accurate pressure drop involves knowing the several contributions to that drop. Figures 1 and 5 show that the pressure taps were located in a diverging/converging plenum region on either side of the filter housing. Therefore the pressure drop is not only the drop along the porous filter tube, but it also includes the effects of the tube sheet inserts, expansion and contraction into the plenums, and the diverging and converging plenums themselves (where the pressure taps are located). A rough calculation determined that the actual axial pressure drop along just the porous section of tube is between 60% and 70% of the measured drop. Another aspect of Fig. 11 is the several data points shown for each combination of pressure drop and velocity. The system pressure at the filter was increased three fold from approximately 5 to 15 psig which resulted in filtrate fluxes from approximately 0.1 gpm/ft² to 0.5 gpm/ft². The increased pressure had a insignificant effect on the axial pressure drop as can be seen from the grouping of point in Fig. 11.

The effect of system pressure on filtrate flux at a fixed axial velocity is apparent in Fig. 12. The lines on the graph are isobars, or better, lines of constant transmembrane pressure (TMP). These data were obtained by adjusting the valves on the test rig to maintain a constant axial velocity while changing the system pressure. The highest TMP measured was at 4.4 psid due to the limitation of measuring filtrate flux to a maximum of 0.53 gpm/ft². This limitation existed because the expected filtrate flowrate of slurry was to be between 0.02 and 0.2 gpm/ft². Therefore, a flowmeter was calibrated to accurately measure that target range. However, it did limit measurement with water. Near the end of the experiment another meter was installed to measure up to 2.2 gpm/ft², so the final water-run (2.22) has higher TMPs.

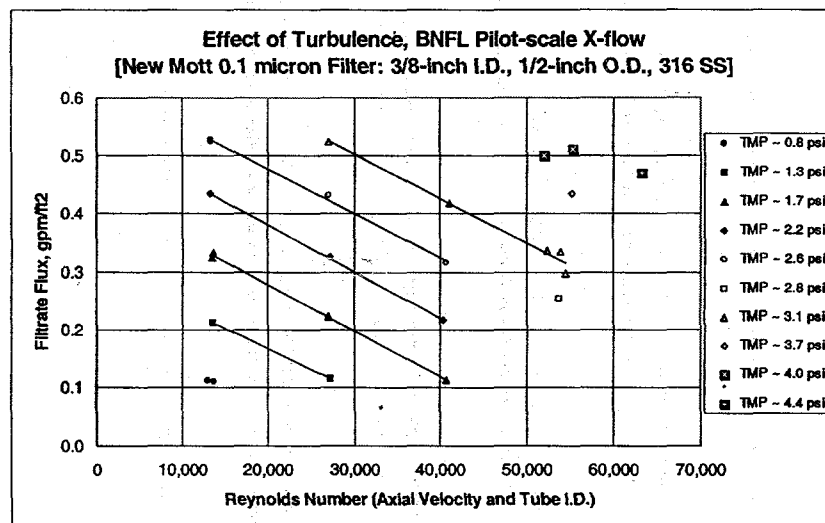


Figure 12. Filtrate flux vs. axial velocity of water in the cross-flow filter

What is interesting in Fig. 12 is that for a constant TMP, the filtrate flux decreases as the velocity increases. A cross-flow filter is really only useful when there is something to filter. Without solids only the fluid dynamics affect the flow. As can be seen in Fig. 13 the increase axial velocity leads to an increase in the Reynolds number.

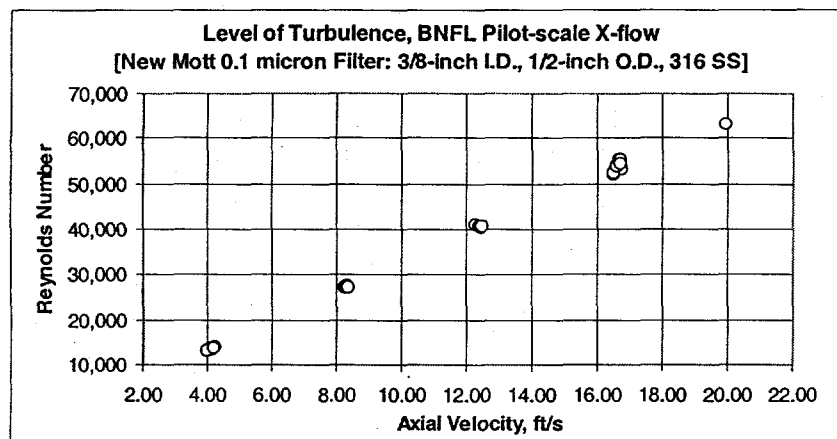


Figure 13. Reynolds vs. axial velocity of water in the cross-flow filter

This is not surprising since the Reynolds number is directly proportional to the velocity, along with the diameter of the flow stream, and inversely proportional to the kinematic viscosity. The purpose of Fig. 13 is to show the intensity of turbulence. As turbulence increases, the laminar sublayer decreases, an inertial sublayer is created and increases, and the scale of energy dissipating eddies become increasingly smaller (18). What this means is that increasing the shear environment at the tube wall forces the water to enter into the main stream more than forcing the water through the thin laminar sublayer which coats the porous-tube wall.

Finally, due to the added degree of freedom, the filtrate flux cannot be simply determined from just the axial flow velocity; the TMP must also be specified, leading to the family of curves in Fig. 12. However, an attempt was made to collapse those curves into a single curve to be more useful. Figure 14 show the results of that attempt.

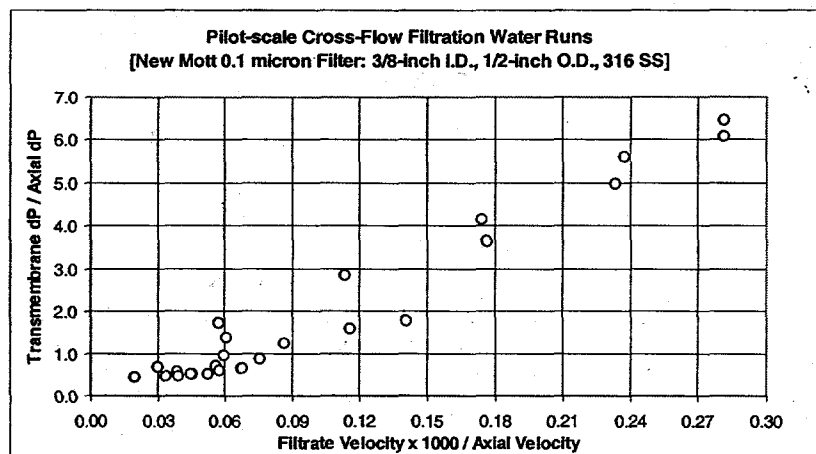


Figure 14. Normalized TMP vs. filtrate velocity in the cross-flow filter

RESULTS AND DISCUSSION

General

The different phases of the test matrix that we will discuss are: initial water baseline, low solids concentration, high solids concentration, slurry wash, plugging, cleaning, and final water baseline. After a discussion on some of the analytical and washing results, a discussion of the hydraulic results will follow the chronological order with the exception of the water and cleaning runs. Those runs will be given together in order to see any lasting effect of the slurry on the filter medium and thereby have a clear perspective of these test runs. The test matrix (3) was:

Run	Test Duration minutes	Slurry Velocity ft/s	TMP psid	Condition
2.00	120	12.2	40	Water
2.01	120	6.6	30	Low Solids Concentration
2.02	120	6.6	40	Low Solids Concentration
2.03	120	3.3	30	Low Solids Concentration
2.04	120	6.6	15	Low Solids Concentration
2.05	120	6.6	30	Low Solids Concentration
2.06	120	9.1	20	Low Solids Concentration
2.07	120	12.2	40	Low Solids Concentration
2.08	120	12.2	55	Low Solids Concentration
2.09	120	12.2	70	Low Solids Concentration
2.10	120	9.1	Best	Low Solids Concentration
2.11	120	15.2	Best	Low Solids Concentration
2.12	120	12.2	55	Low Solids Concentration
2.13	120	6.6	30	Low Solids Concentration
2.14	120	Best	Best	High Solids Concentration
2.15	N/A	12.2	40	Wash*
2.16	N/A	12.2	55	Wash*
2.17	N/A	12.2	70	Wash*
2.18	N/A	9.1	Best	Wash*
2.19	N/A	15.2	Best	Wash*
2.20	N/A	Best	Best	Plugging
2.21	N/A	N/A	N/A	Cleaning 1 M NaOH
2.22	N/A	N/A	N/A	Water

*These were to be pre-wash runs but were done as wash runs

Figure 15. Test matrix as stated in the test specification (3)

Test Run Sequence

As will be explained in the following sections, there were some deviations from the Test Matrix shown in Fig. 15. For example run, 2.10 was done three times and referred to as 2.10, 2.10b, and 2.10c. It was repeated for the Best Permeability and the Best Filtrate Flux flow conditions, since they were different. After run 2.13, run 2.07 (chosen for the its flow settings since it had the best filtrate flux results) was repeated too, i.e., 2.07b and 2.07c. At the suggestion of the task leader, and with the concurrence of the customer, 2.07b was a 7+ hour run without backpulsing to see if an asymptotic value for the filtrate flux could be reached. Run 2.07c was another all-day run but this time there were a series of different backpulsing frequencies, i.e., 30, 15, and 5 minutes. After run 2.07c the test rig had an unplanned pluggage while attempting to raise the solids concentration in the slurry for run 2.14. This plugging caused some down time to clean the test rig and

make more simulant. In attempting to unplug the test rig the simulant became slightly more dilute than required for the test. Therefore, run 2.14 was done as if it already went through one washing cycle. That is, run 2.17 was left out of the matrix when doing washing runs 2.15 to 2.19 because of the more dilute starting point. However, time allowed a repeat of runs 2.14 to 2.19 with a new batch of simulant, therefore those runs were referred to as 2.14b to 2.19b. Runs 2.20b, 2.21b, 2.22b are not repeat runs but have a "b" included because they were done after run 2.19b. Finally, runs 2.21b and 2.22b are broken down further as 2.21b1 and b2 and 2.22 b1 and b2 to illustrate different aspects of the same run.

Analytical Test Results

[See Appendix E for the entire set of data sheets.]

Filter Effectiveness

First and foremost, the task objective was to determine if the nominal rated 0.1-micron Mott filter could remove all the insoluble solids from the simulant. As already mentioned in the preceding experimental section of this report, the insoluble solids were made of 7 compounds: 6 metals (Al, Ca, Cr, Fe, Mn, and Ni) with Chromium being the largest quantity by mass, and Sodium Oxalate, which was the largest single quantity by mass (Fig. 8). Based on a real-sample analysis (Fig. 9a), the particle sizes purchased for the solids ranged from 0.5 to 5 microns. Fig. 9b indicates the sizes of solids used were close to the target values. From Tbl. 1 it is apparent that the filter removed all the solids. Note, the table shows that the analytical results only indicated the solids present in the filtrate were less than values shown (see Appendix E).

Run No.	Insoluble Solids	
	in Slurry, wt%	in Filtrate, wt%
Target (LS)	0.5	0
2.01	0.45	<0.003
2.13	0.29	<0.003
2.14b	8.2	<0.01*
2.16b	5.5	<0.01
2.20b start	5	<0.01
2.20b end	16.2**	<0.004
Target (HS)	20	0
*From run 2.15b because a measurement for 2.14b was not made		
**Estimated from remaining slurry volume		
LS = Low insoluble solids concentration		
HS = High insoluble solids concentration		

Table 1. Insoluble solids in the slurry and the filtrate throughout the test

The filter was very effective in removing all the insoluble solids. Furthermore, the basic sizes of the solid particles did not change during the course of the experiment. Particles smaller than 0.1 micron could have compromised the filter. Figure 16 shows that the particle diameter (by a volume distribution analysis) started at approximately 2.5 microns and remained that size. The standard deviations were on the same order of magnitude as the particle diameters. This was expected since the purchased solids were requested to be

between 0.5 and 5 microns. However, the largest number of particles was closer to 1 micron. When analyzing the particles by a number distribution, Fig. 17, the mean particle size is very close to 1 micron with one standard deviation being 0.4 micron. As seen in Figs. 16 and 17, one measurement from each had a bimodal distribution. These bimodal distributions could have been caused by the clumping of particles while samples awaited analysis, or by agglomerated solids that were not fully broken down when the samples were mixed before measurements were taken. In general, the particle sizes did conform to the required sizes and the particle sizes remained basically intact throughout the experiment. See Appendix E for details on the particle size analyses.

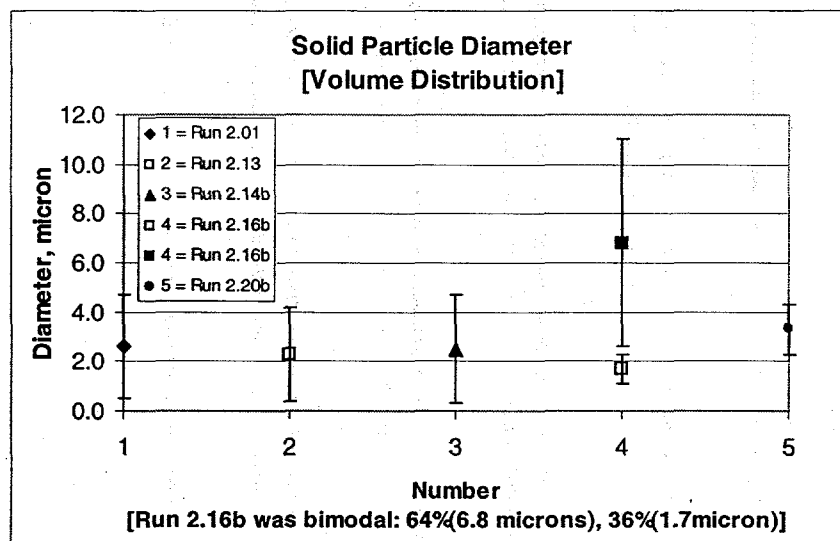


Figure 16. Particle size based on a volume distribution

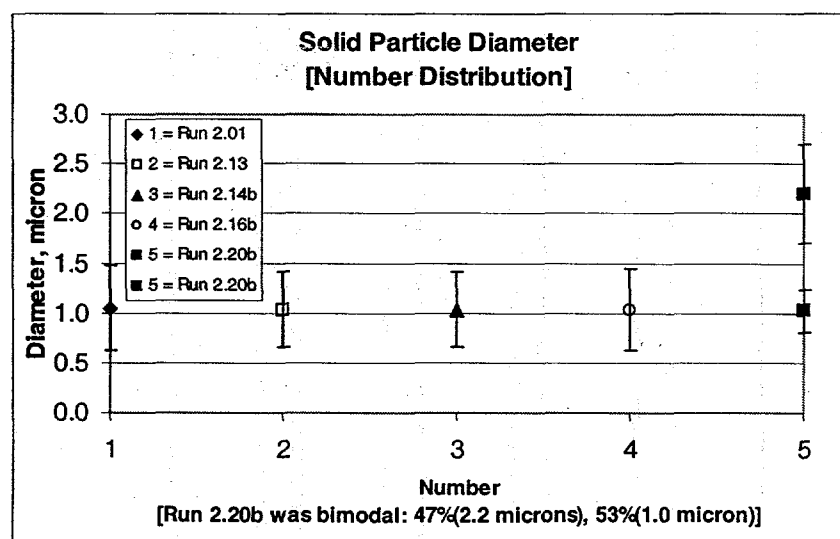


Figure 17. Particle size based on a number distribution

Washed Slurry

As already mentioned, there were two sets of washing runs: 2.15 to 2.19 and 2.15b to 2.19b. During the first set, run 2.17 was not done because during the concentrating run 2.14 the test rig plugged and in the process of unplugging the rig the slurry was diluted. The slurry for run 2.14 received enough water that it made the slurry equivalent to an initial wash run. Therefore, to keep the number of wash runs the same, run 2.17 was omitted. Further, because of the dilution it was thought best to make another batch of slurry to redo 2.14, which became 2.14b, which thereby allowed the wash runs to be repeated. While there are some differences between the two set of test runs, the data are similar and only those for test runs 2.15b to 2.19b are discussed here (see Appendix E for all the data).

*** Sodium ***

One of the major reasons for washing is to reduce sodium content. Figure 18 shows the Na^+ reduction.

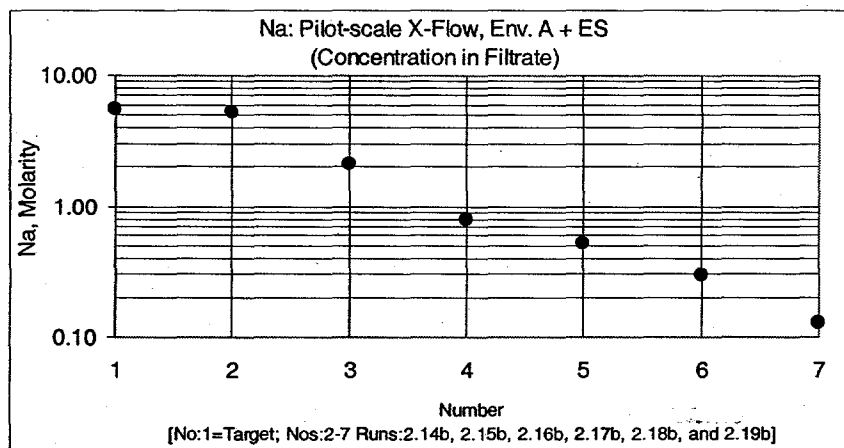


Figure 18. Reduction of sodium with successive washings

Point number 1 was the target sodium concentration of 5.5 M. Point number 2 shows the actual sodium concentration for run 2.14b was 5.2 M. Numbers 3 to 7 show the sodium level after each batch of 50 liters of water was added to the slurry reservoir that held approximately 50 liters of slurry. The line of points in Fig. 18 from number 2 to 7 is fairly straight on the semi-log scale, which was not unexpected. Figs. 19 and 20 show how the filtrate density and viscosity changed as the sodium level decreased from approximately 5 M to 0.1 M.

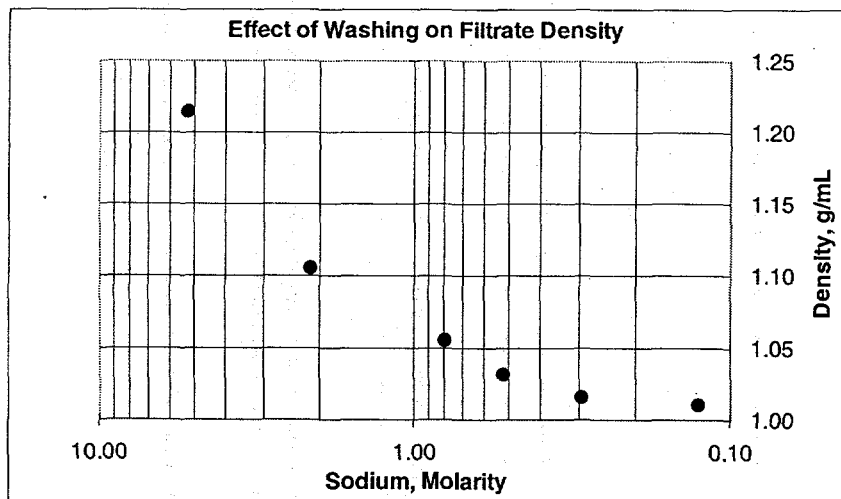


Figure 19. Filtrate density vs. sodium during washing

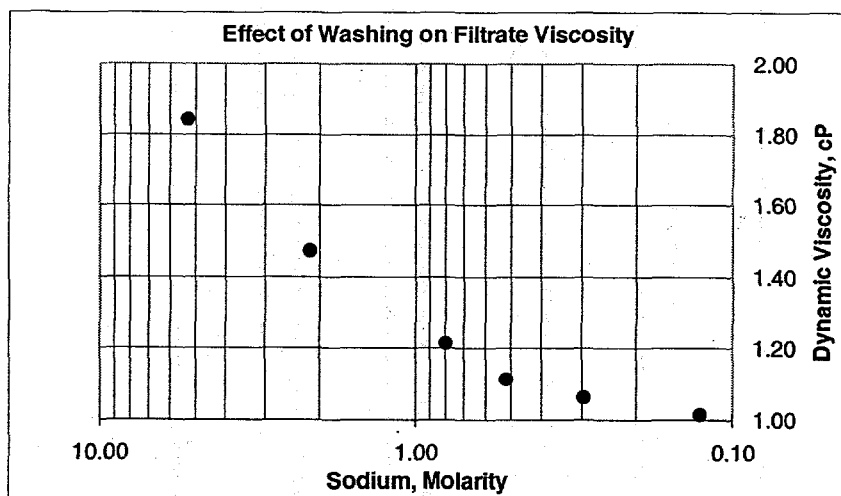


Figure 20. Filtrate viscosity vs. sodium during washing

*** Oxalate ***

A chemical that may have had an impact on the changes in solids loading was the chemical compound of oxalate. As seen in Fig. 8, approximately 50% of the "insoluble" solids that were added to the slurry was comprised of sodium oxalate. Of all the solids this one was expected to give the largest problem because of it being more readily dissolved in the simulant than any of the others. However, the simulant was designed such that the oxalates added as insoluble solids should have stayed undissolved. The liquid portion of the simulant, the supernate, was to be saturated with sodium oxalate before adding the solids.

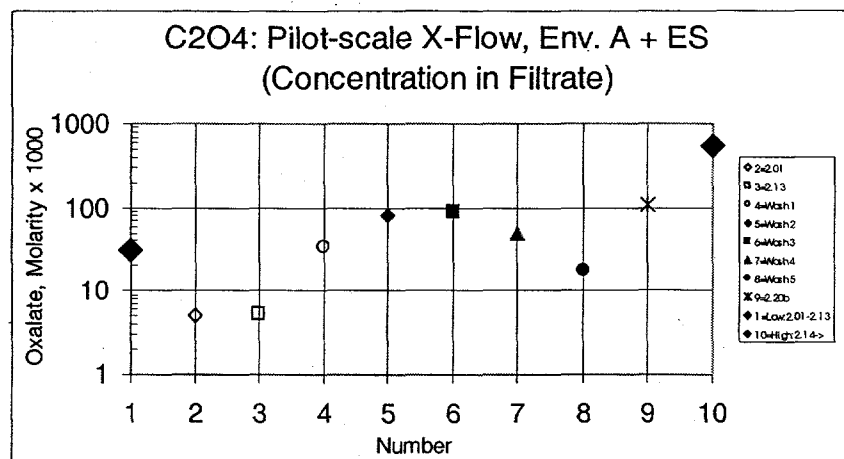


Figure 21. Oxalate changes in the filtrate during the test
 [Note: Except for nos. 1 and 10 all oxalate values are from the filtrate]

Figure 21 implies that most of the oxalates in solid form remained that way. The oxalate concentration in the filtrate, nos 2 and 3, for the low concentration runs of 2.01 and 2.13, was approximately 0.005 M. Number 1 is the value of the oxalate concentration from all its sources in the slurry, 0.03 M, and of this amount 0.004 was already included in the supernate. This indicates that after the solids were introduced, the liquid picked up about another 10 % in oxalates, i.e., $0.001 \text{ M} + 0.004 \text{ M} = 0.005 \text{ M}$. It is assumed that the supernate was fully saturated with oxalate at 0.005 M. The value of number 10, i.e., 0.55 M, is the amount of oxalates in the slurry for all test runs starting with run 2.14. The oxalate values for numbers 4 through 9 are from the filtrate samples that came from the slurry with this higher oxalate concentration. However, the supernate of the slurry before washing should have still been saturated at the 0.005-M level. Therefore, the oxalate concentration could only increase as the saturation level increased during the wash runs. Looking at the results from all the wash runs 2.15b to 2.19b (numbers 4 to 8) the oxalate in the supernate does increase as more and more water is added but it showed a maximum of 0.089 M on the third wash. Afterwards, the concentration decreased on the fourth and fifth wash runs. Note that all 5 wash runs were done in succession, and all on the same day. The time frame was short between water additions and the oxalate values, i.e., 4 to 8, may not be from a mixture at equilibrium. The oxalate value in the filtrate at the beginning of run 2.20b is 0.11 M, shown as No. 9 in Fig. 21. This filtrate sample was taken from the same dilute slurry that gave the result for run 2.19b, no. 8. The only difference is that run 2.19b was finished at 8 p.m. on one night and the sample for the beginning of run 2.20b was taken at 11 a.m. on the following day. That is, the slurry sat for 15 hours. This may indicate that the slurry was not at equilibrium on the preceding day, but then it was allowed to reach its full saturation level, which may be 0.11 M of oxalate. In any case, this still left $0.55 \text{ M} - 0.11 \text{ M} = 0.44 \text{ M}$ of oxalate in the slurry which probably stayed in the solid forms of sodium oxalate and calcium oxalate.

Therefore, there seems to be some loss of the sodium oxalate solids into the supernate but not all. Figure 8 shows that sodium oxalate comprised approximate 50% of the mass of the solids. The data indicate that only 10 to 30% of the oxalate solids was incorporated into the supernate.

For further information on the concentration of the many species in the simulant slurry, see Appendix E. All the analytical data taken and graphical results for many of the chemical concentrations can be found behind Table E1 in that appendix.

Hydraulic Test Results

Water Test Runs 2.00 and 2.22b and the Cleaning Run 2.21b

[See Appendix A for the entire set of data sheets.]

Permission to start the test was received on 5/12/99 and testing began on 5/14/99 with the first required test: water. As explained in the shakedown section, the filtrate flowmeter could only measure a maximum of 0.53 gpm/ft². As can be seen from Fig. 22, for run 2.00, at 0.43 gpm/ft², the TMP was only 3 psid and therefore the 40 psid requested by the test specification was not possible. The intention was to repeat the final water run, 2.22, with the same TMP so a comparison could be made. Figure 22 shows the results.

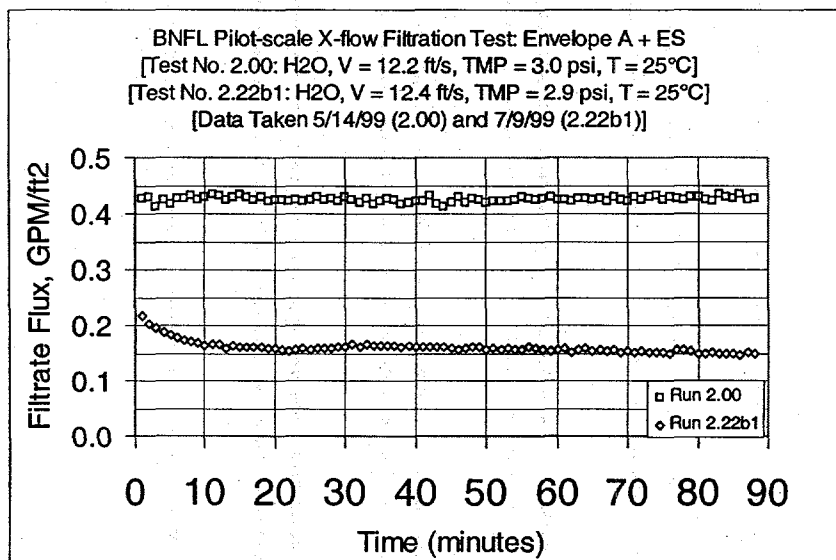


Figure 22. Water runs before and after the Env. A test

It is clear from the figure that the more than 60 hours of filter operation with slurry took its toll. The new-filter filtrate flux of approximately 0.43 gpm/ft² was reduced to 0.16 gpm/ft². However, there are at least two reasons, which mitigate this significant difference: 1. new filter and 2. low TMP.

1. New filter – Since this test started with a brand new filter it is not surprising the filter would have a reduced filtrate flux after many hours of slurry filtration. The filter was cleaned for more than 36 hours, as per the test specification, with a 1 M NaOH solution. Figure 23 shows results of two portions of the cleaning run. Since the flow parameters were changed several times during the run only two were chosen for this figure. The different run numbers, 2.21b1 and 2.21b2 only indicate that different TMPs were used. The slope of those curves in Fig. 23 decrease very slowly with time indicating that while the filter may be clean some residue remains. There was enough time to clean the filter twice, so another 20 hours of cleaning was done. The data in Figure 23 were taken during the second cleaning cycle. It appears that further cleaning would not return the filter to its original state.

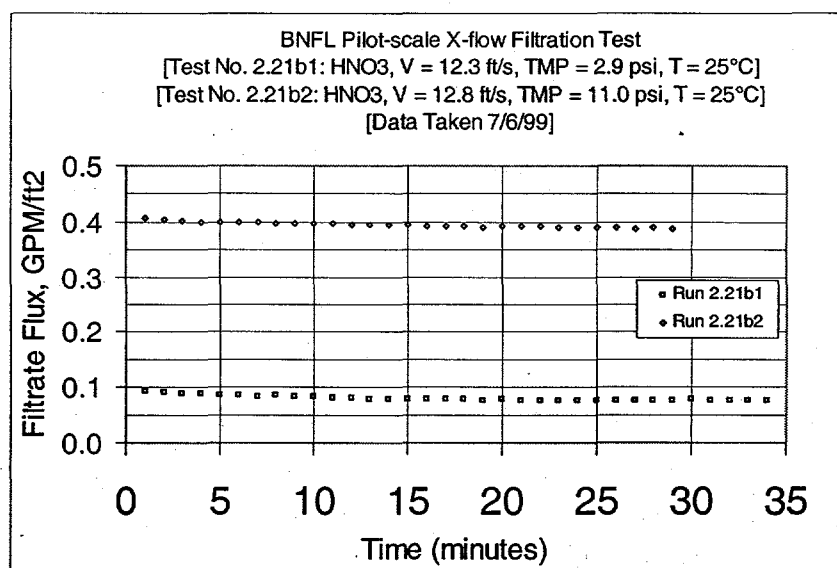


Figure 23. Cleaning run

2. Low TMP – A TMP of 3 psid was not easy to maintain for run 2.22b. Backpulsing was not effective because the filtrate flowrate would not return after a backpulse. To obtain data the TMP had to be increased until the filtrate flow was established, then the TMP could be reduced to 3 psid. (This was not the case for the new filter.) The difficulty to reestablish flow clearly indicated that the filter was not returned to the same level of cleanliness as when it was new. This dynamic stability could only be maintained as long as a backpulse was not done at this low TMP. Some of the smallest solid particles from the slurry must have lodged within the filtrate wall making its removal more difficult. However, the intention is to operate the filter with a TMP of more than 10 times this low-pressure difference, therefore this effect at the higher operational TMP will be insignificant.

On 7/13/99 another filtrate flowmeter, Q3, with a larger flow range, was installed on the test rig, in series with the original flowmeter, Q2, see Fig. 1. This allowed higher filtrate fluxes to be measured in run 2.22b. Figure 24 show those results.

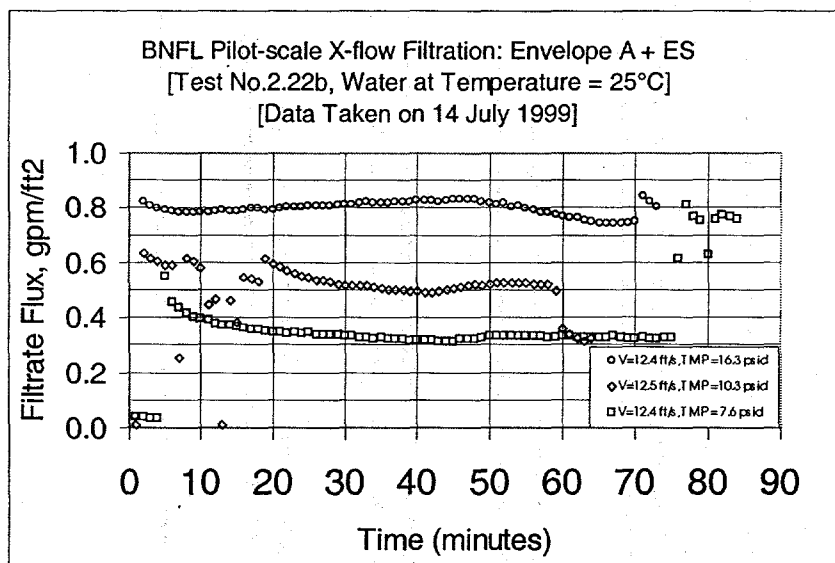


Figure 24. Water run at higher TMP using flowmeter Q3

Low Solids Concentration Test Runs 2.01 to 2.13

[See Appendix B for the entire set of data sheets.]

Included in this series of test runs are 13 planned runs and 4 unplanned runs (2.07b, 2.07c, 2.10b, and 2.10c). By far, this series of runs comprised the largest amount of data taken.

* Overall comparison *

Figure 25 is an attempt to compare all the low solids concentration test runs together. Unfortunately, a direct comparison among all the runs is not straight forward because run times differed for many reasons. Therefore several methods of comparison were chosen. Figure 25 show three different filtrate flux values: The mean value over the entire time of the test between backpulses, the value at $\frac{1}{2}$ hour after a backpulse, and an integrated value for the first $\frac{1}{2}$ hour of filtering. (Note that the numbers on the abscissa of the graph correspond to the numbers in the table below the graph.)

In general, it appears the integrated value is always larger than the mean or point value. This makes sense because the integrated value is only for the first $\frac{1}{2}$ hour, which includes the high filtrate flux just after a backpulse. (The period of $\frac{1}{2}$ hour was chosen because there are only approximately 22 minutes of data for run 2.03 and the largest interval between backpulses for run 2.07c is $\frac{1}{2}$ hour.) Now, the mean value also includes the data near the backpulse, but the mean is taken over the entire time of the test run which

reduces the weighing of those points. (Run 2.07b is the exception because it lasted 7.5 hours. For that run, the mean value was obtained for the first 2 hours after the backpulse so that it could be compared to the other runs.) Coincidentally, the point value of ½ hour is generally equal to the mean value, based on approximately 2 hours of data. While this is an interesting fact, and maybe useful to know, it is only a coincidence. Some other exceptions are: For number 3 (run 2.03) because of having only 22 minutes of run time an extrapolation of the data to 30 minutes was done to obtain the ½-hour value and the integrated value at ½ hour of the filtrate fluxes. Number 17 (run 2.07c) had backpulsing every 30 minutes (for 3 hours), 15 minutes (for 2 hours), and 5 minutes (for 1.5 hours), therefore there is no one-hour value. Therefore, the mean filtrate flux is based on the first 30 minutes, which give a high values and is closer to the integrated value than the point value at ½ hour.

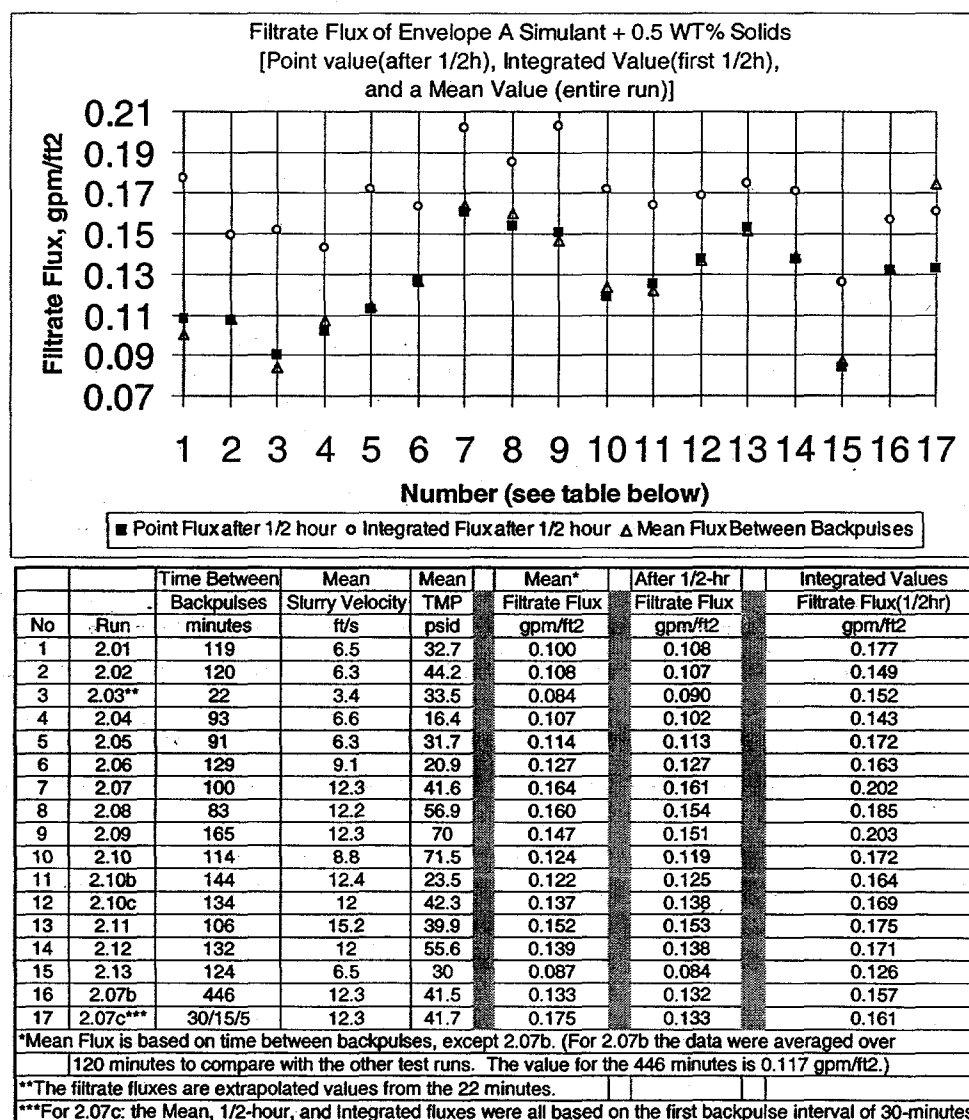


Figure 25. Composite of all 17 low solids concentration test runs

From Fig. 25 it would appear that the flow conditions of either number 7 (run 2.07), 9 (run 2.09), or 13 (run 2.11) could produce the best filtrate flux. Of interest is that for runs 2.07 and 2.09 the axial slurry velocity is the same, 12 ft/s, but the TMP differs by 30 psid. It would appear that the added TMP is not very effective in increasing filtrate flow. Run 2.11 has the same TMP as run 2.07 but the slurry velocity is higher by 3 ft/s. When comparing 2.07 with 2.11 it would not appear that the added velocity helps. However, what needs to be considered is the fact that with time the filter flow is affected by how the filter becomes dirty and by the size of the solids particles. A look at Fig. 26 shows the reduction of filtrate flux for similar slurry velocity and TMP conditions.

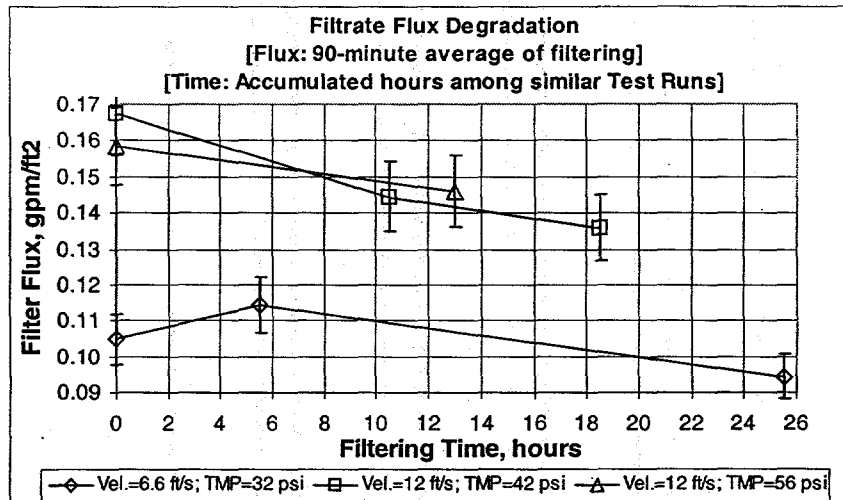


Figure 26. Effect of time on filtrate flow

[Filtrate Flux = 90-minute average of filtering]

[Filtering Time = accumulated filtering hours among Runs with the same flow conditions]

The error bars included in Fig. 26 are from the calculated measurement uncertainty of 6.72% for filtrate flux that can be found in Appendix F. Note that time shown is based on the number of accumulated filtering hours among tests with the same flow conditions, and not the number of hours of the entire test program. For example, the zero time for the three tests that had the flow conditions: slurry velocity = 6.6 ft/s, TMP = 32 psid, is the time that the first of those three tests began, etc. As stated, this filtrate flux reduction is due to the slurry becoming more difficult to filter (smaller particles) or the filter becoming filled with solids that do not dislodge with a backpulse. While the former effect did exist, it was insignificant. From the analytical measurements in Appendix E the measurement of the particle sizes can be found before and after the low solids concentration runs. Those results are repeated here:

Test Run	Insoluble Solids Loading	Avg Particle Diam. (by Volume)	Avg. Particle Diam.(by Number)
2.01	0.5 wt%	2.59 microns	1.031 microns
2.13	0.3 wt%	2.32 microns	1.027 microns

A portion of the "insoluble" particles seems to have been lost or dissolved into the slurry liquid since a measurement of the solids loading indicate a decrease of 40%. Because of the small quantities of insoluble solids the measurement uncertainty may make this difference insignificant. However, there did seem to be a 10% decrease in particle size (by Volume). If particle reduction occurred, some of that reduced mass could have been lodged within the walls of the porous filters. Still, this possible depth fouling was small compared to the surface fouling since a backpulse would increase the flux by about four fold (for example, see the right hand side of Fig. 29 after the final backpulse was made).

Even with filtrate flux degradation occurring, comparisons can be made among the many test runs to determine an appropriate set of flow conditions to operate the cross-flow filter. During the first 16 runs only the TMP and the Axial slurry velocity were changed. (For number 17, run 2.07c, the backpulse frequency was varied.) Therefore, a closer look at that those changes should elicit the information necessary.

* Filtrate Flux as a function of TMP *

Figures 27a, b, c, and d show a composite of four graphs; each for a constant axial slurry velocity. Figure 27a is for slurry velocity of 6.5 ft/s and a TMP from 16 to 44 psid.

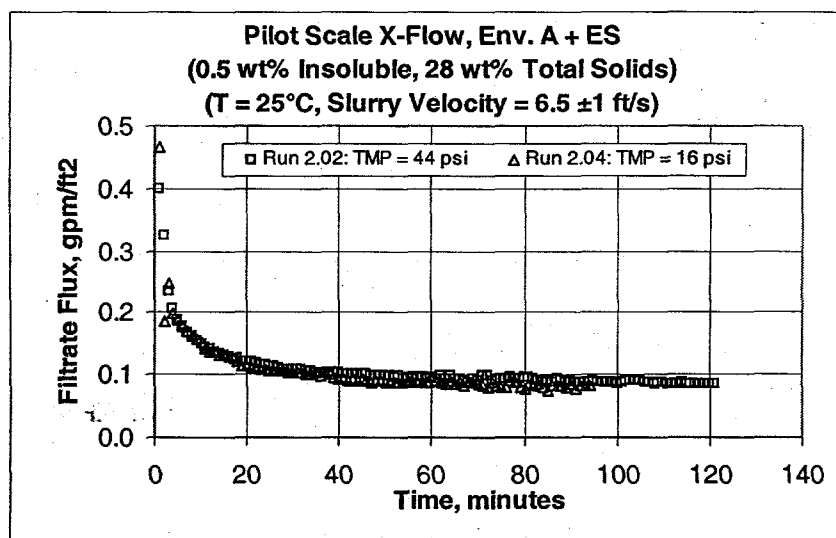


Figure 27a. Effect of TMP at a slurry velocity of 6.5 ft/s

For all intents and purposes both data curves in Fig. 27a are the same. This indicates that the filtrate flux is at best a weak function of TMP. In fact, that pattern repeats itself in Fig. 27b. In Fig. 27b the two curves are practically on top of each other; it appears that the large TMP increase from 20 psid to 70 psid is just wasted energy.

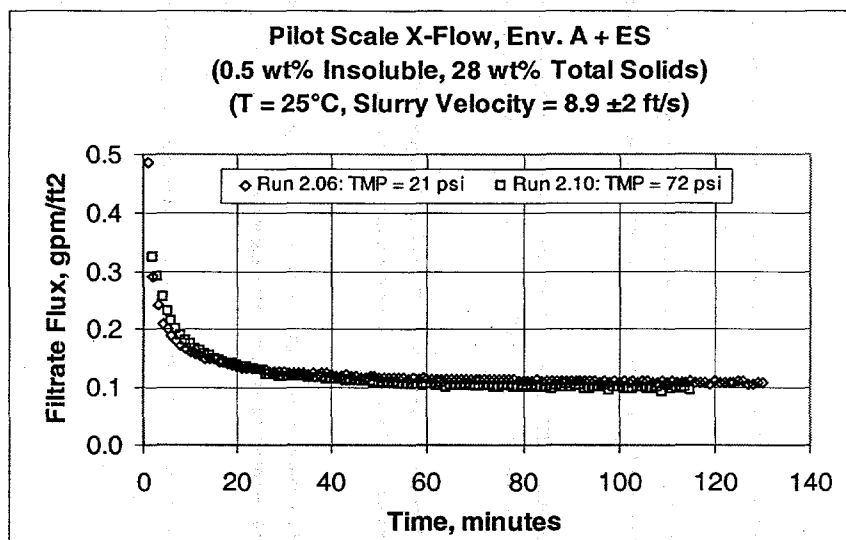


Figure 27b. Effect of TMP at a slurry velocity of 9 ft/s

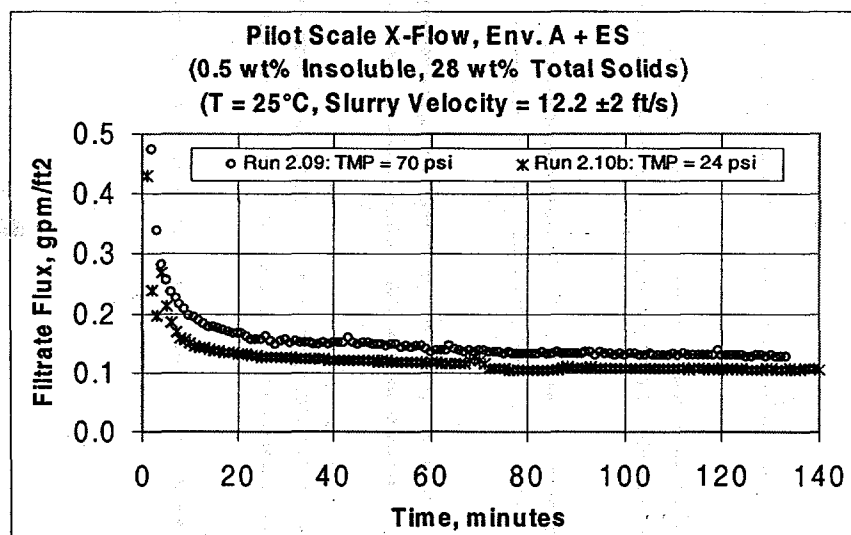


Figure 27c. Effect of TMP at a slurry velocity of 12 ft/s

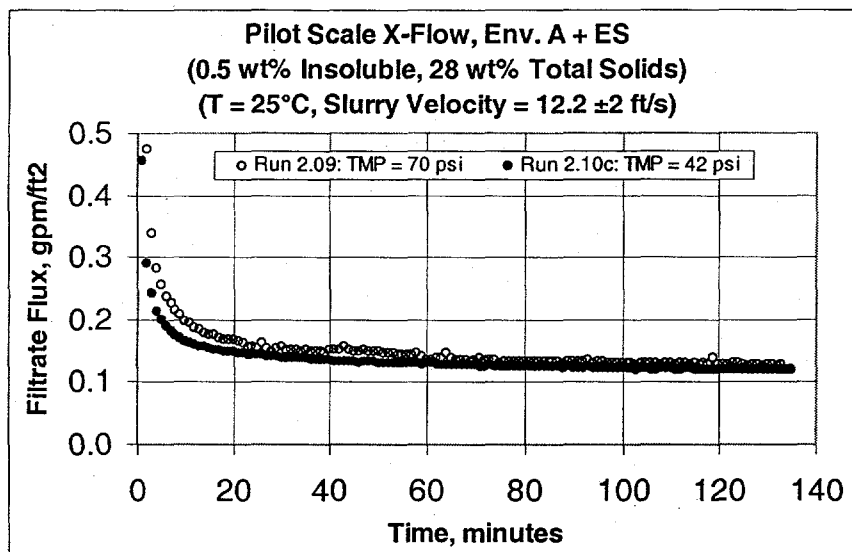


Figure 27d. Effect of TMP at a slurry velocity of 12 ft/s

From Fig. 27c, the higher TMP does seem to play a role when the slurry velocity increases. At a slurry velocity of 12 ft/s there is an approximate 20% increase in filtrate flux when the TMP is increased from 24 psid to 70 psid. Since the measurement uncertainty of the filtrate flux is $\pm 7\%$ this increase is significant. However, a TMP increase to 70 psid may not be necessary. Figure 27d shows that by increasing the pressure from 24 psid to 42 psid, the filtrate flux is within 7% of the 70-psid curve, which is a statistically insignificant difference.

*** Filtrate Flux as a function of Axial Slurry Velocity ***

Figures 28a, b, and c show a composite of three graphs; each for a constant TMP. Figure 28a is for a constant TMP of 20 psid. At that pressure only two runs were done at slurry velocities of 9 and 12 ft/s. The two curves are almost exactly the same, which could mean that velocity has no effect on filtrate flux but since the TMP is very low and the velocities are close, more data are needed. Figure 28b doubles the TMP to 42 psid. Here there is a significant difference between the curve for a slurry velocity of 6 ft/s and 15 ft/s.

Specifically, the filtrate flux is approximately 60% higher at 15 ft/s than at 6 ft/s. Moreover, it must be noted that there was approximately 20 hours of filtering between these two runs, 2.02 and 2.11, see Fig. 15. During that time period Fig. 26 indicates that under similar conditions the filtrate flux decreased by about 20%. Therefore, the top curve (run 2.11) in Fig. 28b could have been 20% higher if data were taken at the same time as the bottom curve (run 2.02). This means the filtrate flux could have conceivably been 80% higher at 15 ft/s than at 6 ft/s! Even between the top two curves (runs 2.10c and 2.11) there is a 12% increase in the filtrate flux. These two runs were done consecutively on the same day so there should have been no effect of time. However, this 12% difference is just barely significant.

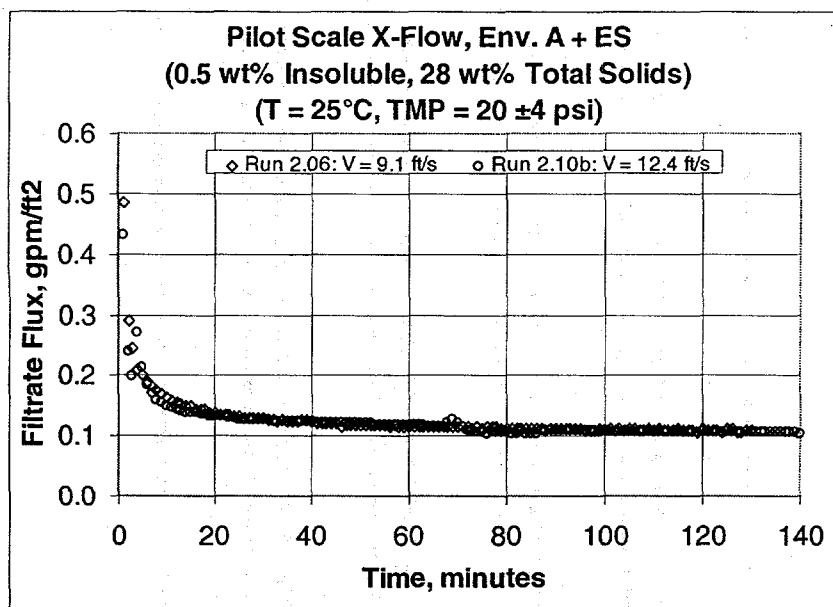


Figure 28a. Effect of axial slurry velocity at a TMP of 20 psid

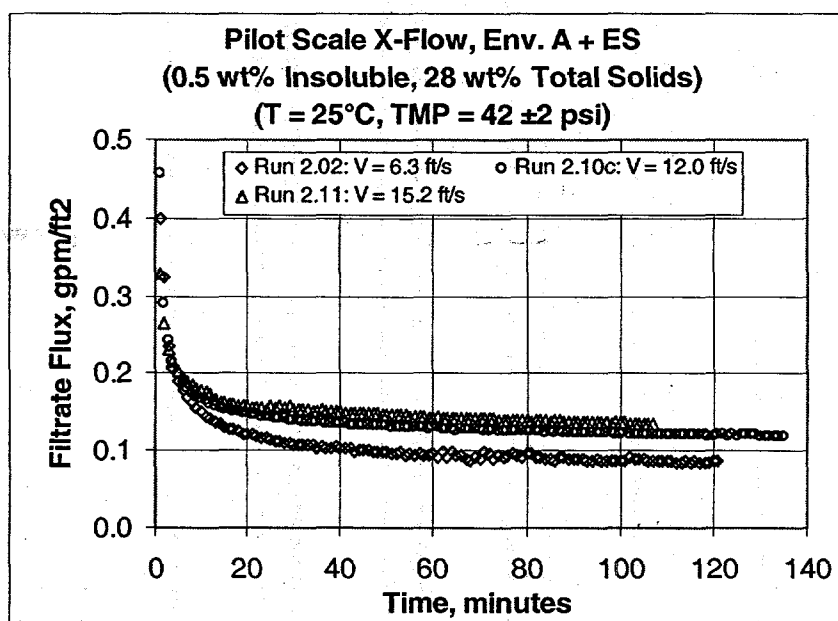


Figure 28b. Effect of axial slurry velocity at a TMP of 42 psid

Fig. 28c clearly shows a significant improvement in the filtrate flux (30%) when the slurry velocity of 9 ft/s is increased to 12 ft/s at a constant TMP of 71 psid. Once again, these two runs (2.09 and 2.10) were done consecutively so the slurry filter and slurry characteristics should have been the same. Except for the lowest TMP, 20 psid, the relationship between filtrate flux and axial slurry velocity appears to be linear. That is, for a 10% increase in velocity there is approximately a corresponding 10% increase in filtrate flux.

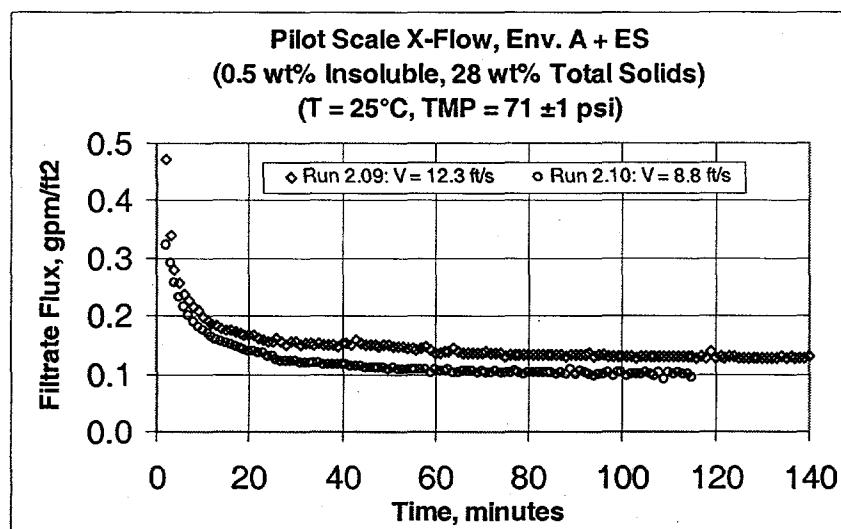


Figure 28c. Effect of axial slurry velocity at a TMP of 71 psid

Finally, backpulsing clearly improved throughput of filtrate but that improvement must be balanced against the downtime caused by the increased frequency of cleaning. That is, excessive backpulsing can be detrimental to long-term performance, depending on the type filter used. For this task, the filter manufacturer recommends that the backpulse frequency be no greater than once an hour; the longer the time between backpulses the better. Even though the filter elements used had a thick wall (0.0625 inch as opposed to a thin membrane filter), it is made to function as a surface, and not a depth, filter. The solids to be removed from the slurry are to remain on the surface of the filter and not lodged within the filter wall. As the filter cake builds, it itself becomes a filter removing smaller particles than the fixed filter on which it lies. When a backpulse occurs, most, or all of the filter cake is knocked off the fixed filter surface, which allows a higher filtrate flux, but also exposes the filter substrate to smaller solid particles. Over time these smaller particles will cause depth fouling and a reduced performance that cannot be improved though backpulsing. Fortunately, the long-term performance, without backpulsing, still gave an adequate filtrate flux. Figure 29 show the results of a test done over more than seven hours between backpulses. At the end of the test, the filtrate flux was still above 0.10 gpm/ft² and by the asymptotic behavior, the flux appears fairly constant after 7 hours and possibly could have been maintained for many more hours without a backpulse. (Note, the sudden drop at the end of the run was caused by taking a

filtrate sample which involves opening the filtrate flow system, thus causing a reduction in system pressure.) The mean filtrate flux over the 446 minutes of the test was 0.118 gpm/ft² (see Fig. B16 and the accompanying data in Appendix B).

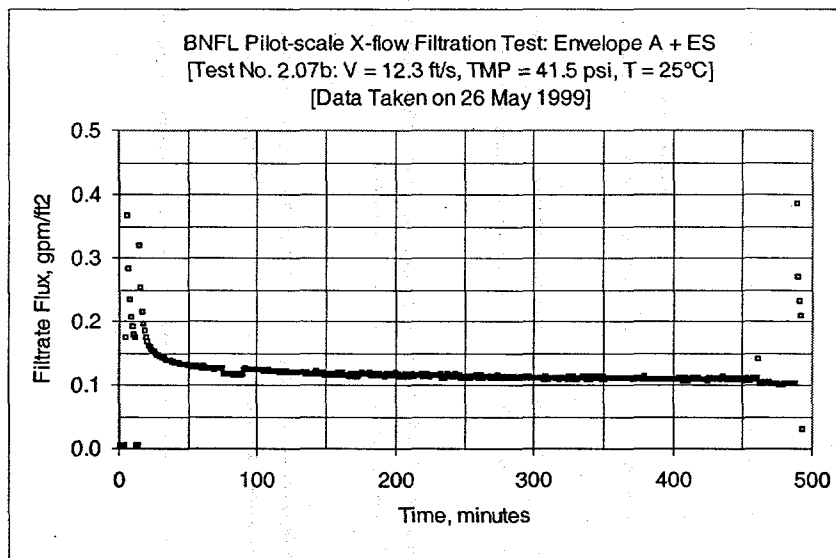


Figure 29. Long term filter operation between backpulses

Even though there are reasons to minimize backpulsing, there was interest in knowing how increasing the backpulse frequency increases the filtrate flux. Figure 30 compares the results from 3 runs that had similar flow conditions (see Fig. 25 for the conditions and actual times): 2.07b (with ~ 7.5 hours between backpulses), 2.10c (with ~ 2 hours between backpulses), and 2.07c (with 30, 15, and 5 minutes between backpulses; see Figs B17a and B17b in Appendix B); the increase is significant. That is, by increasing the backpulse frequency by a factor of 90, $[(7.5 \text{ hrs} / (5 \text{ min}/60)) = 90]$, the filtrate flux increased, but only 2 fold, [from 0.12 to 0.25 gpm/ft²]. Many studies (19, 20, 21, 22) clearly show the advantage of increasing the backpulse frequency, even to frequencies of 10 to 20 Hz. However, filters that work well at those frequencies are very thin membranes where depth fouling is generally not a factor, i.e., a particle that manages to enter a filter pore just goes right through because of the thin membrane. For the robust sintered-metal filter, used in this task, depth fouling cannot be ruled out. Therefore, it must be reiterated that an increase in filtrate flux may come at the expense of an increased rate of depth fouling. Figure 26 implies that for runs with approximately a 2-hour backpulse frequency, the filtrate flux is reduced by 10 to 15% over a 24-hour period of continuous filtering. Time did not allow evaluation of the long-term consequences on filtrate flux for other backpulse frequencies, but it seems logical that the steady-state flux would decrease faster as the frequency increased. Since high frequency backpulsing means the fixed filter surface remains freer of a filter cake, the smallest solids particles in the slurry would have more time to challenge the filter wall.

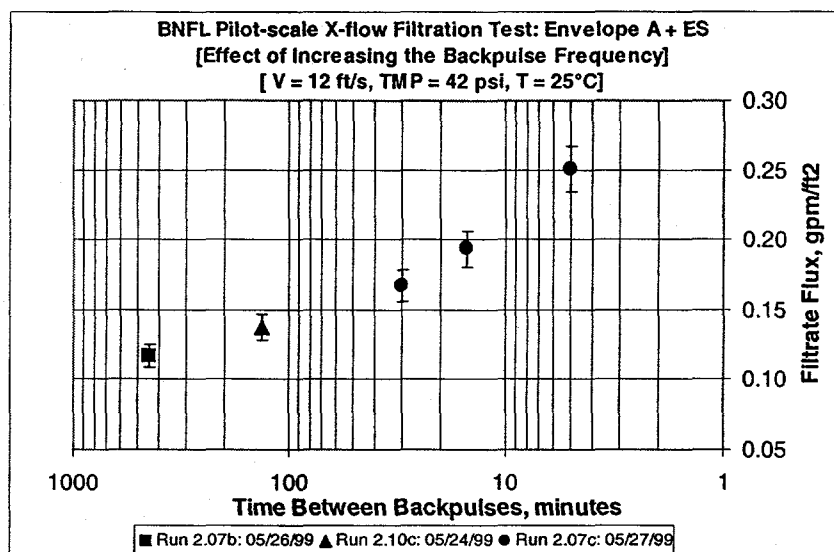


Figure 30. Filter operation with an increasing backpulse frequency

High Solids Concentration Test Runs 2.14, 2.14a (Pre-wash)

[See Appendix C for the entire set of data sheets.]

Two test runs were done before washing occurred. Originally, there was to be only one run, 2.14, before washing, but in concentrating the slurry the test rig became plugged. In an attempt to free the plug from the test rig the slurry became diluted with water. Subsequently, the washing runs, 2.15 to 2.19 were done, with 2.14 assumed to be the first wash run because of the added water. However, time allowed the mixing of another batch of simulant, thus a new set of runs was done starting with 2.14b. While there were two pre-wash runs, the solids loading was never brought above the required 20 wt% because of plugging concerns. Furthermore, instead of straight dewatering, the slurry was concentrated by adding solids directly to the slurry after a fixed amount of filtrate was removed. This method was used to allow for a much smaller starting volume of slurry. Theoretically, this method was possible because the two quantities, i.e., supernate and insoluble solids, were thought not to interact with each other except for physical space. Unfortunately, after removing 37 liters of filtrate from the 75 liters of slurry, problems occurred on adding the solids to the supernate. When the insoluble solids loading was between 10 wt% and 15 wt% the test rig became plugged. In an attempt to prevent a long shut down and free up the test rig immediately, the 37 liters of filtrate was returned to the slurry. The added filtrate did not relieve the plug so three separate additions of DIF water were added, for a total of 38 liters. Despite the water addition, the test rig remained plugged and had to be shut down. The majority of the dilute slurry was drained from the test rig, which was then dismantled to remove the pluggage. [Note: When the test rig was disassembled the plug was found in the test-rig piping and not the filter. The pluggage occurred because of the way the solids were incorporated into the slurry. In pouring the solids directly into the slurry reservoir of the test rig some of the solids did not have time to become well mixed in the slurry; isolated clumps of solids were found in the pipes. Those clumps contained dry solids that did not mix with

the liquid and when a clump met a bend in a pipe it stuck, which prevented further flow. The second batch of simulant was made in a separate tank to make sure the slurry was well mixed before introducing it into the test rig.]

After the test rig was cleaned, the experiment continued. Run 2.14 was done with the remaining slurry, which had a calculated insoluble solids content of 9 wt%. A subsequent measurement showed the solids loading to be closer to 7 wt%. This difference may have come from some of the solid sodium oxalate dissolving in the more dilute slurry.

Based on the low-solids concentration runs, the best combination of axial slurry velocity and TMP was chosen to be 12 ft/s and 40 psid, respectively. Figure 31 shows that a relatively high filtrate flux was obtained despite the 7 wt% insoluble solids loading. However, since the slurry was diluted with water and the sodium level is estimated to have been close to 3 M, instead of the original 5 M. [Note, that there are two curves in Fig. 31 because the run was restarted to adjust the TMP, which drifted high.] As already stated above, since time allowed, the slurry was adjusted to raise the sodium level back to over 5 M to redo the run, which was called run 2.14b.

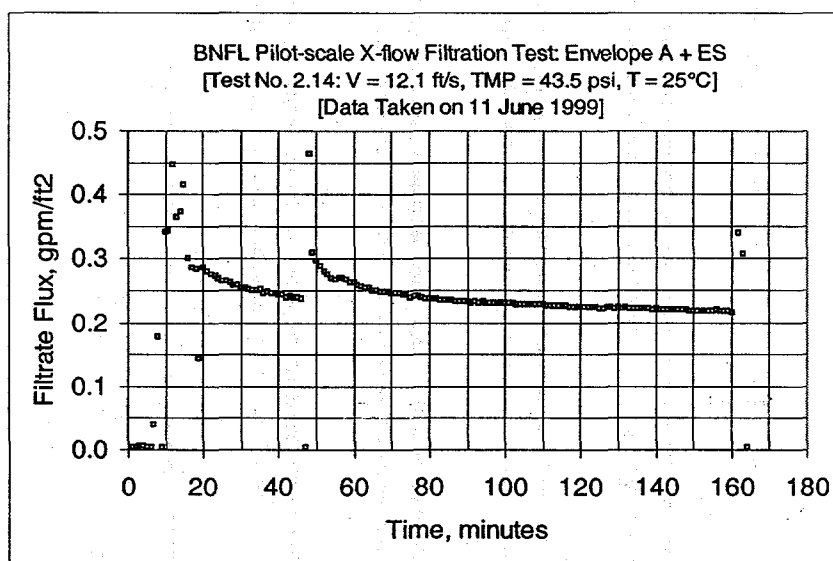


Figure 31. Run 2.14: 7 wt% insoluble solids; 26 wt% total solids

Figure 32 shows the results of the new run with the sodium level back over 5 M. The insoluble solids loading was calculated at 11 wt% but a subsequent sample analysis indicated a value closer to 8 wt%. The filtrate flux over the entire run stayed above 0.1 gpm/ft² and in fact was very similar to the last low-concentration continuous run, 2.07b which had very similar flow conditions (see Fig. B16 in Appendix B). This indicates the added insoluble solids had an insignificant effect on filter operation. From this experience higher pre-wash slurry concentrations are possible and maybe even reaching

and surpassing the target 20 wt%. However, because of the aforementioned circumstances there are no quantitative data to make a more definitive statement.

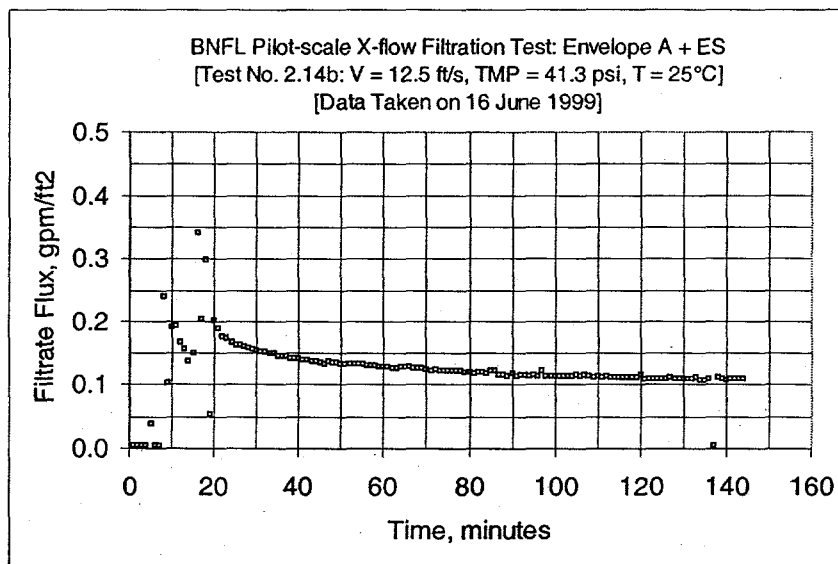


Figure 32. Run 2.14b: 8 wt% insoluble solids; 36 wt% total solids

Wash Test Runs 2.15-2.19 and 2.15b-2.19b

[See Appendix D for the entire set of data sheets.]

There were nine different wash test runs. Test runs 2.15-2.19 were repeated when a new batch of slurry was made to repeat run 2.14. The new tests are referred to as 2.14b-2.19b, with the first wash run beginning with 2.15b. From all these runs the hydraulic aspects are best illustrated by run 2.15, Fig. 33.

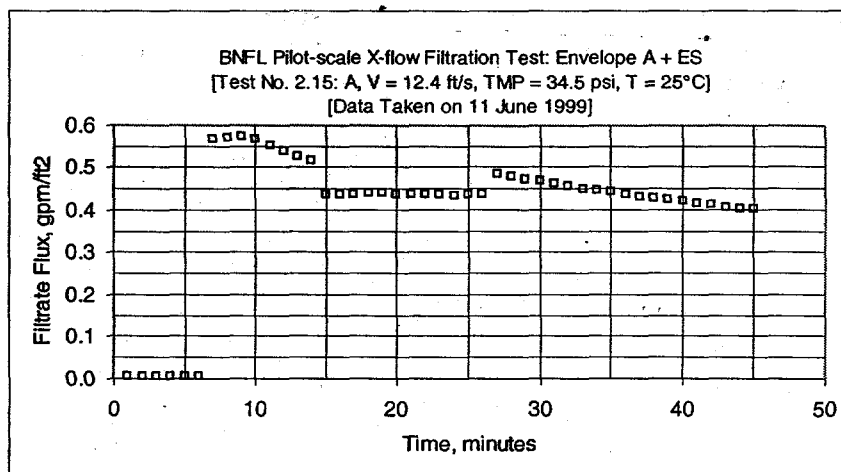


Figure 33. Typical wash test run

Figure 33 shows two different characteristics: 1. A descending curve, typical of a cross-flow filter curve for slurry after a backpulse, and 2. a relatively flat curve that lasted approximately twelve minutes. This flat curve occurred when the filtrate system was opened to remove 45 liters of filtrate. (These numbers match the data in Fig. 33, because $45 \text{ L} / 3.785 \text{ L/gal} / 12 \text{ min.} / 2.29 \text{ ft}^2 = 0.43 \text{ gpm/ft}^2$, which is close to graphical result shown.) That is, to dewater the slurry, so that the next charge of washing water could be introduced into the test rig, the filtrate system was opened using valve V13 in Fig. 1; the filtrate was collected and sampled. While the filtrate was collected, the open valve allowed the pressure in the filtrate loop to drop since it was not forced back to the slurry loop. This reduced pressure caused the flow parameters, i.e., slurry velocity and TMP, to change. Therefore, the initial flow conditions were set so that when the filtrate valve was opened the flow conditions came close to the test specification requirements. It was not always easy to set the correct flow and therefore many of the data sheets for the washing runs show quite a bit of adjustment before the filtrate was actually drawn from the test rig.

During the washing runs there was a concern about the filtrate flux increasing above the measurable limit of 0.53 gpm/ft^2 . Because of the water additions, the filtrate flux was expected to increase as the slurry became successively more dilute. As mentioned, run 2.15 was considered the second wash run since the slurry for run 2.14 was already diluted with water because of the test rig pluggage. In Fig. 33, the first couple of points after the backpulse are above the calibrated range of the filtrate flowmeter and are therefore meaningless. As a backup measurement, a bucket and stopwatch technique was used to verify the filtrate flux when filtrate was drawn. Fortunately, the portion of the curve when the filtrate was being drawn was always below the threshold of the filtrate flowmeter for all test runs.

Dewatering/Plugging Test Run 2.20b

[See Appendix C for the entire set of data sheets.]

Figure 34 shows the result of this relatively short test of 50 minutes from the backpulse. The goal was to dewater/concentrate the post-washed slurry to the point that filtration was no longer possible, due to either the filter plugging or for some other operational reason. Starting with approximately 80 liters of slurry in the test rig, the slurry was dewatered by removing filtrate in batches of approximately 7.3 liters. After each batch removal, the density of the slurry was measured and samples were taken three times to have information on the slurry as it approached possible plugging. A total of 6 full batches of filtrate were removed before stopping during a 7th batch, which reduce the slurry volume to less than 35 liters. (The actual final volume was closer to 30 liters.) The filtering never stopped and while the filtrate flux decreased throughout the test, at the end it still was filtering at 0.25 gpm/ft^2 when the insoluble solids loading was estimated at approximately 16 wt% [see Table 1 (page 26), run 2.20b end].

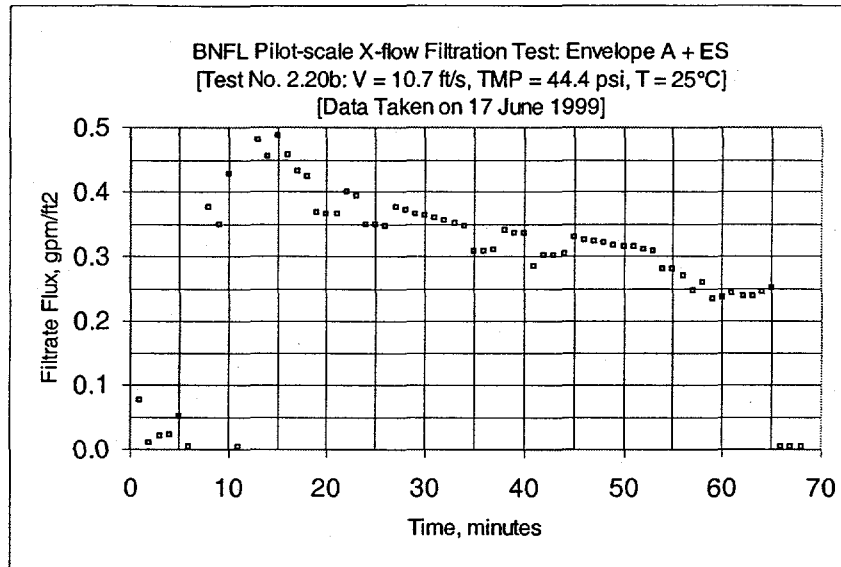


Figure 34. Dewatering/Plugging test run

Figure 35 shows how the density of the post-washed slurry increased after each of the 6 batches of filtrate was removed. Included in Fig. 35 are three measurements of solids loading that were made. The middle set of numbers (at 65 liters of slurry remaining) has no reading for insoluble solids because the analytical measurement was in error and had to be discarded. Finally, in attempting the 7th batch the test rig was stopped when flow could not be maintained. The test rig needed 26 liters to keep it liquid solid and the extra 4 liters of the remaining 30 liters of thickened slurry were not sufficient to maintain the pump suction pipe full. The slurry was spread around the tank such that a good sample could not be taken, therefore a final density was not obtained

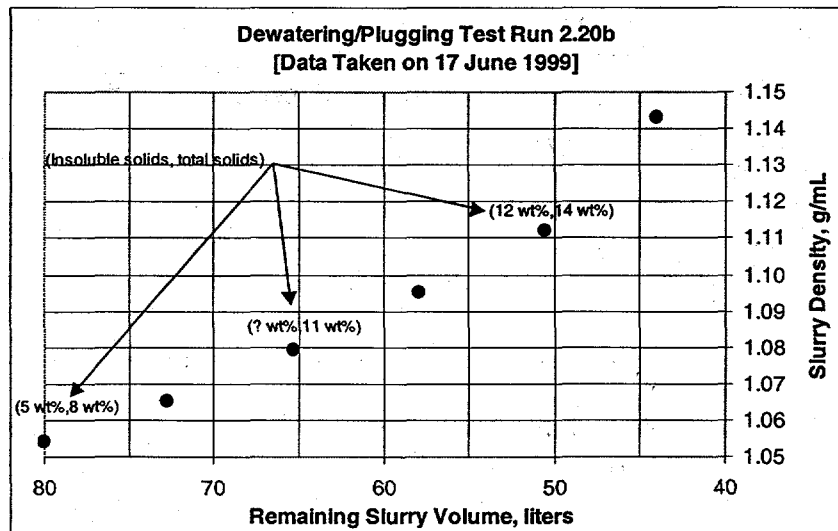


Figure 35. Dewatering/Plugging test run with post-washed slurry

CONCLUSIONS

The following conclusions are for the nominal rated 0.1 micron Mott cross-flow filter which was used under the conditions stated herein at a slurry temperature of 25°C.

Filter Effectiveness

1. There was no measurable quantity of insoluble solids in the filtrate under any circumstance from the filtered slurry that had a solids loading from 0.5 wt% to greater than 16 wt% and for particle sizes measured as small as 0.76 micron.

