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DESIGN, CONSTRUCTION, OPERATION AND EVALUATION OF A PROTOTYPE
CULM COMBUSTION BOILER/HEATER UNIT

Final Design of Prototype Unit

October 1980

Work Performed Under Contract AC21-78ET12307

Curtiss-Wright Corporation
Wood-Ridge, New Jersey

and

Dorr-Oliver Incorporated
Stamford, Connecticut

and

Stone & Webster Engineering Corporation
New York, New York

U. S. DEPARTMENT OF ENERGY



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Price: Printed Copy A04
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**DESIGN, CONSTRUCTION, OPERATION AND EVALUATION OF A
PROTOTYPE CULM COMBUSTION BOILER/HEATER UNIT**

FINAL DESIGN OF PROTOTYPE UNIT

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October 1980

Prepared for:

**The United States Department of Energy
Under Contract No. ET-78-C-01-3269
with the
Shamokin Area Industrial Corporation**

ABSTRACT

A final design of a prototype anthracite culm combustion boiler has been accomplished under Phase I of DOE Contract ET-78-C-01-3269. The prototype boiler has been designed to generate 20,000 pounds per hour of 150 psig saturated steam using low Btu (4,000 Btu per pound) anthracite culm as a fuel. This boiler will be located at the industrial park of the Shamokin Area Industrial Corporation (SAIC). This program is directed at demonstrating the commercial viability of anthracite culm fueled FBC steam generation systems.

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Reference 1 - Construction Bid Package Specification SP-N-901

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1.0 INTRODUCTION

Anthracite culm is a generic term for any non-salable by-product resulting from production of marketable anthracite coal. It contains an appreciable amount of coal and is essentially a low cost, poor quality fuel reserve. About 910 million cubic yards of refuse is found in Northeastern Pennsylvania. The refuse banks are eyesores which not only occupy valuable land, but pollute the air, land, and water of the region as a result of spontaneous combustion and acid runoff.

The burning of anthracite culm in a fluidized bed combustion boiler is considered to be a feasible, cost effective way of utilizing this fuel in an environmentally acceptable manner. The fluidized bed combustion is essentially a furnace which can burn a variety of fuels including culm at relatively low temperature (1400°F ~ 1700°F). The sulfur dioxide release can be controlled within environmentally acceptable levels by use of limestone or dolomite as a sulfur sorbent. The relative low combustion temperatures also keep the nitrogen oxide level low. The use of boiler tubes in the fluidized bed to extract heat is a very efficient method of steam generation due to the high heat transfer coefficient.

Toward this goal an anthracite-culm-fueled fluidized bed boiler to produce 20,000 pounds per hour of steam has been designed under the sponsorship of the DOE. This boiler will be located at an industrial park of the Shamokin Area Industrial Corporation (SAIC) in Paxinos, Pennsylvania. The boiler will be fueled by anthracite culm having a heat content of 4,000 Btu per pound. The boiler will supply 150 psig saturated steam for the manufacturing processes of a paper products manufacturer at the industrial park.

The objectives of this contract are to design, construct and operate a boiler utilizing anthracite culm in a fluidized bed combustion system for the generation of steam for industrial use. Data from this plant will be used for the evaluation of larger FBC steam generating units.

This report describes the final design for the Shamokin FBC Boiler. An artist's conceptual drawing is presented in Figure 1.1.

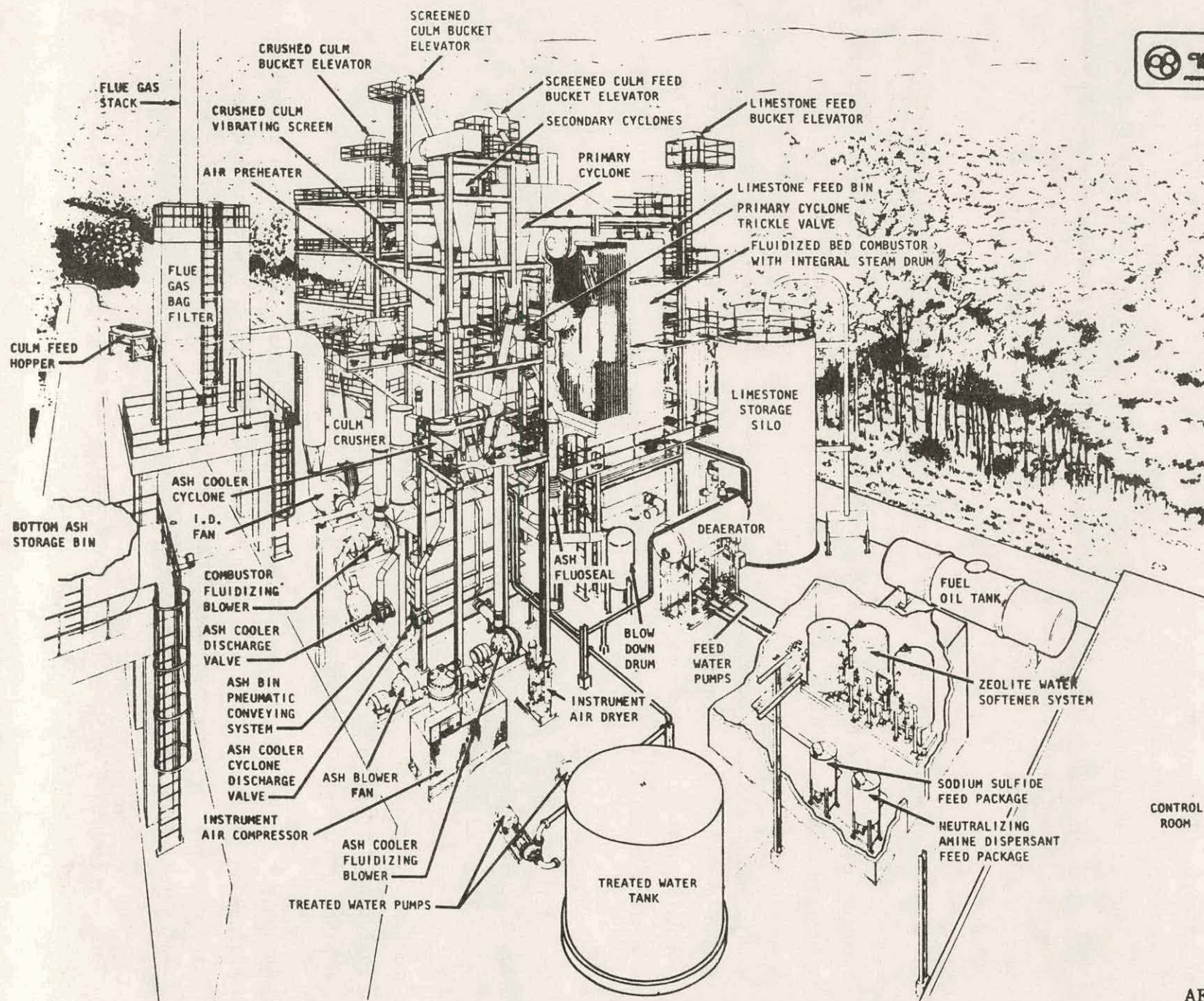


Figure 1.1

ATMOSPHERIC FLUIDIZED BED BOILER

DEPARTMENT OF ENERGY PLANT - SHAMOKIN, PA

AFB-53B

2.0 PROCESS DESCRIPTION

The prototype boiler system is to furnish 20,000 lb/hr of 150 psig steam using anthracite culm as the fuel. The process flow diagrams are shown in Drawings 75-D1 (Figure 2.1), F2 (Figure 2.2), and F3 (Figure 2.3). The flows presented are based on using a culm with a HHV of 4000 Btu/lb. However, all the equipment are sized to handle culms with heating values ranging from 3000 to 5000 Btu/lb.

The normal range of operating conditions possible with this unit are:

Fluidization Velocity	3.5 to 6 fps
Combustion Temperature	1450 to 1650°F
Excess Air	20 - 50%
Bed Height	3 - 6 ft
Steam Turndown	2.5 to 1
Culm Feed Rate Turndown	5 to 1
Limestone Feed Rate Turndown	10 to 1

2.1 Feed Preparation and Storage

The anthracite culm fuel will be delivered by truck in the size range from 1 to 4 inches. It will be deposited into an unloading area from which a front end loader will transfer the culm to a conveying system. This will transport the culm to a crushing and classifying system. Here it will be sized to 4 mesh x 0 material. From this operation, it will be conveyed to the prepared culm hopper. The prepared culm hopper is sized to store a 32-hour feed supply (for 4000 Btu/lb culm). From this hopper it will be transported to the culm feed bin which holds approximately 4 hours of feed.

Sized limestone (minus 1/4 inch size) will be delivered to the site via truck and pneumatically conveyed to a limestone storage silo. This silo will store approximately a week's supply of stone. From the silo the material will pass through a screw feeder and bucket elevator and then into the limestone feed hopper. This feed hopper is designed to hold a day's supply of material.

The feed preparation and filling of feed hoppers will occur during day shifts only. Therefore all the equipment has been sized accordingly.

2.2 Feeding

Both culm and limestone will be fed to the boiler via screw feeders. Two feeders will be used for the culm, and one for the limestone. The designs of these feeders are based on Dorr-Oliver's extensive experience in feeding fluidized beds. Variable speed motor drives will be used on each feeder to permit culm feed rate to follow steam demand in accordance with combustion control system and combustion temperature, and to allow limestone feed rate to vary with the SO₂ emission control feedback signal.

2.3 Fluidized Bed Boiler System

A fluidized bed combustor boiler of water wall design with in-bed boiler tubes and a convection section for the generation of steam is used. The bed contains 100 square feet of fluidizing area.

This boiler application calls for the delivery of 20,000 lb/hr of 150 psig saturated steam to battery limit. The fluidized bed boiler is designed to generate this steam capacity with in-bed, water wall and convection section tubes. The steam generated will be at 200 psi and saturated but will be reduced in pressure before delivery to the user.

To aid in start-up and turndown, the air plenum chamber is divided into three zones, each with its own air supply. One zone covering 64% of the bed area will not contain in-bed tubes. This area is always fluidized when steam is being generated and is the first bed section to be fluidized during start-up. The other two bed sections split the remaining 36% of the bed equally. These each contain in-bed boiler tubes and can be defluidized during turndown conditions.

An oil fired burner is also included to serve as a start-up burner. This burner will bring the bed up to culm combustion temperature.

2.4 Primary and Secondary Cyclones

Flue gas effluent from the boiler system enters the primary cyclone which is a refractory lined cyclone of conventional design. It serves as the primary combustion gas cleanup stage and recycles the collected ash and unreacted particulates back to the combustor. This recycle ensures high combustion efficiency, high limestone utilization, high heat transfer and good fluidization. Provision has also been made to purge off some of the cyclone catch, in lieu of 100% recycle. This permits greater operating flexibility in the boiler system.

The flue gases leaving the primary cyclone are further cleaned in twin cyclones. The dust collected here is exhausted to the ash cooler. When the boiler is turned down, one cyclone is bypassed to maintain a high cyclone efficiency in the other cyclone.

2.5 Ash Cooler

The ash cooler receives ash from the FBC boiler and the primary and secondary cyclones, and cools the ash to approximately 250°F. The ash cooler is a fluidized bed containing in-bed cooling coils. The cooling coils utilize boiler feed water permitting this system to recover some of the sensible heat from the hot ash and transmits it to the boiler feed water. Over 1×10^6 Btu/hr are recovered in this equipment item.

The ash cooler has its own air supply system and cyclone. The ash for this system is discharged through rotary valves to a pneumatic transfer system to ash storage and disposal.

2.6 Air Preheater

The flue gases exit the twin cyclones at 660°F. To improve the energy efficiency of the boiler system, additional energy is extracted from these gases in the air preheater before they are vented to the atmosphere. The hot flue gases flow inside the tubes of an air to gas shell and tube preheater and exit at 350°F.

On the shell side, combustion air from the fluidizing blower is heated to 425°F before entering the combustor. The design of this preheater is similar to those conventionally used in FluoSolids operations.

2.7 ID Fan

An induced draft fan is located between the air preheater and bag filter. This fan is used to control the pressure above the fluidized bed at a slightly negative level (i.e., -0.2 inches water).

