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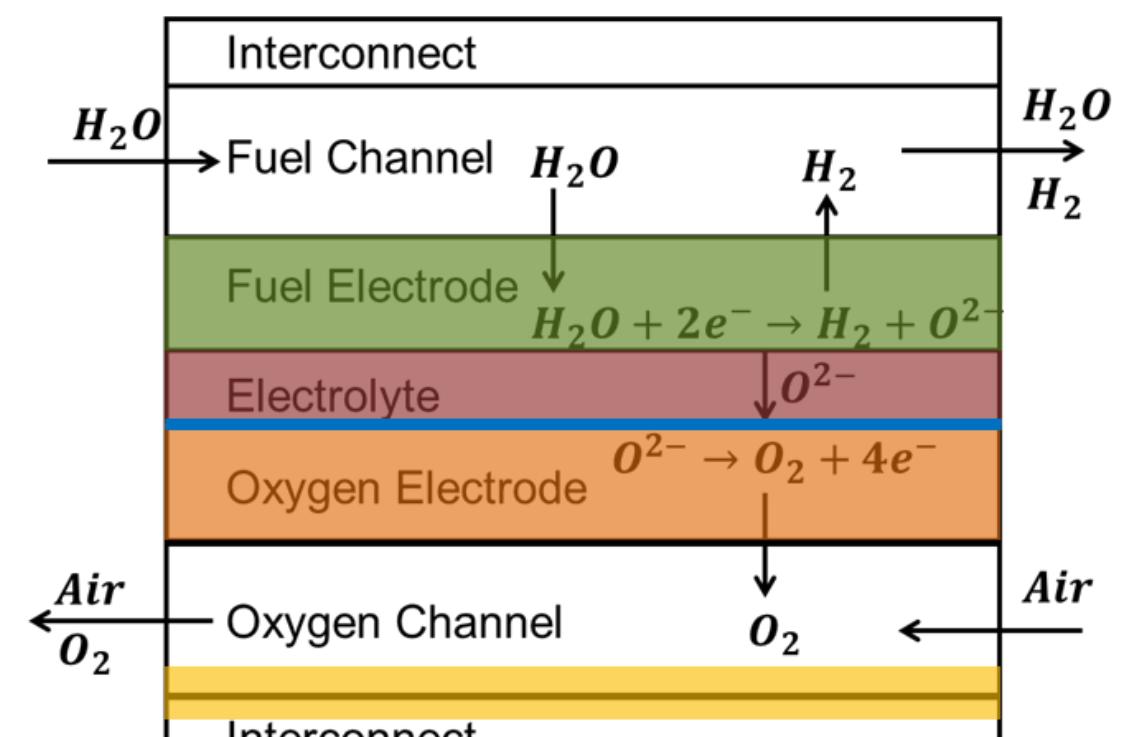
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Background

Solid-Oxide Cells (SOC) that produce H₂ through steam electrolysis, at high theoretical efficiency.

Slow microstructure degradation phenomena decrease efficiency and can lead to premature failure of the SOC.

Reducing degradation is often considered a materials design problem.



Combatting degradation through long-term optimization

Optimization minimize $f(x)$



First Principles SOEC Flowsheet
• 2D, non-isothermal cell model
• Detailed BOP equipment models

Microstructure Degradation
Oxygen electrode degradation mechanisms
Chromium oxide scale growth
Lanthanum zirconate scale growth
Fuel electrode degradation phenomena
Ni agglomeration and volatilization
Electrode degradation phenomena
YSZ electrolyte delamination