Slurry Wash

2. Using 4 equal quantities of distilled and filtered water (each quantity equaling the volume of the slurry to be washed), the sodium molarity of the filtrate decreased from 5.2 M to 0.29 M, while the dynamic viscosity decreased from 1.8 cP to 1.1 cP and the density decreased from 1.214 g/mL to 1.015 g/mL. For a fifth wash those numbers decreased to 0.13 M, 1.01 cP, and 1.0095, respectively.

Hydraulic Characteristics

3. Water flux through a used cleaned filter may be as low as a third that of a new filter.
4. Surface fouling of the filter is the dominant mechanism of fouling.
5. Higher slurry velocities and higher transmembrane pressures lead to higher filtrate fluxes. However, the increase in filtrate flux is strongly affected by the slurry velocity but only weakly by TMP.
6. Slurry velocities for steady-state operation should be 12 ft/s or higher.
7. A TMP of 40 psid or 55 psid, with the velocity in conclusion 6, will give close to the best filter flux performance. Increasing the TMP to 70 psid will increase the filtrate flux slightly but that small increase may not justify the larger energy expenditure for the higher pressure. Also, the lower TMP will increase the life of the cross-flow filter due to a lower cleaning frequency.
8. For a low concentrations of insoluble solids (0.5 wt%), based on conclusion 7, run 2.07, shown in Fig. 25, gave the best overall filtrate flux of 0.20 gpm/ft² at the conditions of a slurry velocity of 12.3 ft/s and a TMP of 42 psid. This flux is based on an integrated value of the measured flux for the first one half hour of operation. Even for the run that lasted more than 7 hours without backpulsing (Fig. 29), the mean filtrate flux was still 0.12 gpm/ft², and it appeared that this flux could be easily sustained for many more hours.
9. For high concentrations of insoluble solids (8 wt%) the filtrate flux remains above 0.10 gpm/ft² for at least 2 hours after a backpulse.
10. The cross-flow filter still functions satisfactorily for an insoluble solids loading of 16 wt%; the post-washed slurry had filtrate fluxes better than 0.2 gpm/ft².
11. An average filtrate flux of 0.12 gpm/ft² can be maintained for at least 7 hours without backpulsing. It can be increased to 0.16 gpm/ft² with a backpulse interval of 30 minutes.


12. In all the test runs the filtrate flux was never lower than the River Protection Project waste treatment plant design basis of 0.037 gpm/ft^2 , and typically it was above three times that value.
13. A backpulse filtrate volume of 0.036 gal/ft^2 with a filter overpressure of 30 psi was found to be sufficient to knock the filter cake off the filter element. A backpulse frequency of 30 minutes leads to a filtrate flux loss of 0.0012 gpm/ft^2 rate, which is only a few percent of the lowest steady-state filtrate flux measured of 0.05 gpm/ft^2 .


RECOMMENDATIONS

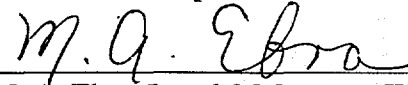
The following recommendations are for the nominal rated 0.1 micron Mott cross-flow filter when used for an Envelope A slurry at a temperature of 25°C .


1. Use a slurry axial velocity of at least 12 ft/s. Lower velocities significantly reduce filtrate flux.
2. Use a transmembrane pressure of 40 to 55 psid. Lower pressures significantly reduce filtrate flux and higher pressures do not increase the filtrate flux significantly.
3. Backpulse the filter twice to three times in a 24-hour period of continuous use to maintain an average filtrate flux of 0.1 gpm/ft^2 and to minimize filter cleaning.
4. Backpulse the filter every 30 minutes during continuous use to increase the average filtrate flux to 0.16 gpm/ft^2 .
5. Use a backpulse of 0.036 gal/ft^2 to minimize the loss of filtrate flux.

APPROVALS


H. N. Guerrero, Technical Reviewer, WSRC/SRTC


D. B. Burns, Experimental Thermal Fluids Group Manager, WSRC/SRTC


M. A. Ebra, Level 3 Manager, WSRC/SRTC


S. T. Wach, Waste Processing Technology Manager, WSRC/SRTC

Not Required as per BNF-003-98-0239, April 24, 2000
P. S. Townson, Ultrafiltration Development Manager, BNFL

2/29/00
Date

4/19/2000
Date

4/23/2000
Date

4/19/00
Date

4/24/2000 ^{MRD}
Date

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APPENDIX A

EXPERIMENTAL DATA: WATER AND CLEANING

Appendix Contents

1. Nomenclature sheet for data tables
2. Experimental data:

Fig.	Run	Solution	Done on
A1	2.00,	Water	5/14/99
A3	2.22b1	Water	7/9/99
A3	2.22b2	Water	7/14/99 (added filtrate flowmeter, Q3)
A4	2.21b,	1 M NaOH Cleaning	7/6/99

General Note: For measurement uncertainties see Appendix F

Special Notes:

- a. The data for every test run are highlighted with two graphs: Filtrate Flux vs. Time and Permeability vs. Time. Those graphs include all the data taken during the run period.
- b. The beginning and end of the data for most graphs show large deviations from the overall series of points. Those deviations were caused by backpulsing the filter that temporarily stopped the flow of filtrate.
- c. All columns of data, in all the tables, are ended with several statistical values of that column, i.e., Average, Maximum, Median, Minimum, Standard Deviation, and Number of Points used (in calculating the 5 statistical quantities).
- d. To calculate those quantities mentioned in item c, only those data points that start from the end of a backpulse to just before the ending backpulse were included. This is the reason why the quantity of Number of Points Used was given.
- e. The data for the graphs, and all the data taken for the individual test run that the graphs represent, immediately follow the specific figure.

Nomenclature For Data Sheets

(See Figure 1: Main Test Rig - Pilot Scale Cross Flow for the Instrument Location)

Column	Heading *		Full Heading	Explanation
A =	DATE	=	DATE	Day the test was done
B =	TIME	=	TIME	Time data entry was made
C =	SOLENOID	=	SOLENOID	1=yes, 0=no: for the pressure to the backpulse piston
D =	FLTRT (deg)	=	FLTRT (deg C) T2	Filtrate Temperature in Filter at exit of the Filter Housing
E =	CL LOOP (deg)	=	CL LOOP (deg C) T3	Temperature of Liquid in the Cleaning Loop
F =	SL LOOP (deg)	=	SL LOOP (deg C) T1	Temperature of Liquid in the Slurry Loop at the Reservoir Tank
G =	UP AMB (deg)	=	UP AMB (deg C) T4	Ambient Temperature at the top of the Test Rig - 3rd level
H =	BOT AMB (deg)	=	BOT AMB (deg C) T5	Ambient Temperature at the bottom of the Test Rig - 1st level
I =	T6 (deg C) S	=	T6 (deg C) SPARE	Spare Thermocouple - Currently Not Being Used
J =	BOT DP (psid)	=	BOT DP (psid) dP2	Differential Pressure between the Filter Slurry Entrance and the bottom Filtrate Exit
K =	FLTR (psig)	=	FLTR (psig) P1	Gauge Pressure at the Filter Slurry Entrance
L =	FLTR DP (psid)	=	FLTR DP (psid) dP1	Differential Pressure between the Filter Slurry Entrance and Exit
M =	TOP DP (psid)	=	TOP DP (psid) dP3	Differential Pressure between the Filter Slurry Exit and the Top Filtrate Exit
N =	FLTRATE (psig)	=	FLTRATE (psig) P2	Gauge Pressure at the Filter Filtrate Exit
O =	PISTON (psig)	=	PISTON (psig) P3	Air Gauge Pressure Applied to Backpulse Piston
P =	SL FLOW (gpm)	=	SL FLOW (gpm) Q1	Flow Rate of the Slurry Flow
Q =	FLTR FLOW (gpm)	=	FLTR FLOW (gpm) Q2	Flow Rate of the Filtrate Flow
R =	V9	=		Spare Channel Not Used

The following columns are calculated results based on the appropriate columns

S =	Number	=	Number	Data number which is equivalent to 1 minute since this was the acquisition frequency
T =	Vel, ft/s	=	Vel, ft/s	Axial slurry velocity = [Column P] / 7.48 gal/ft ² / 60 sec/min / flow area (=0.005369 ft ²)
U =	TMP, PSI	=	TMP, PSI	Transmembrane Pressure = ([Column J] + [Column M])/2
V =	TMP, bar	=	TMP, bar	[Column U] / 14.504 bar/psi
W =	GPM/FT ²	=	GPM/FT ²	[Column Q] / inside diameter filter surface area (= 2.29 ft ²)
X =	GPM/FT ²	=	GPM/FT ² at 25°C	Test Spec. correction factor: [Column W] x exp(2500 x ((1/(273+[Column T]))-(1/298)))
Y =	PERMEABILITY	=	PERMEABILITY (gpm/ft ² /psi)	[Column X] / [Column U]
Z =	x 1000	=	PERMEABILITY x 1000	[Column Z] x 1000
AA =	PERMEABILITY	=	PERMEABILITY (m/day/bar)	[Column Y] x conversion factor (= 851.0145 m/day/bar / gpm/ft ² /bar)

*Axial slurry flow area is based on 7 porous tubes with an inside diameter of 3/8 inch: $7 \times \pi / 4 \times (0.375 \text{ inch} / 12 \text{ inches/ft})^2 = 0.005369 \text{ ft}^2$ **Inside diameter filter surface area for 7 tubes with an inside diameter of 3/8 inch, 40-inches long: $7 \times \pi \times (0.375 \text{ inch}) \times 40 \text{ inches} / 144 \text{ in}^2/\text{ft}^2 = 2.29 \text{ ft}^2$

Exceptions:

- For Run 2.21b (Cleaning); This run was carried out over a three different periods on three days therefore there are two NUMBER COLUMNS: S & T. Column S is continuous and Column T is continuous but starts over for each period. All the columns to the right of Column S are shifted by one.
- For Run 2.22b (Water); After July 10, 1999 a second filtrate flow meter was added to measure flow rates from 1.2 to 5 gpm. The final water test run (Run 2.22b) has an extra filtrate flow rate column. Column R, the spare column, was made the new flow rate:

R = **Q3, FLTR F** = Q3, FLTR FLOW (gpm) Flow Rate of the Filtrate Flow (above 1.2 gpm), installed after 7/10/99

also Run 2.22b has two NUMBER columns (like Run 2.21b) so Exception 1 also applies.

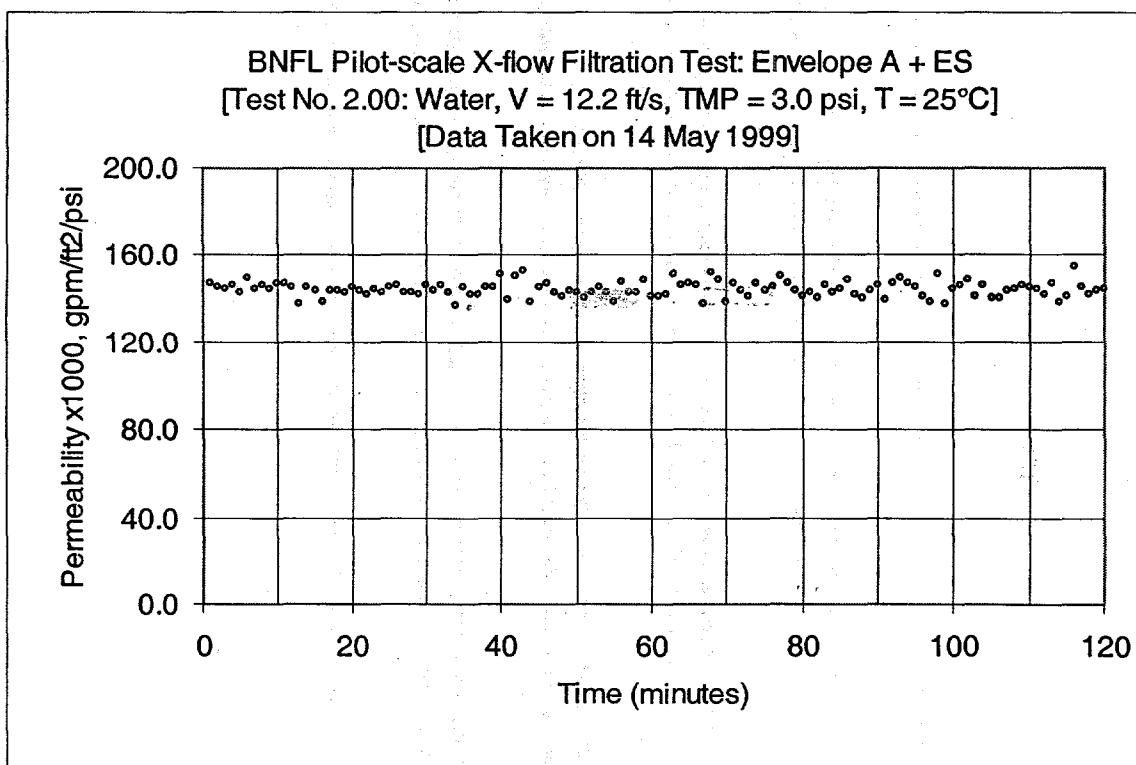
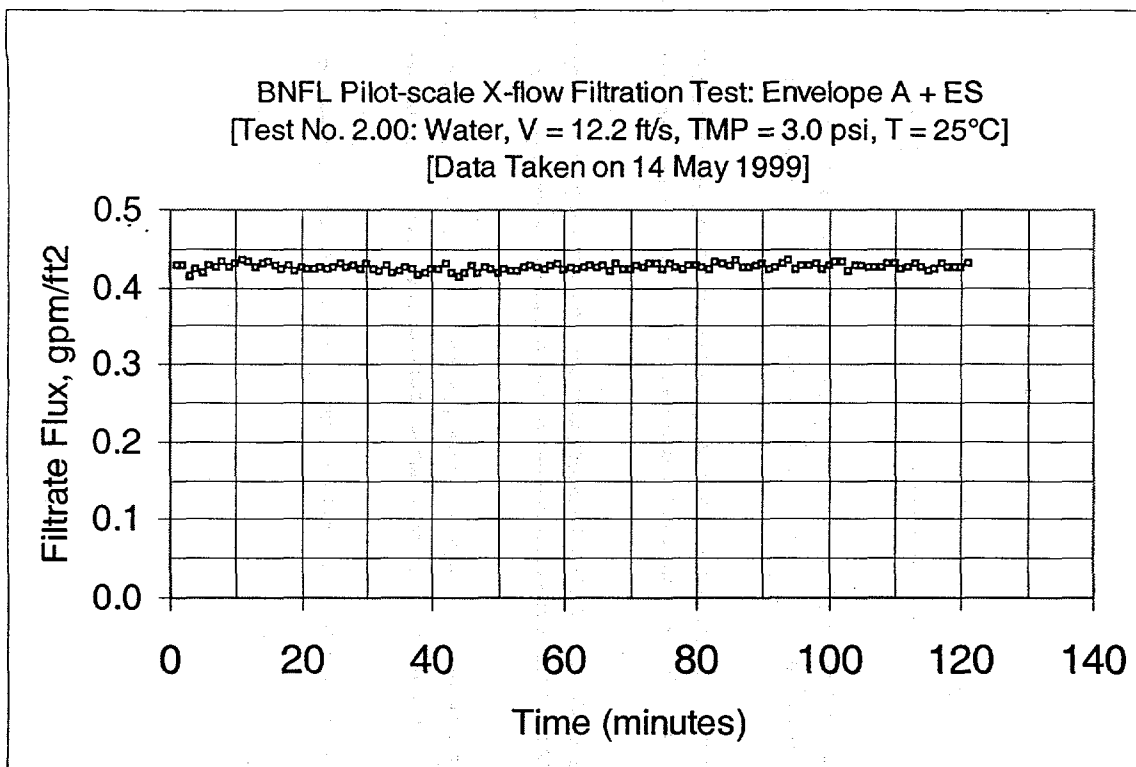


Figure A1: Test Run 2.00, Deionized and Filtered (0.2 micron) Water

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.00

DATE		TIME		C		D		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																									
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	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
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11	16	23	31	38	45	52	59	66	73	80	87	94	101	108	115	122	129	136	143	150	157	164	171	178	185	192	199
12	17	24	32	39	46	53	60	67	74	81	88	95	102	109	116	123	130	137	144	151	158	165	172	179	186	193	200
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18	23	30	38	45	52	59	66	73	80	87	94	101	108	115	122	129	136	143	150	157	164	171	178	185	192	199	206
19	24	31	39	46	53	60	67	74	81	88	95	102	109	116	123	130	137	144	151	158	165	172	179	186	193	200	207
20	25	32	40	47	54	61	68	75	82	89	96	103	110	117	124	131	138	145	152	159	166	173	180	187	194	201	208
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25	30	37	45	52	59	66	73	80	87	94	101	108	115	122	129	136	143	150	157	164	171	178	185	192	199	206	213
26	31	38	46	53	60	67	74	81	88	95	102	109	116	123	130	137	144	151	158	165	172	179	186	193	200	207	214
27	32	39	47	54	61	68	75	82	89	96	103	110	117	124	131	138	145	152	159	166	173	180	187	194	201	208	215
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31	36	43	51	58	65	72	79	86	93	100	107	114	121	128	135	142	149	156	163	170	177	184	191	198	205	212	219
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33	38	45	53	60	67	74	81	88	95	102	109	116	123	130	137	144	151	158	165	172	179	186	193	200	207	214	221
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40	45	52	60	67	74	81	88	95	102	109	116	123	130	137	144	151	158	165	172	179	186	193	200	207	214	221	228
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51	56	63	71	78	85	92	99	106	113	120	127	134	141	148	155	162	169	176	183	190	197	204	211	218	225	232	239
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57	62	69	77	84	91	98	105	112	119	126																	

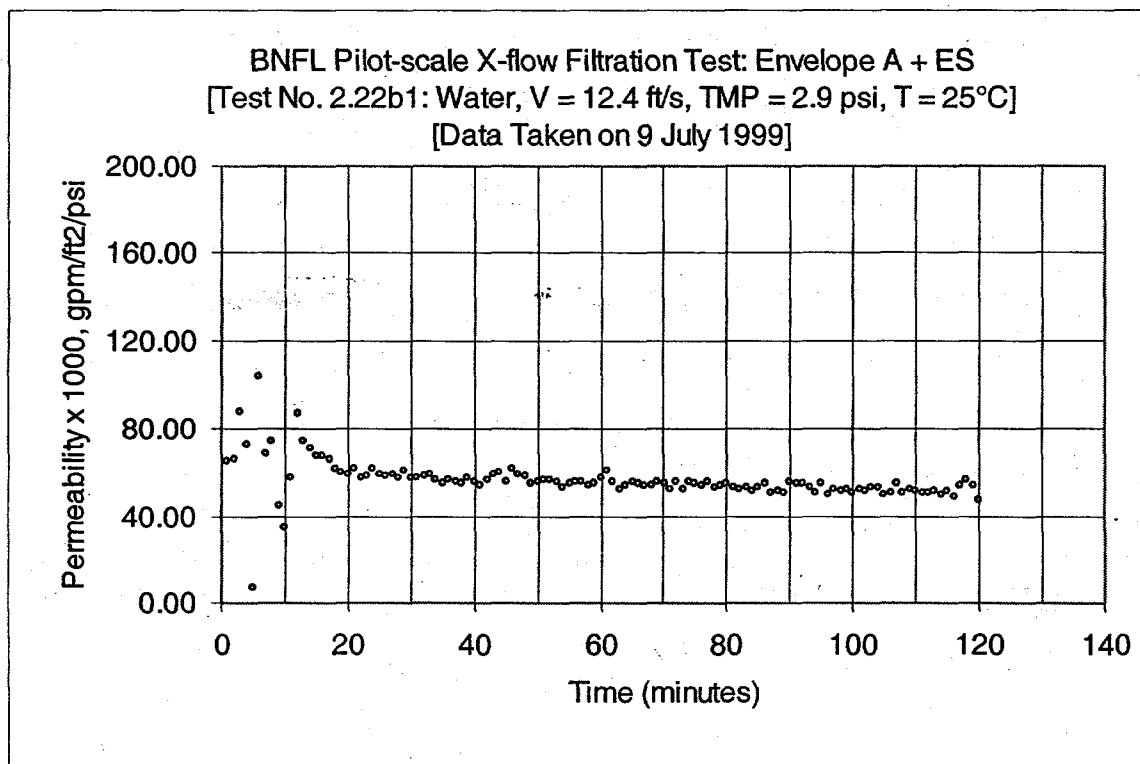
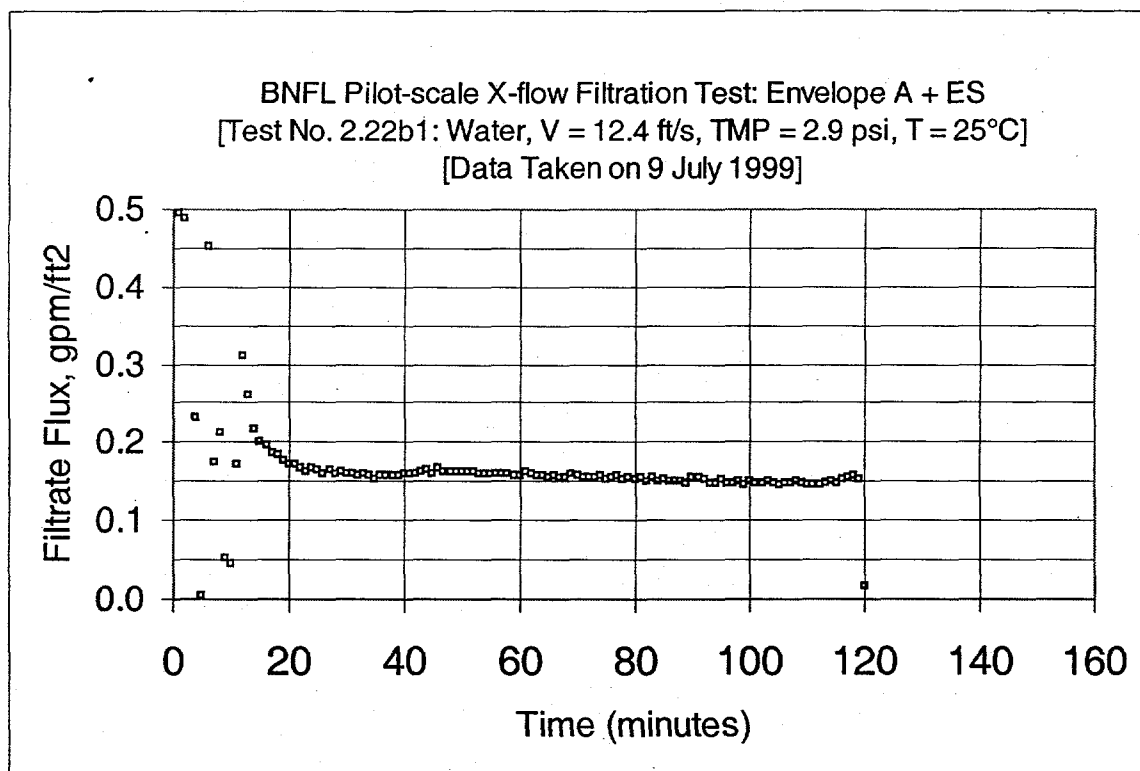


Figure A2: Test Run 2.22b1, Deionized and Filtered (0.2 micron) Water

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.22b1

[illegible]

7/8/1999	11:02-22 AM	0	25.336	26.261	25.354	24.658	21.748	4.464	9.06	3.633	1.308	4.39	0.644	29.88	0.342	0.001	76	12.4	2.9	0.2	0.16	0.16	0.054	54.17
7/8/1999	11:11-22 AM	0	25.351	25.316	24.659	24.655	21.738	4.459	9.202	3.676	1.105	4.39	0.018	29.848	0.346	0.001	77	12.4	2.6	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:22-22 AM	0	25.311	25.319	24.659	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	77	12.4	2.6	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:23-22 AM	0	25.552	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	77	12.4	2.6	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:23-22 AM	0	25.672	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	77	12.4	2.6	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:23-22 AM	0	25.672	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	77	12.4	2.6	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:24-22 AM	0	25.752	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	81	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:24-22 AM	0	25.752	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	82	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:24-22 AM	0	25.752	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	82	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
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7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
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7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
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7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
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7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0	25.807	25.316	25.319	24.655	21.741	4.462	9.234	3.659	1.103	4.39	0.018	29.848	0.346	0.001	83	12.4	2.9	0.2	0.16	0.16	0.054	55.35
7/8/1999	11:25-22 AM	0																						

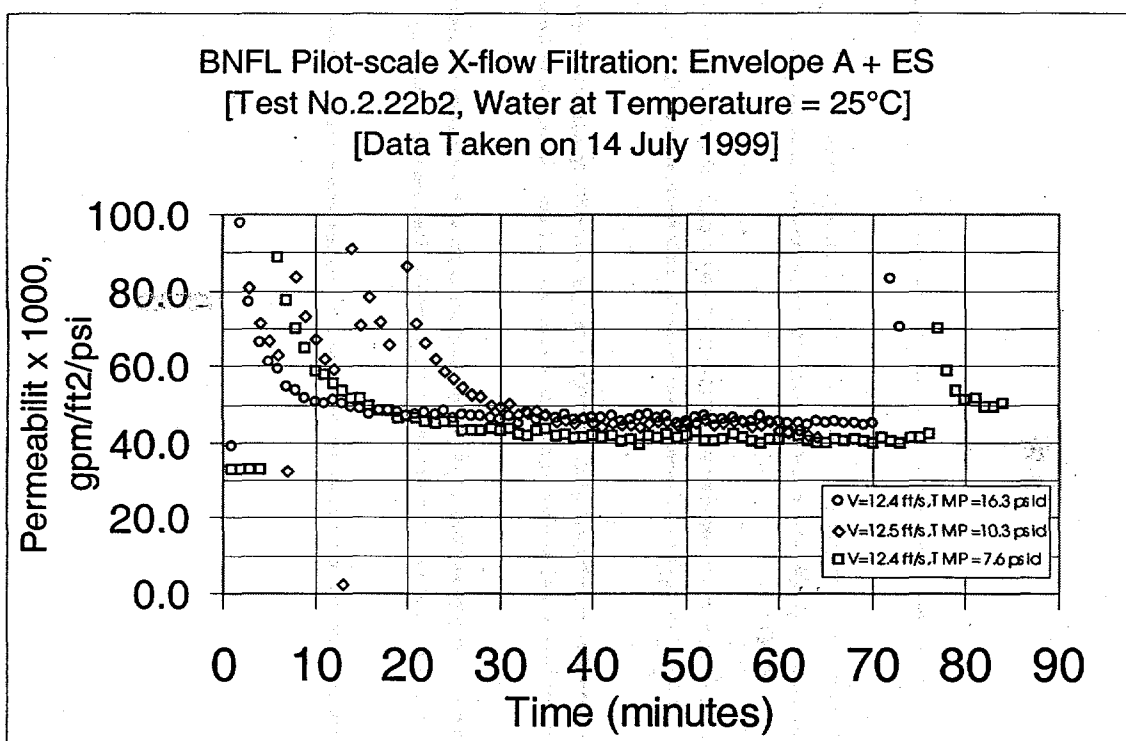
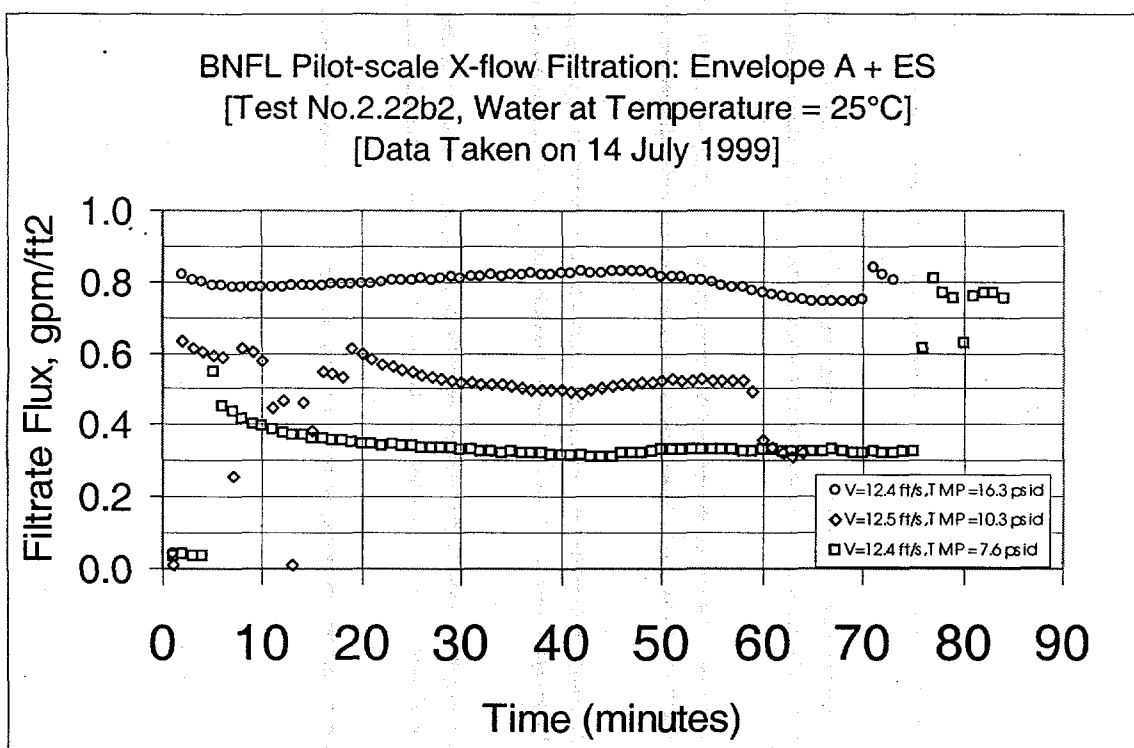


Figure A3: Test Run 2.22b, Deionized and Filtered (0.2 micron) Water

A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	AB
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28
29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56
57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84
85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100	101	102	103	104	105	106	107	108	109	110	111	112
113	114	115	116	117	118	119	120	121	122	123	124	125	126	127	128	129	130	131	132	133	134	135	136	137	138	139	140
141	142	143	144	145	146	147	148	149	150	151	152	153	154	155	156	157	158	159	160	161	162	163	164	165	166	167	168
169	170	171	172	173	174	175	176	177	178	179	180	181	182	183	184	185	186	187	188	189	190	191	192	193	194	195	196
197	198	199	200	201	202	203	204	205	206	207	208	209	210	211	212	213	214	215	216	217	218	219	220	221	222	223	224
225	226	227	228	229	230	231	232	233	234	235	236	237	238	239	240	241	242	243	244	245	246	247	248	249	250	251	252
253	254	255	256	257	258	259	260	261	262	263	264	265	266	267	268	269	270	271	272	273	274	275	276	277	278	279	280
281	282	283	284	285	286	287	288	289	290	291	292	293	294	295	296	297	298	299	300	301	302	303	304	305	306	307	308
309	310	311	312	313	314	315	316	317	318	319	320	321	322	323	324	325	326	327	328	329	330	331	332	333	334	335	336
337	338	339	340	341	342	343	344	345	346	347	348	349	350	351	352	353	354	355	356	357	358	359	360	361	362	363	364
365	366	367	368	369	370	371	372	373	374	375	376	377	378	379	380	381	382	383	384	385	386	387	388	389	390	391	392
393	394	395	396	397	398	399	400	401	402	403	404	405	406	407	408	409	410	411	412	413	414	415	416	417	418	419	420
421	422	423	424	425	426	427	428	429	430	431	432	433	434	435	436	437	438	439	440	441	442	443	444	445	446	447	448
449	450	451	452	453	454	455	456	457	458	459	460	461	462	463	464	465	466	467	468	469	470	471	472	473	474	475	476
477	478	479	480	481	482	483	484	485	486	487	488	489	490	491	492	493											

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.22b2

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	AB
171	7/14/1999	3:23:40 PM	0	24.323	22.612	23.745	23.982	23.982	30.802	30.802	44.316	3.399	15.011	23.614	-0.042	29.737	1.218	1.748	164	164	164	164	164	164	164	164	164	164
172	7/14/1999	3:24:40 PM	0	24.027	22.597	23.541	23.862	23.862	30.625	30.625	44.284	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	165	165	165	165	165	165	165	165	165	165
173	7/14/1999	3:25:40 PM	0	23.911	22.612	23.424	23.862	23.862	30.744	30.744	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	166	166	166	166	166	166	166	166	166	166
174	7/14/1999	3:26:40 PM	0	23.911	22.612	23.424	23.862	23.862	30.744	30.744	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	167	167	167	167	167	167	167	167	167	167
175	7/14/1999	3:27:40 PM	0	23.715	22.612	23.283	23.862	23.862	30.625	30.625	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	168	168	168	168	168	168	168	168	168	168
176	7/14/1999	3:28:40 PM	0	23.520	22.612	23.142	23.862	23.862	30.507	30.507	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	169	169	169	169	169	169	169	169	169	169
177	7/14/1999	3:29:40 PM	0	23.324	22.612	23.001	23.862	23.862	30.389	30.389	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	170	170	170	170	170	170	170	170	170	170
178	7/14/1999	3:30:40 PM	0	23.128	22.612	22.860	23.862	23.862	30.271	30.271	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	171	171	171	171	171	171	171	171	171	171
179	7/14/1999	3:31:40 PM	0	22.932	22.612	22.719	23.862	23.862	30.153	30.153	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	172	172	172	172	172	172	172	172	172	172
180	7/14/1999	3:32:40 PM	0	22.736	22.612	22.576	23.862	23.862	30.035	30.035	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	173	173	173	173	173	173	173	173	173	173
181	7/14/1999	3:33:40 PM	0	22.540	22.612	22.424	23.862	23.862	29.917	29.917	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	174	174	174	174	174	174	174	174	174	174
182	7/14/1999	3:34:40 PM	0	22.344	22.612	22.228	23.862	23.862	29.799	29.799	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	175	175	175	175	175	175	175	175	175	175
183	7/14/1999	3:35:40 PM	0	22.148	22.612	22.032	23.862	23.862	29.681	29.681	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	176	176	176	176	176	176	176	176	176	176
184	7/14/1999	3:36:40 PM	0	21.952	22.612	21.836	23.862	23.862	29.563	29.563	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	177	177	177	177	177	177	177	177	177	177
185	7/14/1999	3:37:40 PM	0	21.756	22.612	21.640	23.862	23.862	29.445	29.445	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	178	178	178	178	178	178	178	178	178	178
186	7/14/1999	3:38:40 PM	0	21.560	22.612	21.444	23.862	23.862	29.327	29.327	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	179	179	179	179	179	179	179	179	179	179
187	7/14/1999	3:39:40 PM	0	21.364	22.612	21.248	23.862	23.862	29.209	29.209	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	180	180	180	180	180	180	180	180	180	180
188	7/14/1999	3:40:40 PM	0	21.168	22.612	21.052	23.862	23.862	29.091	29.091	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	181	181	181	181	181	181	181	181	181	181
189	7/14/1999	3:41:40 PM	0	20.972	22.612	20.856	23.862	23.862	28.973	28.973	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	182	182	182	182	182	182	182	182	182	182
190	7/14/1999	3:42:40 PM	0	20.776	22.612	20.660	23.862	23.862	28.855	28.855	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	183	183	183	183	183	183	183	183	183	183
191	7/14/1999	3:43:40 PM	0	20.580	22.612	20.464	23.862	23.862	28.737	28.737	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	184	184	184	184	184	184	184	184	184	184
192	7/14/1999	3:44:40 PM	0	20.384	22.612	20.268	23.862	23.862	28.619	28.619	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	185	185	185	185	185	185	185	185	185	185
193	7/14/1999	3:45:40 PM	0	20.188	22.612	20.072	23.862	23.862	28.501	28.501	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	186	186	186	186	186	186	186	186	186	186
194	7/14/1999	3:46:40 PM	0	19.992	22.612	19.876	23.862	23.862	28.383	28.383	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	187	187	187	187	187	187	187	187	187	187
195	7/14/1999	3:47:40 PM	0	19.796	22.612	19.680	23.862	23.862	28.265	28.265	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	188	188	188	188	188	188	188	188	188	188
196	7/14/1999	3:48:40 PM	0	19.600	22.612	19.484	23.862	23.862	28.147	28.147	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	189	189	189	189	189	189	189	189	189	189
197	7/14/1999	3:49:40 PM	0	19.404	22.612	19.288	23.862	23.862	28.029	28.029	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	190	190	190	190	190	190	190	190	190	190
198	7/14/1999	3:50:40 PM	0	19.208	22.612	19.092	23.862	23.862	27.911	27.911	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	191	191	191	191	191	191	191	191	191	191
199	7/14/1999	3:51:40 PM	0	19.012	22.612	18.896	23.862	23.862	27.793	27.793	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	192	192	192	192	192	192	192	192	192	192
200	7/14/1999	3:52:40 PM	0	18.816	22.612	18.700	23.862	23.862	27.675	27.675	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	193	193	193	193	193	193	193	193	193	193
201	7/14/1999	3:53:40 PM	0	18.620	22.612	18.504	23.862	23.862	27.557	27.557	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	194	194	194	194	194	194	194	194	194	194
202	7/14/1999	3:54:40 PM	0	18.424	22.612	18.308	23.862	23.862	27.439	27.439	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	195	195	195	195	195	195	195	195	195	195
203	7/14/1999	3:55:40 PM	0	18.228	22.612	18.112	23.862	23.862	27.321	27.321	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	196	196	196	196	196	196	196	196	196	196
204	7/14/1999	3:56:40 PM	0	18.032	22.612	17.916	23.862	23.862	27.203	27.203	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	197	197	197	197	197	197	197	197	197	197
205	7/14/1999	3:57:40 PM	0	17.836	22.612	17.720	23.862	23.862	27.085	27.085	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	198	198	198	198	198	198	198	198	198	198
206	7/14/1999	3:58:40 PM	0	17.640	22.612	17.524	23.862	23.862	26.967	26.967	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	199	199	199	199	199	199	199	199	199	199
207	7/14/1999	3:59:40 PM	0	17.444	22.612	17.328	23.862	23.862	26.849	26.849	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	200	200	200	200	200	200	200	200	200	200
208	7/14/1999	4:00:35 PM	0	17.248	22.612	17.132	23.862	23.862	26.731	26.731	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	201	201	201	201	201	201	201	201	201	201
209	7/14/1999	4:01:35 PM	0	17.052	22.612	16.936	23.862	23.862	26.613	26.613	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	202	202	202	202	202	202	202	202	202	202
210	7/14/1999	4:02:35 PM	0	16.856	22.612	16.740	23.862	23.862	26.495	26.495	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	203	203	203	203	203	203	203	203	203	203
211	7/14/1999	4:03:35 PM	0	16.660	22.612	16.544	23.862	23.862	26.377	26.377	44.316	3.407	15.011	23.539	-0.042	29.735	1.218	1.748	204	204	204	204	204	204	204	204	204	204
212	7/14/1999	4:04:35 PM	0	16.464	22.612	16.348	23.862	23.862	26.259	26.259	44.316	3.407	15.011	23.539	-0.042	29.735												

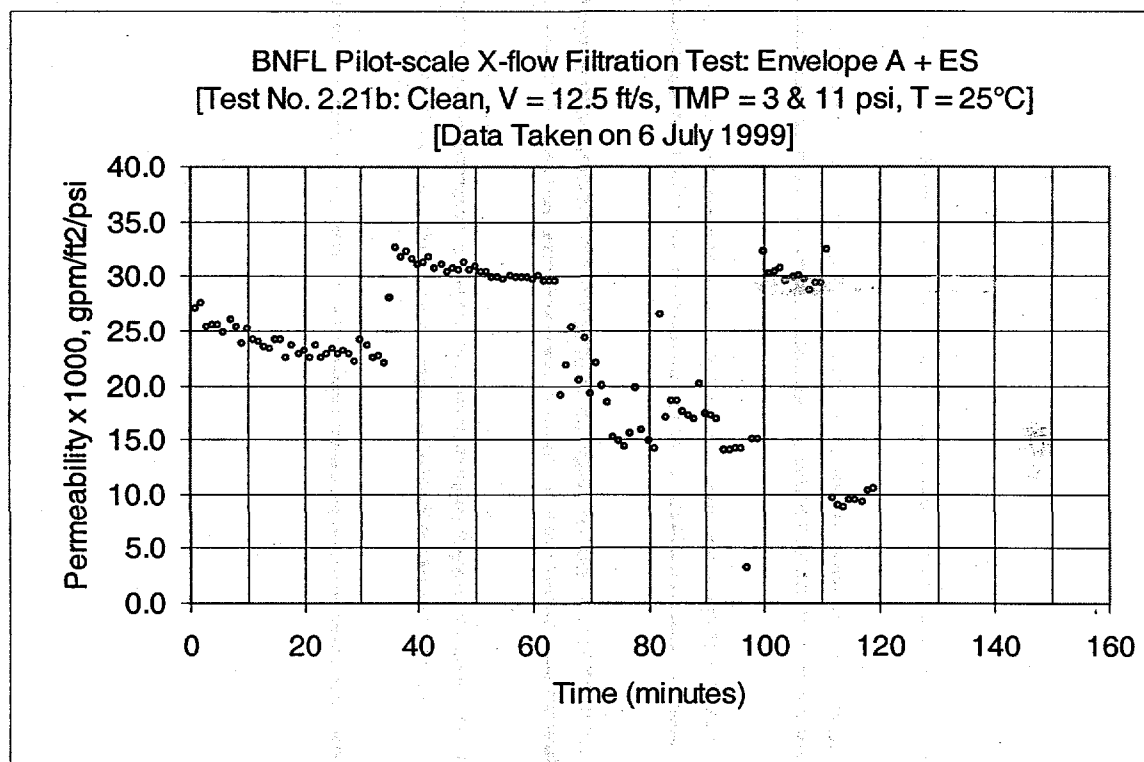
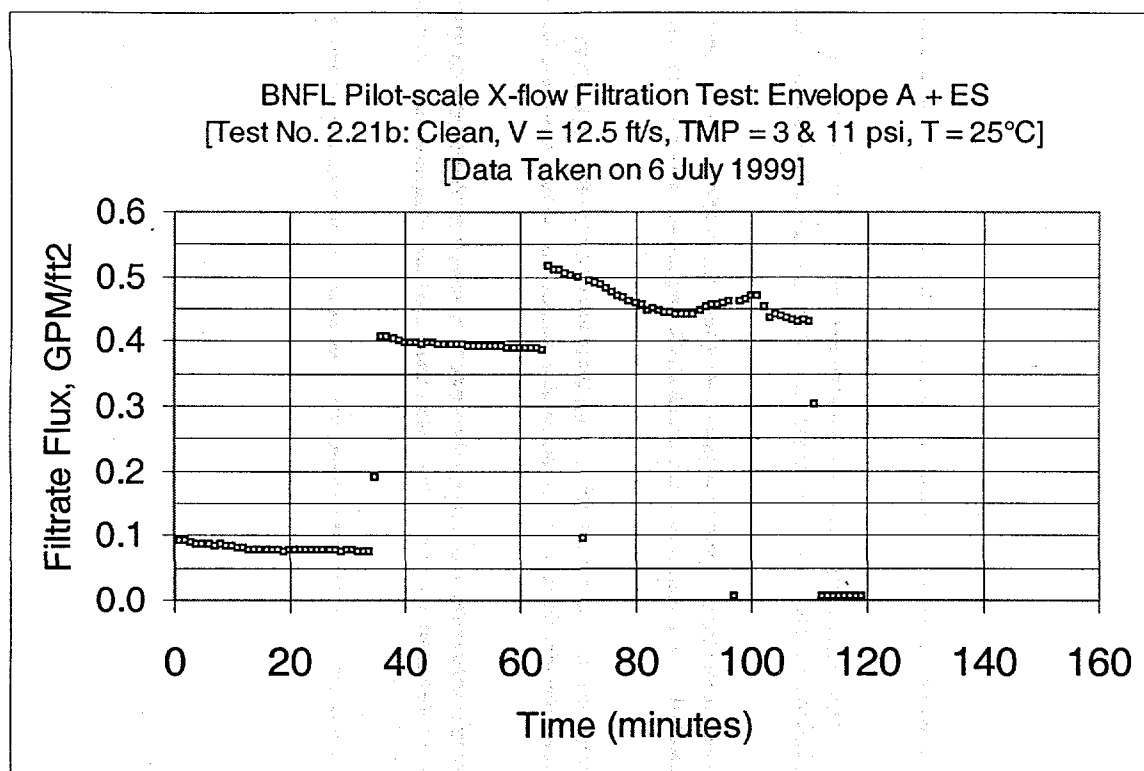


Figure A4: Test Run 2.21b, 1 M NaOH Cleaning

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.21b

[illegible]

APPENDIX B**EXPERIMENTAL DATA: LOW SOLIDS CONCENTRATION**Appendix Contents

1. Nomenclature sheet for data tables

2. Experimental data:

Fig.	Run	Solution	Done on
B1	2.01	0.5 wt% Solids	5/17/99
B2	2.02	0.5 wt% Solids	5/18/99
B3	2.03	0.5 wt% Solids	5/18/99
B4	2.04	0.5 wt% Solids	5/18/99
B5	2.05	0.5 wt% Solids	5/19/99
B6	2.06	0.5 wt% Solids	5/19/99
B7	2.07	0.5 wt% Solids	5/19/99
B8	2.08	0.5 wt% Solids	5/19/99
B9	2.09	0.5 wt% Solids	5/20/99
B10	2.10	0.5 wt% Solids	5/20/99
B11	2.10b	0.5 wt% Solids	5/24/99
B12	2.10c	0.5 wt% Solids	5/24/99
B13	2.11	0.5 wt% Solids	5/24/99
B14	2.12	0.5 wt% Solids	5/25/99
B15	2.13	0.5 wt% Solids	5/25/99
B16	2.07b	0.5 wt% Solids	5/26/99
B17	2.07c	0.5 wt% Solids	5/27/99

General Note: For measurement uncertainties see Appendix F

Special Notes:

- The data for every test run are highlighted with two graphs: Filtrate Flux vs. Time and Permeability vs. Time. Those graphs include all the data taken during the run period.
- The beginning and end of the data for most graphs show large deviations from the overall series of points. Those deviations were caused by backpulsing the filter that temporarily stopped the flow of filtrate.
- All columns of data, in all the tables, are ended with several statistical values of that column, i.e., Average, Maximum, Median, Minimum, Standard Deviation, and Number of Points used (in calculating the 5 statistical quantities). Most of the data with time were maintain constant, and therefore the statistics are meaningful for normally distributed data, however Filtrate Flux and Permeability decrease with time and therefore are not normally distributed.
- To calculate those quantities mentioned in item c, only those data points that start from the end of a backpulse to just before the ending backpulse were included. This is the reason why the quantity of Number of Points Used was given.
- The data for the graphs, and all the data taken for the individual test run that the graphs represent, immediately follow the specific figure.

- f. Run 2.03 only has about 35 minutes of data. The run was made for the full two hours required, but the data acquisition system was accidentally stopped in the middle, and was not noticed until the run was complete.
- g. Run 2.10 was redone twice, Runs 2.10b and 2.10c, because the meaning of "best" run by filtrate flux and permeability were also evaluated.
- h. Run 2.07 was redone, Runs 2.07b and 2.07c, after Run 2.13 to investigate the filter operation over a longer period than just two hours. Run 2.07b was one continuous run without interruption from a backpulse and Run 2.07c was done with varying backpulse frequencies.

Nomenclature For Data Sheets

(See Figure 1: Main Test Rig - Pilot Scale Cross Flow for the Instrument Location)

Column	Heading		Full Heading	Explanation
A =	DATE	=	DATE	Day the test was done
B =	TIME	=	TIME	Time data entry was made
C =	SOLENOID	=	SOLENOID	1=yes, 0=no: for the pressure to the backpulse piston
D =	FLTRT (deg C)	=	FLTRT (deg C) T2	Filtrate Temperature in Filter at exit of the Filter Housing
E =	CL LOOP (deg C)	=	CL LOOP (deg C) T3	Temperature of Liquid in the Cleaning Loop
F =	SL LOOP (deg C)	=	SL LOOP (deg C) T1	Temperature of Liquid in the Slurry Loop at the Reservoir Tank
G =	UP AMB (deg C)	=	UP AMB (deg C) T4	Ambient Temperature at the top of the Test Rig - 3rd level
H =	BOT AMB (deg C)	=	BOT AMB (deg C) T5	Ambient Temperature at the bottom of the Test Rig - 1st level
I =	T6 (deg C)	=	T6 (deg C) SPARE	Spare Thermocouple - Currently Not Being Used
J =	BOT DP (psid)	=	BOT DP (psid) dP2	Differential Pressure between the Filter Slurry Entrance and the bottom Filtrate Exit
K =	FLTR (psig)	=	FLTR (psig) P1	Gauge Pressure at the Filter Slurry Entrance
L =	FLTR DP (psid)	=	FLTR DP (psid) dP1	Differential Pressure between the Filter Slurry Entrance and Exit
M =	TOP DP (psid)	=	TOP DP (psid) dP3	Differential Pressure between the Filter Slurry Exit and the Top Filtrate Exit
N =	FLTRATE (psig)	=	FLTRATE (psig) P2	Gauge Pressure at the Filter Filtrate Exit
O =	PISTON (psig)	=	PISTON (psig) P3	Air Gauge Pressure Applied to Backpulse Piston
P =	SL FLOW (gpm)	=	SL FLOW (gpm) Q1	Flow Rate of the Slurry Flow
Q =	FLTR FLOW (gpm)	=	FLTR FLOW (gpm) Q2	Flow Rate of the Filtrate Flow
R =	V9	=		Spare Channel Not Used

The following columns are calculated results based on the appropriate columns

S =	Number	=	Number	Data number which is equivalent to 1 minute since this was the acquisition frequency
T =	Vel, ft/s	=	Vel, ft/s	Axial slurry velocity = [Column P] / 7.48 gal/ft ² / 60 sec/min / flow area (=0.005369 ft ²)
U =	TMP, PSI	=	TMP, PSI	Transmembrane Pressure = ([Column J] + [Column M])/2
V =	TMP, bar	=	TMP, bar	[Column U] / 14.504 bar/psi
W =	GPM/FT2	=	GPM/FT2	[Column Q] / inside diameter filter surface area (= 2.29 ft ²)
X =	GPM/FT2	=	GPM/FT2 at 25°C	Test Spec. correction factor: [Column W] x exp(2500 x ((1/(273+(Column T)))-(1/298)))
Y =	PERMEABILITY	=	PERMEABILITY (gpm/ft ² /psi)	[Column X] / [Column U]
Z =	x 1000	=	PERMEABILITY x 1000	[Column Z] x 1000
AA =	PERMEABILITY	=	PERMEABILITY (m/day/bar)	[Column Y] x conversion factor (= 351.0145 m/day/bar / gpm/ft ² /bar)

*Axial slurry flow area is based on 7 porous tubes with an inside diameter of 3/8 inch: $7 \times \pi / 4 \times (0.375 \text{ inch} / 12 \text{ inches/ft})^2 = 0.005369 \text{ ft}^2$ **Inside diameter filter surface area for 7 tubes with an inside diameter of 3/8 inch, 40-inches long: $7 \times \pi \times (0.375 \text{ inch}) \times 40 \text{ inches} / 144 \text{ in}^2/\text{ft}^2 = 2.29 \text{ ft}^2$ **Exceptions:**

- For Run 2.21b (Cleaning); This run was carried out over a three different periods on three days therefore there are two NUMBER COLUMNS: S & T. Column S is continuous and Column T is continuous but starts over for each period. All the columns to the right of Column S are shifted by one.
- For Run 2.22b (Water); After July 10, 1999 a second filtrate flow meter was added to measure flow rates from 1.2 to 5 gpm. The final water test run (Run 2.22b) has an extra filtrate flow rate column. Column R, the spare column, was made the new flow rate:

R = **Q3, FLTR F** = Q3, FLTR FLOW (gpm) Flow Rate of the Filtrate Flow (above 1.2 gpm), Installed after 7/10/99

also Run 2.22b has two NUMBER columns (like Run 2.21b) so Exception 1 also applies.

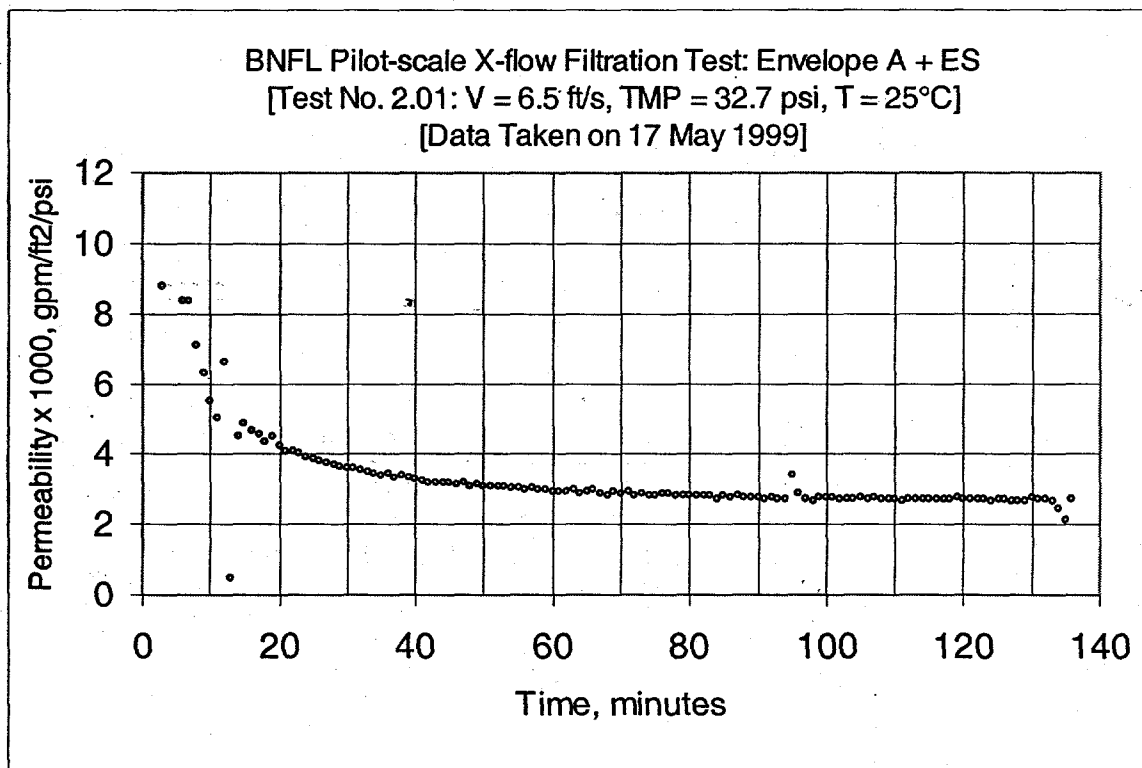
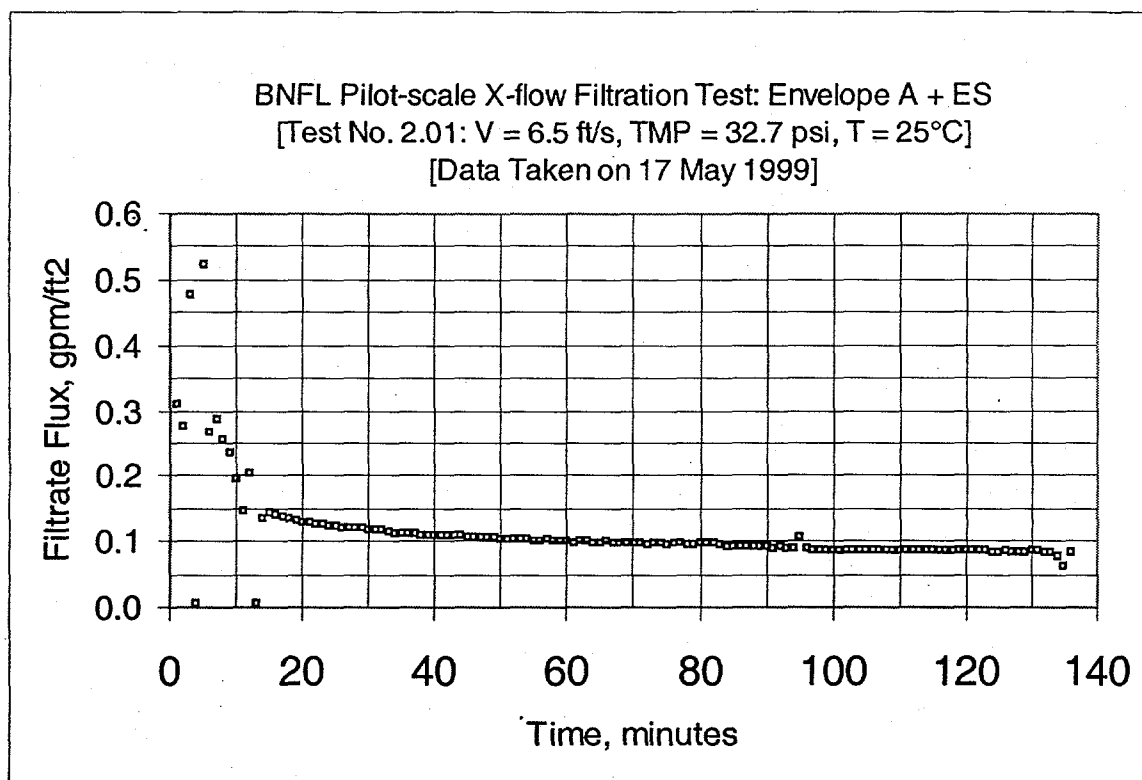


Figure B1: Test Run 2.01, 0.5 wt% Insoluble Solids Concentration

1		2		3		4		5		6		7		8		9		10		11		12		13		14		15		16		17		18		19		20		21		22		23		24		25		26		27		28		29		30		31		32		33		34		35		36		37		38		39		40		41		42		43		44		45		46		47		48		49		50		51		52		53		54		55		56		57		58		59		60		61		62		63		64		65		66		67		68		69		70		71		72		73		74		75		76		77		78		79		80		81		82		83		84		85		86		87		88		89		90		91		92		93		94		95		96		97		98		99		100		101		102		103		104		105		106		107		108		109		110		111		112		113		114		115		116		117		118		119		120		121		122		123		124		125		126		127		128		129		130		131		132		133		134		135		136		137		138		139		140		141		142		143		144		145		146		147		148		149		150		151		152		153		154		155		156		157		158		159		160		161		162		163		164		165		166		167		168		169		170		171		172		173		174		175		176		177		178		179		180		181		182		183		184		185		186		187		188		189		190		191		192		193		194		195		196		197		198		199		200		201		202		203		204		205		206		207		208		209		210		211		212		213		214		215		216		217		218		219		220		221		222		223		224		225		226		227		228		229		230		231		232		233		234		235		236		237		238		239		240		241		242		243		244		245		246		247		248		249		250		251		252		253		254		255		256		257		258		259		260		261		262		263		264		265		266		267		268		269		270		271		272		273		274		275		276		277		278		279		280		281		282		283		284		285		286		287		288		289		290		291		292		293		294		295		296		297		298		299		300		301		302		303		304		305		306		307		308		309		310		311		312		313		314		315		316		317		318		319		320		321		322		323		324		325		326		327		328		329		330		331		332		333		334		335		336		337		338		339		340		341		342		343		344		345		346		347		348		349		350		351		352		353		354		355		356		357		358		359		360		361		362		363		364		365		366		367		368		369		370		371		372		373		374		375		376		377		378		379		380		381		382</	
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Pilot Scale X-Flow Filtration Test: Env. A, Run 2.01

	A	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
1	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
2	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
3	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
4	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
5	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
6	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
7	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
8	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
9	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
10	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
11	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
12	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
13	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
14	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
15	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
16	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
17	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
18	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
19	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
20	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
21	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
22	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
23	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
24	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
25	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
26	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
27	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
28	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
29	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
30	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
31	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
32	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
33	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
34	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
35	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
36	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
37	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
38	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
39	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
40	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
41	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
42	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
43	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
44	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
45	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739	34.832	41.007	4.762	33.54	6.106	0.004	15.525	0.263	0	71	8.4	33.8	2.3	0.112	0.097	0.0028	2.89	2
46	5/17/1999	1:35:14 PM	30.45	23.853	28.933	28.981	25.633	34.739																		

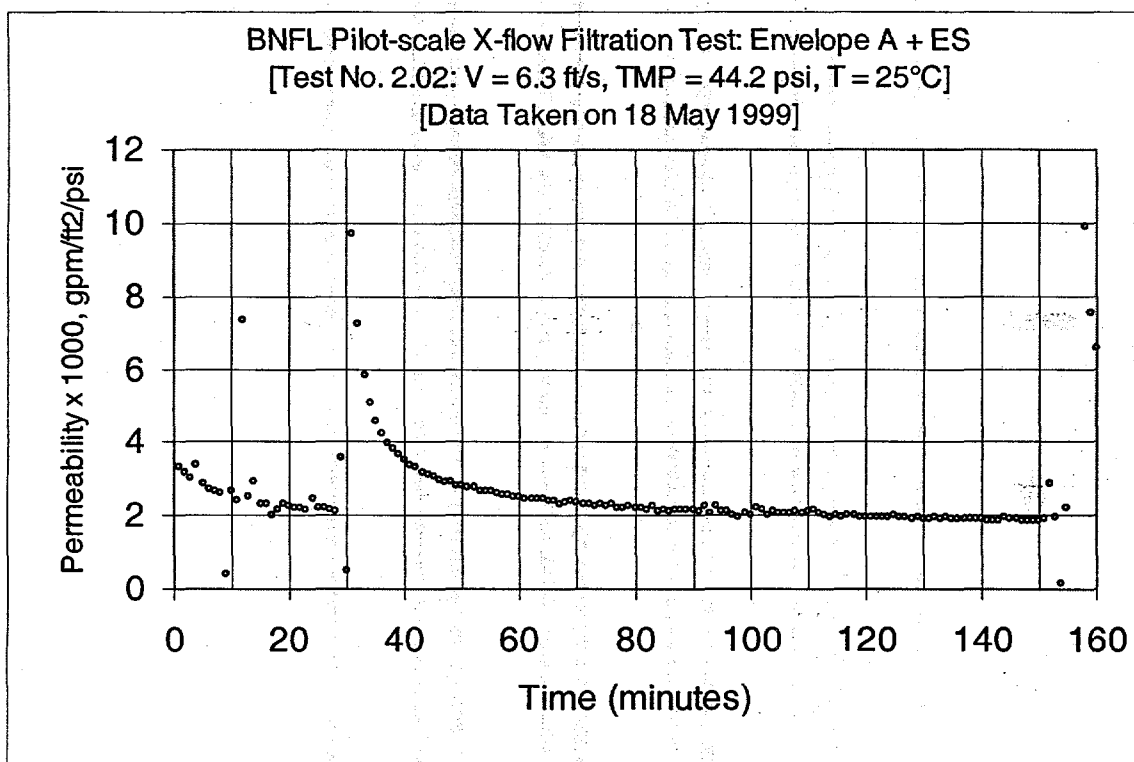
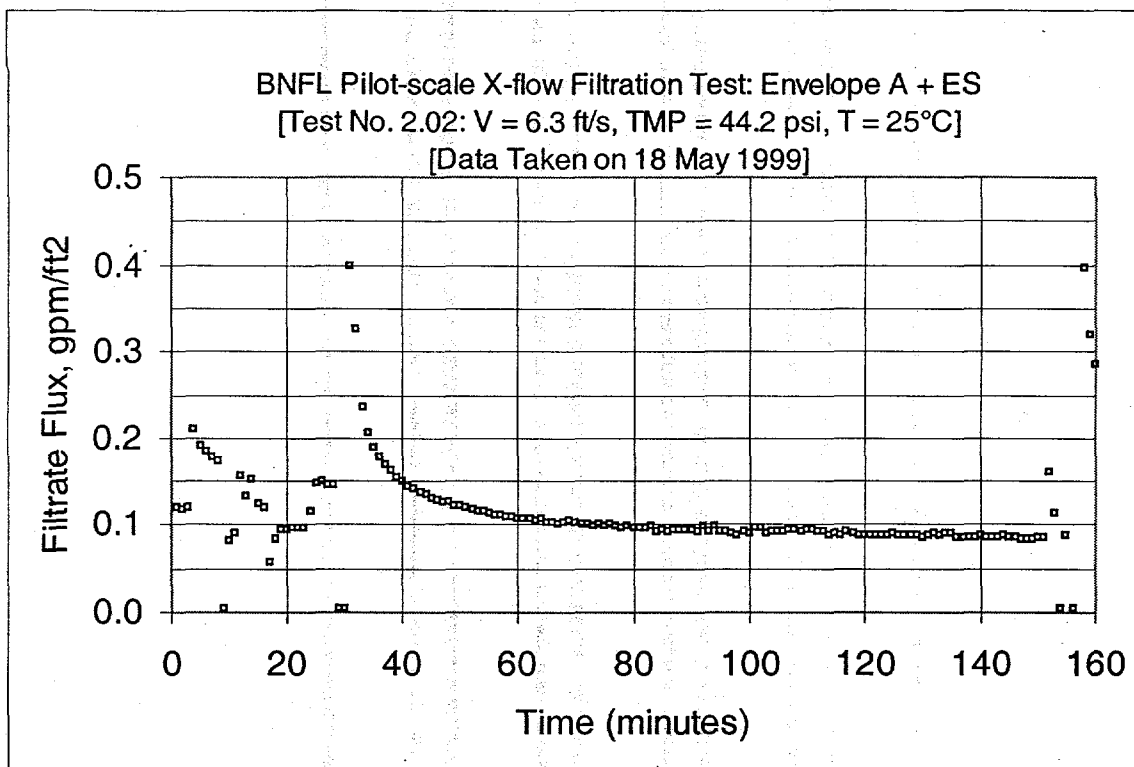


Figure B2: Test Run 2.02, 0.5 wt% Insoluble Solids Concentration

[illegible]

	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
0	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	AM
1	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
2	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
3	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
4	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
5	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
6	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
7	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
8	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
9	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
10	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
11	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
12	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
13	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
14	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
15	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3.0	0.05	0.038	0.002	2.3	
16	24.335	22.72	23.74	24.94	24.94	23.35	30.48	44.73	31.57	2.65	42.9	1.63	-0.88	15.28	0.21	0	71	6.4	43.9	3					

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.02

[illegible]

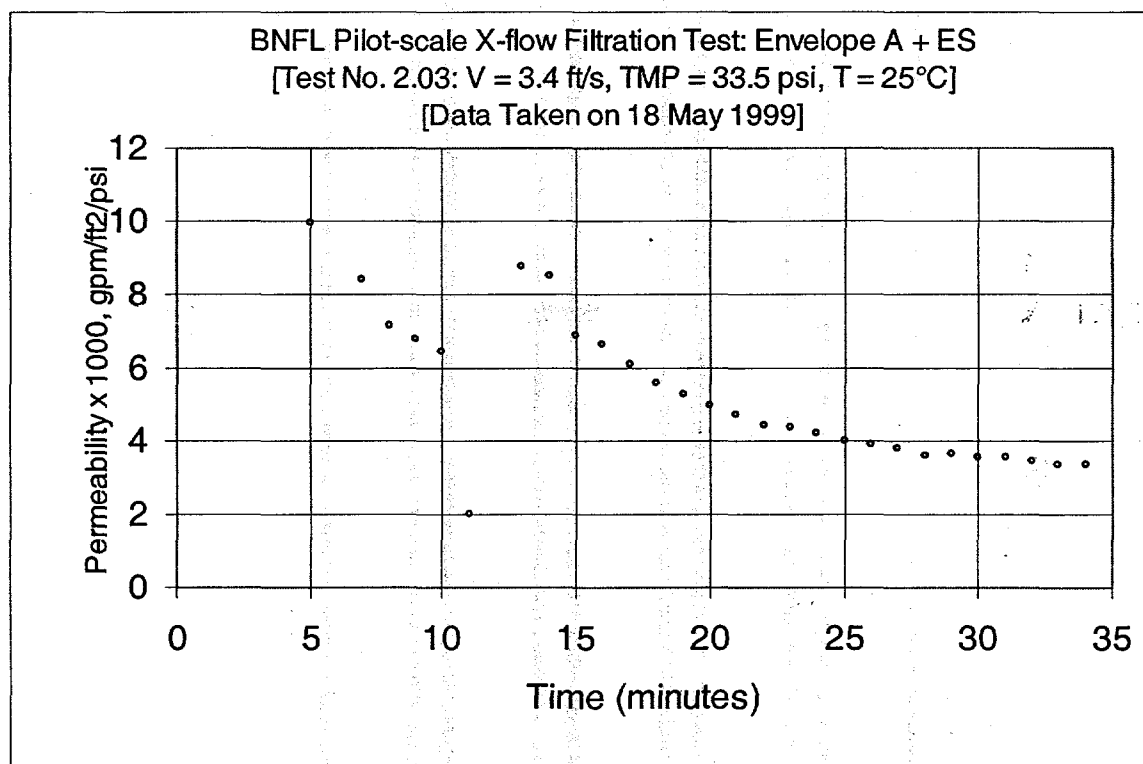
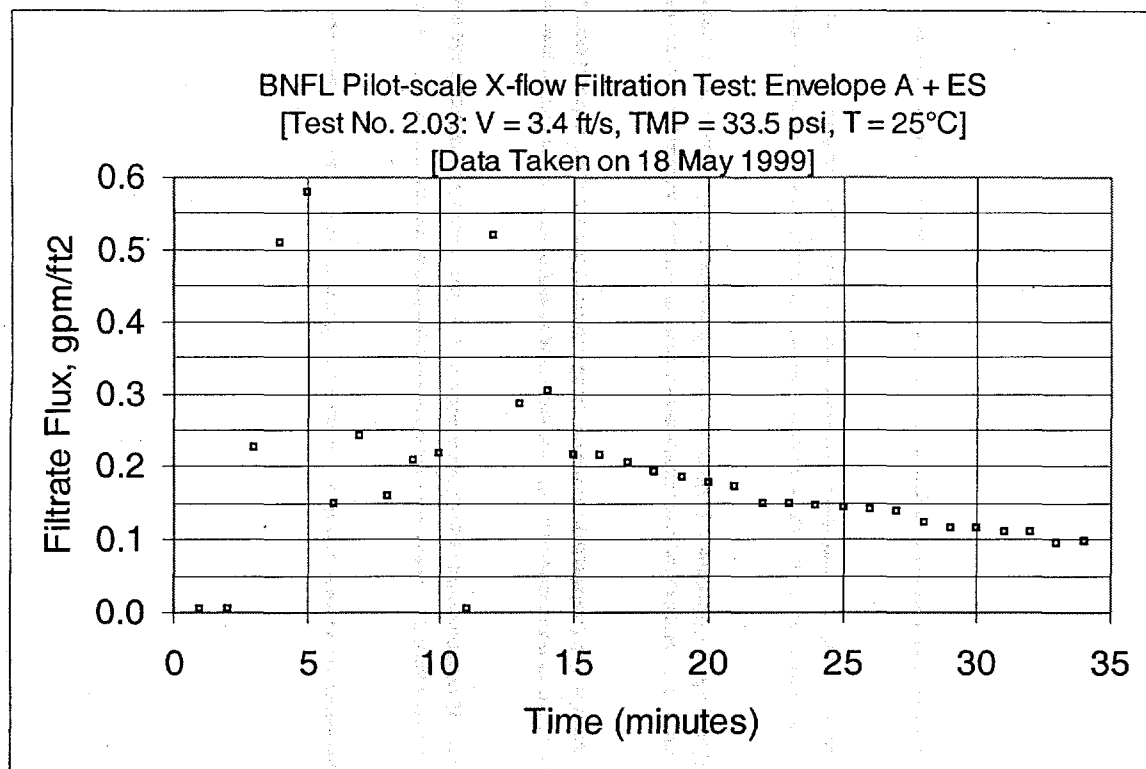


Figure B3: Test Run 2.03, 0.5 wt% Insoluble Solids Concentration

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.03

DATE		TIME	SOLAR	NO. OF PANELS	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
TIME		TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME	TIME
8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	8:10:07 AM	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024	0.03	-0.057	-0.13	-0.095	0.011	0	0	0	0	0	0	0	0	0	0.008	0.0126	10.7	
0	21434	21098	20705	21644	21538	29806	0.124	-0.041	-0.024																		

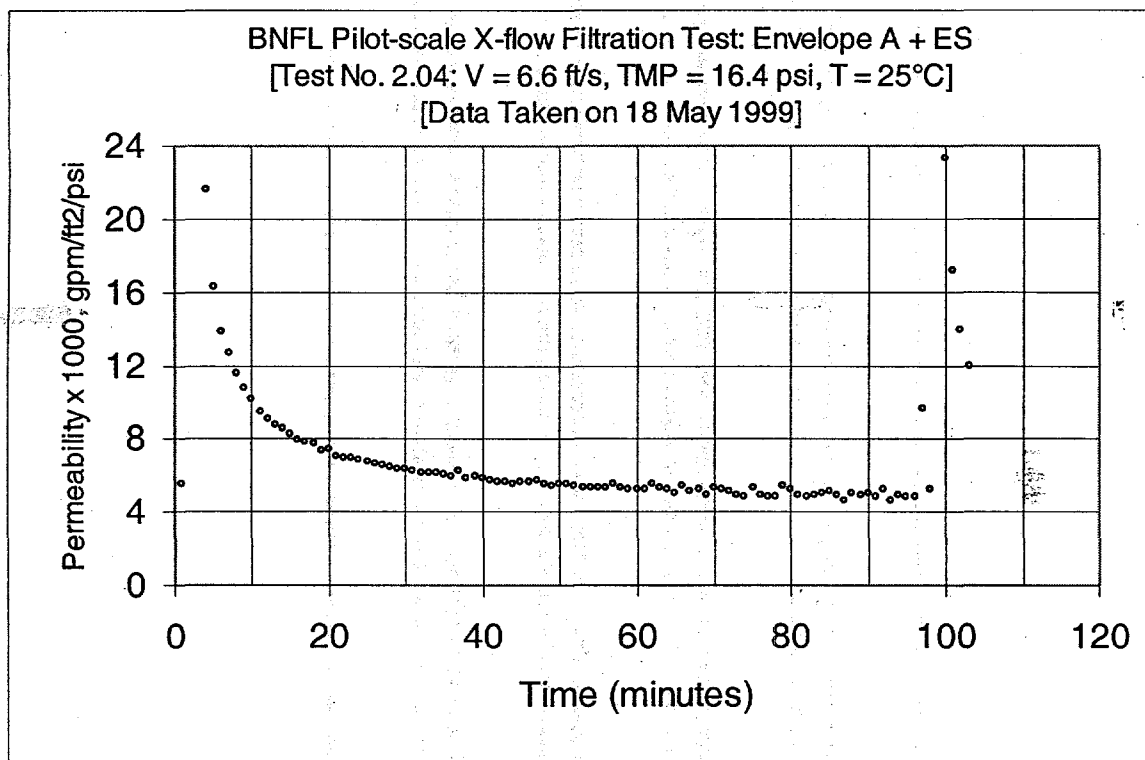
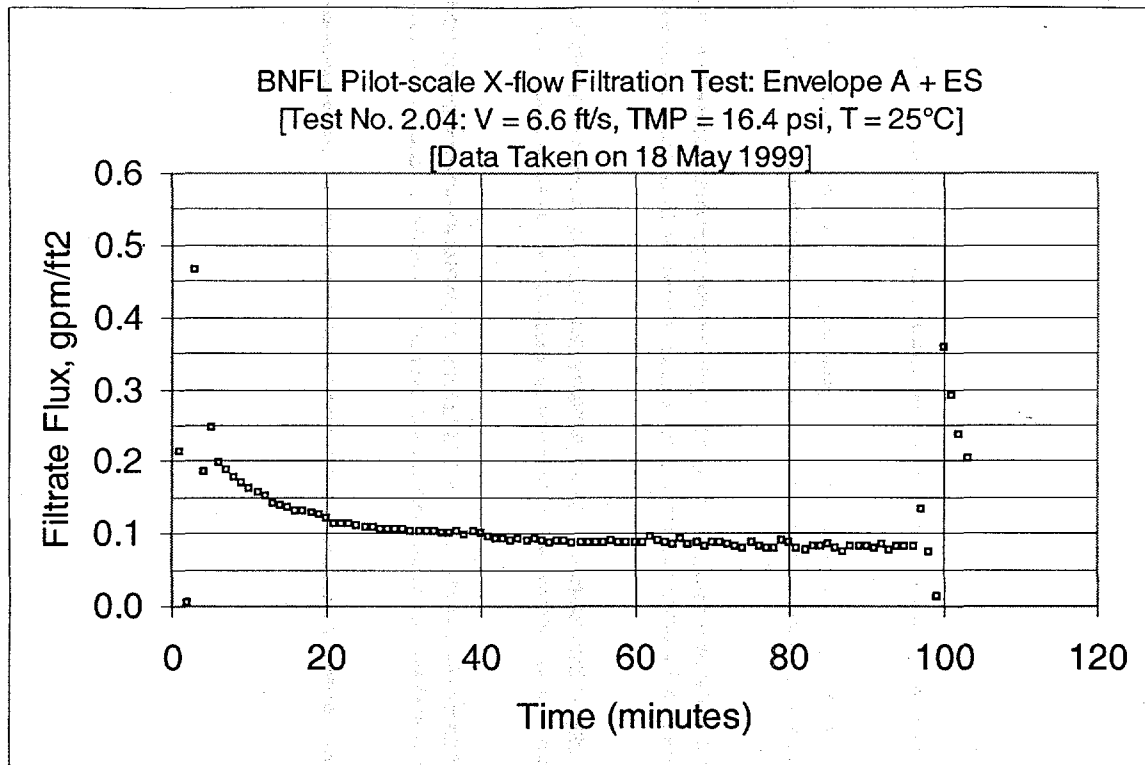