2.8 Bag Filter

A conventional blow-back bag filter system is used to provide the final removal of particulates from the combustion gases before they are vented to the atmosphere. This system is designed to meet the federal and local particulate emissions codes.

2.9 Steam/Water Circuit

The design condition calls for 20,000 lb/hr of feed water to be vaporized as the exported steam. Besides this amount, approximately 10% more feed water is used in blowdown, and as steam is released from the deaerator and blowdown drum.

City water is used as the source of boiler feed water. This water is softened with a zeolite system. The treated water is fed through the ash cooler cooling circuit where it is heated, and then passes through the deaerator for oxygen removal. Oxygen in the feed water is further scavenged in the deaerator by the addition of sodium sulfite. From the deaerator, the feed water is pumped to the steam drum. A neutralizing amine treatment is used to further prevent chemical attack of the boiler metallurgy.

Two boiler feed water pumps are used. One pump is electrically driven and the second is turbine driven. The turbine drive is used in the event of a power outage and as a back-up for the electrically driven pump. Both pumps are interchangeable as the primary pump to facilitate maintenance rotation.

Water from the steam drum feeds the three steaming circuits of the boiler:

1. The Water Walls
2. The In-Bed Tubes
3. The Convection Section

This boiler is designed with all natural circulation circuits.

The steam/water mixtures from the three circuits exhaust to the steam drum where the water and steam are separated. The drum is at 200 psig.

Some of the steam produced is used within the system for the deaerator and turbine driven BPW pump. The bulk of the steam, 20,000 lb/hr, is reduced in pressure to 150 psig and sent to the user.

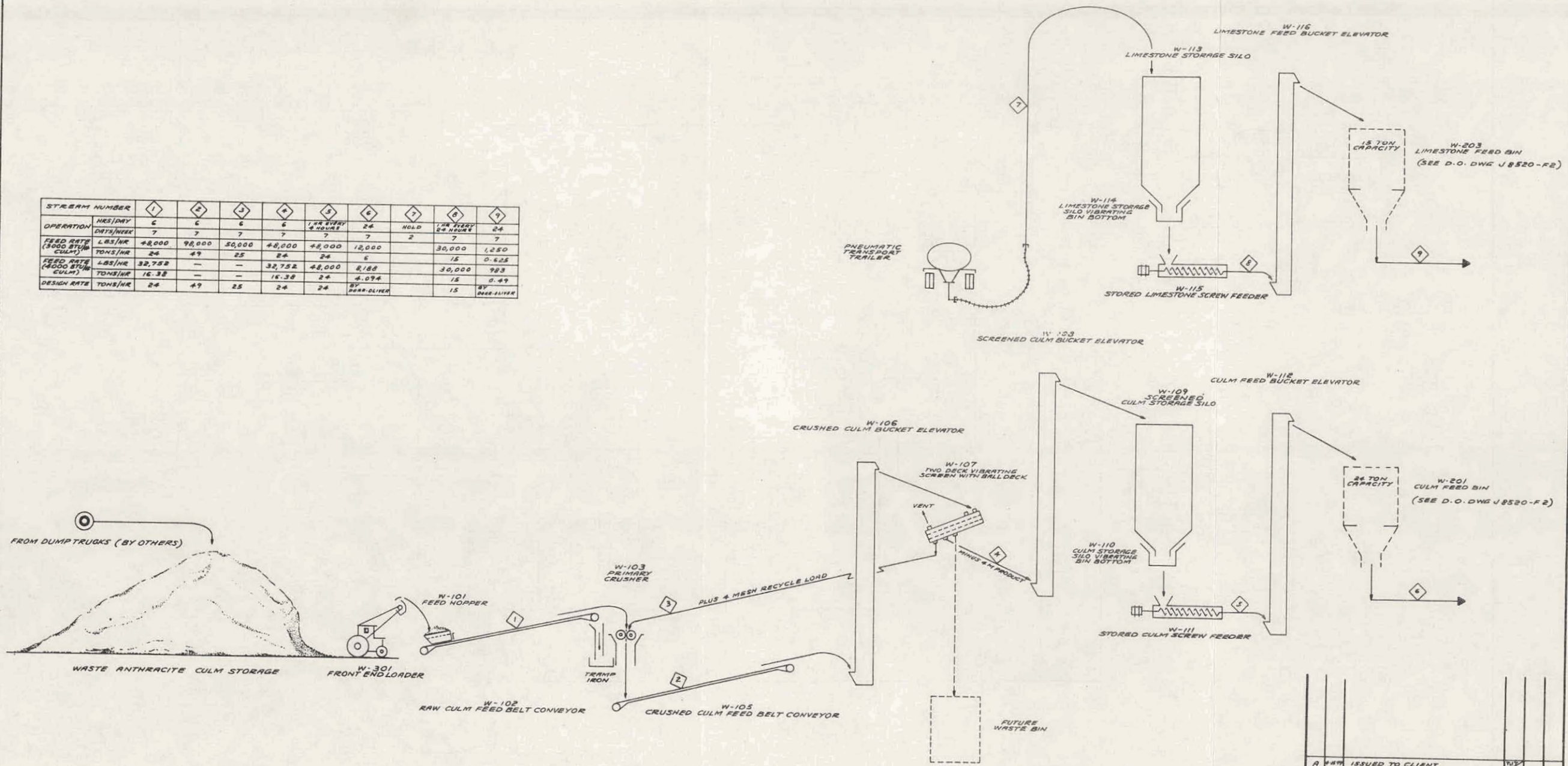
3.0 MASS AND ENERGY BALANCES

Based on a laboratory combustion study, flow diagrams for both the solids and gas, and water and steam sides of the plant were drawn and shown in Figures 2.1, 2.2 and 2.3. Mass and energy balances were generated on the following process basis:

Steam Delivered, Saturated	20,000 lbs/hr at 150 psig
Combustion Temperature	1550°F
Fluidization Velocity	5.5 ft/sec
Culm Fuel - HHV	4012 Btu/lb
Excess Air	30%

Mass and energy balances are shown in Tables 1 and 2. This design is directed toward achieving an overall efficiency of 69.5%. Culm with a heating value of 4012 Btu/lb was used for design purposes. Culm analysis is given in Table 3. Anthracite culm ash analysis is given in Table 4. A Ca/S ratio of 5.8 will be used to achieve an 88% sulfur capture. Meckley limestone will be used as a sorbent and its analysis is given in Table 5.

STREAM NUMBER	1	2	3	4	5	6	7	8	9
OPERATION	HRS/DAY	6	6	6	6	1 HR EVERY 4 HOURS	24	HOLD	1 HR EVERY 24 HOURS
FEED RATE (3000 STUB CULM)	LBS/HR	48,000	96,000	50,000	48,000	48,000	12,000	30,000	1,250
	TONS/HR	24	49	25	24	24	6	15	0.625
FEED RATE (4000 STUB CULM)	LBS/HR	32,752	—	—	32,752	48,000	2,188	30,000	983
	TONS/HR	16.38	—	—	16.38	24	4.094	15	0.49
DESIGN RATE	TONS/HR	24	49	25	24	24	BY OPER-OLIVER	15	BY OPER-OLIVER



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STONE & WEBSTER ENGINEERING CORPORATION CLIENT CONTRACT NO. ET-78-C-01-3269 DEPARTMENT OF ENERGY SHAMOKIN AREA INDUSTRIAL CORPORATION ANTHRACITE CULM COMBUSTION GULF CENTER UNIT SHAMOKIN, PENNSYLVANIA TITLE PROCESS FLOW DIAGRAM CULM CRUSHING & CULM AND LIMESTONE STORAGE AREA J. O. NUMBER 13258 DWG. NO. 75-D1 ISSUE A			

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Figure 2.1

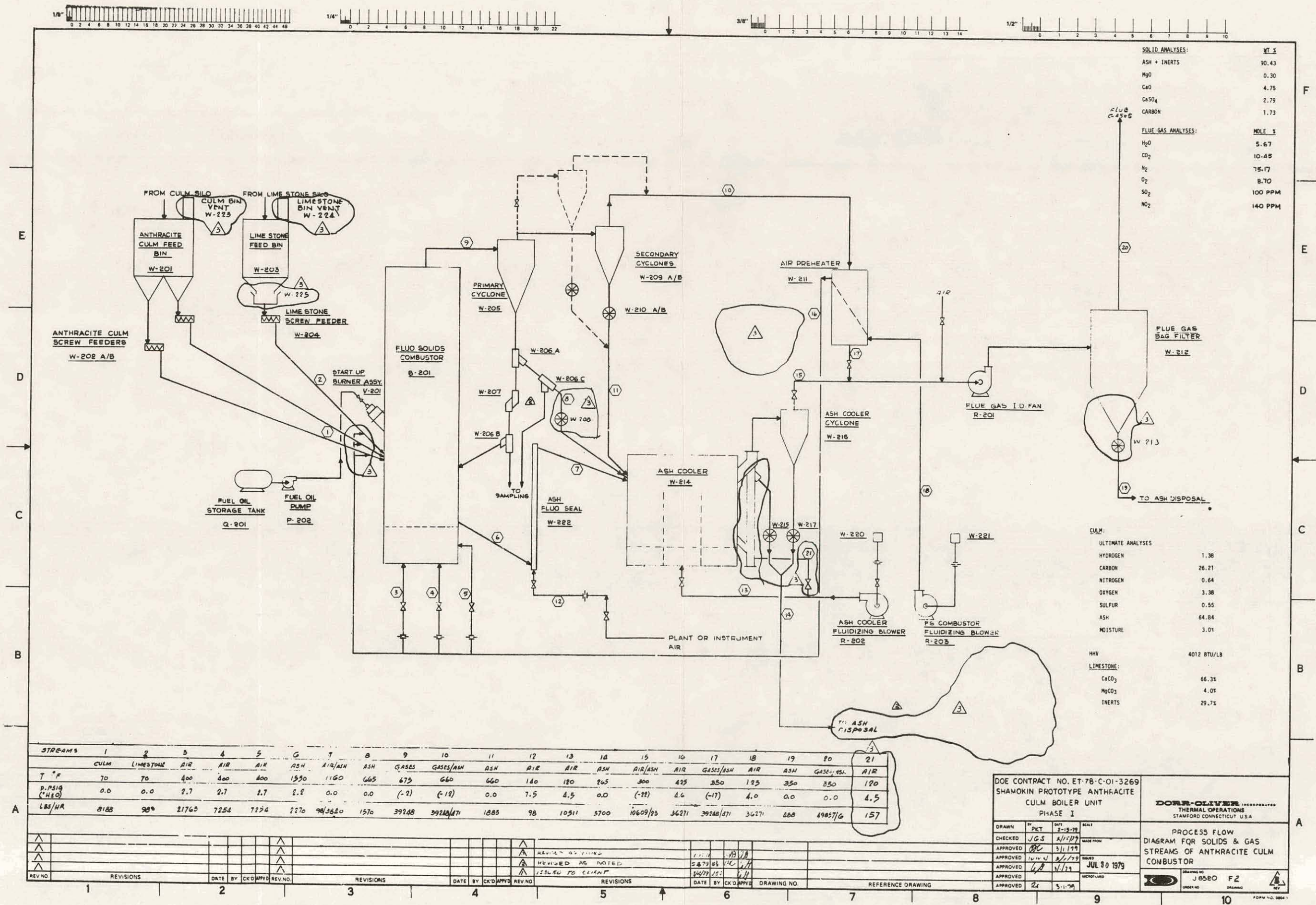


Figure 2.2

TABLE 1

GENERAL MATERIAL BALANCE

IN:

	<u>LBS/HR</u>
Culm	8,188
Limestone	983
Air	46,880
Water	<u>22,100</u>
Total	78,151

OUT:

Ash	6,194
Gases	49,857
Steam	20,100
Blowdown	<u>2,000</u>
Total	78,151

TABLE 2
GENERAL ENERGY BALANCE

HEAT IN:

	<u>BTU/HR</u>
Culm	32.85 x 10 ⁶
Sulfation	<u>0.33 x 10⁶</u>
	33.18 x 10 ⁶

HEAT OUT:

Gases	5.31 x 10 ⁶
Steam	22.84 x 10 ⁶
Blowdown	0.61 x 10 ⁶
Calcination	0.50 x 10 ⁶
Solids	0.31 x 10 ⁶
Losses	<u>3.61 x 10⁶</u>
	33.18 x 10 ⁶

TABLE 3
ULTIMATE ANALYSIS - ANTHRACITE CULM

	<u>% (DRY BASIS)</u>
Carbon	27.02
Hydrogen	1.42
Nitrogen	0.66
Oxygen	3.48
Sulfur	0.57
Ash	66.85
Heating Value, HHV	4,198 Btu/lb

TABLE 4
ANTHRACITE CULM ASH ANALYSIS

Total CaO, %	0.133
Na, ppm	1,495
K, ppm	12,500
Fe, %	1.96
Al ₂ O ₃ , %	27.51
SiO ₂ , %	59.25
Sulfate Sulfur, %	0.085
Cl, ppm	100

TABLE 5
LIMESTONE ANALYSIS

Total CaO, %	37.15
Available CaO, %	0.095
MgO, %	1.92
Na, ppm	248
K, ppm	242
Fe, %	1.37
Al ₂ O ₃ , %	2.31
SiO ₂ , %	15.86
Acid Insolubles, %	22.55
Cl, ppm	200
Acid Evolution CO ₂ , %	31.73
LOI at 1000°C, %	32.22

4.0 OPERATING AND TURNDOWN CONDITIONS

4.1 Operating Conditions

The culm boiler is designed to operate at 1550°F and 5.5 ft/sec superficial fluidization velocity during full load operation. The fluidizing air will be supplied to the boiler at the rate of 36,271 lbs/hr. At this design condition, the boiler will utilize culm and limestone at the rate of 8,188 lbs/hr and 983 lbs/hr, respectively. The boiler will be operated at 30% excess air. Complete performance at design condition is shown in Table 6.

