LEGIBILITY NOTICE

A major purpose of the Technical Information Center is to provide the broadest dissemination possible of information contained in DOE's Research and Development Reports to business, industry, the academic community, and federal, state and local governments.

Although a small portion of this report is not reproducible, it is being made available to expedite the availability of information on the research discussed herein.

CONF-9010113--1

LA-UR -90-2538

LA-UR--90-2538

DE90 015055

Los Alamos National Laboratory is operated by the University of California for the United States Department of Energy under contract W-7405-ENG-36

TITLE THE PHYSICAL AND CHEMICAL STATE OF WESTINGHOUSE PHOSPHORIC ACID FUEL CELL ASSEMBLIES AFTER LONG TERM OPERATION: SURFACE AND NEAR SURFACE ANALYSIS

AUTHOR(S) M.T. Paffett, W. Hutchinson, J.D. Farr, P. Papin, J.G. Beery, S. Gottesfeld and J. Feret

SUBMITTED TO Electrochemical Society Proceedings Volume entitled "ELECTROCHEMISTRY OF CARBON AND CARBON COMPOSITES" In conjuction with ECS Fall Meeting, Seattle, WA. Oct. 14-19, 1990

DISCLAIMER

Los Alamos National Laboratory
Los Alamos, New Mexico 87545

THE PHYSICAL AND CHEMICAL STATE OF WESTINGHOUSE PHOSPHORIC ACID FUEL CELL ASSEMBLIES AFTER LONG TERM OPERATION: SURFACE AND NEAR - SURFACE ANALYSIS

M. T. Paffett, W. Hutchinson, J. D. Farr, P. Papin,
J. G. Beery[1], S. Gottesfeld[1], and J. Feret[2]

Chemical and Laser Sciences Division
[1]Electronics Research Group
Los Alamos National Laboratory
Los Alamos, NM 87545

[2]Westinghouse Electric Corporation
Box 10564
Pittsburgh, PA 15236

7/1/90

to be submitted to the Electrochemical Society Proceedings Volume entitled Electrochemistry of Carbon and Carbon Composites to be held Oct 14-19 1990, Seattle, WA

Summary

An attempt was made to correlate performance losses with materials compatibility and compositional changes in Phosphoric Acid Fuel Cell (PAFC) electrode assemblies as a function of operation time. Westinghouse PAFC stacks were run under a constant operating regime and portions of some of the single cells were analysed after stack operation for 5000 hrs and for 16000 hrs along with appropriate reference samples. The PAFC assemblies were disassembled, sectioned where appropriate and analyzed using scanning and transmission electron microscopy (SEM and TEM), Rutherford backscattering spectroscopy (RBS), electron microprobe analysis (EMP), and x-ray photoelectron spectroscopy (XPS). The profiles of the Pt catalyst in both the anode and the cathode layer did not show any preferential loss or peaking. The most pronounced change in cell composition detected following stack operation for 5000 and for 16000 hours was the increase in Pt/C ratio, that was related to loss of carbon from the cathode electrocatalyst. In contrast, the anode catalyst layer maintains the same ratio of Pt:C following 16000 hours of operation. The loss of carbon is thought to occur by an electrochemical mechanism and is enhanced at the higher potentials experienced by the air cathode in the fuel cell. In addition, TEM results clearly demonstrate the well recognized phenomenon of Pt particle agglomeration in the cathode catalyst layer, which is seen to be quite substantial after 5000 hours of stack operation. The mechanical integrity of the assemblies was found to be quite satisfactory after 5000 hours, but much less so after 16000 hours. Questions regarding carbon and Pt corrosion, Pt migration, and the mechanical and physical integrity of the PAFC structures are addressed and are all postulated to be contributing to the observed cell performance losses.

Introduction

In the development of phosphoric acid fuel cell (PAFC) systems there have been several scientific and engineering obstacles to overcome if this technology is to be competitive with other more conventional electrical energy sources. One of the key problems that is crucial for this technology to succeed is a stable long term operation of the PAFC. Within the operational goals of the Westinghouse PAFC program a degradation in cell voltage at a constant load of 267 mA per cm^2 of 4 mV/1000 hr is now considered feasible [1]. This performance loss is a significant improvement over previous performance degradation results [2]. However, an even lower degradation rate during long term operation is a desirable goal. Specifically, questions regarding carbon corrosion, Pt corrosion, and Pt migration through the PAFC assembly have all been postulated to be contributing to the observed cell performance loss. The present body of work attempts to assess analytically several materials degradation problems as they occur in the PAFC. In the interest of addressing these issues directly, we have examined the surface and near surface regions of a series of Westinghouse PAFC assemblies that have been run under an essentially continuous power load for various time intervals up to 16000 hours. We have directly addressed the pertinent questions listed above and present the results herein.

The experimental approach to these issues has been as follows: Westinghouse PAFC stacks were run under a constant operating regime. Portions of cell assemblies were sent to LANL for analysis after stack operation for 5000 hrs and for 16000 hrs along with appropriate reference samples. The PAFC assemblies were disassembled, sectioned where

appropriate and analyzed using scanning and transmission electron microscopy (SEM and TEM), Rutherford backscattering spectroscopy (RBS), electron microprobe analysis (EMP), and x-ray photoelectron spectroscopy (XPS). The information obtained and the strengths and weaknesses of each of these techniques is briefly summarized at the beginning of the relevant section. The SEM results will be presented together with the EMP results because both of these analyses were run sequentially in the same instrument.

EMP and SEM Results

Electron microprobe analysis (EMP) allows one to quantify the near surface region of metallographic specimens for elements of $Z > 3$. The instrumentation involves exciting the near-surface volume with 10-25 KeV electrons and analyzing the intensity of the characteristic x-ray emission from the elements present in the sample. The method provides excellent lateral spatial analysis (0.1 micron resolution) of elements detected with routine detection limits on the order of 0.1 % (weight percent). The excitation volume, the x-ray fluorescence cross-section, and a variety of instrumental detection and efficiency parameters all influence the measured intensity of the observed x-ray emission [3]. The PAFC assembly samples, examined by EMP, were mounted edge on end in metallographic epoxy, polished to reveal the distinct layers in the PAFC assembly, and then washed with water and evacuated in a vacuum oven. The latter step was necessary to achieve an adequate background pressure in the EMP (outgassing from the phosphoric acid and residual water , was the primary problem). In the present case a 10 micron^2 15 KeV electron beam was

scanned across the cross section of the fuel cell assemblies and the x-ray emission from the elements present in greater than 1 weight percent was analyzed. Secondary electron micrograph (SEM) photographs were also taken of selected PAFC cross sections. In most cases the distinct layers making up the assemblies are easily identified and are labeled in the figure. Image maps of targeted elements are shown along with the respective SEM photos. The element maps are constructed from the output of either the wavelength or energy dispersive detector(s) and contain some noise associated with these measurements. For the lateral, semi-quantitative line plots the background noise was subtracted to derive the apparent concentration (in weight percent). PAFC electrode assemblies are not the most ideal structures for this type of analysis because of their fairly porous, extremely rough structure. Because of thenonideal nature of the surface the concentrations should be viewed as only semi-quantitative. However, the EMP technique does allow one to assess the extent of Pt migration, nonuniformity of Pt loading, and other materials problems that arise during long term operation.

In Fig. 1 a SEM of a sectioned, reference (unused) anode is shown along with a Pt x-ray map for the same region. The SEM clearly shows the nice delineation between the porous carbon cloth backing and the rolled electrocatalyst layer. Note also that the Pt distribution is quite uniform within the electrocatalyst layer and matches the SEM demarcation exactly. The nonzero intensity of the image obtained in the area of the backing is caused by background (noise) effects. In Fig. 2, a SEM of the reference (unused) cathode is shown denoting the various layers comprising the cathode assembly as received. Note that the mat layer, the SiC matrix, the rolled electrocatalyst layer, and the porous carbon cloth backing are all

clearly delineated and show extremely good edge retention following sample preparation. The layer thicknesses are also consistent with reported values [2]. In Figs. 3 and 4, line scans taken over the electrocatalytic layers and the regions immediately adjacent to them are presented for the same electrodes shown in Figs. 1 and 2, respectively. For the reference anode the weight percent concentration of the elements C, O, F (top half of Fig. 3) Cl, P, and Pt (bottom half of Fig. 3) is shown as a function of position across the porous backing and the electrocatalytic layer. Note that the Pt concentration varies somewhat across the electrocatalyst layer but in general runs around 3-4 weight percent. This value is markedly lower than the stated nominal value of 10% weight loading for the the electrocatalytic layer and serves to point out the difficulties of quantification on very porous, rough samples. Due to this limitation the reported numbers should be directly compared with the reference samples for soem understanding of how the Pt and C concentrationa are varying in a relative sense. The C concentration runs at 75 $\pm$ 5 weight percent for both the anode and cathode and will prove to be a key number for comparison to the used electrode assemblies. Also of note, is the higher concentration of F in the porous backing. The statistical variation in elemental concentration is quite pronounced in the porous backing and is largely due to the very rough, spongy nature of the substrate. Some Cl is observed in the electrocatalyst layer. The origin of this Cl is not entirely clear, although some residual contamination from the potting compound (epoxy) is suspect. Figure 4 displays the elemental line scans from the reference cathode performed across the layers shown in Fig. 2. The Pt weight concentration is approximately 2-3 percent and, again, the F concentration is slightly

higher in the porous backing. In general, the two reference electrode assemblies appear to be very close in elemental concentrations.

Samples labeled 2-4 and 6-4 were received after being operated approximately 5000 hours in a Westinghouse PAFC stack. For brevity, only the 2-4 data set is presented in this report. Analysis of the 6-4 electrode assembly produced analogous results. In Fig. 5, a SEM of a cross sectioned 2-4 cell assembly is shown with the assembly layers appropriately labeled. Note that the edge relief is still fairly good although some retraction of the middle sections (anode, mat, SiC, and cathode) is occurring. Figure 6 contains a SEM enlargement of the cathode-SiC-mat assembly, along with a Pt x-ray map. The x-ray map clearly indicates that the Pt distribution is still uniform in the cathode electrocatalyst layer with no noticeable loss of Pt at the front edge of the layer. Questions regarding Pt agglomeration are addressed in the TEM results section below. Figure 7 contains the elemental (C, O, P, F, Pt) line scans for the PAFC 2-4 electrode assembly sample shown in Fig. 5. For both the anode and cathode layers the Pt weight concentration is running 2-5 percent with the concentration slightly higher in the cathode layer. The sharp drop in C, O, and F at the interface regions is largely due to the void noted in the SEM photo. This void is apparently caused by partial delamination of adjoining layers in the assembly. In general, the elemental distributions appear uniform except in those regions where the electron beam is sampling void regions. Across the anode and cathode regions of the 2-4 assemblies the C weight concentration varies from 45-65 percent, a value considerably below that for either reference electrocatalyst layer. The Pt/C ratio averages 0.06 $\pm$ 0.05, and 0.11 $\pm$ 0.05 in the 2-4 anode and cathode regions, respectively. These

numbers compare with values of 0.04 and 0.035 for the reference anode and cathode regions, respectively.