Figure B4: Test Run 2.04, 0.5 wt% Insoluble Solids Concentration

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.04

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.04

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	
1	5701959	42021 PA	23.33	31.059	24.107	23.85	15.563	5.757	-0.042	15.94	0	72	6.8	16.7	1.2	0.080	0.0049	0.082	0.080	0.082	0.080	0.082	0.080	0.082	0.080	0.082	0.080	0.082
2	5701959	43002 PA	23.35	30.845	24.015	23.87	15.533	5.767	-0.042	16.017	0	72	6.8	16.7	1.2	0.080	0.0049	0.082	0.080	0.082	0.080	0.082	0.080	0.082	0.080	0.082	0.080	0.082
3	5701959	43004 PA	23.64	31.009	23.58	23.58	15.564	5.796	-0.042	15.965	0.197	0	75	6.6	16.4	1.1	0.080	0.0050	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
4	5701959	43005 PA	24.75	30.845	24.015	23.87	15.533	5.767	-0.042	16.032	0.187	0	76	6.7	16.7	1.2	0.080	0.0050	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
5	5701959	43006 PA	24.756	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	77	6.6	16.4	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
6	5701959	43007 PA	24.836	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	78	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
7	5701959	43008 PA	24.836	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	79	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
8	5701959	43009 PA	24.997	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	80	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
9	5701959	43010 PA	25.077	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	81	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
10	5701959	43011 PA	25.237	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	82	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
11	5701959	43012 PA	25.237	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	83	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
12	5701959	43013 PA	25.237	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	84	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
13	5701959	43014 PA	25.352	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	85	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
14	5701959	43015 PA	25.477	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	86	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
15	5701959	43016 PA	25.558	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	87	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
16	5701959	43017 PA	25.558	30.859	24.031	23.882	15.568	5.767	-0.042	16.032	0.187	0	88	6.6	16.5	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080	0.081	0.080
17	5701959	43018 PA	25.633	30.84	25.587	25.446	31.13	17.857	23.624	2.685	15.536	5.562	-0.042	15.945	0.184	0	89	6.6	16.6	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080
18	5701959	43019 PA	25.633	30.84	25.587	25.446	31.13	17.857	23.624	2.685	15.536	5.562	-0.042	15.945	0.184	0	90	6.6	16.6	1.1	0.080	0.0049	0.081	0.080	0.081	0.080	0.081	0.080
19	5701959	43020 PA	25.835	30.814	25.587	25.446	31.339	17.729	24.187	2.807	15.487	5.562	-0.042	15.855	0.192	0	91	6.6	16.5	1.1	0.080	0.0048	0.080	0.079	0.080	0.080	0.079	0.080
20	5701959	43021 PA	25.913	30.824	25.587	25.446	30.905	17.712	23.832	2.445	15.467	5.621	-0.042	15.925	0.184	0	92	6.6	16.6	1.1	0.080	0.0048	0.080	0.079	0.080	0.080	0.079	0.080
21	5701959	43022 PA	25.753	30.834	25.587	25.446	30.944	17.941	24.228	2.545	15.587	5.621	-0.042	15.786	0.179	0	93	6.6	16.7	1.2	0.080	0.0047	0.078	0.078	0.078	0.078	0.078	0.078
22	5701959	43023 PA	25.558	30.834	25.587	25.446	30.944	17.941	24.228	2.545	15.587	5.621	-0.042	15.786	0.179	0	94	6.6	16.7	1.2	0.080	0.0047	0.078	0.078	0.078	0.078	0.078	0.078
23	5701959	43024 PA	25.558	30.834	25.587	25.446	30.944	17.941	24.228	2.545	15.587	5.621	-0.042	15.786	0.179	0	95	6.6	16.7	1.2	0.080	0.0047	0.078	0.078	0.078	0.078	0.078	0.078
24	5701959	43025 PA	25.477	30.859	24.81	23.768	23.817	27.877	24.581	2.601	15.344	5.621	-0.042	15.742	0.165	0	96	6.5	17.0	1.2	0.080	0.0048	0.081	0.081	0.081	0.081	0.081	0.081
25	5701959	43026 PA	25.362	30.84	24.836	23.842	23.957	14.504	24.258	2.569	13.933	8.756	-0.089	15.894	0.933	0	97	6.5	14.4	0.0	0.073	0.0135	0.0368	0.0368	0.0368	0.0368	0.0368	0.0368
26	5701959	43027 PA	25.362	30.84	24.836	23.842	23.957	14.504	24.258	2.569	13.933	8.756	-0.089	15.894	0.933	0	98	6.5	14.4	0.0	0.073	0.0135	0.0368	0.0368	0.0368	0.0368	0.0368	0.0368
27	5701959	43028 PA	25.362	30.84	24.836	23.842	23.957	14.504	24.258	2.569	13.933	8.756	-0.089	15.894	0.933	0	99	6.5	14.4	0.0	0.073	0.0135	0.0368	0.0368	0.0368	0.0368	0.0368	0.0368
28	5701959	43029 PA	25.327	30.849	24.039	26.019	20.892	2.727	6.118	5.505	-3.318	2.892	-0.042	20.166	0.031	0	99	11.7	0.2	0.0	0.014	0.014	0.014	0.014	0.014	0.014	0.014	0.014
29	5701959	43030 PA	25.312	30.819	23.924	26.064	20.032	30.045	16.272	27.856	1.7	14.321	11.005	-0.042	12.438	0.746	0	100	5.2	15.4	1.1	0.348	0.355	0.253	0.253	0.253	0.253	0.253
30	5701959	43031 PA	25.616	23.719	23.809	26.109	23.917	30.846	18.07	24.997	2.402	10.005	1.016	-0.042	15.833	0.647	0	101	6.6	17.0	1.2	0.882	0.232	0.232	0.232	0.232	0.232	0.232
31	5701959	43032 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	102	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
32	5701959	43033 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	103	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
33	5701959	43034 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	104	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
34	5701959	43035 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	105	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
35	5701959	43036 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	106	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
36	5701959	43037 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	107	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
37	5701959	43038 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	108	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
38	5701959	43039 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	109	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
39	5701959	43040 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	110	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
40	5701959	43041 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	111	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
41	5701959	43042 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	112	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
42	5701959	43043 PA	24.581	30.925	23.834	26.154	23.862	30.413	18.01	24.107	2.35	15.737	5.562	-0.042	15.879	0.623	0	113	6.6	16.9	1.2	0.298	0.236	0.236	0.236	0.236	0.236	0.236
43	5701959	43044 PA	24.581																									

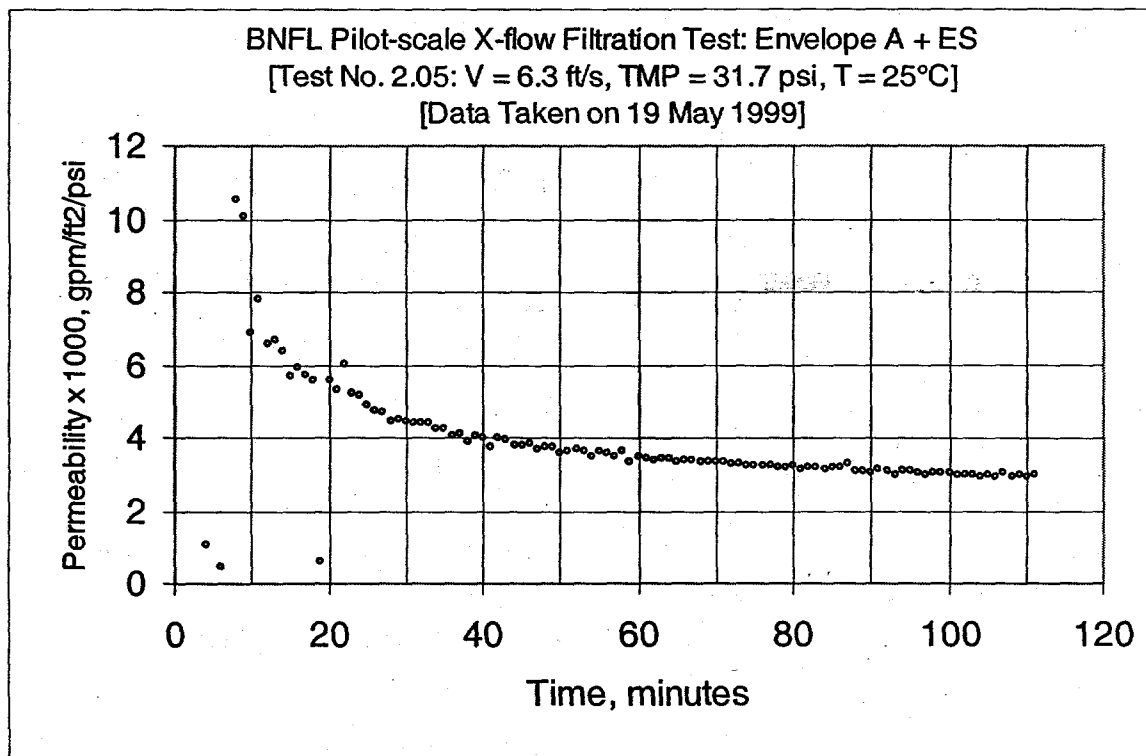
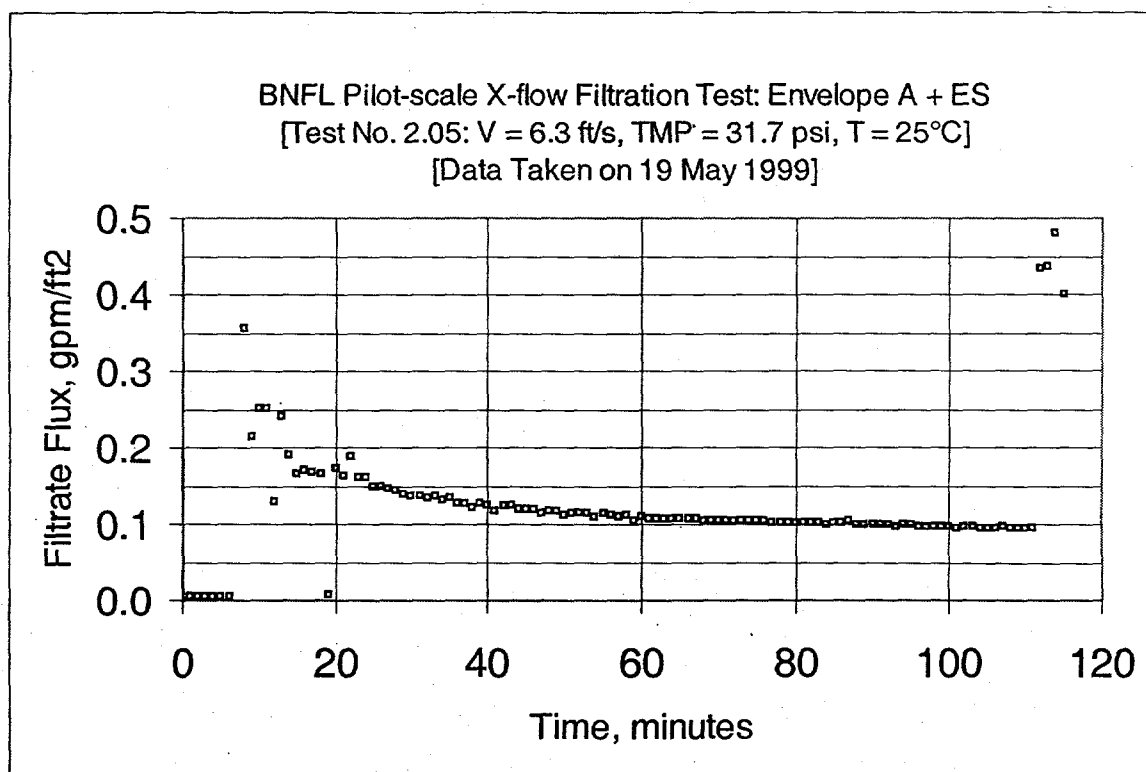


Figure B5: Test Run 2.05, 0.5 wt% Insoluble Solids Concentration

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.05

[illegible]

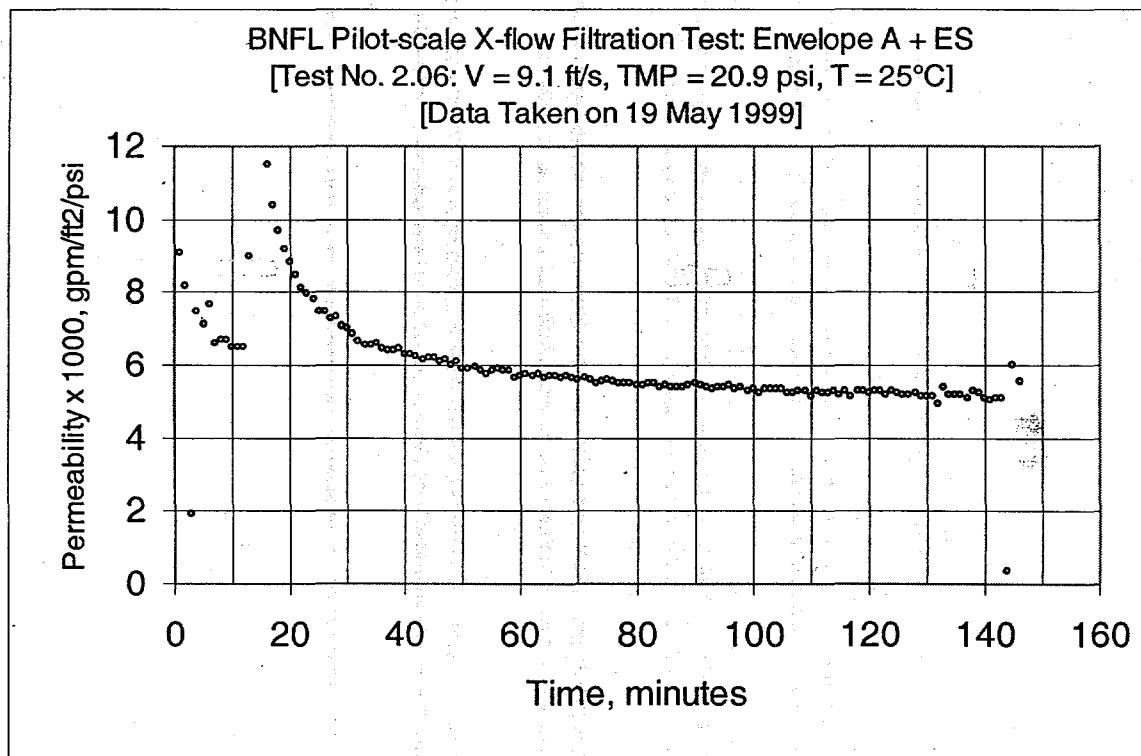
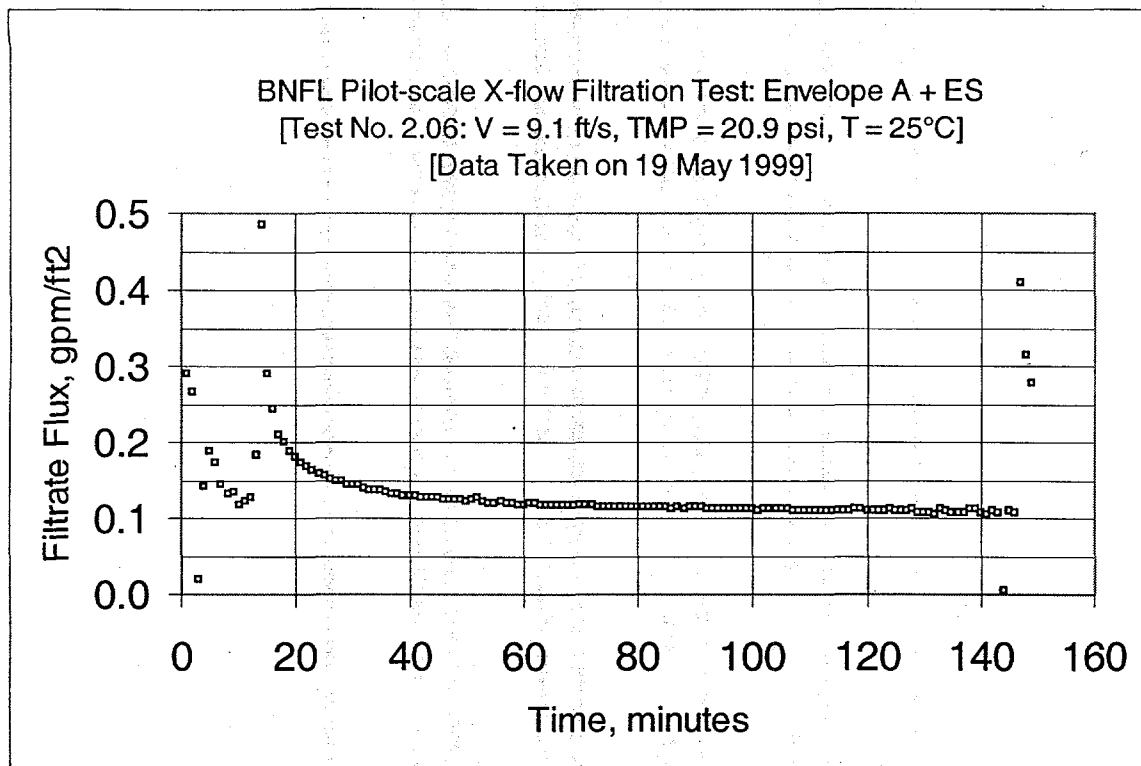


Figure B6: Test Run 2.06, 0.5 wt% Insoluble Solids Concentration

[illegible]

[illegible]

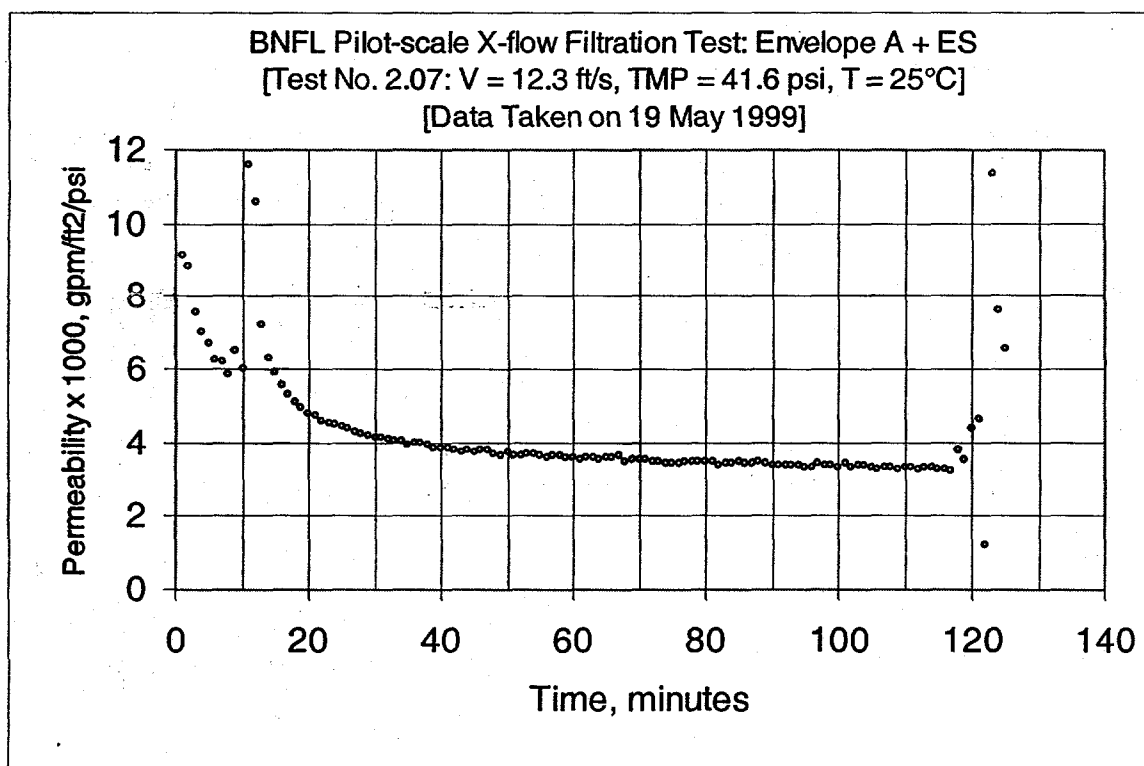
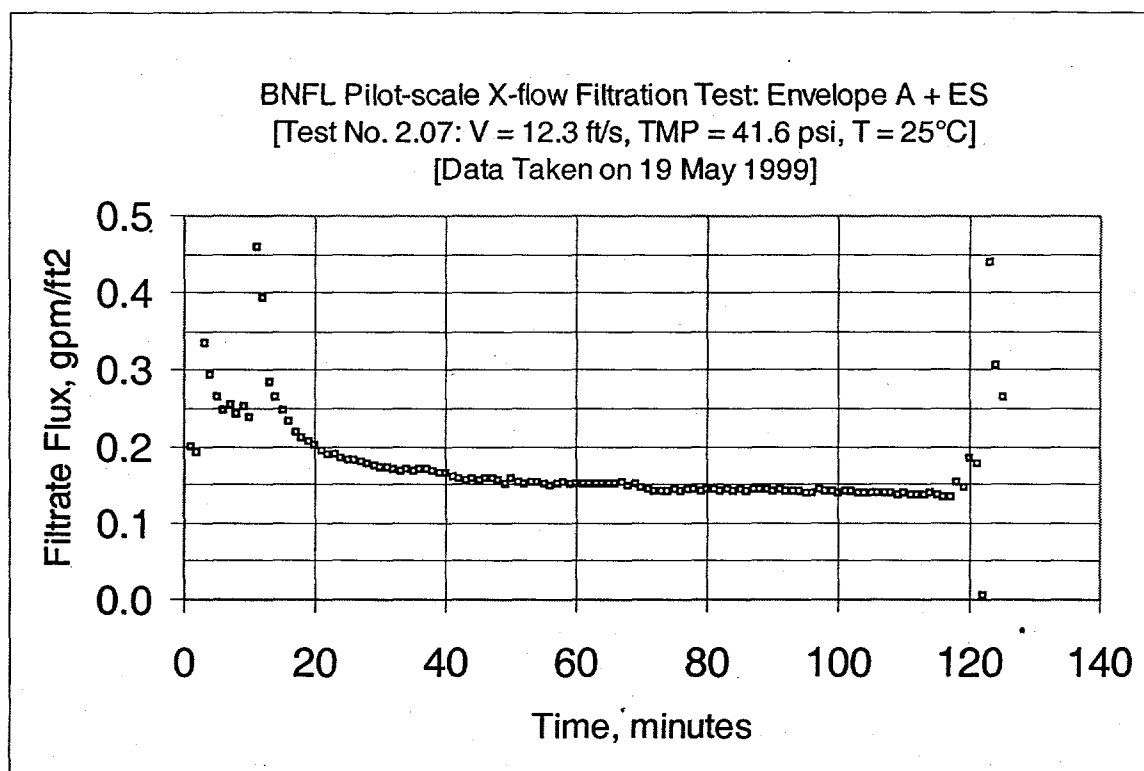


Figure B7: Test Run 2.07, 0.5 wt% Insoluble Solids Concentration

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07

A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
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07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32
07	08	09	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28</				

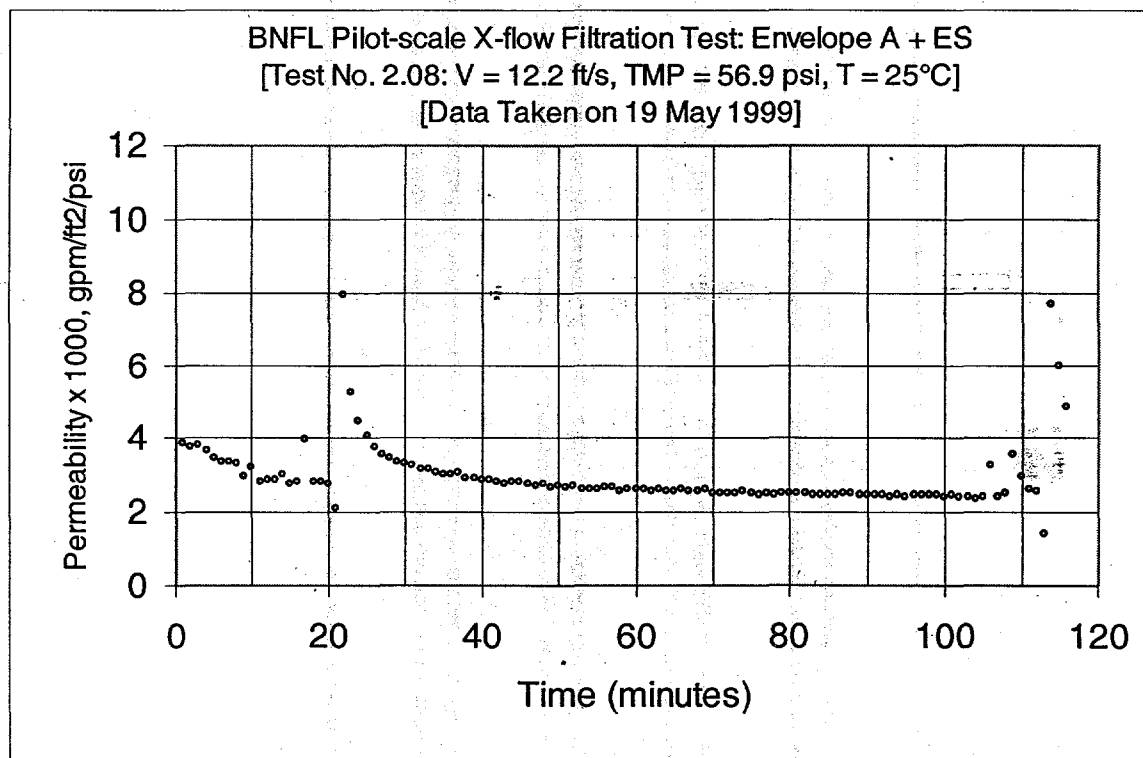
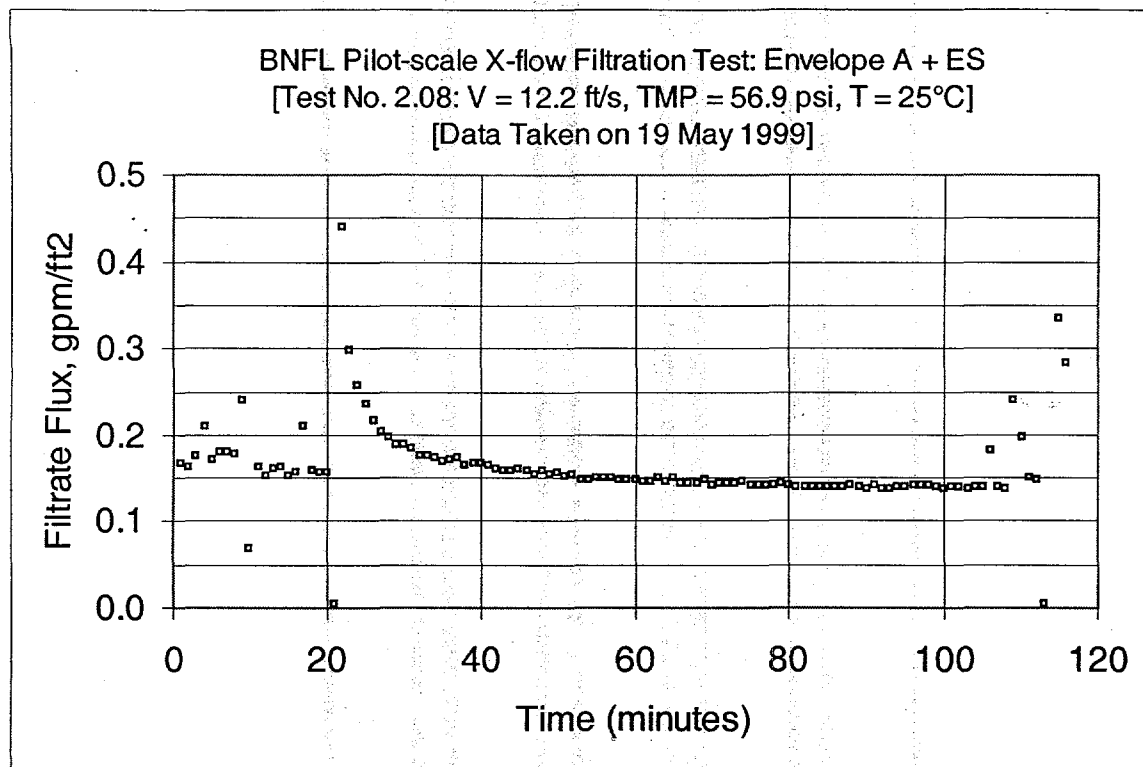


Figure B8: Test Run 2.08, 0.5 wt% Insoluble Solids Concentration

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.08

[illegible]

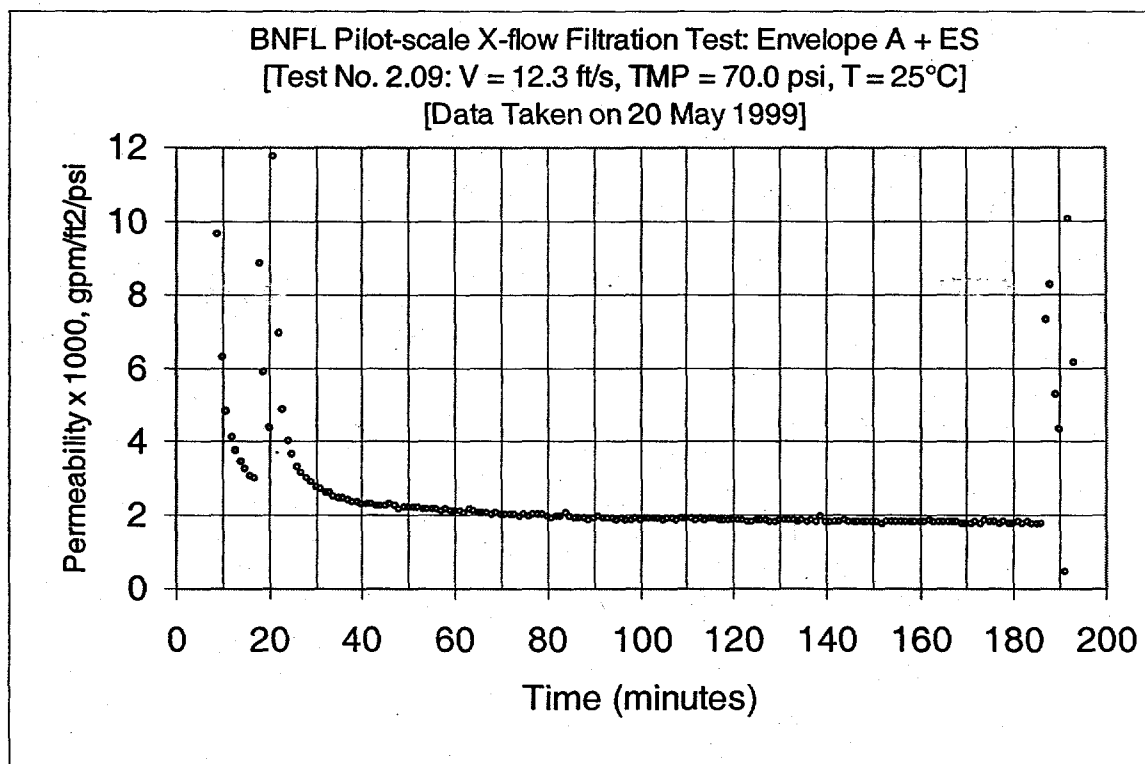
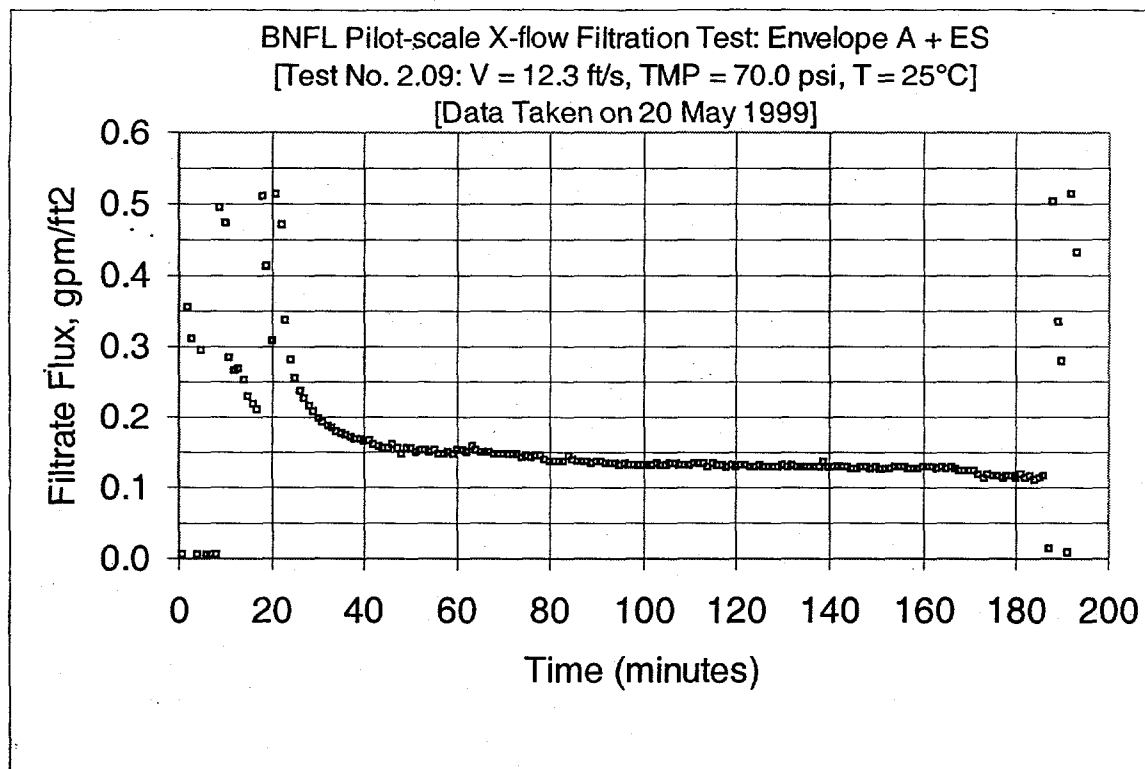


Figure B9: Test Run 2.09, 0.5 wt% Insoluble Solids Concentration

LINE	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	DATE	TIME	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q
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Pilot Scale X-Flow Filtration Test: Env. A, Run 2.09

[illegible]

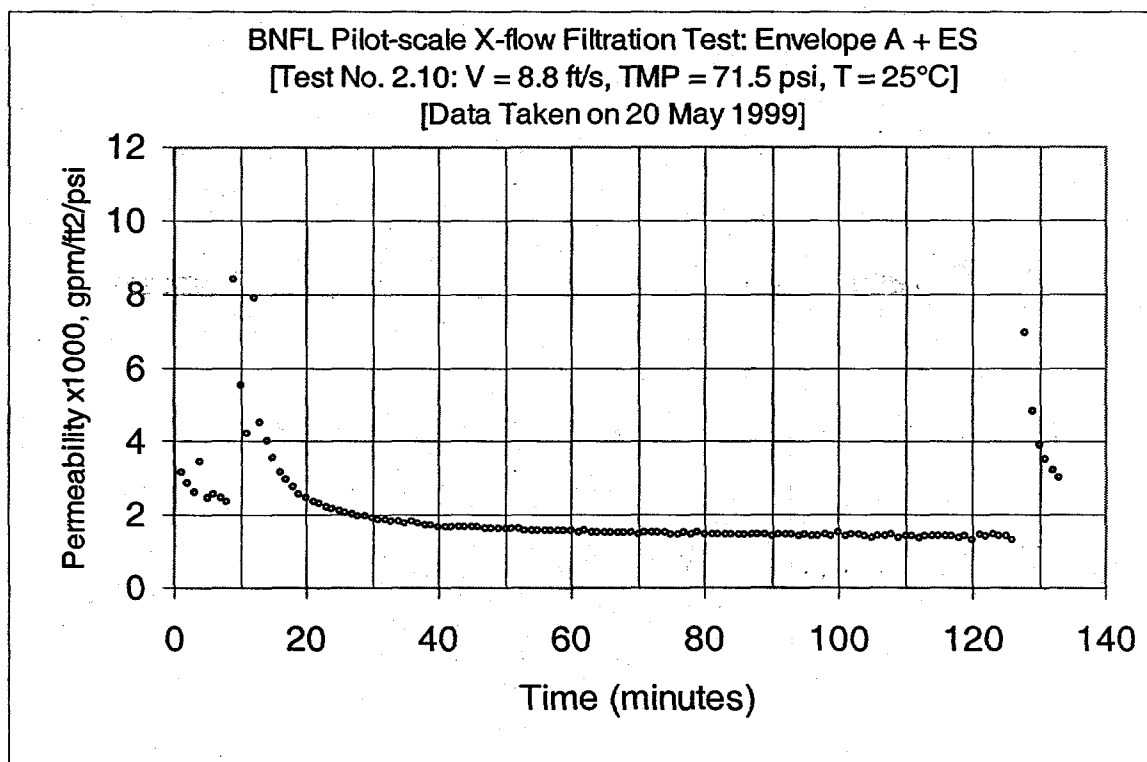
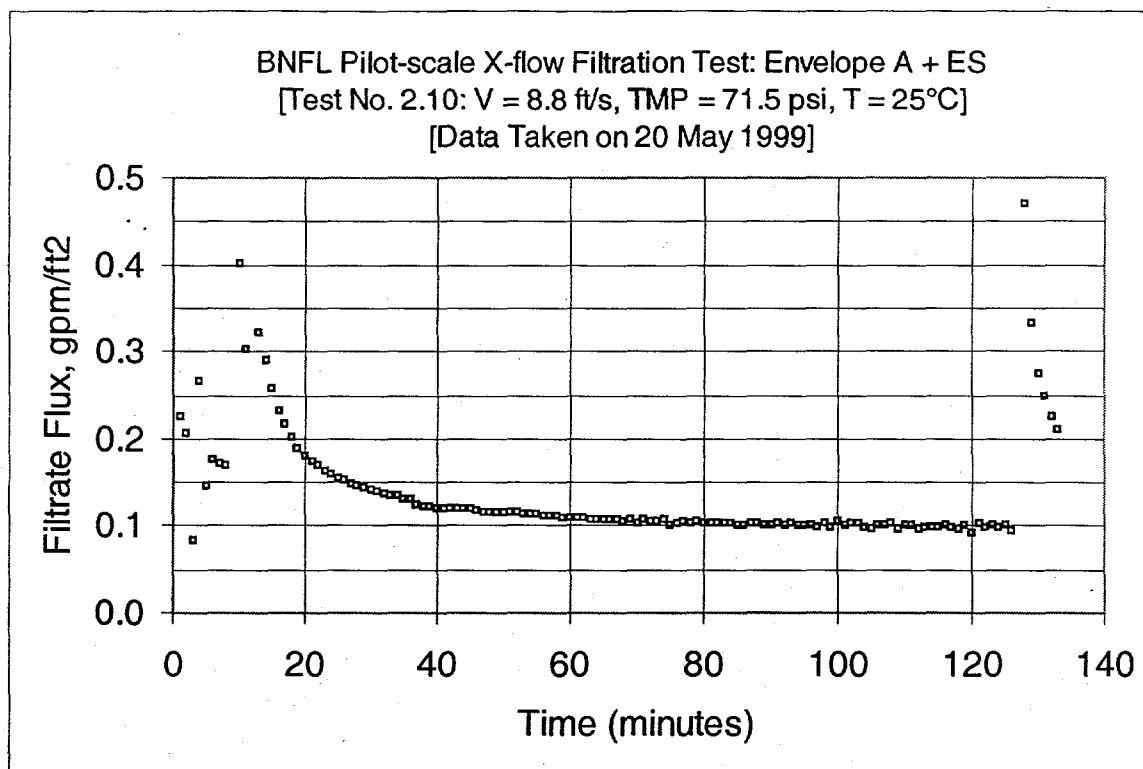


Figure B10: Test Run 2.10, 0.5 wt% Insoluble Solids Concentration

[illegible]

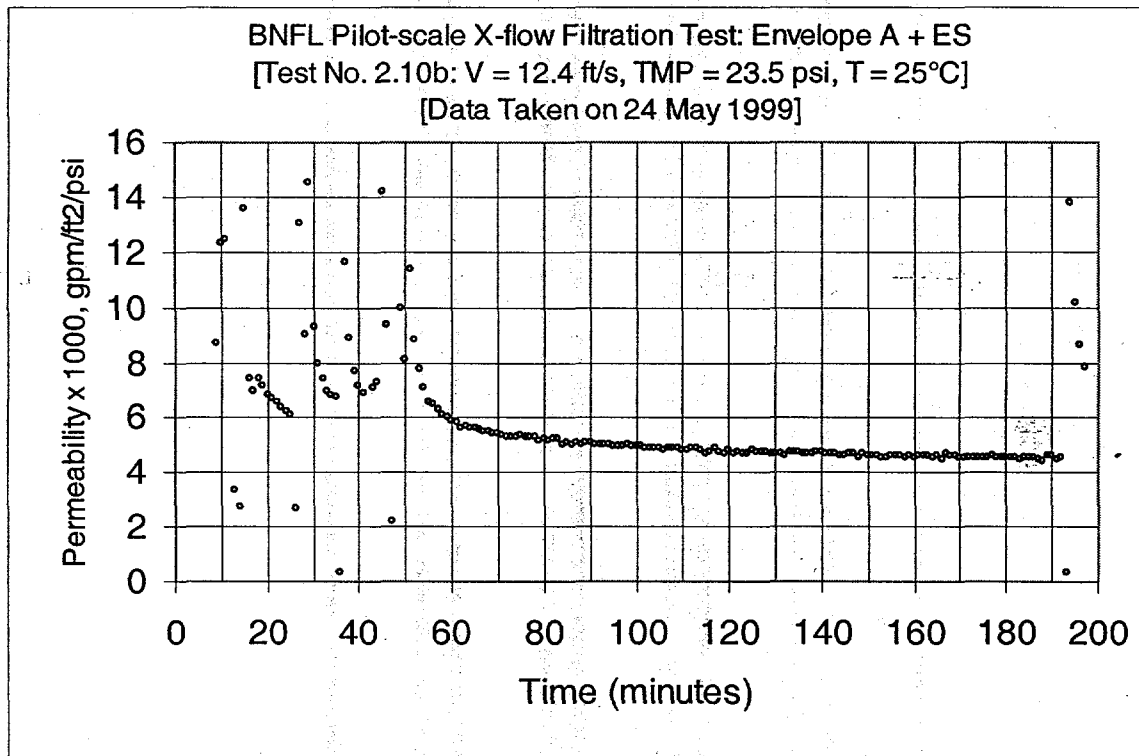
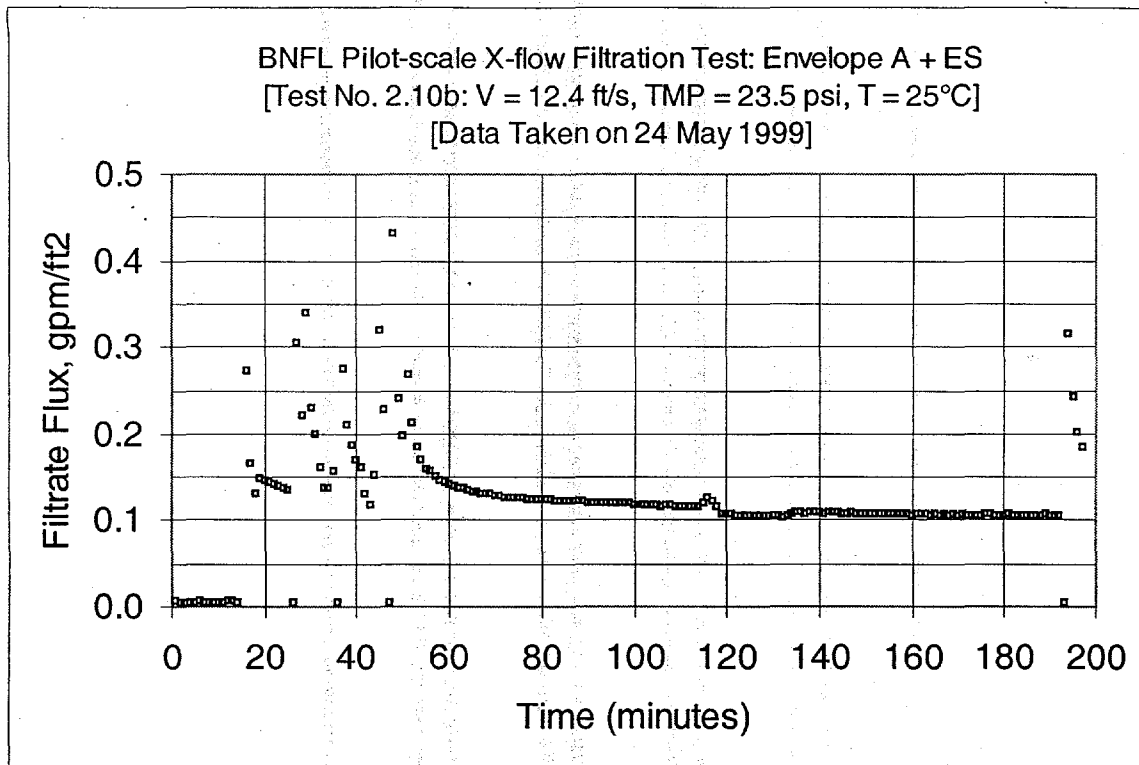


Figure B11: Test Run 2.10b, 0.5 wt% Insoluble Solids Concentration

[illegible]

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.10b

A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
163	15/24/1999 11:36:41 AM	0	25.359	22.863	24.933	25.411	25.374	31.151	26.221	33.153	6.307	20.355	6.599	-0.181	30.146	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0045	4.59	3.9
164	15/24/1999 11:37:40 AM	0	25.435	23.014	24.949	25.486	25.292	32.172	25.756	33.192	6.271	20.301	6.559	-0.181	30.041	0.243	0	157	12.5	23.0	1.6	0.106	0.106	0.0046	4.61	3.9
165	15/24/1999 11:38:41 AM	0	25.393	22.869	24.903	25.381	25.006	32.845	26.252	33.119	6.423	20.437	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.58	3.9
166	15/24/1999 11:39:42 AM	0	25.355	23.014	24.949	25.338	25.051	32.845	26.252	33.253	6.295	20.369	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.61	3.9
167	15/24/1999 11:40:41 AM	0	25.353	23.014	24.949	25.338	25.051	32.845	26.252	33.253	6.295	20.369	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.61	3.9
168	15/24/1999 11:41:40 AM	0	25.435	23.014	24.949	25.338	25.051	32.845	26.252	33.253	6.295	20.369	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.59	3.9
169	15/24/1999 11:42:41 AM	0	25.435	23.014	24.949	25.338	25.051	32.845	26.252	33.253	6.295	20.369	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.59	3.9
170	15/24/1999 11:43:40 AM	0	25.435	23.014	24.949	25.338	25.051	32.845	26.252	33.253	6.295	20.369	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.59	3.9
171	15/24/1999 11:44:41 AM	0	25.435	23.014	24.949	25.338	25.051	32.845	26.252	33.253	6.295	20.369	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.59	3.9
172	15/24/1999 11:45:42 AM	0	25.435	23.014	24.949	25.338	25.051	32.845	26.252	33.253	6.295	20.369	6.568	-0.181	30.023	0.244	0	158	12.5	23.3	1.6	0.107	0.107	0.0046	4.59	3.9
173	15/24/1999 11:46:41 AM	0	25.424	23.004	24.938	24.965	22.073	33.182	26.038	33.023	6.303	20.372	6.568	-0.181	30.041	0.243	0	166	12.5	23.3	1.6	0.106	0.106	0.0045	4.59	3.9
174	15/24/1999 11:47:42 AM	0	25.424	23.004	24.938	24.965	22.073	33.182	26.038	33.023	6.303	20.372	6.568	-0.181	30.041	0.243	0	166	12.5	23.3	1.6	0.106	0.106	0.0045	4.59	3.9
175	15/24/1999 11:48:45 AM	0	25.424	23.004	24.938	24.965	22.073	33.182	26.038	33.023	6.303	20.372	6.568	-0.181	30.041	0.243	0	166	12.5	23.3	1.6	0.106	0.106	0.0045	4.59	3.9
176	15/24/1999 11:49:41 AM	0	25.459	23.053	24.983	24.904	22.226	32.875	25.449	33.009	6.06	20.538	6.568	-0.181	30.041	0.243	0	169	12.5	23.3	1.6	0.106	0.106	0.0046	4.61	3.9
177	15/24/1999 11:50:41 AM	0	25.414	22.985	24.848	24.904	22.226	32.875	25.449	33.009	6.06	20.538	6.568	-0.181	30.041	0.243	0	169	12.5	23.3	1.6	0.106	0.106	0.0046	4.61	3.9
178	15/24/1999 11:51:40 AM	0	25.414	22.985	24.848	24.904	22.226	32.875	25.449	33.009	6.06	20.538	6.568	-0.181	30.041	0.243	0	169	12.5	23.3	1.6	0.106	0.106	0.0046	4.61	3.9
179	15/24/1999 11:52:41 AM	0	25.414	22.985	24.848	24.904	22.226	32.875	25.449	33.009	6.06	20.538	6.568	-0.181	30.041	0.243	0	169	12.5	23.3	1.6	0.106	0.106	0.0046	4.61	3.9
180	15/24/1999 11:53:40 AM	0	25.448	23.048	24.902	24.882	22.226	32.875	25.449	33.009	6.06	20.538	6.568	-0.181	30.041	0.243	0	169	12.5	23.3	1.6	0.106	0.106	0.0046	4.61	3.9
181	15/24/1999 11:54:41 AM	0	25.448	23.048	24.902	24.882	22.226	32.875	25.449	33.009	6.06	20.538	6.568	-0.181	30.041	0.243	0	169	12.5	23.3	1.6	0.106	0.106	0.0046	4.61	3.9
182	15/24/1999 11:55:42 AM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
183	15/24/1999 11:56:35 AM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
184	15/24/1999 11:57:40 AM	0	25.448	23.053	24.917	24.882	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
185	15/24/1999 11:58:41 AM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
186	15/24/1999 11:59:40 AM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
187	15/24/1999 12:00:41 PM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
188	15/24/1999 12:01:40 PM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
189	15/24/1999 12:02:41 PM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
190	15/24/1999 12:03:38 PM	0	25.403	22.943	24.817	24.813	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
191	15/24/1999 12:04:41 PM	0	25.448	23.053	24.917	24.882	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
192	15/24/1999 12:05:40 PM	0	25.448	23.053	24.917	24.882	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
193	15/24/1999 12:06:41 PM	0	25.448	23.053	24.917	24.882	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
194	15/24/1999 12:07:40 PM	0	25.448	23.053	24.917	24.882	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
195	15/24/1999 12:08:42 PM	0	25.448	23.053	24.917	24.882	22.457	32.379	25.386	33.143	6.243	20.437	6.538	-0.181	30.023	0.242	0	175	12.5	23.3	1.6	0.105	0.105	0.0045	4.53	3.9
196	15/24/1999 12:09:41 PM	0	25.414	23.074	24.928	25.705	24.074	30.644	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	188	12.5	23.7	1.6	0.105	0.105	0.0044	4.53	3.8
197	15/24/1999 12:10:42 PM	0	25.424	23.074	24.928	25.705	24.074	30.644	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	188	12.5	23.7	1.6	0.105	0.105	0.0044	4.53	3.8
198	15/24/1999 12:11:41 PM	0	25.424	23.074	24.928	25.705	24.074	30.644	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	188	12.5	23.7	1.6	0.105	0.105	0.0044	4.53	3.8
199	15/24/1999 12:12:44 PM	0	25.424	23.074	24.928	25.705	24.074	30.644	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	188	12.5	23.7	1.6	0.105	0.105	0.0044	4.53	3.8
200	15/24/1999 12:13:45 PM	1	25.489	23.13	24.903	25.811	23.699	31.652	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	191	12.5	23.5	1.6	0.106	0.106	0.0045	4.50	3.8
201	15/24/1999 12:14:46 PM	0	25.489	23.13	24.903	25.811	23.699	31.652	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	191	12.5	23.5	1.6	0.106	0.106	0.0045	4.50	3.8
202	15/24/1999 12:15:45 PM	0	25.489	23.13	24.903	25.811	23.699	31.652	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	191	12.5	23.5	1.6	0.106	0.106	0.0045	4.50	3.8
203	15/24/1999 12:16:42 PM	0	25.489	23.13	24.903	25.811	23.699	31.652	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	191	12.5	23.5	1.6	0.106	0.106	0.0045	4.50	3.8
204	15/24/1999 12:17:37 PM	0	25.48	23.14	24.904	25.802	23.699	31.651	26.644	33.643	6.439	20.673	6.538	-0.181	30.086	0.241	0	191	12.5	23.5	1.6	0.106	0.106	0.0045	4.50	3.8
205	Averages		25.4	22.8	24.9	24.9	22.9	31.7	26.4	33.5	6.3	20.7	6.5	-0.2	29.9	0.278	0.0		12.4							

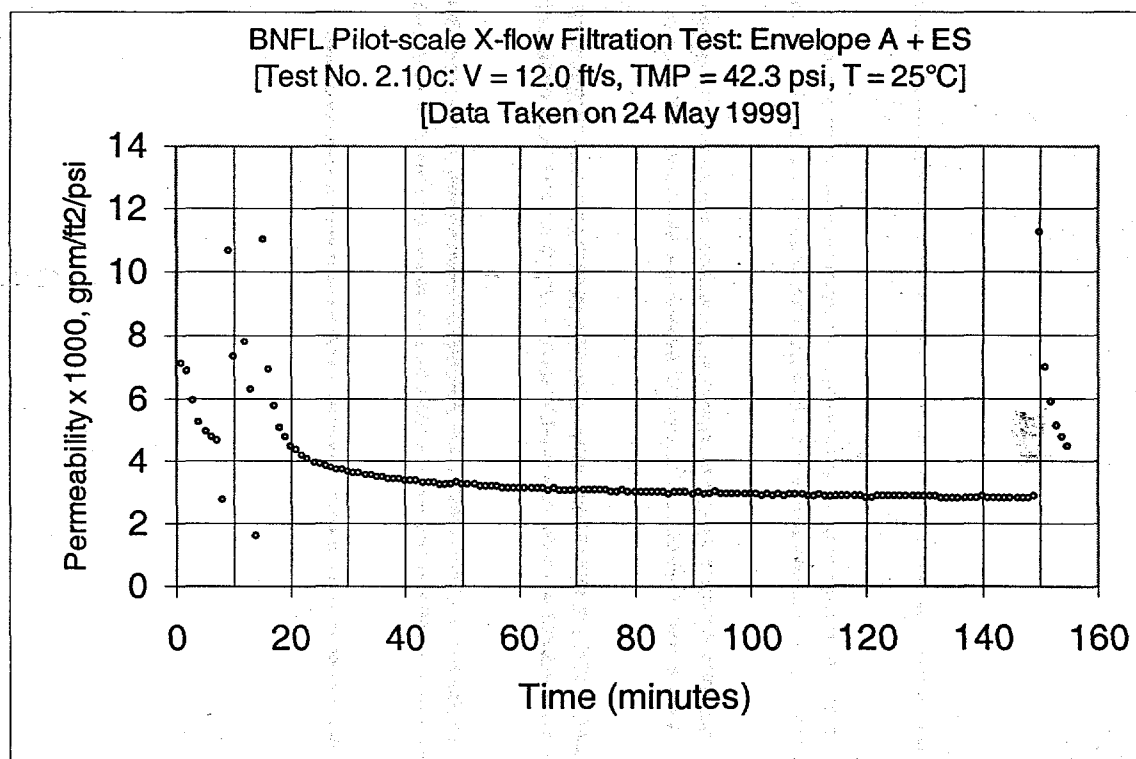
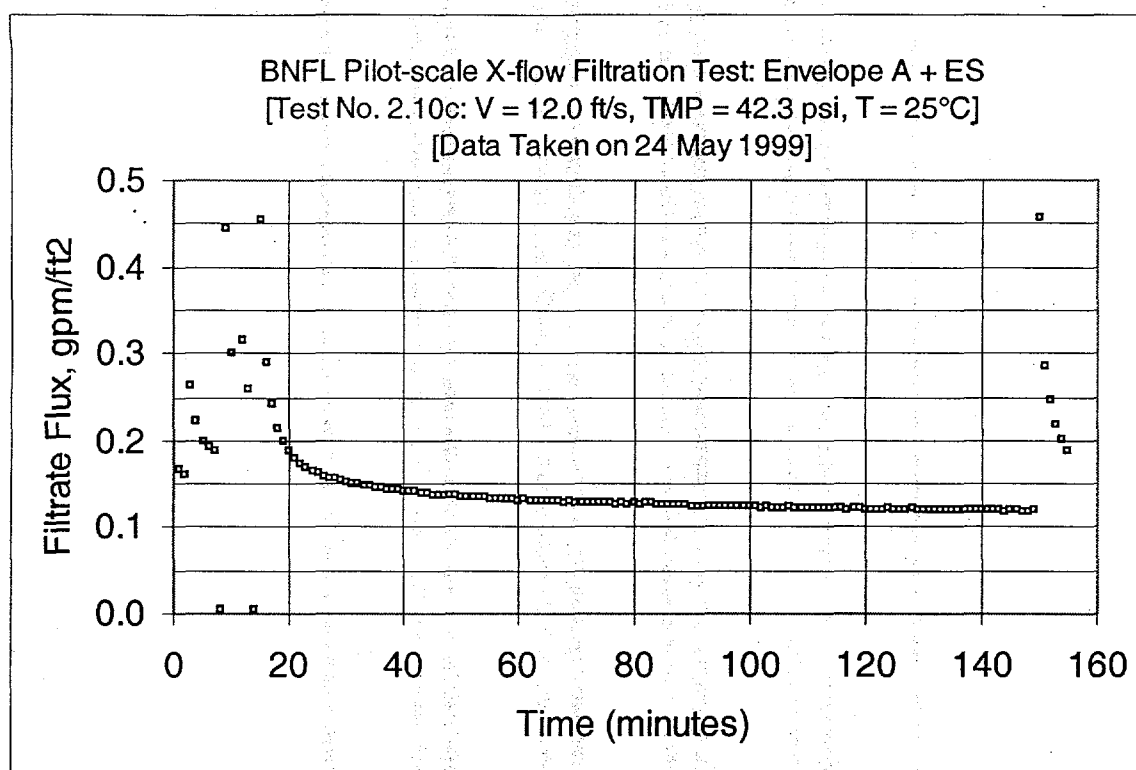


Figure B12: Test Run 2.10c, 0.5 wt% Insoluble Solids Concentration

[illegible]

[illegible]

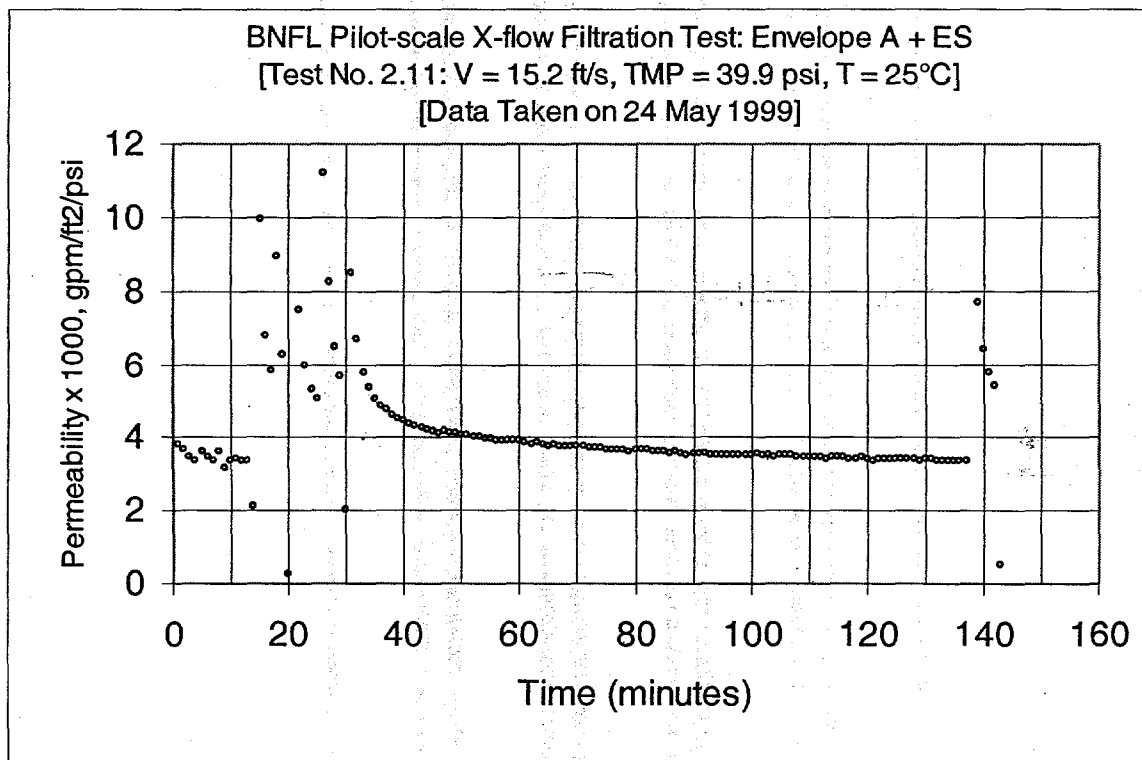
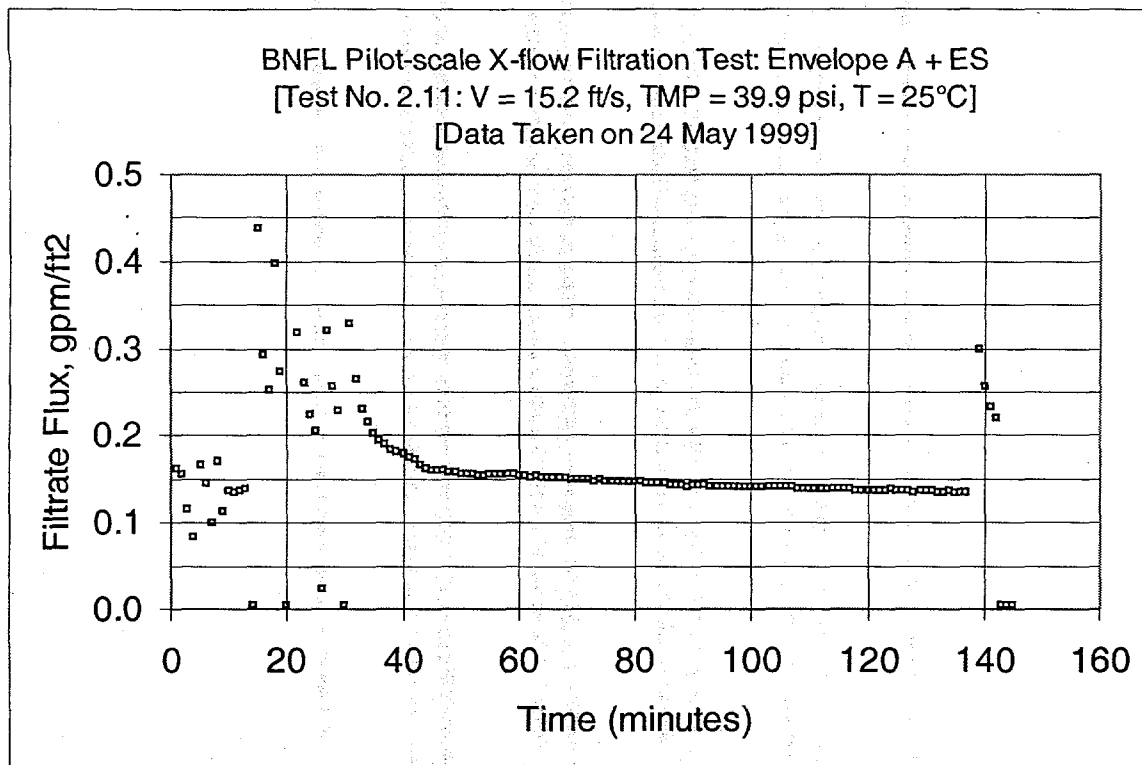


Figure B13: Test Run 2.11, 0.5 wt% Insoluble Solids Concentration

[illegible]

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
1	52041999	4.1335 PM	0	25.054	23.797	25.568	26.185	23.11	32.182	33.888	50.807	6.537	36.058	8.414	-0.135	39.461	0.343	0.008	75	15.1	40.1	2.8	0.150	0.147	0.037	3.69	3.69
2	52041999	4.1404 PM	0	25.974	23.797	25.568	26.185	23.03	31.983	34.606	51.76	8.844	35.65	8.414	-0.135	39.323	0.344	0	76	15.1	40.1	2.8	0.150	0.148	0.037	3.69	3.69
3	52041999	4.1435 PM	0	25.974	23.797	25.568	26.185	23.03	32.072	34.617	51.76	8.844	35.65	8.414	-0.135	39.353	0.344	0	77	15.1	40.1	2.8	0.150	0.148	0.037	3.69	3.69
4	52041999	4.1464 PM	0	25.974	23.797	25.568	26.185	23.03	31.983	34.622	51.76	8.844	35.65	8.414	-0.135	39.382	0.342	0	78	15.0	40.1	2.8	0.149	0.147	0.036	3.67	3.67
5	52041999	4.1493 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.632	51.76	8.844	35.65	8.414	-0.135	39.418	0.341	0	79	15.0	40.1	2.8	0.149	0.147	0.036	3.67	3.67
6	52041999	4.1523 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.644	51.76	8.844	35.65	8.414	-0.135	39.452	0.341	0	80	15.1	40.1	2.8	0.148	0.147	0.036	3.65	3.65
7	52041999	4.1553 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.654	51.76	8.844	35.65	8.414	-0.135	39.486	0.341	0	81	15.0	40.1	2.8	0.148	0.147	0.036	3.65	3.65
8	52041999	4.1583 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.664	51.76	8.844	35.65	8.414	-0.135	39.520	0.341	0	82	15.0	40.1	2.8	0.148	0.147	0.036	3.64	3.64
9	52041999	4.1613 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.674	51.76	8.844	35.65	8.414	-0.135	39.554	0.341	0	83	15.0	40.1	2.8	0.148	0.147	0.036	3.64	3.64
10	52041999	4.1643 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.684	51.76	8.844	35.65	8.414	-0.135	39.588	0.341	0	84	15.0	40.1	2.8	0.148	0.147	0.036	3.64	3.64
11	52041999	4.1673 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.694	51.76	8.844	35.65	8.414	-0.135	39.622	0.341	0	85	15.0	40.1	2.8	0.148	0.147	0.036	3.64	3.64
12	52041999	4.1703 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.704	51.76	8.844	35.65	8.414	-0.135	39.656	0.341	0	86	15.1	40.1	2.8	0.147	0.146	0.036	3.61	3.61
13	52041999	4.1733 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.714	51.76	8.844	35.65	8.414	-0.135	39.690	0.341	0	87	15.1	40.1	2.8	0.147	0.146	0.036	3.61	3.61
14	52041999	4.1763 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.724	51.76	8.844	35.65	8.414	-0.135	39.724	0.341	0	88	15.1	40.1	2.8	0.147	0.146	0.036	3.61	3.61
15	52041999	4.1793 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.734	51.76	8.844	35.65	8.414	-0.135	39.758	0.341	0	89	15.1	40.1	2.8	0.147	0.146	0.036	3.61	3.61
16	52041999	4.1823 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.744	51.76	8.844	35.65	8.414	-0.135	39.792	0.341	0	90	15.1	40.1	2.8	0.147	0.146	0.036	3.61	3.61
17	52041999	4.1853 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.754	51.76	8.844	35.65	8.414	-0.135	39.826	0.341	0	91	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
18	52041999	4.1883 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.764	51.76	8.844	35.65	8.414	-0.135	39.860	0.341	0	92	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
19	52041999	4.1913 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.774	51.76	8.844	35.65	8.414	-0.135	39.894	0.341	0	93	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
20	52041999	4.1943 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.784	51.76	8.844	35.65	8.414	-0.135	39.928	0.341	0	94	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
21	52041999	4.1973 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.794	51.76	8.844	35.65	8.414	-0.135	39.962	0.341	0	95	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
22	52041999	4.2003 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.804	51.76	8.844	35.65	8.414	-0.135	39.996	0.341	0	96	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
23	52041999	4.2033 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.814	51.76	8.844	35.65	8.414	-0.135	40.030	0.341	0	97	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
24	52041999	4.2063 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.824	51.76	8.844	35.65	8.414	-0.135	40.064	0.341	0	98	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
25	52041999	4.2093 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.834	51.76	8.844	35.65	8.414	-0.135	40.098	0.341	0	99	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
26	52041999	4.2123 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.844	51.76	8.844	35.65	8.414	-0.135	40.132	0.341	0	100	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
27	52041999	4.2153 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.854	51.76	8.844	35.65	8.414	-0.135	40.166	0.341	0	101	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
28	52041999	4.2183 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.864	51.76	8.844	35.65	8.414	-0.135	40.200	0.341	0	102	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
29	52041999	4.2213 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.874	51.76	8.844	35.65	8.414	-0.135	40.234	0.341	0	103	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
30	52041999	4.2243 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.884	51.76	8.844	35.65	8.414	-0.135	40.268	0.341	0	104	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
31	52041999	4.2273 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.894	51.76	8.844	35.65	8.414	-0.135	40.302	0.341	0	105	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
32	52041999	4.2303 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.904	51.76	8.844	35.65	8.414	-0.135	40.336	0.341	0	106	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
33	52041999	4.2333 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.914	51.76	8.844	35.65	8.414	-0.135	40.370	0.341	0	107	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
34	52041999	4.2363 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.924	51.76	8.844	35.65	8.414	-0.135	40.404	0.341	0	108	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
35	52041999	4.2393 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.934	51.76	8.844	35.65	8.414	-0.135	40.438	0.341	0	109	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
36	52041999	4.2423 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.944	51.76	8.844	35.65	8.414	-0.135	40.472	0.341	0	110	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
37	52041999	4.2453 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.954	51.76	8.844	35.65	8.414	-0.135	40.506	0.341	0	111	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
38	52041999	4.2483 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.964	51.76	8.844	35.65	8.414	-0.135	40.540	0.341	0	112	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
39	52041999	4.2513 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.974	51.76	8.844	35.65	8.414	-0.135	40.574	0.341	0	113	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
40	52041999	4.2543 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	34.984	51.76	8.844	35.65	8.414	-0.135	40.608	0.341	0	114	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
41	52041999	4.2573 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	34.994	51.76	8.844	35.65	8.414	-0.135	40.642	0.341	0	115	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
42	52041999	4.2603 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	35.004	51.76	8.844	35.65	8.414	-0.135	40.676	0.341	0	116	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
43	52041999	4.2633 PM	0	25.974	23.797	25.568	26.185	23.11	32.072	35.014	51.76	8.844	35.65	8.414	-0.135	40.710	0.341	0	117	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
44	52041999	4.2663 PM	0	25.974	23.797	25.568	26.185	23.03	31.914	35.024	51.76	8.844	35.65	8.414	-0.135	40.744	0.341	0	118	15.2	40.1	2.8	0.146	0.145	0.036	3.58	3.58
45	52041999	4.2693 PM	0	25.974	23.797	25.568																					

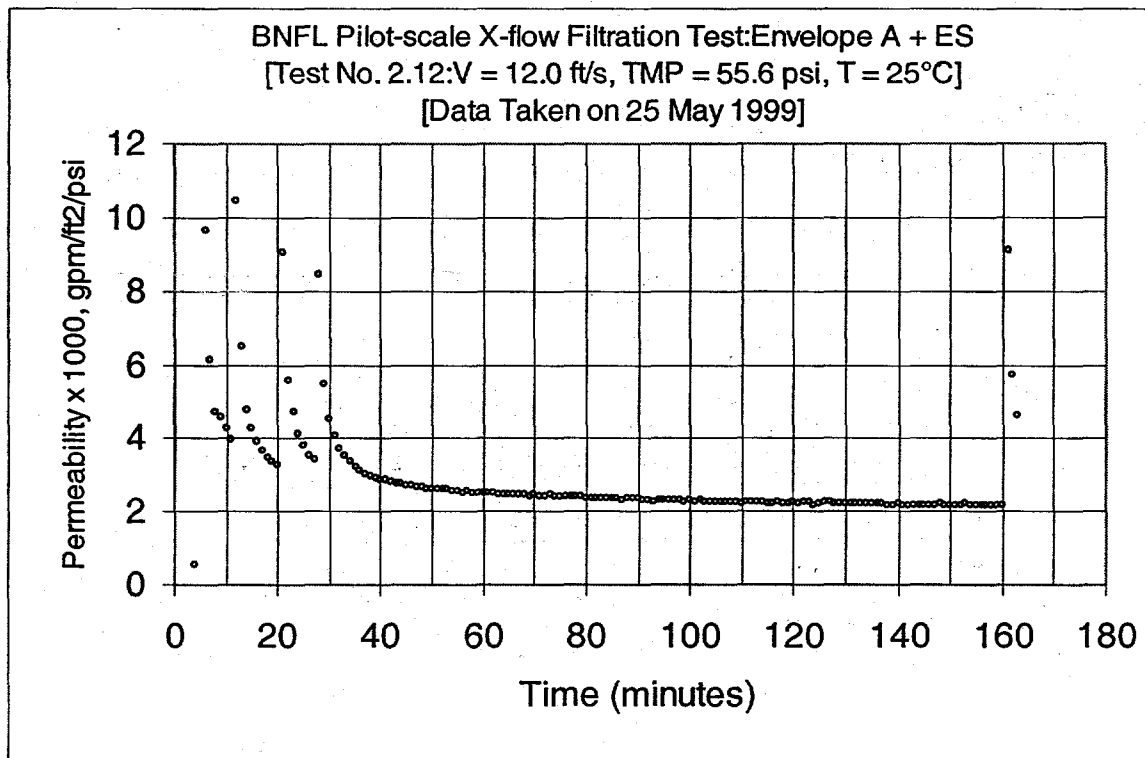
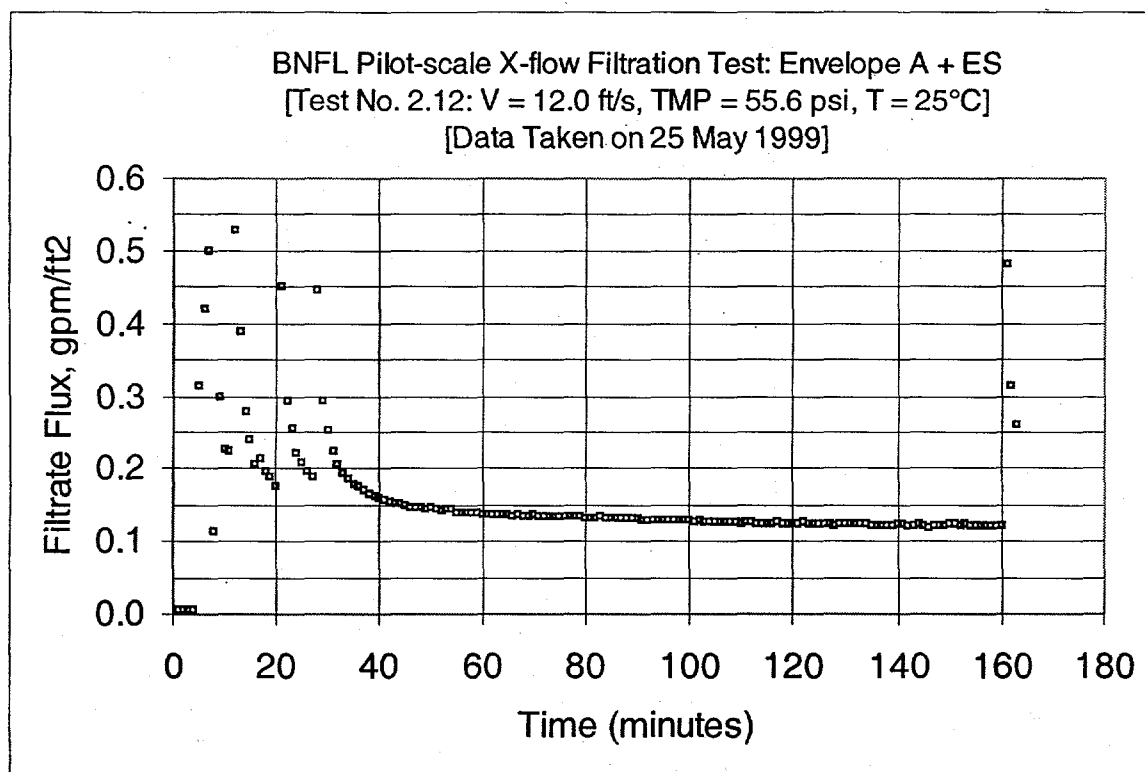


