

Algae Biomass Summit 2022

Mass transfer coefficients, k_L , and air-CO₂ ingassing rates in 3.4 m² and 1-acre raceway ponds

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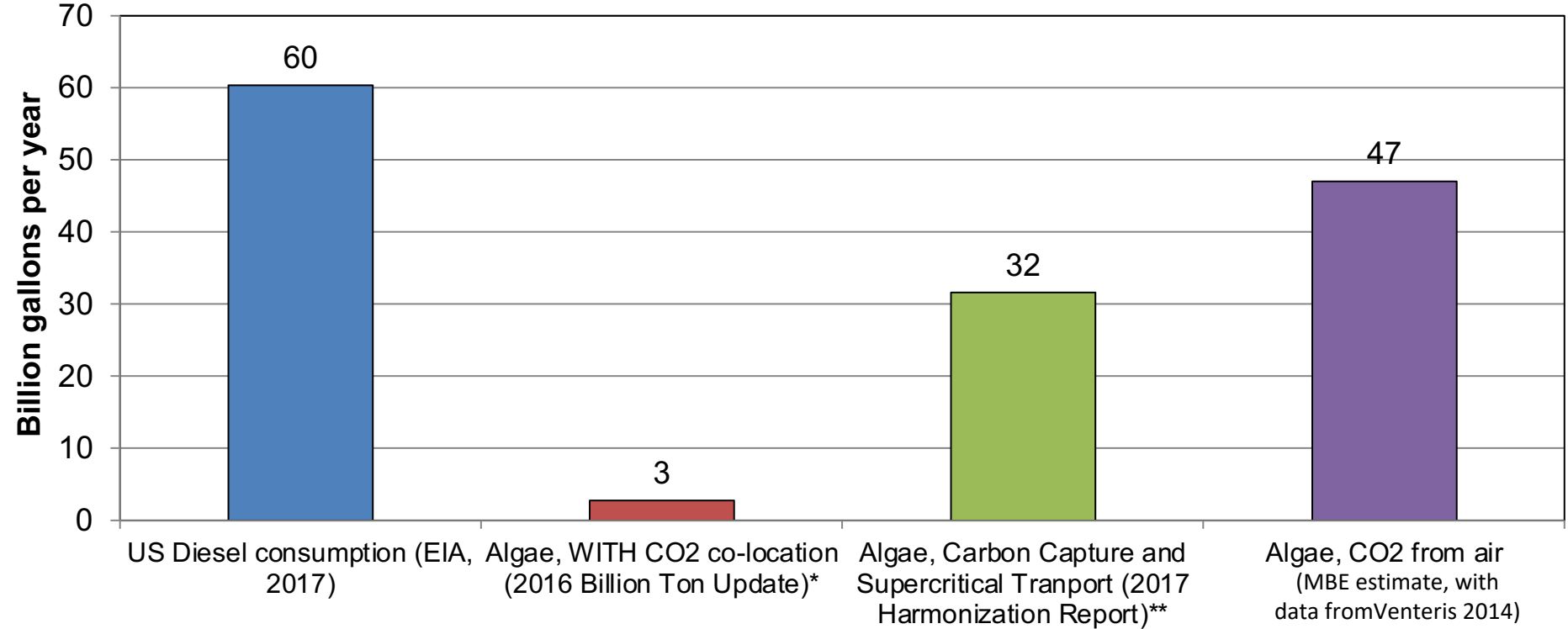
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Why grow algae on CO₂ from air?

CO₂ point-source co-location limits algal resource potential to less than 5 BGY

Direct, in-pond air-CO₂ capture can increase resource potential nearly 10-fold



*freshwater and saltwater scenario, present productivity. Assume 0.35 g diesel/gas per g of biomass.

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The CO_2 mass-transfer rate, J_{CO_2} , is proportional to the mass transfer coefficient, k_L , and the 'driving force' for mass transfer. E accounts for chemical reactions.

$$J_{\text{CO}_2} [=] \frac{\text{g C}}{\text{m}^2\text{-day}} = k_L * \underbrace{\left(P_{\text{CO}_2}^{\text{air}} * H - C_{\text{CO}_2}^{\text{bulk}}(x = \delta) \right)}_{\text{Driving force}} * \underbrace{E}_{\text{Enhancement factor (if reactions present)}}$$

\downarrow Piston velocity \downarrow Back pressure

When $C_{\text{CO}_2}^{\text{bulk}}(x = \delta) > P_{\text{CO}_2}^{\text{air}} * H$:

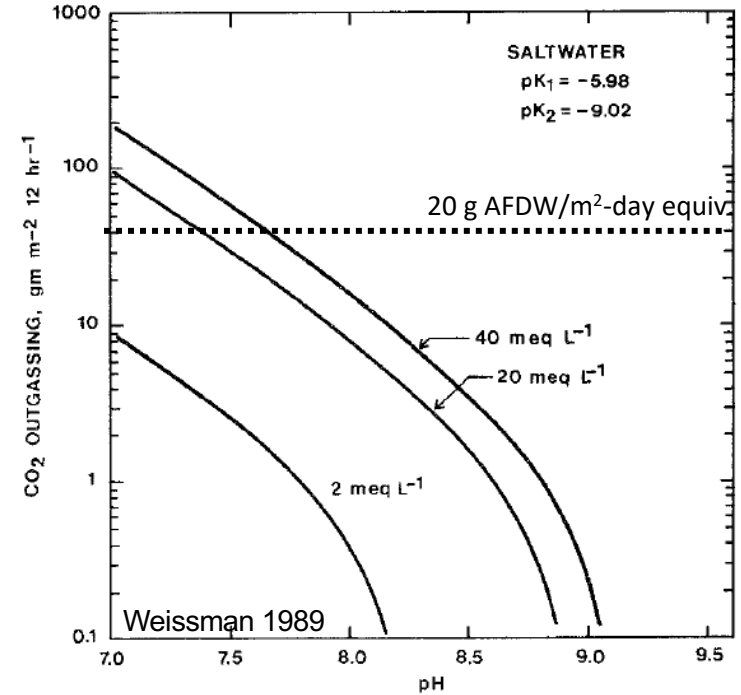
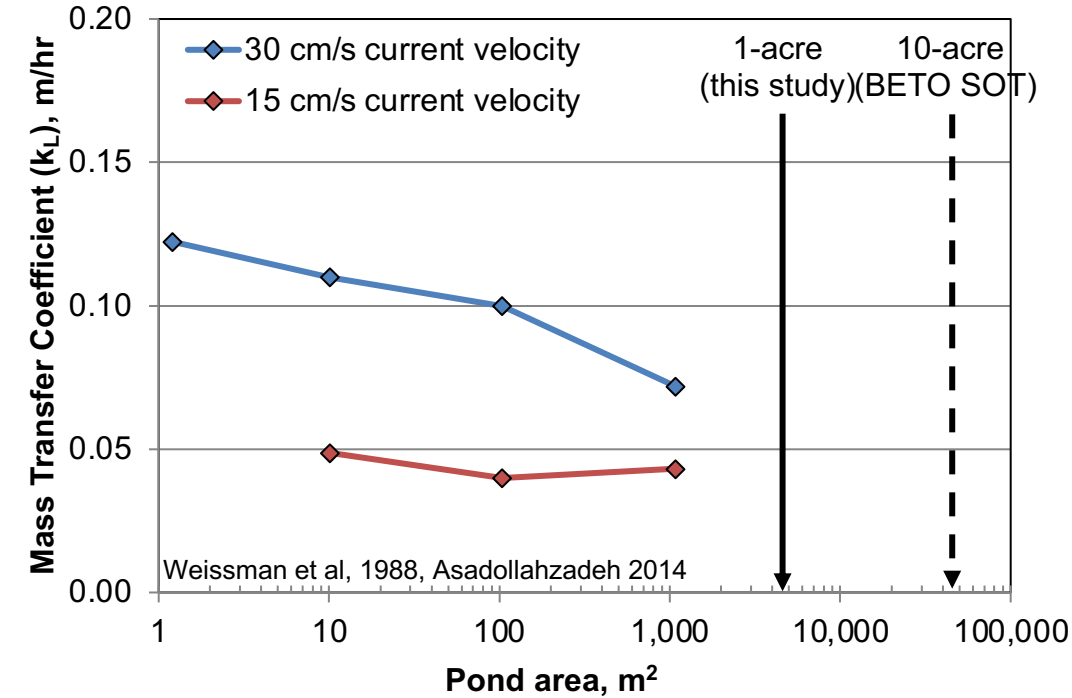
- Driving force is negative
- CO_2 lost from pond to atmosphere
- Net CO_2 'outgassing' rate

When $C_{\text{CO}_2}^{\text{bulk}}(x = \delta) < P_{\text{CO}_2}^{\text{air}} * H$

- Driving force is positive
- Air- CO_2 transfer from atmosphere to pond
- Net CO_2 'ingassing' rate
- Influence of reactions accounted with 'E'

Outgassing rates must be minimized to achieve high carbon utilization efficiency
Ingassing rates of are interest for direct algae air- CO_2 capture

k_L is between 0.05-0.1 m/hr for small ponds, unmeasured in large (1-acre +) ponds
 At elevated alkalinity, pH 7.5 – 8.0, CO₂ outgassing rates approach the daily gain in biomass

