

Electrochimica Acta

Enhancing the Activity of Fe-N-C Oxygen Reduction Reaction Electrocatalysts by High-Throughput Exploration of Synthesis Parameters

--Manuscript Draft--

Manuscript Number:	
Article Type:	VSI: SAE 2022
Keywords:	Iron; Electrocatalyst; Non-PGM; ORR; mass activity; EXAFS
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Abstract:	The most active class of platinum group metal-free (PGM-free) oxygen reduction reaction (ORR) electrocatalysts in acidic electrolytes are those synthesized by heat treatment of iron, carbon, nitrogen precursors (Fe-N-C). Due to the large number of possible precursor compounds, a small fraction of the synthesis variable space has been explored. Correlation of synthesis variables with Fe speciation and ORR activity have been limited. In this work, an automation platform and a multi-port ball-milling were utilized to evaluate the effects of synthesis variables, such as identity of iron precursor, iron loading, and carbon and nitrogen sources on the oxygen reduction reaction (ORR) activity of iron-nitrogen-carbon catalysts in acidic electrolyte. The ORR activity is correlated with catalyst Fe speciation determined using Fe K-edge X-ray absorption spectroscopy (XAFS).

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4 **Enhancing the Activity of Fe-N-C Oxygen Reduction Reaction Electrocatalysts by High-**
5 **Throughput Exploration of Synthesis Parameters**
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28 **ABSTRACT**
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31 The most active class of platinum group metal-free (PGM-free) oxygen reduction reaction
32 (ORR) electrocatalysts in acidic electrolytes are those synthesized by heat treatment of iron,
33 carbon, nitrogen precursors (Fe-N-C). Due to the large number of possible precursor compounds,
34 a small fraction of the synthesis variable space has been explored. Correlation of synthesis
35 variables with Fe speciation and ORR activity have been limited. In this work, an automation
36 platform and a multi-port ball-milling were utilized to evaluate the effects of synthesis variables,
37 such as identity of iron precursor, iron loading, and carbon and nitrogen sources on the oxygen
38 reduction reaction (ORR) activity of iron-nitrogen-carbon catalysts in acidic electrolyte. The ORR
39 activity is correlated with catalyst Fe speciation determined using Fe K-edge X-ray absorption
40 spectroscopy (XAFS).
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4 **1. INTRODUCTION**
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7 Polymer electrolyte fuel cells (PEFCs) are electrochemical devices that convert the chemical
8 energy in hydrogen to electrical energy with high efficiency and, as such, are being implemented
9 to eliminate the emission of carbon dioxide from light [1] and heavy-duty vehicles [2]. While light-
10 duty fuel cell electric vehicles were first commercialized in 2014 [3], significant reductions in fuel
11 cell stack cost and hydrogen cost are needed for these vehicles to be cost competitive with the
12 incumbent internal combustion engine-fossil fuel powered vehicles [4,5]. A major contributor to
13 the high cost of PEFC stacks is the high loading of platinum-based electrocatalyst needed to drive
14 the kinetically sluggish oxygen reduction reaction (ORR). An extensive effort has been underway
15 for more than fifty years to replace the platinum-based ORR catalyst with a platinum group metal-
16 free (PGM-free) catalyst comprising earth-abundant materials [6]. Although significant progress
17 has been made over the past decade in increasing both the ORR activity and durability of PGM-
18 free catalysts [7-14], further improvements in these materials, especially in durability and
19 hydrogen-air performance are needed for them to be viable for vehicle power [15]. The highest
20 ORR activities for PGM-free materials have been obtained from catalysts derived from iron salts
21 and metal-organic frameworks or carbon-nitrogen-containing polymers [14-18], though the ORR
22 turnover frequencies and volumetric active site densities of these materials are still approximately
23 one order of magnitude lower than that those of state-of-the-art Pt alloy nanoparticle catalyst [12].
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25 For the general class of pyrolyzed iron-nitrogen-carbon PGM-free materials, variables such as
26 the iron precursor, carbon and nitrogen sources, their relative concentrations, as well as the
27 temperature and atmosphere of pyrolysis are important in determining the activity and stability of
28 the resulting catalysts [13,16,19,20]. Changing the synthesis variable and testing their effect on
29 the resulting catalyst properties, such as iron speciation, and, most importantly, ORR activity, is a
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4 very time-consuming process and only a limited portion of the composition and temperature space
5 have been explored for this broad class of materials [21].
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8 In 2011, Dodelet et al. [16] developed a new synthetic method for Fe-N-C catalysts using
9 physical mixing, through ball milling, of a zeolitic imidazolate framework (ZIF-8), 1,10-
10 phenanthroline, and iron precursors. Ball milling involves high energy movement of beads/milling
11 media which can break chemical bonds, hence, triggering solid–solid reactions, can change the
12 materials' morphology, and possibly forming structural defects that can increase the density of
13 active catalytic sites [22,23]. Unlike liquid phase synthesis of doped ZIFs, high-energy ball milling
14 followed by controlled thermal annealing is an easy and scalable synthetic method in which type
15 of precursors and concentrations can be readily varied [24].
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18 This paper describes a subset of the data from our exploration of the synthesis parameter space
19 of Fe-N-C catalysts derived from ball-milled mixtures of iron salts and carbon and nitrogen-
20 containing compounds. This is aided by the application of high-throughput synthesis methodology
21 to explore the effects of identity of the iron precursor, carbon and nitrogen source, ratio of carbon
22 and nitrogen sources, and iron loading on the activity of iron-based ORR electrocatalysts. Other
23 variables studied and reported upon elsewhere are temperature ramp rate, heat treatment
24 temperature, cooling rate [25] and presence of additional transition metals. A robotic platform and
25 multi-port high-energy ball milling apparatus were utilized to synthesize numerous compositions
26 that were subsequently characterized for ORR activity using aqueous acidic electrolyte rotating
27 ring-disk electrode measurements. The ORR activity is correlated with the Fe speciation
28 determined using Fe K-edge X-ray absorption spectroscopy data.
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2. EXPERIMENTAL