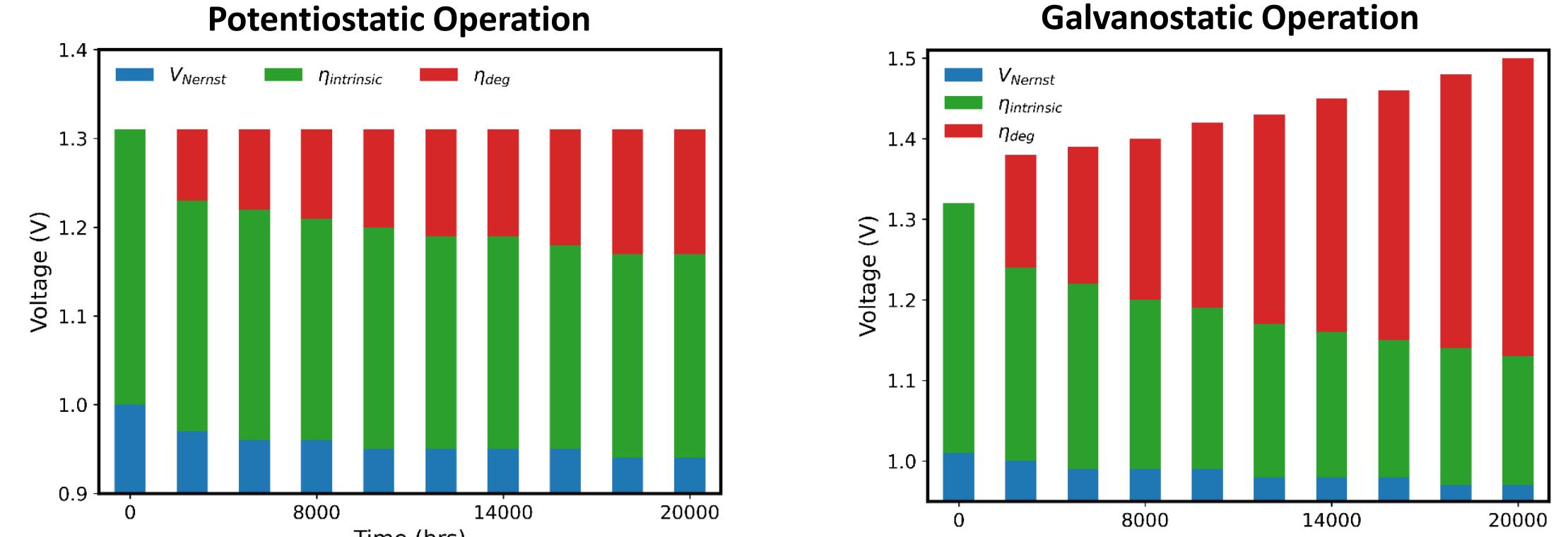
Long-term Performance Degradation

Voltage losses increase the required voltage for electrolysis

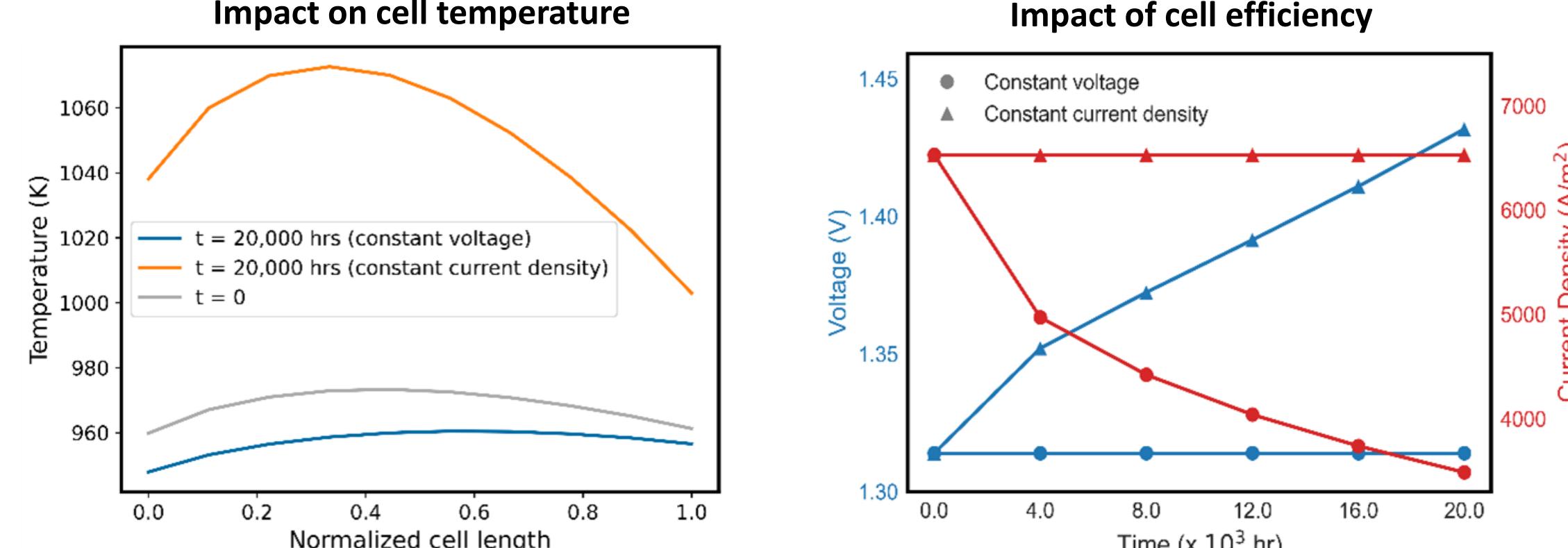
$$V_{cell} = V_{Nernst} + \eta_{activation} + \eta_{Ohmic} + \eta_{degradation}$$

