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Energy and Environment Division**

**July 1996**



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**TWO- AND THREE-DIMENSIONAL NATURAL  
AND MIXED CONVECTION SIMULATION  
USING MODULAR ZONAL MODELS**

by

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# Two- and Three-Dimensional Natural and Mixed Convection Simulation Using Modular Zonal Models

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## Abstract

We demonstrate the use of the zonal model approach, which is a simplified method for calculating natural and mixed convection in rooms. Zonal models use a coarse grid and use balance equations, state equations, hydrostatic pressure drop equations and power law equations of the form  $m = C\Delta^n$ . The advantages of the zonal approach and its modular implementation are discussed. The zonal model resolution of nonlinear equation systems is demonstrated for three cases: a 2-D room, a 3-D room and a pair of 3-D rooms separated by a partition with an opening. A sensitivity analysis with respect to physical parameters and grid coarseness is presented. Results are compared to computational fluid dynamics (CFD) calculations and experimental data.

## 1 Introduction

The study of air flow in buildings is important for the evaluation of energy consumption, moisture and pollutant transport, and comfort. The physical phenomena at work are natural or forced convection.

Natural convection has been extensively studied from theoretical, numerical and experimental points of view. The theory considers laminar boundary layer similarity or non-similarity solutions, as for example in [Bej84], [SY71], [CE76] and [KJH87]. Many results have been obtained on standard problems, such as the "window problem", in which natural convective flow occurs in a room with both hot and cold surfaces ([BGKG80], [Dav82], [Dav83], [MP83], [MP84]). Variations in geometry have been addressed ([SGT81], [TG82]). Real rooms, with or without forced convection, have for the most part been analyzed using CFD, as in [Gad80], [SM91], [NvdK93], and, with obstacles, in [GAC91]. CFD has also been used for large rooms and whole buildings ([LYT93], [BNIS91], [SS93]).

The major difficulty with CFD, especially in three dimensions, is that the calculations are very slow and require large amounts of memory. Some methods, like the multi-grid method [LHF93], mitigate the problem but still require significant computational resources. Furthermore, the sheer size of the output requires considerable effort in post-processing and visualization.

Other methods bypass the fluid mechanics equations. An example is the one-air-node approach, which is often used for multizone air flow calculations ([FA89], [HC91]). The main drawback of this approach is the coarseness of the results. This method, when coupled with CFD as is sometimes done ([SM91], [CCN95]), suffers from the inherent difficulties of the CFD approach.

An intermediate approach is needed that allows the flow pattern inside a room to be determined without the computational investment of CFD. One such approach is the "zonal method."

## 2 The Zonal Method

### 2.1 Previous Work

The zonal method, which is not new, is based on heat and mass balance equations in macroscopic volumes. Added to this is a relationship between mass flow and pressure difference. The zonal method should not be confused with models used to calculate air flow between rooms ([Wal84], [Oku87], [FA89], [HC91], [TS93]).

Initial work on the zonal method emphasized how to partition the computational domain in two dimensions ([LN87], [How85], [Ina88]). A systematic attempt to use the zonal method with power law equations on arbitrary geometries in two dimensions is described in [BD91], in which convergence problems were encountered and the results did not agree well with measurements.

The present work treats the 3-D simulation case, with natural or mixed convection. Results were validated against CFD calculations and measurements. In addition we coupled 3-D zonal models with models for thermal comfort, wall conduction and directed flow. Other studies ([RAC93], [RAC94]) have considered the 3-D case, but did not couple to other models and were not validated.

### 2.2 Presentation of the method

In the 3-D zonal method the room air is partitioned into 3-D zones. Adjacent zones exchange mass and energy. The following mass and energy balance equations apply to each zone:

$$\sum q_m + q_{source} - q_{sink} = 0$$

$$\sum \Phi + \Phi_{source} - \Phi_{sink} = 0$$

where  $\sum q_m$  is the sum of mass flows across the interfaces of the zones,  $q_{source}$  is the mass flow from sources in the zone,  $q_{sink}$  is the mass flow to sinks in the zone,  $\sum \Phi$  is the sum of heat transfers through the interfaces of the zone,  $\Phi_{source}$  is the heat transfer from sources in the zone and  $\Phi_{sink}$  is the heat transfer to sinks in the zone.

We assume that a zone has uniform temperature and density and that the pressure at the middle of a zone obeys the perfect gas law:

$$P_{middle} = \rho \frac{R}{M} T$$

where  $\rho$  is the density,  $R$  the perfect gas constant,  $M$  the molar mass and  $T$  the absolute temperature.

The pressure at height  $z$  above the bottom of a zone is given by

$$P = P_0 - \rho g z$$

where  $P_0$  is the pressure at the bottom of the zone.

Assuming that the zones are rectangular parallelopipeds with edges oriented along the coordinate axes. the gist of the zonal model lies in the following equations:  
for horizontal interfaces.

$$q_{m_{vert}} = C \rho S (P - P_{top})^n$$

for vertical interfaces.

$$\Delta P = \Delta P_0 - \Delta \rho g z$$

$$z_n = \frac{\Delta P_0}{\Delta \rho g}$$

$$q_{m_{sup}} = Cl \rho (\Delta \rho g)^n \frac{(h - z_n)^{n+1}}{n+1}$$

$$q_{m_{inf}} = Cl \rho (\Delta \rho g)^n \frac{(z_n)^{n+1}}{n+1}$$

$$q_m = q_{m_{sup}} + q_{m_{inf}}$$

Here  $P_{top}$  is the pressure at the top of the zone.  $q_m$  are mass flows,  $C$  is an empirical constant equal to  $0.83 \text{ m}^2 \text{s}^{-1} \text{Pa}^{-n}$  [Ina88],  $l$  is the width of a zone,  $h$  is the height of a zone.  $n$  is a fractional exponent,  $\Delta$  is a difference operator between two horizontally adjacent zones,  $z_n$  is the height of the neutral point (the point at which pressures on either side of the interface between two zones are equal),  $\rho$  is the volumetric mass,  $vert$  is an index for vertical mass flow,  $m_{sup}$  an index for horizontal mass flow above the neutral point and  $m_{inf}$  is an index for horizontal mass flow below the neutral point. It is assumed that flow is incompressible and pressure drop is hydrostatic.

Energy fluxes are calculated using the following equations. which are valid for temperatures typically found in buildings and which, for now, neglect humidity:

$$\Phi_{horiz} = q_{m_s} c_p T_s + q_{m_e} c_p T_e$$

$$\Phi_{vert} = q_{m_{vert}} c_p T_{vert}$$

where  $\Phi$  denotes a heat flux,  $horiz$  stands for horizontal and  $vert$  for vertical. Here  $q_{m_s}$  denotes mass flow leaving the zone and  $q_{m_e}$  denotes mass flow entering the zone.  $T_s$  is the temperature of the air leaving the zone, which is the same as the zone temperature, and  $T_e$  the temperature of the air entering the zone.  $T_{vert}$  is the zone temperature for vertical flow out of the zone and is the adjacent zone temperature for vertical flow into the zone. We use a sign convention such that a mass flow is positive when the flow is in the positive direction of an  $x$ ,  $y$  or  $z$  axis, and negative when in the negative direction of an axis.

## 2.3 Physical Considerations

Several remarks can be made about the validity of the model. (1) Coarse grids and high temperature gradients may make uniform temperature in a zone a poor assumption. (2) Temperature and velocity boundary layers are not accounted for. (3) The hydrostatic pressure approximation is valid only for flows with parallel streamlines. (4) Only one neutral point per vertical interface between zones is allowed, which, depending on the gridding, affects the qualitative behavior of the solution. (5) Along the lines of [BD91], the Bernoulli equation used amounts to assuming that kinetic energy is fully dissipated within the bounds of a single zone, and so does not apply to plumes or jets that span two or more zones, as rediscovered in [RAC93].