A series of PAFC assemblies run for 16000 hours labeled 8-3, 8-5, 8-7, and 9-8 were analyzed in the same manner as those described above. Again, for brevity only one set of results for the 16000 hour set will be described. In general, the results were consistent among the sets and details regarding those assemblies not described are available upon request. Starting with the SEM photo of the 8-3 PAFC electrode assembly (Fig. 8) one notes that the overall middle section has thinned considerably and in some of the assemblies (not shown) has lost a lot of the mechanical integrity. The mechanical integrity assists in maintaining good edge retention in the metallographic preparation of the cross sectional mounts. For most of the 16,000 PAFC electrode assemblies the SiC layer has diminished to such a degree as to be nondistinct. This is brought out in the middle third of Fig. 8 where a Si X-ray map is shown of the same region that the SEM photo is recorded from. Some regions of localized Si are seen, but in general the layer has lost most of its integrity. In the bottom third of Fig. 8 the Pt x-ray fluorescence map is shown over the same SEM region. As seen in the prior electrode assemblies the Pt distribution appears uniform with no noticeable Pt loss at the cathode and no replating of the Pt occurring at the anode. A higher concentration of Pt appears in both the cathode and the anode, and is also evident in the elemental line scans that follow in Fig. 9. Continuing the trend seen with the 5000 hour electrode assemblies, the weight % of C has further decreased to 40-45 percent (Fig. 9). The most plausible interpretation of this decrease in C weight concentration (or increase in Pt to C ratio) is a severe long term carbon corrosion and loss. Notice also that after 16000 hours of cell operation, the

concentration of Pt in the mat is comparable to that in the catalyst layers, (Fig. 9).

XPS Results

PAFC assemblies were peeled apart, rinsed with ultra pure water and examined using XPS. Special care was required to delaminate the 16000 hour assemblies. For these electrode structures the surface of the cathode was scraped lightly to create an artificial break at the electrocatalyst-porous backing interface. The electrocatalyst layer was then peeled up and XPS spectra were recorded of the back side of the electrocatalyst layer. For all of the anode structures and for the reference and 5000 hour cathodes the front sides (side facing the anode) surface of the electrode was simply scraped to remove the tenacious SiC matrix. For these samples, however, some Si was always seen in the broadscan survey spectra that were run prior to recording the narrow regions for the analytical lines of interest. XPS is considerably more surface sensitive than EMP (analysis layer depth of ~50 A vs 1-5 microns), and therefore, one should be aware of the different information content in each technique. Whereas EMP can provide quantitative elemental information for well behaved samples, XPS can be used to analyze the chemical valency of specific elements present in the surface layer (e.g., C present as C, -CO, -COOH, or $-CF_x$). For the present samples, the C 1s energy region was specifically examined to shed light on the nature of loss of carbon in the electrocatalytic layers. The most informative XPS data are shown in Figs. 10 and 11. In Fig. 10, the C 1s lineshape for the reference anode and cathode is shown stack plotted with the corresponding data from 2-4 and 6-4

(5000 hour) electrode structure. In the reference data note that there are two very distinct C 1s peaks appearing at 284.0 eV and approximately 291 eV binding energy. These two peaks are assigned to the graphite from the electrocatalyst support and the Teflon blended into the structure, respectively. The peak arising from the Teflon component was noticed to shift dramatically, consistent with the Teflon particles charging during the XPS experiment. In most cases an electron flood gun was utilized to shift this feature to reported values [4]. The use of charge neutralization had a minimal effect on the C 1s feature arising from the graphite. The effect of charging on the C_{tef} can be seen in the spectrum recorded from 2-4 cathode, where charge neutralization was not used. Other spectral features arising from -COH and -COOH functionalities can be fit to the region between the two prominent peaks. The ratio of the integrated intensity of the C_{tef} to C_{gr} peaks is 0.6 ± 0.1 for both the reference anode and cathode surfaces Note that for both sets of data the used cathode electrode surfaces display a severe loss of intensity in the C_{gr} feature. For the 2-4 and 6-4 anode surfaces the C 1s spectral lineshape remains essentially the same as the reference data. In Fig. 11 a similar set is shown stack plotted for two of the 16000 hour electrode sets. The other two 16000 hour assemblies produced similar results and are not shown for brevity. Essentially the same result is seen in the C 1s spectra as seen in the 5000 hour electrodes, namely an extreme loss of the C_{gr} feature in the cathode electrocatalyst structures. These XPS results immediately confirm the hypothesis that graphite corrosion is a particularly severe problem in the cathode structures and manifests itself even at 5000 hours of operation.

TEM Results

We used transmission electron microscopy (TEM) to observe the platinum particle size distribution in the cathodes. The TEM samples were prepared by scraping the cathodes with a scalpel over TEM grids and dropping petroleum ether on the grids. This spreads the cathode material and causes it to adhere to the grid. Figure 12 is a composite of reference cathode C381-2 and cathode 6-4. Generally, the platinum particles are much larger in the 5000-hour and 16000-hour cathodes, than in the unused cathode. We did not do an extensive Pt particle size analysis in the TEM examination, although it is immediately apparent from inspection of Fig. 12 that the particle sizes have increased to approximately 200 A after operation for 5000 hours.

RBS Results

Rutherford backscattering (RBS) was used to obtain depth profiles of the catalyst distributions. All these analyses were done with the ion beam normal to the sample surface. We used 2 MeV alpha particles to obtain an accurate Pt/C ratio to a depth of 2×10^{19} atoms cm^{-2}, and 3 MeV protons to obtain profiles down to a depth of 10^{20} atoms cm^{-2}. The depth profiles are given on a scale of atoms cm^{-2} rather than on a distance scale, since the electrodes are rather porous, rough and the physical density of the material is not well defined. Despite this limitation, the Pt/C ratio is obtained by measuring the heights of the Pt and carbon edges and calculating the Pt/C ratio by using the known scattering cross sections for Pt and C. These cross sections are proportional to Z^2 so the Pt edge is extremely enhanced relative to the carbon edge. Figure 13 is an example of the RBS data for cathode 7-8-

C (16000 hours). The solid line is a computer simulation with a Pt/C atomic ratio of 0.0297 (2.97%). The small edges around channel 260, 320, and 445 are for oxygen, flourine, and phosphorus, respectively. The key numbers are the heights of the platinum and carbon edges. Figures 14 and 15 display the same type of RBS data for a 5000 hour cathode (cell 6-4) and the reference cathode (C381-2). The edge at channel 425 in Fig. 15 is from silicon. The Pt/C ratio for Fig. 14 is 1.45% and is 0.64% for Fig. 16. RBS with 2 MeV alpha particles provides Pt/C atomic ratios with good accuracy, but only probes to a depth of 2×10^{19} atoms cm^{-2}. For deeper profiles (10^{20} atoms cm^{-2}), we used 3 MeV protons. The scattering at this energy for protons is not purely elastic (Rutherford) so the Pt/C ratio is inaccurate. Figure 15 is an example of a proton RBS spectrum for cathode 3-8-C. It shows that the Pt distribution is relatively constant to a depth of 10^{20} atoms cm^{-2}. No information can be gained on the atomic ratios since for the lighter elements (C, O, F) the scattering is non-Rutherford; that is, it has a significant contribution from nuclear effects. Figure 17 and Table 1 contain the Pt/C atomic concentration ratio for the cathodes measured. There is a significant increase in the Pt/C ratio with operating time which we interpret as a carbon loss.

Discussion

An extensive literature base on carbon corrosion exists in the electrochemical fuel cell literature [5]. In general, the relative kinetic inertness of a variety of carbon types has been experimentally verified [5] and in general accounts for the widespread use of a variety of carbon types as electrocatalyst supports. Work by Kinoshita [6] on the corrosion of

carbon under PAFC operation conditions has previously demonstrated that for short term operation the effect of the Pt electrocatalyst did not have an effect on the net carbon corrosion rate. In a study of carbon corrosion in alkaline solutions, Ross and Sokol [7] however, have previously demonstrated that a supported Co oxide electrocatalyst produced a notable increase in the overall carbon corrosion process when compared to the bare carbon corrosion rate. In light of these previous results the long term corrosion of the carbon electrocatalyst support under long term PAFC operation conditions appears to be a subject that has been widely noted but not extensively reported in the electrochemical community.

The change in Pt distribution for long term PAFC operation has been studied by Aragone et al [8] using EMP and TEM methods and by Hyde [9] et al using particle induced x-ray emmission and RBS methods. In both cases the corrosion of Pt was noted to be quite severe at the cathode front surface, followed by migration of the Pt through the cell and redeposition at the PAFC anode front surface. Previous work from this laboratory using Pt cathode and Pd anode PAFC single cells coupled with RBS analysis has also demonstrated this corrosion and migration of Pt through the cell assembly [10]. These observations of Pt migration and corrosion point to the very careful control that PAFC assemblies require during their operational history. Any open circuit condition at high temperature, however short in duration, can potentially produce the serious observed Pt cathode corrosion and migration problems.

In view of these previous studies, and from the results obtained in the characterization of the PAFC assemblies of this work, we can summarize as follows.

(1) The profiles of the Pt catalyst in both the anode and the cathode layer did not show any preferential loss or peaking. This shows that because of the quality of the fabricated catalyst and the mode of operation of the stack during the long term testing, loss of Pt from the cathode catalyst, and Pt redeposition on the front surface of the anode was not detected, even after about 16000 hours of testing. This aspect is stressed because the pattern of Pt migration from cathode to the front surface of the anode in operating PAFCs has been identified in the past in several similar analytical efforts [8-10], and it was gratifying to find out that it did not take place in the Westinghouse cells examined. This is a testament to the operational control and procedures implemented in the operation of the Westinghouse PAFC stack.

