

# Algae Biomass Summit 2022

## *Mass transfer coefficients, $k_L$ , and air- $CO_2$ ingassing rates in 3.4 m<sup>2</sup> and 1-acre raceway ponds*

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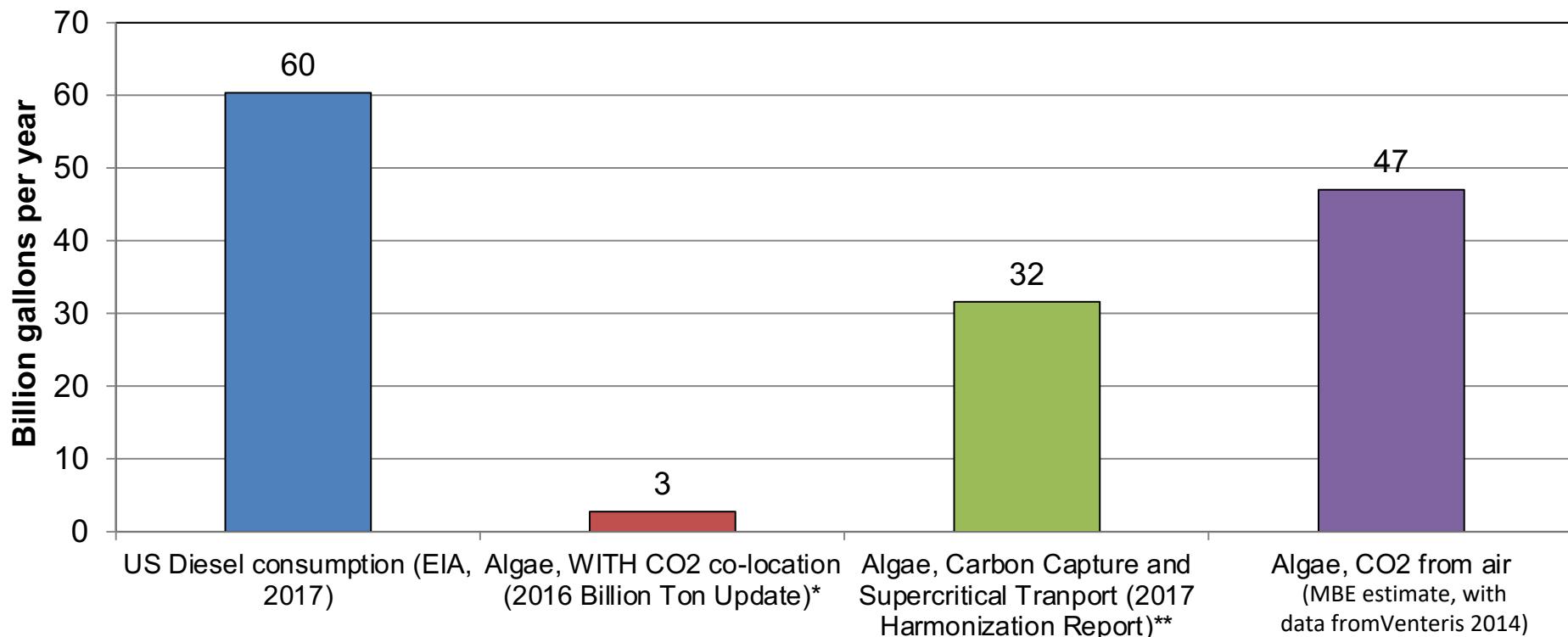
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## Why grow algae on CO<sub>2</sub> from air?

CO<sub>2</sub> point-source co-location limits algal resource potential to less than 5 BGY

Direct, in-pond air-CO<sub>2</sub> capture can increase resource potential nearly 10-fold



\*freshwater and saltwater scenario, present productivity. Assume 0.35 g diesel/gas per g of biomass.

\*\*Assume 0.35 g diesel/gas per g of biomass (for comparison to the 2016 BTU case)

The  $\text{CO}_2$  mass-transfer rate,  $J_{\text{CO}_2}$ , is proportional to the mass transfer coefficient,  $k_L$ , and the ‘driving force’ for mass transfer.  $E$  accounts for chemical reactions.

When  $C_{CO_2}^{bulk}(x = \delta) > P_{CO_2}^{air} * H$ :