Figure B14: Test Run 2.12, 0.5 wt% Insoluble Solids Concentration

Pilot Scale X-Flow Filtration Test: Env. A; Run 2.12

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.12

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.12

[illegible]

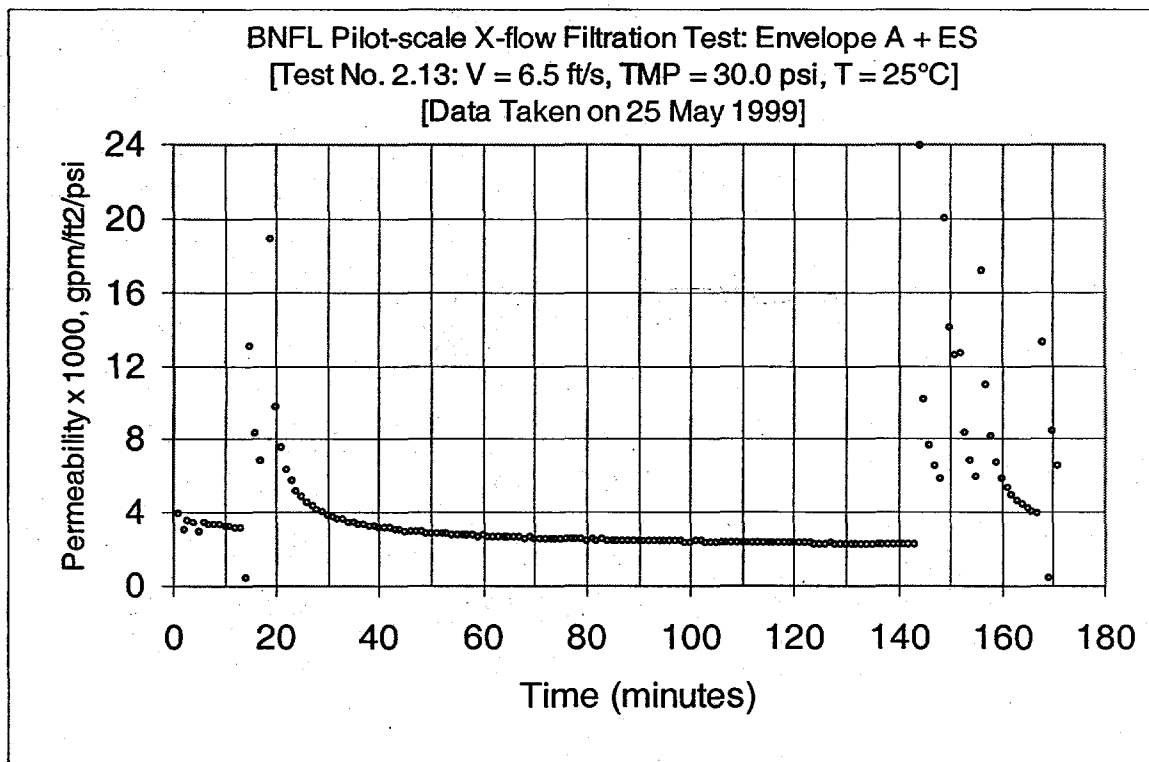
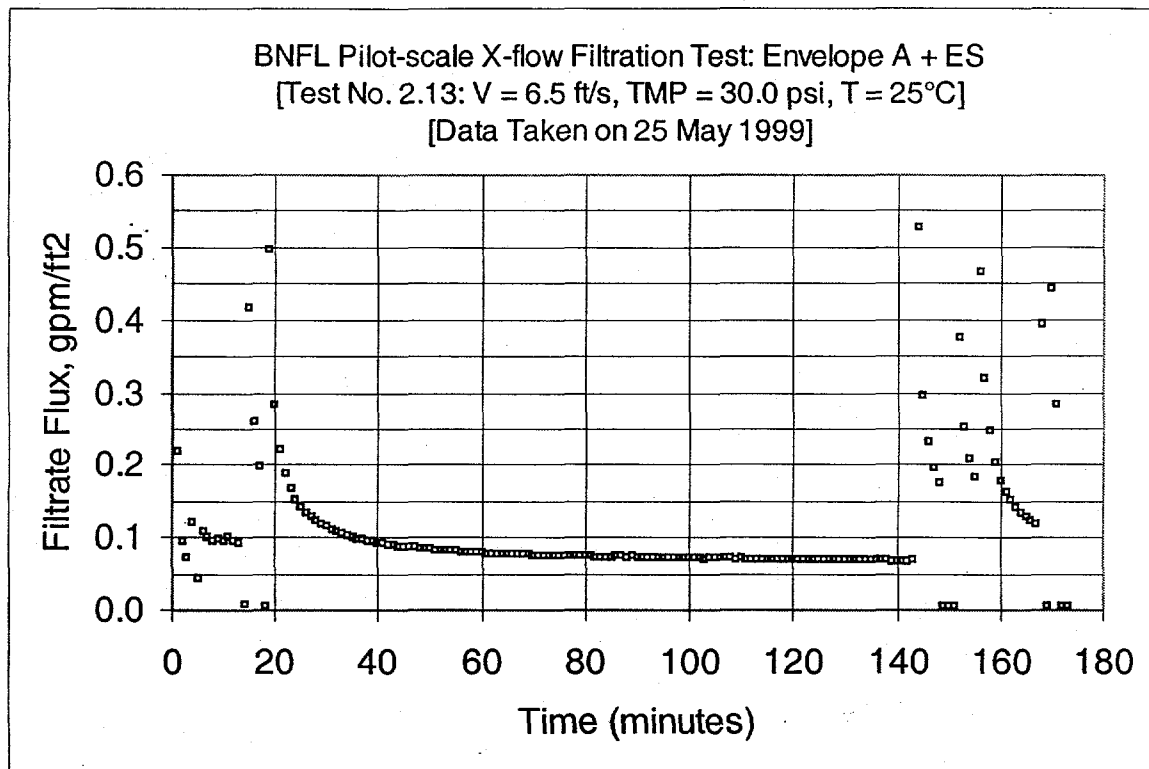


Figure B15: Test Run 2.13, 0.5 wt% Insoluble Solids Concentration

[illegible]

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
1	5251959	1143354	0	2323	2343	23835	23734	21632	32854	30737	37813	21817	28322	6445	0089	15839	0185	0	78	5	237	20	0072	004	0025	251	
2	5251960	1153734	0	24556	23916	2381	25409	21848	30701	21657	28364	21657	28364	6445	0089	15839	0185	0	77	5	236	21	0072	004	0025	248	
3	5251961	1163434	0	24556	23916	2381	25409	21848	30701	21657	28364	21657	28364	6445	0089	15839	0185	0	77	5	236	21	0072	004	0025	248	
4	5251962	1173534	0	24591	23933	24026	23824	21923	32446	30754	28669	28618	28618	6445	0089	15839	0185	0	79	5	236	20	0072	004	0025	249	
5	5251963	1183434	0	24672	23933	24026	23824	21923	32446	30754	28669	28618	28618	6445	0089	15839	0185	0	79	5	236	20	0072	004	0025	249	
6	5251964	1193434	0	24672	23933	24026	23824	21923	32446	30754	28669	28618	28618	6445	0089	15839	0185	0	79	5	236	20	0072	004	0025	249	
7	5251965	1203354	0	24707	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
8	5251966	1203354	0	24707	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
9	5251967	1213354	0	24707	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
10	5251968	1223434	0	24707	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
11	5251969	1233434	0	24707	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
12	5251970	1233434	0	24707	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
13	5251971	1243354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
14	5251972	1243354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
15	5251973	1253354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
16	5251974	1253354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
17	5251975	1263354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
18	5251976	1263354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
19	5251977	1273354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
20	5251978	1273354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
21	5251979	1283354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
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24	5251982	1293354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
25	5251983	1303354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
26	5251984	1303354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
27	5251985	1313354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
28	5251986	1313354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
29	5251987	1323354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
30	5251988	1323354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
31	5251989	1333354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
32	5251990	1333354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
33	5251991	1343354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
34	5251992	1343354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
35	5251993	1353354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
36	5251994	1353354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
37	5251995	1363354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
38	5251996	1363354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
39	5251997	1373354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
40	5251998	1373354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
41	5251999	1383354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
42	5252000	1383354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
43	5252001	1393354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
44	5252002	1393354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
45	5252003	1403354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
46	5252004	1403354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
47	5252005	1413354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
48	5252006	1413354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	
49	5252007	1423354	0	24832	23938	24105	25604	22506	31576	30737	27555	28632	28632	6445	0089	15839	0185	0	81	5	236	20	0072	003	0025	245	

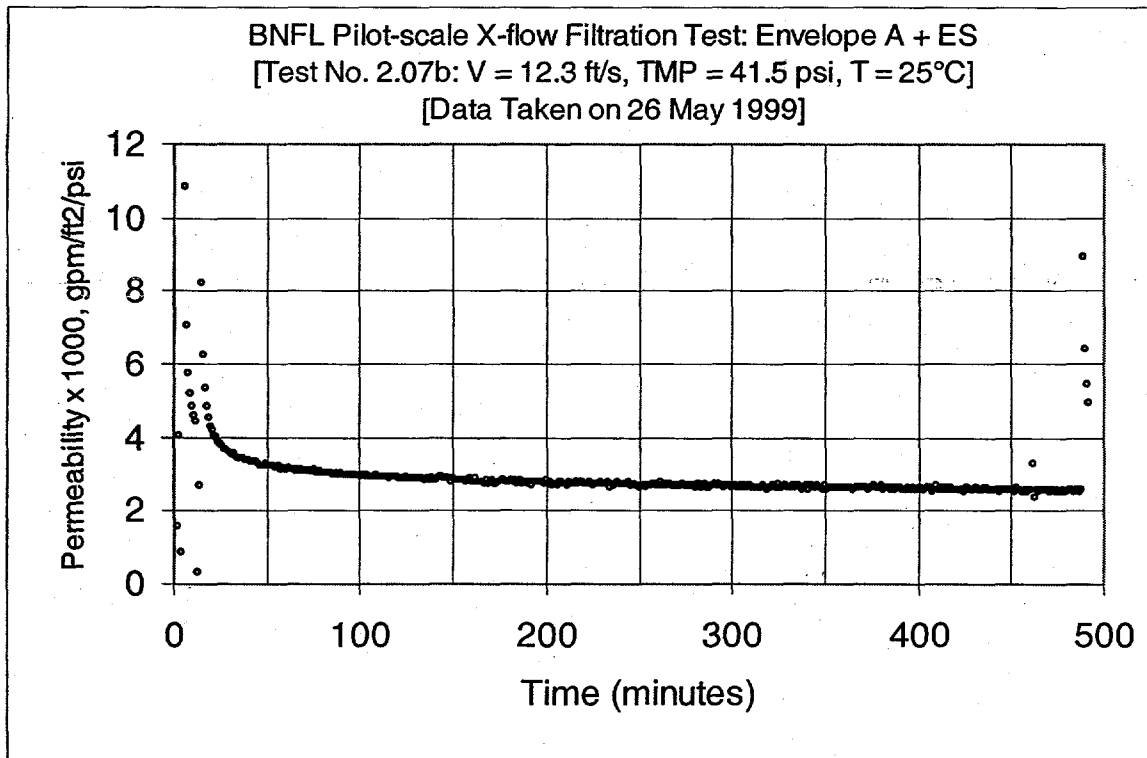
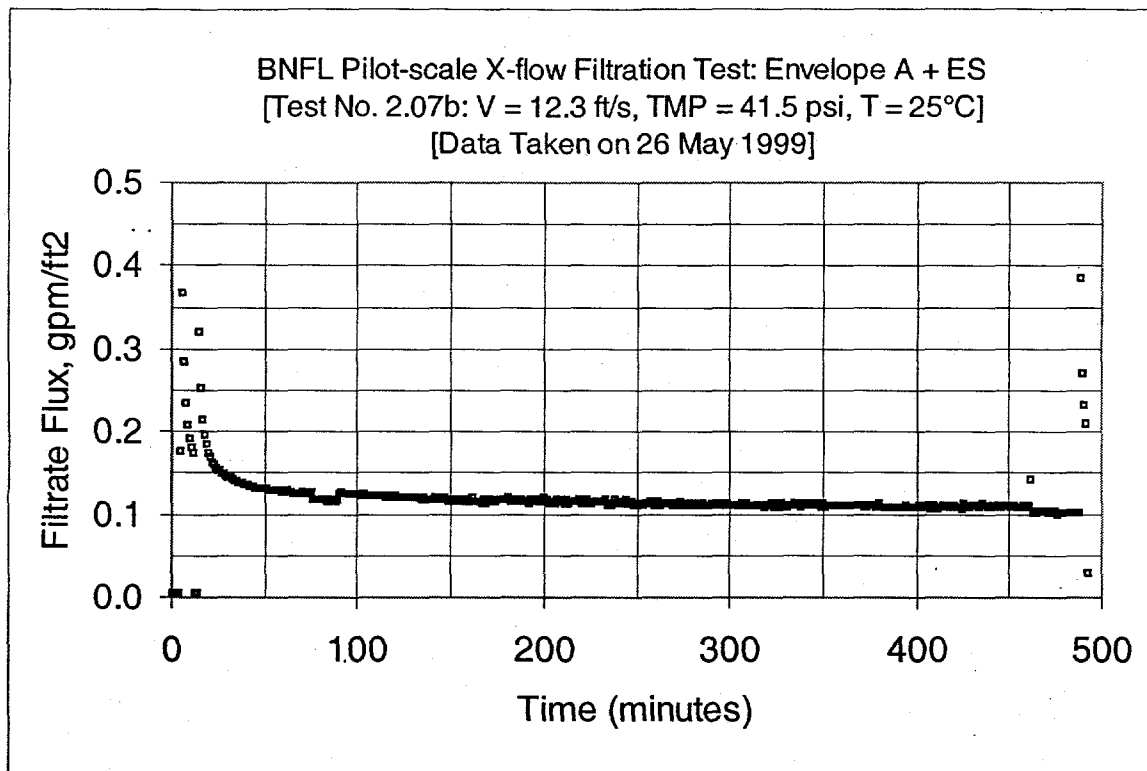


Figure B16: Test Run 2.07b, 0.5 wt% Insoluble Solids Concentration

[illegible]

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07b

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
163	5/26/1999	12:05:40 PM	0	27.503	23.164	27.257	25.796	22.066	32.286	44.229	52.431	6.471	38.558	7.216	-0.089	30.117	0.285	0	154	12.5	41.4	2.9	0.124	0.117	0.0028	2.82	2.4
164	5/26/1999	12:06:40 PM	0	27.583	23.084	27.257	25.796	22.066	32.162	44.539	52.675	6.483	38.625	7.216	-0.089	30.104	0.285	0	155	12.5	41.4	2.9	0.125	0.117	0.0028	2.82	2.4
165	5/26/1999	12:07:40 PM	0	27.583	23.084	27.257	25.796	22.066	32.162	44.539	52.675	6.483	38.625	7.216	-0.089	30.104	0.285	0	156	12.5	41.4	2.9	0.124	0.116	0.0028	2.81	2.4
166	5/26/1999	12:08:40 PM	0	27.628	23.164	27.337	25.796	22.066	32.003	44.010	51.578	6.335	38.558	7.216	-0.089	30.133	0.282	0	157	12.5	41.3	2.9	0.125	0.115	0.0028	2.79	2.4
167	5/26/1999	12:09:41 PM	0	27.708	23.164	27.337	25.796	22.066	32.003	43.702	51.578	6.303	38.558	7.185	-0.089	30.148	0.284	0	158	12.4	41.1	2.9	0.124	0.116	0.0028	2.82	2.4
168	5/26/1999	12:10:41 PM	0	27.683	23.164	27.337	25.796	22.066	32.162	44.105	51.882	6.439	38.558	7.218	-0.089	30.194	0.289	0.003	159	12.5	41.3	2.9	0.126	0.118	0.0029	2.86	2.4
169	5/26/1999	12:11:41 PM	0	27.743	23.164	27.417	25.841	22.066	31.843	44.942	52.889	6.439	38.625	7.218	-0.089	30.025	0.286	0.003	160	12.5	41.8	2.9	0.125	0.117	0.0028	2.79	2.4
170	5/26/1999	12:12:41 PM	0	27.743	23.164	27.417	25.841	22.066	32.003	44.136	51.821	6.407	38.684	7.185	-0.089	30.133	0.28	0	161	12.5	41.1	2.8	0.122	0.114	0.0028	2.78	2.4
171	5/26/1999	12:13:41 PM	0	27.823	23.164	27.417	25.841	22.066	32.241	43.95	51.791	6.359	38.321	7.218	-0.089	30.025	0.292	0.003	162	12.5	41.1	2.8	0.127	0.119	0.0029	2.90	2.5
172	5/26/1999	12:14:41 PM	0	27.743	23.164	27.497	26.001	23.041	32.162	44.229	52.278	6.399	38.625	7.218	-0.089	30.01	0.282	0	163	12.5	41.4	2.9	0.123	0.115	0.0028	2.77	2.4
173	5/26/1999	12:15:41 PM	0	27.823	23.164	27.497	25.841	23.008	32.083	44.353	52.126	6.483	38.49	7.216	-0.089	30.056	0.284	0	164	12.5	41.4	2.9	0.124	0.116	0.0028	2.79	2.4
174	5/26/1999	12:16:41 PM	0	27.823	23.164	27.497	25.841	23.041	32.083	43.981	51.882	6.375	38.423	7.246	-0.042	30.04	0.28	0.003	165	12.5	41.2	2.8	0.122	0.114	0.0028	2.77	2.4
175	5/26/1999	12:17:41 PM	0	27.902	23.164	27.497	25.796	23.041	31.989	43.919	51.852	6.359	38.389	7.218	-0.089	30.071	0.282	0	166	12.5	41.2	2.8	0.123	0.115	0.0028	2.79	2.4
176	5/26/1999	12:18:41 PM	0	27.902	23.164	27.577	25.958	23.041	32.241	44.683	52.309	6.343	38.321	7.218	-0.042	30.179	0.279	0	167	12.5	41.5	2.9	0.122	0.113	0.0027	2.73	2.3
177	5/26/1999	12:19:42 PM	0	27.902	23.245	27.577	25.796	23.041	32.241	44.322	52.401	6.383	38.321	7.215	-0.089	30.102	0.288	0	168	12.5	41.3	2.9	0.126	0.117	0.0028	2.83	2.4
178	5/26/1999	12:20:42 PM	0	27.902	23.21	27.537	25.921	23.096	31.944	44.322	52.401	6.511	38.625	7.154	-0.089	30.148	0.277	0	169	12.5	41.5	2.9	0.121	0.113	0.0027	2.73	2.3
179	5/26/1999	12:21:42 PM	0	27.823	23.164	27.178	25.878	23.041	32.048	44.136	52.035	6.423	38.592	7.092	-0.042	30.056	0.279	0.003	170	12.5	41.4	2.9	0.122	0.115	0.0028	2.77	2.4
180	5/26/1999	12:22:42 PM	0	27.743	23.245	26.963	25.958	23.121	32.207	44.229	52.098	6.319	38.882	7.123	-0.089	29.733	0.282	0	171	12.3	41.5	2.9	0.123	0.116	0.0028	2.80	2.4
181	5/26/1999	12:23:42 PM	0	27.683	23.164	26.778	25.958	23.121	31.924	44.725	52.584	6.239	39.302	7.092	-0.089	29.626	0.277	0	172	12.3	42.0	2.9	0.121	0.115	0.0027	2.74	2.3
182	5/26/1999	12:24:42 PM	0	27.503	23.164	26.684	26.081	23.201	32.003	44.415	52.309	6.283	39.268	7.092	-0.042	29.61	0.273	0	173	12.3	41.8	2.9	0.119	0.114	0.0027	2.72	2.3
183	5/26/1999	12:25:42 PM	0	27.489	23.21	26.504	26.001	23.247	32.207	44.818	52.708	6.311	39.301	7.061	-0.089	29.549	0.277	0	174	12.3	41.9	2.9	0.121	0.116	0.0028	2.77	2.4
184	5/26/1999	12:26:42 PM	0	27.309	23.29	26.344	26.081	23.247	31.989	44.508	52.157	6.16	39.335	7.031	-0.042	29.564	0.276	0	175	12.3	41.9	2.9	0.121	0.117	0.0028	2.79	2.4
185	5/26/1999	12:27:42 PM	0	27.229	23.21	26.219	26.081	23.247	32.003	44.787	52.828	6.391	39.268	6.969	-0.089	29.503	0.28	0	176	12.2	42.0	2.9	0.122	0.118	0.0028	2.81	2.4
186	5/26/1999	12:28:42 PM	0	27.149	23.21	26.024	26.081	23.168	31.89	44.942	52.553	6.303	39.268	6.969	-0.042	29.533	0.278	0	177	12.3	42.1	2.9	0.121	0.118	0.0028	2.80	2.4
187	5/26/1999	12:29:42 PM	0	26.944	23.29	25.844	26.001	23.247	32.003	44.725	52.401	6.303	39.301	6.938	-0.042	29.503	0.276	0	178	12.2	42.0	2.9	0.120	0.117	0.0028	2.79	2.4
188	5/26/1999	12:30:42 PM	0	26.83	23.21	25.784	26.081	23.247	32.048	45.159	52.736	6.287	39.471	6.877	-0.042	29.487	0.274	0.003	179	12.2	42.3	2.9	0.117	0.113	0.0028	2.77	2.4
189	5/26/1999	12:31:42 PM	0	26.87	23.29	25.704	26.181	23.247	32.066	45.035	52.523	6.279	39.403	6.877	-0.089	29.518	0.273	0	180	12.3	42.2	2.9	0.119	0.117	0.0028	2.77	2.4
190	5/26/1999	12:32:43 PM	0	26.59	23.29	25.624	26.081	23.247	32.128	45.221	52.889	6.319	39.471	6.877	-0.089	29.334	0.277	0	181	12.2	42.3	2.9	0.121	0.119	0.0028	2.81	2.4
191	5/26/1999	12:33:43 PM	0	26.51	23.29	25.508	26.081	23.327	32.048	44.632	52.065	6.407	39.166	6.784	-0.089	29.871	0.268	0	182	12.4	41.9	2.9	0.117	0.115	0.0028	2.75	2.3
192	5/26/1999	12:34:43 PM	0	26.27	23.29	25.384	26.048	23.168	32.093	44.384	51.899	6.311	38.828	6.753	-0.089	29.764	0.273	0	183	12.4	41.6	2.9	0.119	0.118	0.0028	2.83	2.4
193	5/26/1999	12:35:43 PM	0	26.27	23.336	25.269	26.001	23.168	31.931	44.508	51.913	6.387	39.031	6.753	-0.042	29.671	0.264	0	184	12.4	41.8	2.9	0.115	0.114	0.0027	2.74	2.3
194	5/26/1999	12:36:43 PM	0	26.155	23.255	25.189	26.048	23.212	31.731	44.88	52.098	6.375	38.964	6.722	-0.089	29.749	0.268	0	185	12.3	41.9	2.9	0.117	0.116	0.0028	2.78	2.4
195	5/26/1999	12:37:43 PM	0	26.075	23.336	25.109	26.048	23.247	32.093	44.415	51.78	6.399	39.099	6.722	-0.042	29.81	0.269	0	186	12.4	41.8	2.9	0.117	0.117	0.0028	2.80	2.4
196	5/26/1999	12:38:43 PM	0	25.915	23.255	25.029	26.126	23.292	32.41	45.531	52.858	6.375	39.065	6.692	-0.089	29.672	0.263	0	187	12.3	42.3	2.9	0.115	0.115	0.0027	2.71	2.3
197	5/26/1999	12:39:43 PM	0	25.833	23.301	24.869	26.048	23.212	32.014	45.273	52.728	6.335	39.065	6.692	-0.042	29.625	0.265	0	188	12.4	42.0	2.9	0.116	0.116	0.0028	2.76	2.4
198	5/26/1999	12:40:43 PM	0	25.755	23.253	24.789	26.001	23.212	31.835	45.273	52.34	6.447	39.335	6.661	-0.089	29.654	0.264	0	189	12.4	42.2	2.9	0.115	0.116	0.0027	2.75	2.3
199	5/26/1999	12:41:43 PM	0	25.675	23.336	24.709	26.126	23.212	31.835	44.983	52.065	6.407	39.065	6.661	-0.089	29.81	0.261	0	190	12.4	41.8	2.9	0.114	0.115	0.0027	2.74	2.3
200	5/26/1999	12:42:43 PM	0	25.515	23.381	24.708	26.208	23.292	32.764	44.725	51.943	6.415	38.93	6.63	-0.042	29.718	0.263	0.003	191	12.3	41.6	2.9	0.115	0.116	0.0028	2.77	2.4
201	5/26/1999	12:43:43 PM	0	25.48	23.336	24.754	26.172	23.257	32.138	44.911	51.852	6.335	39.504	6.63	-0.042	29.779	0.258	0	192	12.4	42.2	2.9	0.113	0.113	0.0027	2.69	2.3
202	5/26/1999	12:44:44 PM	0	25.4	23.301	24.754	26.252	23.132	32.217	45.262	52.492	6.447	39.302	6.63	-0.042	29.795	0.265	0	193	12.4	42.3	2.9	0.116	0.116	0.0028	2.78	2.3
203	5/26/1999	12:45:44 PM	0	25.4	23.381	24.548	26.092	23.177	31.98	45.159	52.34	6.439	39.099	6.63	-0.042	29.779	0.262	0	194	12.4	42.1	2.9	0.114	0.116	0.0027	2.75	2.3
204	5/26/1999	12:46:44 PM	0	25.32	23.381	24.674	26.092	23.257	32.217	44.725	51.821	6.311	39.065	6.568	-0.089	29.933	0.264	0	195	12.4	41.9	2.9	0.115	0.116	0.0028	2.78	2.4
205	5/26/1999	12:47:44 PM	0	25.24	23.301	24.513	26.137	23.303	32.455	44.818	51.974	6.479	39.997	6.568	-0.089	29.948	0.261										

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07b

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
244	5/26/1999	1:28:48 PM	0	24.356	23.574	23.95	26.784	23.737	32.611	44.601	51.621	6.375	38.862	6.507	-0.042	29.764	0.252	0.003	235	12.4	41.7	2.9	0.110	0.113	0.0027	2.72	2.3
245	5/26/1999	1:27:48 PM	0	24.356	23.574	24.03	26.809	23.737	32.294	44.973	52.187	6.391	38.896	6.476	-0.089	29.733	0.248	0	236	12.3	41.9	2.9	0.108	0.111	0.0027	2.65	2.3
246	5/26/1999	1:28:48 PM	0	24.436	23.54	24.03	26.809	23.817	32.057	44.849	52.035	6.511	39.065	6.507	-0.042	29.795	0.253	0.003	237	12.4	42.0	2.9	0.110	0.114	0.0027	2.71	2.3
247	5/26/1999	1:29:48 PM	0	24.436	23.82	24.11	26.729	23.817	32.974	44.973	52.248	6.458	39.099	6.507	-0.089	29.81	0.261	0	238	12.4	42.0	2.9	0.110	0.117	0.0028	2.78	2.4
248	5/26/1999	1:30:48 PM	0	24.516	23.64	24.191	26.889	23.817	32.77	44.766	51.913	6.463	38.93	6.507	-0.042	29.887	0.253	0	239	12.4	41.8	2.9	0.110	0.113	0.0027	2.70	2.3
249	5/26/1999	1:31:48 PM	0	24.516	23.54	24.191	26.729	23.496	33.324	44.88	51.943	6.311	39.268	6.536	-0.042	29.733	0.257	0	240	12.3	42.1	2.9	0.112	0.115	0.0027	2.73	2.3
250	5/26/1999	1:32:48 PM	0	24.442	23.65	24.236	26.889	23.857	33.087	44.322	51.908	6.399	38.794	6.507	-0.042	29.784	0.252	0	241	12.4	41.8	2.9	0.110	0.112	0.0027	2.70	2.3
251	5/26/1999	1:33:48 PM	0	24.596	23.665	24.271	26.809	23.416	33.166	44.57	51.913	6.439	39.031	6.536	-0.042	29.835	0.254	0	242	12.4	41.8	2.9	0.111	0.113	0.0027	2.71	2.3
252	5/26/1999	1:34:48 PM	0	24.677	23.82	24.271	26.809	23.416	33.403	44.663	52.065	6.447	39.166	6.536	-0.042	29.871	0.256	0.003	243	12.4	41.9	2.9	0.112	0.114	0.0027	2.72	2.3
253	5/26/1999	1:35:48 PM	0	24.757	23.82	24.351	26.729	23.014	33.641	44.973	51.913	6.439	38.828	6.536	-0.042	29.733	0.261	0	244	12.3	41.9	2.9	0.114	0.116	0.0028	2.77	2.4
254	5/26/1999	1:36:48 PM	0	24.757	23.82	24.431	26.729	23.014	33.754	44.942	51.882	6.463	38.967	6.536	-0.042	29.841	0.252	0.003	245	12.4	42.0	2.9	0.110	0.112	0.0027	2.66	2.3
255	5/26/1999	1:37:48 PM	0	24.791	23.82	24.386	26.884	22.808	33.72	44.663	51.488	6.199	38.997	6.566	-0.089	29.764	0.257	0	246	12.4	41.8	2.9	0.112	0.114	0.0027	2.73	2.3
256	5/26/1999	1:38:48 PM	0	24.872	23.655	24.466	26.764	22.808	33.912	44.88	52.126	6.487	39.166	6.536	-0.042	29.825	0.258	0	247	12.4	42.0	2.9	0.113	0.114	0.0027	2.72	2.3
257	5/26/1999	1:39:48 PM	0	24.872	23.609	24.5	26.718	22.521	33.875	44.291	51.639	6.423	38.794	6.536	-0.042	29.841	0.249	0	248	12.4	41.8	2.9	0.109	0.110	0.0027	2.65	2.3
258	5/26/1999	1:40:50 PM	0	24.908	23.609	24.5	26.718	22.521	33.788	44.911	52.187	6.399	38.828	6.536	-0.042	29.81	0.255	0	249	12.4	41.9	2.9	0.111	0.113	0.0027	2.70	2.3
259	5/26/1999	1:41:50 PM	0	24.966	23.644	24.581	26.718	22.475	33.709	45.004	52.248	6.343	38.794	6.566	-0.042	29.871	0.251	0	250	12.4	41.9	2.9	0.110	0.111	0.0026	2.65	2.3
260	5/26/1999	1:42:50 PM	0	24.941	23.644	24.535	26.753	22.475	33.664	45.004	51.943	6.303	39.2	6.536	-0.089	29.795	0.253	0	251	12.4	42.1	2.9	0.110	0.112	0.0027	2.66	2.3
261	5/26/1999	1:43:50 PM	0	24.975	23.679	24.618	26.788	22.514	33.935	44.88	51.882	6.358	39.031	6.566	-0.042	29.841	0.254	0	252	12.4	42.0	2.9	0.111	0.112	0.0027	2.69	2.3
262	5/26/1999	1:44:50 PM	0	25.056	23.698	24.65	26.788	22.349	33.696	44.446	51.835	6.423	38.997	6.566	-0.042	29.825	0.251	0.003	253	12.4	41.7	2.9	0.110	0.111	0.0027	2.65	2.3
263	5/26/1999	1:45:50 PM	0	25.01	23.633	24.604	26.662	22.303	33.691	44.777	51.913	6.431	39.064	6.566	-0.042	29.917	0.249	0	254	12.4	41.7	2.9	0.109	0.110	0.0026	2.63	2.2
264	5/26/1999	1:46:51 PM	0	25.08	23.713	24.639	26.457	22.459	33.213	44.88	52.248	6.327	39.031	6.566	-0.042	29.871	0.256	0.003	255	12.4	42.0	2.9	0.112	0.113	0.0027	2.69	2.3
265	5/26/1999	1:47:51 PM	0	25.125	23.669	24.719	26.697	22.469	33.054	44.57	51.578	6.391	38.828	6.566	-0.089	29.948	0.255	0	256	12.4	41.7	2.9	0.111	0.112	0.0027	2.69	2.3
266	5/26/1999	1:48:51 PM	0	25.125	23.668	24.719	26.697	22.58	32.738	45.159	52.37	6.447	39.133	6.566	-0.042	29.825	0.255	0	257	12.4	42.1	2.9	0.111	0.112	0.0027	2.66	2.3
267	5/26/1999	1:49:51 PM	0	25.16	23.622	24.754	26.652	22.695	32.693	45.126	52.126	6.471	39.727	6.566	-0.042	29.841	0.26	0	258	12.4	41.8	2.9	0.114	0.114	0.0027	2.73	2.3
268	5/26/1999	1:50:51 PM	0	25.24	23.622	24.834	26.652	22.821	32.651	44.601	52.187	6.503	38.794	6.566	-0.042	29.81	0.258	0.003	259	12.4	41.7	2.9	0.113	0.113	0.0027	2.71	2.3
269	5/26/1999	1:51:51 PM	0	25.24	23.657	24.834	26.732	22.89	32.727	44.446	51.547	6.423	38.828	6.566	-0.042	29.887	0.244	0	260	12.4	41.6	2.9	0.111	0.111	0.0027	2.68	2.3
270	5/26/1999	1:52:51 PM	0	25.194	23.657	24.869	26.811	22.81	32.931	44.446	51.689	6.369	38.862	6.566	-0.089	29.871	0.255	0	261	12.4	41.7	2.9	0.111	0.112	0.0027	2.68	2.3
271	5/26/1999	1:53:51 PM	0	25.275	23.657	24.869	26.786	22.971	32.41	44.415	51.882	6.487	39.781	6.566	-0.042	29.979	0.254	0	262	12.4	41.8	2.9	0.115	0.116	0.0028	2.78	2.4
272	5/26/1999	1:54:51 PM	0	25.226	23.737	24.949	26.666	22.89	32.49	44.849	52.096	6.468	39.166	6.566	-0.042	29.948	0.257	0	263	12.4	42.0	2.9	0.111	0.111	0.0027	2.65	2.3
273	5/26/1999	1:55:51 PM	0	25.275	23.737	24.969	26.666	23.132	32.252	44.973	52.187	6.431	38.863	6.599	-0.042	29.948	0.259	0	264	12.4	41.8	2.9	0.113	0.113	0.0027	2.71	2.3
274	5/26/1999	1:56:51 PM	0	25.355	23.657	24.949	26.656	23.051	32.41	45.159	52.431	6.35	39.133	6.599	-0.042	29.984	0.256	0	265	12.4	42.0	2.9	0.112	0.112	0.0027	2.67	2.3
275	5/26/1999	1:57:51 PM	0	25.355	23.737	25.029	26.846	23.132	32.093	44.291	51.456	6.351	39.456	6.63	-0.042	29.856	0.258	0	266	12.4	41.4	2.9	0.113	0.113	0.0027	2.72	2.3
276	5/26/1999	1:58:51 PM	0	25.435	23.737	25.029	26.721	23.092	32.014	44.229	51.395	6.255	38.727	6.63	-0.042	29.871	0.258	0	267	12.4	41.5	2.9	0.113	0.113	0.0027	2.71	2.3
277	5/26/1999	1:59:52 PM	0	25.435	23.612	25.029	26.846	23.247	32.014	44.725	52.126	6.487	39.794	6.63	-0.042	29.902	0.257	0	268	12.4	41.8	2.9	0.112	0.112	0.0027	2.68	2.3
278	5/26/1999	2:00:52 PM	0	25.389	23.737	25.064	26.721	23.212	32.048	44.105	51.364	6.318	39.2	6.63	-0.042	29.856	0.256	0	269	12.4	41.7	2.9	0.112	0.112	0.0027	2.68	2.3
279	5/26/1999	2:01:52 PM	0	25.389	23.692	24.964	26.721	23.453	32.014	44.446	51.78	6.511	38.625	6.63	-0.042	29.917	0.254	0	270	12.4	41.5	2.9	0.111	0.111	0.0027	2.67	2.3
280	5/26/1999	2:02:52 PM	0	25.515	23.657	25.109	26.786	23.373	31.969	44.446	51.852	6.416	38.794	6.63	-0.089	29.887	0.255	0	271	12.4	41.6	2.9	0.111	0.111	0.0027	2.67	2.3
281	5/26/1999	2:03:52 PM	0	25.47	23.692	25.109	26.786	23.373	32.014	44.322	51.639	6.391	38.93	6.63	-0.042	29.856	0.258	0	272	12.4	41.6	2.9	0.113	0.112	0.0027	2.70	2.3
282	5/26/1999	2:04:52 PM	0	25.515	23.737	25.109	26.666	23.292	32.014	44.663	51.869	6.311	38.997	6.63	-0.042	29.933	0.256	0.003	273	12.4	41.8	2.9	0.112	0.111	0.0027	2.66	2.3
283	5/26/1999	2:05:52 PM	0	25.516	23.657	25.109	26.666	23.292	31.776	44.57	51.73	6.438	38.997	6.63	-0.042	29.856	0.262	0	274	12.4	41.6	2.9	0.114	0.114	0.0027	2.73	2.3
284	5/26/1999	2:06:52 PM	0	25.515	23.783	25.109	26.666	23.292	32.172	44.57	52.096	6.431	38.862	6.599	-0.042	29.948	0.256	0	275	12.4	41.7	2.9	0.113	0.113	0.0027	2.67	2.3
285	5/26/1999	2:07:52 PM	0	25.596	23.657	25.189	26.666	23.292	32.055	44.787	52.279	6.455	39.133	6.63	-0.042	29.887	0.258	0	276	12.4	42.0	2.9	0.113	0.112	0.0027	2.68	2.3
286	5/26/1999	2:08:53 PM	0	25.595	23.783	25.189	26.652	23.257	32.138	44.538	51.913	6.447	38.727	6.63	-0.042	29.984	0.253	0	277	12.4	41.6	2.9	0.111	0.111			

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07b

[illegible]

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07b

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
406	5/26/1999	4:09:06 PM	0	25.32	23.944	24.914	26.652	22.856	33.801	44.756	51.699	6.343	38.896	8.507	-0.042	29.871	0.249	0.003	397	12.4	41.8	2.9	0.109	0.109	0.0026	2.61	2.2
407	5/26/1999	4:10:06 PM	0	25.355	23.978	24.869	26.732	22.814	33.643	44.694	51.813	6.399	38.862	8.507	-0.042	29.964	0.247	0	398	12.4	41.8	2.9	0.108	0.108	0.0026	2.59	2.2
408	5/26/1999	4:11:06 PM	0	25.355	23.978	24.869	26.686	22.869	33.696	44.597	52.37	6.471	39.065	8.507	-0.042	29.917	0.247	0	399	12.4	42.1	2.9	0.108	0.108	0.0026	2.57	2.2
409	5/26/1999	4:12:06 PM	0	25.355	23.933	24.803	26.561	22.362	33.519	45.066	52.308	6.391	38.862	8.507	-0.042	29.948	0.249	0	400	12.4	42.0	2.9	0.109	0.109	0.0026	2.60	2.2
410	5/26/1999	4:13:06 PM	0	25.389	24.013	24.803	26.561	22.443	33.316	45.159	52.279	6.423	39.065	8.507	-0.042	29.871	0.245	0	401	12.4	42.1	2.9	0.109	0.109	0.0026	2.60	2.2
411	5/26/1999	4:14:06 PM	0	25.344	23.968	24.864	26.481	22.362	33.033	44.639	51.678	6.335	39.099	8.507	-0.042	29.848	0.247	0	402	12.4	41.8	2.9	0.108	0.108	0.0026	2.58	2.2
412	5/26/1999	4:15:06 PM	0	25.424	23.968	25.016	26.596	22.476	32.837	45.252	52.462	6.455	38.794	8.538	-0.042	29.933	0.248	0	403	12.4	42.0	2.9	0.108	0.108	0.0026	2.57	2.2
413	5/26/1999	4:16:06 PM	0	25.424	24.048	25.096	26.471	22.336	32.479	44.725	51.791	6.463	38.828	8.568	-0.042	29.902	0.252	0	404	12.4	41.8	2.9	0.110	0.110	0.0026	2.63	2.2
414	5/26/1999	4:17:06 PM	0	25.459	24.048	25.133	26.516	22.918	32.513	44.353	51.456	6.255	38.893	8.568	-0.042	29.825	0.252	0	405	12.4	41.8	2.9	0.110	0.110	0.0026	2.64	2.2
415	5/26/1999	4:18:06 PM	0	25.539	23.957	25.213	26.391	22.789	32.573	44.725	52.096	6.503	39.065	8.568	-0.042	29.779	0.251	0	406	12.4	41.9	2.9	0.110	0.109	0.0026	2.60	2.2
416	5/26/1999	4:19:06 PM	0	25.574	24.063	25.283	26.345	22.95	32.31	44.694	52.096	6.431	39.967	8.568	-0.042	29.825	0.246	0	407	12.4	41.8	2.9	0.107	0.107	0.0025	2.55	2.2
417	5/26/1999	4:20:06 PM	0	25.654	23.957	25.408	26.265	22.859	32.31	44.694	51.913	6.479	39.2	8.599	-0.042	29.825	0.249	0	408	12.4	41.9	2.9	0.109	0.107	0.0026	2.56	2.2
418	5/26/1999	4:21:06 PM	0	25.734	24.038	25.408	26.345	22.96	32.072	44.539	52.035	6.431	38.794	8.599	-0.042	29.779	0.257	0	409	12.4	41.7	2.9	0.112	0.111	0.0027	2.66	2.3
419	5/26/1999	4:22:06 PM	0	25.814	24.038	25.484	26.3	22.869	32.182	45.035	52.309	6.455	38.964	8.599	-0.042	29.933	0.251	0	410	12.4	42.0	2.9	0.110	0.108	0.0026	2.57	2.2
420	5/26/1999	4:23:06 PM	0	25.849	23.992	25.568	26.38	23.11	32.345	44.694	51.974	6.447	38.693	8.63	-0.042	29.81	0.248	0	411	12.4	41.7	2.9	0.108	0.107	0.0026	2.56	2.2
421	5/26/1999	4:24:06 PM	0	25.829	23.992	25.603	26.22	23.03	32.026	44.57	51.821	6.447	39.065	8.63	-0.042	29.887	0.256	0	412	12.4	41.8	2.9	0.111	0.109	0.0026	2.61	2.2
422	5/26/1999	4:25:06 PM	0	25.929	23.992	25.603	26.3	23.145	32.026	44.88	52.37	6.239	39.403	8.692	-0.042	29.518	0.254	0.003	413	12.3	42.1	2.9	0.111	0.109	0.0026	2.59	2.2
423	5/26/1999	4:26:06 PM	0	26.009	23.992	25.763	26.22	23.226	32.107	44.818	52.278	6.303	39.268	8.722	-0.042	29.533	0.259	0	414	12.3	42.0	2.9	0.113	0.111	0.0026	2.63	2.2
424	5/26/1999	4:27:06 PM	0	26.009	24.072	25.763	26.3	23.145	32.107	45.221	52.675	6.271	39.504	8.722	-0.042	29.487	0.254	0	415	12.2	42.4	2.9	0.111	0.109	0.0026	2.56	2.2
425	5/26/1999	4:28:06 PM	0	26.089	24.072	25.843	26.14	22.965	31.948	44.818	52.401	6.295	38.794	8.753	-0.042	29.487	0.258	0.003	416	12.2	41.8	2.9	0.112	0.109	0.0026	2.61	2.2
426	5/26/1999	4:29:06 PM	0	26.169	23.992	25.923	26.3	23.306	32.186	44.91	52.675	6.231	39.302	8.753	-0.042	29.503	0.254	0.003	417	12.2	42.1	2.9	0.113	0.110	0.0026	2.57	2.2
427	5/26/1999	4:30:06 PM	0	26.249	23.992	25.878	26.095	23.1	31.71	44.942	52.34	6.255	39.302	8.753	-0.042	29.38	0.259	0.003	418	12.2	42.1	2.9	0.113	0.110	0.0026	2.62	2.2
428	5/26/1999	4:31:06 PM	0	26.329	23.992	26.003	26.14	23.145	31.71	45.035	52.623	6.215	39.099	8.784	-0.042	29.503	0.256	0	419	12.2	42.1	2.9	0.112	0.109	0.0026	2.58	2.2
429	5/26/1999	4:32:06 PM	0	26.329	23.992	25.843	26.14	23.065	31.948	45.097	52.353	6.279	39.335	8.753	-0.042	29.533	0.257	0.003	420	12.3	42.2	2.9	0.112	0.110	0.0026	2.60	2.2
430	5/26/1999	4:33:06 PM	0	26.329	23.992	25.796	26.3	23.065	31.869	45.262	52.675	6.168	39.403	8.753	-0.042	29.441	0.256	0	421	12.2	42.3	2.9	0.112	0.108	0.0026	2.56	2.2
431	5/26/1999	4:34:06 PM	0	26.204	24.072	25.763	26.175	22.965	31.948	44.849	52.278	6.223	39.369	8.722	-0.042	29.457	0.253	0	422	12.2	42.1	2.9	0.110	0.108	0.0026	2.57	2.2
432	5/26/1999	4:35:06 PM	0	26.169	24.072	25.763	26.3	23.065	32.265	45.262	52.767	6.287	39.268	8.692	-0.042	29.441	0.255	0.003	423	12.2	42.3	2.9	0.111	0.109	0.0026	2.58	2.2
433	5/26/1999	4:36:06 PM	0	26.169	23.992	25.603	26.255	22.965	32.265	45.19	52.492	6.303	39.403	8.661	-0.042	29.441	0.252	0	424	12.2	42.3	2.9	0.110	0.108	0.0026	2.56	2.2
434	5/26/1999	4:37:06 PM	0	26.089	24.072	25.523	26.38	23.145	32.107	45.331	53.193	6.415	39.302	8.661	-0.042	29.457	0.248	0	425	12.2	42.4	2.9	0.108	0.107	0.0025	2.52	2.1
435	5/26/1999	4:38:06 PM	0	26.089	23.992	25.443	26.3	23.065	32.026	45.262	52.628	6.267	39.504	8.63	-0.042	29.441	0.259	0	426	12.2	42.4	2.9	0.113	0.112	0.0026	2.63	2.2
436	5/26/1999	4:39:06 PM	0	26.009	23.992	25.363	26.3	23.363	31.79	44.601	52.035	6.223	39.2	8.63	-0.042	29.457	0.254	0	427	12.2	41.9	2.9	0.111	0.110	0.0026	2.58	2.2
437	5/26/1999	4:40:06 PM	0	25.97	23.992	25.283	26.22	23.065	31.948	44.818	52.196	6.111	39.504	8.63	-0.042	29.441	0.254	0	428	12.2	42.3	2.9	0.110	0.109	0.0026	2.58	2.2
438	5/26/1999	4:41:06 PM	0	25.974	24.038	25.328	26.14	23.191	31.472	45.066	52.34	6.247	39.741	8.599	-0.042	29.457	0.252	0.003	429	12.2	42.4	2.9	0.110	0.109	0.0026	2.57	2.2
439	5/26/1999	4:42:06 PM	0	25.974	24.038	25.248	26.185	23.226	31.755	44.942	51.943	6.176	39.572	8.599	-0.042	29.395	0.253	0.003	430	12.2	42.3	2.9	0.110	0.110	0.0026	2.60	2.2
440	5/26/1999	4:43:06 PM	0	25.814	24.038	25.168	26.105	23.11	31.834	44.818	52.004	6.198	39.268	8.599	-0.042	29.38	0.253	0.003	431	12.2	42.0	2.9	0.110	0.110	0.0026	2.61	2.2
441	5/26/1999	4:44:06 PM	0	25.779	24.038	25.088	26.185	23.11	32.072	45.19	52.187	6.16	39.673	8.599	-0.042	29.441	0.255	0	432	12.2	42.4	2.9	0.111	0.111	0.0026	2.62	2.2
442	5/26/1999	4:45:06 PM	0	25.734	24.038	25.068	26.185	23.191	32.182	45.903	53.224	6.311	39.707	8.568	-0.042	29.334	0.254	0	433	12.2	42.8	2.9	0.111	0.111	0.0026	2.58	2.2
443	5/26/1999	4:46:06 PM	0	25.654	24.063	25.053	26.391	23.236	32.117	45.438	52.553	6.247	40.113	8.568	-0.042	29.334	0.25	0	434	12.2	42.8	3.0	0.109	0.109	0.0025	2.55	2.2
444	5/26/1999	4:47:06 PM	0	25.699	24.003	24.973	26.391	23.156	31.879	45.469	52.889	6.295	39.91	8.568	-0.042	29.349	0.251	0	435	12.2	42.7	2.9	0.110	0.110	0.0026	2.57	2.2
445	5/26/1999	4:48:06 PM	0	25.619	24.048	24.973	26.391	23.236	31.81	45.221	52.814	6.223	39.843	8.568	-0.042	29.318	0.256	0	436	12.2	42.5	2.9	0.112	0.112	0.0026	2.63	2.2
446	5/26/1999	4:49:06 PM	0	25.619	24.003	24.893	26.391	23.236	31.841	45.035	52.584	6.319	39.843	8.538	-0.042	29.288	0.252	0	437	12.2	42.4	2.9	0.110	0.110	0.0026	2.60	2.2
447	5/26/1999	4:50:06 PM	0	25.584	24.048	24.813	26.391	23.397	31.796	45.693	52.863	6.263	39.707	8.538	-0.042	29.36	0.251	0	438	12.2	42.7	2.9	0.110	0.110	0.0026	2.58	2.2
448	5/26/1999	4:51:06 PM	0	25.524	24.048	24.748	26.391	23.442	31.896	45.278	52.78	6.113	39.707	8.538	-0.042	29.334	0.248	0	439	12.2	42.6	2.9	0.108				

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07b

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
487	5/26/1999	5:30:14 PM	0	25.846	24.069	24.834	26.297	23.484	31.98	42.825	52.348	6.495	36.583	8.88	-0.042	29.984	0.233	0	478	12.4	39.8	2.7	0.100	0.101	0.0026	2.55	2.2
488	5/26/1999	5:31:14 PM	0	25.688	24.069	24.679	26.332	23.383	32.453	42.818	52.096	6.415	36.8	8.88	-0.042	29.994	0.229	0	479	12.4	39.7	2.7	0.100	0.100	0.0025	2.53	2.1
489	5/26/1999	5:32:14 PM	0	25.688	24.15	24.799	26.377	23.303	32.455	42.835	52.37	6.319	37.307	8.88	-0.089	29.716	0.231	0.003	480	12.3	40.1	2.8	0.101	0.101	0.0025	2.53	2.2
490	5/26/1999	5:33:14 PM	0	25.606	24.069	24.799	26.457	23.383	32.378	42.825	52.187	6.287	36.8	8.91	-0.042	29.487	0.231	0	481	12.2	39.7	2.7	0.101	0.101	0.0026	2.56	2.2
491	5/26/1999	5:34:15 PM	0	25.526	24.069	24.719	26.492	23.484	32.024	42.401	52.096	6.263	36.969	8.91	-0.042	29.457	0.232	0	482	12.2	39.7	2.7	0.101	0.102	0.0026	2.57	2.2
492	5/26/1999	5:35:15 PM	0	25.365	24.069	24.719	26.537	23.383	32.342	42.587	52.157	6.199	37.104	8.91	-0.042	29.457	0.232	0	483	12.2	39.8	2.7	0.101	0.102	0.0026	2.56	2.2
493	5/26/1999	5:36:15 PM	0	25.365	24.069	24.639	26.537	23.303	32.104	43.175	52.645	6.311	37.341	8.941	-0.042	29.441	0.231	0	484	12.2	40.3	2.8	0.101	0.102	0.0025	2.53	2.2
494	5/26/1999	5:37:15 PM	0	25.285	24.069	24.639	26.457	23.484	31.787	42.556	52.187	6.353	36.766	8.849	-0.089	29.61	0.23	0	485	12.3	39.7	2.7	0.100	0.101	0.0026	2.56	2.2
495	5/26/1999	5:38:15 PM	0	25.285	24.069	24.639	26.457	23.303	32.183	42.649	52.248	6.423	36.867	8.849	-0.042	29.841	0.23	0	486	12.3	39.8	2.7	0.100	0.101	0.0026	2.55	2.2
496	5/26/1999	5:39:15 PM	0	25.285	24.069	24.639	26.457	23.383	32.342	42.535	52.614	6.431	37.273	8.849	-0.042	29.872	0.23	0	487	12.3	40.1	2.8	0.100	0.101	0.0025	2.53	2.2
497	5/26/1999	5:40:15 PM	0	25.205	24.069	24.604	26.457	23.223	32.421	42.88	52.492	6.439	37.003	8.88	-0.042	29.596	0.23	0	488	12.3	39.8	2.7	0.100	0.102	0.0025	2.55	2.2
498	5/26/1999	5:41:16 PM	0	25.285	24.069	24.604	26.582	23.303	32.262	46.058	52.187	6.215	40.147	6.821	-0.042	30.01	0.871	0	489	12.5	43.1	3.0	0.380	0.384	0.0069	8.92	7.8
499	5/26/1999	5:42:16 PM	0	25.09	24.115	24.479	26.502	23.348	32.228	44.758	51.689	6.191	39.606	6.26	-0.089	29.917	0.611	0	490	12.4	42.2	2.9	0.287	0.271	0.0064	6.42	5.3
500	5/26/1999	5:43:16 PM	0	25.09	24.115	24.524	26.502	23.268	32.468	45.068	51.76	6.247	39.806	6.137	-0.042	29.856	0.522	0.003	491	12.4	42.3	2.9	0.228	0.231	0.0055	5.46	4.8
501	5/26/1999	5:44:16 PM	0	25.01	24.115	24.444	26.502	23.348	32.545	44.894	51.73	6.223	39.572	6.229	-0.042	29.841	0.47	0	492	12.4	42.1	2.9	0.205	0.208	0.0049	4.95	4.2
502	5/26/1999	5:45:16 PM	0	25.09	24.115	24.444	26.502	23.348	32.228	-6.137	-1.688	0.439	-6.441	3.795	-0.042	-0.065	0.068	0	493	0.0	-6.3	-0.4	0.029	0.029	-0.0047	-4.65	-4.0
503																											
504		Average		25.8	23.4	25.1	26.1	23.1	32.1	44.4	51.7	6.3	38.7	6.7	-0.1	29.6	0.270	0.0		12.3	41.5	2.9	0.118	0.117	0.003	2.8	2.4
505		Maximum		27.9	24.1	27.6	27.1	24.6	33.9	45.9	53.3	6.8	40.3	7.3	0.0	30.2	0.765	0.0		12.5	43.0	3.0	0.394	0.320	0.008	8.2	7.0
506		Median		25.5	23.6	24.9	26.3	23.1	32.1	44.8	52.0	6.4	38.9	6.6	0.0	29.9	0.259	0.0		12.4	41.8	2.9	0.113	0.113	0.003	2.7	2.3
507		Minimum		24.2	22.0	23.8	24.3	21.9	29.9	41.3	48.1	5.7	35.3	6.2	-0.1	27.4	0.241	0.0		11.4	38.4	2.6	0.105	0.107	0.003	2.5	2.1
508		Std Dev		0.9	0.6	0.9	0.7	0.4	0.8	0.9	0.9	0.2	0.8	0.3	0.0	0.5	0.039	0.0		0.2	0.8	0.1	0.017	0.016	0.003	0.4	0.4
509		Number of Points Used		447	447	447	447	447	447	447	447	447	447	447	447	447	447	447		447	447	447	447	447	447	447	447

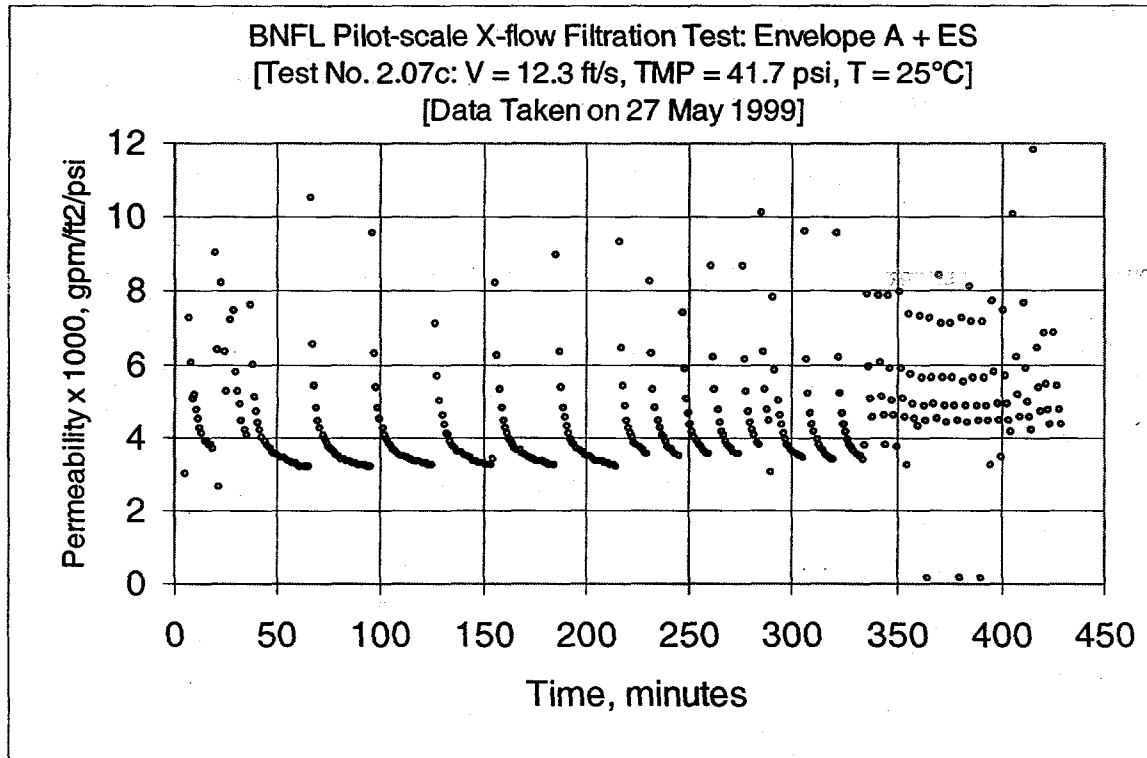
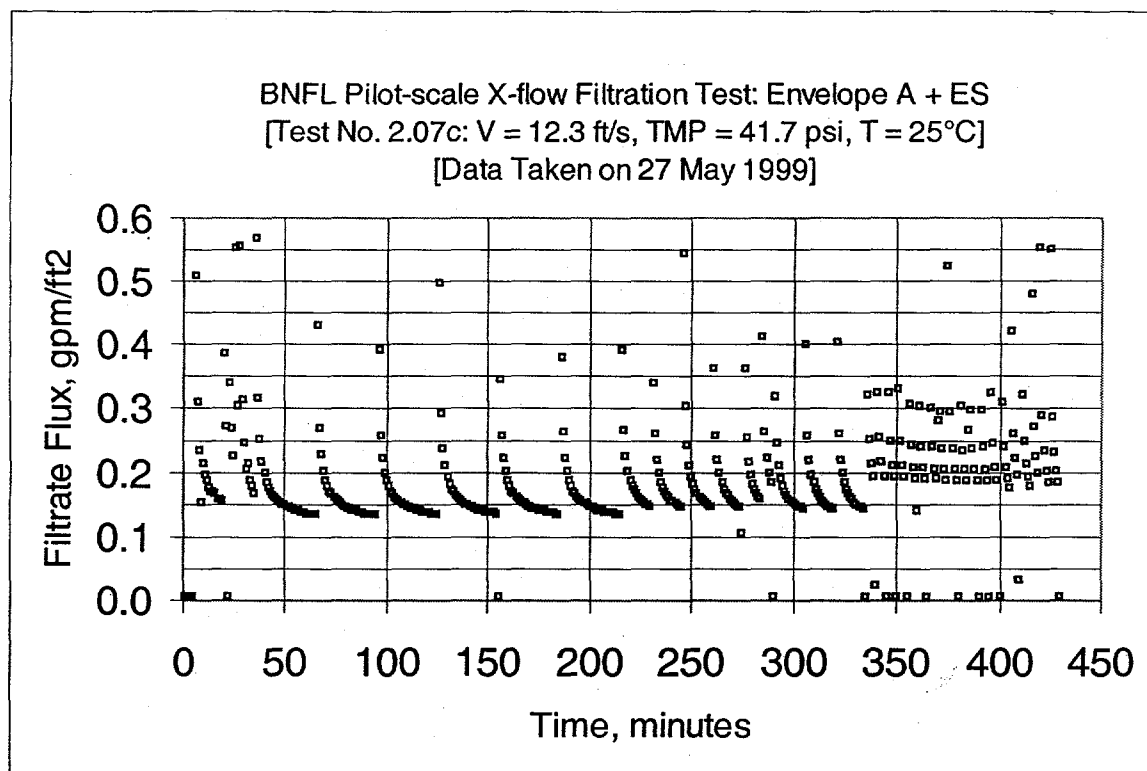


Figure B17a: Test Run 2.07c, 0.5 wt% Insoluble Solids Concentration (Entire Run)

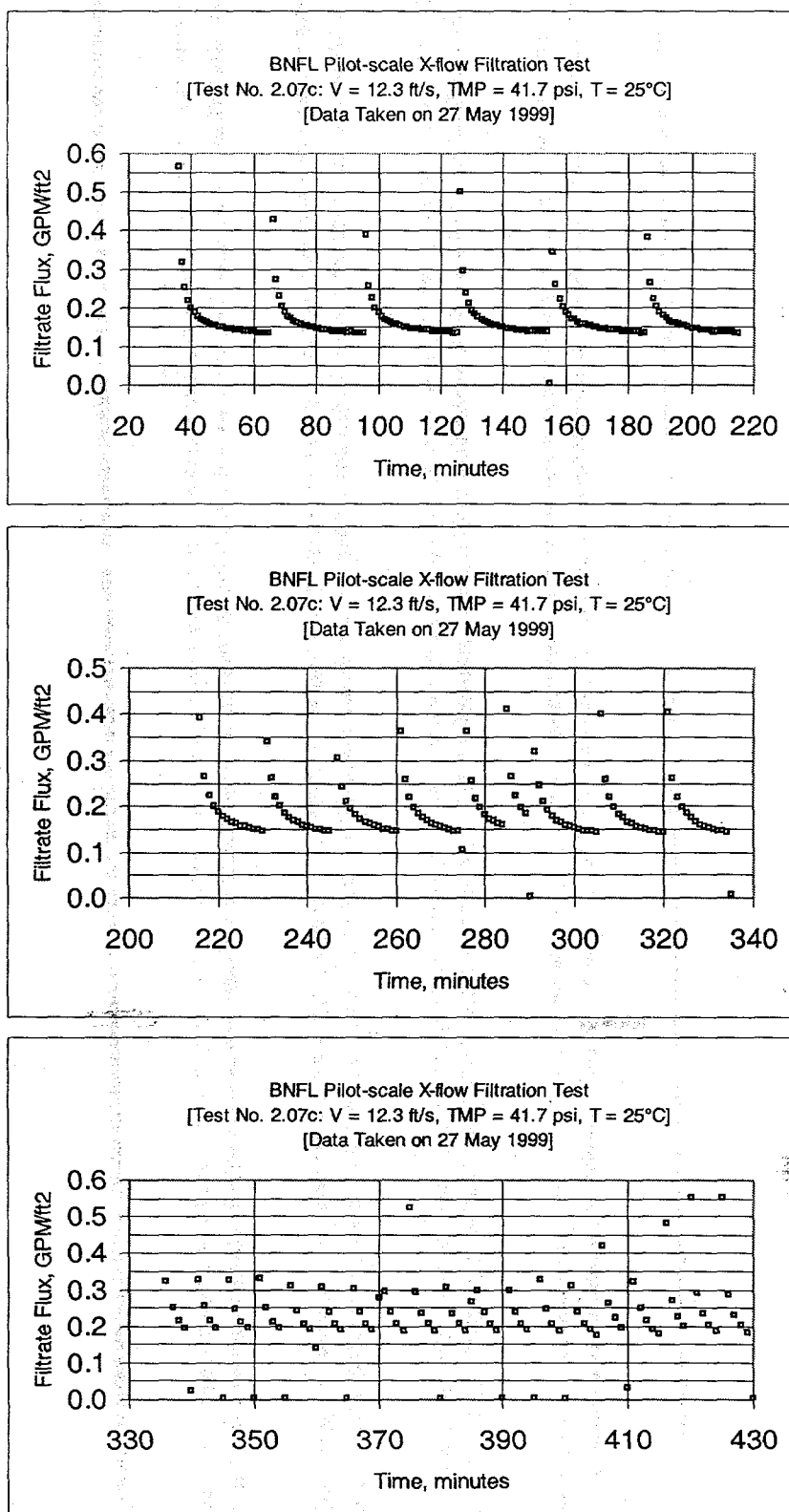


Figure B17b: Test Run 2.07c, 0.5 wt% Insoluble Solids Concentration (30, 15, & 5 min. Backpulsing)

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07c

A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	AB	AC	AD	AE	AF	AG	AH	AI	AJ	AK	AL	AM	AN	AO	AP	AQ	AR	AS	AT	AU	AV	AW	AX	AY	AZ	BA	BB	BC	BD	BE	BF	BG	BH	BI	BJ	BK	BL	BM	BN	BO	BP	BQ	BR	BS	BT	BU	BV	BW	BX	BY	BZ	CA	CB	CC	CD	CE	CF	CG	CH	CI	CJ	CK	CL	CM	CN	CO	CP	CQ	CR	CS	CT	CU	CV	CW	CX	CY	CZ	DA	DB	DC	DD	DE	DF	DG	DH	DI	DJ	DK	DL	DM	DN	DO	DP	DQ	DR	DS	DT	DU	DV	DW	DX	DY	DZ	EA	EB	EC	ED	EE	EF	EG	EH	EI	EJ	EK	EL	EM	EN	EO	EP	EQ	ER	ES	ET	EU	EV	EW	EX	EY	EZ	FA	FB	FC	FD	FE	FF	FG	FH	FI	FJ	FK	FL	FM	FN	FO	FP	FQ	FR	FS	FT	FU	FV	FW	FX	FY	FZ	GA	GB	GC	GD	GE	GF	GG	GH	GI	GJ	GK	GL	GM	GN	GO	GP	GQ	GR	GS	GT	GU	GV	GW	GX	GY	GZ	HA	HB	HC	HD	HE	HF	HG	HH	HI	HJ	HK	HL	HM	HN	HO	HP	HQ	HR	HS	HT	HU	HV	HW	HX	HY	HZ	IA	IB	IC	ID	IE	IF	IG	IH	II	IJ	IK	IL	IM	IN	IO	IP	IQ	IR	IS	IT	IU	IV	IW	IX	IY	IZ	JA	JB	JC	JD	JE	JF	JG	JH	JI	JJ	JK	JL	JM	JN	JO	JP	JQ	JR	JS	JT	JU	JV	JW	JX	JY	JZ	KA	KB	KC	KD	KE	KF	KG	KH	KI	KJ	KK	KL	KM	KN	KO	KP	KQ	KR	KS	KT	KU	KV	KW	KX	KY	KZ	LA	LB	LC	LD	LE	LF	LG	LH	LI	LJ	LK	LL	LM	LN	LO	LP	LQ	LR	LS	LT	LU	LV	LW	LX	LY	LZ	MA	MB	MC	MD	ME	MF	MG	MH	MI	MJ	MK	ML	MN	MO	MP	MQ	MR	MS	MT	MU	MV	MW	MX	MY	MZ	NA	NB	NC	ND	NE	NF	NG	NH	NI	NJ	NK	NL	NM	NO	NP	NQ	NR	NS	NT	NU	NV	NW	NX	NY	NZ	OA	OB	OC	OD	OE	OF	OG	OH	OI	OJ	OK	OL	OM	ON	OO	OP	OQ	OR	OS	OT	OU	OV	OW	OX	OY	OZ	PA	PB	PC	PD	PE	PF	PG	PH	PI	PJ	PK	PL	PM	PN	PO	PP	PQ	PR	PS	PT	PU	PV	PW	PX	PY	PZ	QA	QB	QC	QD	QE	QF	QG	QH	QI	QJ	QK	QL	QM	QN	QO	QP	QQ	QR	QS	QT	QU	QV	QW	QX	QY	QZ	RA	RB	RC	RD	RE	RF	RG	RH	RI	RJ	RK	RL	RM	RN	RO	RP	RQ	RR	RS	RT	RU	RV	RW	RX	RY	RZ	SA	SB	SC	SD	SE	SF	SG	SH	SI	SJ	SK	SL	SM	SN	SO	SP	SQ	SR	SS	ST	SU	SV	SW	SX	SY	SZ	TA	TB	TC	TD	TE	TF	TG	TH	TI	TJ	TK	TL	TM	TN	TO	TP	TQ	TR	TS	TT	TU	TV	TW	TX	TY	TZ	UA	UB	UC	UD	UE	UF	UG	UH	UI	UJ	UK	UL	UM	UN	UO	UP	UQ	UR	US	UT	UU	UV	UW	UX	UY	UZ	VA	VB	VC	VD	VE	VF	VG	VH	VI	VJ	VK	VL	VM	VN	VO	VP	VQ	VR	VS	VT	VU	VV	VW	VX	VY	VZ	WA	WB	WC	WD	WE	WF	WG	WH	WI	WJ	WK	WL	WM	WN	WO	WP	WQ	WR	WS	WT	WU	WV	WW	WX	WY	WZ	XA	XB	XC	XD	XE	XF	XG	XH	XI	XJ	XK	XL	XM	XN	XO	XP	XQ	XR	XS	XT	XU	XV	XW	XX	XY	XZ	YA	YB	YC	YD	YE	YF	YG	YH	YI	YJ	YK	YL	YM	YN	YO	YP	YQ	YR	YS	YT	YU	YV	YW	YX	YY	YZ	ZA	ZB	ZC	ZD	ZE	ZF	ZG	ZH	ZI	ZJ	ZK	ZL	ZM	ZN	ZO	ZP	ZQ	ZR	ZS	ZT	ZU	ZV	ZW	ZX	ZY	ZZ																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																																												
DATE		TIME		SOLNO		FLTR		Q		F		S		L		O		H		T		K		P		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA		AB		AC		AD		AE		AF		AG		AH		AI		AJ		AK		AL		AM		AN		AO		AP		AQ		AR		AS		AT		AU		AV		AW		AX		AY		AZ		BA		BB		BC		BD		BE		BF		BG		BH		BI		BJ		BK		BL		BM		BN		BO		BP		BQ		BR		BS		BT		BU		BV		BW		BX		BY		BZ		CA		CB		CC		CD		CE		CF		CG		CH		CI		CJ		CK		CL		CM		CN		CO		CP		CQ		CR		CS		CT		CU		CV		CW		CX		CY		CZ		DA		DB		DC		DD		DE		DF		DG		DH		DI		DJ		DK		DL		DM		DN		DO		DP		DQ		DR		DS		DT		DU		DV		DW		DX		DY		DZ		EA		EB		EC		ED		EE		EF		EG		EH		EI		EJ		EK		EL		EM		EN		EO		EP		EQ		ER		ES		ET		EU		EV		EW		EX		EY		EZ		FA		FB		FC		FD		FE		FF		FG		FH		FI		FJ		FK		FL		FM		FN		FO		FP		FQ		FR		FS		FT		FU		FV		FW		FX		FY		FZ		GA		GB		GC		GD		GE		GF		GG		GH		GI		GJ		GK		GL		GM		GN		GO		GP		GQ		GR		GS		GT		GU		GV		GW		GX		GY		GZ		HA		HB		HC		HD		HE		HF		HG		HH		HI		HJ		HK		HL		HM		HN		HO		HP		HQ		HR		HS		HT		HU		HV		HW		HX		HY		HZ		IA		IB		IC		ID		IE		IF		IG		IH		II		IJ		IK		IL		IM		IN		IO		IP		IQ		IR		IS		IT		IU		IV		IW		IX		IY		IZ		JA		JB		JC		JD		JE		JF		JG		JH		JI		JJ		JK		JL		JM		JN		JO		JP		JQ		JR		JS		JT		JU		JV		JW		JX		JY		JZ		KA		KB		KC		KD		KE		KF		KG		KH		KI		KJ		KK		KL		KM		KN		KO		KP		KQ		KR		KS		KT		KU		KV		KW		KX		KY		KZ		LA		LB		LC		LD		LE		LF		LG		LH		LI		LJ		LK		LL		LM		LN		LO		LP		LQ		LR		LS		LT		LU		LV		LW		LX		LY		LZ		MA		MB		MC		MD		ME		MF		MG		MH		MI		MJ		MK		ML		MN		MO		MP		MQ		MR		MS		MT		MU		MV		MW		MX		MY		MZ		NA		NB		NC		ND		NE		NF		NG		NH		NI		NJ		NK		NL		NM		NO		NP		NQ		NR		NS		NT		NU		NV		NW		NX		NY		NZ		OA		OB		OC		OD		OE		OF		OG		OH		OI		OJ		OK		OL		OM		ON		OO		OP		OQ		OR		OS		OT		OU		OV		OW		OX		OY		OZ		PA		PB		PC		PD		PE		PF		PG		PH		PI		PJ		PK		PL		PM		PN		PO		PP		PQ		PR		PS		PT		PU		PV		PW		PX		PY		PZ		QA		QB		QC		QD		QE		QF		QG		QH		QI		QJ		QK		QL		QM		QN		QO		QP		QQ		QR		QS		QT		QU		QV		QW		QX		QY		QZ		RA		RB		RC		RD		RE		RF		RG		RH		RI		RJ		RK		RL		RM		RN		RO		RP		RQ		RR		RS		RT		RU		RV		RW		RX		RY		RZ		SA		SB		SC		SD		SE		SF		SG		SH		SI		SJ		SK		SL		SM		SN		SO		SP		SQ		SR		SS		ST		SU		SV		SW		SX		SY		SZ		TA		TB		TC		TD		TE		TF		TG		TH		TI		TJ		TK		TL		TM		TN		TO		TP		TQ		TR		TS		TT		TU		TV		TW		TX		TY		TZ		UA		UB		UC		UD		UE		UF		UG		UH		UI		UJ		UK		UL		UM		UN		UO		UP		UQ		UR		US		UT		UU		UV		UW		UX		UY		UZ		VA		VB		VC		VD		VE		VF		VG		VH		VI		VJ		VK		VL		VM		VN		VO		VP		VQ		VR		VS		VT		VU		VV		VW		VX		VY		VZ		WA		WB		WC		WD		WE		WF		WG		WH		WI		WJ		WK		WL		WM		WN		WO		WP		WQ		WR		WS		WT		WU		WV		WW		WX		WY		WZ		XA		XB		XC		XD		XE		XF		XG		XH		XI		XJ		XK		XL		XM		XN		XO		XP		XQ		XR		XS		XT		XU		XV		XW		XX		XY		XZ		YA		YB		YC		YD	

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07c

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	
1	1.62711999	1.00158 AM	0.2654	22.299	26.977	24.824	24.184	33.168	44.777	51.534	5.189	33.592	4.746	-0.135	29.825	0.36	78	12.4	41.5	2.9	0.166	0.157	0.0038	3.79	3.1	3.2	MA	
2	26.983	22.299	24.779	24.894	33.052	44.167	51.69	6.511	33.768	4.746	0.163	33.592	4.746	-0.135	29.825	0.36	78	12.4	41.5	2.9	0.163	0.157	0.0038	3.79	3.1	3.2		
3	26.983	22.299	24.779	24.894	33.052	44.167	51.69	6.511	33.768	4.746	0.163	33.592	4.746	-0.135	29.825	0.36	78	12.4	41.5	2.9	0.163	0.157	0.0038	3.79	3.1	3.2		
4	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
5	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
6	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
7	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
8	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
9	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
10	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
11	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
12	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
13	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
14	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
15	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
16	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
17	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
18	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
19	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
20	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
21	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
22	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
23	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
24	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
25	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
26	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
27	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
28	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
29	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
30	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
31	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
32	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
33	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
34	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
35	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
36	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
37	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
38	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
39	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
40	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
41	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
42	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
43	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9	0.158	0.147	0.0033	3.53	3.0	3.1	
44	27.458	22.264	27.368	24.899	24.28	33.177	44.522	51.458	6.375	39.683	6.391	39.761	6.391	-0.089	29.933	0.362	0	78	12.4	41.5	2.9</							

[illegible]

	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
244	527/199	12:44:15 PM	24.559	24.327	26.485	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
245	527/199	12:45:15 PM	24.559	24.327	26.534	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
246	527/199	12:46:15 PM	24.559	24.327	26.583	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
247	527/199	12:47:15 PM	24.559	24.327	26.632	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
248	527/199	12:48:15 PM	24.559	24.327	26.681	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
249	527/199	12:49:15 PM	24.559	24.327	26.730	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
250	527/199	12:50:15 PM	24.559	24.327	26.779	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
251	527/199	12:51:15 PM	24.559	24.327	26.828	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
252	527/199	12:52:15 PM	24.559	24.327	26.877	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
253	527/199	12:53:15 PM	24.559	24.327	26.926	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
254	527/199	12:54:15 PM	24.559	24.327	26.975	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
255	527/199	12:55:15 PM	24.559	24.327	27.024	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
256	527/199	12:56:15 PM	24.559	24.327	27.073	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
257	527/199	12:57:15 PM	24.559	24.327	27.122	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.0041	4.08	
258	527/199	12:58:15 PM	24.559	24.327	27.171	22.025	33.826	43.361	82.033	6.311	38.727	6.853	0.004	26.765	0.381	0.003	237	12.4	41.6	2.9	0.165	0.170	0.004		

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.07c

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APPENDIX C

EXPERIMENTAL DATA: HIGH SOLIDS CONCENTRATION

Appendix Contents

1. Nomenclature sheet for data tables

2. Experimental data:

Fig.	Run	Solution	Done on
C1	2.14	7 wt% Solids	6/11/99
C2	2.14b	8 wt% Solids	6/16/99
C3	2.20b	5 to 16 wt% Solids	6/17/99

General Note: For measurement uncertainties see Appendix F

Special Notes:

- The data for every test run are highlighted with two graphs: Filtrate Flux vs. Time and Permeability vs. Time. Those graphs include all the data taken during the run period.
- The beginning and end of the data for most graphs show large deviations from the overall series of points. Those deviations were caused by backpulsing the filter that temporarily stopped the flow of filtrate.
- All columns of data, in all the tables, are ended with several statistical values of that column, i.e., Average, Maximum, Median, Minimum, Standard Deviation, and Number of Points used (in calculating the 5 statistical quantities). Most of the data with time were maintain constant, and therefore the statistics are meaningful for normally distributed data, however Filtrate Flux and Permeability decrease with time and therefore are not normally distributed.
- To calculate those quantities mentioned in item c, only those data points that start from the end of a backpulse to just before the ending backpulse were included. This is the reason why the quantity of Number of Points Used was given.
- The data for the graphs, and all the data taken for the individual test run that the graphs represent, immediately follow the specific figure.
- Run 2.14 was done after the test rig was cleaned due plugging when the solids concentration was increased from 0.5 wt% to between 10 and 15.wt%. In an attempt to unplug the test rig in a hurry the slurry was diluted with water. Therefore, the slurry for this run had a sodium concentration closer to 3 M instead of the target of 5.5 M. After the wash run another batch of slurry was made and a new run was done and called 2.14b.
- Run 2.20b was not a steady-state run like 2.14 and 2.14b, where the filtrate returns to the slurry to maintain its concentration. Run 2.20b was done to successively make the slurry more concentrated until the filter plugged. That is why the Filtrate Flux graph of Fig. C3 appears to have steps. Starting with approximately 80 liters of post-washed slurry, approximately 7.3 liters of filtrate was removed 6 times and the remaining 36 liters just barely covered the bottom of the slurry reservoir. The run had to stop because the cooling coils were totally exposed and couldn't cool the slurry which became very hot and the pumps began to draw in air because the thick slurry

couldn't supply the suction line with slurry fast enough. Fortunately, the filter did not plug at all.