(2) The most pronounced change in cell composition detected following testing for 5000 and 16000 hours was the increase in Pt/C ratio. This was clearly detected with both the EMP and the RBS techniques. Since the latter is the more quantitative tool (though associated with a smaller penetration depth), further discussion is based upon RBS results presented in Fig. 17. These results show an increase in Pt/C ratio in the cathode by about a factor of three after 5000 hours and by a factor of 5-6 after 16000 hours. Assuming that the loss of Pt is relatively small, as concluded from the lack of any indication of Pt migration to the anode and only a low level of Pt found in the mat layer (see below), the only way to interpret this increase in Pt/C ratio is by the loss of carbon. This loss is, however, very substantial. If the initial concentration of Pt in the cathode catalyst is 10%, an increase in the ratio Pt/C by a factor of 6 means a loss of about 80% of the carbon (!) from the cathode catalyst layer after 16000 hours. This behavior is clearly unique for the cathode catalyst, whereas the anode catalyst layer maintains the same

ratio of Pt:C following the 16000 hours of operation (Fig. 17). This clearly demonstrates that the loss of carbon occurs by an electrochemical mechanism and is enhanced at the higher potentials experienced by the air cathode in the fuel cell. A direct correlation between the severe loss of carbon from the cathode catalyst and the continuous loss of cell voltage in this stack (ca. 8mV/1000 hours) could not be established by the analytical results presented here alone. However, it would be surprising if a loss of 80% of the mass of the carbon in the cathode catalyst layer could take place without any consequence. Indeed, it is quite amazing that after having lost 80% of the carbon in the carbon in the cathode catalyst layer, the cell is functioning with a loss of only 130 mV in voltage. The explanation for this surprising preservation of cell performance may be that the mechanical pressure continously applied across the cells allows the maintainence of a reasonable electronic connectivity within the shrinking catalysts layer, even following such a severe carbon loss. These results suggest an obvious R&D effort on searching for carbon materials with lower electrochemical corrosion rates.

(3) The XPS results presented in this report help to clarify the nature of the increase in Pt/C ratio in the cathode catalyst layer. These results have the advantage of distinguishing clearly between carbon associated with the catalyst support (XC-72) and the carbon in the Teflon additive. The XPS results could thus prove in an unequivocal way that the carbon lost is from the support material - not from the Teflon.

(4) A small level of Pt, estimated at 15% of the overall initial loading, is found in the mat layer after 5000 hours (and somewhat more after 16000 hours), according to both the EMP and the RBS results.

(5) The TEM results presented in Fig. 12 clearly demonstrate the well recognized phenomenon of Pt particle agglomeration in the cathode catalyst layer, which is seen to be quite substantial after 5000 hours of stack operation. This is obviously a process that could contribute to performance loss.

6) The mechanical integrity of the assemblies was found to be quite satisfactory after 5000 hours, but much less so after 16000 hours. In particular, the SiC has been very difficult to detect in the samples run for 16000 hours.

Acknowledgements

The work at Los Alamos was supported by the Morgantown Energy Technology Center and is gratefully acknowledged.

References

1. J.M. Feret, M.K. Wright, L.L. France, J.L. Kelley, A.J. Pereira and A.Kush, Proceedings of the the First Annual Fuel Cells Contractors Meeting, DOE/METC-89/6105, 1989, pg. 287.

2. A.J. Appleby, in: Energy (Special Issue) 11, Ed. S.S. Penner, Pergamon Press, 1986.

3. L. Feldman and J.W. Mayer, "Fundamentals of Surface and Thin Film Analysis", North-Holland, New York, 1986, Chapter 10.

4. C.D. Wagner, W.M. Riggs, L.E. Davis, J.F. Moulder, and G.E. Muilenberg, "Handbook of X-ray Photoelectron Spectroscopy", Perkin-Elmer Corp.-Physical Electronics Division, Eden Prairie, MN, 1979.

5. for example see A.J. Appleby in Electrochemical Society Proceedings Volume 84-5, The Electrochemistry of Carbon, The Electrochemical Society, 1984, Pennington, NJ, pg.251 and references contained therein.

6. K. Kinoshita, Electrochemical Society Proceedings Volume 84-5, The Electrochemistry of Carbon, The Electrochemical Society, 1984, Pennington, NJ, pg.273.

7. P.N. Ross and H. Sokol, J. Electrochem. Soc., 131 (2984) 1742.

8. J.Aragane, T. Murahashi, and T. Odaka, J. Electrochem. Soc., 135 (1988) 844.

9. P.J. Hyde, C.J, Maggiore, and S. Srinivasan, J. Electroanal.Chem., 168 (19884) 383.

10. L. Borodovsky, J.G. Beery, and M.T. Paffett, Nuclear Instruments and Methods in Physics Research B24/25 (1987) 568.

Figure Captions

Fig.1 Top: Secondary electron micrograph (SEM) of a cross sectioned reference anode taken at 400X magnification. Dashed bar indicates path of the electron beam in line scan data presented in fig. 3.
Bottom: Pt x-ray fluorescence image recorded over the same region as shown in top.

Fig.2 SEM of a cross-sectioned reference cathode assembly at 100X magnification. Parts of the electrode assembly are labeled.

Fig.3 Concentrations in weight percent recorded over the line scan shown fig. 1 (reference anode).

Fig.4 Concentrations in weight percent recorded over a line scan of assembly shown in fig. 2 (cathode reference).

Fig.5 SEM of fuel cell electrode assembly 2-4 operated for 5000 hours. Portions of the assembly are denoted at the top of the fig.

Fig.6 Top: expanded view of the mat, SiC, and cathode layers in elctrode assembly 2-4.
Bottom: Pt x-ray fluorescence image of the same region as the top.

Fig.7 Weight concentrations determined from the x-ray fluorescence along the line scan denoted in fig. 5. Portions of the electrode assembly are denoted on the fig.

Fig.8 Top: SEM of PAFC electrode asembly 3-8C operated for 16000 hours. Portions of the assembly are denoted.
Middle: Si x-ray fluorescence map over the same region as shown in top.
Bottom: Pt x-ray fluorescence image of the same region as the top.

Fig.9 Weight concentrations determined from the x-ray fluorescence along the line scan denoted in fig. 8. Portions of the electrode assembly are denoted on the fig.

Fig.10 X-ray photoelectron spectra (XPS) recorded over the C 1s region from the respective electrocatalyst layers (reference and 5000 hour operated electrodes). The excitation source was an unmonochromatic Mg anode (1253.6 eV) and spectra were recorded at 50 eV pass energy. The C 1s contributions due to the graphite (284.6 eV) and teflon (291 eV) are denoted on the figure. The high binding energy of cathode assembly 2-4 is shown to illustate the inherent charging of the teflon particles (charge compensation was used in all of the other spectra).

Fig.11 XPS data recorded over the C 1s regions of PAFC electocatalyst layers operated for 16000 hours. Other variables as in fig. 10.

Fig.12 Transmission electron micrographs of the reference cathode and 5000 hour operated cathode electrocatalyst.

Fig.13 Rutherford backscattered spectrum (RBS) recorded from a 16000 hour operated cathode electrocatalyst layer. The incident ion was 2.0 Mev alpha particles. Composition of the assemblies was accomplished using the RUMP code as described in text and the fit is shown on the fig.

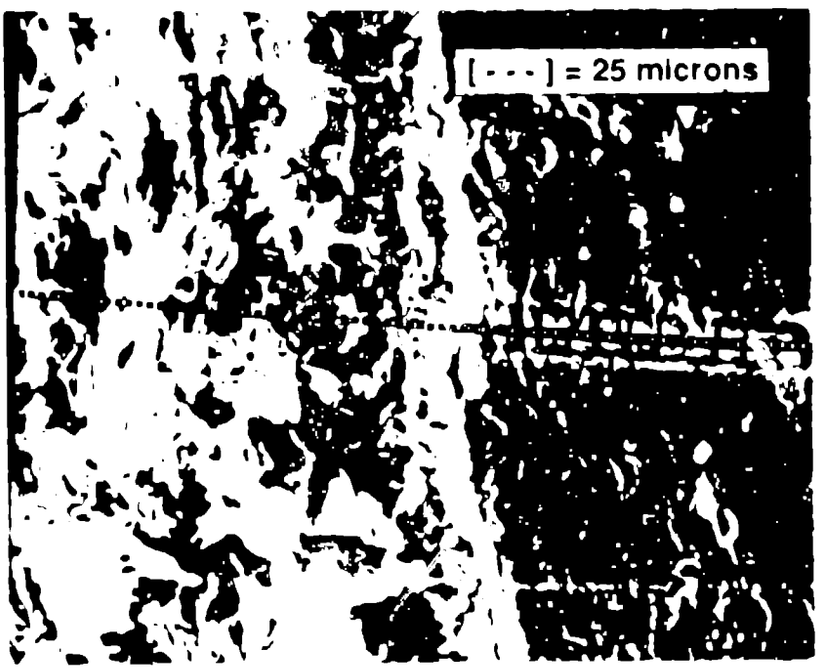
Fig.14 Same as Fig. 13 except for a 5000 hour operated cathode electrocatalyst layer.

Fig.15 Same as fig. 13 except recorded from a reference cathode electrocatalyst layer.

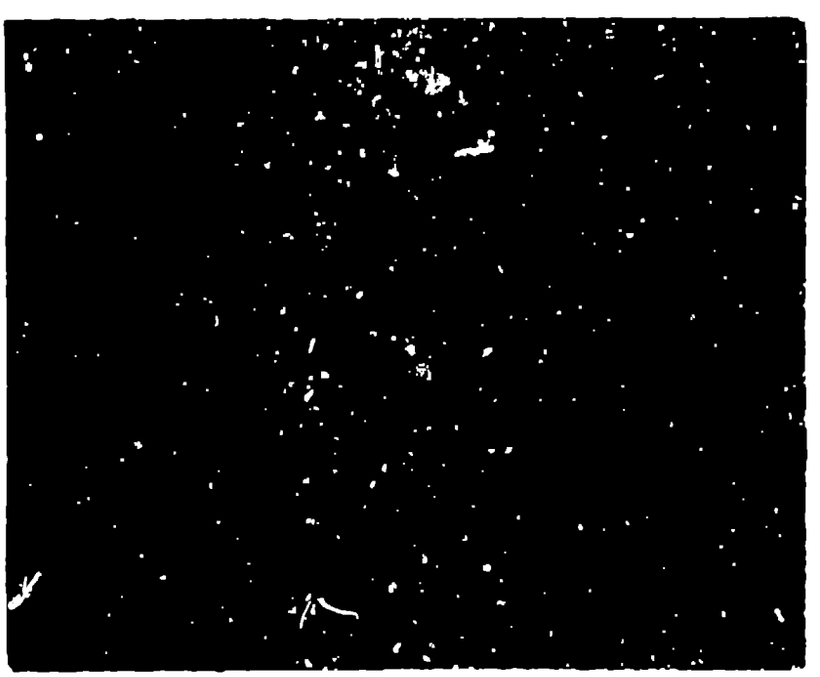
Fig.16 RBS spectrum recorded from a 5000 hour cathode electrocatalyst layer using 3.5 MeV alpha particles. The elemental edges are denoted on the fig.

