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Hanford MOX Fuel Lead Assemblies Data Report for the Surplus Plutonium Disposition Environmental Impact Statement

Fissile Materials Disposition Program

MANAGED AND OPERATED BY
LOCKHEED MARTIN ENERGY RESEARCH CORPORATION
FOR THE UNITED STATES
DEPARTMENT OF ENERGY

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Engineering Technology Division

HANFORD MOX FUEL LEAD ASSEMBLIES DATA REPORT FOR THE SURPLUS PLUTONIUM DISPOSITION ENVIRONMENTAL IMPACT STATEMENT

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ACRONYMS

ACL	administrative control level
AEC	U.S. Atomic Energy Commission
AL	analytical laboratory
ALARA	as low as reasonably achievable
ANL–W	Argonne National Laboratory–West (at INEEL)
ARF	airborne release fraction
ASTM	American Society for Testing and Materials
BRET	Breeder Reprocessing Engineering Test
BWR	boiling-water reactor
CAA	Clean Air Act
CCCTF	Core Conduction Cooldown Test Facility
CEDE	committed effective dose equivalent
CERCLA	Comprehensive Environmental Response, Compensation, and Liability Act of 1980
CFA	Central Facilities Area (ANL–W)
CFR	*Code of Federal Regulations*
CH	contact-handled
CMC	confirmatory measurement counter
CMR	Chemistry and Metallurgy Research
CRBR	Clinch River Breeder Reactor
CS	containment and surveillance
CST	Chemical Science and Technology
CWA	Clean Water Act of 1972
D&D	decontamination and decommissioning
D&R	dismantling and rearrangement
dc	direct current
DOE	U.S. Department of Energy
DWPF	defense waste processing facility
EA	environmental assessment
EBR-I	Experimental Breeder Reactor-I
EBR-II	Experimental Breeder Reactor-II
EIS	environmental impact statement
EJ	environmental justice
EPA	Environmental Protection Agency
ER	Environmental Report
ETB	Engineering Test Bay
FAA	Fuel Assembly Area
FCF	Fuel Cycle Facility
FCFS	Fueled Clad Fabrication System
FEMA	Federal Emergency Management Agency
FFTF	Fast-Flux Test Facility
FMEF	Fuels and Materials Examination Facility
FMF	Fuel Manufacturing Facility
FONSI	finding of no significant impact
FR	fire resistive
FTE	full-time equivalent
HAP	hazardous air pollutant
HEPA	high-efficiency particulate air
HEU	highly enriched uranium
HFEF/S	Hot Fuel Examination Facility South
HM	heavy metal

HP	Health Physics
HPFL	High-Performance Fuel Laboratory
HVAC	heating, ventilating, and air conditioning
HWMA	Hazardous Waste Management Act of 1983
I&C	Instrumentation and Controls
IDAPA	Idaho Administrative Procedures Act
IFEL	Irradiated Fuels Examination Laboratory
IFR	Integral Fast Reactor
IMGA	Irradiated Microsphere Gamma Analyzer
INEEL	Idaho National Engineering and Environmental Laboratory
INRAD	Intrinsic Radiation Bay
LA	lead assembly
LACEF	Los Alamos Critical Experiments Facility
LANL	Los Alamos National Laboratory
LLMW	low-level mixed waste
LLRW	low-level radioactive waste
LLW	low-level waste
LLNL	Lawrence Livermore National Laboratory
LMES	Lockheed Martin Energy Systems, Inc.
LMITCO	Lockheed Martin Idaho Technologies Company
LTA	lead-test assembly
LUA	lead-use assembly
LWR	light-water reactor
MAA	Material Access Area
M&C	Metals and Ceramics
MC&A	material control and accountability
MD	Office of Fissile Materials Disposition (DOE)
MFP	multiple fission products
MOX	mixed oxide
MT	metric ton
MW	mixed waste
NDA	nondestructive assay
NDT	nondestructive testing
NEPA	National Environmental Policy Act of 1969
NGVD	National Geodetic Vertical Datum
NMS&S	Nuclear Material Stabilization and Storage Division
NMSS	Office of Nuclear Material Safety and Safeguards
NPDES	National Pollutant Discharge Elimination System
NRC	Nuclear Regulatory Commission
ORNL	Oak Ridge National Laboratory
ORR	Oak Ridge Reservation
PA	protected area
PDAC	pit disassembly and conversion
PF	Plutonium Facility
PFP	Plutonium Finishing Plant
PIDAS	Perimeter Intrusion and Detection Assessment System
PIE	postirradiation examination
PPE	personal protective equipment
PSF	Plutonium Storage Facility
PWR	pressurized-water reactor
QA	quality assurance
R&D	research and development
RAMROD	Radioactive Materials Research, Operations, and Demonstration Facility
RCRA	Resource Conservation and Recovery Act of 1976

RCT	Radiological Control Technician
RF	respirable fraction
RH	remote handled
RLWTF	Radioactive Liquid Waste Treatment Facility
RMAL	Radioactive Materials Analytical Laboratory
ROD	record of decision
RPSF	Radioisotope Power Systems Facility
RSSF	Radioactive Sodium Storage Facility
RSWF	Radioactive Scrap and Waste Facility
S&D	storage and disposition
S&S	safeguards and security
SAF	secure automated facility
SCDHEC	South Carolina Department of Health and Environmental Control
SEM	scanning electron microscope
SIP	Space Isotope Program
SNF	spent nuclear fuel
SNFM	spent nuclear fuel material
SNM	special nuclear material
SPSP	Space Power Systems Project
SRS	Savannah River Site
SRTC	Savannah River Technology Center
SST	safe secure transport
TA	Technical Area
TAP	toxic air pollutant
TEDE	total effective dose equivalent
TREAT	Transient Reactor Test Facility
TRU	transuranic
TSCA	Toxic Substances Control Act
TSDF	treatment, storage, and/or disposal facility
UBC	Uniform Building Code
USF	Uranium Solidification Facility
W	Westinghouse
WAG	Waste Area Group
WCL	Waste Characterization Laboratory
WCRRF	Waste Characterization, Reduction, and Repackaging Facility
WG	weapons grade
WIPP	Waste Isolation Pilot Plant
WOC	White Oak Creek
WRAP	Waste Receiving and Processing Plant
WSRC	Westinghouse Savannah River Company
ZPPR	Zero Power Physics Reactor

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ABSTRACT

The purpose of this document is to support the U.S. Department of Energy (DOE) Fissile Materials Disposition Program's preparation of the draft surplus plutonium disposition environmental impact statement. This is one of several responses to data call requests for background information on activities associated with the operation of the lead assembly (LA) mixed-oxide (MOX) fuel fabrication facility.

The DOE Office of Fissile Materials Disposition (DOE-MD) has developed a "dual-path" strategy for disposition of surplus weapons-grade plutonium. One of the paths is to disposition surplus plutonium through irradiation of MOX fuel in commercial nuclear reactors. MOX fuel consists of plutonium and uranium oxides (PuO_2 and UO_2), typically containing 95% or more UO_2.

DOE-MD requested that the DOE Site Operations Offices nominate DOE sites that meet established minimum requirements that could produce MOX LAs. Six initial site combinations were proposed: (1) Argonne National Laboratory–West (ANL–W) with support from Idaho National Engineering and Environmental Laboratory (INEEL), (2) Hanford, (3) Los Alamos National Laboratory (LANL) with support from Pantex, (4) Lawrence Livermore National Laboratory (LLNL), (5) Oak Ridge Reservation (ORR), and (6) Savannah River Site (SRS). After further analysis by the sites and DOE-MD, five site combinations were established as possible candidates for producing MOX LAs: (1) ANL–W with support from INEEL, (2) Hanford, (3) LANL, (4) LLNL, and (5) SRS. Pantex was removed as a supporting organization to LANL because Pantex did not have facilities available that met the desired programmatic criteria. One of the criteria was that existing buildings would be used for the mission. Pantex had no available existing buildings that it was willing to propose for this limited mission. ORR was removed by DOE-MD from consideration because it lacked adequate Safeguards and Security (S&S) Category I facilities, which would limit the quantity of material that could be processed at a given time.

Hanford has proposed an LA MOX fuel fabrication approach that would be done entirely inside an S&S Category I area. An alternate approach would allow fabrication of fuel pellets and assembly of fuel rods in an S&S Category II or III facility, with storage of bulk PuO_2 and assembly, storage, and shipping of fuel bundles in an S&S Category I facility. In all, a total of three LA MOX fuel fabrication options were identified by Hanford that could accommodate the program. In every case, only minor modification would be required to ready any of the facilities to accept the equipment necessary to accomplish the LA program.

A commercial reactor operator has not been identified for the LA irradiation. Postirradiation examination (PIE) of the irradiated fuel will take place at either Oak Ridge National Laboratory or ANL–W. The only modifications required at either PIE site would be to accommodate full-length irradiated fuel rods.

Results from this program are critical to the overall plutonium distribution schedule.

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1. INTRODUCTION AND SCHEDULE

As part of the overall mission to disposition weapons-grade (WG) plutonium as fuel for commercial nuclear power plants, a lead assembly (LA) program is needed to qualify mixed-oxide (MOX) fuel as a safe and reliable fuel. The LA program will provide key data regarding the performance of MOX fuel in U.S. commercial reactors and supply information needed to modify current U.S. Nuclear Regulatory Commission (NRC) licenses. The program will also provide information necessary to validate and verify computer codes used in the reactor core design and accident analyses. In addition to qualifying the MOX fuel and validating and verifying the codes, the LA program will serve to verify that the United States can indeed execute each technical step necessary in the process of dispositioning plutonium as MOX fuel, except NRC licensing of facilities.

A simplified diagram showing each of the required process steps for the LA program is shown in Fig. 1. The LA program will include every step needed to complete the reactor portion of the plutonium disposition mission (including transportation and storage), with the exception of placement of the spent fuel in the geologic repository. In all likelihood, some of the LA program MOX fuel bundles will make their way to the geologic repository, but subsequent disposal in the repository is analyzed in other environmental documents. Detailed descriptions of the process required to fabricate MOX fuel, irradiate the fuel, and perform postirradiation examinations (PIE) of the spent fuel will be provided in Chaps. 3 and 10.

As previously stated, the goals of the LA program are to qualify the MOX fuel, confirm codes, and demonstrate that the United States can perform the steps necessary to disposition plutonium using MOX fuel. For the LA program these steps start with receipt of acceptable plutonium oxide (PuO_2) that is derived from "pits" and processed in the United States. At each step in the process, safeguards and security (S&S) measures, material control and accountability (MC&A) measures, transportation issues, storage issues, and material handling issues will be addressed. As shown in Fig. 1, the PuO_2 is mixed and blended with

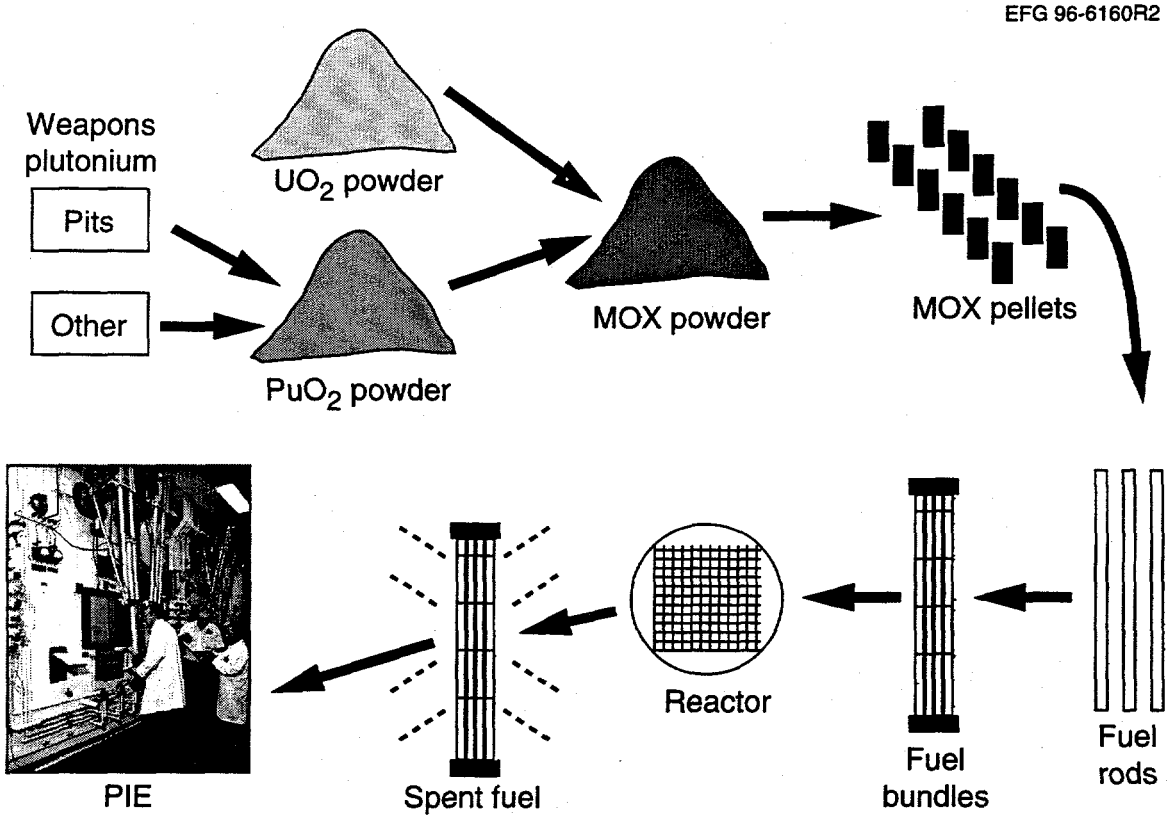

Fig. 1. Simplified LA process diagram.

uranium oxide (UO_2) to arrive at the fissile content requested by the utility fuels engineer. Pellets are then pressed, sintered, and assembled into rods. The rods are then assembled into fuel assemblies and packaged for shipping to the reactor site for irradiation. After irradiating the fuel for one cycle, some of the rods are removed from the irradiated assemblies and taken to a laboratory for PIE. Additional rods will be removed after the second, third, and fourth cycles (if the chosen reactor has a third and fourth cycle), and PIE will be performed to confirm that the structural integrity of the MOX fuel, cladding, and assembly materials is maintained and that the computer codes accurately predict the fuel performance and evolution of fission products.

Figure 2 shows the anticipated schedule for the LA program relative to the plutonium disposition mission. Los Alamos National Laboratory (LANL) is currently developing the processes necessary to fabricate MOX fuel. The U.S. Department of Energy Office of Fissile Materials Disposition (DOE-MD) plans to choose a consortium before the end of 1998 to disposition excess plutonium using reactors, at which time this consortium will choose the DOE site(s) and associated facilities to fabricate the LA MOX fuel. At that same time the consortium will begin design, licensing, and construction of the mission MOX fuel fabrication facility. The fabrication process used for the LAs will be as close as possible to that of the MOX fabricator in the consortium. Fabrication of the LA MOX fuel will begin in late 2002. The first LAs [shown as lead test assemblies (LTAs) in Fig. 2] will be available for insertion in a commercial reactor in late 2003. PIE will begin 6 months after completion of the first reactor cycle with results available by the end of the second LA reactor cycle. After two LA cycles (18–24 months per cycle), the mission MOX fuel fabrication will begin if the PIE produces satisfactory confirmation of fuel performance. PIE will be done after each LA reactor cycle to ensure that fuel performance meets or exceeds expected results. Table 1 provides the schedules associated with the design, modification, operation, decontamination and decommissioning (D&D), and/or conversion of the LA MOX fuel fabrication facility. Table 2 provides the time frames associated with the LA testing.

To maintain LA fabrication capability, should it be needed for any reason, the LA fuel fabrication facility will be maintained in standby for 4 years between the end of the facility's scheduled operation and its scheduled D&D. During this time the capability to produce lead assemblies will be maintained.

A maximum of ten LAs will be produced to meet the LA program mission goals. Table 3 provides the anticipated quantities of constituent materials that will be needed annually and in total to complete the LA program. Several assumptions were made to arrive at the quantities in Table 3, and these are listed in Table 4.

A total of four assemblies are anticipated to be required for use as LAs in the chosen mission reactor. It is possible a second set of four LAs will be needed for either a second reactor or for use in the same reactor. In addition, sufficient rods will be produced to assemble two archive LAs.

A total of eight LA MOX fuel assemblies will be temporarily stored in the LA fabrication facility until they are shipped to the reactors for irradiation. The rods for the two remaining assemblies, and possibly the MOX rods from four assemblies not used, will be retained in the LA shipping and storage area as archive rods. These archive rods will be used if needed as replacement rods in the reactor or they may be used for tests of the LA MOX fuel fabrication process. If they are not needed, or until they are needed, these rods will be stored at the LA MOX fuel fabrication facility until the end of that facility's mission. The LAs will then be shipped to the mission MOX fabrication facility for storage until the end of the Fissile Materials Disposition Program, at which time they will either be retained by the consortium as active rods, or irradiated in a mission reactor.

Due to the uncertainty associated with the final design of the LA MOX fuel, the assemblies may consist of either all MOX fuel rods or a combination of low-enriched uranium (LEU) and MOX rods. A bounding approach was taken in considering environmental impacts. The bounds that were considered for this report were based on the number of MOX fuel rods per assembly. A lower bound of one-third of the fuel rods being MOX rods results in the need to ship the remaining two-thirds of the required LEU rods to the LA fuel fabrication facility. The upper bound of all MOX rods in the assembly provides the bounding case for resource needs, safety considerations, accident analyses, and postirradiation examination.

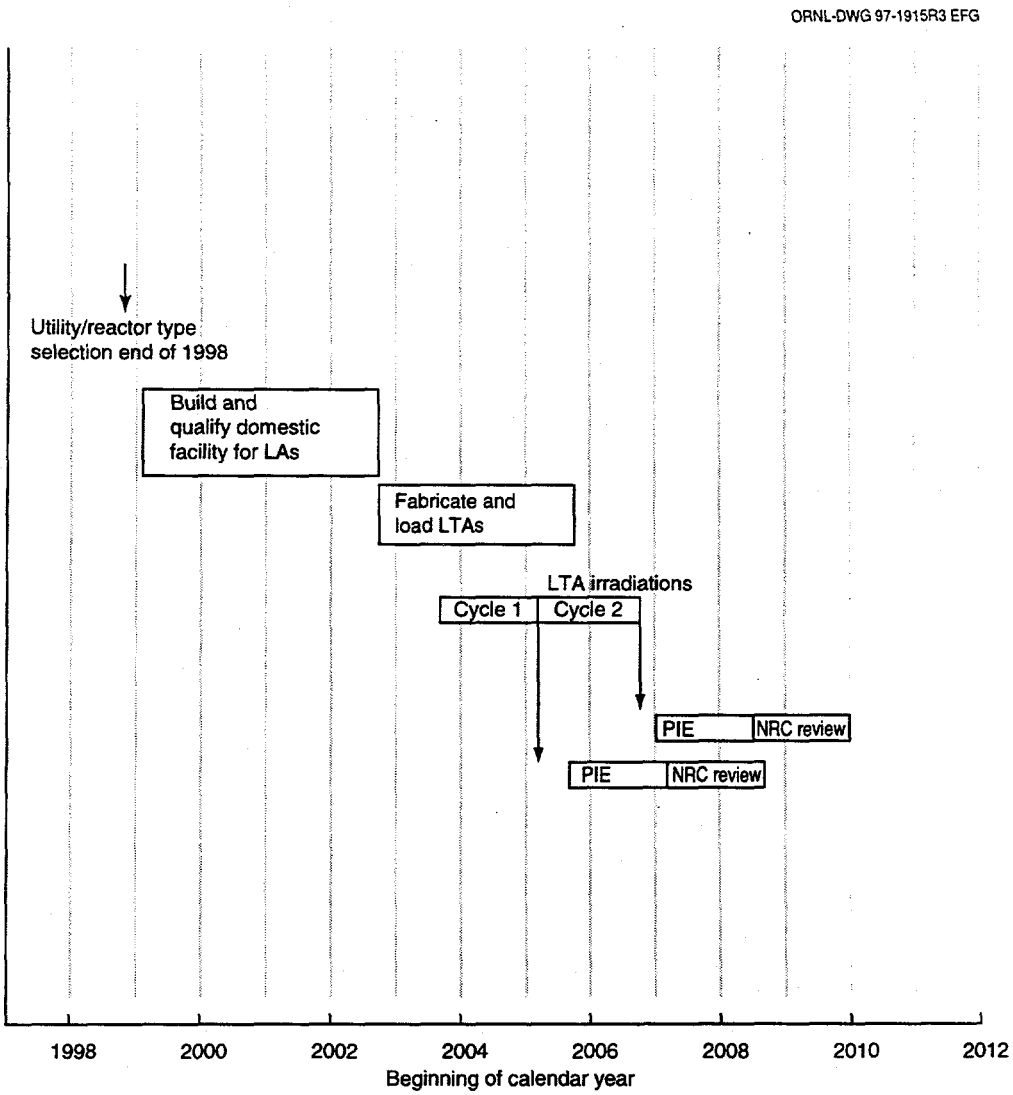

Fig. 2. LA program schedule.

Table 1. LA fabrication facility schedule

Activity	Time frame (beginning and end)
Equipment procured	June 2000–December 2001
Facility design	February 1999–January 2001
Facility permitting	January 2000–January 2002
Facility modification	January 2000–February 2002
Facility startup	February 2002–October 2002
LA fabrication (operation)	October 2002–October 2005
LA fabrication facility standby	October 2005–January 2010
D&D and/or conversion phase	January 2010–January 2013

Table 2. LA testing schedule

Activity	Time frame (beginning and end)
Irradiation	September 2003–October 2006
Removal (cooldown)	March 2005–October 2006 (6 months cooldown after removal before PIE, March 2005–April 2007)
PIE	September 2005–October 2008 (about 18 months for PIE for each reactor cycle)

Table 3. LA MOX fuel material requirements

Material	Startup requirement	Startup scrap/recyclable	Maximum annual requirement	Maximum annual scrap/ recyclable	Total quantity
Plutonium, kg heavy metal (HM)	21	13	120	20	321
Depleted uranium, kg HM	867	250	2,400	400	6,867
Pellets	221,760		532,224		1,552,320
Rods	440		1,162		3,344
Bundles			4		10

Note: In the event LEU rods are used in place of some MOX rods in the assembly, the total quantities of plutonium will be reduced by the amount of LEU introduced. The maximum contribution of LEU rods is two-thirds of the total assembly rods.

Table 4. Assumptions made to determine LA MOX fuel material requirements

1. Material and process requirements are based on producing pressurized-water reactor (PWR) fuel.
2. PuO_2 powder will meet the American Society for Testing and Materials (ASTM) specification C 757-90 as received.
3. Depleted UO_2 powder will meet the ASTM specification as received.
4. Depleted UO_2 (no PuO_2) will be used to perform all system shakedown tests before introducing plutonium.
5. Table 3 is in terms of HM. The factor for converting PuO_2 and depleted UO_2 to HM is 88%.
6. All waste plutonium will be canned and sent to the Immobilization Program for final disposition.
7. All plutonium scrap will be recycled using a dry process.
8. All liquid wastes generated are ancillary to the base process (i.e., laundry, mop water, etc.).
9. Sintering furnaces will stay at temperature during the entire 3-year mission and 1-year startup.
10. Sintering furnaces will be purged with a mixture of argon and 6% hydrogen at a rate of 10 L/min.
11. Powder glove boxes will be purged with nitrogen to reduce the potential for oxidizing UO_2.
12. All calculated numbers have a precision of no more than two significant figures.
13. Homogenization of the PuO_2 will be done at the LA fuel fabrication facility, as will gallium removal operations.

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2. SITE MAP AND PROPOSED LA FACILITY DESCRIPTIONS

2.1 HANFORD SITE LOCATION

The Hanford Site is a 1450-km^2 (560-mile^2) tract of semiarid land in the Columbia River Basin in southeastern Washington State. It is ~80 km (50 miles) north of the Oregon border. Much of the last free-flowing stretch of the Columbia River in the United States is within the Hanford site boundary. The majority of the site is located west and south of this section of the river, which is commonly called the Hanford Reach. Originally, the U.S. Government acquired 1605 km^2 (620 mile^2) of publicly and privately owned land for Hanford Site use. Several parcels of land have been released, reducing the site to its present size. Figure 3 is a map of the Hanford Site.[1]

2.2. DISCUSSION OF FACILITY OPTIONS

The Hanford site has proposed two facilities that meet the necessary criteria to perform the Lead Assembly mission. These are the Fuel Assembly Area (FAA) portion of the Fuels and Materials Examination Facility (FMEF) in the 400 Area and the 325 Building in the 300 Area. These facilities were proposed with special nuclear material (SNM) content limited to Category II amounts. Both of these Category II options include the use of the 2736-Z Vaults at the Plutonium Finishing Plant (PFP) in the 200 West Area to receive and store Category I quantities of plutonium feed materials and completed fuel assemblies.

In addition, feedback from the Site Evaluation Board recognized that the FMEF and FAA could also support LA fabrication involving Category I quantities of plutonium. There are two possible locations within the FMEF/FAA where storage could occur. In one case, the operating vault in the 427 Building would be used. The other possibility is to reconfigure some of the existing, below-grade storage tubes in the FAA to accommodate feed plutonium storage.

2.2.1 Fuel Assembly Area

The Fuel Assembly Area (FAA) is appended to the southeastern end of the Fuels and Materials Examination Facility (FMEF) located in the 400 Area (see Figs. 4 and 5). The FAA shares a common wall on the west with the FMEF entry wing. The 32 m by 55 m (104 ft by 181 ft) lower level provides the space for fuel pin, target pin, and assembly fabrication. Included are areas for storage of powder, pellets, pins, and completed assemblies. This area also contains the electrical switchgear for the entry wing and one of two FMEF uninterruptible power supplies. The upper level contains independent ventilation equipment for the FAA and the entry wing.

The FMEF consists of several connected buildings. Building 427, a six-level processing building, is the main structure of the facility, with an attached single-level mechanical wing on the west side and an emergency power wing at the northwest corner, which also provides emergency electrical power to the FAA. The other building within the FMEF complex is a two-level building (Building 4862), which is connected on the south side of the process building. Building 4862 is divided into two portions: the administrative portion, known as the entry wing; and the operations portion, designed as the FAA for fabrication of fuel and test assemblies for the Fast Flux Test Facility.

In 1991, an extensive engineering study was performed that addressed fabrication of MOX fuel for the Fast Flux Test Facility in the FAA. That study included preparation of a preliminary safety analysis report that covered the following major activities:

- receiving fuel (powder and pellets) pins and fuel assemblies;
- fuel material storage;
- receiving nondestructive assay of fuels and waste materials;
- fuel pellets fabrication;
- driver fuel pin loading, end cap welding, pin finishing, and inspection;
- limited test fuel pin fabrication; and
- driver fuel assembly inspection.

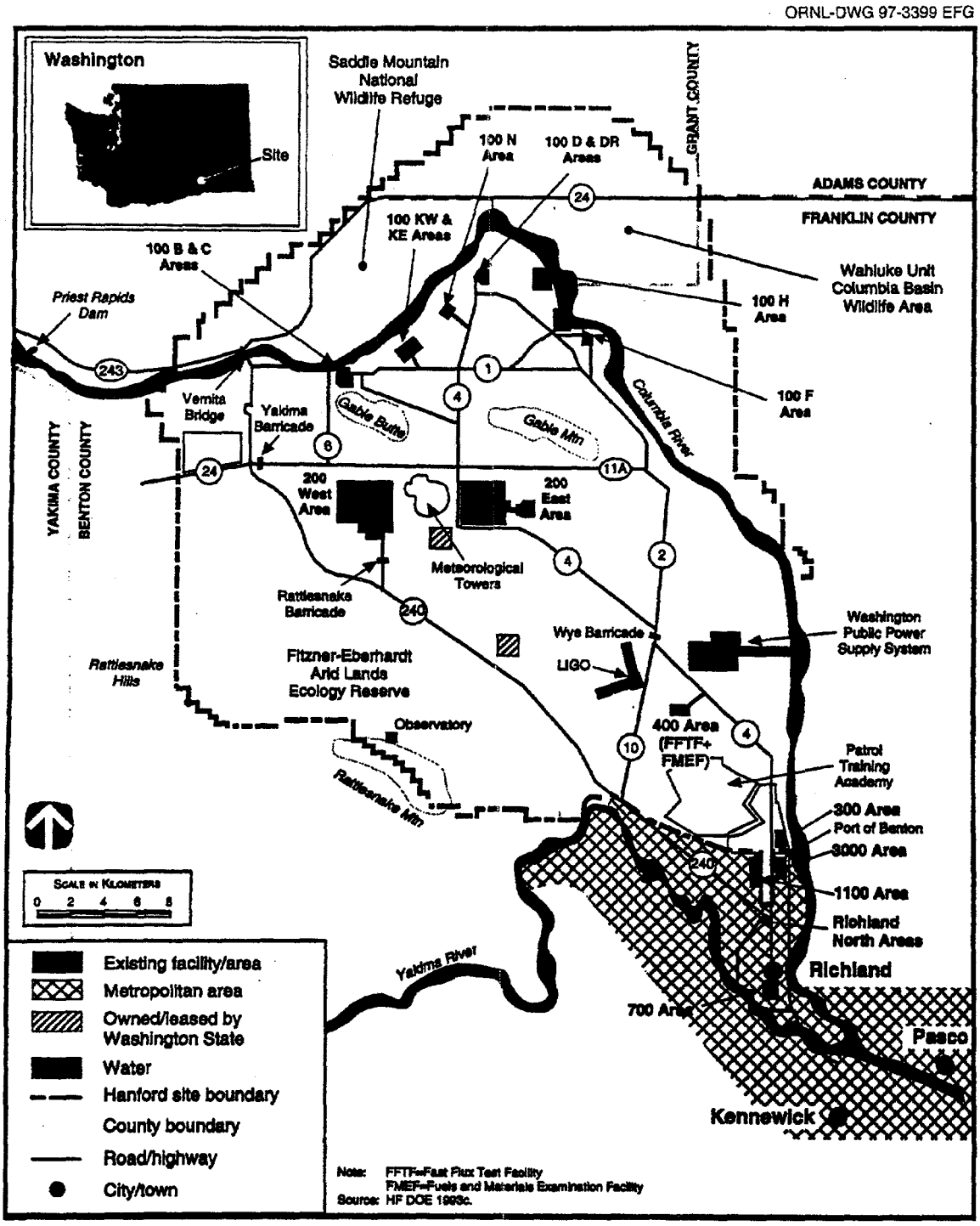

Fig. 3. Hanford site map. *Source: Storage and Disposition of Weapons-Usable Fissile Materials Final Programmatic Environmental Impact Statement*, Vol. 1, DOE/EIS-0229, U.S. Department of Energy, December 1996.