Nomenclature For Data Sheets

(See Figure 1: Main Test Rig - Pilot Scale Cross Flow for the Instrument Location)

Column	Heading	Full Heading	Explanation
A =	DATE	= DATE	Day the test was done
B =	TIME	= TIME	Time data entry was made
C =	SOLENOID	= SOLENOID	1=yes, 0=no: for the pressure to the backpulse piston
D =	FLTRT (deg)	= FLTRT (deg C) T2	Filtrate Temperature in Filter at exit of the Filter Housing
E =	CL LOOP (deg)	= CL LOOP (deg C) T3	Temperature of Liquid in the Cleaning Loop
F =	SL LOOP (deg)	= SL LOOP (deg C) T1	Temperature of Liquid in the Slurry Loop at the Reservoir Tank
G =	UP AMB (deg)	= UP AMB (deg C) T4	Ambient Temperature at the top of the Test Rig - 3rd level
H =	BOT AMB (deg)	= BOT AMB (deg C) T5	Ambient Temperature at the bottom of the Test Rig - 1st level
I =	T6 (deg C) SPARE	= T6 (deg C) SPARE	Spare Thermocouple - Currently Not Being Used
J =	BOT DP (psid)	= BOT DP (psid) dP2	Differential Pressure between the Filter Slurry Entrance and the bottom Filtrate Exit
K =	FLTR (psig) P1	= FLTR (psig) P1	Gauge Pressure at the Filter Slurry Entrance
L =	FLTR DP (psid)	= FLTR DP (psid) dP1	Differential Pressure between the Filter Slurry Entrance and Exit
M =	TOP DP (psid)	= TOP DP (psid) dP3	Differential Pressure between the Filter Slurry Exit and the Top Filtrate Exit
N =	FLTRATE (psig) P2	= FLTRATE (psig) P2	Gauge Pressure at the Filter Filtrate Exit
O =	PISTON (psig) P3	= PISTON (psig) P3	Air Gauge Pressure Applied to Backpulse Piston
P =	SL FLOW (gpm) Q1	= SL FLOW (gpm) Q1	Flow Rate of the Slurry Flow
Q =	FLTR FLOW (gpm) Q2	= FLTR FLOW (gpm) Q2	Flow Rate of the Filtrate Flow
R =	V9	=	Spare Channel Not Used

The following columns are calculated results based on the appropriate columns

S =	Number	=	Number	Data number which is equivalent to 1 minute since this was the acquisition frequency
T =	Vel, ft/s	=	Vel, ft/s	Axial slurry velocity = [Column P] / 7.48 gal/ft ² / 60 sec/min / flow area (=0.005369 ft ²)
U =	TMP, PSI	=	TMP, PSI	Transmembrane Pressure = ([Column J] + [Column M])/2
V =	TMP, bar	=	TMP, bar	[Column U] / 14.504 bar/psi
W =	GPM/FT2	=	GPM/FT2	[Column Q] / inside diameter filter surface area (= 2.29 ft ²)
X =	GPM/FT2	=	GPM/FT2 at 25°C	Test Spec. correction factor: [Column W] x exp(2500 x ((1/(273+[Column T]))-(1/298)))
Y =	PERMEABILITY	=	PERMEABILITY (gpm/ft ² /psi)	[Column X] / [Column U]
Z =	x 1000	=	PERMEABILITY x 1000	[Column Z] x 1000
AA =	PERMEABILITY	=	PERMEABILITY (m/day/bar)	[Column Y] x conversion factor (= 851.0145 m/day/bar / gpm/ft ² /bar)

*Axial slurry flow area is based on 7 porous tubes with an inside diameter of 3/8 inch: $7 \times \pi / 4 \times (0.375 \text{ inch} / 12 \text{ inches/ft})^2 = 0.005369 \text{ ft}^2$

**Inside diameter filter surface area for 7 tubes with an inside diameter of 3/8 inch, 40-inches long: $7 \times \pi \times (0.375 \text{ inch}) \times 40 \text{ inches} / 144 \text{ in}^2/\text{ft}^2 = 2.29 \text{ ft}^2$

Exceptions:

- For Run 2.21b (Cleaning); This run was carried out over a three different periods on three days therefore there are two NUMBER COLUMNS: S & T. Column S is continuous and Column T is continuous but starts over for each period. All the columns to the right of Column S are shifted by one.
- For Run 2.22b (Water); After July 10, 1999 a second filtrate flow meter was added to measure flow rates from 1.2 to 5 gpm. The final water test run (Run 2.22b) has an extra filtrate flow rate column. Column R, the spare column, was made the new flow rate:

R = **Q3, FLTR F** = Q3, FLTR FLOW (gpm) Flow Rate of the Filtrate Flow (above 1.2 gpm), Installed after 7/10/99

also Run 2.22b has two NUMBER columns (like Run 2.21b) so Exception 1 also applies.

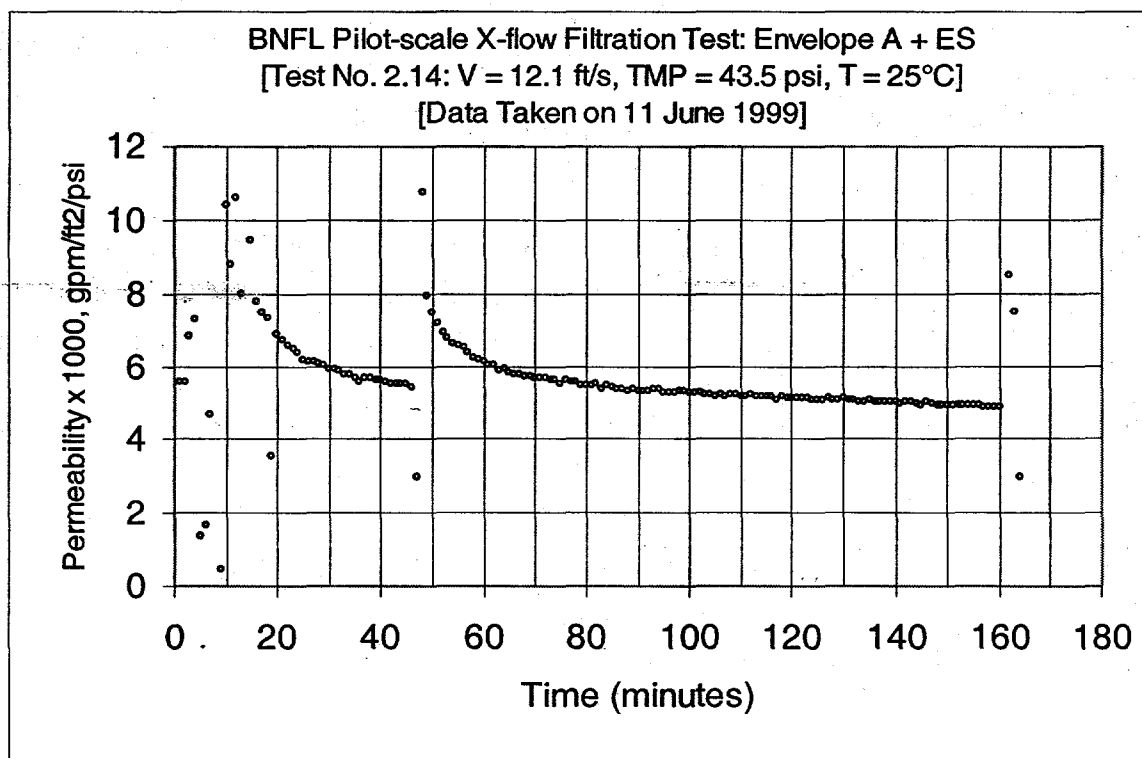
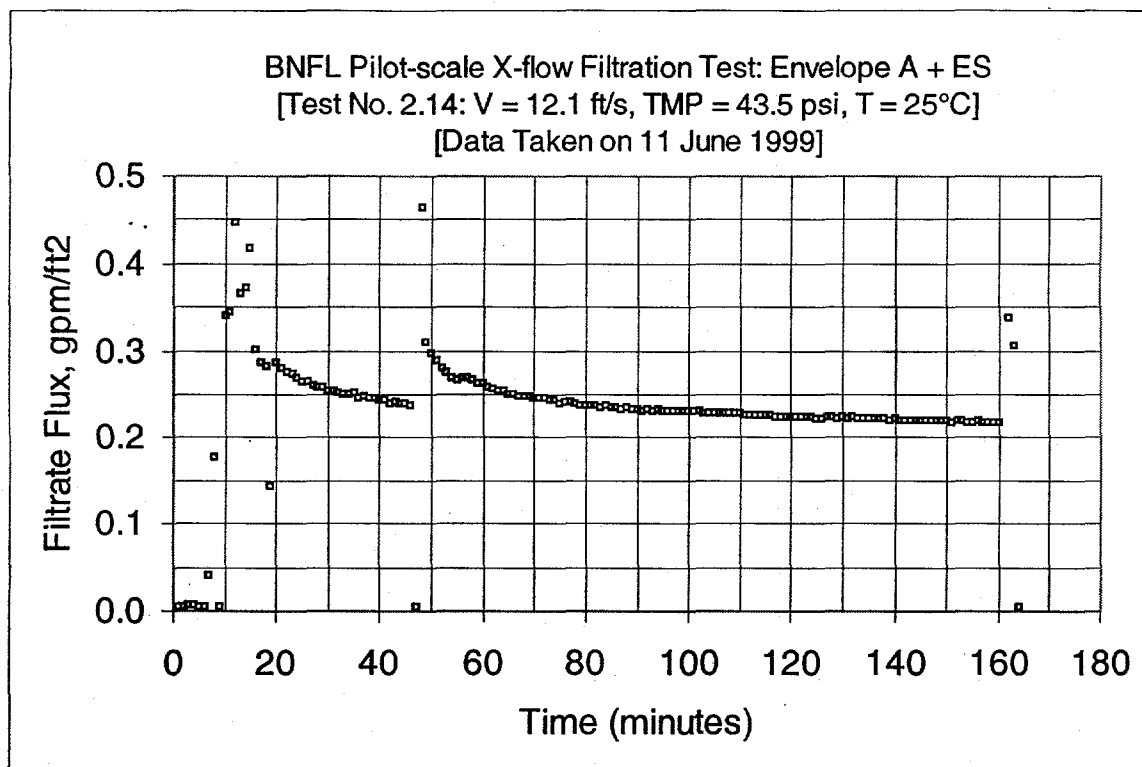


Figure C1: Test Run 2.14, 7 wt% Insoluble Solids Concentration

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.14

[illegible]

[illegible]

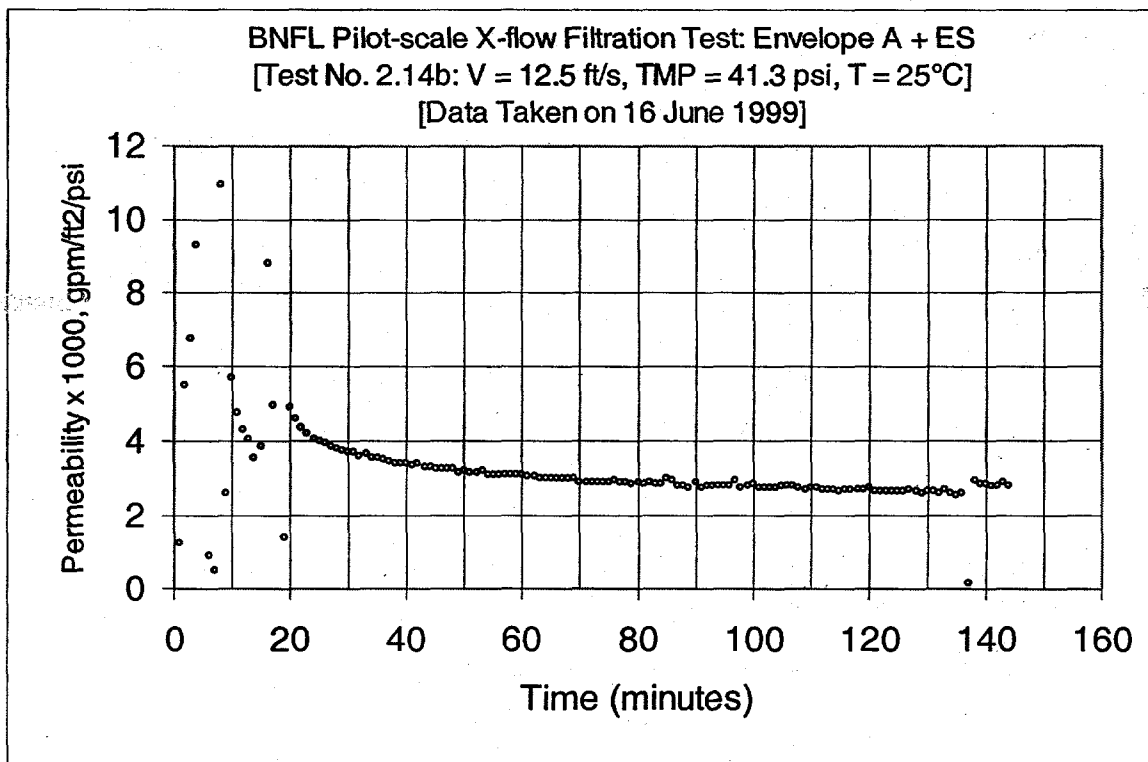
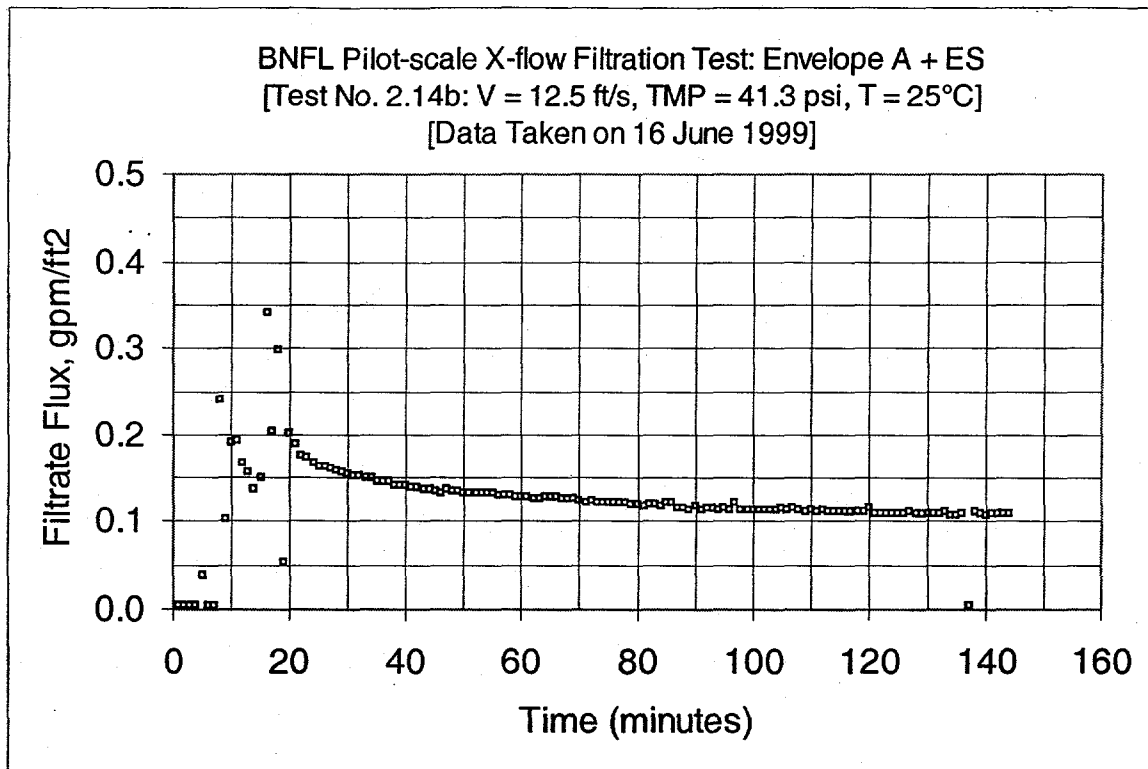


Figure C2: Test Run 2.14b, 8 wt% Insoluble Solids Concentration

[illegible]

[illegible]

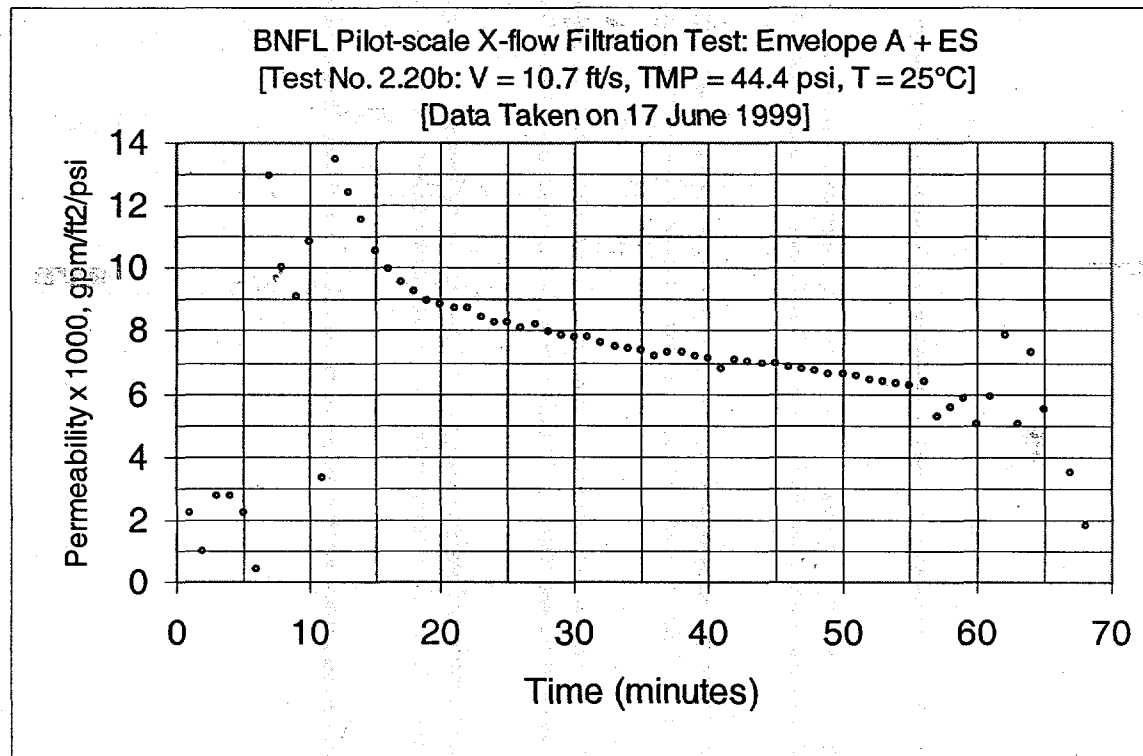
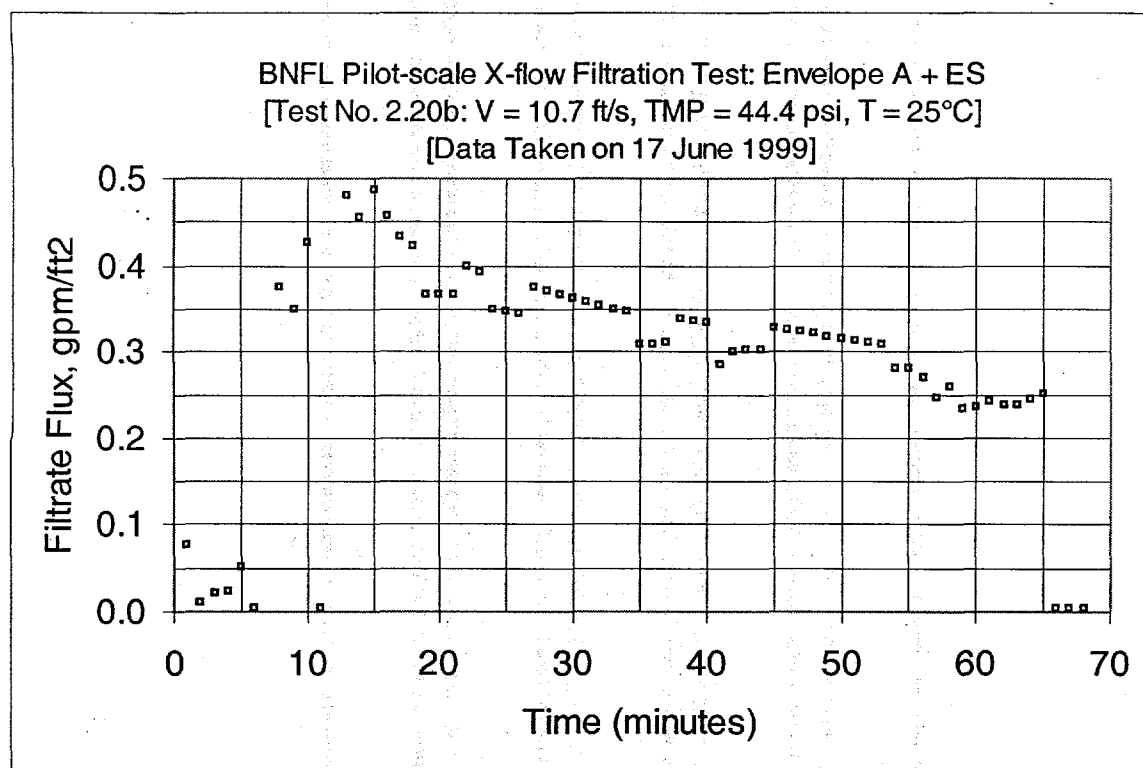


Figure C3: Test Run 2.20b, 5 wt% to 16 wt% Insoluble Solids Concentration

[illegible]

APPENDIX D

EXPERIMENTAL DATA: SLURRY WASH

Appendix Contents

1. Nomenclature sheet for data tables

2. Experimental data:

Fig.	Run	Solution	Done on
D1	2.15	First Wash 1	6/11/99
D2	2.16	First Wash 2	6/14/99
D3	2.18	First Wash 3	6/14/99
D4	2.19	First Wash 4	6/14/99
D5	2.15b	Second Wash 1	6/16/99
D6	2.16b	Second Wash 2	6/16/99
D7	2.17b	Second Wash 3	6/16/99
D8	2.18b	Second Wash 4	6/16/99
D9	2.19b	Second Wash 5	6/26/99

General Note: For measurement uncertainties see Appendix F

Special Notes:

- Run 2.17 was not done because run 2.14 began with a dilute slurry that was taken as a first wash run.
- The data for every test run are highlighted with the top two graphs in each figure: Filtrate Flux vs. Time and Permeability vs. Time. Those graphs include all the data taken during the run period.
- The bottom graph of each figure is a subset of the Filtrate Flux vs. Time data during the period that the filtrate was being removed to prepare for another charge of water.
- The beginning and end of the data for most graphs show large deviations from the overall series of points. Those deviations were caused by backpulsing the filter that temporarily stopped the flow of filtrate.
- All columns of data, in all the tables, are ended with several statistical values of that column, i.e., Average, Maximum, Median, Minimum, Standard Deviation, and Number of Points used (in calculating the 5 statistical quantities). Most of the data with time were maintain constant, and therefore the statistics are meaningful for normally distributed data, however Filtrate Flux and Permeability decrease with time and therefore are not normally distributed.
- To calculate those quantities mentioned in item e, only those data points that start from the end of a backpulse to just before the ending backpulse were included. This is the reason why the quantity of Number of Points Used was given.
- The data for the graphs, and all the data taken for the individual test run that the graphs represent, immediately follow the specific figure.
- As second set of statistical values is given for the time period just during when filtrate was removed from the test rig. This is shown as the bottom graph of all the figures as explained in item

- i. Note, the flowmeter for the filtrate flux, Q2, could only measure up to 0.533 gpm/ft². Any data above that value is meaningless.

Nomenclature For Data Sheets

(See Figure 1: Main Test Rig - Pilot Scale Cross Flow for the Instrument Location)

Column	Heading	Full Heading	Explanation
A =	DATE	= DATE	Day the test was done
B =	TIME	= TIME	Time data entry was made
C =	SOLENOID	= SOLENOID	1=yes, 0=no: for the pressure to the backpulse piston
D =	FLTRT (deg	= FLTRT (deg C) T2	Filtrate Temperature in Filter at exit of the Filter Housing
E =	CL LOOP (c	= CL LOOP (deg C) T3	Temperature of Liquid in the Cleaning Loop
F =	SL LOOP (c	= SL LOOP (deg C) T1	Temperature of Liquid in the Slurry Loop at the Reservoir Tank
G =	UP AMB (de	= UP AMB (deg C) T4	Ambient Temperature at the top of the Test Rig - 3rd level
H =	BOT AMB (= BOT AMB (deg C) T5	Ambient Temperature at the bottom of the Test Rig - 1st level
I =	T6 (deg C) S	= T6 (deg C) SPARE	Spare Thermocouple - Currently Not Being Used
J =	BOT DP (ps	= BOT DP (psid) dP2	Differential Pressure between the Filter Slurry Entrance and the bottom Filtrate Exit
K =	FLTR (psig)	= FLTR (psig) P1	Gauge Pressure at the Filter Slurry Entrance
L =	FLTR DP (p	= FLTR DP (psid) dP1	Differential Pressure between the Filter Slurry Entrance and Exit
M =	TOP DP (ps	= TOP DP (psig) dP3	Differential Pressure between the Filter Slurry Exit and the Top Filtrate Exit
N =	FLTRATE (= FLTRATE (psig) P2	Gauge Pressure at the Filter Filtrate Exit
O =	PISTON (ps	= PISTON (psig) P3	Air Gauge Pressure Applied to Backpulse Piston
P =	SL FLOW (g	= SL FLOW (gpm) Q1	Flow Rate of the Slurry Flow
Q =	FLTR FLOW	= FLTR FLOW (gpm) Q2	Flow Rate of the Filtrate Flow
R =	V9	=	Spare Channel Not Used

The following columns are calculated results based on the appropriate columns

S =	Number	=	Number	Data number which is equivalent to 1 minute since this was the acquisition frequency
T =	Vel, ft/s	=	Vel, ft/s	Axial slurry velocity = [Column P] / 7.48 gal/ft ² / 60 sec/min / flow area (=0.005369 ft ²)
U =	TMP, PSI	=	TMP, PSI	Transmembrane Pressure = ([Column J] + [Column M])/2
V =	TMP, bar	=	TMP, bar	[Column U] / 14.504 bar/psi
W =	GPM/FT2	=	GPM/FT2	[Column Q] / inside diameter filter surface area (= 2.29 ft ²)
X =	GPM/FT2	=	GPM/FT2 at 25°C	Test Spec. correction factor: [Column W] x exp(2500 x ((1/(273+[Column T]))-(1/298)))
Y =	PERMEABILITY	=	PERMEABILITY (gpm/ft ² /psi)	[Column X] / [Column U]
Z =	x 1000	=	PERMEABILITY x 1000	[Column Z] x 1000
AA =	PERMEABILITY	=	PERMEABILITY (m/day/bar)	[Column Y] x conversion factor (= 851.0145 m/day/bar / gpm/ft ² /bar)

*Axial slurry flow area is based on 7 porous tubes with an inside diameter of 3/8 inch: $7 \times \pi / 4 \times (0.375 \text{ inch} / 12 \text{ inches/ft})^2 = 0.005369 \text{ ft}^2$

**Inside diameter filter surface area for 7 tubes with an inside diameter of 3/8 inch, 40-inches long: $7 \times \pi \times (0.375 \text{ inch}) \times 40 \text{ inches} / 144 \text{ in}^2/\text{ft}^2 = 2.29 \text{ ft}^2$

Exceptions:

- For Run 2.21b (Cleaning): This run was carried out over a three different periods on three days therefore there are two NUMBER COLUMNS: S & T. Column S is continuous and Column T is continuous but starts over for each period. All the columns to the right of Column S are shifted by one.
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R = Q3, FLTR F = Q3, FLTR FLOW (gpm) Flow Rate of the Filtrate Flow (above 1.2 gpm), Installed after 7/10/99

also Run 2.22b has two NUMBER columns (like Run 2.21b) so Exception 1 also applies.

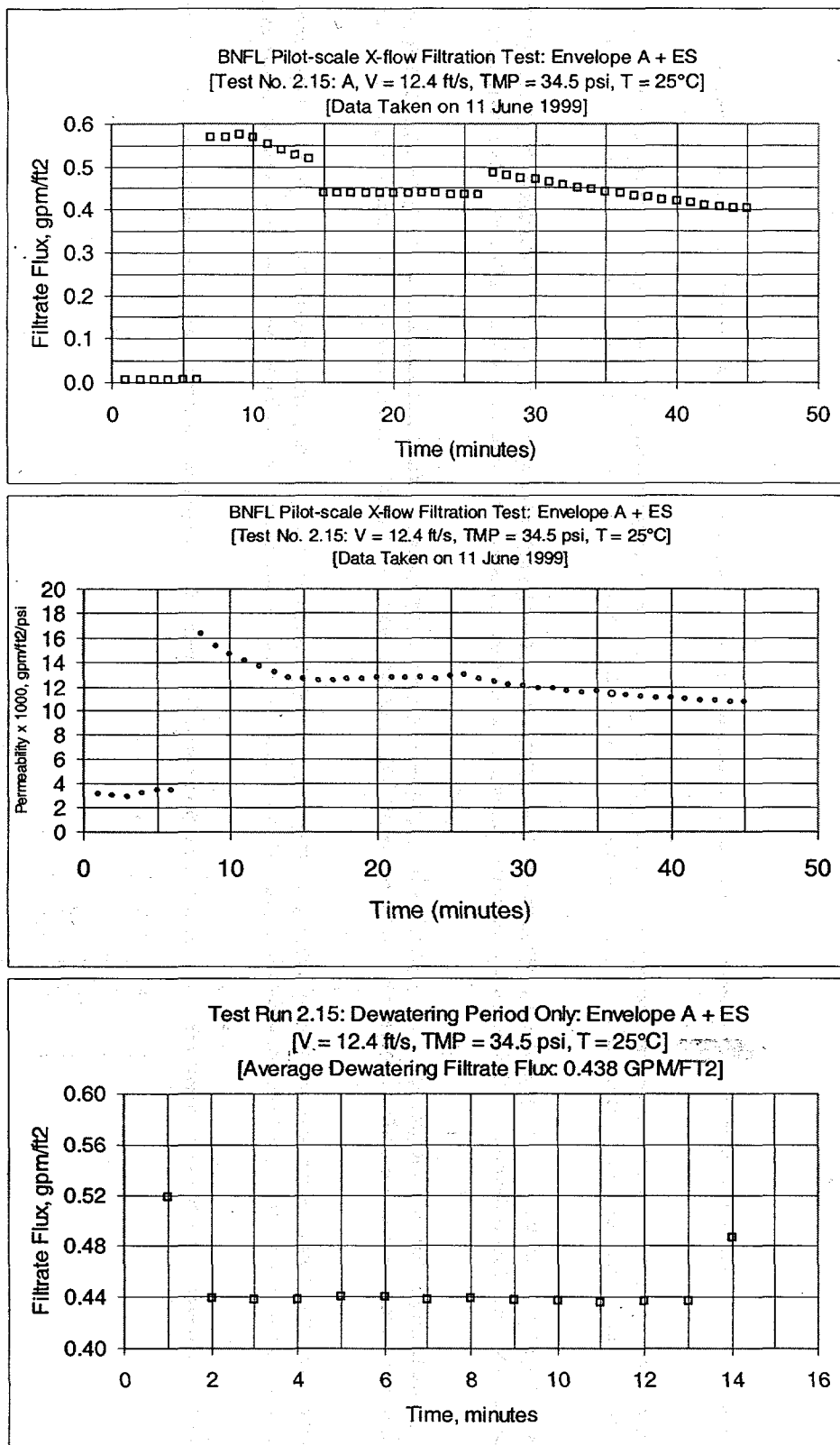


Figure D1: Test Run 2.15, First Wash 1

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.15

DATE		TIME		SOLNO		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR		FLTR	
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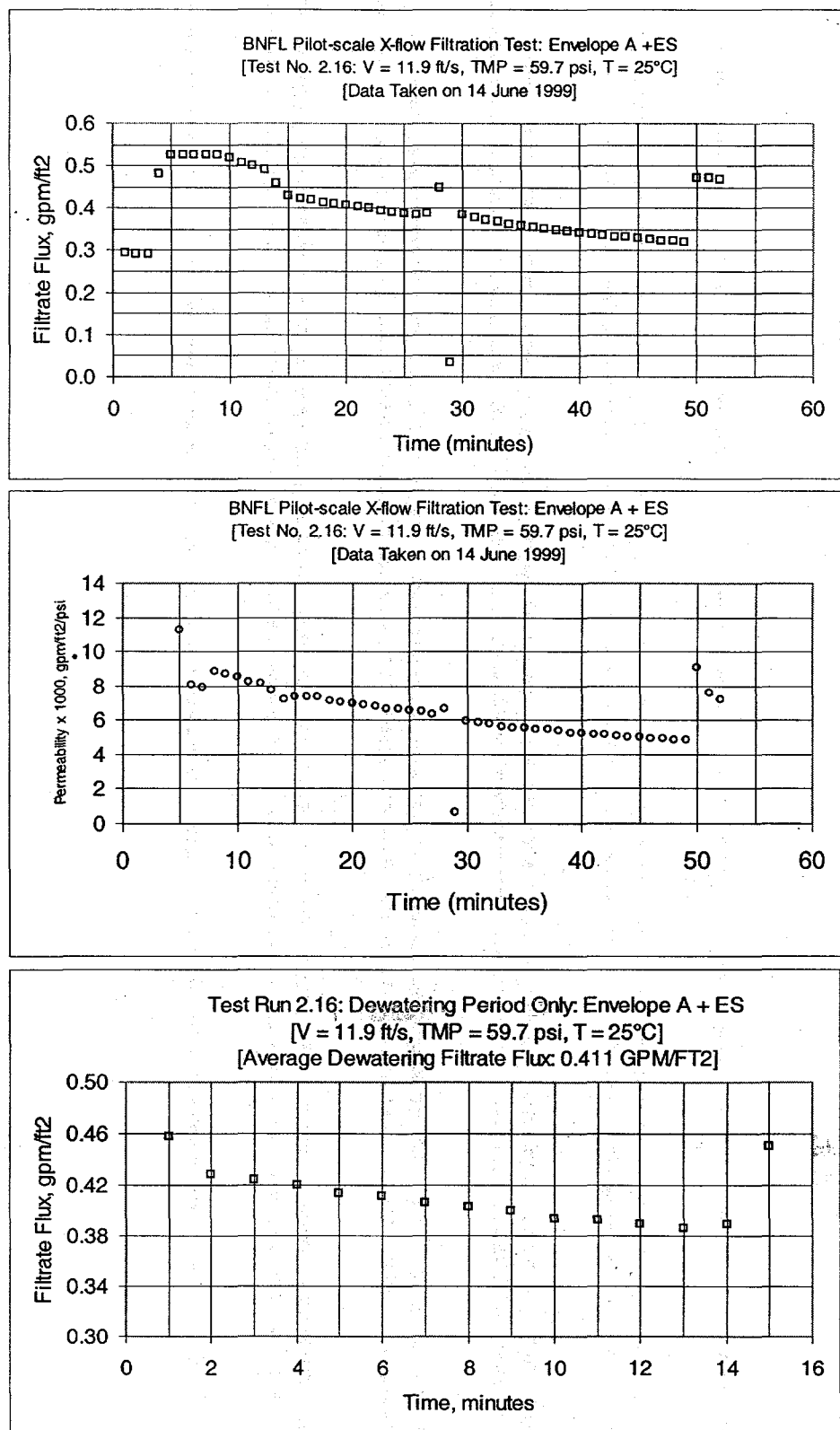


Figure D2: Test Run 2.16, First Wash 2

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.16

A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
DATE	TIME	SOLENOID	FLTRT (deg)	CL LOOP	SL LOOP	UP AMB (°C)	BP AMB (°C)	T6 (deg C)	BP J (°C)	FLTR K (°C)	FLTR L (°C)	FLTR M (°C)	FLTR N (°C)	FLTR O (°C)	FLTR P (°C)	FLTR Q (°C)	FLTR R (°C)	FLTR S (°C)	FLTR T (°C)	FLTR U (°C)	FLTR V (°C)	FLTR W (°C)	FLTR X (°C)	FLTR Y (°C)	FLTR Z (°C)	FLTR AA (°C)
8/14/1999	8:54:06 AM	0	22.759	21.824	23.067	22.139	31.352	-0.002	0.02	-0.024	0.016	-0.119	0.05	-0.08	0.011	0	0	0	0	0	0	0	0	0	0	0
8/14/1999	8:56:23 AM	0	22.759	22.057	21.824	23.067	31.352	-0.002	0.02	-0.024	0.016	-0.119	0.05	-0.08	0.011	0	0	0	0	0	0	0	0	0	0	0
8/14/1999	8:57:25 AM	0	22.759	22.182	21.87	23.132	31.393	-0.003	0.02	-0.024	0.017	-0.119	0.004	-0.08	0.011	0	0	0	0	0	0	0	0	0	0	0
8/14/1999	8:58:23 AM	0	22.678	22.102	21.87	23.212	31.159	-0.003	0.02	-0.024	0.017	-0.119	0.004	-0.08	0.011	0	0	0	0	0	0	0	0	0	0	0
8/14/1999	1:28:18 PM	0	26.485	23.245	26.379	26.516	22.839	32.969	19.881	26.759	2.202	19.321	8.786	0.05	21.715	0.703	0	1	9.0	19.5	1.3	0.307	0.295	0.0151	15.14	12.9
8/14/1999	1:30:19 PM	0	26.499	23.184	26.139	26.516	22.839	33.192	20.952	26.009	2.489	18.712	8.844	0.059	21.731	0.693	0	2	9.0	19.8	1.4	0.303	0.293	0.0148	14.77	12.6
8/14/1999	1:31:19 PM	0	26.339	23.245	25.819	26.516	22.397	33.226	20.642	27.491	2.138	19.591	8.582	0.059	21.654	0.686	0	3	9.0	20.1	1.4	0.300	0.294	0.0146	14.59	12.4
8/14/1999	1:32:19 PM	1	26.054	23.199	25.534	26.391	22.432	33.068	6.478	85.45	4.253	6.44	81.763	80.716	29.994	1.119	0	4	12.4	0.0	0.0	0.488	0.481	25.3269	25326.94	21553.6
8/14/1999	1:33:19 PM	0	25.939	23.28	25.453	26.391	22.432	33.226	48.073	83.866	3.949	45.049	34.443	0.05	30.04	1.216	0	5	12.5	46.6	3.2	0.532	0.525	0.0113	11.28	9.6
8/14/1999	1:34:19 PM	0	26.054	23.234	26.328	26.345	22.432	33.068	86.143	86.793	2.282	64.692	20.128	0.05	22.483	1.216	0	6	9.3	65.4	4.5	0.532	0.527	0.0081	8.05	6.9
8/14/1999	1:35:19 PM	0	25.974	23.154	25.408	26.345	22.447	33.023	89.49	82.921	6.511	63.914	12.933	0.059	30.891	1.216	0	7	15.3	66.7	4.6	0.532	0.526	0.0079	7.88	6.7
8/14/1999	1:36:19 PM	0	25.974	23.154	25.383	26.345	22.708	34.978	86.048	86.048	6.511	63.914	12.933	0.059	30.891	1.216	0	8	12.9	59.4	4.1	0.532	0.526	0.0069	8.87	7.5
8/14/1999	1:37:19 PM	0	25.929	23.189	25.408	26.48	22.863	32.344	82.568	71.965	4.852	58.133	7	0.099	30.317	1.203	0	9	12.6	60.5	4.2	0.532	0.526	0.0067	8.69	7.4
8/14/1999	1:38:19 PM	0	25.929	23.189	25.363	26.48	22.863	32.32	82.784	70.42	4.297	58.978	8.507	0.05	30.01	1.203	0	10	12.5	60.9	4.2	0.525	0.520	0.0065	8.54	7.3
8/14/1999	1:39:20 PM	0	25.929	23.189	25.363	26.62	22.743	33.137	82.85	70.146	4.506	60.396	6.014	0.05	30.01	1.176	0	11	12.5	61.7	4.3	0.513	0.508	0.0062	8.24	7.0
8/14/1999	1:40:20 PM	0	25.849	23.189	25.283	26.62	22.802	33.216	83.663	70.755	4.5	59.823	5.675	0.05	29.825	1.157	0	12	12.4	61.7	4.3	0.505	0.501	0.0061	8.12	6.9
8/14/1999	1:41:20 PM	0	25.849	23.189	25.236	26.54	22.802	33.25	84.5	70.999	4.556	62.393	5.376	0.059	29.702	1.134	0.003	13	12.3	63.4	4.4	0.495	0.492	0.0078	7.75	6.6
8/14/1999	1:42:20 PM	0	25.804	23.269	25.236	26.495	22.378	32.978	84.696	71.243	4.332	61.953	5.274	0.05	29.395	1.056	0	14	12.2	63.3	4.4	0.461	0.458	0.0072	7.23	6.2
8/14/1999	1:43:20 PM	0	25.804	23.224	25.236	26.495	22.378	32.854	89.62	71.823	4.332	62.005	11.068	0.05	29.196	0.988	0	15	12.1	58.0	4.0	0.451	0.428	0.0074	7.36	6.3
8/14/1999	1:44:20 PM	0	25.804	23.224	25.236	26.258	22.537	32.255	89.572	71.518	4.348	55.801	10.978	0.05	29.068	0.978	0.003	16	12.1	57.7	4.0	0.427	0.424	0.0073	7.35	6.3
8/14/1999	1:45:20 PM	0	25.804	23.304	25.236	26.415	22.696	32.255	88.487	70.542	4.181	55.888	10.883	0.05	28.965	0.989	0	17	12.0	57.2	3.9	0.423	0.420	0.0073	7.35	6.3
8/14/1999	1:46:20 PM	0	25.758	23.304	25.236	26.335	22.696	32.3	86.644	72.707	4.436	56.138	10.78	0.059	28.973	0.985	0	18	12.0	58.4	4.0	0.417	0.414	0.0071	7.10	6.0
8/14/1999	1:47:20 PM	0	25.724	23.224	25.236	26.37	22.859	32.141	89.572	71.701	4.508	56.848	10.698	0.059	28.95	0.984	0.003	19	12.0	58.2	4.0	0.414	0.411	0.0071	7.06	6.0
8/14/1999	1:48:21 PM	0	25.724	23.224	25.236	26.37	22.859	32.141	89.572	71.701	4.508	56.848	10.698	0.059	28.95	0.984	0.003	20	12.0	58.5	4.0	0.409	0.407	0.0070	6.95	5.9
8/14/1999	1:49:21 PM	0	25.678	23.234	25.236	26.415	22.859	32.068	86.44	72.971	4.311	57.152	10.878	0.05	28.796	0.939	0.003	21	12.0	58.9	4.1	0.406	0.403	0.0069	6.85	5.8
8/14/1999	1:50:21 PM	0	25.604	23.224	25.157	26.578	22.939	31.936	86.008	71.731	4.261	57.355	10.482	0.05	28.704	0.921	0	22	11.9	58.7	4.0	0.402	0.400	0.0069	6.82	5.8
8/14/1999	1:51:21 PM	0	25.724	23.224	25.236	26.495	22.859	32.141	86.781	72.585	4.228	57.727	10.421	0.05	28.766	0.909	0	23	11.9	59.3	4.1	0.397	0.394	0.0067	6.65	5.7
8/14/1999	1:52:21 PM	0	25.604	23.304	25.157	26.578	22.859	32.141	86.781	72.585	4.228	57.727	10.359	0.05	28.643	0.904	0	24	11.9	59.4	4.1	0.395	0.393	0.0066	6.61	5.6
8/14/1999	1:53:21 PM	0	25.724	23.224	25.236	26.578	22.859	32.062	86.404	72.463	4.221	58.099	10.328	0.05	28.643	0.896	0	25	11.9	59.5	4.1	0.392	0.389	0.0065	6.54	5.6
8/14/1999	1:54:21 PM	0	25.884	23.304	25.396	26.655	22.939	31.963	81.059	72.524	4.269	57.781	10.297	0.05	28.044	0.894	0	26	11.6	59.4	4.1	0.390	0.386	0.0065	6.50	5.5
8/14/1999	1:55:21 PM	0	25.964	23.224	25.584	26.655	23.019	32.062	82.578	74.14	3.942	60.026	10.39	0.05	27.137	0.906	0.003	27	11.3	61.3	4.2	0.396	0.389	0.0064	6.35	5.4
8/14/1999	1:56:21 PM	0	26.189	23.224	25.796	26.735	23.1	31.963	86.467	74.656	4.133	66.619	4.888	0.05	27.23	1.055	0.003	28	11.3	67.5	4.7	0.461	0.450	0.0067	6.67	5.7
8/14/1999	1:57:21 PM	0	26.364	23.224	26.163	26.735	23.1	31.963	83.636	74.567	3.774	52.284	20.036	0.059	26.922	0.981	0	29	11.2	53.1	3.7	0.035	0.034	0.0006	0.65	0.5
8/14/1999	1:58:21 PM	0	26.524	23.33	26.358	26.68	23.018	32.062	86.981	75.42	4.117	63.103	8.105	0.05	27.045	0.913	0.003	30	11.2	64.6	4.5	0.399	0.384	0.0059	5.94	5.1
8/14/1999	1:59:21 PM	0	26.604	23.35	26.507	26.86	23.1	31.79	86.528	75.534	3.973	62.683	8.048	0.05	26.83	0.905	0	31	11.1	64.4	4.4	0.385	0.378	0.0059	5.85	5.0
8/14/1999	2:00:22 PM	0	26.969	23.269	26.502	26.735	23.145	31.472	85.389	74.475	3.822	63.035	7.653	0.05	26.892	0.896	0	32	11.2	64.2	4.4	0.392	0.379	0.0058	5.80	4.9
8/14/1999	2:01:22 PM	0	27.204	23.269	26.962	26.78	23.306	31.631	86.422	75.207	4.053	63.644	7.771	0.059	27.061	0.892	0	33	11.2	65.0	4.5	0.385	0.369	0.0057	5.67	4.8
8/14/1999	2:02:22 PM	0	27.280	23.269	27.167	26.86	23.366	31.79	86.296	75.42	4.125	63.779	7.847	0.05	27.014	0.883	0	34	11.2	65.0	4.5	0.385	0.363	0.0056	5.58	4.7
8/14/1999	2:03:22 PM	0	27.653	23.315	27.327	26.78	23.422	31.785	86.67	75.115	3.79	63.914	7.385	0.05	26.861	0.881	0	35	11.1	65.3	4.5	0.385	0.360	0.0055	5.52	4.7
8/14/1999	2:04:22 PM	0	27.732	23.315	27.486	26.825	23.351	31.914	86.732	75.42	3.942	64.015	7.482	0.05	26.723	0.873	0	36	11.1	65.4	4.5	0.381	0.356	0.0054	5.44	4.6
8/14/1999	2:05:22 PM	0	27.892	23.294	27.648	26.79	23.422	31.721	86.08	74.567	3.694	63.576	7.4	0.05	26.769	0.869	0	37	11.1	64.8	4.5	0.379	0.352	0.0054	5.44	4.6
8/14/1999	2:06:22 PM	0	26.017	23.28	27.771	26.87	23.557	31.8	86.979	75.207	3.934	63.644	7.308	0.05	26.736	0.866	0	38	11.1	65.3	4.5	0.378	0.350	0.0054	5.36	4.6
8/14/1999	2:07:22 PM	0	26.097	23.325	27.93	26.87	23.603	31.959	87.041	75.512	4.063	64.117	7.08	0.059	26.815	0.86	0	39	11.1	65.6	4.5	0.375	0.346	0.0053	5.28	4.6
8/14/1999	2:08:22 PM	0	26.361	23.325	26.135	26.636	23.523	32.355	87.537	76.213	4.005	63.811	7.123	0.05	26.799	0.855	0	40	11							

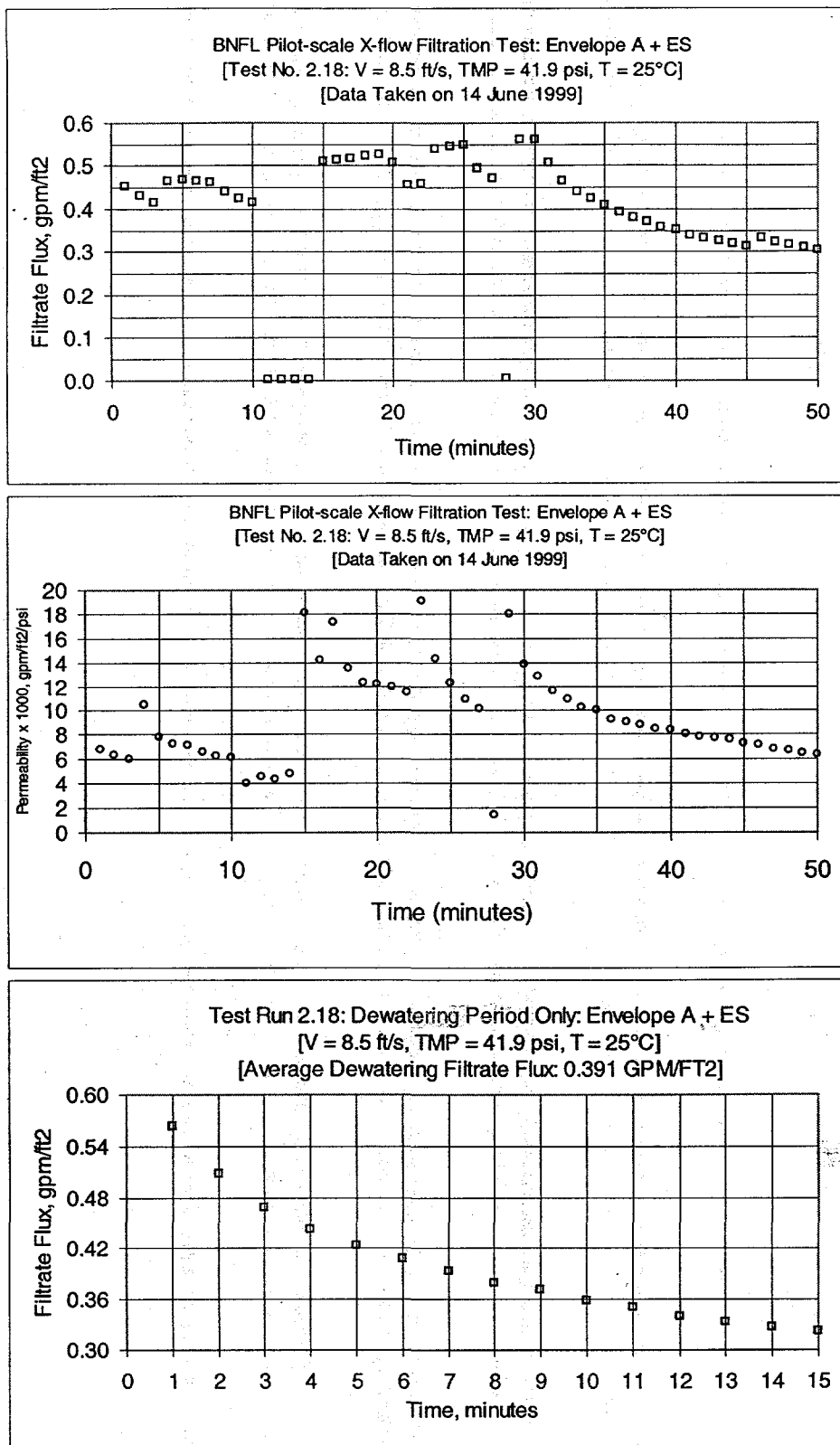


Figure D3: Test Run 2.18, First Wash 3

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.18

DATE		TIME	SOLAR		CLOCK		E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
DATE		TIME	SOLAR		CLOCK		E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
8/14/1999	8:54:05 AM	0	22:756	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	1	10.9	67.0	4.6	0.315	0.454	0.0066	6.78	5.8			
8/14/1999	8:54:23 AM	0	22:759	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	2	10.9	68.1	4.7	0.432	0.455	0.0066	6.80	5.9			
8/14/1999	8:54:41 AM	0	22:762	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	3	10.9	69.2	4.8	0.449	0.456	0.0066	6.82	6.0			
8/14/1999	8:54:59 AM	0	22:765	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	4	10.9	70.3	4.9	0.466	0.457	0.0066	6.84	6.1			
8/14/1999	8:55:17 AM	0	22:768	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	5	10.9	71.4	5.0	0.483	0.458	0.0066	6.86	6.2			
8/14/1999	8:55:35 AM	0	22:771	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	6	10.9	72.5	5.1	0.500	0.459	0.0066	6.88	6.3			
8/14/1999	8:55:53 AM	0	22:774	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	7	10.9	73.6	5.2	0.517	0.460	0.0066	6.90	6.4			
8/14/1999	8:56:11 AM	0	22:777	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	8	10.9	74.7	5.3	0.534	0.461	0.0066	6.92	6.5			
8/14/1999	8:56:29 AM	0	22:780	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	9	10.9	75.8	5.4	0.551	0.462	0.0066	6.94	6.6			
8/14/1999	8:56:47 AM	0	22:783	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	10	10.9	76.9	5.5	0.568	0.463	0.0066	6.96	6.7			
8/14/1999	8:57:05 AM	0	22:786	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	11	10.9	78.0	5.6	0.585	0.464	0.0066	6.98	6.8			
8/14/1999	8:57:23 AM	0	22:789	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	12	10.9	79.1	5.7	0.602	0.465	0.0066	7.00	6.9			
8/14/1999	8:57:41 AM	0	22:792	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	13											
8/14/1999	8:58:00 AM	0	22:795	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	14											
8/14/1999	8:58:18 AM	0	22:798	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	15											
8/14/1999	8:58:37 AM	0	22:801	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	16											
8/14/1999	8:58:55 AM	0	22:804	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	17											
8/14/1999	8:59:14 AM	0	22:807	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	18											
8/14/1999	8:59:32 AM	0	22:810	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	19											
8/14/1999	8:59:51 AM	0	22:813	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	20											
8/14/1999	9:00:09 AM	0	22:816	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	21											
8/14/1999	9:00:28 AM	0	22:819	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	22											
8/14/1999	9:00:46 AM	0	22:822	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	23											
8/14/1999	9:01:05 AM	0	22:825	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	24											
8/14/1999	9:01:23 AM	0	22:828	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	25											
8/14/1999	9:01:42 AM	0	22:831	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	26											
8/14/1999	9:02:00 AM	0	22:834	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	27											
8/14/1999	9:02:19 AM	0	22:837	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	28											
8/14/1999	9:02:37 AM	0	22:840	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	29											
8/14/1999	9:02:56 AM	0	22:843	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	30											
8/14/1999	9:03:14 AM	0	22:846	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	31											
8/14/1999	9:03:33 AM	0	22:849	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	32											
8/14/1999	9:03:51 AM	0	22:852	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	33											
8/14/1999	9:04:10 AM	0	22:855	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	34											
8/14/1999	9:04:28 AM	0	22:858	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	35											
8/14/1999	9:04:47 AM	0	22:861	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	36											
8/14/1999	9:05:05 AM	0	22:864	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	37											
8/14/1999	9:05:24 AM	0	22:867	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	38											
8/14/1999	9:05:42 AM	0	22:870	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	39											
8/14/1999	9:06:01 AM	0	22:873	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	40											
8/14/1999	9:06:19 AM	0	22:876	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	41											
8/14/1999	9:06:38 AM	0	22:879	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	42											
8/14/1999	9:06:56 AM	0	22:882	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	43											
8/14/1999	9:07:15 AM	0	22:885	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	44											
8/14/1999	9:07:33 AM	0	22:888	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	45											
8/14/1999	9:07:52 AM	0	22:891	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	46											
8/14/1999	9:08:10 AM	0	22:894	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	47											
8/14/1999	9:08:29 AM	0	22:897	22:057	21:824	21:067	22:139	31:353	-0.063	0.016	-0.024	0.018	-0.119	0.018	-0.08	0.011	0	48											
8/14/1999	9:08:47 AM	0	22:900	22:057	21:824	21:067	22:139	31:353</																					

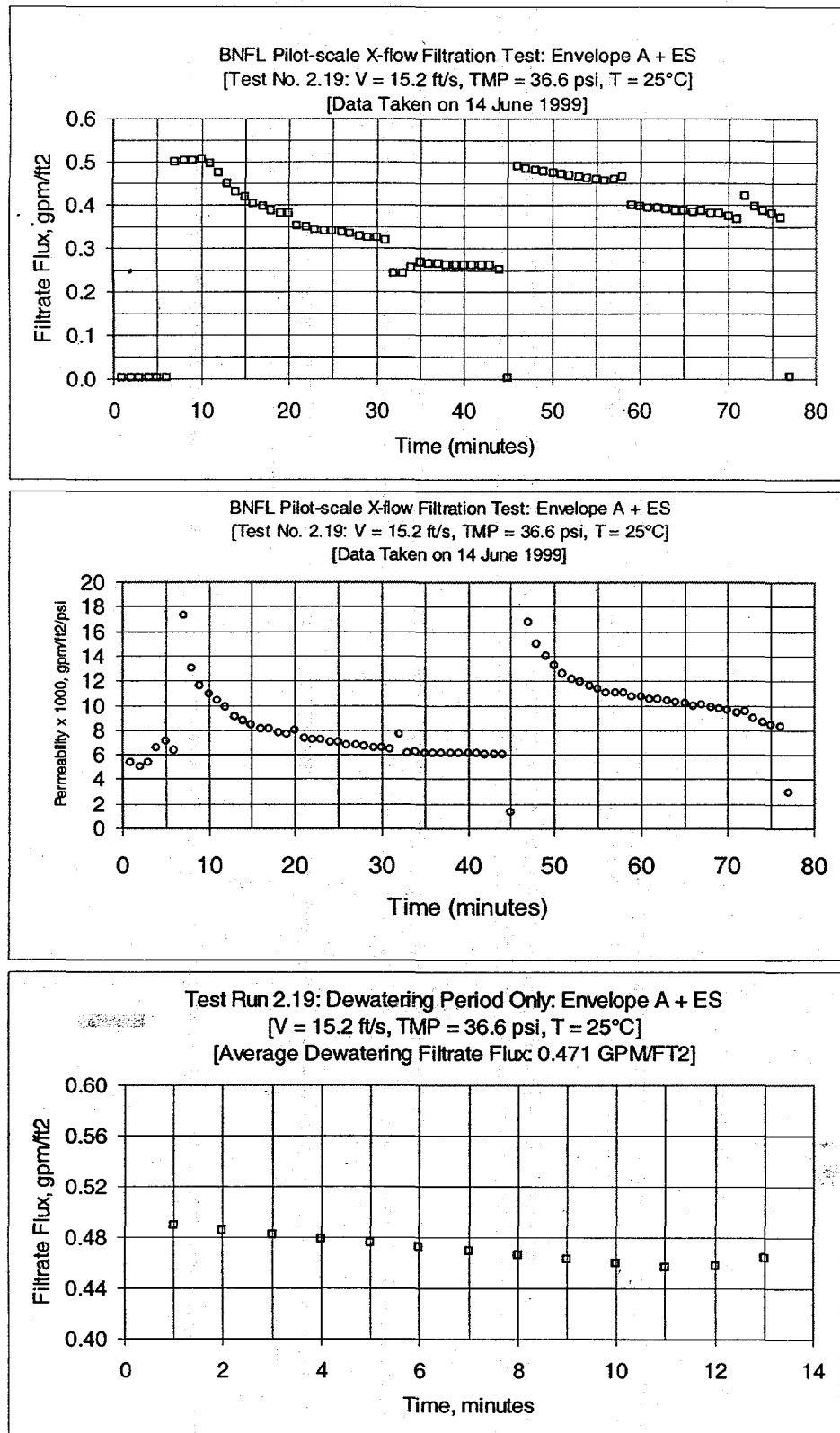


Figure D4: Test Run 2.19, First Wash 4

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.19

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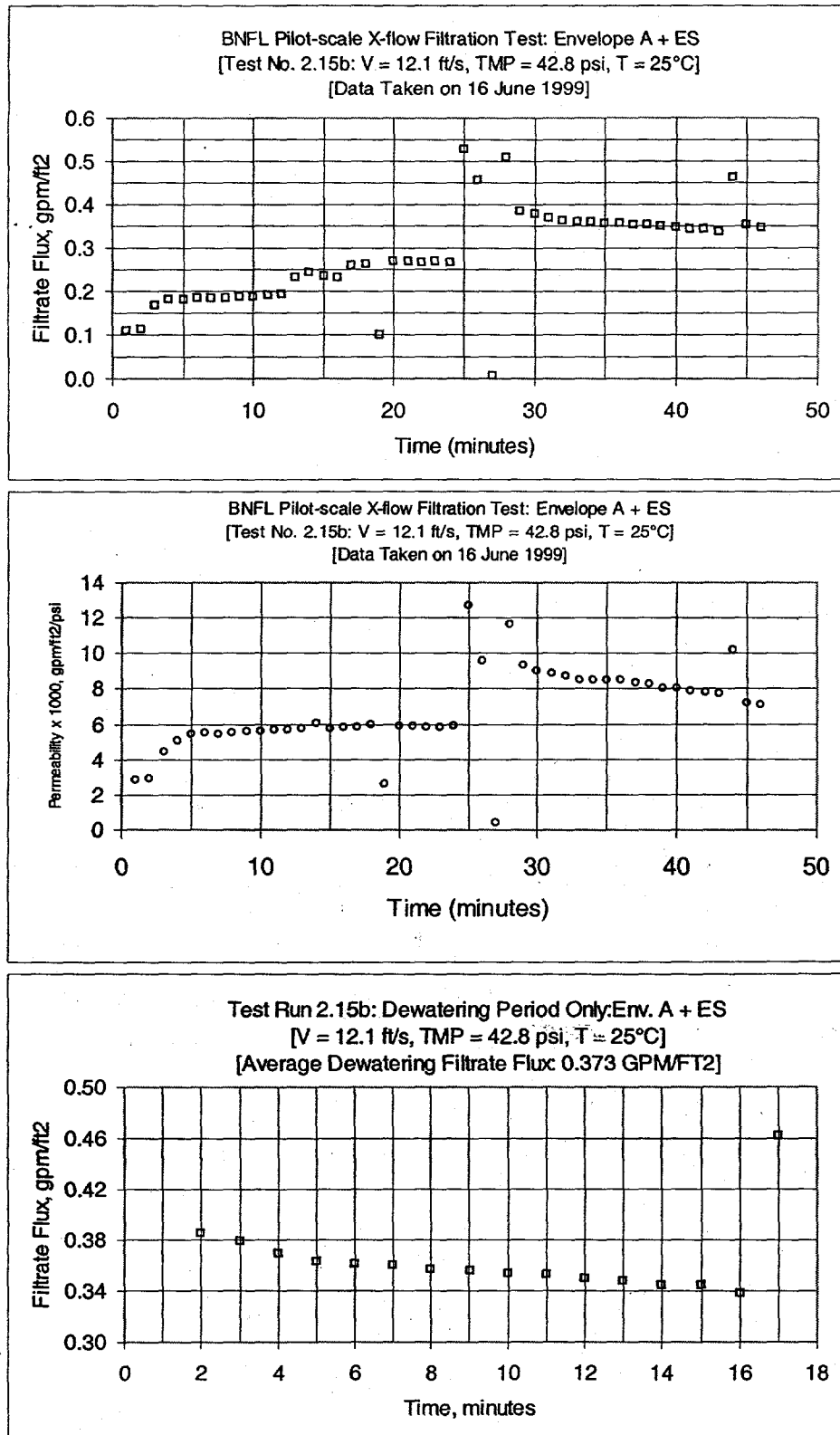


Figure D5: Test Run 2.15b, Second Wash 1

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.15b

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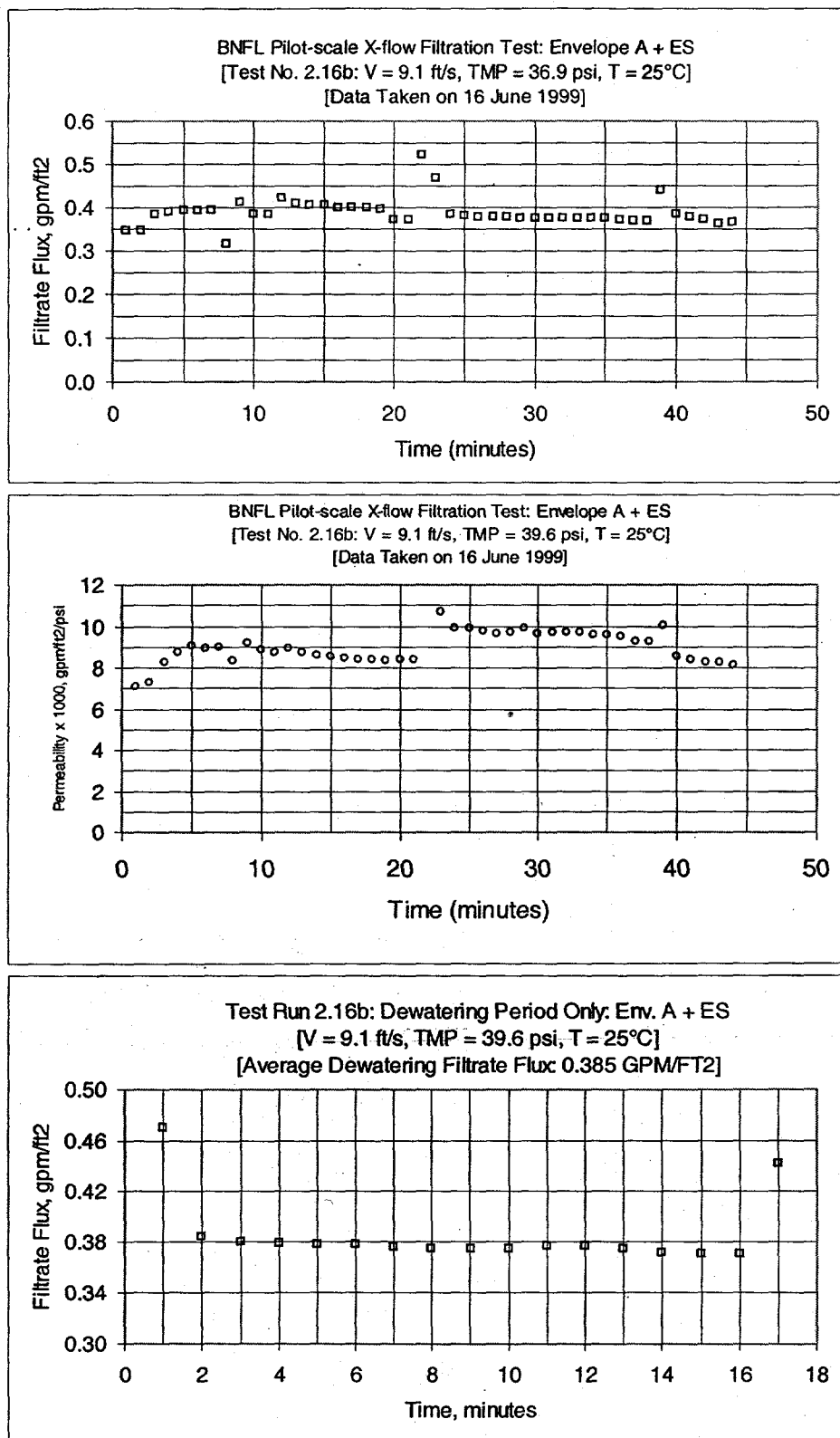


Figure D6: Test Run 2.16b, Second Wash 2

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.16b

A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA	AB	AC	AD	AE	AF	AG	AH	AI	AJ	AK	AL	AM	AN	AO	AP	AQ	AR	AS	AT	AU	AV	AW	AX	AY	AZ	BA	BB	BC	BD	BE	BF	BG	BH	BI	BJ	BK	BL	BM	BN	BO	BP	BQ	BR	BS	BT	BU	BV	BW	BX	BY	BZ	CA	CB	CC	CD	CE	CF	CG	CH	CI	CJ	CK	CL	CM	CN	CO	CP	CQ	CR	CS	CT	CU	CV	CW	CX	CY	CZ	DA	DB	DC	DD	DE	DF	DG	DH	DI	DJ	DK	DL	DM	DN	DO	DP	DQ	DR	DS	DT	DU	DV	DW	DX	DY	DZ	EA	EB	EC	ED	EE	EF	EG	EH	EI	EJ	EK	EL	EM	EN	EO	EP	EQ	ER	ES	ET	EU	EV	EW	EX	EY	EZ	FA	FB	FC	FD	FE	FF	FG	FH	FI	FJ	FK	FL	FM	FN	FO	FP	FQ	FR	FS	FT	FU	FV	FW	FX	FY	FZ	GA	GB	GC	GD	GE	GF	GG	GH	GI	GJ	GK	GL	GM	GN	GO	GP	GQ	GR	GS	GT	GU	GV	GW	GX	GY	GZ	HA	HB	HC	HD	HE	HF	HG	HH	HI	HJ	HK	HL	HM	HN	HO	HP	HQ	HR	HS	HT	HU	HV	HW	HX	HY	HZ	IA	IB	IC	ID	IE	IF	IG	IH	II	IJ	IK	IL	IM	IN	IO	IP	IQ	IR	IS	IT	IU	IV	IW	IX	IY	IZ	JA	JB	JC	JD	JE	JF	JG	JH	JI	JJ	JK	JL	JM	JN	JO	JP	JQ	JR	JS	JT	JU	JV	JW	JX	JY	JZ	KA	KB	KC	KD	KE	KF	KG	KH	KI	KJ	KL	KM	KN	KO	KP	KQ	KR	KS	KT	KU	KV	KW	KX	KY	KZ	LA	LB	LC	LD	LE	LF	LG	LH	LI	LJ	LK	LL	LM	LN	LO	LP	LQ	LR	LS	LT	LU	LV	LW	LX	LY	LZ	MA	MB	MC	MD	ME	MF	MG	MH	MI	MJ	MK	ML	MN	MO	MP	MQ	MR	MS	MT	MU	MV	MW	MX	MY	MZ	NA	NB	NC	ND	NE	NF	NG	NH	NI	NJ	NK	NL	NM	NO	NP	NQ	NR	NS	NT	NU	NV	NW	NX	NY	NZ	OA	OB	OC	OD	OE	OF	OG	OH	OI	OJ	OK	OL	OM	ON	OO	OP	OQ	OR	OS	OT	OU	OV	OW	OX	OY	OZ	PA	PB	PC	PD	PE	PF	PG	PH	PI	PJ	PK	PL	PM	PN	PO	PP	PQ	PR	PS	PT	PU	PV	PW	PX	PY	PZ	QA	QB	QC	QD	QE	QF	QG	QH	QI	QJ	QK	QL	QM	QN	QO	QP	QQ	QR	QS	QT	QU	QV	QW	QX	QY	QZ	RA	RB	RC	RD	RE	RF	RG	RH	RI	RJ	RK	RL	RM	RN	RO	RP	RQ	RR	RS	RT	RU	RV	RW	RX	RY	RZ	SA	SB	SC	SD	SE	SF	SG	SH	SI	SJ	SK	SL	SM	SN	SO	SP	SQ	SR	SS	ST	SU	SV	SW	SX	SY	SZ	TA	TB	TC	TD	TE	TF	TG	TH	TI	TJ	TK	TL	TM	TN	TO	TP	TQ	TR	TS	TT	TU	TV	TW	TX	TY	TZ	UA	UB	UC	UD	UE	UF	UG	UH	UI	UJ	UK	UL	UM	UN	UO	UP	UQ	UR	US	UT	UU	UV	UW	UX	UY	UZ	VA	VB	VC	VD	VE	VF	VG	VH	VI	VJ	VK	VL	VM	VN	VO	VP	VQ	VR	VS	VT	VU	VV	VW	VX	VY	VZ	WA	WB	WC	WD	WE	WF	WG	WH	WI	WJ	WK	WL	WM	WN	WO	WP	WQ	WR	WS	WT	WU	WV	WW	WX	WY	WZ	XA	XB	XC	XD	XE	XF	XG	XH	XI	XJ	XK	XL	XM	XN	XO	XP	XQ	XR	XS	XT	XU	XV	XW	XX	XY	XZ	YA	YB	YC	YD	YE	YF	YG	YH	YI	YJ	YK	YL	YM	YN	YO	YP	YQ	YR	YS	YT	YU	YV	YW	YX	YY	YZ	ZA	ZB	ZC	ZD	ZE	ZF	ZG	ZH	ZI	ZJ	ZK	ZL	ZM	ZN	ZO	ZP	ZQ	ZR	ZS	ZT	ZU	ZV	ZW	ZX	ZY	ZZ																																																													
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100	101	102	103	104	105	106	107	108	109	110	111	112	113	114	115	116	117	118	119	120	121	122	123	124	125	126	127	128	129	130	131	132	133	134	135	136	137	138	139	140	141	142	143	144	145	146	147	148	149	150	151	152	153	154	155	156	157	158	159	160	161	162	163	164	165	166	167	168	169	170	171	172	173	174	175	176	177	178	179	180	181	182	183	184	185	186	187	188	189	190	191	192	193	194	195	196	197	198	199	200	201	202	203	204	205	206	207	208	209	210	211	212	213	214	215	216	217	218	219	220	221	222	223	224	225	226	227	228	229	230	231	232	233	234	235	236	237	238	239	240	241	242	243	244	245	246	247	248	249	250	251	252	253	254	255	256	257	258	259	260	261	262	263	264	265	266	267	268	269	270	271	272	273	274	275	276	277	278	279	280	281	282	283	284	285	286	287	288	289	290	291	292	293	294	295	296	297	298	299	300	301	302	303	304	305	306	307	308	309	310	311	312	313	314	315	316	317	318	319	320	321	322	323	324	325	326	327	328	329	330	331	332	333	334	335	336	337	338	339	340	341	342	343	344	345	346	347	348	349	350	351	352	353	354	355	356	357	358	359	360	361	362	363	364	365	366	367	368	369	370	371	372	373	374	375	376	377	378	379	380	381	382	383	384	385	386	387	388	389	390	391	392	393	394	395	396	397	398	399	400	401	402	403	404	405	406	407	408	409	410	411	412	413	414	415	416	417	418	419	420	421	422	423	424	425	426	427	428	429	430	431	432	433	434	435	436	437	438	439	440	441	442	443	444	445	446	447	448	449	450	451	452	453	454	455	456	457	458	459	460	461	462	463	464	465	466	467	468	469	470	471	472	473	474	475	476	477	478	479	480	481	482	483	484	485	486	487	488	489	490	491	492	493	494	495	496	497	498	499	500	501	502	503	504	505	506	507	508	509	510	511	512	513	514	515	516	517	518	519	520	521	522	523	524	525	526	527	528	529	530	531	532	533	534	535	536	537	538	539	540	541	542	543	544	545	546	547	548	549	550	551	552	553	554	555	556	557	558	559	560	561	562	563	564	565	566	567	568	569	570	571	572	573	574	575	576	577	578	579	580	581	582	583	584	585	586	587	588	589	590	591	592	593	594	595	596	597	598	599	600	601	602	603	604	605	606	607	608	609	610	611	612	613	614	615	616	617	618	619	620	621	622	623	624	625	626	627	628	629	630	631	632	633	634	635	636	637	638	639	640	641	642	643	644	645	646	647	648	649	650	651	652	653	654	655	656	657	658	659	660	661	662	663	664	665	666	667	668	669	670	671	672	673	674	675	676	677	678	679	680	681	682	683	684	685	686	687	688	689	690	691	692	693	694	695	696	697	698	699	700	701	702	703	704	705	706	707	708	709	710	711	712	713	714	715	716	717	718	719	720	721	722	723	724	725	726	727	728	729	730	731	732	733	734	735	736	737	738	739	740	741	742	743	744	745	746	747	748	749	750	751	752	753	754	755	756	757	758	759	7