Fig.17 The Pt/C ratio determined from the RBS data analysis for various anode and cathode electrocatalyst layers.

REFERENCE ANODE



A

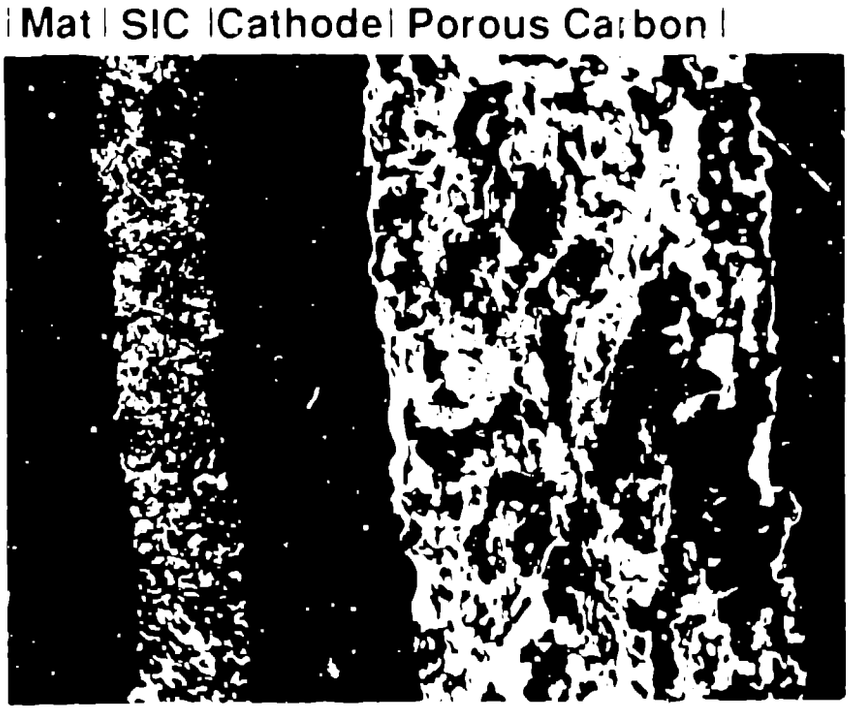


B

Los Alamos

CLS-90-9925

REFERENCE CATHODE



Los Alamos

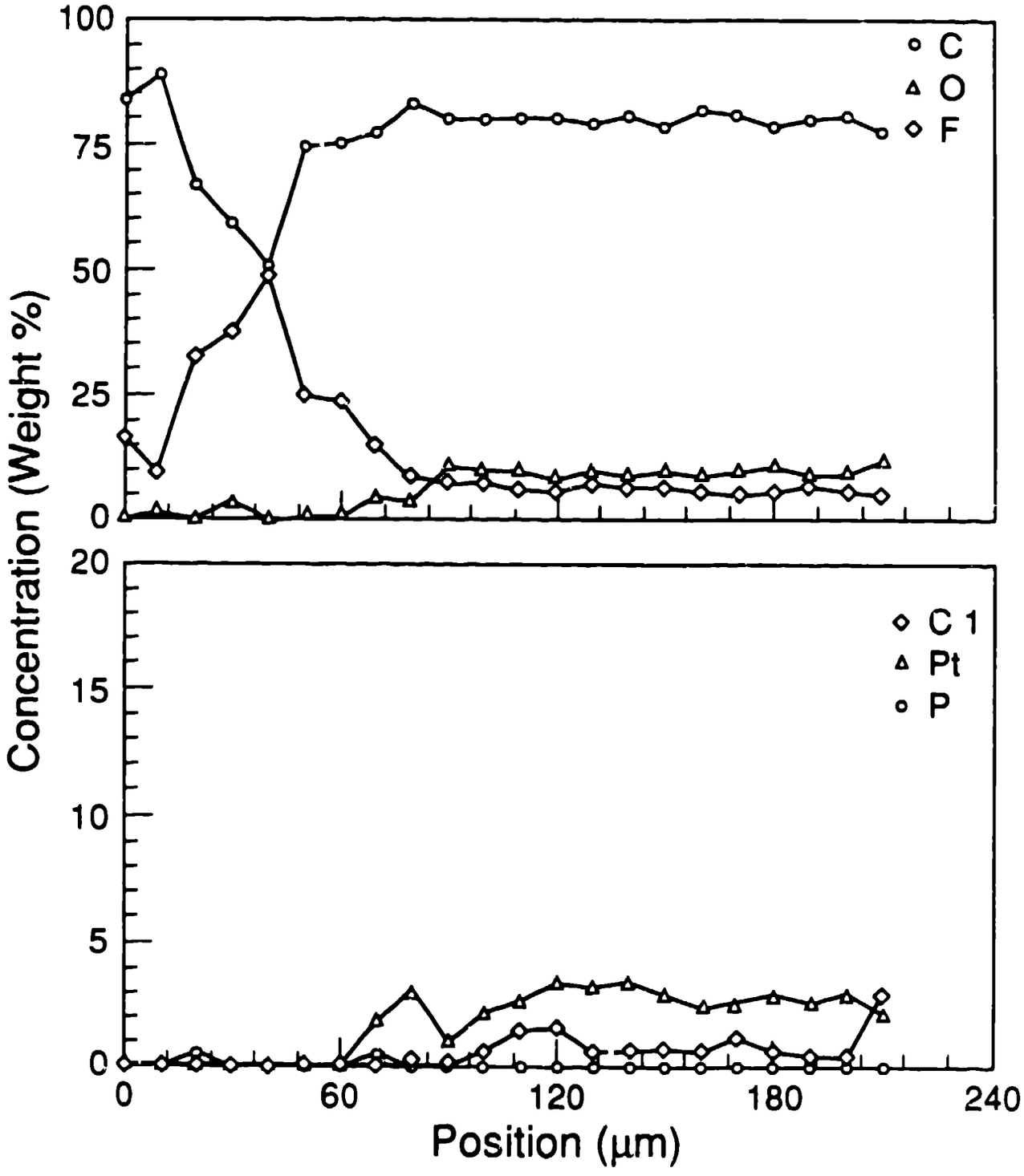
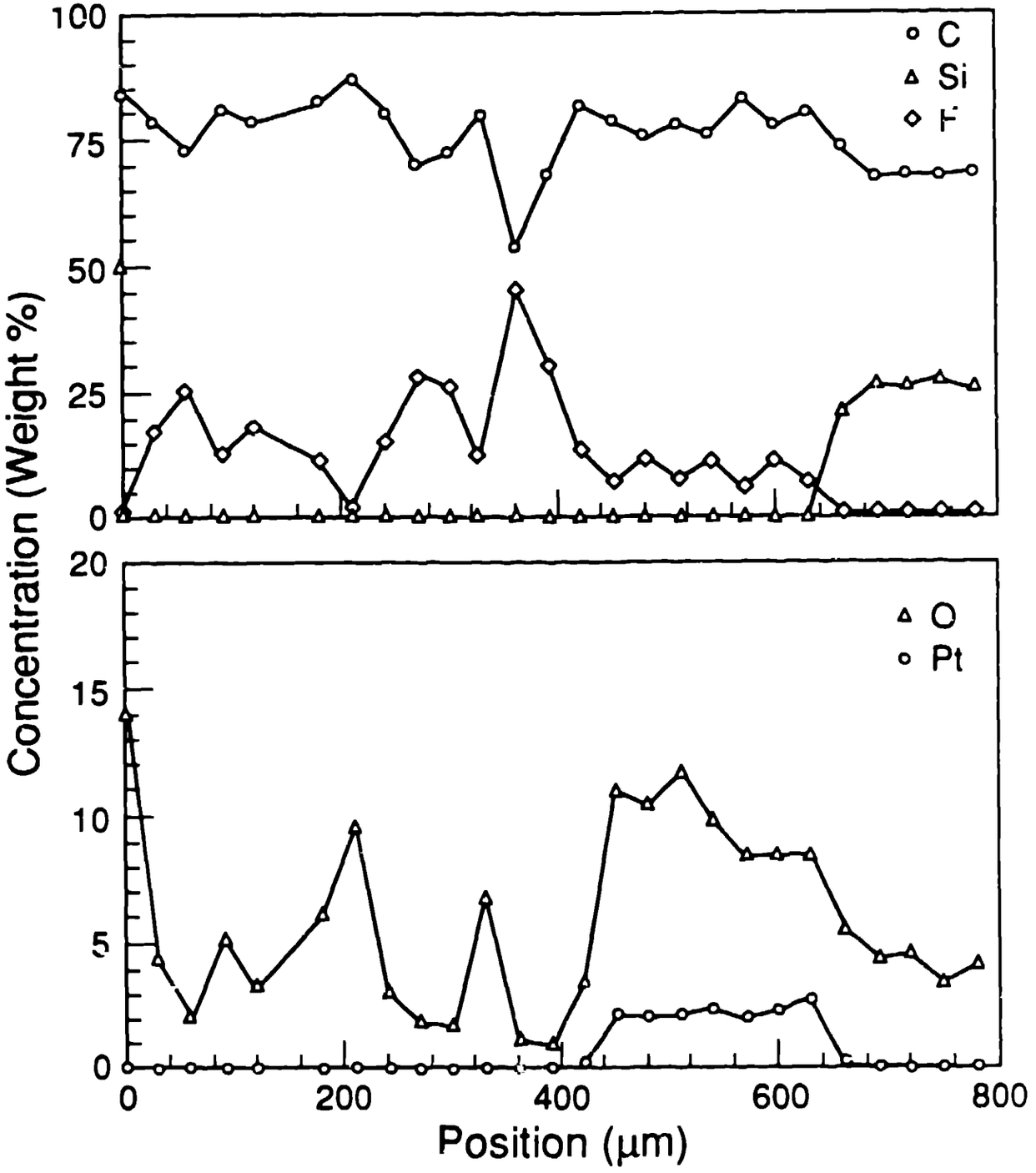