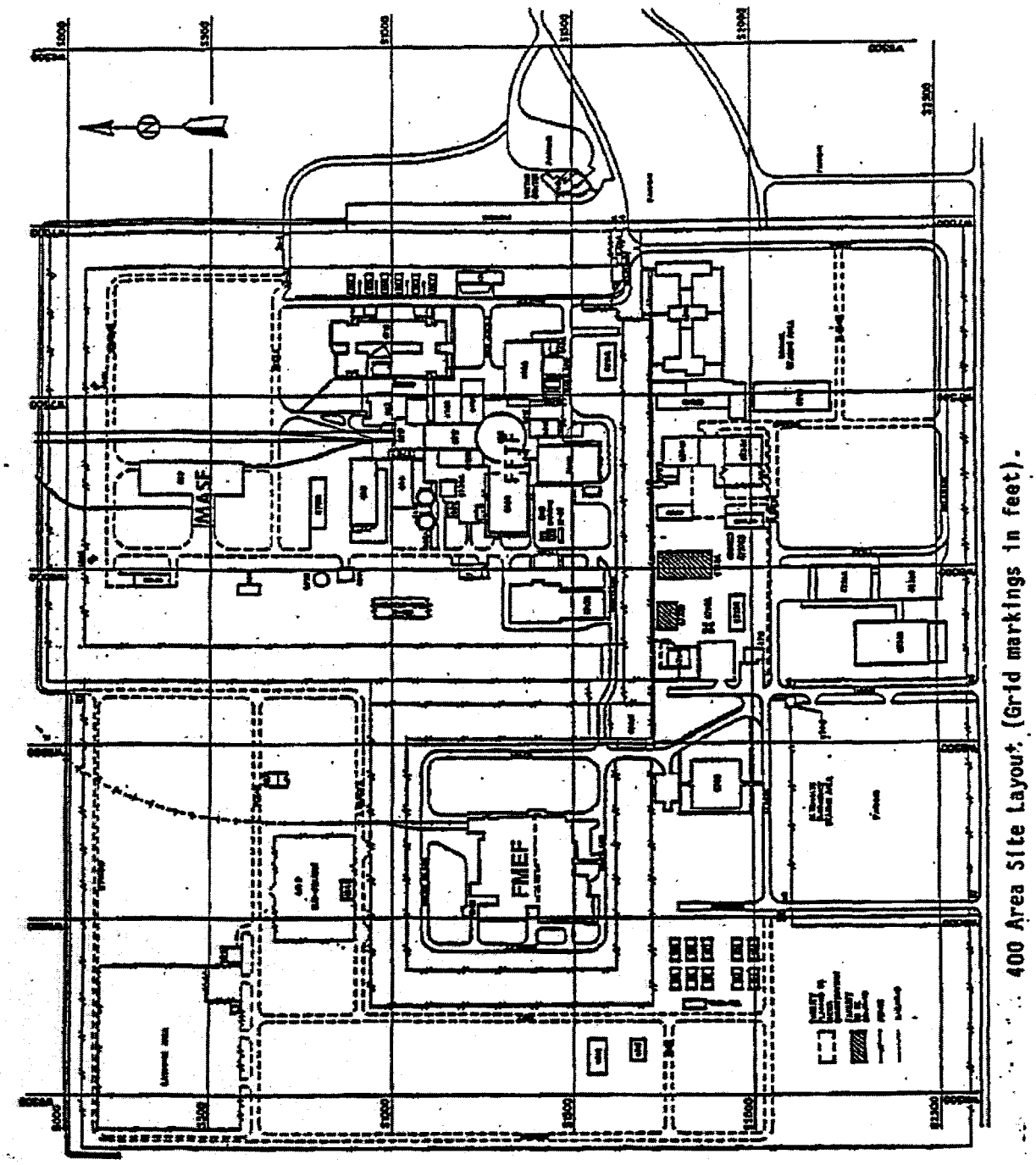

Fig. 4. 400 Area site layout (grid markings in feet).

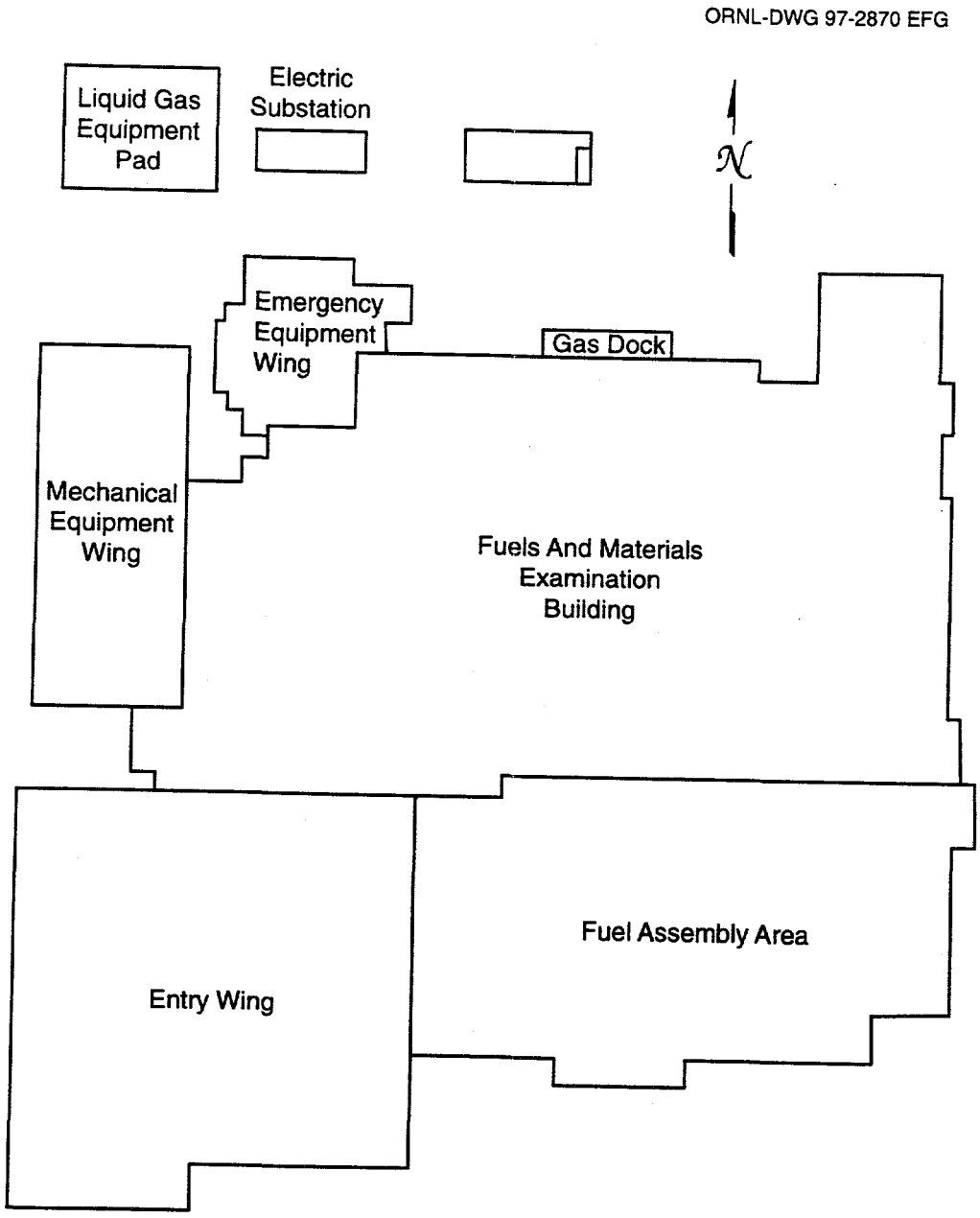

Fig. 5. Main Fuels and Materials Facility structures.

2.2.2 Building 325

Building 325, located in the 300 Area of the Hanford Site (Fig. 6), was designed to provide space for radiochemical research to support projects and programs being carried out at Hanford. Building 325 houses laboratories and specialized facilities designed for work with nonradioactive materials, microgram-to-kilogram quantities of fissionable materials, and up to megacurie quantities of other radionuclides.

Building 325 consists of (1) a central portion (completed in 1953) that contains general-purpose laboratories modified for low-level radiochemical work; (2) a south (front) wing that contains office space, locker rooms, a lunchroom, and maintenance shops; and (3) east and west wings that provide shielded enclosures with remote manipulators for high-level radiochemical work. The exhaust fans and final stages of the high-efficiency particulate air (HEPA) filters are housed in a detached structure along the west side of the building at the north end (filter addition area). The waste tank vault, which is below ground level along the east side of the building, has been used to store contaminated solutions. A back dock contains a gas cylinder dock and gas manifolds.

The central portion of the building is 59.1 m by 59.8 m (194 ft by 196 ft) on three floors (basement, ground, and second) and contains over 100 laboratories and offices. The second floor and basement also house mechanical areas (supply fans, switchgear, steam lines, etc.). The south wing is 22.6 m by 40.5 m (74 ft by 133 ft) on two floors and contains offices, a conference room, a machine shop, a lunchroom, and rest rooms. The east wing (325A), housing the high-level radiochemistry facility, truck lock, and manipulator repair, is 14.6 m by 39.6 m (48 ft by 130 ft) with a 12.2-m by 12.8-m (40-ft by 42-ft) service area/truck lock addition. The west wing (325B) is 16.2 m by 16.5 m (53 ft by 54 ft) and houses the shielded analytical laboratory (Fig. 7).

2.2.3 Plutonium Finishing Plant Vaults

The 2736-Z Building plutonium storage vaults and two ancillary structures are part of a group of buildings called the Plutonium Finishing Plant (PFP). The PFP is a group of buildings located in an enhanced security portion of the 200 West Area (Fig. 8). The center of the PFP is Building 234-5Z, a multilevel industrial structure that was built in 1949–1950 (Fig. 9). The 2736-Z Vaults are located immediately south of Building 234-5Z and provide ~8224 storage spaces for plutonium. Building 2736-Z is approximately 65 ft long by 56 ft wide by 11.5 ft high. The 2736-Z storage complex structures are reinforced concrete and were designed to 0.25 g design-basis earthquake seismic design criteria, compared to the current site requirement of 0.20 g. Ventilation for 2736-Z is supplied by fans located in Building 2736-ZB, room 602. These two fans, running simultaneously, supply 12,000 ft^3/min of air to 2736-Z. Automatically adjusted dampers control the air supply to each room in 2736-Z. Exhaust ventilation for 2736-Z is supplied by two exhaust fans located in Building 2736-ZA. These fans, running simultaneously, provide an exhaust flow rate of 12,000 ft^3/min through the 296-Z-5 stack projecting 30 in. above 2736-ZA. Air discharged from 2736-Z passes through two stages of high-efficiency particulate air (HEPA) filtration.

The PFP support services include the following:

- SNM shipping and receiving;
- nondestructive assay for SNM receipt and nuclear material accountability;
- heating, ventilating, and air conditioning (HVAC) service building;
- analytical laboratory (within the plant);
- developmental laboratory (within the plant);
- maintenance shops (within the plant);
- fabrication shops;
- administrative offices;
- security features;
- medical services;
- fire protection;
- steam and water; and
- electrical power.

PFP is an active, fully staffed, and qualified facility that presently handles Category I quantities of plutonium. Total headcount billing against PFP is $95 million (~615) people). Sufficient operational floor space is available to accommodate the shipping and receiving and storage functions required to support the LTA work.

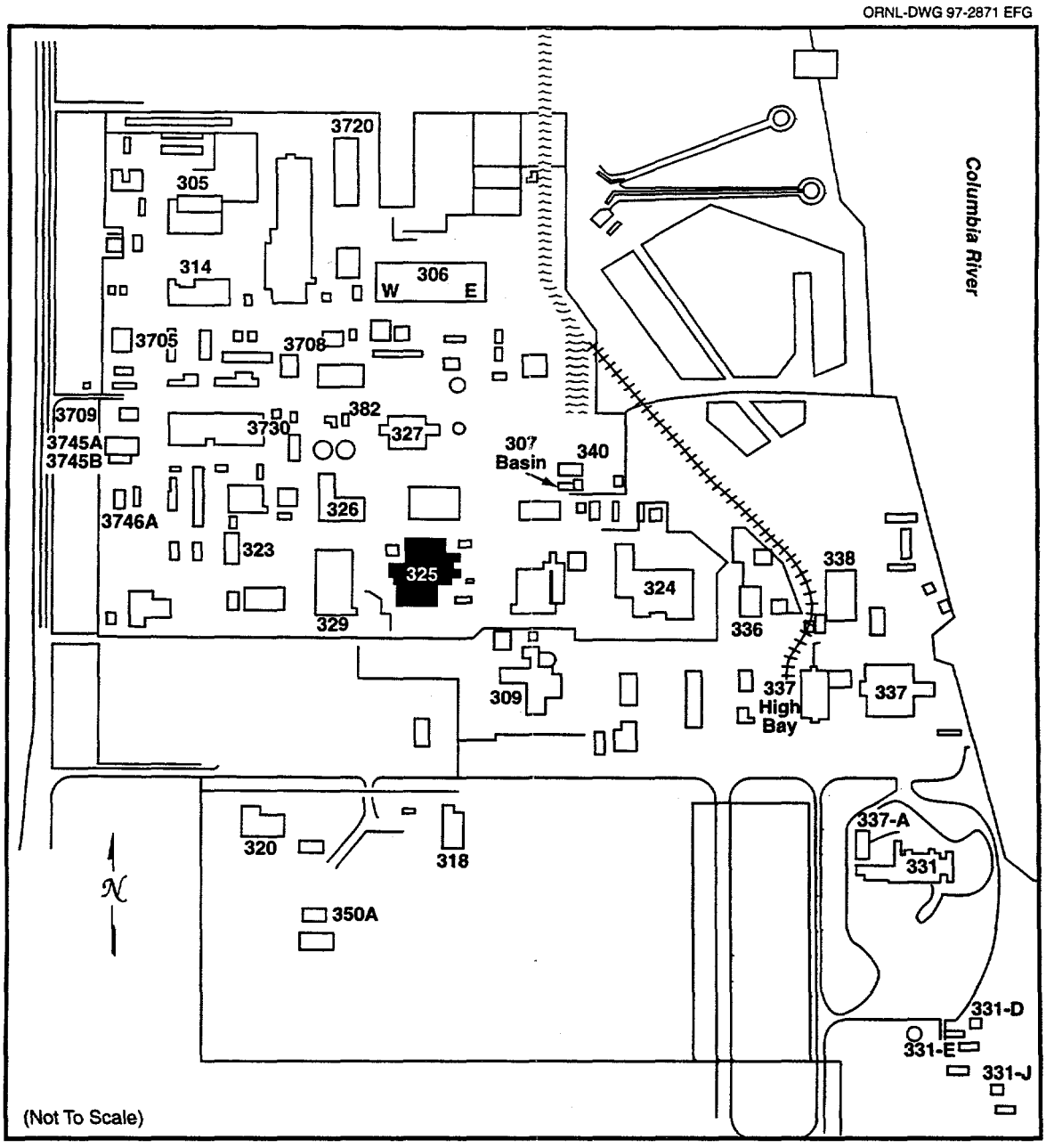

Fig. 6. Location of Building 325 in the 300 Area.

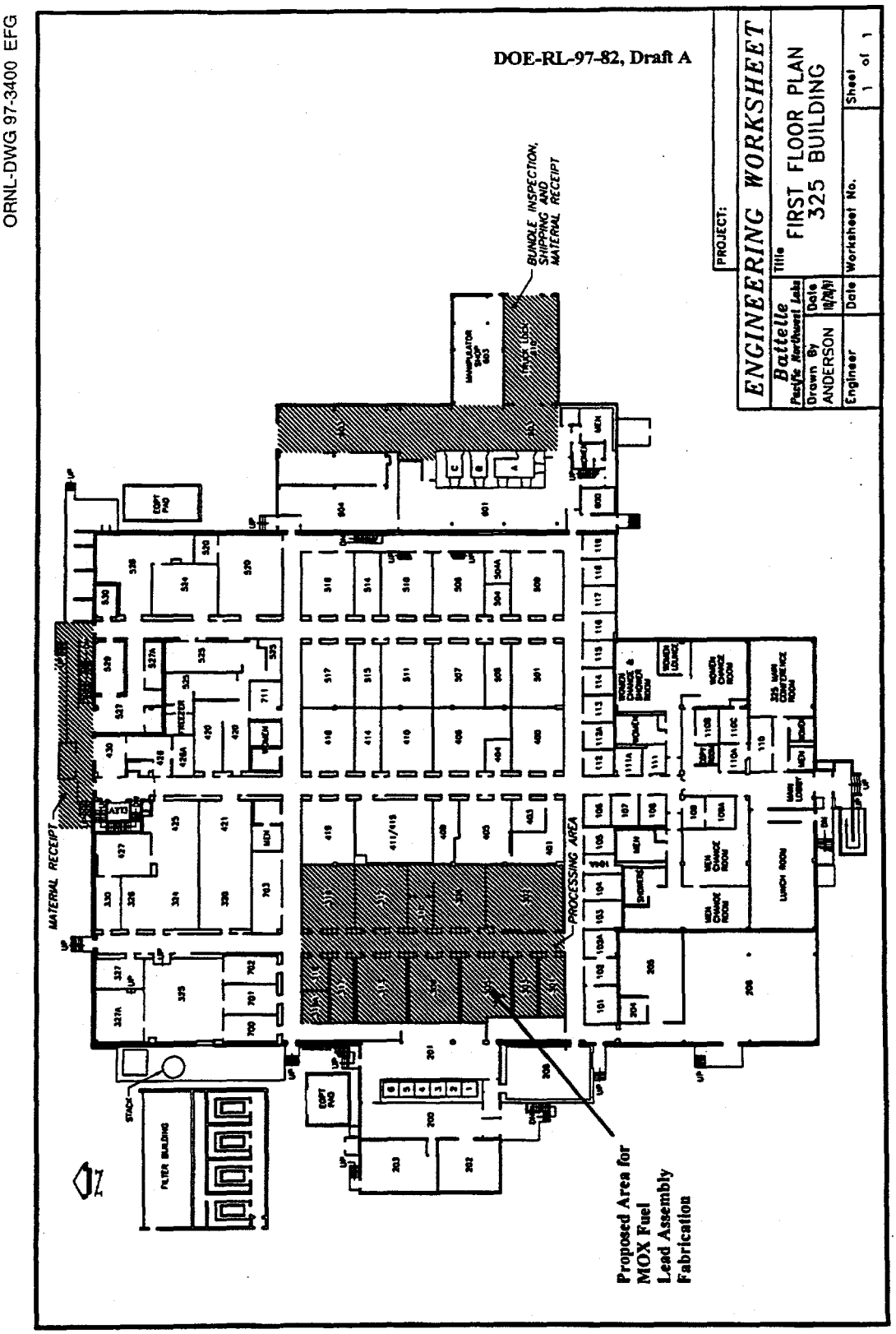

Fig. 7. Floor plan of building 325.

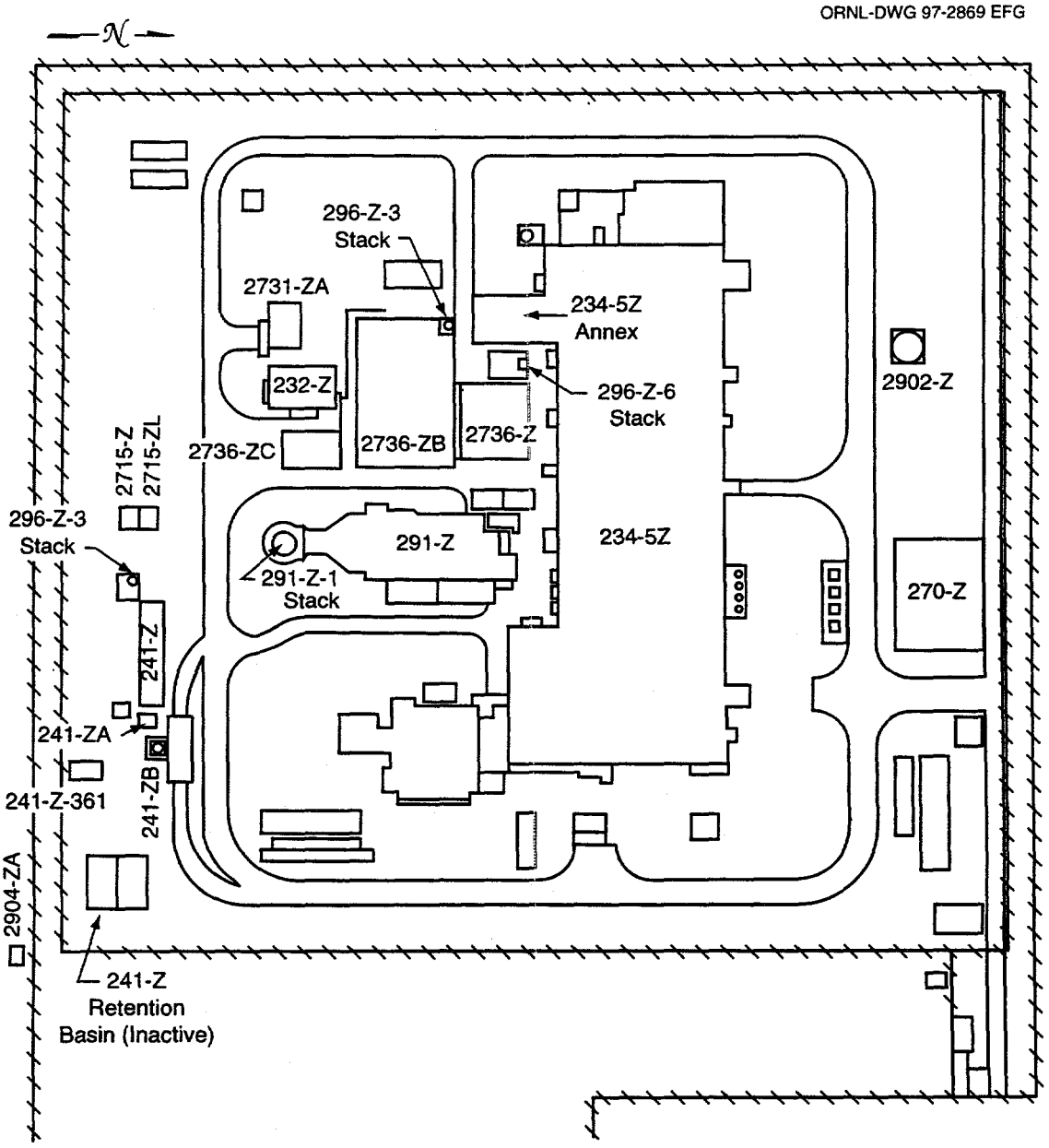

Fig. 8. PFP site layout in the 200-W Area.

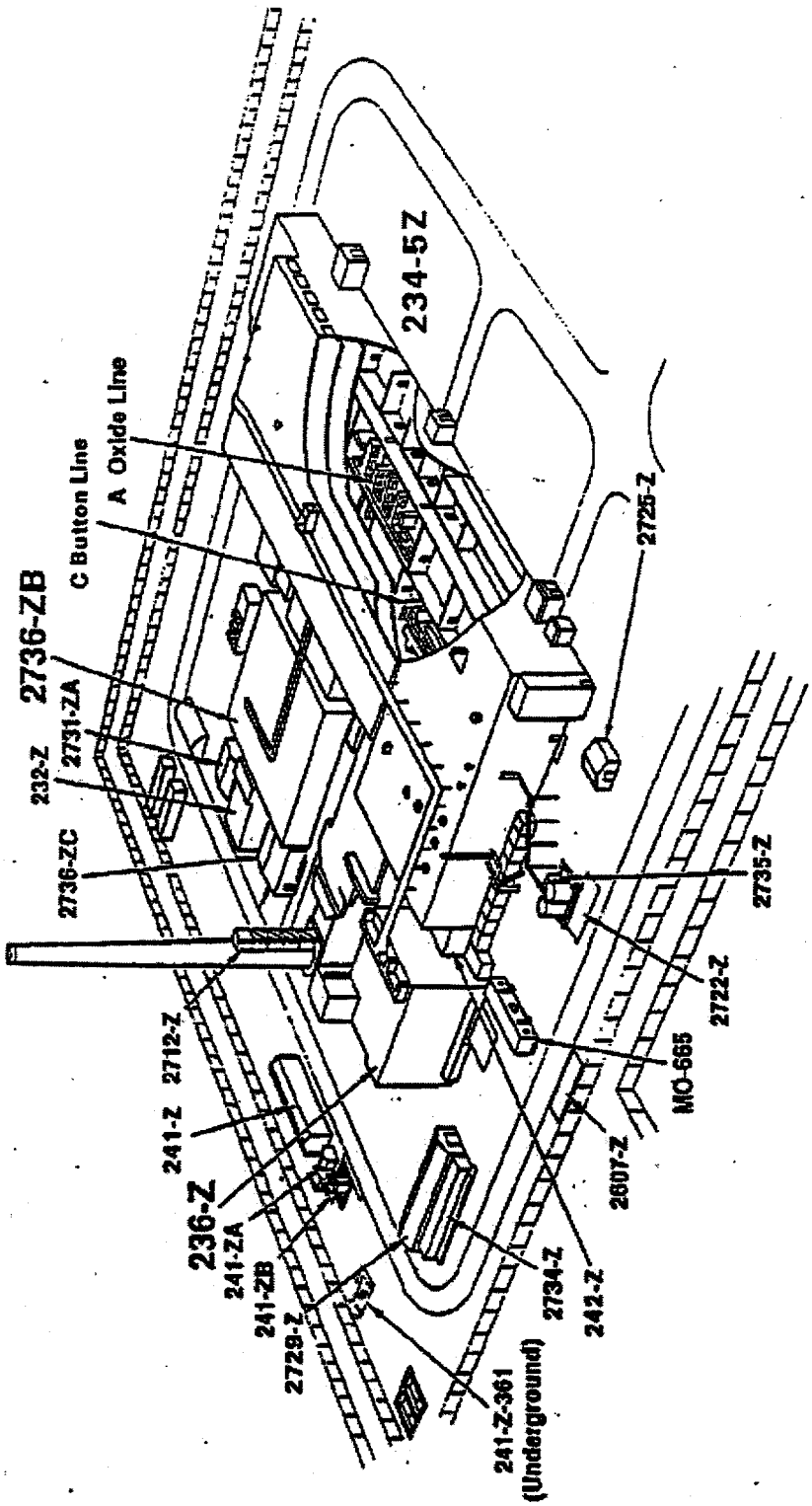

Fig. 9. Aerial view of PFP with cutaway view of Building 234-5Z.

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3. PROCESS DESCRIPTIONS

3.1 PROCESS FLOW DIAGRAM

A process block flow diagram is provided in Fig. 10. Assumptions for the process were given in Table 4. Figure 10 provides the total quantity of HM throughput that is anticipated at each step of the process for an entire year of operations after the facility reaches steady state.

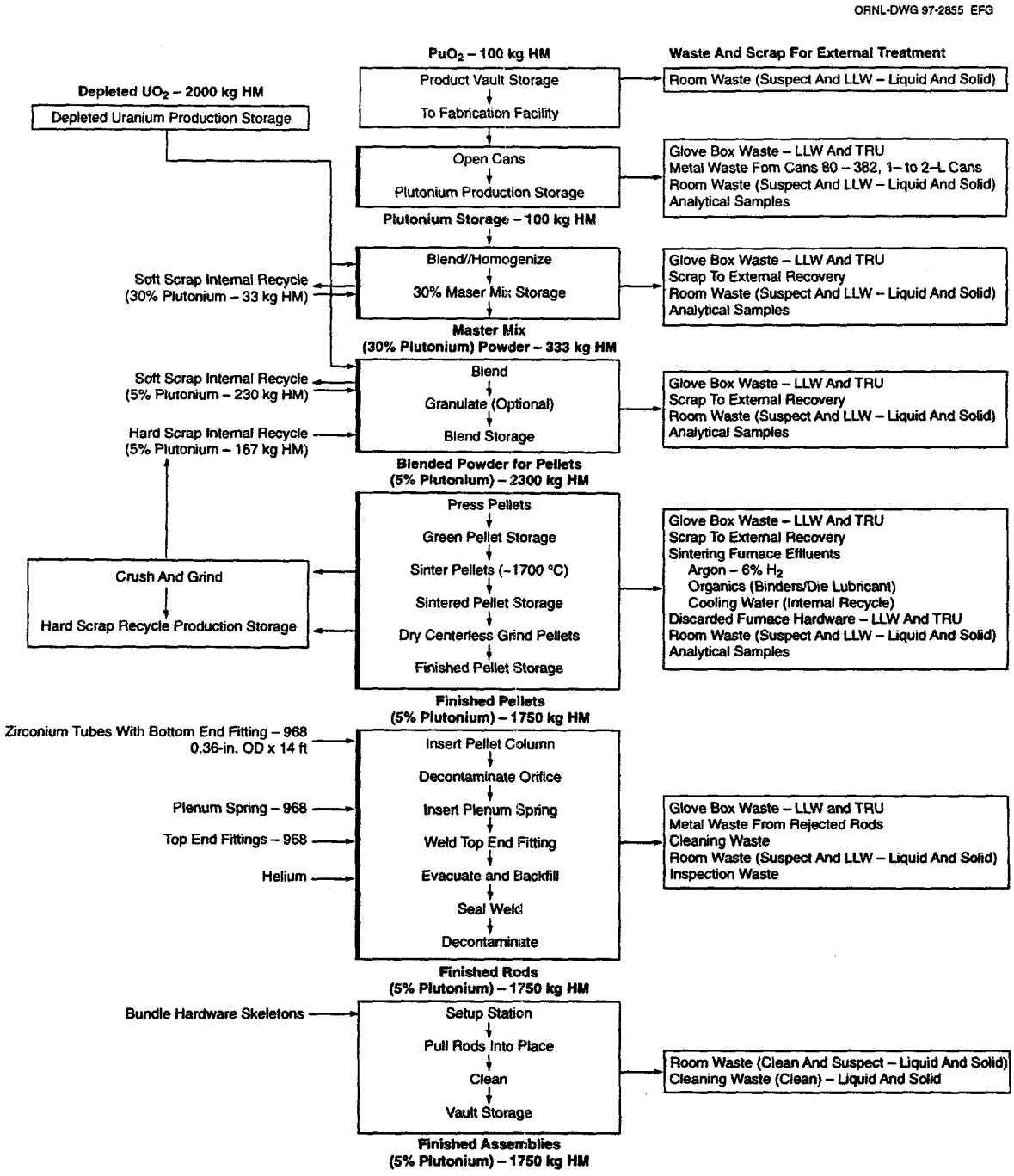
To achieve a state of reliable operations for the new facility, cold startup and hot startup phases are anticipated to be necessary. Table 5 provides the anticipated material requirements for each phase of the startup and operations for the LA MOX fuel fabrication facility. The cold startup consists of using only depleted UO_2 in the fuel fabrication process to develop acceptable processing steps.

Hot startup consists of using the final MOX fuel blend to determine that each processing step meets acceptable standards of fuel quality and repeatability. This phase of startup is anticipated to require at least 6 months.

3.2 WASTE MANAGEMENT FLOW DIAGRAMS

Figure 11(*a*) and (*b*) are simplified flow diagrams that indicate how all forms of waste from the LA MOX fuel fabrication facility will be handled and disposed. These flow diagrams are generic examples of how waste will be handled for each site. Of course, each site will have some site-specific variations from the given flow diagrams, but for the purposes of this study the given material flow diagrams should be adequate.

