

Life Cycle Analysis of Hydrogen Production via Plasma Pyrolysis of Natural Gas



Impact of Different Co-Product Management Strategies

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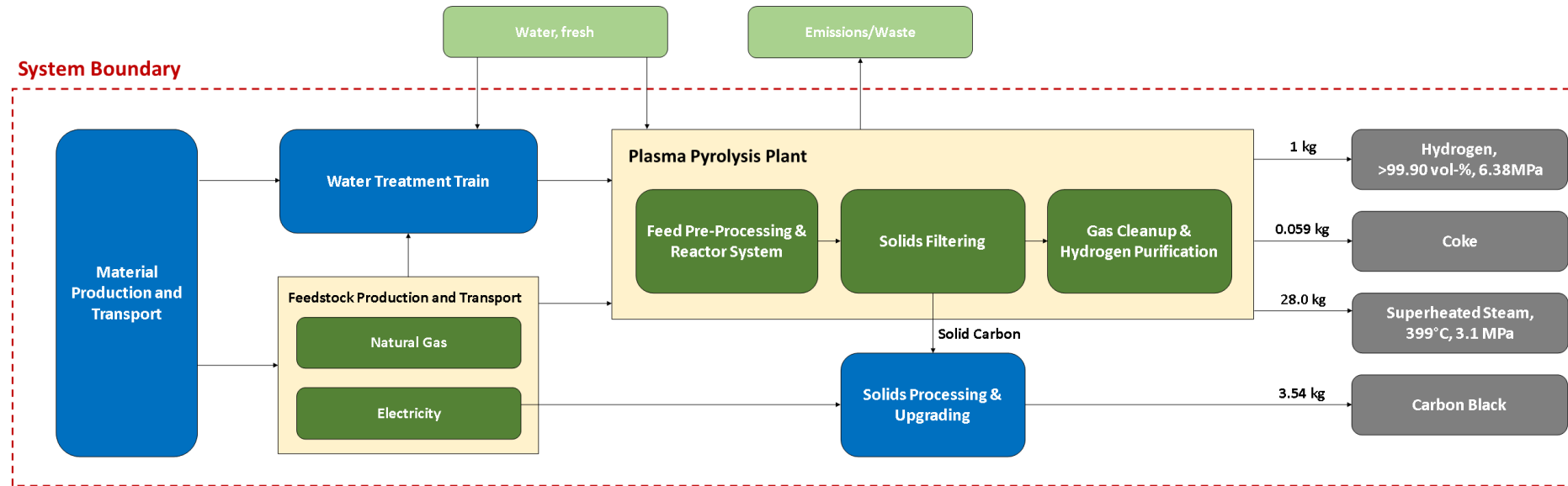


- A 2023 Department of Energy report exploring technology and market cost drivers related to hydrogen production identified methane pyrolysis as a promising emerging technology [1].
- Methane pyrolysis involves the decomposition of methane into gaseous hydrogen and solid carbon by-products, including nanoparticles.
- Several methane pyrolysis concepts exist, including catalytic, thermal, and plasma.
- Plasma pyrolysis is the most advanced methane pyrolysis concept, with a technology readiness level of 6 to 8 [2].
- NETL evaluated the cost and emissions of hydrogen produced by a natural gas plasma pyrolysis system by performing a techno-economic analysis (TEA) and life cycle analysis (LCA).

- Study meets the general requirements of ISO 14040 and ISO 14044 [3,4].
- Goal: Evaluate the life cycle impacts of plasma pyrolysis system and compare results to conventional technologies.
- Scope: Includes U.S. Average, Midwest, and Renewables scenarios.
- Functional Unit(s): Hydrogen, >99.90 vol-%, 6.38 Mpag; carbon black; coke; superheated steam, 399 °C, 3.10 MPa.
- Life Cycle Impact Assessment: Considers global warming potential (GWP) using characterization factors from Intergovernmental Panel on Climate Change (IPCC) Sixth Assessment Report (AR6) using a 100-year time horizon [5].

