



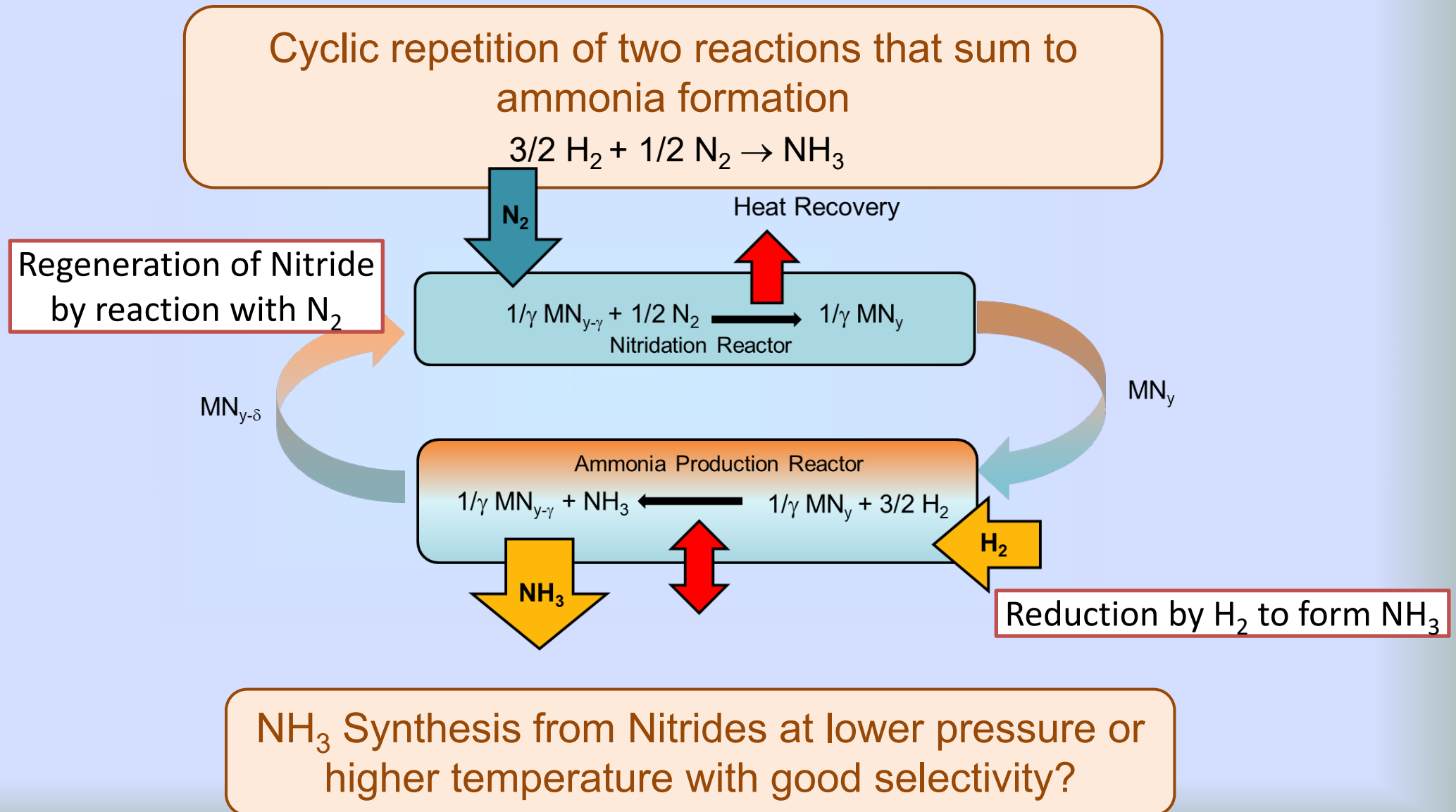
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# Solar Ammonia Production via Novel Two-step Thermochemical Looping of a $\text{Co}_3\text{Mo}_3\text{N}/\text{Co}_6\text{Mo}_6\text{N}$ pair

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Presented by James E. Miller

**Arizona State University**





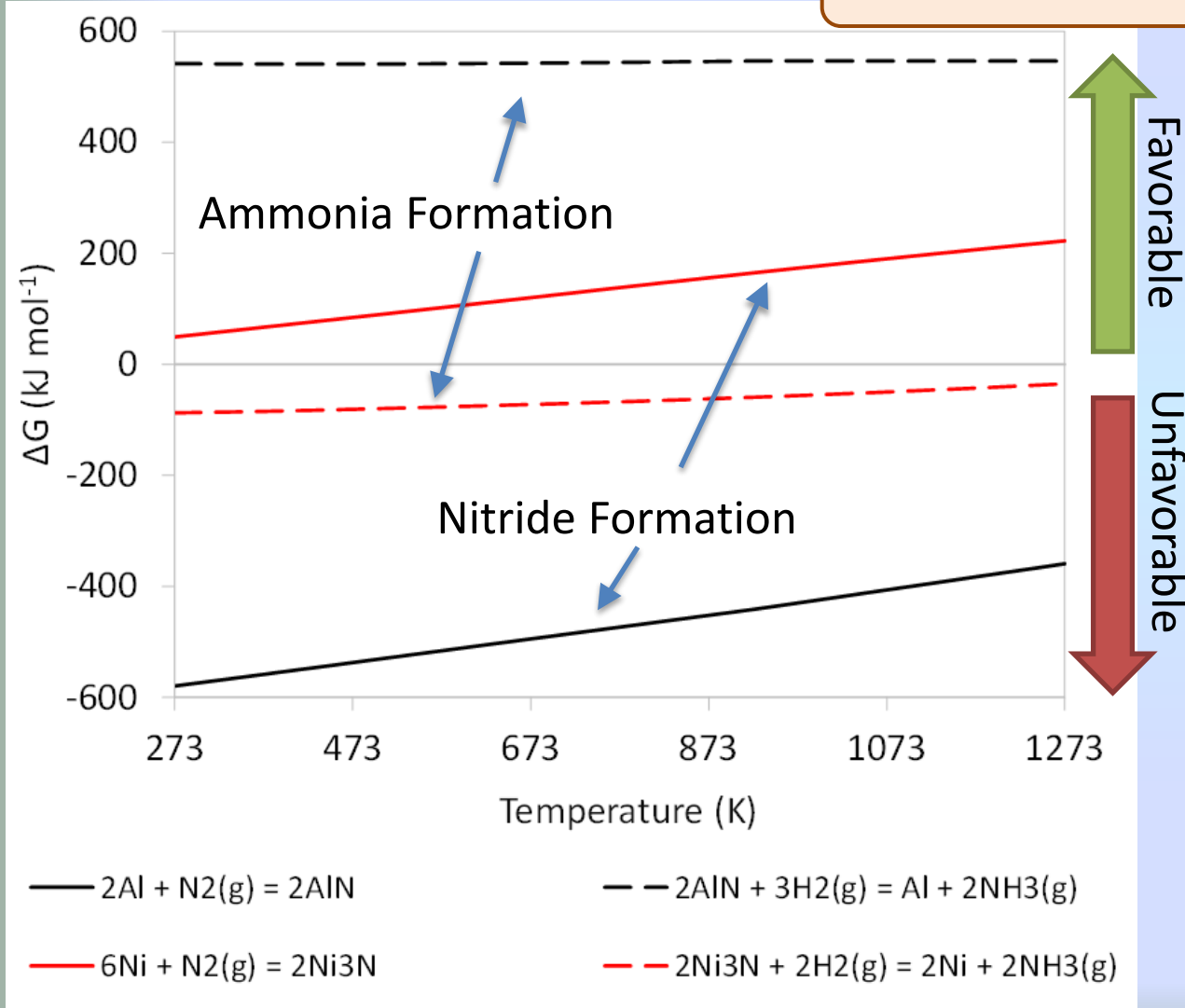
## Challenge: Identify and optimize a metal nitride

- Tuning the nitride thermodynamics to the reaction
- Reaction with the bulk, not (exclusively) surface-catalyzed
  - $\text{NH}_3$  dissociates (thermodynamically unfavorable relative to  $\text{H}_2 + \text{N}_2$ ) at high temperature
- Nitrogen diffusion in metal nitrides slow? (~~nitrogen conductors~~)
- Nitride synthesis can be difficult – e.g. reacting under flowing  $\text{NH}_3$  at high temperature

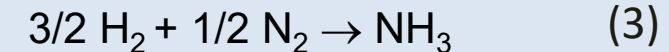
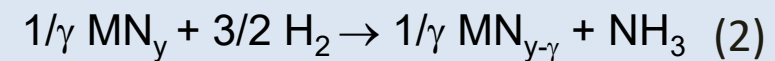
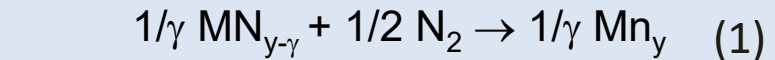




## Basic Thermodynamic Principles



- Thermodynamic of the two reactions comprising the cycle inextricably linked.