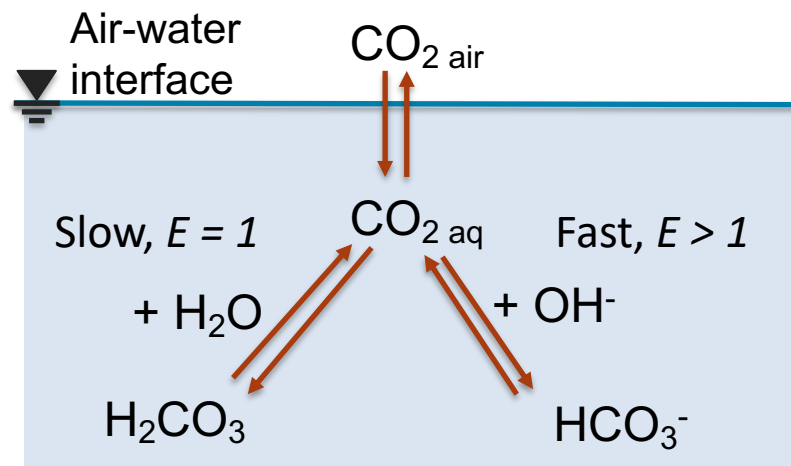


Influence of k_L , pond scale on the ingassing rate is uncertain, dependent on E

At elevated pH, the $\text{CO}_{2,\text{aq}} + \text{OH}^-$ reaction pathway appreciably increases air- CO_2 flux, known as chemical enhancement

Without chemical enhancement, $E = 1$, and air- CO_2 flux is given by:

$$J_{\text{CO}_2} = k_L * (C_{\text{CO}_2}^{\text{sat}} - C_{\text{CO}_2}^{\text{bulk}}) * E$$



Where:

$C_{\text{CO}_2}^{\text{sat}}$ = $\text{CO}_{2,\text{aq}}$ at the air-water interface, in equilibrium with the gas phase, $\sim 10 \mu\text{M}$

$C_{\text{CO}_2}^{\text{bulk}}$ = $\text{CO}_{2,\text{aq}}$ in pond 'bulk', $\sim 0 \mu\text{M}$ at $\text{pH} > 10$

k_L = mass transfer coefficient, $\sim 0.1 \text{ m/hr}$ for ponds, a measure of turbulence as it relates to mass transfer

Under non-enhanced ($E = 1$) conditions:

$$J_{\text{CO}_2} = 0.1 \frac{\text{m}}{\text{hr}} (10 - 0 \mu\text{M}) = 0.3 \frac{\text{g C}}{\text{m}^2 \text{day}} \approx 0.6 \frac{\text{g AFDW}}{\text{m}^2 \text{day}}$$

E must be ~ 30 to support $20 \text{ g AFDW/m}^2\text{-day!}$

Depending on the assumed mass-transfer regime, estimates for E range from 2 to 40 at $\text{pH } 10.5$

Hypothesis: E is sufficient to support high rates of carbon uptake, at a biologically compatible high pH