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4 **2.1 Materials**
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6 ZIF-8 (Sigma Aldrich), 1,10-phenanthroline, (abbreviated as phen) (Sigma-Aldrich), and
7 oxidized BP (Black Pearls 2000 pretreated in 70% nitric acid at 80 °C for 8 h) were dried under
8 vacuum for ~15 h at 80 °C. Iron precursors (iron (II) acetate (99.99%, Sigma Aldrich), iron (II)
9 chloride tetrahydrate (98%, Sigma Aldrich), iron (III) chloride anhydrous (99.99%, Sigma
10 Aldrich), iron (III) acetylacetone (97%, Sigma-Aldrich), iron (III) nitrate nonahydrate (98%,
11 Sigma Aldrich), iron (II) sulphate heptahydrate (>99%, Sigma Aldrich), iron (III) meso-tetra (2,4,6
12 trimethylphenyl) porphine chloride (Frontier Scientific), ferrocenium tetrafluoroborate (Sigma
13 Aldrich), iron (III) oxalate dihydrate (99%, Sigma-Aldrich), iron (III) meso-tetraphenylporphine
14 μ-oxodimer (Frontier Scientific), 2,3,7,8,12,13,17,18-octaethyl-21h,23h-porphine iron (III)
15 acetate, (97%, Sigma Aldrich), iron (III) phthalocyanine-4,4',4'',4'''-tetrasulfonic acid, with
16 oxygen monosodium salt hydrate (Sigma Aldrich), 5,10,15,20-tetraphenyl-21h,23h-porphine iron
17 (III) chloride (Sigma Aldrich), iron (III) meso-tetra (4-sulfonatophenyl) porphine chloride (acid
18 form) (Frontier Scientific), iron (III) meso-tetra(4-carboxylphenyl) porphine chloride (Frontier
19 Scientific), 5,10,15,20-tetrakis(pentafluorophenyl)-21h-,23h-porphyrin iron (III) chloride (Sigma
20 Aldrich) and bis(cyclopentadienyl)iron (98%, Sigma Aldrich)) were used as received.
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46 **2.2 High-Throughput Catalysis Synthesis**
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48 An automated synthesis platform (Big Kahuna, Unchained Labs Inc.) in a custom-built N₂-
49 filled glovebox (MB 200B, MBraun) in Argonne National Laboratory's High-throughput Research
50 Laboratory was used for several steps in the catalyst synthesis. Matrices of experiments and
51 protocols were designed in Library Studio while Automation Studio (LEA software) was used for
52 running the protocols. The solid precursors were dispensed through disposable shaker vials and
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4 weighed using an automated balance (± 0.2 mg accuracy). The synthesis method was inspired by
5 and was similar to the one reported by Zitolo et al. [8]. A mixture of carbon source (Black Pearls)
6 and carbon-nitrogen source (ZIF-8 and phen) and the iron precursor were taken out of the glove
7 box after weighing and placed into 50 mL stainless steel ball mill jars and ball milled at 400 rpm
8 for 2 h in a high-throughput planetary ball mill (PM 400, Retsch). The samples were then heated
9 in a flowing argon atmosphere to 1050 °C, at a heating rate of 5 °C min⁻¹, and held at 1050 °C for
10 1 h. The sample was then cooled to 900 °C in Ar and exposed to a flowing pure NH₃ atmosphere
11 for 5 min before cooling down naturally to room temperature in Ar.
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2.3 Rotating Disk Electrode (RDE)

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28 The ORR half-wave potential ($E_{1/2}$) and the mass activity were evaluated for each catalyst using
29 the thin-film rotating disk electrode (RDE) technique (E7R9 ThinGap RRDE Tips PTFE, Pine
30 Research) and a CHI potentiostat (CH Instruments, Inc.) [26]. Half-wave potential is a valid way
31 to compare ORR activities of catalysts when using the same areal loading of catalyst on the disk
32 electrode [27], but mass activity provides a metric that can be used to compare activities of
33 catalysts evaluated at different loadings and is more useful for translating to the fuel cell
34 performance. The RRDE was immersed in oxygen-saturated room-temperature 0.5 M H₂SO₄
35 electrolyte also containing a graphite rod counter electrode and Ag/AgCl reference electrode. A
36 catalyst-ionomer ink was prepared by dispersing 5 mg of catalyst in 20 μ L of Nafion dispersion (5
37 wt% Nafion, D521, Ion Power, Inc.) and 0.5 mL of isopropanol. The mixture was sonicated in an
38 ultrasonic ice water bath for 30 min. The catalyst ink was deposited onto the glassy carbon
39 electrode of the RRDE in four aliquots, resulting in a catalyst loading of 0.6 mg cm⁻². The Ag/AgCl
40 reference electrode was calibrated versus a platinum electrode in H₂-purged 0.5 M H₂SO₄
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4 electrolyte; all potentials are reported versus this reversible hydrogen electrode (RHE). The
5 catalyst layer was pre-conditioned in cyclic voltammetric scans from 0 to 1.0 V at a scan rate of
6 100 mV/s to remove impurities and ensure fully wetting of the catalyst layer and stable cyclic
7 voltammograms (CVs). The capacitance of selected catalysts, as a relative measure of the surface
8 area of the catalysts exposed to the electrolyte, was calculated using the double layer charging
9 current region with potentials ranging from 0.1 to 0.4 V. Steady-state ORR polarization curves
10 were recorded in oxygen-saturated 0.5 M H₂SO₄ electrolyte using staircase voltammetry from 1.0
11 to 0 V with a potential step of 20 mV and a step period of 20 sec. The rotation rate of the RRDE
12 was 900 rpm.
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2.4 Catalyst Characterization