For the Hanford site, liquid low-level waste (LLW) will be solidified at the point of generation, solid LLW will be disposed of by burial in the 200 Area LLW burial grounds, mixed waste will be stored in buildings in the 200 Area until decisions can be made regarding final disposal, and TRU waste will be stored above ground in the 200 Area until final disposal at the Waste Isolation Pilot Plant (WIPP).



Note: 1. Heavy borders are glove box process operations.
2. A total of 20% of pellets will be recycled.

Fig. 10. LA MOX fuel flow sheet outline with annual throughputs.

Table 5. LA MOX fuel fabrication requirements

	Units/bundle	Product produced[a]		Production capacity required[a]						Total
		Output—3 years	Output—1 year	Cold startup	Hot startup (6 months)	Rejection rate[b]	Capacity/3 years	Capacity/1 year	Capacity/d (200 d/year)	
Base requirements and assumptions										
Bundles/year [pressurized-water reactor (PWR) 17 × 17]		10	3			0%	10	3.3		10
Rods	264	2,640	880	220	220	10%	2,904	968	5	3,344
Pellets (0.327-in. diam × 0.4 in. × 14 ft)	110,880	1,108,800	369,600	110,880	110,880	20%	1,330,560	443,520	2,218	1,552,320
Plutonium and depleted uranium required										
Plutonium (5% in depleted uranium), kg HM[c]	25	250	83		21	20%	300	100	0.5	321
Depleted uranium, kg HM	500	5,000	1,667	450	417	20%	6,000	2,000	10	6,867
Total plutonium + depleted uranium, kg HM[c]	525	5,250	1,750	450	438	20%	6,300	2,100	11	7,188
Scrap generation										
Total scrap depleted uranium, kg HM				450						450[d]
Total scrap plutonium (mixed with depleted uranium), kg HM					13		51	17	0.1	64[d]
Total scrap depleted uranium (mixed with plutonium), kg HM					250		1,000	333	2	1,250
Recycle and recovery scrap and waste quantities										
Recycled hard scrap[e] (mixed with depleted uranium), kg HM					6.25		25	8		31
Recycled hard scrap depleted uranium (mixed with plutonium), kg HM					125		500	167		625
Scrap plutonium to recovery (mixed with depleted uranium), kg HM					5		21	7		26
Scrap depleted uranium to recovery (mixed with plutonium), kg HM					100		400	133		500
Waste plutonium[f] (mixed with depleted uranium), kg HM					1.25		6	2		7
Waste depleted uranium (mixed with plutonium), kg HM					25		100	33		125
Waste volumes										
Volume of transuranic (TRU) waste generated,[g] m^3					10		120	40	0.2	130
Volume of low-level waste (LLW) generated, m^3				10	10		120	40	0.2	140
Volume of mixed LLW generated, m^3				0.4	0.4		3	1		4
Volume of liquid LLW generated, L				40,000	40,000		480,000	160,000	800	560,000
Volume of liquid TRU generated, L					50		600	200	1	650
Volume of nonhazardous solid, m^3				650	650		3,900	1,300		5,200
Volume of nonhazardous sanitary liquid, L				800,000	800,000		4,800,000	1,600,000		6,400,000

[a] In the event LEU rods are used in place of MOX rods in the assembly, the amount of plutonium processed in the LA fuel fabrication facility will be reduced accordingly, as will the amount of waste generated.

[b] Assumed that pellets in rejected rods can be reused.

[c] Three plutonium concentrations are required; 5% is nominal plutonium concentration.

[d] Total uranium and plutonium scrap will be sent to the immobilization alternative for disposition.

[e] Hard scrap is from centerless grinding of pellets and rejected sintered pellets; 50% of hard scrap is assumed to be recycled. Soft scrap, consisting of off-specification powder blends, will be recycled within process line and is not considered in this table.

[f] Plutonium is contained in glove box waste consisting of filters, gloves, wipes, and discarded process hardware. This value is based on 10% of scrap plutonium and is considered an upper bounding value.

[g] The volume of TRU waste includes mixed TRU waste: solid waste volumes were estimated in number of 200-L drums generated.

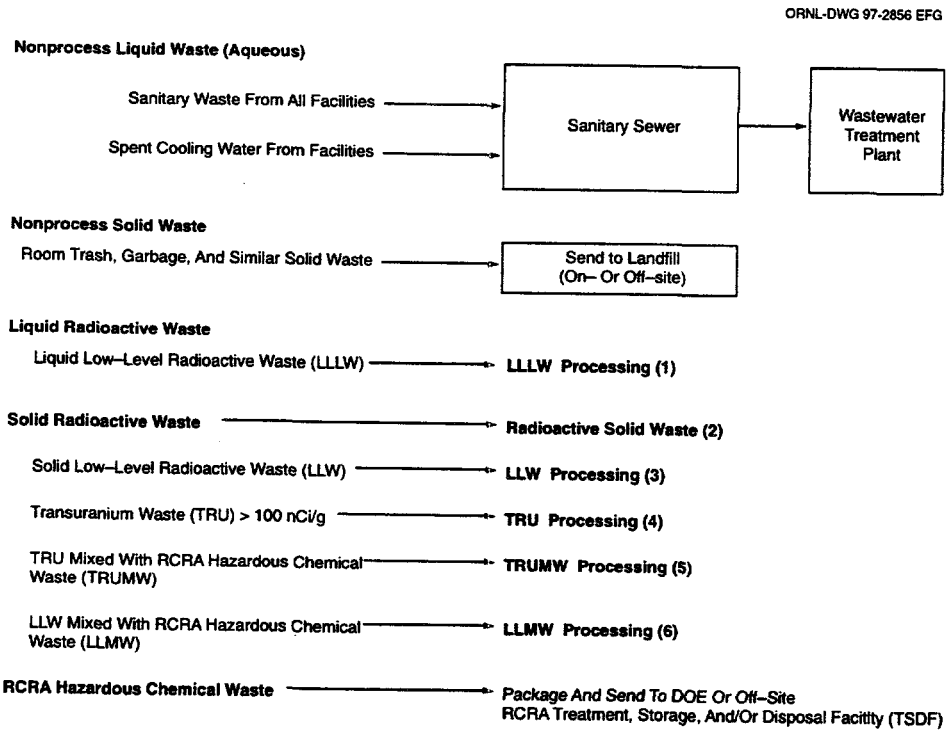


Fig. 11(*a*). Waste generated during LA MOX fuel fabrication facility operation.

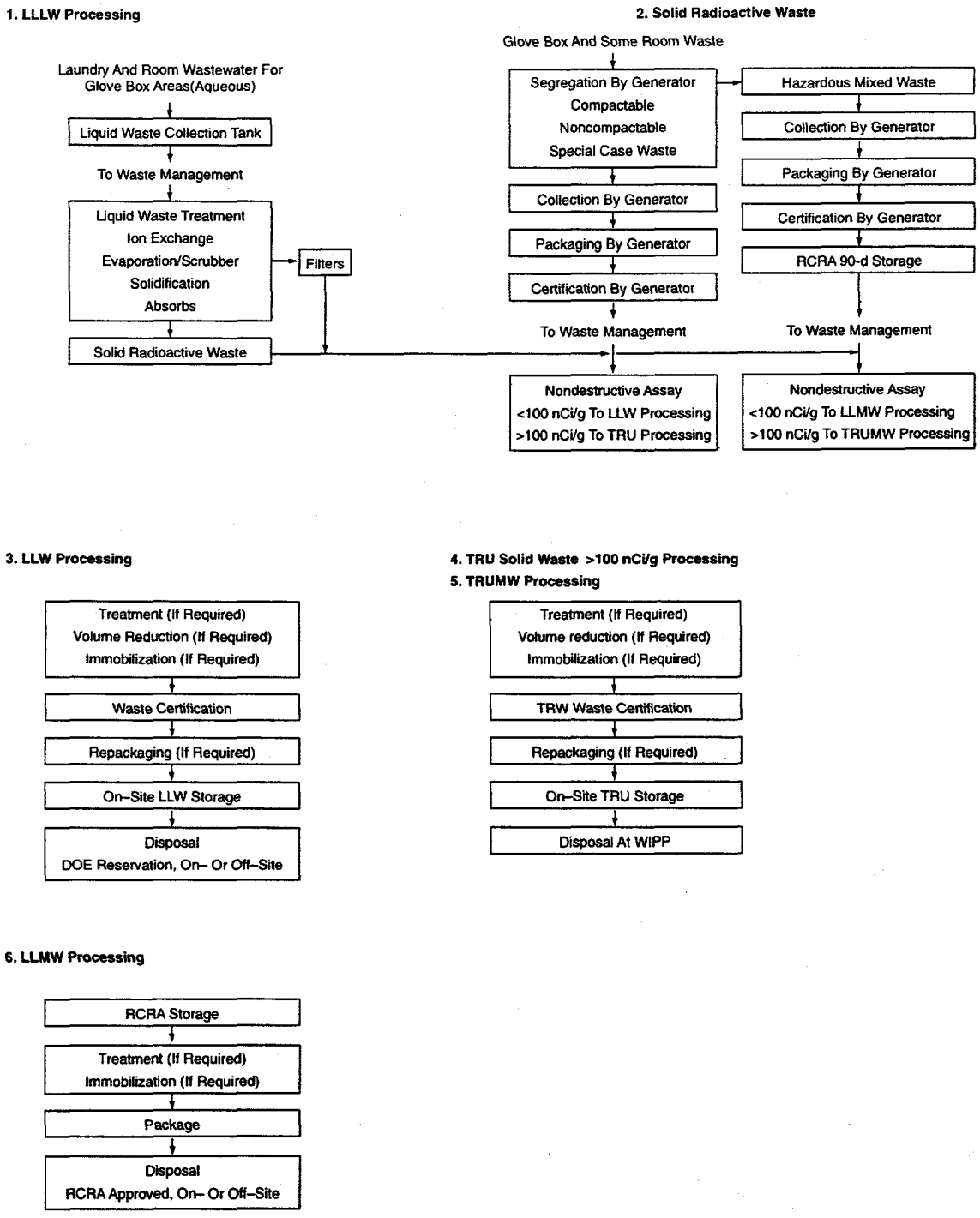


Fig. 11(*b*). Waste generated during LA MOX fuel fabrication facility operation.

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4. RESOURCE NEEDS

4.1 CONSTRUCTION RESOURCE NEEDS

Of the Hanford Site facilities identified in Chap. 2 that would support the LA fabrication mission, only Building 325 would require modifications for the S&S non-Category I option. No facility modifications would be required for the S&S Category I option.

No significant, sensitive, or unusual resources are required for the facility modification necessary to prepare all facilities for the LA fabrication program.

4.2 OPERATIONAL RESOURCE NEEDS

The initial scaling factor for resource requirements for the LA fabrication facility is based on a linear measure derived from the capacity of the MOX fuel fabrication facility. The annual quantity of surplus plutonium [3.5 metric tons (MT) plutonium (4.0 MT PuO_2)] and the MOX fuel fabrication facility requirements were obtained from the LANL *Response to the Surplus Plutonium Disposition Environmental Impact Statement Data Call for a Mixed Oxide Fuel Fabrication Facility Located at the Pantex Plant.*[2] The annual quantity requirement for uranium [88 MT HM (100 MT UO_2)] was obtained from the Initial Data Report and *Response to the Surplus Plutonium Disposition Environmental Impact Statement Data Call for the UO_2 Supply.*[3]

The annual plutonium and uranium capacity requirements and the scaling factors are calculated as follows:

1. LA fabrication facility plutonium capacity

   Plutonium required for production = 250 kg HM plutonium
   Plutonium required including rejection rate of 20% = 250 kg HM plutonium × 120% = 300 kg HM plutonium (50 kg HM to be recycled)
   Annualized plutonium requirements = (300 kg HM plutonium)/3 years = 100 kg HM plutonium
   Annualized MT HM plutonium capacity = (100 kg HM plutonium)/(1000 kg/MT) = 0.1 MT HM plutonium

2. LA fabrication facility uranium capacity

   Uranium required for production = 5000 kg HM uranium
   Uranium required including rejection rate of 20% = 5000 kg HM uranium × 120% = 6000 kg HM uranium (1000 kg HM to be recycled)
   Annualized uranium requirements = (6000 kg HM uranium)/3 years = 2000 kg HM uranium
   Annualized MT HM uranium capacity = (2000 kg HM uranium)/(1000 kg/MT) = 2.0 MT HM uranium

3. LA fabrication facility capacity

   Annual LA capacity = (0.1 plutonium + 2.0 uranium) MT HM = 2.1 MT HM MOX
   Annual mission surplus plutonium = 3.5 MT HM plutonium
   Annual uranium requirements for mission MOX at 5% plutonium = 66.5 MT HM uranium
   Annual MOX production = (3.5 plutonium + 66.5 uranium) MT HM MOX = 70 MT HM MOX

4. Scaling factor = (2.1/70) MT HM MOX = 0.03% = 3%

This report assumes that 3% of the MOX fuel fabrication facility requirements is the initial base requirement of the LA fabrication facility. Resource requirements and contingencies in addition to 3% are noted separately for each resource. In situations where requirement scaling is not applicable, full calculations of resource requirements are provided. Resources needed for the LA fabrication facility are summarized in Table 6. (In the event LEU rods are used in place of some MOX rods, the resource needs will be reduced proportionately.)

Table 6. Resource needs during operation of the LA fabrication facility

Resource requirement	Annual average consumption
Utilities	
Electricity	720 MWh
Peak demand	<300 kW(e)
Fuel	
Electricity (for heating)	514 MWh
Diesel fuel (for generator)	4,600 L (1,200 gal)
Gasoline (for vehicles)	6,900 L (1,825 gal)
Water	
Groundwater	1,600,000 L (411,000 gal)
Peak demand	No peak requirements anticipated
Surface water	None required for this process
Process chemicals and compounds[a]	
Gases	
Argon	16,000 m^3 (565,000 ft^3)
Helium	10 m^3 (350 ft^3)
Hydrogen	1,000 m^3 (35,500 ft^3)
Nitrogen	5,300 m^3 (187,000 ft^3)
Oxygen	5,000 m^3 (174,000 ft^3)
Liquids	
Hydrochloric acid (HCl)	0.5 kg (1 lb)
Nitric acid (HNO_3)	1 kg (2 lb)
Polyethylene glycol	20 kg (<45 lb)
Sulfuric acid (H_2SO_4)	2 kg (5 lb)
Solids, kg (lb)	
Sodium hydroxide (NaOH)	16 kg (34 lb)
Sodium nitrate ($NaNO_3$)	85 kg (<200 lb)
Zinc stearate	20 kg (<45 lb)
Nonprocess chemicals	
Liquids	
Alcohol	225 L (60 gal)
Hydraulic fluid	4.5 kg (10 lb)
General cleaning fluids	225 L (60 gal)
Radioactive process materials	
Plutonium dioxide (PuO_2)	
Hot startup	23.6 kg (52 lb)
Annually for 3 years	113.5 kg (250 lb)
Uranium dioxide (UO_2)	
Cold startup	510 kg (1,125 lb)
Hot startup	475 kg (1,045 lb)
Annually for 3 years	2,270 kg (5,000 lb)

[a]Requirements for insignificant amounts will most likely be met from existing site inventory.

4.2.1 Utilities

Utility connections at the sites being considered for the LA fabrication facility are currently installed and in use. For analysis purposes, it is not anticipated that additional connections will be required. Utility requirements beyond those necessary for maintenance of the building's present usage are based on those for the MOX fuel fabrication facility, scaled to 3%, and then increased by a 200% contingency factor for bounding purposes. The original MOX requirements were developed from the NRC environmental report for the Westinghouse Recycle Fuels Plant (see Ref. 2, Appendix A) with a 200-MT MOX fabrication capacity. The annual requirements are calculated as

$$24{,}000 \text{ MWh} \times (100 \text{ MT}/200 \text{ MT}) \times 3\% \times 200\% = 720 \text{ MWh} \ .$$

The peak demand is based the MOX fabrication facility's peak demand of <5 MW(e) and is calculated as

$$<5 \text{ MW(e)} \times 1000 \text{ kW(e)/MW(e)} \times 3\% \times 200\% < 300 \text{ kW(e)} \ .$$

4.2.2 Fuel Resources

Fuel resource requirements for the LA fabrication facility are site dependent. Based on the MOX fabrication facility's generic fuel needs, it is assumed that the Hanford LA fabrication facility will use electricity for heating and electricity for sintering. Oil products or gasoline will be necessary for operation of two small generators and a small fleet of motorized vehicles.

Electricity requirements for heating are calculated as

$$(1{,}950{,}000 \text{ ft}^3 \times 900 \text{ Btu/ft}^3) \times (0.293 \times \text{Wh/Btu}) \times (1 \text{ MW}/1 \times 10^6 \text{ W}) = 514 \text{ MWh} \ .$$

The Hanford options would use all electricity. The site receives power from the Bonneville Power Administration grid with the majority of generation from hydroelectric sources.

Oil products in the form of diesel fuel are required for operation of emergency generators. Based on technical specifications and testing requirements for generator operability,[4] each of two generators will operate 30 h/year. Testing is required for 1 h each month for verification of operation, 1 h twice a year for full-load and manual synchronization, and 24 h every 18 months to confirm capability for continuous operation. Assuming that peak capacity is 300 kW(e) and that approximately 50% of peak demand should be available for glove box ventilation, emergency lighting, and other required electrical support, two 150-kW capacity generators will be necessary at the LA fabrication facility. Based on a consumption rate of 38 L/h (10 gal/h), requirements for oil products are calculated as follows:

$$38 \text{ L/h} \times 30 \text{ h/year} \times 2 \text{ generators} \times 200\% \text{ contingency} = 4560 \text{L/year} \cong 4600 \text{ L/year} \ .$$

Because of the facility size and the potential distances between areas being used to support the LA mission, a distance of up to 2.5 miles (4 km) between the LA fabrication facility and other areas is assumed. An estimate of gasoline required for operation of motorized vehicle usage is based on requirements of 5 miles round-trip for 10 trips daily at ~0.38 L/mile (0.1 gal/mile). The standard days of operation are calculated in Sect. 5.1 as 365 d/year. The fuel consumption for motorized vehicles at the LA fabrication facility is estimated as

$$10 \text{ trips/d} \times 5 \text{ miles/trip} \times 0.38 \text{ L/mile} \times 365 \text{ d/year} = 6935 \text{ L/year} \cong 6900 \text{ L/year} \ .$$

The total requirement for oil products is ~11,500 L/year (3,040 gal/year).

4.2.3 Water

Based on the MOX fuel fabrication facility's water requirement of 25 gal/d (95 L/d) per employee, 24 employees working 250 d at the LA fabrication facility on the first shift, and 12 employees performing shift work for 365 d, the annual sanitary water resource usage is calculated as

$$(25 \text{ gal/d}) \times [(24 \text{ employees} \times 250 \text{ d/year}) + (12 \text{ employees} \times 365 \text{ d/year} \times 2 \text{ shifts}) + (12 \text{ employees} \times 115 \text{ d/year})] = 403{,}500 \text{ gal/year} ,$$

where calculations of the number of employees are in Sect. 5.1.

Nonsanitary water requirements are based on scaling the MOX fuel fabrication facility[2] with a 100-MT capacity to 10% of requirements. The 10% factor was used in lieu of 3% based on the nonlinear requirements for staffing between the MOX fuel fabrication facility and the LA fabrication facility. The usage is calculated as follows:

$$191 \text{ gal/d} \times 10\% \times (365 \text{ d/year}) = 6972 \text{ gal/year} .$$

Total groundwater usage is rounded to 411,000 gal/year (1,600,000 L/year).

4.2.4 Process and Nonprocess Chemicals and Compounds

Process and nonprocess chemicals in gas, liquid, and solid form will be required in the operation of the LA fabrication facility. Those chemicals required in significant quantities are identified in Table 6. Most of the chemicals required will be available from existing site inventory.

It is assumed that the sintering furnace will have a purge rate of 30 L/min, requiring ~94% argon and 6% hydrogen for operations. This number is derived as a function of the purge rates for large production furnaces that are typically on the order of 10 ft^3/min. Assuming that the sintering furnace for the LA program will require one-tenth of the typical purge rate, a rate of 1 ft^3/min would be reasonable. There are 28.3 L/ft^3, which rounds up to 30 L/ft^3, resulting in a 30-L/min purge rate.

Because of requirement calculations for some chemicals resulting in minimal quantities, the amounts required have been rounded upward for bounding purposes. The quantities of process and nonprocess chemicals required in quantifiable amounts were calculated based on projected uses and requirements that follow.

Alcohol: for process and nonprocess cleaning purposes
5 gal/month × 12 months/year = 60 gal/year

Argon: required for sintering furnaces
(30 L/min) × (525,600 min/year) × 0.001 m^3/L = 15,768 m^3/year ≅ 16,000 m^3/year

General cleaning fluids: for nonprocess cleaning purposes
5 gal/month × 12 months/year = 60 gal/year

Helium: required as process gas
0.2 m^3/week × 52 weeks/year = 10 m^3/year

Hydraulic fluid: lubricant
0.2 lb/week × 52 weeks/year ≅ 10 lb/year

Hydrochloric acid: required in service laboratory
5 lb × 20% = 1 lb/year

Hydrogen: required in sintering furnaces
(30 L/min) × (525,600 min/year) × 0.001 m^3/L × 6% = 946 m^3/year ≅ 1000 m^3/year

Nitric acid: required in service laboratory
8 lb × 20% = 1.6 lb/year ≅ 2 lb/year

Nitrogen: required in glove boxes
(1 L/min) × (525,600 min/year) × 0.001 m^3/L × 10 glove boxes = 5256 m^3/year ≅ 5300 m^3/year

Oxygen: required for dry recycle process—assume 580 h/year dry recycle processing
(5 ft^3 O_2/min) × (60 min/h) × (680 h/year) = (174,000 ft^3 O_2/year) ≅ 4927 m^3 ≅ 5000 m^3 O_2/year

Polyethylene glycol: required in blending process
700 lb × 3% × 200% = 44 lb/year ≅ 45 lb/year

Sodium hydroxide: required in laboratory scrubber
170 lb × 20% = 34 lb/year

Sodium nitrate: required in laboratory scrubber
3100 lb × 3% × 200% ≅ 186 lb/year ≅ 200 lb/year

Sulfuric acid: required in service laboratory
17 lb × 20% = 3.4 lb/year ≅ 5 lb/year

Zinc stearate: required in pellet pressing process
670 lb × 3% × 200% = 40.2 lb/year ≅ 45 lb/year

4.2.5 Radioactive Process Materials

The radioactive process materials used at the LA fabrication facility are PuO_2 and UO_2. Based on the bounding case of 100 g plutonium per rod, 264 rods per assembly (full MOX), 5% plutonium for rods, and 10 full-MOX assemblies produced over a 3-year period, 113.5 kg (250 lb) of PuO_2 and 2270 kg (5000 lb) UO_2 would be required annually. The calculations are provided in Sects. 4.2.5.1 and 4.2.5.2.

4.2.5.1 Plutonium requirements

The conversion factor for plutonium to PuO_2 = (mol wt PuO_2)/(mol wt plutonium) = 271.0/239.0 = 1.1339.

Plutonium required for 3-year LA mission = 250 kg HM plutonium (Table 5)
Annual plutonium with rejection rate of 20% = 250 kg HM plutonium × 120%/3 years
= 100 kg HM plutonium/year
100 kg HM plutonium × 1.1339 = 113.39 kg PuO_2 ≅ 113.5 kg PuO_2/year

The plutonium requirements for hot startup operations are

(250 kg HM plutonium)/(3 years) × 25% × 1.1339 = 23.6 kg PuO_2 .

Total plutonium requirements for the LA fabrication facility for the 3-year mission are 364 kg PuO_2.

4.2.5.2 Uranium requirements

The conversion factor for uranium to UO_2 = mol wt UO_2/mol wt uranium = 270.03/238.03 = 1.1344.

Uranium required for 3-year LA mission = 5000 kg HM uranium (Table 5)
Annual uranium with rejection rate of 20% = 5000 kg HM uranium × 120%/3 years
= 2000 kg HM uranium/year
2000 kg HM uranium × 1.1344 = 2268.8 kg UO_2 ≅ 2270 kg UO_2/year

The uranium requirements for cold and hot startup operations during the first year of production follow.

Hot: (5000 kg HM uranium)/(3 years) × 25% × 1.1344 = 472.67 kg UO_2 ≅ 475 kg UO_2
Cold: (5000 kg HM uranium)/(3 years) × 27% × 1.1344 = 510.49 kg UO_2 ≅ 510 kg UO_2

Total uranium requirements for the LA fabrication facility for the 3-year mission are slightly less than 7,800 kg (17,200 lb) UO_2.

5. EMPLOYMENT REQUIREMENTS

5.1 ANNUAL EMPLOYMENT REQUIREMENTS DURING OPERATION OF THE LA FABRICATION FACILITY

Table 7 provides the annual number of employees by labor category, the number of shifts, the number of employees per shift, and the number of operating days per year for the LA fabrication facility. It is assumed that the facility will operate continuously with the primary work effort during standard business days of operation at the selected site. The standard days of operation were calculated as follows:

$$(365 \text{ d/year}) - [(104 \text{ weekend days}) + (11 \text{ holidays})] = 250 \text{ d/year} .$$

The 11 holidays considered are New Year's Day, Martin Luther King Day, Good Friday, Memorial Day, Independence Day (2 days), Labor Day, Thanksgiving (2 days), and Christmas (2 days).

The number of employees in Table 7 was derived from a reduction in personnel required for the MOX fuel fabrication facility with consideration given for the nature of operations necessary to maintain 24-h performance.[2] Twenty-four employees will be required on the standard operation shift. Twelve additional employees will be required on each of two alternate shifts, resulting in total staffing needs of 60 employees.

Many of these positions probably will be filled by existing employees at the site. This estimate is generic in nature, and some of the sites under consideration may require fewer employees based on existing infrastructure. For example, facilities with on-site plutonium processing facilities may require only a nominal increase in support personnel and management. Industrial support organizations (such as site superintendent, site security, emergency response, health services, and personnel support) and atmospheric and groundwater monitoring will be provided by the site operator because these facilities are currently being serviced by the site.

Based on the estimates for the MOX fuel fabrication facility, a personnel requirement was established if more than 80% effort of a full-time equivalent (FTE) was charged out to support the LA fabrication facility operation.[2] Those efforts requiring less than 80% of an FTE were considered part of operations of the existing site. The assumptions used in consideration of staffing levels for the LA fabrication facility are given in Table 8.

5.2 RADIATION DOSES (WHOLE BODY) TO INVOLVED WORKERS DURING MODIFICATION OF THE LA FABRICATION FACILITY

Of the Hanford Site facilities identified in Chap. 2 that would support this mission, only Building 325 requires modifications for the S&S non-Category I option. The radiation doses associated with modifications of this building are summarized in Table 9. No radiation dose would be associated with the S&S Category I option because no facility modification is anticipated.

5.3 RADIATION DOSES (WHOLE BODY) TO INVOLVED WORKERS DURING OPERATION OF THE LA FABRICATION FACILITY

The provided dose estimates to workers are based on those found in 10 *Code of Federal Regulations* (CFR) 835 and the administrative control level (ACL) found in DOE N 441.1. Fissile material processing for the LA program will be conducted at a DOE site and should be subject to DOE N 441.1, a DOE notice that establishes a maximum allowable dose of 2 rem/year (see Table 10). ALARA will be the goal in all operations. The primary hazard in the LA program will be processing PuO_2 powder and the possibility of inhalation of the PuO_2 dust.

Estimated dose to radiation workers for handling 3013 cans during PuO_2 powder homogenization operations and blending with UO_2 powder will be below the ACL found in DOE N 441.1.

Table 7. Annual employment requirements during operation of the LA fabrication facility

Labor category[a]	Number of employees on one shift of 250 d/year	Number of employees on each of three alternate shifts of 365 d/year[b]
Officials and managers	1	0
Professionals	4	0
Technicians	10	7
Office and clerical	2	0
Craft workers (skilled)	2	1
Operatives (semiskilled)	2	2
Service workers	3	2
Total	24	12

[a]All fractional manpower requirements are rounded up to whole numbers.
[b]Two 365 d/year shifts and one 115 d/year shift.

Table 8. Assumptions used in consideration of staffing levels for the LA fabrication facility

1. The facility will be built on an existing DOE site with an estimate of 4500 ft^2 available space (3000 ft^2 for MOX rod processing, 1000 ft^2 for bundling activities, and 500 ft^2 for fuel bundle storage).
2. The site will have an existing infrastructure in place to accept the LA mission.
3. Personnel will be required to support a process capacity of ~2 MT HM per year.
4. Personnel involved in SNM operations must work in pairs and follow specific safety precautions detailed by the site.
5. Personnel must attend required site training. A staffing requirement for training purposes has been included in this estimate.
6. Space will be allocated for safe secure transports (SSTs) carrying plutonium and transportation for uranium so that loading can be accomplished on a follow-up operating shift if the transport arrives near or following the close of standard business.
7. As with the MOX fuel fabrication facility estimate, the staffing requirements assume that ~20% of the employee's time will be taken through training, vacation, personal leave, or illness. Even though employees cannot necessarily transition from one position to another, a contingency was added to account for nonproductive time.

Table 9. Radiation doses (whole body) to involved workers during modification of the LA fabrication facility (Building 325) for the S&S non-Category I option

Average annual dose to all involved workers at the facility, mrem	10[a]
Maximum dose to an involved worker at the facility, mrem	180[a]
Total number of involved workers	15[b]

[a]Assumes one-half of facility preparatory work is performed inside the building radiation zone.
[b]Includes making facility ready to receive new glove boxes and equipment.

Table 10. Radiation doses (whole body) to involved workers during operation of the LA fabrication facility

Average maximum target annual dose to all involved workers at the facility, mrem	500
Maximum allowable administrative dose limit,[a] mrem	2000
Total number of involved workers	55

[a]DOE Notice DOE N 441.1 establishes an ACL of 2 rem/year for TEDE.

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6. WASTES, EMISSIONS, AND EXPOSURES

6.1 WASTES GENERATED DURING FACILITY MODIFICATION

No Resource Conservation and Recovery Act of 1976 (RCRA)-regulated waste streams would be associated with the modification of Building 325 for the S&S non-Category I option.

The solid and liquid wastes generated during construction include the equipment previously installed and sanitary wastewater. Some radioactive solid waste (contaminated equipment) is expected. It is assumed that some items will be decontaminated and packaged as solid LLW while others will be packaged as TRU waste, which will be stored at the site until a waste repository is available. No radioactive liquid waste is expected.

The total quantities of solid and liquid wastes generated during the facility modification are shown in Table 11.

No radioactive emissions are anticipated as a result of these facility modifications.

Table 11. Total wastes generated during construction

Waste category	Quantity
Sanitary wastewater, L (gal)	30,000 (7,000)
TRU waste, m^3 (ft^3)	10 (350)
Solid LLW, m^3 (ft^3)	100 (3,500)

6.2 WASTES GENERATED DURING OPERATION OF THE FACILITY

Table 12 provides the annual volume, total estimated volume, description, and anticipated treatment method by waste category for liquids and solids anticipated during operation of the LA fabrication facility. Only very small quantities of chemical emissions are anticipated from analytical operations resulting from sampling.