Approach – Identify conditions to meet the target air-CO₂ flux

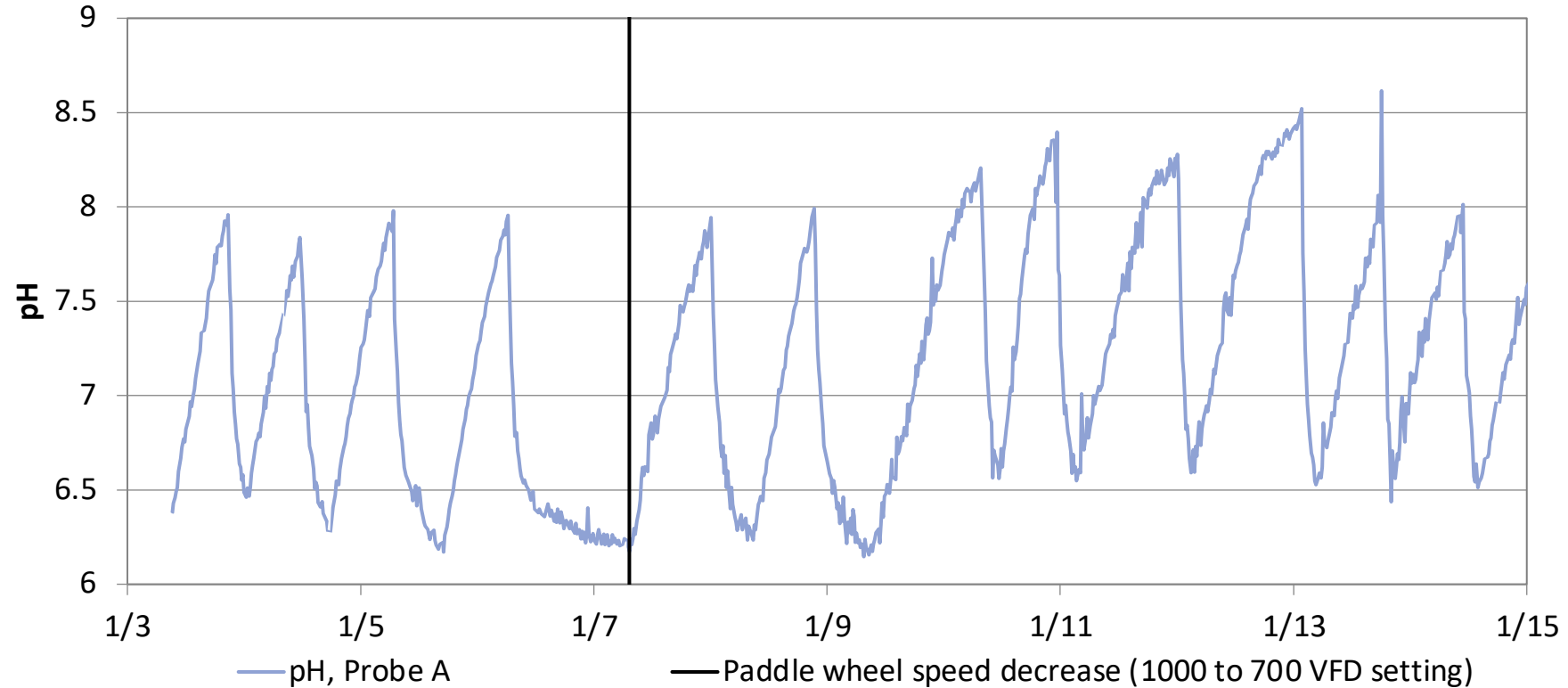
- Measure air-CO₂ exchange rates via abiotic (without algae) trials in 1-acre ponds.
 - k_L is measured in ‘outgassing trials’, by supersaturating the pond with CO₂, then measuring the rate of pH increase.
 - Air-CO₂ flux, J_{CO_2} , at elevated pH is measured by displacing the pond from air-equilibrium with a strong base, then measuring the rate of return to equilibrium (pH decrease)