System Boundary

Plasma Pyrolysis

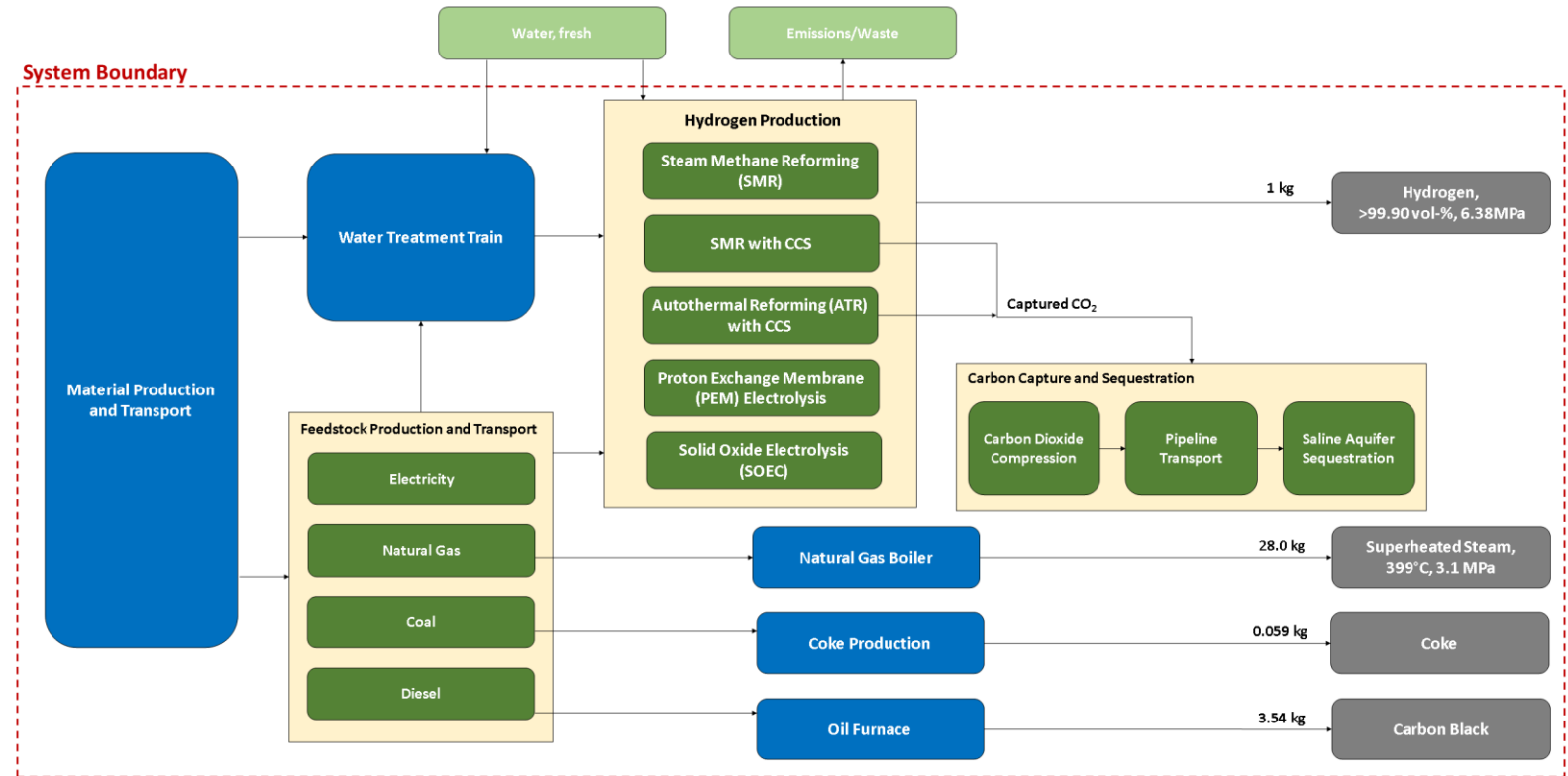


- The system boundary includes operation of the plasma pyrolysis plant, inclusive of all upstream energy and material production.
- The system boundary excludes construction of the plasma pyrolysis plant (assumed negligible).

System Boundary

Comparison System

- System boundary of comparison system is consistent with plasma pyrolysis facility.
- Conventional hydrogen production scenarios include:
 - Steam methane reforming (SMR).
 - SMR with carbon capture and storage (CCS).
 - Autothermal reforming (ATR) with CCS.
 - Proton exchange membrane (PEM) electrolysis.
 - Solid oxide electrolysis (SOEC).