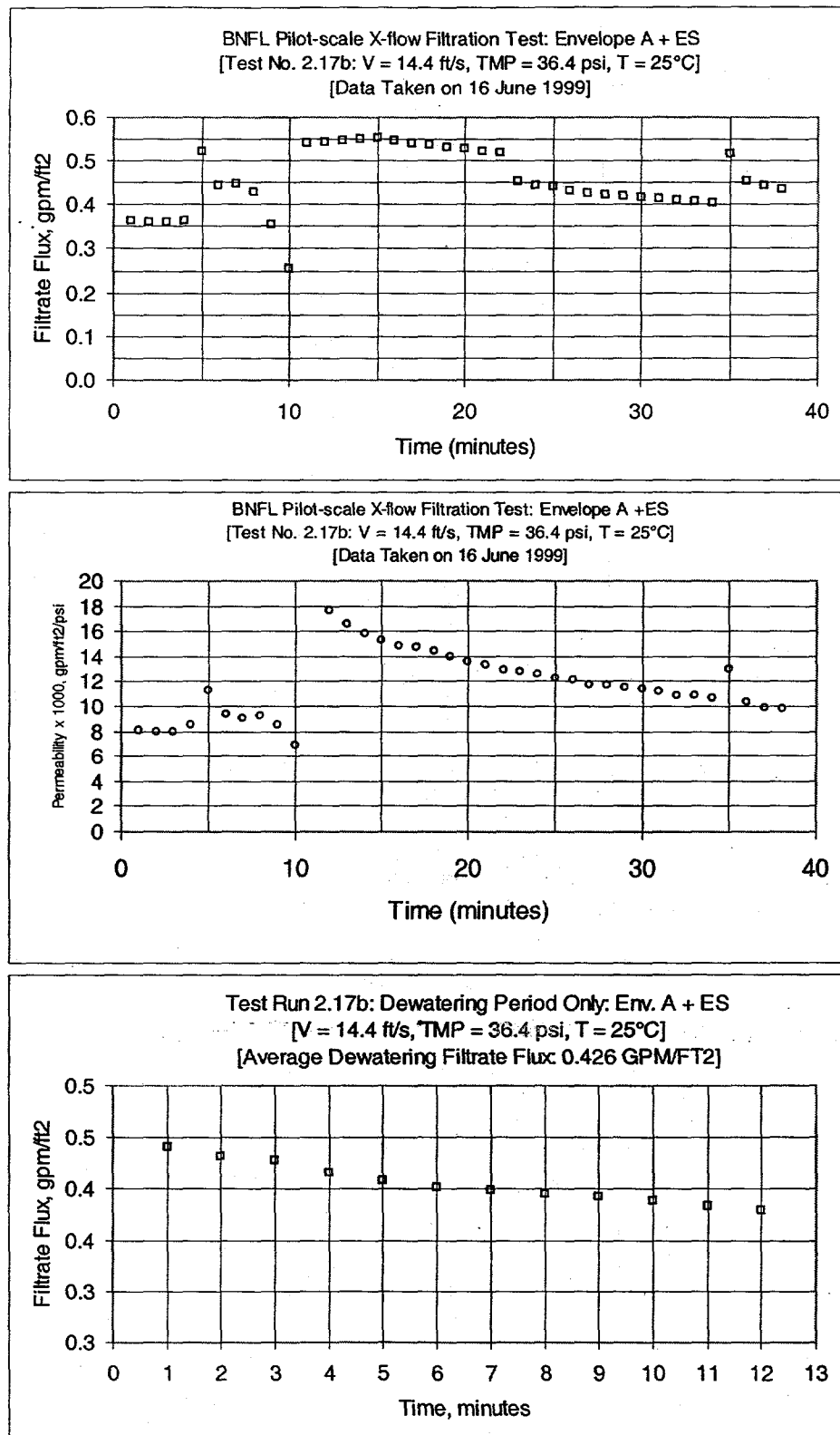


Figure D7: Test Run 2.17b, Second Wash 3

[illegible]

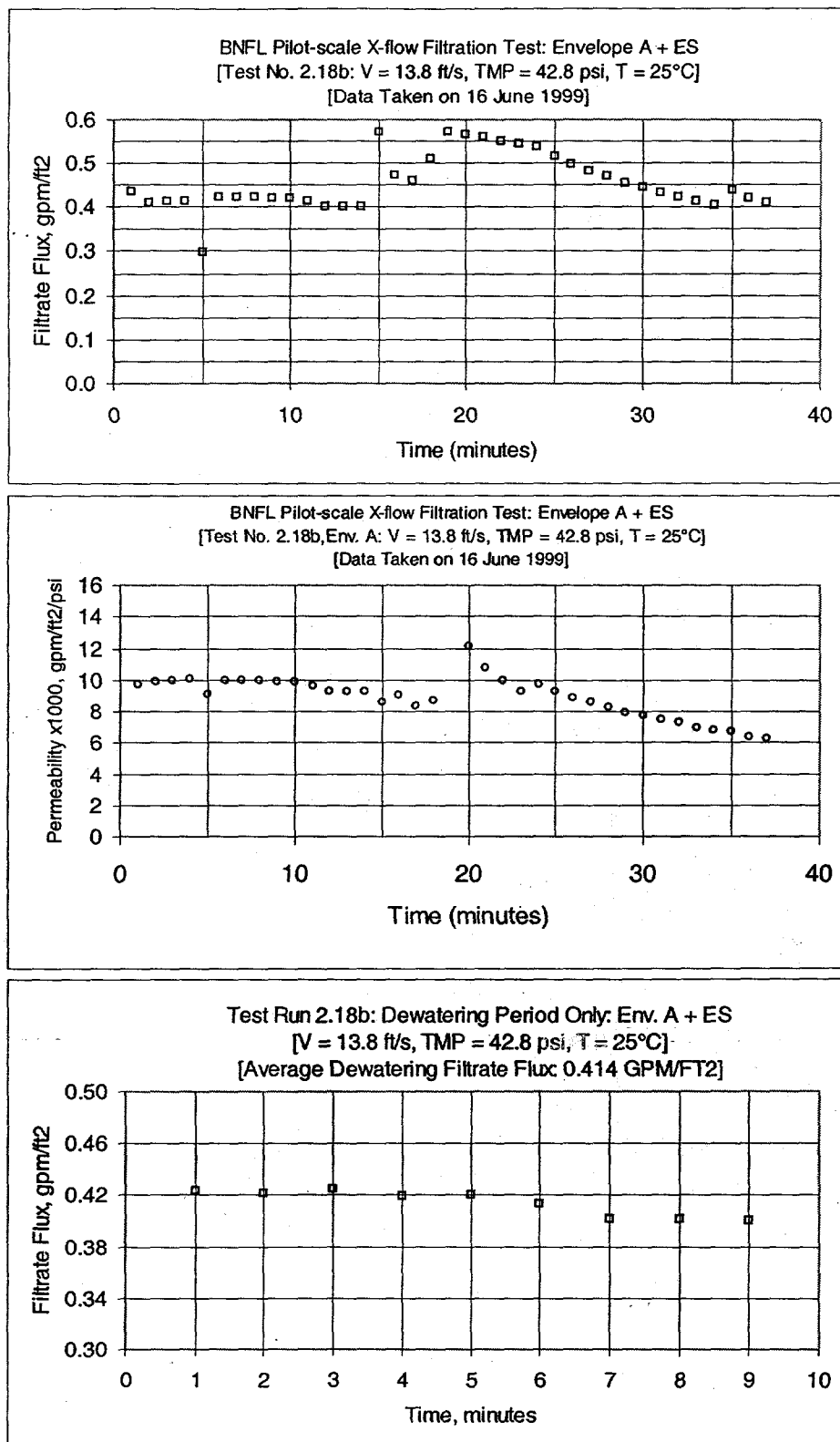


Figure D8: Test Run 2.18b, Second Wash 4

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.18b

A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S	T	U	V	W	X	Y	Z	AA
DATE	TIME	SOLENOID	FLTRT (deg)	CL LOOP	SL LOOP	UP AMB (deg)	BOY AMB	T6 (deg C)	BOY DP (deg)	FLTR (deg)	FLTR DP	TOP DP (deg)	FLTRATE (deg)	HPISTON (deg)	SL FLOW	FLTR FLOW	V9	Number	Vel. ft/s	TMP. psi	TMP. bar	GPM/FT2	PERMADAT2	PERMADAT3	PERMADAT4	PERMADAT5
8/10/1999	8:10:19 AM	0	22.448	22.113	21.603	22.303	21.067	31.645	-0.062	-0.041	0.016	-0.088	-0.135	-0.08	0.011	0	0	1	13.3	44.9	3.1	0.454	0.434	0.0097	9.68	8.2
8/10/1999	8:12:12 AM	0	22.448	22.113	21.603	22.303	21.067	31.645	-0.062	-0.041	0.016	-0.088	-0.135	-0.08	0.011	0	0	2	13.2	41.6	2.9	0.421	0.412	0.0099	9.90	8.4
8/10/1999	8:13:12 AM	0	22.448	22.113	21.558	22.258	21.264	31.001	-0.082	-0.041	0.024	0.05	-0.119	-0.089	-0.08	0.011	0	3	13.5	41.2	2.8	0.416	0.412	0.0100	10.01	8.5
8/10/1999	8:14:12 AM	0	22.448	22.113	21.558	22.258	21.264	30.968	-0.082	-0.041	0.024	0.05	-0.119	-0.089	-0.08	0.011	0	4	13.7	41.0	2.8	0.413	0.413	0.0101	10.07	8.8
8/10/1999	8:15:09 PM	0	25.227	23.333	24.42	24.121	22.199	31.491	44.839	51.78	5.027	40.248	6.168	-0.089	32.851	0.942	0	5	13.8	42.5	2.9	0.417	0.424	0.0100	9.97	8.5
8/10/1999	8:16:09 PM	0	24.907	23.286	24.179	23.995	22.199	31.57	44.353	50.937	4.891	40.417	6.26	-0.089	33.051	0.944	0	6	13.7	42.4	2.9	0.412	0.422	0.0100	9.96	8.5
8/10/1999	8:17:07 PM	0	24.666	23.286	23.904	23.995	22.244	31.57	44.839	51.78	5.027	40.248	6.168	-0.089	32.851	0.942	0	7	13.6	42.4	2.9	0.411	0.424	0.0100	10.01	8.5
8/10/1999	8:18:07 PM	0	24.425	23.333	23.663	24.076	22.154	31.411	44.756	51.273	4.803	40.282	6.075	-0.089	32.913	0.925	0	8	13.7	42.5	2.9	0.404	0.419	0.0098	9.86	8.4
8/10/1999	8:19:07 PM	0	24.185	23.286	23.377	24.076	22.199	31.57	44.801	51.273	4.939	40.2	5.963	-0.089	32.867	0.919	0	9	13.6	42.6	2.9	0.401	0.420	0.0099	9.85	8.4
8/10/1999	8:20:07 PM	0	23.944	23.333	23.218	23.995	22.325	31.65	45.655	51.78	5.096	40.383	5.705	-0.089	33.251	0.9	0	10	13.6	43.0	3.0	0.393	0.413	0.0096	9.61	8.2
8/10/1999	8:21:07 PM	0	23.703	23.286	22.975	24.04	22.36	31.729	45.562	51.458	5.13	40.756	5.821	-0.089	33.312	0.899	0	11	13.8	43.2	3.0	0.379	0.402	0.0093	9.31	7.9
8/10/1999	8:22:07 PM	0	23.542	23.286	22.815	23.915	22.36	31.65	45.672	51.608	5.268	40.857	5.459	-0.089	33.573	0.864	0	12	13.9	43.4	3.0	0.377	0.401	0.0093	9.25	7.9
8/10/1999	8:23:07 PM	0	23.382	23.286	22.493	23.915	22.325	31.729	45.5	51.608	5.268	40.756	5.459	-0.089	33.573	0.864	0	13	13.9	43.1	3.0	0.373	0.401	0.0093	9.29	7.9
8/10/1999	8:24:07 PM	0	23.141	23.286	22.493	23.995	22.199	31.729	45.5	51.608	5.268	40.756	5.459	-0.089	33.573	0.864	0	14	13.9	43.1	3.0	0.373	0.401	0.0093	9.29	7.9
8/10/1999	8:25:07 PM	0	23.06	23.286	22.493	23.995	22.199	31.729	45.5	51.608	5.268	40.756	5.459	-0.089	33.573	0.864	0	15	13.9	43.1	3.0	0.373	0.401	0.0093	9.29	7.9
8/10/1999	8:26:07 PM	0	23.141	23.286	22.493	23.915	22.119	31.808	45.48	52.889	6.058	49.681	7.061	-0.089	37.183	1.01	0	16	14.4	52.6	3.6	0.441	0.474	0.0090	9.00	7.3
8/10/1999	8:27:07 PM	0	23.141	23.286	22.493	23.915	22.119	31.729	45.503	53.095	6.846	50.095	6.846	-0.089	28.612	0.979	0.003	17	11.9	54.6	3.8	0.427	0.459	0.0084	8.37	7.1
8/10/1999	8:28:07 PM	0	23.141	23.286	22.493	23.915	22.119	31.808	45.48	52.889	6.058	49.681	7.061	-0.089	28.612	0.979	0.003	18	12.2	58.6	4.1	0.475	0.510	0.0087	8.66	7.4
8/10/1999	8:29:07 PM	0	23.06	23.286	22.413	23.915	22.038	31.888	45.48	52.889	6.058	49.681	7.061	-0.089	30.685	1.218	0	19	12.7	58.6	4.1	0.475	0.510	0.0087	8.66	7.4
8/10/1999	8:30:07 PM	0	23.06	23.286	22.734	23.915	22.038	31.888	45.48	52.889	6.058	49.681	7.061	-0.089	30.685	1.218	0	20	12.7	58.6	4.1	0.475	0.510	0.0087	8.66	7.4
8/10/1999	8:31:07 PM	0	23.382	23.286	23.218	23.915	21.958	31.888	45.48	52.889	6.058	49.681	7.061	-0.089	30.685	1.218	0	21	12.5	52.2	3.6	0.532	0.559	0.0107	10.72	9.1
8/10/1999	8:32:07 PM	0	23.588	23.243	23.698	23.995	22.073	31.922	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	22	12.4	55.2	3.8	0.532	0.552	0.0100	10.00	8.6
8/10/1999	8:33:07 PM	0	24.22	23.286	24.215	23.87	21.960	31.922	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	23	12.2	58.6	4.0	0.532	0.544	0.0093	9.27	7.9
8/10/1999	8:34:07 PM	0	24.701	23.243	24.698	23.79	22.073	31.922	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	24	12.3	55.0	3.8	0.532	0.536	0.0097	9.75	8.3
8/10/1999	8:35:07 PM	0	25.022	23.286	25.176	23.79	22.154	31.922	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	25	12.3	55.0	3.8	0.532	0.536	0.0097	9.75	8.3
8/10/1999	8:36:07 PM	0	25.663	23.196	25.737	23.79	21.963	31.922	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	26	12.2	56.3	3.9	0.509	0.499	0.0086	8.56	7.9
8/10/1999	8:37:07 PM	0	26.143	23.243	26.297	23.79	22.073	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	27	12.3	56.2	3.9	0.499	0.482	0.0086	8.56	7.9
8/10/1999	8:38:07 PM	0	26.578	23.196	26.656	23.709	22.154	32.002	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	28	12.1	56.8	3.9	0.495	0.470	0.0083	8.27	7.0
8/10/1999	8:39:07 PM	0	27.297	23.196	27.53	23.744	21.948	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	29	12.0	57.7	4.0	0.488	0.455	0.0079	7.88	6.7
8/10/1999	8:40:07 PM	0	27.776	23.278	28.043	23.684	21.948	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	30	12.1	57.1	3.9	0.483	0.444	0.0078	7.77	6.6
8/10/1999	8:41:07 PM	0	28.529	23.278	28.726	23.684	21.963	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	31	12.0	58.1	4.0	0.480	0.433	0.0075	7.46	6.3
8/10/1999	8:42:07 PM	0	29.131	23.196	29.362	23.744	21.963	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	32	12.0	57.8	4.0	0.476	0.422	0.0073	7.30	6.2
8/10/1999	8:43:07 PM	0	29.644	23.278	30.078	23.744	21.963	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	33	11.8	59.1	4.1	0.476	0.414	0.0070	7.00	6.0
8/10/1999	8:44:07 PM	0	30.36	23.153	30.783	23.698	22.224	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	34	11.8	59.3	4.1	0.476	0.405	0.0068	6.84	5.8
8/10/1999	8:45:07 PM	0	31.12	23.196	31.483	23.78	22.36	31.957	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	35	11.7	64.9	4.5	0.523	0.437	0.0067	6.74	5.7
8/10/1999	8:46:07 PM	0	31.789	23.196	32.097	23.825	22.43	30.722	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	36	11.7	65.6	4.5	0.511	0.421	0.0064	6.41	5.5
8/10/1999	8:47:07 PM	0	32.389	23.196	32.538	23.825	22.691	30.887	45.966	56.56	3.822	53.366	11.407	-0.089	29.979	1.218	0	37	11.7	65.7	4.5	0.505	0.411	0.0063	6.25	5.3
47 Values	Average		27.9	23.2	27.9	23.9	22.2	31.5	45.9	56.9	4.2	52.2	10.7	-0.1	29.8	1.074	0.0		12.4	54.0	3.7	0.469	0.432	0.008	8.2	7.0
48 For	Maximum		32.4	23.3	32.6	24.2	22.6	32.0	46.3	57.4	5.1	64.3	15.5	0.0	32.9	1.197	0.0		13.7	65.7	4.5	0.523	0.517	0.010	10.1	8.6
49 Close-loop	Median		27.1	23.3	27.2	23.8	22.2	31.8	45.8	56.4	4.0	55.5	12.6	-0.1	29.2	1.103	0.0		12.1	57.0	3.9	0.482	0.427	0.008	8.1	6.9
50 operation	Minimum		25.0	23.2	24.7	23.7	21.9	30.7	45.2	51.2	3.7	30.1	4.9	-0.1	28.1	0.877	0.0		11.7	52.7	2.3	0.296	0.298	0.006	6.3	5.9
51 Std Dev			2.2	0.1	2.5	0.2	0.2	0.4	8.9	9.4	0.4	9.6	3.2	0.0	1.7	0.122	0.0		0.7	9.3	0.6	0.053	0.045	0.001	1.3	1.1
52 Number of Points Used			18	18	18	18	18	18	18	18	18	18	18	18	18	18	18		18	18	18	18	18	18	18	18
54 Values	Average		24.2	23.3	23.4	24.0	22.3	31.8	45.0	51.4	5.0	40.5	5.9	-0.1	33.1	0.908	0.0		13.8	42.8	3.0	0.396	0.414	0.010	9.7	8.2
55 During	Maximum		25.2	23.3	24.4	24.1	22.4	31.7	45.9	51.8	5.3	40.9	6.4	0.0	33.8	0.955	0.0		13.9	43.4	3.0	0.401	0			

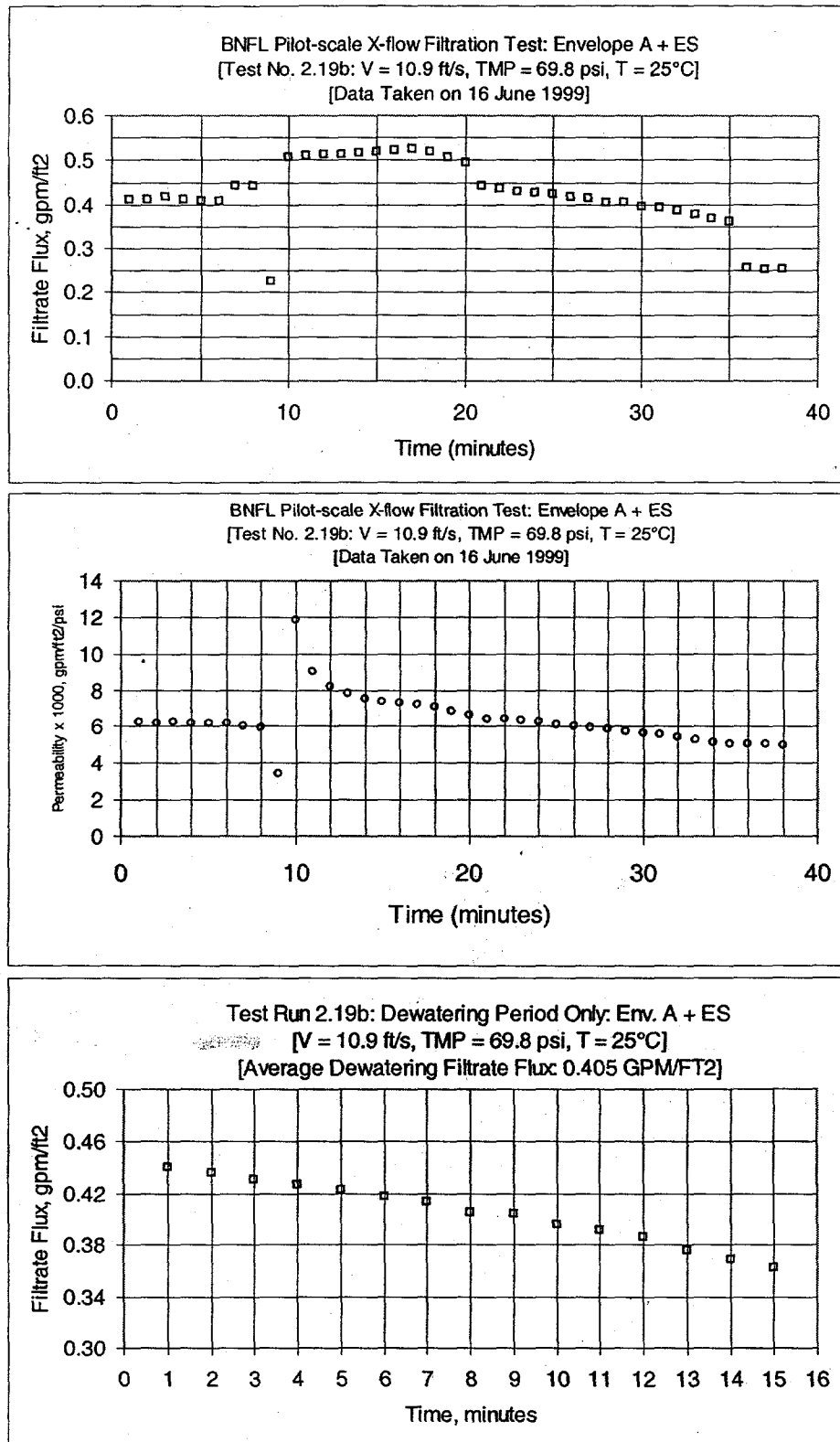


Figure D9: Test Run 2.19b, Wash 5

Pilot Scale X-Flow Filtration Test: Env. A, Run 2.19b

DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F		G		H		I		J		K		L		M		N		O		P		Q		R		S		T		U		V		W		X		Y		Z		AA	
DATE		TIME		B		SOLVENT		FLOW RATE (cc/L)		E		F																																											

APPENDIX E

ANALYTICAL DATA

Appendix Contents

1. Eleven pages of Table E1 contain all of the analytical data.
2. Slurry Rheology: Fig. E1, Run 2.13; Fig. E2, Run 2.14b, Fig. E3, Run 2.20b
2. Graphs of selected chemical element concentrations throughout the test by molarity
Figures E4-E17 are Al, Ca, Cl, Cr, F, Fe, K, Mn, Mo, Na, Ni, P, Pb, and Si
3. Graphs of selected chemical compounds concentration throughout the test by molarity.
Figures E18-E20 are: Oxalate, Phosphate, and Sulfate
4. Graphs and tabular data on the particle distributions throughout the test
Figure E21 is: particle distribution from a real waste sample
Figures E22A, E22B, to E29A, and E29B are for test runs: Pre-test, 2.01, 2.13, 2.14, 2.16, 2.14b, 2.16b, 2.

Special Notes:

- a. There are no measurement uncertainties listed because the measurement uncertainties for analytical data are beyond the scope and control of this task. There is reason to believe that all analytical data can be at least 15% accurate but no quantitative data are given to this effect. Density and filtrate viscosity are the only slurry property data that were obtained at the test rig location and the uncertainty of those data can be stated as:
Density: $\leq 0.5\%$ of reading by calibration
Viscosity: 0.34 wt% of reading by manufacturer's statement.
- b. Only three figure, E1, E2, E3 are given for the slurry rheology because the rheology was similar for all samples. The slurry basically act as a Newtonian fluid but at the highest solids loading there is a small amount of yield stress which drops off very rapidly after the slurry is put into motion.
- c. Each particle analysis was done by a Volume and a Number distribution, thus there are two figures for each, e.g., 19A and 19B.)

	A	B	C	D	E	F
1	TEST RUN ----->		Most Recent Entry Date		2.00	2.00
2	BNFL Sample ID ----->		February/22/2000	Pre-Test Sample	BNF-SXF2055-A+ES_01a	BNF-SXF2055-A+ES_01b
3	ADS Sample ID ----->			3-126787	3-127887	3-127888
4	Type Sample ----->			slurry	slurry loop	slurry loop
5	Sample Size ----->	mL		125	15	15
6	Measurement(s) Made ----->	(SEE NOMENCLATURE TO EXPLAIN LETTERS)			SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS	SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS
7	Item Measured	Units	Analyst Name			
8	Density	g/mL	Thermal Fluids Lab	1.20	water before test 2.00	water after test 2.00
9	Al	ug/mL	Frank Pennebaker	15650	<0.6	<0.6
10	B	ug/mL	Frank Pennebaker	15.7	<0.3	<0.3
11	Ba	ug/mL	Frank Pennebaker	<0.5	<0.1	<0.1
12	Ca	ug/mL	Frank Pennebaker	39.1	<0.4	<0.4
13	Cd	ug/mL	Frank Pennebaker	<0.5	<0.1	<0.1
14	Cl	ug/mL	Robert Ray/Joyce Cartledge	3766	N/A	N/A
15	Cl Sample	ug/mL	Robert Ray/Sarah Brown	N/A	342.47	N/A
16	Co	ug/mL	Frank Pennebaker	<0.5	<0.1	<0.1
17	Cr	ug/mL	Frank Pennebaker	329	<0.1	<0.1
18	Cu	ug/mL	Frank Pennebaker	<0.5	<0.1	<0.1
19	F (Fluoride) -(only rough rdg)	ug/mL	Robert Ray/Joyce Cartledge	<20	N/A	N/A
20	F Sample	ug/mL	Robert Ray/Sarah Brown	N/A	<1	N/A
21	Fe	ug/mL	Frank Pennebaker	25.1	<0.2	<0.2
22	HCOO (Formate)	ug/mL	Robert Ray/Joyce Cartledge	1447	N/A	N/A
23	K	ug/mL	Sarah Brown	N/A	0.918	N/A
24	La	ug/mL	Frank Pennebaker	N/A	<0.28	<0.28
25	Li	ug/mL	Frank Pennebaker	<6.6	<1.2	<1.2
26	Mg	ug/mL	Frank Pennebaker	6.2	<0.1	<0.1
27	Mn	ug/mL	Frank Pennebaker	7.8	<0.1	<0.1
28	Mo	ug/mL	Frank Pennebaker	30.4	<0.1	<0.1
29	Na	ug/mL	Frank Pennebaker	98700	14	12
30	Ni	ug/mL	Frank Pennebaker	<0.6	<0.15	<0.15
31	NO2 (Nitrite)	ug/mL	Robert Ray/Joyce Cartledge	44946	N/A	N/A
32	NO3 (Nitrate)	ug/mL	Robert Ray/Joyce Cartledge	57471	N/A	N/A
33	C2O4 (Oxalate)	ug/mL	Robert Ray/Joyce Cartledge	743	N/A	N/A
34	P	ug/mL	Frank Pennebaker	69.3	<2	<2
35	PO4 (Phosphate)	ug/mL	Robert Ray/Joyce Cartledge	405	N/A	N/A
36	Pb	ug/mL	Frank Pennebaker	<5	<1	<1
37	Si	ug/mL	Frank Pennebaker	126	<1	<1
38	Sn	ug/mL	Frank Pennebaker	<4	<0.8	<0.8
39	SO4 (Sulfate)	ug/mL	Robert Ray/Joyce Cartledge	343	N/A	N/A
40	Sr	ug/mL	Frank Pennebaker	<1	<0.1	<0.1
41	Ti	ug/mL	Frank Pennebaker	<0.5	<0.1	<0.1
42	V	ug/mL	Frank Pennebaker	<1.5	<0.1	<0.1
43	Zn	ug/mL	Frank Pennebaker	11.1	<0.1	<0.1
44	Zr	ug/mL	Frank Pennebaker	<1.5	<0.3	<0.3
45	Total Organic Carbon	ug/mL	Robert Ray	1509	35.24	N/A
46	Total Inorganic Carbon	ug/mL	Robert Ray	1924	0.41	N/A
47	Suspended Solids	wt%	Beverly Burch	N/A	<0.003	N/A
48	Total Solids	wt%	Beverly Burch	N/A	N/A	N/A
49	Mean Particle Size by Volume	micron	Don Blankenship	2.4/309	N/A	N/A
50	Mean Particle Size by Number	micron	Don Blankenship	N/A	N/A	N/A
51	Kinematic Viscosity	cSt	CONE/TNX-CAPILLARY/TFL	N/A	N/A	N/A
52	Dynamic Viscosity	cP	Calculated	N/A	N/A	N/A
53	Comment			bimodel particle distribution	water before test	water after test

Table E1: Analytical – All data, Page1

	G	H	I	J	K	L
1	TEST RUN ----->		2.01	2.01	2.01	2.01
2	BNFL Sample ID ----->		Unplanned Sample	BNF-SXF2055-A+ES_02	BNF-SXF2055-A+ES_03	No Sample Kept
3	ADS Sample ID ----->		TNX Sample/No Number	3-127890	3-127891	No Sample Number
4	Type Sample ----->		slurry	slurry	slurry	filtrate
5	Sample Size ----->	mL	150	50	15	100mL/returned to mixture
6	Measurement(s) Made ----->		TS/SS/VISCOSITY/DENSITY	MICROTRAC	TS/SS	DENSITY ONLY
7	Item Measured	Units				
8	Density	g/mL	1.240	1.232	1.232	1.231
9	Al	ug/mL	N/A	N/A	N/A	N/A
10	B	ug/mL	N/A	N/A	N/A	N/A
11	Ba	ug/mL	N/A	N/A	N/A	N/A
12	Ca	ug/mL	N/A	N/A	N/A	N/A
13	Cd	ug/mL	N/A	N/A	N/A	N/A
14	Cl	ug/mL	N/A	N/A	N/A	N/A
15	Cl Sample	ug/mL	N/A	N/A	N/A	N/A
16	Co	ug/mL	N/A	N/A	N/A	N/A
17	Cr	ug/mL	N/A	N/A	N/A	N/A
18	Cu	ug/mL	N/A	N/A	N/A	N/A
19	F (Fluoride) -(only rough rdg)	ug/mL	N/A	N/A	N/A	N/A
20	F Sample	ug/mL	N/A	N/A	N/A	N/A
21	Fe	ug/mL	N/A	N/A	N/A	N/A
22	HCOO (Formate)	ug/mL	N/A	N/A	N/A	N/A
23	K	ug/mL	N/A	N/A	N/A	N/A
24	La	ug/mL	N/A	N/A	N/A	N/A
25	Li	ug/mL	N/A	N/A	N/A	N/A
26	Mg	ug/mL	N/A	N/A	N/A	N/A
27	Mn	ug/mL	N/A	N/A	N/A	N/A
28	Mo	ug/mL	N/A	N/A	N/A	N/A
29	Na	ug/mL	N/A	N/A	N/A	N/A
30	Ni	ug/mL	N/A	N/A	N/A	N/A
31	NO2 (Nitrite)	ug/mL	N/A	N/A	N/A	N/A
32	NO3 (Nitrate)	ug/mL	N/A	N/A	N/A	N/A
33	C2O4 (Oxalate)	ug/mL	N/A	N/A	N/A	N/A
34	P	ug/mL	N/A	N/A	N/A	N/A
35	PO4 (Phosphate)	ug/mL	N/A	N/A	N/A	N/A
36	Pb	ug/mL	N/A	N/A	N/A	N/A
37	Si	ug/mL	N/A	N/A	N/A	N/A
38	Sn	ug/mL	N/A	N/A	N/A	N/A
39	SO4 (Sulfate)	ug/mL	N/A	N/A	N/A	N/A
40	Sr	ug/mL	N/A	N/A	N/A	N/A
41	Ti	ug/mL	N/A	N/A	N/A	N/A
42	V	ug/mL	N/A	N/A	N/A	N/A
43	Zn	ug/mL	N/A	N/A	N/A	N/A
44	Zr	ug/mL	N/A	N/A	N/A	N/A
45	Total Organic Carbon	ug/mL	N/A	N/A	N/A	N/A
46	Total Inorganic Carbon	ug/mL	N/A	N/A	N/A	N/A
47	Suspended Solids	wt%	0.52	N/A	0.4509	N/A
48	Total Solids	wt%	30.57	N/A	28.26	N/A
49	Mean Particle Size by Volume	micron	N/A	2.59	N/A	N/A
50	Mean Particle Size by Number	micron	N/A	1.05	N/A	N/A
51	Kinematic Viscosity	cSt	2.4	N/A	N/A	N/A
52	Dynamic Viscosity	cP	3.0	N/A	N/A	N/A
53	Comment		HAAKE/SPINNING CONE			

Table E1: Analytical – All data, Page2

	M	N	O	P	Q	R
1	TEST RUN		2.01	2.13	2.13	2.13
2	BNFL Sample ID		BNF-SXF2055-A+ES_04	BNF-SXF2055-A+ES_02b	BNF-SXF2055-A+ES_03b	Unplanned Sample
3	ADS Sample ID		3-127889	3-128290	3-128291	TNX Sample/No Number
4	Type Sample		filtrate	slurry	slurry	slurry
5	Sample Size	ml	15	50	15	150
6	Measurement(s) Made		SS/CP-ES/AA/TIC-TOC/SE/C-ANIONS	MICROTRAC	TS/SS	TS/SS/VISCOSITY/DENSITY
7	Item Measured	Units				
8	Density	g/mL	N/A	1.232	1.240	1.256
9	Al	ug/mL	17900	N/A	N/A	N/A
10	B	ug/mL	25	N/A	N/A	N/A
11	Ba	ug/mL	<0.1	N/A	N/A	N/A
12	Ca	ug/mL	0.5	N/A	N/A	N/A
13	Cd	ug/mL	<0.1	N/A	N/A	N/A
14	Cl	ug/mL	3644	N/A	N/A	N/A
15	Cl Sample	ug/mL	5186.57	N/A	N/A	N/A
16	Co	ug/mL	<0.1	N/A	N/A	N/A
17	Cr	ug/mL	<0.1	N/A	N/A	N/A
18	Cu	ug/mL	<0.1	N/A	N/A	N/A
19	F (Fluoride) -(only rough rdg)	ug/mL	206	N/A	N/A	N/A
20	F Sample	ug/mL	219	N/A	N/A	N/A
21	Fe	ug/mL	2.7	N/A	N/A	N/A
22	HCOO (Formate)	ug/mL	1529	N/A	N/A	N/A
23	K	ug/mL	3480.6255	N/A	N/A	N/A
24	La	ug/mL	<0.28	N/A	N/A	N/A
25	Li	ug/mL	<1.2	N/A	N/A	N/A
26	Mg	ug/mL	<0.1	N/A	N/A	N/A
27	Mn	ug/mL	<0.1	N/A	N/A	N/A
28	Mo	ug/mL	35	N/A	N/A	N/A
29	Na	ug/mL	112000	N/A	N/A	N/A
30	Ni	ug/mL	<0.15	N/A	N/A	N/A
31	NO2 (Nitrite)	ug/mL	47422	N/A	N/A	N/A
32	NO3 (Nitrate)	ug/mL	67777	N/A	N/A	N/A
33	C2O4 (Oxalate)	ug/mL	452	N/A	N/A	N/A
34	P	ug/mL	85	N/A	N/A	N/A
35	PO4 (Phosphate)	ug/mL	155	N/A	N/A	N/A
36	Pb	ug/mL	<1	N/A	N/A	N/A
37	Si	ug/mL	93	N/A	N/A	N/A
38	Sn	ug/mL	<0.8	N/A	N/A	N/A
39	SO4 (Sulfate)	ug/mL	304	N/A	N/A	N/A
40	Sr	ug/mL	<0.1	N/A	N/A	N/A
41	Ti	ug/mL	<0.1	N/A	N/A	N/A
42	V	ug/mL	<0.1	N/A	N/A	N/A
43	Zn	ug/mL	5.8	N/A	N/A	N/A
44	Zr	ug/mL	<0.3	N/A	N/A	N/A
45	Total Organic Carbon	ug/mL	1553	N/A	N/A	N/A
46	Total Inorganic Carbon	ug/mL	493.5	N/A	N/A	N/A
47	Suspended Solids	wt%	<0.003	N/A	0.2875	0.83
48	Total Solids	wt%	N/A	N/A	28.50	30.95
49	Mean Particle Size by Volum	micron	N/A	2.32	N/A	N/A
50	Mean Particle Size by Numb	micron	N/A	1.03	N/A	N/A
51	Kinematic Viscosity	cSt	N/A	N/A	N/A	2.4
52	Dynamic Viscosity	cP	N/A	N/A	N/A	3.0
53	Comment					HAAKE/SPINNING CONE

Table E1: Analytical – All data, Page 3

	S	T	U	V	W	X
1	TEST RUN ----->		2.13	2.14	2.14	2.14
2	BNFL Sample ID ----->		BNF-SXF2055-A+ES_04b	No Sample Kept	BNF-SXF2055-A+ES_05	BNF-SXF2055-A+ES_06
3	ADS Sample ID ----->		3-128292	No Sample Number	3-129261	TNX Sample/No Number
4	Type Sample ----->		filtrate	filtrate	slurry	slurry
5	Sample Size ----->	mL	15	100mL/returned to mixture	50	150
6	Measurement(s) Made ----->		SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS	DENSITY ONLY	MICROTRAC/IC-ANIONS	TS/SS/VISCOSITY/DENSITY
7	Item Measured	Units				
8	Density	g/mL	N/A	1.144	1.202	1.186
9	Al	ug/mL	17700	N/A	N/A	N/A
10	B	ug/mL	28	N/A	N/A	N/A
11	Ba	ug/mL	<0.2	N/A	N/A	N/A
12	Ca	ug/mL	<2	N/A	N/A	N/A
13	Cd	ug/mL	<0.5	N/A	N/A	N/A
14	Cl	ug/mL	4539	N/A	2509	N/A
15	Cl Sample	ug/mL	5401.07	N/A	N/A	N/A
16	Co	ug/mL	<0.5	N/A	N/A	N/A
17	Cr	ug/mL	1.1	N/A	N/A	N/A
18	Cu	ug/mL	<0.5	N/A	N/A	N/A
19	F (Fluoride) - (only rough rdg)	ug/mL	<20	N/A	72	N/A
20	F Sample	ug/mL	814.8	N/A	N/A	N/A
21	Fe	ug/mL	3.2	N/A	N/A	N/A
22	HCOO (Formate)	ug/mL	1724	N/A	991	N/A
23	K	ug/mL	3908.9460	N/A	N/A	N/A
24	La	ug/mL	<1.4	N/A	N/A	N/A
25	Li	ug/mL	<6.6	N/A	N/A	N/A
26	Mg	ug/mL	<0.5	N/A	N/A	N/A
27	Mn	ug/mL	<0.5	N/A	N/A	N/A
28	Mo	ug/mL	324	N/A	N/A	N/A
29	Na	ug/mL	101850	N/A	N/A	N/A
30	Ni	ug/mL	<0.6	N/A	N/A	N/A
31	NO2 (Nitrite)	ug/mL	52524	N/A	30508	N/A
32	NO3 (Nitrate)	ug/mL	72581	N/A	38503	N/A
33	C2O4 (Oxalate)	ug/mL	469	N/A	10676	N/A
34	P	ug/mL	780	N/A	N/A	N/A
35	PO4 (Phosphate)	ug/mL	161	N/A	234	N/A
36	Pb	ug/mL	<5	N/A	N/A	N/A
37	Si	ug/mL	99	N/A	N/A	N/A
38	Sn	ug/mL	1.2	N/A	N/A	N/A
39	SO4 (Sulfate)	ug/mL	317	N/A	207	N/A
40	Sr	ug/mL	<0.5	N/A	N/A	N/A
41	Ti	ug/mL	<0.5	N/A	N/A	N/A
42	V	ug/mL	<1.2	N/A	N/A	N/A
43	Zn	ug/mL	4.3	N/A	N/A	N/A
44	Zr	ug/mL	<1.5	N/A	N/A	N/A
45	Total Organic Carbon	ug/mL	2284	N/A	N/A	N/A
46	Total Inorganic Carbon	ug/mL	0.89	N/A	N/A	N/A
47	Suspended Solids	wt%	<0.003	N/A	N/A	6.87
48	Total Solids	wt%	N/A	N/A	N/A	25.81
49	Mean Particle Size by Volume	micron	N/A	N/A	1.63/4.89/223	N/A
50	Mean Particle Size by Number	micron	N/A	N/A	1.03	N/A
51	Kinematic Viscosity	cSt	N/A	N/A	N/A	2.1
52	Dynamic Viscosity	cP	N/A	N/A	N/A	2.5
53	Comment				Trimodal partical distribution	HAAKE/SPINNING CONE

Table E1: Analytical – All data, Page 4

	Y	Z	AA	AB	AC	AD
1	TEST RUN		2.14b	2.14b	2.14b	2.14b
2	BNFL Sample ID		BNF-SXF2055-A+ES_05b	BNF-SXF2055-A+ES_05c	BNF-SXF2055-A+ES_05c	BNF-SXF2055-A+ES_06b
3	ADS Sample ID		3-129114	3-130102	3-130102	TNX Sample/No Number
4	Type Sample		slurry	slurry (diluted&filtered)	slurry (solids were dissolved)	slurry
5	Sample Size	ml	50	15	16	150
6	Measurement(s) Made		MICROTRAC	TS/SS/ICP-ES/IC-ANIONS	ICP-ES	TS/SS/VISCOSITY/DENSITY
7	Item Measured	Units				
8	Density	g/mL	1.281	1.281	1.281	1.275
9	Al	ug/mL	N/A	16350	16805	N/A
10	B	ug/mL	N/A	<1.3	N/A	N/A
11	Ba	ug/mL	N/A	<0.2	6	N/A
12	Ca	ug/mL	N/A	1420	1513	N/A
13	Cd	ug/mL	N/A	<0.2	<5.1	N/A
14	Cl	ug/mL	N/A	3886	3887	N/A
15	Cl Sample	ug/mL	N/A	N/A		N/A
16	Co	ug/mL	N/A	<0.5	<13	N/A
17	Cr	ug/mL	N/A	3100	4411	N/A
18	Cu	ug/mL	N/A	2.3	<13	N/A
19	F (Fluoride) -(only rough rdg)	ug/mL	N/A	187	N/A	N/A
20	F Sample	ug/mL	N/A	N/A	N/A	N/A
21	Fe	ug/mL	N/A	406	1606	N/A
22	HCOO (Formate)	ug/mL	N/A	1481	N/A	N/A
23	K	ug/mL	N/A	N/A	N/A	N/A
24	La	ug/mL	N/A	<1.4	<15.1	N/A
25	Li	ug/mL	N/A	<7	<25.1	N/A
26	Mg	ug/mL	N/A	16	<22.52	N/A
27	Mn	ug/mL	N/A	265	298	N/A
28	Mo	ug/mL	N/A	37	43	N/A
29	Na	ug/mL	N/A	120000	119178	N/A
30	Ni	ug/mL	N/A	73	455	N/A
31	NO2 (Nitrite)	ug/mL	N/A	45950	N/A	N/A
32	NO3 (Nitrate)	ug/mL	N/A	61214	N/A	N/A
33	C2O4 (Oxalate)	ug/mL	N/A	10698	N/A	N/A
34	P	ug/mL	N/A	151	<170.2	N/A
35	PO4 (Phosphate)	ug/mL	N/A	299	N/A	N/A
36	Pb	ug/mL	N/A	<5	<151	N/A
37	Si	ug/mL	N/A	665	43065	N/A
38	Sn	ug/mL	N/A	<4	<65.1	N/A
39	SO4 (Sulfate)	ug/mL	N/A	266	N/A	N/A
40	Sr	ug/mL	N/A	3.1	<2.51	N/A
41	Ti	ug/mL	N/A	1	<35.1	N/A
42	V	ug/mL	N/A	<1.2	<32.53	N/A
43	Zn	ug/mL	N/A	1.5	<92.57	N/A
44	Zr	ug/mL	N/A	<0.15	N/A	N/A
45	Total Organic Carbon	ug/mL	N/A	N/A	N/A	N/A
46	Total Inorganic Carbon	ug/mL	N/A	N/A	N/A	N/A
47	Suspended Solids	wt%	N/A	8.17	N/A	8.23
48	Total Solids	wt%	N/A	36.2	N/A	34.48
49	Mean Particle Size by Volume	micron	2.49	N/A	N/A	N/A
50	Mean Particle Size by Number	micron	1.028	N/A	N/A	N/A
51	Kinematic Viscosity	cSt	N/A	N/A	N/A	2.4
52	Dynamic Viscosity	cP	N/A	N/A	N/A	3.1
53	Comment			Acid Diluent affected solids	Solids Info for Comparison	HAAKE/SPINNING CONE

Table E1: Analytical – All data, Page 5

	AE	AF	AG	AH	AI	AJ
1	TEST RUN ----->>		2.14b	2.15	2.15b	2.16
2	BNFL Sample ID ----->>		No Sample Kept	BNF-SXF2055-A+ES_07	BNF-SXF2055-A+ES_07b	BNF-SXF2055-A+ES_08
3	ADS Sample ID ----->>		No Sample Number	3-129284	3-129117	3-129262
4	Type Sample ----->>		filtrate	filtrate	filtrate	slurry
5	Sample Size ----->>	mL	100mL/returned to mixture	15	15	50
6	Measurement(s) Made ----->>		VISCOSITY/DENSITY	SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS	SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS	MICROTRAC
7	Item Measured	Units				
8	Density	g/mL	1.214	1.080	1.105	1.082
9	Al	ug/mL	N/A	5160	7115	N/A
10	B	ug/mL	N/A	7.6	10	N/A
11	Ba	ug/mL	N/A	<0.5	<0.05	N/A
12	Ca	ug/mL	N/A	<2	0.9	N/A
13	Cd	ug/mL	N/A	<0.2	<0.05	N/A
14	Cl	ug/mL	N/A	1255	1773	N/A
15	Cl Sample	ug/mL	N/A	1336.7	1841	N/A
16	Co	ug/mL	N/A	<0.5	<0.05	N/A
17	Cr	ug/mL	N/A	2	2.2	N/A
18	Cu	ug/mL	N/A	<0.4	<0.05	N/A
19	F (Fluoride) -(only rough rdg)	ug/mL	N/A	46	63	N/A
20	F Sample	ug/mL	N/A	53.95	<10	N/A
21	Fe	ug/mL	N/A	<0.6	0.88	N/A
22	HCOO (Formate)	ug/mL	N/A	532	721	N/A
23	K	ug/mL	N/A	1076.8566	1594.698	N/A
24	La	ug/mL	N/A	<1.4	<0.14	N/A
25	Li	ug/mL	N/A	<7	<0.7	N/A
26	Mg	ug/mL	N/A	<0.5	<0.03	N/A
27	Mn	ug/mL	N/A	<0.4	<0.02	N/A
28	Mo	ug/mL	N/A	12.7	15	N/A
29	Na	ug/mL	N/A	38550	49000	N/A
30	Ni	ug/mL	N/A	<0.6	0.1	N/A
31	NO2 (Nitrite)	ug/mL	N/A	16553	21918	N/A
32	NO3 (Nitrate)	ug/mL	N/A	25451	35660	N/A
33	C2O4 (Oxalate)	ug/mL	N/A	4383	2969	N/A
34	P	ug/mL	N/A	23	63	N/A
35	PO4 (Phosphate)	ug/mL	N/A	67	272	N/A
36	Pb	ug/mL	N/A	<0.5	<0.5	N/A
37	Si	ug/mL	N/A	32	62	N/A
38	Sn	ug/mL	N/A	<0.5	<0.4	N/A
39	SO4 (Sulfate)	ug/mL	N/A	96	154	N/A
40	Sr	ug/mL	N/A	<0.5	<0.05	N/A
41	Ti	ug/mL	N/A	<0.5	<0.05	N/A
42	V	ug/mL	N/A	<1.2	<0.12	N/A
43	Zn	ug/mL	N/A	1.0	2	N/A
44	Zr	ug/mL	N/A	<1.5	<0.15	N/A
45	Total Organic Carbon	ug/mL	N/A	1998	543	N/A
46	Total Inorganic Carbon	ug/mL	N/A	1774	524	N/A
47	Suspended Solids	wt%	N/A	<0.02	<0.01	N/A
48	Total Solids	wt%	N/A	N/A	N/A	N/A
49	Mean Particle Size by Volume	micron	N/A	N/A	N/A	1.61/4.91/213
50	Mean Particle Size by Number	micron	N/A	N/A	N/A	1.03
51	Kinematic Viscosity	cSt	1.51	N/A	1.33	N/A
52	Dynamic Viscosity	cP	1.84	N/A	1.47	N/A
53	Comment		viscosity done by capillary		viscosity done by capillary	Trimodal particle distribution

Table E1: Analytical - All data, Page 6

	AK	AL	AM	AN	AO	AP
1	TEST RUN ----->		2.16	2.16	2.16	2.16b
2	BNFL Sample ID ----->		Unplanned Sample	BNF-SXF2055-A+ES_09	BNF-SXF2055-A+ES_10	BNF-SXF2055-A+ES_08b
3	ADS Sample ID ----->		TNX Sample/No Number	3-129288	3-129285	3-129115
4	Type Sample ----->		slurry	slurry	filtrate	slurry
5	Sample Size ----->> mL		150	15	15	50
6	Measurement(s) Made ----->>		VISCOSITY ONLY	TS/SS	SS/CP-ES/AA/TIC-TOC/ISE/C-ANIONS	MICROTRAC
7	Item Measured	Units				
8	Density	g/mL	1.082	1.082	1.045	N/A
9	Al	ug/mL	N/A	N/A	2685	N/A
10	B	ug/mL	N/A	N/A	3.7	N/A
11	Ba	ug/mL	N/A	N/A	<0.5	N/A
12	Ca	ug/mL	N/A	N/A	<2	N/A
13	Cd	ug/mL	N/A	N/A	<0.2	N/A
14	Cl	ug/mL	N/A	N/A	528	N/A
15	Cl Sample	ug/mL	N/A	N/A	645.4	N/A
16	Co	ug/mL	N/A	N/A	<0.5	N/A
17	Cr	ug/mL	N/A	N/A	0.8	N/A
18	Cu	ug/mL	N/A	N/A	<0.4	N/A
19	F (Fluoride) - (only rough rdg)	ug/mL	N/A	N/A	26	N/A
20	F Sample	ug/mL	N/A	N/A	11.5	N/A
21	Fe	ug/mL	N/A	N/A	<0.6	N/A
22	HCOO (Formate)	ug/mL	N/A	N/A	233	N/A
23	K	ug/mL	N/A	N/A	490.297	N/A
24	La	ug/mL	N/A	N/A	<1.4	N/A
25	Li	ug/mL	N/A	N/A	<7	N/A
26	Mg	ug/mL	N/A	N/A	<0.5	N/A
27	Mn	ug/mL	N/A	N/A	<0.4	N/A
28	Mo	ug/mL	N/A	N/A	6.9	N/A
29	Na	ug/mL	N/A	N/A	23400	N/A
30	Ni	ug/mL	N/A	N/A	<0.6	N/A
31	NO2 (Nitrite)	ug/mL	N/A	N/A	7286	N/A
32	NO3 (Nitrate)	ug/mL	N/A	N/A	10353	N/A
33	C2O4 (Oxalate)	ug/mL	N/A	N/A	9419	N/A
34	P	ug/mL	N/A	N/A	11	N/A
35	PO4 (Phosphate)	ug/mL	N/A	N/A	30	N/A
36	Pb	ug/mL	N/A	N/A	<5	N/A
37	Si	ug/mL	N/A	N/A	13	N/A
38	Sn	ug/mL	N/A	N/A	<4	N/A
39	SO4 (Sulfate)	ug/mL	N/A	N/A	44	N/A
40	Sr	ug/mL	N/A	N/A	<0.5	N/A
41	Ti	ug/mL	N/A	N/A	<0.5	N/A
42	V	ug/mL	N/A	N/A	<1.2	N/A
43	Zn	ug/mL	N/A	N/A	5.1	N/A
44	Zr	ug/mL	N/A	N/A	<1.5	N/A
45	Total Organic Carbon	ug/mL	N/A	N/A	3370	N/A
46	Total Inorganic Carbon	ug/mL	N/A	N/A	1124	N/A
47	Suspended Solids	wt%	N/A	4.85	<0.02	N/A
48	Total Solids	wt%	N/A	10.518	N/A	N/A
49	Mean Particle Size by Volume	micron	N/A	N/A	N/A	1.7/6
50	Mean Particle Size by Number	micron	N/A	N/A	N/A	1.046
51	Kinematic Viscosity	cSt	<1.8	N/A	N/A	N/A
52	Dynamic Viscosity	cP	<2	N/A	N/A	N/A
53	Comment		HAAKE/SPINNING CONE			bimodal particle distribution

Table E1: Analytical - All data, Page 7

	AQ	AR	AS	AT	AU	AV
1	TEST RUN		2.16b	2.16b	2.17b	2.18
2	BNFL Sample ID		BNF-SXF2055-A+ES_09b	BNF-SXF2055-A+ES_10b	BNF-SXF2055-A+ES_11b	BNF-SXF2055-A+ES_12
3	ADS Sample ID		3-129123	3-129118	3-129119	3-129286
4	Type Sample		slurry	filtrate	filtrate	filtrate
5	Sample Size	mL	15	15	15	15
6	Measurement(s) Made		TS/SS	SSICP-ESA/ATIC-TOC/ISE/C-ANIONS	SSICP-ESA/ATIC-TOC/ISE/C-ANIONS	SSICP-ESA/ATIC-TOC/ISE/C-ANIONS
7	Item Measured	Units				
8	Density	g/mL	N/A	1.055	1.031	1.025
9	Al	ug/mL	N/A	3180	1535	1320
10	B	ug/mL	N/A	4.9	2.5	<1.5
11	Ba	ug/mL	N/A	<0.05	<0.05	<0.5
12	Ca	ug/mL	N/A	1.2	3.1	<2
13	Cd	ug/mL	N/A	<0.05	<0.05	<0.05
14	Cl	ug/mL	N/A	735	295	233
15	Cl Sample	ug/mL	N/A	1973	360	319.3
16	Co	ug/mL	N/A	<0.05	<0.05	<0.2
17	Cr	ug/mL	N/A	1.1	0.7	<0.5
18	Cu	ug/mL	N/A	<0.05	<0.05	<0.4
19	F (Fluoride) - (only rough rdg)	ug/mL	N/A	36	18	13
20	F Sample	ug/mL	N/A	<10	<10	7.35
21	Fe	ug/mL	N/A	0.31	0.23	<0.6
22	HCOO (Formate)	ug/mL	N/A	320	140	96
23	K	ug/mL	N/A	689.5910	303.408	250.207
24	La	ug/mL	N/A	<0.14	<0.14	<1.4
25	Li	ug/mL	N/A	<0.7	<0.7	<7
26	Mg	ug/mL	N/A	<0.03	<0.03	<0.5
27	Mn	ug/mL	N/A	<0.02	<0.02	<0.4
28	Mo	ug/mL	N/A	7.2	3.3	3.9
29	Na	ug/mL	N/A	18300	11850	12450
30	Ni	ug/mL	N/A	<0.06	<0.06	<0.6
31	NO2 (Nitrite)	ug/mL	N/A	9718	4279	3527
32	NO3 (Nitrate)	ug/mL	N/A	14285	5487	4686
33	C2O4 (Oxalate)	ug/mL	N/A	7057	7755	6325
34	P	ug/mL	N/A	29	13	<9
35	PO4 (Phosphate)	ug/mL	N/A	67	36	11
36	Pb	ug/mL	N/A	<0.5	<0.5	<5
37	Si	ug/mL	N/A	30	17	<6
38	Sn	ug/mL	N/A	<0.4	<0.4	<4
39	SO4 (Sulfate)	ug/mL	N/A	57	25	23
40	Sr	ug/mL	N/A	<0.05	<0.05	<0.5
41	Ti	ug/mL	N/A	<0.05	<0.05	<0.5
42	V	ug/mL	N/A	<0.12	<0.12	<1.2
43	Zn	ug/mL	N/A	1	0.2	5.2
44	Zr	ug/mL	N/A	<0.15	<0.15	<1.5
45	Total Organic Carbon	ug/mL	N/A	966	1039	2492
46	Total Inorganic Carbon	ug/mL	N/A	298	199	498
47	Suspended Solids	wt%	5.49	<0.1	<0.1	<0.02
48	Total Solids	wt%	12.88	N/A	N/A	N/A
49	Mean Particle Size by Volume	micron	N/A	N/A	N/A	N/A
50	Mean Particle Size by Number	micron	N/A	N/A	N/A	N/A
51	Kinematic Viscosity	cSt	N/A	1.15	1.08	N/A
52	Dynamic Viscosity	cP	N/A	1.21	1.11	N/A
53	Comment			viscosity done by capillary	viscosity done by capillary	

Table E1: Analytical - All data, Page 8

	AW	AX	AY	AZ	BA	BB
1	TEST RUN		2.18b	2.19	2.19b	2.20b
2	BNFL Sample ID		BNF-SXF2055-A+ES_12b	BNF-SXF2055-A+ES_13	BNF-SXF2055-A+ES_13b	BNF-SXF2055-A+ES_14b
3	ADS Sample ID		3-129120	3-129287	3-129121	3-129116
4	Type Sample		filtrate	filtrate	filtrate	slurry (80-liter starting volume)
5	Sample Size	mL	15	15	15	50
6	Measurement(s) Made		SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS	SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS	SS/CP-ES/AA/TIC-TOC/ISE/IC-ANIONS	MICROTRAC
7	Item Measured	Units				
8	Density	g/mL	1.015	1.010	1.0095	from 1.054 to 1.143
9	Al	ug/mL	845	680	367	N/A
10	B	ug/mL	1.5	<1.5	0.9	N/A
11	Ba	ug/mL	<0.05	<0.5	<0.05	N/A
12	Ca	ug/mL	<0.2	<2	<0.2	N/A
13	Cd	ug/mL	<0.05	<0.2	<0.05	N/A
14	Cl	ug/mL	149	127	61	N/A
15	Cl Sample	ug/mL	542	159.3	445	N/A
16	Co	ug/mL	<0.05	<0.5	<0.05	N/A
17	Cr	ug/mL	<0.1	<0.5	<0.1	N/A
18	Cu	ug/mL	<0.05	<0.4	<0.05	N/A
19	F (Fluoride) - (only rough rdg)	ug/mL	11	8	6	N/A
20	F Sample	ug/mL	<10	3.05	<10	N/A
21	Fe	ug/mL	0.16	<0.6	0.07	N/A
22	HCOO (Formate)	ug/mL	76	59	37	N/A
23	K	ug/mL	159.9815	131.8985	62.0455	N/A
24	La	ug/mL	<0.14	<1.4	<0.14	N/A
25	Li	ug/mL	<0.7	<7	<0.7	N/A
26	Mg	ug/mL	<0.03	<0.5	<0.03	N/A
27	Mn	ug/mL	<0.02	<0.4	<0.02	N/A
28	Mo	ug/mL	1.8	2.7	0.8	N/A
29	Na	ug/mL	6735	6665	2905	N/A
30	Ni	ug/mL	<0.06	<0.6	<0.06	N/A
31	NO2 (Nitrite)	ug/mL	2254	1850	868	N/A
32	NO3 (Nitrate)	ug/mL	3652	2897	1281	N/A
33	C2O4 (Oxalate)	ug/mL	4294	3888	1564	N/A
34	P	ug/mL	7	<9	3	N/A
35	PO4 (Phosphate)	ug/mL	19	<10	4	N/A
36	Pb	ug/mL	<0.5	<5	<0.5	N/A
37	Si	ug/mL	12	<6	8.6	N/A
38	Sn	ug/mL	<0.4	<4	<0.4	N/A
39	SO4 (Sulfate)	ug/mL	13	12	6	N/A
40	Sr	ug/mL	<0.05	<0.5	<0.05	N/A
41	Ti	ug/mL	<0.05	<0.5	<0.05	N/A
42	V	ug/mL	<0.12	<1.2	<0.12	N/A
43	Zn	ug/mL	0.06	<0.4	<0.03	N/A
44	Zr	ug/mL	<0.15	<1.5	<0.15	N/A
45	Total Organic Carbon	ug/mL	581	1589	262	N/A
46	Total Inorganic Carbon	ug/mL	143	336	88	N/A
47	Suspended Solids	wt%	<0.01	<0.02	<0.01	N/A
48	Total Solids	wt%	N/A	N/A	N/A	N/A
49	Mean Particle Size by Volume	micron	N/A	N/A	N/A	3.33
50	Mean Particle Size by Number	micron	N/A	N/A	N/A	1.016/2.164
51	Kinematic Viscosity	cSt	1.04	N/A	1.00	N/A
52	Dynamic Viscosity	cP	1.06	N/A	1.01	N/A
53	Comment		viscosity done by capillary		viscosity done by capillary	Post-wash De-watering

Table E1: Analytical – All data, Page 9

	BC	BD	BE	BF	BG	BH
1	TEST RUN ----->		2.20b	2.20b	2.20b	2.20b
2	BNFL Sample ID ----->		BNF-SXF2055-A+ES_15b	BNF-SXF2055-A+ES_16b	Viscosity 2	Viscosity 3
3	ADS Sample ID ----->		3-129124	TNX Sample/No Number	TNX Sample/No Number	TNX Sample/No Number
4	Type Sample ----->		slurry (80-liter starting volume)	slurry (80-liter starting volume)	slurry (57.9 liters remain)	slurry (43.1 liters remain)
5	Sample Size ----->	mL	15	150	150	150
6	Measurement(s) Made ----->		TS/SS	TS/SS/VISCOSITY/DENSITY	TS/SS/VISCOSITY/DENSITY	TS/SS/VISCOSITY/DENSITY
7	Item Measured	Units				
8	Density	g/mL	1.054	1.053	1.077	1.106
9	Al	ug/mL	N/A	N/A	N/A	N/A
10	B	ug/mL	N/A	N/A	N/A	N/A
11	Ba	ug/mL	N/A	N/A	N/A	N/A
12	Ca	ug/mL	N/A	N/A	N/A	N/A
13	Cd	ug/mL	N/A	N/A	N/A	N/A
14	Cl	ug/mL	N/A	N/A	N/A	N/A
15	Cl Sample	ug/mL	N/A	N/A	N/A	N/A
16	Co	ug/mL	N/A	N/A	N/A	N/A
17	Cr	ug/mL	N/A	N/A	N/A	N/A
18	Cu	ug/mL	N/A	N/A	N/A	N/A
19	F (Fluoride) -(only rough rdg)	ug/mL	N/A	N/A	N/A	N/A
20	F Sample	ug/mL	N/A	N/A	N/A	N/A
21	Fe	ug/mL	N/A	N/A	N/A	N/A
22	HCOO (Formate)	ug/mL	N/A	N/A	N/A	N/A
23	K	ug/mL	N/A	N/A	N/A	N/A
24	La	ug/mL	N/A	N/A	N/A	N/A
25	Li	ug/mL	N/A	N/A	N/A	N/A
26	Mg	ug/mL	N/A	N/A	N/A	N/A
27	Mn	ug/mL	N/A	N/A	N/A	N/A
28	Mo	ug/mL	N/A	N/A	N/A	N/A
29	Na	ug/mL	N/A	N/A	N/A	N/A
30	Ni	ug/mL	N/A	N/A	N/A	N/A
31	NO2 (Nitrite)	ug/mL	N/A	N/A	N/A	N/A
32	NO3 (Nitrate)	ug/mL	N/A	N/A	N/A	N/A
33	C2O4 (Oxalate)	ug/mL	N/A	N/A	N/A	N/A
34	P	ug/mL	N/A	N/A	N/A	N/A
35	PO4 (Phosphate)	ug/mL	N/A	N/A	N/A	N/A
36	Pb	ug/mL	N/A	N/A	N/A	N/A
37	Si	ug/mL	N/A	N/A	N/A	N/A
38	Sn	ug/mL	N/A	N/A	N/A	N/A
39	SO4 (Sulfate)	ug/mL	N/A	N/A	N/A	N/A
40	Sr	ug/mL	N/A	N/A	N/A	N/A
41	Ti	ug/mL	N/A	N/A	N/A	N/A
42	V	ug/mL	N/A	N/A	N/A	N/A
43	Zn	ug/mL	N/A	N/A	N/A	N/A
44	Zr	ug/mL	N/A	N/A	N/A	N/A
45	Total Organic Carbon	ug/mL	N/A	N/A	N/A	N/A
46	Total Inorganic Carbon	ug/mL	N/A	N/A	N/A	N/A
47	Suspended Solids	wt%	5.04	4.97	N/A	11.69
48	Total Solids	wt%	6.98	7.85	10.79	14.36
49	Mean Particle Size by Volume	micron	N/A	N/A	N/A	N/A
50	Mean Particle Size by Number	micron	N/A	N/A	N/A	N/A
51	Kinematic Viscosity	cSt	N/A	1.6	1.5	1.4
52	Dynamic Viscosity	cP	N/A	1.6	1.6	1.6
53	Comment		Post-wash De-watering	HAAKE/SPINNING CONE	HAAKE/SPINNING CONE	HAAKE/SPINNING CONE

Table E1: Analytical – All data, Page 10

	BI	BJ	BK	BL
1	TEST RUN ----->		2.20b	Final Concentrate
2	BNFL Sample ID ----->		BNF-SXF2055-A+ES_17b	BNF-SXF2055-A+ES_18b
3	ADS Sample ID ----->		3-129122	3-130103
4	Type Sample ----->		filtrate	filtrate (~30 liters left)
5	Sample Size ----->>	mL	15	15
6	Measurement(s) Made ----->>		SS/ICP-ES/AA/TIC-TOC/ISE/IC-ANIONS	TS/SS / ICP-ES
7	Item Measured	Units		
8	Density	g/mL	1.019	1.019
9	Al	ug/mL	705	16.6
10	B	ug/mL	1.4	<0.13
11	Ba	ug/mL	<0.05	<0.02
12	Ca	ug/mL	<0.2	3.3
13	Cd	ug/mL	<0.05	0.1
14	Cl	ug/mL	116	N/A
15	Cl Sample	ug/mL	145	N/A
16	Co	ug/mL	<0.05	<0.02
17	Cr	ug/mL	1	1.5
18	Cu	ug/mL	<0.05	0.07
19	F (Fluoride) -(only rough rdg)	ug/mL	9	N/A
20	F Sample	ug/mL	<10	N/A
21	Fe	ug/mL	0.07	21.4
22	HCOO (Formate)	ug/mL	60	N/A
23	K	ug/mL	131.1485	N/A
24	La	ug/mL	<0.14	<0.14
25	Li	ug/mL	<0.7	<0.7
26	Mg	ug/mL	<0.03	1.1
27	Mn	ug/mL	<0.02	0.16
28	Mo	ug/mL	1.5	0.15
29	Na	ug/mL	8475	38.7
30	Ni	ug/mL	<0.06	1.2
31	NO2 (Nitrite)	ug/mL	1817	N/A
32	NO3 (Nitrate)	ug/mL	2885	N/A
33	C2O4 (Oxalate)	ug/mL	9453	N/A
34	P	ug/mL	6	<0.9
35	PO4 (Phosphate)	ug/mL	12	N/A
36	Pb	ug/mL	<0.5	1.5
37	Si	ug/mL	13	1.4
38	Sn	ug/mL	<0.4	<0.4
39	SO4 (Sulfate)	ug/mL	11	N/A
40	Sr	ug/mL	<0.05	<0.05
41	Ti	ug/mL	<0.05	0.56
42	V	ug/mL	<0.12	<0.12
43	Zn	ug/mL	<0.03	0.33
44	Zr	ug/mL	<0.15	0.15
45	Total Organic Carbon	ug/mL	1184	N/A
46	Total Inorganic Carbon	ug/mL	163	N/A
47	Suspended Solids	wt%	<0.01	<0.004
48	Total Solids	wt%	N/A	N/A
49	Mean Particle Size by Volume	micron	N/A	N/A
50	Mean Particle Size by Number	micron	N/A	N/A
51	Kinematic Viscosity	cSt	N/A	N/A
52	Dynamic Viscosity	cP	N/A	N/A
53	Comment			find out remaining solids