4.2 Turndown Conditions

The bed area is divided into three segments to achieve maximum turndown capability of 2.5/1. Various steam demands can be met by controlling the following variables:

1. Operating Temperature

Reducing bed operating temperature from 1550°F to 1450°F can reduce the steam production by 10%.

2. Fluidization Velocity

Fluidization velocity in the bed can be reduced from 5.5 ft/sec to 3.5 ft/sec. This can reduce the steam production by 20%.

3. Bed Area

Defluidizing the 36% bed zones can reduce the steam production to 64%. This reduction can be achieved in two stages; by defluidizing 18% of bed area which reduces the steam production to 82%, and then by defluidizing the other 18% of bed area which will bring the steam production to 64%.

4. Bed Depth

Over a longer period the steam production from the bed coils can be varied by changing the bed depth.

Steam production can be reduced to 40% of design rate by a combination of the above variables.

A schedule of load following turndown is presented in Table 7, and schematically in Figure 5.1.

TABLE 6
PERFORMANCE ANALYSIS

Combustion Efficiency, %	95
Sulfur Capture, %	88
Excess Air, %	30
Fluidization Velocity, fps	5.5
Combustion Temperature, °F	1,550
Culm Heating Value, HHV, Btu/lb	4,012
Culm Rate, lbs/hr	8,188
Limestone Rate, lbs/hr	983
Ca/S Ratio	5.8

TABLE 7

LOAD FOLLOWING TURNDOWN SCHEDULE

<u>Load Range</u>	<u>Bed Temperature</u>	<u>Space Rate</u>	<u>Zones Fluidized</u>	<u>Bed Height</u>
100-110%	1550-1650°F	5.5 FPS	1,2,3	5 Ft
90-100%	1450-1550°F	5.5 FPS	1,2,3	5 Ft
70-90%	1450°F	3.5-5.5 FPS	1,2,3	5 Ft
65-70%	1450-1550°F	5.5 FPS	1,2	5 Ft
58-65%	1450°F	3.5-5.5 FPS	1,2	5 Ft
58-58%	1450-1550°F	5.5 FPS	1	5 Ft
45-50%	1450°F	3.5-5.5 FPS	1	5 Ft
40-45%	1450°F	3.5 FPS	1	3-5 Ft

5.0 PROCESS CONTROL AND INSTRUMENTATION

As is true for most steam generators, steam drum pressure is the primary controlled variable. The amount of fuel feed is controlled to maintain the boiler pressure at the control setpoint. The fuel flow is regulated by the control in order to maintain drum pressure. Bed temperature, space rate, fluidizing zones and bed height are also varied in accordance with turndown schedule shown on Figure 5.1. The process control computer provides the logic and loop controls necessary to accomplish this capability for turndown. The instrumentation to achieve this control is fully defined in the P&ID's and the strategy is defined in Figure 5.2, Control System Schematic Diagram.

At varying culm feed rates, the limestone feed rate will be roughly controlled according to a preset ratio. This ratio will depend on the limestone activity. The limestone feed rate will be fine tuned within controlled limits by feedback from the SO₂ analyzer.

For a given steam flow either one, two or all three windboxes will be used. Again, which ones used will be predetermined in the digital computer. In no case will the excess air level in the combustion gases fall below 15%. This low limit will be controlled by feedback from the oxygen analyzer.

In order to achieve maximum turndown, reduced bed heights will be used. Signals from the digital computer will control the bed height setpoint. Bed height is adjusted by the rate of ash removal from the bed to the ash cooler. The actual bed height is determined by measurement of the Δp across the bed.

For efficient dust removal prior to the air preheater, either one or both of the secondary cyclones will be used, depending on airflow rates. Therefore, at a given minimum airflow rate one cyclone is isolated.

The baghouse filter is protected from overheating by a temperature controller. This controller adjusts the bleed rate of ambient air into the hot gases flowing to the filter.

LOAD-FOLLOWING TURN-DOWN SCHEDULE INCREASING VS DECREASING LOAD

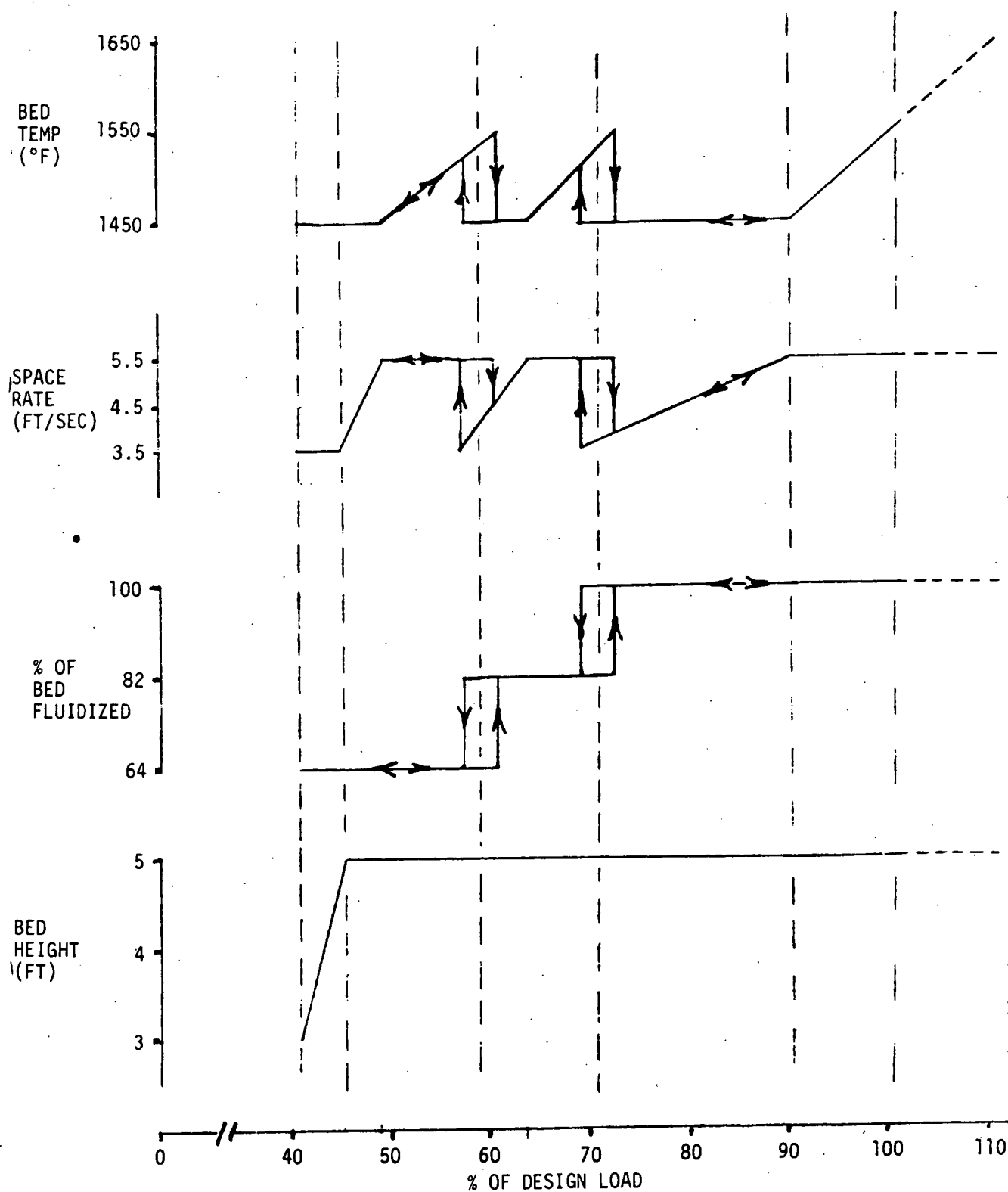


Figure 5.1

Besides these controls, standard steam/water side controls are used. Controls to switch from the electrically driven boiler feed water pump to the turbine driven pump in the event of a pump failure or power outage are also provided.

Analyses of the flue gases will be performed on line and continuously. The analyses include CO, CO₂, O₂, NO_x, and SO₂ determinations. The gases will be sampled downstream of the secondary cyclone. Provision has also been included for the addition of flue gas stack sampling and further opacity monitoring.

In addition to these controls, numerous temperature, pressure, differential pressure, flow rate and level sensing devices will be used to permit heat and material balance calculations, performance calculations and to aid in troubleshooting.

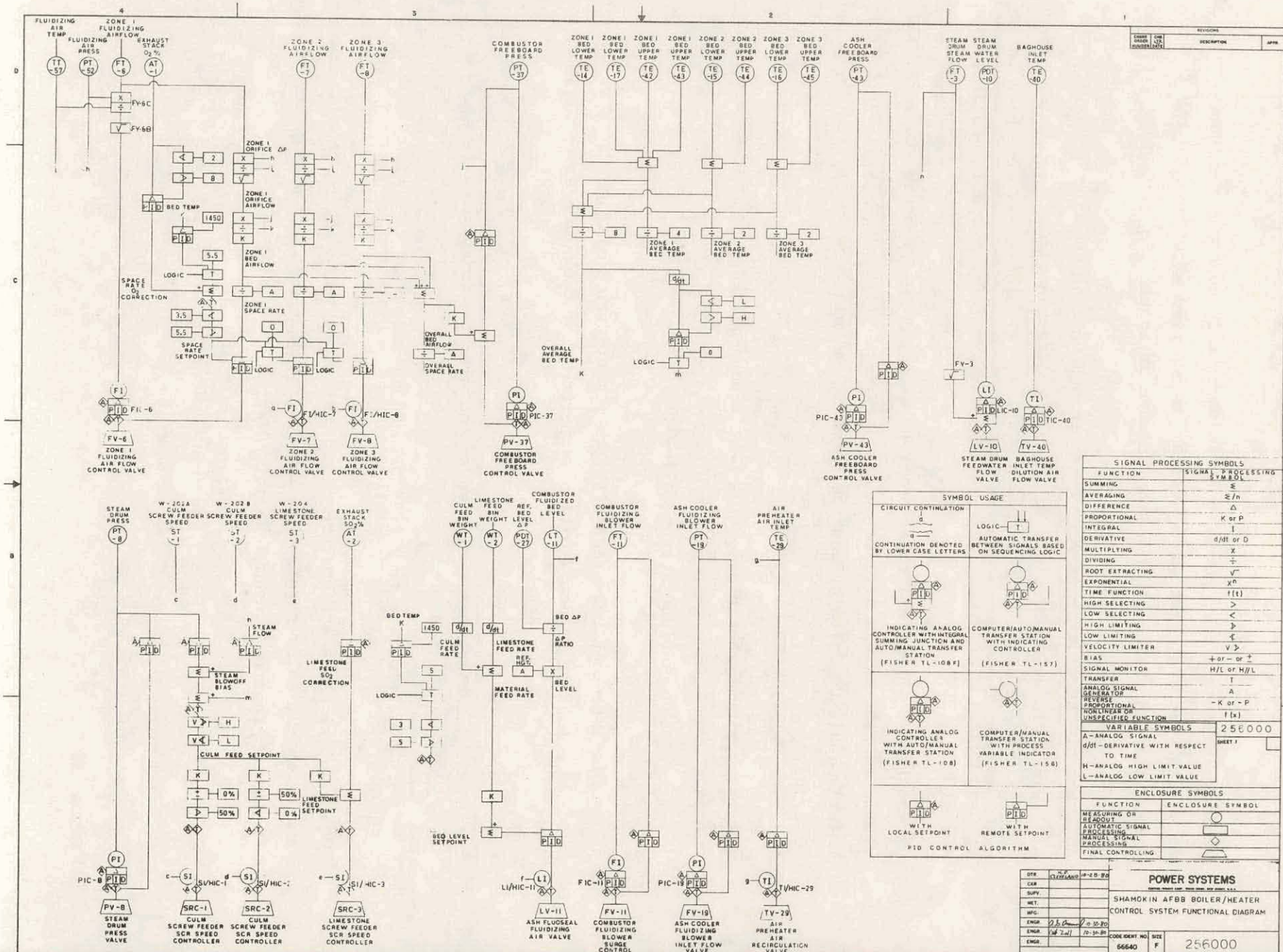
Necessary alarms and interlocking have been provided to permit safe operation.