Thermodynamic Minimum Intrinsic Losses Degradation Losses

Distribution of degradation losses after 20,000 hours of degradation



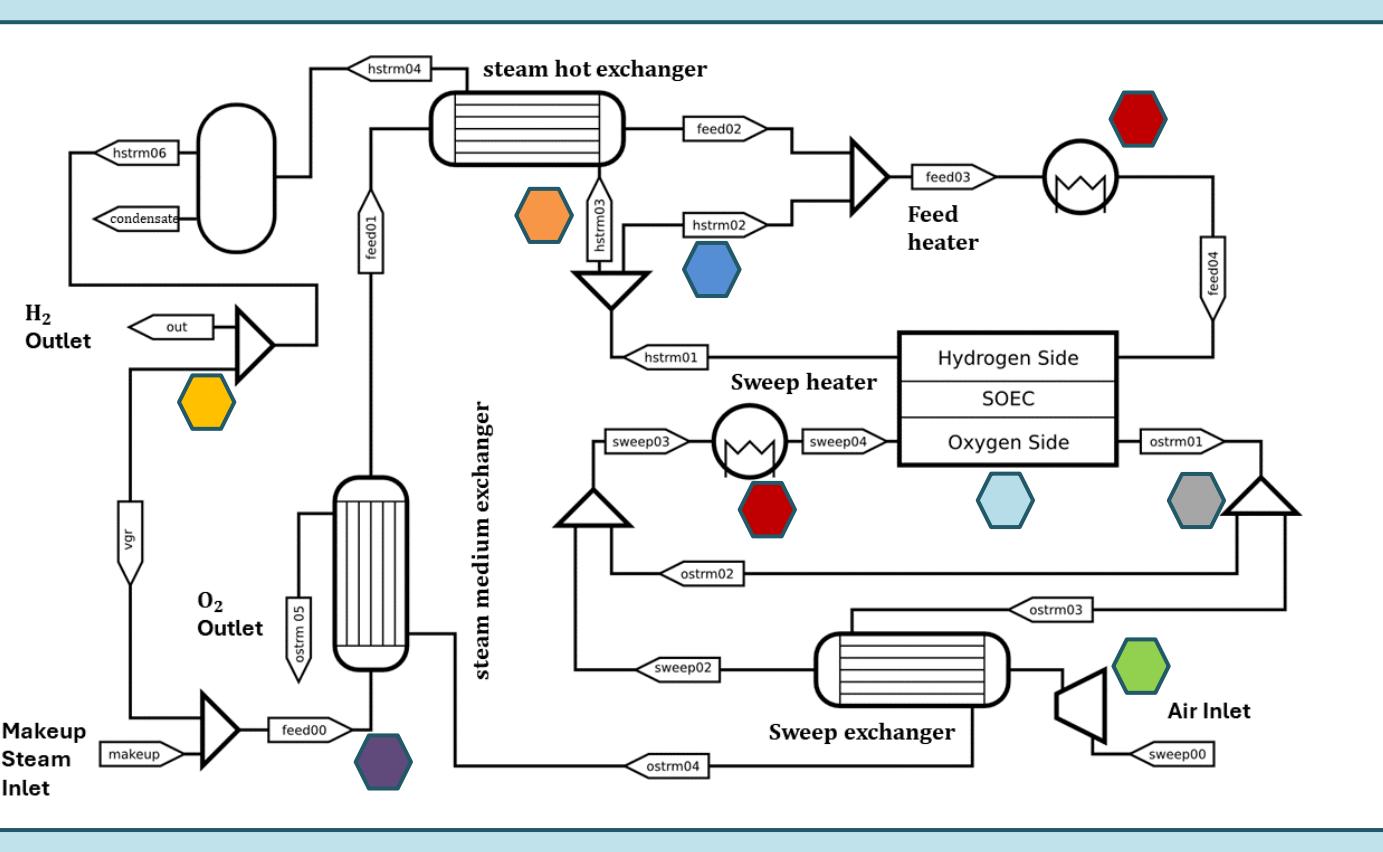
Impact of degradation on cell performance