- Compare ingassing rates over a wider current velocity range in more easily managed 3.4 m² ponds
- Compare experimental results to model predictions to identify the appropriate mass-transfer model



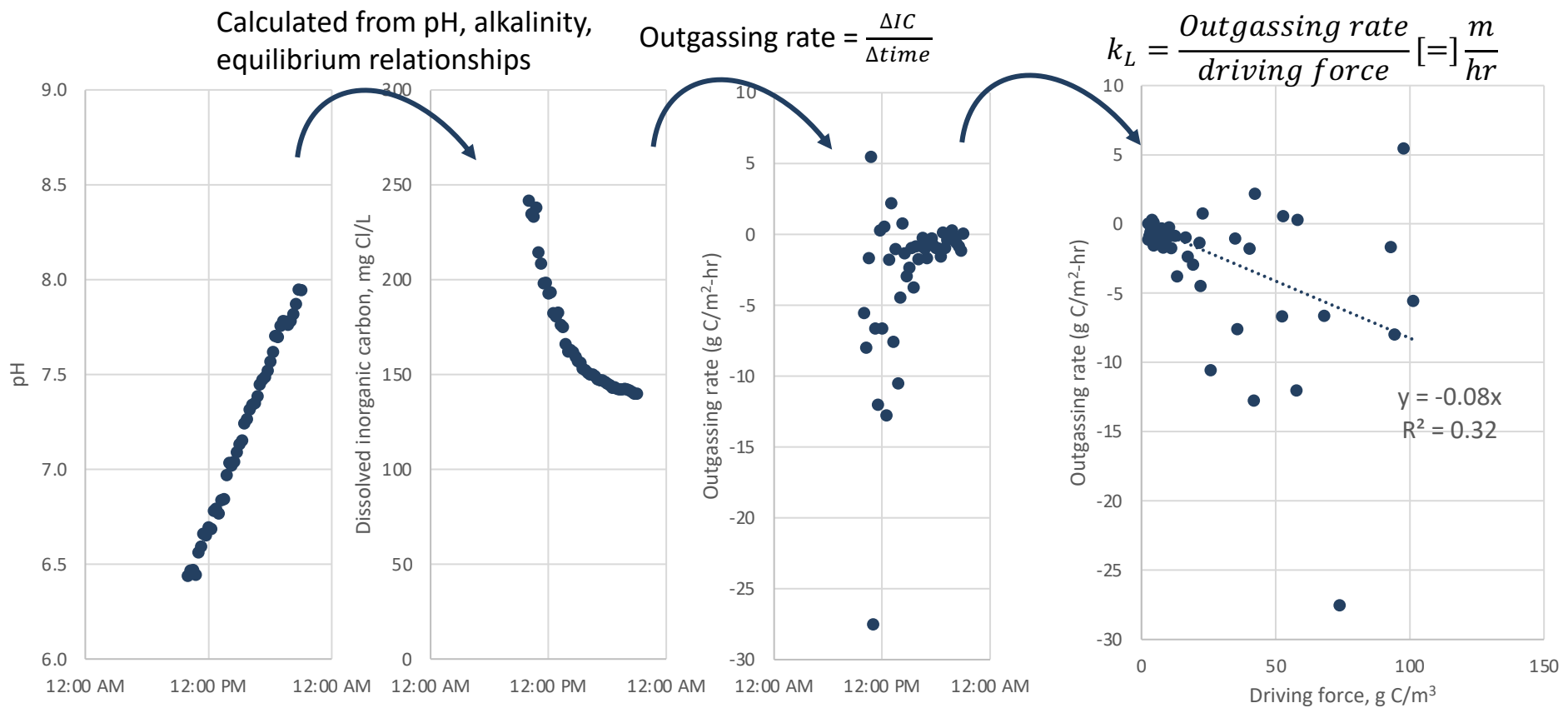
Top: 1-acre ponds at QH, used to measure ingassing rates at a commercially relevant scale. Bottom: MBE 3.4 m² used to more fully parameterize air-CO₂ flux.