Co-Product Management

General Approach

ISO 14044 procedure for allocation includes the following hierarchy [4]:

1. Avoid allocation
 - a. By subdividing processes.
 - b. By expanding the product system.
2. Allocate based on the underlying physical relationships between products.
3. Allocate based on other relationships between products.

*Primary method applied

Co-product management methods explored in this analysis include:

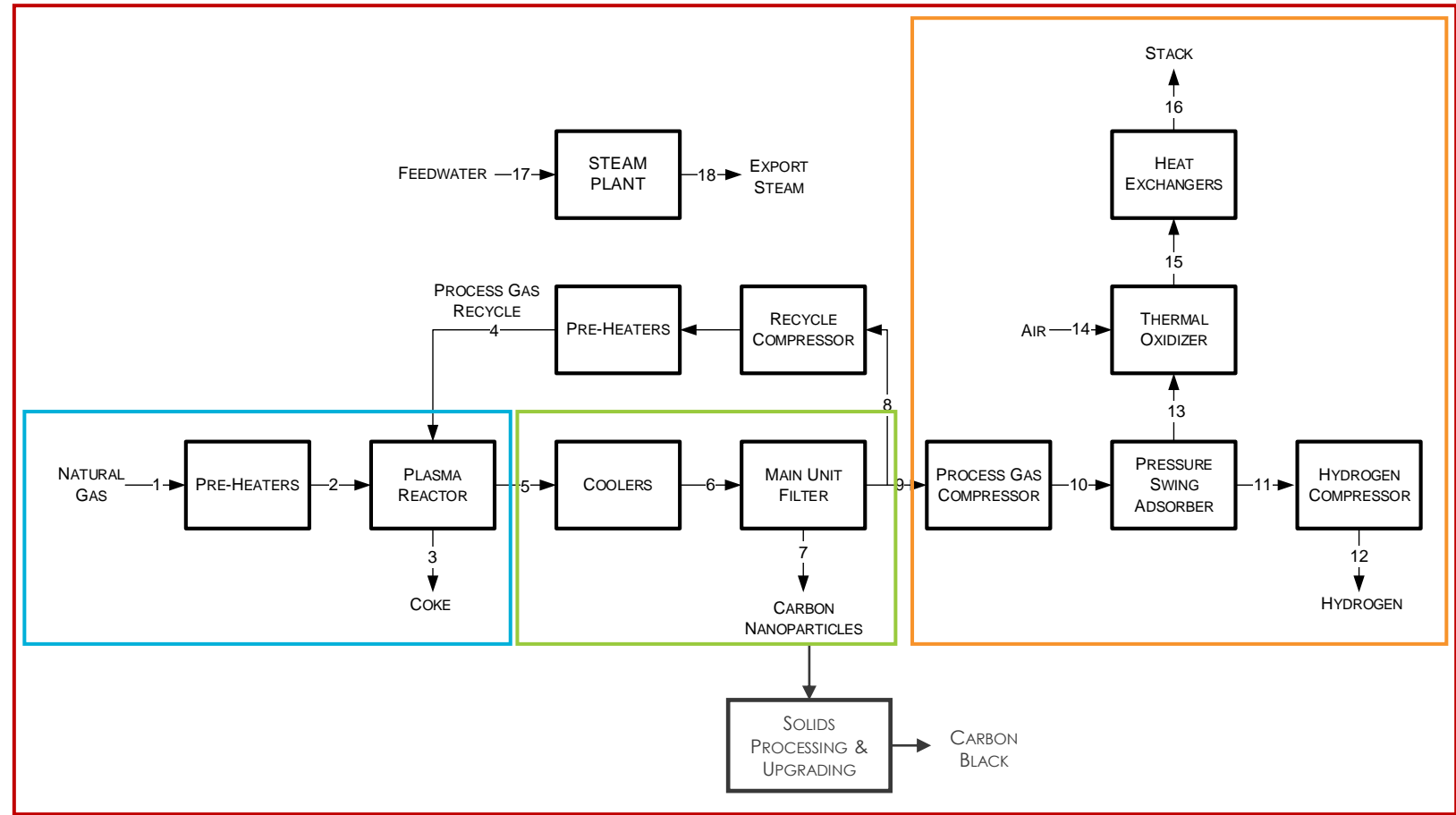
- System expansion*
- System expansion + displacement
- Causal allocation
- Mass allocation
- Energy allocation

