



BNL-228501-2025-JAAM

GRP-COSC-14

Conformal high-entropy oxide coatings enable fast and durable surface oxygen reactions

F. He, K. Sasaki

To be published in "Joule"

June 2025

Chemistry Department
Brookhaven National Laboratory

U.S. Department of Energy

USDOE Office of Energy Efficiency and Renewable Energy (EERE), Office of Sustainable Transportation. Hydrogen Fuel Cell Technologies Office (HFTO)

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1 Conformal High-entropy Oxide Coatings Enable 2 Fast and Durable Surface Oxygen Reactions

3 Fan He¹, Hao Liu¹, Yangsen Xu¹, Feng Zhu¹, Kotaro Sasaki², YongMan
4 Choi^{3**}, Ying Liu^{4***}, and Yu Chen^{1*}

5 ¹School of Environment and Energy, South China University of Technology, 382 East Road,
6 Higher Education Mega Center, Guangzhou 510006, P. R. China.

7 ²Chemistry Division, Brookhaven National Laboratory, Upton, NY 11973, USA

8 ³College of Photonics, National Yang Ming Chiao Tung University, Tainan 71150, Taiwan

9 ⁴Research Institute of Renewable Energy and Advanced Materials, Zijin Mining Group Co., Ltd.,
10 Xiamen, Fujian 361101, China

11 *Correspondence: eschenyu@scut.edu.cn

12 **Correspondence: ymchoi@nycu.edu.tw

13 **Correspondence: liu_ying@zijinmining.com

15 SUMMARY

16 Developing active and durable air electrodes for efficient oxygen reactions is challenging for protonic
17 ceramic cells (PCCs), especially at temperatures below 550 °C, due to the sluggish oxygen reaction kinetics
18 and insufficient structural stability in high humidity conditions. Here, we report a rational-designed conformal
19 coating with a high-entropy $\text{PrNi}_{0.2}\text{Mn}_{0.2}\text{Co}_{0.2}\text{Fe}_{0.2}\text{Cu}_{0.2}\text{O}_{3-\delta}$ (PNMCFC) perovskite structure on the surface
20 of a state-of-the-art $\text{PrBaCo}_2\text{O}_{5+\delta}$ (PBC) air electrode. The formed hybrid air electrode (PNMCFC-PBC)
21 shows faster surface oxygen kinetics and a more stable phase structure in high-humidity air than the bare
22 PBC electrode, as demonstrated by the electrical conductivity relaxations and surface composition
23 analyses. Further density functional theory (DFT) calculations suggest that the conformal coating can
24 mitigate Ba segregation at the interface and improve oxygen-related reactions, enhancing overall stability
25 and electrocatalytic performance. The cells with the developed hybrid electrodes show encouraging
26 electrochemical performance at 550 °C: a polarization resistance of $0.72 \Omega \text{ cm}^2$, a peak power density of
27 1.30 W cm^{-2} , an electrolysis current density of -1.36 A cm^{-2} at 1.3 V, and reasonable operating stabilities
28 ($\sim 200 \text{ h}$ at 550 °C). Our progress in this study offers valuable guidance for the design of next-generation
29 PCC air electrodes.

30 KEYWORDS

31 Protonic ceramic cells; High-entropy materials; Air electrodes; Activity; Conformal coating.

33 INTRODUCTION

34 Energy conversion and storage technologies continuously innovate to establish a sustainable system
35 with a cheaper and more efficient energy supply.¹⁻⁴ Among all types of technologies, reversible protonic
36 ceramic cells (PCCs) are one of the most efficient devices with excellent fuel flexibility, versatile
37 functionality, and emission-free power generation.⁵⁻⁹ However, their inclusion in competitive
38 commercialization requires further maturation on the operating temperature, cost, and lifetime.¹⁰⁻¹²
39 Reduction in operating temperatures often causes a dramatic increase in electrochemical resistance of cell
40 components, especially of air electrodes, due to the sluggish activation of oxygen exchange kinetics at low
41 temperatures.¹³⁻¹⁵ More commercially viable attention has been drawn to electrodes with superior durability
42 against high-concentration steam and high activity for the oxygen reduction and evolution reactions (ORR
43 and OER) under realistic operating conditions of PCCs.

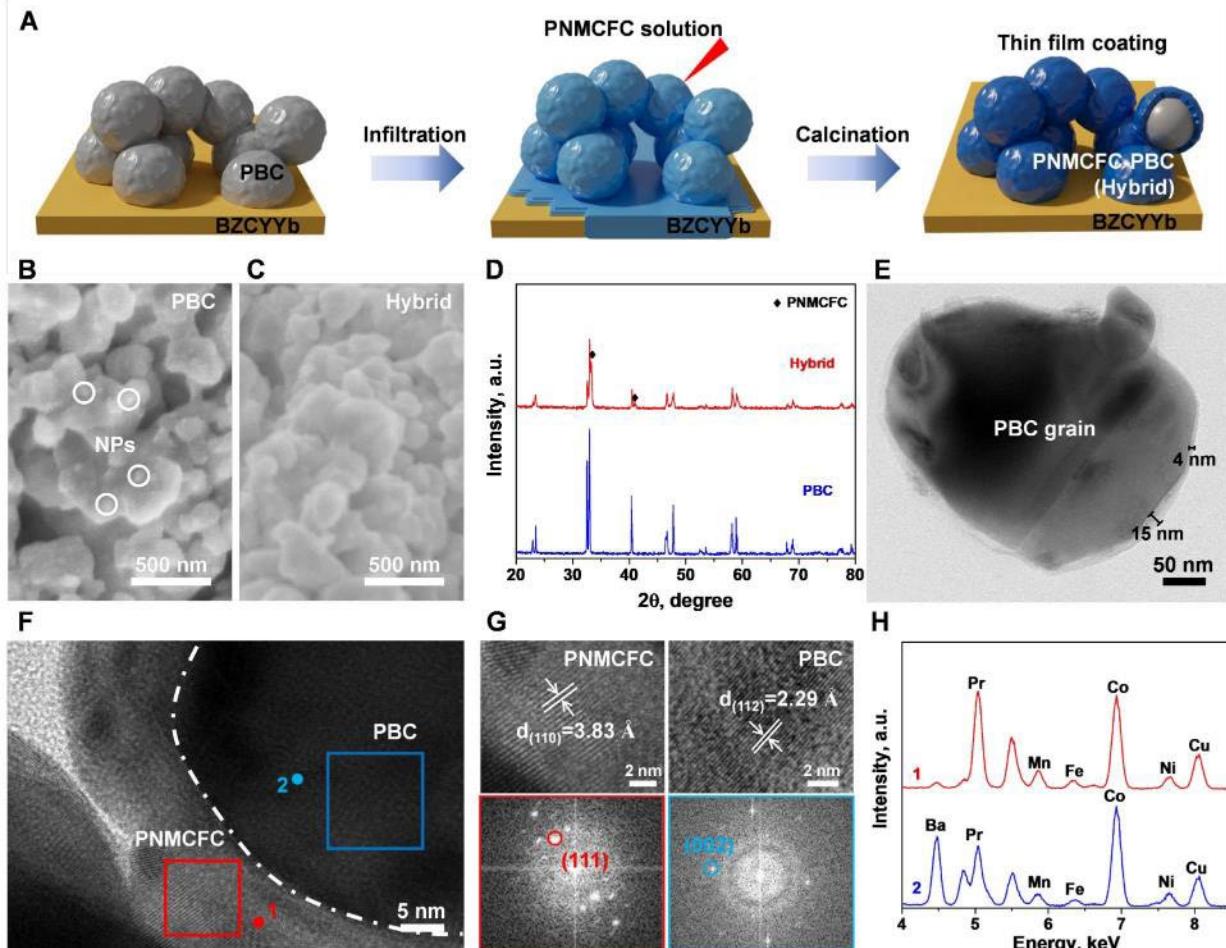
44 Managing the impact of humidity on the phase structure and catalytic activity became a key technical
45 direction for improving the durability and electrochemical performance of electrodes in PCCs.¹⁶⁻¹⁸ Many
46 state-of-the-art electrodes, such as $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$ (LSCF),¹⁹ $\text{Ba}_{0.5}\text{Sr}_{0.5}\text{Co}_{0.8}\text{Fe}_{0.2}\text{O}_{3-\delta}$ (BSCF),²⁰
47 $\text{PrBaCo}_2\text{O}_{5+\delta}$ (PBC),²¹ and $\text{PrBa}_{0.5}\text{Sr}_{0.5}\text{Co}_2\text{O}_{5+\delta}$ (PBSC),²² have demonstrated excellent mixed conductivity