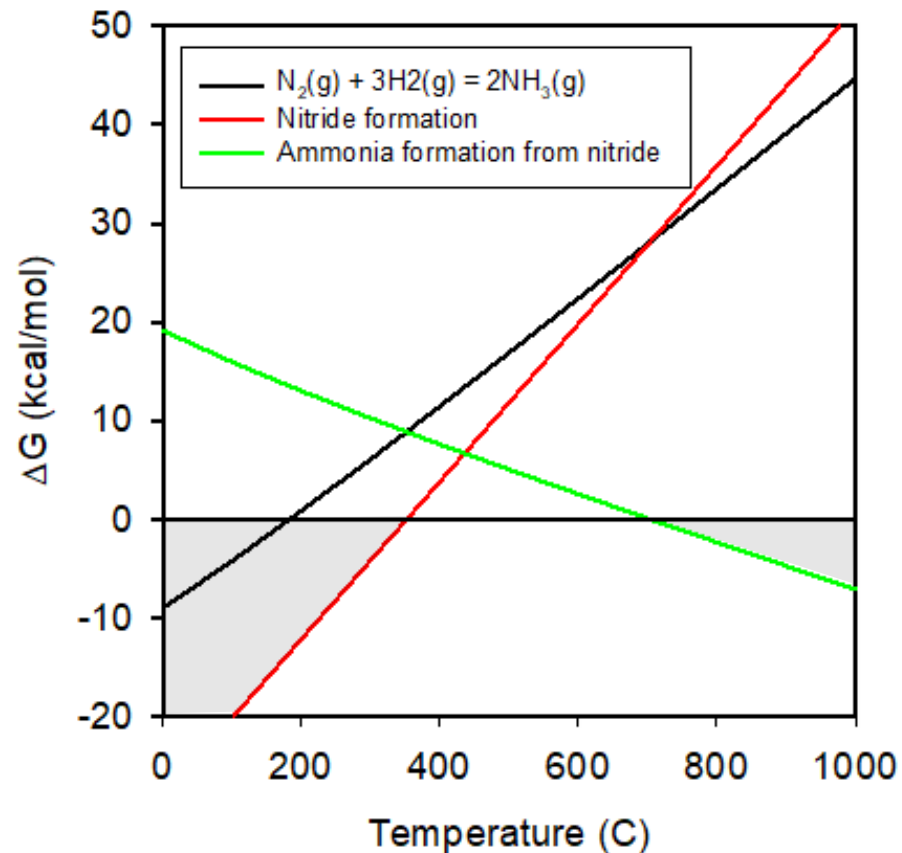


$$\Delta G_1 + \Delta G_2 = \Delta G_3$$

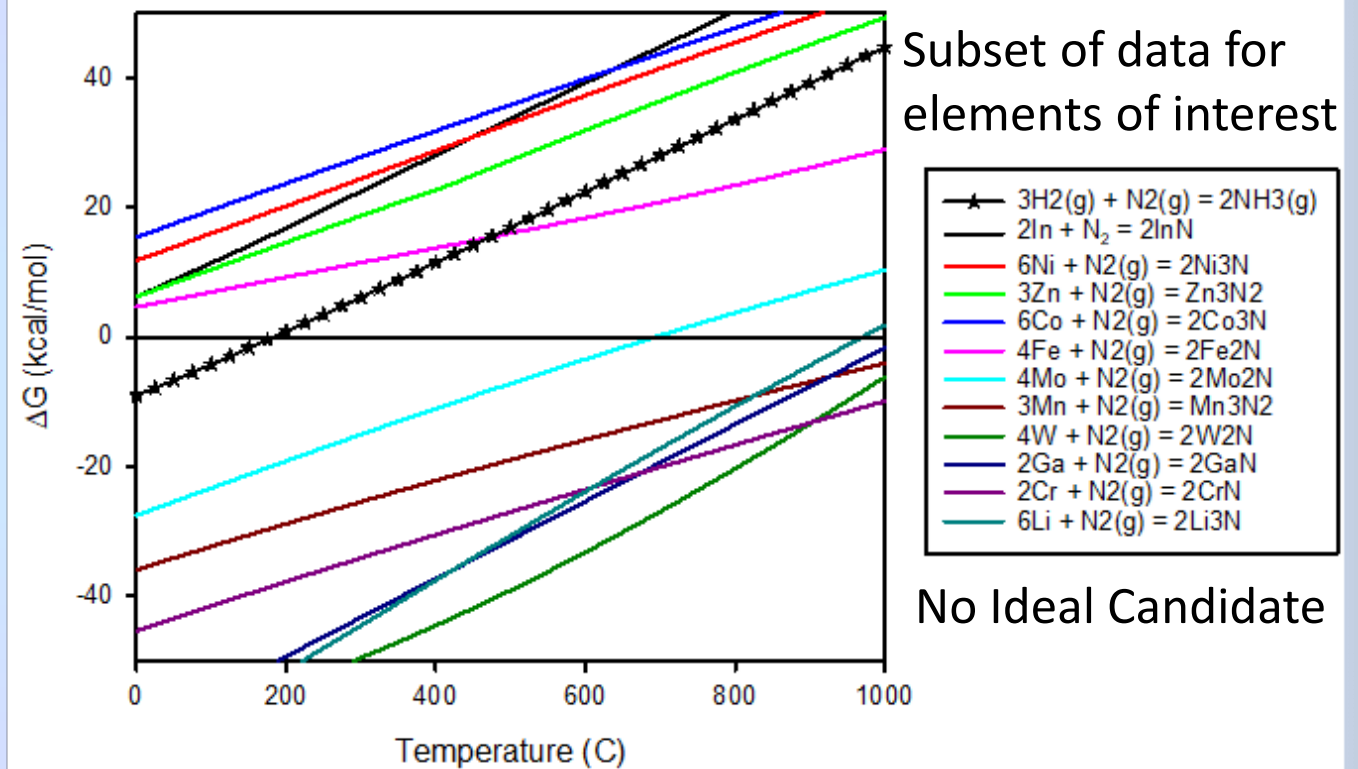
- The more favorable is nitridation, the less favorable is ammonia production, and vice versa.
- Ammonia formation is exothermic – unconventional for a cycle.