A total of 0.4 mg/year of plutonium is estimated to be released to the air during the operation of the LA MOX facility. This plutonium release corresponds to a total activity of 94 μCi/year. The total plutonium release includes two contributions; 0.3 mg/year is expected to be released during normal operation of the plant and an additional 0.1 mg/year during a one-time abnormal event (spilling the powder of one 3013 can).

The release during normal operation has been estimated from the releases reported in Ref. 2 for a 100-MT HM/year MOX plant with two lines. Reference 2 reports a release of 0.6 mg/year of plutonium. The LA MOX facility has only one line and a smaller capacity (about 2.5 MT HM/year). For conservatism, one-half of the releases of the large MOX plant (with two lines) has been estimated for the small LA MOX facility (with only one line); therefore, the value is 0.3 mg/year. No scaling consideration has been given to the much smaller capacity of the LA MOX facility (about 1/40 of the large MOX plant).

The release during the abnormal event has been calculated by dropping one 3013 can containing 4.5 kg of plutonium. From Ref. 5 (Table 4-13) the following factors were selected:

- ARF (airborne release fraction) = 3.3×10^{-3}
- RF (respirable factor) = 0.62

Also, the efficiency of the HEPA filters in the glove box has been assumed to be 99.9% (equivalent to a release factor of 10^{-3}) and the efficiency of the building HEPA filters as 99% (equivalent to a release factor of 10^{-2}). Overall, the air emission for this event is

$$4500\ g \times 3.3 \times 10^{-3} \times 0.62 \times 10^{-3} \times 10^{-2} = 0.092\ mg/year \cong 0.1\ mg/year\ .$$

Table 12. Estimated waste generated during operation of the LA fabrication facility[a]

Waste category	Annual volume (m^3 or L)	Annual volume (ft^3 or gal)	Total volume (m^3 or L)	Total volume (ft^3 or gal)	Waste description	Anticipated treatment	Disposal method
TRU—solid (m^3 or ft^3)	40	1,413	130	4,591	Glove box gloves Bag-in plastic Empty bottles Filters Scrapped equipment items Furnace hardware Wipes Metal cans Metallography waste	Compaction	Off-site at Waste Isolation Pilot Plant (WIPP)
TRU-mixed (m^3 or ft^3)[b]	<1	<35	<1	<35	Organics from sintering Sludges from liquids Analytical waste	From liquid treatment absorption to TRU solid	Off-site at WIPP
TRU—liquids (L or gal)	200	53	650	172	Sludges from liquids Analytical waste Metallography waste	Absorption to TRU solid or liquid LLW	As solid off-site at WIPP
LLW—solid (m^3 or ft^3)	40	1,413	140	4,944	Room trash Blotter paper Wipes Mop heads Gloves/shoe covers Solidified sludges Ion exchange resins Discarded C-clothing Metal cans and rods	Incineration Compaction Solidification Metal melting	DOE on- or off-site disposal
LLW—mixed (L or gal)	1	0.3	4	1.1	Solvents from cleaning Analytical waste Sludges from liquids	Incineration Solidification	RCRA-approved disposal DOE on- or off-site Commercial off-site
LLW—liquid (L or gal)	160,000	42,267	560,000	147,935	Decontaminated wastewater Laundry wastewater Analytical wastewater	Ion exchange Evaporation/ scrubber Solidification	Evaporation NPDES[c] permitted discharge
Hazardous (L or gal)	1.5	0.4	4		Process ends	Recycle	
Nonhazardous—solid (m^3 or ft^3)	1,300	45,910	5,200	183,638	Office and lunch room trash Packaging materials Sewage sludges	Compaction Landfill	DOE on- or off-site landfill
Nonhazardous—liquid (L or gal)	1,600,000	411,000	6,400,000	1,644,000	Sewage waste	Sewage treatment	NPDES permitted discharge

[a]Base numbers were generated in metric system to two significant figures; English units are conversions using factors provided in data call.
[b]The volume of TRU-mixed waste is a portion of TRU solid waste volume; mixed TRU waste is likely to come from sludges from wastewater treatment.
[c]NPDES = National Pollutant Discharge Elimination System.
Note: Estimates are based on historical experience from other programs and current programs.

7. ACCIDENT ANALYSIS

7.1 INTRODUCTION

The LA fabrication process represents a very small scale process replication of the large 100-MT/year MOX fuel fabrication facility. The LA assembly fabrication will likely take place in an existing building complex. The process is envisioned to consist of a number (10–20) of glove boxes along with several hoppers, a press, a furnace, and a rod/bundle assembly area. The process can be done in a single large room, but it may also be done using several rooms (or buildings) with the material at the end stage of certain steps involving transportation and/or storage at another building. A generalized approach was taken because these specifics were unknown. Section 7.2 describes the accident analysis approach and mitigating design features that are assumed to be available. Section 7.3 describes the events that were selected for EIS evaluation and the estimated source terms that were chosen for all sites. These source terms are characterized here as "evaluation basis" because the facilities already exist and may have other design basis accidents that may or may not be similar to these accidents. Chemical source terms for the facility are discussed in Sect. 7.4. Site-specific aspects are discussed in Sect. 7.5.

7.2 GENERAL APPROACH AND GENERIC DESIGN ASSUMPTIONS

7.2.1 Accident Analysis Approach

In Ref. 2, a preliminary hazards analysis (PHA) was referenced for a 100-MT/year MOX fuel fabrication plant. This analysis identified 32 accidents which resulted from a variety of events. Specific events for the design-basis and beyond-design basis accidents were then selected from the hazard analysis to be further analyzed in the EIS. In that analysis, four design basis accidents and two beyond-design basis accidents were selected.

Several accident scenarios can be postulated for processing facilities, and many do not result in a source term that leaves the building. The objective of this accident analysis is to examine the frequency and estimated source terms of several events that are expected to result in a significant release from the building. Ventilation system design assumptions such as the use of HEPA filters that affect the leak-path factor are discussed in the next section. Using the methodology in Ref. 5, source terms are derived based on the combination of the material at risk, damage ratio, release fractions, respirable fractions, and the building leak-path factor.

The many unknowns and options associated with the LA fabrication plant did not warrant the performance of a building-/process-specific PHA for the LA facility. Currently, several different proposed fuel fabrication processes are combined with five sites. Knowledge concerning the PHA in Ref. 2 was combined with a knowledge of what the LA plant would generally be expected to look like. These aspects, along with a conservative estimate of the expected material flows of the plant, were used to select conservative accident source terms for the LA EIS analysis. Even though the scale of the LA plant is much smaller, it is thought that the LA facility will have many of the same accident initiators. Selected accident scenarios and the materials at risk were combined with bounding airborne release fractions and respirable fractions from DOE HDBK-3010-94 (Ref. 5) to derive conservative source terms.

With respect to estimated frequencies, the same approach that was taken in Ref. 2 is used. Frequency categories of anticipated (10^{-1}/year to 10^{-2}/year), unlikely (10^{-2}/year to 10^{-4}/year), extremely unlikely (10^{-4}/year to 10^{-6}/year), and beyond the evaluation basis ($<10^{-6}$/year for most events) were usually assigned in this assessment.

No attempt was made to quantify all of the site-specific features that affect the accident analysis. Rather, a generic set (six events are evaluated) of source term magnitudes was used at each site. This set of source terms was derived based on a specified plant process and some general assumptions regarding facility mitigators. No claim is made that the accident source terms cited here bound or are bounded by the existing site-specific analysis. Some site specifics such as stack heights and seismic frequencies were deemed to be a necessary input. The site-specific characteristics used for this site are discussed in Sect. 7.5.

The generic facility design assumptions that are made which are not site-specific are discussed in Sect. 7.2.2.

7.2.2 Facility Design Assumptions

7.2.2.1 Plutonium isotopics and MOX fuel

The isotopic compositions of the plutonium and various MOX blends are shown in Table 13. With respect to both the master mix and fuel blend, the uranium dominates (a minimum of 90%) the weight percent of the mix. However, the radiological contribution of the low specific activities of the uranium isotopes (~5 orders of magnitude) are so low (as compared to the plutonium isotopes) that they are ignored in the calculation of the source terms. In the event LEU rods are used in place of some MOX rods, the radiological contribution from the LEU rods will also be very low compared to the plutonium contribution. Therefore, the accident analyses only considered full MOX assemblies. The respective isotopic activities for the plutonium oxide powder and the MOX powder (conservatively assuming 10% enrichment) or fuel are shown in this table. For each accident scenario, the appropriate (PuO_2, master mix, or fuel blend) isotopic ratios are applied to the quantities at risk to determine the material at risk. This number is then multiplied by the leak-path factor, damage ratio, airborne release fraction, and respirable fraction to determine the released source terms. The leak-path factor incorporates the assumption as to whether the release is filtered.

7.2.2.2 Ventilation system

A complete description of site-specific existing facility ventilation system specifics is beyond the scope of this section. However, in many process buildings, ventilation flows are maintained such that fresh air is taken through the cleanest radiological areas (such as adjacent offices) first. The air flow path is then drawn through the rooms where radiological work is performed. Most facility systems are designed such that glove boxes in these rooms are run at pressures lower than the room pressure to limit the spread of contamination in the event of glove box failure. Contamination would be drawn in to the glove box filter to limit contamination in the room. The exact facility specifics and credit for mitigating design features involved in accident situations will vary, depending on the facility selected and any facility modifications needed to support the LA mission. The intent of this section is to clearly describe the mitigators associated with the ventilation system that are credited in this analysis.

Generally, a number of filters and prefilters would exist in the release path for a typical processing building that supports plutonium processing. Usually one or more filters are at the ventilation outlet of the glove box. These filters are generally accessible in the room where the glove box is located. However, no credit in source term reduction was taken for these filters in this analysis. This approach was taken because arguments could be made that the events in question jeopardize the integrity of nearby filters. For the EIS purposes, this approach was deemed appropriate. However, this does not mean that in the safety analysis (which would be performed after the building has been selected) of various glove box designs, credit could never be taken for those (or other) filters. The decision of what equipment will be qualified (and credit assumed for in the various events) will be made during the subsequent safety review of the facility (e.g., after facility selection). This decision is beyond the scope of this EIS analysis because many facility specific aspects are not known at this stage of the analysis.

The glove box system may be served by a dedicated ventilation system that often ties into the overall system upstream of a series of HEPA filters. With respect to the analysis of events in which overall building confinement is maintained, credit (for the source term reduction) is taken for two serial HEPA filters that generally lie outside the building confinement. The efficiency is assumed to be 99.9% for the first filter. A HEPA filter at the factory is rated at 99.97%, but when installed may test to 99.95%. The facility may run with this for a while and allow some degradation in performance during the operating period. Thus, in practice, a 99.9% efficiency is judged to be appropriate for this filter (roughing filters and prefilters are ignored). A reduced efficiency of 99.0% is used for the second filter (resulting in a combined leak-path factor of 1×10^{-5}). These filters are considered in this analysis where confinement is assumed to be intact and to provide significant source term reduction.

Table 13. Specific activities for process powders (source of isotopics—Ref. 2)

Isotope[a]	Weight percent	Specific activity (Ci/g)[b]	Activity in PuO_2 mix (Ci/g mix)[c]	Activity in 30% PuO_2 enriched MOX mix (Ci/g mix)[d]	Activity in 10% PuO_2 enriched MOX mix (Ci/g mix)[d]
^{238}Pu	0.03	1.712×10^{1}	4.530×10^{-3}	1.359×10^{-3}	4.530×10^{-4}
^{239}Pu	92.44	6.204×10^{-2}	5.045×10^{-2}	1.514×10^{-2}	5.045×10^{-3}
^{240}Pu	6.47	2.270×10^{-1}	1.293×10^{-2}	3.879×10^{-3}	1.293×10^{-3}
^{241}Pu	0.05	1.030×10^{2}	4.542×10^{-2}	1.363×10^{-2}	4.542×10^{-3}
^{242}Pu	0.10	3.926×10^{-3}	3.463×10^{-6}	1.039×10^{-6}	3.463×10^{-7}
^{241}Am	0.90	3.428×10^{0}	2.721×10^{-3}	8.163×10^{-3}	2.721×10^{-3}

[a]The activity of ^{235}U and ^{238}U are ignored for all mixes because of their low specific activities as compared tc the plutonium isotopes.

[b]Specific activities are taken from *Table of Radioactive Isotopes* by Browne and Firestone.[6]

[c]Based on PuO_2 mix being 88.2% plutonium by weight.

[d]30% is master mix; 10% is a conservative estimate for fuel blend.

7.2.2.3 Process flows

Table 14 shows the process inventories and material flows used for the accident analysis. The average plutonium enrichment is nominally taken to be 5% for the fuel. However, because some fuel blends could go higher, an upper bound of 10% plutonium enrichment was selected. Table 14 was generally constructed on that basis. A 30% master mix blend was also selected. Table 14 was not intended to rigidly define the fuel fabrication material process because a number of candidate processes (with different material balances) may be used in the facility. Because the purpose of this table is to provide materials at risk, a conservative estimate of the maximum amount of material at a process station or in interim storage at a certain location was made.

Table 14. Estimated maximum station inventories for LA fabrication plant[a]

Location/material station	Quantity (g)	PuO_2 or MOX	Physical form	Barriers to release (to the room)
Plutonium storage vault	400,000	PuO_2	Fine powder	Storage cans/vault
Plutonium oxide (2 cans in process)	10,000	PuO_2	Fine powder	3013 can[7]
Plutonium oxide loading vessel	16,000	PuO_2	Fine powder	Steel vessel/glove box
Master mix vessel	53,000	MOX (30% blend)	Fine powder	Steel vessel/glove box
Master mix powder storage	107,000	MOX (30% blend)	Fine powder	Interim storage cans/glove box
V-blender	40,000	MOX (10% blend)	Fine powder	Rotating steel vessel/glove box
MOX blend storage	320,000	MOX (10% blend)	Fine powder	Interim storage cans/glove box
MOX granulation area	10,000	MOX (10% blend)	Pressed/very coarse powder	Machinery/glove box
MOX pellet press	1,000	MOX (10% blend)	Pressed to 0.6 theoretical density (TD)	Inside of press/glove box
MOX green pellet storage (in pellet press area)	80,000	MOX (10% blend)	Pressed to 0.6 TD	Interim storage cans/glove box
Pellet sintering furnace	40,000	MOX (10% blend)	Green and sintered	Inside furnace/glove box
Sintered pellet storage	160,000	MOX (10% blend)	Sintered pellets	Interim storage cans/glove box
Pellet grinding area/ground sintered pellets	10,000	MOX (10% blend)	Grindings of sintered pellets	Containers/glove box
Pellet grinding area/dust control area	100	MOX (10% blend)	Fine powder	Loose dust/glove box
Pellet inspection	4,000	MOX (10% blend)	Finished pellets	Trays/glove box
Fuel rod loading, inspection, and storage	20,000	MOX (10% blend)	Finished pellets	About ten rods if cladded
Bundle assembly and storage (end of fabrication)	7,200,000	MOX (5% average blend)	Finished pellets	Cladded in ten bundles
Scrap recovery area	10,000	MOX and PuO_2	Mostly green and sintered pellets	Few dispersibles

[a]No more than 32 kg of PuO_2 (a batch) is used in the process line.
Source: Ref. 7.

It is important to remember that with respect to assumed process flows, no more than 32 kg of plutonium oxide is ever assumed to be in the process line between the plutonium oxide vessel and the fuel rod loading step. As a result, no more than 32 kg of plutonium oxide (which is about 28 kg of pure plutonium) would be at risk in the process line, except for events that involve the vault (which is involved in beyond-evaluation basis events). The 32 kg of oxide does not include the two cans containing 5 kg of pure plutonium oxide that are assumed to be in process between the vault and the oxide loading vessel. Thus, a total of 42 kg of oxide in powder form has been considered in this analysis. Finished fuel rods are not considered because they are generally nondispersible as compared to powder. No effort has been made to model site-specific process flows and distinguish corresponding risk differences because there are so many process and facility unknowns at present. Rather, a generic (but thought to be generally conservative) process flow assumption has been made for all sites. Site-specific differences considered in the analysis are discussed in Sect. 7.5.

For most, if not all accident scenarios, materials at risk will be subjected to orders of magnitude multipliers in the calculation to determine the released source term. Thus, a high level of accuracy is not warranted at this stage of the analysis. Table 14 was used in combination with Ref. 5 and knowledge of the accident dynamics to obtain the source terms for the LA fabrication facility. In each accident scenario, a material at risk assumption is made at each station, depending on the event and energetics. Table 14 also lists the barriers to release that would be found inside the glove box. Generally, those materials that are inside interim storage cans were considered to be the most vulnerable to dispersion.

It is assumed that large amounts of PuO_2 powder would be safely stored in appropriate containers[7] inside a vault or existing storage location. Considerable credit is taken for this vault (and/or the plutonium oxide containers), and it is assumed that the entire plutonium material feed requirement is in the vault at the start of the mission. It was conservatively assumed that 400 kg of oxide powder is in the vault at the start of the process. This inventory is held in 80 cans, each of which holds 5 kg of oxide powder (4.4 kg of plutonium).

The overall layout of the facility is such that from 10–20 glove boxes are accommodated. The equipment is considered to be located in the same room, and generally, little credit is taken for segregation of the processes. Little credit is also taken for the glove boxes. The glove boxes are generally assumed to fail in the postulated events. This may or may not accurately portray the process line once it is designed (because glove boxes with a robust design may be used). However, this approach is thought to be conservative.

Finished fuel assemblies and clad rods were considered in this analysis but are thought to be generally nondispersible. Accidents that involve this inventory are thought to be bounded by the accidents involving the vault and the other in-process steps where dispersible powders are involved.

7.3 SELECTED EVENTS FOR THE LA EIS ANALYSIS

7.3.1 Criticality Event

7.3.1.1 Discussion

The prevention of criticality events is a major goal of the criticality safety program and is an important part of the overall conduct of operations for the facility. Within the nuclear processing industry, such prevention programs have successfully reduced the number of inadvertent criticalities over the years. The goal of the criticality safety program is to attempt (as much as is reasonably possible) to make the possibility of a criticality less than credible (generally accepted to be $<1 \times 10^{-6}$/year frequency). Reference 8 establishes the DOE's nuclear criticality safety program requirements. Similarly, NRC also requires a criticality safety program, and those requirements are assumed to be implemented at the LA fabrication facility.

The risk impact associated with an inadvertent criticality event is highest with respect to workers located in the immediate vicinity (health impacts up to and including death could occur from prompt gamma and neutron doses). Collocated workers and the public would be affected to a lesser degree. The major dose pathways for these impacts are likely to be cloud shine (noble gases) and inhalation (mostly associated with the radioiodines).

With respect to the LA fabrication plant, criticalities could be postulated in several areas (i.e., powder storage, the glove boxes involved in mixing, the furnace, and possibly the fuel rod storage area). The estimated frequencies associated with these events will vary depending on the controls in place, the number of operator movements, and the amount of fissile material present. A generic approach was taken with respect to the selection of the specifics of this event rather than selecting a criticality scenario associated with a specific operation in the LA fabrication.

7.3.1.2 Source term

The significant quantities of fissile materials in LA necessitate consideration of a criticality event. Because a limited number of rods are being made, a criticality event associated with a large array of fuel rods was not selected for this event. Because sources of moderation may be assumed to be either accidentally or inadvertently introduced into the glove boxes/equipment, the limiting fission yield for the facility was based on a scenario for a moderated powder or moderated solid criticality. In Ref. 9 (p. 6-24) dry powder and metal criticalities are quoted at a conservative yield of 1×10^{17} fissions. A reference yield of 1×10^{18} fissions is considered conservative for fully moderated and reflected solids. Therefore, a conservative selection of 1×10^{18} fissions was made for the evaluation of this criticality event.

It is acknowledged that a dry criticality could potentially aerosolize surrounding plutonium and generate respirable particles. The amount of aerosolization is expected to be very small, and the presence of multiple filters would be an effective mitigator against the spread of plutonium out of the ventilation system. Thus, no plutonium was assumed to constitute the source term with respect to exposure of the collocated workers and the public that are outside of the building. Other events involving significant plutonium releases are discussed later.

With respect to release fractions associated with the fission products, it would be expected that a powder would have a surface area such that all noncondensible gases (such as the nobles) and all radioiodines would escape. However, if the criticality involved plutonium, which was in a relatively low surface area to volume ratio, the release fraction associated with the noble gases and radioiodines would be considerably less. In consideration of the present unknown specifics associated with this event, it was deemed conservative and appropriate to select the release fractions for both the nobles and the radioiodines as 1.0. Fission product yields from Table 6-9 of Ref. 5 (a plutonium solution of unknown isotopics for a reference yield of 1×10^{19} fissions) were selected, and consideration of the selected yield of 1×10^{18} fissions resulted in scaling the source terms.

The chosen source term specifics for the evaluation basis criticality event are shown in Table 15. As previously discussed a conservative fission yield (moderated vs dry criticality) was combined with a conservative release fraction (for a powder vs moderated criticality). Thus, the source term in Table 15 is judged to be very conservative. The release height should be selected as the appropriate stack height for the facility where dose consequences are being calculated. The leak-path factor was taken as 1.0.

7.3.1.3 Frequency Estimate

Criticalities have occurred considerably less frequently than in the earlier days of nuclear research, development, and operations. A number of these accidents are discussed in Ref. 10. None of these accidents are specifically associated with dry plutonium powder. However, several accidents involving dry metal, moderated metals, and fuel rods have occurred during the last 50 years. The fact that 30–40 criticalities in the United States have historically (mostly in the 1940s, 1950s, and 1960s) occurred suggests that the accident spectrum analyzed for this facility should contain a criticality at a low estimated frequency. As was the case in Ref. 2, a frequency estimate of extremely unlikely (1×10^{-4} to 1×10^{-6}/year) is still judged to be appropriate for this event. However, the frequency of this event is judged to be somewhat less (perhaps 1 order of magnitude) than that at the large plant (100 MT/year vs 2 MT/year) because of the simplicity of the LA plant and the lower amounts of fissile material being handled.

Table 15. Source term for the evaluation basis criticality event (stack release with a relatively short duration)

Isotope	Released radioactivity (Ci)
^{83m}Kr	1.1×10^{1}
^{83m}Kr	7.1×10
^{85}Kr	8.1×10^{-4}
^{87}Kr	4.3×10^{1}
^{88}Kr	2.3×10^{1}
^{89}Kr	1.3×10^{3}
^{131m}Xe	1.0×10^{-2}
^{133m}Xe	2.2×10^{-1}
^{133}Xe	2.7×10
^{135m}Xe	3.3×10^{2}
^{135}Xe	4.1×10^{1}
^{137}Xe	4.9×10^{3}
^{138}Xe	1.1×10^{3}
^{131}I	1.1×10
^{132}I	1.2×10^{2}
^{133}I	1.6×10^{1}
^{134}I	4.3×10^{2}
^{135}I	4.5×10^{1}

7.3.2 Evaluation Basis Seismic Event

7.3.2.1 Discussion

A seismic event appropriate for the facility's evaluation basis was selected. In this event, major portions of the process line glove boxes are assumed to be breached with the contents available for release. In such an event, the focus was on the dispersible powders that would be at the powder blending stations. The storage vault and receiving area are assumed to have suitable containers for plutonium oxide that will survive the earthquake (3013 cans with double containment).[7] In-process material in glove boxes is, however, more vulnerable as are powder storage areas that may exist. Finished pellets and fuel rods are thought to be generally nondispersible even though they may escape the glove boxes. In this seismic event, the glove boxes are breached and assumed to fail based on a scenario of falling debris and equipment inside the room. The building confinement and ventilation system are assumed to remain intact, resulting in a filtered stack release.

7.3.2.2 Source term

Because the material in the vault is assumed to be in 3013 cans (which have double containment), no material was judged to be released from this area in this event. Table 16 shows the materials in process along with the release fractions and respirable fractions that were used. The total isotopic source term is shown summarized at the bottom for each plutonium isotope, as is the total amount of plutonium released. Because only 32 kg of plutonium oxide is allowed in a single batch, it was assumed that this batch was split in inventory between the master mix and fuel blend mix stations. This material was assumed to be in temporary storage cans at their respective stations. Another 10 kg of plutonium oxide in the form of powder is assumed to be at risk and open within the glove box. This material is from two cans that are taken out of the vault and prepared for loading (no credit for the 3013 can double containment).

Table 16. Source term for the evaluation basis seismic event

Processing station	Material at risk (g)	Physical form	Damage ratio	Airborne release fraction	Respirable fraction	Leak-path factor	^{238}Pu released	^{239}Pu released	^{240}Pu released	^{241}Pu released	^{242}Pu released	^{241}Am released
Plutonium oxide (2 cans)	10,000	Fine powder PuO_2	1.00	1.00×10^{-2}	0.20	1.00×10^{-5}	9.06×10^{-7}	1.01×10^{-5}	2.59×10^{-6}	9.08×10^{-6}	6.93×10^{-10}	5.44×10^{-6}
Master mix powder storage	53,000	Fine powder MOX (30% blend)	1.00	1.00×10^{-3}	0.10	1.00×10^{-5}	7.20×10^{-8}	8.02×10^{-7}	2.06×10^{-7}	7.22×10^{-7}	5.51×10^{-11}	4.33×10^{-7}
MOX blend storage	160,000	Fine powder MOX (10% blend)	1.00	1.00×10^{-3}	0.10	1.00×10^{-5}	7.25×10^{-8}	8.07×10^{-7}	2.07×10^{-7}	7.27×10^{-7}	5.54×10^{-11}	4.35×10^{-7}
Total isotopic source term, Ci							1.05×10^{-6}	1.17×10^{-5}	3.00×10^{-6}	1.05×10^{-5}	8.03×10^{-10}	6.31×10^{-6}
Total source term, Pu/Am mix, g								2.0454×10^{-4}				

In a seismic event, powders in various pieces of equipment will be subjected to many different damage ratios and release fractions. For the pure oxide powder at the feed station, the entire amount was conservatively subjected to a release fraction corresponding to debris falling into powder (no credit for the two open cans, utilizing a 1×10^{-2} airborne release fraction and 0.2 respirable fraction for the total release fraction from Ref. 5). With respect to the 32-kg batch of in-process powder, the powder stored in interim containers is assumed to be subjected to damage. A 1×10^{-3} airborne release fraction and 0.1 respirable fraction for the total release fraction was selected from Ref. 5 based on falling equipment impacting storage cans of powder. No credit is taken for the glove boxes that were postulated to fail. However, other portions of the process operation were assumed to be resistant to the event because of the material form. Finished pellets and fuel rods were not considered to constitute a significant portion of dispersible material. The source term is assumed to be filtered (leak-path factor of 1×10^{-5}) and released to a stack.

7.3.2.3 Frequency estimate

The frequency estimate for this event varies widely, depending on the site selected (and its respective seismic profile), the building used (and its evaluation basis), and the internal arrangement of equipment (see Sect. 7.5). Generally, a frequency estimate of 1×10^{-2} to 1×10^{-4} is used for this event (the frequency is usually closer to lower end of this range).

7.3.3 Evaluation Basis Fire Event

7.3.3.1 Discussion

A large spectrum of fire events ranging from small fires with no impacts to large multiroom fires with major impacts can be postulated for the LA fabrication building. Unlike the large MOX fabrication facility, the LA mission will take place in an existing building. While many existing buildings within the DOE complex are adequately covered by an existing fire protection program, it is reasonable to conclude that existing buildings might be more susceptible to fires (as compared to a new facility where fire protection can be incorporated into the design). However, the existing buildings must still meet the appropriate DOE orders.

A source of combustible material such as hydraulic fluid, alcohol, contaminated combustibles, or some other material is assumed to be present in the room. In addition, adjoining facilities such as offices may exist in the building and add to the risk of fires in the facility. The glove boxes are assumed to fail in the fire. This event is assumed to be a moderate-size room fire. The MOX powder that is in interim storage is assumed to be at risk and subjected to the thermal stress of the fire, because the glove box fails. Because of the limited combustible material and/or the existence of mitigators such as a fire protection system or arrival of the firefighting unit, the event is assumed to be terminated. The severity of this fire is not enough to jeopardize the overall confinement characteristics of the building.

7.3.3.2 Source term

Table 17 shows the materials in process along with the release fractions that were used. With respect to the oxide containers (10 kg), a high release fraction was selected based on a pressurized gas release combined with powder. This corresponds to a highly pressurized, strong, single can that ruptures under a high thermal stress because of pressure and ejects powder from the breached container. A 10% damage ratio (thus, 500 g of powder are subjected to the release fraction) was selected on the basis that the release fraction does not apply universally to all of the powder in the can (the release fraction will go down as larger cans of powder are subjected to the energetics).

The 32-kg inventory in the process area was assumed to be evenly split between the master mix and MOX fuel blend storage areas. The entire interim storage inventory of MOX powder is assumed to be subjected to a release fraction corresponding to thermal stress (6×10^{-3} airborne release fraction and 0.01 respirable fraction from Ref. 5). Green pellets, finished pellets, and fuel rods were not considered to constitute a significant portion of dispersible material. The material is assumed to be filtered and released to a stack. The scrap area was assumed to contain mostly solid material and was not judged to be a significant

Table 17. Source term for the evaluation basis fire

Processing station	Material at risk (g)	Physical form	Damage ratio	Airborne release fraction	Respirable fraction	Leak-path factor	^{238}Pu released	^{239}Pu released	^{240}Pu released	^{241}Pu released	^{242}Pu released	^{241}Am released
Plutonium oxide (2 cans)	10,000	Fine powder PuO_2	0.10	1.00×10^{-1}	0.70	1.00×10^{-5}	3.17×10^{-6}	3.53×10^{-5}	9.05×10^{-6}	3.18×10^{-5}	2.42×10^{-9}	1.90×10^{-5}
Master mix powder storage	53,000	Fine powder MOX (30% blend)	1.00	6.00×10^{-3}	0.01	1.00×10^{-5}	4.32×10^{-8}	4.81×10^{-7}	1.23×10^{-7}	4.33×10^{-7}	3.30×10^{-11}	2.60×10^{-7}
MOX blend storage	160,000	Fine powder MOX (10% blend)	1.00	6.00×10^{-3}	0.01	1.00×10^{-5}	4.35×10^{-8}	4.84×10^{-7}	1.24×10^{-7}	4.36×10^{-7}	3.32×10^{-11}	2.61×10^{-7}
Total isotopic source term, Ci							3.26×10^{-6}	3.63×10^{-5}	9.30×10^{-6}	3.27×10^{-5}	2.49×10^{-9}	1.96×10^{-5}
Total source term, Pu/Am mix, g								6.343×10^{-4}				

source of dispersible material. As with other source terms no credit was taken for in-facility filters, as these may fail because of the fire. The source term is filtered and released to a stack.

7.3.3.3 Frequency estimate

The frequency estimate of fires depends on the conduct of operations, the building selected, the adequacy of the fire protection program, and a number of other variables. A frequency estimate of between 1×10^{-2}/year and 1×10^{-4}/year (unlikely) is judged to be appropriate for this event because a relatively small area is assumed to be involved.