Fig. 3

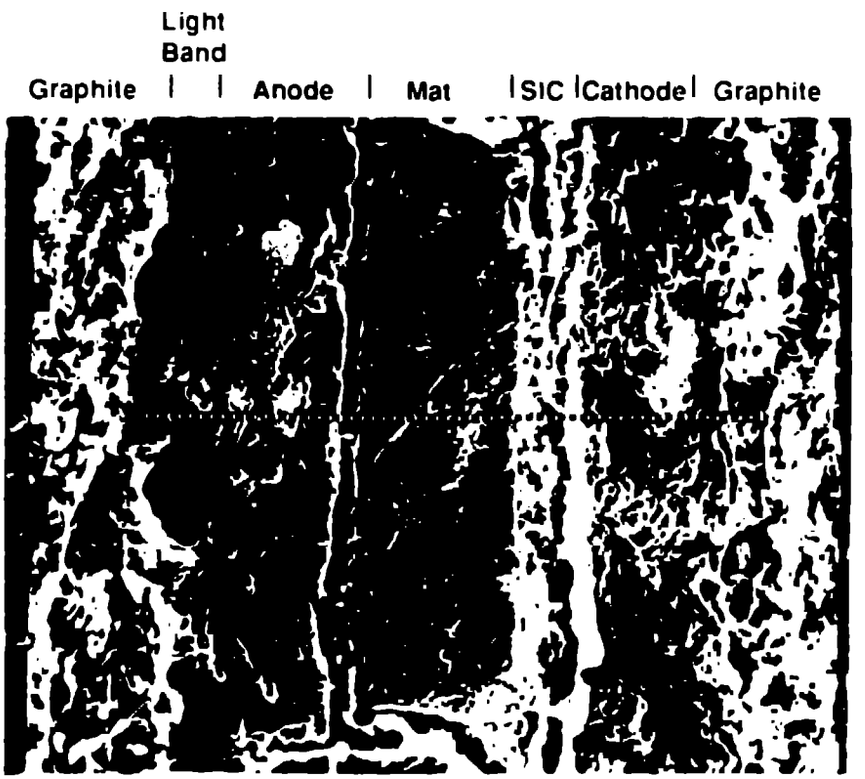
Los Alamos

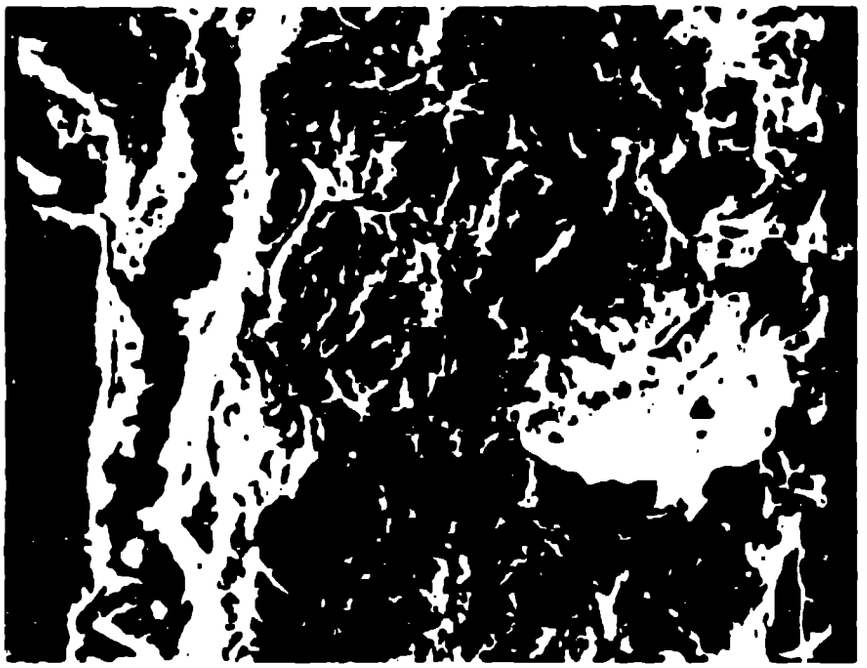
CLS-90-9889



Los Alamos

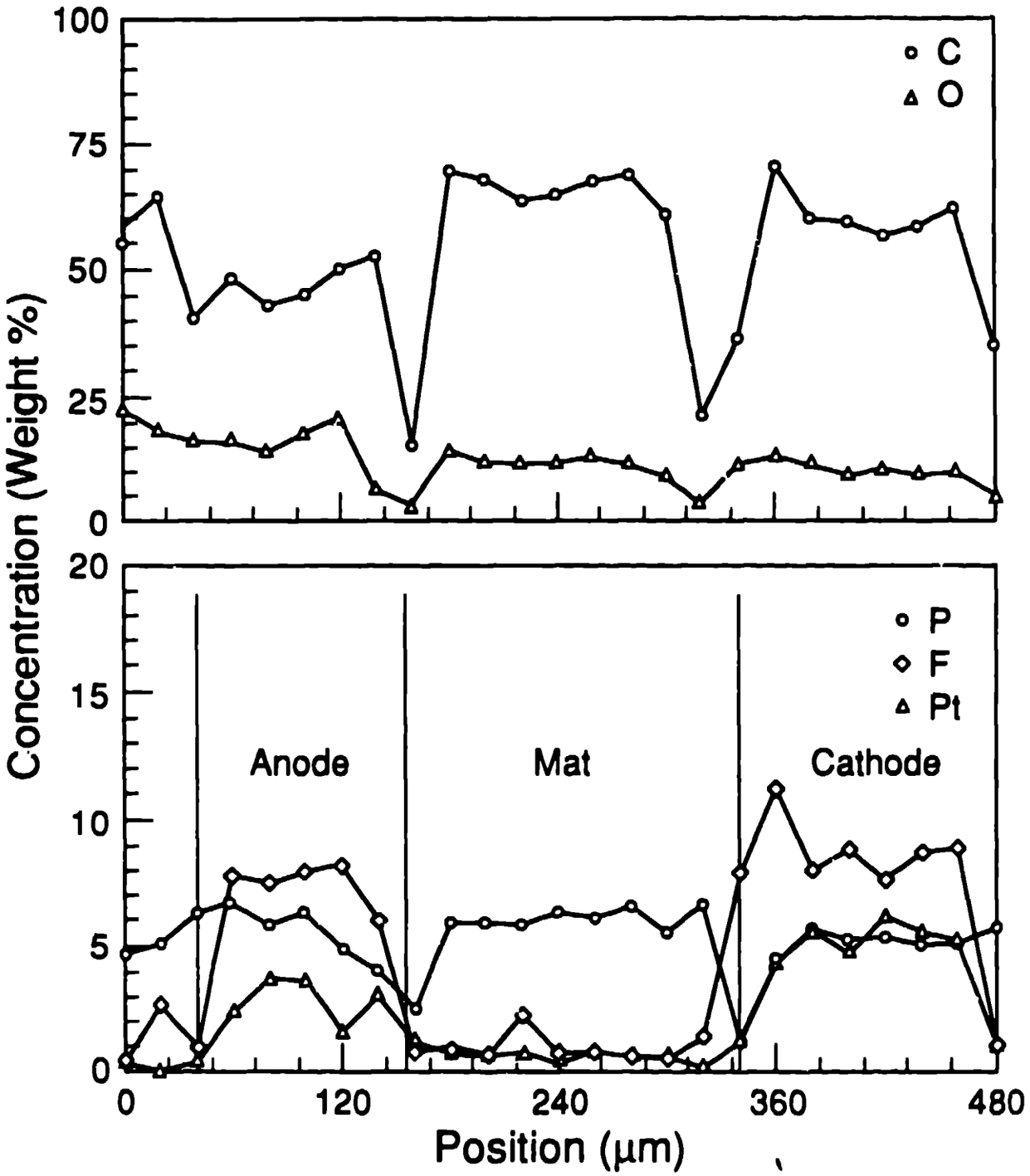
CLS-90-9890


Light
Band
Graphite
Anode
Mat
SIC
Cathode
Graphite



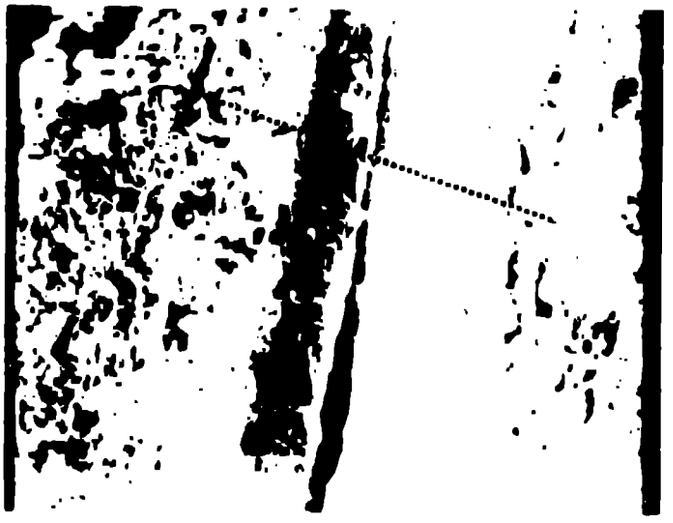