## Begin with Survey of Binary Nitrides & “Conventional” Cycle Construct



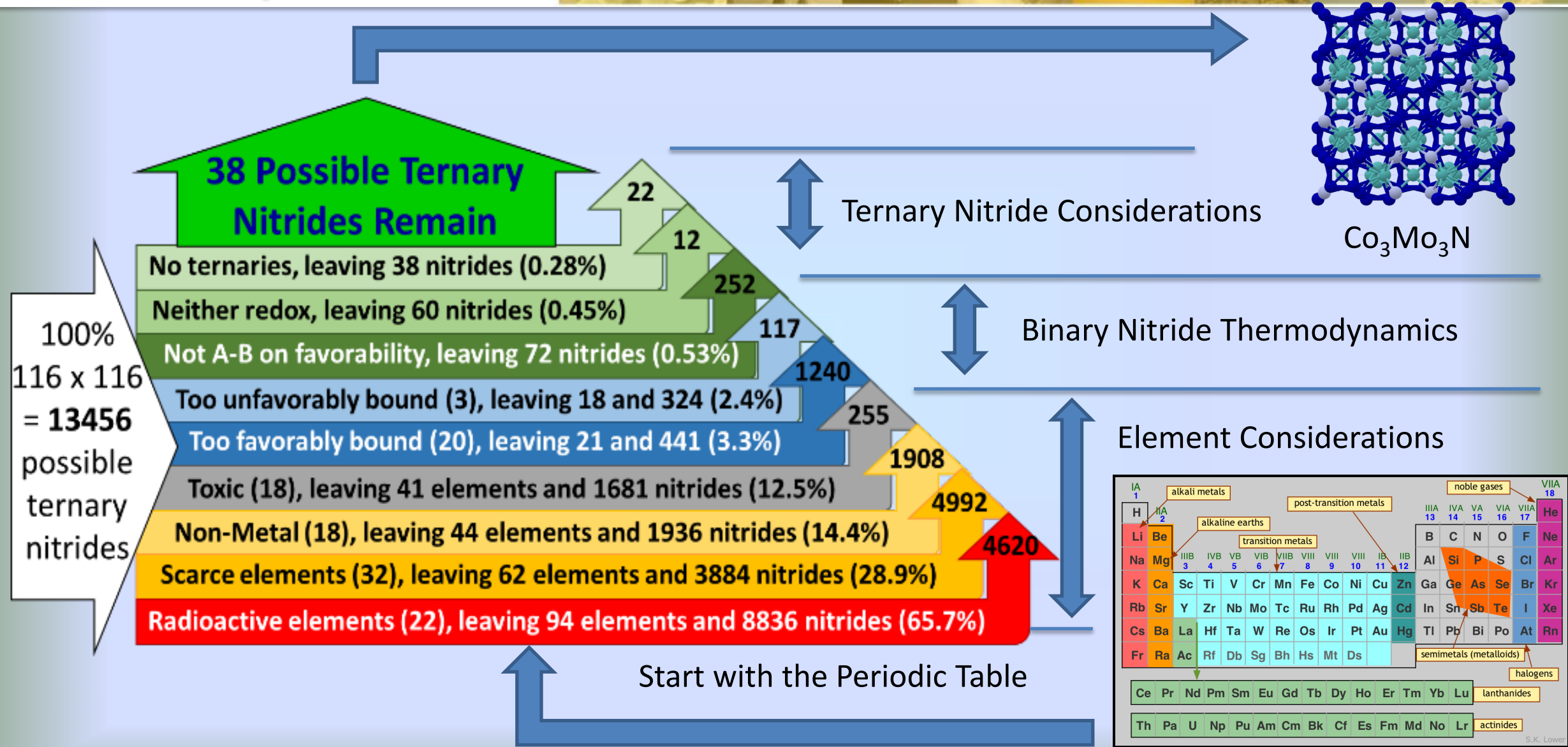
Rethink these cycles a bit –  
e.g. impact of pressure



Subset of data for  
elements of interest

No Ideal Candidate

Ternaries (two metals) offer the opportunity to tune  
the thermo to that required for a two step cycle.





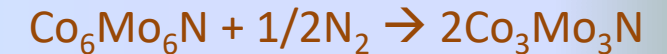
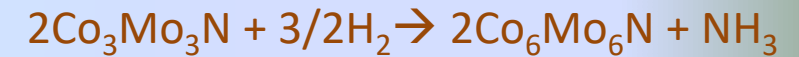


## After Ternary Considerations 38(+) Combinations of Interest

			Cation Redox Active						Cation Redox Inactive					
Element			Cr	Fe	Mn	Mo	V	W	Ba	Ga	Li	Mg	Na	Sr
kJ mol <sup>-1</sup>			-56.3	-13.8	-33.1	-60.2	-178	-42.8	-137	-83.3	-132	-174	-3.94	-135
Cation Redox Active	Co	30.5		8.3	-1.3	-14.8	-73.7	-6.1	-53.4		-50.5	-71.5	13.3	-52.2
	Cu	119.3			43.1				-9.0	18.0	-6.1	-27.1		-7.8
	Ge	2.1	-27.1	-5.9	-15.5		-87.9		-67.6		-64.7	-85.7	-0.9	-66.4
	Ni	22.8		4.5	-5.2	-18.7	-77.5	-10.0	-57.3		-54.4	-75.4	9.4	-56.1
Cation Redox Inactive	Sn	46.0	-5.2		6.4									
	Zn	38.7	-8.8	12.4	2.8	-10.7	-69.6							

### Co<sub>3</sub>Mo<sub>3</sub>N (CMN331)

Can undergo reversible phase change to CMN661, losing 50 mol% of nitrogen:



Both phases crystallize in same space group (Fd-3m) – facilitate kinetics?

Reports that material can be regenerated directly by N<sub>2</sub>

\*Hunter, S.M., McKay, D., Smith, R.J., Hargreaves, J.S.J., Gregory, D.H., 2010, Chemistry of Materials, 22(9), pp. 2898-2907.  
Gregory, D.H., Hargreaves, J.S.J., Hunter, S.M., Catalysis Letters, 2011, 141(1), pp. 22-26.



Solution:  
 $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O} +$   
 $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot$   
 $4\text{H}_2\text{O}$