| Product | Mass Produced (kg) | Mass Allocation Factor | Higher Heating Value (MJ/kg) | Energy Allocation Factor |
|-------------------|--------------------|------------------------|------------------------------|--------------------------|
| Hydrogen | 1 | 0.0307 | 139 | 0.414 |
| Carbon Black | 3.54 | 0.109 | 29.9 | 0.314 |
| Coke | 0.0590 | 0.00181 | 29.6 | 0.00517 |
| Superheated Steam | 28.0 | 0.859 | 3.21 | 0.267 |

Co-Product Management

Causal Allocation Approach

- Black box is subdivided into three sections.
- Subdivision cuts out steam generation and solid carbon upgrading.
- At each subdivided block, mass or molar allocation is applied according to stream table data.



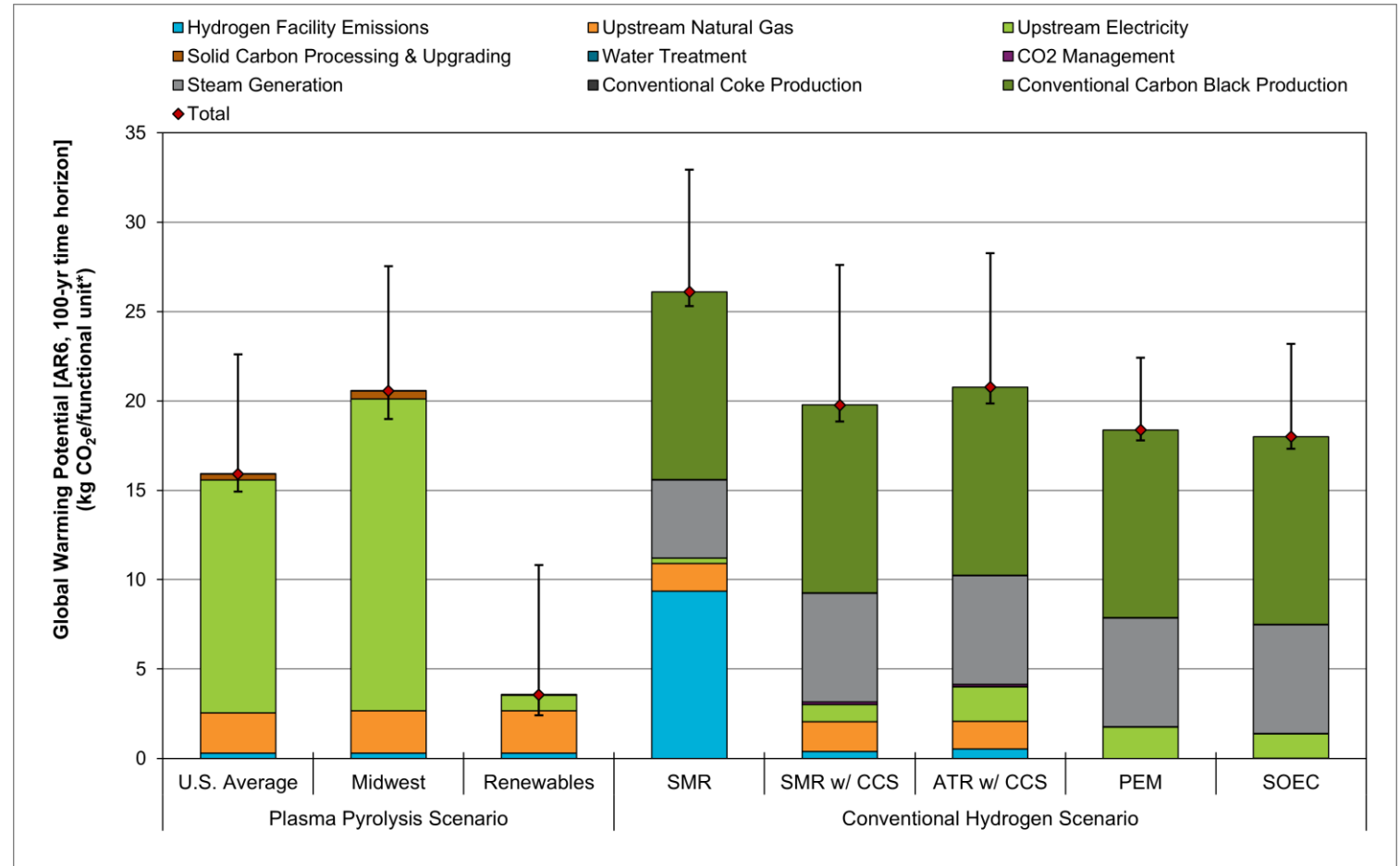
Types and Sources of Data

| Category | Source | Sensitivity |
|--|--|---|
| Plasma Pyrolysis Facility Data | NETL Plasma Pyrolysis Report (Unpublished) | None. |
| Solids Processing & Upgrading | Diab et al. 2022 [6] | None. |
| Upstream Electricity | NETL Electricity Life Cycle Inventory [7], NETL CO ₂ U Renewables Mix [8] | U.S. Average and Midwest: Monte Carlo analysis with 1,000 simulations run on emissions data with lognormal uncertainty. Renewables: low represented by 100% wind, high represented by 100% solar. |
| Upstream Natural Gas | NETL Natural Gas Baseline [9] | U.S. Average: low represented by Gulf of Mexico Offshore gas, high represented by Uinta Conventional gas. Midwest: low represented by Appalachian Shale gas, high represented by Uinta Conventional gas. |