2.4.1 X-ray absorption spectroscopy

X-ray absorption spectroscopy (XAFS) measurements at the Fe *K*-edge were carried out in either transmission or fluorescence mode at the 10-ID and 10-BM beam lines at Argonne National Laboratory's Advance Photon Source. The near-edge regions of the XAFS spectra (7105 to 7155 eV) were fit using the linear combination algorithm of the *Athena* software (version 0.8.054), based on the *IFEFFIT* code [28], to the spectra for two Fe-containing standards: an oxygen adduct of Iron(III) phthalocyanine-4,4',4'',4'''-tetrasulfonic acid (Fe(III)pc) and iron carbide (Fe₃C). Fe(III)pc is a widely-used standard for the first-shell coordination environment of the Fe species typically observed in this class of catalysts and Fe in a first shell coordination environment similar to that of Fe(III)pc or its pyridinic rather than pyrrolic analog have been proposed to be the associated with the active site [8]. The Fe₃C was chosen as the other primary component of the

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4 synthesized materials based on the presence of characteristic features of Fe₃C in the k-space
5 representation and Fourier transform of the extended regions of the XAFS spectra.
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2.4.2 Inductively coupled plasma optical emission spectroscopy (ICP-OES)

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14 The weight loading of Fe in these catalyst samples were analyzed utilizing elemental analyses
15 by ICP-OES performed by Galbraith Laboratories.
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21 3. RESULTS AND DISCUSSION

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26 3.1 Effect of Carbon Source

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Black pearls carbon (BP) was used as the carbon source for the Fe-N-C catalysts as it has a high surface area and high electronic conductivity [29]. The weight percentage of phen with respect to the total weight of phen and BP was varied between 0 and 75 wt.% phen, while keeping the content of iron acetate constant (0.5 wt.% Fe with respect to total weight of precursors before heat treatment). Phen content higher than 75 wt.% (with respect to the weight of phen plus BP) resulted in heat treated powders that could not be dispersed into a usable ink for the evaluation of ORR activity. The Fourier transforms of the iron *K*-edge EXAFS data for the materials obtained after heat treatment and for the model compounds (Fe(III)pc and Fe₃C) are plotted in Fig. 1A. At phen contents between 25 and 60 wt.%, the Fourier transforms are similar to that of Fe(III)pc suggesting that the majority Fe in the samples is in a local coordination environment similar to that of Fe(III)pc (i.e., FeN₄O_x). The concentration of N-coordinated pyridinic or pyrrolic Fe sites has been experimentally correlated with ORR activity and these sites have been modeled to be the most active ORR active sites in Fe-based catalysts [8,30-36]. Iron carbide species, when encapsulated

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4 by N-doped carbon, have also been reported to be ORR active, however, FeN_x sites have been
5 reported to be more active for the four-electron reduction and to produce less peroxide [37]. As
6 noted in the Fourier transforms of the EXAFS data, there is a clear shift of the first shell $\text{Fe}-\text{N}/\text{O}$
7 bond length observed in the catalysts compared to that in the structurally well-defined $\text{Fe}(\text{III})\text{pc}$
8 [38]. According to Li et al., the shortening of the $\text{Fe}-\text{N}$ bond leads to changes in electronic
9 structure, such as positive shifting of the 3d-orbitals of central Fe and a larger charge transfer from
10 Fe to adjacent N facilitating oxygen adsorption on the FeN_4 sites [38]. Linear combination fitting
11 (LCF) of the XANES data for the catalysts to that of the Fe_3C and $\text{Fe}(\text{III})\text{pc}$ standards (Fig. 1B)
12 shows that the catalyst derived from precursor contains a mixture of Fe in coordination
13 environments similar to the two standards. When there is no phen in the initial mixture (i.e., no
14 nitrogen source in the precursors), the molar ratio of $\text{Fe}(\text{III})\text{pc}$ -like species determined from LCF
15 is 0.4, with nitrogen presumably derived from the ammonia treatment [16]. However, the ammonia
16 treatment alone is not enough to provide a high FeN_x content. The mole fraction of Fe in FeN_4O_x
17 coordination increases linearly with the concentration of the nitrogen-containing precursor up to
18 40 wt.% phen and plateaus between 40 and 50 wt.% phen. With increasing phen content, the mole
19 fraction of $\text{Fe}(\text{III})\text{pc}$ -like coordination increases to 0.74 at 50 wt.% phen. At higher phen contents,
20 the $\text{Fe}(\text{III})\text{pc}$ -like coordination decreases until reaching a mole fraction of 0.4 at 75 wt.% phen.
21 The ORR mass activity at 0.8 V correlates with the fraction of Fe in FeN_4O_x coordination between
22 25 and 60 wt.% phen, with a maximum ORR activity of 1.8 A/g ($E_{1/2} = 0.75$ V) at 50 wt.% phen.
23 When the initial concentration of phen is increased, there are various phenomena that might occur
24 simultaneously that explain the observed correlations. Phen, which contains N, contributes to the
25 increased formation of N-containing species while at the same time, during pyrolysis, loss of
26 carbon from the mixture will be higher when compared to the more thermally stable BP-rich
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4 samples. This leads to an increase in both the fraction of Fe in FeN_4O_x sites and the final total iron
5 content with increasing phen content. One can speculate that at higher concentrations of phen,
6 above 50 wt.%, there is a loss of both carbon and nitrogen, such that the overall iron content is
7 higher than the N content necessary to form the FeN_x sites and thus iron carbide is formed. It can
8 also be speculated that with increasing phen there is less carbon to stabilized FeN_x sites in the
9 graphene plane and hence more iron carbide prevails.
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21 When ZIF-8 is used (instead of BP), species with FeN_4O_x coordination are observed
22 predominantly in all samples from 0 to 75 wt.% phen (Fig. 2A), as determined from the Fourier
23 transform of the EXAFS data. At phen contents higher than 50 wt.%, the powders obtained after
24 pyrolysis were not dispersible in ionomer-solvent inks for RRDE ORR activity evaluation,
25 therefore characterization was not performed on these materials. The mole fractions of Fe in $\text{Fe}-$
26 N_4O_x and Fe_3C -like coordination and the ORR mass activity are plotted as a function of the phen
27 wt.% (relative to the weight of phen plus ZIF-8) in Fig. 2B. In the absence of phen, the initial mole
28 fraction of FeN_4O_x species is 0.8. This molar fraction remains constant up to 10% phen, decreases
29 at higher phen contents, then increases again to 40% phen. The initial decrease in FeN_x with
30 increasing phen is most likely due to the lower N content in phen (16 wt.%) versus that of ZIF-8
31 (25 wt.%). When comparing BP- vs ZIF-based syntheses (Fig. 1B vs 2B), ZIF clearly leads to a
32 higher mole fraction of FeN_4O_x species (maximum of 0.8 mole fraction versus 0.74). This is
33 certainly due to the additional nitrogen provided by ZIF-8 compared to the carbon-only BP. The
34 ORR mass activity shows a complex dependence on phen to ZIF-8 ratio and a complex relationship
35 with FeN_4O_x content, which was not observed in the case of the phen/BP system. By combining
36 two precursors that are undergoing major structural and chemical changes during heat treatment,
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4 one might expect synergetic or antagonist effects also dependent on the ratio of these two
5 precursors to the Fe content in the precursors. In addition, the presence of Fe_3C might boost the
6 ORR activity of nearby FeN_4 [39] such that the ultimate ORR activity of the material depends not
7 only on the absolute FeN_4 content, but on the proximity of Fe_3C to the FeN_4 sites. The highest
8 ORR activity was obtained at 40 wt. % phen, as was the case with the phen/BP system, with an
9 ORR mass activity of 8.6 A/g and a $E_{1/2}$ of 0.809 V, which is also the catalyst with the highest mole
10 fraction of FeN_4O_x . Proietti *et al.* studied the effect of phen content (0 to 75 wt. % versus ZIF-8)
11 and reported the highest fuel cell (tested in $\text{H}_2\text{-O}_2$) power density for a catalyst prepared using
12 20 wt.% phen, but found that the catalyst activity was independent of the phen content except for
13 0 and 75 wt.% [16].
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3.2 Effect of Fe loading