Key interlocks provided are as follows:

1. Interlock culm feed with bed temperature to prevent feed of culm below the proper ignition temperature or operation at excessively high bed temperature.
2. Interlock the fuel feed system with the drum water level.
3. Interlocking fuel feed with fluidizing air.

Other interlocking systems are as schematically indicated on the P&I Diagrams and as specifically detailed on the Electrical Elementary Wiring Diagrams and Figure 5.2, Control System Schematic Diagram.

Figure 5.2



6.0 EQUIPMENT SPECIFICATIONS AND DETAILED DESIGN

6.1 Equipment List, Instrumentation and Control System

Relevant equipment is herein identified on Pages 27 thru 34 by Equipment Number and Description. The 300 Series Equipment (Curtiss-Wright) relates to a conventional front loader. The make and model is to be determined at time of purchase.

The Instrument and Control System is identified in the Construction Bid Package, Specification SP-N-90, Section J. The Control Panel is identified by Curtiss-Wright Specification E-90085. The related Instrument Loop Diagrams are identified on the following Curtiss-Wright Drawings:

Loop Number

2301 - 2339

2401 - 2421

3101 - 3106

3201 - 3204

3206 - 3209

Total number of loops are 74.

The Data Acquisition, Control and Gas Analysis Systems can be described in general terms as follows:

Process Computer System - Curtiss-Wright Specification E-90080

Vendor - Fisher Controls Co.

1. DC² Process Computer System - W/Accessories:
 - a. Input/Output Subsystems
 - b. CRT
 - c. Printer
 - d. Provox Application Software Package for Data Acquisition and Process Control

Analog Control System - Curtiss-Wright Specification E-90081

Vendor - Fisher Controls Co.

1. TL-Series Instruments
 - a. Computer/Manual Transfer Station
 - b. Computer/Auto/Manual Controllers
 - c. Analog Controllers
2. KM-Series Instruments
 - a. Computing Modules
 - b. Alarm Modules
3. Power Supplies
4. Cabinets

Gas Analysis System - Curtiss-Wright Specification E-90082

Vendor - Pace Associates, Inc.

1. CO₂ Analyzer
2. NO_x Analyzer
3. CO Analyzer
4. SO₂ Analyzer
5. O₂ Analyzer
6. Self-Cleaning Filter Purge System
7. Calibration Accessories

Annunciator - Curtiss-Wright Specification E-90084

Vendor - Ronan, Inc.

1. Multipoint Annunciator
 - a. First Alert Logic
 - b. Horn for Audible Annunciation

Digital Temperature Monitoring System - Curtiss-Wright Specification E-90086

Vendor - Omega

1. Digital Panel Meter with Thermocouple Signal Conditioning
2. Multipoint Selector Switch

STONE & WEBSTER ENGINEERING CORPORATION
PROCESS INDUSTRIES GROUP

ANTHRACITE CULM FLUIDIZED BED
BOILER UNIT

EQUIPMENT LIST INDEX

J.O. NO.

13258

DATE

MAR. 16, 1979

CLIENT

CURTISS-WRIGHT

LOCATION

SHAMOKIN, PA.

TYPE OF UNIT

ACFB

PAGE

1

OF

8

ACCOUNT
CODE

DESCRIPTION

PAGE

REV.
NO.

PAGE
REV.

100 SERIES

STONE & WEBSTER EQUIPMENT

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GENERAL EQUIPMENT

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2

P

PUMPS

2

Q

TANKS

2

N

SOLIDS HANDLING EQUIPMENT

3, 4 & 5

△

V

SPECIAL EQUIPMENT

4

△

S

STACKS

5

△

200 SERIES

DORR-OLIVER EQUIPMENT

B

FLUID BED BOILER

6

△

G

GENERAL EQUIPMENT

6

△

M

DRUMS

6

△

P

PUMPS

6

△

Q

TANKS

6

△

R

FANS

6

△

V

SPECIAL EQUIPMENT

6

△

W

SOLIDS HANDLING EQUIPMENT

7 & 8

△

300 SERIES

CURTISS-WRIGHT EQUIPMENT

W

SOLIDS HANDLING EQUIPMENT

9

△

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

REVISION	1	2	3	4	5	6	7	8	9	10
DATE	4-5-79	4-30-79	5-18-79	7-2-79	9-14-79	1-10-80	2-20-80			

STONE & WEBSTER ENGINEERING CORPORATION							J.O. NO.		
PROCESS INDUSTRIES GROUP							13258		
EQUIPMENT LIST - STONE & WEBSTER EQUIP.					DATE		ACCOUNT CODE		
					MAR. 16 1979		-		
CLIENT		LOCATION		TYPE OF UNIT		PAGE			
CURTISS-WRIGHT		SHAMOKIN, PA.		ACFB		2 OF 8			

EQUIPMENT NUMBER	DESCRIPTION	REV. NO.	ITEM REV. (✓)
G-101	ZEOLITE SOFTENER SYSTEM		
G-102	NEUTRALIZING AMINE/DISPERSANT FEED PKG.		
G-102-VI	AGITATOR		
GM-102-VI	AGITATOR MOTOR		
G-102-PI	FEED PUMP		
GM-102-PI	FEED PUMP MOTOR		
G-102-QI	FEED TANK		
G-103	SODIUM SULFITE FEED PACKAGE		
G-103-VI	AGITATOR		
GM-103-VI	AGITATOR MOTOR		
G-103-PI	FEED PUMP		
GM-103-PI	FEED PUMP MOTOR		
G-103-QI	FEED TANK		
G-104	DEAERATOR		⚠
M-102	BLOW DOWN DRUM		
P-101 A+B	BOILER FEEDWATER PUMPS		
PM-101A	MOTOR		
PT-101B	TURBINE		
P-102 A+B	TREATED WATER PUMPS		
PM-102A	MOTOR		
PM-102B	MOTOR		
Q-101	TREATED WATER TANK		

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

REVISION	1	2	3	4	5	6	7	8	9	10
DATE	4-5-79	4-30-79	5-18-79	7-2-79	9-14-79	1-10-80	2-20-80			

STONE & WEBSTER ENGINEERING CORPORATION						J.O. NO. 13258	
PROCESS INDUSTRIES GROUP						ACCOUNT CODE -	
EQUIPMENT LIST - STONE & WEBSTER EQUIP.				DATE MAR. 16, 1979			
CLIENT CURTISS-WRIGHT		LOCATION SHAMOKIN, PA.		TYPE OF UNIT ACFB		PAGE 3 OF 8	

EQUIPMENT NUMBER	DESCRIPTION	REV. NO.	ITEM REV. (✓)
W-101	FEED HOPPER WITH VIBRATING PAN		
WM-101	PAN MOTOR	A	
W-102	RAW CULM FEED BELT CONVEYOR		
WM-102	RAW CULM FEED BELT CONVEYOR MOTOR		
W-103	CRUSHER	A	
WM-103	CRUSHER MOTOR	A	
W-104	deleted	A	
W-105	deleted	A	
W-106	CRUSHED CULM BUCKET ELEVATOR		
WM-106	CRUSHED CULM BUCKET ELEVATOR MOTOR		
W-107	CRUSHED CULM VIBRATING SCREEN		
WM-107	CRUSHED CULM VIBRATING SCREEN MOTOR		
W-108	SCREENED CULM BUCKET ELEVATOR		
WM-108	SCREENED CULM BUCKET ELEVATOR MOTOR		
W-109	SCREENED CULM STORAGE SILO		
W-110	SCREENED CULM STR. SILO VIBRATING BIN BOTTOM		
WM-110	VIBRATING BIN BOTTOM MOTOR		
W-111	SCREENED CULM SCREEN CONVEYOR		
WM-111	SCREENED CULM SCREEN CONVEYOR MOTOR		

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

REVISION	1	2	3	4	5	6	7	8	9	10
DATE	4-5-79	4-30-79	5-18-79	7-2-79	9-14-79	1-10-80	2-20-80			

STONE & WEBSTER ENGINEERING CORPORATION							J.O. NO.		
PROCESS INDUSTRIES GROUP							13258		
EQUIPMENT LIST - STONE & WEBSTER EQUIP.					DATE		ACCOUNT CODE		
					MAR. 16, 1979		-		
CLIENT			LOCATION		TYPE OF UNIT		PAGE		
CUTISS-WRIGHT			SHAMOKIN, PA		ACFB		4 of 6		

EQUIPMENT NUMBER	DESCRIPTION	REV. NO.	ITEM REV. (✓)
W-112	SCREENED CULM FEED BUCKET ELEVATOR		
WM-112	SCREENED CULM FD. BUCKET ELEVATOR MOTOR		
W-113	LIMESTONE STORAGE SILO		
W-114	LIMESTONE STG. SILO VIBRATING BIN BOTTOM		
WM-114	VIBRATING BIN BOTTOM MOTOR		
W-115	STORED LIMESTONE SCREEN FEEDER		
WM-115	STORED LIMESTONE SCREEN FEEDER MOTOR		
W-116	LIMESTONE FEED BUCKET ELEVATOR		
WM-116	LIMESTONE FD. BUCKET ELEV. MOTOR		
W-117	deleted	2	
W-118	deleted	2	
W-119	ASH PNEUMATIC CONVEYING SYSTEM	3	
W-119M	BLOWER MOTOR		
W-120	ASH BIN	3	
W-121	ASH BIN ACTIVATOR	3	
W-121M	MOTOR		
W-122	BIN VENT DUST COLLECTION	3	
W-123	POWER AIR SLIDE GATE VALVE	3	
	TELESCOPING CHUTE		
V-101	deleted	4	

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

REVISION	1	2	3	4	5	6	7	8	9	10
DATE	4-5-79	4-30-79	5-18-79	7-2-79	8-11-79	1-10-80	2-20-80			

STONE & WEBSTER ENGINEERING CORPORATION						J.O. NO.		13258	
PROCESS INDUSTRIES GROUP						DATE		ACCOUNT CODE	
EQUIPMENT LIST - <i>Stone & Webster Equip</i>						JULY 2, 1979		-	
CLIENT		LOCATION		TYPE OF UNIT		PAGE		OF	
<i>CURTIS - WRIGHT</i>		<i>SHAMOKIN, PA</i>		<i>ACFB</i>		<i>5</i>		<i>8</i>	