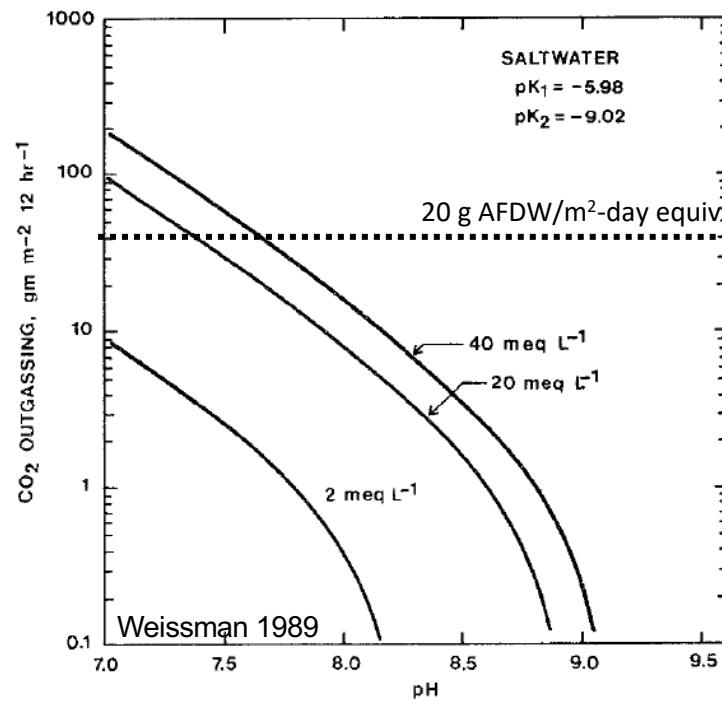
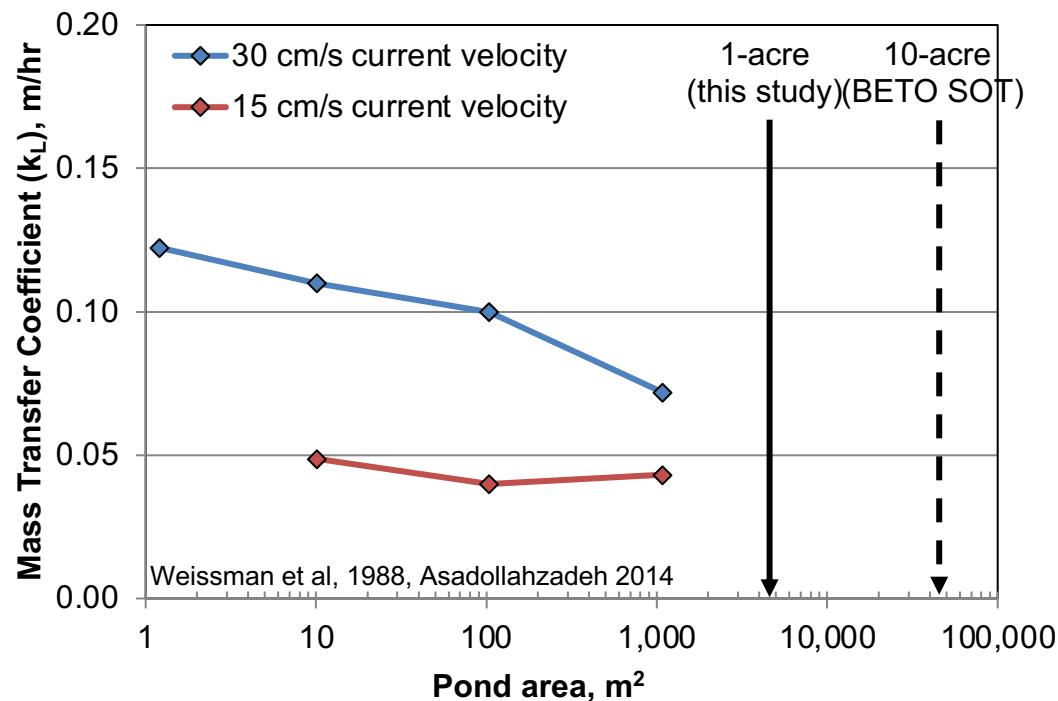
- Driving force is negative
- $\text{CO}_2$  lost from pond to atmosphere
- Net  $\text{CO}_2$  ‘outgassing’ rate

When  $C_{CO2}^{bulk}(x = \delta) < P_{CO2}^{air} * H$

- Driving force is positive
- Air- $\text{CO}_2$  transfer from atmosphere to pond
- Net  $\text{CO}_2$  ‘ingassing’ rate
- Influence of reactions accounted with ‘E’

**Outgassing rates must be minimized to achieve high carbon utilization efficiency  
Ingassing rates of are interest for direct algae air- $\text{CO}_2$  capture**

$k_L$  is between 0.05-0.1 m/hr for small ponds, unmeasured in large (1-acre +) ponds  
 At elevated alkalinity, pH 7.5 – 8.0,  $\text{CO}_2$  outgassing rates approach the daily gain in biomass

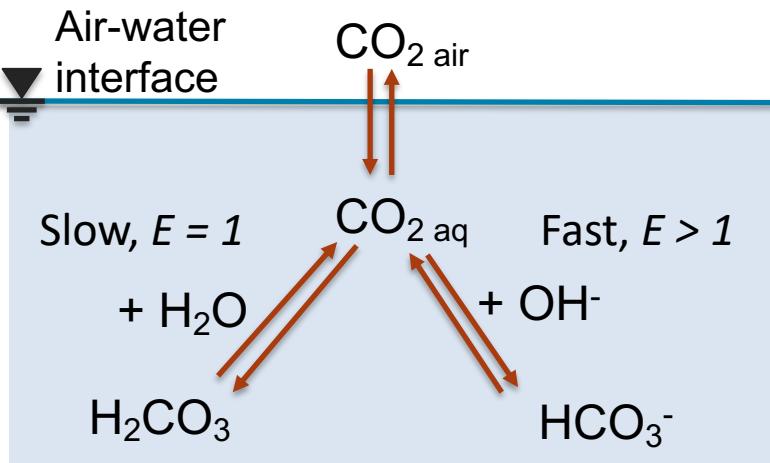


Influence of  $k_L$ , pond scale on the ingassing rate is uncertain, dependent on  $E$