31 Using the phen and ZIF-8 contents resulting in the highest ORR mass activity and $E_{1/2}$ in the
32 0.5 wt.% Fe study described above (40 and 60 wt.%, respectively), the loading of iron (II) acetate
33 in the precursors was varied to give an Fe content from 0 to 1.0 wt.%. Fig. 3A shows the Fourier
34 transform of the EXAFS data. The final Fe loading in the catalyst and the mass activity as a
35 function of the initial Fe loading in the precursor are shown in Fig. 3B, while the speciation is
36 shown in Fig. 3C. Increasing the Fe content in the precursors up to 0.70 wt.% leads to an increase
37 in both the total Fe content and the Fe-N_x content in the catalyst (2.12 wt.% in the final catalyst)
38 and a decrease at precursor Fe contents > 0.70 wt.%. The loading of Fe_3C was found to increase
39 monotonically with increasing Fe precursor content (Fig. 3C). According to Li *et al.*, only a limited
40 number of ultra-fine FeO_x clusters formed during the heat treatment of Fe precursors can transform
41 into atomically-dispersed Fe-N_x , likely limited by the number of N-containing vacancies in the
42 catalyst. The effect of the Fe loading on the ORR activity is shown in Fig. 3D. The mass activity
43 increases with increasing Fe loading, reaching a maximum at 0.70 wt.% Fe loading and then
44 decreasing. The $E_{1/2}$ also increases with increasing Fe loading, reaching a maximum at 0.70 wt.% Fe
45 loading and then decreasing. The Fe-N_x content in the catalyst increases with increasing Fe loading,
46 reaching a maximum at 0.70 wt.% Fe loading and then decreasing. The Fe_3C content in the catalyst
47 increases with increasing Fe loading, reaching a maximum at 0.70 wt.% Fe loading and then
48 decreasing. The FeO_x content in the catalyst decreases with increasing Fe loading, reaching a minimum
49 at 0.70 wt.% Fe loading and then increasing. The Fe-N_x content in the catalyst increases with
50 increasing Fe loading, reaching a maximum at 0.70 wt.% Fe loading and then decreasing. The
51 Fe_3C content in the catalyst increases with increasing Fe loading, reaching a maximum at 0.70 wt.% Fe
52 loading and then decreasing. The FeO_x content in the catalyst decreases with increasing Fe loading,
53 reaching a minimum at 0.70 wt.% Fe loading and then increasing. The Fe-N_x content in the catalyst
54 increases with increasing Fe loading, reaching a maximum at 0.70 wt.% Fe loading and then
55 decreasing. The Fe_3C content in the catalyst increases with increasing Fe loading, reaching a maximum at
56 0.70 wt.% Fe loading and then decreasing. The FeO_x content in the catalyst decreases with increasing Fe
57 loading, reaching a minimum at 0.70 wt.% Fe loading and then increasing. The Fe-N_x content in the catalyst
58 increases with increasing Fe loading, reaching a maximum at 0.70 wt.% Fe loading and then
59 decreasing. The Fe_3C content in the catalyst increases with increasing Fe loading, reaching a maximum at
60 0.70 wt.% Fe loading and then decreasing. The FeO_x content in the catalyst decreases with increasing Fe
61 loading, reaching a minimum at 0.70 wt.% Fe loading and then increasing. The Fe-N_x content in the catalyst
62 increases with increasing Fe loading, reaching a maximum at 0.70 wt.% Fe loading and then
63 decreasing. The Fe_3C content in the catalyst increases with increasing Fe loading, reaching a maximum at
64 0.70 wt.% Fe loading and then decreasing. The FeO_x content in the catalyst decreases with increasing Fe
65 loading, reaching a minimum at 0.70 wt.% Fe loading and then increasing.

