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GAS-PHASE THERMAL DISSOCIATION OF URANIUM  
HEXAFLUORIDE: INVESTIGATION BY THE TECHNIQUE  
OF LASER-POWERED HOMOGENEOUS PYROLYSIS

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# CONTENTS

	<u>Page</u>
LIST OF FIGURES . . . . .	v
LIST OF TABLES . . . . .	vii
SUMMARY . . . . .	ix
INTRODUCTION . . . . .	1
A BRIEF INTRODUCTION TO UNIMOLECULAR REACTIONS . . . . .	2
PREVIOUS ESTIMATES OF $\text{UF}_6$ THERMAL DISSOCIATION RATE . . . . .	2
LASER-POWERED HOMOGENEOUS PYROLYSIS . . . . .	4
EXPERIMENTAL . . . . .	8
GAS-HANDLING SYSTEM . . . . .	8
CELL CONSTRUCTION . . . . .	10
STANDARDS, CALIBRATION, AND DETECTION OF REAGENT GASES . . . . .	12
$\text{CO}_2$ LASER SYSTEM . . . . .	14
RESULTS AND DISCUSSION . . . . .	16
SELECTION OF A SENSITIZER . . . . .	16
SELECTION OF A "THERMOMETER" GAS . . . . .	18
SELECTION OF AN ATOMIC FLUORINE TRAPPING AGENT . . . . .	22
LPHP OF $\text{UF}_6$ WITH $\text{SIF}_4$ SENSITIZER AND $\text{CF}_3\text{Cl}$ REAGENT . . . . .	31
ACKNOWLEDGMENTS . . . . .	35
REFERENCES . . . . .	37
APPENDIX: APPLICATION OF THE RICE-RAMSPERGER-KASSEL THEORY . . . . .	45



# LIST OF FIGURES

Figure No.	Title	Page No.
1	Schematic for LPHP Experiment . . . . .	9
2	Nitrogen Mass Flow Rate with the Use of MB-41 Pump . . .	11
3	Reactor Cell Construction . . . . .	12
4	Calibration for $\text{CF}_4$ Concentration in $\text{CF}_3\text{Cl}$ Diluent, as Measured by FTIR Spectroscopy (6-cm Optical Pathlength . . . . .	15
5	Production of $\text{CF}_4$ Indicator, as Monitored by FTIR Spectroscopy, During Pulsed-Laser Pyrolysis of $\text{UF}_6$ with $\text{SiF}_4$ Sensitizer . . . . .	17
6	Production of Ethylene ( $\text{C}_2\text{H}_4$ ), as Monitored by FTIR Spectroscopy, During Pulsed-Laser Pyrolysis of Ethyl Chloride ( $\text{C}_2\text{H}_5\text{Cl}$ ) with $\text{SiF}_4$ Sensitizer . . . . .	21
7	UV-Absorption Cross-Sections ( $\epsilon'$ , $\text{torr}^{-1}$ , $\text{cm}^{-1}$ ) for $\text{UF}_6$ , $\text{Cl}_2$ , and $\text{ClF}$ . . . . .	26
8	Relative Change in IR Absorbance by $\text{UF}_6$ and $\text{ClF}$ During Photolysis of a Mixture of $\text{UF}_6$ and $\text{Cl}_2$ at 266 nm . . . . .	27
9	FTIR Scans of a Mixture of Gases with the Initial Room-Temperature Composition: $\text{UF}_6$ (1 torr), $\text{N}_2$ (4 torr), $\text{CF}_3\text{Cl}$ (10 torr), and $\text{SiF}_4$ (15 torr) . . . . .	30
A-1	Listing of RRK.BAS (Numerical Integration of RRK Integral) . . . . .	50
A-2	Sample Screen Output of RRK.BAS . . . . .	52
A-3	Listing of Program to Compute $S_{\text{eff}}(T)$ Using Harmonic Oscillator Frequencies . . . . .	55
A-4	Sample Screen Output from Execution of Fig. A-3 Example for $\text{UF}_6$ Reactant at 1300 K) . . . . .	56
A-5	Data of Schug and Wagner (1977) Plotted in an Empirical Manner to Yield an Estimate for the High-Pressure Limiting Rate Expression . . . . .	59

# LIST OF FIGURES (Continued)

Figure No.	Title	Page No.
A-6	Data of Schug and Wagner (1977): RRK Predictions Using $S_{\text{eff}} = U_{\text{vib}}/RT$ , With $\lambda$ as the Adjusted Parameter . . . . .	61
A-7	Data of Schug and Wagner (1977): RRK Predictions Using $S_{\text{eff}} = C_{\text{vib}}/R$ , With $\lambda$ as the Adjusted Parameter . . . . .	62
A-8	Gas-Phase Unimolecular Reaction Rate Predictions for $\text{UF}_6$ . Solid Curves: RRK Predictions, With $S_{\text{eff}} = C_{\text{vib}}/R$ and $\lambda = 1$ . Symbols: RRKM Predictions for $T = 700, 800, 900$ , and $1000 \text{ K}$ (Lyman and Holland, Unpublished Results, May 1985) . . . . .	63



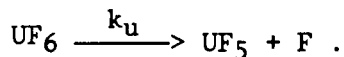
# LIST OF TABLES

Table No.	Title	Page No.
1	Laser-Powered Sensitized Thermal Reactions . . . . .	6
2	Bond Dissociation Energies ( $D_{298}^{\circ}$ ) for Selected Compounds . . . . .	8
3	Gas Mixtures for Laser-Powered Homogeneous Pyrolysis . .	10
4	Effect of $\text{SiF}_4$ Concentration on Apparent $\text{UF}_6$ Thermal Decomposition Rate . . . . .	16
5	High-Pressure-Limiting Arrhenius Parameters for Selected Unimolecular Reactions . . . . .	20
6	Thermal Decomposition of Ethylene ( $\text{C}_2\text{H}_4$ ) . . . . .	22
7	Estimated Rate Constants for Selected Reactions . . . .	24
8	Laser-Powered Homogeneous Pyrolysis of $\text{UF}_6$ - Data Summary . . . . .	32
9	Laser-Powered Homogeneous Pyrolysis of $\text{UF}_6$ -Derived Arrhenius Parameters . . . . .	33
10	Estimates of the High-Pressure-Limiting Arrhenius Parameters for $\text{UF}_6$ Thermal Dissociation . . . . .	33
A-1	Some Physical Parameters for Selected Molecules . . . .	49
A-2	Estimates of RRK Parameters for Selected Reactant Molecules . . . . .	57
A-3	Unimolecular Rate Constants for $\text{UF}_6$ in Argon Medium [Data from Schug and Wagner (1977)] . . . . .	58
A-4	RRK.BAS: Selected Parameters for Predicting the Gas- Phase Thermal Dissociation of $\text{UF}_6$ . . . . .	64

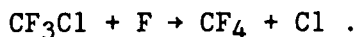


## SUMMARY

In the gas-phase, uranium hexafluoride decomposes thermally in a quasi-unimolecular reaction to yield uranium pentafluoride and atomic fluorine:



We have investigated this reaction using the relatively new technique of laser-powered homogeneous pyrolysis, in which a megawatt infrared laser is used to generate short pulses of high gas temperatures under strictly homogeneous conditions. In our investigation,  $\text{SiF}_4$  is used as the sensitizer to absorb energy from a pulsed  $\text{CO}_2$  laser and to transfer this energy by collisions with the reactant gas. Ethyl chloride is used as an external standard "thermometer" gas to permit estimation of the unimolecular reaction rate constants by a relative rate approach. When  $\text{UF}_6$  is the reactant,  $\text{CF}_3\text{Cl}$  is used as reagent to trap atomic fluorine reaction product, forming  $\text{CF}_4$  as a stable indicator which is easily detected by infrared spectroscopy:



Using these techniques, we estimate the  $\text{UF}_6$  unimolecular reaction rate constant near the high-pressure limit:

$$k_\infty = 1.1 \times 10^{16} \exp[-(71.3 \pm 4) \text{ kcal mol}^{-1}/RT] \text{ s}^{-1} .$$

This rate expression agrees with that derived by Schug and Wagner (1977) using the shock tube technique:

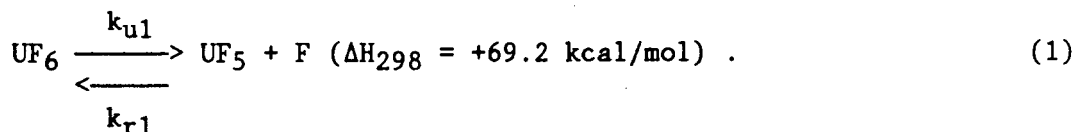
$$k_\infty = 3.3 \times 10^{16} \exp[-(70.3 \pm 4) \text{ kcal mol}^{-1}/RT] \text{ s}^{-1} .$$

In the Appendix, we describe a computer program, written for the IBM PC, which predicts unimolecular rate constants based on the Rice-Ramsperger-Kassel theory. Parameterization of the theoretical model is discussed, and recommendations are made for "appropriate" input parameters for use in predicting the gas-phase unimolecular reaction rate for  $\text{UF}_6$  as a function of temperature and gas composition and total pressure.

## INTRODUCTION

Uranium hexafluoride ( $\text{UF}_6$ ) is used in large quantities in the gaseous diffusion and gas centrifuge uranium enrichment enterprises, where its relative volatility (sublimation at  $56.5^\circ\text{C}$ ) and thermal stability make it suitable for this application [Bacher and Jacob (1982)]. It is thus a key intermediate in the production of other uranium compounds for nuclear fuel processing.

The present investigation seeks to better define the thermal dissociation rate of  $\text{UF}_6$ , which proceeds in the gas phase by unimolecular decay [Schug and Wagner (1977)]:

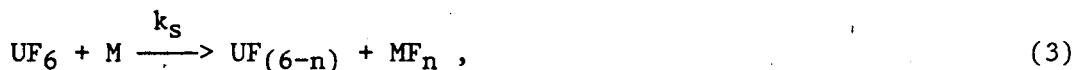


(The parenthetic term,  $\Delta H_{298}$ , represents the net enthalpy change at 298 K for the forward reaction. A positive value of  $\Delta H_{298}$  indicates an endothermic reaction, whereas a negative value represents an exothermic reaction. Thermodynamic values used to compute  $\Delta H_{298}$  in this work are taken from the National Bureau of Standards compilation of Wagman et al., 1982. Unless indicated otherwise, all reactants and products are assumed to be in the gas phase). The symbol "k" denotes the reaction rate constant, the temperature dependence of which is conventionally summarized in the form of an Arrhenius equation, i.e.,

$$k = A \exp(-E_a/RT) , \quad (2)$$

where the term A is the so-called pre-exponential factor,  $E_a$  is the energy of activation, and R is the gas constant ( $1.987 \text{ cal deg}^{-1} \text{ mol}^{-1}$ ).

The thermodynamic stability of  $\text{UF}_6$  has long been recognized [see Tumanov (1968), Galkin and Tumanov (1971), Hassan and Deese (1974), Lau and Hildenbrand (1982), Leitnaker (1983)], but, until recently, little was known about the unimolecular decay kinetics. This is due largely to the difficulties in handling  $\text{UF}_6$  at elevated temperatures. Uranium hexafluoride is a strong oxidizing and fluorination agent and tends to react with hot container surfaces, i.e.,



where M in Eq. (3) is any oxidizable material. The heterogeneous reaction [Eq. (3)] may predominate over the homogeneous reaction [Eq. (1)], which, together with the effects of recombination, makes it very difficult to assess the true unimolecular rate constant [Eq. (1)] using conventional measurement techniques.

## A BRIEF INTRODUCTION TO UNIMOLECULAR REACTIONS

As previously indicated, thermal dissociation of  $\text{UF}_6$  in the gas phase is believed to be a pseudounimolecular reaction. The unique properties of unimolecular reactions and some procedures used to model and predict their reaction rates are described in several standard texts and reviews [see Kassel (1932), Laidler (1965), Robinson and Holbrook (1972), Mulcahy (1973), and Troe (1975)].

In a unimolecular reaction, the activated complex is a single reactant which has gained the necessary energy of activation by collisions with other molecules [Laidler (1965)]. The reaction may be an isomerization or a decomposition. In general, the process may be represented as follows:



where  $\text{A}^*$  represents an energized molecule, and M represents a collision partner which transfers energy. At high gas pressures (high collision rate), the reaction of the energized molecule is rate limiting, and the empirical rate expression is first order with respect to the reacting species; as the pressure is decreased, the concentration dependence gradually changes to second order (i.e., the rate of activation by collision with species M becomes the rate-limiting step).

Many subtle theoretical formulations have been proposed to model and predict the pressure-dependent "fall-off" of  $k_u$ . A useful treatment is known as the Rice-Ramsperger-Kassel theory, described in the Appendix.

## PREVIOUS ESTIMATES OF $\text{UF}_6$ THERMAL DISSOCIATION RATE

In earlier work, Galkin and Tumanov (1971) used a variant of classical theory to predict the decomposition rate of  $\text{UF}_6$ , based on analogy to

other inorganic polyhalides. The results of their computations, as presented in Fig. 3 of their text, yield the rate expression (in Arrhenius form):

$$k_{u1} = 4.6E9 \exp[-(70.2) \text{ kcal mol}^{-1}/RT] \text{ s}^{-1} . \quad (6)$$

[In our notation, 4.6E9 represents  $4.6 \times 10^9$  and is Galkin and Tumanov's estimate for the Arrhenius "pre-exponential" term [A-term, Eq.(2)] for  $k_{u1}$  in Eq. (1)]. In their classical model, Galkin and Tumanov assumed that only 3 "effective" oscillators (of the 15 total harmonic oscillators in  $\text{UF}_6$ ) participate in the reaction (see Appendix), thus yielding a low value for the pre-exponential term (vide infra).

Schug and Wagner (1977) have used the conventional, single-pulse shock-tube technique to experimentally determine the thermal decomposition rate for  $\text{UF}_6$  diluted in argon (total gas density  $3E-6$  to  $4E-5$  mol/cm<sup>3</sup>, temperature range 1100 to 1450 K). Using this technique, relatively high temperatures can be obtained rapidly (from collisional translation-vibration (T-V) energy transfer from the argon propellant to the polyatomic reactant) and can be maintained for a convenient observation time (on the order of microseconds to milliseconds). Because of the shortness of the temperature pulse, little heat is transferred to the reactor walls, and homogeneous gas phase reactions may be studied. Some of the advantages and limitations of this technique are discussed by Belford and Strehlow (1969).

In the Schug and Wagner experiment, the real-time decrease in initial  $\text{UF}_6$  concentration during the shock was monitored by ultraviolet (UV) light absorption. Radiation was supplied by a 200-W xenon-mercury lamp, with filtering at the detector side of the reactor to wavelengths between 220 and 370 nm. Light with wavelengths  $<415$  nm is energetic enough to photolytically decompose  $\text{UF}_6$  to yield fragments identical to those produced by thermal decomposition [Lewis et al. (1979); Lyman et al. (1985)]:



where  $\beta\text{-UF}_5 (\text{s})$  is the condensation product of  $\text{UF}_5$  [Lyman et al.(1985)]

It is unknown whether the monitoring technique used in the Schug and Wagner experiment significantly contributed to the magnitude of the observed reaction rate. Only the initial portion of absorption-time data were used in the calculation of reaction rates; at times greater than  $\sim 100 \mu\text{s}$ , the absorption-vs-time signal became distinctly nonlinear, presumably due to  $\text{UF}_5 + \text{F}$  recombination or to light absorption by  $\text{UF}_5$  or its condensation products.

The pressure dependency of the measured rates suggested that the data were obtained in the transition between the low and high pressure-limiting domains. Schug and Wagner used a variant of the Kassel theory to extrapolate the data to estimate the first-order rate constant at the theoretical high-pressure limit ( $k_{\infty}$ ):

$$k_{\infty} = 3.3E16 \exp[-(70.3 \pm 4) \text{ kcal mol}^{-1}/RT] \text{ s}^{-1} . \quad (8)$$

Note that the pre-exponential term in Eq. (8) is several orders of magnitude greater than the theoretical estimate in Eq. (6) [Schug and Wagner have assumed 12.4 "effective" harmonic oscillators at 1300 K (see Appendix)]. Oref and Rabinovitch (1968) have criticized the use of "theoretical" methods such as the Kassel function to extrapolate rate data from the "fall-off" domain to the high-pressure limit, due to the difficulty in establishing an appropriate value for the number of "effective" oscillators to approximate the experimental curvature; however, we have applied an empirical procedure (such as Oref and Rabinovitch propose) to the Schug and Wagner data and have obtained a similar estimate for the high-pressure limit (see Appendix):

$$k_{\infty} = 1.1E16 \exp[-(67.8 \pm 2) \text{ kcal mol}^{-1}/RT] \text{ s}^{-1} . \quad (9)$$

In addition, Lyman and Holland (1985) have applied the Rice-Ramsperger-Kassel-Marcus (RRKM) quantum theory to the data reported by Schug and Wagner; the high-pressure limit derived from this treatment was predicted to be:

$$k_{\infty} = 2.6E16 \exp[-69.7 \text{ kcal mol}^{-1}/RT] \text{ s}^{-1} . \quad (10)$$

Although there is good agreement for the extrapolated high-pressure limit using Schug and Wagner's data [see Eqs. (8-10)], we concluded that there was sufficient uncertainty in the actual data to warrant an independent investigation using different techniques for homogeneous pyrolysis and for product detection. These techniques are described in detail in the following sections.

#### LASER-POWERED HOMOGENEOUS PYROLYSIS

Laser-powered homogeneous pyrolysis (LPHP) is a relatively new technique in which a megawatt infrared (IR) laser is used to generate high bath temperatures for gas-phase reactions under strictly homogeneous conditions [Shaub and Bauer (1975)]. The bath gas mixture contains a sensitizer gas that absorbs the infrared laser radiation strongly and then collisionally transfers a significant portion of the energy to the

desired reactant molecule without itself decomposing or chemically participating in the reaction process [Danen and Jang (1981)]. In typical experiments (see Table 1), total gas densities are on the order of 5 to 100 torr at ambient temperature (i.e.,  $2.7\text{E-}7$  to  $5.4\text{E-}6$  mol/cm<sup>3</sup>). At these densities, with use of a pulsed laser for multiphoton excitation, effective thermalization occurs within a few tens of nanoseconds, and heating continues for  $\sim 5$  to  $15$   $\mu\text{s}$  until the gas mixture is cooled by isentropic expansion behind a compression wave which moves radially outward at near-sonic velocity [McMillen et al. (1982)]. The short reaction time, together with diffusional mixing between laser pulses, minimizes side reactions. As in the shock tube technique, the reactor walls remain near ambient temperature, minimizing surface-catalyzed effects.