| Municipal Water Treatment | EPA Drinking Water Treatment Models [10] | None. |
| Conventional Hydrogen Production | NETL Fossil Hydrogen Baseline [11], Henriksen et al. 2024 [12] | None. |
| CO ₂ Transport and Storage | NETL Gate-to-Grave LCA of Saline Aquifer Sequestration of Carbon Dioxide [13] | None. |
| Conventional Steam Generation (natural gas boiler, 85% efficiency) | NETL Fossil Hydrogen Baseline [11] | None. |
| Conventional Carbon Black Production (oil furnace method) | Ecoinvent [14], NETL Petroleum Baseline [15] | None. |
| Conventional Coke Production (destructive distillation of bituminous coal) | U.S. Life Cycle Inventory [16], EPA AP-42 Chapter 12 [17], NETL Coal Mining and Delivery Baseline [18] | Monte Carlo analysis with 1,000 simulations run on upstream coal parameters, primarily impacting coal mine methane emissions. |

Results

Multi-Product Functional Unit

- GWP of plasma pyrolysis scenarios:
 - U.S. Average: 15.9 kg CO₂e/FU.
 - Midwest: 20.6 kg CO₂e/FU.
 - Renewables: 3.56 kg CO₂e/FU.
- In all cases, significant high-end uncertainty is driven by natural gas techno-basin.
- U.S. average plasma pyrolysis scenario is lower than electrolysis cases, and Midwest plasma pyrolysis scenario is comparable to ATR with CCS.
- Results show that electricity source has a major impact on the resulting GWP of the plasma pyrolysis system.