# At elevated pH, the $\text{CO}_{2,\text{aq}} + \text{OH}^-$ reaction pathway appreciably increases air- $\text{CO}_2$ flux, known as chemical enhancement

Without chemical enhancement,  $E = 1$ , and air- $\text{CO}_2$  flux is given by:

$$J_{\text{CO}_2} = k_L * (C_{\text{CO}_2}^{\text{sat}} - C_{\text{CO}_2}^{\text{bulk}}) * E$$



Where:

$C_{\text{CO}_2}^{\text{sat}}$  =  $\text{CO}_{2,\text{aq}}$  at the air-water interface, in equilibrium with the gas phase,  $\sim 10 \mu\text{M}$

$C_{\text{CO}_2}^{\text{bulk}}$  =  $\text{CO}_{2,\text{aq}}$  in pond 'bulk',  $\sim 0 \mu\text{M}$  at pH > 10

$k_L$  = mass transfer coefficient,  $\sim 0.1 \text{ m/hr}$  for ponds, a measure of turbulence as it relates to mass transfer

Under non-enhanced ( $E = 1$ ) conditions:

$$J_{\text{CO}_2} = 0.1 \frac{\text{m}}{\text{hr}} (10 - 0 \mu\text{M}) = 0.3 \frac{\text{g C}}{\text{m}^2 \text{day}} \approx 0.6 \frac{\text{g AFDW}}{\text{m}^2 \text{day}}$$

$E$  must be  $\sim 30$  to support 20 g AFDW/m<sup>2</sup>-day!

Depending on the assumed mass-transfer regime, estimates for  $E$  range from 2 to 40 at pH 10.5

Hypothesis:  $E$  is sufficient to support high rates of carbon uptake, at a biologically compatible high pH

## Approach – Identify conditions to meet the target air-CO<sub>2</sub> flux

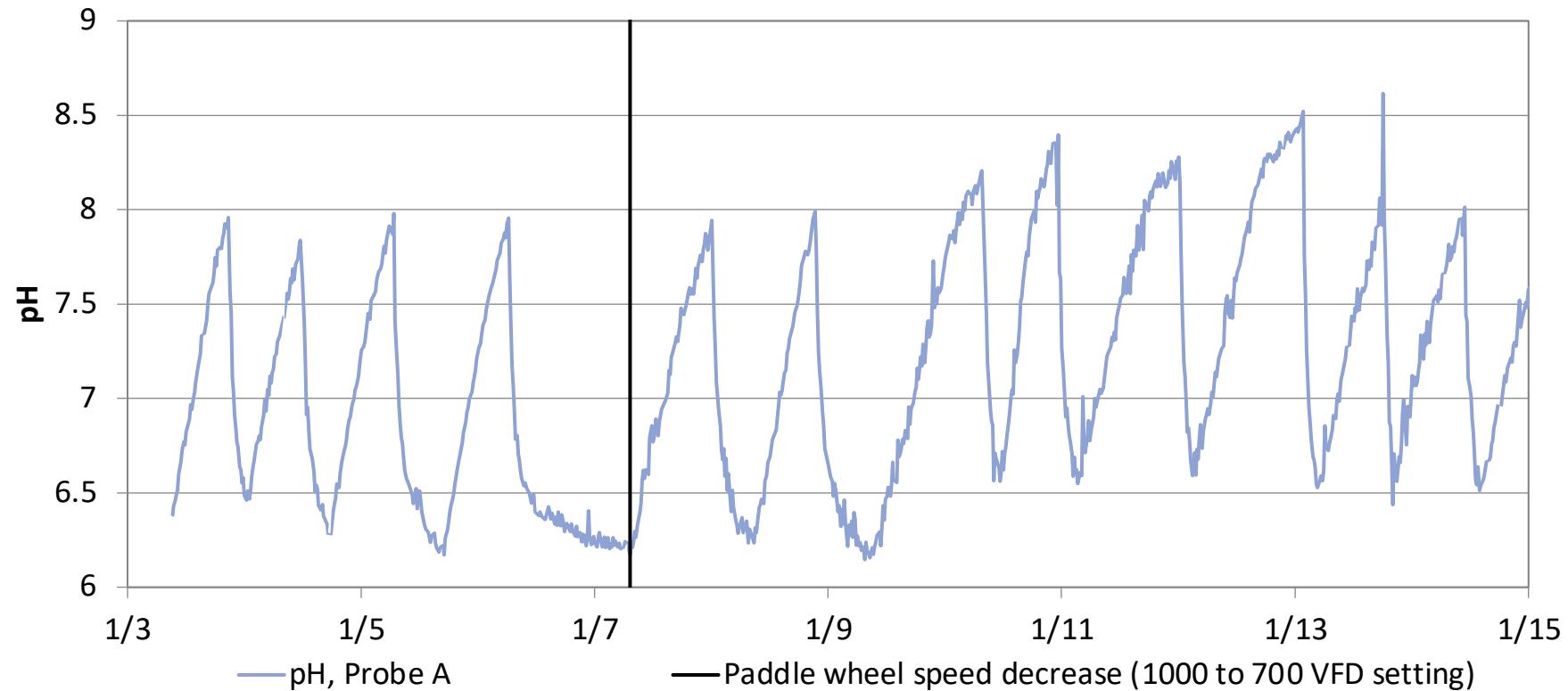
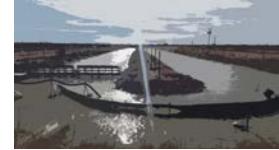
- Measure air-CO<sub>2</sub> exchange rates via abiotic (without algae) trials in 1-acre ponds.
  - $k_L$  is measured in ‘outgassing trials’, by supersaturating the pond with CO<sub>2</sub>, then measuring the rate of pH increase.
  - Air-CO<sub>2</sub> flux,  $J_{CO_2}$ , at elevated pH is measured by displacing the pond from air-equilibrium with a strong base, then measuring the rate of return to equilibrium (pH decrease)
- Compare ingassing rates over a wider current velocity range in more easily managed 3.4 m<sup>2</sup> ponds
- Compare experimental results to model predictions to identify the appropriate mass-transfer model