48 and fast ORR/OER kinetics whereas displayed dramatic performance degradations under the operating
49 conditions of PCCs (500-600 °C and high steam concentration). A steam-containing environment is
50 commonly encountered during the operation of PCCs, while steam-mediated phase segregations have
51 been recently reported near the surface of most Sr(Ba)-based perovskite oxides or electrode-electrolyte
52 interface.^{23,24} One modification strategy is essential for structural improvement against negative water-
53 mediated segregation. Sr (Ba)-free electrodes have been investigated as the first candidate for enhanced
54 stability in PCC, such as La(Ni, Fe)O_{3-δ}, nano-fiber Pr₂NiO₄, and Ca₃Co₄O_{9-δ}.^{25,26} The high- or medium-
55 entropy concept has been introduced to develop new electrode materials and architectures with good
56 resistance to steam.^{27,28} Although the chemical system of those compounds becomes more and more
57 complicated,²⁹ the durability of the high-entropy air electrode has been largely improved under realistic cell
58 conditions with high concentrations of steam.^{22,30} A more facile and economical method for surface
59 modification is wet-chemical solution infiltration, which has been extensively utilized in electrocatalysis,
60 photocatalysis, membrane reactors, and fuel cells.³¹⁻³³

61 Most solution infiltrations are to decorate abundant highly active catalysts on the surface of the
62 substrates. However, the discrete nano-catalysts may play an unsatisfactory role in the structural stability
63 against surface segregation since the steam penetrates the pores within the surface layer.³⁴ The driving
64 forces to element segregation may originate from the electrostatic interaction between A-site cations with
65 negative charges and surface oxygen vacancies with positive charges, which is mainly associated with the
66 surface adsorbates.²⁴ A few studies demonstrated that dense La_{0.85}Sr_{0.15}MnO_{3-δ} (LSM) conformally coated
67 porous LSCF catalyst can effectively suppress Sr segregation for an enhanced stability of solid oxide fuel
68 cells (SOFCs).^{1,35} The porous LSCF backbone functions as a channel for the fast transport of oxygen ions
69 and electrons, while dense thin-film LSM coating diminishes the surface electrostatic force of LSCF for
70 enhanced durability.³⁵ However, the air electrodes in PCCs face higher concentrations of steam in the air
71 (up to 30 vol%).⁶ Maintaining the structural stability of PCC air electrodes is much more difficult than the
72 traditional cathode for oxygen-ion conducting solid oxide fuel cells (O-SOFCs). Thus, one pivotal strategy
73 is to develop a desired coating that should possess a conformal coverage of the backbone, excellent
74 activities for ORR and OER, and high structural tolerance to steam and even to carbon dioxide encountered
75 in reversible PCC operation.

76 Inspired by the aforementioned methods and requirements, we showcase a Ba(Sr)-free high-entropy
77 conformal perovskite coating, PrNi_{0.2}Mn_{0.2}Co_{0.2}Fe_{0.2}Cu_{0.2}O_{3-δ} (PNMCFc), successfully covered onto the
78 PBC backbone for enhanced electrocatalytic activity and durability of PCCs. The selection of B-site cations
79 close to Co ions in the PNMCFc perovskite may lead to the fast oxygen exchange kinetics and versatile
80 functionalities as a so-called “Cocktail” effect,³⁶ as determined by electrical conductivity relaxations (ECR)
81 results and low polarization resistances (R_p). According to the equation of $ΔG_{mix} = ΔH_{mix} - TΔS_{mix}$, the
82 structural stability of high-entropy PNMCFc ($ΔS_{mix} > 1.5R$, R is gas constant) is largely enhanced compared
83 to the PBC electrode.³⁷ Additionally, density functional theory (DFT) calculations were applied to support
84 the experimental findings by investigating the enhanced electronic interactions, efficient surface oxygen
85 kinetics, and migration of Ba cations facilitated by the conformal coating on the PBC backbone using the
86 high-entropy PNMCFc. When compared with the PBC electrode, the conformal PNMCFc-coated PBC
87 electrode (hybrid electrode) performs lower area-specific resistance and higher electrochemical
88 performances in fuel-cell mode (2.29 W cm⁻² at 650 °C) and electrolysis mode (-3.12 A cm⁻² at 1.3V and
89 650 °C) modes. Our high-entropy conformal coating strategy could optimize the mixed ion-conducting air
90 electrode materials to realize structural stability against high-concentration steam encountered in realistic
91 PCC operation. Not limited to fuel-cell stability in ambient air, the cells with the hybrid electrode also exhibit
92 excellent stabilities in electrolysis and reversible cycling under conditions of highly humidified air (30% H₂O)
93 and large current density (-1A cm⁻²).