Heat the solution  
to 80°C:  
Purple precipitate

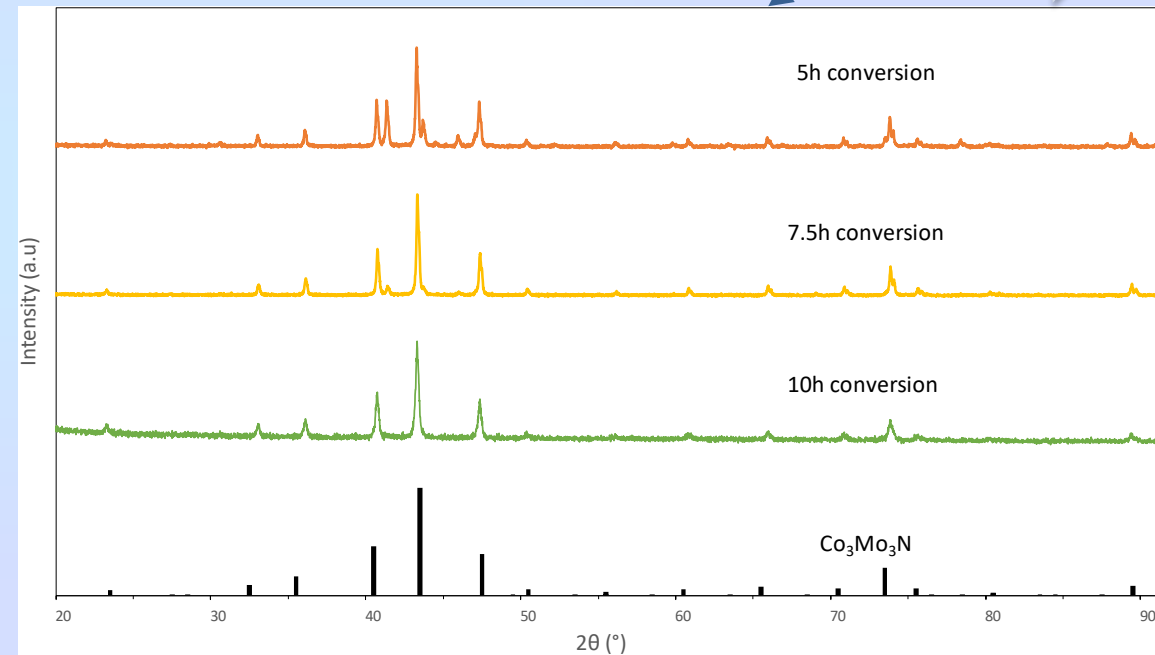
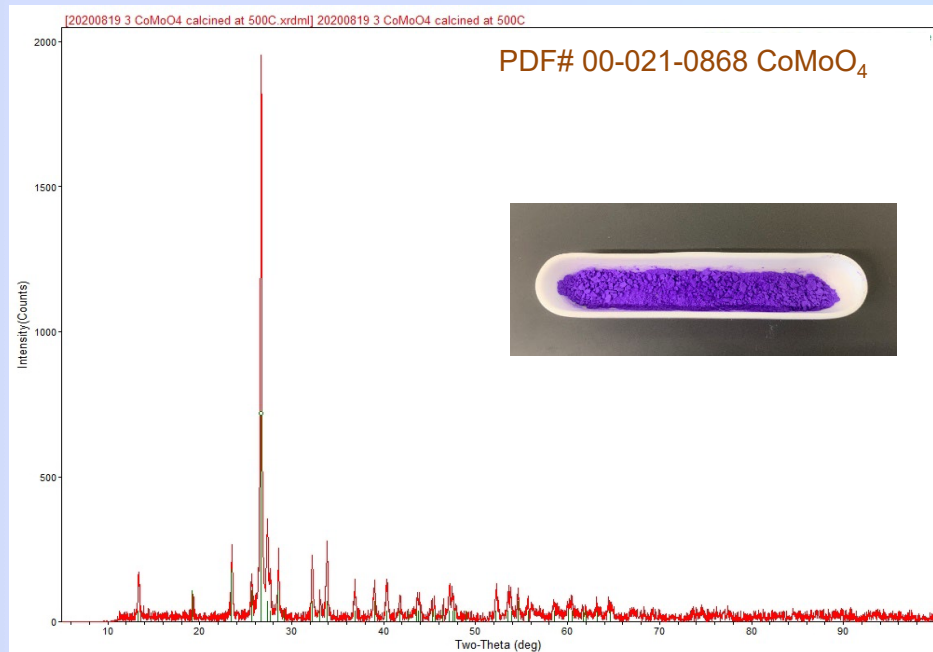
Vacuum  
filtration

Dry overnight at  
150°C:  
 $\text{CoMoO}_4 \cdot x\text{H}_2\text{O}$

Calcine at 500°C  
for 3h:  
 $\text{CoMoO}_4$

React at 785 °C,  
10%  $\text{H}_2/\text{N}_2$

$\text{Co}_3\text{Mo}_3\text{N}$



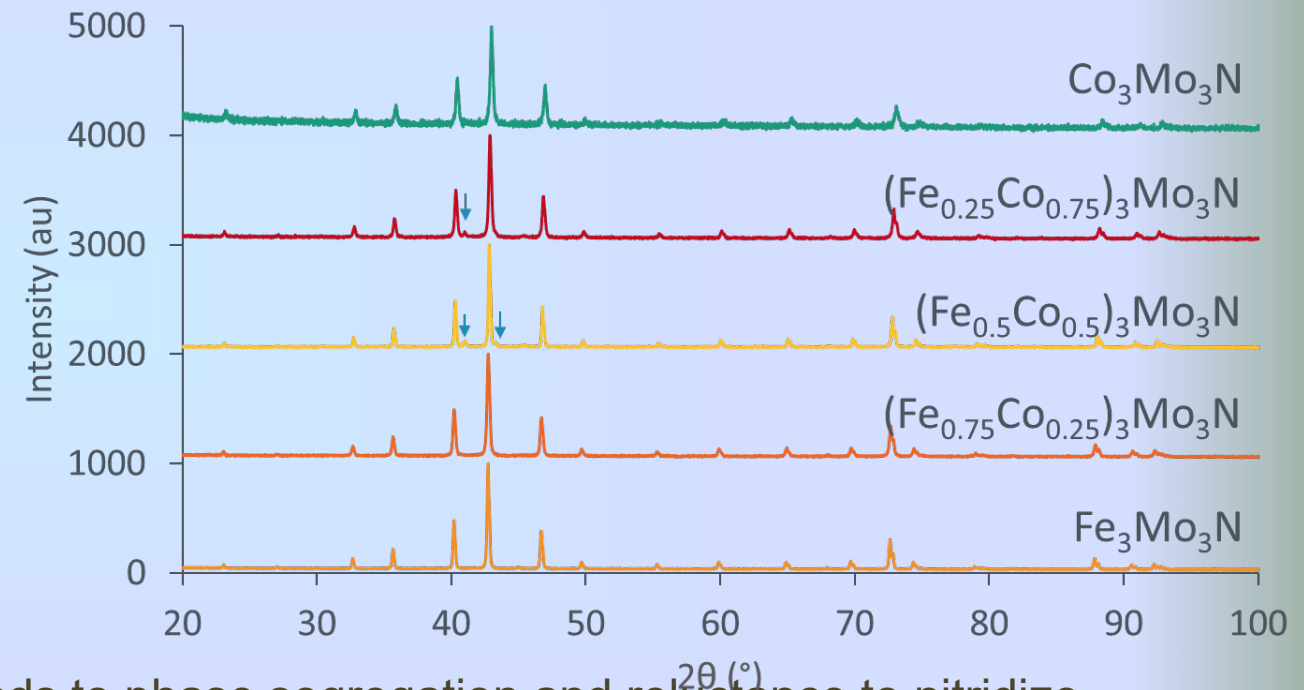
Synthesis of oxide precursor followed by nitridation in 10%  $\text{H}_2$  results in single phase  $\text{Co}_3\text{Mo}_3\text{N}$  (somewhat milder synthesis conditions than reported ammonolysis<sup>1</sup>)





A family of single-phase  $A_3B_xN$  ( $A=Co, Ni, Fe$ ;  $B=Mo, W$ ;  $x = 2, 3$ ) ternary and quaternary nitride solid solutions has been synthesized