The mass transfer coefficient was measured at two paddle wheel speed settings over 13 cycles

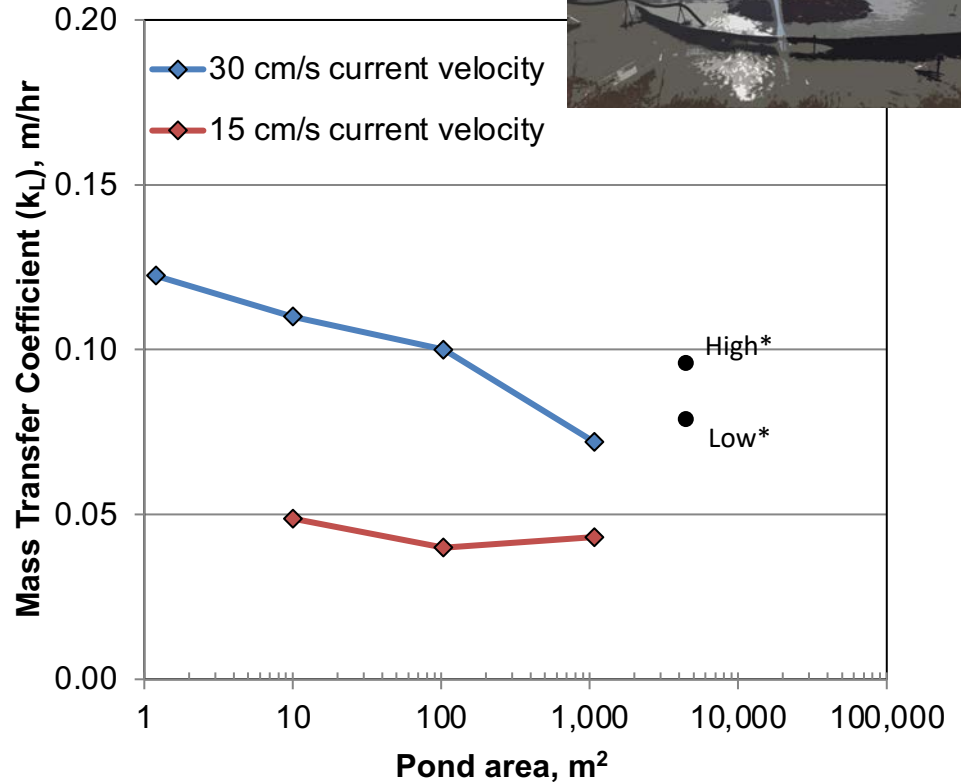


k_L is calculated from pH vs. time curves



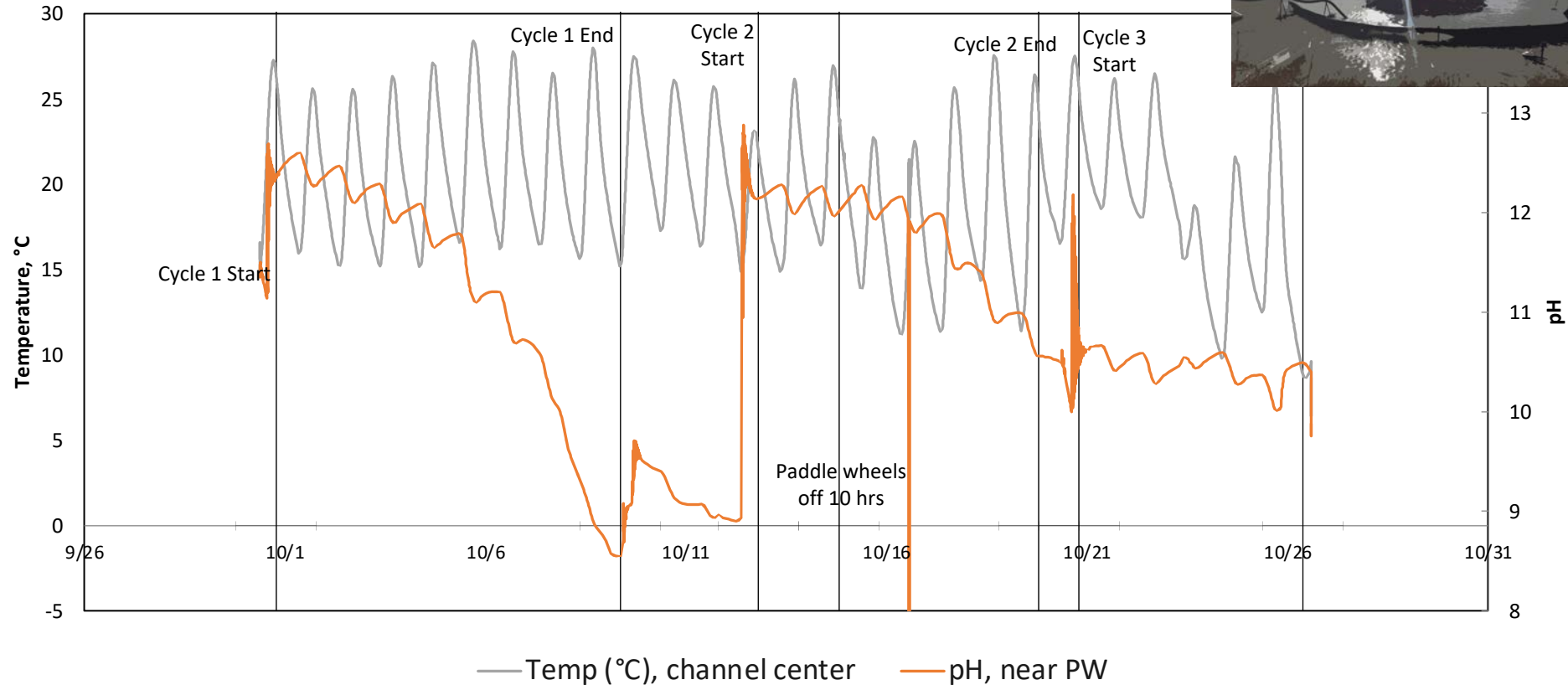
k_L measured 0.08 – 0.10, higher than hypothesized

Cycle #	High	Low
1	0.11	
2	0.08	
3	0.09	
4	0.11	
5		0.09
6		0.08
7		0.11
8		0.19*
9		0.07
10		0.07
11		0.09
12		0.08
13		0.07
AVG:	0.10	0.08
STDEV:	0.01	0.01
RSD:	13.6%	16.3%