For quantitative work, the thermal profile must be known as a function of position and time throughout the reaction cell. These profiles can be estimated using gas dynamic models, but a simplified (and more accurate) procedure is to use an internal standard reactant (or "thermometer gas") with known kinetics similar to those of the compound under study [Dai et al. (1982), McMillen et al. (1982)]. Using a "relative-rate" approach [analogous to the comparative rate, single-pulse, shock-tube technique--see Belford and Strehlow (1969)], only an approximate estimate of the temporal and spatial variation of the temperature (as may be provided by a gas dynamic model) is required for accurate rate constant measurements [Dai et al. (1982)].

McMillen and co-workers (1982) derived a simplified data treatment which eliminates the need for explicit knowledge of the temperature corresponding to a particular measurement of a rate constant,  $k_u$ . In their formulation [see also Dai et al. (1982)],

$$\begin{aligned} \log F_u = \log A_u + (1 - E_u/E_s) \log t - (E_u/E_s) \log A_s \\ + (E_u/E_s) \log F_s, \end{aligned} \quad (11)$$

where  $A$  and  $E$  are Arrhenius terms [see Eq. (2)], subscripts  $u$  and  $s$  refer to the molecules with "unknown" and "standard" (i.e., known) kinetic properties,  $t$  is effective reaction time (s), and  $F = kt \sim \Delta P/P_0$  is the fractional decomposition per laser shot.

Both  $\text{SF}_6$  and  $\text{SiF}_4$  have frequently been used as sensitizers for multiphoton excitation by  $\text{CO}_2$  lasers (see Table 1). However,  $\text{SF}_6$  itself has been found to decompose under conditions of modest fluence from a pulsed  $\text{CO}_2$  laser [Danen and Jang (1981), Olszyna et al. (1977)]. In addition to its self-decomposition (primarily to  $\text{SF}_4$ ), excited  $\text{SF}_6$  can rapidly transfer near-resonant vibrational energy to  $\text{UF}_6$  (the reactant of interest in our investigation); the R-branch of the  $\nu_4$  band of  $\text{SF}_6$  overlaps the  $\nu_3$  band of  $\text{UF}_6$  [Karve et al. (1981)]. Karve et al. report rapid vibrational energy exchange between  $\text{SF}_6$  and  $\text{UF}_6$  (within a few tens of nanoseconds) after absorption of laser radiation by  $\text{SF}_6$  and specifically rule out a significant pyrolytic contribution in the multiphoton



Table 1. Laser-powered sensitized thermal reactions

Reference	CO <sub>2</sub> laser system	Sensitizer	Substrate	"Thermometer" gas	"Bath" gas <sup>a</sup>	Total gas density (mol/cm <sup>3</sup> )	Nominal reaction time (μs)	Effective temperature range (K)
Schaub and Bauer (1975)	CW, chopped at 1 Hz (λ = 10.67 μm)	SF <sub>6</sub>	Various organic compounds	Cyclopropane, etc.	Ar	(5.4-8.1)E-6	≥500	~700-1000
Farneth et al. (1976)	Pulsed (λ = 9.55 μm)	CH <sub>3</sub> F	Tetra methyl-1,2-dioxetane	(Chemiluminescence)	CH <sub>3</sub> F	(0.1-1.6)E-6	--	~400-500
Steel et al. (1979)	Pulsed (λ = 9.29 μm)	NH <sub>3</sub>	Cyclobutanone	(Cyclobutanone)	NH <sub>3</sub>	2.7E-6	~10-20	~1020-1320
Lewis et al. (1980)	Pulsed (λ = 10.57 μm)	SF <sub>6</sub>	Aromatic nitro compounds	--	SF <sub>6</sub> + Ar	(1.7-2.3)E-6	[~20] <sup>b</sup>	~1000-1200
Smith and Laine (1981)	Pulsed (λ = 10.59 μm)	SF <sub>6</sub>	Fe(CO) <sub>5</sub>	CH <sub>4</sub> (IR emission)	SO <sub>2</sub>	5.4E-6	~10	~1000
Comita et al. (1981)	Pulsed (λ = 9.73 μm)	SIF <sub>4</sub>	Tetralin	--	SIF <sub>4</sub>	(2.7-5.4)E-6	--	~900-1900 (T <sub>max</sub> )
Tsang et al. (1982)	Pulsed (λ = 9.74 μm)	SIF <sub>4</sub>	1,2-dichloropropane	--	SIF <sub>4</sub>	8.6E-7	>1	~1100
McMillen et al. (1982)	Pulsed (λ = 10.59 μm)	SF <sub>6</sub>	AZO compounds	t-butyl acetate, etc.	CO <sub>2</sub>	5.4E-6	~5-15	~780-1060
Dal et al. (1982)	Pulsed (λ = 9.73 μm)	SIF <sub>4</sub>	Chloroalkanes	Ethyl chloride	SIF <sub>4</sub>	2.8E-7	~10-30	~1150-1350
Jasinski and Estes (1985)	Pulsed (λ = 9.76 μm)	SIF <sub>4</sub>	Silane	Chloropropane	SIF <sub>4</sub>	1.1E-6	[~10] <sup>b</sup>	~750-1000
This work	Pulsed (λ = 9.73 μm)	SIF <sub>4</sub>	UF <sub>6</sub>	Ethyl chloride (external standard)	CF <sub>3</sub> Cl + SIF <sub>4</sub>	(1.6-8.1)E-6	[~20] <sup>b</sup>	~1050-1350

<sup>a</sup>Major constituent in mixture.<sup>b</sup>Assumed value.

excitation (at  $947\text{ cm}^{-1}$ ) of a mixture of  $\text{SF}_6$  and  $\text{UF}_6$ . Angelie and co-workers (1982) have also examined  $\text{SF}_6$ -sensitized dissociation of  $\text{UF}_6$ , with and without  $\text{H}_2$  as a scavenger for atomic fluorine reaction product. When  $\text{SF}_6$  itself was irradiated with a  $\text{CO}_2$  laser, the main decomposition product was  $\text{SF}_4$  (i.e., self-decomposition). When  $\text{UF}_6$  was added to the  $\text{SF}_6$ , dissociation of  $\text{SF}_6$  was drastically quenched. They propose several potential reaction mechanisms to account for this observation--the first is efficient deactivation of  $\text{SF}_6$  by (near-resonant) V-V energy transfer to  $\text{UF}_6$ :



[In Eq. (15), "M" designates a "third-body" collision partner for energy transfer.] An alternative mechanism is  $\text{SF}_6$  dissociation, followed by an efficient reaction with  $\text{UF}_6$  to regenerate  $\text{SF}_6$ :



Either mechanism would account for the preferential reduction of  $\text{UF}_6$  in the presence of  $\text{SF}_6$ .

We concluded that use of  $\text{SF}_6$  as a sensitizer for LPHP of  $\text{UF}_6$  would be unsatisfactory due to the possibility of nonpyrolytic mechanisms, including near-resonant V-V energy transfer and decomposition of  $\text{SF}_6$ , to produce species which may be directly reactive with  $\text{UF}_6$  [see Eq. (16)]. Silicon tetrafluoride ( $\text{SiF}_4$ ) is stable at considerably higher laser fluence values due to its high bond dissociation energy (see Table 2). Olszyna et al. (1977) have discussed the advantages of  $\text{SiF}_4$  as an inert sensitizer, and we have used it for this purpose in the current investigation.

Table 2. Bond dissociation energies ( $D_{298}^{\circ}$ ) for selected compounds

Compound	Bond	Bond dissociation energy (kcal/mol at 298 K)	Reference
SiF <sub>4</sub>	F-SiF <sub>3</sub>	160	Walsh (1981)
		142	Danen and Jang (1981)
UF <sub>4</sub>	F-UF <sub>3</sub>	148.2	Lau and Hildenbrand (1977)
HF	F-H	136.2	CRC, 66th ed. (1985)
CF <sub>4</sub>	F-CF <sub>3</sub>	130	Walsh (1981)
CF <sub>3</sub> Cl	F-CF <sub>2</sub> Cl	117	CRC, 66th ed. (1985)
	Cl-CF <sub>3</sub>	86	
HCl	H-Cl	103.1	CRC, 66th ed. (1985)
UF <sub>5</sub>	F-UF <sub>4</sub>	102	CRC, 66th ed. (1985)
SF <sub>6</sub>	F-SF <sub>5</sub>	92	Lyman (1977)
C <sub>2</sub> H <sub>5</sub> Cl	Cl-C <sub>2</sub> H <sub>5</sub>	80.4	Howlett (1952)
UF <sub>6</sub>	F-UF <sub>5</sub>	69.2 ± 4.6	Compton (1977)
		68.3 ± 3.5	Hildenbrand (1977)
		67.7 ± 5.6	Schug and Wagner (1977)
FCl	F-Cl	61.2	CRC, 66th ed. (1985)
Cl <sub>2</sub>	Cl-Cl	58.1	CRC, 66th ed. (1985)
F <sub>2</sub>	F-F	37.8	CRC, 66th ed. (1985)

## EXPERIMENTAL

## GAS-HANDLING SYSTEM

The experimental arrangement is schematically depicted in Fig. 1. Prior to each experiment, the gas-handling system is evacuated, then refilled from the gas manifold. The constituent with the lowest partial pressure in the final mixture is added first, with subsequent addition of reagent gases in the order of increasing partial pressure. Each gas addition is monitored by pressure change and the final total system

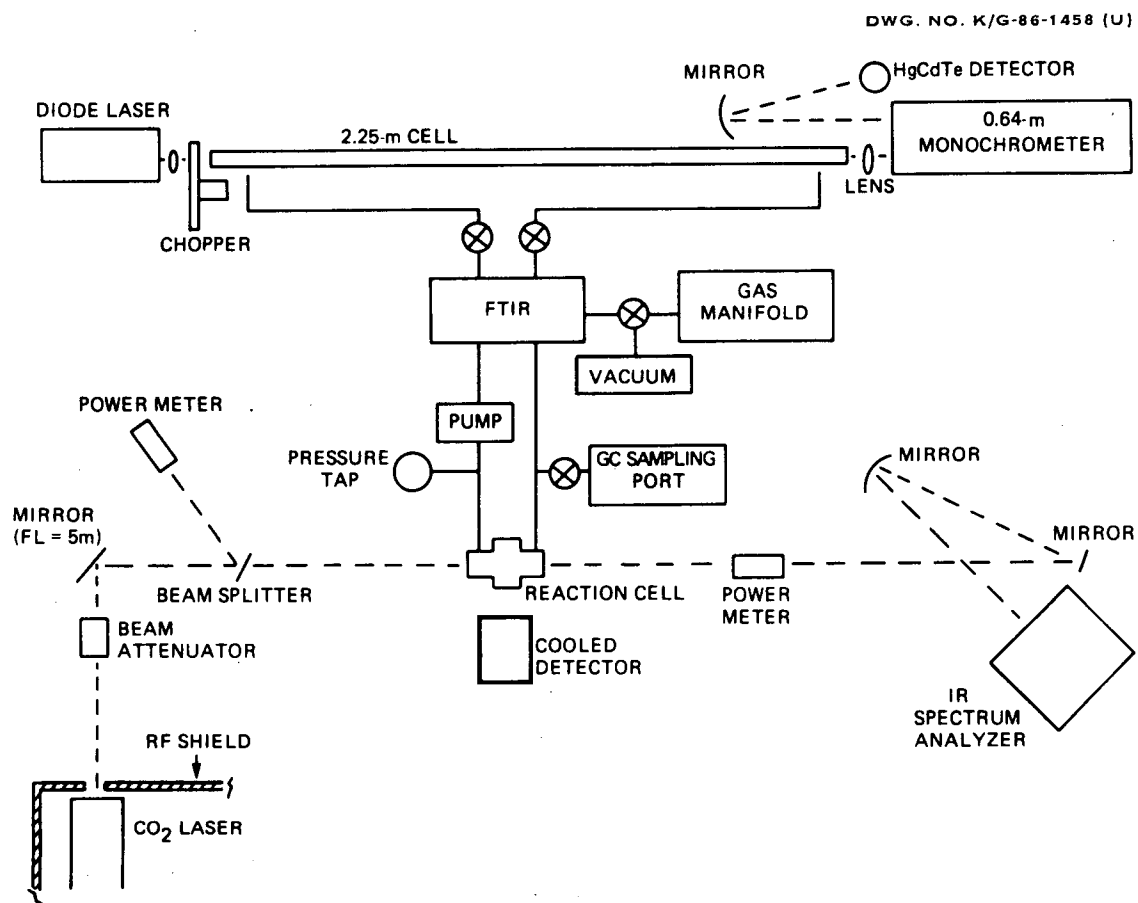


Fig. 1. Schematic for LPHP experiment.

pressure. Between each addition, the system is valved off and the manifold and fill lines evacuated. Then the manifold pressure of the next constituent to be added is raised to a pressure value slightly above that of the previous mixture. The valve to the gas circulation system is opened, and the total system pressure is adjusted to the target value by addition of the appropriate constituent. Gas mixture compositions for the major experiments described in the text are given in Table 3.

Table 3. Gas mixtures for laser-powered homogeneous pyrolysis

Data set	P = partial pressure (torr) at 25°C (298 K) [M] = density (mole/cm <sup>3</sup> )			
	SiF <sub>4</sub>	Reactant gas	CF <sub>3</sub> Cl	Total
A	P = 15 [M] = 8.1E-7	P = 5 [M] = 2.7E-7	P = 10 [M] = 5.4E-7	P = 30 [M] = 1.6E-6
B	P = 15 [M] = 8.1E-7	P = 10 [M] = 5.4E-7	P = 50 [M] = 2.7E-7	P = 75 [M] = 4.0E-6
C	P = 15 [M] = 8.1E-7	P = 10 [M] = 5.4E-7	P = 100 [M] = 5.4E-7	P = 125 [M] = 6.7E-6

Gases within the system are mixed and recirculated using a Metal Bellows Corporation, Model MB-41, pump; components of the pump contacting the gas stream are made from series 300 stainless steel or Teflon. Performance of this pump assembly in our system was measured with a Hastings All-1KP flow meter using nitrogen gas (see Fig. 2). Gas transfer lines were assembled from 1/4-in. (0.64-cm) ID nickel tubing with nickel-plated copper fittings.

The entire gas-handling system, including optical cells, was pre-conditioned by the batch-wise exposure to ClF<sub>3</sub> at room temperature. Passivation of surfaces was considered satisfactory when UF<sub>6</sub> (partial pressure ~10 torr in N<sub>2</sub> diluent) demonstrated long-term stability (i.e., for several hours) when recirculated through the system.

#### CELL CONSTRUCTION

For some preliminary experiments, a relatively long (~42-cm) reaction cell was constructed from series 304 stainless steel Varian Conflats® (see Fig. 3A). A KBr lens (focal length = 47 cm) was placed before the front window, producing a softly focused beam (~1 mm) at the center of the cell. An emission window, either synthetic sapphire (for visible and near IR) or AgCl (for extended-range IR), was located at the center of the cell, orthogonal to the laser beam path. A cooled detector

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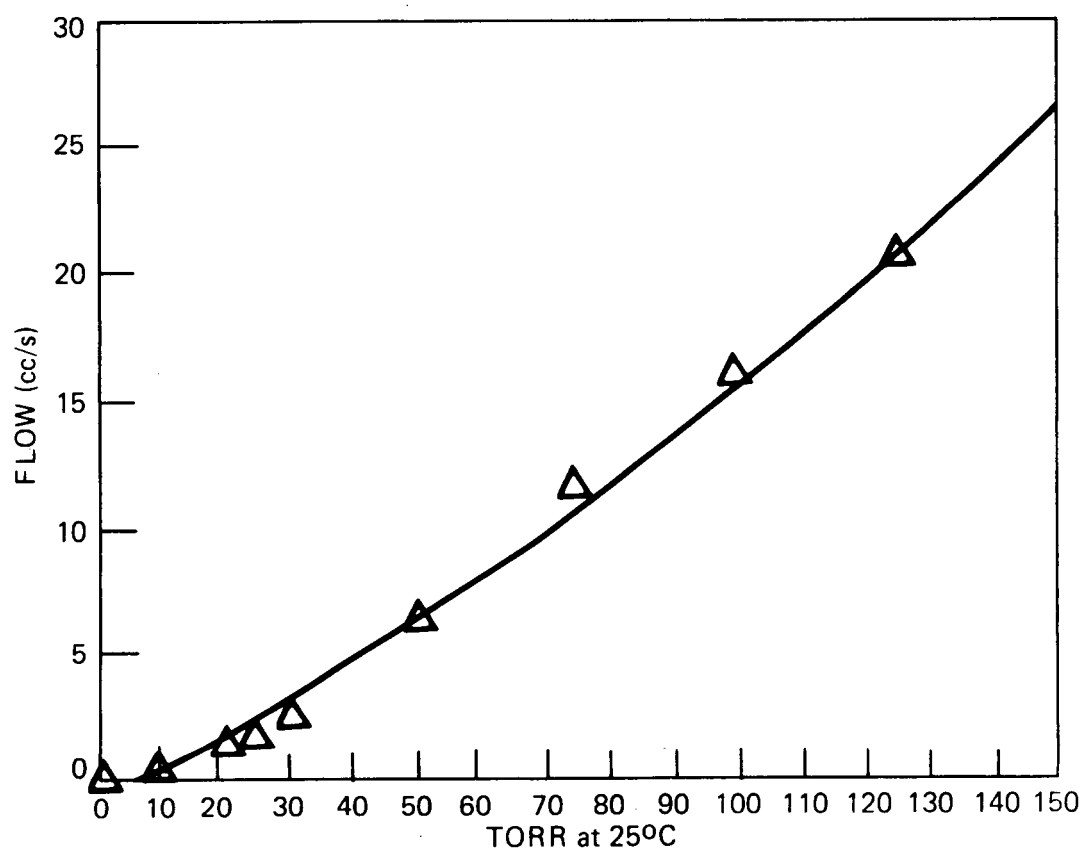
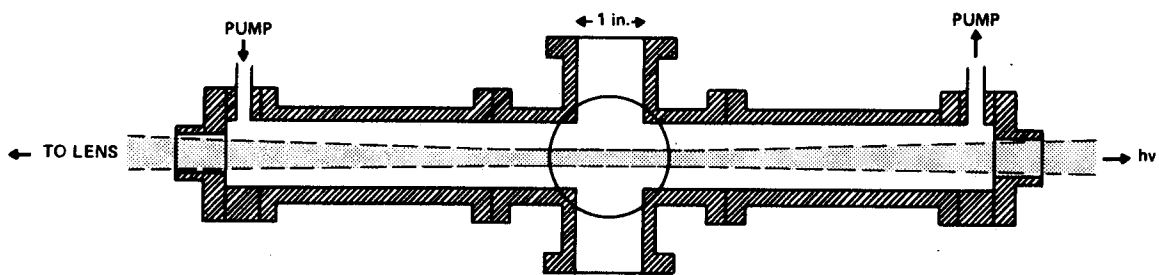
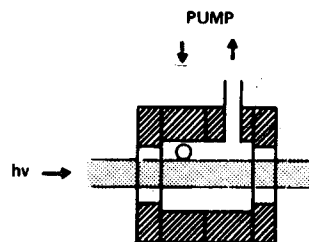


Fig. 2. Nitrogen mass flow rate with the use of MB-41 pump.