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4 carbon structure formed during heat treatment of ZIF-8 [38]. Excess Fe can react with the abundant
5 carbon in the system to form carbide. Iron is also known to enhance graphitization, which explains
6 the increase of Fe_3C with Fe concentration in the precursor [40,41]. The highest ORR activity,
7 9.45 A/g, was observed with 0.8 wt.% Fe in the precursor (1.90 wt.% Fe in the catalyst) with a $E_{1/2}$
8 of 0.816 eV, which is substantially higher than the previously-reported ORR mass activity of
9 2.8 A/g for this class of materials [42].
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21 **3.3 Effect of Fe precursors**
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24 The ORR mass activities at 0.8V for catalysts derived from twelve different Fe precursors (in
25 addition to Fe acetate) are shown in Table 1 with the optimized composition (40 : 60 weight ratio
26 of phenanthroline to ZIF-8 and 0.8 wt.% Fe of the mixture phen-ZIF). The iron precursors were
27 chosen because they contain porphyrin or phthalocyanine structure-like. The catalyst derived from
28 the precursor mixture containing iron acetate was found to be by far the most active, followed by
29 iron acetylacetone. All other catalysts were substantially less active than the iron acetate-derived
30 catalyst. A plot of ORR mass activity versus electrochemical capacitance for the catalysts derived
31 from the different iron precursors indicates that the ORR mass activity may be correlated with
32 catalyst surface area, with the exception of the catalyst derived from the iron acetate precursor
33 (Fig. 4). There are apparently additional effects of iron acetate on the physicochemical properties
34 of the resulting catalyst that are beneficial to the catalyst's ORR activity needing further
35 exploration.
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55 **Table 1.** Mass activity at 0.8V for catalysts derived from various iron precursors (40 : 60 weight
56 ratio of phenanthroline to ZIF-8 and 0.8 wt.% Fe of the mixture phen-ZIF).
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Iron Precursors	Mass activity (A/g)
Iron (II) acetate	9.45
Iron (III) acetylacetone	4.41
Iron (III) meso-tetra (2,4,6 trimethyl phenyl) porphine chloride	3.13
Ferrocenium tetrafluoroborate	3.95
Iron (II) oxalate dihydrate	4.81
Iron (III) meso-tetraphenylporphine u-oxodimer	3.99
2,3,7,8,12,13,17,18-octaethyl-21h,23h-porphine iron (III) acetate	4.07
Iron (III) phthalocyanine-4,4',4'',4'''-tetrasulfonic acid	2.52
5,10,15,20-tetraphenyl-21h,23h-porphine iron (III) chloride	3.01
Iron (III) meso-tetra (4-sulfonatophenyl) porphine chloride (acid form)	2.03
Iron (III) meso-tetra(4-carboxylphenyl) porphine chloride	1.22
5,10,15,20-tetrakis(pentafluorophenyl)-21h-,23h-porphyrin iron (III) chloride	0.99
Bis(cyclopentadienyl)iron	4.51

The short-term stability of the catalyst synthesized using the optimized conditions determined in this study was evaluated by measuring successive ORR traces, as shown in Fig. 5. There is an initial loss of 6 mV after the second potential cycle, but no additional losses were observed in the third potential cycle.

4. CONCLUSIONS

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4 This work evaluated the synthesis variables of identity of iron precursor, iron loading, and
5 carbon and nitrogen source content (black pearls carbon, phenanthroline, and ZIF-8) on the ORR
6 activity in acidic electrolyte of Fe-N-C catalysts obtained after heat treatment of the precursor
7 mixture. The ORR activities determined using the thin-film RDE technique are correlated with Fe
8 speciation in the catalysts determined using Fe K-edge X-ray absorption spectroscopy (XAFS).
9 The major findings of this work are:
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18 • Increasing phenanthroline content in the ball-milled mixture of Fe, phenanthroline, and BP
19 carbon precursor promotes formation of species with Fe phthalocyanine-like first shell
20 coordination (FeN_4O_x) at intermediate concentrations and formation of Fe carbide at high
21 concentrations, with the ORR mass activity correlated with FeN_4O_x content;
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27 • Use of ZIF-8 versus the black pearls-phenanthroline source of carbon and nitrogen
28 promotes formation of species with FeN_4O_x first shell coordination;
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31 • The weight percentage of species with FeN_4O_x first shell coordination increases linearly
32 with increasing Fe content in the precursor up to 0.5 wt.% and reached the maximum at 0.8
33 wt.% then decreases at higher Fe contents. A decrease in total Fe content and formation of
34 Fe carbide are responsible for this limitation to the maximum content of Fe species with
35 FeN_4O_x first shell coordination;
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38 • When using different Fe-N-C compounds as the source of Fe, the different Fe compounds
39 resulted in different catalyst electrochemical surface area, as evidenced by changes in the
40 double layer capacitance, and ORR activity was correlated with the surface area with the
41 exception of the catalyst derived from iron acetate;
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44 • The maximum ORR activity observed in this study of Fe-N-C catalysts derived from ball-
45 milled iron salt, nitrogen, carbon precursors was observed for a catalyst synthesized using
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4 60 wt.% ZIF, 40 wt.% phenanthroline and 0.8 wt.% Fe in the precursor and iron acetate as
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6 the Fe source.
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ACKNOWLEDGMENTS

14 The authors would like to thank Ulises Martinez from Los Alamos National Laboratory for
15
16 providing oxidized Black Pearls. This work was supported by the U.S. Department of Energy,
17
18 Energy Efficiency and Renewable Energy, Hydrogen and Fuel Cell Technologies Office under the
19 auspices of the Electrocatalysis Consortium (ElectroCat). This research used the resources of the
20 Advanced Photon Source (APS), a U.S. Department of Energy (DOE) Office of Science User
21
22 Facility operated for the DOE Office of Science by Argonne National Laboratory under Contract
23 No. DE-AC02-06CH11357. Argonne National Laboratory is managed for the U.S Department of
24 Energy by the University of Chicago Argonne, LLC, also under contract DE-AC-02-06CH11357.
25
26 XAFS data were acquired at MRCAT at the APS. MRCAT operations are supported by the
27
28 Department of Energy and the MRCAT member institutions.
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List of Figures

Fig. 1. Fourier transforms of the Fe K-edge EXAFS data as a function of 1,10-phenanthroline loading (wt.%) in the initial mixture of phenanthroline and BP (not phase corrected, Fe(III)pc and Fe₃C data shown for comparison) (A) mole fraction of Fe₃C-like and Fe(III)pc-like coordination, determined by XANES LCF, and ORR mass activity at 0.8V as a function of 1,10-phenanthroline loading (initial target loading of 0.5 wt.% Fe using iron (II) acetate) (B).