*Top:* 1-acre ponds at QH, used to measure ingassing rates at a commercially relevant scale. *Bottom:* MBE 3.4 m<sup>2</sup> used to more fully parameterize air-CO<sub>2</sub> flux.

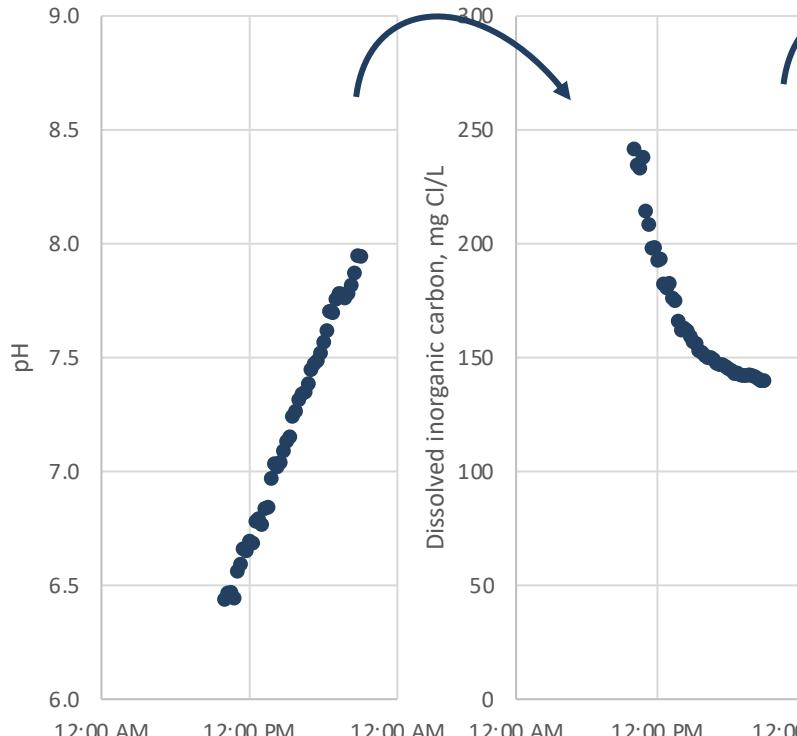


# The mass transfer coefficient was measured at two paddle wheel speed settings over 13 cycles

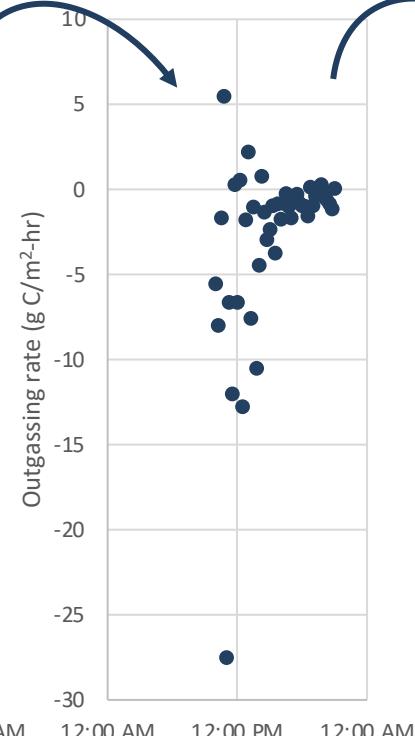


# $k_L$ is calculated from pH vs. time curves

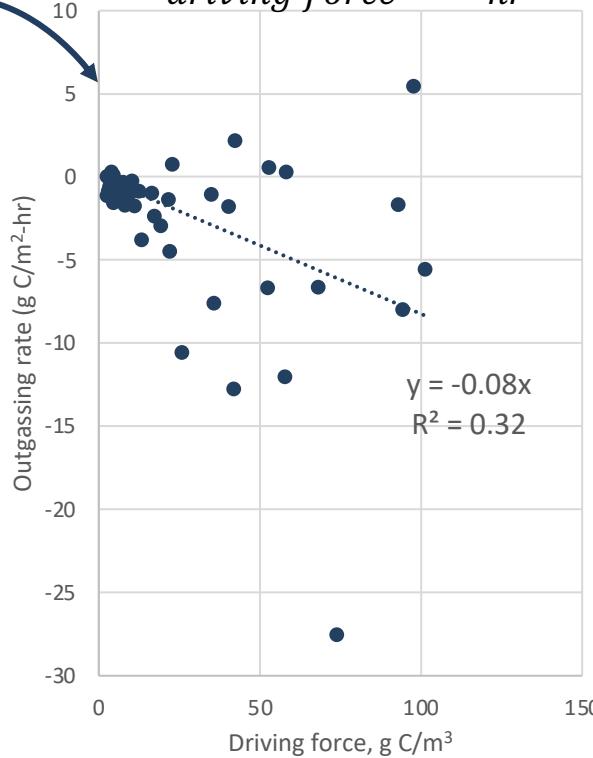
Calculated from pH, alkalinity, equilibrium relationships