A) CELL GEOMETRY USED IN INITIAL STUDIES



B) CELL GEOMETRY USED IN FINAL STUDIES

Fig. 3. Reactor cell construction.

(photomultiplier tube or copper-doped germanium detector) was mounted at the emission window. For this configuration, beam volume within the cylindrical reaction cell, as estimated from burn patterns, was  $\sim 11 \text{ cm}^3$ , and total volume (exclusive of manifold, but including the long-path IR monitoring cell) was  $1229.6 \text{ cm}^3$ .

Initially, cell windows were KBr with a  $\text{CaF}_2$  evaporative coating on the inner surface. These windows demonstrated adequate resistance against chemical attack by corrosive gaseous fluorides [see also Swope (1971)], but they were readily damaged by high fluence IR laser radiation. Zinc selenide windows, antireflectance (AR) coated on both sides to withstand  $50 \text{ GW/cm}^2$ , were subsequently used; the AR coating on the inner surface was evaporated  $\text{PbF}_2$  (Type IV, II-VI Corp.). These windows demonstrated excellent stability to high-fluence IR radiation and to corrosive gases, although the windows did tend to form a film on the inner surface with a long-duration exposure to  $\text{UF}_6$  pyrolysis products. Each window transmitted  $\sim 61\%$  of the laser beam at the  $9.73\text{-}\mu\text{m}$  wavelength.

The long-path (2.25-m) IR-monitoring cell depicted in Fig. 1 was used in conjunction with a Laser Analytics diode laser spectrometer to increase detection sensitivity. A diode operating in the vicinity of  $760 \text{ cm}^{-1}$  in the P branch of  $\text{ClF}$  allowed detection of that species at partial pressures of  $\sim 0.005$  to  $0.10$  torr. A diode operating near  $1280 \text{ cm}^{-1}$  was used to monitor  $\text{CF}_4$  in some preliminary studies.

For the majority of experiments described in the text, we used a shorter cylindrical reaction cell, 1.5 in. (3.8 cm) ID  $\times$  2 in. (5.3 cm) long (active volume  $\sim 58 \text{ cm}^3$ ) as shown in Fig. 3B. For the partial pressures of  $\text{SiF}_4$  used in these experiments, the path length was optically thin, and (without the use of the KBr lens) energy deposition was essentially uniform; this helps prevent nonuniform axial temperatures and longitudinal acoustic waves. In this configuration, beam volume within the cell was  $\sim 8.2 \text{ cm}^3$ , and total volume (exclusive of manifold and long-path IR cell) was  $169.8 \text{ cm}^3$ .

#### STANDARDS, CALIBRATION, AND DETECTION OF REAGENT GASES

Normal assay  $\text{UF}_6$  was obtained from a large inventory manufactured by National Lead of Ohio and was purified by flashing off noncondensables and high-vapor pressure fractions. The remaining  $\text{UF}_6$  was then fractionally sublimed to separate  $\text{UF}_6$  from less volatile components.

Liquid chloroethane ( $\text{C}_2\text{H}_5\text{Cl}$ ) was purchased from Eastman Kodak Company (Catalog No. 1075). Lecture bottles of Freon 13 ( $\text{CF}_3\text{Cl}$ ), Freon 14 ( $\text{CF}_4$ ), silicon tetrafluoride, and ethylene (stated purities  $\geq 99\%$ ) were purchased from Matheson Gas Products.

The  $\text{CF}_3\text{Cl}$  reagent gas, as received, appeared to contain  $\sim 1\%$   $\text{CF}_4$  as an impurity, as determined from IR spectroscopy. A sample of this reagent was transferred to a smaller cylinder equilibrated in a n-propanol,



liquid N<sub>2</sub> slush bath at -123°C [see Rabek (1982)], and the more volatile CF<sub>4</sub> component was preferentially removed by fractional distillation. The residual CF<sub>4</sub> component in the purified CF<sub>3</sub>Cl was ~0.13% (mole basis).

The concentration of various gases was measured in a 6-cm path IR flow cell with silver chloride windows, mounted in a Nicolet Analytical Instruments, Model MX-1, Fourier transform infrared (FTIR) spectrophotometer, at nominal resolutions of 1 or 2 cm<sup>-1</sup>. Partial pressures of UF<sub>6</sub> were monitored at 626 or 631 cm<sup>-1</sup>; CF<sub>4</sub> at 1281 or 1283 cm<sup>-1</sup>; C<sub>2</sub>H<sub>5</sub>Cl at 677, 686, or 1298 cm<sup>-1</sup>; C<sub>2</sub>H<sub>4</sub> at 949 cm<sup>-1</sup>; and C<sub>2</sub>H<sub>2</sub> at 730 cm<sup>-1</sup>. Because total pressures were low ( $\leq 150$  torr at 25°C), pressure-broadening effects in complex gas mixtures were estimated by dilution of the constituent of interest in CF<sub>3</sub>Cl solution (major constituent of the reaction mixture in the LPHP experiment, see Table 1); a typical calibration curve is illustrated in Fig. 4. The calibration for organic constituents was also checked by withdrawing a sample of gas mixture for independent analysis by gas chromatography (GC) as seen in Fig. 1; GC of gas mixtures containing corrosive UF<sub>6</sub> was not attempted.

#### CO<sub>2</sub> LASER SYSTEM

A Lumonics Model TEA-103-2 grating-tuned CO<sub>2</sub> laser, operating on the 9 P(40) line (1027.4 cm<sup>-1</sup>) was used to excite the strong  $\nu_3$  band of SiF<sub>4</sub> (1029.6 cm<sup>-1</sup>). Laser frequency was verified using an Optical Engineering, Inc., Model 16-A, CO<sub>2</sub> laser spectrum analyzer. Each laser pulse consisted of an initial sharp feature of ~70-ns duration, followed by a long, but much less intense, tail. Typical laser output at this transition was ~1.5 J, with a pulse-to-pulse variation of  $\pm 10\%$  at a repetition rate of ~0.15 s<sup>-1</sup>. A slow repetition rate allows complete mixing by diffusion and convection (see Fig. 2) between two consecutive laser shots; small fractional conversion, coupled with efficient mixing, helps to minimize the effect of any secondary reactions.

The output coupler of the laser was AR-coated germanium (51 mm in diam  $\times$  5 mm thick); side 1 (inner) had a radius of 25 m, with 84% reflectivity, and side 2 (outer) had a radius of 10.75 m. An intercavity aperture was used to reduce transverse modes from the laser, and an external aperture was used to select the nearly uniform energy central portion of the beam. The beam profile was approximately Gaussian.

The beam path is illustrated in Fig. 1. Beam energy was attenuated in steps by placing uncoated potassium bromide or germanium flats in the beam path, giving average pulse energies of 0.5 to 1.5 J. The beam reflects off a copper mirror with a radius of 0.5 m to give a soft focus in the center of the reaction cell; nominal beam area (estimated from burn patterns) is ~1.6 cm<sup>2</sup> (reactor cross-section is ~11.4 cm). Approximately 5% of the input beam is directed from a potassium bromide beam splitter into a Laser Precision Corp., Model RJP-736, large-area (20 cm<sup>2</sup>) disk calorimeter, and the signal is monitored using a Laser Precision Corp., Model RJ7200, energy ratiometer. This served as the power meter for laser input energy to the pyrolysis cell. Energy transmitted

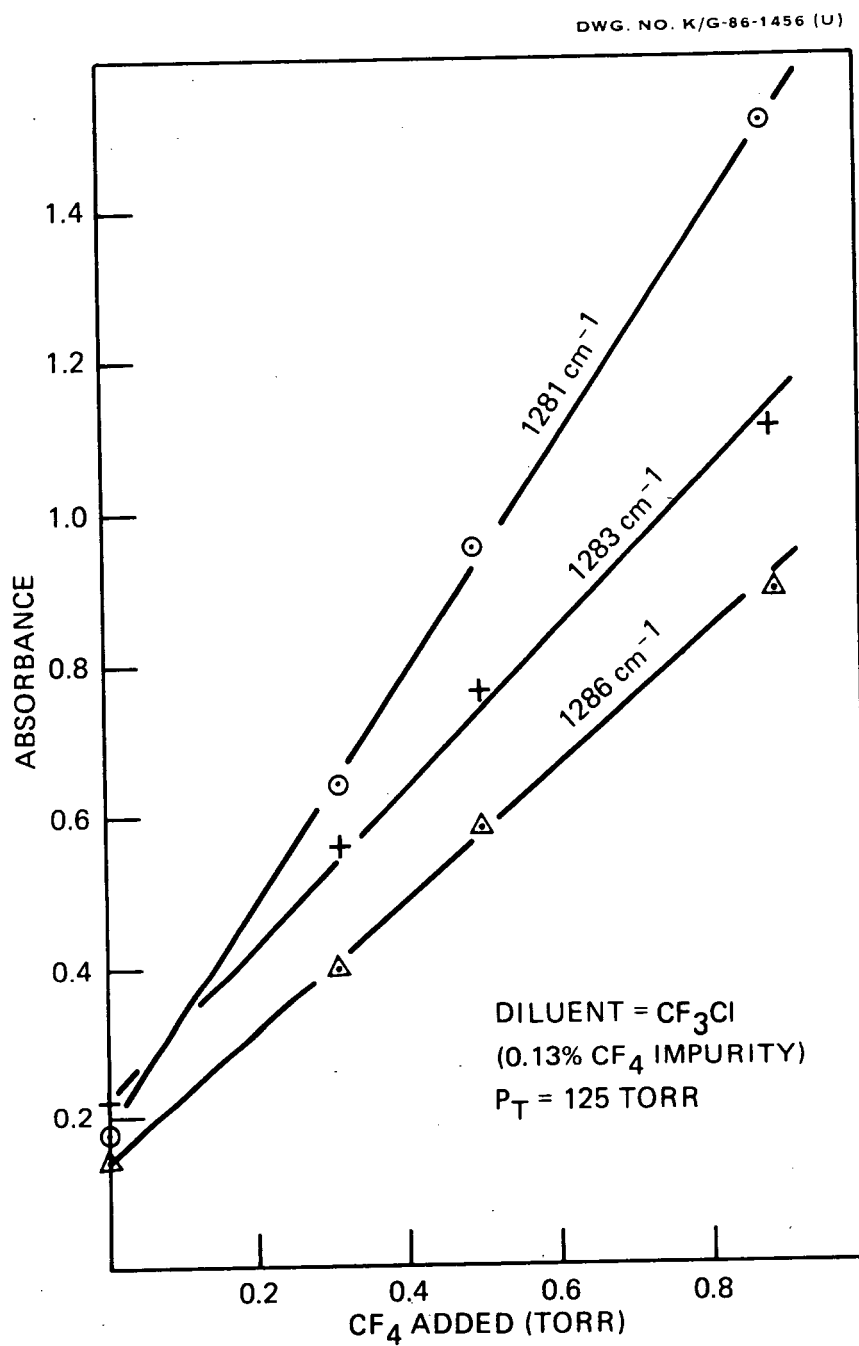


Fig. 4. Calibration for CF<sub>4</sub> concentration in CF<sub>3</sub>Cl diluent, as measured by FTIR spectroscopy (6-cm optical pathlength).

through the reaction cell was monitored by a second Laser Precision power meter assembly. These power meter measurements were periodically calibrated against a previously calibrated Scientech, Model 38-0102, volume-absorbing calorimeter with isoperibol enclosure.

## RESULTS AND DISCUSSION

### SELECTION OF A SENSITIZER

As illustrated in Table 4, the  $\text{SiF}_4$  partial pressure in the LPHP reaction mixture had a significant effect on the effective temperature produced within the pyrolysis cell, as judged by the yield of  $\text{CF}_4$  indicator species for atomic fluorine decomposition product from  $\text{UF}_6$  (see section titled Selection of an Atomic Fluorine Trapping Agent). In Table 4, mixtures I-IV represent room-temperature  $\text{SiF}_4$  partial pressures

Table 4. Effect of  $\text{SiF}_4$  concentration on apparent  $\text{UF}_6$  thermal decomposition rate

Mix	Gas composition ( $\text{mol}/\text{cm}^3$ ) $\times$ E6					$\Delta (\text{CF}_4/\text{N})^*$ ( $\text{mol}/\text{cm}^3$ ) $\times$ 1E11
	$\text{SiF}_4$	$\text{UF}_6$	$\text{CF}_3\text{Cl}$	$\text{N}_2$	Total	
I	0.27	0.27	0.27	0.53	1.34	-0.02
II	0.53	0.27	0.27	0.27	1.34	0.19
III	0.80	0.27	0.27	0	1.34	1.25
IV	1.07	0.27	0.27	0	1.61	2.97
V	1.07	0	0.27	0	1.34	0.40

\* $\Delta (\text{CF}_4/\text{N})$  is the change in  $\text{CF}_4$  concentration within the irradiation zone per laser pulse at an average incident fluence of  $1.45 \pm 0.04$  J. (Reactor geometry as in Fig. 3A; ratio of irradiated zone to total volume = 1:18.7.)

of 5, 10, 15, and 20 torr, respectively. Figure 5 illustrates the change in  $\text{CF}_4$  concentration (as monitored by FTIR spectroscopy) during LPHP using gas mix III, Table 4 (i.e., at 15 torr  $\text{SiF}_4$ ). At the lowest  $\text{SiF}_4$  partial pressure tested, there was essentially no change in the  $\text{CF}_4$  indicator upon laser irradiation; higher partial pressures produced significant indicator species. Apparently, at the laser fluence used in this study, there is a minimum threshold concentration of sensitizer necessary to produce detectable decomposition of  $\text{UF}_6$ . However, as shown by the data from mix V in Table 4, some production of  $\text{CF}_4$  indicator can occur without  $\text{UF}_6$  at high concentrations of sensitizer coupled to high

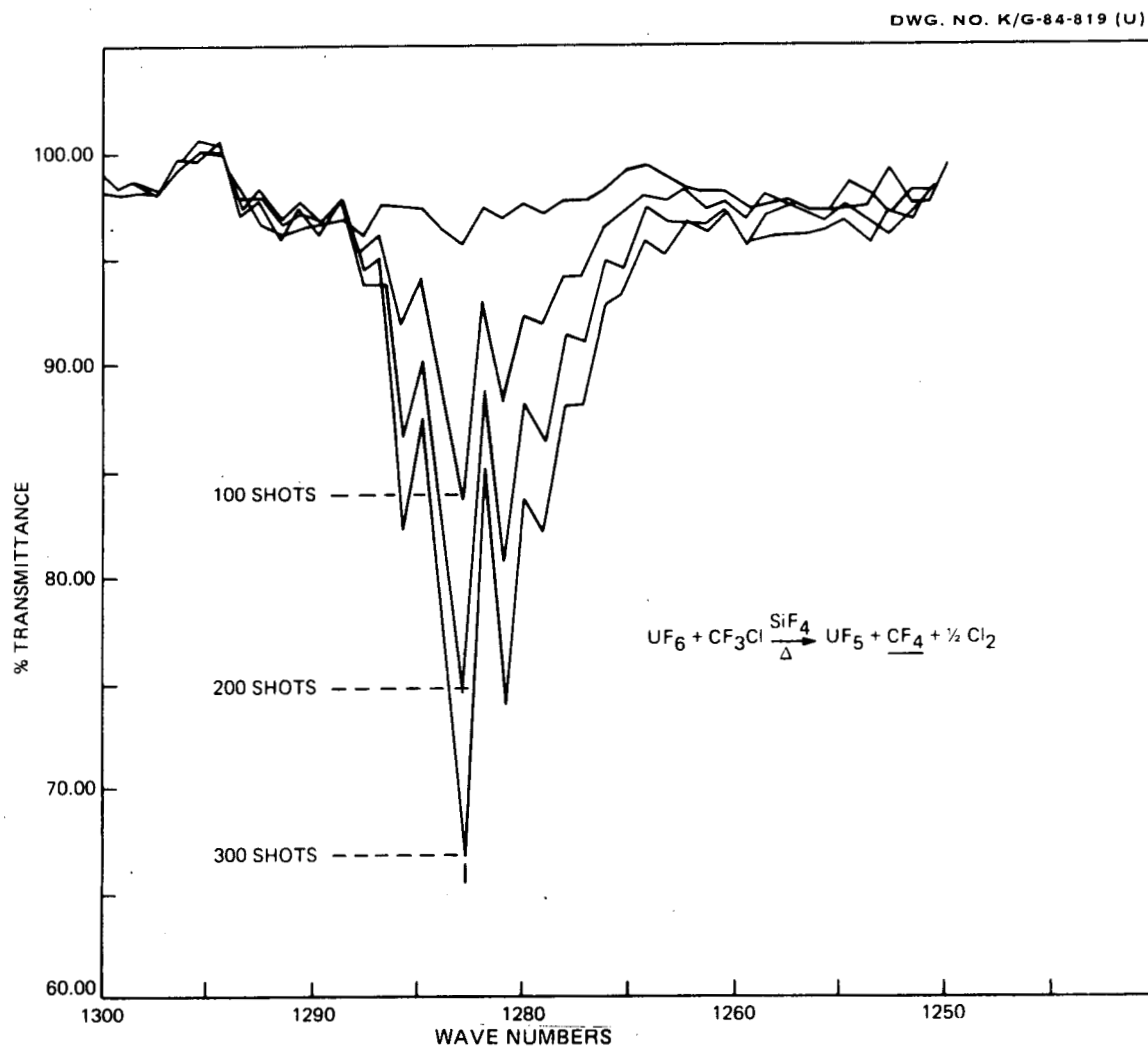


Fig. 5. Production of  $\text{CF}_4$  indicator, as monitored by FTIR spectroscopy, during pulsed laser pyrolysis of  $\text{UF}_6$  with  $\text{SiF}_4$  sensitizer.

laser fluence; at a partial pressure of 20 torr  $\text{SiF}_4$ , this "blank" rate of indicator production is ~13% of the rate observed in the presence of  $\text{UF}_6$  reactant. The origin of this "blank" reaction is not known but is probably related to the dissociation of the  $\text{Cl-CF}_3$  bond (86 kcal/mol, see Table 2), to produce  $\text{CF}_3$  radical, which then abstracts a fluorine atom to form  $\text{CF}_4$ . To minimize the production of indicator species from sources other than  $\text{UF}_6$  decomposition, we have used a room-temperature partial pressure of 15 torr ( $8.0\text{E-}7$  mol/cm<sup>3</sup>)  $\text{SiF}_4$  sensitizer in our LPHP experiments, and effective reaction temperature was varied by variation of laser fluence.