94
95 **RESULTS AND DISCUSSION**

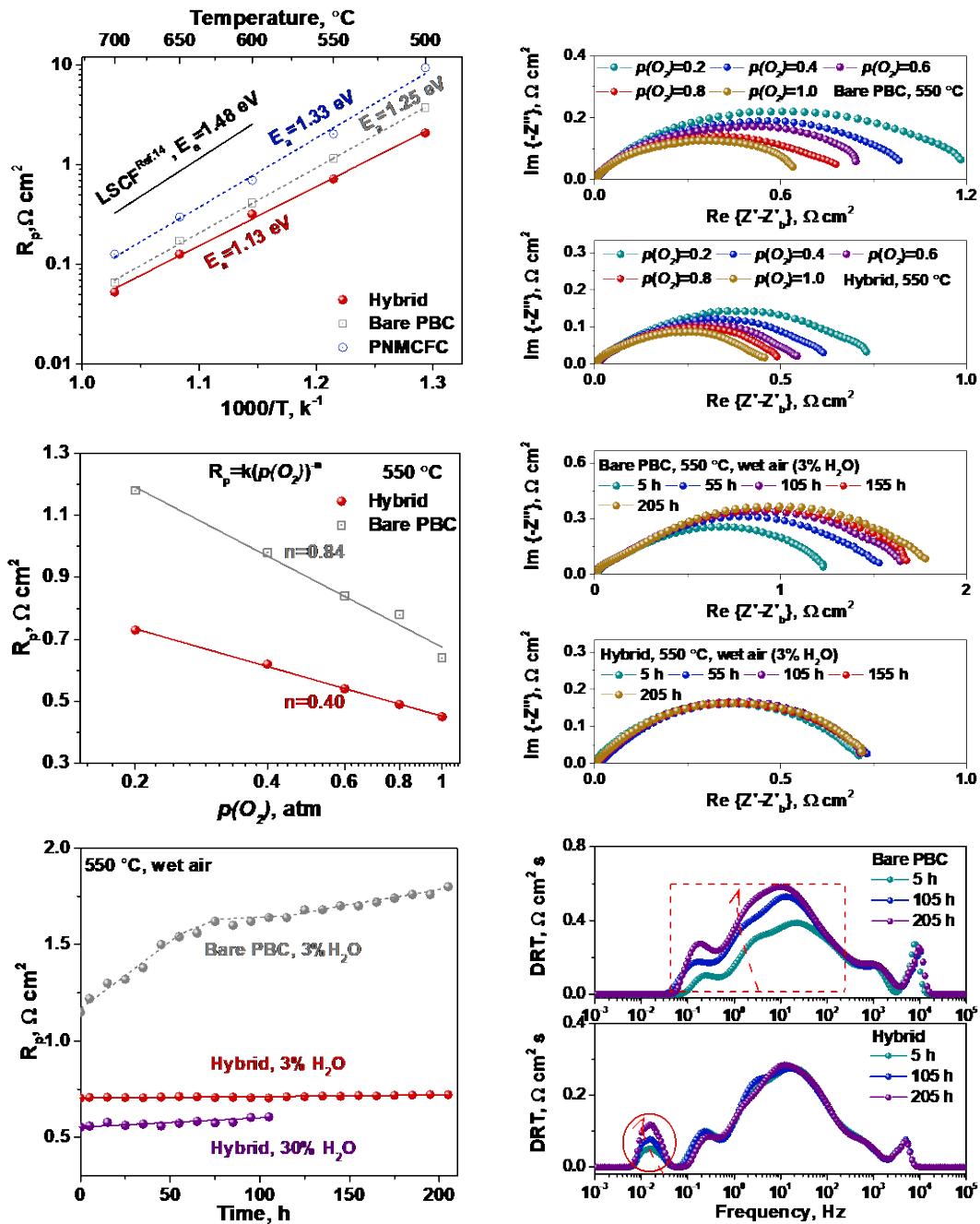


96
97 **Figure 1. Morphology and crystal structure of the hybrid electrode.**

98 (A) Schematic of a PBC electrode backbone covered with a conformal high-entropy PNMCFc coating.
99 (B) and (C) SEM images of the PBC and (C) PNMCFc-coated PBC hybrid electrodes.
100 (D) XRD patterns of the PBC and PNMCFc-coated PBC hybrids.
101 (E) STEM image of a whole PBC grain covered by a conformal PNMCFc coating.
102 (F) A high resolution-TEM image of the PBC grains covered with a conformal PNMCFc coating.
103 (G) Enlarged TEM images of PNMCFc coating and PBC backbone (top); the bottoms are the FFT patterns
104 from the red and blue rectangles in (F).
105 (H) EDS spectra from points 1 and 2, indicating that the outer surface is mainly PNMCFc (point 1) while
106 the inside is PBC and PNMCFc hybrid grains (point 2).

107
108 **Structural characterization of high-entropy conformal perovskite coating**

109 Ba (Sr)-free high-entropy perovskite, $\text{PrNi}_{0.2}\text{Mn}_{0.2}\text{Co}_{0.2}\text{Fe}_{0.2}\text{Cu}_{0.2}\text{O}_{3-\delta}$ (PNMCFc), displayed an
110 orthorhombic structure with the space group of *Pnma* and lattice parameters of $a=5.4340\text{ \AA}$, $b=7.6744\text{ \AA}$,
111 and $c=5.4506\text{ \AA}$ ($\chi^2=0.47$, **Figure S1** and **Table S1**). The actual atomic ratio of each element in as-
112 synthesized PNMCFc was examined by inductively coupled plasma-mass spectrometry (ICP-MS), which
113 closely approaches the nominal chemical stoichiometric ratio (**Table S2**). When employed to cover the
114 whole surface of a porous PBC electrode, differing from the modifications with nanoparticles, the conformal
115 thin-film PNMCFc coating enables complete isolation of the PBC backbone from steam exposure during
116 harsh PCC operational conditions, thereby probably enhancing system durability. The structural similarity
117 of PNMCFc to PBC facilitates the conformal growth of a dense and well-connected coating during high-
118 temperature thermal calcination (**Table S1**). **Figure 1A** schematically exhibits the whole process of the thin-



119

120

Figure 2. Electrochemical performance and durability of the hybrid electrodes.121
122

(A) Arrhenius plots of the polarization resistance of bare PBC, PNMCFC and hybrid (PNMCFC-PBC) electrodes.

123

(B) EIS of bare PBC and hybrid electrodes as a function of $p(O_2)$ at 550 °C.

124

(C) Dependence of each R_p of bare PBC and hybrid electrodes as a function of $p(O_2)$ at 550 °C.125
126(D) EIS of bare PBC (top) and hybrid electrodes (bottom) at different testing times in wet air (3% H_2O) and 550 °C.

127

(E) Time dependence of R_p of bare PBC and hybrid electrodes in wet air (3% and 30% H_2O) at 550 °C.

128

(F) DRT analysis of bare PBC (top) and hybrid electrodes (bottom) at different testing times according to the EIS data in (d).