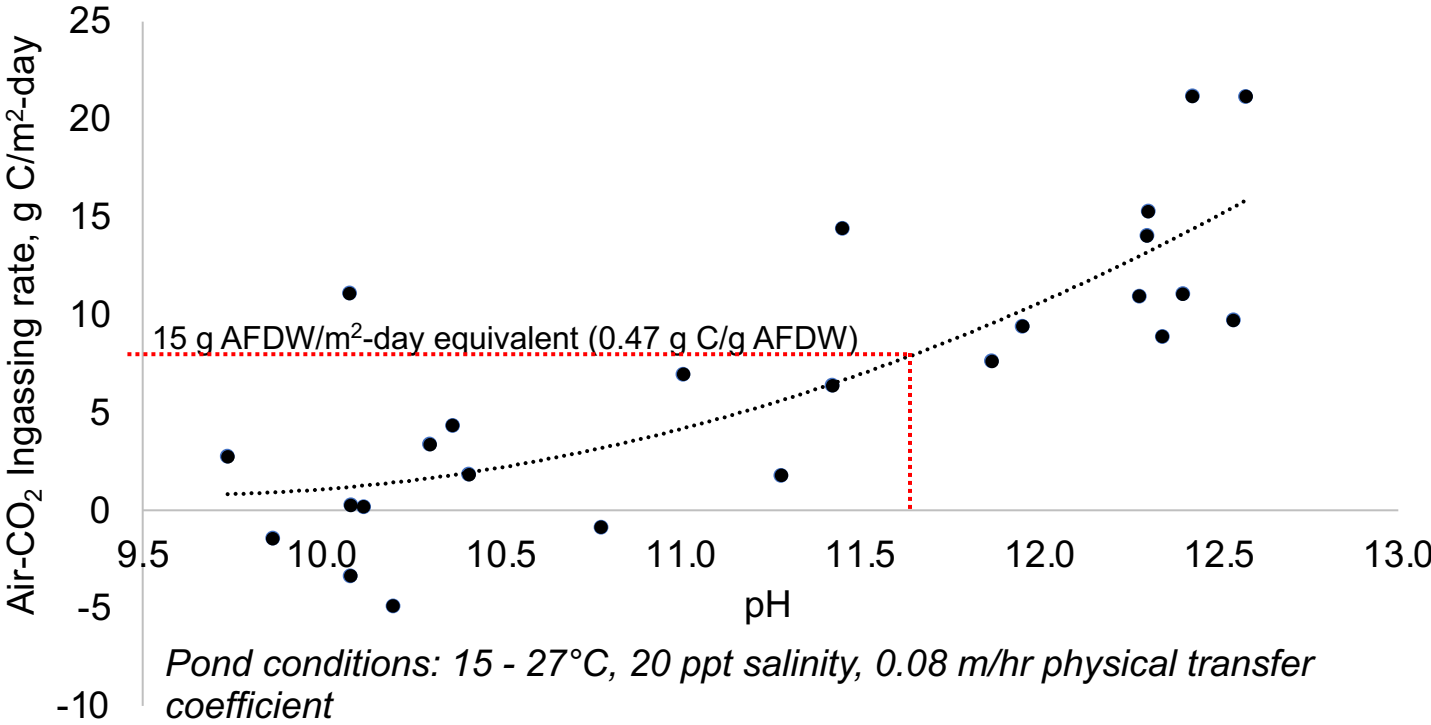


*Current velocity during 1-acre pond measurements TBD

Abiotic air-CO₂ ingassing rates were measured over three cycles, beginning above pH 12



1-acre pond ingassing rates rates increase with pH due to chemical enhancement; pH > 11.7 required to support 15 g AFDW/m²-day



> pH 12 required to support 2025 DOE productivity target

Mass-transfer model predictions of E , for two limiting cases:

Second order instantaneous reversible reaction, 'Diffusion Limited' (Olander 1960)

$$J_{CO_2} = k_L * (P_{CO_2}^{air} * H - C_{CO_2}^*(x = \delta)) * \left[1 + \frac{D_{OH^-} \cdot D_{HCO_3^-} \cdot K [OH^-]}{D_{CO_2} (K \cdot CO_{2(aq)}^* \cdot D_{HCO_3^-} + D_{OH^-})} \right] \quad K = \frac{[HCO_3^-]}{[OH^-][CO_2]}$$

\downarrow
Flux increases proportionally to turbulence

\swarrow
pH dependent, but not influenced by $CO_2 + OH^-$ reaction rate

First-order, finite reaction rate, 'Reaction Rate Limited' (Hatta 1932)

$$J_{CO_2} = (P_{CO_2}^{air} * H - C_{CO_2}^*(x = \delta)) * \left[\sqrt{D_{CO_2} * k_{tot} * [OH^-]} * \coth \left(\sqrt{\frac{D_{CO_2} * k_{tot}}{(k_L)^2}} \right) \right]$$

\downarrow
Square root reaction rate dependance

\downarrow
*Turbulence independent when $\sqrt{\frac{D_{CO_2} * k_{tot}}{(k_L)^2}} < \sim 2$*

Transfer coefficient measurements repeated in 3.4 m² ponds, aiming to find paddle wheel setting, depth yielding 'fast' and 'slow' k_L in follow-on ingassing trial