Table E1: Analytical – All data, Page 11

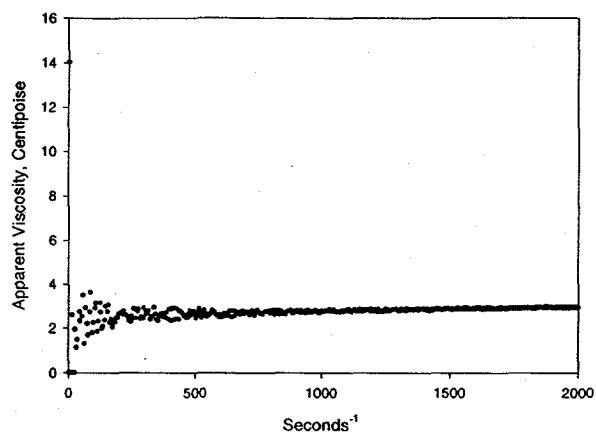


Figure E1. Slurry at 0.5 wt% insoluble solids and 29 wt% total solids: Run 2.13

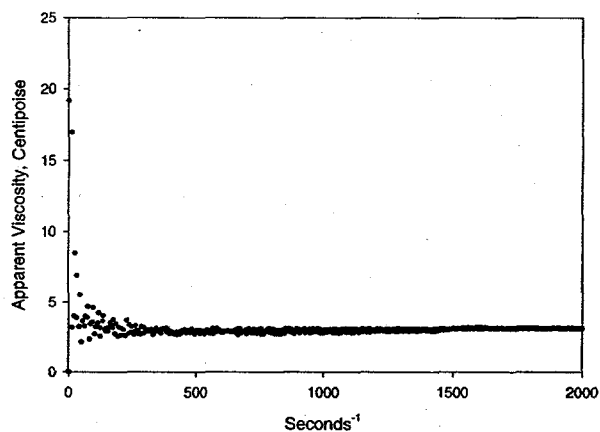


Figure E2. Slurry at 8 wt% insoluble solids and 36 wt% total solids: Run 2.14b

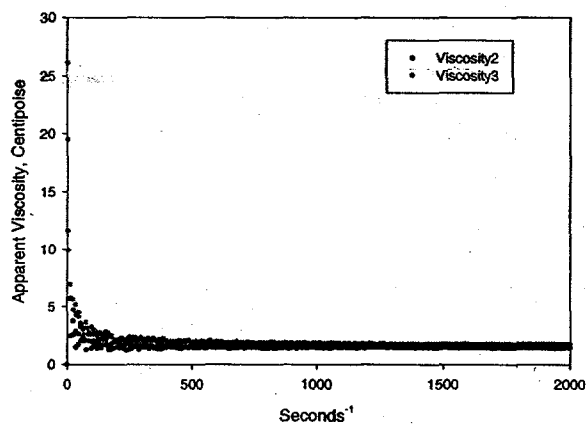


Figure E3. Slurry at 12 wt% insoluble solids and 14 wt% total solids: Run 2.20b

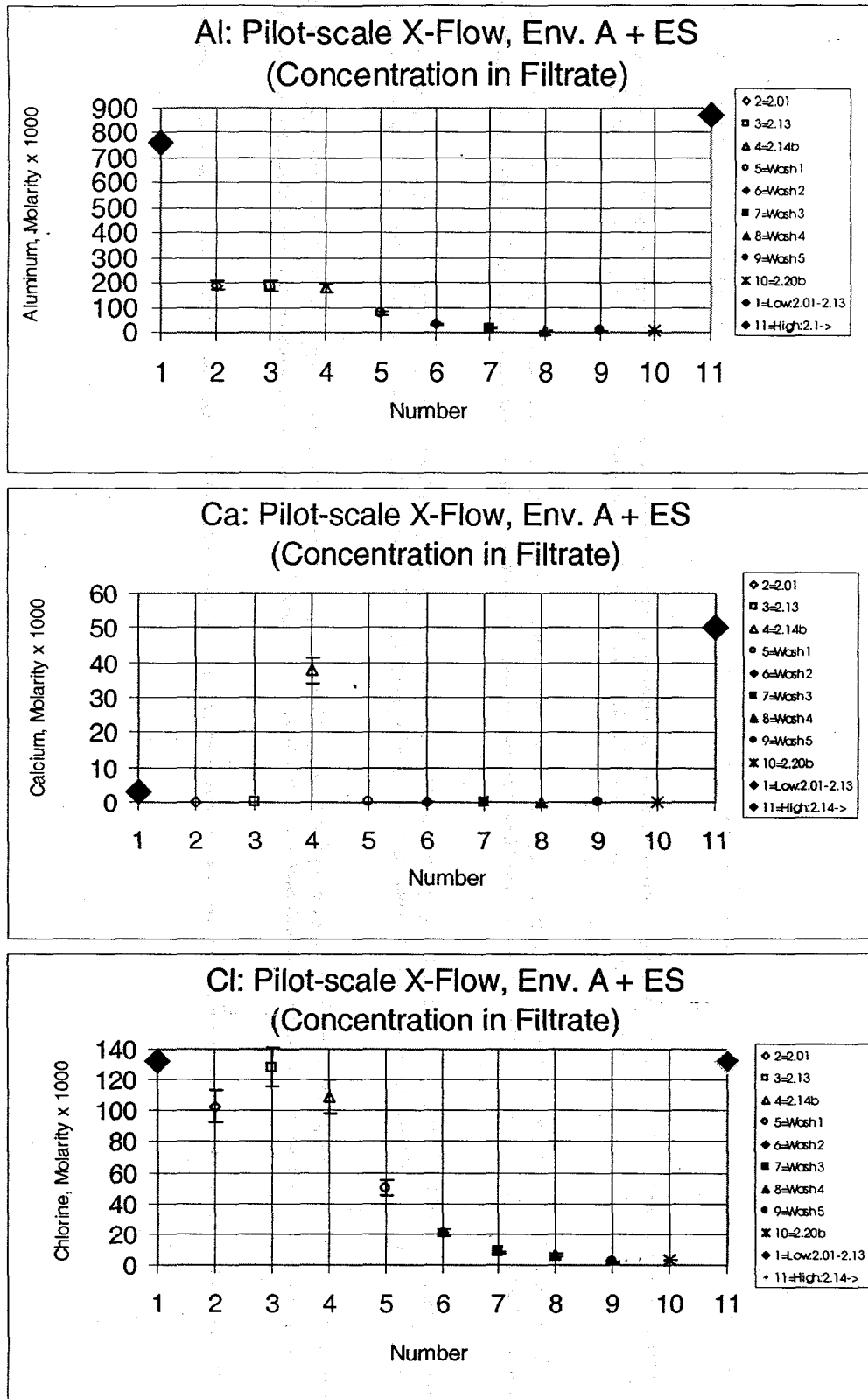


Figure E4, E5, and E6. Aluminum, Calcium, and Chlorine, respectively

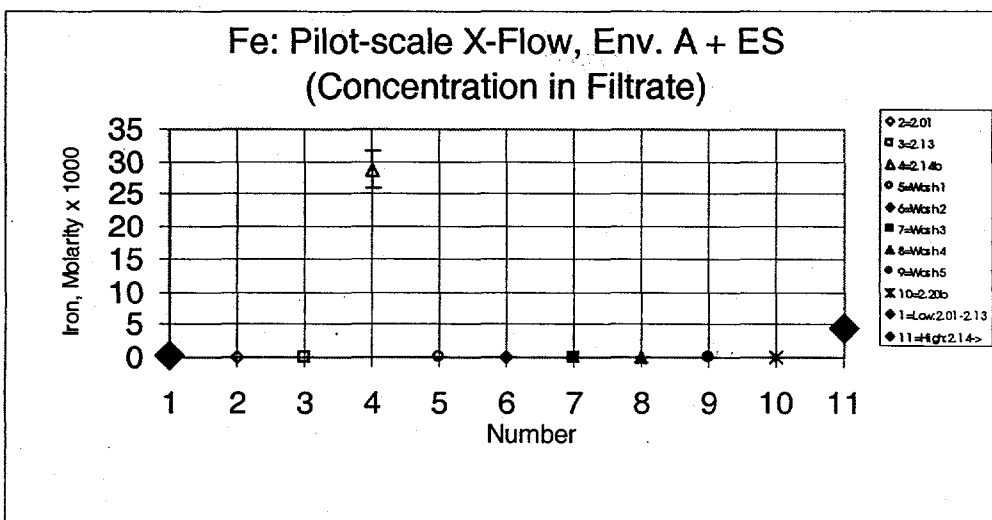
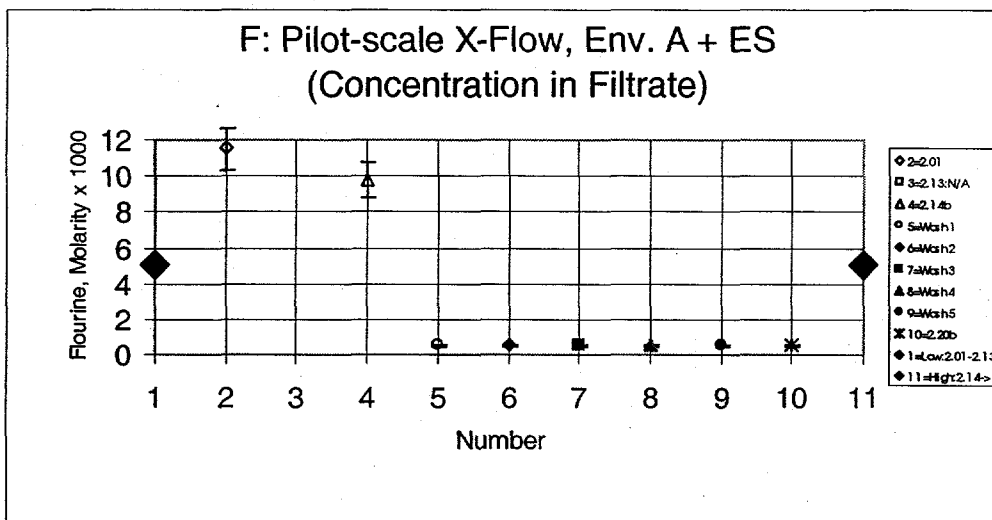
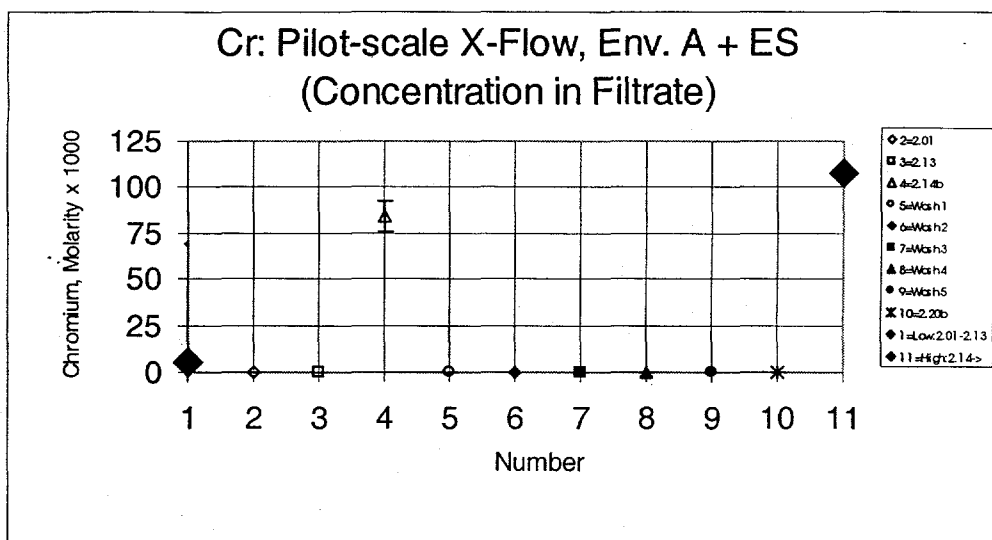


Figure E7, E8, and E9. Chromium, Fluorine, and Iron, respectively

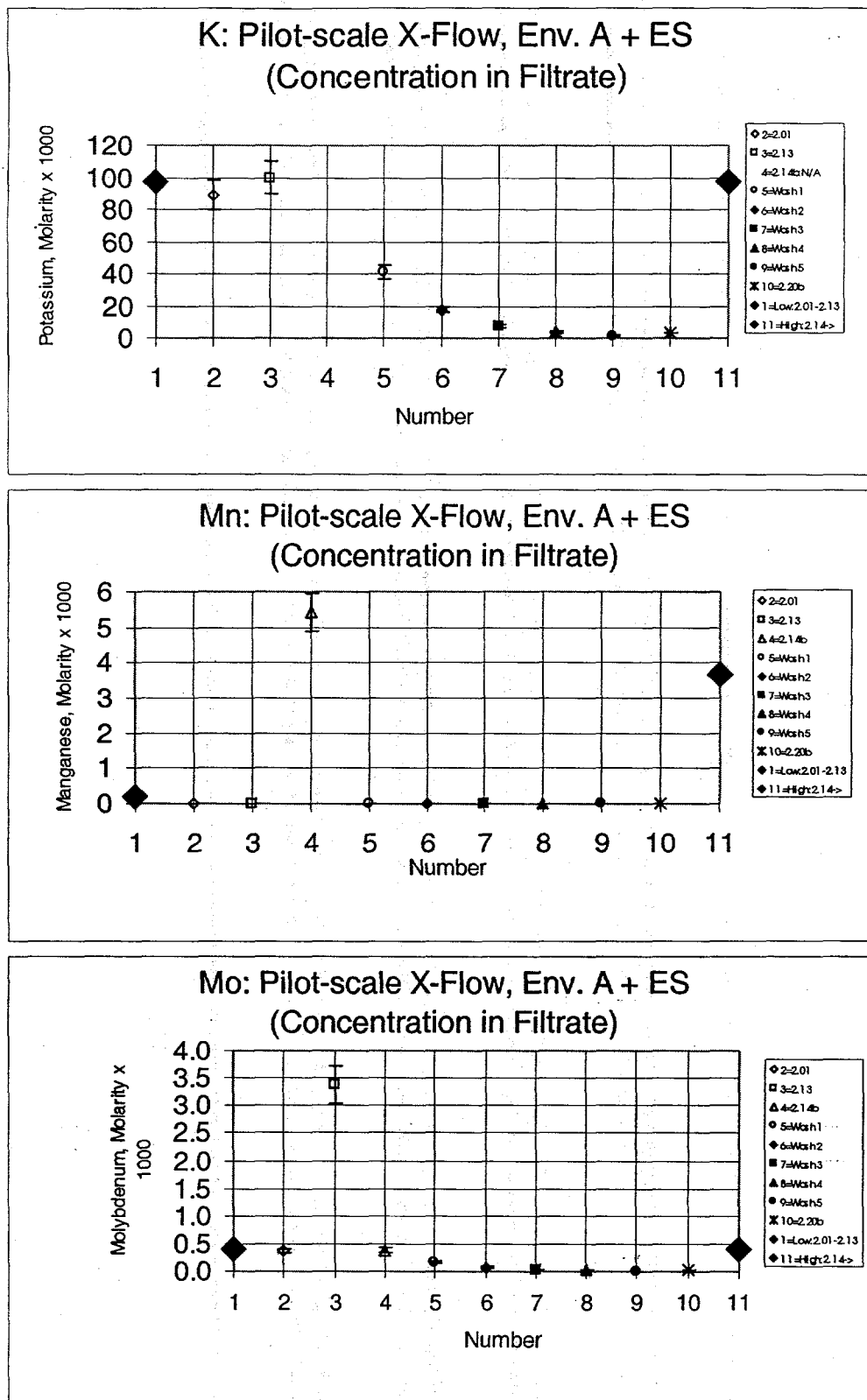


Figure E10, E11, and E12. Potassium, Manganese, and Molybdenum, respectively

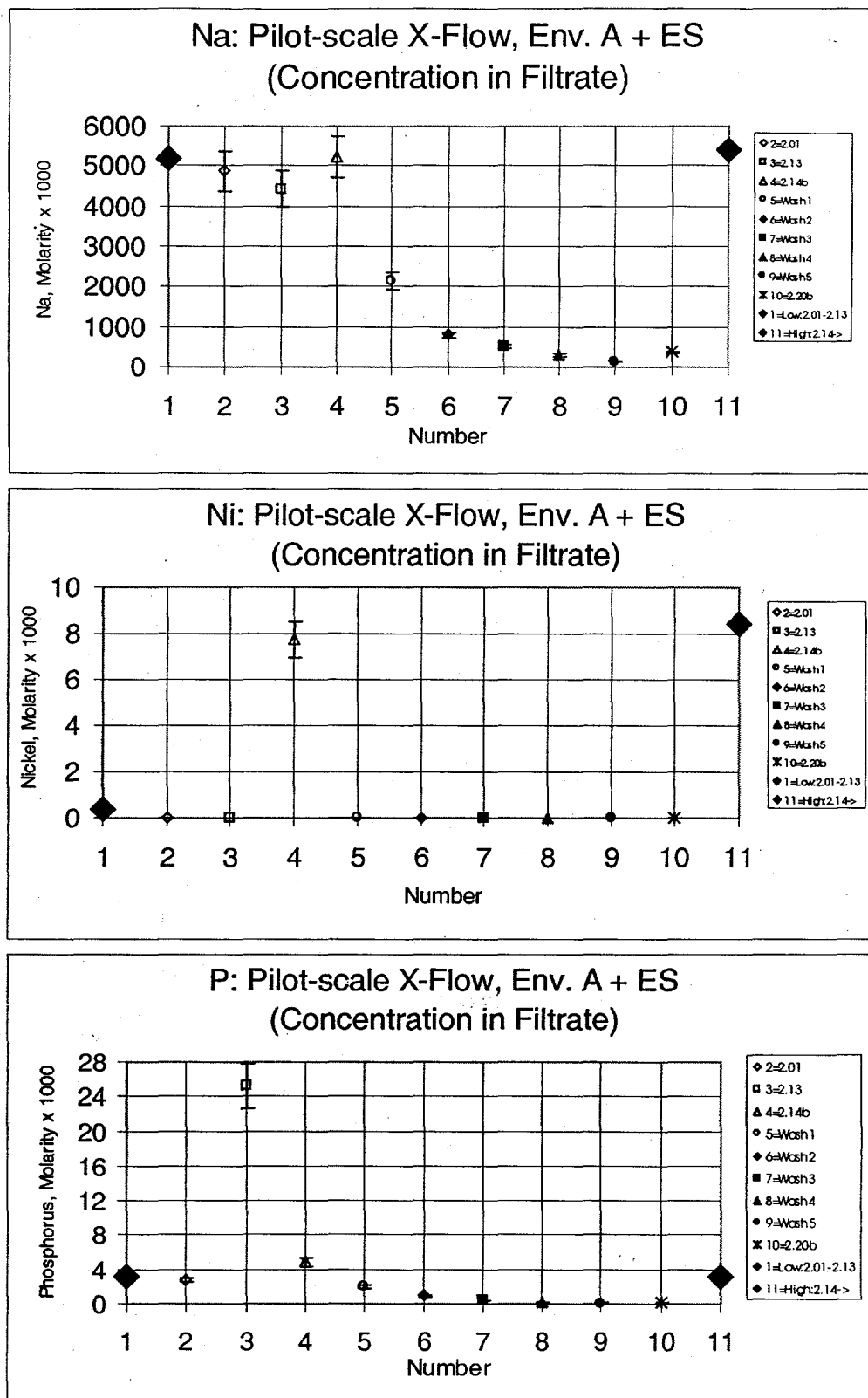


Figure E13, E14, and E15. Sodium, Nickel, and Phosphorous, respectively

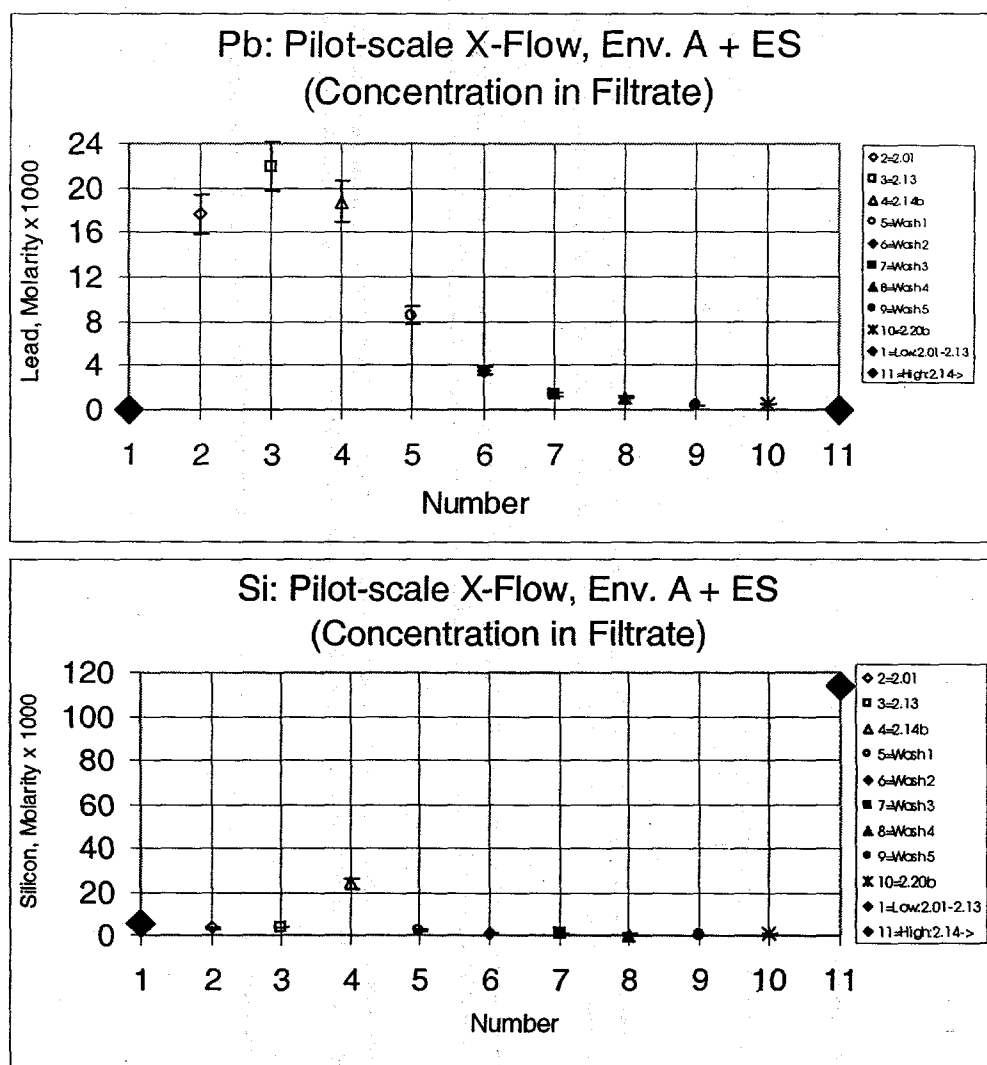


Figure E16 and E17. Lead and Silicon, respectively

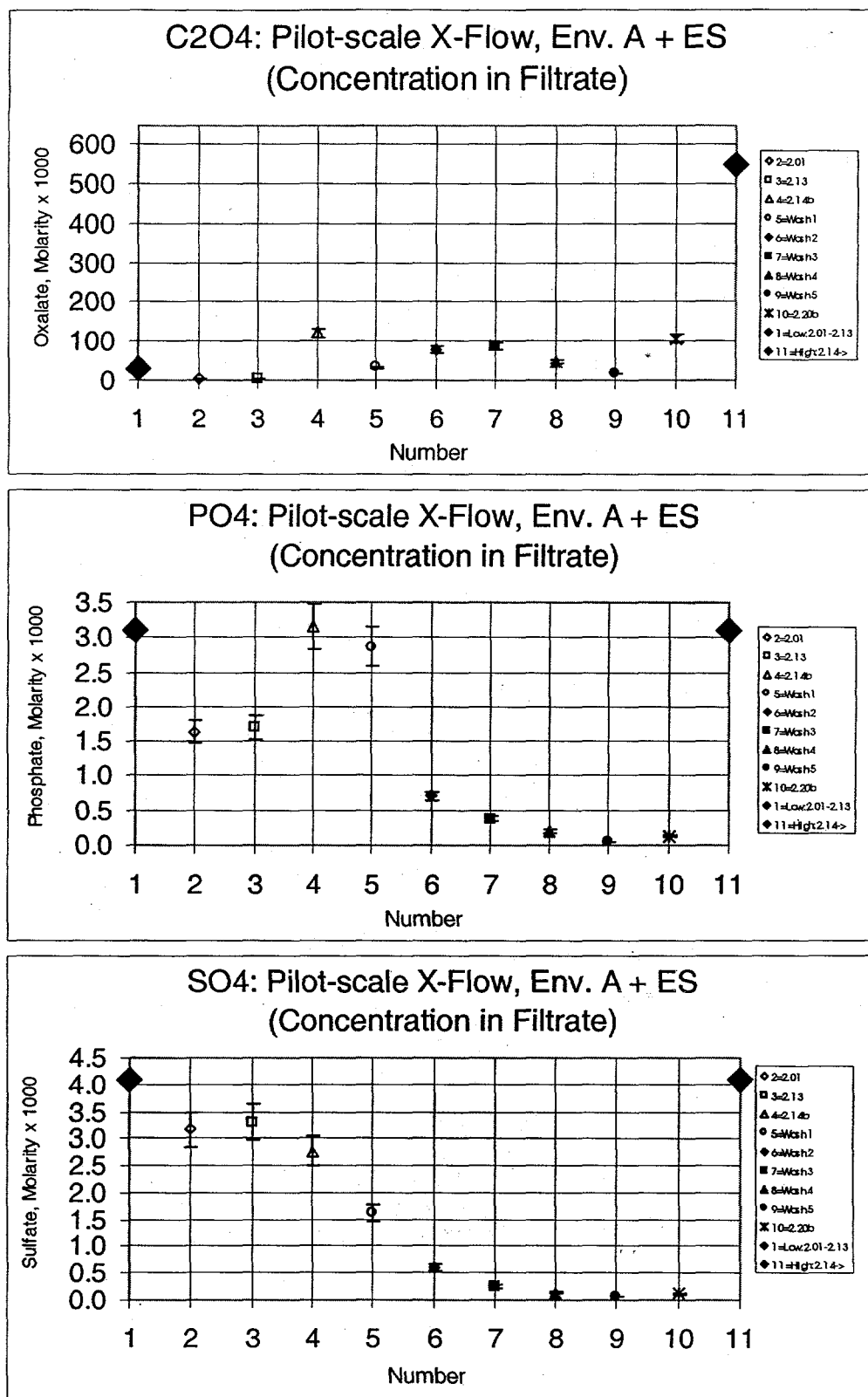


Figure E18, E19, and E20. Oxalate, Phosphate, and Sulfate, respectively

Particle Size Info

Source: "Results of Dilution Studies with Waste from Tank 241-AN-105" by D. L. Herting, HNF-SD-DTR-046, Rev. 0, 10/10/1997.

Undiluted whole tank composite sample of 241-AN-105 had as follows:

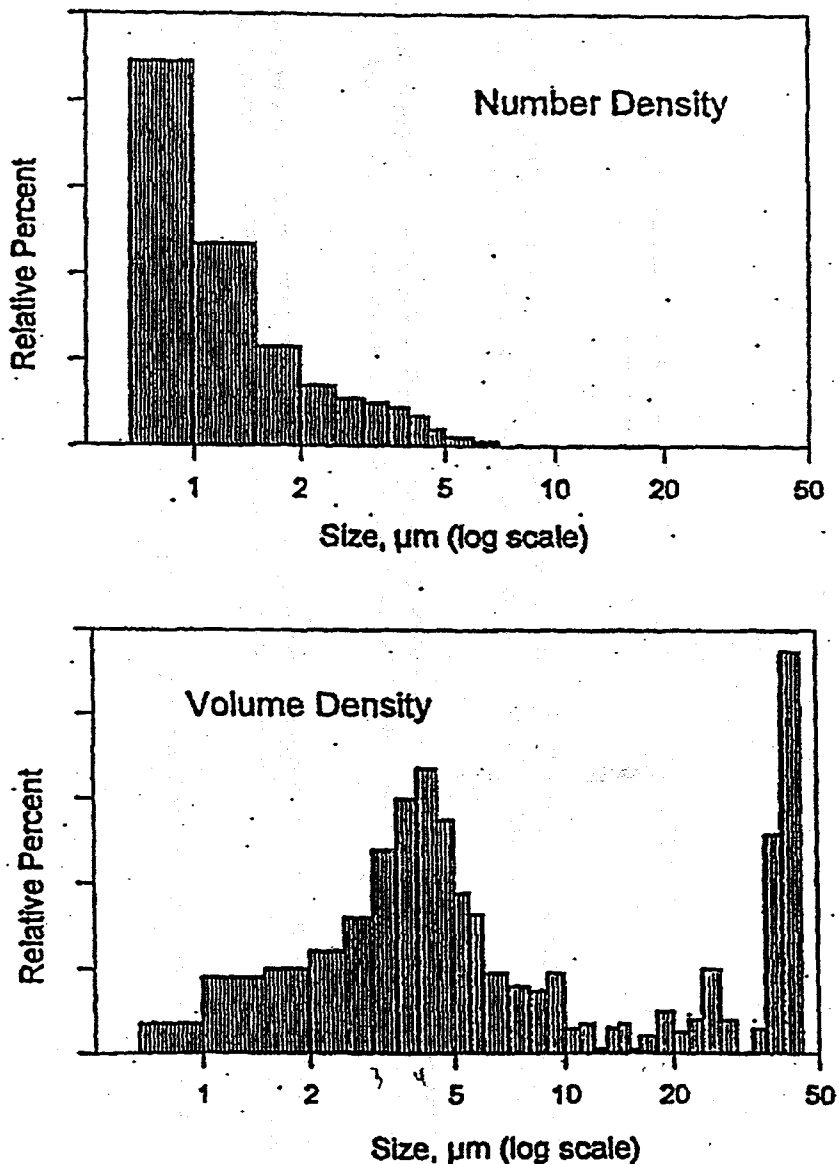


Figure E21. Insoluble Solids Distribution from Actual Tank AN-105 Waste Sample

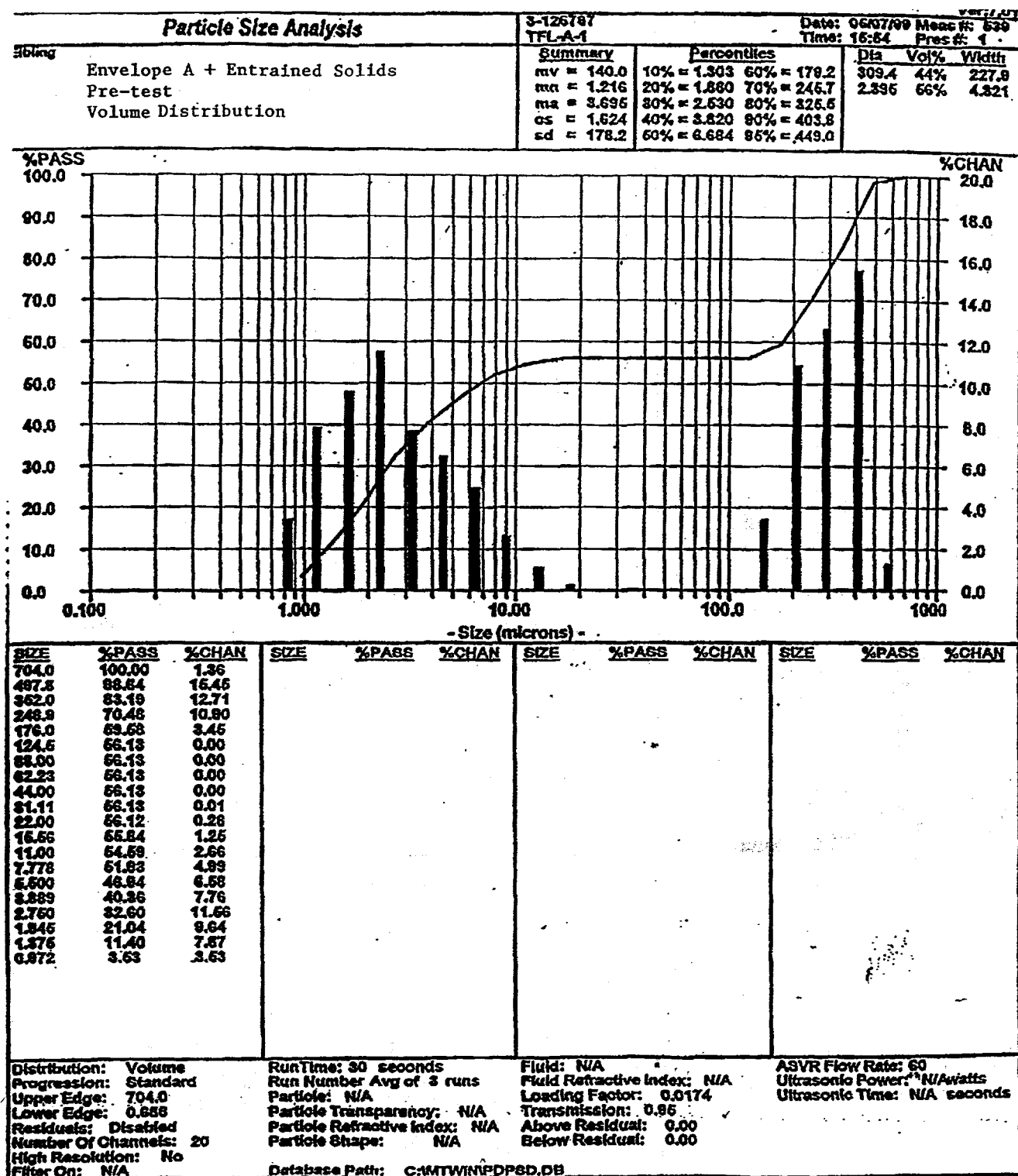


Figure E22A.Envelope A+ES Insoluble Solids Volume Distribution: Pre-test Sample
(125 mL sample of simulant was made prior to large batch)

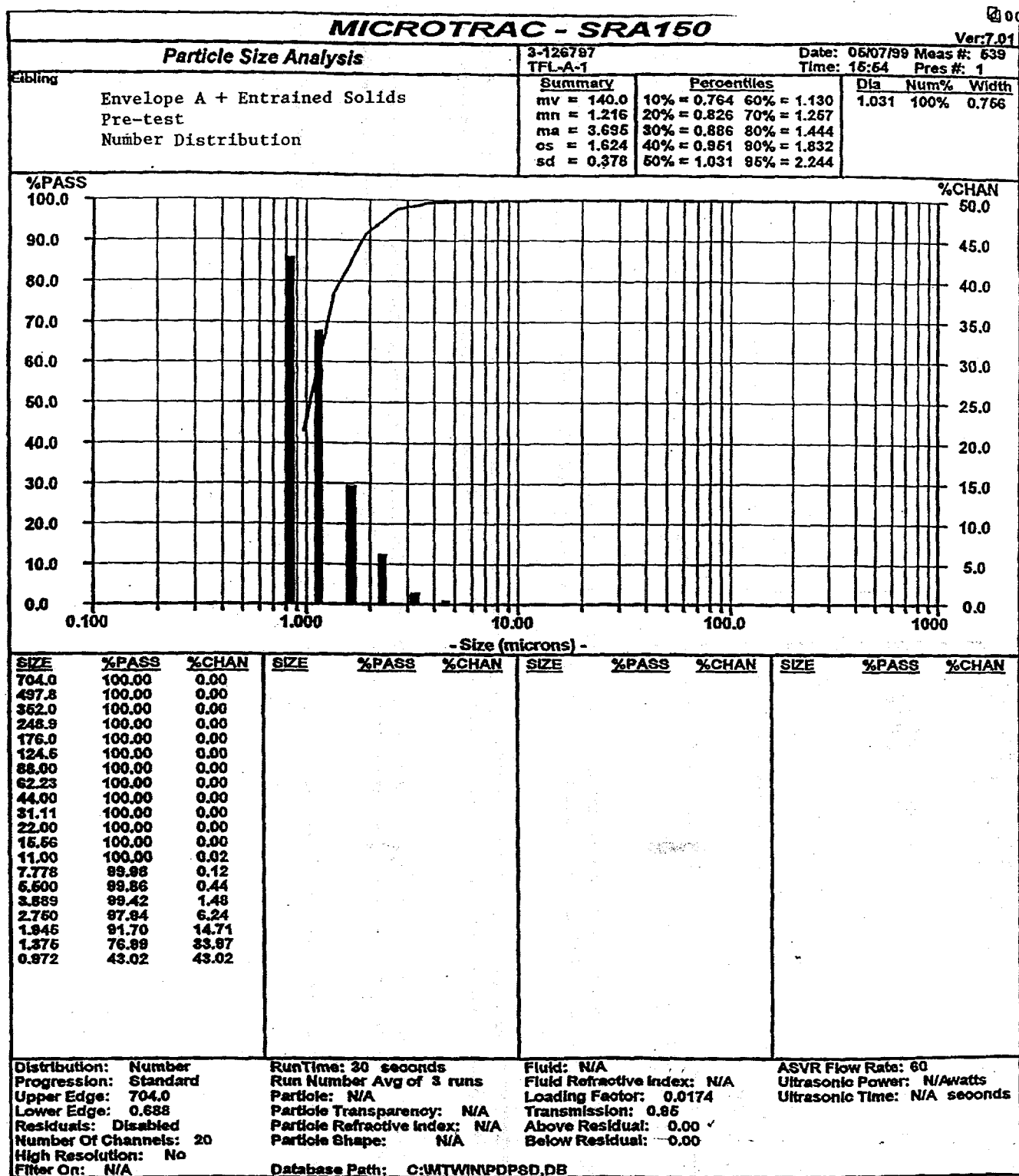


Figure E22B. Envelope A+ES Insoluble Solids Number Distribution: Pre-test Sample
 (125 mL sample of simulant was made prior to large batch)

06/10/99 THU 11:00 FRA

Ver:7.01

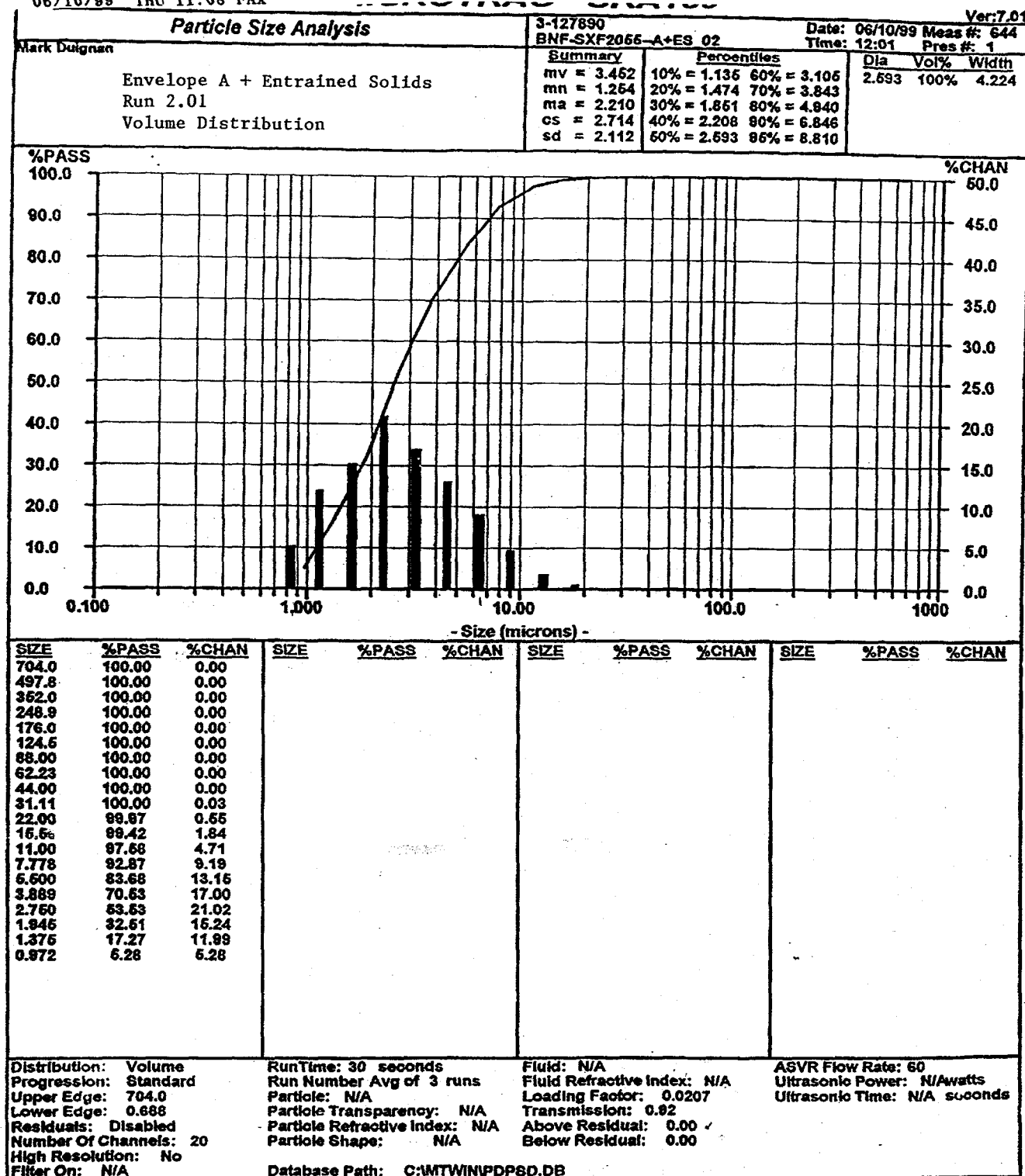


Figure E23A. Envelope A+ES Insoluble Solids Volume Distribution: Run 2.01
(Low-solids-concentration slurry experienced about 1 hour of circulation)

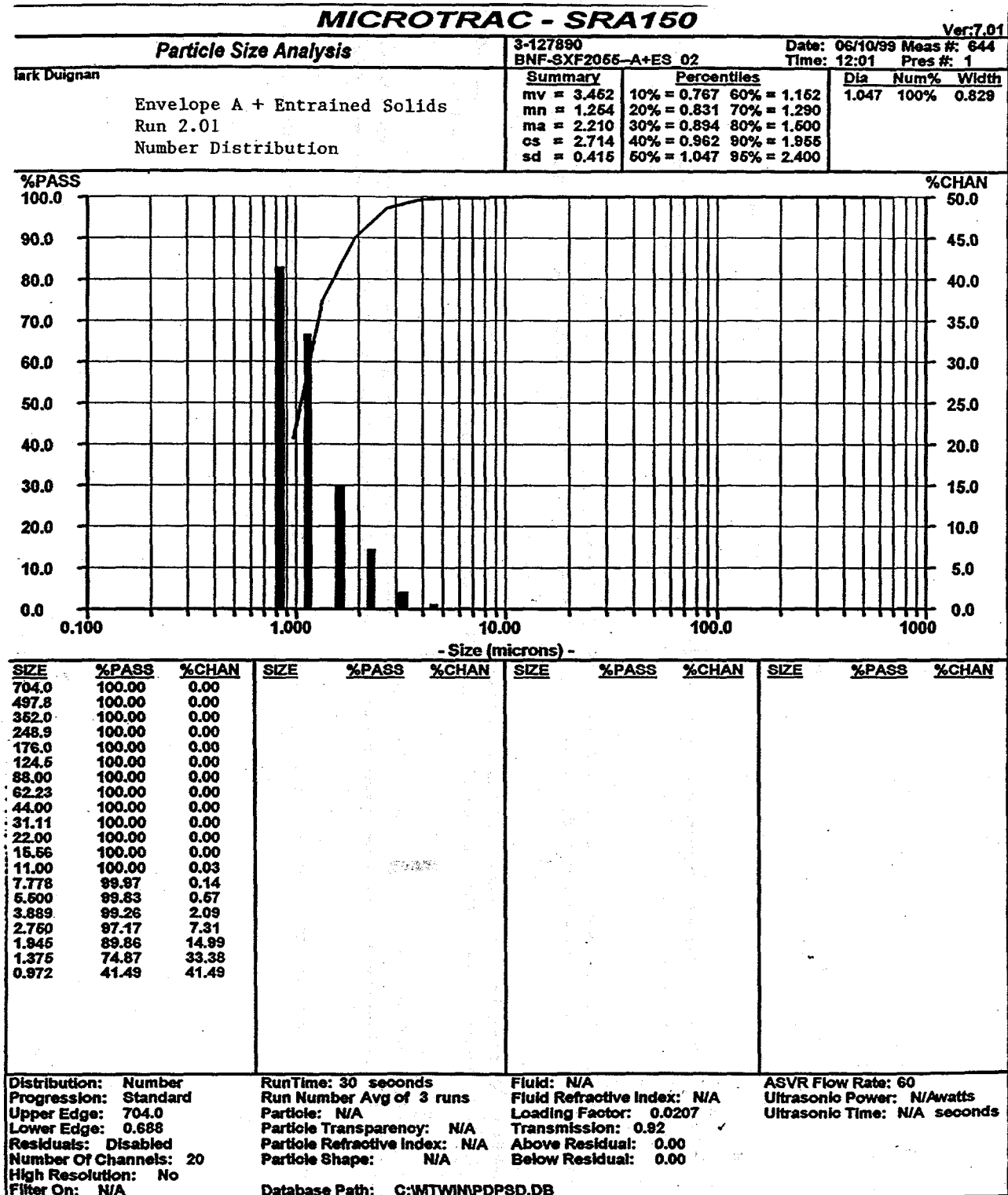


Figure E23B. Envelope A+ES Insoluble Solids Number Distribution: Run 2.01
 (Low-solids-concentration slurry experienced about 1 hour of circulation)

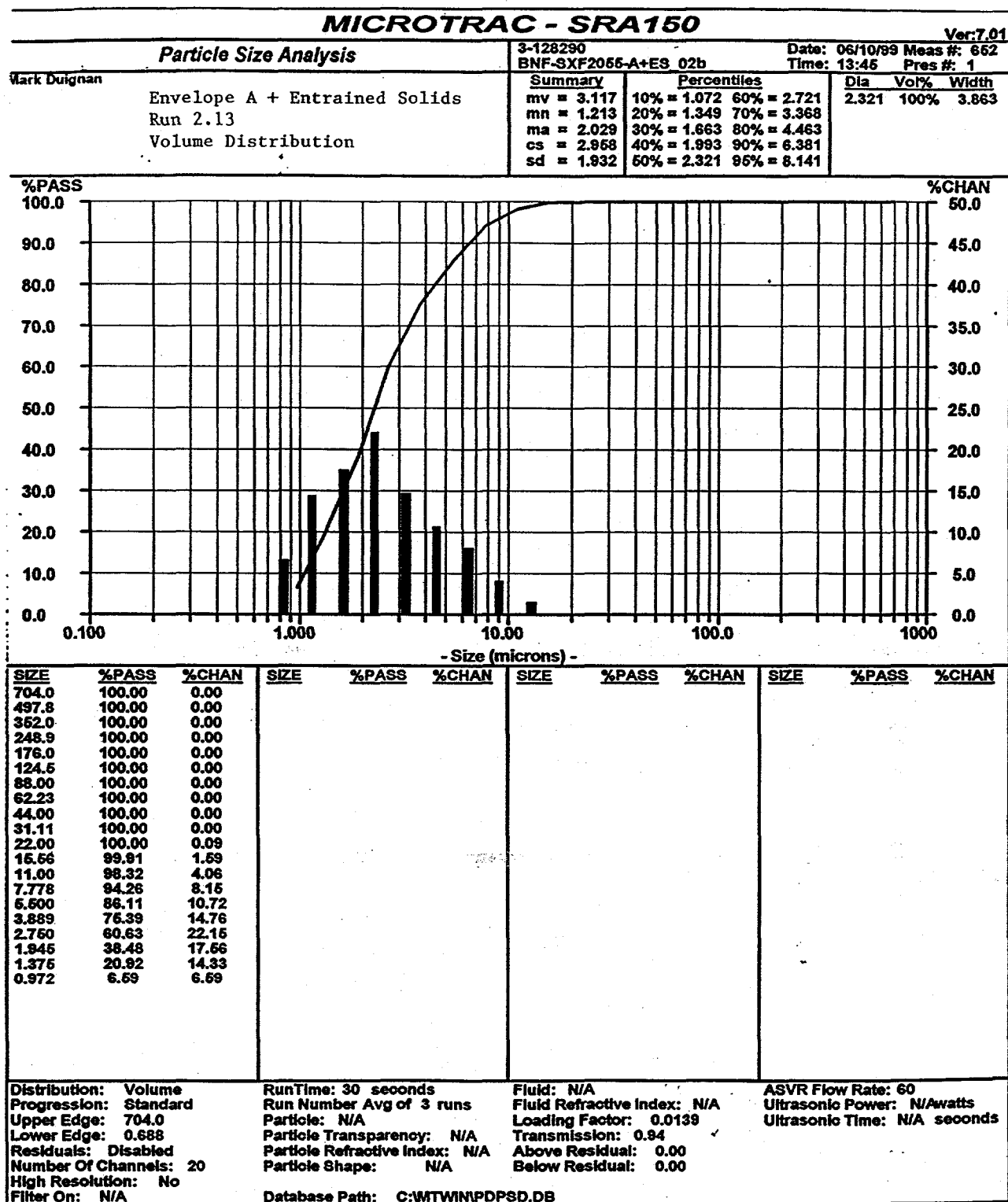


Figure E24A. Envelope A+ES Insoluble Solids Volume Distribution: Run 2.13
 (Low-solids-concentration slurry experienced about 24 hours of circulation)

06/10/99 THU 13:00 FAX

003

MICROTRAC - SRA150

Ver: 7.01

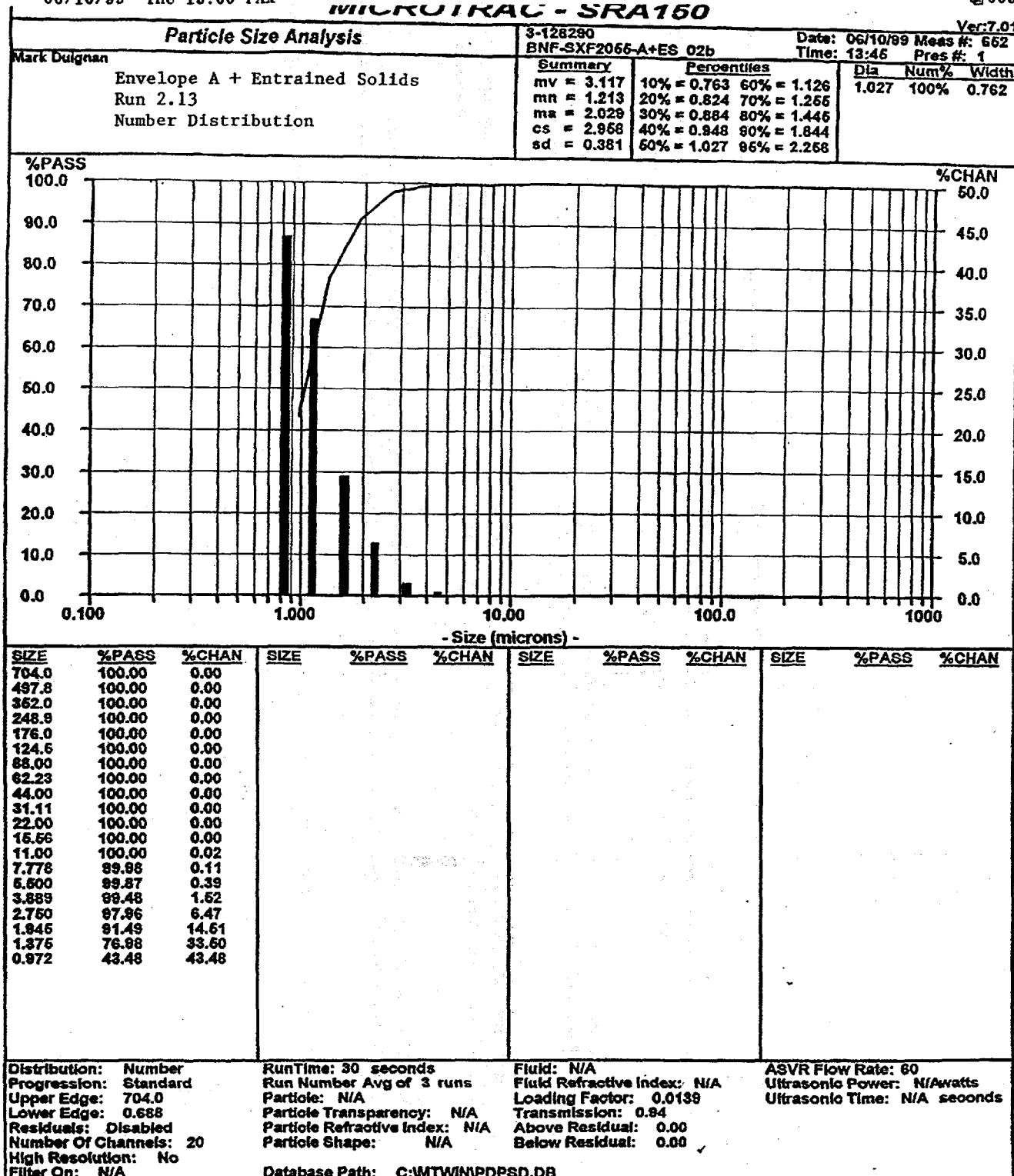


Figure E24B.Envelope A+ES Insoluble Solids Number Distribution: Run 2.13
(Low-solids-concentration slurry experienced about 24 hours of circulation)

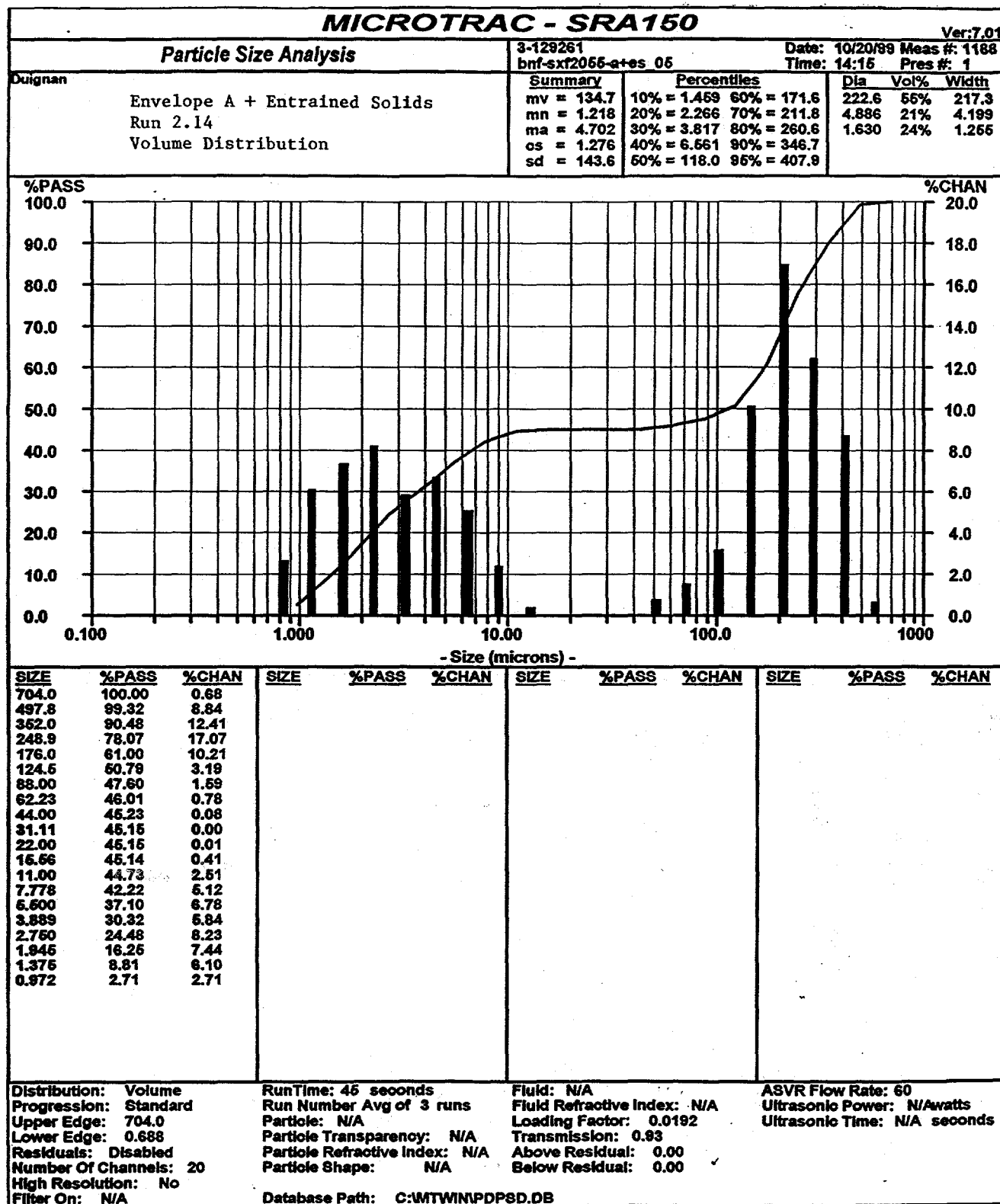


Figure E25A. Envelope A+ES Insoluble Solids Volume Distribution: Run 2.14
 (Slurry after new solids were added: Concentration approximately 9 wt%)

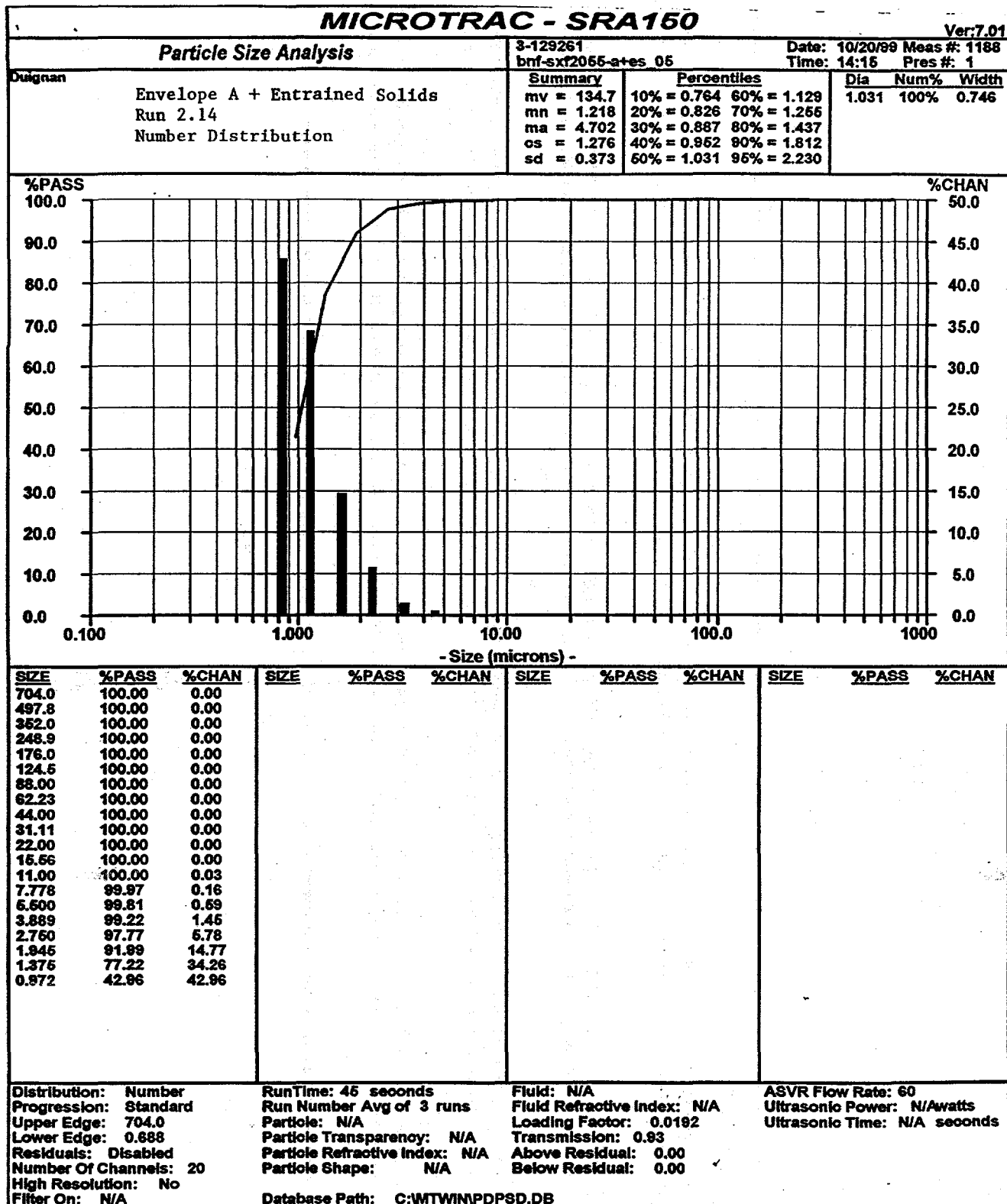


Figure E25B.Envelope A+ES Insoluble Solids Number Distribution: Run 2.14
(Slurry after new solids were added: Concentration approximately 9 wt%)

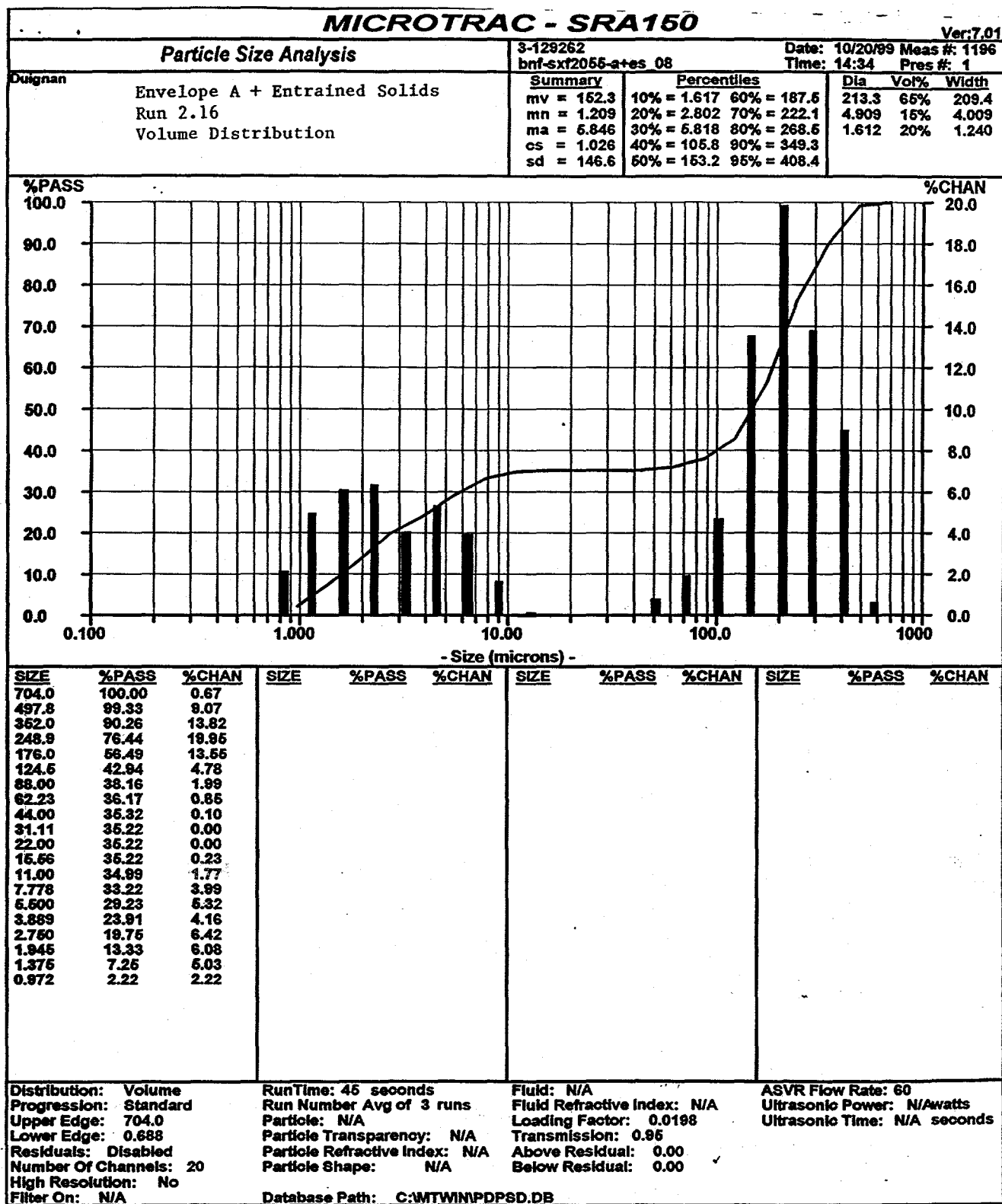


Figure E26A. Envelope A+ES Insoluble Solids Volume Distribution: Run 2.16
(Slurry after 2nd Wash)

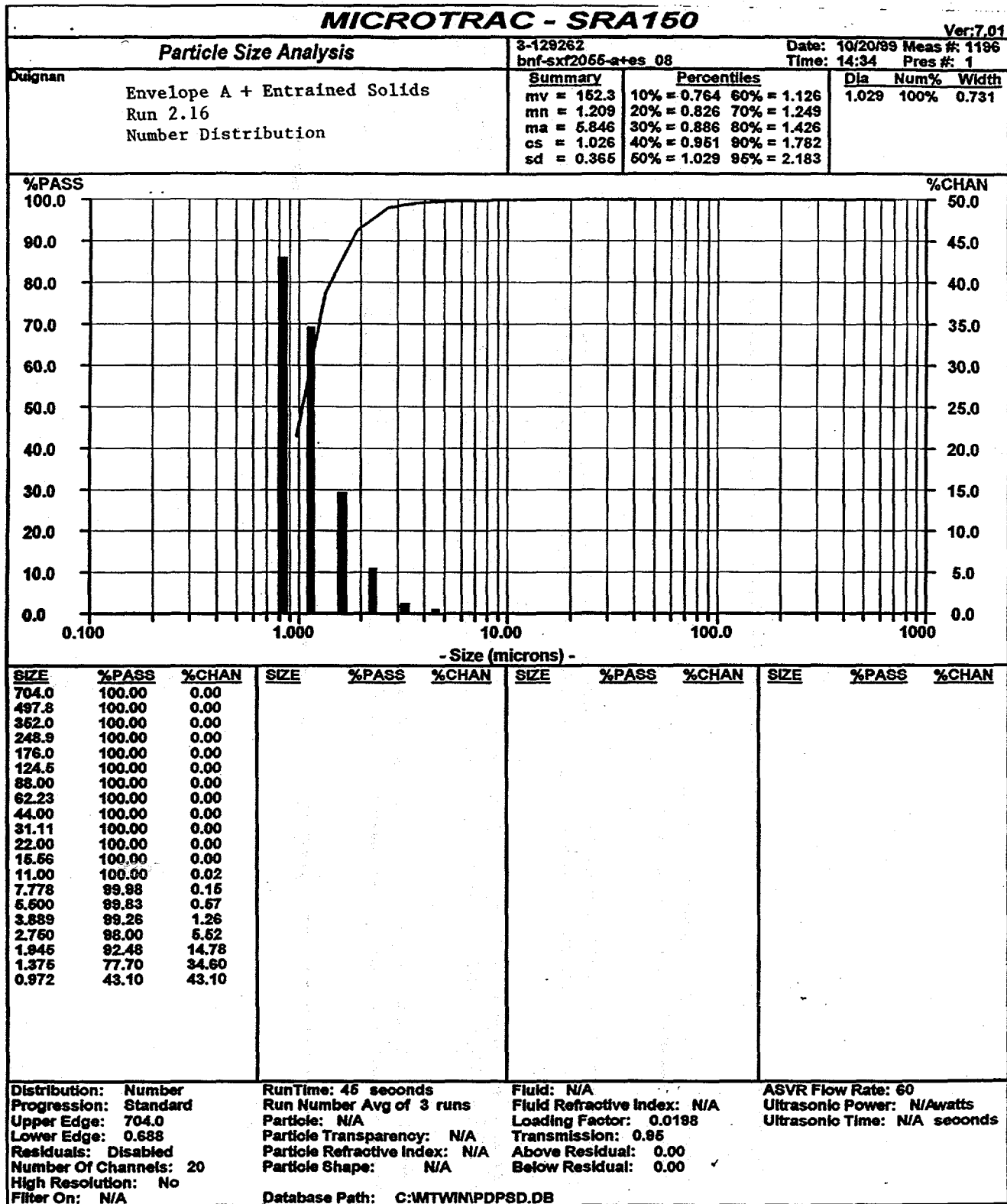


Figure E26B.Envelope A+ES Insoluble Solids Number Distribution: Run 2.16
(Slurry after 2nd Wash)

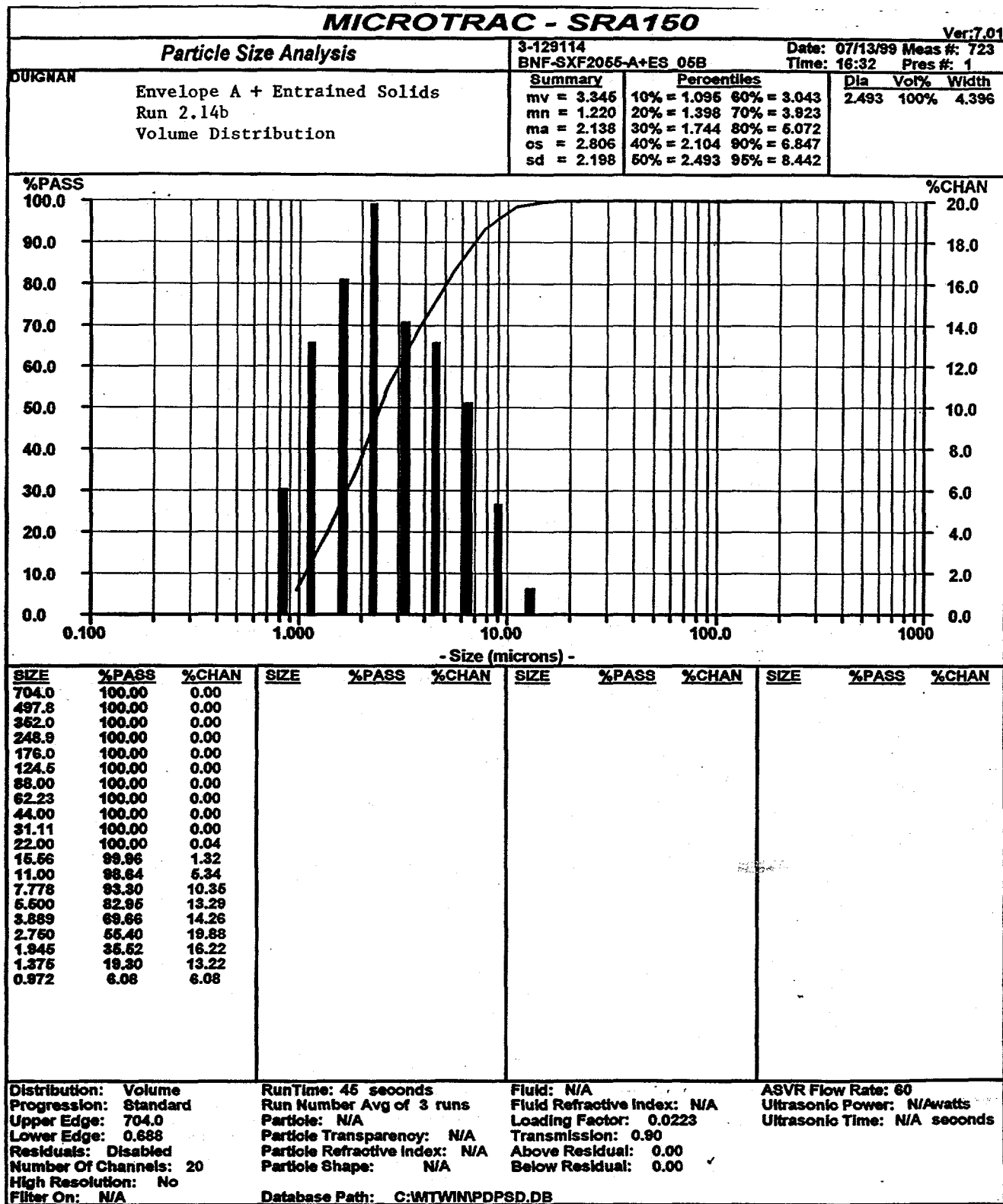


Figure E27A. Envelope A+ES Insoluble Solids Volume Distribution: Run 2.14b
 (Run 2.14 was redone after the slurry Na⁺ concentration was raised above 5 M)

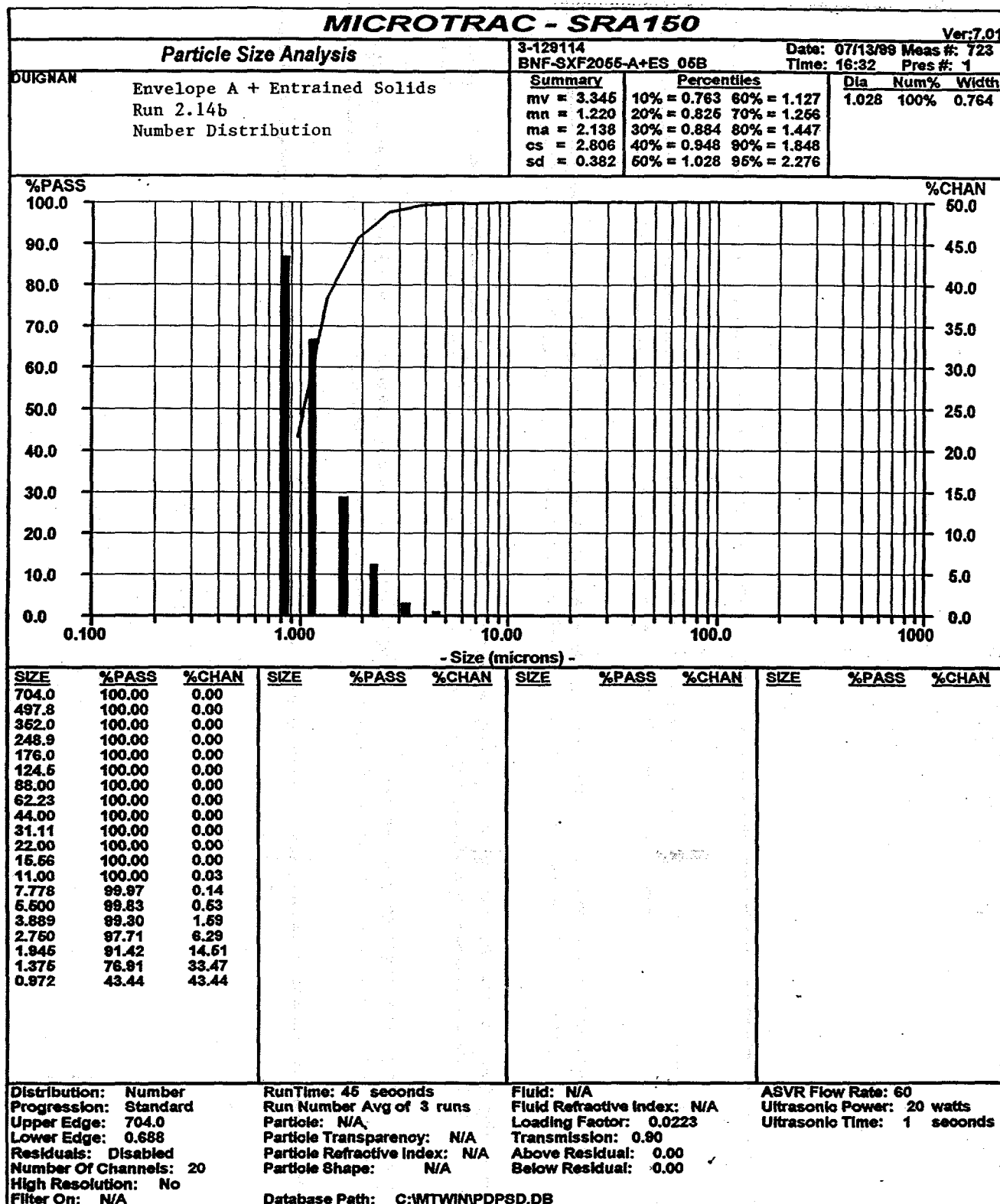


Figure E27B. Envelope A+ES Insoluble Solids Number Distribution: Run 2.14b
 (Run 2.14 was redone after the slurry Na⁺ concentration was raised above 5 M)

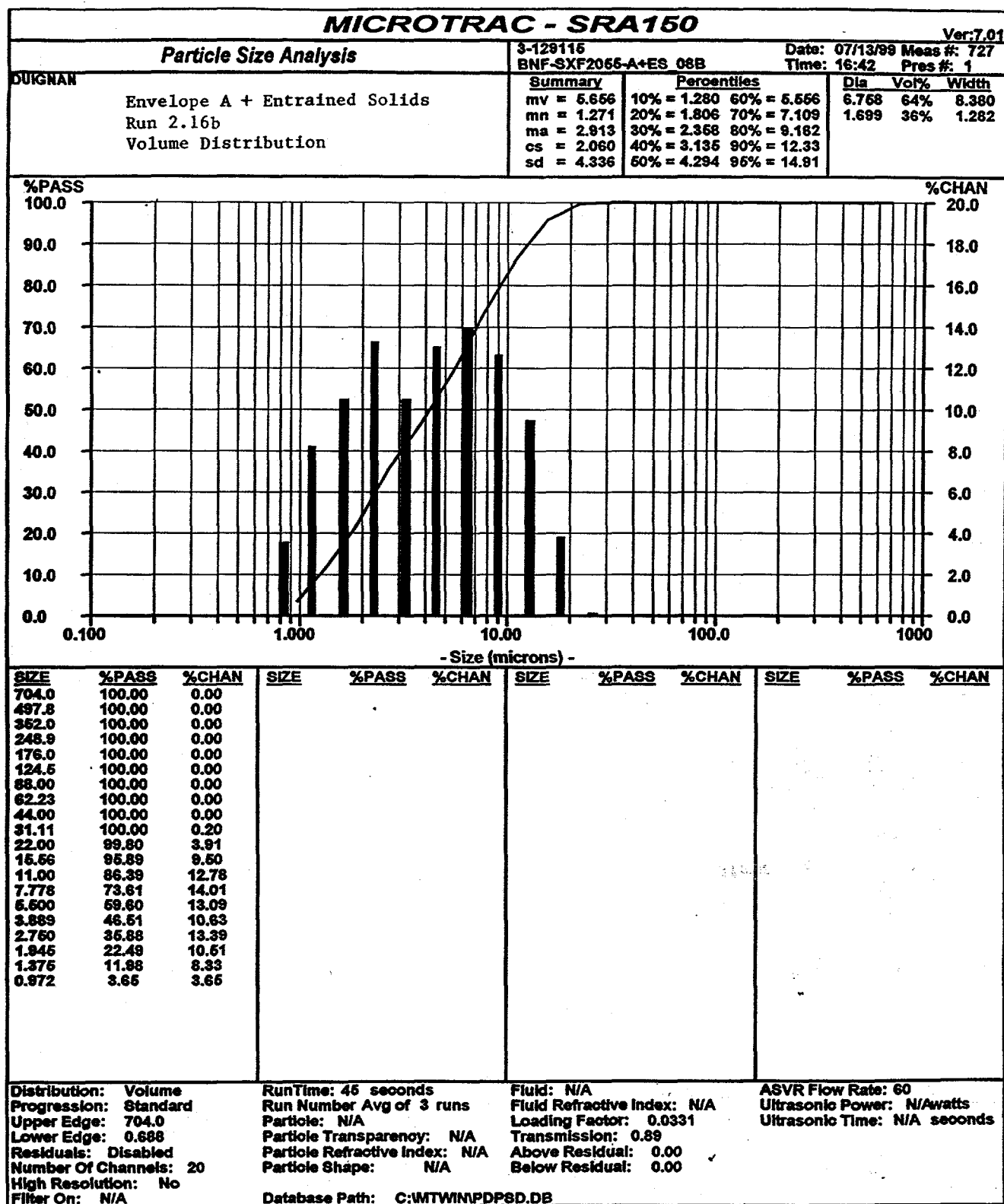


Figure E28A. Envelope A+ES Insoluble Solids Volume Distribution: Run 2.16b
(Slurry after 2nd Wash; 2nd attempt)

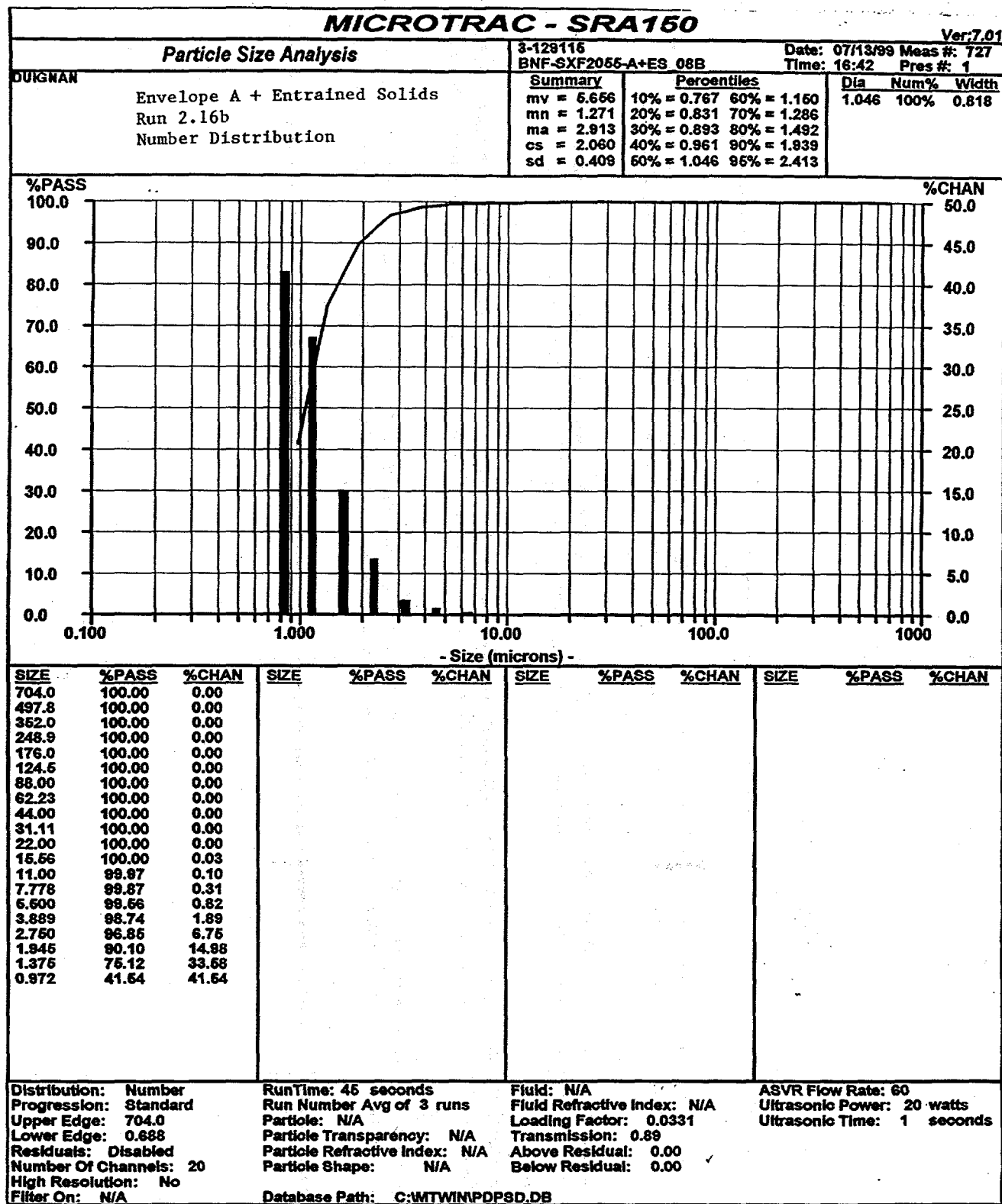


Figure E28B.Envelope A+ES Insoluble Solids Number Distribution: Run 2.16b
(Slurry after 2nd Wash; 2nd attempt)

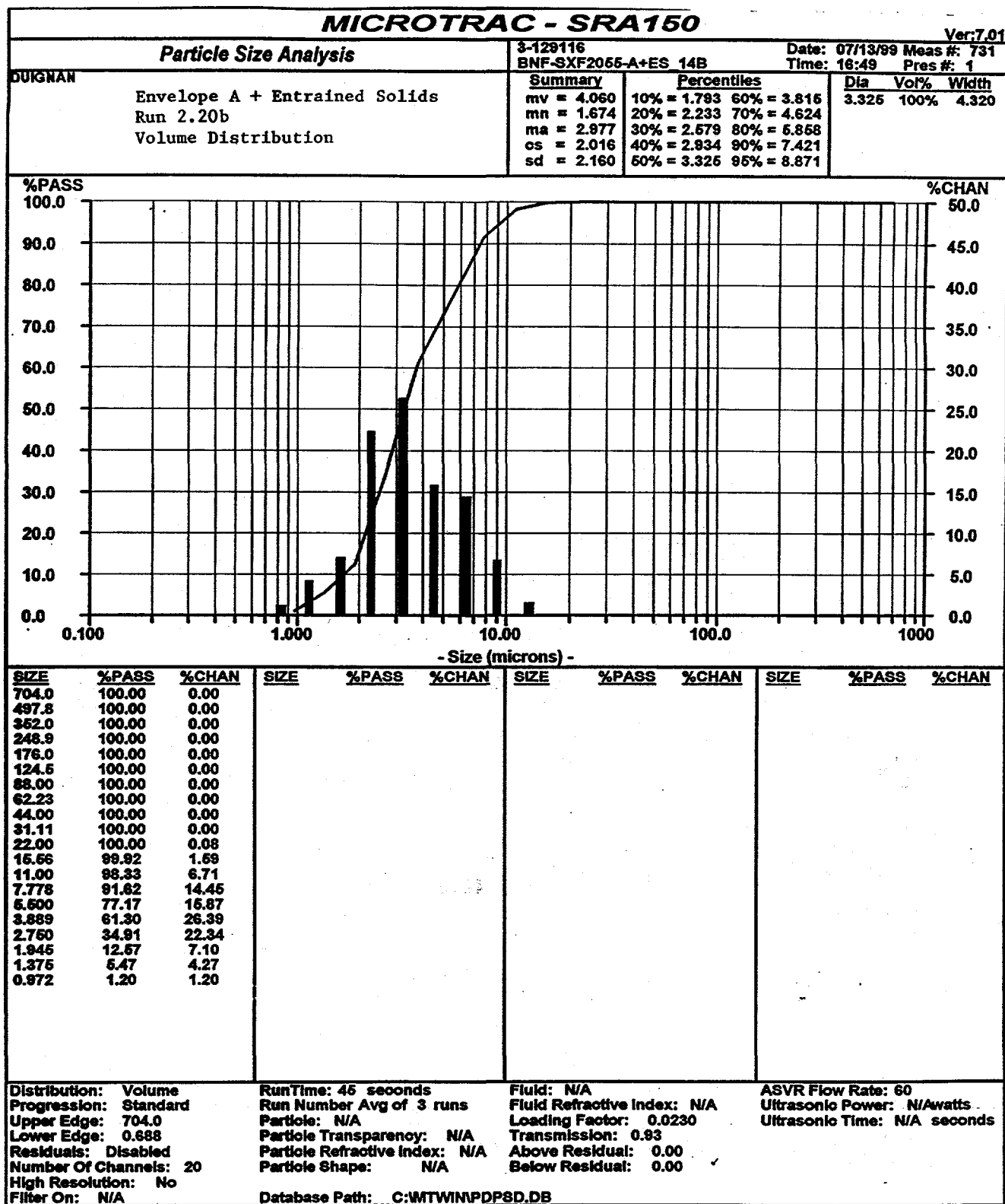


Figure E29A. Envelope A+ES Insoluble Solids Volume Distribution: Run 2.20b
 (Dewatering after wash test runs: sample was taken before dewatering)

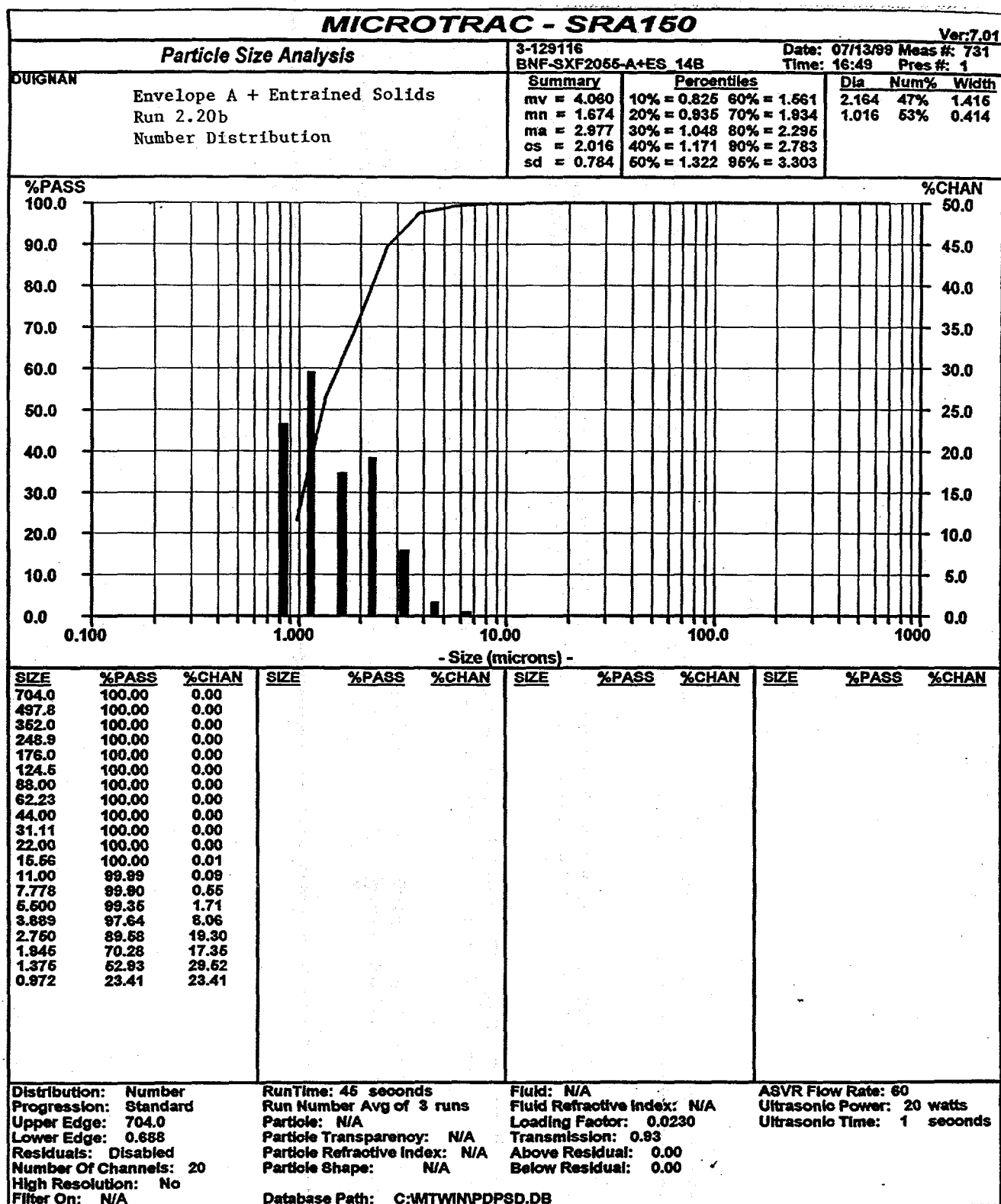


Figure E29B.Envelope A+ES Insoluble Solids Number Distribution: Run 2.20b
 (Dewatering after wash test runs: sample was taken before dewatering)

APPENDIX F

INSTRUMENTATION AND MEASUREMENT UNCERTAINTY

Appendix Contents

1. Experimental measurement uncertainty
2. Figure F1. Instrumentation used with their transfer functions
3. Figure F2. Pressure transducer locations
3. Figures F3 to F16. Calibration sheet for the 14 instruments

Special Note:

As mentioned in Appendix E, there are no measurement uncertainties listed for the analytical data they are beyond the scope and control of this task. There is reason to believe that all analytical data can be at least 15% accurate but no quantitative data are given to this effect.