7.3.4 Evaluation Basis Explosion Event

7.3.4.1 Discussion

As was the case in Ref. 2, an explosion event was postulated for the sintering furnace in the LA fabrication facility. A nonexplosive mixture of 6% hydrogen and 94% argon is used in the furnace. Multiple equipment and operator errors would have to occur to enable an explosive mixture of hydrogen mixed with air to build up in the box. As a result of the explosion, green pellets are assumed to be subjected to the direct force of the resultant shock waves. Unlike Ref. 3, where the facility layout can accommodate segregation (in effect limiting the explosion damage), it is assumed that the glove boxes involved in powder blending are damaged indirectly by the explosion. It is not expected that the shock wave impacting this area would be severe enough to significantly damage all of the storage inventory because interim storage cans would provide some mitigation.

7.3.4.2 Source term

The split in the material at risk (between green pellets, pellets in the furnace, and powder storage areas) is shown in Table 18 for the 32-kg batch. No specific release fractions are given in the literature for deflagration forces on green pellets that are pressed to ~60% theoretical density. Reference 5, Sect. 4.3.3, discusses a formulation for determining the product of the airborne release fraction and respirable fraction (ARF*RF) for dropped uranium dioxide pellets. A release fraction (combined ARF*RF) of 1×10^{-4} was deemed to be conservative for all material (40,000 g) in the furnace subjected to explosive forces. This same release and respirable fraction was also used for the green pellets that would be pressed and likely near the furnace. The 80,000 g of green pellets would be a little further from the blast and in trays or containers. The same release fraction was applied to these green pellets and is thought to be conservative.

The remaining part of the 20-kg batch was assumed to be split between the MOX master blend and powder storage stations. The MOX powder in the blending areas would likely be in a different glove box and somewhat removed from the blast. These glove boxes are assumed to be indirectly damaged from the explosion. As previously stated, most of the storage powder would be in interim cans that would merely be displaced. Powders in a glove box that undergo damage from external explosions are discussed in Ref. 5 (p. 4-69). A release fraction (and respirable fraction) of 5×10^{-3} (and 0.3) were used and conservatively applied to all of the powder. The total source term is shown in Table 18. The building confinement is judged to be still intact resulting in a filtered stack release.

7.3.4.3 Frequency estimate

Because no definitive designs for the furnace and glove boxes currently exist, estimation of the probability of this event is difficult at this time. A judgment was made that the frequency of this event is extremely unlikely (between 1×10^{-4}/year and 1×10^{-6}/year). Such an explosion of sufficient size from the furnace to impact the glove boxes would only be possible because of a combination of equipment failure and human error.

Table 18. Source term for the evaluation basis explosion

Processing station	Material at risk (g)	Physical form	Damage ratio	Airborne release fraction	Respirable fraction	Leak-path factor	^{238}Pu released	^{239}Pu released	^{240}Pu released	^{241}Pu released	^{242}Pu released	^{241}Am released
Master mix powder storage	33,000	Fine powder MOX (30% blend)	1.00	5.00×10^{-3}	0.3	1.00×10^{-5}	6.73×10^{-7}	7.49×10^{-6}	1.92×10^{-6}	6.75×10^{-6}	5.14×10^{-10}	4.04×10^{-6}
MOX blend storage	100,000	Fine powder MOX (10% blend)	1.00	5.00×10^{-3}	0.3	1.00×10^{-5}	6.79×10^{-7}	7.57×10^{-6}	1.94×10^{-6}	6.81×10^{-6}	5.19×10^{-10}	4.08×10^{-6}
MOX green pellet storage (in pellet press area)	80,000	Pressed to 0.6 TD, MOX (10% blend)	1.00	1.00×10^{-4}	1	1.00×10^{-5}	3.62×10^{-8}	4.04×10^{-7}	1.03×10^{-7}	3.63×10^{-7}	2.77×10^{-11}	2.18×10^{-7}
Pellet sintering furnace	40,000	Assume all green pellets MOX (10% blend)	1.00	1.00×10^{-4}	1	1.00×10^{-5}	1.81×10^{-8}	2.02×10^{-7}	5.17×10^{-8}	1.82×10^{-7}	1.39×10^{-11}	1.09×10^{-7}
Total isotopic source term, Ci							1.41×10^{-6}	1.57×10^{-5}	4.02×10^{-6}	1.41×10^{-5}	1.08×10^{-9}	8.45×10^{-6}
Total source term, Pu/Am mix, g								2.739×10^{-4}				

7.3.5 Beyond-Evaluation Basis Seismic Event

7.3.5.1 Discussion

In this analysis an event much more severe in consequences than what might be expected to be the design basis (or evaluation basis) is examined. For some existing DOE facilities, the estimated seismic frequency for beyond-design basis events can be greater than 1×10^{-6}/year. The design basis for every building in the complex varies considerably depending on site specifics and the type of construction used in the building. A damage assessment of the facility is further complicated by the fact that seismic considerations could also be incorporated in the glove box design of the facility. In reality, such a catastrophic event may or may not demolish the building and/or the glove boxes. However, for the purposes of illustrating a high consequence accident (which occurs at a very low frequency), total demolition of the building has been assumed. In this event, no credit is taken for the building, the filters, or the glove boxes.

7.3.5.2 Source term

In the evaluation basis seismic event previously discussed, credit was taken for the 3013 cans (which have double containment) in the vault storage area. In this event, however, a total building collapse is used, and a judgment was made that a few of the containers may fail. A damage ratio of 0.05 was used; it equates to 4 out of 80 cans in the vault area. For the source term evaluation of the remainder of the in-process material (including the two cans that feed the process), the release fractions were selected to be the same as in the evaluation basis seismic event. However, because it is assumed that the building collapses and the ventilation system is severed, no credit is taken for filtration. This results in a building leak-path factor of 1.0. The source term is assumed to be released at or near ground level (10 m). Table 19 shows the source term for this event.

7.3.5.3 Frequency

As discussed previously there is great difficulty in assigning a frequency for this event, especially because facilities are not analyzed for very high seismic events that occur with very infrequent return periods. Site specifics make the frequency assessment of this event very uncertain as well. For the sake of this analysis, a frequency value of 1×10^{-6} or less is thought to be appropriate for the EIS purposes.

7.3.6 Beyond-Evaluation Basis Major Building Fire

7.3.6.1 Discussion

Fuel manufacturing operations do not lend themselves to the use of large significant amounts of combustible material. In this scenario, however, it is assumed that the building is burned for a considerable length of time, resulting in a total collapse of the building. This event could also roughly be characterized as a large fire following a total building collapse.

7.3.6.2 Source term

Some thought was given to the stability of the 3013 cans in the vault which would be subjected to prolonged heat during a large fire. Because of the double containment and high-pressure rating for the cans, it was judged that the cans could withstand a large building fire. However, because a major building fire breaches the confinement, it is assumed that the building structure could collapse. This happens in large buildings subjected to high heat loads for long periods of time. As a result of this consideration, four of the cans in the vault area were assumed to have breached, just as in the beyond-evaluation seismic event. For the two oxide cans in process, it was conservatively assumed that they burst (previously discussed in the evaluation-basis fire scenario). The remainder of the 32-kg inventory was assumed to be subjected to a

Table 19. Source term for beyond the evaluation basis seismic event (total building collapse assumed)

Processing station	Material at risk (g)	Physical form	Damage ratio	Airborne release fraction	Respirable fraction	Leak-path factor	^{238}Pu released	^{239}Pu released	^{240}Pu released	^{241}Pu released	^{242}Pu released	^{241}Am released
Plutonium storage vault	400,000	Fine powder PuO_2	0.05	1.00×10^{-3}	0.10	1.00×10^{0}	9.06×10^{-3}	1.01×10^{-1}	2.59×10^{-2}	9.08×10^{-2}	6.93×10^{-6}	5.44×10^{-2}
Plutonium oxide (2 cans)	10,000	Fine powder PuO_2	1.00	1.00×10^{-2}	0.20	1.00×10^{0}	9.06×10^{-2}	1.01×10^{0}	2.59×10^{-1}	9.08×10^{1}	6.93×10^{-5}	5.44×10^{-1}
Master mix powder storage	53,000	Fine powder MOX (30% blend)	1.00	1.00×10^{-3}	0.10	1.00×10^{0}	7.20×10^{-3}	8.02×10^{-2}	2.06×10^{-2}	7.22×10^{-2}	5.51×10^{-6}	4.33×10^{-2}
MOX blend storage	160,000	Fine powder MOX (10% blend)	1.00	1.00×10^{-3}	0.10	1.00×10^{0}	7.25×10^{-3}	8.07×10^{-2}	2.07×10^{-2}	7.27×10^{-2}	5.54×10^{-6}	4.35×10^{-2}
Total isotopic source term, Ci							1.14×10^{-1}	1.27×10^{0}	3.26×10^{-1}	1.14×10^{-0}	8.72×10^{-5}	6.85×10^{-1}
Total source term, Pu/Am mix, g								22.22				

release fraction corresponding to falling debris in cans (similar to a seismic event). The total estimated source term is shown in Table 20. However, because considerable heat is produced by the fire, a significant plume rise would occur. Therefore, a release height of 100 m was judged to be appropriate for this event.

7.3.6.3 Frequency

Assigning a frequency for this event is difficult because significant combustible loads are not placed in close proximity to the process. This is a very low frequency noncredible event, which requires the introduction of significant combustibles that would create a fire large enough to collapse the structure. For the sake of this analysis, a frequency value of much less than 1×10^{-7} is thought to be appropriate for the EIS purposes.

7.4 EVALUATION OF POTENTIAL CHEMICAL SOURCE TERMS

Chemical and radiological materials used in this facility were previously given in Table 6. With respect to radiological effects, the source terms associated with plutonium oxide constitute an overwhelming majority of the radiological risk. With respect to the chemical hazards associated with depleted UO_2 (which are released in conjunction with the plutonium oxide in the scenarios outlined in the previous sections), no specific source terms have been generated in this analysis. As discussed in previous sections, only small amounts of plutonium (generally <1 g) constitute the source terms. If treated similarly (from a release standpoint), small amounts of the depleted uranium that may accompany the plutonium oxide that escapes the building are judged to be inconsequential.

Table 6 also gives the other chemicals and compounds that will be used annually by the facility and lists the yearly consumption of gases, liquids, and solids. With respect to any possibly chemical source term, the gases listed (i.e., helium, hydrogen, nitrogen, and oxygen) do not constitute an inhalation or exposure hazard in the context of LA fabrication operations. Reportable quantities of various chemical compounds are cited in 40 CFR 302, Table 302.4. If a chemical company operator spills less than these quantities, the Environmental Protection Agency is not notified. While this is not an absolute criterion that guarantees the lack of off-site consequences, it is illustrative to examine the yearly flow of chemicals based on these reported quantities.

Table 21 compares the annual usage of chemicals to the reportable quantities for that material. While not all materials are listed, the comparison shows that the LA facility does not constitute a major source of chemical inventories. The chemicals listed are either in a liquid or solid form, and the gases listed are not hazardous from an inhalation perspective. Typical occupational chemical exposure incidents, such as acid burns to a worker, are certainly credible. A significant release scenario (inhalation risk, ingestion risk, or skin contact risk) that constitutes a source term (with a magnitude of reasonable concern) to a receptor is difficult to credibly postulate at this stage of the facility analysis. Because of the small size of the facility and the small quantities of chemicals that are expected to be on hand, it is concluded that no chemical source terms are worthy of analysis (that are beyond what is found in small standard industrial facilities). The amounts that would be in use by this facility are certainly considered to be well within the scope of typical industrial hazards found in laboratory environments.

7.5 SITE SPECIFICS FOR HANFORD BUILDING 4862

The following seismic evaluations do not consider the equipment specifics that would be involved in the MOX LA fabrication line and represent an estimate for the building and confinement-related ventilation system. Cross-comparisons of frequencies and evaluation basis values for sites must be performed with caution. Such simple comparisons do not take into account the differences in analytical approaches that were used at each site to estimate the building response, acceleration, or estimated frequency for the site. As a general rule for all sites, it is expected that the evaluation basis frequency for a seismic event would be from 1×10^{-2}/year to 1×10^{-4}/year and would likely be between 1×10^{-3}/year and 1×10^{-4}/year.

7.5.1 Stack Release Height for Building 4862 (Category I)

For Building 4862, the stack release height is ~36.6 m (~120 ft).

7.5.2 Evaluated Seismic Attributes for Building 4862 (Category I)

For Building 4862, the current peak ground acceleration value of the evaluated basis earthquake for the building is 0.25 g, with an estimated frequency of 5×10^{-4}/year.

7.5.3 Stack Release Height for Building 325 (Non-Category I)

For Building 325, the stack release height is ~27 m (~88.5 ft).

7.5.4 Evaluated Seismic Attributes for Building 325 (Non-Category I)

For Building 325, the current peak ground acceleration value of the evaluated basis earthquake is 0.139 g, with an estimated frequency of 2×10^{-4}/year.

Table 20. Source term for beyond the evaluation basis major building fire/building collapse (total building collapse assumed to result; source term release height = 100 m)

Processing station	Material at risk (g)	Physical form	Damage ratio	Airborne release fraction	Respirable fraction	Leak-path factor	^{238}Pu released	^{239}Pu released	^{240}Pu released	^{241}Pu released	^{242}Pu released	^{241}Am released
Plutonium storage vault	400,000	Fine powder PuO_2	0.05	1.00×10^{-3}	0.10	1.00×10^{0}	9.06×10^{-3}	1.01×10^{-1}	2.59×10^{-2}	9.08×10^{-2}	6.93×10^{-6}	5.44×10^{-2}
Plutonium oxide (2 cans)	10,000	Fine powder PuO_2	0.10	1.00×10^{-1}	0.70	1.00×10^{0}	3.17×10^{-1}	3.53×10^{0}	9.05×10^{-1}	3.18×10^{0}	2.42×10^{-4}	1.90×10^{0}
Master mix powder storage	53,000	Fine powder MOX (30% blend)	1.00	1.00×10^{-3}	0.10	1.00×10^{0}	7.20×10^{-3}	8.02×10^{-2}	2.06×10^{-2}	7.22×10^{-2}	5.51×10^{-6}	4.33×10^{-2}
MOX blend storage	160,000	Fine powder MOX (10% blend)	1.00	1.00×10^{-3}	0.10	1.00×10^{0}	7.25×10^{-3}	8.07×10^{-2}	2.07×10^{-2}	7.27×10^{-2}	5.54×10^{-6}	4.35×10^{-2}
Total isotopic source term, Ci							3.41×10^{-1}	3.79×10^{0}	9.72×10^{-1}	3.42×10^{0}	2.60×10^{-4}	2.05×10^{0}
Total source term, Pu/Am mix, g								66.32				

Table 21. Comparison of LA facility annual usage and reportable quantity per 40 CFR 302

Item	Annual average consumption	Reportable quantity
Liquids		
Hydrochloric acid	1 lb	5,000 lb
Nitric acid	2 lb	1,000 lb
Polyethylene glycol	<45 lb	Not listed
Sulfuric acid	5 lb	1,000 lb
Solids		
Sodium hydroxide	34 lb	1,000 lb
Sodium nitrate	<200 lb	Not listed
Zinc stearate	<45 lb	Not listed
Nonprocess chemicals		
Alcohol	60 gal	Not listed
Hydraulic fluid	10 lb	Not listed
General cleaning fluids	60 gal	Not listed

8. TRANSPORTATION

8.1 OPERATIONS-RELATED TRANSPORTATION REQUIREMENTS

Production of MOX fuel LAs, irradiation of the LAs in commercial reactors, and subsequent PIE will result in a number of packaging and transportation operations to (1) obtain the necessary feed materials to manufacture LAs, (2) package and transport the completed fuel assemblies from the fabrication facility to the commercial reactor, and (3) package and transport the irradiated fuel assemblies from the commercial reactor to another facility for PIE.

Plans for MOX fuel LA testing involve manufacture of up to ten MOX fuel LAs, with up to eight LAs undergoing irradiation while the remaining LAs are maintained as unirradiated archives. Each LA could contain from as few as one-third MOX rods (with the balance of the rods being LEU) to an entire assembly composed of MOX rods. Under these circumstances, production of LA will require that LEU and MOX fuel rods be combined in a single assembly. This activity could occur at either the LA fabrication facility or at the reactor facility. While reactors generally have the ability to substitute individual rods within an assembly (due to detected damage), it is expected that exchanging as many as one-third of the LEU assembly rods with MOX rods would occur at the LA facility.

8.1.1 Feed Materials

Table 22 provides information about the shipment of PuO_2. Table 23 provides information about the shipment of depleted UO_2. Depleted UO_2 can be obtained by the consortium, or DOE will provide either depleted uranium fluoride (DUF_6) or depleted uranium oxide (DUO_3) for conversion by the consortium. Other materials (e.g., new empty fuel rods, end plugs, grid spacers, and other assembly hardware) are not "regulated" materials for transportation. Their shipment would not require special packaging, other than to protect the economic value of the commodity. The specific LA design is uncertain. Some designs may have every fuel rod contain MOX, while other designs may have both MOX and UO_2 fuel rods within a bundle. In the latter case, it would be necessary to either ship enriched UO_2 fuel rods (or UO_2 fuel rods in LEU fuel assemblies) to the MOX fabrication facility or to ship MOX fuel rods from the fabrication facility to the commercial fuel fabrication site (for insertion in LEU fuel assemblies shipped separately to the reactor). If the MOX LA will contain a large fraction of MOX rods (one-third or more), it is expected that the LA facility will need to receive LEU fuel assemblies (possibly, with unfilled rod positions) from a commercial fuel vendor. The LA fuel facility would then place MOX rods within the assembly and package the MOX LA for shipment to the reactor. Table 24 provides information on the shipment of LEU fuel assemblies to the MOX LA fuel facility, if needed.

8.1.2 Fresh MOX Fuel Assemblies

Table 25 provides information about the transport of fresh (unirradiated) MOX fuel from the fabrication facility to the commercial reactor, while Table 26 provides the fresh MOX fuel isotopic contents. The same package identified for shipment of the MOX fuel assemblies (the MO-1) would also be used to ship groups of individual MOX fuel rods to a commercial fuel fabrication site for insertion in a MOX fuel bundle if this approach is used.

8.1.3 Spent MOX Fuel Assemblies

Tables 27 and 28 provides information about the transport of spent (irradiated) MOX fuel from the commercial reactor to the PIE facility. Table 29 provides information regarding existing casks that could be used to transport spent MOX fuel to the PIE facility. The number of shipments of spent MOX fuel will depend on the actual plans for LA irradiation and plans for subsequent PIE. Based on the schedule described in Fig. 2, up to eight shipments of LA spent fuel could be transported between the reactor and the PIE facility.

Table 22. Transportation of PuO_2 to support LA fabrication

Number of shipments to LA fabrication site[a]	1 or more
Assuming 321 kg HM of plutonium as PuO_2 is needed for startup and to produce 10 LTAs	
Would require about 73 packages (4.4 kg HM/package). SST could accommodate 30 to 35 packages per trailer. Single SST convoy (three trailers) could deliver entire PuO_2 supply for LTA campaign.	
Container types used for shipments	Type B
Availability of containers	Yes
Likely candidate package would be 9968 or 9975, perhaps SAFKEG	
Only 9968 is currently certified	
Average shipping container weight	165 kg (360 lb)
Average material weight loaded into container	4.4–4.5 kg HM
Average isotopic contents	*b*
Average exposure rate at 1 m	0.1 mrem/h
Maximum anticipated dose rate at 1 m	10 mrem/h
Will need to be determined	
Regulatory limits are 200 mrem/h at surface of package (1000 mrem/h for closed transport vehicles, exclusive use, cargo secured); 200 mrem/h (outer surface of vehicle); 10 mrem/h at point 2 m from package surface; and 2 mrem/h (in occupied spaces) (i.e., crew cab, etc.)	

[a]For the bounding case of all MOX rods in assemblies.
[b]See Table 26.

Table 23. Transportation of depleted UO_2 to support LA fabrication[a,b]

Number of shipments to LA fabrication site	1
UO_2 is shipped in standard metal drums	
Truck could accommodate 40,000 lb (~72 drums)	
Mission would only require about 28 drums UO_2	
Container types used for shipments	208-L drum
A strong-tight container (open head 55-gal drum)	
Probably use UN1A2 (steel drum)	
Availability of containers	Yes
Average shipping container weight, kg (lb)	275 kg (600 lb)
Average material weight loaded into container	250 kg
Average isotopic contents	Depleted uranium[a]
Average exposure rate at 1 m	~0
Maximum anticipated dose rate at 1 m	10 mrem/h
Will need to be determined	
Regulatory limits are 200 mrem/h at surface of package (1000 mrem/h for closed transport vehicles, exclusive use, cargo secured); 200 mrem/h (outer surface of vehicle); 10 mrem/h at point 2 m from package surface; and 2 mrem/h (in occupied spaces) (i.e., crew cab, etc.)	

[a]See Ref. 3 for more information on depleted uranium. Refer to Table 26 for uranium isotopic content.
[b]Unlike UF_6 cylinders, depleted UO_2 is purified, with daughter products removed that result in potential doses.

Table 24. Transportation of materials to support LA fabrication (LEU fuel assemblies)

Number of shipments of LA fabrication site Assuming that all 10 LEU assemblies could be shipped on a single commercial vehicle (just as LEU fuel is shipped currently). Would require use of 5 LEU fuel packages.	1
Container types used for shipments	Type AF
Availability of containers	Yes
Average shipping container weight, kg (lb)	2900 kg (6300 lb) to 3800 kg (8400 lb)
Average material weight loaded into container	1400 kg (3000 lb)
Average isotopic contents	LEU, up to 5% ^{235}U
Average exposure rate at 1 m, mR/h	~0 (not measurable)
Maximum anticipated dose rate at 1 m, mR/h Will need to be determined Regulatory limits are 200 mrem/h at surface of package (1000 mrem/h for closed transport vehicles, exclusive use, cargo secured); 200 mrem/h (outer surface of vehicle); 10 mrem/h at point 2 m from package surface; and 2 mrem/h (in occupied spaces) (i.e., crew cab, etc.)	10 mrem/h

Table 25. Transportation of LAs to generic reactor site

Number of SST shipments of LAs to generic reactor Assuming two shipments (four assemblies) each to two different reactors, with two additional assemblies archived	4
Type of containers used for shipments Likely candidate is the MO-1, USA/9069/B Potential problems—NRC may require additional analysis to continue inclusion of MOX contents on package certificate. Also, MO-1 certificate lists 85% fissile plutonium in total plutonium. WG MOX would be ~94%, so additional analysis is needed to ensure that LTAs can be transported in MO-1 (may need to enhance criticality controls). No package currently available in the United States for boiling-water reactor (BWR) MOX assemblies; probably could amend MO-1 certificate to allow two BWR assemblies	Type B package
Availability of containers	Only two MO-1 packages exist
Average shipping container weight Gross weight, including two pressurized-water reactor (PWR) fuel assemblies	3900 kg (8600 lb)
Average material weight loaded into shipping container	~1400 kg (3000 lb)
Average isotopic content (by isotope, mass % content)	*a*
Average exposure rate at 1 m Will need to be determined, both for worker doses as well as transportation risk assessment Should be fairly low	0.1 mrem/h
Maximum anticipated dose rate at 1 m Will need to be determined Regulatory limits are 200 mrem/h at surface of package (1000 mrem/h for closed transport vehicles, exclusive use, cargo secured); 200 mrem/h (outer surface of vehicle); 10 mrem/h at point 2 m from package surface; and 2 mrem/h (in occupied spaces) (i.e., crew cab, etc.)	10 mrem/h

[a]See Table 26.

Table 26. Fresh MOX fuel isotopic content[a]

Average isotopic content (%)	Mass content (%)
^{235}U, 0.2	0.1915
^{238}U, 99.8	95.556
^{236}Pu, <1 ppb	–
^{238}Pu, 0.03	0.00053
^{239}Pu, 92.44	3.995
^{240}Pu, 6.47	0.2485
^{241}Pu, 0.05	0.00592
^{242}Pu, 0.1	0.00249
^{241}Am, 0.9	0.004

[a] *Source*: Ref. 2.

Note: MOX fuel will be produced with various plutonium concentrations depending on the mission reactors.

Table 27. Transportation of irradiated LAs to PIE site

Number of shipments of irradiated LAs to PIE site	Up to 8
Depending on cask selection, see Table 29	
Types of container used for shipments	Type B
Availability of shipping containers	Yes
Several available choices dependent on previous commitments, ability of facilities to handle particular packages	
Possible choices—NAC-LWT or NLI. Each would hold one PWR or two BWR assemblies	
Average shipping container weight	25–40 tons
Average material weight	700–2100 kg (1500–4500 lb)
Average isotopic content	See Table 28
Uranium, transuranics, fission products (dependent on burnup and decay time)	
Average exposure rate at 1 m (mrem/h) dependent on burnup and decay time	~10 mrem/h[a]
Maximum anticipated dose rate at 1 m	Unknown
Dependent on fuel burnup and decay plus selection of package	
Must be below regulatory limits	

[a] Each cask will be loaded to the maximum capacity without exceeding regulatory dose limits.

Table 28. Spent MOX fuel isotopic content

Isotope	Mass content[a] (g/assembly)
	Actinides
^{234}U	1.28×10^{1}
^{235}U	3.56×10^{2}
^{236}U	1.13×10^{2}
^{238}U	4.25×10^{5}
^{237}Np	8.42×10^{1}
^{238}Pu	9.70×10^{1}
^{239}Pu	6.99×10^{3}
^{240}Pu	4.06×10^{3}
^{241}Pu	1.49×10^{3}
^{242}Pu	7.50×10^{2}
^{241}Am	1.04×10^{3}
^{242}Am	3.22×10^{0}
^{243}Am	2.03×10^{2}
^{242}Cm	8.39×10^{-3}
^{243}Cm	8.73×10^{-1}
^{244}Cm	5.38×10^{1}
^{245}Cm	5.40×10^{0}
	Fission products
^{90}Sr	1.31×10^{2}
^{106}Ru	1.77×10^{-1}
^{106}Ru	1.77×10^{-1}
^{106}Ru	1.77×10^{-1}
^{126}Sb	1.06×10^{-6}
^{134}Cs	2.81×10^{0}
^{137}Cs	6.21×10^{2}
^{144}Ce	2.21×10^{-2}
^{147}Pm	6.71×10^{0}
^{148}Nd	2.25×10^{2}
^{154}Eu	1.30×10^{1}

[a]Spent fuel composition is for MOX containing 4.56 wt % plutonium at a burnup of 45 GWd/MT, 10 years after discharge. Table includes only most significant isotopes.

Source: Memorandum, B. D. Murphy to R. T. Primm III, "Computational Support to Yucca Mountain Project Environmental Impact Statement Data Call," September 12, 1997.

Table 29. Examples of casks for LWR spent fuel

Name	Owner	Certification No.	Gross weight (lb)	Cavity size	Contents
NAC-LWT	NAC International, Norcross, GA	USA/9225/B(U)F	51,200	181 in. long by 13.4-in. diam	1 PWR or 2 BWR assemblies
NLI-1/2	NAC International, Norcross, GA	USA/9010/B( )F	49,250	178 in. long by 13.4-in. diam	1 PWR or 2 BWR assemblies
TN-8L	Transnuclear, Hawthorne, NY	USA/9015/B( )F	79,380	3 cavities, 9 in. × 9 in. × 168.5 in.	3 PWR assemblies
TN-9	Transnuclear, Hawthorne, NY	USA/9016/B( )F	79,200	7 cavities, ~6 in. × 6 in. × 178 in.	7 BWR assemblies

9. QUALITATIVE DECONTAMINATION AND DECOMMISSIONING DISCUSSION

9.1 INTRODUCTION

The DOE facilities that will be used in the fabrication of MOX LAs have been used previously in the handling of nuclear materials. Because most of the facilities are contaminated to some degree, the MOX mission should have few incremental effects on the ultimate D&D of these facilities. The intent of the FMDP is to decontaminate the facilities to levels that would permit unrestrictive further use of the facilities.

9.2 PROCESS PLAN

The development of a detailed D&D plan will be necessary to minimize waste generation. Waste minimization during D&D begins with the design of the MOX facility as discussed below. During the D&D phase, waste minimization measures would be similar to those required in the operation of any nuclear contamination zone. This includes reducing the number of items taken into a contamination zone to the minimum necessary to perform the job.

9.3 D&D OPERATIONS

Because plutonium is primarily an alpha emitter, containment of contamination is a principle concern in the design and operation of a MOX plant. The process involves two distinctly different areas concerning contamination: (1) pellet fabrication where dusty powders of plutonium and uranium oxides are handled and (2) the rod and bundle assembly areas where little if any contamination should be present. At least 95% of the waste that will be generated during D&D will be from the pellet fabrication area.

In the pellet fabrication area, a principle concern must be containment of the potential contamination from the copious quantities of plutonium and uranium dust that will be generated during operation of the dry processes. To minimize future D&D costs, the containment of this potential contamination at its source of generation must be considered in the design of the MOX facility. This design should include local filtration at the source with no contamination allowed in the duct systems.

The rod and bundle assembly areas will use about 50% of the total space in the MOX facility and should be relatively contamination free. This space could be returned to beneficial occupancy soon after completion of the mission by simply removing the process equipment. Most of the uncontaminated rod and bundle assembly equipment will likely be useful in the full-scale MOX plant and could be shipped to that facility in the future.

Most of the waste generated during D&D will come from the pellet fabrication area in the disassembly and disposal of contaminated process equipment items and excess glove boxes. The waste generated during D&D, in addition to the contaminated equipment items and glove boxes, will be similar to the waste generated during operation of the MOX plant. This will consist of solid and liquid radioactive waste in similar types and volumes that will be generated during operations. The ratio of TRU to LLW likely will be higher during D&D from the cleanup of the plutonium contamination in the glove boxes. The emissions during D&D should be no more than during the operating phase of the LA MOX plant.

Complete decontamination probably will not be possible for most of the glove boxes and contaminated equipment items, and disposal as either LLW or TRU waste will be required. Most of the large equipment items and excess glove boxes likely will be packaged in large B-25 (4 ft × 4 ft × 6 ft) metal waste boxes. Size reduction of some equipment items and glove boxes likely will be required to fit within these boxes. The assay of the TRU content in some contaminated equipment items will be difficult to determine because of the difficulty of establishing calibration standards for the assay equipment. Also, the waste acceptance criteria for such "difficult to certify" TRU waste items for WIPP disposal have not been completely resolved by DOE.

The equipment in the rod and bundle assembly areas either will not be contaminated or probably can be decontaminated to clean release standards for unrestricted use. The disposal of this equipment should present no particular problem.

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10. PIE

The two sites being considered for the PIE are Argonne National Laboratory–West (ANL–W) and ORNL. The facilities and infrastructure required to complete all PIE activities for the LA program currently exist at both sites. Accommodation of full-length fuel rods is the only modification required at ANL–W or ORNL to process the materials associated with this program. Both sites currently process equivalent materials to those expected in this program, and program activities will be routine.

Table 30 shows the wastes estimated during the LA PIE. Table 31 shows the possible employee radiation doses involved during PIEs of the LAs, and Table 32 lists the estimated PIEs for the EIS.