Operating Decisions

1. Flowsheet and cell level setpoints

Symbol	Decision Variable
Cell Potential / Current Density	
Feed recycle splitter outlet H ₂ O mole fraction	
Feed / Sweep electric heater duties	
Condenser splitter recycle split fraction	
Feed medium exchanger inlet flowrate	
Feed recycle splitter split fraction	
Sweep recycle splitter split fraction	
Sweep blower molar flowrate	



Cell degradation impacts the operation of the Balance of Plant (BOP) and decreases system efficiency

2. Choice of long-term operating mode

Potentiostatic (Constant Voltage) Galvanostatic (Constant H₂ Production) Flexible

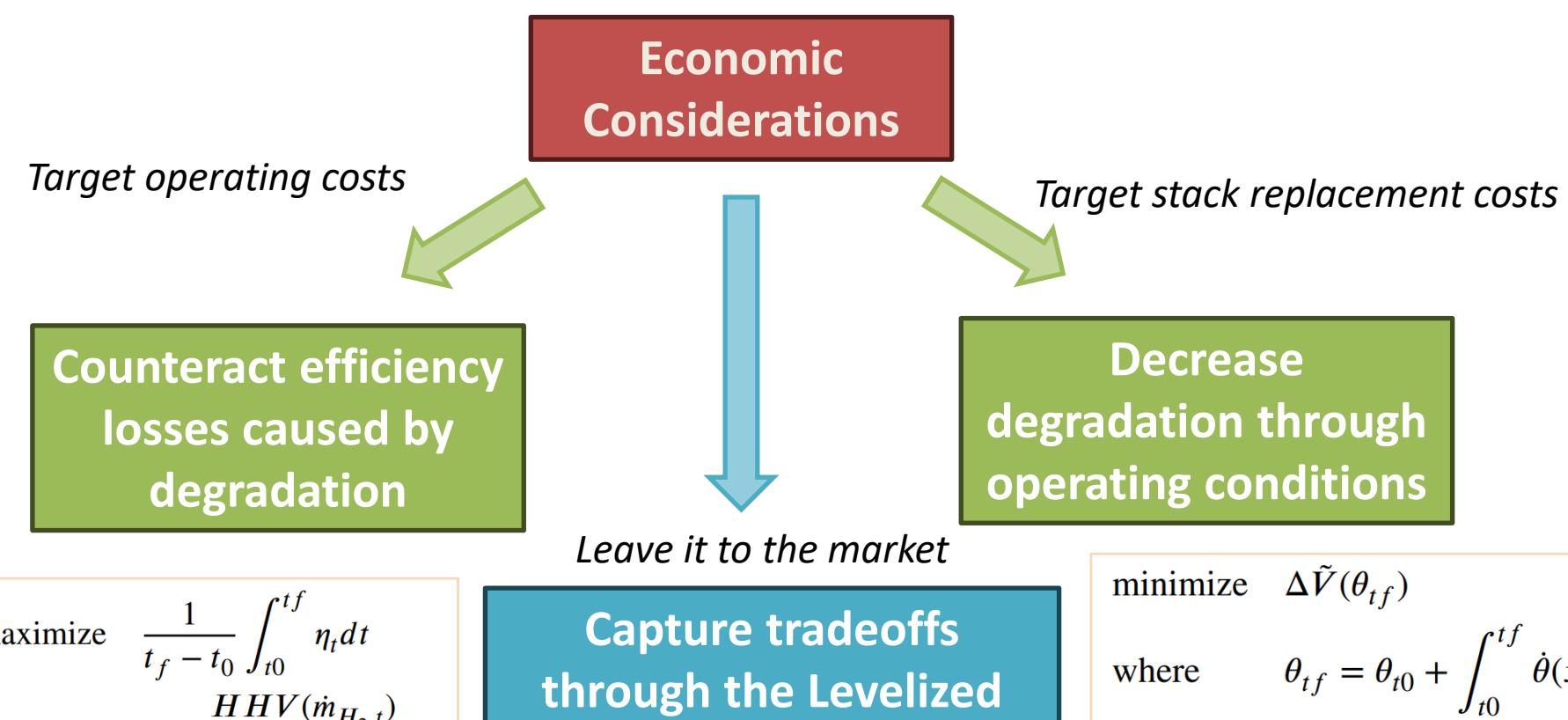
A flexible mode of operation allows both potential and current density to vary simultaneously