## 2.4 Numerical Considerations

An obvious property of the above equations is their nonlinearity. The  $n = 0.5$  exponent is a source of particular numerical difficulty since it is well known that standard Newton-Raphson iteration (without relaxation) does not converge when there are square-root dependencies. An additional source of trouble is that, because they depend on flow direction, the equations must be piecewise defined, even if they are formally unified, as in [HvdMR93]. Finally, 3-D problems generally lead to a fairly large number of equations. This "dimensional curse" also exists for zonal models. For example, some problems analyzed with zonal methods require resolving more than 2000 equations.

## 2.5 Insight on a Simplified Case: the Window Problem

### 2.5.1 Two-Zone Case

We consider now the application of the zonal model to the well-known "window" problem in which a two-dimensional rectangular cavity is heated by a warm isothermal wall on the left and cooled by a cold window (in our case, actually a cold isothermal wall) on the right. The ceiling and floor are assumed to be adiabatic. For this configuration the room air density will, on average, be smaller on the left, and the resulting circulation will be clockwise. We divide the room into two zones, one on the left and one on the right. Because of buoyancy effects we expect the air to flow from left to right at the top of the room and from right to left at the bottom. We assume that there are no mass sources or sinks, that the convection at the walls is Newtonian and that  $n = 0.5$ . The solution will be given in terms of the widths,  $l_1$  and  $l_2$ , of the left and right zones, respectively, the height,  $h$  of the zones, the convective heat transfer coefficients,  $h_h$  and  $h_c$ , of the hot and cold walls, respectively, the hot and cold wall temperatures,  $t_h$  and  $t_c$ , respectively, and the total room air mass,  $m$ .

### 2.5.2 Algebraic Simplification in the Two-Zone Case

Simplification by substitution produces a nonlinear system of two equations and two unknowns. The simplification was done automatically using the MACSYMA computer algebra program [MIT83]. The simplification algorithm that was used is described in [Nat92]. Basically, the algorithm transforms the equation system into a graph and then uses graph theory to find a small number of iteration variables.

During the simplification process MACSYMA asks questions, such as whether the neutral point is located above the height of a zone or not, which zone has the higher specific air mass,  $\rho$ , etc. The answers to these questions are unique, even though, in some cases, an intermediate calculation of the sign of expressions is required (such as whether  $h_c(t_c - t_1) + h_h(t_h - t_1) > 0$ ). The resulting simplified system of equations is also unique.

The unknowns remaining after simplification by MACSYMA are  $t_2$  and  $\rho_2$ , the air temperature and density, respectively, of the right-hand zone. However, this simplification is not complete, due to the presence of fractional powers, which lead to alternative solutions that MACSYMA cannot resolve. Further simplification can be carried out, producing one (very nonlinear) equation in  $\rho_2$  that can be solved numerically. Note that if fractional power simplification is turned on in MACSYMA, two equations, in  $\rho_2$  and  $z_n$ , result.

Results from the computer algebra reduction agree with numerical results obtained with an independent numerical solver, called SPARK, which is described in section 3. However, the final equations are too unwieldy to use, and there are two of them, in terms of moderately interesting variables. We would be more interested in only one final equation (since resolution of one nonlinear equation, however complicated, can be done efficiently and safely), possibly in terms of one mass flow,  $q_m$ , for example (since what we are mainly interested in is the heat transfer and the mass circulation). The conclusion of interest of this model is the global heat transfer, from the left wall to the right wall.

Reordering the set of equations and reformulating the pressure power law equations to express them with the  $\rho$ 's solved for, one can actually get down to one equation with residual unknown  $\rho_2$ . The (large) surviving equation given by the MACSYMA implementation of the reduction algorithm is:

$$\begin{aligned}
 H/2 = & \\
 & (\text{SQRT}(G)*\text{SQRT}(H)*\text{SQRT}(L1)*\text{SQRT}((L2+L1)*\text{RH02}+(-L2-L1)*\text{RH0})*((2*\text{SQRT}(2)*C# \\
 & P*\text{HHOT}*K*L2+2*\text{SQRT}(2)*CP*\text{HHOT}*K*L1)*R*\text{RHO}*\text{RH02}+(-2*\text{SQRT}(2)*CP*\text{HHOT}*K*L2-2*\text{SQRT}# \\
 & (2)*CP*\text{HHOT}*K*L1)*R*\text{RHO}^2)*\text{THOT}+((2*\text{SQRT}(2)*CP*\text{HCOLD}*K*L2+2*\text{SQRT}(2)*CP*\text{HCOLD}*K# \\
 & *L1)*R*\text{RHO}*\text{RH02}+(-2*\text{SQRT}(2)*CP*\text{HCOLD}*K*L2-2*\text{SQRT}(2)*CP*\text{HCOLD}*K*L1)*R*\text{RHO}^2)*\text{TC}# \\
 & \text{OLD}+((\text{SQRT}(2)*CP*G*H*\text{HHOT}+\text{SQRT}(2)*CP*G*H*\text{HCOLD})*K*L2+(\text{SQRT}(2)*CP*G*H*\text{HHOT}+\text{SQRT}# \\
 & (2)*CP*G*H*\text{HCOLD})*K*L1)*\text{MAIR}*\text{RHO}*\text{RH02}+(-\text{SQRT}(2)*CP*G*H*\text{HHOT}-\text{SQRT}(2)*CP*G*H*\text{HC}# \\
 & \text{OLD})*K*L2+(-\text{SQRT}(2)*CP*G*H*\text{HHOT}-\text{SQRT}(2)*CP*G*H*\text{HCOLD})*K*L1)*\text{MAIR}*\text{RHO}^2)+(12*\text{HC}# \\
 & \text{OLD}*\text{HHOT}*L1*L2*R*\text{RH02}+(-12*\text{HCOLD}*\text{HHOT}*L1*L2-12*\text{HCOLD}*\text{HHOT}*L1^2)*R*\text{RHO})*\text{THOT}+12# \\
 & *\text{HCOLD}*\text{HHOT}*L1^2*R*\text{RH02}*\text{TCOLD}+(6*G*H*\text{HCOLD}*\text{HHOT}*L1*L2+6*G*H*\text{HCOLD}*\text{HHOT}*L1^2)*M# \\
 & \text{AIR}*\text{RH02}+(-6*G*H*\text{HCOLD}*\text{HHOT}*L1*L2-6*G*H*\text{HCOLD}*\text{HHOT}*L1^2)*\text{MAIR}*\text{RHO})/(\text{SQRT}(G)*\text{SQ}# \\
 & \text{RT}(H)*\text{SQRT}(L1)*\text{SQRT}((L2+L1)*\text{RH02}+(-L2-L1)*\text{RH0})*((2*\text{SQRT}(2)*CP*G*\text{HHOT}+2*\text{SQRT}(2)*CP*G*\text{HCOLD})*K*L1)*\text{MAIR}*\text{RHO}*\text{R}# \\
 & \text{H02}+(-2*\text{SQRT}(2)*CP*G*\text{HHOT}-2*\text{SQRT}(2)*CP*G*\text{HCOLD})*K*L2+(-2*\text{SQRT}(2)*CP*G*\text{HHOT}-2*\text{SQRT}(2)*CP*G*\text{HCOLD})*K*L1)*\text{MAIR}*\text{RHO}^2)+(12*G*\text{HCOLD}*\text{HHOT}*L1*L2+12*G*\text{HCOLD}*\text{HHOT}*L1^2)*\text{MAIR}*\text{RHO}^2+(-12*G*\text{HCOLD}*\text{HHOT}*L1*L2-12*G*\text{HCOLD}*\text{HHOT}*L1^2)*\text{MAIR}*\text{RHO})
 \end{aligned}$$

In the above, the previous notations are capitalized. Thus  $H$  is the zone height  $h$ ,  $G$  the acceleration of gravity  $g$ ,  $L1$  the length of the left zone, etc...