#### SELECTION OF A "THERMOMETER" GAS

The use of an internal standard, with well-accepted Arrhenius parameters, facilitates the estimation of corresponding parameters for the "unknown" reactant using Eq. (11) or similar treatment [McMillen et al. (1982), Dai et al. (1982)]. In particular, the use of a "thermometer gas" compensates for uncertainties in the temporal and spatial distribution of thermal energy in the reaction vessel. McMillen (1982) discusses the conditions under which data reduction using Eq. (11) is valid and most accurate.

The better the Arrhenius parameters of the "standard" and the "unknown" reactants are "matched," the less the relative yields depend on the exact temperature-time profile. For example, the energy of activation for the "unknown" is derived in Eq. (11) from the ratio  $E_u/E_s$ , so that the resulting estimate of the activation energy of the "unknown" compound is very "rugged" in the sense that rate ratios will be much closer to the high-pressure limiting values than are the absolute rates themselves [Dai et al. (1982)]. McMillen observes that for  $0.9 < (E_u/E_s) < 1.1$ , even a tenfold error in the estimated reaction time,  $t$ , will result in an error in the derived estimate of  $\log A_u$  of only 0.1 log units; such error is smaller than, or comparable in magnitude to, the typical uncertainty in parameter estimates from "average" experimental measurements of absolute rates. Benson and O'Neal (1970) estimate the probable error in the Arrhenius A-factor due to the uncertainty in activation energy:

$$\Delta(\log A) = \Delta(E_a)/2.3RT, \quad (18)$$

where  $\Delta(E_a)$  is the uncertainty in the activation energy (typically on the order of 5%). (e.g., a 4-kcal uncertainty in an activation energy of 70 kcal, measured at a mean temperature of 1300 K [see Eq. (8)] would be associated with an uncertainty in  $\log A$  of  $\pm 0.7$  log units).

In our data reduction using Eq. (11), we have assumed a median effective reaction time,  $t$ , of 20  $\mu\text{s}$ , comparable in magnitude to the

reaction times estimated or assumed by other investigators using the LPHP technique in reactors of similar geometry and with similar gas densities (see Table 1). In our experiment, we attempted a direct estimate of the time evolution of the temperature in the heated region by measuring the laser-induced IR thermal fluorescence emission of gas constituents triggered by the laser pulse; a similar technique was used to derive estimates of effective reaction times in the experiments reported by Smith and Laine (1981), McMillen et al. (1982), and Dai et al. (1982). However, RF noise pickup from our laser or microphonics in our detector (mounted orthogonally to laser beam propagation, see Fig.1) precluded accurate measurement of fluorescence emission during the first 30  $\mu$ s subsequent to the laser pulse. Qualitatively, the remainder of the recorded signal for gas mixture A (see Table 3) strongly resembled the data reported by Dai et al. (1982), with apparent cooling (due to gas expansion) between  $\sim 30$  to 100  $\mu$ s, followed by a slight reheating (attributed to the reflected shockwave) peaking at about 160  $\mu$ s.

Due to the aggressive reaction between  $\text{UF}_6$  and hydrocarbons, especially at elevated temperature, it was necessary to use the thermometer gas in a separate LPHP experiment (i.e., as an "external standard"), replacing  $\text{UF}_6$  as the reagent gas, under otherwise identical conditions of laser fluence and composition of other gases (see Table 2).

Cyclopropane ( $\text{c-C}_3\text{H}_6$ ) and ethyl chloride ( $\text{C}_2\text{H}_5\text{Cl}$ ) are good candidates for a thermometer gas; some reported estimates for their high-pressure Arrhenius parameters are given in Table 5 (note that there is a considerable range of estimated Arrhenius parameters, even for well-studied unimolecular reactions). As seen in the table, the Arrhenius parameters for cyclopropane are somewhat more similar to those reported by Schug and Wagner for  $\text{UF}_6$  than are the parameters for ethyl chloride, i.e.,  $E_u/E_s$  ratios of  $\sim 1.1$  for cyclopropane standard vs 1.2 for  $\text{C}_2\text{H}_5\text{Cl}$  standard. However, use of  $\text{SiF}_4$  sensitizer (as described previously) with  $\text{CO}_2$ -laser excitation at a 9.73- $\mu$ m wavelength could result in direct photolytic dissociation of cyclopropane, because the spectrum of cyclopropane (as well as propene product) overlaps that of  $\text{SiF}_4$  in this spectral region. In addition, high temperature shock-tube data for cyclopropane isomerization are reported to demonstrate "anomalous" kinetics [see Barnard et al. (1974)].

We elected to use ethyl chloride for our "thermometer gas," using the high-pressure Arrhenius parameters defined by Holbrook and Marsh (1967) (see Table 5). Ethyl chloride has little or no absorbance at 9.73  $\mu$ m; ethylene product has only weak absorbance at this wavelength (even when pressure-broadened at high gas density); and acetylene, the unimolecular decomposition product of ethylene, is transparent at this wavelength. For quantitation of ethyl chloride decomposition, we monitored ethylene and acetylene concentrations (see Experimental section). Figure 6 illustrates the increase in ethylene ( $\text{C}_2\text{H}_4$ ) product during an LPHP experiment in a mixture of  $\text{C}_2\text{H}_5\text{Cl}$ ,  $\text{CF}_3\text{Cl}$ , and  $\text{SiF}_4$ , as monitored by FTIR spectroscopy (at 2- $\text{cm}^{-1}$  resolution). At high laser fluence, LPHP of  $\text{C}_2\text{H}_5\text{Cl}$  also produced a new absorption at 730  $\text{cm}^{-1}$ , characteristic of acetylene ( $\text{C}_2\text{H}_2$ ); this was assumed to be due to subsequent thermal

Table 5. High pressure-limiting Arrhenius parameters for selected unimolecular reactions

Reaction	Log A	Ea (kcal/mol)	Log $k_{\infty}^a$ (T = 1000 K)	Reference
$\text{UF}_6 \rightarrow \text{UF}_5 + \text{F}$	16.52	70.3 ( $\pm 4$ )	+1.16	Schug and Wagner (1977)
Cyclopropane $\rightarrow$ Propene	15.16	65.4	+0.87	Benson and O'Neal (1970) <sup>b</sup>
	15.17	65.0	+0.96	Pritchard et al. (1953); Chambers and Kistiakowsky (1934)
	15.27	65.6	+0.94	Yau and Pritchard (1978)
	15.45	65.6	+1.11	Dillard and Heydtmann (1977)
	15.52	65.5	+1.21	Furue and Pacey (1982)
Ethyl chloride $\rightarrow$ Ethylene + HCl	13.2	56.5	+0.85	Benson and O'Neal (1970) <sup>b</sup>
	14.03 ( $\pm 0.4$ )	58.43 ( $\pm 1.5$ )	+1.26	Holbrook and Marsh (1967)
	13.8	57.4	+1.26	Dai et al. (1982) <sup>b</sup>
	13.33 ( $\pm 0.1$ )	56.3 ( $\pm 0.3$ )	+1.03	Heydtmann et al. (1975)
	14.6	60.8	+1.31	Howlett (1952)
	13.84	57.8	+1.21	Evans et al. (1978)

<sup>a</sup>Log  $k_{\infty} = \text{Log A} - E_a/2.3RT$ .

<sup>b</sup>Values assumed for calculations in cited text.

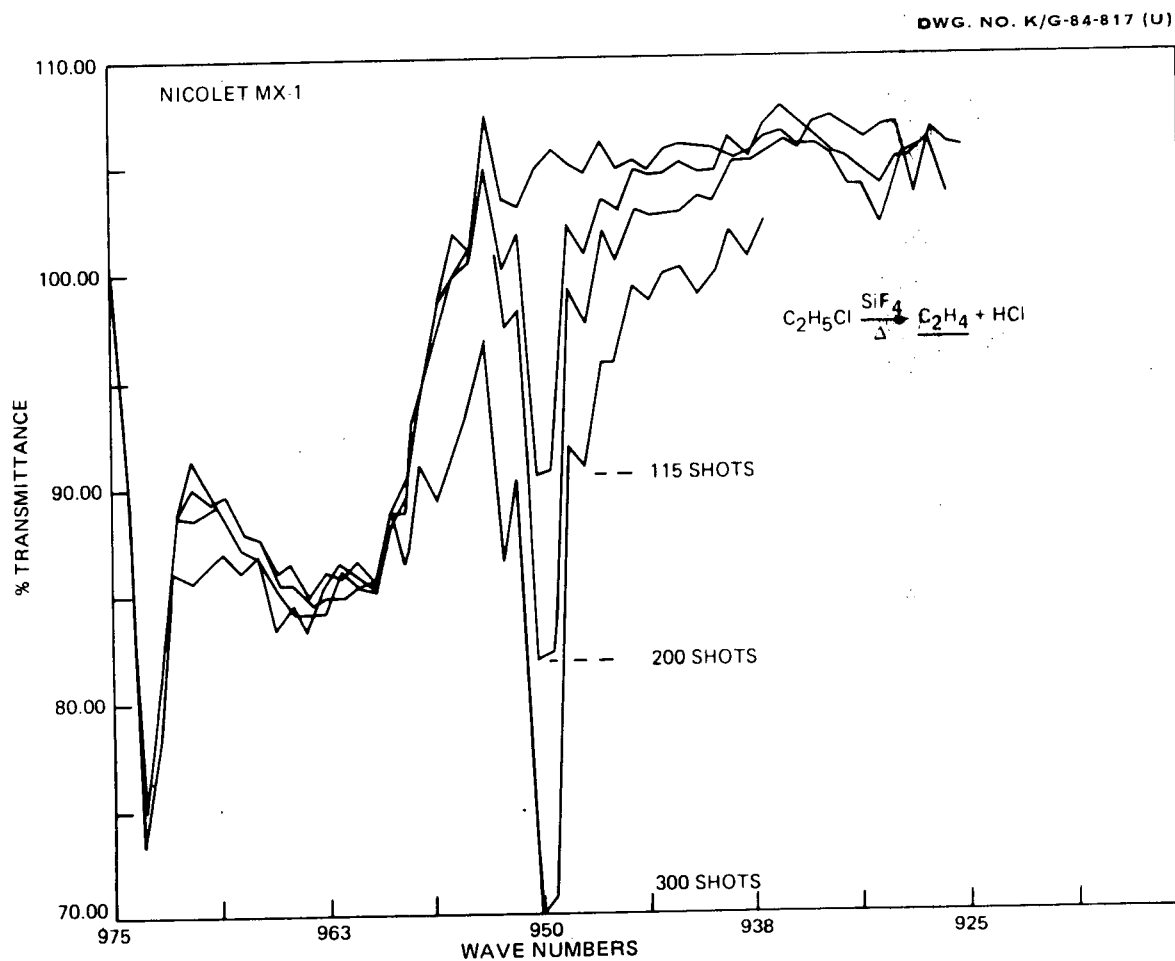


Fig. 6. Production of ethylene ( $\text{C}_2\text{H}_4$ ), as monitored by FTIR spectroscopy, during pulsed laser pyrolysis of ethyl chloride ( $\text{C}_2\text{H}_5\text{Cl}$ ) with  $\text{SiF}_4$  sensitizer.



dissociation of  $C_2H_4$ . LPHP with  $C_2H_4$  as the reactant gas (conditions as in Table 3, data set A), vs  $C_2H_5Cl$  as an "external standard," yielded the Arrhenius parameters for  $C_2H_4$  given in Table 6, in which our results are compared with those reported previously using shock tube techniques and conventional static thermal reactors. As in the shock tube experiments, the LPHP decomposition product was  $C_2H_2$ , with no indication (by IR spectroscopy) of other hydrocarbons formed from surface-catalyzed chain reactions (cf static reactors). The activation energies determined by the LPHP and shock tube experiments are in good agreement; the Arrhenius pre-exponential factor determined from the LPHP experiment may be somewhat high, perhaps reflecting a minor photolytic contribution to the overall dissociation.

Table 6. Thermal decomposition of ethylene ( $C_2H_4$ )

Technique	Conditions	Predominant mechanism <sup>a</sup>	Log A	Ea (kcal/mol)	Reference
Shock tube	$C_2H_4$ in Ar T = 1250 - 1800 K P = 1700 - 4300 torr	Uni	8.41	40	Kozlov and Knorre (1963)
	T = 1300 - 1800 K 1170 - 1425 K	Uni	8.87 11.95	46.5 65	Skinner and Sokolski (1960)
	T = 1400 - 300 K	Uni	?	73	Asaba et al. (1962)
LPHP	$C_2H_4$ in $SiF_4 + CF_3Cl$ (M = $8E - 7$ mol/cm <sup>3</sup> ) T = 1140 - 1290 K	Uni	14.73 ( $\pm 0.1$ )	66.2 ( $\pm 0.6$ )	This work
Static	Self-medium T near 725 K	Chain	14.7	70.8	Delliste et al. (1981)
	T = 770 - 870 K P = 50 - 300 torr	Chain	14.82	64	Boyd et al. (1968)
	T near 825 K	Chain	?	60 $\pm$ 6	Nazarov and Torban (1966)

<sup>a</sup>Uni = Unimolecular ( $C_2H_4 \rightarrow C_2H_2 + H_2$ ). Chain = radical reaction ( $C_2H_2 + C_2H_6 + C_4H_8$ , etc.).

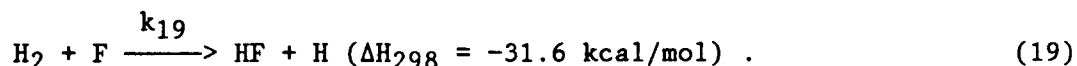
## SELECTION OF AN ATOMIC FLUORINE TRAPPING AGENT

The recombination reaction between  $UF_5$  and atomic fluorine [reverse reaction Eq. (3)] is relatively rapid [Lyman et al. (1985)]. (Note that  $UF_5$  which does not recombine with atomic fluorine tends to polymerize and to condense out as solid  $\beta$ - $UF_5$  near room temperature [Lewis (1979), Lyman (1985)]).

If one is to determine the unimolecular decomposition of  $UF_6$ , one must either follow the real-time change in  $UF_6$  composition during the first few milliseconds of the reaction (as in the Schug and Wagner experiment), or (because it is difficult to make selective, real-time measurements of the transient, highly reactive  $UF_5$  or F products), one must trap

the atomic fluorine product by a rapid indicator reaction to yield a stable, easily monitored species.

Reaction kinetics for many reactions of atomic fluorine have been reviewed [see Zetzsch (1976), Jones and Skolnik (1976), Foon and Kaufman (1975), Baulch et al. (1981)]. Estimated rate constants for some reactions of interest, including selected reactions of atomic fluorine, are given in Table 7. Molecular hydrogen reacts very rapidly with atomic fluorine (see Table 7), and it has been used as a trapping agent for atomic fluorine produced by the UV-photolysis of  $\text{UF}_6$  [see Lewis et al. (1979), Andreoni et al. (1980), Lyman et al. (1985)]:



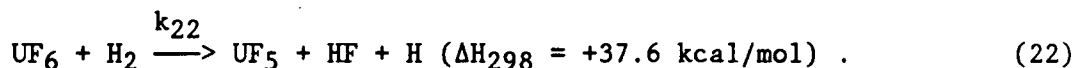
The primary quantum yield ( $\phi$ ) for a photolytic reaction of the type:



is defined (see Rabek, 1982) as

$$\phi = \frac{\text{number of molecules, radicals, or ions of B formed}}{\text{number of quanta absorbed by A}} . \quad (21)$$

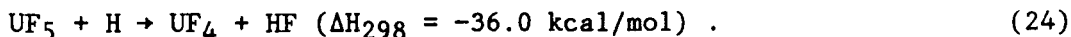
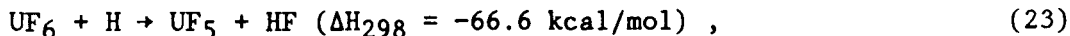
In the absence of trapping agent, the apparent quantum yield for the photolysis of  $\text{UF}_6$  at moderate gas densities is less than unity, due to  $\text{UF}_5 + \text{F}$  recombination; however in the presence of  $\text{H}_2$ , the apparent quantum yield is substantially above unity [Andreoni et al. (1980), Lewis et al. (1979)]. This indicates a net reduction of  $\text{UF}_6$  by  $\text{H}_2$  or fluorine abstraction from  $\text{UF}_6$  by atomic hydrogen. The mechanism and kinetics of the gas phase reactions between  $\text{UF}_6$  and  $\text{H}_2$  are complicated, with solid  $\text{UF}_4$  being formed at elevated temperatures [Tumanov and Galkin (1971), Myerson and Chuldzinski (1981), Barber (1985)]. Barber (1985) suggests that the initial step in the reduction of  $\text{UF}_6$  by  $\text{H}_2$  is the following:



The endothermic nature of reaction Eq. (22) suggests that F abstraction by atomic hydrogen is important in  $\text{UF}_6$  reduction by hydrogen [Barber (1985)]:

Table 7. Estimated rate constants for selected reactions

Text eqn.	Reaction	Log k = log A - Ea/2.3 RT			Reference
		Log <sub>10</sub> A	Ea (kcal/mol)	k (T)	
(1)	UF <sub>6</sub> → UF <sub>5</sub> + F	16.52	70.3	k (1200 K) = 5.2E-3 (s <sup>-1</sup> )	Schug and Wagner (1977)
(1)	UF <sub>5</sub> + F → UF <sub>6</sub>	~12.6	~0.72	k (300 K) = 1.2E-12 k (1200 K) = 3E-12 (cm <sup>3</sup> /mol-s)	Lyman et al. (1985) and personal communication
(15)	F + F + M → F <sub>2</sub> + M (M = Ar)	8.51	3.19	k (1200 K) = 4E-9 (cm <sup>6</sup> mol <sup>-2</sup> s <sup>-1</sup> )	Baulch et al. (1981)
(19)	H <sub>2</sub> + F → HF + H	13.4	0.9	k (300 K) = 1.5E-13 (cm <sup>3</sup> /mol-s)	Jones and Skolnik (1976)
(22)	UF <sub>6</sub> + H <sub>2</sub> → UF <sub>5</sub> + HF + H	15.9	34.5	k (300 K) = 5.9E-10 k (800 K) = 2.9E-6 (cm <sup>3</sup> /mol-s)	Barber (1985)
(23)	UF <sub>6</sub> + H → UF <sub>5</sub> + HF	14	4.2	k (300 K) = 8.7E-10 (cm <sup>3</sup> /mol-s)	Rienacker (1981)
(25)	Cl <sub>2</sub> + F → ClF + Cl	14.74	1.4	k (300 K) = 5.2E-13 (cm <sup>3</sup> /mol-s)	Warnatz et al. (1971)
(28)	Cl <sub>2</sub> + M → Cl + Cl + M (M = Ar)	13.36	23.6	k (1200 K) = 6.5E-4 (cm <sup>3</sup> /mol-s)	Baulch et al. (1981)
(30)	CF <sub>3</sub> Cl + F → ClF + CF <sub>3</sub>	13.8	20.9	k (300 K) = 0.04 k (1200 K) = 9.7E+6  k (300 K) ≤ 1E+9 (cm <sup>3</sup> /mol-s)	Foon and Tait (1972)  Zetzsch (1971)



Because of the anticipated complications with use of hydrogen with  $\text{UF}_6$ , we sought alternative F-atom reagents. In some initial studies, we investigated the use of chlorine, which is known to react rapidly and quantitatively with atomic fluorine:



Atomic chlorine product ( $\text{Cl}$ ) can react with the reactor walls or with another gaseous constituent of the reaction mixture, or two atoms of  $\text{Cl}$  can recombine in a three-body collision with an energy acceptor:



In a qualitative experiment, a mixture of ~75 torr each of  $\text{UF}_6$  and  $\text{Cl}_2$  were irradiated with 266-nm wavelength light from a Nd:YAG laser (frequency quadrupled). (The reported UV-absorption cross-sections for  $\text{UF}_6$ ,  $\text{Cl}_2$ , and  $\text{ClF}$  are presented in Fig. 7.) The 6-cm cubic irradiation cell had sapphire windows at two opposing faces to transmit UV radiation and silver chloride windows mounted orthogonally to permit IR scanning of the cell contents. Subsequent to UV irradiation, the IR spectrum indicated a loss of  $\text{UF}_6$  (as monitored at 1160 and at 1290  $\text{cm}^{-1}$ ), and new absorption bands concurrently appeared at 760 and 785  $\text{cm}^{-1}$ , characteristic of  $\text{ClF}$  [see Eq. (25) and Fig. 8].