Fig. 2. Fourier transform of Fe K-edge EXAFS data (not phase corrected) as a function of 1,10-phenanthroline loading (wt.%) in the initial mixture of 1,10-phenanthroline and ZIF-8; data for Fe(III)pc and Fe₃C standards shown for comparison (A), mole fraction of Fe₃C-like and Fe(III)pc-like coordination determined by LCF, and ORR mass activity at 0.8V as a function of 1,10-phenanthroline loading (initial target loading of 0.5 wt.% Fe using iron (II) acetate) (B).

Fig. 3. Fourier transform of Fe K-edge EXAFS data (not phase corrected) as a function of Fe content (wt.%) in the initial mixture of 1,10-phenanthroline and ZIF-8; Fe(III)pc and Fe₃C standard data shown for comparison (A), actual Fe loading determined by ICP and mass activity at 0.8 V (B), Fe(III)pc and Fe₃C loading (wt.%) determined by XANES LCF (C), at 40 wt.% 1,10-phenanthroline and 60 wt.% ZIF-8 (iron (II) acetate used as precursor).

Fig. 4. Mass activity as a function of capacitance for all the catalysts using various Fe precursors from Table 1 in blue dots (except using iron acetate, red dot).

Fig. 5. First, second, and third ORR potential sweeps for the Fe-N-C catalyst derived from precursors with 0.8 wt.% (iron (II) acetate), 40 wt.% 1,10-phenanthroline, and 60 wt.% ZIF-8. Conditions: 0.6 mg-cat/cm², 900 rpm, O₂-saturated 0.5 M H₂SO₄.