EQUIPMENT NUMBER	DESCRIPTION	REV. NO.	ITEM REV. (✓)
<i>W-124</i>	<i>deleted</i>	<i>6</i>	
<i>WM-124</i>	<i>deleted</i>	<i>6</i>	
<i>W-125</i>	<i>deleted</i>	<i>6</i>	
<i>W-126</i>	<i>deleted</i>	<i>6</i>	
<i>WM-126</i>	<i>deleted</i>	<i>6</i>	
<i>W-127</i>	<i>deleted</i>	<i>6</i>	
<i>W-128</i>	<i>deleted</i>	<i>6</i>	
<i>W-129</i>	<i>CULM & LIMESTONE DUST COLLECTION SYSTEM</i>	<i>6</i>	
<i>WV-129-1</i>	<i>DUST COLLECTOR BLOWER MOTOR</i>	<i>6</i>	
<i>WM-129-2</i>	<i>DUST COLLECTOR ROTARY AIR LOCK MOTOR</i>	<i>6</i>	
<i>W-130</i>	<i>FLY ASH DISCHARGE POWER AIR SLIDE GATE</i>		
	<i>VALVE & TELESCOPING CHUTE SYSTEM</i>	<i>6</i>	
<i>WM-130-1</i>	<i>HOIST MOTOR</i>	<i>6</i>	
<i>WM-130-2</i>	<i>FAN MOTOR</i>	<i>6</i>	
<i>MM-104</i>	<i>STEAM VENT SILENCER</i>	<i>6</i>	
<i>S-101</i>	<i>FLUE GAS STACK</i>	<i>5</i>	

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

REVISION	1	2	3	4	5	6	7	8	9	10
DATE	—	—	—	7-2-79	7-12-79	1-10-80	2-20-80			

STONE & WEBSTER ENGINEERING CORPORATION PROCESS INDUSTRIES GROUP							J.O. NO. 13258			
EQUIPMENT LIST - DOZEE-OLIVER EQUIP.							DATE MAR. 16, 1979		ACCOUNT CODE -	
CLIENT CURTISS-WRIGHT			LOCATION SHAMOKIN, PA.			TYPE OF UNIT ACFB		PAGE 6 OF 8		

EQUIPMENT NUMBER	DESCRIPTION	REV. NO.	ITEM REV. (✓)
B-201	FLUO-SOLIDS COMBUSTOR	1	
	WITH INTEGRAL STEAM DRUM	2	
V-201	START-UP BURNER ASSEMBLY (WITH B-201)		
VM-201	BURNER BLOWER MOTOR	1	✓
G-201	INSTRUMENT AIR DRYER		
P-201	deleted	2	
M-201	deleted	3	
P-201	deleted	2	
P-202	FUEL OIL PUMP	1	
PM-202	MOTOR		
R-201	FUEL OIL STORAGE TANK	1	
R-201	FLUE GAS I.D. FAN		
RM-201	MOTOR		
R-202	ASH COOLER FLUIDIZING BLOWER		
RM-202	MOTOR		
R-203	F.S. COMBUSTOR FLUIDIZING BLOWER		
RM-203	MOTOR		
R-204	deleted	5	
RM-204	deleted	5	
R-205	INSTRUMENT AIR COMPRESSOR		
RM-205	MOTOR		
V-202	CO ₂ FIRE PROTECTION SYSTEM FOR W-211	1	✓
V-203	WATER SEAL	1	✓

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

REVISION	1	2	3	4	5	6	7	8	9	10
DATE	4-5-79	4-30-79	5-13-79	7-2-79	7-11-79	1-10-80	2-20-80			

STONE & WEBSTER ENGINEERING CORPORATION							J.O. NO.			
PROCESS INDUSTRIES GROUP							13258			
EQUIPMENT LIST - DORR-OLIVER EQUIP.					DATE MAR. 16, 1979		ACCOUNT CODE —			
CLIENT CURTISS-WRIGHT			LOCATION SHAMOKIN, PA.		TYPE OF UNIT ACFB		PAGE 7 OF 8			

EQUIPMENT NUMBER	DESCRIPTION	REV. NO.	ITEM REV. (✓)
W-201	ANTHRACITE CULM FEED BIN		
W-202 A+B	ANTHRACITE CULM SCREEN FEEDERS		
WM-202 A+B	MOTORS		
W-203	LIMESTONE FEED BIN		
W-204	LIMESTONE SCREEN FEEDER		
WM-204	MOTOR		
W-205	PRIMARY CYCLONE	△	
W-206 A,B,C	PRIMARY CYCLONE SPLITTER VALVES	△	
W-207	PRIMARY CYCLONE TRICKLE VALVE	△	
W-208	PRIMARY CYCLONE DISCHARGE VALVE	△	
WM-208	MOTOR		
W-209 A+B	SECONDARY CYCLONES	△	
W-210 A+B	SECONDARY CYCLONE DISCHARGE VALVES	△	
WM-210 A+B	MOTORS		
W-211	AIR PREHEATER		
W-212	FLUE GAS BAG FILTER		
W-213	FLUE GAS BAG FILTER DISCHARGE VALVE	△	
WM-213	MOTOR	△	

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

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DATE	4-5-79	4-30-79	5-19-79	7-2-79	9-11-79	1-10-80	2-20-80			

STONE & WEBSTER ENGINEERING CORPORATION
PROCESS INDUSTRIES GROUP

J.O. NO. 13258

EQUIPMENT LIST - DORR-OLIVER EQUIP.

DATE MAR. 16, 1979

ACCOUNT CODE -

CLIENT CURTISS-WRIGHT

LOCATION SHAMOKIN, PA

TYPE OF UNIT ACFB

PAGE 8 OF 8

EQUIPMENT NUMBER	DESCRIPTION	REV. NO.	ITEM REV. (✓)
W-214	ASH COOLER		
W-215	ASH COOLER DISCHARGE VALVE		
WM-215	MOTOR		
W-216	ASH COOLER CYCLONE		
W-217	ASH COOLER CYCLONE DISCHARGE VALVE		
WM-217	MOTOR		
W-218	deleted	3	
W-219	deleted	3	
W-220	ASH COOLER FLUIDIZING BLOWER INLET FILTER		
W-221	F.S COMBUSTOR FLUIDIZING BLOWER INLET FILTER		
W-222	ASH FLUD SEAL	4	
W-223	ANTHRACITE CULM FEED BIN VENT	4	
W-224	LIMESTONE FEED BIN VENT	4	
W-225	LIMESTONE FEED BIN VIBRATING BOTTOM	4	
WM-225	MOTOR	4	

CHECK (✓) INDICATES ITEM WAS CHANGED IN LATEST REVISION.

REVISION	1	2	3	4	5	6	7	8	9	10
DATE	4-5-79	4-30-79	5-13-79	7-2-79	9-14-79	1-10-80	2-20-82			

6.2 P&I Diagrams

The following Drawings and Lists are provided herein:

<u>Figure Number</u>	<u>Title</u>
6.1	General Notes and Index
6.2	Culm Crushing and Culm and Limestone Storage
6.3	Fluid Bed Combustor System
6.4	Flue Gas and Ash Handling System
6.5	Water Treatment and Boiler Feed System
6.6	Fluid Bed Combustor System Steam Generation
6.7	Utility Distribution System and Details
6.8	Line Designation Table Index
6.9	Line Designation Table