129

130

131 film formation of a high-entropy catalyst coating onto a PBC backbone. Many nanoparticles (NPs) were
132 covered on the surface of the PBC electrode, which was likely associated with the $\text{BaCoO}_{3-\delta}$ phase (**Figure**
133 **1B**). While the hybrid (PNMCFC-PBC) electrode maintained a relatively smooth surface with a larger
134 average grain size of 550 nm (**Figure 1C** and **S2**). According to the X-ray diffraction (XRD) patterns (**Figure**
135 **1D** and **Figure S3**), the PNMCFC phase was successfully observed on the hybrid electrode. Briefly, 3 μL
136 of 0.1 M PNMCFC nitrate organic solution was infiltrated into the PBC backbone (loading of $\sim 0.3 \text{ mg cm}^{-2}$),
137 followed by thermal calcination at 950 $^{\circ}\text{C}$ for 5 h to form the PNMCFC coating PBC hybrid electrode. **Figure**
138 **1E** demonstrated that the PBC surface was coated by a conformal and continuous PNMCFC thin film with
139 a projected thickness of 4-15 nm. The high-temperature calcination and structural similarity led to the
140 coherent coating, which can be commonly observed (**Figure S4**). As obtained by high-resolution
141 transmission electron microscopy (HR-TEM), the space distances of 3.83 and 2.29 \AA were assigned to the
142 (110) plane of PNMCFC and (112) plane of PBC, respectively (**Figure 1F** and **1G**, top). The two different
143 phases of surface coating and bulk grain were well distinguished via the fast Fourier transform (FFT) on
144 the red and blue rectangles in **Figure 1F**. The marked diffraction spots corresponded to the (111) plane of
145 PNMCFC and the (002) plane of PBC, which was consistent with the XRD refinement (**Figure 1G**, bottom).
146 The X-ray energy dispersive spectrum (EDS) spectra (**Figure 1H**) indicated that the surface coating is
147 mainly PNMCFC (point 1), while the bulk substrate is composed of PNMCFC and PBC hybrid phases (point
148 2). The slight cation thermal diffusion also occurred between PNMCFC and PBC after thermal calcination
149 at 950 $^{\circ}\text{C}$ for 5 h, as checked by the peak belonging to Ba at point 1. The discrepancy in the elemental
150 composition with the line scanning from bulk to surface further supported the formation of the unique
151 architecture of PNMCFC thin-film coated PBC (**Figure S5**).
152

153 **Electrochemical performance and durability**

154 Shown in **Figure 2A** are the Arrhenius plots of the polarization resistance (R_p) of the BZCYYb-
155 supported symmetrical cells with the bare PBC, PNMCFC and hybrid electrodes, combined with the
156 comparison of the typical commercial LSCF electrode as reported.¹⁶ The hybrid electrode achieved a lower
157 R_p ($0.72 \Omega \text{ cm}^2$ at 550 $^{\circ}\text{C}$) and activated energy (E_a , 1.13 eV) than the PBC ($1.16 \Omega \text{ cm}^2$ at 550 $^{\circ}\text{C}$, 1.25
158 eV) and PNMCFC electrode ($2.04 \Omega \text{ cm}^2$ at 550 $^{\circ}\text{C}$, 1.33 eV), much better than the LSCF electrode recently
159 reported (**Figure S6**).¹⁶ The R_p of the hybrid electrodes showed no apparent decrease when the
160 concentration of infiltration solution increased from 0.1 to 0.2 M, leading to the solution concentration fixed
161 at 0.1 M (**Figure S7**). The influence of the PNMCFC coating on PBC electrode surface reaction kinetics
162 was further investigated via the electrochemical resistances measured under different oxygen partial
163 pressures ($p(O_2)$) (**Figure 2B**). The specific rate-limiting step for surface oxygen exchange kinetics can be
164 fitted by R_p dependence on $p(O_2)$, which is expressed as the equation of $R_p = k(p(O_2))^{-n}$ (n is reaction order,
165 k is constant).³⁸ Clearly, note that the n value of the hybrid electrode is largely changed from the original
166 0.84 of the PBC electrode to 0.40 (**Figure 2C**). $n=0.84$ of the PBC electrode may be related to the gas
167 diffusion on the electrode surface.^{39,40} When $n=0.375$, the first charge transfer reaction of ($\text{O}_{\text{ads}} + \text{e}^- +$
168 $\text{V}_{\text{O}_{(\text{s})}}^{\bullet\bullet} \leftrightarrow \text{O}_{(\text{s})}^{\bullet}$) is a key rate-limiting step for hybrid electrodes.^{39,40} This result indicates that the ORR
169 process of PNMCFC-PBC is mainly controlled by the surface oxygen vacancy concentration,⁴¹ differing
170 from that of the PBC electrode (which is controlled by the mass transfer). To verify this, we analyzed O 1s
171 X-ray photoelectron spectroscopy (XPS) spectra of PBC, PNMCFFC, and PNMCFC-PBC (**Figure S8**). It
172 was found that the $\text{O}_{\text{ad}}/\text{O}_{\text{lattice}}$ ratio of the PNMCFC-PBC was reduced to 2.08 compared to the PBC (its
173 $\text{O}_{\text{ad}}/\text{O}_{\text{lattice}}$ ratio is 2.43), suggesting the surface oxygen vacancy concentration of the hybrid sample
174 decreased. The electrical conductivities of the PNMCFC and PNMCFC-PBC reached $1.5\text{-}4.8 \text{ S cm}^{-1}$ and
175 $564\text{-}1175 \text{ S cm}^{-1}$ at 400-750 $^{\circ}\text{C}$, respectively, which were lower than those ($620\text{-}1215 \text{ S cm}^{-1}$ at 400-750
176 $^{\circ}\text{C}$) of the PBC (**Figure S9**). Thus, the surface vacancy concentration and electrical conductivities of the
177 PNMCFC coating may lead to changes in hybrid electrode kinetics from surface gas diffusion (rate-limiting
178 step of PBC) to the charge transfer reaction.

179 Numerous highly active air electrodes are closely associated with $\text{Sr}(\text{Ba})\text{CoO}_3$ -based perovskite
180 oxides,²³ while their stability under humidified air is poor due to phase segregation, especially in reversible