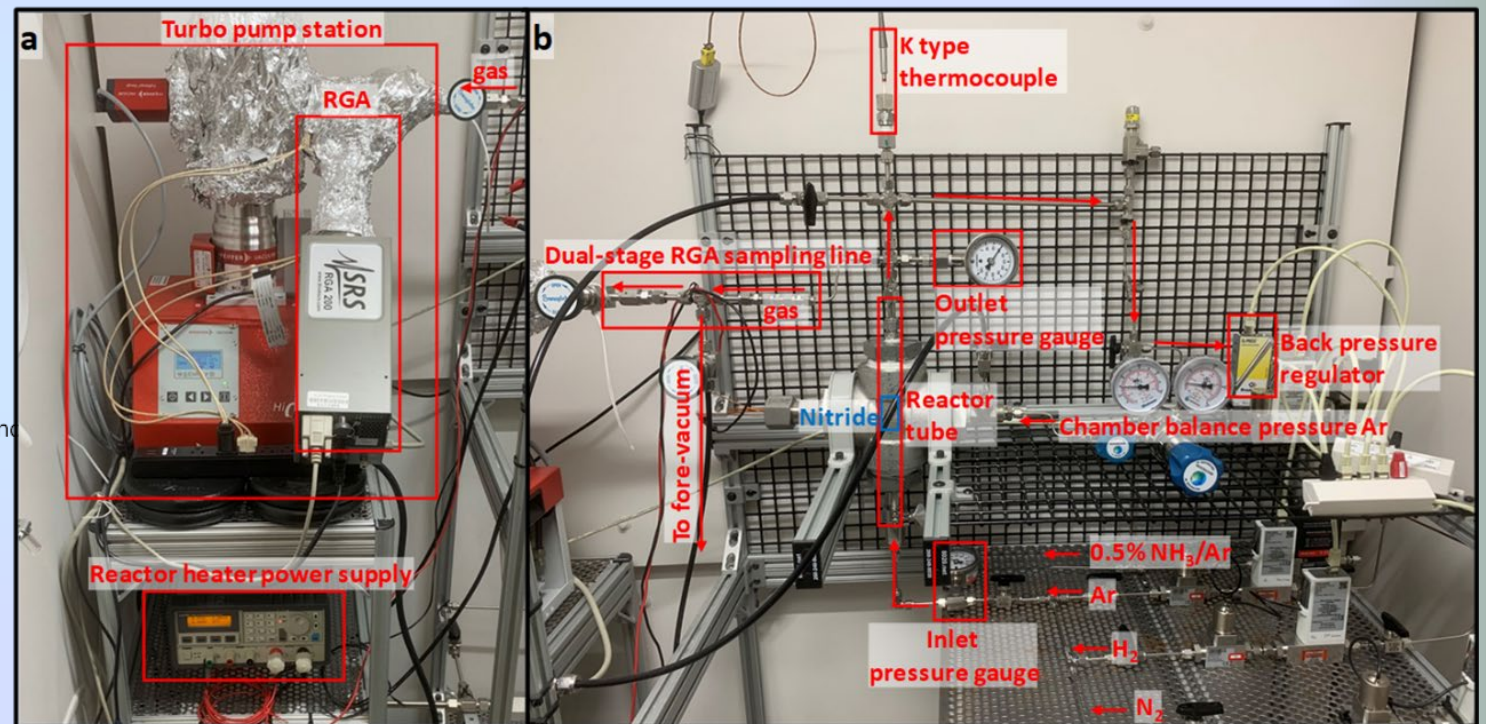
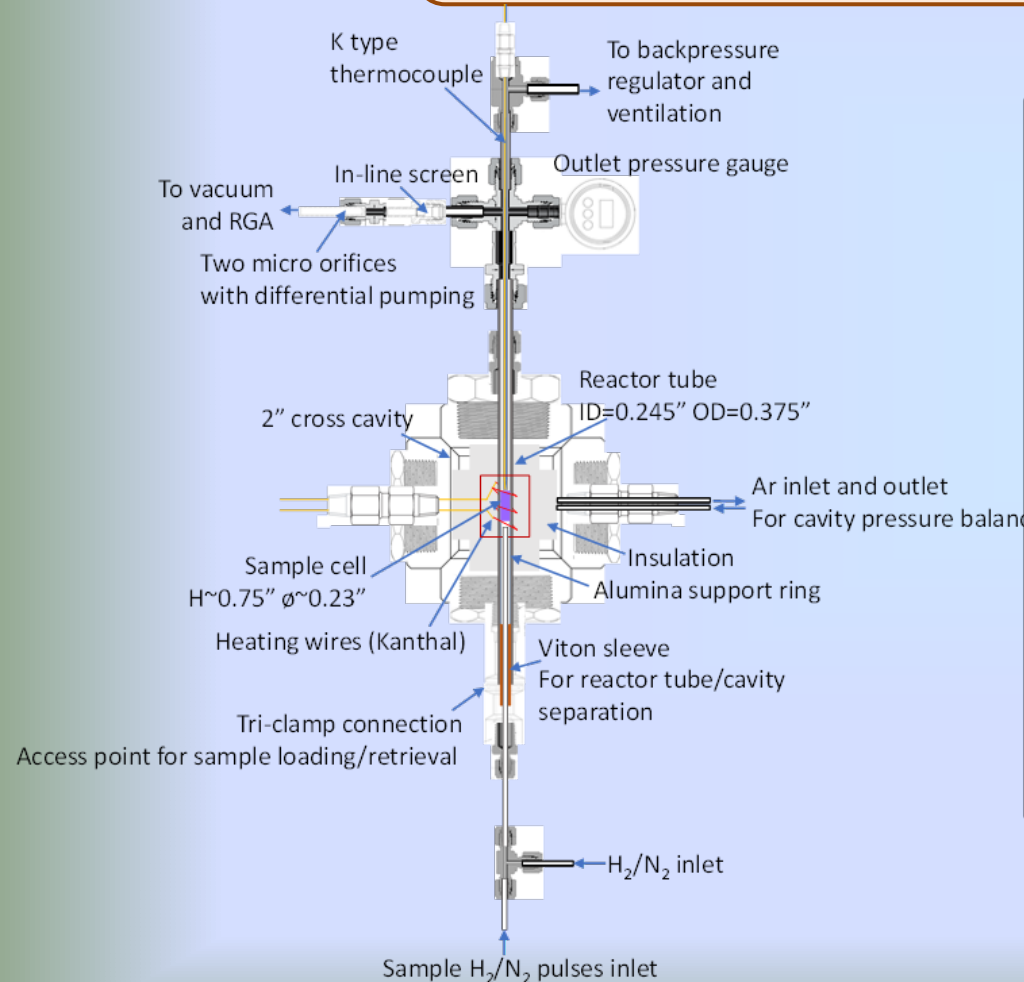
Composition Target	Phase (> 95% via XRD)
$Co_3Mo_3N$	331
$(Co_xNi_{1-x})_2Mo_3N$ ( $x = 0.25, 0.5, 0.75$ )	231
$Ni_2Mo_3N$	231
$(Fe_xNi_{1-x})_2Mo_3N$ ( $x = 0.25, 0.5$ )	231
$Fe_3Mo_3N$	331
$(Co_xFe_{1-x})_3Mo_3N$ ( $x = 0.25, 0.5, 0.75$ )	331
$Co_3(W_xMo_{1-x})_3N$ ( $x = 0.005 - 0.05$ )	331
$(Ni_xCo_{1-x})_3Mo_3N$ ( $x = 0.005 - 0.05$ )	331



- W > 5% in  $Co_3Mo_3N$  ("331") B-site substitution leads to phase segregation and reluctance to nitridize
- Ni > 5% in  $Co_3Mo_3N$  or  $Fe_3Mo_3N$  A-site substitution leads to phase segregation and preference of  $Ni_2Mo_3N$  ("231") structure