Figure 6.1

GENERAL NOTES		SYMBOLS		EQUIPMENT LIST				DRAWING INDEX			
EXCEPT AS OTHERWISE NOTED ON THE FLOW DIAGRAMS, THE FOLLOWING INFORMATION APPLIES:				ITEM	SHEET	ITEM	SHEET	ITEM	SHEET	DWG. NO.	DESCRIPTION
1. WHILE NOT SHOWN ON THE DIAGRAMS, 3/4" VALVED VENT CONNECTIONS ARE TO BE PROVIDED FOR TRAPPED HIGH POINTS OF PIPING 2" AND LARGER. 3/4" VALVED DRAIN CONNECTIONS SHALL BE FURNISHED FOR LOW POINTS OF LINES ABOVE GRADE.		1. GATE VALVE		G-101	73-D1	W-110	72-D2	R-202	72-D4	W-217	72-D4
2. ALL VALVED VENTS & DRAINS ARE FITTED WITH NIPPLE & CAPPED OR BLINDED, EXCEPT PUMP VENTS & DRAINS.		2. GLOBE VALVE		G-102	73-D1	W-110	72-D2	R-202	72-D4	W-217	72-D4
3. UNDESHATED PIPING & VALVING ON EQUIPMENT SHALL FOLLOW THE CLASS OF THE LOCAL PIPING.		3. PLUS COCK		G-102-VI	73-D1	W-111	72-D2	R-203	72-D4	W-220	72-D4
4. IN GENERAL, INSTRUMENTATION IS PER I.S.A. STANDARD S.S.I.		4. BUTTERFLY VALVE		G-102-VI	73-D1	W-111	72-D2	R-203	72-D4	W-221	72-D4
5. ALL PRESSURE INSTRUMENTS SHALL BE FURNISHED WITH A PROCESS BLOCK VALVE WITH INSTRUMENT END TO BE TREADED 3/4" NPT.		5. CONTROL VALVE		G-103	73-D1	W-112	72-D2	W-222	72-D3		
6. FLOW METER ORIFICE FLANGES ARE IN ACCORDANCE WITH THE PIPE LINE SPECIFICATION BUT WITH A MINIMUM RATING & FACE OF 500 P.S.F.		6. CONTROL VALVE WITH HANDWHEEL		G-103-VI	73-D1	W-113	72-D2	W-301	72-D2		
7. ORIFICE FLANGE VALVES ARE NOT SHOWN ARE PART OF PIPING SUPPLY.		7. HAND CONTROL VALVE		G-103-P1	73-D1	W-114	72-D2	W-129	72-D2		
8. EXTERNAL FLOAT SWITCHES (1" NPT) SHALL BE PROVIDED WITH 1" SHUT-OFF VALVES & 3/4" DRAIN VALVE. THE VALVES WILL NOT BE SHOWN ON THE DIAGRAMS.		8. CHECK VALVE		G-104	73-D1	W-114	72-D2	W-129-2	72-D2		
9. EXTERNAL GAGE TYPE LEVEL INSTRUMENTS SHALL BE PROVIDED WITH 2" SHUT-OFF VALVES & 3/4" DRAIN VALVE NOT SHOWN ON THE DIAGRAMS.		9. BALL VALVE		H-101	73-D1	W-115	72-D2	W-130	72-D4		
10. LEVEL GAGES WILL BE FURNISHED COMPLETE WITH VALVES BY INSTRUMENT.		10. CHECK VALVE		H-102	73-D1	W-116	72-D2	W-130-2	72-D4		
11. ALL LEVEL COLUMNS (STANDPIPES) ARE TO BE 2", EXCEPT AS NOTED.		11. NON-RETURN		M-102	73-D1	W-117	72-D2	W-223	72-D3		
12. TEMPERATURE WELLS FOR OPERATING INSTRUMENTS ARE NOT SHOWN.		12. ANGLE VALVE		M-104	73-D1	W-118	72-D2	W-224	72-D3		
13. FOR FREEZE PROTECTION DURING COLD WEATHER, ALL UNHEATED WATER SYSTEMS WILL BE EMPTIED THROUGH LOW POINT DRAINS DURING PERIODS OF WINTERIZATION. WATER WILL BE CIRCULATED THROUGH EQUIPMENT ON STANDBY. (SEE NOTE 15 BELOW)		13. ROTAMETER		P-101A & B	73-D1	W-119	72-D4	W-225	72-D3		
14. TYPICAL FUNCTION SYMBOL FOR DIGITAL CONTROL SYSTEM (TMS SC-1) LOCATED IN CONTROL ROOM. SEE SPECIFICATION NO. KB10 FOR FULL FUNCTIONAL DETAILS.		14. ROTAMETER		P-101B	73-D1	W-120	72-D4	W-226	72-D3		
15. ALL ITEMS OF EQUIPMENT SHOWN INSIDE PACKAGE BOUNDARY LINES ARE INCLUDED WITH THE PARTICULAR PACKAGE.		15. ROTAMETER		Q-101	73-D1	W-121	72-D4	W-227	72-D3		
16. ALL PUMP STRAINERS WILL HAVE THE FOLLOWING MESH SIZE EXCEPT WHERE NOTED OTHERWISE AS AN ITEM.		16. ROTAMETER		Q-101	73-D1	W-122	72-D4	W-228	72-D3		
17. ALL ELECTRIC MOTOR DRIVERS IN SOLID HANDLING SERVICE TO HAVE LOCAL AMMETERS, NOT SHOWN ON E.P.D.'S.		17. ROTAMETER		Q-101	73-D1	W-123	72-D4	W-229	72-D3		
18. ELECTRICAL TRACING WILL BE APPLIED WHERE SHOWN ON THE DIAGRAMS, WHERE INDICATED WITHIN PACKAGE BOUNDARIES, TRACING WILL BE DONE BY OTHERS.		18. ROTAMETER		Q-101	73-D1	W-124	72-D4	W-230	72-D3		
19. ALL THERMOWELL CONNECTIONS ON C.V. VESSELS & PIPING 3" & LARGER SHALL BE 1" TREADED. PIPING LESS THAN 3" SHALL BE SWAGED TO 3" ALLOY & S.S. PIPING TO HAVE 1/2" FLANGED THERMOWELL CONNECTIONS.		19. ROTAMETER		Q-101	73-D1	W-125	72-D4	W-231	72-D3		
		20. ROTAMETER		Q-101	73-D1	W-126	72-D4	W-232	72-D3		
		21. ROTAMETER		Q-101	73-D1	W-127	72-D4	W-233	72-D3		
		22. ROTAMETER		Q-101	73-D1	W-128	72-D4	W-234	72-D3		
		23. ROTAMETER		Q-101	73-D1	W-129	72-D4	W-235	72-D3		
		24. ROTAMETER		Q-101	73-D1	W-130	72-D4	W-236	72-D3		
		25. ROTAMETER		Q-101	73-D1	W-131	72-D4	W-237	72-D3		
		26. ROTAMETER		Q-101	73-D1	W-132	72-D4	W-238	72-D3		
		27. ROTAMETER		Q-101	73-D1	W-133	72-D4	W-239	72-D3		
		28. ROTAMETER		Q-101	73-D1	W-134	72-D4	W-240	72-D3		
		29. ROTAMETER		Q-101	73-D1	W-135	72-D4	W-241	72-D3		
		30. ROTAMETER		Q-101	73-D1	W-136	72-D4	W-242	72-D3		
		31. ROTAMETER		Q-101	73-D1	W-137	72-D4	W-243	72-D3		
		32. ROTAMETER		Q-101	73-D1	W-138	72-D4	W-244	72-D3		
		33. ROTAMETER		Q-101	73-D1	W-139	72-D4	W-245	72-D3		
		34. ROTAMETER		Q-101	73-D1	W-140	72-D4	W-246	72-D3		
		35. ROTAMETER		Q-101	73-D1	W-141	72-D4	W-247	72-D3		
		36. ROTAMETER		Q-101	73-D1	W-142	72-D4	W-248	72-D3		
		37. ROTAMETER		Q-101	73-D1	W-143	72-D4	W-249	72-D3		
		38. ROTAMETER		Q-101	73-D1	W-144	72-D4	W-250	72-D3		
		39. ROTAMETER		Q-101	73-D1	W-145	72-D4	W-251	72-D3		
		40. ROTAMETER		Q-101	73-D1	W-146	72-D4	W-252	72-D3		
		41. ROTAMETER		Q-101	73-D1	W-147	72-D4	W-253	72-D3		
		42. ROTAMETER		Q-101	73-D1	W-148	72-D4	W-254	72-D3		
		43. ROTAMETER		Q-101	73-D1	W-149	72-D4	W-255	72-D3		
		44. ROTAMETER		Q-101	73-D1	W-150	72-D4	W-256	72-D3		
		45. ROTAMETER		Q-101	73-D1	W-151	72-D4	W-257	72-D3		
		46. ROTAMETER		Q-101	73-D1	W-152	72-D4	W-258	72-D3		
		47. ROTAMETER		Q-101	73-D1	W-153	72-D4	W-259	72-D3		
		48. ROTAMETER		Q-101	73-D1	W-154	72-D4	W-260	72-D3		
		49. ROTAMETER		Q-101	73-D1	W-155	72-D4	W-261	72-D3		
		50. ROTAMETER		Q-101	73-D1	W-156	72-D4	W-262	72-D3		
		51. ROTAMETER		Q-101	73-D1	W-157	72-D4	W-263	72-D3		
		52. ROTAMETER		Q-101	73-D1	W-158	72-D4	W-264	72-D3		
		53. ROTAMETER		Q-101	73-D1	W-159	72-D4	W-265	72-D3		
		54. ROTAMETER		Q-101	73-D1	W-160	72-D4	W-266	72-D3		
		55. ROTAMETER		Q-101	73-D1	W-161	72-D4	W-267	72-D3		
		56. ROTAMETER		Q-101	73-D1	W-162	72-D4	W-268	72-D3		
		57. ROTAMETER		Q-101	73-D1	W-163	72-D4	W-269	72-D3		
		58. ROTAMETER		Q-101	73-D1	W-164	72-D4	W-270	72-D3		
		59. ROTAMETER		Q-101	73-D1	W-165	72-D4	W-271	72-D3		
		60. ROTAMETER		Q-101	73-D1	W-166	72-D4	W-272	72-D3		
		61. ROTAMETER		Q-101	73-D1	W-167	72-D4	W-273	72-D3		
		62. ROTAMETER		Q-101	73-D1	W-168	72-D4	W-274	72-D3		
		63. ROTAMETER		Q-101	73-D1	W-169	72-D4	W-275	72-D3		
		64. ROTAMETER		Q-101	73-D1	W-170	72-D4	W-276	72-D3		
		65. ROTAMETER		Q-101	73-D1	W-171	72-D4	W-277	72-D3		
		66. ROTAMETER		Q-101	73-D1	W-172	72-D4	W-278	72-D3		
		67. ROTAMETER		Q-101	73-D1	W-173	72-D4	W-279	72-D3		
		68. ROTAMETER		Q-101	73-D1	W-174	72-D4	W-280	72-D3		
		69. ROTAMETER		Q-101	73-D1	W-175	72-D4	W-281	72-D3		
		70. ROTAMETER		Q-101	73-D1	W-176	72-D4	W-282	72-D3		
		71. ROTAMETER		Q-101	73-D1	W-177	72-D4	W-283	72-D3		
		72. ROTAMETER		Q-101	73-D1	W-178	72-D4	W-284	72-D3		
		73. ROTAMETER		Q-101	73-D1	W-179	72-D4	W-285	72-D3		
		74. ROTAMETER		Q-101	73-D1	W-180	72-D4	W-286	72-D3		
		75. ROTAMETER		Q-101	73-D1	W-181	72-D4	W-287	72-D3		
		76. ROTAMETER		Q-101	73-D1	W-182	72-D4	W-288	72-D3		
		77. ROTAMETER		Q-101	73-D1	W-183	72-D4	W-289	72-D3		
		78. ROTAMETER		Q-101	73-D1	W-184	72-D4	W-290	72-D3		
		79. ROTAMETER		Q-101	73-D1	W-185	72-D4	W-291	72-D3		
		80. ROTAMETER		Q-101	73-D1	W-186	72-D4	W-292	72-D3		
		81. ROTAMETER		Q-101	73-D1	W-187	72-D4	W-293	72-D3		
		82. ROTAMETER		Q-101	73-D1	W-188	72-D4	W-294	72-D3		
		83. ROTAMETER		Q-101	73-D1	W-189	72-D4	W-295	72-D3		
		84. ROTAMETER		Q-101	73-D1	W-190	72-D4	W-296	72-D3		
		85. ROTAMETER		Q-101	73-D1	W-191	72-D4	W-297	72-D3		
		86. ROTAMETER		Q-101	73-D1	W-192	72-D4	W-298	72-D3		
		87. ROTAMETER		Q-101	73-D1	W-193	72-D4	W-299	72-D3		
		88. ROTAMETER		Q-101	73-D1	W-194	72-D4	W-300	72-D3		
		89. ROTAMETER		Q-101	73-D1	W-195	72-D4	W-301	72-D3		
		90. ROTAMETER		Q-101	73-D1	W-196	72-D4	W-302	72-D3		
		91. ROTAMETER		Q-101	73-D1	W-197	72-D4	W-303	72-D3		
		92. ROTAMETER		Q-101	73-D1	W-198	72-D4	W-304	72-D3		
		93. ROTAMETER		Q-101	73-D1	W-199	72-D4	W-305	72-D3		
		94. ROTAMETER		Q-101	73-D1	W-200	72-D4	W-306	72-D3		
		95. ROTAMETER		Q-101	73-D1	W-201	72-D4	W-307	72-D3		
		96. ROTAMETER		Q-101	73-D1	W-202	72-D4	W-308	72-D3		
		97. ROTAMETER		Q-101	73-D1	W-203	72-D4	W-309	72-D3		
		98. ROTAMETER		Q-101	73-D1	W-204	72-D4	W-310	72-D3		
		99. ROTAMETER		Q-101	73-D1	W-205	72-D4	W-311	72-D3		
		100. ROTAMETER		Q-101	73-D1	W-206	72-D4	W-312	72-D3		
		101. ROTAMETER		Q-101	73-D1	W-207	72-D4	W-313	72-D3		
		102. ROTAMETER		Q-101	73-D1	W-208	72-D4	W-314	72-D3		
		103. ROTAMETER		Q-101	73-D1	W-209	72-D4	W-315	72-D3		
		104. ROTAMETER		Q-101	73-D1	W-210	72-D4	W-316	72-D3		
		105. ROTAMETER		Q-101	73-D1	W-211	72-D4	W-317	72-D3		
		106. ROTAMETER		Q-101	73-D1	W-212	72-D4	W-318	72-D3		
		107. ROTAMETER		Q-101	73-D1	W-213	72-D4	W-319	72-D3		
		108. ROTAMETER		Q-101	73-D1	W-214	72-D4	W-320	72-D3		
		109. ROTAMETER		Q-101	73-D1	W-215	72-D4	W-321	72-D3		
		110. ROTAMETER		Q-101	73-D1	W-216	72-D4	W-322	72-D3		
		111. ROTAMETER		Q-101	73-D1	W-217	72-D4	W-323	72-D3		
		112. ROTAMETER		Q-101	73-D1	W-218	72-D4	W-324	72-D3		
		113. ROTAMETER		Q-101	73-D1	W-219	72-D4	W-325	72-D3		
		114. ROTAMETER		Q-101	73-D1	W-220	72-D4	W-326	72-D3		
		115. ROTAMETER		Q-101	73-D1	W-221	72-D4	W-327	72-D3		
		116. ROTAMETER		Q-101	73-D1	W-222	72-D4	W-328	72-D3		
		117. ROTAMETER		Q-101	73-D1	W-223	72-D4	W-329	72-D3		
		118. ROTAMETER		Q-101	73-D1	W-224	72-D4	W-330	72-D3		
		119. ROTAMETER		Q-101	73-D1	W-225	72-D4	W-331	72-D3		
		120. ROTAMETER		Q-101	73-D1	W-226	72-D4	W-332	72-D3		
		121. ROTAMETER		Q-101	73-D1	W-227	72-D4	W-333	72-D3		
		122. ROTAMETER		Q-101	73-D1	W-228	72-D4	W-334	72-D3		
		123. ROTAMETER		Q-101	73-D1	W-229	72-D4	W-335	72-D3		
		124. ROTAMETER		Q-101	73-D1	W-230	72-D4	W-336	72-D3		
		125. ROTAMETER		Q-101	73-D1	W-231	72-D4	W-337	72-D3		
		126. ROTAMETER		Q-101	73-D1	W-232	72-D4	W-338	72-D3		
		127. ROTAMETER		Q-101	73-D1	W-233	72-D4	W-339	72-D3		