This equation can be simplified by invoking of various simplifiers from the MACSYMA functions. After simplification, the output is:

$$\begin{aligned}
 & \text{SQRT}(2)*CP*\text{SQRT}(G)*\text{SQRT}(H)*K*\text{SQRT}(L1)*(L2+L1)^(3/2)*R*\text{RHO}*(\text{RH02}-\text{RH0})^{-(3/2)} \\
 & *(\text{HHOT}*\text{THOT}+\text{HCOLD}*\text{TCOLD})+6*\text{HCOLD}*\text{HHOT}*L1*R*(L2*\text{RH02}-L2*\text{RHO}-L1*\text{RHO})*\text{THOT} \\
 & +6*\text{HCOLD}*\text{HHOT}*L1^2*R*\text{RH02}*\text{TCOLD}=0
 \end{aligned}$$

which leads to the third order polynomial equation:

$$2*CP^2*G*H*K^2*L1*(L2+L1)^3*RHO^2*(RH02-RHO)^3*(HHOT*THOT+HCOLD*TCOLD)^2 - (6*HCOLD*HHOT*L1*(L2*RH02-L2*RHO-L1*RHO)*THOT+6*HCOLD*HHOT*L1^2*RH02*TCOLD)^2$$

This equation has the form  $ax^3 = (x - c)^2$  where  $a$  and  $c$  are positive, where  $x$  is  $\rho_2 - \rho$  the reduced cold zone air density, where

$$c = \frac{l_1(T_{hot} - T_{cold})}{l_1 T_{cold} + l_2 T_{hot}} \rho$$

is proportional to the temperature difference. and where

$$a = \frac{2c_p^2 g h k^2 (l_1 + l_2)^3 \rho^2 (h_{hot} T_{hot} + h_{cold} T_{cold})^2}{36 h_{cold}^2 h_{hot}^2 l_1^2 (l_1 T_{cold} + l_2 T_{hot})^2}$$

The order of magnitude of  $c$  is  $\frac{1}{300}$ . and of  $a$  is  $510^5$ .

It can be shown graphically that this 3rd order equation has a real solution between 0 and  $X$ . where

$$X = \frac{l_1(T_{hot} - T_{cold})}{l_1 T_{cold} + l_2 T_{hot}} \rho$$

Furthermore, we know that the solution can be expressed in closed form by radicals (since we are dealing with a 3rd order polynomial). Solving the equation using the following input values

```
[hhot=4, hcold=4., h=3., l=2., l1=3., l2=3., mair=0.029, r=8.314,
rho=1.205, cp=1004., g=9.81, k=0.83, thot=303., tcold=283.];
```

gives 1.206244948428609 as the value of the only one of three roots that is real. This is acceptable and expected (the air is denser on the cold side). Numerical back propagation (or substitution) of this *symbolic* solution to the other variables of interest leads to:

```
RH02 = 1.206244948428609
RH01 = 1.203755051571391
T1 = 293.3027135161184
T2 = 292.6972864838816
QMLOW = 0.3828828788442727
PHI = 232.7348756131578
P1 = 101219.9750313746
P2 = 101219.9750902376
P10 = 101237.6882869585
P20 = 101237.7249846537
```

By inspection we see that these results are reasonable. In particular, the middle pressures are equal, which is expected from the finding that the neutral point is exactly at mid height.

Comparison with a *numerical* solution of the same problem in slightly different units (degrees Celsius and reduced pressures instead of degrees Kelvin and absolute pressures), using zonal models and the SPARK environment, yields

```

RH02 = 1.206010E+00
RH01 = 1.203521E+00
T1 = 2.030105E+01 + 273 = 293.3
T2 = 1.969943E+01 + 273 = 292.7
QMLOW = 3.827173E-01
PHI = 2.326966E+02
P1 = -6.948886E+01 + 101325 = 101255
P2 = -6.948892E+01 + 101325 = 101255
P20 = -5.173599E+01 + 101325 = 101374
P10 = -5.177318E+01 + 101325 = 101374

```

The agreement is uneven. The pressures differ by about 35 pascals. However, the symbolic simulation assumes a perfectly tight room, which the numerical simulation does not.

Another (small) cause of discrepancy is that the power law used in the symbolic simulation is multiplied by a default density, whereas the numerical simulation uses the upstream density.

On the other hand, the temperatures, the mass flows and the heat transfers agree almost perfectly.

### 2.5.3 Qualitative Observations in the Two-Zone case

Qualitatively, we see that  $\rho_2$  decreases when  $a$  increases (i.e., when the height or permeability coefficient increases, or when the convective heat transfer at the wall decreases). On the other hand,  $\rho_2$  increases when  $c$  increases.

Also, we see that  $\rho_2$  increases when the wall-to-wall temperature difference,  $T_{hot} - T_{cold}$ , increases. This is because  $c$  is proportional to  $T_{hot} - T_{cold}$  and  $a$  is slowly varying since it is the square of a homographic function.

Finally, since  $a$  is large, it can be shown graphically that the physical root of  $ax^3 = (x - c)^2$  is close to the root of  $ax^3 = c^2$ , or  $x = c^{2/3}a^{-1/3}$ . This trend confirms and sharpens the above statements. For example,  $\rho_2 - \rho$  varies like  $h^{-1/3}$ .

### 2.5.4 Global heat transfer in the two-zone case

With computer algebra we automatically obtain the set of substitutions needed to calculate the other unknowns. The variable of interest, the global heat transfer,  $\phi$ , is obtained from the following sequence of substitutions:

```

PHI = H*HHOT*L*THOT-H*HHOT*L*T1
QMSUP = QMLOW
T1 = (HHOT*THOT+HCOLD*TCOLD-HCOLD*T2)/HHOT
T2 = (CP*HHOT*QMLOW*THOT+(CP*HCOLD*QMLOW+H*HCOLD*HHOT*L)*TCOLD)/((CP*HHOT+CP*H#
COLD)*QMLOW+H*HCOLD*HHOT*L)
QMLOW = -(2*SQRT(G)*K*L*RHO*SQRT(RHO2-RHO1)*SQRT(H-ZN)*ZN-2*SQRT(G)*H*K*L*RHO*#
SQRT(RHO2-RHO1)*SQRT(H-ZN))/3
ZN = H/2
RH01 = -(L2*RHO2+(-L2-L1)*RHO)/L1

```

We note that the neutral point for this simple case is always at mid height. The final equation for  $\phi$  is:

```

PHI = H*HHOT*L*THOT-H*L*(-HCOLD*(CP*SQRT(G)*H^(3/2)*HHOT*K*L*RHO*SQRT((#
L2*RHO2+(-L2-L1)*RHO)/L1+RHO2)*THOT/(3*SQRT(2))+(CP*SQRT(G)*H^(3/2)*HCOLD*K*L*#
RHO*SQRT((L2*RHO2+(-L2-L1)*RHO)/L1+RHO2)/(3*SQRT(2))+H*HCOLD*HHOT*L)*TCOLD)/(S#
QRT(G)*H^(3/2)*(CP*HHOT+CP*HCOLD)*K*L*RHO*SQRT((L2*RHO2+(-L2-L1)*RHO)/L1+RHO2)#
/(3*SQRT(2))+H*HCOLD*HHOT*L)+HHOT*THOT+HCOLD*TCOLD)

```

The ratio  $Nu$  (Nusselt number) of  $\phi$  to the purely conductive flux

$\frac{h}{k_{air}} \frac{T_{hot}-T_{cold}}{l_1+l_2}$

is

```

SQRT(G) SQRT(H) (CP HCOLD HHOT K L2 + CP HCOLD HHOT K L1) RHO
SQRT((L2 + L1) RH02 + (- L2 - L1) RHO)
/(SQRT(G) SQRT(H) (CP HHOT + CP HCOLD) K KAIR RHO
SQRT((L2 + L1) RH02 + (- L2 - L1) RHO) + 3 SQRT(2) HCOLD HHOT KAIR SQRT(L1))

```

This is a rational function in  $\sqrt{\rho_2 - \rho}$ . Further simplification leads to:

$$Nu = \frac{\frac{l_1+l_2}{k_{air}}}{\left(\frac{1}{h_{hot}} + \frac{1}{h_{cold}}\right) + \frac{3\sqrt{2}\sqrt{\frac{l_1}{l_1+l_2}}}{c_p\sqrt{ghk}\frac{1}{\rho\sqrt{\rho_2-\rho}}}}$$

For the problem under consideration we obtain

$$Nu = \frac{1}{0.0021 + \frac{0.0000023}{\sqrt{\rho_2-1.205}}}$$

which is about 465.