Matl SIC | Cathode

Fig. 6



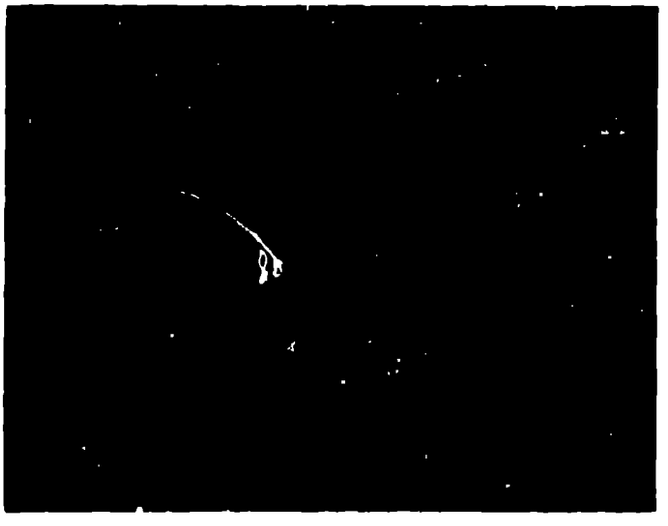
Los Alamos

CLS-90-9888



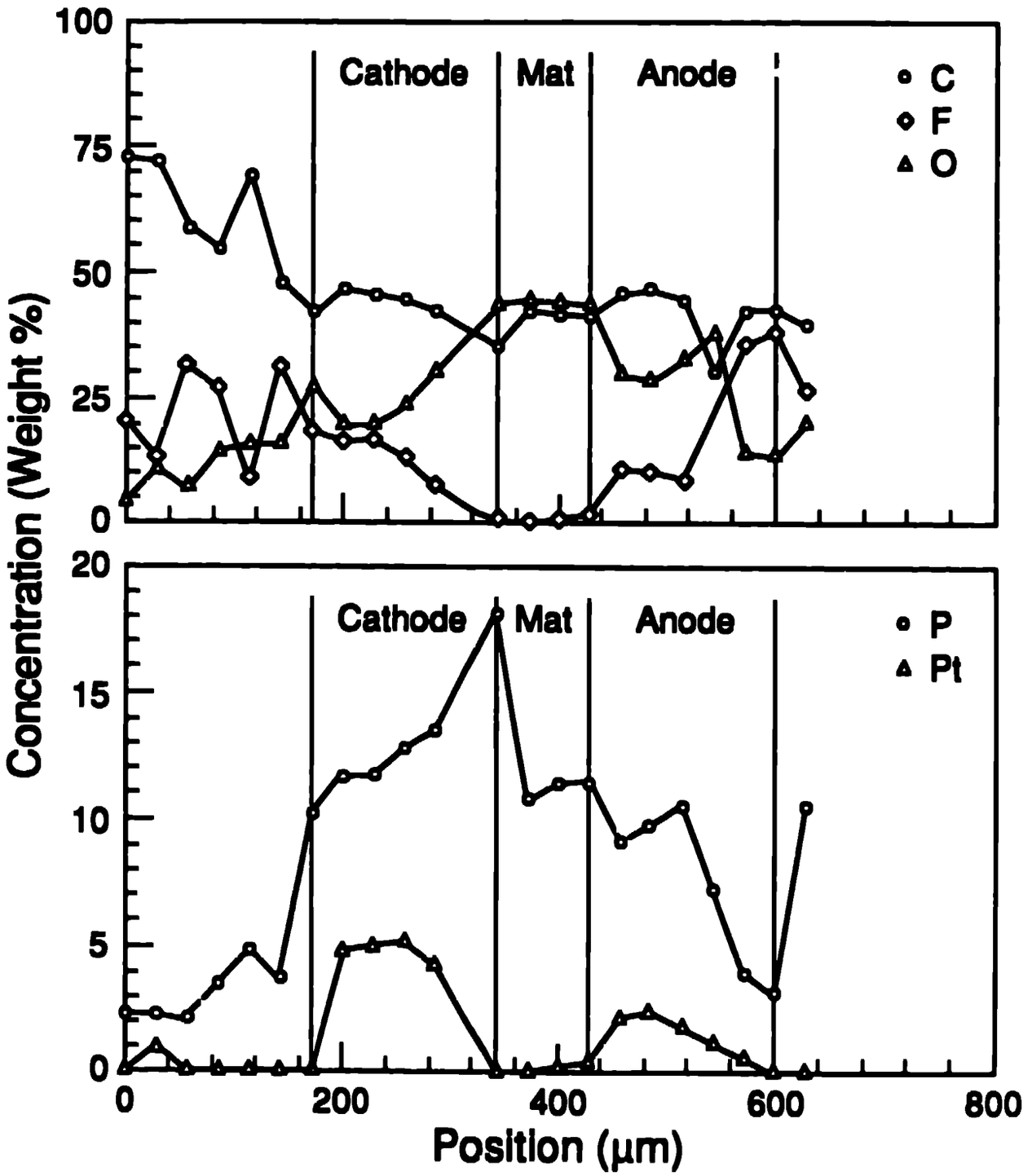
A

B



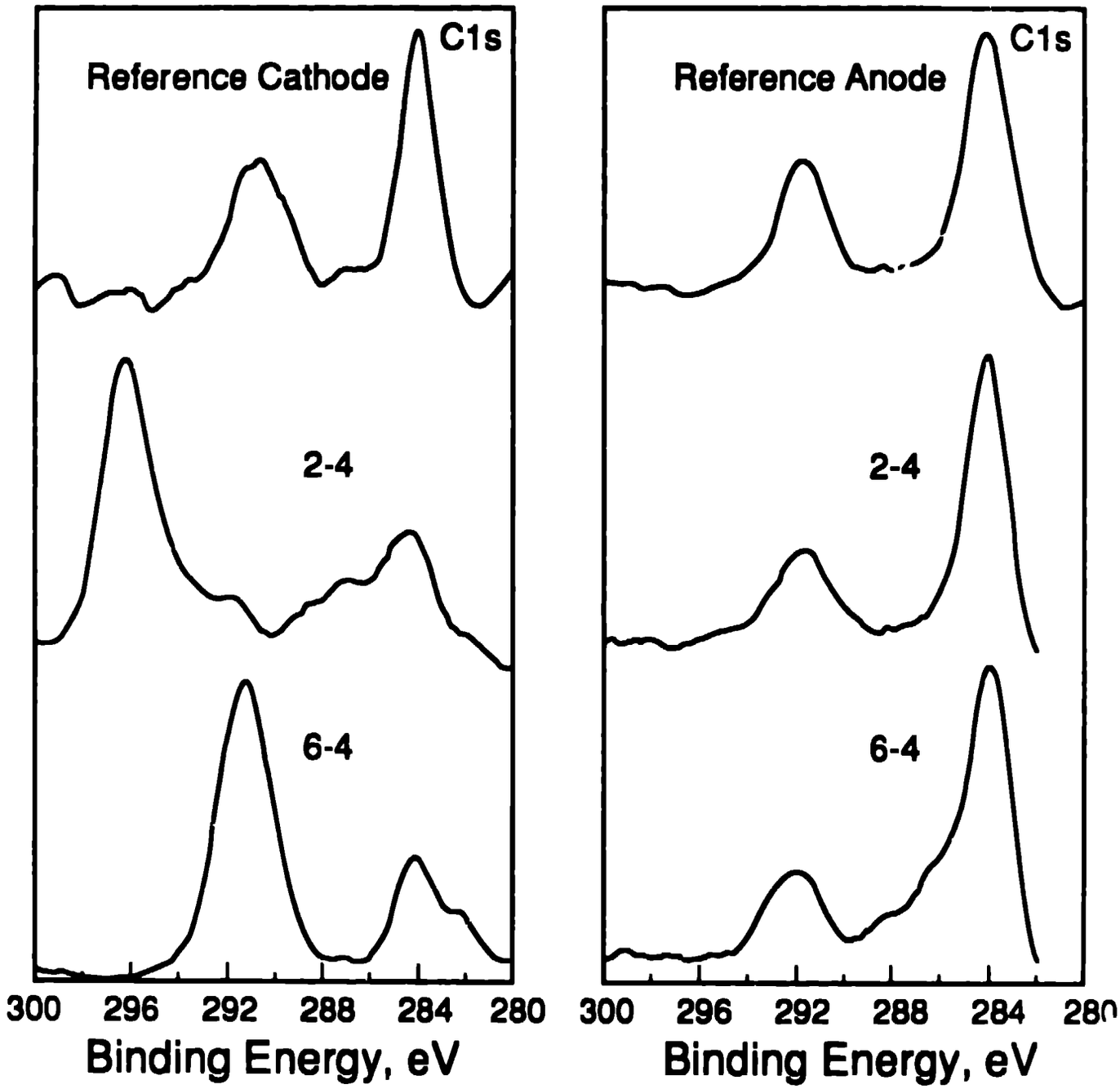
C

Fig. 6



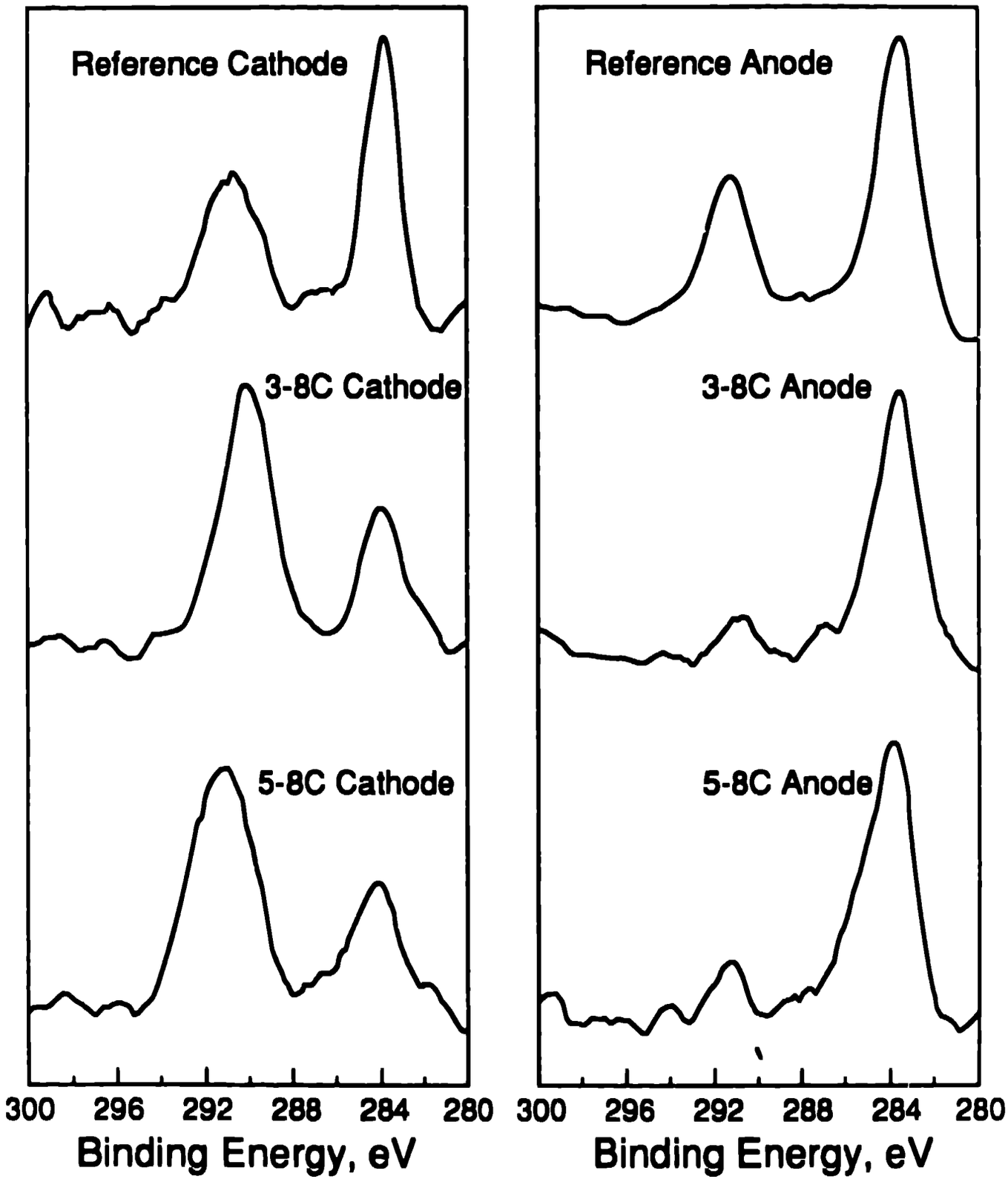
Los Alamos

CLS-90-9886