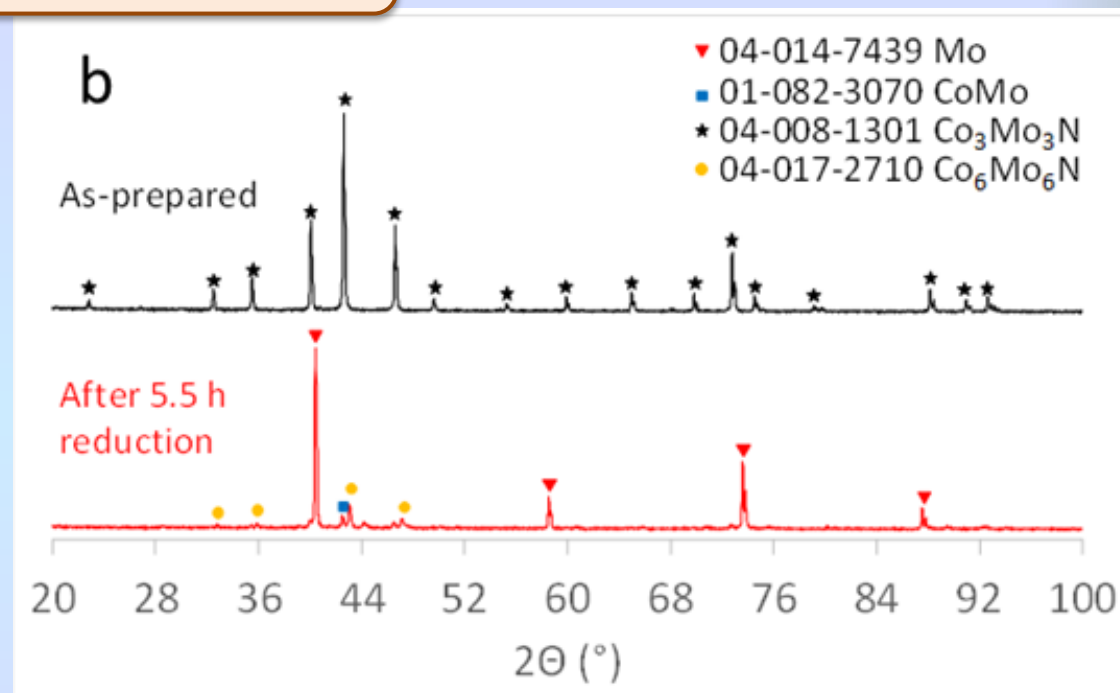
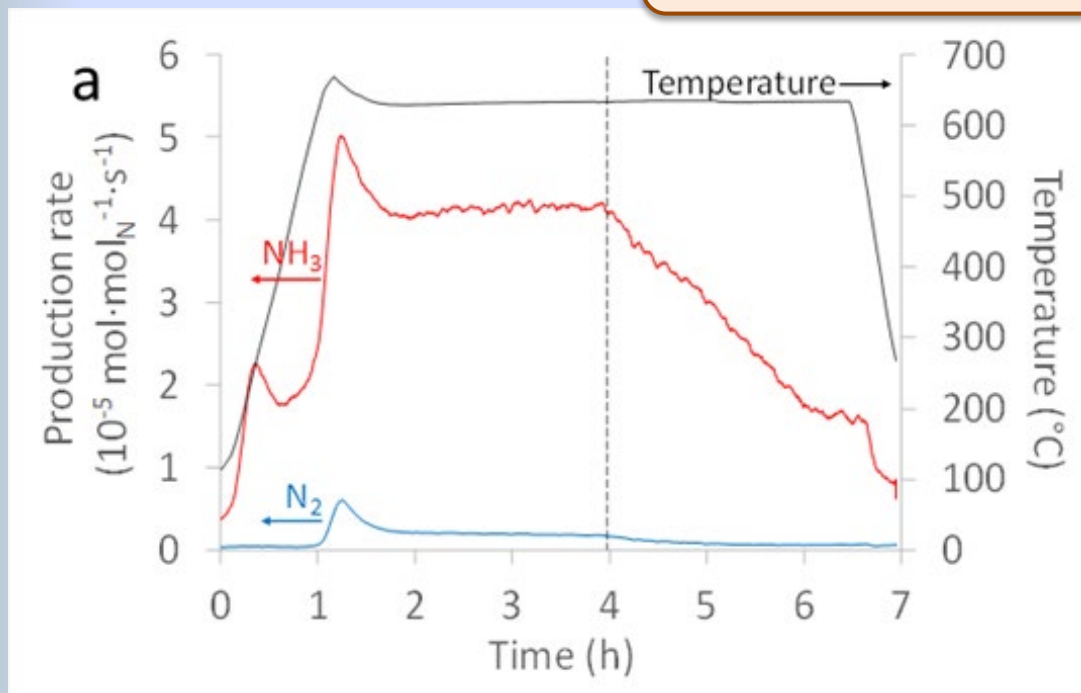
Reactor designed to perform  $\text{NH}_3$  synthesis and nitridation under variable pressure and temperature, up to 30 bar and 800 °C, respectively







## Reactions of $\text{Co}_3\text{Mo}_3\text{N}$



Two regions apparent in extended reduction experiments

Nearly constant rate – 331 (662) → 661

Linearly decreasing rate – 661 → Metal



Steady production rates were calculated using averages of the last 10 min of stabilized rate data before cool-down

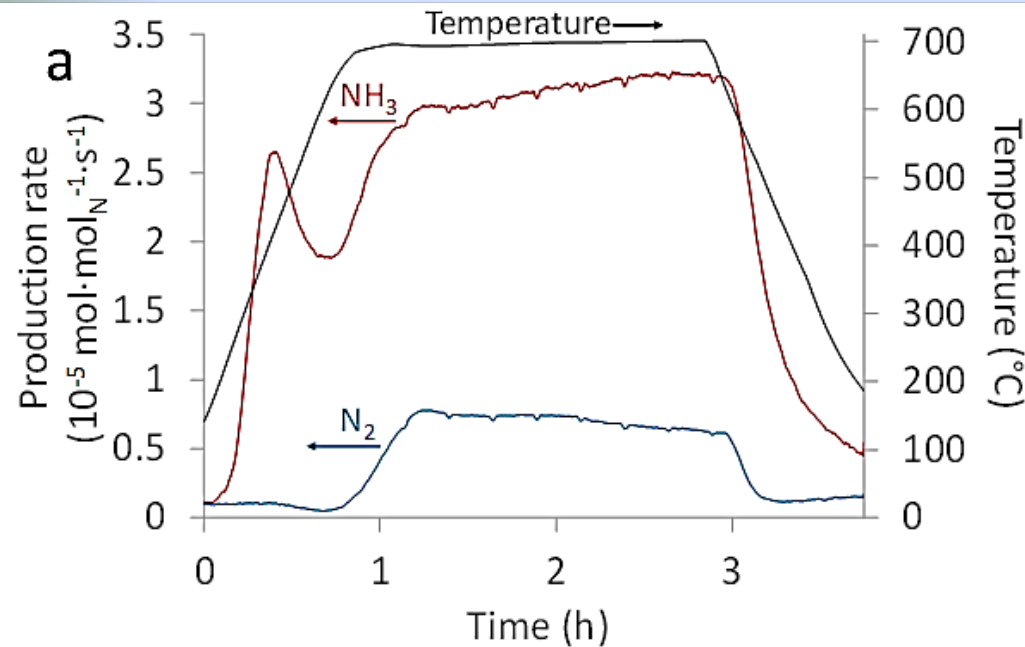
Reacted solid-state nitrogen was calculated by adding  $\text{NH}_3$  yield and two times of  $\text{N}_2$  yield (theoretical max  $\text{CMN331} \rightarrow \text{CMN661} = 0.5$ )

Selectivity to  $\text{NH}_3$  was calculated by percentage of  $\text{NH}_3$  yield in the reacted solid-state nitrogen

Reduction step	$P(\text{H}_2)$ bar	$T_{\text{hold}}$ °C	$t_{\text{hold}}$ h	Steady $r(\text{NH}_3)$ $10^{-5} \text{ mol mol}_N^{-1} \text{ s}^{-1}$	Steady $r(\text{N}_2)$ $10^{-5} \text{ mol mol}_N^{-1} \text{ s}^{-1}$	$\text{NH}_3$ yield $\text{mol/mol}_N$	$\text{N}_2$ yield $\text{mol/mol}_N$	Reacted solid-state nitrogen $\text{mol mol}_N^{-1}$	Selectivity to $\text{NH}_3$
2	20	700	2	2.32	0.455	0.121	0.0610	0.243	49.8%
3	20	700	2	2.93	0.923	0.151	0.111	0.372	40.5%
4	20	700	2	4.27	0.985	0.271	0.113	0.498	54.5%
5	20	700	2	2.86	0.413	0.154	0.0496	0.253	60.8%
6	20	700	2	3.20	0.643	0.183	0.0742	0.331	55.2%
7	20	700	2	3.29	0.792	0.225	0.0842	0.393	57.2%

- All re-nitridation steps were performed with 20 bar of 10%  $\text{H}_2/\text{N}_2$  at 700 °C
- Sample held at 5 sccm  $\text{H}_2$  / 15 sccm Ar overnight, 1.2 atm, 120 °C