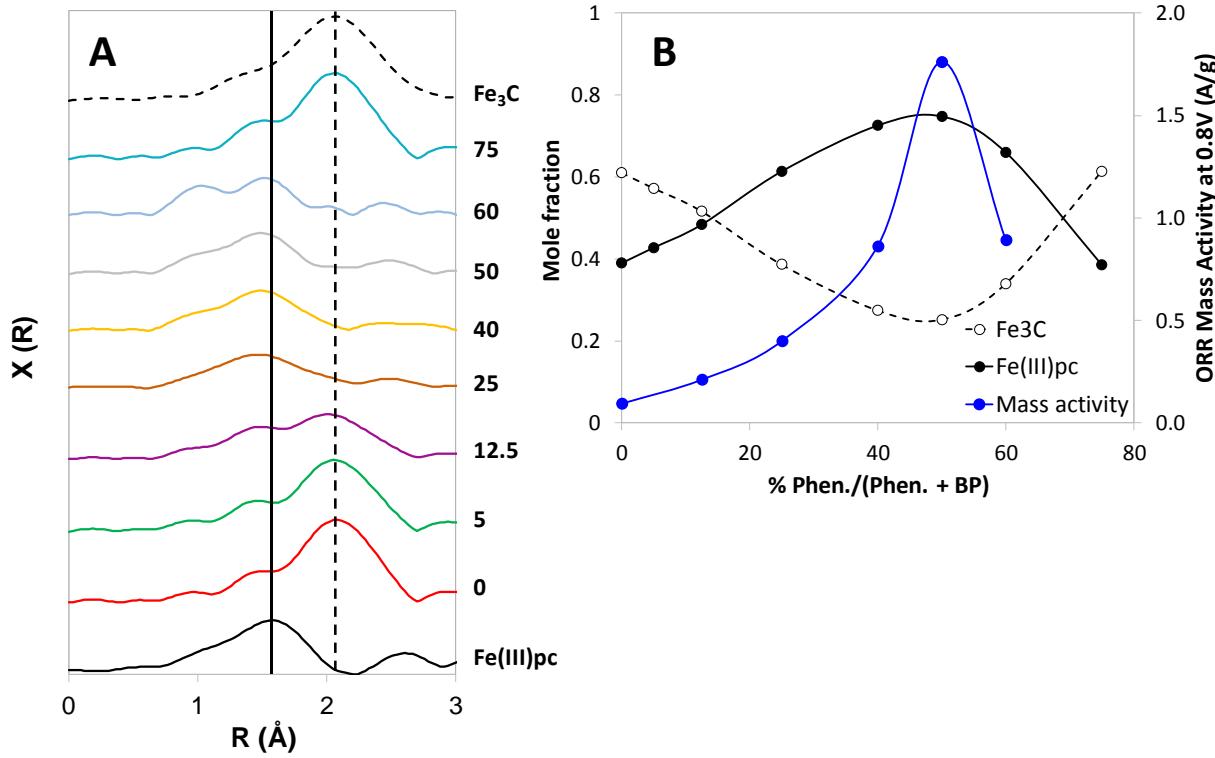


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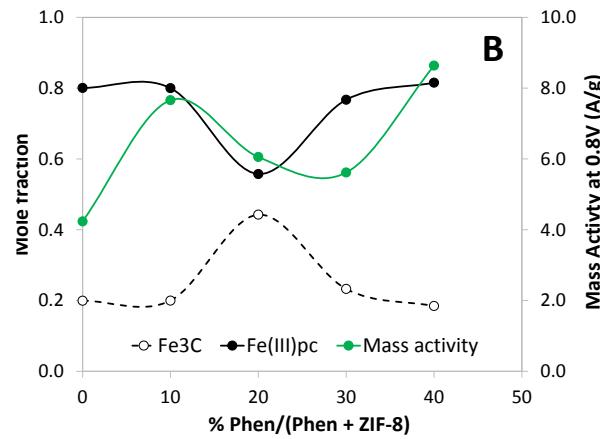
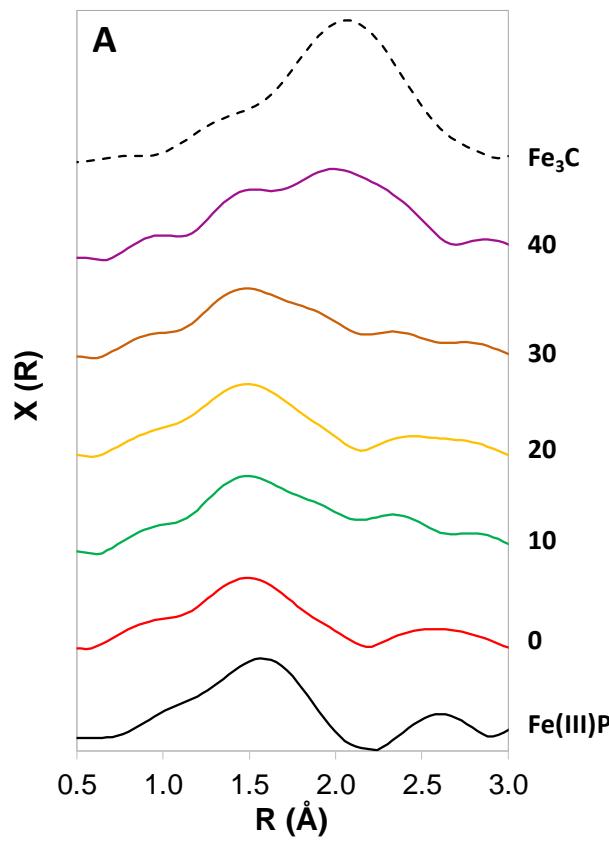


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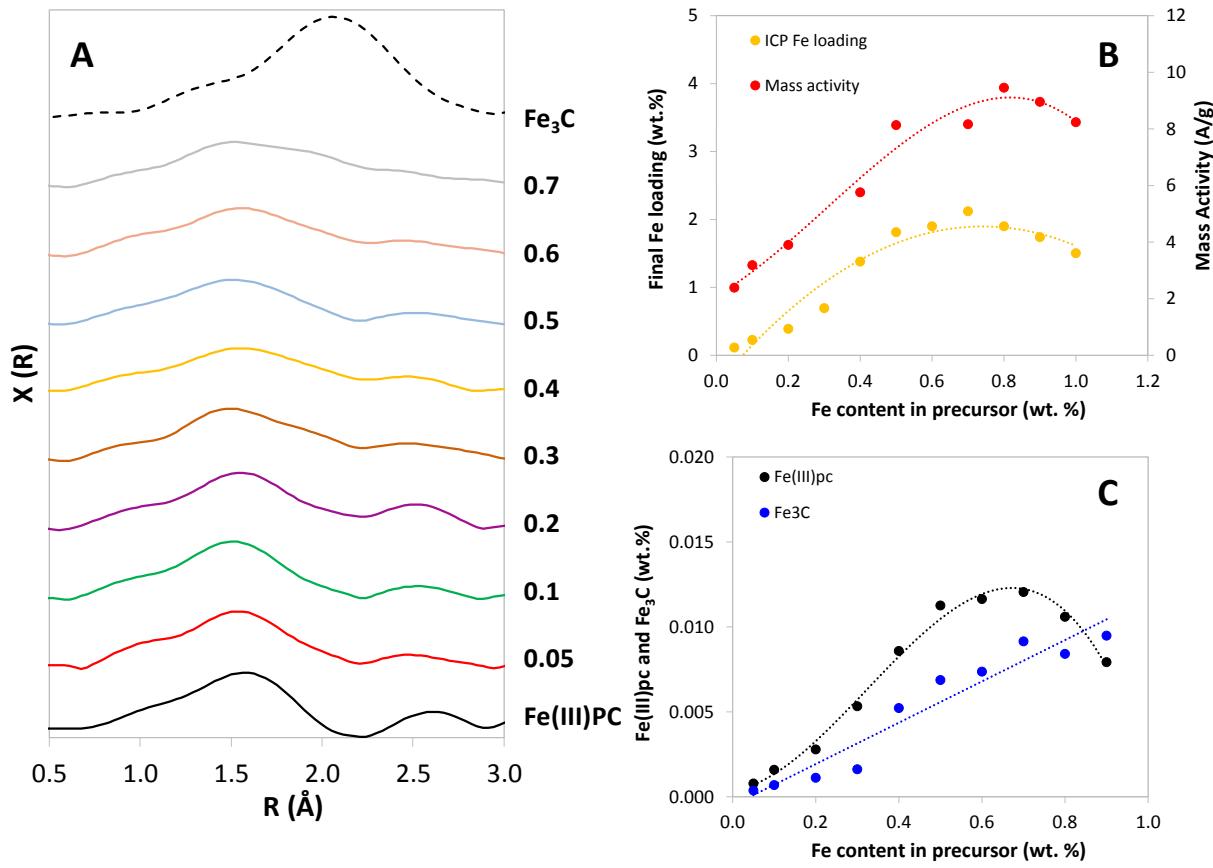