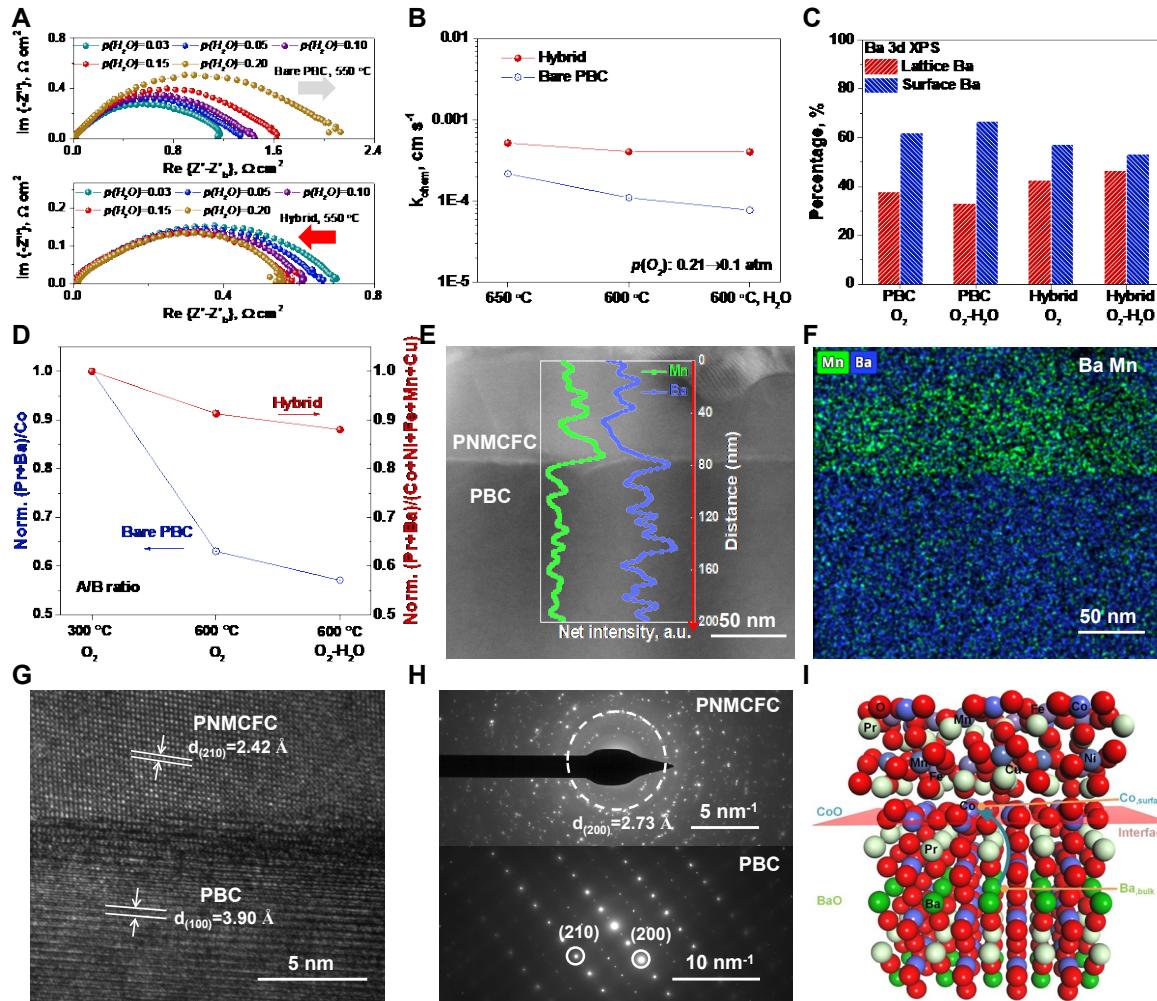


Figure 3. Investigation on the enhanced durability of the hybrid electrode.

(A) EIS of bare PBC and hybrid PNCFC-PBC as a function of $p(\text{H}_2\text{O})$ at 550 °C.
 (B) k_{chem} of bare PBC and PNCFC-PBC measured at 650 °C, and 600 °C before and after a treatment in wet air (10% H_2O) for 100 h.
 (C) Surface Ba composition of PBC and hybrid catalyst at 600 °C measured under different conditions: pure O_2 at 600 °C, and humidified gas mixture (10% H_2O -90% O_2) at 600 °C.
 (D) $(\text{Pr}+\text{Ba})/\text{Co}$ ratio of PBC and $(\text{Pr}+\text{Ba})/(\text{Co}+\text{Ni}+\text{Fe}+\text{Mn}+\text{Cu})$ ratio of hybrid catalyst when measured under different conditions: pure O_2 at 300 °C, pure O_2 at 600 °C, and humidified gas mixture (10% H_2O -90% O_2) at 600 °C; the ratio of A-site and B-site cations was normalized by that obtained in O_2 at 300 °C.
 (E) Cross-sectional TEM micrograph of a conformal PNCFC-deposited PBC substrate; inset is EDS linear profile across the PNCFC coating to PBC substrate along the red arrow.
 (F) EDS mapping of Ba and Mn element distributions.
 (G and H) (G) HR-TEM and (H) SAED images of PNCFC coating (top) and PBC substrate (bottom).
 (I) Schematic illustration of Ba cation segregation from the bulk to the surface of PBC(001) following the conformal coating of PNCFC. The segregation energy of the Ba cation is calculated to be 2.36 eV for the PNCFC-coated PBC(001), compared to 0.48 eV for bare PBC(001).
 PCCs. As shown in **Figures 2D** and **2E**, the PBC electrode demonstrated a dramatic R_p deterioration rate of 0.317 $\Omega \text{ cm}^2$ per 100 h at 550 °C in wet air (3% H_2O). The high-entropy PNCFC coating efficiently enhances structural tolerance against steam, as indicated by an R_p deterioration rate of only 0.008 $\Omega \text{ cm}^2$ per 100 h for comparison. Even in the air with higher humidity (30% H_2O), the R_p of the PNCFC-PBC

203 hybrid electrode can remain relatively stable, which slightly increased from 0.553 to 0.607 Ω cm². The
204 surface electrode kinetics evolutions can be ascertained by the distribution of relaxation time (DRT) analysis
205 on the EIS spectra at different times. Each DRT curve seems to have at least three processes for the
206 electrode reactions, which correspond to low frequency (LF, $\leq 10^0$ Hz, mass transfer near the interface),
207 intermediate frequency (IF, 10^0 - 10^3 Hz, surface exchange processes), and high frequency (HF, $\geq 10^3$ Hz,
208 charge transfer), respectively.³⁸ The lasting increases in R_p of the PBC electrode were concentrated in the
209 intermediate frequency range of 10^2 - 10^1 Hz, while the extra low-frequency peaks at 10^{-1} - 10^{-2} Hz appeared
210 on the DRT curves of the hybrid electrode, which included the main R_p variations (**Figure 2F** and **Figure**
211 **S10**). Compared to the DRT curves of the PBC electrode, the extra low-frequency peaks at 10^{-1} - 10^{-2} Hz
212 are likely associated with the surface electrode reaction of PNMFC coating.³⁸ Thus, the PNMFC coating
213 may alter the mass transfer process on the electrode surface while ensuring that the PBC backbone
214 maintains structural integrity and fast bulk ion transfer.
215

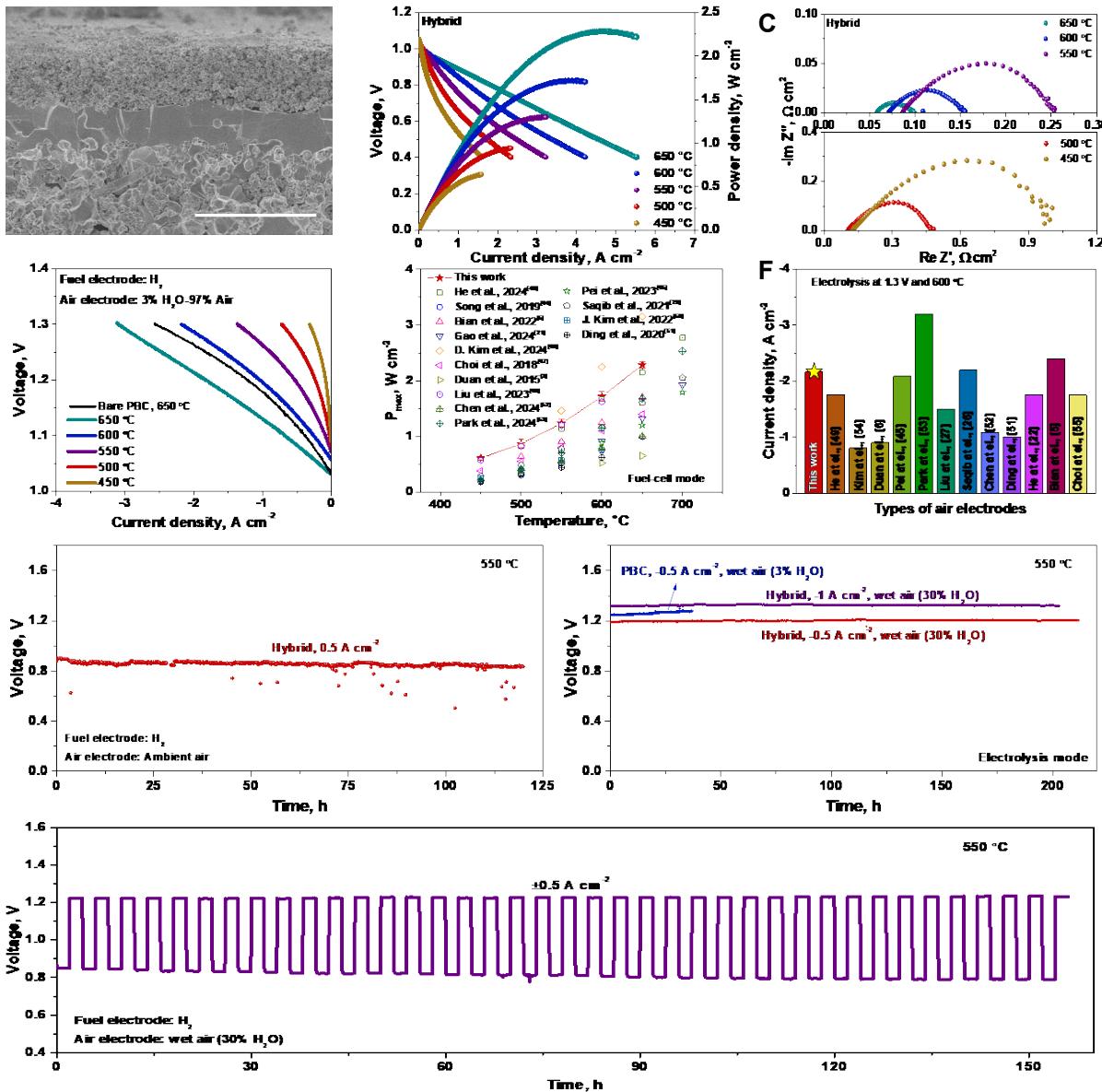
216 **Origin of the durability improvement**

217 Changing steam partial pressure ($p(H_2O)$) from 3 to 20 vol% makes a dramatic decrease in the R_p of
218 the hybrid electrode from 0.69 to 0.54 Ω cm² (**Figure 3A**, bottom). The electrochemical reactions of the
219 hybrid electrode can be deconvoluted by DRT analysis on the EIS in the air containing different $p(H_2O)$
220 (**Figure S11**). As fitted by the equation of $R_p = k(pH_2O)^m$, the reaction order of m value can determine the
221 rate-limiting step of isolated electrode reaction at each frequency range. The R_p of peaks at the low-
222 frequency range (reaction order m of 0.83) are more sensitive to $p(H_2O)$. Note that m=1, $H_{TPB}^+ + OH_{TPB}^- \rightarrow$
223 H_2O_{TPB} and $H_2O_{TPB} \rightarrow H_2O_{(g)}$ are highly associated with the key rate-limiting steps.⁴² These results
224 indicate that the electrochemical reactions of the PNMFC-PBC in wet air are likely controlled by mass
225 transfer and gas diffusion on the electrode surface. In addition, the impedances of the peaks at intermediate
226 and low frequencies were dramatically reduced, corresponding to the ionic diffusion and mass transfer
227 process, respectively. This result suggests that PNMFC coating can optimize the PBC electrode
228 electrochemical processes of ionic diffusion and mass transfer. The behavior of the bare PBC electrode is
229 distinctive from that of the hybrid electrode, which performed a sharp increase from 1.15 to 2.13 Ω cm²
230 under identical conditions (**Figure 3A**, top). Water-induced phase segregation may occur at the surface of
231 the PBC electrode, impacting the surface exchange kinetics of oxygen reactions. To prove this hypothesis,
232 the surface exchange coefficients (k_{chem}) of the PBC and PNMFC-PBC were further investigated by ECR
233 (**Figure S12** and **3B**). The hybrid electrode exhibits higher k_{chem} than the PBC electrode at 500-650 °C,
234 resulting in better electrochemical performance (**Figure S12**). A more obvious decrease of k_{chem} at 600 °C
235 was obtained on the PBC electrode compared to the hybrid electrode after the interaction with the steam
236 (10% H₂O) for 100 h (**Figure 3B** and **S13**). The corresponding surface chemistry of the PBC and hybrid
237 samples was investigated via X-ray photoelectron spectroscopy (XPS), quantified from Ba 3d_{5/2}, Co 2p_{3/2},
238 and O 1s spectra (**Figure 3C**, **S14**, and **S15**). Compared to the PBC sample measured in O₂ at 600 °C, the
239 surface Ba contents were induced for segregation from 62% to 66% with the steam (10% H₂O) injecting
240 (**Figure 3C** and **S14A**). Differing from PBC, the PNMFC-PBC performed a contrary tendency from 57%
241 to 54% after the identical steam pretreatments (**Figure 3C** and **S14B**), indicating that the Ba segregation
242 of PBC was suppressed by the PNMFC thin-film coating. Combined with the O1s results, a large amount
243 of Ba segregation at the PBC surface caused vacancy formation for the increased adsorbed oxygen (O_{ad})
244 (**Figure S15**). The phase structure of the PNMFC-PBC remains stable before and after the treatment of
245 humidified oxygen, as checked from the Ba 3d and O1s XPS (**Figure 3C** and **S15**). To more visually reveal
246 how the PNMFC coating inhibits the element segregation, we provided the surface atomic information of
247 PBC and hybrid samples by XPS analyses under different measured conditions of O₂ at 300 °C, O₂ at 600
248 °C, and 10% H₂O-90% O₂ at 600 °C, which are expressed as the ratio of A-site and B-site cations (**Figure**
249 **3D** and **Table S3**). The samples were firstly decarbonized for normalization in pure O₂ at 300 °C, then
250 heated to 600 °C, and finally exposed to the humidified O₂ (10% H₂O). The (Pr+Ba)/Co ratio of PBC
251 dramatically decreased in such an operating process due to the severe Ba segregation under

252 oxygen/steam-rich conditions. In contrast, the surface of the PNMCFc-PBC performed a relatively
253 balanceable A/B-site ratio, efficiently enhancing the structural stability of the PBC substrate.