We see that the larger value of  $\rho_2$  (due, for example, to an increase in temperature difference), produces a larger value of  $Nu$ .

### 2.5.5 Comparison of the Two-Zone Case with Theory

In laminar natural convection (see [Bej84], for example),  $Nu$  depends on the Rayleigh number,  $Ra_h$ , according to  $Nu = 0.364 \frac{l_1+l_2}{h} Ra_h^{1/4}$ . A rough evaluation using  $Ra_h = 107000000h^3\Delta T = 57780000000$ , an approximation valid at those temperatures, yields  $Nu = 356$ . Thus,  $Nu$  increases as  $h^{3/4}$  and as  $\Delta T^{1/4}$ . For turbulent natural convection  $Nu$  varies as  $\Delta T^{1/3}$  since  $Nu = 0.065 Gr_h^{1/3} \left(\frac{h}{l_1+l_2}\right)^{-1/9}$  according to the Jakob correlation. Numerical application to our problem yields  $Nu = 304$ .

Thus, the coarse-grained two-zone zonal model overestimates the ratio of convective to conductive heat transfer by 30 to 50%.

The zonal model applied to two continuous zones exhibits a qualitatively appropriate behavior: an increase in  $h$  or  $\Delta T$  does increase  $Nu$  if the other parameters are held constant.

We should also take into account the temperature dependence of the wall heat transfer coefficients,  $h_{hot}$  and  $h_{cold}$ , to better account for the temperature dependence of  $Nu$ .  $Nu$  depends on the harmonic mean of the wall heat transfer coefficients, which, in turn, go as  $Ra^{1/4}$ . Thus, the qualitative behavior of the zonal model, even in the simple two-zone case, is consistent with the theoretical and experimental natural convection if the wall heat transfer coefficients are chosen appropriately.

### 2.5.6 Two-Zone Case with Inlet Air

A generalization of the two-zone problem is to allow air to flow in (at the left, for example) at a specified rate. Assuming that circulation still exists, i.e., that the inlet flow is small enough not to disturb the flow pattern, we can again reduce the overall system to two equations in unknowns  $\rho_2$  and  $z_n$ . One equation is a second-order polynomial in  $\sqrt{\rho_2 - \rho}$  that can be eliminated by solving for  $\rho_2$ , leaving a single equation in  $z_n$ . However, this equation contains large, nonpolynomial expressions. Thus little can be said on the parameter dependency of its solutions, unlike in the previous case.

## 3 Numerical Implementation: the SPARK Environment

### 3.1 Presentation and History

The Simulation Problem Analysis and Research Kernel (SPARK) is a modular environment that automates writing code for systems of nonlinear equations. It was developed for building science but is applicable to other fields. It is related to simulation environments like TK!Solver [KJ85], TRNSYS [Sol88], CLIM2000 [BCGR89], IDA [Sah88], and Allan.Simulation [Fra92].

Some key features of SPARK are:

- It has a front end that allows the user to build complex simulations by connecting smaller elements that are objects (single equations) or macro-objects (equation subsystems). It shares this feature with TRNSYS, CLIM2000 and Allan.Simulation.
- Using graph-theoretic techniques, it reduces the size of the equation system by automatically determining a small set of iteration variables for which the other unknowns can be solved. This step can be viewed as “smart” elimination of variables. SPARK’s Newton-Raphson solver works on the reduced equation set and, after convergence, the remaining unknowns are solved for. This is a unique feature. Allan.Simulation, for example, generates code that inverts the full Jacobian matrix.
- Its output is a C program that is automatically compiled and executed. This program accepts user-specified input at run time and is computationally efficient because it iterates on a reduced set of variables.
- Passing from a simulation problem to a design problem (i.e., having unknowns become inputs and inputs become unknowns) is simply a matter of keyword exchange in SPARK.

Originally written in 1986 for steady state problems [And87], it was extended in 1989 to handle transient problems by adding time integrator objects [SBN89]. Recent enhancements include

- Automatic generation of objects from equations expressed symbolically ( [SNW90], [NW94] ).
- Strong component decomposition to reduce execution time [BEN<sup>+</sup>93].
- User control of solution method to enhance convergence.

### 3.2 Implementation of the Zonal Model

Implementation of zonal models in SPARK is straightforward. The main object classes correspond to the *zones* and to the *interfaces* between *zones*. A *zone* class consists of the balance equations for the zone, the pressure drop equation and the perfect gas law. An *interface* class consists of the neutral point calculation and the relationship between mass flow and pressure difference.

These classes are instantiated as many times as needed to define the simulation. For example, if a 3-D room is divided into eight parallelopipeds (two in each of the x, y and z directions), there will be eight zone objects and 36 interface objects (12 zone-to-zone interfaces and 24 zone-to-surface interfaces). In the general 3-D case, if the x, y and z axes are divided into L, M and N sections, respectively, there will be  $LMN$  zone objects and  $3(LM+MN+LN)$  interface objects. In 2-D there will be  $LM$  zone objects and  $LM$  zone-to-zone interface objects and  $2LM$  zone-to-surface interface objects.

After instantiation, the objects are linked, i.e., the variables shared by objects are identified. Then the objects and their linked variables are stored in a file that specifies the overall problem and its inputs.

### 3.3 Efficiency

The efficiency of a simulation environment depends on the time and resources needed to solve a simulation problem. SPARK obtains a near-optimal simplification of the problem, without loss of precision, by automatically reducing the number of iteration variables. The reduction can be more than 10-fold, which corresponds to a roughly 1000-fold decrease in Jacobian inversion time. SPARK also makes it easy to create a simulation from scratch by using symbolic processing to create the simulation building blocks (equation objects) from equations written by the user [NW94]. In the present work even the linking of objects was automated ([NW93],[Wur95]).

To facilitate interpretation of results, a graphical postprocessor was written to visualize temperatures and air flows.

## 4 The 2-D "window" Problem

### 4.1 Description

A 2-D,  $6m \times 2.4m$  shallow enclosure has its left wall maintained at 12C, its right wall at 20C, and its floor and ceiling at 15C. The surface heat transfer is assumed to be linear in surface-to-air temperature difference, with convective heat transfer coefficient,  $h$ , of 4.1, 1.0 and  $5.7 \text{ W m}^{-1} \text{ K}^{-1}$  at the walls, floor and ceiling, respectively [Ina88].

Two different grids were used for the zonal model,  $3 \times 3$  and  $6 \times 6$ , which yield 108 and 432 equations, respectively. After reduction in SPARK, there were 18 and 72 equations, respectively. The iteration variables chosen were the temperature and midpoint pressure of each zone.

### 4.2 Numerical Validation

The calculated flow field is shown qualitatively in Figure 1. The expected circulation pattern is observed, i.e., downward flow across the cold wall and upward flow across the

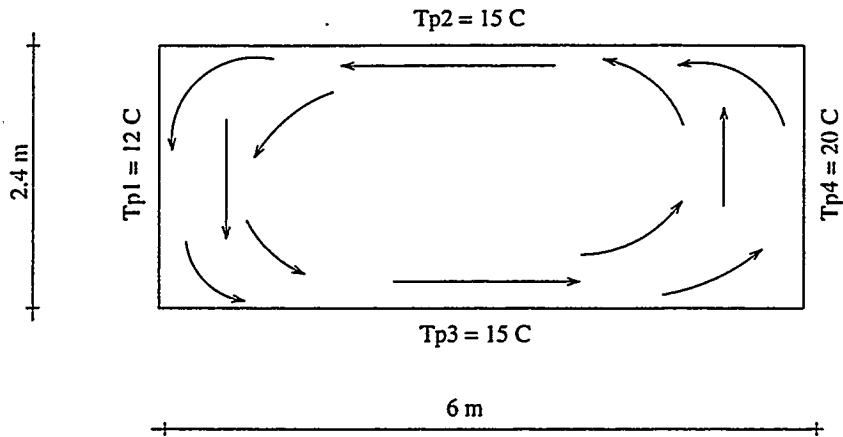


Figure 1: Natural convective flow in the 2-D "window" model

warm wall. The results were compared to runs using the CFD code Fluent [Ina88], which is based on the finite volume method and uses uniform gridding, logarithmic velocity profiles near surfaces, and the  $k - \epsilon$  turbulence model.