Some solid residue appeared on the cell windows; the cell was evacuated, and the nonvolatile residue remaining on the windows was scanned to reveal absorption bands at approximately 620 and 560  $\text{cm}^{-1}$ , and a strong absorption feature at lower wavenumbers. An in-house reference spectrum for  $\beta\text{-UF}_5$  displayed absorption features at ~625, 570, and 430  $\text{cm}^{-1}$ , whereas Jacob (1973) reports the spectrum of  $\beta\text{-UF}_5$  to contain features at ~605, 573, and 512  $\text{cm}^{-1}$ , with a broad band at 390  $\text{cm}^{-1}$ . It appears probable that the nonvolatile residue in our photolysis experiment was  $\beta\text{-UF}_5$  condensation product, similar to that reported by Lewis et al. (1979).

Attempts at quantitative estimates of the quantum yield [see Eq. (21)] for photolysis of  $\text{UF}_6$  (reactant) in the presence of  $\text{Cl}_2$ , based on laser diode detection of  $\text{ClF}$  as the indicator species for  $\text{UF}_6$  dissociation, produced values of ~2 (i.e., ~2 moles of  $\text{ClF}$  were formed per Einstein of radiation absorbed by  $\text{UF}_6$  at wavelengths of 266 and 355 nm). (A more precise estimate of the quantum yield was hampered by the modest

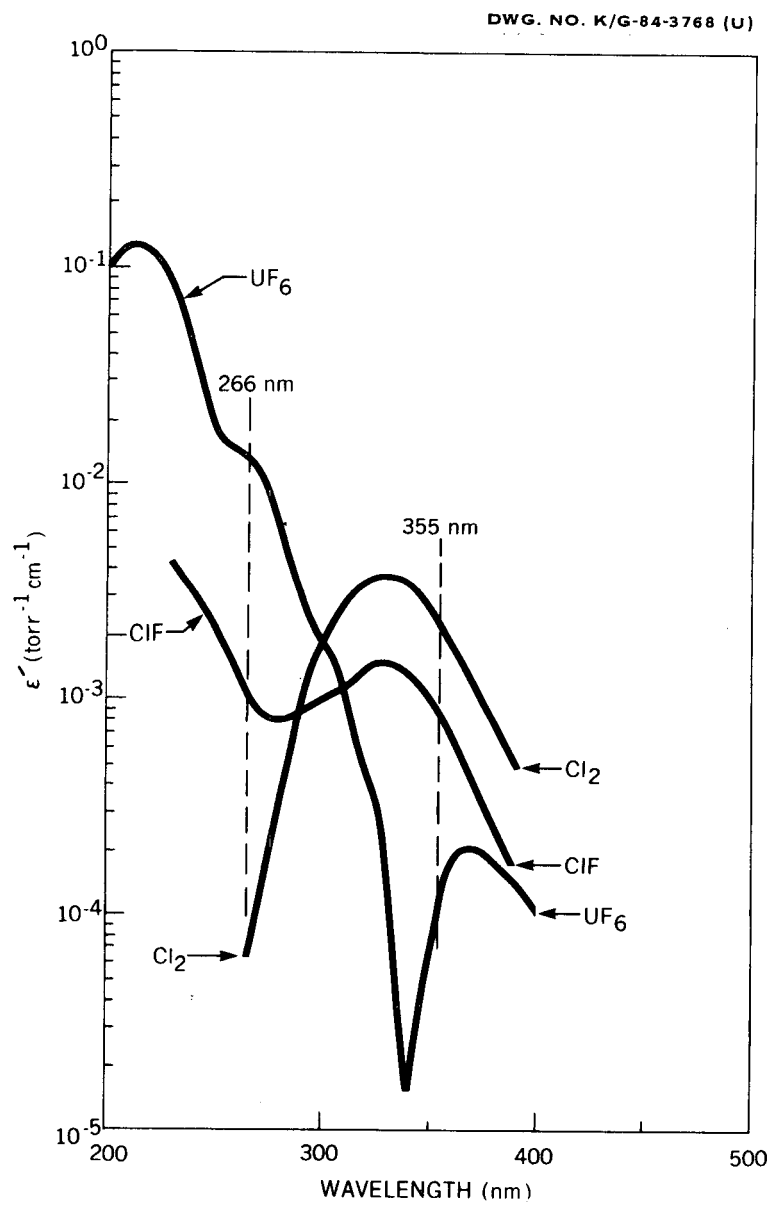


Fig. 7. UV-absorption cross-sections ( $\epsilon'$ ,  $\text{torr}^{-1} \text{cm}^{-1}$  for  $\text{UF}_6$ ,  $\text{Cl}_2$ , and  $\text{CIF}$ ).

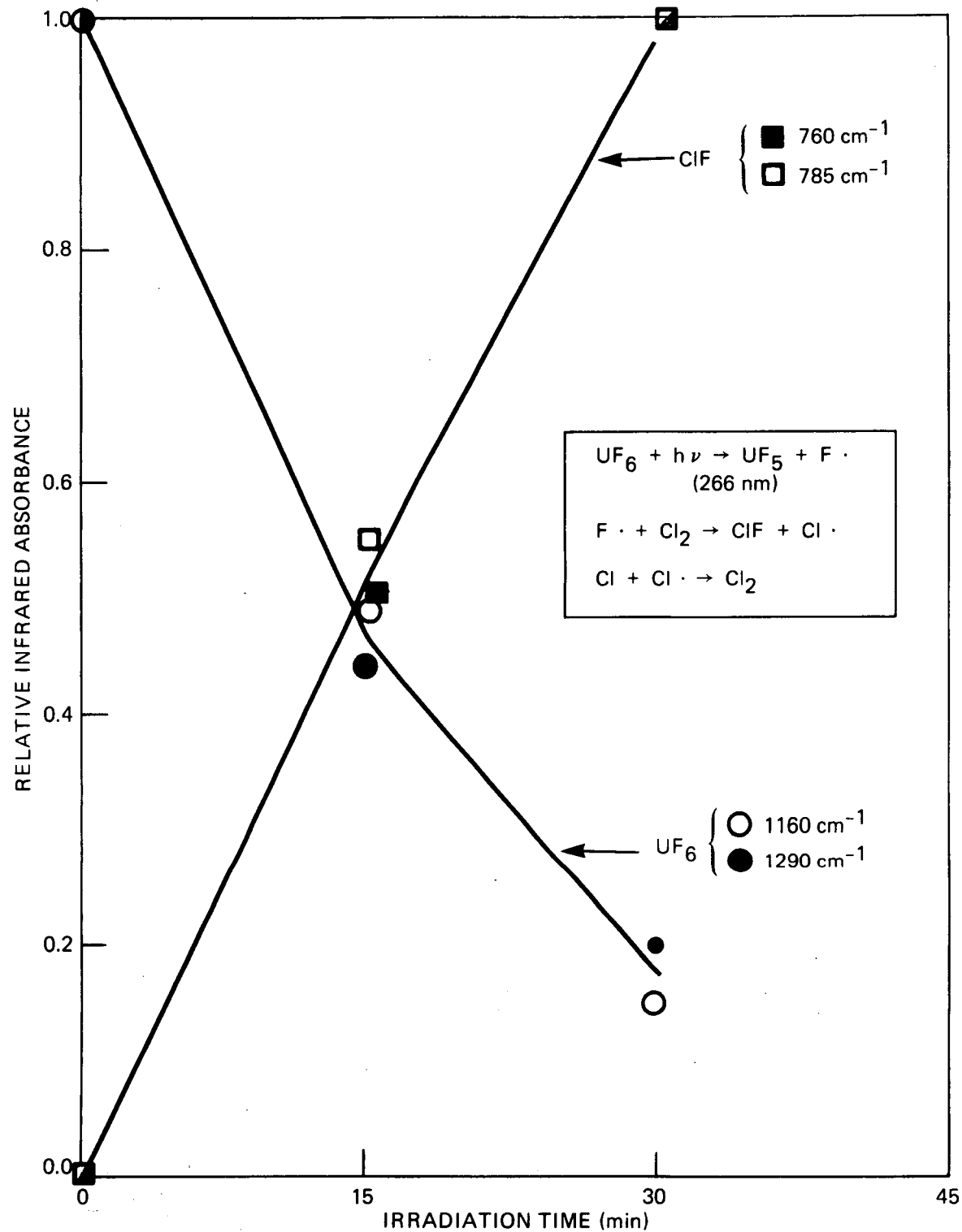
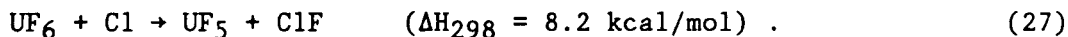


Fig. 8. Relative change in IR absorbance by UF<sub>6</sub> and ClF during photolysis of a mixture of UF<sub>6</sub> and Cl<sub>2</sub> at 266 nm.

stability of dilute ClF used as a calibration standard.) An apparent UV-photolysis quantum yield greater than unity suggests that atomic chlorine (produced by the photolysis of Cl<sub>2</sub> reagent) may react directly with UF<sub>6</sub>:

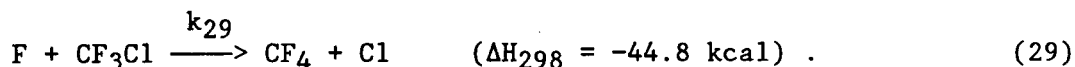


Reaction (27) is only slightly endothermic at room temperature and may become energetically favorable at elevated temperature or when UF<sub>6</sub> is in a vibrationally excited state.

We attempted a few semiquantitative UF<sub>6</sub> thermal dissociation studies using Cl<sub>2</sub> reagent. Detectable amounts of ClF were generated in the LPHP experiment, using SiF<sub>4</sub> as the sensitizer. Yields of ClF appeared to be higher than expected and somewhat erratic. We felt that this may be due to the ready thermolysis of Cl<sub>2</sub> reagent [see Eq. (28)] during the experiment (see Table 2: both Cl<sub>2</sub> and ClF bond dissociation energies are nearly 10 kcal more labile than the F-UF<sub>5</sub> bond), and the subsequent reaction [see Eq. (27)] between the atomic chlorine radical and UF<sub>6</sub>.

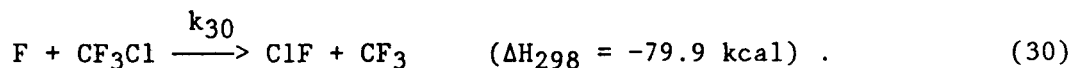


We sought a trapping agent which would be effective at elevated temperature and which itself would be thermally stable. One attractive candidate is CF<sub>3</sub>Cl (Freon 13). Homann and MacLean (1971) propose an energetically favorable fluorine atom substitution reaction in a sequence observed using a fluorine flame near 2000 K:

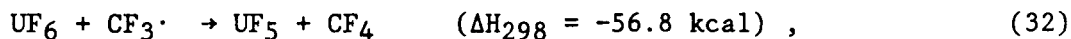


Both CF<sub>3</sub>Cl and CF<sub>4</sub> are thermally stable (see Table 2). The indicator species, CF<sub>4</sub>, is easily detected by IR spectroscopy, with a sensitivity ~400 times that for IR detection of ClF product. Again, it is possible for Cl coproduct to subsequently react with UF<sub>6</sub> [see Eq. (27)], but this does not generate additional CF<sub>4</sub> indicator, and because only small fractional decompositions (<2%) of UF<sub>6</sub> are needed, this would not significantly alter the UF<sub>6</sub> concentration.

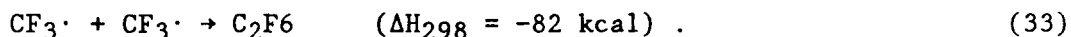
The reaction of F atoms with compounds of the series CF(x)Cl(4-x) results in abstraction of a Cl atom at room temperature and replacement of a Cl atom at flame temperatures (Jones and Skolnik, 1976). Foon (1972, 1975) proposed a different mechanism for the reaction between atomic fluorine and CF<sub>3</sub>Cl at lower temperatures:



For abstraction from  $\text{UF}_6$ , Eq. (31) becomes



which is energetically less favorable than  $\text{CF}_3\cdot$  radical combination:



Although Eq. (30) is energetically favorable, it may be slow kinetically. Zetzsch (1971) reacted atomic fluorine (generated from a microwave discharge) with several halogenated methanes (including  $\text{CF}_3\text{Cl}$ ), yielding an upper estimate of the rate constant at 300 K of  $1\text{E9 cm}^3/\text{mol-s}$ . Foon made indirect, relative rate measurements for a series of halogenated methanes with molecular fluorine and from rate ratios and thermodynamic theory, estimated the Arrhenius parameters for the rate constant for Eq. (30):

$$k_{30} = 6\text{E}13 \exp(-20.9 \text{ kcal mol}^{-1}/RT) \text{ cm}^3/\text{mol-s} \quad (34)$$

At 300 K, Eq. (34) yields  $k_{30} = 0.04 \text{ cm}^3/\text{mol-s}$  (vs the Zetzsch estimate of  $1\text{E9 cm}^3/\text{mol-s}$ ; see also Table 7). There were enough uncertainties in the derivation of Eq. (34) to question its usefulness for the prediction of absolute reaction rate, but it does suggest that there is an appreciable activation barrier to the reaction.

We attempted a room-temperature UV photolysis of  $\text{UF}_6$  in  $\text{CF}_3\text{Cl}$  diluent, with IR monitoring for both  $\text{CF}_4$  and  $\text{ClF}$  product. Almost no indicator species of either kind were formed; this may confirm that the room-temperature reaction between  $\text{CF}_3\text{Cl}$  and  $\text{F}$  is indeed slow, relative to  $\text{UF}_5 + \text{F}$  recombination. Alternately, the poor UV-photolysis quantum yield may have been due to the effectiveness of halomethanes as collision partners in quenching photolytically excited  $\text{UF}_6$  prior to dissociation [Wampler (1979)].