EXPERIMENTAL MEASUREMENT UNCERTAINTY

As always, any measurement made has an attributed error which must be known before a level of confidence can be attained for the results obtained. This error may come from one or all of the following: the measurement instrument, the way an instrument is set up to make a measurement in relation to the experimental phenomenon to be measured, and the person using the instrument. It is not the purpose of this section to exhaust all possible avenues of measurement uncertainty, but rather to illustrate the level of measurement uncertainty in the results presented in Appendices A, B, C, D. (Outside of density and capillary viscometer measurements taken, the measurement uncertainty of the analytical data in Appendix E is beyond the scope of this task.) In general, the measurement uncertainties present here are for a reading or calculation at any instant. That is, the fluctuations that occur during experimentation are not addressed here. The magnitude of measurement fluctuations with time that occur during an experimental run can be seen at the bottom of each data table from the preceding appendices. Each column of data includes the average value of those data and their standard deviation.

In all the data sheets included in Appendices A, B, C, D there are raw data columns (all columns to the left of the Number column, which is usually column S) and there are calculated data columns to the right of the Number column. The uncertainty of a raw data measurement is the calibrated uncertainty of the individual instrument.

Example to find the measurement uncertainty of a raw data point:

1. Find the data column D in any Appendix A through D.
2. Check the column heading against the Nomenclature, included in the beginning of each Appendix, to find that the data in column D were obtained by Thermocouple T2.
3. Look up Thermocouple T2 on Fig. F1 in this Appendix to see that the average* calibrated uncertainty is 1.2°C (95% confidence level**). If a closer look on how that specific systematic error was obtained is desired, then check the appropriate calibration sheet. Thermocouple T2 is shown as Fig. F4. (The calibration sheets are in order of the fourteen instruments that are listed in Fig. F1, with the first instrument T1 shown in Fig. F3 and the last instrument Q3 shown in Fig. F16.)

[*A pre- and post-test calibration was done on each instrument. For this example, the measurement uncertainties for T2 were 1.3°C and 1.1°C respectively, see Fig. F1. The true instrument uncertainty was somewhere between the pre- and post-test results. For this task each uncertainty was given equal weight, therefore an "average" of the two numbers was used, i.e., 1.2°C.

**The confidence level comes from the Student's *t* distribution function used in determining an instrument uncertainty.]

4. The magnitude of the random error can be obtained from the standard deviation shown at the bottom of each column of raw data. The standard deviation from the average value, obtained from a specific instrument for a specific test run, will be a good indication of random error for all but the filtrate flowrates, Q2 and Q3. Temperatures, pressures, and slurry flowrates were maintained constant, therefore the fluctuations around the mean should be normally distributed. The filtrate flowrates decreased with time, due to the nature of the experiment. Therefore, the random error for Q2 and Q3 should only be obtained when the filtrate flowrates reach some

asymptote. (In some rare cases, like on Run 2.20b when the goal was to dewater the slurry until pluggage occurred the temperature could not be held constant, but increased with time. In these cases the standard deviation will not properly represent random fluctuations. To facilitate the evaluation of such occurrences each column of data also has the maximum, minimum, and median values along with the average and standard deviation. Note that the number of points used to determine these values is also given. Extreme points, like when backpulsing occurs were excluded. With the number of data points known the standard error of the mean may be obtained (i.e. standard error = standard deviation / square root (number of points)) [Ref. 16].

Measurement uncertainties for the calculated results can be obtained by the general method of the Law of Propagation of Errors (section 4.7 of Ref. 23). The derivation will not be given here and the following is just one example for one type of relation, albeit a common relation.

For example, a calculated entity has an uncertainty of δa . The entity a is a function of three measured quantities: b , c , and d by the following relationship: $a = b \times c / d$ and these quantities have measurement uncertainties of δb , δc , and δd , respectively. The uncertainty can be shown as:

$$(\delta a)^2 = [(\partial a / \partial b) \delta b]^2 + [(\partial a / \partial c) \delta c]^2 + [(\partial a / \partial d) \delta d]^2,$$

if the error terms are independent and symmetrical. The term δa is squared to capture both the negative and positive error terms.

Then for the relation $a = bc/d$ the relative uncertainty can be shown to be:

$$\delta a/a = [(\delta b/b)^2 + (\delta c/c)^2 + (\delta d/d)^2]^{1/2}. \quad (1)$$

Using the above the relation (1) an uncertainty for velocity, transmembrane pressure, filtrate flux, and permeability are determined. The method of determining the measurement uncertainty of any of the calculated results will be the same as the following analyses. However, only one example of each calculated result is shown below. To show an example, any specific calculated quantity is sufficient. An arbitrary choice of a representative group of results is: Run 2.01 at the 120th minute [The data for Run 2.01 can be found in Appendix B in the first table and the 120th minute is row 135.]

The measurement uncertainty for the following values will be shown:

V, ft/s	TMP, psi	Fc (at 25°C), gpm/ft ² ,	P, gpm/ft ² /psi
6.4	31.8	0.085*	0.00267

*actual temperature was 30.6°C but was adjusted to 25°C as per the customer specification, Ref. 3, therefore Fc means the corrected filtrate flux.

The results of the measurement uncertainties found below at the 95% confidence level are:

Slurry Velocity	=	V	± 8.16 %
Transmembrane Pressure	=	TMP	± 1.07 %
Temperature Corrected Filtrate Flux	=	Fc	± 6.72 %
Permeability	=	P	± 6.80 %

F.1 Velocity [$V = Q1 / A_{\text{cross-section}}$]

This uncertainty is combination of the instrument, $Q1$, uncertainty and from the lack of knowledge of the exact inside diameters of the filter tubes. The instrument uncertainty is obtained for that instrument's calibrated uncertainty. An accurate measurement of the average inside diameter of the filtrate tubes was impossible since it may vary down the length for each filter tube and may vary from tube to tube. Even measuring the diameter at the filter tube ends is difficult because of the weldments to the tube sheets. What will be used is the manufacturer's tolerances. For a Mott 3/8-inch tube the diameter tolerances are stated by the vendor to be +0.025 inch and -0.005 inch. The diameter of the filter tubes can presumably vary anywhere between those tolerances therefore for this task the diameter uncertainty will be taken as the average tolerance, i.e., ±0.015 inch.

The measurement uncertainty estimate:

Calibrated uncertainty (Figs. F1 and F14): $\delta Q1 = \pm 0.25$ gpm

Slurry flow rate: $Q1 = 15.54$ gpm [Run 2.01, Row 135, Column P: Appendix B]

Filter tube inside diameter: $\delta d = \pm 0.015$ inch

Filter tube inside diameter: $d = 0.375$ inch

$$V = Q / A = Q1 / (\pi d^2 / 4)$$

$$\text{In the form of Eq. (1): } \delta V / V = [(\delta Q1 / Q1)^2 + 4(\delta d / d)^2]^{1/2}$$

[Note the multiplier 4. This results from the derivation $\partial V / \partial d$ because of the exponent]

$$\text{Therefore, } [(0.25/15.54)^2 + 4(0.015/0.375)^2]^{1/2} \times 100\% = \pm 8.16 \%$$

The uncertainty of the example V is: 6.4 ± 0.6 ft/s

[since $6.4 \times 0.0816 \sim 0.52$]

F.2 Transmembrane Pressure [$TMP = (dP2 + dP3) / 2$]

This uncertainty is will come from two instruments, $dP2$ and $dP3$. Also, there is another uncertainty do to location of the pressure taps. As seen in Figs. 1 and F2, $dP2$ is located at the bottom to the filter housing (upstream to the filter) and $dP3$ is located at the top of the filter housing (downstream to the filter). Due to the same fluid being in the pressure lines

(water) a liquid-filled system will give the corrected pressure drops, however, the slurry pressures lost upstream to the filter and gained downstream of the filter are not symmetrical and therefore do not cancel out. With this said, this addition to the uncertainty is small compared to the assumption that true TMP is represented by the average of two pressures at the ends of a filter. Because the filter is oriented perpendicular to gravity and the flow causes a pressure and concentration gradient along the entire tube wall it is not clear what TMP would be representative of the entire filter unit. On the other hand, the way measurements were taken probably will be similar to the field use of this filter and therefore a good measurement for design purposes. The uncertainty is actually the uncertainty of two measurement devices, and nothing more. Finally, the Law of Propagation of Errors by Eq. (1) does not lend itself to additive contributions to uncertainties. Fortunately, the two quantities are similar in magnitude and calibrated uncertainty. Equation (1) will be used as long as it give an uncertainty larger than the largest calibrated uncertainty for the two pressure transducers.

The measurement uncertainty estimate:

Calibrated uncertainty (Figs. F1 and F12): $\delta dP2 = \pm 0.23$ psi

Pressure drop: $dP2 = 33.13$ psid [Run 2.01, Row 135, Column J: Appendix B]

Calibrated uncertainty (Figs. F1 and F13): $\delta dP3 = \pm 0.25$ psi

Pressure drop: $dP3 = 30.49$ psid [Run 2.01, Row 135, Column M: Appendix B]

$$TMP = (dP2 + dP3) / 2$$

$$\text{In the form of Eq. (1): } \delta TMP / TMP = [(\delta dP2 / dP2)^2 + (\delta dP3 / dP3)^2]^{1/2}$$

$$\text{Therefore, } [(0.23/33.13)^2 + (0.25/30.49)^2]^{1/2} \times 100\% = \pm 1.07 \%$$

The uncertainty of the example TMP is: 31.8 ± 0.4 psid

[since $31.8 \times 0.0107 \sim 0.34$]

F.3 Filtrate Flux [$F = Q2 / A_{\text{inner-surface}}$]

This uncertainty is combination of the instrument, $Q2$, uncertainty and from the lack of knowledge of the exact inside diameters and length of the filter tubes. The instrument uncertainty is obtained for that instruments calibrated uncertainty. The uncertainty of the inside diameter of the filter tubes has already been addressed in section F.1 and it was estimated at 0.015 inch. The uncertainty of the length of the filter tubes was estimate from in-house measurements. The requested tube length from the manufacturer was 40 inches. Because of weldments at the ends and the center (the 40-inch length was made of two 20-inch tube sections) the active length seemed closer to 39 7/8 inches. However, since it was difficult to get an exact measurement, not being able to measure inside, the 40-inch length was used to determine the inner surface area and the 1/8-inch difference will be used for the length uncertainty.

The measurement uncertainty estimate:

Calibrated uncertainty (Figs. F1 and F15): $\delta Q_2 = \pm 0.009$ gpm

Filtrate flow rate: $Q_2 = 0.227$ gpm [Run 2.01, Row 135, Column Q: Appendix B]

Tube inside diameter uncertainty: $\delta d = \pm 0.015$ inch (from manufacturer)

Tube inside diameter: $d = 0.375$ inch

Tube length uncertainty: $\delta L = \pm 0.125$ inch

Tube length: $L = 40$ inches

$$F = Q/A = Q_2 / \pi d L$$

In the form of Eq. (1): $\delta F/F = [(\delta Q_2/Q_2)^2 + (\delta d/d)^2 + (\delta L/L)^2]^{1/2}$

Therefore, $[(0.009/0.227)^2 + (0.015/0.375)^2 + (0.125/40)^2]^{1/2} \times 100\% = \pm 5.64 \%$

The uncertainty of the example F is: 0.085 ± 0.005 gpm/ft²

[since $0.085 \times 0.0564 \sim 0.0048$]

F.3.1 Effect of Temperature on the Measurement Uncertainty on F

As per the customer specification the filtrate flux was to adjusted such that it would give a result at 25°C. The equation as was stated is:

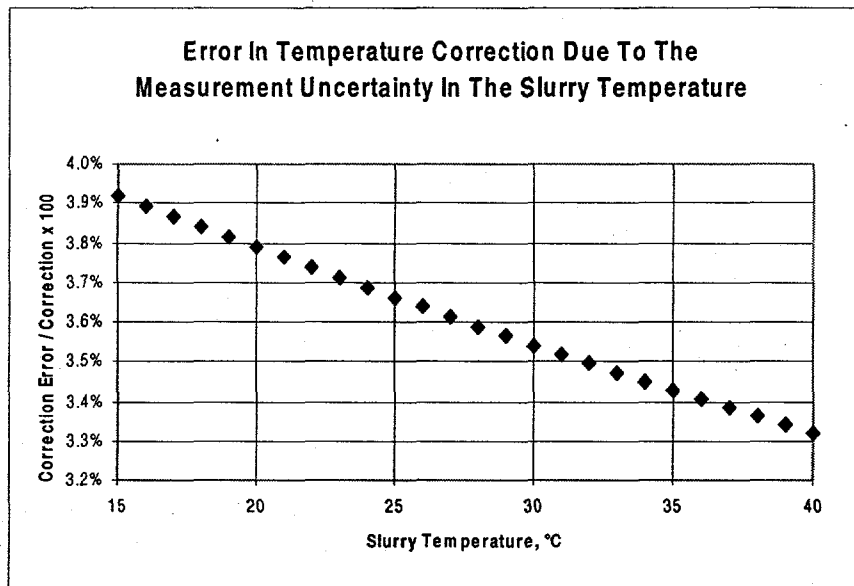
$$F = Q_2(\text{Temperature}) / \text{Area} = Q_2 \times \text{Correction Factor} / \text{Area}$$

$$CF = e^{[2500((1/273 + \text{Slurry Temperature}) - (1/298))]}$$

Only the correction factor's effect on measurement uncertainty is dealt with here. The equation is accepted as error free, i.e., method, constants, etc. Only the uncertainty of the temperature measurement which leads to the correction will be addressed.

Generally, the adjustment to F is small because, whenever possible, the slurry's operational temperature was maintained at 25°C which would result in a zero adjustment. However, the example chosen to show measurement uncertainty had a temperature difference of 5.6°C. That is, for Run 2.01 at the 120th minute the slurry temperature was 30.6°C [Initial test runs were only cooled with water cooling coils which were not sufficient. The temperature was better maintained after the coolant was changed to ethylene glycol.]. Unfortunately, the fact that a temperature correction is applied means the temperature uncertainty will effect the calculated result at any temperature. That is, even if the slurry temperature were 25°C, which would make the correction = 1.0, the uncertainty of that temperature and thereby the correction, leads to an inherent uncertainty of value that is being corrected, i.e, F. For this task the slurry temperature was measured with thermocouple T1, which had a calibrated measurement uncertainty of $\pm 1.3^\circ\text{C}$ [see Fig. F1]. If at 25°C the temperature has an uncertainty of $\pm 1.3^\circ\text{C}$, then the

correction can be either 0.9642 to 1.0374, or approximately $\pm 3.66\%$ [i.e., $((1 - 0.9642) + (1.0374 - 1)) / 2 / 1.00 = 0.0366$]. To show the measurement uncertainty mathematically from the correction equation is beyond the scope of this task, however it can be shown graphically. For a range of slurry temperatures from 15°C to 40°C , then the correction can be shown to change from 1.34 to 0.67, respectively. However, with a measurement uncertainty of $\pm 1.3^\circ\text{C}$ this factor can be in error from approximately 3.9% to 3.3%, respectively, see the Figure below:



Therefore, for the sake of this example the relative uncertainty of the correction factor due to the temperature will be assumed to be 3.7% since most of the data were obtained at 25°C . Using this constant value is not a bad assumption because between 20°C and 30°C this uncertainty only fluctuates by approximately 0.1%.

This increased uncertainty to the filtrate flux is then a combination of two uncertainties already calculated above for F and the correction factor. The analyses still follows Eq. (1) therefore:

The measurement uncertainty estimate:

Filtrate flux relative uncertainty: $\delta F/F = \pm 5.64\%$ [section F.3]

Correction factor relative uncertainty: $\delta CF/CF = \pm 3.66\%$ [section F.2]

$$F_{\text{corrected}} = F \times CF$$

In the form of Eq. (1): $\delta F_c/F_c = [(\delta F/F)^2 + (\delta CF/CF)^2]^{1/2}$

$$\text{Therefore, } [(5.64)^2 + (3.66)^2]^{1/2} = \pm 6.72\%$$

The uncertainty of the example F_c is: 0.085 ± 0.006 gpm/ft²

[since $0.085 \times 0.0672 \sim 0.0057$]

F.4 Permeability [$P = F / TMP$]

This uncertainty is combination of two uncertainties already calculated above, in section F.2 and F.3. The analyses still follows Eq. (1) therefore:

The measurement uncertainty estimate:

Filtrate flux relative uncertainty: $\delta F_c / F_c = \pm 6.72\%$ [section F.3]

TMP relative uncertainty: $\delta TMP / TMP = \pm 1.07\%$ [section F.2]

$$P = F_c / TMP$$

In the form of Eq. (1): $\delta P / P = [(\delta F_c / F_c)^2 + (\delta TMP / TMP)^2]^{1/2}$

Therefore, $[(6.72)^2 + (1.07)^2]^{1/2} = \pm 6.80\%$

The uncertainty of the example F is: 0.00267 ± 0.00018 gpm/ft²/psi

[since $0.00267 \times 0.0680 \sim 0.000182$]

F.5 Second-Order Effects to Measurement Uncertainty

There were other effects on the measurement uncertainty which are not included because they are thought to be of second order. For example, since the test rig was very tall, approximately 30 feet, it was subjected an ambient temperature gradient. Ambient temperatures at the bottom of the rig were usually less than at the top. For the example used in this section, [Run 2.01, Row 135, Columns G and H: Appendix B], the temperatures were 26.1°C and 27.3°C, respectively. This gradient varied hourly and daily for several reasons and it larger or smaller. Most importantly, the 1.2°C temperature variation shown in this example is on the same order of magnitude as the calibrated uncertainties for the thermocouples. Further, the slurry in the loop generally flowed fast, so the residence time in any one section of the rig was small. For Run 2.01 the flow rate was, $Q_1 = 15.5$ gpm. The loop volume was approximately 5 gallons so a fluid particle traversed the loop every $5/15.5 \times 60 \sim 19$ seconds. [Note that the slurry flow rate for Run 2.01 was one of the slowest.] In this example, the slurry temperature was measured to be 30.6°C, from one thermocouple located in the suction line of the pumps. While it is certain that the ambient temperatures had an effect on the slurry temperature it was small and at steady state the effect is incorporated in the slurry temperature. The same is true for the ambient temperature gradient but to a lesser extent and therefore not considered.

INSTRUMENTS USED ON THE BNFL PILOT-SCALE CROSS-FLOW FILTRATION TEST

(PRINTED: March 9, 2000)

Test Rig No.	Instrument	M&TE #	Make	Model	Calibrated Range	Uncertainty (pre-test)	Uncertainty (post-test)	Uncertainty Average**	Curve Fit
T1	Thermocouple	TR-02925	OMEGA	TJ36-CXSS-18U-6-SB-OST-M	0 to 100C	1.2C	1.4C	1.3C	$= 0.00483 + 17.040918 \times \text{mV} - 0.224264 \times \text{mV}^2 + 0.005038 \times \text{m}$
T2	Thermocouple	TR-02926	OMEGA	TJ36-CXSS-18U-6-SB-OST-M	0 to 100C	1.3C	1.1C	1.2C	$= 0.00483 + 17.040918 \times \text{mV} - 0.224264 \times \text{mV}^2 + 0.005038 \times \text{m}$
T3	Thermocouple	TR-02929	OMEGA	TJ36-CXSS-18U-6-SB-OST-M	0 to 100C	1.5C	1.2C	1.3C	$= 0.00483 + 17.040918 \times \text{mV} - 0.224264 \times \text{mV}^2 + 0.005038 \times \text{m}$
T4	Thermocouple	TR-02930	OMEGA	TJ36-CXSS-18U-6-SB-OST-M	0 to 100C	1.2C	1.4C	1.3C	$= 0.00483 + 17.040918 \times \text{mV} - 0.224264 \times \text{mV}^2 + 0.005038 \times \text{m}$
T5	Thermocouple	TR-02927	OMEGA	TJ36-CXSS-18U-6-SB-OST-M	0 to 100C	1.0C	1.4C	1.2C	$= 0.00483 + 17.040918 \times \text{mV} - 0.224264 \times \text{mV}^2 + 0.005038 \times \text{m}$
P1	Pres. Transducer	TR-02917	Rosemount	1151GPE2A100862L4	0 to 100 PSIG	0.13 PSIG	0.21 PSIG	0.17 PSIG	$P(\text{PSIG}) = 6.211 \times \text{mA} - 24.895$
P2	Pres. Transducer	TR-03109	Rosemount	1151DP6E22	-10 to 90 PSIG	0.09 PSIG	0.17 PSIG	0.13 PSIG	$P(\text{PSIG}) = 6.293 \times \text{mA} - 35.524$
P3	Pres. Transducer	TR-02145	Rosemount	11440-0200A22	0 to 150 PSIG	0.38 PSIG	0.41 PSIG	0.40 PSIG	$P(\text{PSIG}) = 9.422 \times \text{mA} - 37.712$
dP1	Pres. Transducer	TR-03495	Rosemount	1151DP5E22	0 to 26 PSID	0.02 PSID	0.068 PSID	0.056 PSID	$P(\text{PSID}) = 1.6249 \times \text{mA} - 6.4930$
dP2	Pres. Transducer	TR-00532	Rosemount	1151AP6E22M301P1	0 to 250 PSIG	0.42 PSID	NA	0.42 PSID	$P(\text{PSID}) = 15.648 \times \text{mA} - 62.400$
dP2 (after 3/25/99)	Pres. Transducer	TR-00532	Rosemount	1151AP6E22M301P1	0 to 100 PSIG	0.13 PSID	0.33 PSID	0.23 PSID	$P(\text{PSID}) = 6.314 \times \text{mA} - 25.227$
dP3	Pres. Transducer	TR-03115	Rosemount	1151DP7E22M301P1	-10 to 100 PSIG	0.19 PSIG	0.30 PSIG	0.25 PSID	$P(\text{PSID}) = 6.898 \times \text{mA} - 37.854$
Q1	Mag. Flowmeter	TR-20350	Fischer-Porter	1001475DK11PL28QD11CAC	0 to 50 GPM	0.19 GPM	0.33 GPM	0.26 GPM	$Q(\text{GPM}) = 3.137 \times \text{mA} - 12.509$
Q2	Mag. Flowmeter	TR-20353	Fischer-Porter	1001475BN01PF28QW12CAC2	0 to 1.2 GPM	0.005 GPM	0.019 GPM	0.012 GPM	$Q(\text{GPM}) = 0.075 \times \text{mA} - 0.299$
Q3	Mag. Flowmeter	TR-03562	Fischer-Porter	1001475CNB11BBL1	0 to 5 GPM	0.02 GPM	0.01 GPM	0.015 GPM	$Q(\text{GPM}) = 0.311 \times \text{mA} - 1.237$
DAS Channel	Instrument			DAS Calibration					Transfer Functions Used with the DAS
6	P1			Chan06 = 0.4975mA - 5E-15					Conversion from mA to Volts
7	P2			Chan07 = 0.4988mA + 0.003					$P(\text{PSIG}) = 12.4844 \times \text{V} - 24.895$
8	P3			Chan08 = 0.498mA + 0.002					$P(\text{PSIG}) = 12.616 \times \text{V} - 35.561$
9	dP1			Chan09 = 0.4988mA + 0.003					$P(\text{PSIG}) = 18.960 \times \text{V} - 37.750$
10	dP2			Chan10 = 0.4975mA + 0.002					$P(\text{PSID}) = 3.267 \times \text{V} - 6.503$
10	dP2 (valid after 3/25, recalibrated on 3/24/99)			Chan10 = 0.4975mA + 0.002					$P(\text{PSID}) = 12.453 \times \text{V} - 62.463$
11	dP3			Chan11 = 0.4983mA + 0.005					$P(\text{PSID}) = 31.453 \times \text{V} - 25.231$
12	Q1			Chan12 = 0.4988mA + 0.007					$P(\text{PSID}) = 13.643 \times \text{V} - 37.923$
13	Q2			Chan13 = 0.4975mA + 0.01					$Q(\text{GPM}) = 6.289 \times \text{V} - 12.553$
14	Q3	Added on 7/14/1999		Chan14 = 0.4988mA + 0.003					$Q(\text{GPM}) = 0.1508 \times \text{V} - 0.2905$
									$Q(\text{GPM}) = 0.6235 \times \text{V} - 1.2553$

Current mA	Channel 6 V, meas.	Channel 6 V, calc.	Channel 7 V, meas.	Channel 7 V, calc.	Channel 8 V, meas.	Channel 8 V, calc.	Channel 9 V, meas.	Channel 9 V, calc.	Channel 10 V, meas.	Channel 10 V, calc.
4	1.99	1.99	2	2.00	1.99	1.99	2	2.00	1.99	1.99
8	3.98	3.98	3.99	3.99	3.99	3.99	3.99	3.99	3.98	3.98
12	5.97	5.97	5.99	5.99	5.98	5.98	5.99	5.99	5.98	5.97
16	7.96	7.96	7.98	7.98	7.97	7.97	7.98	7.98	7.96	7.96
20	9.95	9.95	9.98	9.98	9.96	9.96	9.98	9.98	9.95	9.95
Current mA	Channel 11 V, meas.	Channel 11 V, calc.	Channel 12 V, meas.	Channel 12 V, calc.	Channel 13 V, meas.	Channel 13 V, calc.	Channel 14 V, meas.	Channel 14 V, calc.		
4	2	2.00	2	2.00	2	2.00	2	2.00		
8	3.99	3.99	4	4.00	3.99	3.99	3.99	3.99		
12	5.98	5.98	5.99	5.99	5.98	5.98	5.99	5.99		
16	7.98	7.98	7.99	7.99	7.97	7.97	7.98	7.98		
20	9.97	9.97	9.98	9.98	9.96	9.96	9.98	9.98		

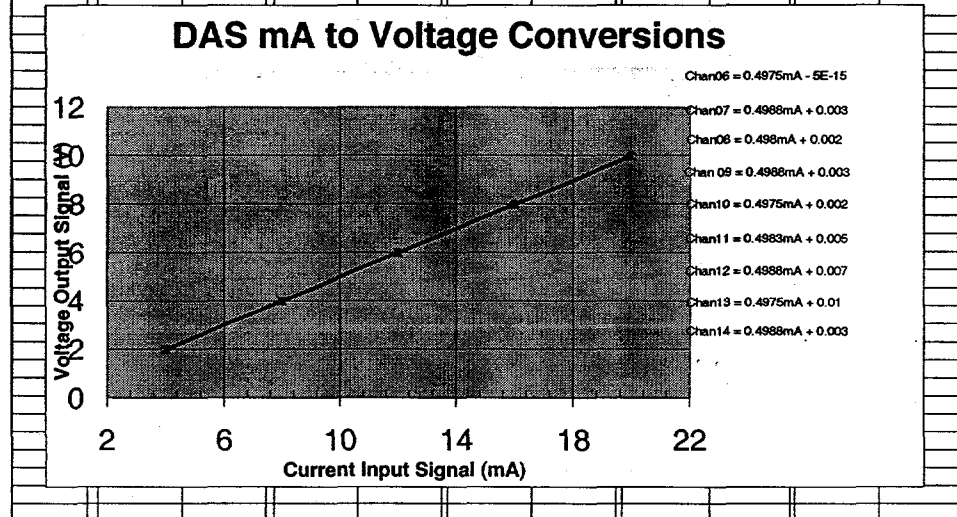


Figure F1. Instrumentation Used with their Transfer Functions

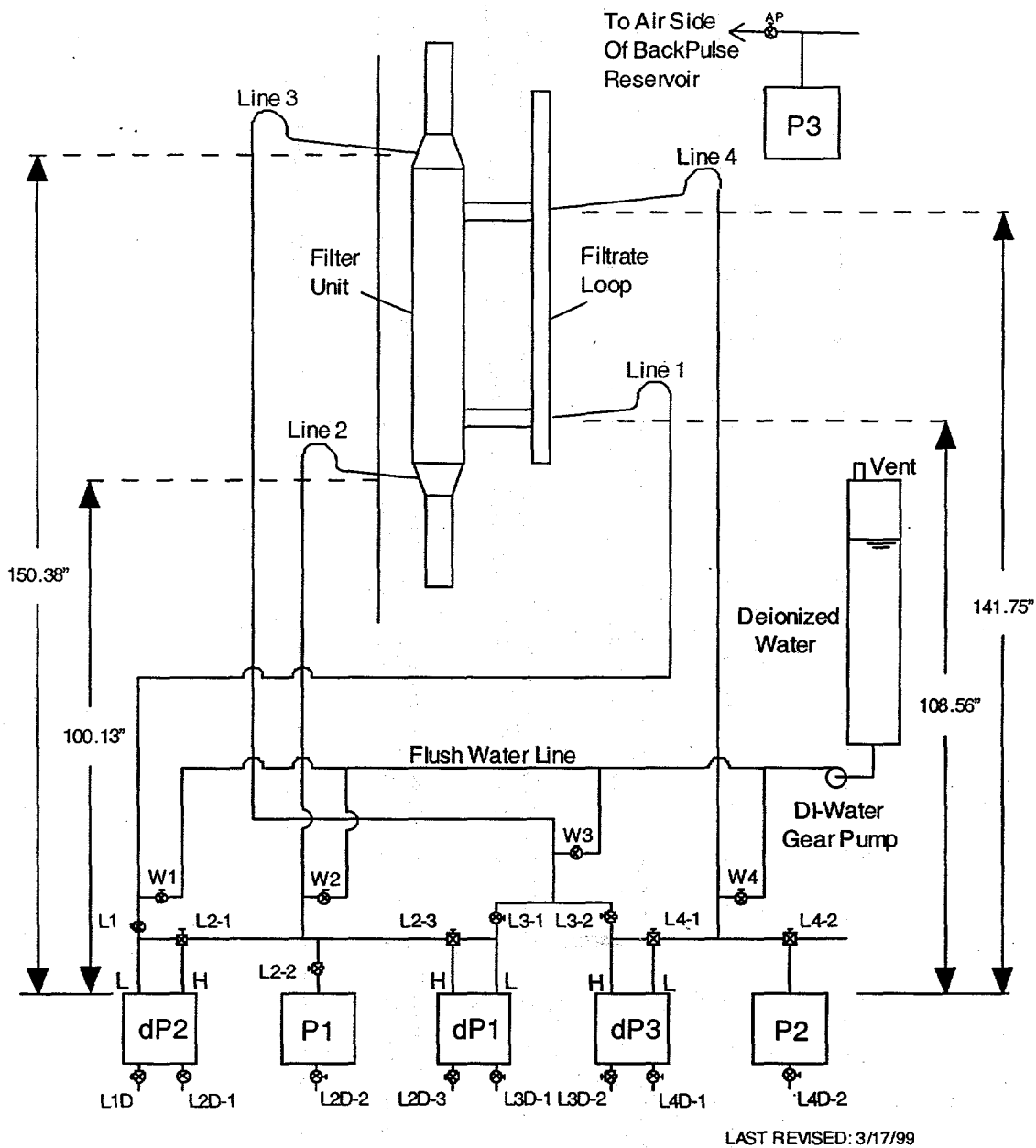


Figure F2. Pressure Transducer Locations

UNCERTAINTY ANALYSIS
REF. WSRC-TR-91-106

TR-2925

 page ____ of ____
 calibration date ____

Calibration Data

Temperature Medium	Standard Temperature (C)	Voltage Output (mV)	Calculated Temperature (eq. 1) (C)	Error (C)
Boiling Water	100.70	6.338	100.28	-0.4
Boiling Water	100.70	6.357	100.56	-0.1
Boiling Water	100.70	6.345	100.39	-0.3
Boiling Water	100.70	6.340	100.31	-0.4
Ice Point	0.00	-0.023	-0.39	-0.4
Ice Point	0.00	-0.017	-0.28	-0.3
Ice Point	0.00	-0.009	-0.15	-0.1
Ice Point	0.00	-0.018	-0.30	-0.3
Room Temp	23.80	1.404	23.50	-0.3
Room Temp	23.80	1.428	23.90	0.1
Room Temp	23.90	1.495	25.00	1.1
Room Temp	23.90	1.466	24.52	0.6

$T (C) = 0.00483 + 17.040918 * mV - 0.224284 * mV^2 + 0.005038 * mV^3$ (eq. 1)
 (Limited Curve Fit, 0-100 C. From N.I.S.T. Reference Tables)

Uncertainty of the Standards: Temperature Curve Fit: +/- 0.010 C
 Thermometer: +/- 0.40 C
 Ice Bath: +/- 0.10 C
 Multimeter: +/- (0.0045 % RDG + 0.0005 mV)
 = +/- 0.012 C @ 6.36 mV

Accepted Tolerance: +/- 1.7 C

Statistical Info.

a	b	n	T	Xbar (C)	Sxx (C^2)	SEE (C^2)	MSE (C^2)
-0.05	1.00	11.00	2.262	43.12	21815.1	1.809	0.2010

Calculated Uncertainties:

standard uncertainty (C)	curve-fit uncertainty (C)	fixed uncertainty (C)	total uncertainty (C)
0.41	1.13	0.24	1.2

PASS CALIBRATION?
YES

Figure F3. Pre-test Calibration Data of Thermocouple T1

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Calibration Data

Temperature Medium	Standard Temperature (C)	Voltage Output (mV)	Calculated Temperature (eq. 1) (C)	Error (C)
Boiling Water	100.70	6.350	100.46	-0.2
Boiling Water	100.70	6.352	100.49	-0.2
Boiling Water	100.70	6.349	100.45	-0.3
Boiling Water	100.70	6.350	100.46	-0.2
Ice Point	0.00	-0.026	-0.44	-0.4
Ice Point	0.00	-0.023	-0.39	-0.4
Ice Point	0.00	-0.019	-0.32	-0.3
Ice Point	0.00	-0.021	-0.35	-0.4
Room Temp	21.10	1.211	20.32	-0.8
Room Temp	21.30	1.178	19.78	-1.5
Room Temp	21.30	1.182	19.84	-1.5
Room Temp	21.30	1.188	19.94	-1.4

$T (^{\circ}C) = 0.00483 + 17.040918 \cdot mV - 0.224284 \cdot mV^2 + 0.005038 \cdot mV^3$ (eq. 1)
(Limited Curve Fit, 0-100 C. From N.I.S.T. Reference Tables)

Uncertainty of the Standards:	Temperature Curve Fit: +/-	0.010	C		
	Thermometer: +/-	0.40	C		
	Ice Bath: +/-	0.10	C		
	Multimeter: +/- (0.0045	% RDG +	0.0005	mV)
	= +/-	0.012	C @	6.35	mV

Accepted Tolerance: +/- 1.7 C

Statistical info.

a	b	n	T	Xbar (C)	Sxx (C^2)	SEE (C^2)	MSE (C^2)
-0.73	1.00	11.00	2.262	42.41	22130.7	2.000	0.2222

Calculated Uncertainties:

standard	curve-fit	fixed	total
uncertainty	uncertainty	uncertainty	uncertainty
(C)	(C)	(C)	(C)
0.41	1.18	0.73	1.5

PASS CALIBRATION?

YES

Figure F5. Pre-test Calibration Data of Thermocouple T3

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calibration date

Calibration Data

Temperature Medium	Standard Temperature (C)	Voltage Output (mV)	Calculated Temperature (eq. 1) (C)	Error (C)
Boiling Water	100.70	6.350	100.46	-0.2
Boiling Water	100.70	6.360	100.61	-0.1
Boiling Water	100.70	6.365	100.68	0.0
Boiling Water	100.70	6.348	100.43	-0.3
Ice Point	0.00	-0.015	-0.25	-0.3
Ice Point	0.00	-0.009	-0.15	-0.1
Ice Point	0.00	-0.003	-0.05	0.0
Ice Point	0.00	-0.009	-0.15	-0.1
Room Temp	23.80	1.416	23.70	-0.1
Room Temp	23.80	1.442	24.13	0.3
Room Temp	23.90	1.501	25.09	1.2
Room Temp	23.90	1.475	24.67	0.8

$$T\text{ (C)} = 0.00483 + 17.040918 \cdot mV - 0.224284 \cdot mV^2 + 0.005038 \cdot mV^3 \quad (\text{eq. 1})$$

(Limited Curve Fit, 0-100 C. From N.I.S.T. Reference Tables)

Uncertainty of the Standards:	Temperature Curve Fit: +/-	0.010	C		
	Thermometer: +/-	0.40	C		
	Ice Bath: +/-	0.10	C		
	Multimeter: +/- (0.0045	% RDG +	0.0005	mV)
	= +/-	0.012	C @	6.37	mV

Accepted Tolerance: +/- 1.7 C

Statistical Info.

a	b	n	T	Xbar (C)	Sxx (C^2)	SEE (C^2)	MSE (C^2)
0.09	1.00	11.00	2.262	43.12	21815.1	1.724	0.1916

Calculated Uncertainties:

standard	curve-fit	fixed	total
uncertainty	uncertainty	uncertainty	uncertainty
(C)	(C)	(C)	(C)
0.41	1.11	0.09	1.2

PASS CALIBRATION?

YES

Figure F6. Pre-test Calibration Data of Thermocouple T4

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calibration date

Calibration Data

Temperature Medium	Standard Temperature (C)	Voltage Output (mV)	Calculated Temperature (eq. 1) (C)	Error (C)
Boiling Water	100.70	6.348	100.43	-0.27
Boiling Water	100.70	6.351	100.48	-0.22
Boiling Water	100.70	6.352	100.49	-0.21
Boiling Water	100.70	6.349	100.45	-0.25
Ice Point	0.00	-0.011	-0.18	-0.18
Ice Point	0.00	-0.001	-0.01	-0.01
Ice Point	0.00	-0.006	-0.10	-0.10
Ice Point	0.00	-0.002	-0.03	-0.03
Room Temp	24.50	1.465	24.50	0.00
Room Temp	24.40	1.460	24.42	0.02
Room Temp	24.70	1.547	25.85	1.15
Room Temp	24.70	1.511	25.26	0.56

$T(^{\circ}C) = 0.00483 + 17.040918 \cdot mV - 0.224284 \cdot mV^2 + 0.005038 \cdot mV^3$ (eq. 1)
(Limited Curve Fit, 0-100 C. From N.I.S.T. Reference Tables)

Uncertainty of the Standards:	Temperature Curve Fit: +/-	0.010	C		
	Thermometer: +/-	0.40	C		
	Ice Bath: +/-	0.10	C		
	Multimeter: +/- (0.0045	% RDG +	0.0005	mV)
	= +/-	0.012	C @	6.35	mV

Accepted Tolerance: +/- 1.70 C

Statistical Info.

a	b	n	T	Xbar (C)	Sxx (C^2)	SEE (C^2)	MSE (C^2)
0.12	1.00	11.00	2.262	43.31	21735.2	1.413	0.1570

Calculated Uncertainties:

standard uncertainty (C)	curve-fit uncertainty (C)	fixed uncertainty (C)	total uncertainty (C)
0.41	1.00	0.18	1.10

PASS CALIBRATION?

YES

Figure F7. Pre-test Calibration Data of Thermocouple T5

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 cal. date:
Calibration Data

Nominal Pressure (psig)	Correction (psig)	Applied Pressure (psig)	Gage Reading (mADC)	Curve Fit (mADC)	Error (mADC)	Error (psig)
0.00	0	0.00	4.01	4.01	-0.002	-0.01
21.00	-0.71	20.29	7.28	7.28	-0.005	-0.03
41.00	-0.71	40.29	10.49	10.50	0.005	0.03
61.00	-0.71	60.29	13.71	13.72	0.006	0.03
81.00	-0.71	80.29	16.93	16.94	0.006	0.04
100.00	-0.71	99.29	20.00	19.99	-0.005	-0.03
0.00	0	0.00	4.01	4.01	-0.002	-0.01
21.00	-0.71	20.29	7.28	7.28	-0.005	-0.03
41.00	-0.71	40.29	10.49	10.50	0.005	0.03
61.00	-0.71	60.29	13.71	13.72	0.006	0.03
81.00	-0.71	80.29	16.93	16.94	0.006	0.04
100.00	-0.71	99.29	20.00	19.99	-0.005	-0.03
0.00	0	0.00	4.01	4.01	-0.002	-0.01
21.00	-0.71	20.29	7.28	7.28	-0.005	-0.03
41.00	-0.71	40.29	10.49	10.50	0.005	0.03
61.00	-0.71	60.29	13.71	13.72	0.006	0.03
81.00	-0.71	80.29	16.94	16.94	-0.004	-0.03
100.00	-0.71	99.29	20.00	19.99	-0.005	-0.03
0.00	0	0.00	4.01	4.01	-0.002	-0.01
21.00	-0.71	20.29	7.28	7.28	-0.005	-0.03
41.00	-0.71	40.29	10.49	10.50	0.005	0.03
61.00	-0.71	60.29	13.71	13.72	0.006	0.03
81.00	-0.71	80.29	16.94	16.94	-0.004	-0.03
100.00	-0.71	99.29	20.00	19.99	-0.005	-0.03

Standard Uncertainties: Multimeter: +/- (0.04 % RDG + 0.0001 mADC)
 Dead Weight Tester: +/- 0.1 psig

Statistical Info:

a	b	n	T	Xbar psig	Sxx psig ²	SEE mADC ²	MSE mADC ²
4.0083	0.1610	24.00	2.07	50.08	27719.23	0.0005	0.0000

Calculated Uncertainties:

standard psig	curve-fit psig	fixed psig	Total Uncertainty psig
0.11	0.07	0.00	0.13

Accepted Tolerance: +/- 2 psig

PASS CALIBRATION? YES
TRANSFER EQUATION PSIG = 6.211 *mA -24.895

Figure F8. Pre-test Calibration Data of Gauge Pressure Transducer P1

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 cal. date:
Calibration Data

Nominal Pressure (psid)	Correction (psid)	Applied Pressure (psid)	Gage Reading (mADC)	Curve Fit (mADC)	Error (mADC)	Error (psid)
-11.00	0.71	-10.29	4.01	4.01	0.000	0.00
0.00	0	0.00	5.65	5.65	-0.005	-0.03
11.00	-0.71	10.29	7.28	7.28	0.001	0.00
31.00	-0.71	30.29	10.46	10.46	-0.001	-0.01
51.00	-0.71	50.29	13.63	13.64	0.007	0.05
71.00	-0.71	70.29	16.81	16.82	0.006	0.04
91.00	-0.71	90.29	20.00	19.99	-0.006	-0.04
-11.00	0.71	-10.29	4.01	4.01	0.000	0.00
0.00	0	0.00	5.65	5.65	-0.005	-0.03
11.00	-0.71	10.29	7.28	7.28	0.001	0.00
31.00	-0.71	30.29	10.46	10.46	-0.001	-0.01
51.00	-0.71	50.29	13.63	13.64	0.007	0.05
71.00	-0.71	70.29	16.81	16.82	0.006	0.04
91.00	-0.71	90.29	20.00	19.99	-0.006	-0.04
-11.00	0.71	-10.29	4.01	4.01	0.000	0.00
0.00	0	0.00	5.65	5.65	-0.005	-0.03
11.00	-0.71	10.29	7.28	7.28	0.001	0.00
31.00	-0.71	30.29	10.46	10.46	-0.001	-0.01
51.00	-0.71	50.29	13.63	13.64	0.007	0.05
71.00	-0.71	70.29	16.81	16.82	0.006	0.04
91.00	-0.71	90.29	20.00	19.99	-0.006	-0.04
-11.00	0.71	-10.29	4.01	4.01	0.000	0.00
0.00	0	0.00	5.65	5.65	-0.005	-0.03
11.00	-0.71	10.29	7.28	7.28	0.001	0.00
31.00	-0.71	30.29	10.46	10.46	-0.001	-0.01
51.00	-0.71	50.29	13.63	13.64	0.007	0.05
71.00	-0.71	70.29	16.81	16.82	0.006	0.04
91.00	-0.71	90.29	20.00	19.99	-0.006	-0.04
-11.00	0.71	-10.29	4.01	4.01	0.000	0.00
0.00	0	0.00	5.65	5.65	-0.005	-0.03
11.00	-0.71	10.29	7.28	7.28	0.001	0.00
31.00	-0.71	30.29	10.46	10.46	-0.001	-0.01
51.00	-0.71	50.29	13.63	13.64	0.007	0.05
71.00	-0.71	70.29	16.81	16.82	0.006	0.04
91.00	-0.71	90.29	20.01	19.99	-0.016	-0.10

Standard Uncertainties:

Multimeter: +/- (0.04	% RDG +	0.0001	mADC)
Dead Weight Tester: +/-	0.01	psid		

Statistical Info:

a	b	n	T	Xbar psid	Sxx psid ²	SEE mADC ²	MSE mADC ²
5.6454	0.1589	28.00	2.12	34.45	33771.99	0.0008	0.0000

Calculated Uncertainties:

standard	curve-fit	fixed	Total Uncertainty
psid	psid	psid	psid
0.05	0.08	0.00	0.09

Accepted Tolerance: +/- 2 psid

PASS CALIBRATION? YES**TRANSFER EQUATION: PSIG = 6.293 *mA -35.524**

Figure F9. Pre-test Calibration Data of Gauge Pressure Transducer P2

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Calibration Data

Nominal Pressure (psig)	Applied Pressure (psig)	Gage Reading (mADC)	Curve Fit (mADC)	Error (mADC)	Error (psig)
0.00	0.00	4.01	3.99	-0.016	-0.15
31.00	31.00	7.28	7.28	-0.003	-0.03
61.00	61.00	10.44	10.45	0.014	0.13
91.00	91.00	13.61	13.63	0.021	0.20
121.00	121.00	16.80	16.81	0.008	0.08
151.00	151.00	20.01	19.99	-0.025	-0.23
0.00	0.00	4.01	3.99	-0.016	-0.15
31.00	31.00	7.28	7.28	-0.003	-0.03
61.00	61.00	10.44	10.45	0.014	0.13
91.00	91.00	13.61	13.63	0.021	0.20
121.00	121.00	16.80	16.81	0.008	0.08
151.00	151.00	20.01	19.99	-0.025	-0.23
0.00	0.00	4.01	3.99	-0.016	-0.15
31.00	31.00	7.28	7.28	-0.003	-0.03
61.00	61.00	10.44	10.45	0.014	0.13
91.00	91.00	13.61	13.63	0.021	0.20
121.00	121.00	16.80	16.81	0.008	0.08
151.00	151.00	20.01	19.99	-0.025	-0.23
0.00	0.00	4.01	3.99	-0.016	-0.15
31.00	31.00	7.28	7.28	-0.003	-0.03
61.00	61.00	10.44	10.45	0.014	0.13
91.00	91.00	13.61	13.63	0.021	0.20
121.00	121.00	16.80	16.81	0.008	0.08
151.00	151.00	20.01	19.99	-0.025	-0.23
0.00	0.00	4.01	3.99	-0.016	-0.15
31.00	31.00	7.28	7.28	-0.003	-0.03
61.00	61.00	10.44	10.45	0.014	0.13
91.00	91.00	13.61	13.63	0.021	0.20
121.00	121.00	16.80	16.81	0.008	0.08
151.00	151.00	20.01	19.99	-0.025	-0.23

Standard Uncertainties:

Multimeter: +/- (0.04	% RDG +	0.0001	mADC)
Dead Weight Tester: +/-	0.1	psig		

Statistical Info:

a	b	n	T	Xbar psig	Sxx psig ²	SEE mADC ²	MSE mADC ²
3.9939	0.1059	24.00	2.07	75.83	63603.33	0.0063	0.0003

Calculated Uncertainties:

standard psig	curve-fit psig	fixed psig	Total Uncertainty psig
0.13	0.35	0.00	0.38

Accepted Tolerance: +/-

3

psig

PASS CALIBRATION? YES**TRANSFER EQUATION PSIG = 9.442 *mA -37.712**

Figure F10. Pre-test Calibration Data of Gauge Pressure Transducer P3

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 cal. date:
Calibration Data

Nominal Pressure (psid)	Applied Pressure (psid)	Gage Reading (mADC)	Curve Fit (mADC)	Error (mADC)	Error (psid)
0.00	0.00	4.00	4.00	-0.004	-0.01
1.00	1.00	4.61	4.61	0.001	0.00
6.00	6.00	7.69	7.69	-0.002	0.00
11.00	11.00	10.76	10.77	0.005	0.01
16.00	16.00	13.84	13.84	0.003	0.00
21.00	21.00	16.92	16.92	0.000	0.00
26.00	26.00	20.00	20.00	-0.003	-0.01
0.00	0.00	4.00	4.00	-0.004	-0.01
1.00	1.00	4.61	4.61	0.001	0.00
6.00	6.00	7.69	7.69	-0.002	0.00
11.00	11.00	10.76	10.77	0.005	0.01
16.00	16.00	13.84	13.84	0.003	0.00
21.00	21.00	16.92	16.92	0.000	0.00
26.00	26.00	20.00	20.00	-0.003	-0.01
0.00	0.00	4.00	4.00	-0.004	-0.01
1.00	1.00	4.61	4.61	0.001	0.00
6.00	6.00	7.69	7.69	-0.002	0.00
11.00	11.00	10.76	10.77	0.005	0.01
16.00	16.00	13.84	13.84	0.003	0.00
21.00	21.00	16.92	16.92	0.000	0.00
26.00	26.00	20.00	20.00	-0.003	-0.01
0.00	0.00	4.00	4.00	-0.004	-0.01
1.00	1.00	4.61	4.61	0.001	0.00
6.00	6.00	7.69	7.69	-0.002	0.00
11.00	11.00	10.76	10.77	0.005	0.01
16.00	16.00	13.84	13.84	0.003	0.00
21.00	21.00	16.92	16.92	0.000	0.00
26.00	26.00	20.00	20.00	-0.003	-0.01

Standard Uncertainties: Multimeter: +/- (0.04 % RDG + 0.0001 mADC)
 Dead Weight Tester: +/- 0.01 psid

Statistical Info:

a	b	n	T	Xbar psid	Sxx psid ²	SEE mADC ²	MSE mADC ²
3.9959	0.6154	28.00	2.06	11.57	2374.86	0.0003	0.0000

Calculated Uncertainties:

standard	curve-fit	fixed	Total Uncertainty
psid	psid	psid	psid
0.017	0.011	0.000	0.020

Accepted Tolerance: +/- 0.500 psid

PASS CALIBRATION? YES
TRANSFER EQUATION: PSID = 1.6249 *mA -6.4930

Figure F11. Pre-test Calibration Data of Differential Pressure Transducer dP1

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Calibration Data

Nominal Pressure (psid)	Applied Pressure (psid)	Gage Reading (mADC)	Curve Fit (mADC)	Error (mADC)	Error (psid)
0.00	0.00	4.00	4.00	-0.004	-0.03
21.00	21.00	7.32	7.32	0.002	0.01
41.00	41.00	10.49	10.49	-0.001	0.00
61.00	61.00	13.65	13.66	0.007	0.04
81.00	81.00	16.82	16.82	0.005	0.03
101.00	101.00	20.00	19.99	-0.008	-0.05
0.00	0.00	4.00	4.00	-0.004	-0.03
21.00	21.00	7.32	7.32	0.002	0.01
41.00	41.00	10.49	10.49	-0.001	0.00
61.00	61.00	13.65	13.66	0.007	0.04
81.00	81.00	16.82	16.82	0.005	0.03
101.00	101.00	20.00	19.99	-0.008	-0.05
0.00	0.00	4.00	4.00	-0.004	-0.03
21.00	21.00	7.32	7.32	0.002	0.01
41.00	41.00	10.49	10.49	-0.001	0.00
61.00	61.00	13.65	13.66	0.007	0.04
81.00	81.00	16.82	16.82	0.005	0.03
101.00	101.00	20.00	19.99	-0.008	-0.05
0.00	0.00	4.00	4.00	-0.004	-0.03
21.00	21.00	7.32	7.32	0.002	0.01
41.00	41.00	10.49	10.49	-0.001	0.00
61.00	61.00	13.65	13.66	0.007	0.04
81.00	81.00	16.82	16.82	0.005	0.03
101.00	101.00	20.00	19.99	-0.008	-0.05
0.00	0.00	4.00	4.00	-0.004	-0.03
21.00	21.00	7.32	7.32	0.002	0.01
41.00	41.00	10.49	10.49	-0.001	0.00
61.00	61.00	13.65	13.66	0.007	0.04
81.00	81.00	16.82	16.82	0.005	0.03
101.00	101.00	20.00	19.99	-0.008	-0.05

Standard Uncertainties: Multimeter: +/- (0.04 % RDG + 0.0001 mADC)
 Dead Weight Tester: +/- 0.1 psig

Statistical Info:

a	b	n	T	Xbar psid	Sxx psid ²	SEE mADC ²	MSE mADC ²
3.9956	0.1584	24.00	2.07	50.83	28403.33	0.0006	0.0000

Calculated Uncertainties:

standard psid	curve-fit psid	fixed psid	Total Uncertainty psid
0.11	0.07	0.00	0.13

Accepted Tolerance: +/- 2 psid

PASS CALIBRATION? YES
TRANSFER EQUATION: PSID = 6.314 *mA -25.227

Figure F12. Pre-test Calibration Data of Differential Pressure Transducer dP2

UNCERTAINTY ANALYSIS
REF. WSRC-TR-91-106, REV. 0

TR-3115

 page ___ of ___
 cal. date:
Calibration Data

Nominal Pressure (psid)	Correction (psid)	Applied Pressure (psid)	Gage Reading (mADC)	Curve Fit (mADC)	Error (mADC)	Error (psid)
-11.00	0.71	-10.29	3.99	4.00	0.006	0.04
0.00	0	0.00	5.48	5.49	0.007	0.05
21.00	-0.71	20.29	8.43	8.43	-0.001	-0.01
41.00	-0.71	40.29	11.34	11.33	-0.012	-0.08
61.00	-0.71	60.29	14.24	14.23	-0.013	-0.09
81.00	-0.71	80.29	17.13	17.13	-0.003	-0.02
101.00	-0.71	100.29	20.01	20.03	0.016	0.11
-11.00	0.71	-10.29	3.99	4.00	0.006	0.04
0.00	0	0.00	5.48	5.49	0.007	0.05
21.00	-0.71	20.29	8.43	8.43	-0.001	-0.01
41.00	-0.71	40.29	11.34	11.33	-0.012	-0.08
61.00	-0.71	60.29	14.24	14.23	-0.013	-0.09
81.00	-0.71	80.29	17.13	17.13	-0.003	-0.02
101.00	-0.71	100.29	20.01	20.03	0.016	0.11
-11.00	0.71	-10.29	3.99	4.00	0.006	0.04
0.00	0	0.00	5.48	5.49	0.007	0.05
21.00	-0.71	20.29	8.43	8.43	-0.001	-0.01
41.00	-0.71	40.29	11.34	11.33	-0.012	-0.08
61.00	-0.71	60.29	14.24	14.23	-0.013	-0.09
81.00	-0.71	80.29	17.13	17.13	-0.003	-0.02
101.00	-0.71	100.29	20.01	20.03	0.016	0.11
-11.00	0.71	-10.29	3.99	4.00	0.006	0.04
0.00	0	0.00	5.48	5.49	0.007	0.05
21.00	-0.71	20.29	8.43	8.43	-0.001	-0.01
41.00	-0.71	40.29	11.34	11.33	-0.012	-0.08
61.00	-0.71	60.29	14.24	14.23	-0.013	-0.09
81.00	-0.71	80.29	17.13	17.13	-0.003	-0.02
101.00	-0.71	100.29	20.01	20.03	0.016	0.11
-11.00	0.71	-10.29	3.99	4.00	0.006	0.04
0.00	0	0.00	5.48	5.49	0.007	0.05
21.00	-0.71	20.29	8.43	8.43	-0.001	-0.01
41.00	-0.71	40.29	11.34	11.33	-0.012	-0.08
61.00	-0.71	60.29	14.24	14.23	-0.013	-0.09
81.00	-0.71	80.29	17.13	17.13	-0.003	-0.02
101.00	-0.71	100.29	20.01	20.03	0.016	0.11

Standard Uncertainties:
 Multimeter: +/- (0.04
 Dead Weight Tester: +/- 0.1 % RDG + psid 0.0001 mADC)
Statistical Info:

a	b	n	T	Xbar psid	Sxx psid ²	SEE mADC ²	MSE mADC ²
5.4875	0.1450	28.00	2.12	41.59	40678.85	0.0026	0.0001

Calculated Uncertainties:

standard psid	curve-fit psid	fixed psid	Total Uncertainty psid
0.11	0.16	0.00	0.19

Accepted Tolerance: +/- 2 psid

PASS CALIBRATION?**YES****TRANSFER EQUATION:****PSID =****6.898*****mA****-37.854**

Figure F13. Pre-test Calibration Data of Differential Pressure Transducer dP3

UNCERTAINTY ANALYSIS
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 page ____ of ____
 calibration date ____

Calibration Data				Calculated Data				
Meter Output (mA)	Water Temp (C)	Water Weight (lbs)	Time Duration (min)	Mass Flow (lbs/min)	Water Density (lb/ft ³)	Volume Flow (ft ³ /min)	Volume Flow (GPM)	Curve Fit Output (mA)
3.977	21.40	0	0.50	0.0	62.29	0.00	0.00	3.99
7.115	21.40	1228	15.00	81.9	62.28	1.31	9.83	7.12
10.434	21.80	1682	10.01	168.1	62.28	2.70	20.19	10.42
13.535	22.00	1246	5.00	249.0	62.28	4.00	29.91	13.52
16.807	22.00	1679	5.01	335.3	62.29	5.38	40.27	16.83
19.889	21.50	2078	5.00	415.5	62.29	6.67	49.90	19.90
19.887	21.40	2079	5.00	415.6	62.29	6.67	49.90	19.90
16.740	21.00	1664	5.00	332.6	62.30	5.34	39.94	16.72
13.594	20.90	1254	5.00	250.6	62.30	4.02	30.09	13.58
10.325	20.80	1652	10.00	165.2	62.30	2.65	19.83	10.31
7.194	20.70	1257	15.01	83.8	62.30	1.34	10.06	7.19
3.978	20.70	0	0.50	0.0	62.30	0.00	0.00	3.99
7.216	20.80	1264	15.00	84.3	62.29	1.35	10.12	7.21
10.379	21.30	1669	10.01	166.8	62.29	2.68	20.03	10.37
13.628	21.90	1258	5.00	251.5	62.28	4.04	30.21	13.62
16.724	21.70	1663	5.00	332.6	62.29	5.34	39.95	16.72
19.813	20.90	2070	5.00	413.9	62.30	6.64	49.70	19.83
3.979	20.90	0	0.50	0.0	62.30	0.00	0.00	3.99

 Density: $\rho = 62.441 - 1.374E-3 \cdot T - 271.818E-6 \cdot T^2 + 194.093E-9 \cdot T^3$
7.4805 gallons = 1 ft³

Uncertainty of the Standards:

Weight: +/-	7.0	lbs
Temperature: +/-	0.40	C
Density: +/-	0.06	lbm/ft ³
Time: +/- (0.20	sec +

500.00 \square sec/sec)

Accepted Tolerance: +/- 0.50 GPM

Statistical Info.				Xbar	Sxx	SEE	MSE
a	b	n	T	(GPM)	(GPM ²)	(mA ²)	(mA ²)
3.988	0.319	18.00	2.120	25.00	5231.96	0.0023	0.0001

Calculated Uncertainties:	standard uncertainty (GPM)	curve-fit uncertainty (GPM)	fixed uncertainty (GPM)	total uncertainty (GPM)
	0.17	0.09	0.00	0.19

PASS CALIBRATION? YES

TRANSFER EQUATION GPM = 3.137 mA -12.509

Figure F14. Pre-test Calibration Data of Magnetic Flowmeter Q1

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TR-20353

 page ____ of ____
 calibration date ____
Calibration Data

Meter Output (mA)	Water Temp (C)	Water Weight (lbs)	Time Duration (min)
4.00	15.50	0.00	0.00
8.21	15.50	13.25	5.03
12.18	16.30	25.48	5.00
16.17	19.50	37.83	5.00
20.18	22.50	50.38	5.00
20.18	23.00	50.44	5.00
16.12	23.10	37.94	5.01
12.28	22.80	25.95	5.00
8.09	22.90	12.83	5.00
4.00	22.90	0.00	0.00
4.00	22.90	0.00	0.00
8.15	22.90	12.95	5.00
12.02	23.00	25.12	5.00
16.05	25.20	37.63	5.00
20.05	25.20	49.98	5.00

Calculated Data

Mass Flow (lbs/min)	Water Density (lb/ft^3)	Volume Flow (ft^3/min)	Volume Flow (GPM)	Curve Fit Output (mA)	Error (mA)	Error (GPM)
0.00	62.36	0.00	0.00	3.99	-0.01	-0.001
2.64	62.36	0.04	0.32	8.21	0.01	0.000
5.09	62.35	0.08	0.61	12.16	-0.03	-0.002
7.56	62.31	0.12	0.91	16.13	-0.04	-0.003
10.07	62.27	0.16	1.21	20.15	-0.03	-0.002
10.08	62.27	0.16	1.21	20.18	0.00	0.000
7.58	62.27	0.12	0.91	16.16	0.04	0.003
5.19	62.27	0.08	0.62	12.31	0.04	0.003
2.56	62.27	0.04	0.31	8.10	0.01	0.001
0.00	62.27	0.00	0.00	3.99	-0.01	-0.001
0.00	62.27	0.00	0.00	3.99	-0.01	-0.001
2.59	62.27	0.04	0.31	8.14	-0.01	-0.001
5.02	62.27	0.08	0.60	12.05	0.03	0.003
7.52	62.24	0.12	0.90	16.07	0.03	0.002
9.99	62.24	0.16	1.20	20.03	-0.01	-0.001

Density: $\rho = 62.441 - 1.374E-3T - 271.818E-6T^2 + 194.093E-9T^3$
 7.4805 gallons = 1 ft^3

Uncertainty of the Standards:

Weight: +/-	0.1	lbs
Temperature: +/-	0.40	C
Density: +/-	0.06	lbm/ft^3
Time: +/- (0.20	sec +
	500.00	sec/sec)

Accepted Tolerance: +/- 0.01 GPM

Statistical Info.

a	b	n	T	Xbar (GPM)	Sxx (GPM^2)	SEE (mA^2)	MSE (mA^2)
3.987	13.366	15.00	2.160	0.61	2.72	0.0087	0.0007

Calculated Uncertainties:

standard uncertainty (GPM)	curve-fit uncertainty (GPM)	fixed uncertainty (GPM)	total uncertainty (GPM)
0.003	0.005	0.000	0.005

PASS CALIBRATION?

YES

TRANSFER EQUATION: GPM = 0.075 mA -0.298

Figure F15. Pre-test Calibration Data of Magnetic Flowmeter Q2

UNCERTAINTY ANALYSIS
 REF. WSRC-TR-91-106

TR-3562

 page ____ of ____
 calibration date ____
Calibration Data

Meter Output (mA)	Water Temp (C)	Water Weight (lbs)	Time Duration (min)
3.97	24.60	0.00	0.00
7.97	25.60	51.79	5.00
11.96	25.20	103.40	5.00
16.08	25.40	125.52	4.00
19.98	25.70	124.58	3.00
3.98	25.90	0.00	0.00
8.01	25.90	52.35	5.00
12.00	25.90	103.82	5.00
15.97	25.90	124.28	4.00
20.03	25.90	124.64	3.00
3.98	25.70	0.00	0.00
8.11	25.70	53.48	5.00
12.04	25.80	104.44	5.00
15.99	25.80	124.75	4.01
20.05	21.70	125.64	3.00
3.98	23.00	0.00	0.00
7.97	23.00	51.92	5.00
11.96	22.90	103.69	5.00
15.97	22.70	124.62	4.00
19.92	22.70	124.36	3.00

Calculated Data

Mass Flow (lbs/min)	Water Density (lb/ft ³)	Volume Flow (ft ³ /min)	Volume Flow (GPM)	Curve Fit Output (mA)	Error (mA)	Error (GPM)
0.00	62.25	0.00	0.00	3.98	0.01	0.004
10.36	62.23	0.17	1.25	7.98	0.01	0.002
20.67	62.24	0.33	2.48	11.95	-0.01	-0.002
31.36	62.23	0.50	3.77	16.07	-0.01	-0.002
41.48	62.23	0.67	4.99	19.98	0.00	-0.001
0.00	62.23	0.00	0.00	3.98	0.00	0.001
10.47	62.23	0.17	1.26	8.02	0.01	0.003
20.75	62.23	0.33	2.49	11.99	-0.01	-0.004
31.05	62.23	0.50	3.73	15.96	-0.01	-0.005
41.55	62.23	0.67	4.99	20.01	-0.02	-0.008
0.00	62.23	0.00	0.00	3.98	0.00	0.001
10.69	62.23	0.17	1.29	8.11	0.00	-0.001
20.87	62.23	0.34	2.51	12.03	-0.01	-0.002
31.13	62.23	0.50	3.74	15.98	-0.01	-0.004
41.87	62.29	0.67	5.03	20.11	0.06	0.020
0.00	62.27	0.00	0.00	3.98	0.00	0.001
10.37	62.27	0.17	1.25	7.98	0.01	0.003
20.73	62.27	0.33	2.49	11.97	0.01	0.004
31.13	62.27	0.50	3.74	15.98	0.01	0.003
41.43	62.27	0.67	4.98	19.95	0.03	0.009

Density: $\rho = 62.441 - 1.374E-3 \cdot T - 271.818E-6 \cdot T^2 + 194.093E-9 \cdot T^3$
 7.4805 gallons = 1 ft³

Uncertainty of the Standards:

Weight: +/-	0.1	lbs
Temperature: +/-	0.40	C
Density: +/-	0.06	lbm/ft ³
Time: +/- (0.20	sec + 500.00 \square sec/sec)

Accepted Tolerance: +/- 0.05 GPM

Statistical Info.				Xbar	Sxx	SEE	MSE
a	b	n	T	(GPM)	(GPM ²)	(mA ²)	(mA ²)
3.982	3.208	15.00	2.160	2.50	46.80	0.0056	0.0004

Calculated Uncertainties:	standard uncertainty (GPM)	curve-fit uncertainty (GPM)	fixed uncertainty (GPM)	total uncertainty (GPM)
	0.007	0.02	0.00	0.02

PASS CALIBRATION? YES
 TRANSFER EQUATION: GPM = 0.3113 mA -1.2370

Figure F16. Pre-test Calibration Data of Magnetic Flowmeter Q3

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