$$\text{Outgassing rate} = \frac{\Delta IC}{\Delta \text{time}}$$

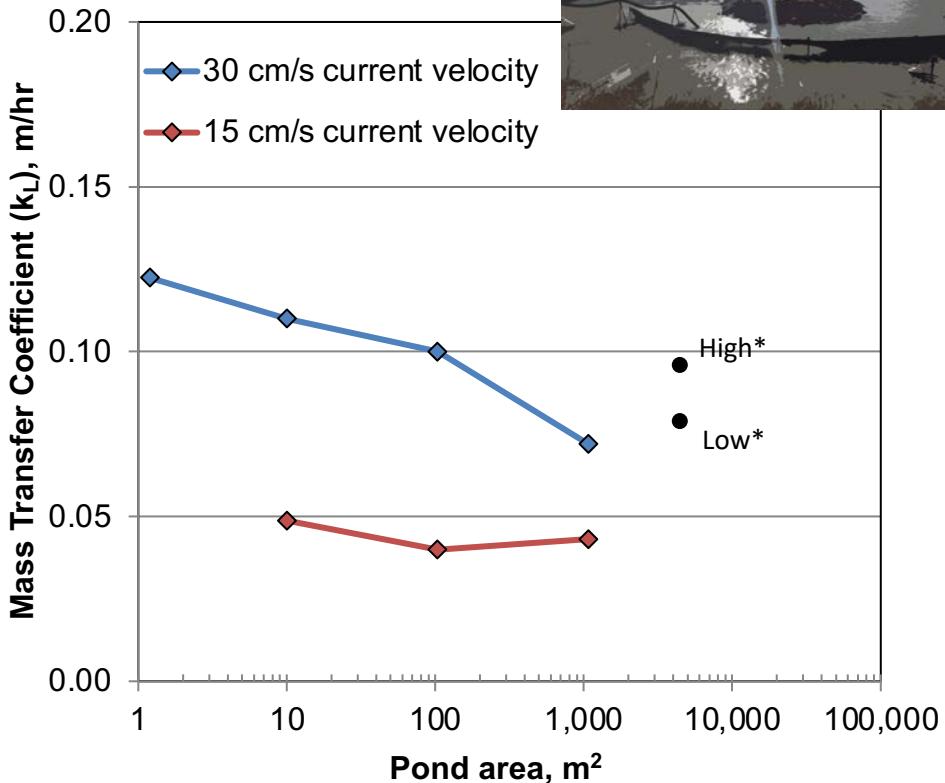


$$k_L = \frac{\text{Outgassing rate}}{\text{driving force}} [=] \frac{m}{hr}$$



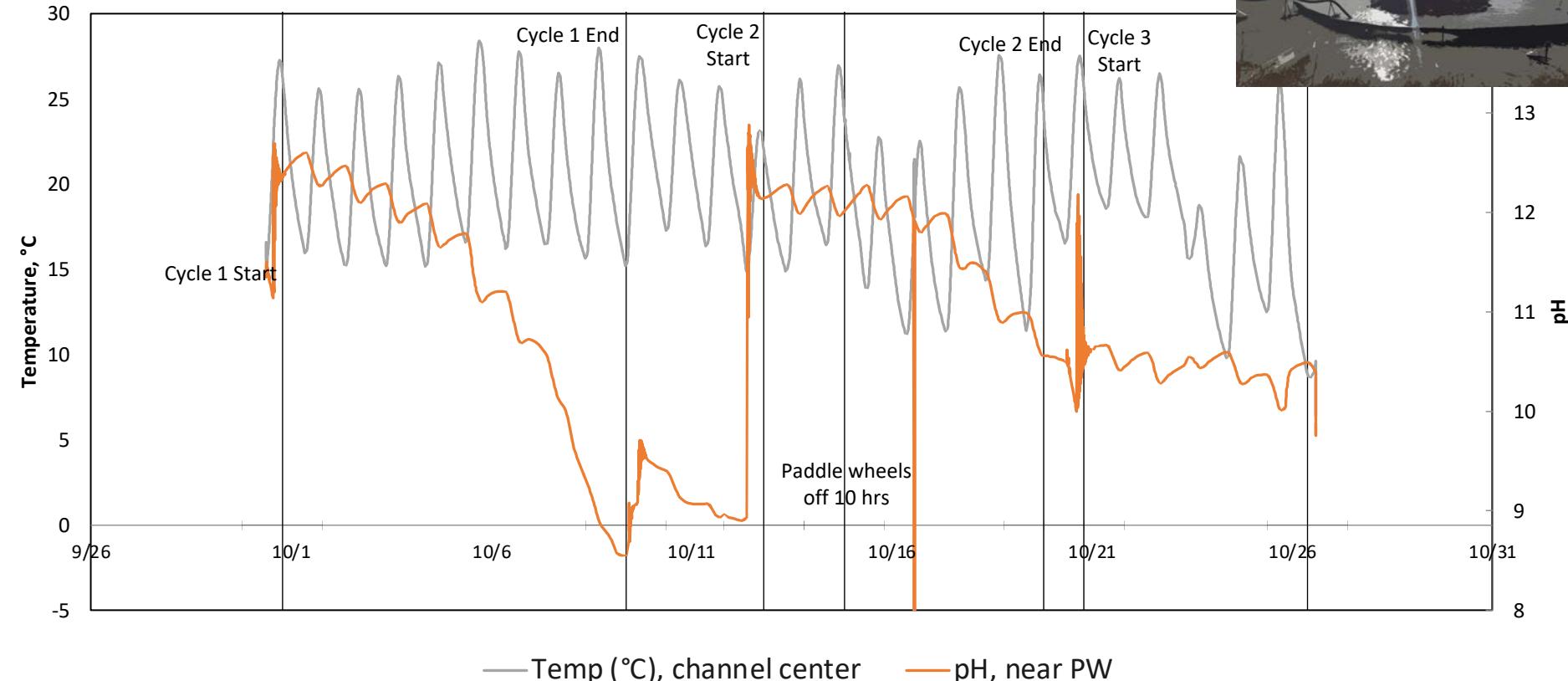
# $k_L$ measured 0.08 – 0.10, higher than hypothesized

Cycle #	High	Low
1	0.11	
2	0.08	
3	0.09	
4	0.11	
5		0.09
6		0.08
7		0.11
8		0.19*
9		0.07
10		0.07
11		0.09
12		0.08
13		0.07
AVG:	<b>0.10</b>	<b>0.08</b>
STDEV:	<b>0.01</b>	<b>0.01</b>
RSD:	<b>13.6%</b>	<b>16.3%</b>