Silicon tetrafluoride-sensitized laser pyrolysis of dilute  $\text{UF}_6$  (at  $\sim 1350 \text{ K}$ ) in the presence of  $\text{CF}_3\text{Cl}$  produced very different results, as indicated in the IR scans illustrated in Fig. 9. During pyrolysis,  $\text{UF}_6$  absorbance decreases, with a concurrent increase in  $\text{CF}_4$  absorbance;



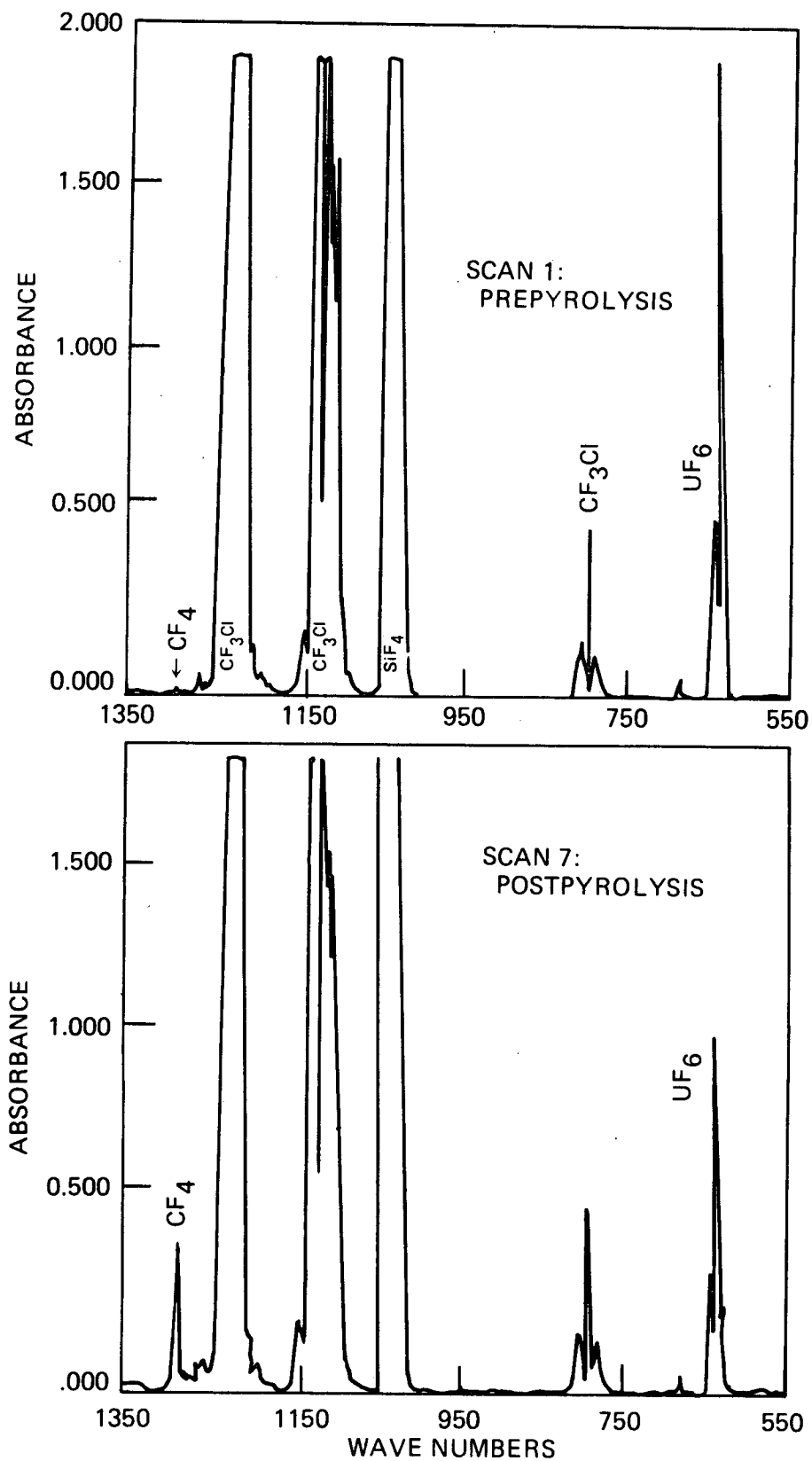


Fig. 9. FTIR scans of a mixture of gases with the initial room-temperature composition:  $\text{UF}_6$  (1 torr),  $\text{N}_2$  (4 torr),  $\text{CF}_3\text{Cl}$  (10 torr), and  $\text{SiF}_4$  (15 torr). Scan 1 was taken before pulsed laser excitation, and scan 7 was taken after 120 laser pulses.

there is no evidence for  $C_2F_6$  [see Eq. (33)], which absorbs very strongly in the monitored spectral region [Nielson et al. (1948)]; this is evidence that the F-atom substitution mechanism [see Eq. (29)] prevails at relatively high temperatures over the abstraction mechanism [see Eqs. (30-31) and (33)]. Additionally, the production of  $CF_4$  was almost stoichiometric with respect to net  $UF_6$  disappearance during pyrolysis (product yield ratio,  $0.9 \pm 0.2$ ), indicating that for each mole of  $UF_6$  which decomposes unimolecularly and which is not reformed by  $UF_5 + F$  recombination, one mole of  $CF_4$  indicator is produced.

#### LPHP OF $UF_6$ WITH $SiF_4$ SENSITIZER AND $CF_3Cl$ REAGENT

Quantitative measurements were performed with the cell geometry shown in Fig. 3B using the gas compositions given in Table 3. Ethyl chloride was used as the thermometer gas in an external standard; approximate temperature estimates for individual data points were derived using Eq. (11), assuming an effective reaction time of 20  $\mu s$  and using the Holbrook and Marsh values (see Table 5) for As and Es at the high-pressure limit. [Note: varying the estimate of effective reaction time will correspondingly alter the estimate of effective temperature for individual data but will not significantly affect the values of the derived Arrhenius parameters; see McMillen et al. (1982).] The derived rate-temperature data parameters are given in Table 8, and the Arrhenius parameters derived from these data are summarized in Table 9.

Data were obtained over a range of total gas densities, using  $CF_3Cl$  as the diluent gas. The reason for this is twofold: first, an increase in atomic fluorine trapping reagent helps to ensure that, by mass-action, the formation of  $CF_4$  product significantly outcompetes  $UF_5 + F$  recombination, and second, to ensure that the thermometer gas is sufficiently near its high-pressure-limiting rate to yield accurate estimates of the high-pressure-limiting rate for the reactant gas [Dai et al. (1982)].

A preliminary chemical dynamic modeling of our experiment at the lowest  $CF_3Cl$  and total densities used (see Table 2, data set A) was performed by J. L. Lyman (personal communication, March 1985); it was suggested that the  $CF_4$  yield could represent as little as 65% of the total unimolecular dissociation under these conditions. (Note: these estimates were based on use of Eq. (34) for the rate of  $CF_3Cl + F$  reaction, and assumed an irreversible gas expansion model for the laser-induced shock wave; a reversible expansion model, with or without more rapid indicator reaction kinetics, would result in a higher estimate of  $CF_4$  yield relative to total  $UF_6$  unimolecular dissociation.) A significant contribution by  $UF_5 + F$  recombination in data set A (see Table 2) would have the effect of producing a lower estimate for log A (see Table 9).

In data sets C and D (see Table 8), the total concentration of  $CF_3Cl$  reagent is  $\sim 10$  times that used in data set A, and the  $CF_4$  yields in

Table 8. Laser-powered homogeneous pyrolysis of  $\text{UF}_6$  - data summary

Data ID	Total gas density (mol/cm <sup>3</sup> )	$\text{UF}_6$ mol fraction	Derived kinetic parameters	
			T(K) <sup>a</sup>	$k_u$ (s <sup>-1</sup> )
A(1-3)	1.67E-6	0.033	1346(±8)	(2.35 ± 0.35) E3
A-4	1.67E-6	0.158	1324	882
A-5	1.61E-6	0.167	1315	1450
A-6	1.61E-6	0.167	1288	940
A-7	1.64E-6	0.164	1223	108
A-8	1.61E-6	0.167	1218	258
A-9	1.61E-6	0.167	1190	74.2
A-10	1.61E-6	0.167	1150	18.8
A-11	1.64E-6	0.148	1114	23.4
A-12	1.61E-6	0.167	1105	7.6
B-1	4.04E-6	0.133	1211	594
B-2	4.14E-6	0.130	1199	501
B-3	4.09E-6	0.132	1117	58.5
B-4	4.11E-6	0.131	1107	48.4
C-1	7.64E-6	0.070	1163	426
C-2	6.62E-6	0.081	1160	424
C-3	6.73E-6	0.080	1098	84
C-4	6.73E-6	0.080	1051	17.4
D-1	8.07E-6	0.067	1098	56.4
D-2	8.07E-6	0.067	1096	64.9

<sup>a</sup>See Eq. (11); effective reaction time assumed to be 2E-5 s.

these experiments would be expected to be equivalent to the total  $\text{UF}_6$  unimolecular dissociation. Pooling data from data sets C and D (total gas densities 6.7E-6 to 8.0E-6 mol/cm; see Table 8) yields the following estimate by our technique for the unimolecular decay rate for  $\text{UF}_6$  near the high-pressure limit:

$$\text{Log } k_u \sim \text{Log } k_{\infty} = (16.04 \pm 0.9) - (71.3 \pm 4.4) \text{ kcal mol}^{-1}/2.3 \text{ RT} , \quad (35)$$

which is nearly identical to the high-pressure limit estimated from the Schug and Wagner data (see Table 10).

In summary, the LPHP and the shock tube techniques agree within experimental error near the high-pressure limit. However, due to the relative rate procedure used in the LPHP technique, it does not necessarily give a true representation of the pressure-dependent rate falloff

for the reactant gas; rather, the Arrhenius parameters estimated using Eq. (11) tend to be closer to the high-pressure limit than to the absolute rate constants at a given gas density.

Table 9. Laser-powered homogeneous pyrolysis of  $\text{UF}_6$  - derived Arrhenius parameters

Data set <sup>a</sup>	Total gas density (mol/cm <sup>3</sup> )	Log $k_u = \text{Log } A - eA/2.3RT$	
		Log A	Ea (kcal/mol)
A	1.6E-6	14.15 ±0.7	66.6 ±0.9
B	4.0E-6	14.76 ±0.4	66.3 ±1.9
C	6.7E-6	15.70 ±0.5	69.4 ±2.3
C + D	(6.7-8.0) E-6	16.04 ±0.9	71.3 ±4.4

<sup>a</sup>See Table 2.

Table 10. Estimates of the high-pressure limiting Arrhenius parameters for  $\text{UF}_6$  thermal dissociation

Experimental data set <sup>a</sup>	Eq. no.	Extrapolation procedure	Log $k_{\infty} = \text{Log } A - Ea/2.3RT$		
			Log A	Ea (kcal/mol)	Log K (1200 K)
S and W	(8)	Kassel theory	16.52 (±0.7)	70.3 (±4)	3.718
	(9)	Empirical	16.04 (±0.3)	67.8 (±2)	3.700
	(10)	RRKM	16.42	69.7	3.727
LPHP	(35)	Relative rate	16.04 (±0.9)	71.3 (±4)	3.056

<sup>a</sup>S and W = data from Schug and Wagner (1977). LPHP = data from this work.



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APPENDIX

APPLICATION OF THE RICE-RAMSPERGER-KASSEL THEORY





The experimental techniques used in the main body of this document provide information primarily for the high-pressure limiting unimolecular decomposition rate for  $\text{UF}_6$ . In engineering applications, there is often a need for expedient estimates of reaction rates beyond the bounds of available experimental data, e.g., to differing regimes of temperature and pressure.

Unimolecular reaction rate theories have been studied for many decades. Techniques for estimating the fundamental behavior of unimolecular rates as a function of temperature, pressure, and intermolecular and intramolecular energy transfer characteristics are available at many levels of sophistication and ease of application. To our knowledge, all theoretical treatments, to the extent that they are applied to experimental data, use some degree of adjustable parameterization to best match the data [see Robinson and Holbrook (1972)]. The problem is thus to select a technique which provides a degree of theoretical validity and accuracy commensurate with the available data and the requirements for the application at hand.

For many applications, the Rice-Ramsperger-Kassel (RRK) theory provides a reasonable compromise. The classical formulation, as given in Mulcahy (1973), is

$$\frac{k_u}{(k_u)_\infty} = \frac{1}{(s-1)!} \int_0^\infty \frac{x^{s-1} \exp(-x) dx}{1 + A\{x/(x + E^*/RT)\}^{s-1}/\lambda Z[M]}, \quad (\text{A-1})$$

where

$x = (E - E^*)/RT$  is the integration variable,

$E$  = total internal energy,

$E^*$  = critical internal energy, approximately equal to  $E_a$ , the Arrhenius activation energy at the high-pressure limit,

$A$  = Arrhenius pre-exponential factor at the high-pressure limit,

$Z$  = collision frequency for the reactant molecule,

$[M]$  = total gas concentration (e.g., molec/cm<sup>3</sup>),

$\lambda$  = "collision-effectiveness parameter,"

$S$  = number of "effective oscillators."

The classical RRK formulation shown in Eq. (A-1) is an adaptation of an equivalent quantum mechanical formulation. Use of the classical

version becomes invalid when the total internal vibrational energy becomes smaller than, or comparable in magnitude to, the energy of individual vibrational quanta. Vibrational frequencies for selected molecules are given in Table A-1. Consider the example of  $\text{UF}_6$  (a seven-atom molecule) at a temperature near 1000 K: the classical average internal vibrational energy would thus be  $(3N-6)RT$  or  $\sim 30,000$  cal/mol as compared with vibrational quanta averaging  $286 \text{ cm}^{-1}$  or  $\sim 818$  cal/mol. For this example, the conditions for use of the classical formulation are well satisfied; however, this may not always be the case for systems such as hydrocarbons [higher mean vibrational frequencies (see Table A-1)] at significantly lower temperatures.

A computer program was written to evaluate this version of the classical RRK formula; a listing of the program, RRK.BAS, is given in Fig. A-1. The main function of the program is to numerically integrate the RRK integral described previously and to calculate the ratio of the unimolecular rate constant to the high-pressure limiting rate constant at otherwise equivalent conditions.

For our purposes, speed and ease of implementation are more important than high precision, and, therefore, numerical integration is achieved to adequate accuracy using the trapezoidal rule. The integration interval is taken as  $(dx = 0.1)$ ; in numerous test cases, the integrand result converged for all values of  $dx$  below 0.5. The RRK integral, as written in Eq. (A-1), is for a semi-infinite range. The integrand, however, diminishes for large values of  $x$ , so that in practice, the integration may be terminated at finite  $(x)$  without loss of precision. In the program, the integration is terminated when two criteria are met: (1) the integrand is falling in value, and (2) the value of the current increment of the integral is less than one part in  $10^6$  of the cumulative integral. The choices of  $(dx)$  and the convergence criteria are encoded into the program but are easily changed.

In the evaluation of factorials in the integral, Stirling's approximation is used; namely,

$$S! \sim \sqrt{2\pi S} (S/e)^S . \quad (\text{A-2})$$

While this approximation is not terribly accurate for small values of  $S$ , it has the advantage of easily permitting computation of factorials for fractional numbers and is sufficiently precise for values of  $S$  considered in this study.

The values for the RRK integral computed using the program listed in Fig. A-1 compare well with the standard values computed and compiled by Emanuel (1969, 1972); note that use of the standard tables is slow and typically requires interpolation for use with real systems. [Some notes on the use of Fig. A-1: (1) RRK.BAS is written for the IBM PC in BASICA; when compiled using the 8087 coprocessor, it runs in  $\sim 1$  s, whereas the

Table A-1. Some physical parameters for selected molecules

Molecule	Molecular weight	Collision diameter (Å) <sup>a</sup>	Fundamental vibrational frequencies (cm <sup>-1</sup> ) <sup>b</sup>
Argon	39.95	3.54	
cyclo-C <sub>3</sub> H <sub>6</sub>	42.1	4.81	$\nu_1 = 3038$ , $\nu_2 = 1479$ , $\nu_3 = 1188$ , $\nu_4 = 1126$ , $\nu_5 = 1070$ , $\nu_6 = 3103$ , $\nu_7(2) = 854$ , $\nu_8(2) = 3025$ , $\nu_9(2) = 1438$ , $\nu_{10}(2) = 1029$ , $\nu_{11}(2) = 866$ , $\nu_{12}(2) = 3082$ , $\nu_{13}(2) = 1188$ , $\nu_{14}(2) = 739$ (geometric mean: 1432)
C <sub>2</sub> H <sub>5</sub> Cl	64.5	4.90	$\nu_1 = 2967$ , $\nu_2 = 2946$ , $\nu_3 = 2881$ , $\nu_4 = 1463$ , $\nu_5 = 1448$ , $\nu_6 = 1385$ , $\nu_7 = 1289$ , $\nu_8 = 1081$ , $\nu_9 = 974$ , $\nu_{10} = 677$ , $\nu_{11} = 336$ , $\nu_{12} = 3014$ , $\nu_{13} = 2986$ , $\nu_{14} = 1448$ , $\nu_{15} = 1251$ , $\nu_{16} = 974$ , $\nu_{17} = 786$ , $\nu_{18} = 251$ (geometric mean: 1268)
SiF <sub>4</sub>	104.1	4.88	$\nu_1 = 800$ , $\nu_2(2) = 268$ , $\nu_3(3) = 1032$ , $\nu_4(3) = 389$ (geometric mean: 537)
CF <sub>3</sub> Cl	104.5	4.86	$\nu_1 = 1106$ , $\nu_2 = 782$ , $\nu_3 = 474$ , $\nu_4(2) = 1217$ , $\nu_5(2) = 560$ , $\nu_6(2) = 350$ (geometric mean: 659)
SF <sub>6</sub>	146.1	5.13	$\nu_1 = 774$ , $\nu_2(2) = 642$ , $\nu_3(3) = 948$ , $\nu_4(3) = 616$ , $\nu_5(3) = 525$ , $\nu_6(3) = 347$ (geometric mean: 592)
UF <sub>6</sub>	352.0	5.97	$\nu_1 = 667$ , $\nu_2(2) = 533$ , $\nu_3(3) = 626$ , $\nu_4(3) = 186$ , $\nu_5(3) = 202$ , $\nu_6(3) = 142$ (geometric mean: 286)

<sup>a</sup>Collision diameters (in Angstra) estimated from Lennard-Jones parameters.

<sup>b</sup>Parenthetic terms designate degeneracies.

```

10 ' RRK7      Numerical Integration of RRK integral from Mulcahey p 200
20 '          LDT 6 Jun 85
30 GOSUB 410:GOSUB 200
40 DEF FNCTORIAL(X)=SQR(6.2838531**X)*(X/2.71828183#)^X
50 DEF FNI(Y,F,T,C,EA)=Y^F*EXP(-Y)/(1+C*(Y/(Y+EA/T))^F)
60 DIM CUM(15)
70 GOSUB 330
80 X=0:I=0:CUM(S)=0
90 CUM(S)=FNI(DX,S-1,T,C,EA)/4*DX      ' (f(0)+f(dx))/2)
100 I=I+1:X=X+DX
110 DC=FNI(X,S-1,T,C,EA)/FNCTORIAL(S-1)*DX
120 CUM(S)=CUM(S)+DC
130 IF I<20 OR DC*1000000! > CUM(S) THEN GOTO 100
140 PRINT
150 KPKI=CUM(S):PRINT USING
    "At    T = ##### K      P = ##### Torr    s = ###.## ";T,P,S
160 PRINT USING
    "Integral converges at #### iterations to K/
    Kinf = #.#####    log = ##.###";I,KPKI,LOG(KPKI)/2.302585
170 KU=KPKI*AO*EXP(-EA/T):PRINT USING
    "          Ku      =##.##^####    log = ##.###";
    KU,LOG(KU)/2.302585
180 PRINT:PRINT:GOTO 70
190 STOP
200 INPUT "Ea ( cal/mole)      ";EA:EA=EA/1.987      ' K
210 INPUT "Ao (1/sec)        ";AO
220 LAMBDA=1      "strong collision"
230      'c==Ao/(Lambda*Z*[A])
240 DX=.1      'integration interval (.5 is max
                value giving limiting value)

250 INPUT "Reactant: Mass (amu) ";M1
260 INPUT "Reactant: Dia. (Ang) ";R1
270 INPUT "Self-medium (Y/N)   ";Q$:Q$=LEFT$(Q$,1):
    IF Q$="y" OR Q$="Y" THEN M2=M1:R2=R1:F=.5:GOTO 310
280 F=1      ' statistical; .5 in self-media
290 INPUT "Diluent : Mass (amu) ";M2
300 INPUT "Diluent : Dia. (Ang) ";R2
310 MU=M1*M2/(M1+M2):SIGMA=1E-08*(R1+R2)/2
320 RETURN
330 INPUT "T(K)              ";T
340 INPUT "Total Pressure (Torr)";P
350 INPUT "RRK S factor      ";S
360 V=SQR(8*8.314E+07*T/3.14159/MU)      ' cm/sec - collision velocity
370 Z=3.14159*SIGMA*SIGMA*V*F      ' cc/molec-sec
380 N=P/760/82.05/T*6.02E+23      ' molec/cc
390 C=AO/Z/N/LAMBDA      ' numeric constant
400 RETURN
410 CLS:PRINT"RRK Unimolecular Kinetics - Numerical Integration of
420      PRINT
    "          RRK integral from Mulcahy p 201"
430 PRINT
440 RETURN

```

Fig. A-1. Listing of RRK.BAS.

interpreted version (i.e., as run directly from BASICA) requires ~30 s; (2) several lines exceed the paper width in Fig. A-1 and are continued on the next line (e.g., line 150); and (3) the collision-efficiency parameter ( $\lambda$ ) is set equal to 1 in line 220 but can easily be altered or treated as an input variable.]