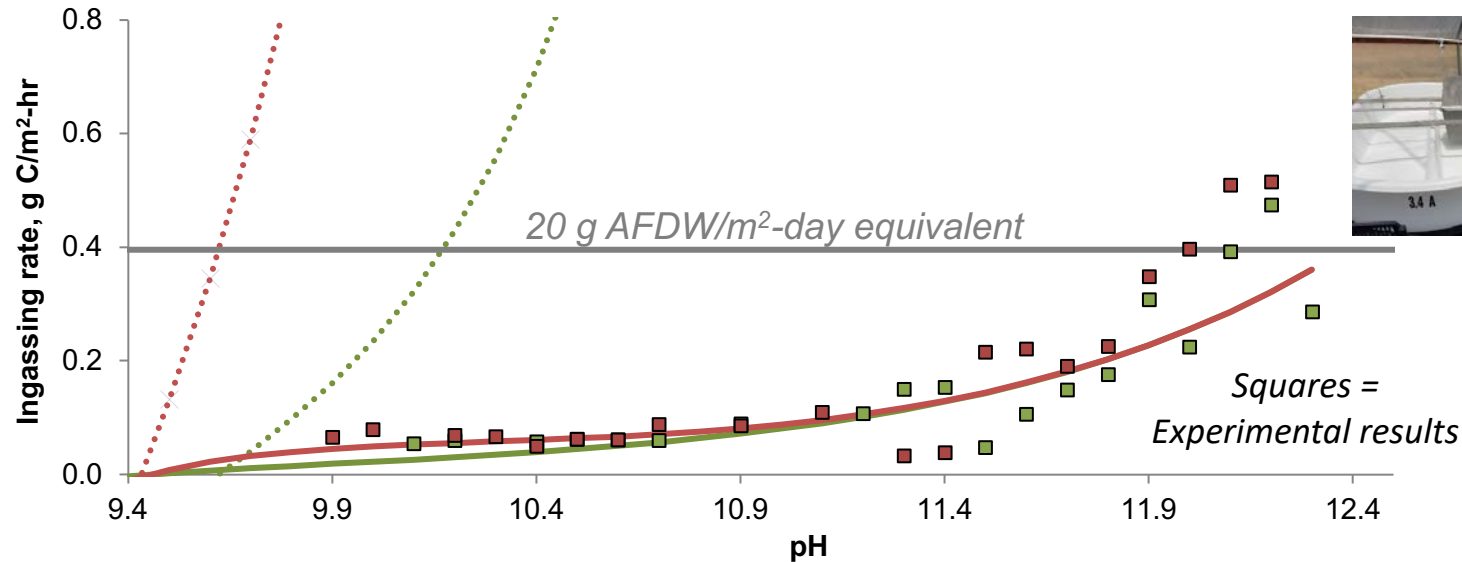
Paddlewheel VFD setting (Hz)	Pond	Depth (cm)	k_L (m/hr)	k_L Error	n
45	A	30	0.22	0.01	84
45	A	25	0.29	0.01	76
45	B	30	0.36	0.02	209
35	A	25	0.20	0.01	485
30	A	30	0.12	0.01	83
30	B	30	0.22	0.01	83
20	A	30	0.06	0.01	26
20	B	30	0.07	0.01	26
15	A	30	0.04	0.01	7
15	B	30	0.05	0.01	7
10	A	30	0.03	0.01	13
10	B	30	0.03	0.01	13



$$k_L = \frac{\text{Outgassing rate}}{\text{driving force}} [=] \frac{m}{hr}$$

Experimental data validates the reaction-rate limited model; air-CO₂ flux is independent of the mass-transfer coefficient, k_L

Model predictions for 'diffusion' (dotted lines) and 'reaction rate' limited (solid lines) transfer, at low ($k_L = 0.06$ m/hr) and high ($k_L = 0.36$ m/hr) turbulence levels



Conclusion: Decreases in turbulence levels in 10-acre ponds are not expected to influence chemically enhanced air-CO₂ flux.

Conclusions


- Chemically enhanced air-CO₂ absorption requires high pH, 12 or above, to support economically viable biomass productivity
- Finding strains that thrive at such a high pH will be a challenge
- Experimentally measured ingassing rates align well with the 'reaction-rate limited' mass-transfer regime; ingassing rates appear minimally influenced by pond scale

Thank you!





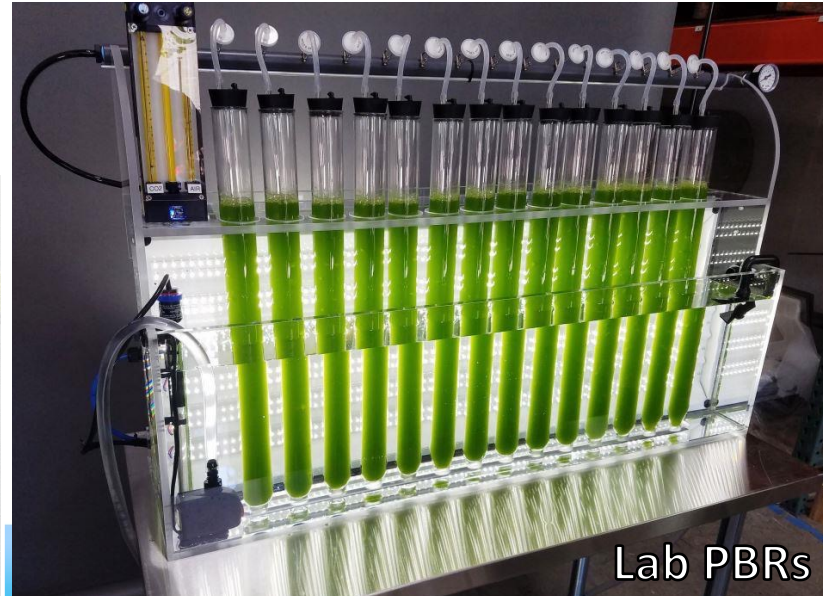
Scale-Up
Design
TEA-LCA



Full-Scale
Equipment



Pilot
Facilities



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