254 To obtain the mechanism for excellent steam-tolerance durability of hybrid electrodes, a more detailed
255 morphology of the lattice maintenance and robust interface growth between PBC and PNMCFc was
256 examined by the focused ion beam (FIB)-TEM. PNMCFc was firstly deposited onto the surface of the dense
257 PBC substrate and then thermally calcined at 950 °C for 5 h. Shown in **Figure 3E** is the cross-sectional
258 TEM image of the PNMCFc deposited PBC dense substrate after the steam (10% H₂O) pretreatments at
259 600 °C. Fewer elements can be utilized for phase differentiation due to the high similarity between PNMCFc
260 and PBC phases and cation thermal diffusion during calcination, and the representative Ba and Mn
261 elements were chosen for linear scanning and mapping. The content of Mn and Ba at the interface is likely
262 caused by the cation thermal diffusion during high-temperature calcination at 950 °C for 5 h. EDS linear
263 profiles and mapping (**Figure 3E (inset), 3F, and S16**) demonstrated that the PNMCFc thin film was
264 conformally coated on the PBC substrate with enhanced durability against steam. According to the element
265 contents from the EDS results (**Figure S17**), the PBC maintains full structural integrity by protecting the
266 conformal PNMCFc coating against a steam-containing environment. As clearly observed by HR-TEM
267 (**Figure 3G**), the PNMCFc phase epitaxially grew and kept well-connected with the PBC substrate to form
268 a robust heterointerface. In addition, the PNMCFc layer maintains crystalline after interacting with steam,
269 of which a space distance of 2.24 Å corresponds to the (211) plane, while the different space distance of
270 3.90 Å belongs to the (100) plane of the PBC lattice. The marked ring (top) and spots (bottom) from the
271 selected area electron diffraction (SAED) can confirm that they can be assigned to the (200) plane of
272 PNMCFc, (210), and (200) planes of PBC, respectively (**Figure 3h**).

273 DFT calculations were performed to investigate the conformal coating of high-entropy PNMCFc on
274 PBC, demonstrating its effectiveness in enhancing PCC performance and stability by mitigating Ba
275 segregation (**Note S1**). As summarized in **Figure S18** and **Table S4**, initial screening calculations were
276 conducted to optimize the most plausible high-entropy bulk PNMCFc structure, yielding the most oxygen
277 vacancy formation energy (E_{vac}) at 2.04 eV. The bulk lattice parameter of PNMCFc was adjusted to match
278 PBC, assuming an ideal conformal coating. The recalculated E_{vac} values of 2.04 eV and 1.83 eV,
279 respectively, showed a 10% reduction, indicating improved bulk properties. Following the surface stability
280 analysis of PBC and PNMCFc surfaces (**Table S5** and **Figure S19**), the most stable surfaces were selected
281 for segregation energy and O 2p-band center calculations. As summarized in **Table S6**, the total O 2p-band
282 center for the hybrid PNMCFc/PBC(001) shifts closer to the Fermi energy (-2.51 eV) compared to the
283 PNMCFc(001) surface (-3.04 eV). For the coated PNMCFc, the O 2p-band center is calculated to be
284 -2.57 eV, highlighting the enhanced electronic interaction and more efficient surface oxygen kinetics.³⁷ The
285 shift indicates increased covalency of oxygen bonding at the interface, enhancing orbital overlap, charge
286 transfer, and oxygen-related surface reactions.⁴³ Besides elucidating surface oxygen kinetics by
287 understanding the O 2p-band center, we conducted the segregation energy calculations of Ba cations from
288 PBC to investigate the improved stability test results. As summarized in **Figures 3I, S19** and **Table S6**, the
289 segregation energy of Ba increases significantly from 0.48 eV (bare PBC) to 2.36 eV (PNMCFc/PBC),
290 verifying that Ba migration to the surface is energetically prohibitive after coating. In summary, the PNMCFc
291 coating suppresses Ba migration by increasing segregation energy, strengthening oxygen bonding
292 interactions, and acting as a physical barrier, resulting in improved structural stability of air electrodes. The
293 state-of-the-art conformal coating approach offers valuable guidance for the rational design of next-
294 generation high-entropy perovskite materials, paving the way for advancements in PCCs.



295
296 **Figure 4. Electrochemical performance and durability of the single cells with the hybrid electrode.**
297 (A) Cross-sectional SEM image of a fuel-electrode-supported single cell with the hybrid (PNMCFC-PBC)
298 electrode.
299 (B and C) (B) Typical I-V-P curves and (C) EIS of single cells with the hybrid electrode at 450-650 °C.
300 (D) Typical I-V curves of single cells with the bare PBC (black line) at 650 °C and hybrid electrodes at 450-
301 650 °C.
302 (E and F) (E) Comparisons of fuel cell P_{max} (**Table S7**) and (F) current densities at 1.3 V and 600 °C (**Table**
303 **S8**).
304 (G) Stability of the single cells at 550 °C applied a current density of 0.5 A cm⁻² (in fuel cell mode).
305 (H) current densities of -0.5 and -1.0 A cm⁻² (in electrolysis mode); (i) Reversible cycling operation at current
306 densities of ± 0.5 A cm⁻² at 550 °C.

308 **Single-cell performance and durability**

309 Shown in **Figure 4A** is the cross-sectional image of the single cell with the construction of Ni-BZCYYb
310 fuel electrode, BZCYYb electrolyte ($\sim 6 \mu\text{m}$), and hybrid (PNMCFC-PBC) air electrode. The I-V-P curves
311 were recorded by fueling H_2 to the fuel electrode and exposing the air electrode to ambient air. The PBC
312 electrode achieved a peak power density of 1.82 W cm^{-2} with an ohmic resistance (R_{ohm}) of $0.061 \Omega \text{ cm}^2$
313 and polarization resistance (R_p) of $0.044 \Omega \text{ cm}^2$ at 650°C (**Figure S20**). More outstanding electrochemical
314 performances were demonstrated on the cell with the hybrid electrode, showing the peak power densities
315 of $2.29, 1.72, 1.30, 0.94$, and 0.64 W cm^{-2} at $650, 600, 550, 500$, and 450°C , respectively (**Figure 4B**). For
316 reasonable comparisons, the R_{ohm} of the two cells kept identical, and the performance discrepancy may be
317 mainly attributed to the decreasing R_p , such as a lower R_p of $0.038 \Omega \text{ cm}^2$ for the hybrid electrode at 650°C
318 than PBC (**Figure 4C**). **Figure 4D** demonstrated the I-V curves of the electrolysis cell using wet air (3%
319 H_2O) as the oxidant at $450\text{-}650^\circ\text{C}$. The current densities of $-3.12, -2.17, -1.36, -0.72$, and -0.32 A cm^{-2} at
320 $650\text{-}450^\circ\text{C}$ and 1.3 V were achieved for the cell with the hybrid electrode, higher than that (-2.57 A cm^{-2} at
321 650°C and 1.3 V) of the cell with the PBC electrode. The impressive peak power densities found with the
322 hybrid electrode are better than most of the state-of-the-art air electrodes reported recently (**Table**
323 **S7**),^{3,5,21,26,44-53} such as $\text{BaCo}_{0.7}(\text{Ce}_{0.8}\text{Y}_{0.2})_{0.3}\text{O}_{3-\delta}$ (0.985 W cm^{-2} at 650°C),⁴⁴ $\text{PrBa}_{0.5}\text{Sr}_{0.5}\text{Co}_{1.5}\text{Fe}_{0.5}\text{O}_{5+\delta}$ (1.40 W cm^{-2} at 650°C)⁴⁷ and $\text{PrNi}_{0.5}\text{Co}_{0.5}\text{O}_{3-\delta}$ (1.7 W cm^{-2} at 600°C in wet O_2)⁵ (**Figure 4E** and **Figure S21**).
325 The interface engineering can further improve electrochemical performance, exemplified by
326 $\text{BaSc}_{0.1}\text{Ta}_{0.1}\text{Co}_{0.8}\text{O}_{3-\delta}$ perovskite air electrode via pulsed laser deposition (PLD) with a power density of 2.25 W cm^{-2} at 600°C .⁴⁶ The obtained top electrolysis performance at 1.3 V and 600°C (**Figure 4F** and **Table**
327 **S8**) signifies that the hybrid electrode exhibits not only an enhanced activity of oxygen reduction reaction
328 and excellent surface kinetics for oxygen evolution reaction.^{5,6,22,26,27,45,49,51-55}