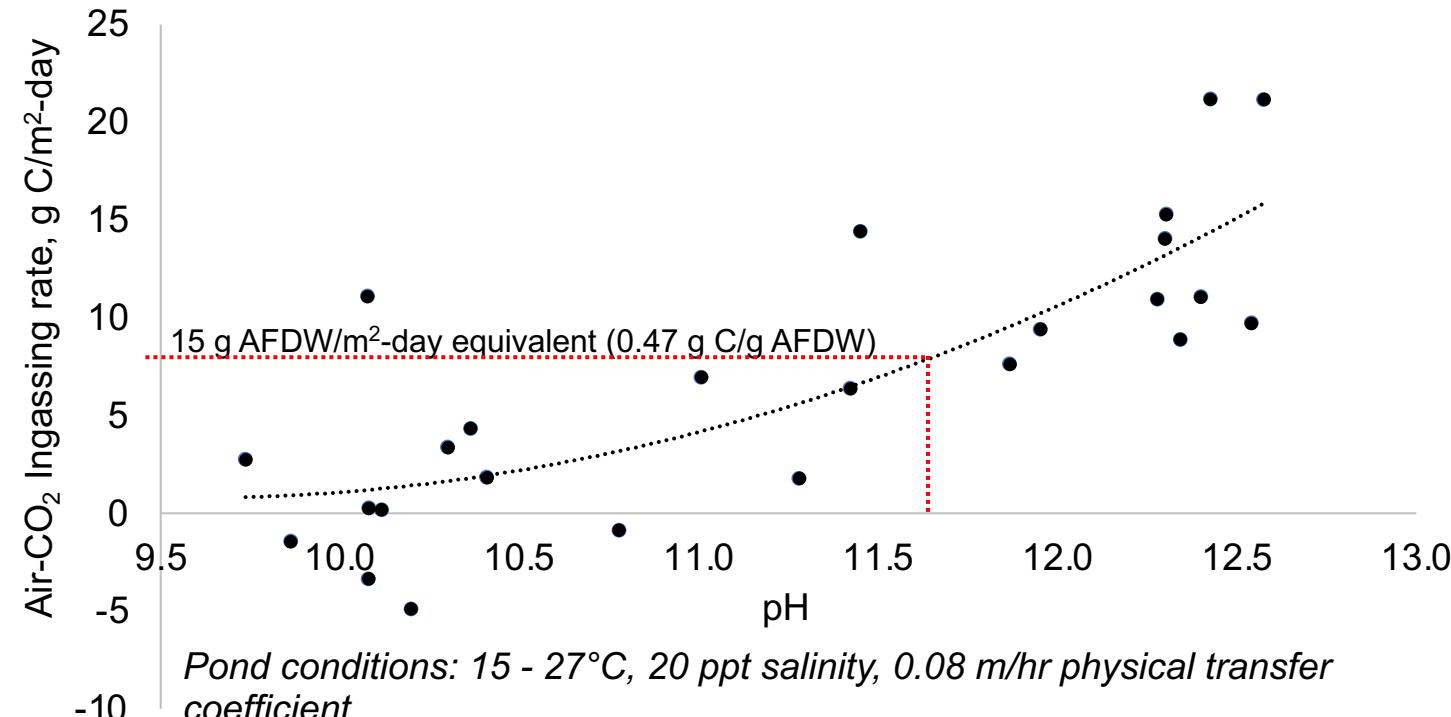


\*Current velocity during 1-acre pond measurements TBD

# Abiotic air- $\text{CO}_2$ ingassing rates were measured over three cycles, beginning above pH 12



# 1-acre pond ingassing rates rates increase with pH due to chemical enhancement; pH > 11.7 required to support 15 g AFDW/m<sup>2</sup>-day



> pH 12 required to support 2025 DOE productivity target

# Mass-transfer model predictions of $E$ , for two limiting cases:

Second order instantaneous reversible reaction, 'Diffusion Limited' (Olander 1960)

$$J_{CO_2} = k_L * \left( P_{CO_2}^{air} * H - C_{CO_2}^*(x = \delta) \right) * \left[ 1 + \frac{D_{OH^-} \cdot D_{HCO_3^-} \cdot K \cdot [OH^-]}{D_{CO_2} (K \cdot CO_{2(aq)}^* \cdot D_{HCO_3^-} + D_{OH^-})} \right]$$

$$K = \frac{[HCO_3^-]}{[OH^-][CO_2]}$$

Flux increases proportionally to turbulence

pH dependent, but not influenced by  $CO_2 + OH^-$  reaction rate

First-order, finite reaction rate, 'Reaction Rate Limited' (Hatta 1932)

$$J_{CO_2} = \left( P_{CO_2}^{air} * H - C_{CO_2}^*(x = \delta) \right) * \left[ \sqrt{D_{CO_2} * k_{tot} * [OH^-]} * \coth \left( \sqrt{\frac{D_{CO_2} * k_{tot}}{(k_L)^2}} \right) \right]$$

Square root reaction rate dependence

Turbulence independent when  $\sqrt{\frac{D_{CO_2} * k_{tot}}{(k_L)^2}} < \sim 2$

# Transfer coefficient measurements repeated in 3.4 m<sup>2</sup> ponds, aiming to find paddle wheel setting, depth yielding 'fast' and 'slow' k<sub>L</sub> in follow-on ingassing trial