Figures 2 and 3 show that the air temperatures for the zonal and CFD models are similar. The maximum difference between the models is 8% along the mid-room horizontal axis and 10% along the mid-room vertical axis.

The zonal model's temperature distribution is more "conductive" than the CFD distribution because the zonal model is diffusive (assumes perfect mixing) and ignores thermal boundary layers.

The agreement between the air flow velocity results (Figures 4 and 5) is less satisfactory than for the temperatures but still acceptable.

The error is above 10% close to the floor and ceiling. Again, the zonal model does less well close to the walls since it does not account for boundary layer effects.

### 4.3 Sensitivity Analysis

We see that changing the grid from 3x3 to 6x6 in the window problem barely changes the results, which indicates that a coarse grid is adequate.

We also tested the sensitivity of the model to the permeability coefficient,  $C$ , and to the wall heat transfer coefficients,  $h$ . The results are given in Figures 6 and 7, which show how the temperature distribution changes with  $C$ , and in Figure 8, which shows how the velocity distribution changes with  $C$ . We see that air temperature and velocity are fairly insensitive to  $C$  and that the best results are obtained with the commonly accepted value of 0.83 [FGG89].

We also found that the results are insensitive to  $h$  (not shown). We conclude that a zonal model with coarse gridding gives acceptable results for the 2-D window problem even with uncertainties in the values of permeability and surface heat transfer coefficients.

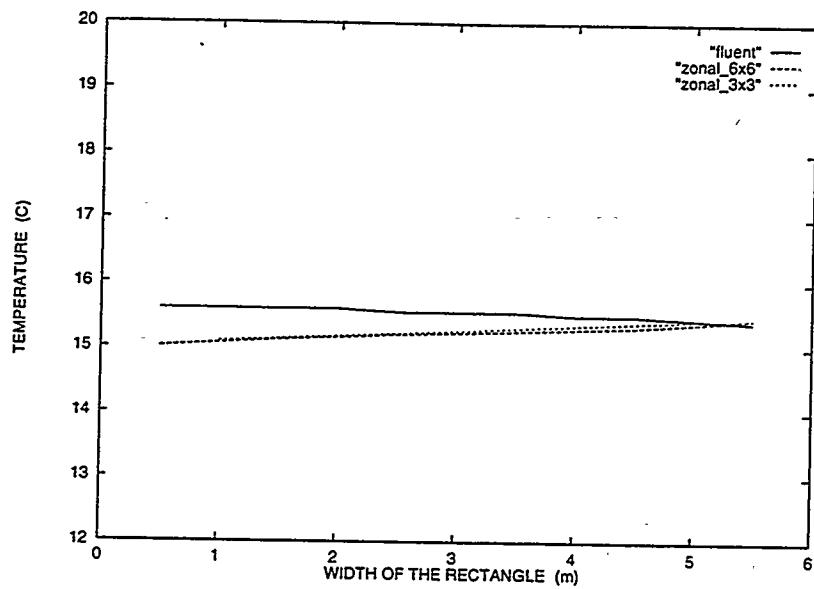


Figure 2: 2-D "window" problem: horizontal distribution of air temperature at mid-height predicted by the zonal model (for 3x3 and 6x6 gridding) and the Fluent CFD calculation.

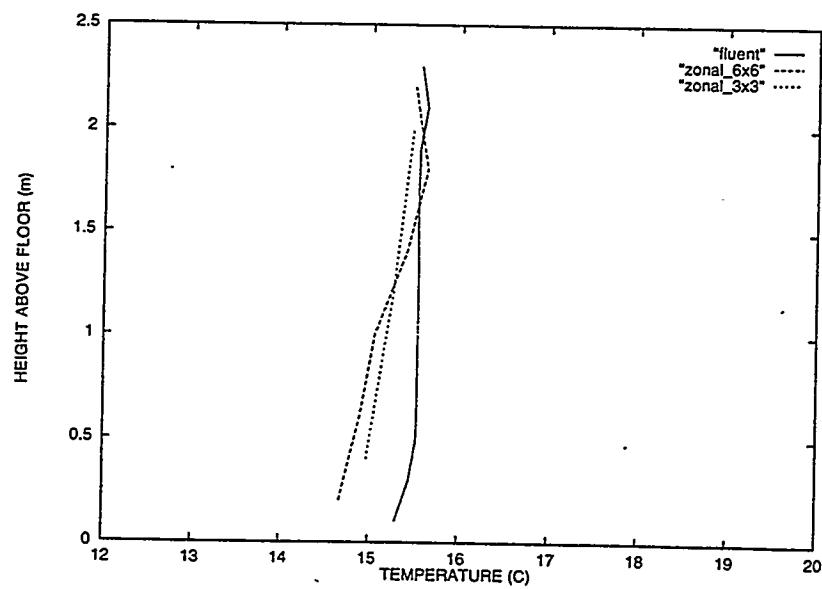


Figure 3: 2-D "window" problem: vertical distribution of air temperature at mid-room predicted by the zonal model (for 3x3 and 6x6 gridding) and the Fluent CFD calculation

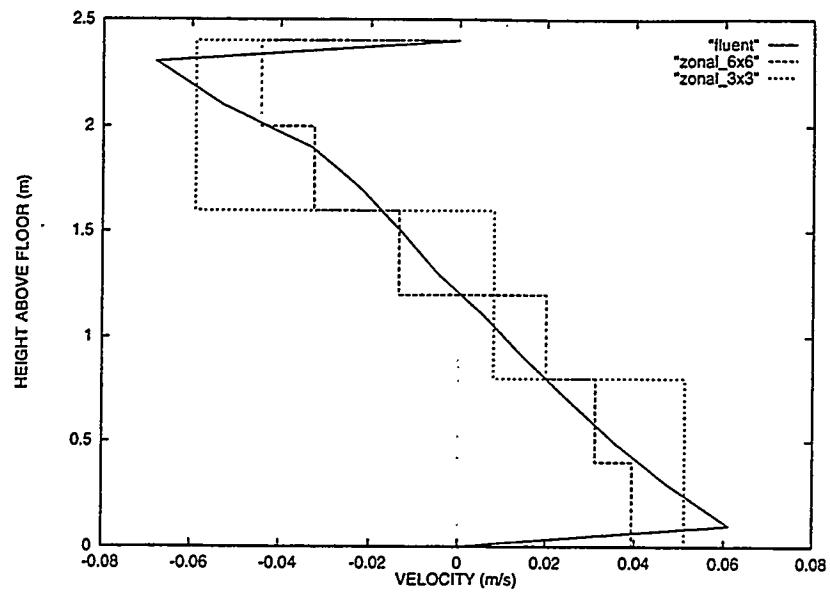


Figure 4: 2-D "window" problem: vertical distribution of horizontal air velocity predicted by the zonal model (for 3x3 and 6x6 gridding) and the Fluent CFD calculation