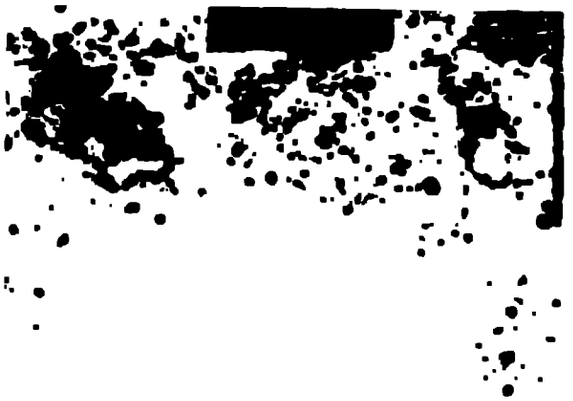
Los Alamos

CLS-90-9885



Los Alamos

CLS-90-9887



1000 Å

REFERENCE CATHODE
C381-2

1000 Å

5000 HOUR
CATHODE 6-4

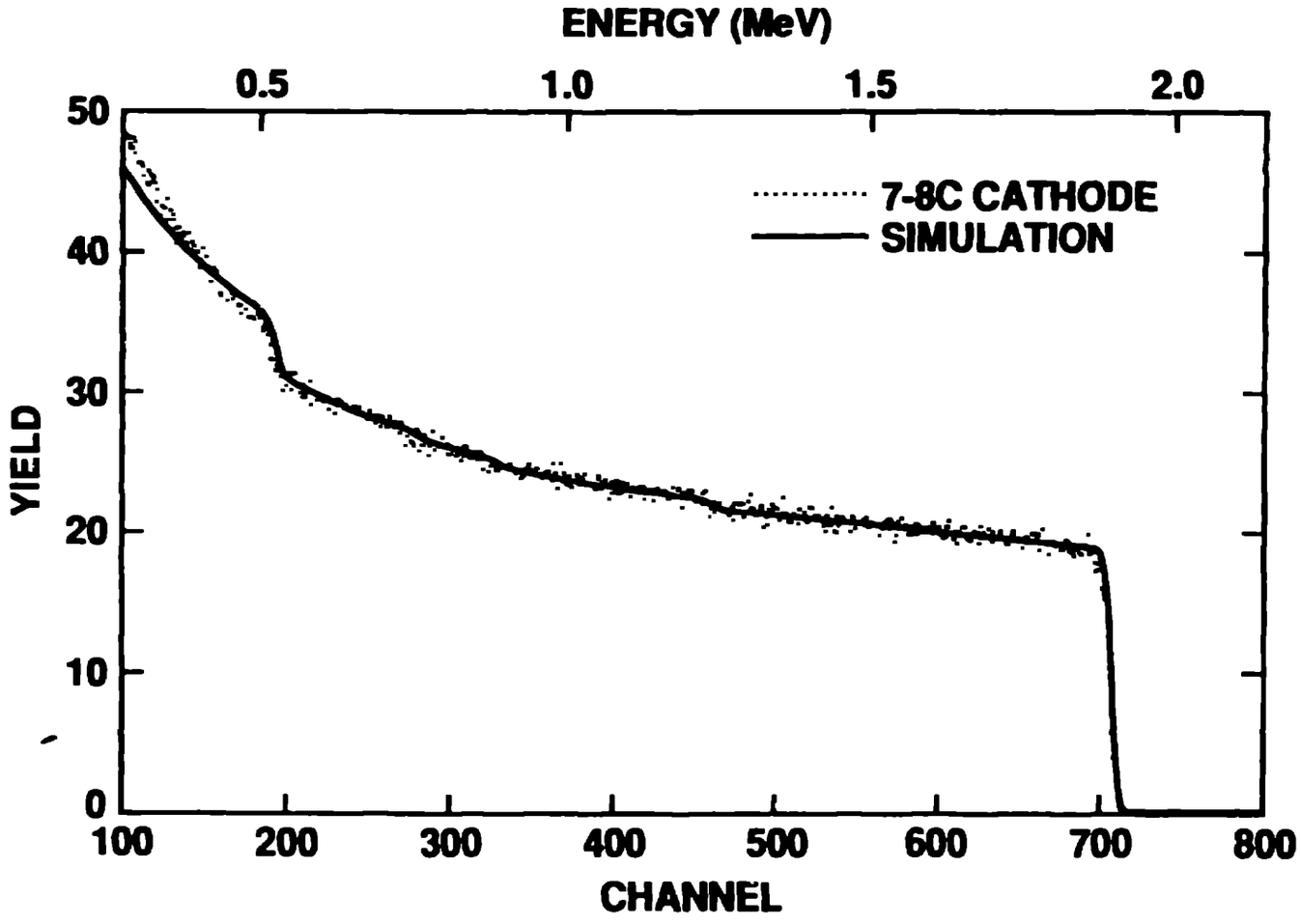
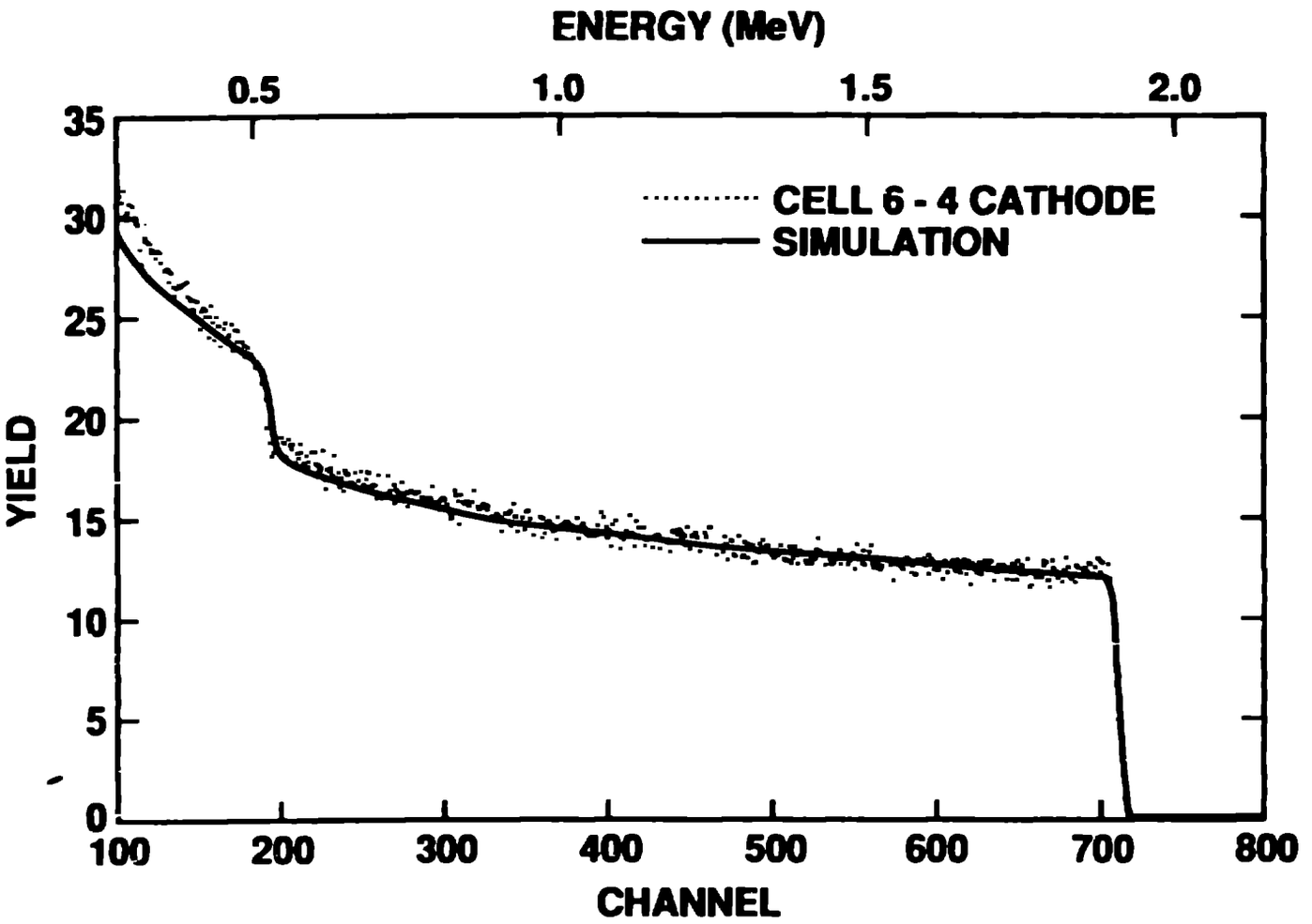
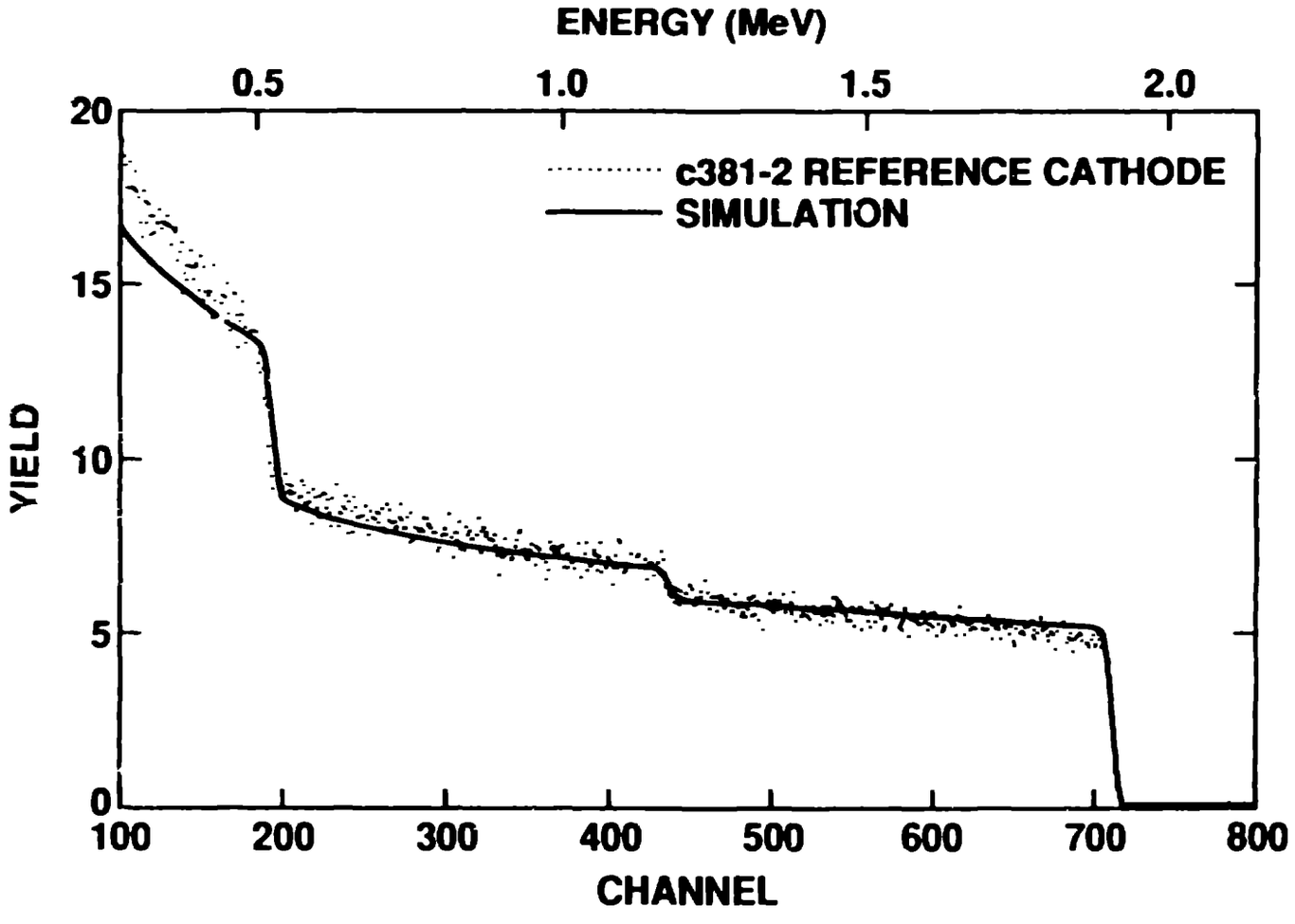