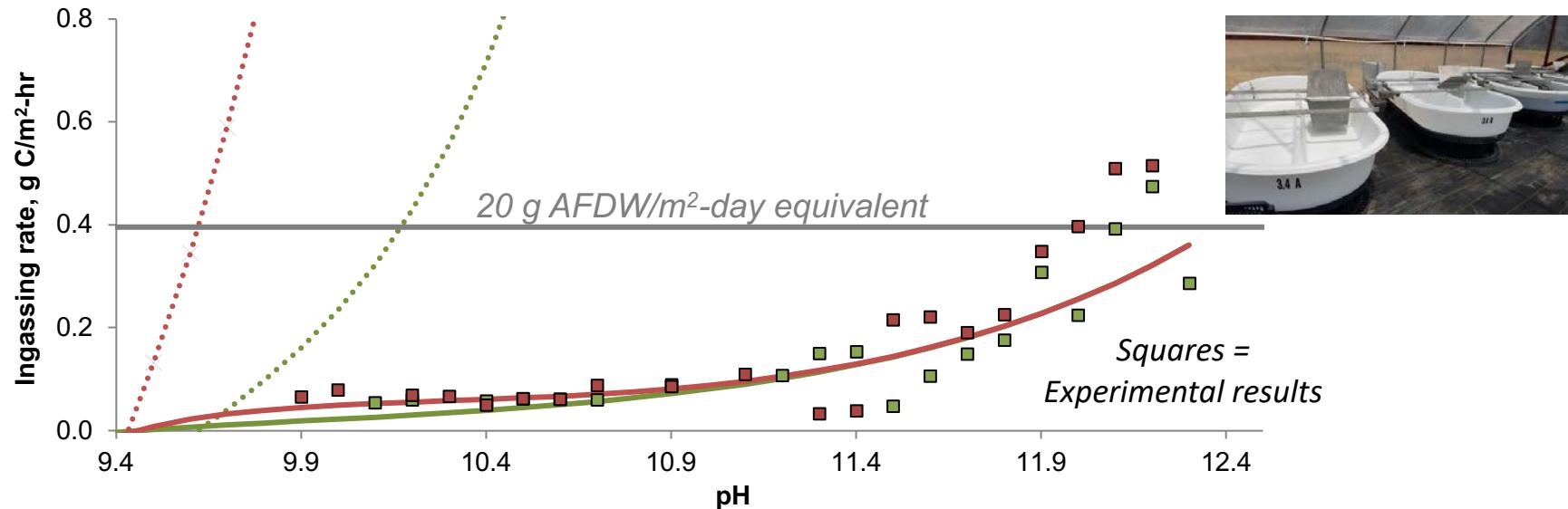
Paddlewheel VFD setting (Hz)	Pond	Depth (cm)	k <sub>L</sub> (m/hr)	kL Error	n
45	A	30	0.22	0.01	84
45	A	25	0.29	0.01	76
<b>45</b>	<b>B</b>	<b>30</b>	<b>0.36</b>	<b>0.02</b>	<b>209</b>
35	A	25	0.20	0.01	485
30	A	30	0.12	0.01	83
30	B	30	0.22	0.01	83
<b>20</b>	<b>A</b>	<b>30</b>	<b>0.06</b>	<b>0.01</b>	<b>26</b>
20	B	30	0.07	0.01	26
15	A	30	0.04	0.01	7
15	B	30	0.05	0.01	7
10	A	30	0.03	0.01	13
10	B	30	0.03	0.01	13



$$k_L = \frac{\text{Outgassing rate}}{\text{driving force}} [=] \frac{\text{m}}{\text{hr}}$$

# Experimental data validates the reaction-rate limited model; air- $\text{CO}_2$ flux is independent of the mass-transfer coefficient, $k_L$

Model predictions for 'diffusion' (dotted lines) and 'reaction rate' limited (solid lines) transfer, at low ( $k_L = 0.06 \text{ m/hr}^{-1}$ ) and high ( $k_L = 0.36 \text{ m hr}^{-1}$ ) turbulence levels



**Conclusion:** Decreases in turbulence levels in 10-acre ponds are not expected to influence chemically enhanced air- $\text{CO}_2$  flux.

## Conclusions

- Chemically enhanced air-CO<sub>2</sub> absorption requires high pH, 12 or above, to support economically viable biomass productivity
- Finding strains that thrive at such a high pH will be a challenge
- Experimentally measured ingassing rates align well with the 'reaction-rate limited' mass-transfer regime; ingassing rates appear minimally influenced by pond scale

Thank you!





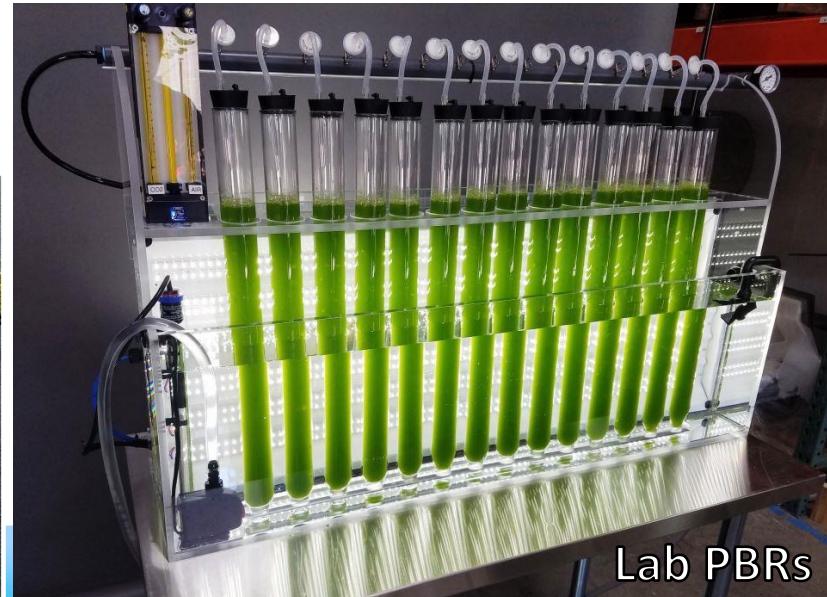
Scale-Up  
Design  
TEA-LCA



Full-Scale  
Equipment



Pilot  
Facilities



Lab PBRs



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