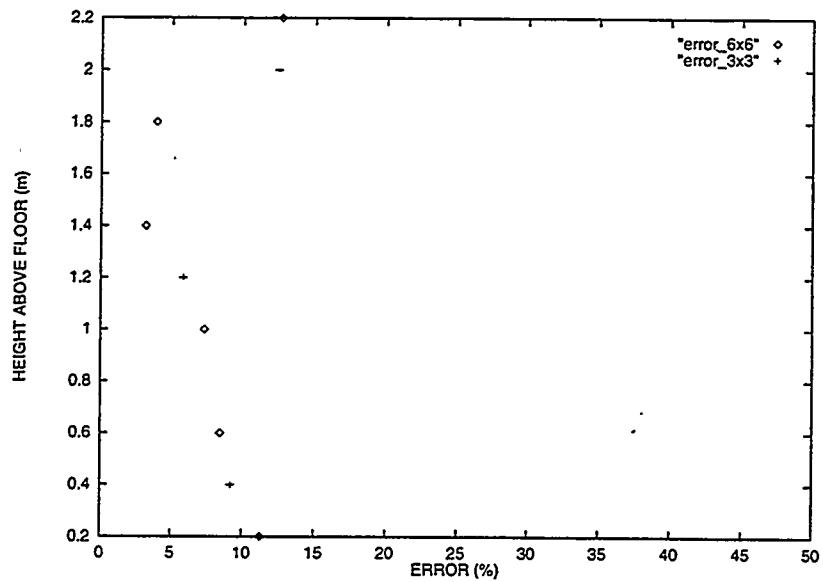


Figure 5: 2-D "window" problem: percent difference in horizontal air flow velocity vs. height above floor between zonal model (for 3x3 and 6x6 gridding) and Fluent CFD calculation

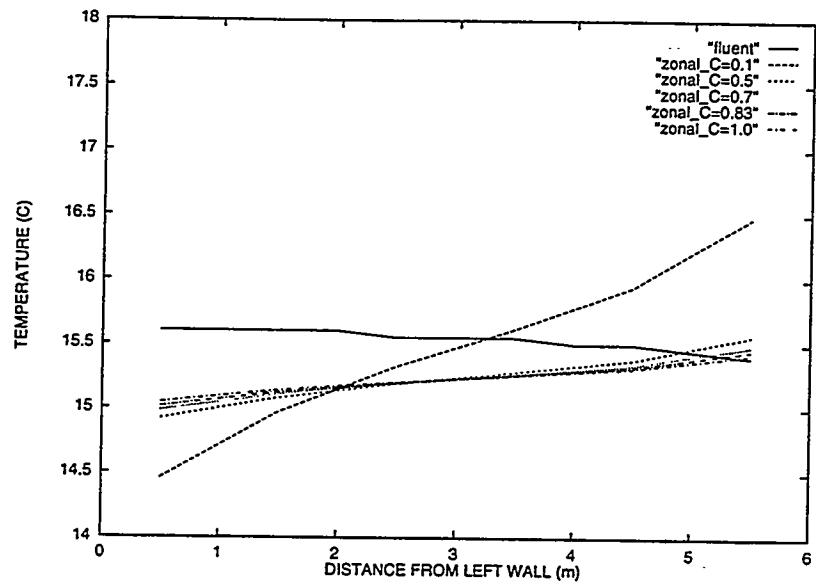


Figure 6: 2D "window problem": Sensitivity to permeability coefficient of the horizontal distribution of air temperature as determined by the zonal model. The prediction of the Fluent CFD model is shown for comparison.

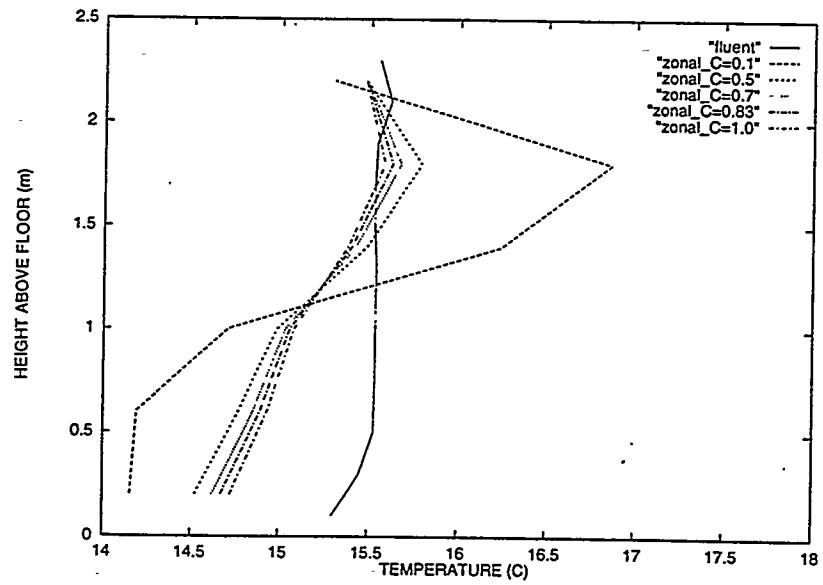


Figure 7: 2D "window problem": Sensitivity to permeability coefficient of the vertical distribution of air temperature as determined by the zonal model. The prediction of the Fluent CDF model is shown for comparison.

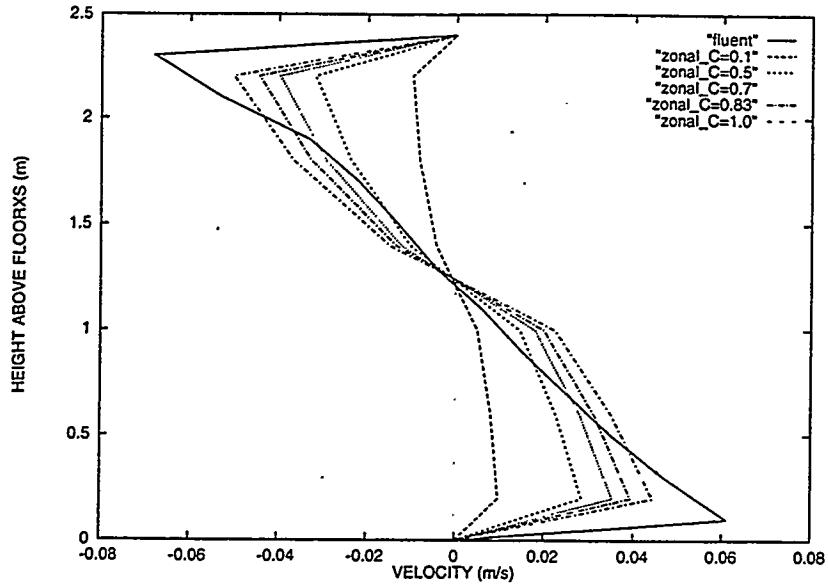


Figure 8: 2D "window problem": Sensitivity to permeability coefficient of the horizontal distribution of vertical air velocity. The prediction of the Fluent CFD model is shown for comparison.

## 5 The 3-D Parallelopiped

### 5.1 Description

A 3-D  $2.6m \times 3.6m \times 2.55m$  cell has the left wall maintained at  $25.5^{\circ}\text{C}$ , the right wall at  $32^{\circ}\text{C}$ , the ceiling at  $26^{\circ}\text{C}$  and the other walls at  $24.5^{\circ}\text{C}$ . The convective heat transfer coefficients at the walls are the same as in the 2-D case.

We chose a grid that was  $4 \times 4 \times 4$ , which produced 2240 equations. With an exponent of 1 in the mass flow equations. SPARK reduced this to 128 equations (a 16 to 1 reduction). Convergence was achieved with a Newton-Raphson relaxation coefficient of 0.5, and by choosing initial values that were close to the final solution.

### 5.2 Validation

The zonal model results were validated numerically and by comparing with experimental results. Numerical validation was done using the Fluent CFD code. A temperature comparison is shown in Figures 9 and 10 and a velocity comparison in Figure 11. The zonal model temperatures are close to the CFD results, and lie between the CFD and measured values. The largest difference between zonal model and measurements, which is about  $2^{\circ}\text{C}$ , occurs near the floor, where the air is cooler and diffusion is smaller. As expected, the difference between the zonal model and measured air velocity is largest near the walls. We found better agreement (not shown) by using smaller zones near the walls.