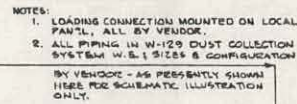


Figure 6.3

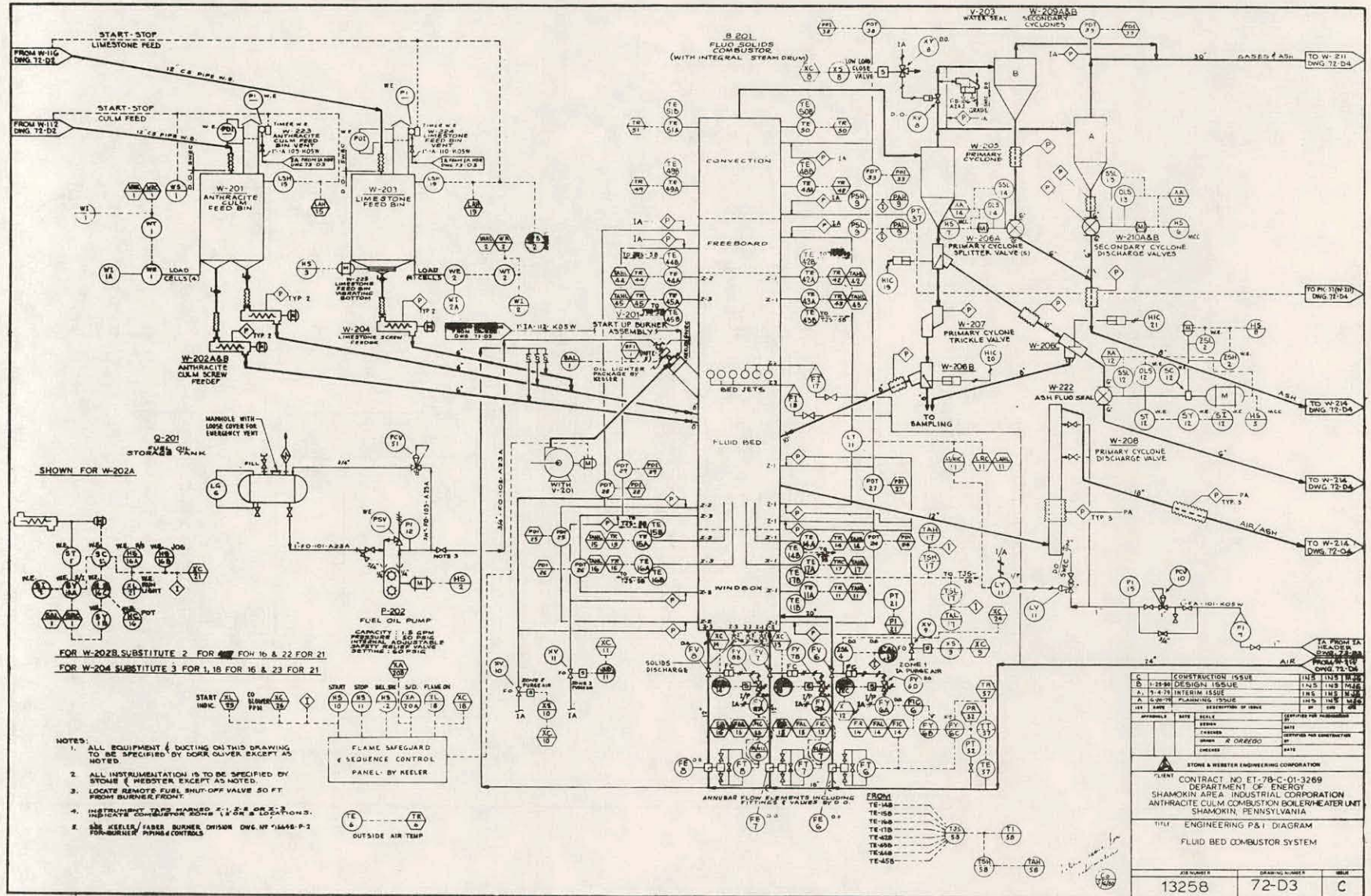


Figure 6.4

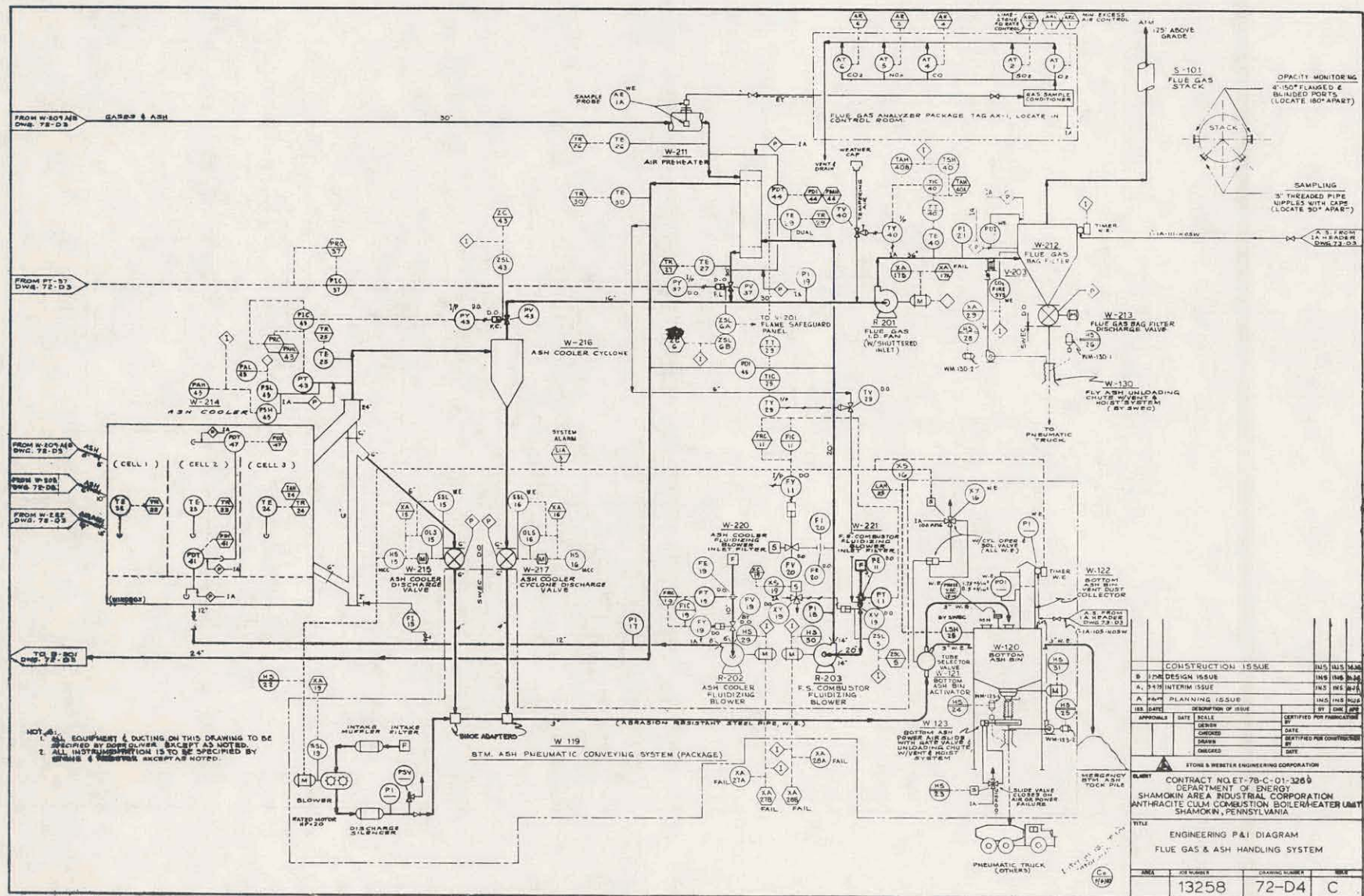


Figure 6.5

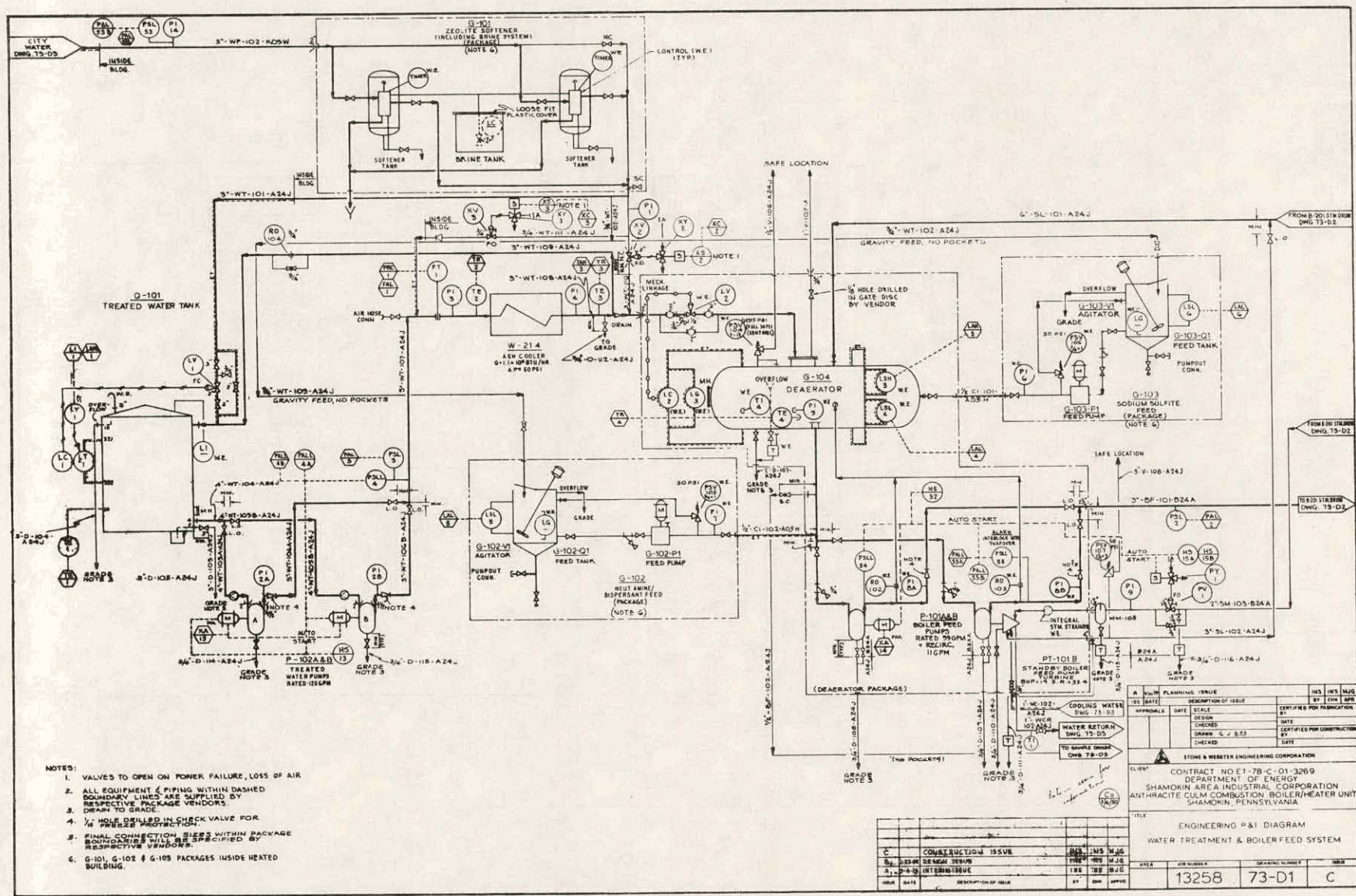


Figure 6.6

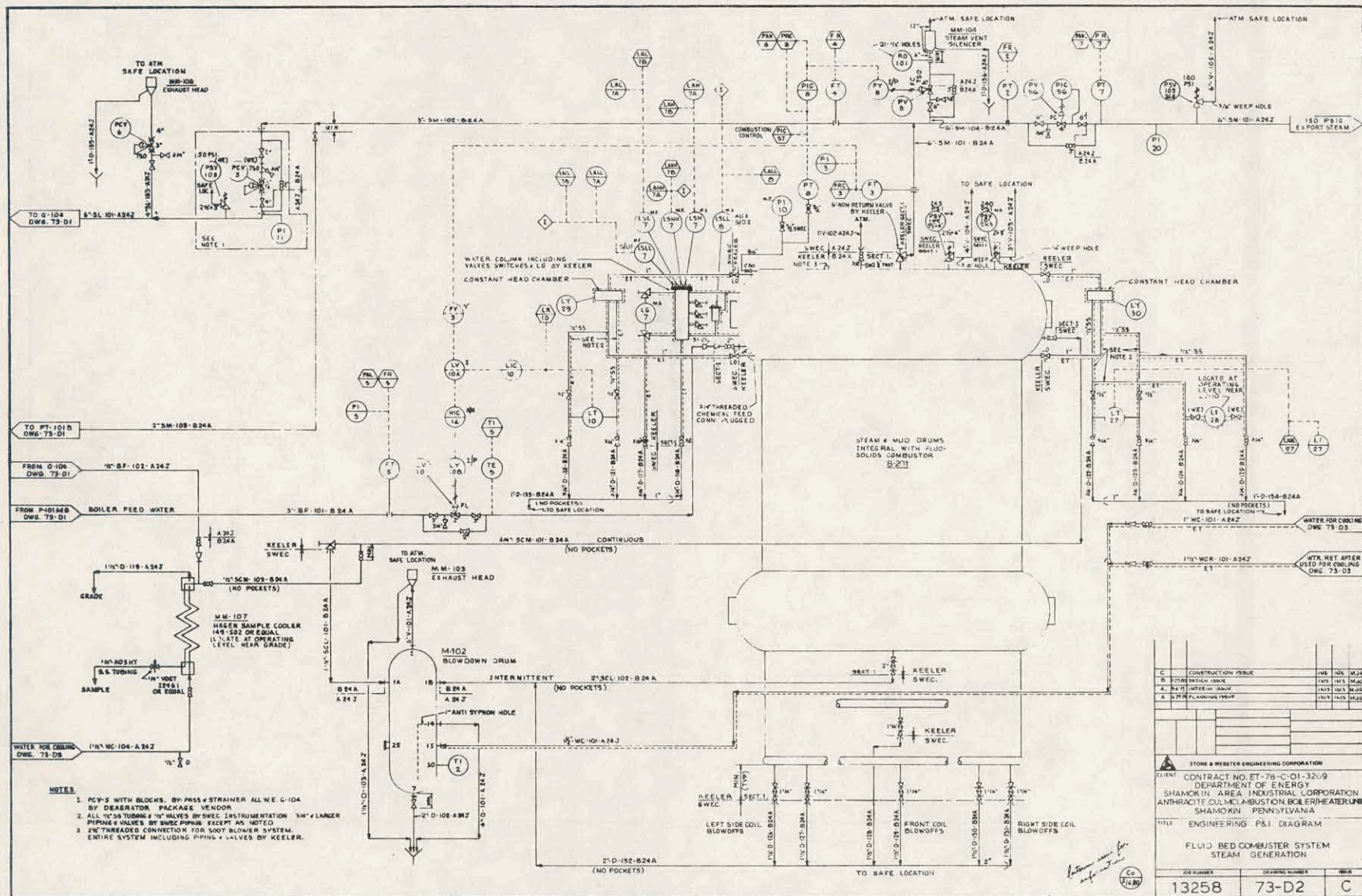
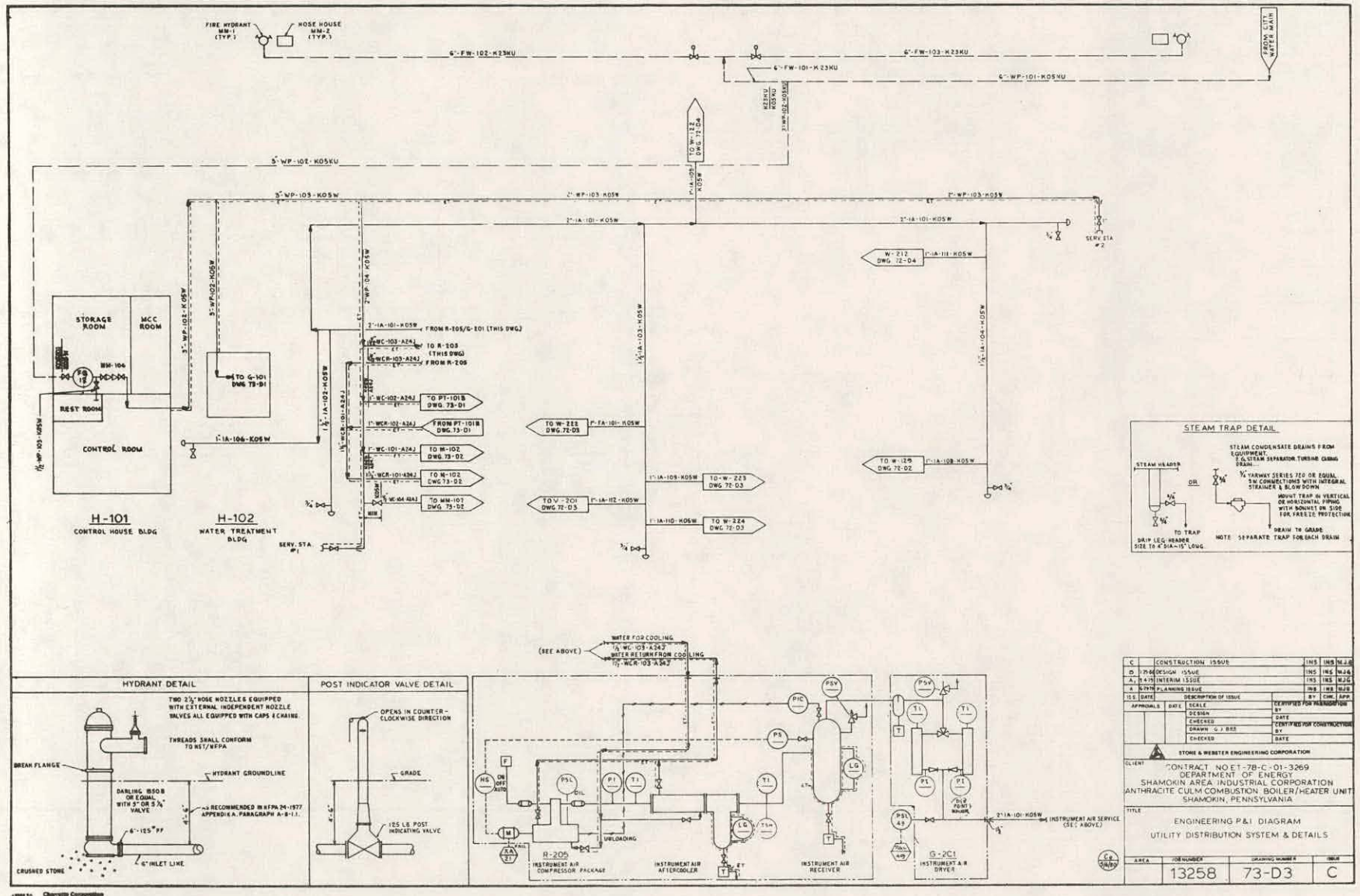


Figure 6.7



LINE DESIGNATION TABLE INDEX

J.O. NO. 13258

CLIENT CURTISS-WRIGHT, SHAMOKIN

ISSUE ⁵⁻⁶⁻⁸³ (C₀) 6-20-79 PAGE 1

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Figure 6.8

LINE DESIGNATION	FLOWING FLUID	PAGE NO.
BF	BOILER FEED WATER	2
CI	CHEMICAL INJECTION	3
D	DRAINS	4, 5, 5A
DS	SANITARY SEWER	
FA	ASH FLO SEAL AIR	6
FO	FUEL OIL	7
FW	FIRE WATER	8
IA	INSTRUMENT AIR	8A
PA	PURGE AIR TO EQUIPMENT	
SA	PLANT AIR	
SCL	LOW PRESSURE STM. CONDENSATE	9
SCM	MEDIUM PRESSURE STM. CONDENSATE	10
SL	LOW PRESSURE STEAM	11
SM	MEDIUM PRESSURE STEAM	12
V	VENT	13

LINE DESIGNATION	FLOWING FLUID	PAGE NO.
WC	WATER FOR COOLING	14
WCR	WATER RETURN AFTER COOLING	15
WP	POTABLE CITY WATER	16
WT	TREATED WATER	17, 18
<u>BOILER CODE (SYMBOL "X" SUFFIX ON CLASS & LINE NOS.)</u>		
BF	BOILER FEED WATER	19
SCM	MEDIUM PRESSURE STM CONDENSATE	20
SM	MEDIUM PRESSURE STEAM	21
V	VENT	22

LINE DESIGNATION TABLE

ISSUE 5-6-80

J.O. NUMBER
13258

CLIENT					PLANT NO.					BY					DATE					PAGE				
CURTISS-WRIGHT, SHAMOKIN										I N SCHOENWETTER					6-20-79					4				
LINE					DESCRIPTION			DESIGN		FLEX	SHORT TERM CONDITIONS			FIELD TEST		INSULATION			FLOW	REMARKS	REV			
SERV. SYMB.	NUMBER	SIZE IN.	SPEC.	SCHEDULE	FLOW MED	FROM	TO	TEMP. F	PRESS. PSIG	TEMP. F	CLASS	TEMP. F	PRESS. PSIG	MED.	PRESS. PSIG	CLASS	THICK IN.	TEMP. F	DIAGRAM					
D	101	4	A24J	40	L	M-102	DRAINS HUB	200	ATM	-	-	-	-	-	-	N23A	1	200	73-02	OVERFLOW	A ₁			