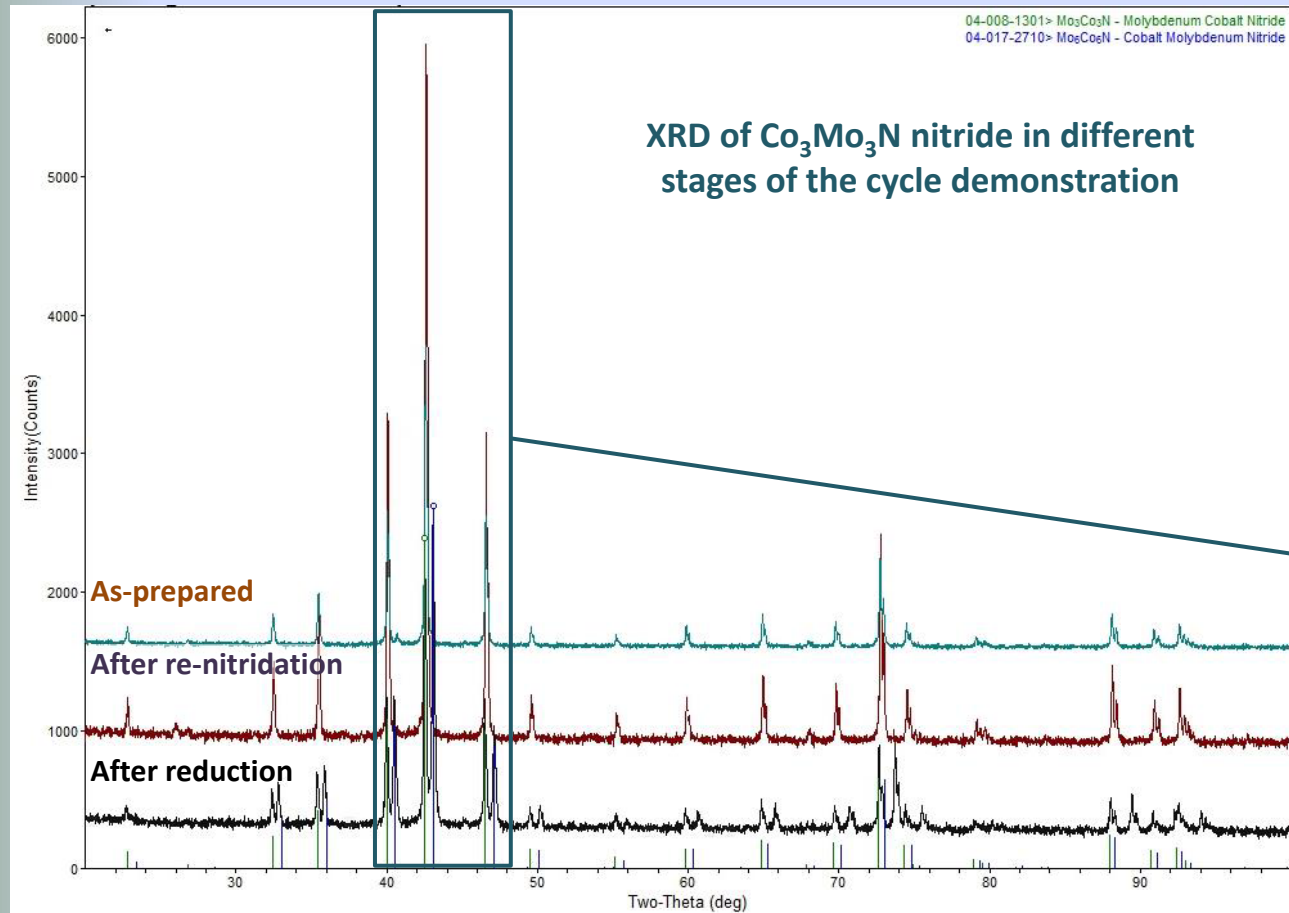
Repetitions on single  $\text{Co}_3\text{Mo}_3\text{N}$  sample – *Reaction is cyclic*



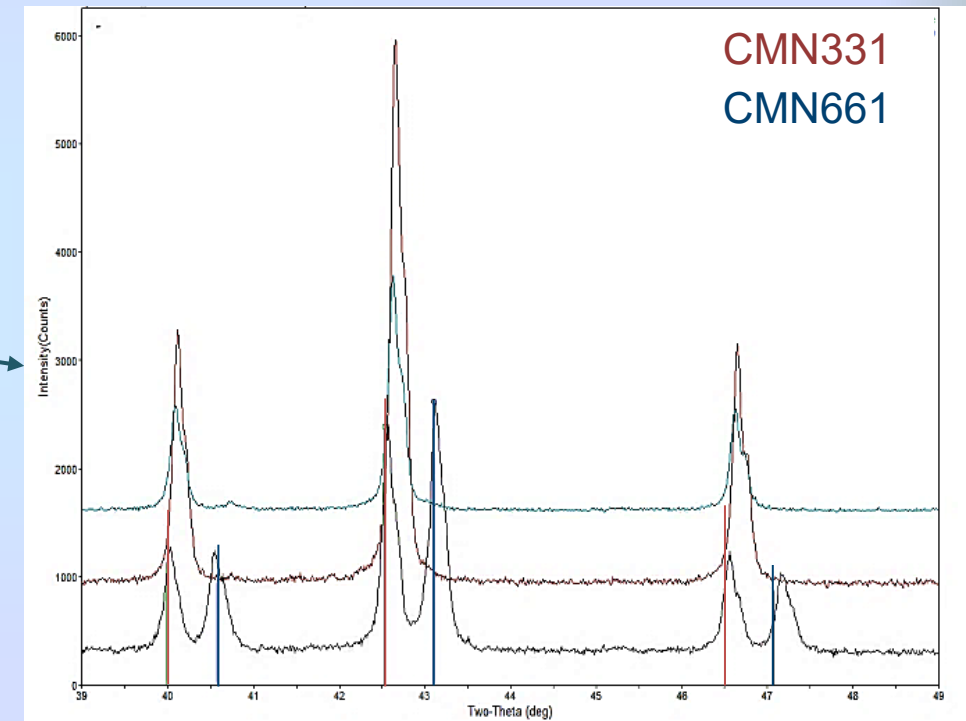
$\text{NH}_3$ ,  $\text{N}_2$  production rates and temperature profile of representative reduction step under 100%  $\text{H}_2$  (Cycle 6)

- Initial  $\text{NH}_3$  peak assumed to be hydrogenation of surface adsorbed  $\text{N}_2$
- At  $T > 600^{\circ}\text{C}$ , consistent co-production of  $\text{NH}_3$  and  $\text{N}_2$  in 100%  $\text{H}_2$  (no external  $\text{N}_2$  feed)
- Production rates fairly flat in all the reduction steps with no evident dependence on the consumed solid-state nitrogen.
- Sample can be re-nitridized under 100%  $\text{N}_2$  at same with no side-reactions observed
  - $P = 20 \text{ bar}$ ,  $T = 700^{\circ}\text{C}$  for both reactions

Results imply that lattice nitrogen participates in  $\text{NH}_3$  production in reversible  $\text{CMN331} \rightarrow \text{CMN661}$  bulk reaction



**XRD Confirms Bulk Reduction and Nitridation**  
**CMN331 → CMN661 → CMN331**



- Partial conversion to 661 after reduction (both 331 and 661 phases observed), consistent with bulk reacted nitrogen calculation of  $< 0.5$
- Regeneration to 331 after re-nitridation with no sign of secondary phase