330 **Figure 4G** demonstrates the stability of a single cell in fuel-cell mode using H_2 as the fuel and air as
331 the oxidant. For an extended duration of $\sim 120 \text{ h}$ under a current density of 0.5 A cm^{-2} at 550°C , the cell
332 showed no noticeable degradation, highlighting the great potential of robust air electrodes. Continuous
333 degradation was found on the voltage of the cells with the PBC electrode at -0.5 A cm^{-2} and 550°C under
334 wet air (3% H_2O) within 38 h (**Figure 4H**). As judged by XRD and Raman spectra, the formation of impurities
335 (likely $\text{Ba}(\text{OH})_2$) may lead to the deactivation of the PBC air electrode and electrolysis performance
336 degradation (**Figure S22**). When the PBC electrode was covered by the conformally high-entropy
337 PNMCFC, the electrolysis stabilities under the applied current densities of -0.5 and -1 A cm^{-2} at 550°C
338 were largely improved for over 200 h , even in the hash humidified air (30% H_2O) (**Figure 4H**). Combined
339 with the durable fuel-cell and electrolysis stability, a 2 h-fast reversible cycling was conducted at 550°C
340 and $\pm 0.5 \text{ A cm}^{-2}$, exhibiting relatively stable with low degradation rates (**Figure 4I**). Faradaic efficiency is a
341 critical standard for energy conversion from the H_2O to valuable H_2 production, theoretically defined as the
342 ratio of the H_2 production rate detected by gas chromatography (GC) to that calculated by electron transfer
343 number. When the applied current density was fixed at -1 A cm^{-2} , the Faradaic efficiencies were increased
344 from 81.8% to 91.1%, with the steam concentration increasing from 3% to 60% (**Figure S23**). Such results
345 were attributed to the high steam concentration, which can inhibit the electronic (electron-hole) conduction
346 and provide more protons via hydration. Therefore, developing highly steam-tolerance air electrodes via
347 high-entropy conformal coating can enhance the Faradaic efficiency for energy conversion and storage in
348 the high-concentration steam electrolysis mode in a system of protonic ceramic cells.

349 Conclusion

351 In summary, the electrocatalytic activity and stability of the PBC electrode have been significantly
352 enhanced by a wet-chemical solution infiltration of a high-entropy PNMCFC, which is more suitable for low-
353 temperature PCCs. As steam is commonly encountered in PCCs, the impact of humidity on the
354 electrocatalytic activity and structural stability of air electrodes is systematically investigated. Compared to
355 the bare PBC electrode, the surface oxygen exchange kinetics of the hybrid electrode can be maintained
356 without obvious deterioration by the high-entropy PNMCFC thin-film coating after interacting in wet air at
357 600°C for 100 h . The surface composition examined by XPS and R_p stability directly indicated that the
358 inherently robust interface between PBC and PNMCFC leads to performance and durability enhancements
359 by suppressing water-mediated segregation. Due to faster oxygen exchange kinetics and unique

360 architecture, the cell with the hybrid electrode obtained a higher power density of 1.30 W cm^{-2} and excellent
361 stability for 120 h at 550°C . Considering enhanced structural tolerance against steam, the hybrid electrode
362 with conformal high entropy coating also exhibits outstanding advantages in the performance and stability
363 of electrolysis modes and reversible cycling under a high-concentration humidified air (30% H_2O).
364

365 **METHODS**

366 The details of materials preparation, cell fabrication, materials characterization, and electrochemical
367 measurements are provided in Supplemental Experimental Procedures.

368

369 **RESOURCE AVAILABILITY**

370 ***Lead contact***

371 Further information and requests for information and resources should be directed to and will be fulfilled
372 by the lead contact, Yu Chen (eschenyu@scut.edu.cn).

373

374 ***Materials availability***

375 The new PNMCFc coating catalysts generated in this study will be made available on request.

376

377 ***Data and code availability***

378 The data generated during this study are available in the main text and the supplemental information.

379

380

381 **ACKNOWLEDGMENTS**

382 This work was financially supported by the Introduced Innovative R&D Team of Guangdong (2021ZT09L392),
383 the National Natural Science Foundation of China (22179039 and 22005105), the Fundamental Research Funds
384 for the Central Universities (2022ZYGXZR002), the Pearl River Talent Recruitment Program (2019QN01C693),
385 the Guangdong Basic and Applied Basic Research Foundation (2021A1515010395), and Zijin Mining Group Co.,
386 Ltd (5405-ZC-2023-00008). YMC acknowledges the National Science and Technology Council (NSTC Grant No.
387 111-2221-E-A49-003-MY3), the National Center for High-performance Computing (NCHC), and the Higher
388 Education Sprout Project of the National Yang Ming Chiao Tung University and Ministry of Education (MOE),
389 Taiwan. DFT calculations were performed using the resources of the Center for Functional Nanomaterials, which
390 is a U.S. DOE Office of Science Facility, at Brookhaven National Laboratory under Contract No. DE-SC0012704.

391

392 **AUTHOR CONTRIBUTIONS**

393 Conceptualization, Y.C.; methodology, Y.C. and Y.L.; investigation, F.H., H.L., Y.X., K.S., and F.Z.; writing—
394 original draft, F.H., Y.C., and Y.M.C.; writing—review & editing, Y.C., and Y.M.C.; funding acquisition, Y.L.,
395 Y.M.C., and Y.C.; resources, Y.M.C., and K.S.; supervision, Y.L., Y.M.C., and Y.C.

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397 **DECLARATION OF INTERESTS**

398 The authors declare no competing interests.

400 **SUPPLEMENTAL INFORMATION**

401 Supplemental Information can be found online at.

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