Figure 12 shows the location of Building 3525 on the ORNL site, and Fig. 13 shows the location of Building 785 on the ANL–W site. These buildings could be used to perform all PIE activities.

10.1 PIE DISCUSSION

PIE begins by shipping either the fuel assembly or the individual rods to the PIE facility. Shipment of selected individual rods is desired as it eliminates a handling step at the PIE facility (disassembly of the fuel assembly) and reduces the amount of irradiated fuel that needs to be handled (because only a fraction of the rods in a bundle is examined), stored, and disposed of at the hot cell.

Once the rods are in the hot cell at the PIE facility they are first subjected to a nondestructive examination. The degree of examination varies, but typically the rods are visually examined for signs of damage or wear, their length and diameter is measured, and individual rods may be weighed. After this simple check, additional examinations include eddy current or ultrasonic testing to locate cracks or flaws; leak testing to determine gas containment; gamma scanning to determine the internal fuel rod integrity, migration of fission products, and burnup; neutron radiography and X-ray radiography to determine the internal physical configuration; and detailed visual examination of any crud or oxide layers on the surface of the clad. The particular techniques employed will depend on the program needs.

After the nondestructive testing has been satisfied, the destructive testing often begins by sampling the fission gas pressure and composition in the rod plenum by puncturing the end of the rod and collecting the gas. The rod may then be cut into segments for fuel examination. Thin sections of the rod are often cut off, mounted in epoxy resin, and polished for metallographic and ceramographic examinations. Additional portions of the fuel rod may be cut up for further fuel and clad examinations. Thin cross sections of the rod may be core drilled for fuel samples and the cores examined by gamma scanning or subjected to radiochemistry examination by dissolution in a chemical solution. The solution may undergo chemical analysis, gamma counting, and/or mass spectrometry for the determination of burnup and fission product composition.

Fuel specimens may undergo density measurements, pore size measurements, thermal diffusivity measurements, specific heat determination, melting point temperature estimation, oxygen to metal ratio measurements, and/or fission gas diffusivity depending on the degree of the investigation and the equipment available.

The rod cross sections may also be mounted in special mounts for examination by microprobe, optical microscope, transmission electron microscopy, and/or scanning electron microscope. Other techniques such as X-ray fluorescence and emission spectroscopy may be used depending on the needs of the investigation. These techniques allow the experimenter to determine the amounts and distribution of fission products, plutonium, uranium, and some trace elements. Such analyses allow the experimenter to compare the results of the irradiation with predictions and to investigate fuel behavior in considerable detail.

Clad specimens for mechanical testing may be prepared by segmenting the fuel rod and sliding the fuel out if possible, drilling the fuel out, or cutting and peeling the clad from the fuel. Once prepared, the clad may be subjected to a wide variety of tests such as tensile testing, burst testing, hardness testing, ductility testing, creep tests, fatigue testing, and chemical surface analysis.

All of these tests are considered to be normal PIE practices. The scope of the required equipment can be as simple as a small numbered scale to complex expensive shielded special purpose microscopes. Two references for PIE work are the *Guidebook on Non-Destructive Examination of Water Reactor Fuel, IAEA*

Table 30. Estimated waste generated during the LA PIE

Waste category	Annual volume	Total estimated volume (based on 4 years)	Waste description (e.g., glove box gloves, cleaning solvent, paper wipes)	Anticipated treatment and/or disposal method (e.g., solidification) (specify on-site or off-site)
TRU			Paper wipes, plastic, glassware, metal containers, fuel debris, clad pieces, radiochemical solutions	Solid material packaged in drums for shipment to WIPP; liquids processed on-site for later off-site disposal as LLW
Liquid	107 L (28.2 gal)	427 L (112.8 gal)		
Solid	2.6 m^3 (91.8 ft^3)	10.4 m^3 (367.3 ft^3)		
Mixed TRU			Oils, solvents, and lead shielding contaminated with TRU materials.	Solid material will be packaged in drums for shipment to WIPP; liquids will be processed on-site for later off-site disposal as LLW
Liquid	1.08 L (0.29 gal)	4.3 L (1.16 gal)		
Solid	0.03 m^3 (0.883 ft^3)	0.1 m^3 (3.53 ft^3)		
LLW[a]			Paper wipes, plastic, glassware, metal containers, clad pieces, equipment	Material will be prepared on-site for shipment to off-site facility
Liquid	107 L (28.2 gal)	427 L (112.8 gal)		
Solid	35 m^3 (1236 ft^3)	140 m^3 (4944 ft^3)		
Mixed LLW[b]			Oils, solvents, and lead shielding contaminated with fission products materials	Material will be sorted and prepared on-site for shipment to off-site facilities
Liquid	1.08 L (0.29 gal)	4.3 L (1.16 gal)		
Solid	0.35 m^3 (12.36 ft^3)	1.4 m^3 (49.4 ft^3)		
Hazardous[c]			Used oils, solvents, resins, glues, containers	Material will be sorted and prepared on-site for shipment to off-site facilities
Liquid	1.08 L (0.29 gal)	4.3 L (1.16 gal)		
Solid	0.35 m^3 (12.36 ft^3)	1.4 m^3 (49.4 ft^3)		
Nonhazardous (sanitary)			Potable water, cleaning, paper, plastic, metal containers, garbage	Materials will be disposed of through laboratory (on-site) nonhazardous waste facility
Liquid	3.79×10^5 L (1.0×10^5 gal)	1.51×10^6 L (4×10^5 gal)		
Solid	50 m^3 (1765 ft^3)	130 m^3 (4591 ft^3)		
Nonhazardous (other) specific by waste			Chemical reagents, oils, cleaners, scrap metal, wood, plastic	Materials will be disposed through laboratory (on-site) nonhazardous waste facility. Scrap may be disposed of through the laboratory to off-site vendors
Liquid	4 L (1.06 gal)	16 L (4.23 gal)		
Solid	0.75 m^3 (26.48 ft^3)	3 m^3 (106 ft^3)		

Note: Estimates are based on historical experience from other programs and current operations. The actual waste stream will be strongly dependent on the type and amount of work performed. The actual waste handling will depend on the laboratory facilities in operation at the time and the current disposal regulations. The final volumes of waste will be smaller depending on the treatment option (drying, compacting, burning).

[a]Liquid LLW is assumed to be 100% of the TRU.

[b]Liquid mixed LLW is assumed to be 1% of LLW.

[c]Hazardous waste is assumed to be 1% of LLW.

Table 31. Radiation doses to involved workers during the LA PIE [whole body committed effective dose equivalent (CEDE)]

Average annual dose to all involved workers at the facility, mrem	177
Maximum dose to an involved worker at the facility, mrem	347
Total number of involved workers	10

Note: Table numbers are averages over 1994, 1995, and 1996 for Building 3525 at ORNL. Values are from the radiation protection representative. It is assumed that the MOX PIE will encounter similar exposures.

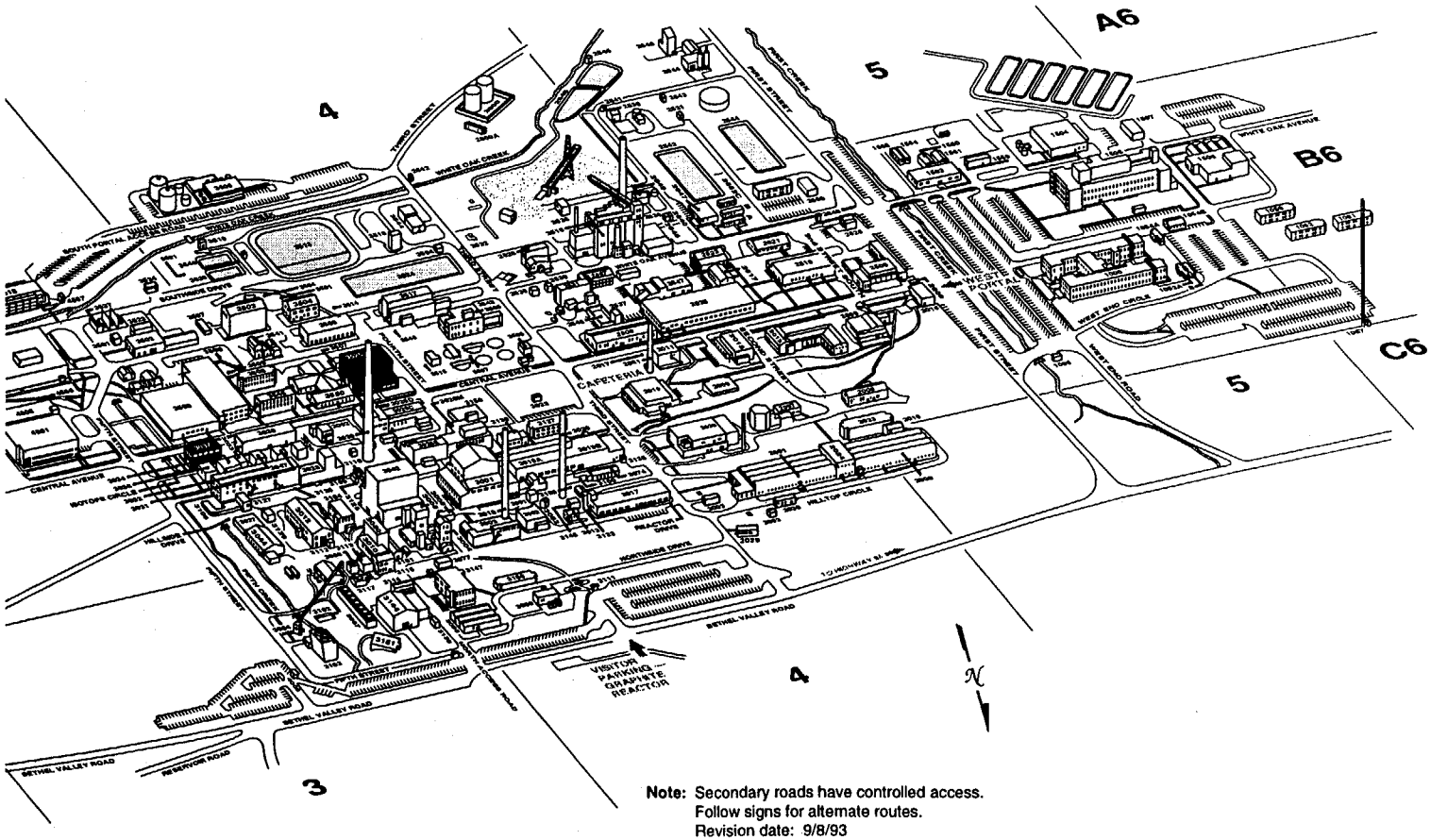
Table 32. PIE estimates for EIS

For planning purposes assume 17 by 17 fuel bundle array		289 rods total
Bundle length		13.50 ft
Pellet size		0.37-in. diam, 0.60-in. length, and 0.06-in.^{3} volume
Approximate density $UO_2 + PuO_2$		11.00 g/cm^3
Mass of pellet		11.43 g
Mass of pellet HM		10.08 g
Pellets per rod		270.00
Pellet mass per rod		3087 g
HM per rod		2721 g
Assume detailed PIE will involve ten rods per bundle and ten bundles		100 rods to be cut up
Estimated samples per rod		10
Total samples		1000
Assume one-third metal mounts		333
Assume one-third clad specimens		333
Assume one-third radiochemical specimens		333
Liquid waste per metal mount	0.5 L	167 L total for metal mounts
Liquid waste per clad specimen	0.1 L	33 L total for clad specimen
Liquid waste per radiochemical specimens	1 L	33 L total for radiochemical
Total specimen liquid waste (TRU)		533 L
Solid waste per metal mount and all mounts	200 cm^3	0.07 m^3 total
Solid waste per clad specimen and all clad specimens	200 cm^3	0.07 m^3 total
Solid waste per radiochemical specimen and all specimens	500 cm^3	0.17 m^3 total
Total specimen solid waste (TRU)		0.30 m^3
Assume two B-25 boxes of equipment		6 m^3
One-half equipment LLW		3 m^3
One-half equipment TRU		3 m^3
Assume one B-25 box per month/48 months		144 m^3
0.9 LLW [personal protective equipment (PPE), wipes, scrap, etc.]		130 m^3
0.1 TRU		14 m^3
Total liquid TRU waste		533 L
Total solid TRU waste		18 m^3

Table 32. (continued)

Total mixed liquid TRU waste	5 L (estimated as 1% of TRU)
Total mixed solid TRU waste	0.18 m^3 (estimated as 1% of TRU)
Total liquid LLW	533 L (estimated same as TRU)
Total solid LLW	133 m^3
Total mixed liquid LLW	5 L (estimated as 1% of LLW)
Total mixed solid LLW	1 m^3 (estimated as 1% of LLW)
Other waste streams	
Liquid hazardous waste	5 L (estimated as 1% of LLW)
Solid hazardous waste	1 m^3 (estimated as 1% of LLW)
Nonhazardous liquid waste	533 L (estimated as 100% LLW)
Nonhazardous solid waste	133 m^3 (estimated as 100% of LLW)
Nonhazardous liquid other waste—chemicals	5 L (estimated as 1% of LLW)
Nonhazardous solid other waste—scrap metal, one B-25 box	3 m^3
Assume that bulk of the fuel rods and fuel bundle will be handled as spent nuclear fuel and sent to Idaho National Engineering and Environmental Laboratory	

ORNL-DWG 97-3219 EFG



Note: Secondary roads have controlled access.
Follow signs for alternate routes.
Revision date: 9/8/93

Fig. 12. ORNL site map.

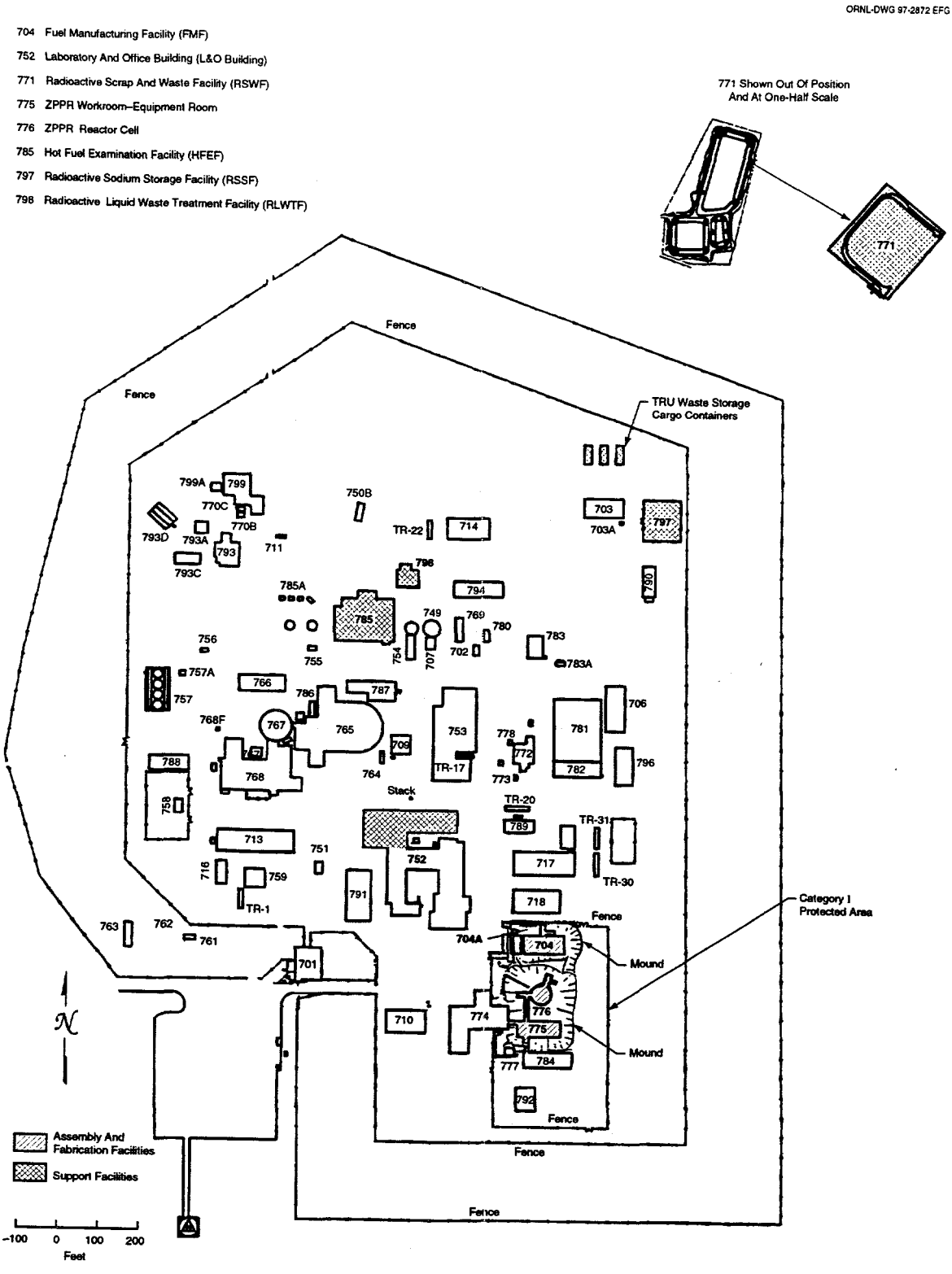


Fig. 13. ANL–W site map.

Technical Reports Series No. 322; and the *Guidebook on Destructive Examination of Water Reactor Fuel, IAEA Technical Reports Series No. 385.*

In addition to materials testing, the segmented fuel may be used as a test subject for accident testing. The segment may be heated to high temperatures in a variety of atmospheres in a complex test apparatus and its releases measured. Other specialized methods also exist; irradiated material may be removed from one experiment and transferred to another in the hot cell for further irradiation.

The fuel rods in the MOX program will employ nondestructive examination as well as many of the destructive techniques. Normal practice is rather broad, and the actual techniques and items of interest will be determined before PIE and will depend on the program's knowledge and confidence level at the time.

10.2 ANL–W

The Hot Fuel Examination Facility (HFEF) is a hot-cell complex for the preparation and examination of irradiated experiments and the characterization and testing of waste forms from conditioning of spent fuel and waste. The HFEF is located on the ANL-W site, which is located in the south-west corner of INEEL. The HFEF facility is located on the north end of a double-fenced compound on the ANL-W site.

HFEF consists of two adjacent shielded hot cells (the main and decon cells), a shielded metallographic loading box, an unshielded Hot Repair Area (HRA) and a Waste Characterization Area (WCA). The building is a three-story structure with a basement support area. The building dimensions are 112 ft wide by 154 ft long with a gross floor area of 56,570 ft^2 and a gross volume of 1,337,200 ft^3.

The metallographic loading box is located outside the main cell in the metallograph room. This room is located on the north side of the building on the main floor and is separated from the main cell by an operating corridor.

The HRA and WCA are located in the high bay area. The area provides access to the ceiling penetrations in the main and decon cells as well as the HRA roof hatch. The high bay is also used as a staging area for the WCA.

Since the shutdown and defueling of the EBR-II reactor, HFEF has been used for many diverse programs. The primary program, since October 1994, has been the support of the EBR-II defueling and decommissioning. HFEF was responsible for receiving all of the fuel and blanket material from EBR-II and preparing the material for storage in the Radioactive Scrap and Waste Facility (RSWF).

In addition to the handling of the EBR-II fuel, HFEF is the examination facility for both the metal and ceramic waste form experiments from FCF. Cladding hulls from the conditioning of fuel in FCF need to be processed for disposal in a repository. The processing of the cladding hulls and the characterization of the waste form is being tested in HFEF. In addition, equipment is being installed and processes tested for the disposal of the plutonium and fission product waste from the conditioning of EBR-II fuel. The testing and characterization of the ceramic waste forms will be performed in HFEF.

HFEF is presently starting facility modification to accept commercial-sized fuel assemblies from the Watts Bar reactor. These assemblies (specifically, tritium production burnable absorber rods) are the initial assemblies being irradiated as part of DOE's commercial LWR tritium production evaluation. All of the examination equipment in the cell and the cask handling systems are being modified to handle commercial-sized casks and fuel rods for examination. These modifications will be complete in mid-1999.

Some of the stainless steel reflector subassemblies used in EBR-II have experienced neutron exposure since the reactor was started in the early 1960s. The neutron damage to these steels is of interest to the commercial power industry, especially in Japan. Two programs are in place where the stainless steels are being prepared for testing of the neutron damage. These programs involve the cutting and preparation of samples for testing at other laboratories.

The north neutron radiography station has been modified to house a neutron generator for neutron assay of waste. Testing is presently being done on developing neutron assay techniques for the waste from the FCF.

In support of the National Spent Fuel Program, HFEF is presently engaged in the examination of degraded EBR-II fuels that have been stored in water pools at the ICPP. The fuel was shipped to ICPP in sealed containers. During the 15 to 20 years of storage in the water basin at ICPP, some of the containers

have leaked, causing the fuel to breach. The characterization and examination of the degraded fuel at the HFEF will determine the chemical condition of the fuel as well as the mechanism for breaching. This program will be ongoing during the next 2 years.

10.2.1 Main Cell

The HFEF main cell is 70 ft long by 30 ft wide by 25 ft high and has an argon gas atmosphere. The argon gas in the cell is maintained as pure as possible; however, a small amount of moisture is needed to help lubricate and cool the brushes on the electric motors used in cell. Because of this, the moisture and oxygen levels are maintained about 40 ppm. The maximum oxygen and moisture levels are kept below 100 ppm. The cell atmosphere is maintained at these levels using a purification system.

An 8-ft deep space that is located beneath removable flooring and covers the entire width of the cell is used for storage of fuel elements during their examination. Also located in this space are the bases of the examination stages, ducts and filters for the main cell cooling system, and pits for the storage of radioactive materials. A total of ten 1-ft diam by 10-ft long storage pipes are located in the center aisle of the cell for storage of Experimental Breeder Reactor-II (EBR-II) subassemblies. These pits are equipped with forced argon cooling for decay heat removal of their contents.

In addition to the subfloor space, two 3-ft diam pits extend 30 ft below the level of the removable floor at workstations 8M and 9M (south-east corner of the cell). These pits are used for storing and handling of long items such as long test loops. Each pit has a corresponding roof penetration so long items can be transferred into the cell and placed in a pit.

The main cell is serviced by two electro-mechanical manipulators (EMMs) rated for 750 lb and two 5-ton bridge cranes. The maximum lift for an EMM in the main cell is 11 ft 8 in. The maximum lift for a crane in the cell is 19 ft 11-5/8 in.

There are 15 workstations in the main cell. Each workstation is equipped with two master/slave (MS) manipulators. Most of the MS manipulators are Central Research Laboratory (CRL) Model J's rated for a 20-lb vertical lift. Five of the workstations are equipped with CRL System 50 manipulators rated for a 50-lb vertical lift.

10.2.2 Decon Cell

The air-filled decon cell is located adjacent to the west end of the main cell and is 30 ft wide by 20 ft long by 25 ft high. There is no subfloor space in the decon cell; however, three 15.5-in. diam by 10-ft deep pits are located at workstation 3D. Another similar pit is located at workstation 4D, and a 3-ft diam by 30-ft deep pit is located at workstation 5D.

The decon cell is equipped with an 8-ft wide by 7-ft deep by 11-ft high spray chamber for decontaminating equipment and nonfissile material using a manipulator-held wand. The wand can be used for spraying either water or steam. A chemical addition tank is connected to the water feed line for the addition of decontamination solutions to the water stream. Items being decontaminated are positioned on a 5-ton turntable inside the chamber so that they can be rotated. Both the roof and back side of the spray chamber can be opened remotely so items being decontaminated can be placed inside the chamber.

Material handling inside the decon cell is performed with one 750-lb EMM and one 5-ton crane. The maximum lifting height of the EMM is 11 ft 8 in. and that of the crane is 19 ft 11 in. In addition to the EMM and crane, the cell is equipped with six sets of MS manipulators. Most of the workstations are equipped with one CRL model E MS, rated for a 20-lb vertical lift, and one CRL model F MS, rated for a 100-lb vertical lift.

Two pneumatic transfer stations are inside the decon cell. One station originates at station 4D and runs to the Fuel Conditioning Facility (FCF). The other station originates inside the spray chamber and runs to the radiation safety office (HP office). The pneumatic transfer station that runs to FCF is used for sending small irradiated samples to FCF then on to the Analytical Laboratory (AL) for analysis.

10.2.3 Metallographic Loading Box

The metallographic loading cell is a shielded, gas-tight cell with inside dimensions of 8 ft wide by 6 ft deep by 5 ft high. The cell is provided to accommodate a Leitz metallograph and a scanning electron microscope (SEM) for performing detailed examination of metallurgical samples. The shielding walls (except the front wall) are constructed of 8-in.-thick lead brick. The front wall is 15-in. thick and is constructed of three 5-in.-thick steel plates. The front wall has a lead-glass window for viewing and two CRL Model L MS manipulators.

10.2.4 HRA

The HRA is a series of rooms located directly above the decon cell and west end of the main cell in the high bay area. The outside dimensions of the HRA are 45 ft by 70 ft. The primary purpose of the HRA is to perform contact maintenance on cell equipment. The HRA is divided into 12 areas:

1. Hot Repair Room (HRR)
2. Suspect Repair Room
3. Equipment Access Room (Cart Room)
4. Isolation Area Room
5. Survey Room
6. Health Physics (HP) Office
7. Unsealed Slave Repair Room
8. Bagout Room
9. Sealed Slave Arm Repair Glove Box Room
10. Stepout Area Room
11. Glovewall Room
12. Ancillary Area Room

Most of the rooms in the HRA are specific-purpose rooms used for the repair of MS manipulators and other facility-specific equipment. The HRR can be used for the transfer of equipment and materials between the decon cell and HRA. Both the HRR and Suspect Repair Room are serviced by a 5-ton bridge crane. The crane uses a removable rotating hook for remote positioning of the hook. With the rotating hook removed, the maximum lift inside the repair rooms is 13 ft 6 in. With the hook in place the maximum lift inside the HRR is 12 ft 1 in. The drum on the crane is provided with enough cable for a 50-ft lift so that it can be used for raising and lowering equipment into the decon cell.

A 10 ft^2 roof hatch is located in the ceiling of the HRR, directly above the decon cell roof hatch. The hatch is provided with a 114-in. diam bagging ring so it can be used for the transfer of equipment and material directly from the high bay area into the decon cell.

The equipment access room (cart room) is designed to be a lock in the transfer path between the high bay area and the HRR. The room is 8 ft^2 by 20 ft high and has a 6 ft 4 $in.^2$ hatch in the ceiling. The room is generally maintained clean so equipment and materials can be transferred from the high bay area to the room through the hatch. A 5-ton equipment cart runs between the cart room and the HRR for moving the equipment and materials between the two rooms.

10.2.5 WCA

The WCA is used for the characterization and sampling of contact-handled transuranic waste (CH TRU) for the WIPP performance assessment. The facility consists of the Preparation Room (PR), Transfer Room, Waste Characterization Chamber (WCC), Sludge Preparation glove box, Operations Room and the Equipment Room.

The PR is used as a staging area for waste going into and out of the WCC. Waste drums awaiting characterization in the WCC are stored in the PR, and waste that has been characterized and is awaiting shipment back to the Radioactive Waste Management Complex (RWMC) is also stored in the room. Personnel access to the PR is through a vestibule on the south-east corner of the room. Waste drums and

equipment are brought into the room using the high bay crane through a 10-ft high by 8-ft wide equipment door on the south wall. High bay crane hook access to the room is through a 2-ft wide by 17-ft-long rollup door on the vertical wall and ceiling above the equipment door. Waste drums and equipment are handled inside the PR by a cantilever-style jib crane rated for a 6000 lb SWL. The crane has a lift height of 12 ft 8 in.

The Transfer Room (TR) is where the waste drums are mated with the WCC. Access to the room is through double doors from the PR. The drums are moved into and out of the TR using a drum cart rated at 2,000 lb SWL. In addition to moving the drums into and out of the room, the cart is used to raise and lower the drums to the drum ports on the bottom of the WCC. Once the drums are bagged to the WCC, they are held in position in the drum ports by turnbuckles which fasten between the bottom of the WCC and an adapter plate under the drums.

The WCC is a 16-ft long by 8-ft high by 8-ft deep glove box used for characterization of CH TRU wastes. The WCC is equipped with shielded viewing windows for personnel protection from low-level gamma and beta radiation. Each window is a three-piece assembly consisting of an inner safety glass, a lexan plate, and leaded glass on the exterior. There are two 200-lb dual Titan 7F manipulators and a 1,500-lb articulated jib crane for handling the waste and equipment inside the glove box. A core boring machine is mounted to the top of the glove box over the west drum port and is used for taking samples from sludge drums. There are 28 glove ports on the WCC. These glove ports are located at various heights for waste handling and equipment repair. A transfer port is located on the east end of the WCC for transferring sludge samples to the Sample Preparation glove box.

The Equipment Room (ER) is located above the WCC and houses the filters, piping, and blowers for the WCC ventilation system. In addition to the ventilation equipment, the ER has a repair glove box for repair of the equipment inside the WCC. The glove box is connected to the west end of the WCC through a transfer tunnel. Equipment is raised and lowered from the repair glove box by a hoist inside the glove box.

The Operations Room (OR) is the area around the WCC and Sample Preparation and Transfer glove boxes. The room provides a mezzanine on the west end of the WCC for the Waste Data Acquisition System (WDAS). The WDAS is used for video taping and audio dubbing of the waste handling operations. A computer controlled switcher is used for switching video sources and recorders. The computer control system for the gas sampling system is mounted on the south end of the WDAS.

In addition to the WDAS, the OR provides monitoring and alarm panels for monitoring the status of the WCA. The panel provides flow and pressure information on the WCC, radiation alarms, breathing air alarms, and fire alarms for the inside of the WCC.

The sludge preparation (SP) glove box is used for preparing sludge samples for shipment to the Idaho Chemical Processing Plant (ICPP) to be analyzed for halogenated VOCs, nonhalogenated VOCs, RCRA heavy metals, and radioassay. After the sludge has been cored, the core section is transferred to the SP glove box where the samples are taken at various locations along the core section. As each sample is taken, it is weighed, placed in a labeled vial, and shipped to ICPP in a Type A container. Some experimentation is being done on real time analysis of the samples using X-ray florescence. The testing of the equipment has not been completed.

10.3 ORNL

The Irradiated Fuels Examination Laboratory (IFEL), Building 3525, has a long history of fuel research and examination. It is part of ORNL and is located in Bethel Valley and Melton Valley, approximately 8 miles southwest of the city of Oak Ridge, Tennessee. For three decades this facility has handled a wide variety of fuels including aluminum clad research reactor fuel, both stainless- and zircaloy-clad LWR fuel, coated-particle gas cooled reactor fuel, and numerous one of a kind fuel test specimens. In addition, the facility has also done iridium isotope processing and irradiated capsule disassembly.