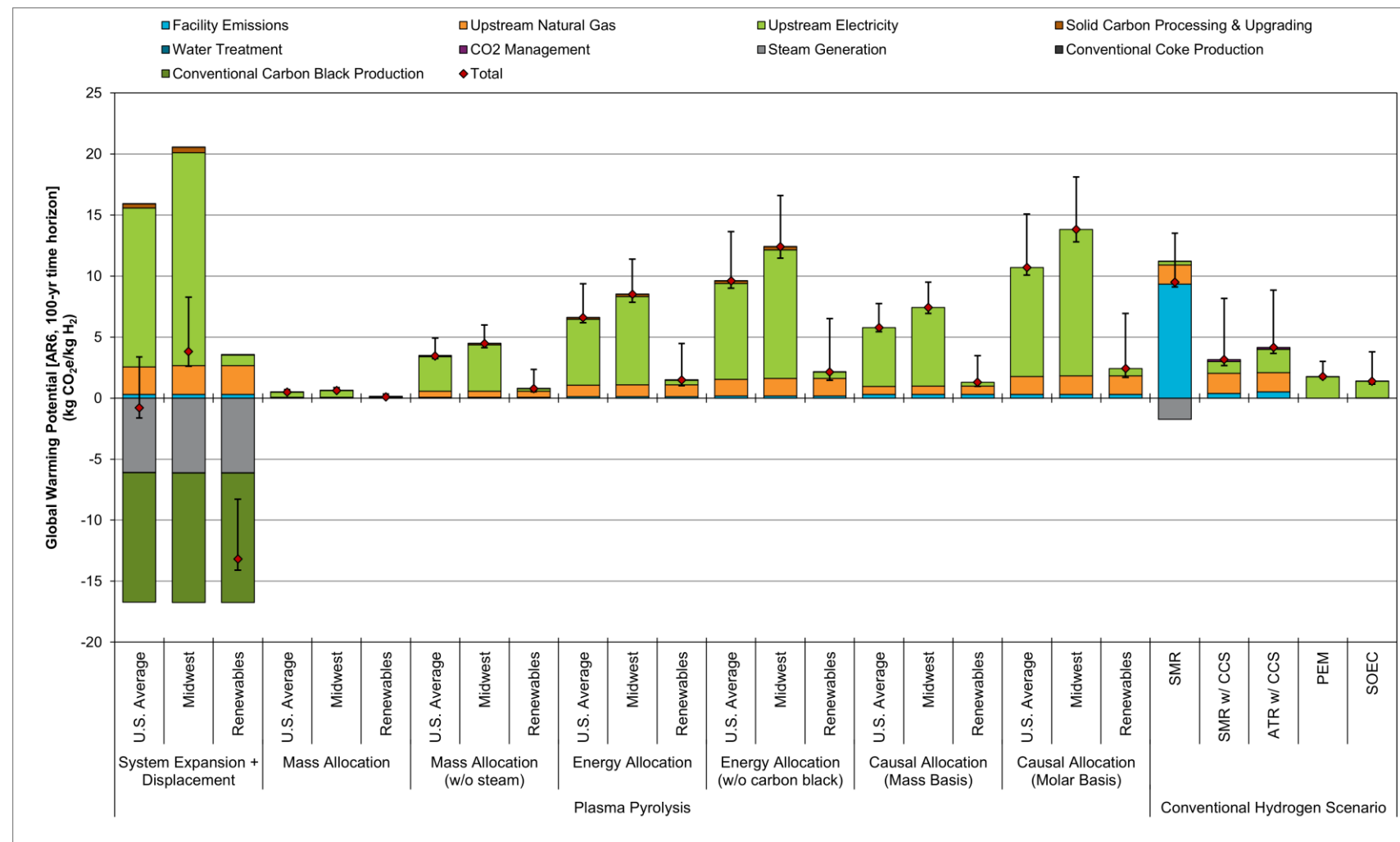


*Functional unit (FU): 1 kg of hydrogen, >99.90 vol-%, 6.38 MPag; 3.54 kg of carbon black; 0.0590 kg of coke; 28.0 kg of superheated steam, 399 °C, 3.1 MPa

Results

Single-Product Functional Unit

- GWP results vary greatly depending on co-product management strategy.
 - For U.S. average, results vary from $-0.791 \text{ kg CO}_2\text{e/kg H}_2$ to $10.7 \text{ kg CO}_2\text{e/kg H}_2$.
- Comparing to conventional hydrogen production:
 - Causal allocation approaches result in a higher GWP than conventional approaches with carbon capture.
 - Mass allocation results are lower than PEM and SOEC.



- Plasma pyrolysis is a promising hydrogen production technology that may play a key role in U.S. domestic energy production.
- Scenarios highlight the importance of electricity source in resulting GWP.
- Natural gas basin variability introduces a significant range in emissions results.
- Co-product management strategy has a significant impact on resulting GWP.
 - This highlights the importance of performing sensitivity analyses with several allocation procedures, an element of ISO 14044 that tends to be overlooked in product LCAs.
 - Such uncertainty is crucial to capture in comparative LCAs, as it may impact the conclusions drawn.