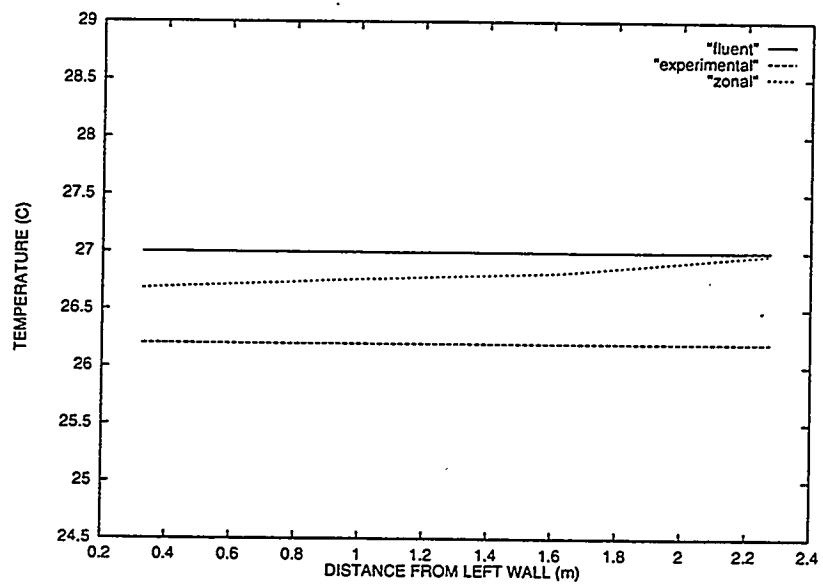


Figure 9: Comparison of the measured horizontal distribution of the air temperature at mid-height with the predictions of the 3-D zonal model and the Fluent CFD calculation.

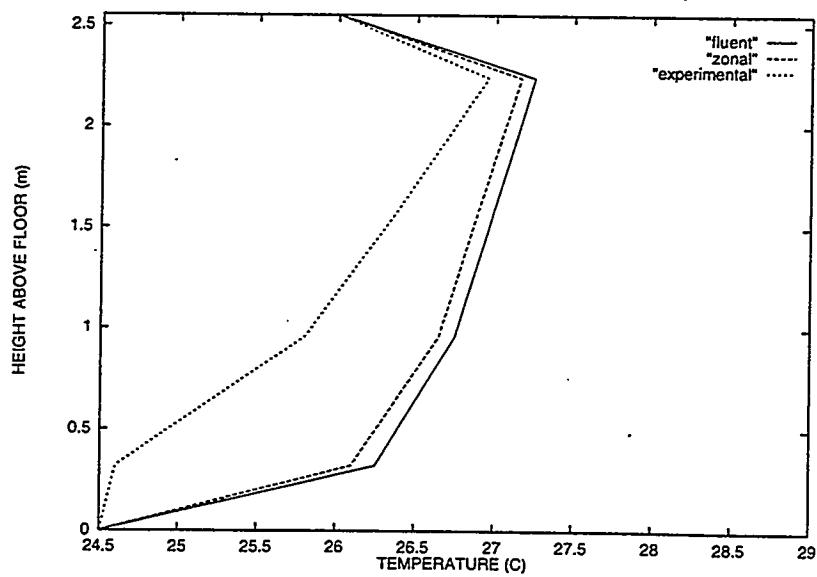


Figure 10: Comparison of the measured vertical distribution of air temperature at room center with the predictions of the 3-D zonal model and the Fluent CFD calculation.

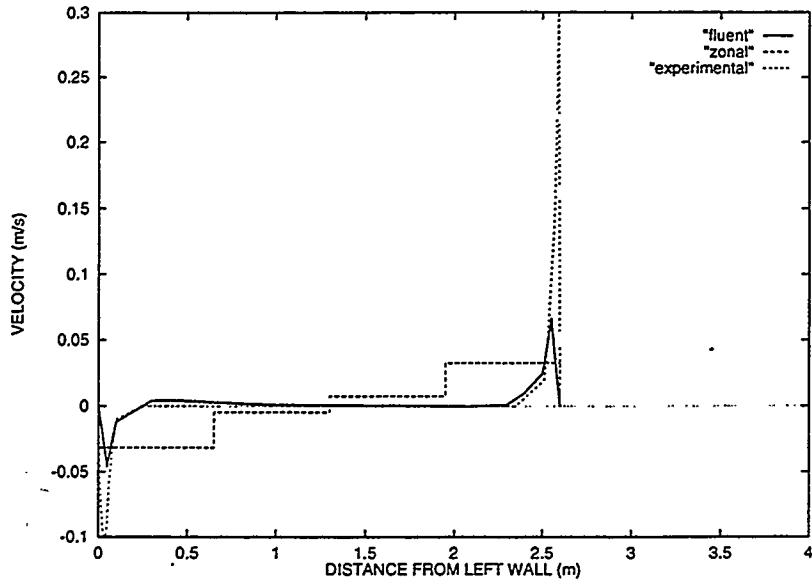


Figure 11: Comparison of the measured horizontal distribution of the vertical air velocity at mid-height with predictions of the zonal model and the Fluent CFD calculation.

## 6 The Minibat Cell

### 6.1 Presentation of the Problem

To test the zonal approach on a more complex problem, we modeled the "Minibat Cell," a test structure at INSA (Institut National des Sciences Appliquées) in Toulouse, France. This  $6.2m \times 3.1m \times 2.5m$  cell is divided into a warm room and a cold room by a partition that has a  $0.77m$  wide by  $1.83m$  high open doorway. The left wall is maintained at  $28.0^\circ\text{C}$ , the right wall at  $22.5^\circ\text{C}$ , the ceiling at  $25.0^\circ\text{C}$  on the warm side and  $24.81^\circ\text{C}$  on the cold side, the floor at  $24.58^\circ\text{C}$  and the other walls at  $24.63^\circ\text{C}$ .

We used a  $6 \times 3 \times 6$  grid, which led to 3744 equations. SPARK reduced this to 216 equations (a 17 to 1 reduction).

### 6.2 Validation

The air temperature distributions calculated by the zonal model on the warm and cold sides are shown in Figures 12 and 13. The air velocity distribution in the doorway is shown in Figure 14. For comparison, these figures also show measured data and the predictions of the StarCD CFD program, which is based on a finite-volume method.

The zonal model's temperature results are satisfactory. They fall, for the most part, between the measured and the CFD values. As in the previous test case, the highest discrepancy occurs near the floor. The overall agreement with measured and CFD results is somewhat better on the warm side of the cell.

The zonal model correctly predicts the qualitative behavior of the air flow in the doorway, but, quantitatively, there are differences up to 25% relative to the measurements. Flows are generally overestimated in the doorway, although the neutral point is correctly calculated. This indicates that better agreement would be obtained by reducing the permeability coefficient in the opening [LIA91].

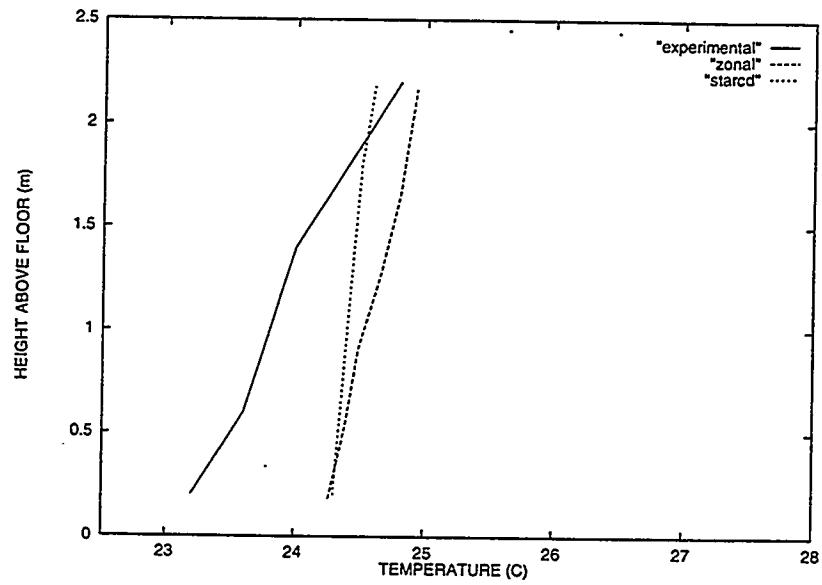


Figure 12: Comparison of the measured vertical distribution of air temperature on the cold side of the Minibat cell with predictions of the zonal model and the StarCD CFD calculation.