The IFEL contains a large horseshoe-shaped array of hot cells which are divided into three work areas (Fig. 14). The hot cells are constructed of 3-ft-thick concrete walls with oil-filled, lead-glass viewing windows. The inside of surfaces of the cell bank are lined with stainless steel to provide containment of particulate matter and to facilitate decontamination. Special penetrations are provided for the sealed entry of services such as instrument lines, lights, and electrical power. A pair of manipulators are located at each

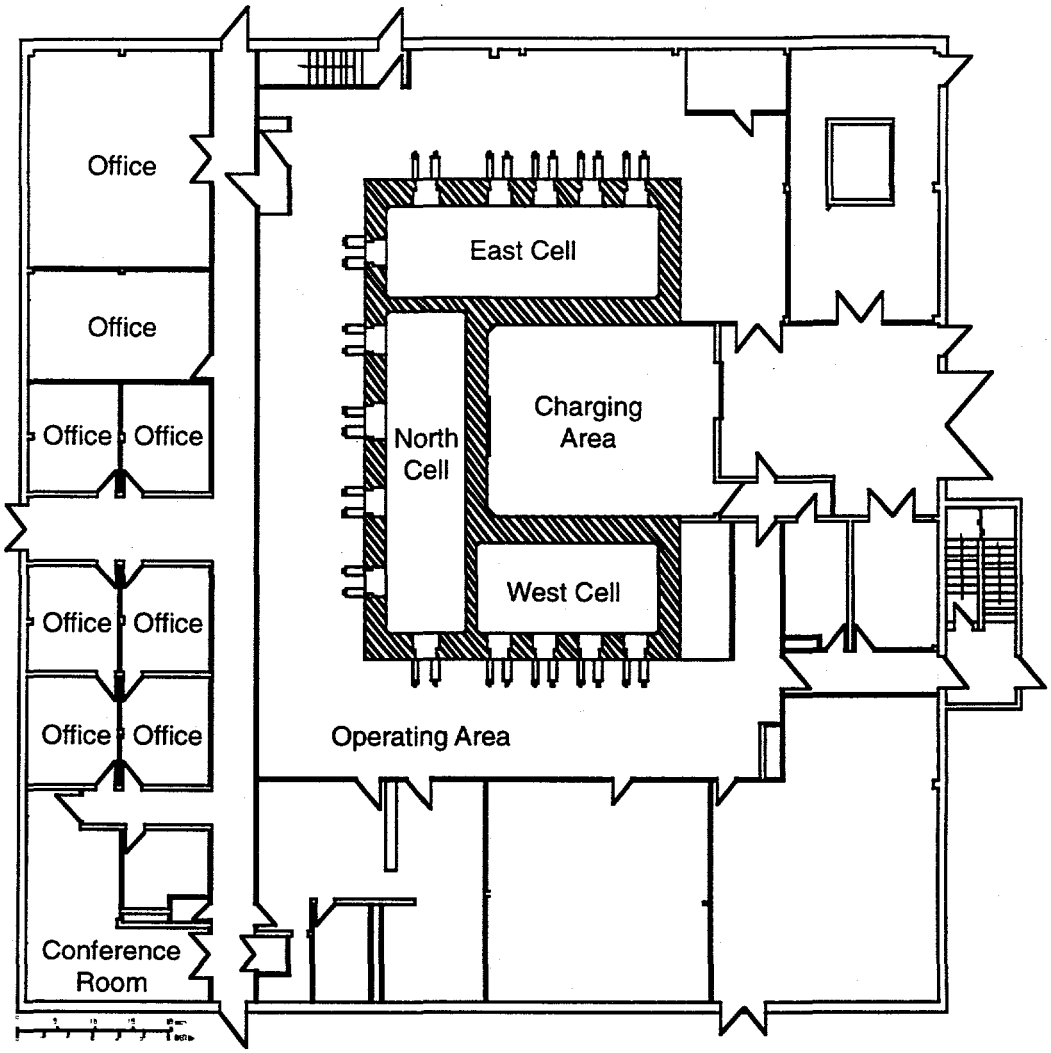


Fig. 14. Building 3525 layout.

of 15 window stations for remote cell operations, and periscopes allow for magnified views of in-cell objects. Heavy objects within each cell bank can be moved by electromechanical manipulators or a 3-ton crane. Fuel materials enter and leave the cells through three shielded transfer stations provided at the rear face of the North cell. Two small diameter (6.5 and 14.5 in.) horizontal transfer stations are used for small objects (less than 8 ft in length). Items up to $4 \times 4 \times 6$ ft in size can be transferred through the shielded air-lock door system.

The remainder of the laboratory outside the hot cell complex is subdivided into: (1) the charging area; (2) the equipment maintenance air lock areas; (3) the operating area; (4) the truck unloading area, the change room, and a work room; and (5) the rooms housing supporting mechanical equipment. Located on the east side of the truck unloading area is a small laboratory which houses the Core Conduction Cooldown Test Facility (CCCTF). The CCCTF is used to test radioactive samples under controlled thermal conditions while monitoring the samples to determine the release rate of radioactive materials.

A decontamination cell and storage cell, located on the second floor of the building, are connected via hatches to the cells below. A maintenance area incorporating glove box facilities for servicing equipment items adjoins the decontamination cell. Sliding doors separate the decontamination cell, storage cell, and glove maintenance room; a remote crane system provides for retrieval of equipment into and transfer of

items between these second-floor facilities. Equipment may be transferred between cells through the second-floor pathway. An upper level of the second floor houses ventilation system ducts, control valves, high efficiency particulate air filters, heat exchangers, and air inlets for the equipment storage area, the decontamination area, and the glove maintenance area.

Gases and particulates exhausted from the cell complex are completely contained and shielded until subjected to sufficient filtration to ensure safe stack disposal. The cell air is maintained at negative pressure with respect to the operating areas to ensure confinement. Liquid effluent from the hot cells is handled in a batch mode for disposal to the ORNL low-level liquid waste system.

A variety of shears, machine tools, and cutoff saws are available within the cell for the gross handling and preparation of fuel specimens. The facility has experience in the handling and cutting of a wide variety of capsule and clad materials such as Inconel, stainless steel, zircaloy, aluminum matrix, and graphite-based materials. A gamma scanner is available for the nondestructive examination of moderate-length fuel rods and individual specimens. Metrology equipment such as mass scales and dimensional tools are routinely used and available.

Metallographic equipment including small cutoff saws, polishers, and a shielded metallograph are available for the preparation, handling, and examination of both fuel specimens and clad material. The facility has prepared samples of oxide fuels, carbide fuels, and metal matrix fuels.

Building 3525 also has other facilities outside the main bank of cells: a scanning electron microscope that can handle radioactive specimens, additional gamma analysis and dosimetry equipment for both centimeter-sized and submillimeter-sized samples, and a small stand-alone hot cell with specialized equipment for the handling and analysis of coated-particle fuels.

Radiochemical specimens can be prepared within the facility and delivered to other ORNL laboratories for detailed analysis. ORNL also has extensive computational abilities that can be used to process the hot cell data for comparison with fuel performance models.

PIE capabilities of the IFEL have provided general support to fuels program, fuel characterization, and analysis of candidate irradiated fuel. Typically, the fuel is received at the IFEL, dimensionally inspected, visually examined for defects, and gamma scanned for internal fuel gaps or cracks along with gross fission product migration. The fuel can then be removed from its casing or clad and fuel and clad specimens prepared for metallographic examination, gamma counting, and radiochemical analysis. Actinide and fission product inventories can be determined along with burnup and radial isotope distributions within the fuel. The mechanical properties of the specimens can also be investigated to determine the state of the fuel and/or clad materials. All work is typically done with proper procedures and documentation after concurrence is obtained from the program participants.

Recent work includes extensive support for the Gas Turbine Modular High-Temperature Gas-Cooled Reactor (GT-MHR) program, the New Production Reactor (NPR), a cooperative gas-cooled reactor agreement with Japan, and handling of legacy fuel under the National Spent Fuel program. Personnel are available with experience in a wide variety of fuel PIE programs and analysis techniques along with the detailed reporting and quality control requirements for nuclear programs. The Metals and Ceramics (M&C) division contains a wealth of experience in fuel fabrication, metal and ceramic material behavior, irradiated material behavior, and material testing. Ongoing programs at ORNL maintain experience in hot cell techniques and analysis. In addition, academic and industrial consultants are available to meet special program needs and to conduct reviews.

REFERENCES

1. U.S. Department of Energy, *Storage and Disposition of Weapons-Usable Fissile Materials Final Programmatic Environmental Impact Statement*, Vol. 1, Chap. 3, DOE/EIS-0229, December 1996.

2. Los Alamos National Laboratory, *Response to the Surplus Plutonium Disposition Environmental Impact Statement Data Call for a Mixed Oxide Fuel Fabrication Facility Located at Pantex Plant*, LA-UR-97-2067, Rev. 3, June 22, 1998.

3. V. S. White, *Initial Data Report and Response to the Surplus Plutonium Disposition Environmental Impact Statement Data Call for the UO_2 Supply*, ORNL/TM-13466, Lockheed Martin Energy Research Corporation, Oak Ridge National Laboratory, November 1997.

4. *Shearon Harris Nuclear Power Plant Technical Specifications*, Sect. 3.8.

5. U.S. Department of Energy, *Airborne Release Fractions/Rates and Respirable Fractions for Nonreactor Nuclear Facilities*, DOE-HDBK-3010-94, Vols. I and II, December 1994.

6. Browne and Firestone, *Table of Radioactive Isotopes*, V. S. Shirley, ed., John Wiley and Sons, 1986.

7. U.S. Department of Energy, *Criteria for Preparing and Packaging Plutonium Metals and Oxides for Long-Term Storage*, DOE-STD-3013-96, September 1996.

8. DOE Order 420.1, Sect. 4.3, Nuclear Criticality Safety.

9. 40 CFR 302.4, Table 302.4, *List of Hazardous Substances and Reportable Quantities.*

10. W. R. Stratton, *A Review of Criticality Accidents*, DOE/NCT-04, March 1989.

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Appendix A—LA FUEL BUNDLE FABRICATION

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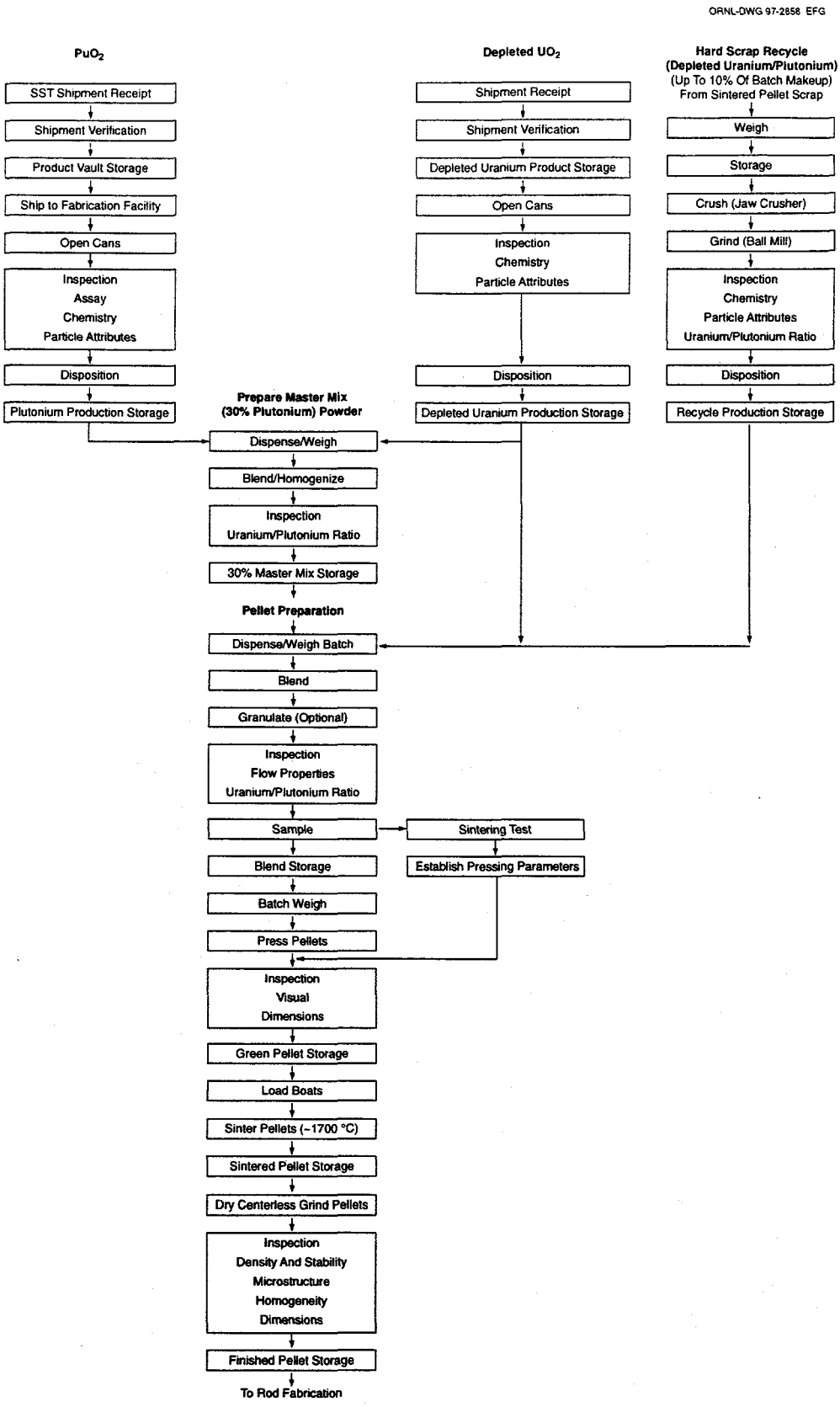

Fig. A.1. LA MOX fuel pellet flow sheet outline.

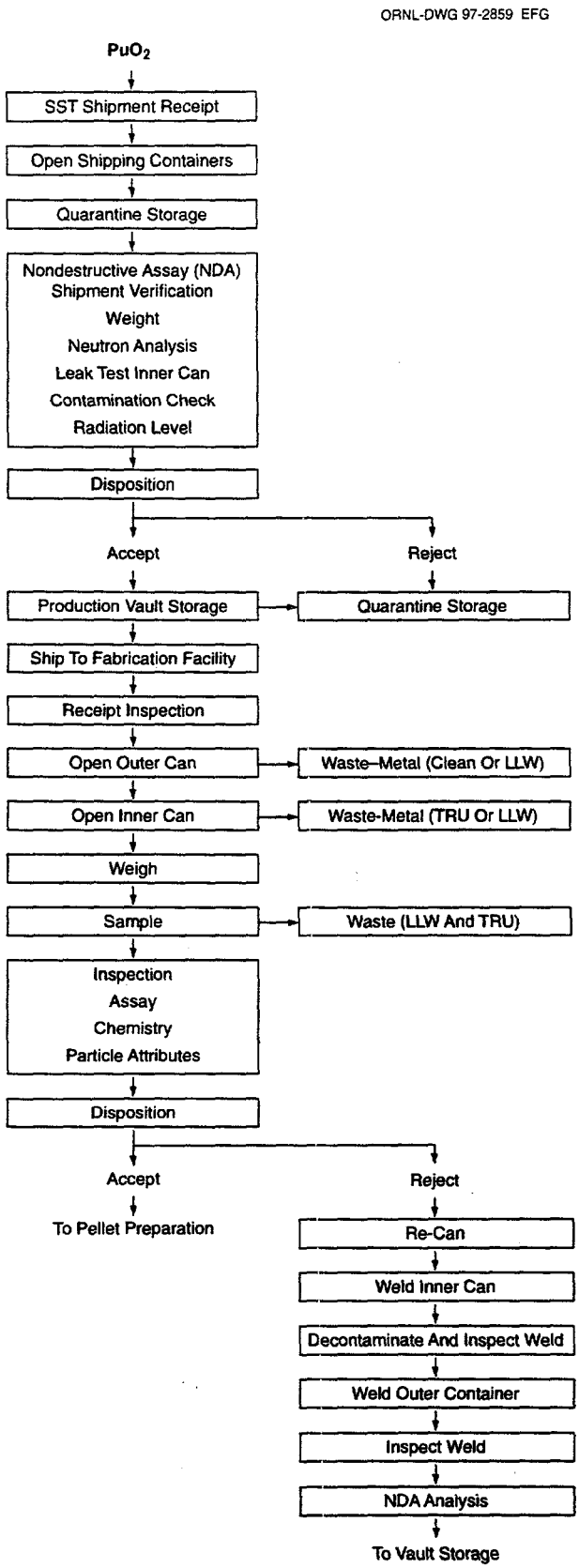

Fig. A.2. LA MOX fuel PuO_2 powder receipt and storage.

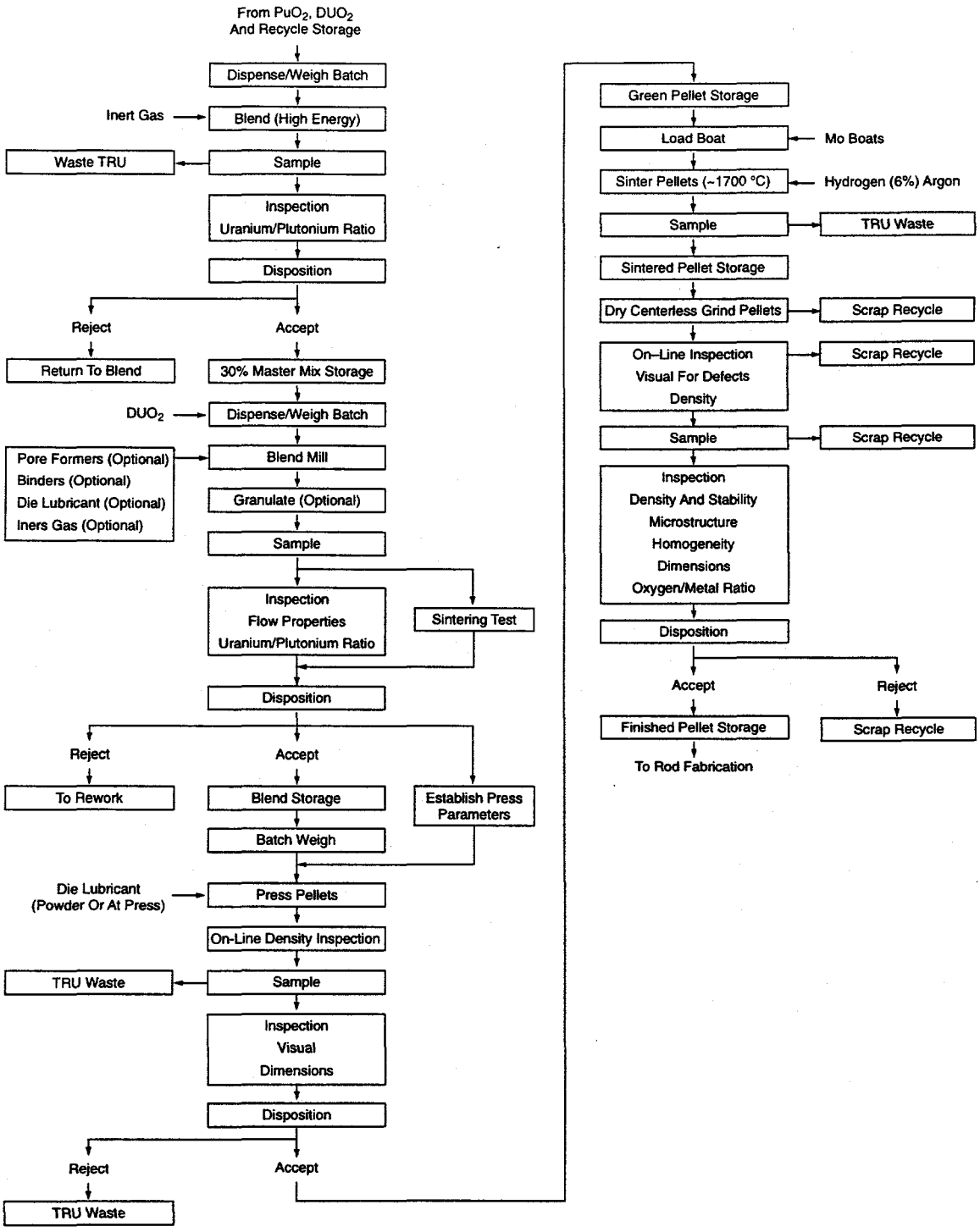

Fig. A.3. Detailed flow sheet of LA pellet fabrication.

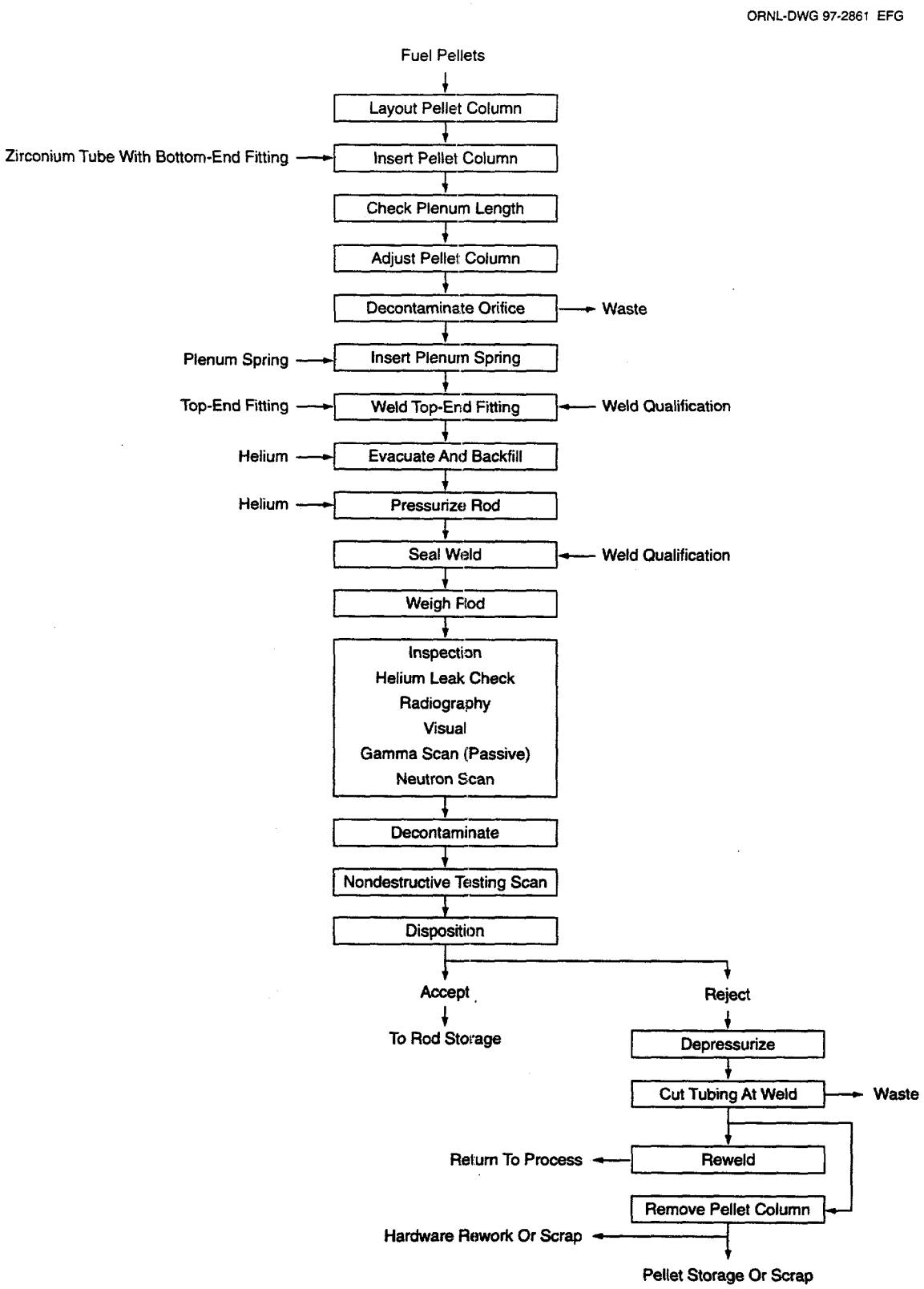

Fig. A.4. Detailed flow sheet of LA rod fabrication.

ORNL-DWG 97-2862 EFG

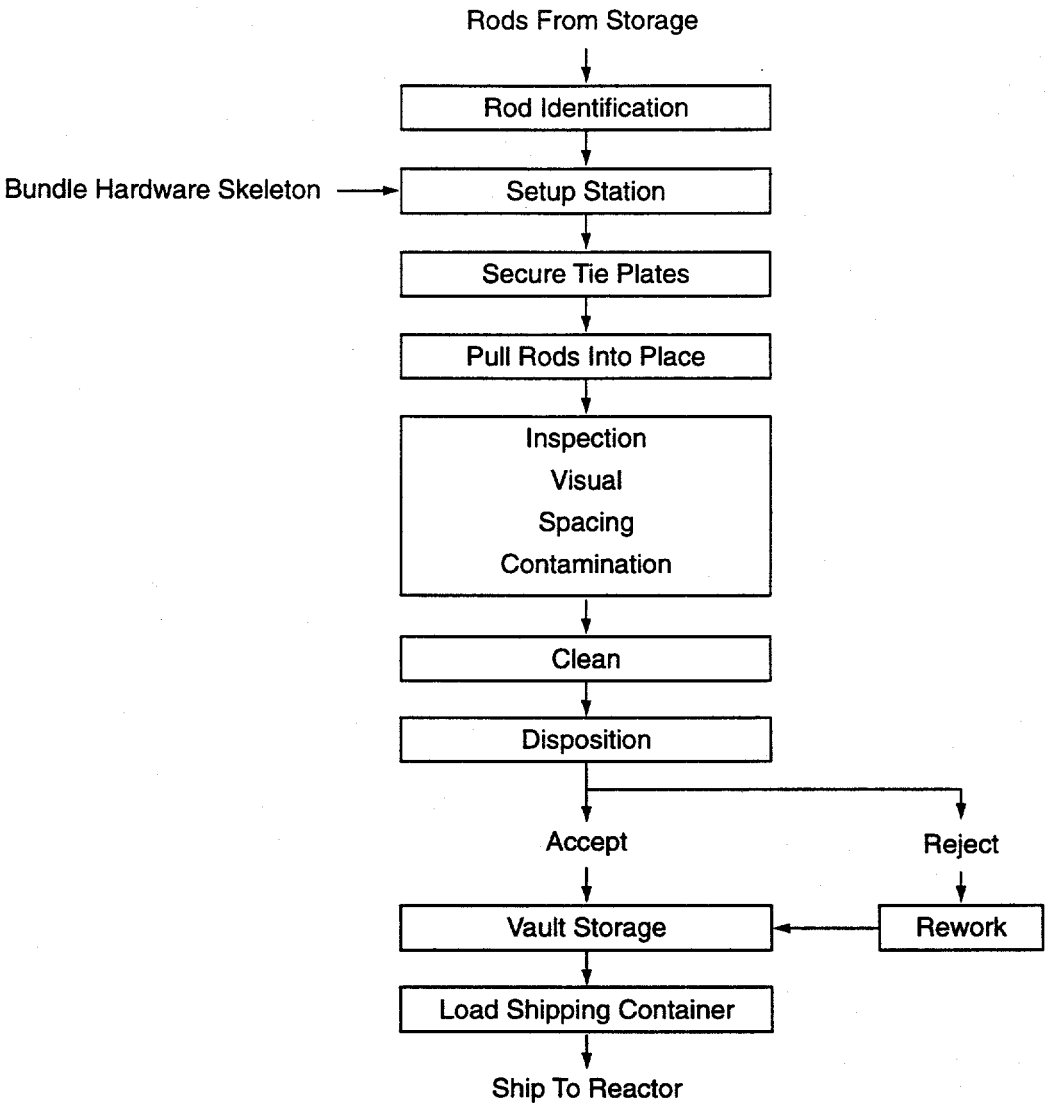

Fig. A.5. Detailed flow sheet of LA bundle assembly (LWR).

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Appendix B—LA EIS DATA REPORT ASSUMPTIONS

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Table B.1. Assumptions used for the LA EIS data reports

1. Material and process requirements are based on producing PWR fuel.
2. PuO_2 powder will meet the ASTM C 757-90 specification as received.
3. Depleted UO_2 powder will meet the ASTM specification as received.
4. Depleted UO_2 (no PuO_2) will be used to perform all system shakedown tests before introducing plutonium.
5. Table 3 is in terms of HM. The factor for converting PuO_2 and depleted UO_2 to HM is 88%.
6. All waste plutonium will be canned and sent to the Immobilization Program for final disposition.
7. All plutonium scrap will be recycled using a dry process.
8. All liquid wastes generated are ancillary to the base process (i.e., laundry, mop water, etc.)
9. Sintering furnaces will stay at temperature during the entire 3-year mission and 1-year startup.
10. Sintering furnaces will be purged with a mixture of argon and 6% hydrogen at a rate of 10 L/min.
11. Powder glove boxes will be purged with nitrogen to reduce the potential for oxidizing UO_2.
12. All calculated numbers have a precision of no more than two significant figures.
13. The facility will be built on an existing DOE site with a minimum of 4500 ft^2 available space (3000 ft^2 for MOX rod processing, 1000 ft^2 for bundling activities, and 500 ft^2 for fuel bundle storage).
14. The site will have an existing infrastructure in place to accept the LA mission.
15. Personnel will be required to support a process capacity of ~2 MT HM per year.
16. Personnel involved in SNM operations must work in pairs and follow specific safety precautions detailed by the site.
17. Personnel must attend required site training. A staffing requirement for training purposes has been included in this estimate.
18. Space will be allocated for safe secure transports (SSTs) carrying plutonium and transportation for uranium so that loading can be accomplished on a follow-up operating shift if the transport arrives near or following the close of standard business.
19. As with the MOX fuel fabrication facility estimate, the staffing requirements assume that ~20% of the employee's time will be taken through training, vacation, personal leave, or illness. Even though employees cannot necessarily transition from one position to another, a contingency was added to account for nonproductive time.
20. Homogenization of the PuO_2 powder will be done at the LA fuel fabrication facility, as will gallium removal operations.

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HANFORD RESPONSE TO THE SUPPLEMENTAL LEAD TEST ASSEMBLY EIS DATA CALL

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HANFORD RESPONSE TO THE SUPPLEMENTAL LEAD TEST ASSEMBLY EIS DATA CALL

1. GENERAL SITE DATA NEEDS

The lead-test assembly (LTA) proposal for the Fuels and Materials Examination Facility (FMEF) located at the Hanford site will utilize facilities covered under existing environmental annual reports and environmental impact statements (EISs).

2. LOCATION-SPECIFIC DATA NEEDS

2.1 GENERAL FACILITIES INFORMATION NEEDS

The FMEF was originally two separate facilities: (1) the FMEF used for examination of irradiated fuels and materials removed from the Fast-Flux Test Facility (FFTF) and (2) the Clinch River Breeder Reactor (CRBR) and the High-Performance Fuel Laboratory (HPFL) used for preparation of fuels for the FFTF and the CRBR. These two facilities were merged into the FMEF. After construction of the FMEF, the Secure Automated Fabrication (SAF) facility was added to the top floor of FMEF. After the FMEF/SAF missions were canceled, the Radioisotope Power Systems Facility (RPSF) was located in the FMEF.

The environmental documentation for each of these projects to be used for this program, including background information on facilities, is described below.