A sample of the CRT screen output from execution of RRK.BAS (see Fig. A-1) is given in Fig. A-2. In this example, the input high-pressure Arrhenius parameters for  $\text{UF}_6$  were taken from Eq. (8) of the main text, and the values for reactant mass and diameter were selected from Table A-1.

### PARAMETERIZATION OF THE RRK MODEL

The RRK theory provides a (relatively) simple technique for estimating the pressure-dependent fall-off in unimolecular reaction rates. Given the high-pressure Arrhenius rate parameters and selected fundamental physical properties of the molecules comprising the system, RRK can be used to fit experimental data with 0, 1, or 2 adjustable parameters ( $S_{\text{eff}}$  and  $\lambda$ ).

The Arrhenius parameters for the high-pressure limiting rate are generally obtained from the experimental data or derived via techniques such as described in the main text of this report. The collision frequency,  $Z$ , derived from the gas kinetic hard-sphere collision rate, is a function of gas component molecular weight, collision diameter, and temperature; some parameters used in computing  $Z$  for selected collision partners are summarized in Table A-1. The total gas composition and concentration affects the rates for activation and deactivation of reactant [see Eq. (4) of the main text].

The term  $\lambda$  is an accommodation coefficient equal to the fraction of collisions of the activated species which result in deactivation; generally, for lack of other information,  $\lambda$  is assumed to be unity in self-medium ("strong collision" approximation). Following this convention,  $\lambda$  thus becomes a measure of "relative collision efficiency," analogous to the  $\beta_c$  term defined by Tardy and Rabinovitch (1968) and can assume values ranging from near zero (for inefficient deactivation--as in V-T energy transfer by "weak" collisions with inert gases) to values near unity (for "strong" collisions with polyatomic molecules, with many vibrational modes, where efficient, near-resonant V-V energy transfer is possible). In practice, one method of obtaining information on the rates of energy transfer between molecules is to study the efficiency of chemically inert gases in maintaining the rate of unimolecular reactions near the low-pressure rate limiting domain [Holbrook (1955), Cottrell and McCoubey (1961)]. In general, it appears that efficiency of energy transfer increases with increasing complexity of the collision partner but that a maximum efficiency (comparable to self-medium) is soon reached; in contrast, the smaller and lighter molecules are very inefficient, in spite of their known efficiency as collision partners for V-T energy transfer.

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RRK Unimolecular Kinetics - Numerical Integration of  
RRK integral from Mulcahy p 201

Ea (cal/mole) ? 70300  
Ao (1/sec) ? 3.3e16  
Reactant: Mass (amu) ? 352  
Reactant: Dia. (Ang) ? 6.0  
Self-medium (Y/N) ? y  
T(K) ? 1000  
Total Pressure (Torr)? 50  
RRK S factor ? 12

At T = 1000 K P = 50 Torr s = 12.0  
Integral converges at 212 iterations to K/Kinf = 0.09234 log = -1.035  
Ku = 1.31E+00 log = 0.119

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Fig. A-2. Sample screen output of RRK.BAS.

From this, Lambert (1977) infers that V-T energy transfer does not play an important role in unimolecular reactions.

When the "strong collision" assumption is invoked for unimolecular reactions in self-medium or in a polyatomic bath gas (i.e.,  $\lambda = 1$ ), the primary remaining adjustable parameter in the RRK model is  $S_{\text{eff}}$ , the number of "effective oscillators" in the reactant molecule, or loosely the number of internal vibrational modes which participate in distributing internal molecular energy. It can have values ranging up to the total  $3N-6$  vibrational degrees of freedom for the (nonlinear)  $N$ -atom polyatomic reactant.  $S_{\text{eff}}$  can be treated as an adjustable parameter to provide best agreement with the available experimental data, and frequently it is thus found to be about one-half of the total number of oscillators [Laidler (1965)] or a somewhat larger fraction for highly symmetric molecules. From quantum and statistical mechanical considerations, one might expect  $S_{\text{eff}}$  to have some dependence on temperature and internal vibrational frequency patterns. Several investigators have proposed formulae to derive  $S_{\text{eff}}$  based on molecular properties.

Benson and co-workers have advocated the use of the molar vibrational heat capacity ( $C_{\text{vib}}$ ) to estimate  $S_{\text{eff}}$  [see Golden et al. (1971)]:

$$S_{\text{eff}} = \frac{C_{\text{vib}}}{R} . \quad (\text{A-3})$$

$C_{\text{vib}}$  may be estimated from tabulated values of  $C_p$ , the total heat capacity at constant pressure, by assuming that each translational and rotational degree of freedom contributes  $1/2 R$  to the total (i.e.,  $C_{\text{vib}} = C_p - 4R$ ). Alternately, the molecular vibrational modes can be approximated as harmonic oscillators and  $C_{\text{vib}}$  computed using the statistical mechanic formula:

$$C_{\text{vib}} = \sum_{i=1}^S \frac{R x_i^2 \exp(-x_i)}{[1 - \exp(-x_i)]^2} , \quad (\text{A-4})$$

where  $x_i = h\nu_i/RT$ ,  $\nu_i$  are the fundamental vibrational frequencies of the molecule, and the summation is taken over all of the  $(3N-6)$  normal harmonic oscillators (degenerate modes contribute identical terms to the summation). When  $\nu_i$  are in units of  $\text{cm}^{-1}$  (see Table A-1),  $x_i = 1.4388 \nu_i/T$ .

Use of the empirical rule given in Eq. (A-3) with classical RRK theory has been demonstrated [Golden et al. (1971) and Skinner and Rabinovitch (1972)] to predict approximately correct unimolecular fall-off curves for a wide variety of thermal reactions, provided  $k_{\infty}$  is greater than about  $10^{-4} \text{ s}^{-1}$ .



An alternative formulation, used by Troe and co-workers [Troe and Wagner (1967), Glanzer and Troe (1972), Troe (1975)], is to estimate  $S_{\text{eff}}$  from the analogous statistical mechanical approximation for the (harmonic oscillator) vibrational internal energy ( $U_{\text{vib}}$ ):

$$S_{\text{eff}} = \frac{E_{\text{vib}}}{RT} \sim \sum_{i=1}^S \frac{x_i}{\exp(x_i) - 1} \quad (\text{A-5})$$

Figure A-3 illustrates a simple program, written in BASICA for the IBM PC, to compute  $S_{\text{eff}}$  based on the formulae given in Eqs. (A-4) and (A-5); a sample CRT screen output from execution of this program (for  $\text{UF}_6$  at 1300 K) is given in Fig. A-4. Schug and Wagner (1977) report estimating  $S_{\text{eff}}$  for  $\text{UF}_6$  at 1300 K to be 12.4, indicating that they used Troe formulation [see Eq. (A-5)] to help parameterize their version of the Kassel theory model.

In Table A-2, we compare the predicted values for  $S_{\text{eff}}$  [as defined in Eqs. (A-4) and (A-5)] with the value obtained by empirical fit ( $S_{\text{eff}}$  as an adjustable parameter, using RRK.BAS) for several compounds for which reliable experimental data or "sophisticated" theoretical predictions are available. Several points are noteworthy. First, within the sometimes considerable scatter of the experimental data,  $S_{\text{eff}}$  as a fitted parameter for a given reactant does not appear to change significantly over a considerable temperature range. Secondly, the predicted values for  $S_{\text{eff}}$  using heat-capacity-based formulae [Eq. (A-4)] are generally close in magnitude to the values obtained by empirical fit to the data, especially for higher temperatures, as has been previously observed by other investigators [Golden et al. (1971), Skinner and Rabinovitch (1972), and Schranz et al. (1982)]. In contrast, values for  $S_{\text{eff}}$  predicted by the Troe formula [Eq. (A-5)] are consistently too low for accurate predictions of unimolecular rates using the classical RRK model as given in Fig. A-1.

In Table A-2, the pressure-dependent data for cyclopropane, as reported by Barnard et al. (1974) and Lewis et al. (1978), were obtained using the shock-tube technique, with argon or helium as the propellant and bath gas. The Barnard et al. data were "corrected" to the corresponding self-medium values using the relative collision efficiencies reported by Snowden et al. (see previous discussion on parameterization of  $\lambda$ ). Lewis et al. (1978) estimate a relative collision efficiency of  $\sim 0.04$  in argon diluent over the temperature range of  $\sim 1000$ – $1200$  K.

#### RRK PARAMETERIZATION FOR GAS-PHASE THERMAL DISSOCIATION OF $\text{UF}_6$

As indicated in the main text, the comparative rate data derived from the laser-powered homogeneous pyrolysis experiment, with effective

```

10  OPTION BASE 1
20  PRINT"Estimate Seff=Cvib/R (Benson) and Seff=Uvib/kt (Troe)"
30  INPUT"number of fundamental harmonic oscillators=";N
40  DIM V(100),G(100),CV(100),FT(100),UV(100)
50  FOR L=1 TO N
60  INPUT"v(cm-1)=";V(L)
70  INPUT"degeneracy="(L)
80  NEXT L
90  INPUT"T(K)=";T
100 SM=0
110 SSM=0
120 FOR L=1 TO N
130 FT(L)=1.4388*V(L)/T
140 NU=1.987*EXP(-FT(L))*FT(L)*FT(L)
150 ND=(1-EXP(-FT(L)))^2
160 CV(L)=NU/ND
170 SF=CV(L)*G(L)
180 SM=SF+SM
190 SSF=SM/1.987
200 UV(L)=FT(L)/(EXP(FT(L))-1)
210 GUV=UV(L)*G(L)
220 SSM=GUV+SSM
230 NEXT L
240 PRINT"Cvib =" ;SM
250 SSF=SM/1.987
260 PRINT"Cvib/R =" ;SSF
270 PRINT "Uvib/kT =" ;SSM
280 GOTO90

```

Fig. A-3. Listing of program to compute  $S_{eff}(T)$  using harmonic oscillator frequency.

```
RUN
Estimate Seff=Cvib/R (Benson) and Seff=Uvib/kt (Troe)
number of fundamental harmonic oscillators=? 6
v(cm-1)=? 667
degeneracy=? 1
v(cm-1)=? 534
degeneracy=? 2
v(cm-1)=? 626
degeneracy=? 3
v(cm-1)=? 186
degeneracy=? 3
v(cm-1)=? 200
degeneracy=? 3
v(cm-1)=? 143
degeneracy=? 3
T(K)=? 1300
Cvib = 29.31294
Cvib/R = 14.75236
Uvib/kT = 12.37343
T(K)=?
```

Fig. A-4. Sample screen output from execution of Fig. A-3  
example for  $\text{UF}_6$  reactant at 1300 K.

Table A-2. Estimates of RRK parameters for selected reactant molecules

Reactant	Diluent	Data source	T(K)	Empirical fit (RRK,BAS): <sup>a</sup>		$S \equiv C_{vib}/R^b$	$S_{eff} \equiv E_{vib}/RT^c$
				$\lambda$	$S_{eff}$		
Cyclopropane	Self	Yau and Pritchard (1978)	763.2	$\equiv 1$	$13.8 \pm 0.5$	11.3	4.84
Cyclopropane	Self	Chambers and Kistiakowski (1934)	777.2	$\equiv 1$	$13.7 \pm 0.3$	11.5	4.96
Cyclopropane	Self (Theory) <sup>d</sup>	Barnard et al. (1974)	800	$\equiv 1$	$\sim 13.9$	11.7	5.15
Cyclopropane	Self	Furue and Pacey	897	$\equiv 1$	$14.0 \pm 0.2$	12.8	5.92
Cyclopropane	Self (Theory) <sup>d</sup>	Barnard et al. (1974)	1100	$\equiv 1$	$\sim 14.6$	14.5	7.35
Cyclopropane	Argon	Lewis et al. (1981)	1100	$\sim 0.04$	$\sim 14.3$	14.5	7.35
Cyclopropane	Self (Theory) <sup>d</sup>	Barnard et al. (1974)	1400	$\equiv 1$	$\sim 15.2$	16.3	9.09
Ethyl Chloride	Self	Holbrook and Marsh (1967)	675	$\equiv 1$	$11.8 \pm 1.6$	9.06	4.17
Ethyl Chloride	Self	Heydtmann et al. (1975)	754.7	$\equiv 1$	$12.0 \pm 0.3$	9.92	4.73
Ethyl Chloride	Self	Holbrook and Marsh (1967)	767	$\equiv 1$	$11.7 \pm 0.6$	10.0	4.82
Ethyl Chloride	Self	Holbrook and Marsh (1967)	794	$\equiv 1$	$12.2 \pm 0.4$	10.3	5.00
Ethyl Chloride	Self	Blades et al. (1962)	922.5	$\equiv 1$	$\sim 12.4$	11.4	5.82
Uranium Hexafluoride	Argon	Schug and Wagner (1977)	1300	$0.05 \pm 0.01$	$\equiv 14.75$	14.75	12.4
			1300	$0.33 \pm 0.06$	$\equiv 12.4$	14.75	12.4

<sup>a</sup>Computed with use of the program listed in Fig. A-1, the physical parameters listed in Table A-1, and the following values for the high-pressure limiting rate ( $k_\infty$ ):

$$k_\infty(\text{C-C}_3\text{H}_6) = 1.48\text{E}15 \exp(-65,000/RT)$$

$$k_\infty(\text{C}_2\text{H}_5\text{Cl}) = 1.07\text{E}14 \exp(-58,430/RT)$$

$$k_\infty(\text{UF}_6) = 1.1\text{E}16 \exp(-67,760/RT)$$

<sup>b</sup>See Eq. (A-4).

<sup>c</sup>See Eq. (A-5).

<sup>d</sup>Data are for reactant in Ar diluent "corrected" to self-medium using various theoretical treatments.

reaction temperature and "dwell time" as confounded parameters, are not readily amenable to interpretation in terms of "true" pressure dependency. Currently, the most complete pressure-dependent rate data are those reported by Schug and Wagner (1977) for  $\text{UF}_6$  in argon diluent; data from their investigation are summarized in Table A-3. Schug and Wagner do not fully describe their selection of parameters but indicate that they used Kassel theory to extrapolate their data to the high-pressure limit. As suggested by Oref and Rabinovitch (1968), we have applied an empirical extrapolation procedure ( $1/k$  vs  $[M]^{-0.5}$ ) to data summarized in Table A-3 to obtain a "preferred" expression for the rate at the high-pressure limit (see Fig. A-5):

$$k_{\infty} = 1.1\text{E}16 \exp(-67,760/RT) \text{ s}^{-1} \quad (9)$$

Table A-3. Unimolecular reaction rate constants for  $\text{UF}_6$   
in argon medium  
[Data from Schug and Wagner (1977)]

[Ar], mol/cm <sup>3b</sup>	log $k_u^a$		
	T = 1200 K	T = 1300 K	T = 1400 K
3E-6	2.794 ± 0.152	3.529 ± 0.134	4.148 ± 0.149
8E-6	2.962 ± 0.154	3.728 ± 0.128	4.393 ± 0.128
1.5E-5	3.074 ± 0.128	3.816 ± 0.126	4.482 ± 0.122
4E-6	3.233 ± 0.120	4.043 ± 0.122	4.736 ± 0.122

<sup>a</sup>Log  $k_u$  as read from Fig. 5 of Schug and Wagner text. Data points were apparently computed from pressure-dependent Arrhenius plots, and "I-bars" are assumed to represent the  $\pm 1\sigma$  error band for estimated rate as derived from the Arrhenius plot.

<sup>b</sup> $P(\text{torr}) = 62361T(K)([M], \text{mol/cm}^3)$ .

For our purposes, Eq. (9) of the main text is "preferred" for use with the RRK.BAS computational program for the following reasons, as will be indicated in later portions of this discussion: (1) when used with the data from Table A-3 and  $S_{\text{eff}}$  defined by  $C_{\text{vib}}/R$ , a "reasonable" value is estimated for the  $\lambda$  parameter for polyatomic reactant in argon medium (i.e., a value consistent with similar investigations in such medium); and (2) when the "strong collision" assumption is made for  $\text{UF}_6$  in self-medium (i.e.,  $\lambda = 1$ ), the predicted rate fall-off (as  $k_u/k_{\infty}$ ) is in good agreement with sample calculations for  $\text{UF}_6$  in self-medium using

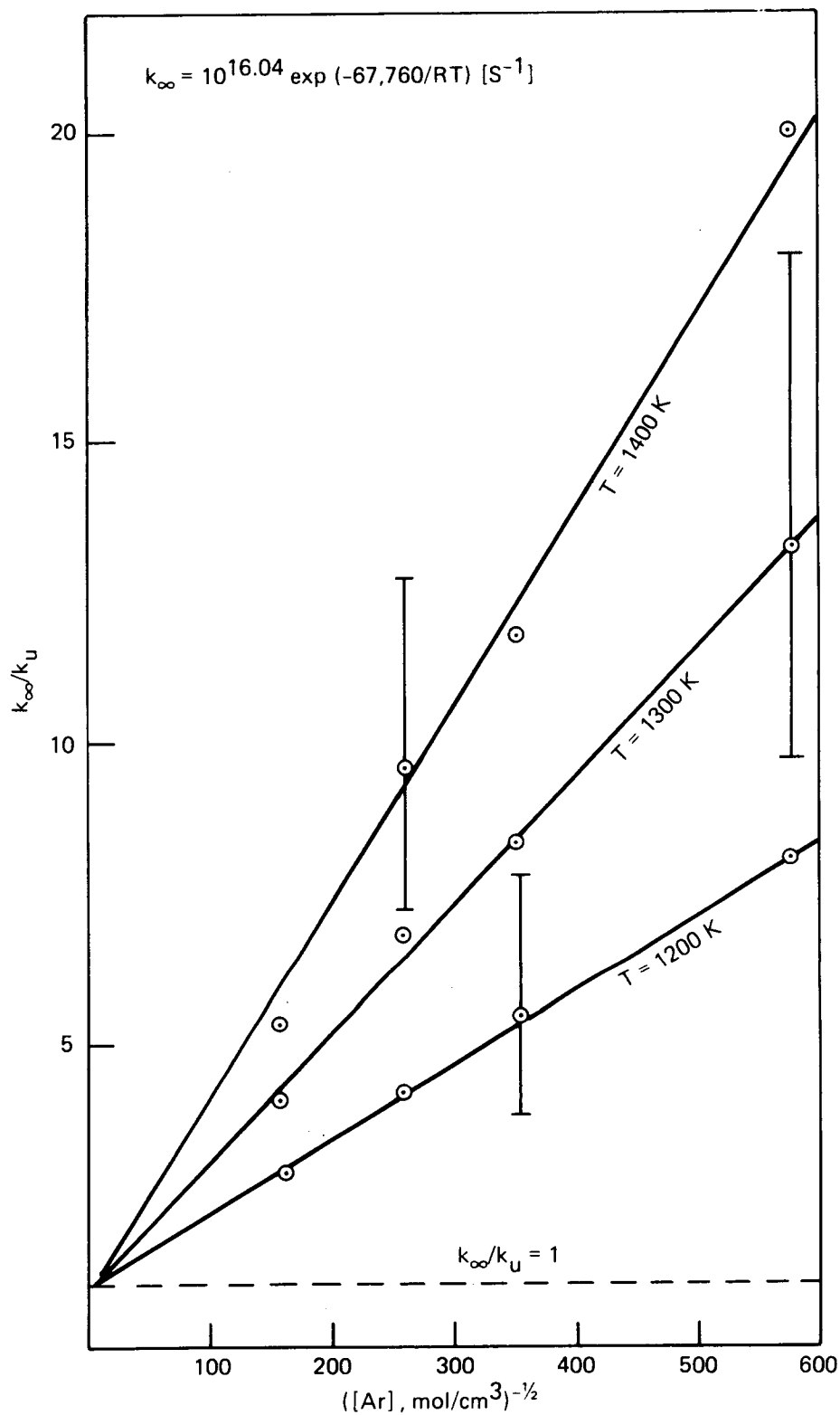


Fig. A-5. Data of Schug and Wagner (1977) plotted in an empirical manner to yield an estimate for the high-pressure limiting rate expression.

the more "sophisticated" Rice-Ramsperger-Kassel-Marcus (RRKM) quantum theory.

Since the data reported by Schug and Wagner are for rates measured in a bath comprised of a "weak" collision partner, modeling via classical RRK theory requires parameterization of both  $S_{\text{eff}}$  and  $\lambda$ , with additional "leverage" from the selected high-pressure Arrhenius parameters [see Furue and Pacey (1982)]. As shown in Figs. A-6 and A-7, essentially equivalent absolute rate predictions can be obtained using various permutations of parameters in the RRK model. From the data of Table A-2 and the previous discussion, we consider  $S_{\text{eff}} = C_{\text{vib}}/R$  [see Eq. (A-3)] to represent an acceptable estimate for this parameter. Defining  $S_{\text{eff}}$  in this manner and using  $\lambda$  as the adjusted parameter, estimates for  $\lambda$  at 1300 K range from  $\sim 0.09$  [using the high-pressure limiting Arrhenius parameters reported by Schug and Wagner [main text Eq. (8)] to  $\sim 0.05$  (using the Arrhenius parameters empirically computed [Eq. (9)]). Using  $S_{\text{eff}} = C_{\text{vib}}/R$  and Eq. (9) for the limiting high-pressure rate with all of the data listed in Table A-3, we obtain best root-mean-square fit for RRK  $\lambda = 0.045$ . These values for the  $\lambda$  term appear realistic compared with reported relative collision efficiencies for other comparable-sized polyatomic molecules in argon (e.g.,  $\beta_c \sim 0.04$ - $0.07$  for cyclopropane in argon). Similarly, Schug and Wagner (1977) estimate  $\beta_c = 0.03$  for  $\text{UF}_6$  in argon.

In contrast, estimates for  $\lambda$  using  $S_{\text{eff}} = U_{\text{vib}}/RT$  appear somewhat high (i.e.,  $\lambda = 0.2$ - $0.3$ ). [The latter estimates are somewhat more consistent with the relative vibrational relaxation time constants for  $\text{UF}_6$  in argon vs self-medium, as reported by Cravens et al. (1979); however, relatively efficient V-T relaxation does not, in general, indicate efficient deactivation in thermal unimolecular reactions.]

Lyman and Holland (unpublished results, May 1985) have applied RRKM quantum theory to  $\text{UF}_6$  thermal dissociation, parameterized to the Schug and Wagner data. We have used sample calculations for  $\text{UF}_6$  in self-medium by the more "sophisticated" (and computationally rigorous) RRKM theory to aid in the parameterization of the "simplified" RRK treatment--subject, of course, to the assumptions employed in the RRKM formulation regarding details of potential surfaces and intermolecular energy transfer processes [a similar parameterization procedure for the "simplified" theory, based on RRKM predictions, is advocated in Troe (1979)]. Agreement between classical RRK predictions (with  $S_{\text{eff}} \equiv C_{\text{vib}}/R$ ) and RRKM theory is expected to be close for  $\text{UF}_6$ , provided the temperature is greater than about 740 K [i.e.,  $k_{\infty} > 1\text{E-}4$ ; see Golden et al. (1971)]. This is confirmed in Fig. A-8, in which the RRK predictions for  $\text{UF}_6$  in self-medium are based on the "strong-collision" assumption (i.e.,  $\lambda = 1$ ) and the input parameters listed in Table A-4. These same parameters (with  $\lambda \sim 0.05$ ) also adequately reproduce the original Schug and Wagner data for  $\text{UF}_6$  in argon diluent, as shown in Fig. A-7.

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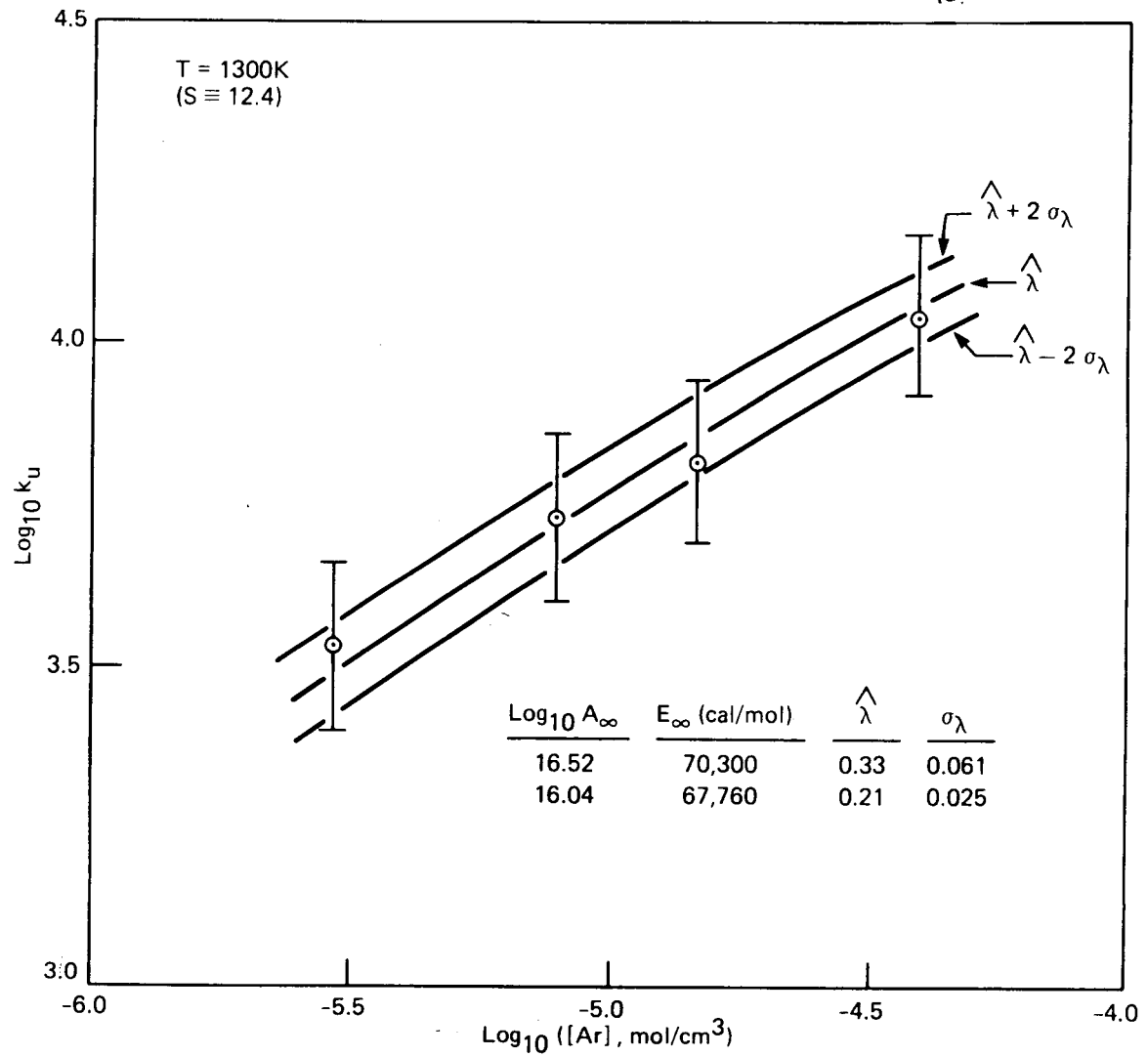


Fig. A-6. Data of Schug and Wagner (1977): RRK predictions using  $S_{\text{eff}} = U_{\text{vib}}/RT$ , with  $\lambda$  as the adjusted parameter.



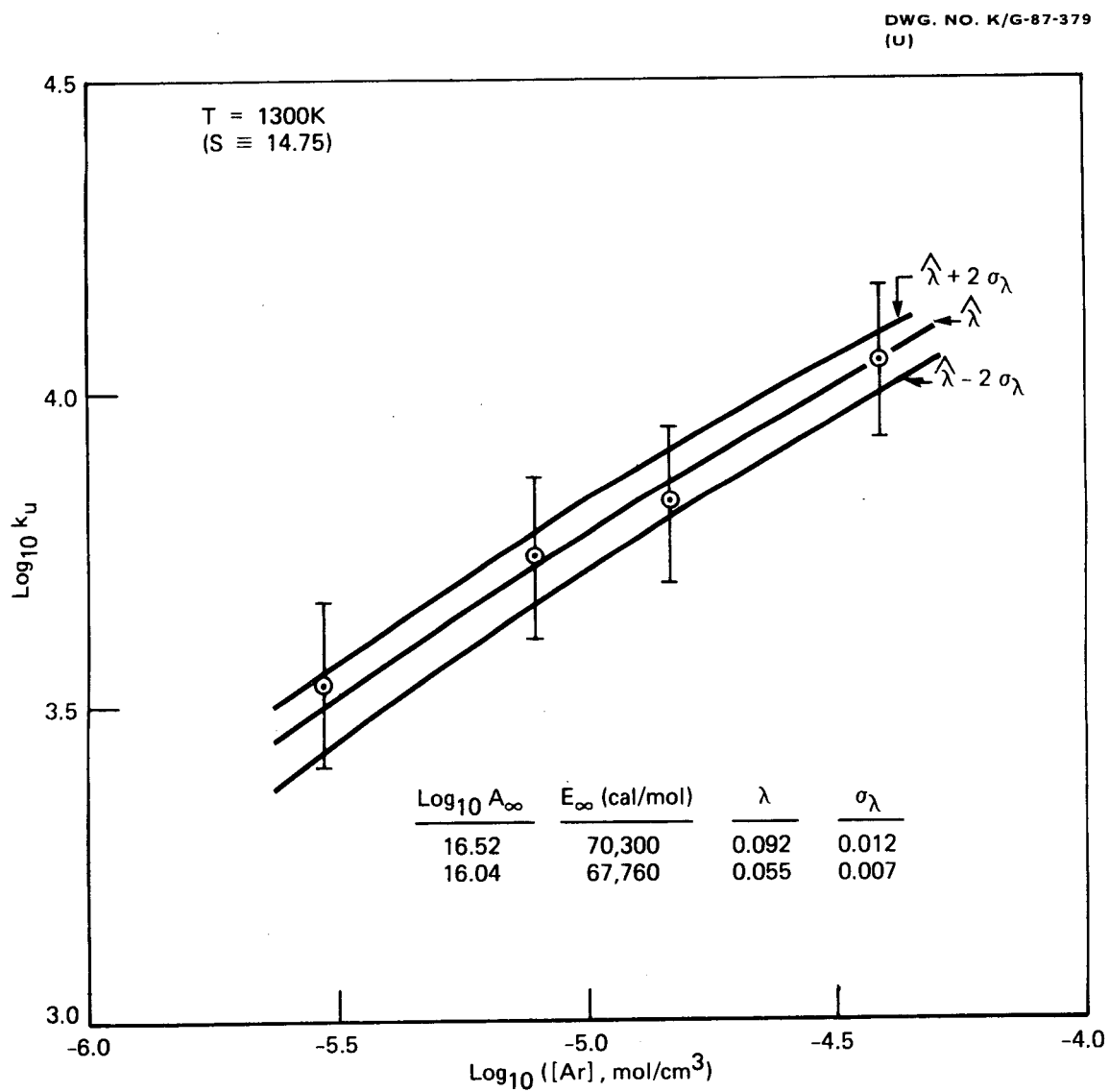


Fig. A-7. Data of Schug and Wagner (1977): RRK Predictions using  $S_{\text{eff}} = C_{\text{vib}}/R$ , with  $\lambda$  as the adjusted parameter.

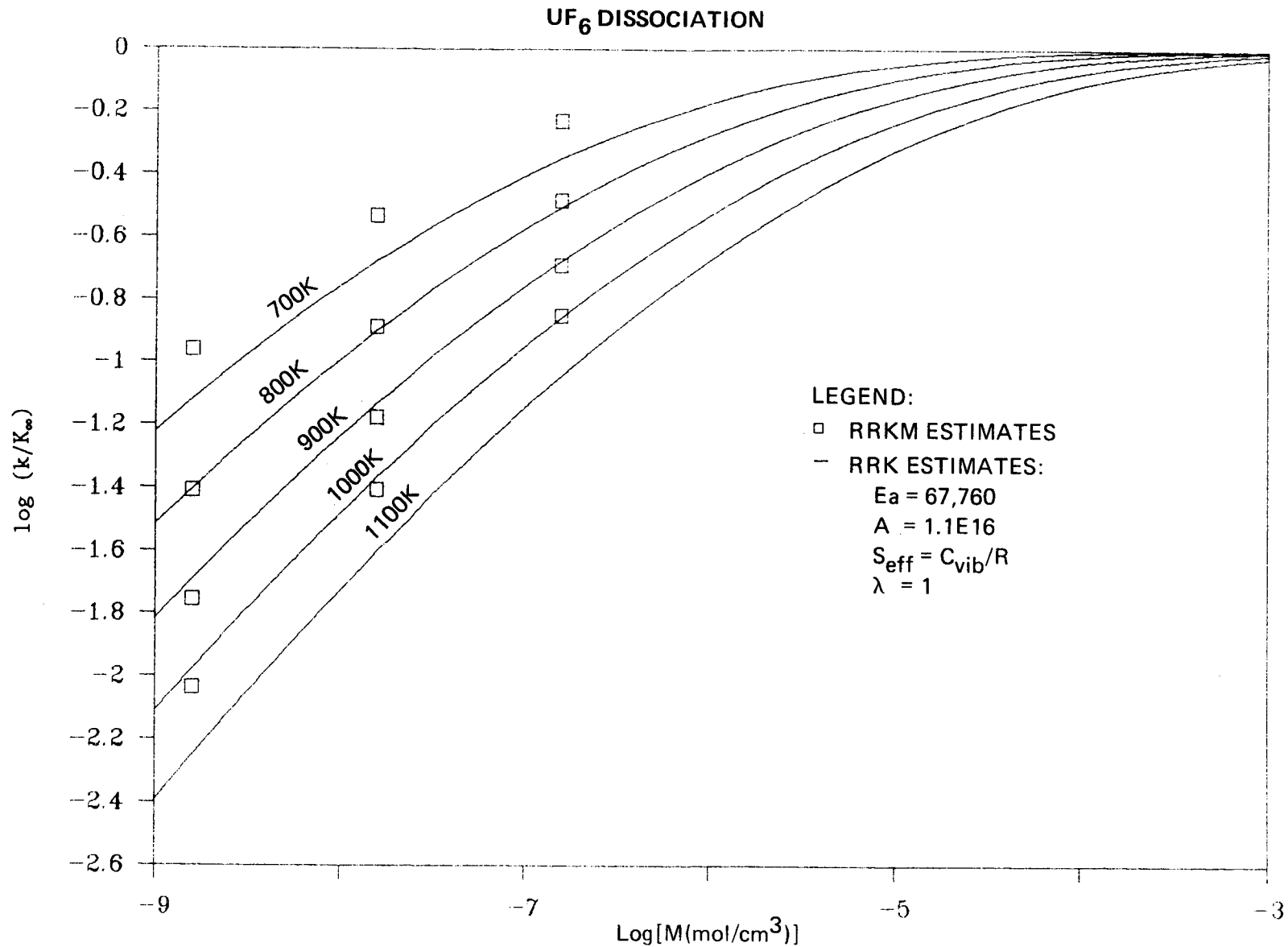


Fig. A-8. Gas-phase unimolecular reaction rate predictions for UF<sub>6</sub>. Solid curves: RRK predictions, with  $S_{\text{eff}} = C_{\text{vib}}/R$  and  $\lambda = 1$ . Symbols: RRKM predictions for  $T = 700, 800, 900$ , and  $1000$  K (Lyman and Holland, unpublished results, May 1985).

Table A-4. RRK.BAS: Selected parameters for predicting the gas-phase thermal dissociation rate for  $\text{UF}_6$

Input parameter	Value selected	Text reference
$E_a$ (cal/mol)	67760	Eq. (9)
$A_o$ (1/s)	1.1E16	Eq. (9)
Reactant mass (amu)	352	Table A-1
Reactant diam. (Ang)	5.97	Table A-1
Diluent diam. (Ang)	(e.g., 3.54 for argon)	Table A-1
$\lambda$	1 (self-medium) 0.045 (argon diluent)	Fig. A-8 Fig. A-7
RRK S factor	$C_{vib}/R$	Eq. (A-3), Table A-3

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