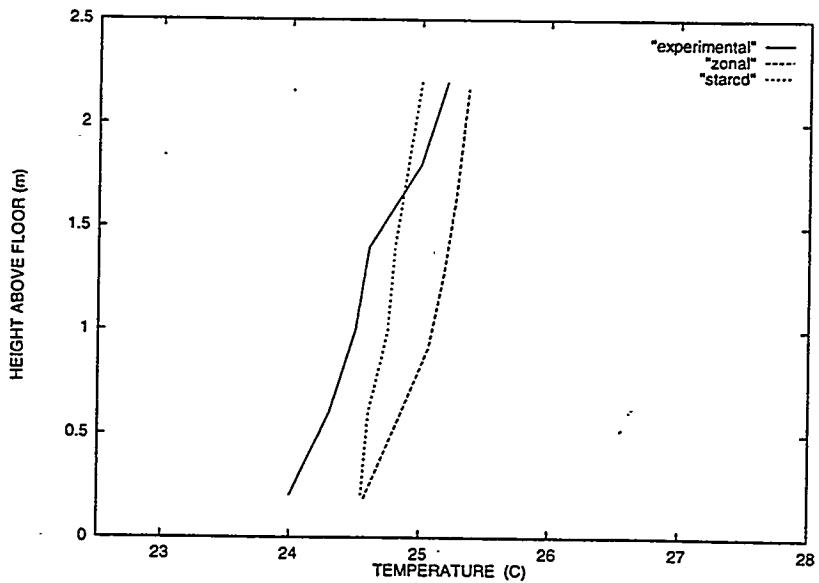


Figure 13: Comparison of the measured vertical distribution of air temperature on the warm side of the Minibat cell with predictions of the zonal model and the StarCD CFD calculation.

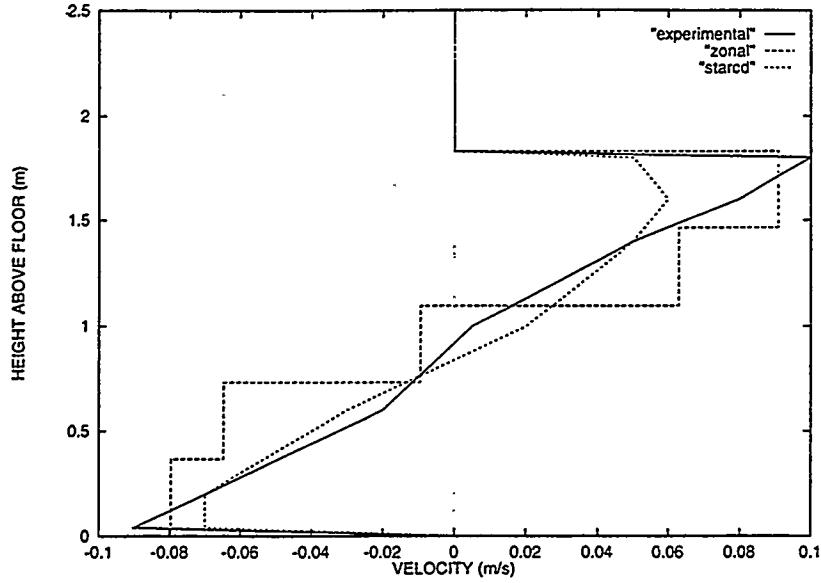


Figure 14: Comparison of the measured vertical distribution of horizontal air velocity in the doorway of the Minibat cell with predictions of the zonal model and the StarCD CFD calculation. Air moving from right to left (from the cold side to the warm side) is considered to have positive velocity.

## 7 Coupling to External Models

Having demonstrated the overall reliability of zonal models, at least for simple rectangular geometries, we demonstrate in this section modularity and reusability in object-based simulation by coupling the zonal model with a comfort model.

### 7.1 Comfort model

We consider a simple, classic comfort model—the Fanger model [Fan73]—which is expressed as

$$CT = H - E - R - C$$

$$PMV = [0.303e^{-0.036M} + 0.028] \times CT$$

Here,  $CT$  is the state of thermal comfort, which is determined by occupant activity level,  $H$ , evaporation rate,  $E$ , radiative heat loss,  $R$ , and convective heat loss,  $C$ .  $PMV$  is the predicted mean vote, for which a zero value of 0 corresponds to feeling comfortable, a positive value to feeling too warm and a negative value to feeling too cold.

Because of the modularity of the SPARK environment, all that was needed to couple the comfort and zonal models was to add the Fanger equations to the zone equations. The results of solving the resulting equation set for the Minibat Cell are shown in Figure 15.

### 7.2 Wall-to-Air coupling

Air flow models should be coupled to realistic wall models. The modularity of the SPARK object-based approach allows wall models to be easily created using the "modal" method

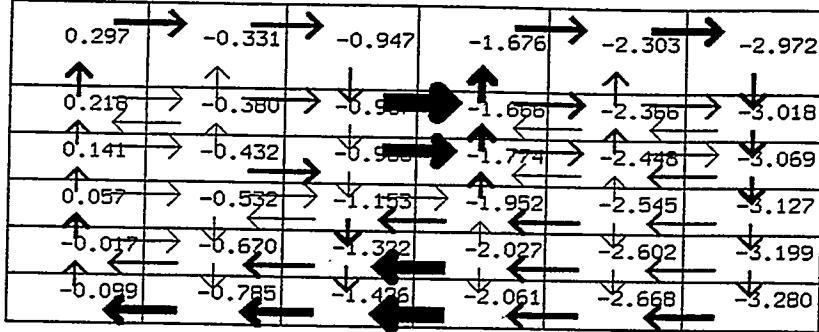


Figure 15: Comfort analysis based on coupling of Fanger model and zonal model: Predicted Mean Vote in vertical-midplane zones of the Minibat Cell. The arrows show air flow between zones.

[FBSN91]. In this method the conduction equations for complex geometries are solved in full and the significant modes are determined. This reduces the complexity of the model with little loss of accuracy.

We incorporated the wall conduction flux from the modal approach into the general energy balance equation for the air zones adjacent to the walls. Given the external conditions, the SPARK solver then determined the surface temperatures as well as the distributions of inside air temperature and air flow.

### 7.3 Coupling to a Hydronic Cooling System

The zonal model was also coupled to an independently developed SPARK simulation of a hydronic radiant cooling system in which the heat transfer to the room air was originally modeled assuming a single air node, i.e., assuming a uniform air temperature [CSW95]. This coupling was accomplished in a straightforward fashion and led to a more accurate model in which the heat transfer from the cooled surfaces to the air took into account the spatial variation of air temperature.

### 7.4 Coupling to Plumes and Jets

The main weakness of zonal models is that they cannot properly represent air jets (from diffusers, for example) or plumes (which are common around heaters), since in these models jets and plumes are (incorrectly) assumed to be fully dissipated in the zone in which they originate. One way around this limitation is to replace zones that contain a jet or plume with a specific jet or plume object. To investigate this possibility we considered the case of a 3-D  $4.75m \times 3m \times 2.5m$  room that had a heater next to a cold wall. A  $6 \times 6 \times 4$  grid was used in which the zonal models for the three zones above the heater were replaced with a plume object. We found in this case that a pure zonal model without a plume object gave unacceptable results (for example, there was an unphysical horizontal diffusion immediately above the heater). However, when a plume object was used a physically reasonable air flow pattern was observed.

## 8 Conclusion and Perspectives

We have shown that, for simple rectangular geometries, the zonal method gives reasonably accurate air flow and air temperature results even in 3-D cases (for which convergence problems are usually encountered when other methods are used). Zonal models are easier to incorporate in modular simulation environments than are CDF models and are much faster executing. However, further work is needed to establish guidelines for optimal partitioning of rooms into zones. In particular, it should be determined whether partitioning can or should be based on the expected flow pattern. Additional effort is also needed to improve the modeling of jets and plumes. It would also be of interest to extend the zonal method to consider moisture and pollutant transport.

## 9 Acknowledgements

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