3. Selection of replacement schedule

$$CAPEX = CC_{BOP} + n_{stack} CC_{Stack}$$

Efficiency loss due to degradation can be counteracted by more frequent stack replacements.

Optimization Formulation



Algorithm to determine optimal replacement schedule

- Parallelly re-optimize stack for different candidate replacement schedules.
- Avoids binary decision variables.
- Stacks replaced when $\Delta\bar{V}_{deg} > 50\%$.
- NLP subproblems solved using ipopt.

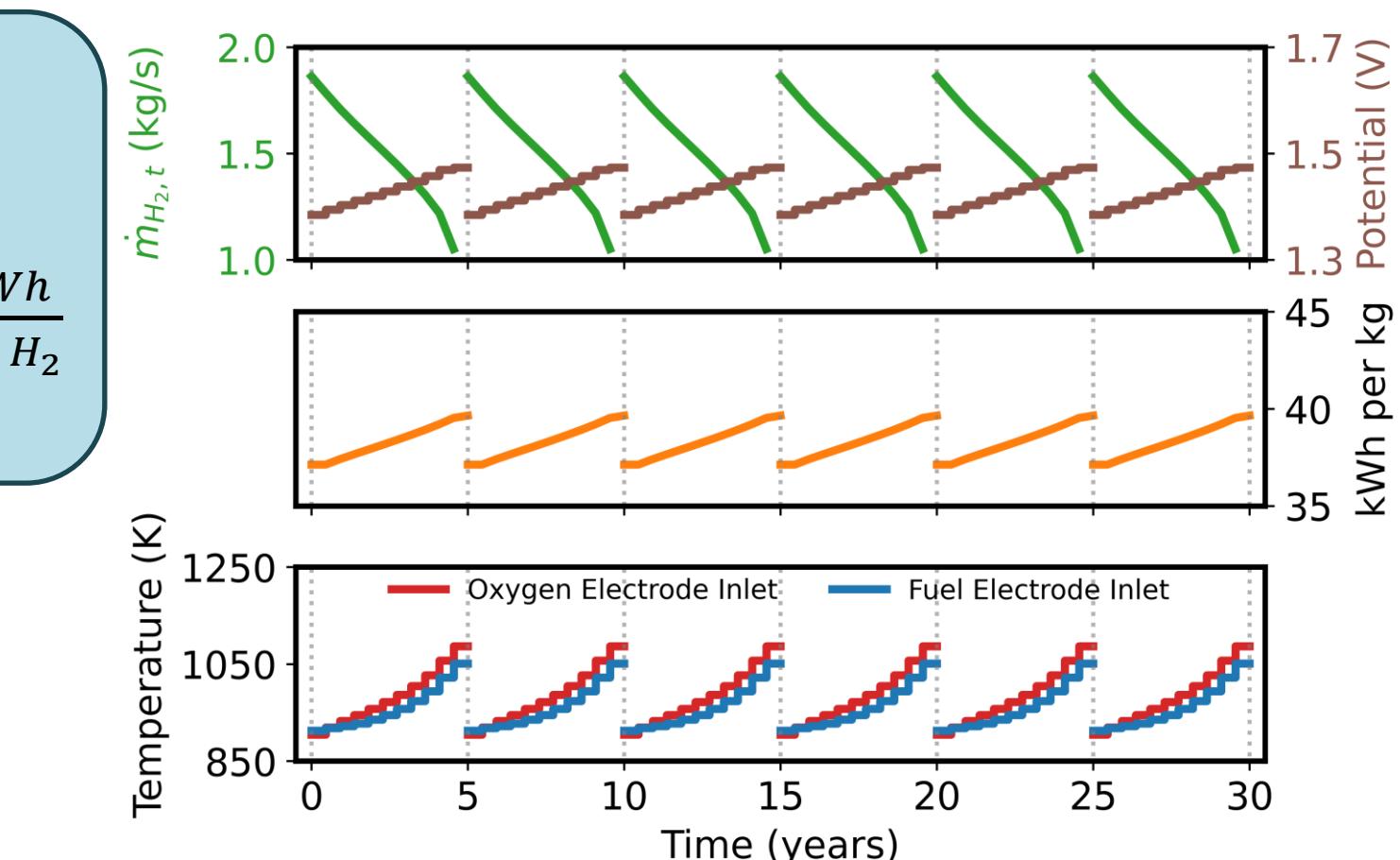
Selected Operating Schedules

Electricity Price = 0.03 \$/kWh

Replacement time = 5 years

Sp. Energy Consumption = 38.0 $\frac{\text{kWh}}{\text{kg H}_2}$

Degradation rate = 3% /khr



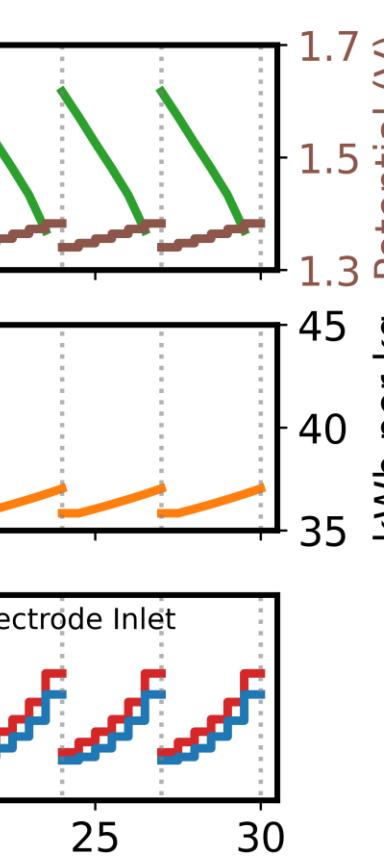
Stack replacement costs dominate the LCOH in markets with low energy costs

Electricity Price = 0.03 \$/kWh

Replacement time = 3 years

Sp. Energy Consumption = 35.8 $\frac{\text{kWh}}{\text{kg H}_2}$

Degradation rate = 4% /khr



Energy costs dominate and shorter replacement times are observed

Given electricity market information, this method automatically derives optimal replacement schedules and operating changes within a stack lifetime that minimize the leveled cost of H₂ (LCOH).

Takeaways

Balancing tradeoffs

The interplay of short-term efficiency and long-term degradation, has a significant impact on the cost of H₂ production by an SOEC system.

Two distinct consequences of degradation

Cell degradation impacts both system efficiency and thermal characteristics.

Higher temperatures induced by degradation result in accelerated

Insights from Optimization

- Combating degradation is both a materials design and an operational optimization problem.
- The tradeoff between efficiency and replacement frequency is captured.
- Flexible long-term operating mode can result in lower LCOH when compared to traditional galvanostatic and potentiostatic operation.

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