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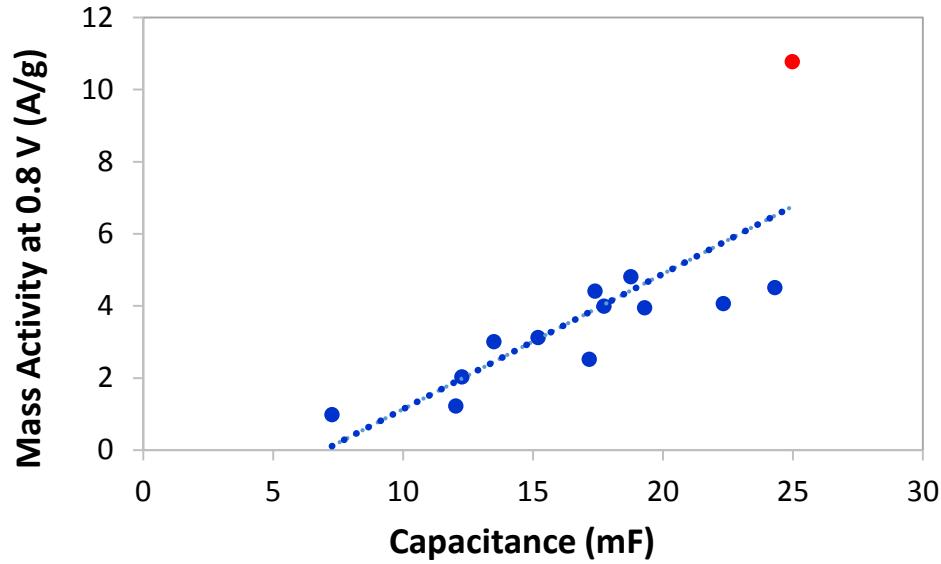


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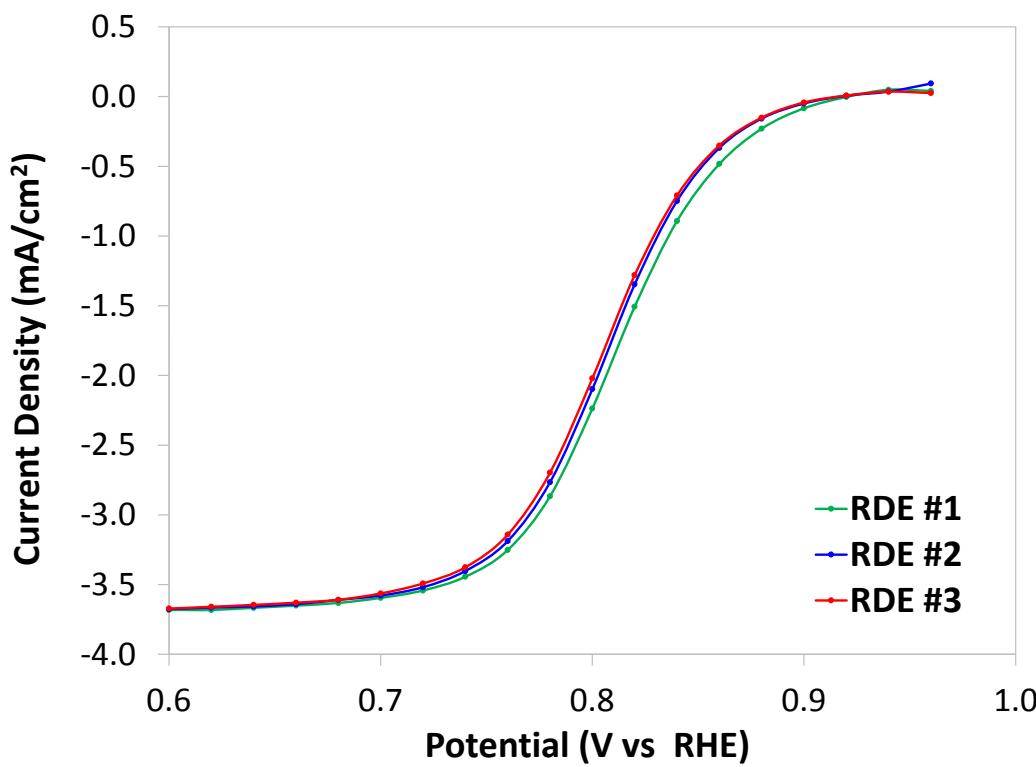


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Subject: Manuscript Submission to Special Issue of *Electrochimica Acta*

Dear Editor,

Please find enclosed our manuscript entitled "*Enhancing the Activity of Fe-N-C Oxygen Reduction Reaction Electrocatalysts by High-Throughput Exploration of Synthesis Parameters*" by Magali S. Ferrandon, Jaehyung Park, Xiaoping Wang, Eric Coleman, A. Jeremy Kropf, and Deborah J. Myers. This paper is in response to your recent message to Dr. Deborah Myers inviting us to submit our work to the special issue on the themed collection on "Single Atom Electrocatalysts".

In our manuscript, an automation platform and a multi-port ball-milling were utilized to evaluate the effects of synthesis variables, such as identity of iron precursor, iron loading, and carbon and nitrogen sources (black pearls carbon, phenanthroline, and ZIF-8) and content on the oxygen reduction reaction (ORR) activity of iron-nitrogen-carbon (Fe-N-C) catalysts in acidic electrolyte. The ORR activities in acidic electrolyte, determined using the thin-film RDE technique, are correlated with Fe speciation in the catalysts determined using Fe K-edge X-ray absorption spectroscopy (XAFS). In summary, in our exploration of the synthesis variables in this class of synthetic procedure for single-atom Fe-N-C ORR catalysts, we obtained the highest ORR activity using 60 wt.% ZIF, 40 wt.% phenanthroline and 0.8 wt.% Fe in the precursor mixture and iron acetate as the Fe source. The ORR activity obtained in our study was greater than three times that reported in the literature for this synthesis method. The ORR activity was correlated with the concentration of Fe in an FeN_4O_x first shell coordination environment, as determined by linear combination fitting of the near-edge region of the XAFS spectra.

We are looking forward to receiving your comments and suggestions.

Sincerely,

Magali Ferrandon, on behalf of all the co-authors.

Declaration of interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests: