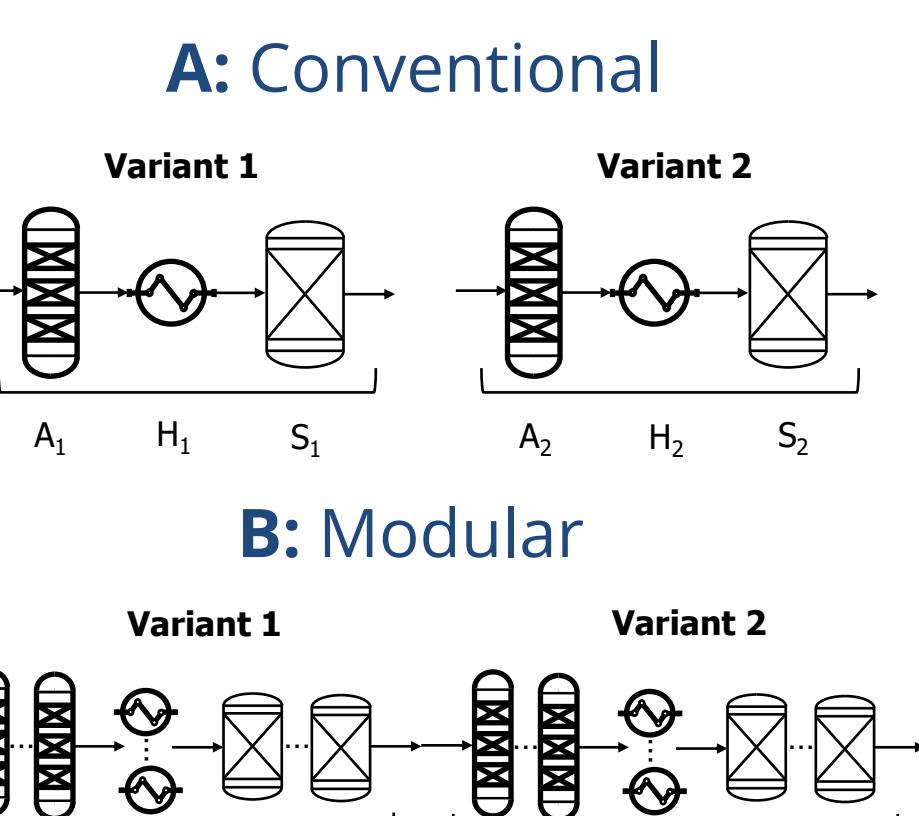


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Motivation[1]

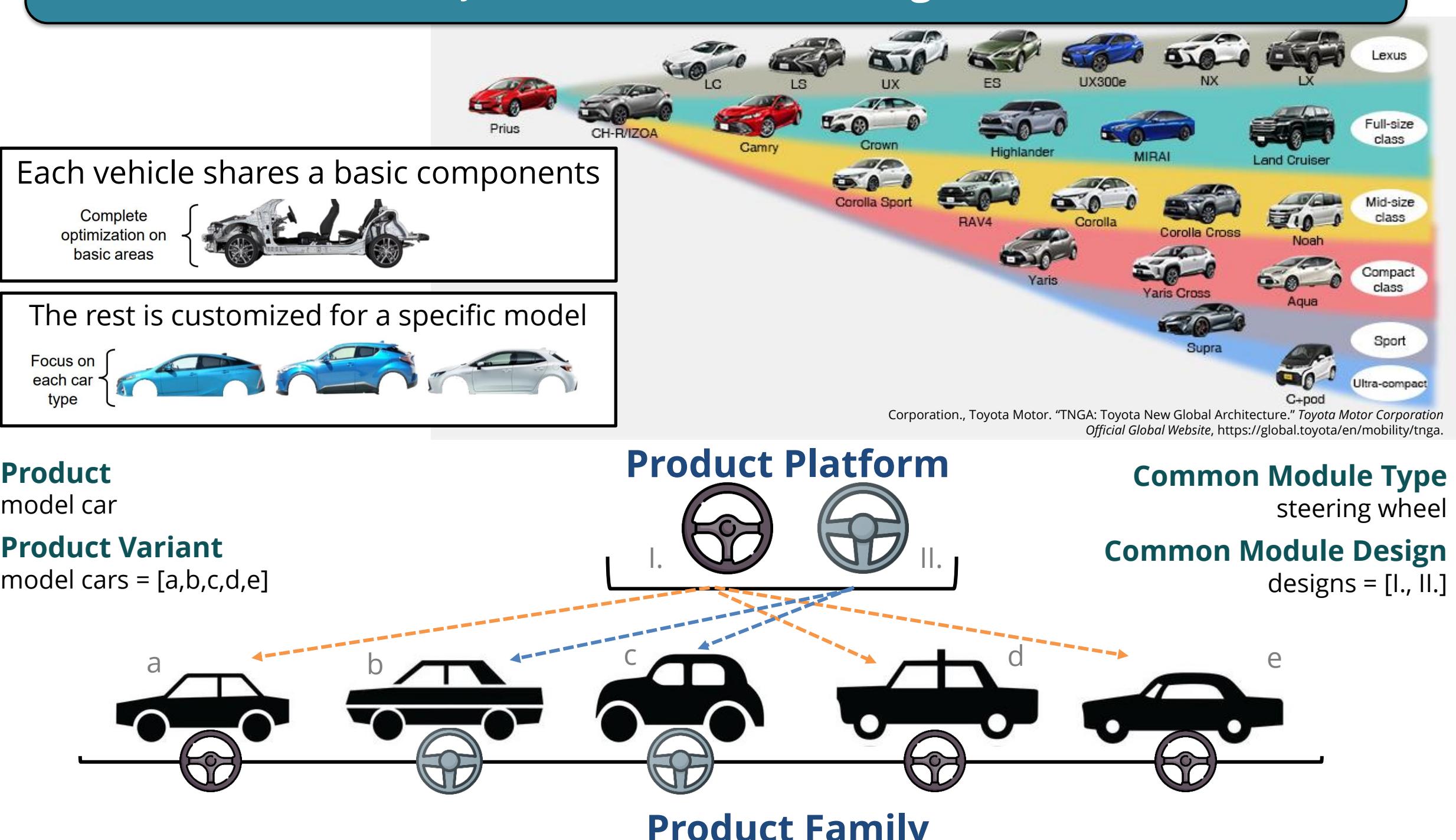
Optimally deploy a process system across decentralized sites with different geographical, environmental and operating requirements.



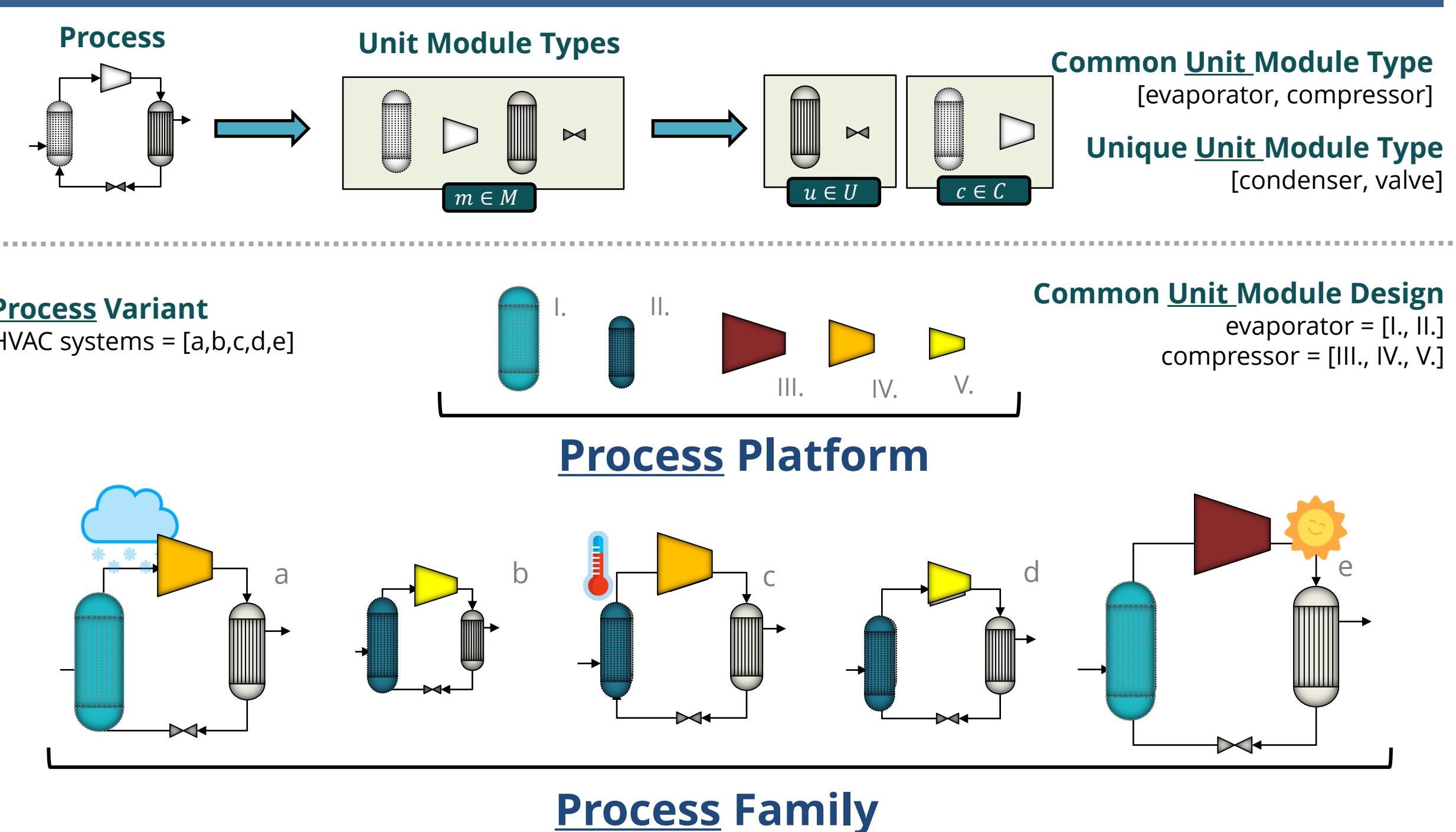
Process Family Design includes the benefits of both.