2.1.1 PFP

The Plutonium Finishing Plant (PFP), 200 Area, is detailed in the *Final Environmental Impact Statement–Plutonium Finishing Plant Stabilization*, May 1996. It is available as document DOE/EIS-0244F and can be found at http://raleigh.dis.anl.gov:81.

2.1.2 HPFL

An EIS was prepared for the HPFL and issued as ERDA-1550 in September 1977. The HPFL was described as a fuel fabrication facility with some supporting analytical chemistry capability. The analytical chemistry utilized methods other than wet chemistry. The HPFL source terms and discharge streams are shown on the attached tabulations.

2.1.3 FMEF

An environmental impact assessment was prepared for the separate FMEF. The Energy Research and Development Administration's (ERDA's) Environment and Safety Division concluded by a memorandum, dated February 17, 1977, that the project would have no significant impact on the environment and an EIS would not be required. The FMEF source terms and discharge streams are shown on the attached tabulations.

2.1.4 Combined Facility FMEF

An environmental assessment (EA) was prepared for the combined HPFL and FMEF. A Finding of No Significant Impact (FONSI) was issued on July 17, 1980. The source terms and discharge streams are shown on the attached tabulations. Note that the FONSI referenced is ERDA-1538, *Final Environmental Impact Statement, Waste Management Operations.*

2.1.5 SAF Facility

A supplement to the combined facility FMEF EA was prepared for the addition of the SAF line. The Department of Energy's (DOE's) National Environmental Policy Act of 1969 (NEPA) Affairs Division concluded by a memorandum, dated October 30, 1981, that no additional review under NEPA was required. The source terms and discharge streams of the combined facility including SAF are shown on the attached tabulations.

2.1.6 RPSF

An Action Description Memorandum was prepared for adding the RPSF to the FMEF. DOE's Environmental, Safety and Health Division determined by a memorandum, dated August 22, 1988, that neither an EA nor an EIS was required.

2 1.7 Building 325

- *Characterization of Stored Defense Production Spent Nuclear Fuel, and Associated Materials at Hanford Site, Richland, Washington*, proposed to characterize stored defense production spent nuclear fuel and associated materials on the Hanford site. DOE identified a need for characterization activities that would establish a basis for determining the types of interim storage modes that would be compatible with the spent nuclear fuel material (SNFM) in its present condition, and the kind and extent of processing, if any, the SNFM would require to make it compatible with alternative storage modes. The EA mentions Building 325 as a possible site of analyses.

- *Management of Hanford Site Non-Defense Production Spent Nuclear Fuel, Hanford Site, Richland, Washington*, addressed the need to provide safe, cost-effective management of Hanford nondefense production reactor spent nuclear fuel. The inventory is currently stored in various facilities across the site, including Building 325.

- *Lead Test Assembly Irradiation and Analysis, Watts Bar Nuclear Plant, Tennessee, and Hanford Site, Richland, Washington*, addressed the need to confirm the viability of using a commercial light-water reactor (LWR) as a potential source for maintaining the nation's supply of tritium. The action selected in the FONSI is a limited-scale confirmatory test that would provide DOE with information needed to assess that option. The LTA postirradiation evaluation and analysis addressed in this EA will be conducted in Building 325.

- *Disposal of Hanford Defense High-Level, Transuranic and Tank Waste, Hanford Site, Richland, Washington*, examined the potential impacts calculated for the final disposal of existing high-level transuranic (TRU) and tank waste stored at the Hanford site since 1943 and future waste. This EIS was both a programmatic EIS, which was intended to support broad decisions about the disposal strategies for the Hanford site waste, and an implementation EIS intended to provide project-specific environmental input for decisions on certain disposal activities and facilities. In the Record of Decision (ROD), DOE decided to conduct additional development and evaluation activities before making final disposal decisions for certain waste classes (single-shell tank wastes, TRU-contaminated waste sites, and pre-1970 buried suspect TRU-contaminated solid waste within the 200 Area plateau). This development and evaluation effort was to focus both on methods to retrieve and process these wastes for disposal as well as to stabilize and isolate the wastes near the surface. Since 1987, some of this research has been conducted in Building 325.

As with safety analysis documentation, numerous environmental documents have been prepared to address NEPA compliance by missions proposed for FMEF. Although not all are current or approved, the following provide an indication of the ongoing effort to address NEPA compliance for proposed FMEF projects.

- *Lead Test Assembly Irradiation and Analysis, Watts Bar Nuclear Plant, Tennessee, and Hanford Site, Richland, Washington*, DOE/EA-1210
  FONSI issued July 1997
- *Management of Hanford Site Non-Defense Production Spent Nuclear Fuel*, DOE/EA-1185
  Hanford Site, Richland, Washington
  FONSI issued March 1997
- *Final Environmental Impact Statement*, DOE/EIS-0244F
  Plutonium Finishing Plant Stabilization
  Issued May 1996
  http://raleigh.dis.anl.gov:81
- *Characterization of Stored Defense Production Spent Nuclear Fuel and Associated Materials*, DOE/EA-1030
  Hanford Site, Richland, Washington
  FONSI issued March 1995
- *FMEF Fuel Assembly Area Environmental Assessment*, DOE/EA-0411 (Revised)
  Mixed-oxide and enriched uranium-oxide fuel fabrication with target fabrication capability (revised to incorporate DOE comments)
  Resubmitted January 1991
  Correspondence number 9003572B R2
- *FMEF Fuel Assembly Area Environmental Assessment*, DOE/EA-0411 (Revised)
  Mixed-oxide, uranium-oxide, and metal fuel fabrication and target assembly for isotope production (removed references to ^{238}Pu mission)
  Submitted October 1990
  Correspondence number 9003572B R1
- *FMEF Fuel Assembly Area Environmental Assessment*
  Storage of unirradiated fueled components in the fuel assembly area (FAA) storage pit
  Submitted August 1990
  Correspondence number 9055760
- *Space Power Systems Project Environmental Assessment* (Revised)
  Irradiated neptunium target assembly reprocessing
  Submitted February 1990
  Correspondence number 9050195
- *Space Power Systems Project (SPSP) Environmental Assessment*
  Irradiated neptunium target assembly reprocessing
  Submitted January 1990
  Correspondence number 9050611
- *FMEF Fuel Assembly Area Environmental Assessment*, DOE/EA-0411
  Mixed-oxide, uranium-oxide, and metal fuel fabrication plus target fabrication (including neptunium)
  Submitted January 1990
  Correspondence number 9050576
- *FMEF Fuel Assembly Area Environmental Assessment*
  Mixed-oxide, uranium-oxide, and metal fuel fabrication plus target fabrication
  Submitted August 1989
  Correspondence number 8954551
- *FMEF Fuel Assembly Area Environmental Analysis*
  Mixed-oxide, enriched uranium-oxide, and driver fuel fabrication also included target and space reactor test pin fabrication
  Submitted April 1989
  Correspondence number 8951830

- *FMEF Fueled Clad Fabrication System (FCFS) Environmental Analysis*
  ^{238}Pu encapsulation for space vehicle heat source power supplies
  Submitted April 1989
  Correspondence number 8951830
- *FMEF Fuel Assembly Area (FAA)*
  Mixed-oxide, enriched uranium-oxide, and uranium metal fuel fabrication plus target fabrication
  Submitted January 1989
  Action Description Memorandum 8857712
- *Space Isotope Program (SIP)*
  Target assembly fabrication and irradiated assembly reprocessing
  Submitted November 1988
  Action Description Memorandum 8856893
- *Radioisotope Power System Fabrication (RPSF)*
  Approval Memorandum (EA or EIS not required) August 1988
  Action Description Memorandum 8852776
- *Disposal of Hanford Defense High-Level, Transuranic and Tank Waste,* DOE/EA-0113
  Hanford Site, Richland, Washington
  ROD issued December 1987
- *Breeder Reprocessing Engineering Test (BRET) Environmental Assessment*, DOE/EA-0258
  Driver fuel assembly reprocessing
  Issued October 1984
- *FMEF Secure Automated Fabrication (SAF) Environmental Assessment Supplement* (Supplement to DOE/EA-0116)
  Memorandum, No Additional Review, October 1981
- *Environmental Assessment for Combined Facility*, DOE/EA-0116
  HPFL and FMEF document addressing a combining of the two missions
  FONSI prepared July 1980
- *High Performance Fuel Laboratory (HPFL) Final Environmental Impact Statement*, ERDA-1550
  Issued September 1977
- *Fuels and Materials Examination Facility (FMEF) Environmental Impact Assessment*
  Postirradiation examination mission
  Submitted December 1976
  Memorandum, No Significant Impact, February 1977 ERDA 7700662

2.2 SPECIFIC FACILITIES INFORMATION NEEDS

Current (1997) employment levels for proposed facilities and buildings follow:

- Building 325—612
- PFP—618

FMEF—40Facility and building worker radiological exposure data for the most recent 3 years for all radiation workers and for all workers, provided in terms of annual average worker dose (mrem) and annual total worker dose (person-rem), are based on 1996 data as follows:

	FMEF	PFP	Building 325
Annual average worker dose (mrem)	0	50	18
Annual total worker dose (person-rem)	0	27.131	11.224

2.2.1 Land Use

Coordinates and elevations for the facilities that will be used at the Hanford site are found in Table 1.

Table 1. Land use information for proposed facility

Location	FAA	PFP	Building 325
Latitude	46°26'05.9" N	46°33'01.9" N	46°22'06.8" N
Longitude	119°21'52.4" N	119°37'59.3" N	119°16'42.0" N
Elevation above National Geodetic Vertical Datum (NGVD), m (ft)	165.6 (543)	205.5 (674)	122.4 (402)

2.2.2 Air Quality

Descriptions of the radionuclide discharges from PFP and Building 325 are given in Attachment 1, *Radionuclide Air Emissions Report for the Hanford Site, Calendar Year 1996*. There are no radionuclide emissions from the FMEF.

For Building 325, estimates of the emissions criteria and regulated toxic air pollutants are given in Table 2. Annual estimated emissions are provided in Table 3.

- A map showing the ambient air quality sampling station nearest to the proposed facility location is provided on p. 96 in PNNL-11139.
- Most recent annual wind rose data from the nearest data station is provided in PNNL-11107.
- Most recent available hourly meteorological data and joint frequency distribution data from the nearest sampling point were provided by e-mail, Sandberg to Gandee, in July 1997.

Table 2. Estimated emissions of criteria and regulated toxic air pollutants for Building 325

Chemical	CAS No.	Release (g/h)
Fluorides		6.2×10^{4}
Nitrogen oxides		8.6×10^{3}
Total reduced sulfur		1.1×10^{3}
Volatile organic compounds		1.5×10^{4}
Total suspended particulate		7.0×10^{-8}
1,1,1-trichloroethane	71-55-6	5.0×10^{1}
1,1,2-trichloro-1,2,2-trifluorethane	76-13-1	2.8×10^{1}
1,2,4-trichlorobenzene	120-82-1	4.0×10^{-1}
1,2-dichlorobenzene	95-50-1	1.6×10^{-2}
2,2,4-trimethylpentane, hydrocarbon kit 22	540-84-1	1.5×10^{1}
2,4,5-trichlorophenol	95-95-4	2.5×10^{-5}

Table 2. (continued)

Chemical	CAS No.	Release (g/h)
2,4,6-trichlorophenol	88-06-2	1.7×10^{-4}
2,4-dinitrophenol	51-28-5	1.0×10^{-4}
2-butoxyethanol	111-76-2	1.1×10^{0}
2-toluidine	95-53-4	6.0×10^{-1}
4-aminobiphenyl	92-67-1	5.6×10^{-4}
4-dimethylaminoazobenzene	60-11-7	1.0×10^{-4}
4-nitrophenol	100-02-7	2.5×10^{-5}
Acetaldehyde	75-07-0	1.0×10^{-2}
Acetic acid	64-19-7	2.4×10^{1}
Acetic anhydride	108-24-7	5.5×10^{-1}
Acetone	67-64-1	2.3×10^{1}
Acetonitrile	75-05-8	1.4×10^{1}
Aluminum	7429-90-5	1.2×10^{-2}
Ammonia	7664-41-7	1.0×10^{2}
Ammonium chloride	2125-02-9	6.2×10^{-3}
Aniline	62-53-3	1.0×10^{-1}
Antimony	7440-36-0	7.2×10^{-4}
Antimony trioxide	1309-54-4	3.1×10^{-3}
Arsenic	7440-38-2	1.1×10^{-3}
Barium	7440-39-3	4.5×10^{-4}
Benzene	71-43-2	4.1×10^{-1}
Beryllium	7440-41-7	5.0×10^{-4}
Bis(2-ethylhexyl)phthalate	117-81-7	5.0×10^{-4}
Borates	1303-96-4	4.0×10^{-3}
Boron oxide	1303-86-2	4.5×10^{-4}
Boron trifluoride	7637-07-2	8.0×10^{-1}
Bromine	7726-95-8	3.0×10^{0}
Bromoform	75-25-2	1.0×10^{1}
Butane	106-97-8	4.0×10^{2}
Cadmium	7440-43-9	2.4×10^{-3}
Calcium hydroxide	1305-62-0	1.9×10^{-3}
Calcium oxide	1305-78-8	1.1×10^{-3}
Carbon black	1333-86-4	1.2×10^{-4}
Carbon disulfide	75-15-0	1.8×10^{0}
Carbon tetrachloride	56-23-5	7.7×10^{0}
Catechol	120-80-9	1.0×10^{-6}
Cesium hydroxide	1351-79-1	5.5×10^{-4}
Chlordane	57-74-9	1.5×10^{-6}
Chlordifuoromethane	75-45-6	2.0×10^{0}
Chloroacetic acid	79-11-8	1.6×10^{-3}
Chlorobenzene	108-90-7	5.2×10^{-1}
Chloroform	67-56-3	5.7×10^{0}
Chromic chloride	0025-73-7	1.8×10^{-3}
Chromium	7440-47-3	2.1×10^{-4}
Cobalt	7440-48-4	4.8×10^{-4}
Copper	7440-50-8	2.5×10^{-2}
Cyanides, as Cn	56-12-5	2.0×10^{-5}
Cyclohexane	110-82-7	8.0×10^{0}
Cyclohexanone	108-94-1	3.6×10^{0}

Table 2. (continued)

Chemical	CAS No.	Release (g/h)
DDT	50-29-3	5.0×10^{-5}
Dibutyl phthalate	84-74-2	2.5×10^{-4}
Dichlorodifluoromethane	75-71-8	2.0×10^{1}
Dicyclopentadienyl iron	102-54-5	5.0×10^{-4}
Diethyl phthalate	84-66-2	3.0×10^{-4}
Dimethylaniline	121-69-7	4.5×10^{-1}
Ethyl acetate	141-78-6	5.2×10^{0}
Ethyl alcohol	64-17-5	3.4×10^{1}
Ethylene dichloride	107-06-2	5.5×10^{0}
Ethylene glycol	107-21-1	1.0×10^{1}
Ethylenediamine	107-15-3	6.0×10^{-1}
Fluoride	6984-48-8	5.0×10^{-4}
Formaldehyde	50-00-0	2.6×10^{0}
Formic acid	64-18-6	1.8×10^{1}
Glutaraldehyde	111-30-8	5.4×10^{-2}
Hafnium metal, powder, wet	7440-58-6	5.0×10^{-4}
Hexane	110-54-3	3.8×10^{1}
Hydrazine	302-01-2	1.5×10^{0}
Hydrofluoric acid	7884-39-3	1.7×10^{1}
Hydrogen bromide	0035-10-6	1.5×10^{1}
Hydrogen chloride	7647-01-0	9.8×10^{1}
Hydrogen peroxide	7722-84-1	3.0×10^{1}
Hydroquinone	123-31-9	1.4×10^{-3}
Indium	7440-74-6	2.9×10^{0}
Iodine	7553-56-2	4.0×10^{-3}
Iodomethane	74-88-4	5.7×10^{-1}
Iron (III) oxide	1309-37-1	7.2×10^{-3}
Isoamyl alcohol	123-51-3	7.7×10^{-1}
Isobutyl alcohol	78-83-1	4.0×10^{-1}
Isopropyl alcohol	67-53-0	1.2×10^{1}
Lead	7439-92-1	7.0×10^{-3}
Lead chromate	7758-97-6	3.4×10^{-4}
Magnesium oxide	1309-48-4	3.8×10^{-3}
Manganese	7439-95-5	2.6×10^{-3}
Mercuric chloride	7487-94-7	3.5×10^{-4}
Mercury	7439-97-6	9.0×10^{0}
Methyl alcohol	67-56-1	9.0×10^{1}
Methyl ethyl ketone	78-93-3	2.3×10^{0}
Methyl isobutyl ketone	108-10-1	4.0×10^{0}
Methyl n-amyl ketone	110-43-0	3.9×10^{-1}
Methyl propyl ketone	107-87-9	3.1×10^{-1}
Methylene chloride	75-09-2	1.1×10^{2}
Molybdenum	7439-98-7	6.1×10^{-4}
Morpholine	110-91-8	1.2×10^{-1}
Naphthalene	91-20-3	4.5×10^{-3}
N-butyl alcohol	71-36-3	3.6×10^{0}
Nickel	7440-02-0	1.7×10^{-3}
Nitric acid	7697-37-2	2.5×10^{2}
Nitric oxide	0102-43-9	6.4×10^{3}

Table 2. (continued)

Chemical	CAS No.	Release (g/h)
Nitrobenzene	98-95-3	6.2×10^{-1}
Nitromethane	75-52-5	1.1×10^{0}
N-nitrosophenylhydroxyl-amine ammonium	135-20-5	2.0×10^{-4}
Osium tetroxide	0816-12-0	1.0×10^{-6}
Oxalic acid	144-62-7	3.7×10^{-2}
Paraffin oil	8012-95-1	4.5×10^{-1}
Pentachlorophenol	87-86-5	1.0×10^{-4}
Pentane	109-66-0	5.0×10^{0}
Pentyl acetate	628-63-7	4.7×10^{0}
Phenol	108-95-2	2.4×10^{0}
Phosphoric acid	7664-38-2	4.8×10^{1}
Phosphorous	7723-14-0	2.5×10^{-4}
Platinum	7440-08-4	7.5×10^{-4}
Potassium antimonyl tartrate	8300-74-5	4.5×10^{-4}
Potassium cyanide	151-50-8	3.5×10^{-4}
Potassium hydroxide	1310-58-3	3.5×10^{-2}
Propyl alcohol	71-23-8	8.8×10^{-2}
Pyridine silylation grade	110-85-1	2.9×10^{0}
Quinoline	91-22-5	4.7×10^{-4}
Rhodium	7440-16-6	4.3×10^{-4}
Selenium	7782-48-2	3.1×10^{-4}
Silver	7440-22-4	4.4×10^{-4}
Sodium azide	6628-22-8	6.0×10^{-4}
Sodium bisulfite	7631-90-5	1.4×10^{-3}
Sodium cyanide	143-33-9	1.2×10^{-3}
Sodium hydroxide	1310-73-2	9.7×10^{-1}
Sodium metabisulfite	7681-57-4	1.9×10^{-3}
Sodium selenate	3410-01-0	8.0×10^{-4}
Sodium selenite	0102-18-8	1.3×10^{-4}
Sulfuric acid	7664-83-9	9.0×10^{1}
Tantalum	7440-25-7	8.0×10^{-4}
Tellurium	3494-80-9	1.0×10^{-4}
Tetrahydrofuran	109-99-9	4.6×10^{0}
Tetrasodium pyrophosphate	7722-88-5	2.8×10^{-3}
Thioglycolic acid	68-11-1	5.0×10^{-4}
Tin	7440-31-5	1.2×10^{-2}
Titanium tetrachloride	7550-45-0	2.4×10^{0}
Toluene	108-88-3	2.1×10^{1}
Tributyl phosphate	126-73-8	2.0×10^{2}
Trichloroacetic acid	76-03-9	8.3×10^{-1}
Triethylamine	121-44-8	2.6×10^{-1}
Trimethylamine	75-50-3	1.0×10^{-1}
Triphenylamine	603-34-9	2.3×10^{-5}
Tungsten	7440-33-7	4.0×10^{-4}
Uranium	7440-51-1	1.9×10^{-3}
Vanadium pentaoxide	1314-62-1	2.0×10^{-3}

Table 2. (continued)

Chemical	CAS No.	Release (g/h)
Xylene	1330-20-7	6.4×10^{0}
Yttrium	7440-65-5	7.5×10^{-4}
Zinc chloride	7646-85-7	4.5×10^{-3}
Zinc oxide	1314-13-2	5.8×10^{-3}
Zirconium	7440-67-7	1.6×10^{-3}

Note: These are estimates of releases from Building 325. Without a source term for lead assembly (LA) activities, it cannot be determined which LA activity would contribute in excess of 1% of the release of the particular pollutant.

Table 3. Annual emissions for Building 325

Radionuclide	Annual emissions (Ci)	Dose (mrem) to MEI—as reported in annual report
^{3}H (as HTO)	1.4–54	$6.8 \times 10^{-4} - 2.47 \times 10^{-3}$
^{3}H (as HT)	$5.1 \times 10^{-1} - 29$	
^{60}Co	ND[a] – 1.0×10^{-8}	
^{65}Zn	6.1×10^{-7}	
^{90}Sr	ND[a] – 8.7×10^{-7}	
^{95}Zr	ND[a]	
^{106}Ru	2.4×10^{-6}	
^{123}Sb	ND[a] – 1.5×10^{-6}	
^{134}Cs	ND[a]	
^{137}Cs	ND[a] – 1.6×10^{-7}	
^{134}Eu	ND[a] – 1.4×10^{-6}	
^{155}Eu	ND[a]	
^{23}Pu	ND[a] – 6.7×10^{-8}	
$^{239/240}Pu$	ND[a] – 9.8×10^{-7}	
^{241}Am	$1.2 \times 10^{-9} - 5.2 \times 10^{-8}$	
Unsp. alpha	$1.5 \times 10^{-7} - 6.5 \times 10^{-7}$	
Total alpha	$8.5 \times 10^{-7} - 1.6 \times 10^{-6}$	
Total beta	$2.4 \times 10^{-6} - 9.9 \times 10^{-5}$	

[a]ND = nondetected.

Radionuclide airborne emissions for Building 325: 1991–1996.

2.2.3 Water

A map showing the locations of all surface water bodies downstream of the facility to the first large river, including continuous and intermittent stream flows, impoundments, lakes, or any other similar features is shown in document DOE/EIS-0229.

Maps of 100- and 500-year floodplains for Hanford do not exist because Federal Emergency Management Agency (FEMA) attention has never been focused on the site. The DOE assessment of flooding potential is documented in RLO-76-4. This document states that the Probable Maximum Flood (1,440,000 ft^3/s) as calculated by the U.S. Corps of Engineers would result in water level at the Hanford

300 Area of 383 ft. The ground surface elevation at Building 325 is 402 ft. Additional information is available in PNL-6515, Rev. 8, pages 4.55–4.61.

Depths to groundwater at the candidate locations may be derived by comparing the elevation data provided in Table 1 on land use with the water table elevations shown in PNL-6415, Rev. 8, pages 4.65 and 4.69–71. Additional details are provided in an excerpt from the *Groundwater Monitoring Report for FY 1996*, Sect. 3.6 (Attachment 2). There are no listed sole-source aquifers beneath the proposed location. Details of the 300 Area water system servicing Building 325 are provided in RL-WSP-94-01.

Additional information on Hanford site groundwater is presented in PNL-6415, Rev. 8, pages 4.63–4.67, in the Storage and Disposition PEIS, Vol. 1, pages 3-34–3-37, and in PNNL-11139, pages 177–234.

The groundwater beneath the proposed facilities is not classified. Groundwater beneath the site is discussed in the Storage and Disposition PEIS, Vol. 1, pages 3-34–3-37 and in PNL-6415, Rev. 8, pages 4.63–4.67.

Table 4 provides requested information for water resources.

Table 4. Requested information for water resources

Requested information	Facility
Flow rates for surface water bodies downstream from the facility to the first large river	
Annual average, m^3/s (ft^3/s)	See PNL-6415, Rev. 8, page 4.53
7-day, 10-year, Low flow, m^3/s (ft^3/s)	See note

Note: The Hanford reach is the last free-flowing stretch of the Columbia River. The hydrograph of the Hanford Reach is significantly altered by the operation of upstream reservoirs that regulate the headwaters in Canada, Idaho, and Montana. Release from Priest Rapid's Dam constitutes the flow in the Hanford Reach. The releases from Priest Rapids are specified by the Federal Energy Regulatory Commission (FERC) in the Vernita Bar Settlement Agreement entered between Public Utility District (PUD) No. 2 Grant County, Washington; PUD No. 1 Chelan County, Washington; PUD No. 1 Douglas County, Washington; the U.S. DOE acting by and through the Bonneville Power Administration; the National Marine Fisheries Service in its own capacity and as delegate for the U.S. Department of Commerce; the State of Washington acting by and through the Washington Department of Fisheries; the State of Oregon acting by and through the Oregon Department of Fish and Wildlife; the Confederated Tribes of the Umatilla Indian Reservation; and the Confederated Tribes of the Colville Indian Reservation.

Attachment 3 provides the FERC Settlement Agreement for Vernita Bar (i.e., Hanford Research).

2.2.4 Biological

Known wetlands or other sensitive habitat within 1.6-km radius of the proposed facility location are as follow:

- FMEF–None
- PFP–None
- Building 325–Columbia River

2.2.5 Infrastructure

Tables 5 and 6 provide requested information for facility infrastructure.

Table 5. Requested information for facility infrastructure for Building 234-5Z–200 West

Utility usage and capacity information for those utilities present at the proposed facility location	Current usage		Current capacity	
Water, L/year (gal/year)	~2×10^7	(5.2×10^6)	>4×10^7	(>1×10^7)
Sanitary wastewater, L/year (gal/year)	7×10^6	(1.8×10^6)	>1×10^7	(>2.7×10^6)
Process wastewater, L/year (gal/year)	N/A			
Electricity, MWh/year	estimated 10^4 MWh/year			
Natural gas, m^3/year (scf/year)[a]	N/A			
Fuel oil, L/year	4000		Unlimited	
Steam, kg/h (lb/h)	Not metered, estimated typical <10^4 kg/h Capacity estimated 2.5×10^4 kg/h			

[a]For gases, standard cubic feet should be measured at 14.7 psia and 60°F.

Table 6. Requested information for facility infrastructure for Building 325

Utility usage and capacity information for those utilities present at the proposed facility location	Current usage		Current capacity	
	Average	Peak	Average	Peak
Water, L/year (gal/year)			16,300 gal/min[a]	
Sanitary wastewater, L/year (gal/year)	300,000	400,000		
Retention process wastewater, L/year (gal/year)	475,000	1.1×10^6		250 gal/min[b]
Electricity, MWh/year	7.6×10^3		Unlimited	Unlimited
Natural gas, m^3/year (scf/year)[c]	N/A	N/A	N/A	N/A
Fuel oil, L/year	N/A	N/A	N/A	N/A
Steam, kg/h (lb/h)	1.5×10^3	8300 lb/h	Per document DOE/RL-89-31 published January 1990, the total rated steam capacity of the 300 Area Powerhouse is 275,000 lb/h of steam	

Note: All values are "requested information" units unless otherwise shown.

[a]Capacity of 300 Area pump at 115 psi.

[b]Peak capacity of 300 Area Treatment Effluent Disposal Facility that accepts Building 325 retention process water.

[c]For gases, standard cubic feet should be measured at 14.7 psia and 60°F.

2.2.6 Waste Management

Tables 7 and 8 provide requested information on waste management.

Table 7. Waste management information for Building 234-5Z

Waste category	Current annual generation rate	Amount in inventory	Available TSD facilities[a]			
			Building name or number	TSD method	Inventory	Capacity
Transuranic (TRU)			Central waste complex and Waste Receiving and Processing Plant (WRAP)	Disposal at Waste Isolation Pilot Plant (WIPP)	~16,500 m^3	WRAP ~1747 m^3/year
Liquid, L (gal)	0					
Solid, m^3 (ft^3)	50.91 m^3	892.54 m^3				
Mixed TRU			Central waste complex and WRAP	Disposal at WIPP treatment not required	Included above ~500,000 m^3	Included above
Liquid, L (gal)	1.5×10^4					
Solid, m^3 (ft^3)	6.87 m^3	346.44 m^3				
LLW			On-site burial	On-site disposal	Disposal on-site 6400 m^3	Unlimited
Liquid, L (gal)	1.3×10^7					
Solid, m^3 (ft^3)	218.59 m^3	610.44 m^3				
Mixed LLW			Central waste complex	Private vendor		Maximum 2000 m^3/year
Liquid, L (gal)	0					
Solid, m^3 (ft^3)	7.71 m^3	8412.62 m^3				
Hazardous			Building 616 storage	Private contract	0	As required
Liquid, L (gal)	0					
Solid, m^3 (ft^3)	1.9 m^3					
Nonhazardous (sanitary)			City of Richland landfill	N/A	N/A	N/A
Liquid, L (gal)	1.4×10^4					
Solid, m^3 (ft^3)	1830 m^3					
Nonhazardous (other)						
Liquid, L (gal)	0					
Solid, m^3 (ft^3)	2.5					

[a]TSD = treatment, storage, and/or disposal.

Table 8. Waste management information for Building 325 Hazardous Waste Treatment Units (HWTUs) and 305-B Storage Units

Waste category	Current annual generation rate	Amount in inventory	Available TSD facilities[a]			
			Building name or number	TSD method	Inventory	Capacity
Transuranic (TRU)			*a*			*b*
Liquid	1 gal	0				
Solid	44.0 ft^3	73.0 ft^3				
Mixed TRU				Storage	0	*b*
Liquid	75.0 L	0	325 HWTUs			
Solid	0.5 m^3	0.22 m^3	*a*			
LLW			325 HWTUs			
Liquid	2000.0 L	1500.0 L	*a*	Storage	0	*c*
Solid	25 m^3	15 m^3	305-B	Storage	0	*c*
Mixed LLW			325 HWTUs		0	
Liquid	500 L	100.0 gal	*a*	Storage/treat	5720 kg (liquid)	*b*
Solid	10 m^3	5.0 m^3	305-B	Storage	735 kg (solid)	*b*
Hazardous			325 HWTUs			
Liquid	271.1 kg	10 gal	*a*	Storage/treat	3751 kg (liquid)	
Solid	165.48 kg	0.1 ft^3	305-B	Storage	2248 kg (solid)	*b*
Nonhazardous (sanitary)		N/A				
Liquid	*d*	0				
Solid	Unknown	Unknown				
Nonhazardous (other)						
Liquid						
Solid						

[a]Other DOE TSDs, Hanford and non-Hanford, are available for these waste streams. WRAP, WIPP, CWC, etc.
[b]Permit limits for hazardous waste 325 HWTUs—tank and container, 305-B—container.
[c]Limited only by available space and radionuclide limit.
[d]See Table 5 information on wastewaters.

No waste management permit modifications are anticipated for Building 325 or Building 234-5Z. Some permit establishments may be needed for FMEF because it has never yet processed radioactive materials.

No other significant waste management issues are anticipated. A notice of construction permits may be required for airborne wastes.

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