ENERGY (MeV)
0.5
1.0
1.5
2.0
50
40
30
20
10
0
YIELD
7-8C CATHODE
SIMULATION
100
200
300
400
500
600
700
800
CHANNEL

Fig. 13


ENERGY (MeV)
0.5
1.0
1.5
2.0
35
30
25
20
15
10
5
0
YIELD
CELL 6 - 4 CATHODE
SIMULATION
100
200
300
400
500
600
700
800
CHANNEL

F. 14


ENERGY (MeV)
0.5
1.0
1.5
2.0
c381-2 REFERENCE CATHODE
SIMULATION
YIELD
20
15
10
5
0
100
200
300
400
500
600
700
800
CHANNEL

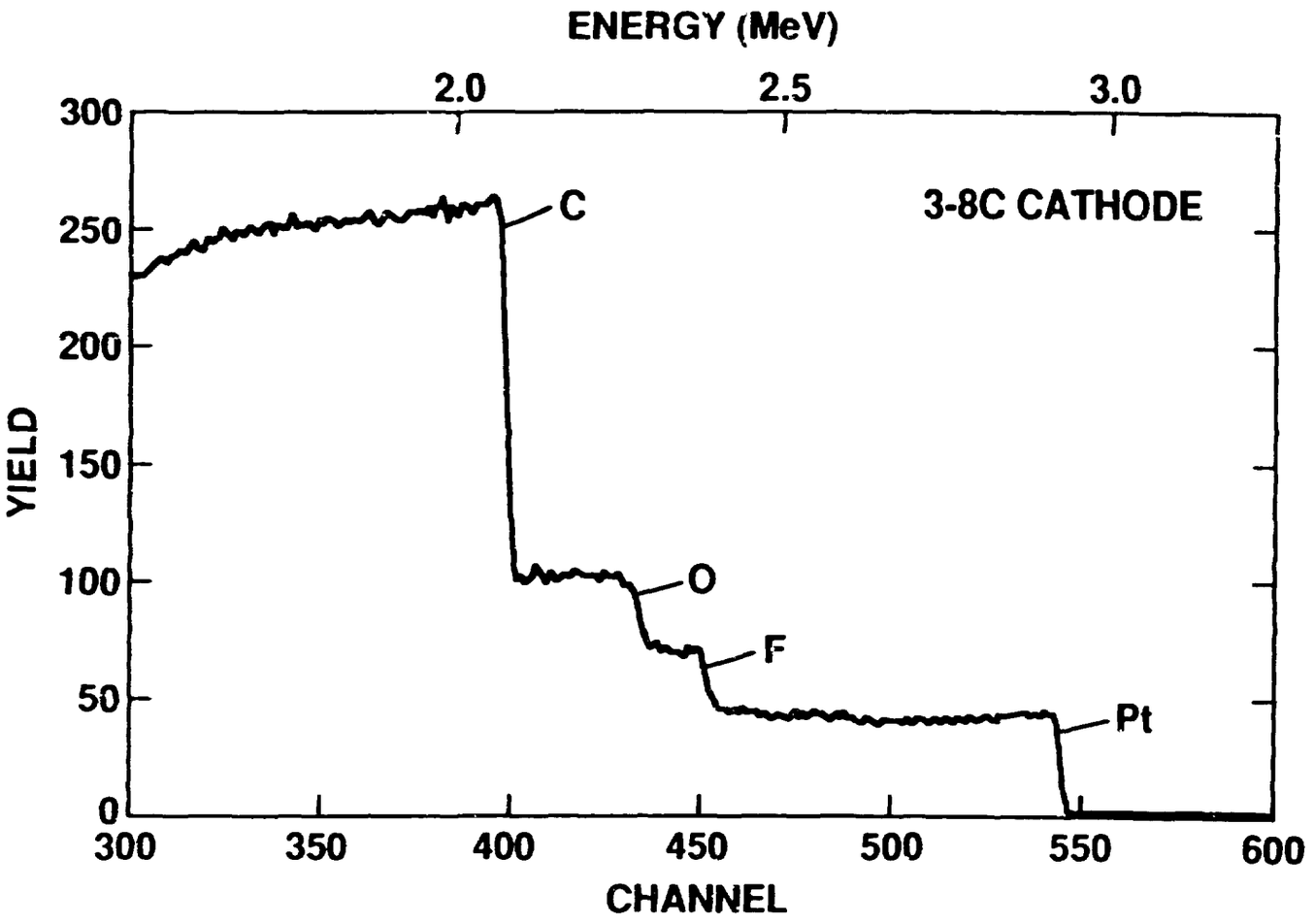
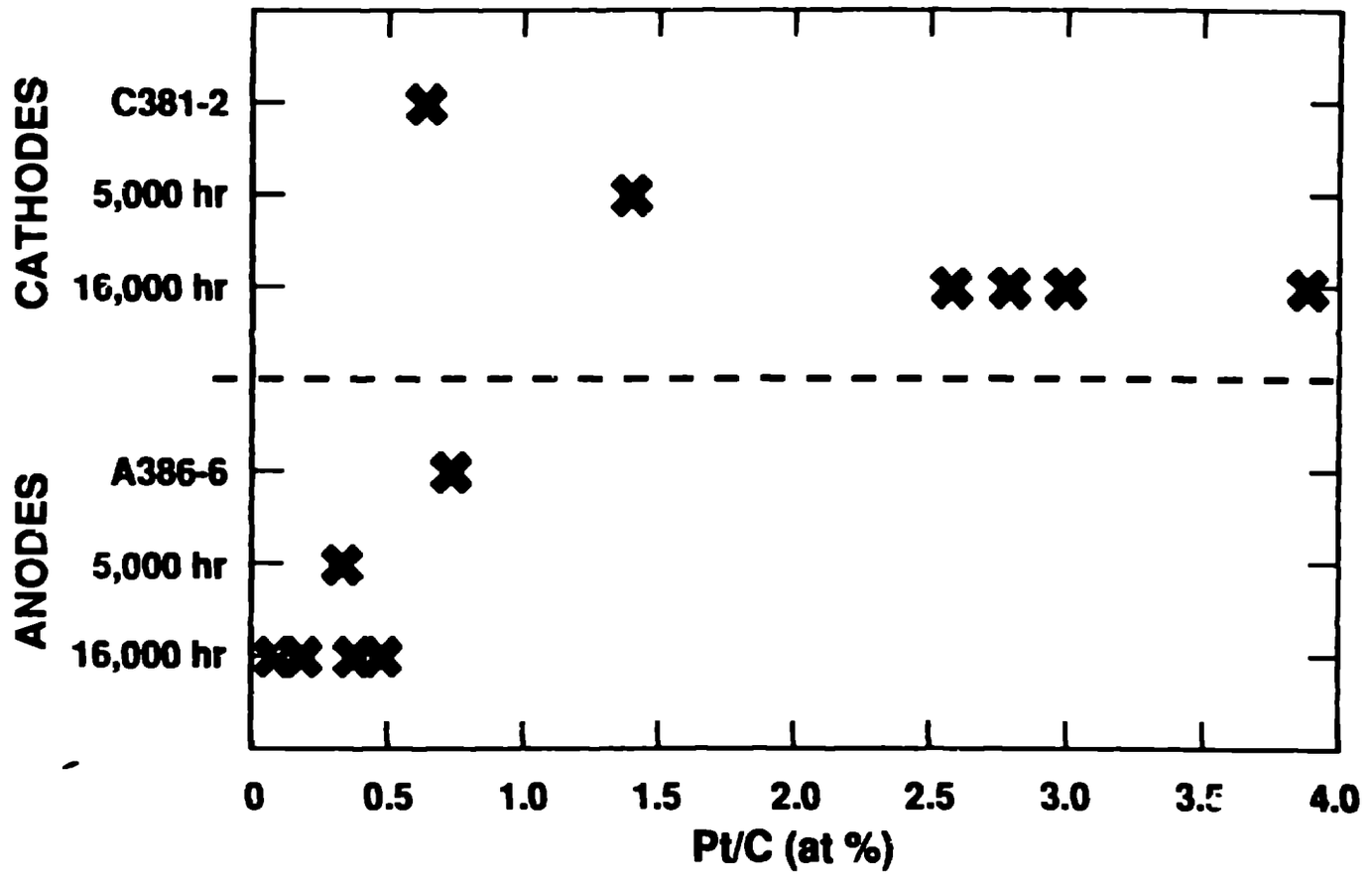

ENERGY (MeV)
2.0
2.5
3.0
300
250
200
150
100
50
0
YIELD
C
O
F
Pt
3-8C CATHODE
300
350
400
450
500
550
600
CHANNEL

Fig 16


CATHODES
C381-2
5,000 hr
16,000 hr
ANODES
A386-6
5,000 hr
16,000 hr
0
0.5
1.0
1.5
2.0
2.5
3.0
3.5
4.0
Pt/C (at %)