Product Family Design[2]

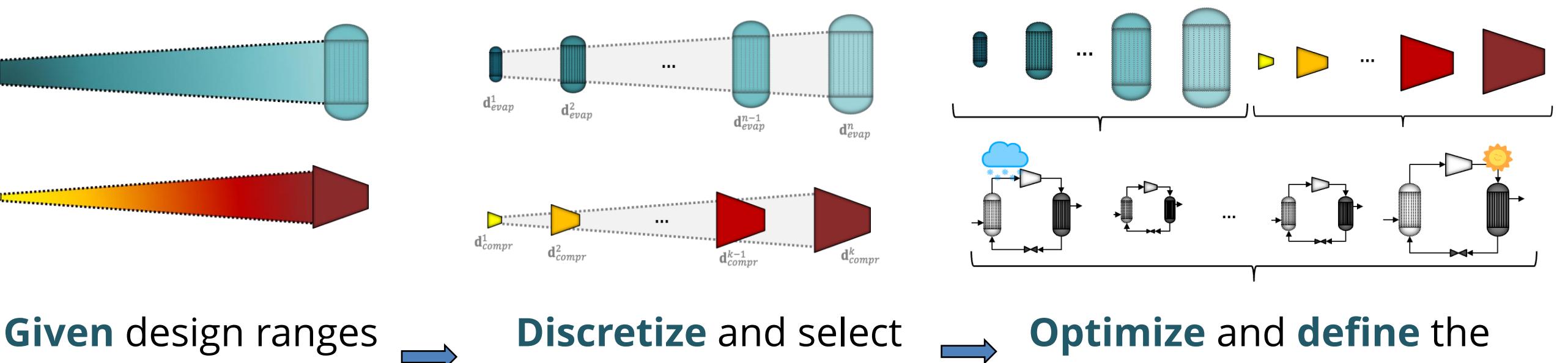
A set of products that share one or more common "element(s)" yet target a variety of different market segments



Mapping to PSE



Discretization Approach[3,4]



Given design ranges $\forall c \in C$ \rightarrow Discretize and select candidate designs L_c \rightarrow Optimize and define the alternatives A_v

Decision Variables (1) which candidate designs $l \in L_c$ are in the platform \mathcal{P} ? $\rightarrow z_{c,l}$
 (2) which $a \in A_v$ is assigned to each variant $v \in V$? $\rightarrow x_{v,a}$

$$\min. \sum_{v \in V} w_v \sum_{a \in A_v} p_{v,a} x_{v,a} \quad (1.1)$$

Minimize the total weighted cost of all variants in the process family

$$\text{s.t. } \sum_{l \in L_c} z_{c,l} \leq M_c \quad \forall c \in C \quad (1.2)$$

Select units for manufacture

$$\sum_{a \in A_v} x_{v,a} = 1 \quad \forall v \in V \quad (1.3)$$

Select 1 alternative

$$x_{v,a} \leq z_{c,l} \quad \forall v \in V, a \in A_v, (c, l) \in Q_a \quad (1.4)$$

Alternative must be manufactured

$$z_{c,s} \in \{0,1\} \quad \forall c \in C, l \in L_c \quad (1.5)$$

$$0 \leq x_{v,a} \leq 1 \quad \forall v \in V, a \in A_v \quad (1.6)$$

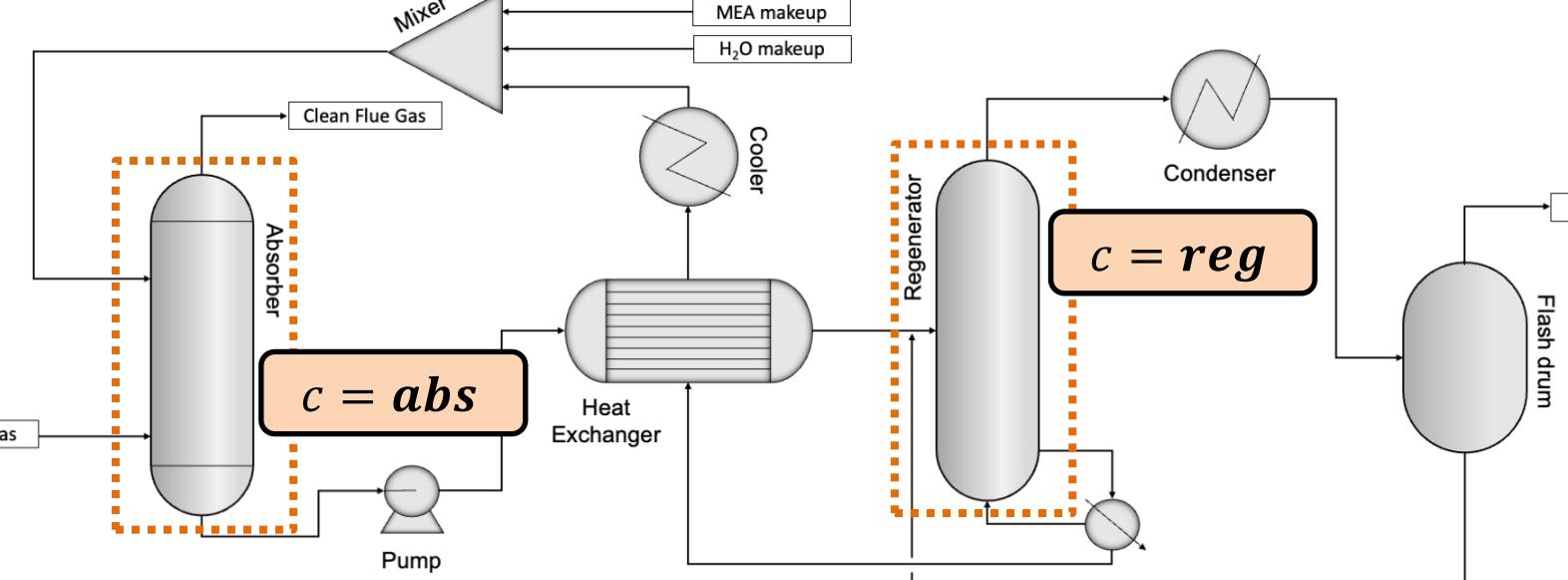
At optimality, the solution will converge to binary under mild assumptions^[5]

ReVelle, Charles S., and Ralph W. Swain. "Central facilities location." Geographical analysis 2.1 (1970): 30-42.

Case Study[7]

Carbon Capture

Monoethanolamine (MEA)

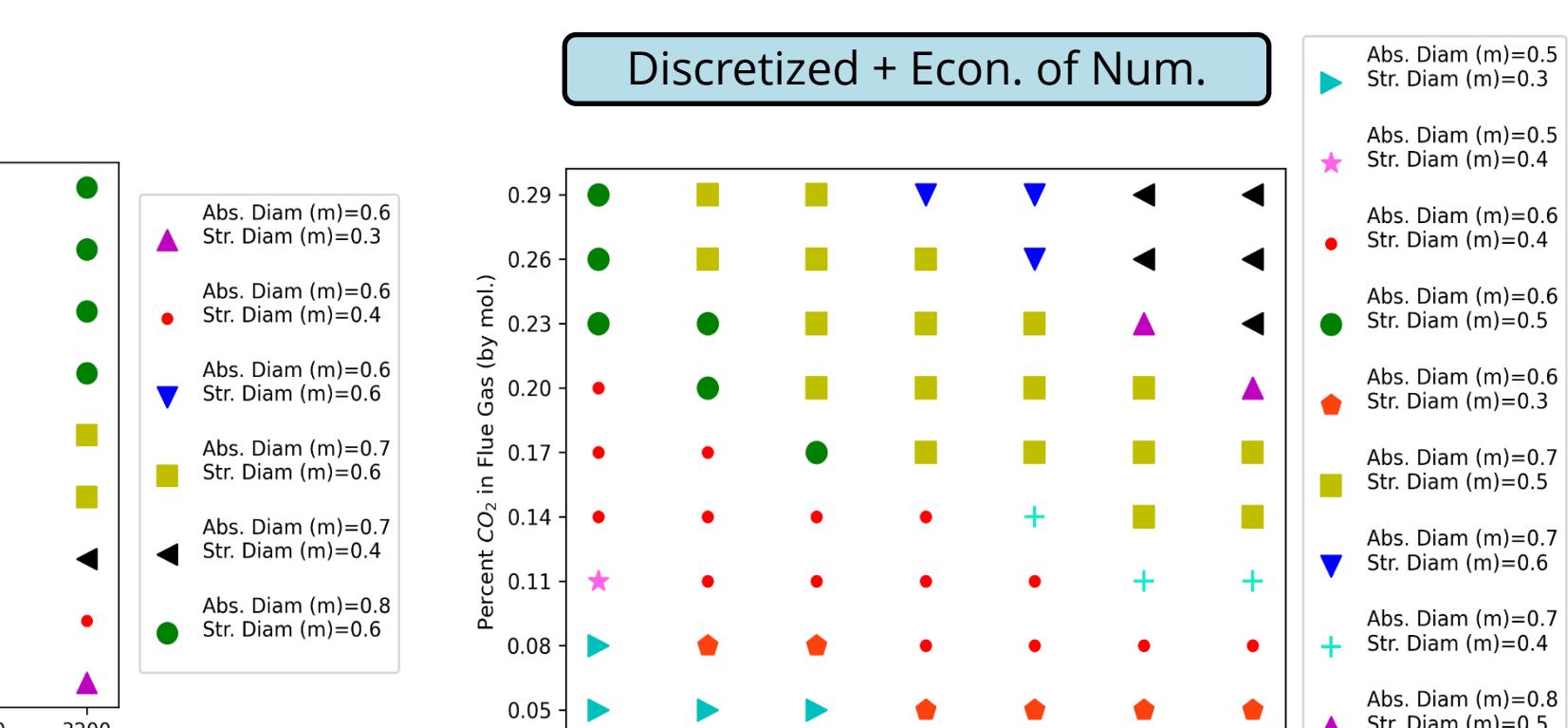


- 1) Diam. of the Absorber
- 2) Diam. of the Regenerator

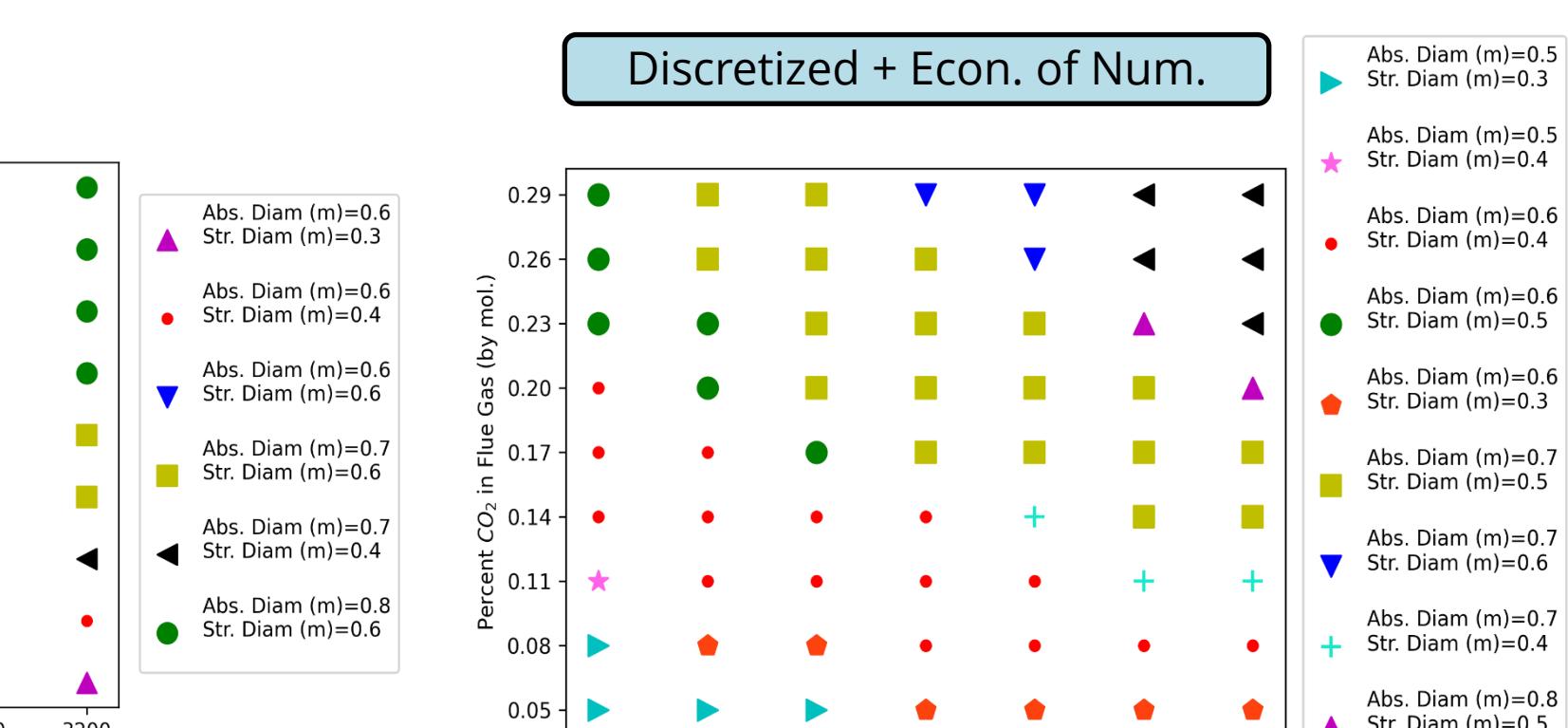
$C = [abs, reg]$

Results

Discretization



Objective: \$75.4M



Objective: \$72.5M

- In the discretization formulation, we need to specify M_c .
- In the EoN formulation, we determine M_c as a part of the optimization.
- \$2.38M annual cost savings compared to discretization approach (~3.3%).
- Considering only capital costs, we gain 26.8% annual cost savings.

Conclusions

- ✓ Reduced manufacturing costs.
 - Economies of numbers (modular concepts at unit level).
 - Economies of scale (customization to design range).
- ✓ Multiple scalable optimization formulations.
- ✓ Economies of Numbers formulation adds cost savings and determines size of platform.
- ✓ Increased annual cost savings using the new approach.

Future Work

- ❑ Perform a rigorous costing analysis for each design approach.
- ❑ Incorporate Econ. of Num. and decomposition for ML Surrogates.
- ❑ Use the explicit equation oriented system model within formulation.

References

- [1] Baldea, M., Edgar, T. F., Stanley, B. L., & Kiss, A. A. (2017). Modular manufacturing processes: Status, challenges, and opportunities. *AIChE journal* 63(10), 4262-4272.
- [2] Simpson, Timothy & Siddique, Zahid & Iiao, Roger. (2006). Product Platform and Product Family Design: Methods and Applications. 10,1007/978-1-4614-7937-6.
- [3] Zhang, C., et al. (2021). Optimization-based Design of Product Families with Common Components. *14th International Symposium on Process Systems Engineering*.
- [4] Stinchfield, G., et al., "Optimization-based Approaches for Design of Chemical Process Families Using Machine Learning Surrogates" in proceedings, FOCAP/CPC 2023.
- [5] Gazzaneo, V., Watson, M., Ramsayer, C. B., Kilwein, Z. A., Viana, F. V., J. *Adv. Manuf. Process.* 2022, e10115. <https://doi.org/10.1002/amp2.10115>
- [6] Weber, Robert S., and Lesley J. Snowden-Swan. "The economics of numbering up a chemical process enterprise." *Journal of Adv. Manuf. & Processing* 1.1-2 (2019): e10011.
- [7] Carbon capture simulation for industry impact (CCSI), v3.2.1. MEA Steady state model. <https://github.com/CCSI-toolset/MEA/ssm/releases/tag/23.2.1> (2022).

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