D	102	2	A24J	80	L	M-102	DRAINS HUB	200	ATM	-	-	-	-	-	-	N23A	1	200	73-02		A ₁			
D	103	1 1/2	A24J	80	L	M-103	DRAINS HUB	200	ATM	-	-	-	-	-	-	N23A	1	200	73-02		B			
D	104	2	A24J	40	L	Q-101	GRADE	100	ATM	-	-	-	-	-	-	N40A	0	-	72-01	OVERFLOW				
D	105	2	A24J	40	L	G-101	GRADE	100	ATM	-	-	-	-	-	-	N40A	0	-	72-01	DRAINS				
D	106	1	A24J	80	L	V-203	GRADE	100	ATM	-	-	-	-	-	-	N10A	0	-	72-03	WATER SEAL DRAIN	C ₀			
D	107	2	A24J	80	L	G-104 DRAIN	GRADE	212	ATM	-	-	-	-	-	-	N23A	1	212	73-01		A ₁			
D	108	3/4	B24A	80	L	P-101A	SPEC BRK	228	290	-	B	228	350	H ₂ O	525	N20A	1	228	73-01	AGITATOR MOTOR (OVER-HEAT) CHECK AGAIN FOR CORRECTION (CURED)	F			
		3/4	A24J	80	L	SPEC BRK	GRADE	212	ATM	-	-	-	-	-	-	N23A	1	212	73-01		F			
D	109	3/4	B24A	80	L	P-101F	SPEC BRK	228	290	-	B	228	350	H ₂ O	525	N20A	1	228	73-01	AGITATOR MOTOR (OVER-HEAT) CHECK AGAIN FOR CORRECTION (CURED)	B			
		3/4	A24J	80	L	SPEC BRK	GRADE	212	ATM	-	-	-	-	-	-	N23A	1	212	73-01		A ₁			
L	110	3/4	B24A	80	L	P-101E	SPEC BRK	388	300	-	-	-	-	-	-	N20A	1	388	73-01	CASING DRAIN				
		3/4	A24J	80	L	SPEC BRK	GRADE	212	ATM	-	-	-	-	-	-	N23A	1	212	73-01		A ₁			
D	111	3/4	A24J	80	L	PT-101B	STM TRAP	228	5	-	-	-	-	-	-	N23A	1	228	73-01		A ₁			
						STM TRAP	GRADE	212	ATM	-	-	-	-	-	-	N23A	1	212	73-01		A ₁			
D	112	3/4	A24J	80	L	LINE WT-109	VALVE	90	55	-	-	-	-	-	-	N40A	0	-	73-01	EMPTY LINE	B			
					L	VALVE	GRADE	90	ATM	-	-	-	-	-	-	N40A	0	-	73-01		B			

6.3 Plot Plan and Arrangement Studies

The following Drawings are provided herein:

<u>Figure Number</u>	<u>Title</u>
6.10	Plot Plan
6.11	Arrangement Study, Elevation - Sheet 1
6.12	Arrangement Study, Elevation - Sheet 2

80-196

Figure 6.10

