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LOFT SHIELD TANK STEADY STATE TEMPERATURES
WITH ADDITION OF GAMMA AND NEUTRON SHIELDING

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IDAHO NATIONAL ENGINEERING LABORATORY

DEPARTMENT OF ENERGY

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REMARKS: Calculation shows that shield design is compatible with shield tank water and reactor vessel nozzle design temperatures. Recommended spacer is incorporated in shield design under Task 521712 (SWR 51024 and 50842).

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THERMAL ANALYSIS

LOFT SHIELD TANK STEADY STATE TEMPERATURES
WITH ADDITION OF GAMMA AND NEUTRON SHIELDING



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IDAHO NATIONAL ENGINEERING LABORATORY
LOFT TECHNICAL REPORT
LOFT PROGRAM

TITLE LOFT Shield Tank Steady State Temperatures with Addition of Gamma and Neutron Shielding		REPORT NO. LTR No. 129-11
AUTHOR G. Kyllingstad <i>G. Kyllingstad</i>	PERFORMING ORGANIZATION Thermal Analysis Branch	GWA NO. 52171-203-000
LOFT APPROVAL <i>J. C. Reed</i> <i>E. R. White</i> 12-8-77 <i>J. K. ...</i> <i>N. Maringa</i>		DATE Published by CDCS 1-18-78 September 29, 1977

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SUMMARY

The effect of introducing a neutron and gamma shield into the annulus between the reactor vessel and the shield tank is analyzed. This addition has been proposed in order to intercept neutron streaming up the annulus during nuclear operations. Its installation will require the removal of approximately 20-1/2 inches of stainless steel foil insulation at the top of the annulus. The resulting conduction path is believed to result in increased water temperatures within the shield tank, possibly beyond the 150°F limit, and/or cooling of the reactor vessel nozzles such that adverse thermal stresses would be generated.

A two dimensional thermal analysis using the finite element code COUPLE/MOD2 was done for the shield tank system illustrated in Figure (1). The reactor was assumed to be at full power, 55 MW (th), with a loop flow rate of 2.15×10^6 lbm/hr (268.4 kg/s) at 2250 psi (15.51 MPa). Calculations indicate a steady state shield tank water temperature of 140°F (60°C). This is below the 150°F (65.56°C) limit. Also, no significant changes in thermal gradients within the nozzle or reactor vessel wall are generated. A spacer between the gamma shield and the shield tank is recommended, however, in order to ensure free air circulation through the annulus.

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1.0 INTRODUCTION

A modification to the radiation shielding for the LOFT reactor has been proposed. This modification is to include the removal of approximately 20-1/2 inches of stainless steel foil insulation at the top of the annulus between the reactor vessel and the shield tank for the installation of a neutron and gamma shield. Figures (1) and (2) present a detailed sketch of the proposed modification.

The neutron shield is to consist of two rows of steel canisters each filled with a mechanical mixture of 90% $TiH_{1.6}$ and 10% B_4C by weight. This is to be compacted to about 60% theoretical density. A 3/8" portion of each container is to be at a 95% theoretical density as shown in Figure (2).

The gamma shield, a 4-1/2" square steel block and 1/2" welded steel support plate, is to be bolted to the shield tank top and is also to provide support to the neutron shield canisters. A gap is to be provided between the gamma shield and the shield tank for free air circulation.

Since this new configuration constitutes an additional conduction path between the reactor vessel and the shield tank, the possibility of exceeding the 150°F (65.56°C) water temperature limit in the shield tank during full power operation (55 MW) needed to be investigated. Adverse temperature gradients within the reactor vessel nozzle were also considered. Thus a thermal analysis was made to determine the water temperature within the shield tank and the temperature profile of the nozzle with the proposed neutron and gamma shield configuration.

2.0 ANALYSIS

In determining the water temperature an energy balance of the shield tank was considered. A one-dimensional system was assumed and the electrical

analogy for a multilayered system was applied. With the appropriate assumptions one equation with one unknown, the water temperature, can be written. The equation

$$Q_{in} + \dot{Q} = Q_{out} \quad \text{can be written as}$$

$$\frac{T_{RV} - T_w}{\sum R_{i_{in}}} + \dot{Q} = \frac{T_w - T_{\infty}}{\sum R_{i_{out}}}$$

where T_{RV} = 574°F (301°C) maximum temperature of the reactor vessel at full power, 55 MW (th)
 T_{∞} = 100°F (37.78°C) temperature of the atmosphere in the containment building

$\sum R_i$ = sum of the thermal resistances

\dot{Q} = gamma and neutron heating of the shield tank water. Previously calculated in Reference (3).

Thermal conductivities and heat transfer coefficients have been calculated in past studies, Reference (3) and (4), and can be easily estimated considering they vary little for the temperature ranges considered. Thermal properties for the neutron shield were estimated from the literature review of $TiH_{1.6}$ and B_4C Reference (6) and (7). See Appendix C.

Hand calculations were made for the unmodified shield tank for comparison with the results of Reference (3) where the two-dimensional heat conduction code SIMIR was used. Hand calculation results were about 8% higher than SIMIR predictions. Therefore, hand calculations for the modified shield tank were also factored down by 8%. Detailed calculations are given in Appendix A.

The nozzle temperature profile was determined by COUPLE/MOD2, a two-dimensional finite element steady-state and transient heat conduction code. The finite element model is presented in Figure (3). Two axes of symmetry

are possible, the center line of the reactor vessel or the center line of the nozzle. Use of either one will generate a distorted representation of the nozzle and shield tank. Choosing the proper axis, however, may minimize the distortion or at least give conservative answers. Choosing the center line of the nozzle will result in excess shielding being generated about the base of the nozzle, i.e., the gamma shield does not encircle the base of the nozzle, but encircles the reactor vessel. This simulation of excess material increases the conduction path between the base of the nozzle and the shield tank which in turn increases the thermal stress placed upon the nozzle. This was assumed to be the most conservative approach. Should no adverse thermal gradients result with this model a more detailed three-dimensional analysis would not be necessary.

The reactor was assumed to be at full power, 55 MW (th), with an intact loop flow of 2.15×10^6 lbm/hr (268.4 kg/s) at 2250 psi (15.51 MPa). Calculations of the various thermal properties used in the computer analysis and a listing of both the input and output data are presented in Appendix B. Thermal properties of the powdered mixture of $TiH_{1.6}$ and B_4C are presented in Appendix C. For simplicity only the powder material at 60% theoretical density was considered in the 20-1/2" annular space. Also the thermal effect of the steel can and supporting structure was considered negligible and hence was ignored.

3.0 RESULTS AND RECOMMENDATIONS

The maximum steady state shield tank water temperature calculated is 140°F (60°C) which is below the 150°F (65.56°C) limit. The temperature profile of the reactor vessel nozzle is given in Figure (4). No significant changes in thermal gradients are induced in the nozzle or reactor vessel wall, therefore, no adverse thermal stresses should be expected. In order

to ensure free air circulation within the annulus between the reactor vessel and the shield tank it is important that a spacer be provided under the gamma shield. This would also reduce the conduction path from the gamma shield to the shield tank. This was assumed in the shield tank water temperature calculations where heat from the gamma shield was assumed to be conducted to the shield tank only through the 1/2 inch bolts.

4.0 REFERENCES

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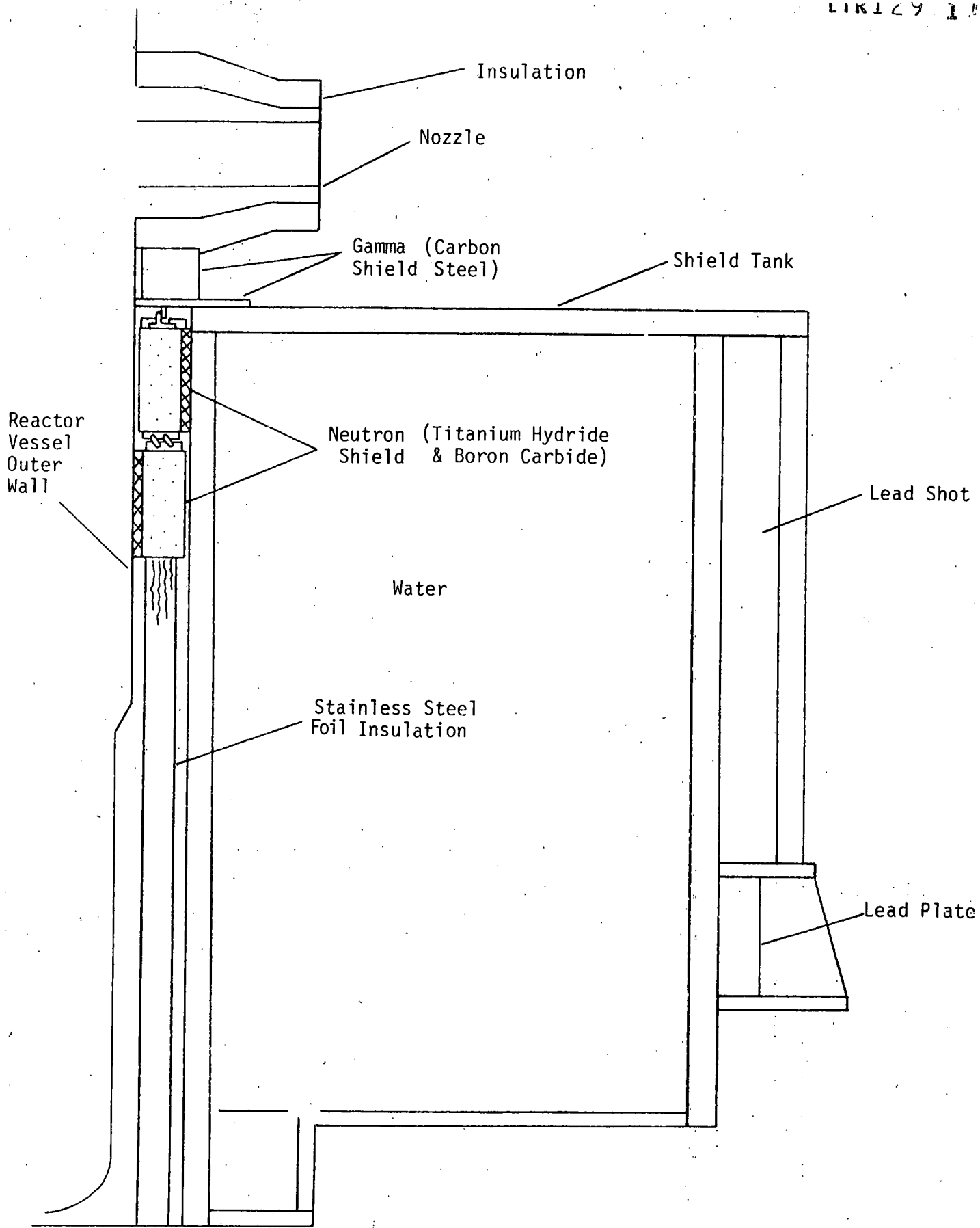


Figure 1. Cross Section of Shield Tank (not to scale)

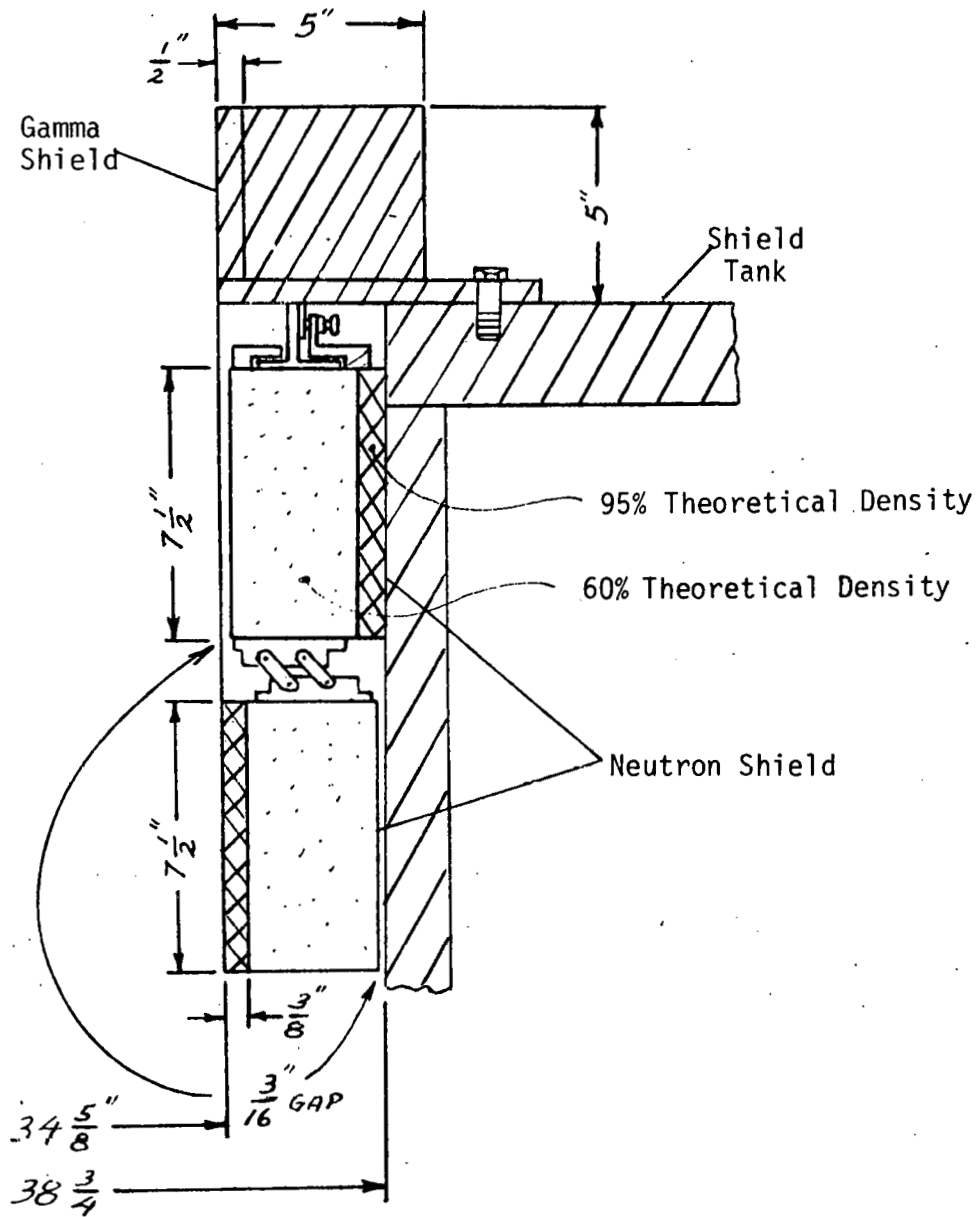


Figure 2. Detail of Gamma and Neutron Shield

COUPLE MOD 2 (MAY-23,77) UPDATE 1 (MAY-23,77) ECL
 LOFT REACTOR VESSEL NOZZLE TEMPERATURE RESPONSE WITH ADDITION OF GAMMA
 AND NEUTRON SHIELD SEP. 07, 1977 COUPLE MOD 2 RUN 01

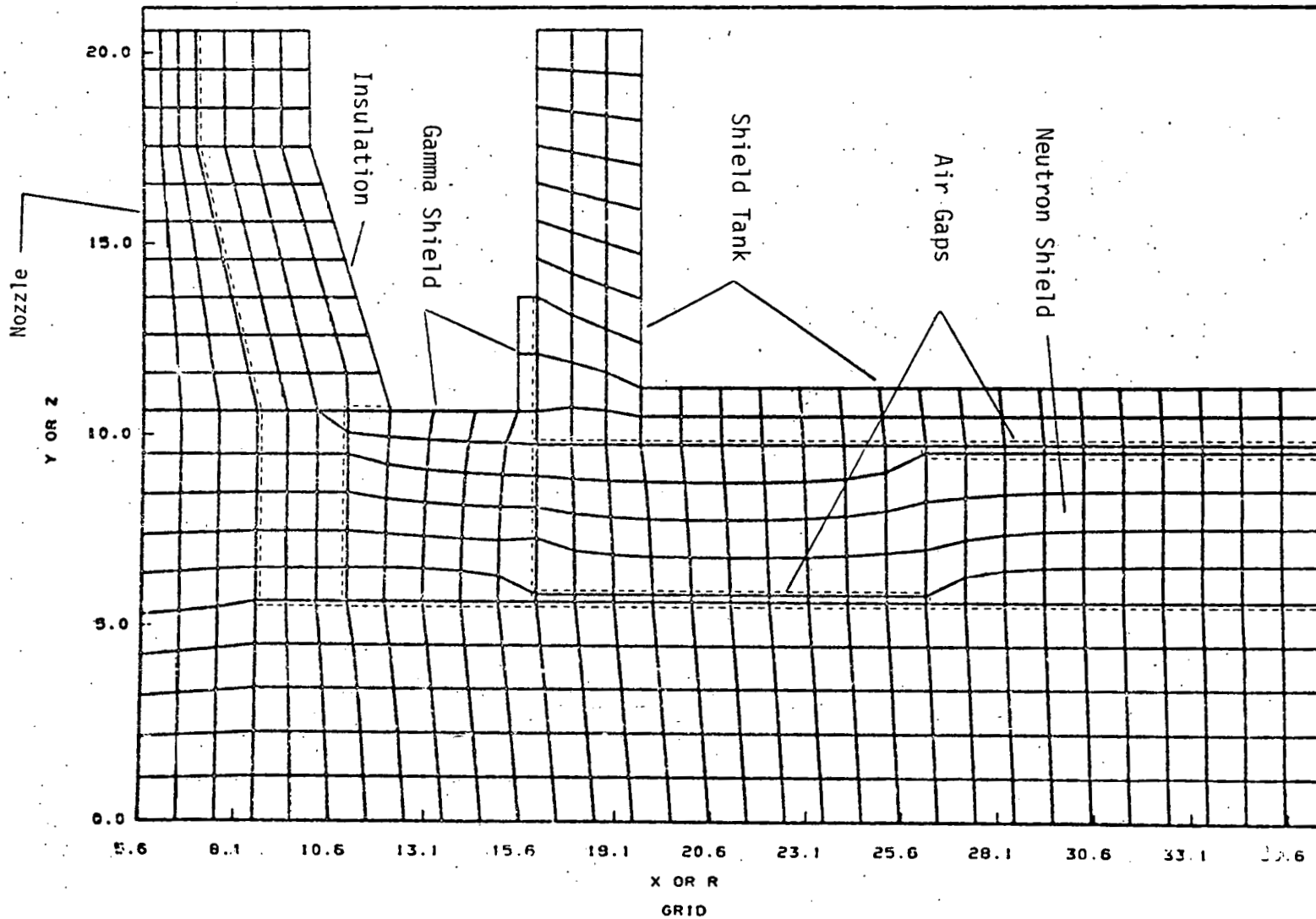


Figure 3. COUPLE/MOD2 Update 1 LOFT Reactor Vessel Nozzle Temperature Response with Addition of Gamma and Neutron Shield - Grid

COUPLE MOD 2 (MAY-23.77) UPDATE 1 (MAY-23.77) ECL
 LOFT REACTOR VESSEL NOZZLE TEMPERATURE RESPONSE WITH ADDITION OF GAMMA
 AND NEUTRON SHIELD SEP. 07. 1977 COUPLE MOD 2 RUN 01

0.00 = TIME FOR SYMBOLS 123456769'S TEMPERATURES ARE RESPECTIVELY
 145.02 187.91 230.81 273.70 316.60 359.49 402.39 445.28 486.18 531.07 573.97

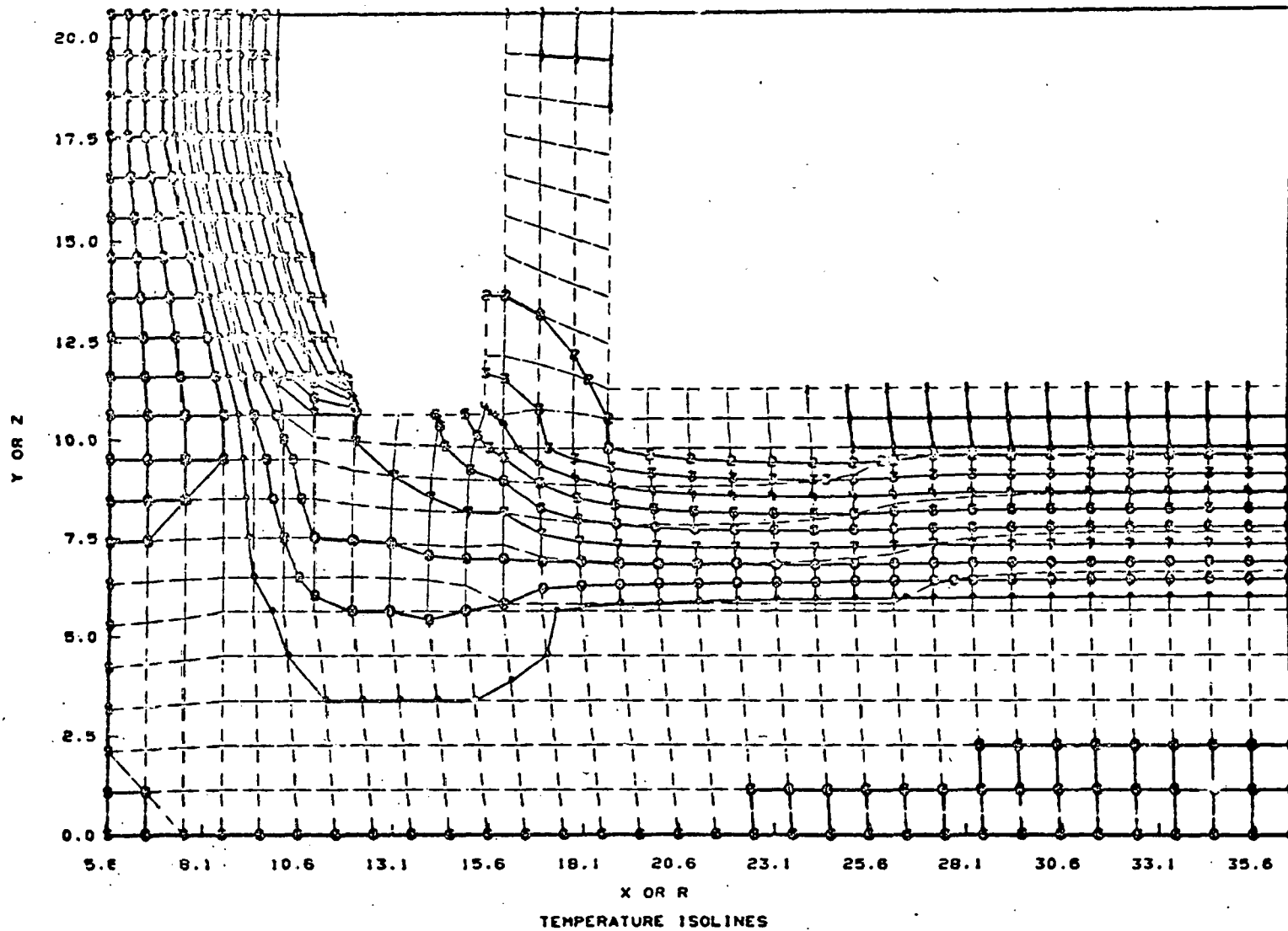


Figure 4. COUPLE/MOD2 Update 1 LOFT Reactor Vessel. Nozzle Temperature Response with Addition of Gamman and Neutron Shield - Temperature Isolines

APPENDIX A

SHIELD TANK WATER TEMPERATURE
CALCULATIONS

In order to determine the water temperature an energy balance of the shield tank is considered.

$$Q_{in} + \dot{Q} = Q_{out}$$

Assuming a one dimensional system and applying the electrical analogy for a multilayered system.

$$Q = \frac{\Delta T}{\sum R_{th}}$$

We can write an equation with one unknown, the water temperature T_w .

$$Q_{out} = \frac{T_w - T_{\infty}}{\sum R_{out}} \quad \text{where } \sum R = \sum \frac{1}{A_i h_i} + \frac{\ln R_r}{2\pi k L_f}$$

$$\dot{Q} = \text{gamma \& neutron heating}$$

$$Q_{in} = \frac{T_{RV} - T_w}{\sum R_{in}}$$

Additional assumptions

- (1) $T_{\infty} = 100^{\circ}F$ the most probable maximum ambient temp. of the containment building.
- (2) $T_{RV} = 574^{\circ}F$ The exterior temperature of the reactor vessel.
- (3) The film coefficients do not vary greatly with temperature and can be estimated for the temperature ranges involved.
- (4) Hinges & attaching clips for the neutron shield are ignored

Detail of gamma & neutron shield is given on page A-3 in Fig. A-2

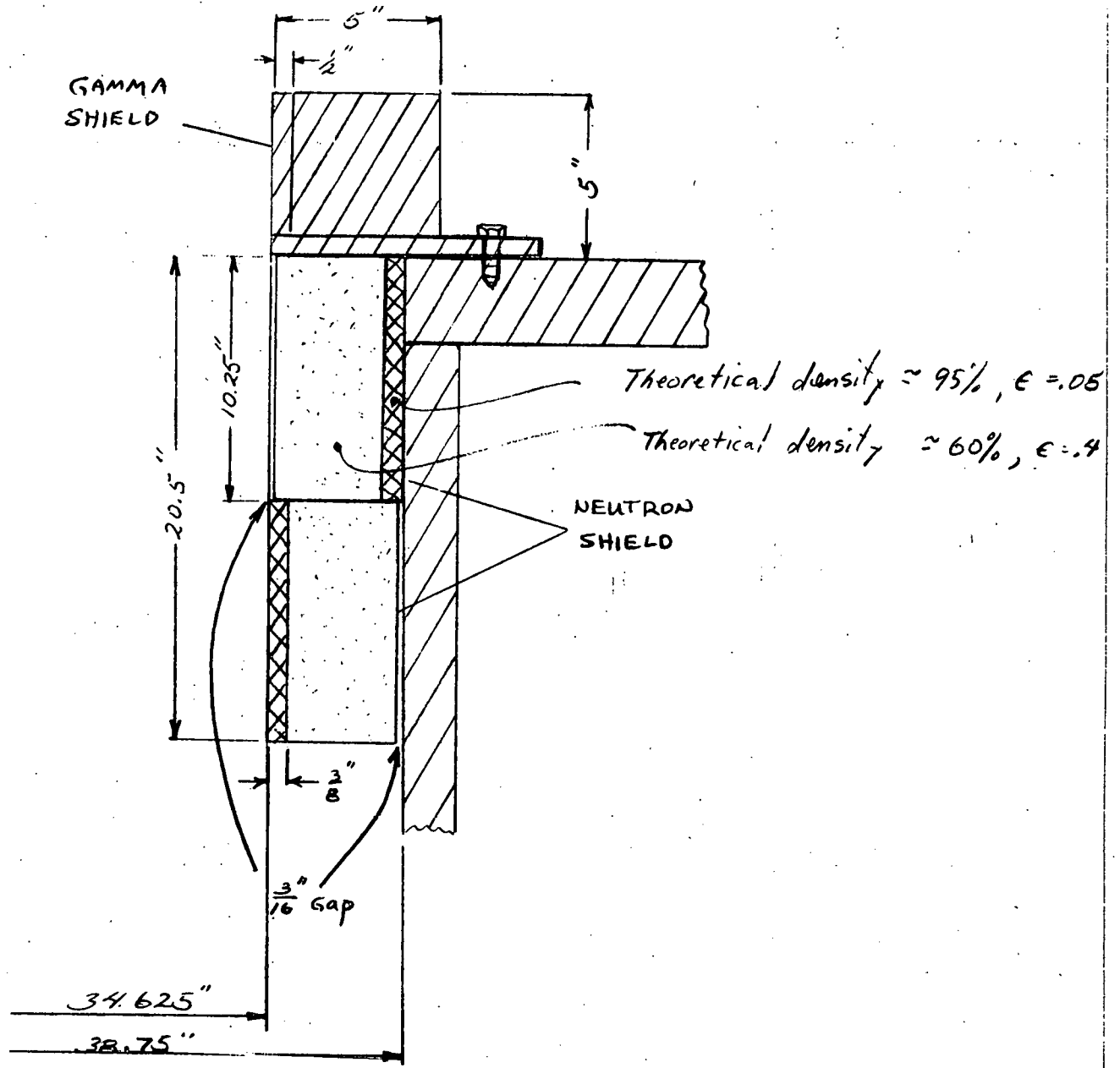


FIGURE A-2 DETAIL OF GAMMA & NEUTRON SHIELD.

Applying hand calculation method to original shield tank configuration for comparison to SIMIA run as an accuracy check Ref. (3)

$$Q_{in} + \dot{Q} = Q_{out}$$

$T_{RV} = 560^{\circ}F$ used in SIMIA program

560 - T_w

$$\frac{1}{2\pi \left(\frac{35}{12}\right) \left(\frac{79.51}{12}\right) h_{air}} + \frac{\ln \frac{38.50}{35.50}}{k_I 2\pi \left(\frac{79.51}{12}\right)} + \frac{\ln \frac{38.75}{38.50}}{k_{air} 2\pi \left(\frac{79.51}{12}\right)} + \frac{\ln \frac{40.25}{38.75}}{k_{steel} 2\pi \left(\frac{79.51}{12}\right)} + \frac{1}{2\pi \left(\frac{40.25}{12}\right) \left(\frac{79.51}{12}\right) h_{out}}$$

$3.9 \frac{Btu}{hr ft^2 F}$ $.05 \frac{Btu}{hr ft^2 F}$ $.142 \frac{Btu}{hr ft^2 F}$ $30.96 \frac{Btu}{hr ft^2 F}$ $45.8 \frac{Btu}{hr ft^2 F}$

560 - T_w

$$\frac{1}{2\pi \left(\frac{34}{12}\right) \left(\frac{78.99}{12}\right) 4} + \frac{\ln \frac{38.5}{35.5}}{.05 (2\pi) \left(\frac{78.99}{12}\right)} + \frac{\ln \frac{38.75}{38.5}}{.142 (2\pi) \left(\frac{78.99}{12}\right)} + \frac{\ln \frac{40.25}{38.75}}{30.96 (2\pi) \left(\frac{78.99}{12}\right)} + \frac{1}{2\pi \left(\frac{40.25}{12}\right) \left(\frac{78.99}{12}\right) (45.8)}$$

560 - T_w

$$\frac{1}{2\pi \left(\frac{35}{12}\right) \left(\frac{28.5}{12}\right) 3.9} + \frac{\ln \frac{38.5}{35.5}}{.05 (2\pi) \left(\frac{28.5}{12}\right)} + \frac{\ln \frac{38.75}{38.5}}{.142 (2\pi) \left(\frac{28.5}{12}\right)} + \frac{\ln \frac{40.25}{38.75}}{30.96 (2\pi) \left(\frac{28.5}{12}\right)}$$

$$+ 9000 \frac{Btu}{hr} + 21,000 \frac{Btu}{hr} = Q_{out}$$

$$or \quad \frac{560 - T_w}{4.229 \times 10^{-2}} + \frac{560 - T_w}{4.265 \times 10^{-2}} + \frac{560 - T_w}{.1178} + 30,000 = Q_{out}$$

In calculating $Q_{out} =$

$$\frac{T_w - 100}{\frac{1}{2\pi \left(\frac{100.5}{12}\right) \left(\frac{107.75}{12}\right) h_{water}} + \frac{\ln \frac{101.5}{100.5}}{h_{steel} (2\pi) \left(\frac{107.75}{12}\right)} + \frac{\ln \frac{104.5}{101.5}}{k_{lead shot} (2\pi) \left(\frac{107.75}{12}\right)} + \frac{\ln \frac{105.25}{104.5}}{k_{steel} (2\pi) \left(\frac{107.75}{12}\right)} + \frac{1}{2\pi \left(\frac{107.75}{12}\right) \left(\frac{105.25}{12}\right) h_{air}}$$

\uparrow 36.4 \uparrow 30.45 \uparrow .29 \uparrow 30.45 \uparrow 1.57

$$+ \frac{T_w - 100}{\frac{1}{2\pi \left(\frac{100.5}{12}\right) (2) (36.4)} + \frac{\ln \frac{101.5}{100.5}}{30.45 (2\pi) (2)} + \frac{\ln \frac{103.5}{101.5}}{k_{lead} (2\pi) z'} + \frac{1}{2\pi \left(\frac{103.5}{12}\right) (2) (1.57)}}$$

\uparrow 20

$$+ \frac{T_w - 100}{\frac{1}{2\pi \left(\frac{100.5}{12}\right) \left(\frac{23}{12}\right) (36.4)} + \frac{\ln \frac{101.5}{101.5}}{30.45 (2\pi) \frac{23}{12}} + \frac{1}{2\pi \left(\frac{101.5}{12}\right) \left(\frac{23}{12}\right) (1.57)}}$$

+ Q_{out} top & bottom of shield tank + Q_{out} flange below lead shot compartment.

For Q_{out} top & bottom of shield tank, an effective area must be determined. $A_H = \frac{12\pi}{144} (100.5^2 - 40.25^2) + \frac{2 \cdot \frac{1}{3}\pi}{144} (100.5^2 - 40.25^2) = 160 ft^2$

$$\therefore Q_{out} \text{ top \& bottom of shield tank} = \frac{T_w - 100}{\frac{1}{160 ft^2 \times 1.57}} = \frac{T_w - 100}{3.98 \times 10^{-3}}$$

The 20% effective heat transfer for the top and the 1/3 effective for the bottom assumption is from Ref. (4)

For the flange, only the bottom one and the 16 vertical webs are considered, and are treated as cooling fins.

From pp 540-542 of Kern Ref. (9)

$$(r_e - r_b) \sqrt{h_f / k y_b} = \sqrt{\frac{1.3}{30.45 \times \frac{1.25}{24}}} \approx 1$$

$$\frac{r_e}{r_b} = \frac{115.5}{103.5} = 1.5 \rightarrow \Omega = .74$$

$$h_b = h_f \Omega = 1.3 \times .74 = .962$$

$$Q_b = h_b \theta_b A_f$$

$$A_f = \frac{2\pi (115.5^2 - 103.5^2)}{144} + \frac{2\pi (115.5)(1.25)}{144} = 121 \text{ ft}^2$$

$$Q = \frac{T_w - 100}{(121)(.962)} = \frac{T_w - 100}{8.591 \times 10^{-3}}$$

For the 16 vertical webs again from Kern

$$Q_b = h_b \theta_b b P \times 16 \quad \text{A.576 of Kern}$$

$$h_b = h_f \Omega \quad \Omega = \frac{\tanh(mb)}{mb}$$

$$m = \left[\frac{h_f P}{k a_x} \right]^{1/2}$$

$$h_f = 1.3 \frac{\text{Btu}}{\text{hr ft}^2 \text{ } ^\circ\text{F}}$$

$$P = \text{Perimeter of fin } \frac{1}{2} + .75 + .75 = 1.67 \text{ ft}$$

$$k = 30.45 \frac{\text{Btu}}{\text{hr ft } ^\circ\text{F}}$$

$$a_x = \text{cross section area of fin} = \frac{1}{2} \times 1.79 = .15 \text{ ft}^2$$

$$b = \text{height of fin} \approx \frac{9}{12} = .75 \text{ ft}$$

$$mb = .517 \quad ; \quad \Omega = \frac{\tanh(.517)}{.517} = .91 \quad , \quad h_b = .91 \times 1.3 = 1.18$$

$$Q = \frac{T_w - 100}{16 h_b b P} = \frac{T_w - 100}{16 (1.18) (.75) (1.67)} = \frac{T_w - 100}{4.7288 \times 10^{-2}}$$

and finally we're assuming annular portion below shield tank

$$\frac{1}{2\pi \left(\frac{56.25}{12}\right) \left(\frac{28.5}{12}\right) (36.4)} + \frac{\ln \frac{56.75}{56.25}}{30.45 (2\pi) \left(\frac{28.5}{12}\right)} + \frac{1}{2\pi \left(\frac{56.75}{12}\right) \left(\frac{28.5}{12}\right) 1.57} = \frac{T_w - 100}{9.438 \times 10^{-3}}$$

collecting terms

$$\frac{560 - T_w}{4.229 \times 10^{-2}} + \frac{560 - T_w}{4.265 \times 10^{-2}} + \frac{560 - T_w}{.1178} + 30,000 = \frac{T_w - 100}{3.135 \times 10^{-3}} + \frac{T_w - 100}{6.22 \times 10^{-3}} + \frac{T_w - 100}{6.552 \times 10^{-3}}$$

$$+ \frac{T_w - 100}{3.981 \times 10^{-3}} + \frac{T_w - 100}{8.591 \times 10^{-3}} + \frac{T_w - 100}{4.229 \times 10^{-2}} + \frac{T_w - 100}{9.438 \times 10^{-3}}$$

$$560(55.58) - (55.58)T_w + 30,000 = (1129.57)T_w - 100(1129.57)$$

$$T_w = \frac{174081.8}{1185.15} = 146.88 \quad \text{SIMIR} \rightarrow 136$$

8% high

Let it then be assumed that hand calculations are 8% on the high side.

Equation to solve:

$$\frac{574^\circ\text{F} - T_w}{\sum R_{in}} + \dot{Q} = \frac{T_w - 100^\circ\text{F}}{\sum R_{out}}$$

$Q_{in} =$
across top plug

$$574 - T_w$$

$$\frac{\ln \frac{38.75}{38.375}}{3.033(2\pi) \frac{10.25}{12}} + \frac{\ln \frac{38.375}{34.6875}}{.187(2\pi) \frac{10.25}{12}} + \frac{\ln \frac{34.6875}{34.625}}{.142(2\pi) \frac{10.25}{12}} + \frac{\ln \frac{40.25}{38.75}}{30.96(2\pi) \frac{10.25}{12}} + \frac{1}{2\pi \left(\frac{40.25}{12}\right) \left(\frac{10.25}{12}\right) (45.8)}$$

$c = .05$

$C = A$

air

steel

water film

across bottom plug

$$574 - T_w$$

$$\frac{\ln \frac{38.75}{38.6875}}{.142(2\pi) \frac{10.25}{12}} + \frac{\ln \frac{38.6875}{35.00}}{.187(2\pi) \frac{10.25}{12}} + \frac{\ln \frac{35.00}{34.625}}{3.033(2\pi) \frac{10.25}{12}} + \frac{\ln \frac{40.25}{38.75}}{30.96(2\pi) \frac{10.25}{12}} + \frac{1}{2\pi \left(\frac{40.25}{12}\right) \left(\frac{10.25}{12}\right) (45.8)}$$

across section from bottom of neutron shield to shoulder in reaction vessel.

$$574 - T_w$$

$$\frac{1}{2\pi \left(\frac{35}{12}\right) \left(\frac{59.01}{12}\right) (3.9)} + \frac{\ln \frac{38.5}{35.5}}{.05(2\pi) \left(\frac{59.01}{12}\right)} + \frac{\ln \frac{38.75}{38.5}}{.142(2\pi) \left(\frac{59.01}{12}\right)} + \frac{\ln \frac{40.25}{38.75}}{30.96(2\pi) \left(\frac{59.01}{12}\right)} + \frac{1}{2\pi \left(\frac{40.25}{12}\right) \left(\frac{59.01}{12}\right) (45.8)}$$

air gap insulation

to bottom of shield tank

$$574 - T_w$$

$$\frac{1}{2\pi \left(\frac{34}{12}\right) \left(\frac{78.99}{12}\right) (4)} + \frac{\ln \frac{38.5}{35.5}}{.05(2\pi) \left(\frac{78.99}{12}\right)} + \frac{\ln \frac{38.75}{38.5}}{.142(2\pi) \left(\frac{78.99}{12}\right)} + \frac{\ln \frac{40.25}{38.75}}{30.96(2\pi) \left(\frac{78.99}{12}\right)} + \frac{1}{2\pi \left(\frac{40.25}{12}\right) \left(\frac{78.99}{12}\right) (45.8)}$$

air gap

thru 2 1/2" section @ bottom of
Shield Tank

$$\frac{574 - T_w}{2\pi \left(\frac{35}{12}\right) \left(\frac{28.5}{12}\right) 3.9} + \frac{\ln \frac{38.5}{35.5}}{.05(2\pi) \left(\frac{28.5}{12}\right)} + \frac{\ln \frac{38.75}{38.50}}{.142(2\pi) \left(\frac{28.5}{12}\right)} + \frac{\ln \frac{40.25}{38.75}}{30.96(2\pi) \left(\frac{28.5}{12}\right)}$$

thru gamma shield & bolts in
Shield Tank

$$\frac{574 - T_w}{\frac{\pi}{4} \frac{(1.5)^2}{144} (45.8)(32)} + \frac{3.25/12}{(30.96) \frac{\pi}{4} \frac{(1.5)^2}{144} (32)}$$

+ 9,000 $\frac{\text{Btu}}{\text{hr}}$ + 21,000 $\frac{\text{Btu}}{\text{hr}}$

↙
Reactor vessel support
lugs

↙
gamma & neutron heating of shield
tank water

= Q_{out}

across lead shot compartment

$$\frac{T_w - 100}{2\pi \left(\frac{100.5}{12}\right) \left(\frac{107.75}{12}\right) (36.4)} + \frac{\ln \frac{101.5}{100.5}}{30.45(2\pi) \left(\frac{107.75}{12}\right)} + \frac{\ln \frac{104.5}{101.5}}{.29(2\pi) \left(\frac{107.75}{12}\right)} + \frac{\ln \frac{105.25}{104.5}}{30.45(2\pi) \left(\frac{107.75}{12}\right)} + \frac{1}{2\pi \left(\frac{107.75}{12}\right) \left(\frac{105.25}{12}\right) 1.57}$$

across lead sheet

$$T_w - 100$$

$$+ \frac{1}{2\pi \left(\frac{100.5}{12}\right) (2) (36.4)} + \frac{\ln \frac{101.5}{100.5}}{30.45 (2\pi) (2)} + \frac{\ln \frac{103.5}{101.5}}{20 (2\pi) (2)} + \frac{1}{2\pi \left(\frac{103.5}{12}\right) (2) (1.57)}$$

across Tank section below flange

$$T_w - 100$$

$$+ \frac{1}{2\pi \left(\frac{100.5}{12}\right) \left(\frac{23}{12}\right) (36.4)} + \frac{\ln \frac{101.5}{100.5}}{30.45 (2\pi) \frac{23}{12}} + \frac{1}{2\pi \left(\frac{101.5}{12}\right) \left(\frac{23}{12}\right) (1.57)}$$

across shield tank
top & bottom

$$T_w - 100$$

$$+ \frac{1}{(160 \text{ ft}^2) (1.57)}$$

across small sections below
shield tank

$$T_w - 100$$

$$+ \frac{1}{2\pi \left(\frac{56.25}{12}\right) \left(\frac{28.5}{12}\right) (36.4)} + \frac{\ln \frac{56.75}{56.25}}{30.45 (2\pi) \left(\frac{28.5}{12}\right)} + \frac{1}{2\pi \left(\frac{56.75}{12}\right) \left(\frac{28.5}{12}\right) (1.57)}$$

three flanges below lead
shot compartment

$$+ \frac{T_w - 100}{\frac{1}{(.962) (121 \text{ ft}^2)}} + \frac{T_w - 100}{\frac{1}{16(.75') (1.67') (1.18)}}$$

$$\frac{574 - T_w}{.105} + \frac{574 - T_w}{.104} + \frac{574 - T_w}{5.222 \times 10^{-2}} + \frac{574 - T_w}{4.265 \times 10^{-2}} + \frac{574 - T_w}{.1178} +$$

$$\frac{574 - T_w}{.7009} + 9,000 + 21,000 = \frac{T_w - 100}{3.135 \times 10^{-3}} + \frac{T_w - 100}{6.22 \times 10^{-3}} + \frac{T_w - 100}{6.552 \times 10^{-3}}$$

$$+ \frac{T_w - 100}{3.981 \times 10^{-3}} + \frac{T_w - 100}{9.438 \times 10^{-3}} + \frac{T_w - 100}{8.591 \times 10^{-3}} + \frac{T_w - 100}{1.229 \times 10^{-2}}$$

$$(574)(71.65) - (71.65)T_w + 30,000 = (1129.57)T_w - 100(1129.57)$$

$$T_w = \frac{184084.1}{1201.22}$$

$$T_w = 153.2 \text{ F} \quad \text{assuming this 8\% high}$$

$$\underline{\underline{T_w = 140^\circ \text{F}}}$$

APPENDIX B

COMPUTER MODEL CALCULATIONS AND
COUPLE/MOD2 INPUT AND OUTPUT LISTING

8/22

Vertical surfaces

$$h_T = h_c + h_r$$

$$h_c = 0.17 (\Delta T_f)^{1/3}$$

$$h_r = \frac{0.122 [T_2^4 - T_1^4]}{10^8 [T_2 - T_1]}$$

2nd horizontal surfaces

$$h_c = 0.22 \Delta t_f^{1/3}$$

$t_2 = 574^\circ F$
 $t_1 = 409^\circ F$ assumed

$$h_r = \frac{0.122 [T_2^4 - T_1^4]}{10^8 [T_2 - T_1]} \quad T_{air} \text{ } ^\circ R$$

$$h_c = 0.22 (174)^{1/3} = 1.23$$

$$h_r = \frac{0.122 [10.34^4 - 8.60^4]}{174} = 9.2$$

$$h_T = 5.41 \frac{Btu}{hr ft^2 ^\circ F}$$

suppose $t_2 = 100^\circ F = 560^\circ R$

$$h_c = 0.22 (474)^{1/3} = 1.715$$

$$h_r = \frac{0.122 [10.34^4 - 5.60^4]}{474} = 2.69$$

$$h_T = 4.41$$

suppose $t_2 = 200^\circ F = 660^\circ R$

$$h_c = 0.22 (374)^{1/3} = 1.585$$

$$h_r = \frac{0.122 (10.34^4 - 6.6^4)}{374} = 3.11$$

$$h_T = 4.7$$

8/3/77

material properties for air gaps COMPLE MOD 2 Input

$\nabla f \equiv$ Stefan-Boltzmann constant times emissivity factor times geometrical shape factor

$F_r = \nabla f \{ (T_\infty + 460) + (T + 460) \} \{ (T_\infty + 460)^2 + (T + 460)^2 \}$ $T_\infty \equiv$ driving temp $^\circ F$

$\nabla f \approx 1 \times 5 \times 0.1714 \times 10^{-8} \frac{Btu}{hr ft^2 R^4} = 8.57 \times 10^{-10} \frac{Btu}{hr ft^2 R^4}$; $K = (F_r + h) \Delta x$
 $\Delta x = \frac{.875}{12}$, $h = 1.4$

$T_\infty = 574$

$T_\infty = 320$

T	T _m	F _r	K _c
200	367	2.18	.261
300	437	2.53	.287
400	487	2.94	.317
500	537	3.40	.350
574	574	3.79	.378

air gap

T	T _m	F _r	K _c
100	200	1.0082	.175
200	260	1.233	.192
320	320	1.5	.211

max air gap

PC

T °F	ρ @ 12.5 psia lbm/ft ³	C Btu/lbm °F	PC $\frac{Btu}{ft^3 °F}$
80.6	.0624	.2402	.015
170.6	.0529	.2410	.013
260.6	.0468	.2422	.011
350.6	.0415	.2438	.010
440.6	.0373	.2459	.0092
530.6	.0340	.2482	.0084
620.6	.0311	.2520	.0078

Ambient air $h_T = 0.19 (\Delta t)^{1/3} + .122 \left[\frac{(560 + \Delta t)^4 - 560^4}{10^6 \Delta t} \right]$

h _T	Δt °F	h _T	Δt °F
1.049	1		
1.193	5		
1.290	10		
1.361	15		
1.420	20		
1.603	40		
1.749	60		
1.877	80		
1.997	100		
2.546	200	3.690	400
3.096	300		

8/3/77

Film Coefficient for water

$$h = A (\Delta t_f)^{1/3}$$

see Figure A-2 of LOFT Report A-70 Note 10/24/69
LOFT Shield Tank Temperature Study for Steady-State
Operating Condition 2.

If the film temperature is assumed to be 140°F
then:

$$h_c / \Delta t^{1/3} = 50.4$$

$$\text{and } h_c = 50.5 \Delta t^{1/3}$$

Δt	h_c
1	50.4
2	63.5
3	72.7
4	80.8
5	86.2
6	91.6
7	96.4
8	100.8
9	104.8
10	108.6
15	124.3
20	136.8

COUPLE MOD 2 Input

10⁴ 2 3 4 5 6 7 8 9
10⁵ 2 3 4 5 6 7 8 9
10⁶ 2 3 4 5 6 7 8 9
10⁷ 2 3 4 5 6 7 8 9

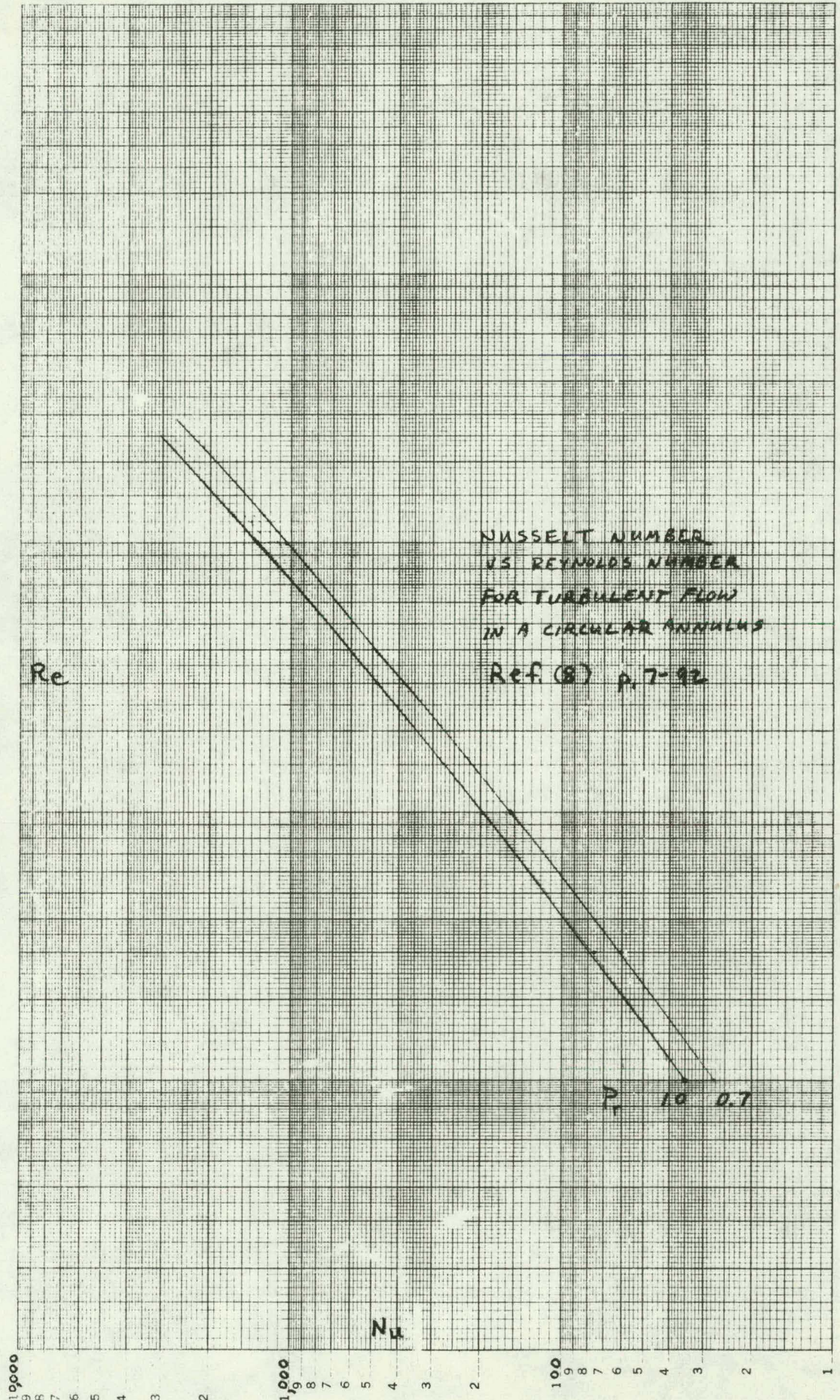


FIGURE B-2

In the 1/4" diameter annulus

9/6/17

$$Re = \frac{D_e G}{\mu}$$

$$D_e = 2(r_o - r_i) = 2 \times \frac{1}{4} = .5" = 0.117 ft$$

from Steam tables

$$G = \rho v$$

$$\text{at } 574^\circ F, 2250 \text{ psi} = 155 \text{ bars}$$

$$v = 1/\rho = .02197$$

$$\rho = 45.5 \text{ lb}_m/\text{ft}^3$$

$$\mu = 918 \times 10^{-6} \times 10^{-5} = 6.169 \times 10^{-5} \frac{\text{lb}_m}{\text{ft sec}}$$

$$\dot{m} = 2.13 \times 10^6 \text{ lb}_m/\text{hr}$$

but thru 1/4" annulus

$$\dot{m} \text{ is } 1/10 \text{ of } 2.13 \times 10^6$$

$$\therefore \dot{m}_{1/4} = 2.13 \times 10^5 \text{ lb}_m/\text{hr}$$

$$\dot{m} = \rho v A$$

$$\rho v = \dot{m}/A = G$$

$$A = \frac{\pi(29 \text{ in}^2 - 28.75 \text{ in}^2)}{144 \text{ in}^2/\text{ft}^2} = .315 \text{ ft}^2$$

$$\therefore G = 2.13 \times 10^5 \frac{\text{lb}_m}{\text{hr}} / (.315 \text{ ft}^2 \times 3600 \frac{\text{sec}}{\text{hr}})$$

$$G = 187.8 \frac{\text{lb}_m}{\text{ft}^2 \text{ sec}}$$

$$Re = \frac{2}{12} (29 - 28.75) \text{ ft} \times (187.8 \frac{\text{lb}_m}{\text{ft}^2 \text{ sec}}) / (6.169 \times 10^{-5} \frac{\text{lb}_m}{\text{ft sec}}) = 1.268 \times 10^5$$

$$Pr = \frac{\hat{C}_p \mu}{k}$$

$$\hat{C}_p^{-1} = .77 \text{ from Steam Table, ASME}$$

$$\hat{C}_p^{-1} \approx 1.3 \frac{\text{Btu}}{\text{lb}_m \text{ } ^\circ\text{F}}$$

$$\mu = 6.169 \times 10^{-5} \frac{\text{lb}_m}{\text{ft sec}} \times 3600 \frac{\text{sec}}{\text{hr}}$$

$$k = .322 \frac{\text{Btu}}{\text{hr ft } ^\circ\text{F}}$$

$$Pr = .896, \text{ from Chart } Pr = .893, \text{ close}$$

From Table 29 p. 7-92 Handbook of Heat Transfer (extrapolated)

$$Nu \approx 235 = \frac{h D_e}{k} \therefore h = \frac{235 \times .322}{.117} \frac{\text{Btu}}{\text{hr ft}^2 \text{ } ^\circ\text{F}} = 1815 \frac{\text{Btu}}{\text{hr ft}^2 \text{ } ^\circ\text{F}}$$

in nozzle

$$D = 11.2''$$

$$A = \frac{\pi}{4} \frac{11.2^2}{144} = .684 \text{ ft}^2$$

$$Re = \frac{DG}{\mu}$$

$$G = \frac{\dot{m}}{A} = \frac{2.13 \times 10^6 \text{ lb/hr}}{.684 \text{ ft}^2 \times 3600 \frac{\text{sec}}{\text{hr}}} = 865 \frac{\text{lbm}}{\text{ft}^2 \text{ sec}}$$

$$Re = \frac{\frac{11.2}{12} \text{ ft} \times 865 \frac{\text{lbm}}{\text{ft}^2 \text{ sec}}}{6.169 \times 10^{-5}} = 1.3087 \times 10^7 \quad \text{turbulent}$$

$$Nu = (0.022) Re^{0.8} Pr^{0.6}$$

Ref(8) Handbook of Heat Transfer eq. 48 p 7-33

$$Re = 1.3087 \times 10^7$$

$$Pr \approx .896$$

$$Nu \approx (0.022) (1.3087 \times 10^7)^{0.8} (.896)^{0.6}$$

$$Nu \approx 10,169$$

$$h = \frac{Nu k}{D} = \frac{10169 \times .322 \frac{\text{Btu}}{\text{hr ft}^\circ \text{F}}}{11.2/12 \text{ ft}}$$

$$h = 3508 \frac{\text{Btu}}{\text{hr ft}^2 \text{F}}$$

COUPLE MOD2 Input

0 1 2 3 4 5 6 7 8
 1234567890123456789012345678901234567890123456789012345678901234567890

TITLE
 LOFT REACTOR VESSEL NOZZLE TEMPERATURE RESPONSE WITH ADDITION OF GAMMA
 AND NEUTRON SHIELD SEP. 07, 1977 COUPLE MOD 2 RUN 01

MATERIAL

1
 1.0 CARBON STEEL
 2.3148E-5 2.3148E-5 NEUTRON SHIELD THICK & 840
 1.0 R.V. INSULATION
 2.3148E-5 2.3148E-5 AIR GAPS BETWEEN R.V. & SHIELD TK
 1.0
 2.3148E-5 2.3148E-5

MESH/TAPE

510 452 0 0 0
 STEP 0.0 3600.0 16 0 574. -10 0

FUNCTIONS

12 2 THERMAL CONDUCTIVITY OF CARBON STEEL BTU/HR,FT,F
 300.0 300.0 150.0 300.0
 350.0 350.0 300.0 300.0
 500.0 27.20 450.0 27.20
 2 12 2 DENSITY * SPECIFIC HEAT OF CARBON STEEL BTU/FT**3,F
 70.0 .5392 .5392 150.0 .5421
 200.0 .5246 .5246 300.0 .4928
 350.0 .4770 .4770 450.0 .4467
 500.0 .4358 .4358 600.0 .4061
 4 2 THERMAL CONDUCTIVITY OF NEUTRON SHIELD BTU/HR,FT,F
 200.0 .3889 .3889 440.6 .3816
 4 2 DENSITY * SPECIFIC HEAT OF NEUTRON SHIELD BTU/FT**3,F
 30.0 219.7849 219.7849 273.6123 440.6 324.1604
 620.0 377.9683
 2 2 THERMAL CONDUCTIVITY OF R. V. INSULATION BTU/HR,FT,F
 100.0 .0504 .0504
 2 2 DENSITY * SPECIFIC HEAT OF R. V. INSULATION BTU/FT**3,F
 100.0 9.8496 9.8496
 7 2 THERMAL COND. IN AIR GAPS BETWEEN R.V. & SHLD TK BTU/HR,FT,F
 100.0 .1750 .1750 300.0 .2110
 400.0 .3170 .3170 574.0 .3780
 8 7 2 DENSITY * SPECIFIC HEAT OF AIR GAPS BTU/FT**3,F
 80.0 .0150 .0150 260.6 .0110
 350.0 .0100 .0100 530.6 .0084

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B-8

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LOGF COUPL MOD 2 (MAY-23,77) UPDATE 1 (MAY-23,77) RCL
 IND NEUTR MOD 2 VESSEL NOZZLE TEMPERATURE RESP. WITH ADDITION OF GAMMA
 SHIELD SEP. 07, 1977 COUPLE MOD 2 RUN 01

N D D E D A T A

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B-11

APPENDIX C

TITANIUM HYDRIDE AND BORON CARBIDE
THERMODYNAMIC PROPERTIES

Material & Thermal Properties of Neutron shield

The neutron shield is to be a powder mixture of $TiH_{1.6}$ 90% by weight and B_4C 10% by weight. Thermal conductivity of each component is strongly dependent on theoretical density or void fraction. Thermal conductivities of TiH_x and B_4C are plotted as a function of void fraction in Figure (c-1). Calculation method is presented in W.H. McAdams, Heat Transmission, McGraw-Hill Book company, Inc. (1954) page 290.

Specific Heat of $TiH_{1.6}$ is estimated from Figure (8), page 18 of the literature review. Ref (6)

C_p of $TiH_{1.6}$

$T (^{\circ}K)$	$C_p (cal/g^{\circ}K)$	
300	1.51	
400	1.78 to 1.87	estimate by extrapolation.
500	2.01 to 2.22	" "
600	2.29 to 2.59	" "

The literature review for B_4C listed the following equation for specific heat see Ref (7)

$$C_p = 22.99 + 5.4 \times 10^{-3} (T) - 10.72 \times 10^{-5} (T)^2$$

where T is in $^{\circ}K$ and C_p in $cal/mole^{\circ}K$

For a MW of 53.7 g/mole the equation becomes

$$C_p = .4281 = 1.006 \times 10^{-4} (T) - 19.963 \times 10^{-3} (T)^2 ; C_p \text{ in } \frac{cal}{gm^{\circ}K} \text{ or } \frac{cal}{gm^{\circ}C}$$

C_p of B_4C

T °K	C_p (cal/g°K)
300	.236
400	.344
500	.399
600	.433

In order to determine properties of the mixture, must determine mole fraction (X_i) of each constituent

Given: $M_{TiH_{1.6}} = .9 M_{mix}$; $M_{B_4C} = .1 M_{mix}$

$$MW_{TiH_{1.6}} = 47.9 + 1.6 = 49.5 \text{ kg/kgmole}$$

$$\% H_2 = 1.6 \times \frac{1.6}{49.5} = 3.2\%$$

$$\therefore \rho_{TiH_{1.6}} \approx 3.8 \times 10^3 \text{ kg/m}^3 \text{ from Fig(10) p. 20 of Lit. Review Ref(6)}$$

If powder is evenly mixed throughout the volume (as if it were a gas),

then:

$$\frac{m_{TiH_{1.6}}}{V_{mix}} = \rho_{TiH_{1.6}} \quad \text{let } V_{mix} = 100 \text{ m}^3$$

$$m_{TiH_{1.6}} = \rho_{TiH_{1.6}} V_{mix} = 3.8 \times 10^3 \times 100 = 3.8 \times 10^5 \text{ kg}$$

$$m_{TiH_{1.6}} = .9 m_{mix} \quad \therefore m_{mix} = \frac{3.8 \times 10^5}{.9} = 4.22 \times 10^5 \text{ kg}$$

$$\text{then } m_{B_4C} = .1 m_{mix} = 4.22 \times 10^5 \text{ kg}$$

Based on an average density of $B_4C = 2.44 \text{ gm/cm}^3$ from Table 1 page 17 of Lit. Review Ref(7)

$$MW_{B_4C} \approx 53.7 \text{ kg/kgmole}$$

Number of moles per constituent (air is negligible)

$$n_{T, H_{1.6}} = \frac{3.8 \times 10^5}{49.5} = 7677$$

$$n_{B_4C} = \frac{4.22 \times 10^4}{53.7} = 785.85$$

$$n_{Total} = 8462.85$$

$$X_{T, H_{1.6}} = \frac{7677}{8462.85} = .907 \approx .9$$

$$\therefore X_{B_4C} = .1 \text{ since } X_{Total} = 1.0$$

@ 60% TD or $\epsilon = .4$

$$k_{mix} = (.311 \frac{W}{m^{\circ}C})(.9) + (.43 \frac{W}{m^{\circ}C})(.1)$$

$$k = .323 \frac{W}{m^{\circ}C} = .187 \frac{Btu}{hr ft^{\circ}F}$$

@ 95% TD or $\epsilon = .05$

$$k = (3.5 \frac{W}{m^{\circ}C})(.9) + (21 \frac{W}{m^{\circ}C})(.1)$$

$$k = 5.25 \frac{W}{m^{\circ}C} = 3.033 \frac{Btu}{hr ft^{\circ}F}$$

$21 \frac{W}{m^{\circ}C}$ is from Fig(9)

Page 25 of Int. Review
Pg (7)

$$C_{p, \text{mix}} = X_{T, H_2O} C_{p, T, H_2O} + X_{BAC} C_{p, BAC}$$

$$T = 300^\circ\text{K}$$

$$C_p = (0.907)(1.51 \frac{\text{cal}}{\text{g}^\circ\text{K}}) + (0.093)(2.236 \frac{\text{cal}}{\text{g}^\circ\text{K}}) = 1.39 \frac{\text{cal}}{\text{g}^\circ\text{K}} @ 300^\circ\text{K}$$

$$T = 400^\circ\text{K}$$

$$C_p = (0.907)(1.87) + (0.093)(3.44) = 1.728 \frac{\text{cal}}{\text{g}^\circ\text{K}} @ 400^\circ\text{K}$$

$$T = 500^\circ\text{K}$$

$$C_p = (0.907)(2.22) + (0.093)(3.99) = 2.05 \frac{\text{cal}}{\text{g}^\circ\text{K}} @ 500^\circ\text{K}$$

$$T = 600^\circ\text{K}$$

$$C_p = (0.907)(2.59) + (0.093)(4.33) = 2.387 \frac{\text{cal}}{\text{g}^\circ\text{K}} @ 600^\circ\text{K}$$

$$\rho_{\text{mix}} @ .7 = .6 \times 4222 \text{ kg/m}^3 = 2533.33 \text{ kg/m}^3$$

Density * Specific heat

T (°K / °F)	$\frac{\text{kJ}}{\text{m}^3 \cdot \text{K}}$	$\frac{\text{Btu}}{\text{ft}^3 \cdot ^\circ\text{F}}$
300 / 50.6	1.474×10^4	219.7849
400 / 260.6	1.835×10^4	273.6128
500 / 440.6	2.174×10^4	324.1604
600 / 620.6	2.535×10^4	377.9883