References



- [1] S. McNaul, C. White, R. Wallace, T. Warner, H. S. Matthews, J. N. Ma, M. Ramezan, E. Lewis, D. Morgan, M. Henriksen, J. White, C. Munson, R. Stevens and T. Shultz, "Hydrogen Shot Technology Assessment: Thermal Conversion Approaches," National Energy Technology Laboratory, Pittsburgh, PA, 2023.
- [2] S. Schneider, S. Bajohr, F. Graf and T. Kolb, "State of the Art of Hydrogen Production via Pyrolysis of Natural Gas," *ChemBioEng Reviews*, vol. 7, no. 5, p. 150–158, 2020.
- [3] ISO, *Environmental management — Life cycle assessment — Principles and framework (ISO 14040:2006)*, International Organization for Standardization, 2006.
- [4] ISO, *Environmental management — Life cycle assessment — Requirements and guidelines (ISO 14044:2006)*, International Organization for Standardization, 2006.
- [5] IPCC, "Climate Change 2023: Synthesis Report. Contribution of Working Groups I, II and III to the Sixth Assessment Report of the Intergovernmental Panel on Climate Change," Intergovernmental Panel on Climate Change, 2023.
- [6] J. Diab, L. Fulcheri, V. Hessel, V. Rohani and M. Frenklach, "Why Turquoise Hydrogen Will Be a Game Changer for the Energy Transition," *International Journal of Hydrogen Energy*, vol. 47, no. 61, p. 25831–25848, 2022.
- [7] T. W. Davis and M. Jamieson, "Electricity Baseline 2022," National Energy Technology Laboratory, Pittsburgh, PA, 2025. <https://edx.netl.doe.gov/dataset/electricity-baseline-2022>
- [8] NETL, "NETL CO2U openLCA LCI Database Version 2.1," National Energy Technology Laboratory, Pittsburgh, 2022.
- [9] H. Khutal, K. M. Kirchner-Ortiz, M. Blackhurst, N. Willems, H. S. Matthews, S. Rai, G. Yanai, K. Chivukula, Priyadarshini, H. Hoffman, M. B. Jamieson and T. J. Skone, "Life Cycle Analysis of Natural Gas Extraction and Power Generation: U.S. 2020 Emissions Profile," National Energy Technology Laboratory, Pittsburgh, 2024.
- [10] EPA, *Drinking Water Treatment Technology Unit Cost Models*, U.S. Environmental Protection Agency, 2018.
- [11] E. Lewis, S. McNaul, J. Matthew, M. S. Henriksen, H. S. Matthews, L. Walsh, J. Grove, T. Shultz, T. J. Skone and R. Stevens, "Comparison of Commercial, State-of-the-Art, Fossil-Based Hydrogen Production Technologies," National Energy Technology Laboratory, Pittsburgh, PA, 2022.
- [12] M. S. Henriksen, H. S. Matthews, J. White, L. Walsh, E. Grol, M. Jamieson and T. J. Skone, "Tradeoffs in life cycle water use and greenhouse gas emissions of hydrogen production pathways," *International Journal of Hydrogen Energy*, vol. 49, pp. 1221-1234, 2024.
- [13] J. Littlefield, J. Marriott, M. Jamieson, R. E. James, G. Cooney and T. J. Skone, "Gate-to-Grave Life Cycle Analysis Model of Saline Aquifer Sequestration of Carbon Dioxide," National Energy Technology Laboratory, Pittsburgh, 2013.
- [14] H.-J. Althaus, R. Hischer, M. Osses, A. Primas, S. Hellweg, N. Jungbluth and M. Chudacoff, "ecoinvent report No. 8: Life Cycle Inventories of Chemicals," ecoinvent, Dübendorf, 2007.
- [15] G. Cooney, M. Jamieson, J. Marriott, J. Bergerson, A. Brandt and T. J. Skone, "Updating the U.S. Life Cycle GHG Petroleum Baseline to 2014 with Projections to 2040 Using Open-Source Engineering-Based Models," *Environmental Science & Technology*, vol. 51, no. 2, pp. 977-987, 2016.
- [16] J. Littlefield, "Metallurgical coke, at plant," Federal LCA Commons, 2015.
- [17] EPA, "Emission Factor Documentation for AP-42 Section 12.2: Coke Production," U.S. Environmental Protection Agency, 2008.
- [18] A. Cutshaw, D. Carlson, M. Henriksen, M. Krynock, M. Jamieson and R. James, "Cradle-to-Gate Life Cycle Analysis Baseline for United States Coal Mining and Delivery," National Energy Technology Laboratory, Pittsburgh, 2023.

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