K_{eff} W/m²C

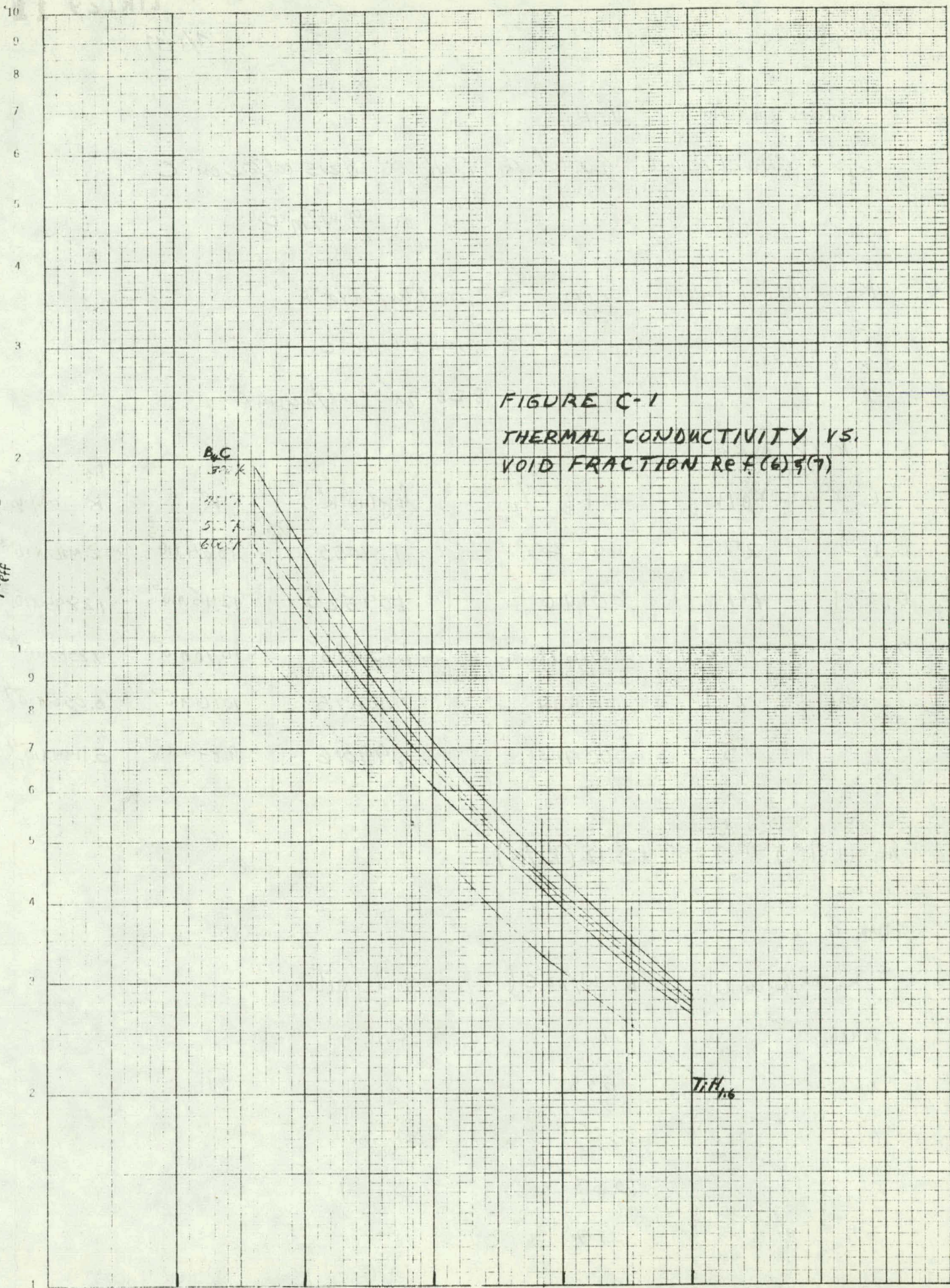


FIGURE C-1
THERMAL CONDUCTIVITY VS.
VOID FRACTION REF. (6) & (7)

7/1/11

Kyllingstad

Thermal conductivity $T_i H_2$

$K_s = \text{thermal conductivity of solid for } T_i H_2 \approx .0215 \text{ cal/sec cm}^\circ\text{C}$
 or $9 \text{ W/m}^\circ\text{C}$

$K_g = \text{thermal conductivity of air} = .02 \text{ BTu/hr ft}^\circ\text{F}$
 $= .0346 \text{ W/m}^\circ\text{C}$
 $= 8.2689 \times 10^{-5} \text{ cal/sec cm}^\circ\text{C}$

$K_s/K_g = 260$

ϵ	K_B/K_g	$K_B \text{ (cal/sec cm)}$	$\log_{10}(10^5 K^*)$	K^*	$K_B + K^*$ $K \text{ (cal/sec cm}^\circ\text{C)}$
0.163	27	.00223	1.27053	18.64×10^{-5}	2.416×10^{-3}
0.284	14	.00116	1.09520	12.45×10^{-5}	1.2845×10^{-3}
0.386	8.2	.000678	1.03278	10.78×10^{-5}	7.858×10^{-4}
0.494	6.1	.000504	1.00675	10.16×10^{-5}	6.056×10^{-4}
0.50	5	.000413	.99316	9.844×10^{-5}	5.1144×10^{-4}

$\log_{10}(10^5 K^*) = 0.859 + 3.12(K_s/a)$

where $a = \epsilon$

$K \text{ (cal/sec cm}^\circ\text{C)}$	$K \text{ (W/m}^\circ\text{C)}$	Void fraction
2.416×10^{-3}	1.011	0.163
1.2845×10^{-3}	.538	0.284
7.858×10^{-4}	.329	0.386
6.056×10^{-4}	.253	0.494
5.1144×10^{-4}	.214	0.50

Thermal conductivity, B_1C

K_s (thermal conductivity of solid, B_1C)

T	K_s 99% TD
300°K (27°C, 80.6°F)	.0675 cal/sec cm°K or cal/sec cm°C
400°K (127°C, 260.6°F)	.061
500°K (227°C, 440.6°F)	.056
600°K (327°C, 620.6°F)	.051

$$\log_{10}(10^5 K^*) = 0.859 + 3.12 (K_s/a)$$

$$[\text{cal/sec cm}^\circ\text{C}] \times 418.68 \text{ W}^\circ\text{C} = \left\{ \frac{\text{W}}{\text{m}^\circ\text{C}} \right\}$$

assume K_g (air) constant @ 8.2689×10^{-5} cal/sec cm°C, .0346 W/m°C

300°K $K_s = .0675$ cal/sec cm°K

$$K_s/K_g = .0675 / 8.2689 \times 10^{-5} = 816$$

ϵ	K_B/K_g	K_B cal/sec cm°C	$\log_{10}(10^5 K^*)$	K^* cal/sec cm°C	$K_B + K^*$ K cal/sec cm°C	K W/m°C
0.163	39	.00322	2.15102	141.6×10^{-5}	4.636×10^{-3}	1.941
0.284	18	.00149	1.60055	39.86×10^{-5}	1.8886×10^{-3}	.791
0.386	10.5	.000868	1.40460	25.39×10^{-5}	1.1219×10^{-3}	.470
0.454	7.5	.000620	1.32288	21.03×10^{-5}	8.303×10^{-4}	.348
0.50	6.	.000496	1.28020	19.06×10^{-5}	6.866×10^{-4}	.287

400°K $K_s = .061$ cal/sec cm°K

$$K_s/K_g = .061 / 8.2689 \times 10^{-5} = 738$$

ϵ	K_B/K_g	K_B cal/sec cm°C	$\log_{10}(10^5 K^*)$	K^* cal/sec cm°C	K cal/sec cm°C	K W/m°C
0.163	37	3.0595×10^{-3}	2.02663	106.3×10^{-5}	4.1275×10^{-3}	1.726
0.284	17.5	1.45×10^{-3}	1.52114	33.82×10^{-5}	1.7882×10^{-3}	.749
0.386	10.1	8.35×10^{-4}	1.35106	22.49×10^{-5}	1.0599×10^{-3}	.444
0.454	7.3	6.04×10^{-4}	1.27821	18.98×10^{-5}	7.938×10^{-4}	.332
0.50	5.99	4.95×10^{-4}	1.23964	17.36×10^{-5}	6.686×10^{-4}	.280

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Thermal conductivity B₉C

500°K

$k_s = .056 \text{ cal/sec cm}^\circ\text{C}$; $k_g = 8.2689 \times 10^{-5} \text{ cal/sec cm}^\circ\text{C}$

$k_s/k_g = 677$

$\log_{10}(10^5 k^*) = 0.859 + 3.12 (k_s/\epsilon)$

$[\text{cal/sec cm}^\circ\text{C}] * 418.604 = [\text{W/m}^\circ\text{C}]$

ϵ	k_B/k_g	$k_B \text{ cal/sec cm}^\circ\text{C}$	$\log_{10}(10^5 k^*)$	$k^* \text{ cal/sec cm}^\circ\text{C}$	$k \text{ cal/sec cm}^\circ\text{C}$	$k \text{ W/m}^\circ\text{C}$
0.163	35	2.8941×10^{-3}	1.93090	8.529×10^{-5}	3.747×10^{-3}	1.569
0.284	17	1.4057×10^{-3}	1.47421	29.80×10^{-5}	1.7037×10^{-3}	.713
0.386	10	8.2689×10^{-4}	1.31164	20.50×10^{-5}	1.0389×10^{-3}	.432
0.454	7.25	5.9950×10^{-4}	1.24385	17.53×10^{-5}	7.748×10^{-4}	.324
0.50	5.9	4.8786×10^{-4}	1.20844	16.16×10^{-5}	6.4946×10^{-4}	.272

600°K

$k_s = .051 \text{ cal/sec cm}^\circ\text{C}$; $k_g = 8.2689 \times 10^{-5} \text{ cal/sec cm}^\circ\text{C}$

$k_s/k_g = 617$

ϵ	k_B/k_g	$k_B \text{ cal/sec cm}^\circ\text{C}$	$\log_{10}(10^5 k^*)$	$k^* \text{ cal/sec cm}^\circ\text{C}$	$k \text{ cal/sec cm}^\circ\text{C}$	$k \text{ W/m}^\circ\text{C}$
0.163	34	2.8114×10^{-3}	1.83520	68.41×10^{-5}	3.4955×10^{-3}	1.463
0.284	16	1.323×10^{-3}	1.41928	26.26×10^{-5}	1.5856×10^{-3}	.664
0.386	9.9	8.1862×10^{-4}	1.27123	18.67×10^{-5}	1.00532×10^{-3}	.421
0.454	7.1	5.8709×10^{-4}	1.20948	16.20×10^{-5}	7.4909×10^{-4}	.314
0.50	5.8	4.796×10^{-4}	1.17724	15.04×10^{-5}	6.3×10^{-4}	.264