Second Set of Experiments with Same Sample of CMN

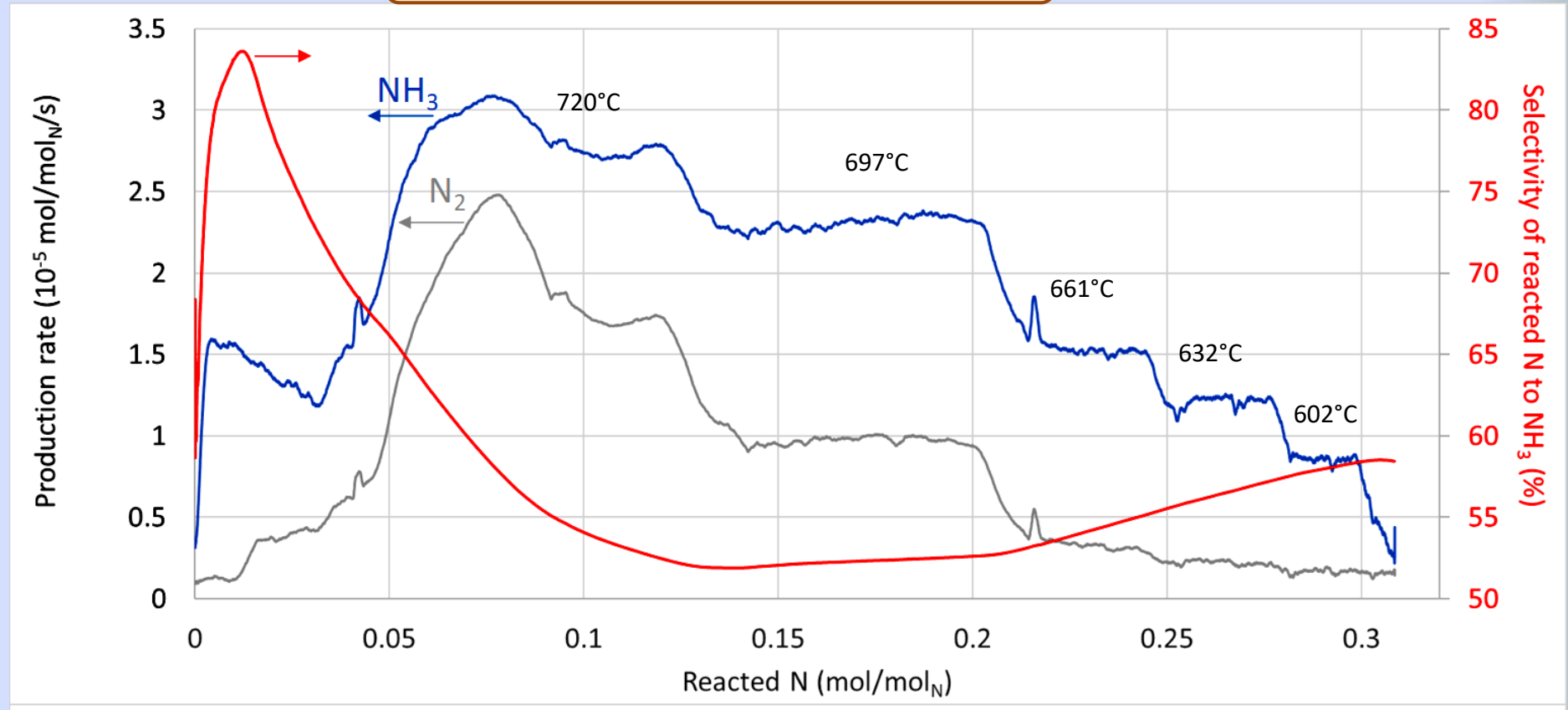
Reduction step	P(H <sub>2</sub> ) bar	T <sub>hold</sub> °C	t <sub>hold</sub> h	Steady r(NH <sub>3</sub> ) 10 <sup>-5</sup> mol mol <sub>N</sub> <sup>-1</sup> s <sup>-1</sup>	Steady r(N <sub>2</sub> ) 10 <sup>-5</sup> mol mol <sub>N</sub> <sup>-1</sup> s <sup>-1</sup>	NH <sub>3</sub> yield mol/mol <sub>N</sub>	N <sub>2</sub> yield mol/mol <sub>N</sub>	Reacted solid-state nitrogen mol mol <sub>N</sub> <sup>-1</sup>	Selectivity to NH <sub>3</sub>
8	20	600-720	0.5×5	--	--				
9	15	600-720	0.5×5	-- T steps at varying pH <sub>2</sub>					
10	10	600-720	0.5×5						
11	5	600-720	0.5×5	--	--				

- All re-nitridation steps were performed with 20 bar of 10% H<sub>2</sub>/N<sub>2</sub> at 700 °C
- Sample held at 5 sccm H<sub>2</sub> / 15 sccm Ar overnight, 1.2 atm, 120 °C



### Typical Data Set

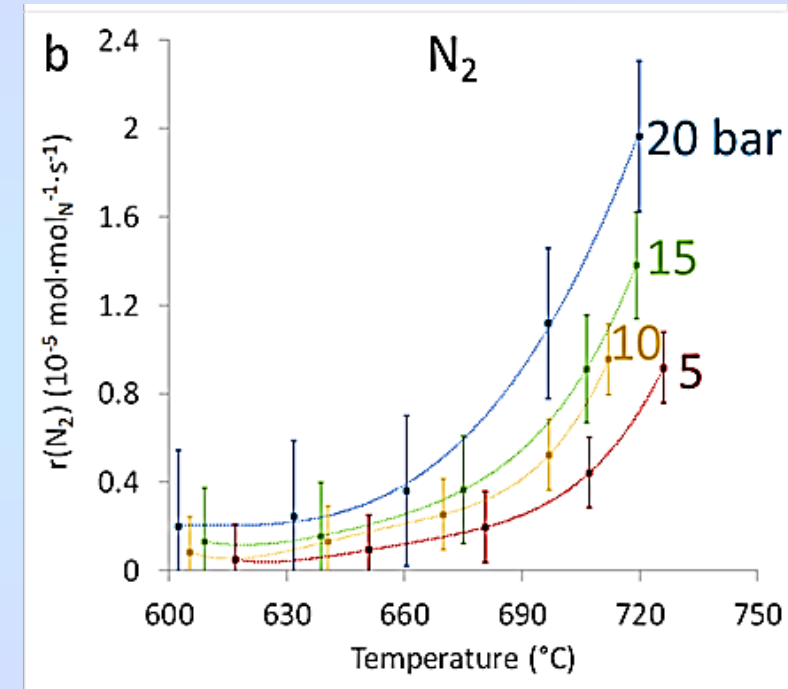
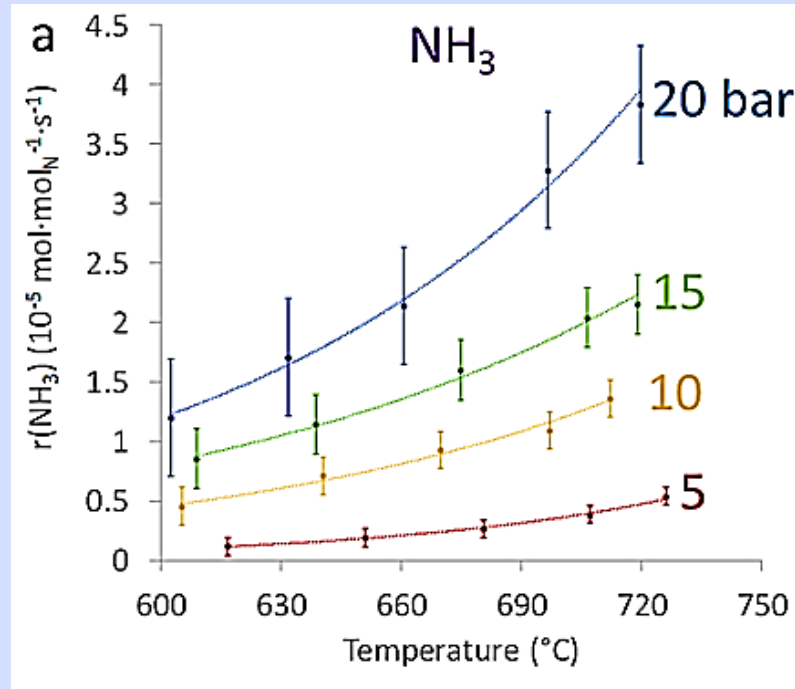
$\text{NH}_3$ ,  $\text{N}_2$  production rates and selectivity of reacted nitrogen to  $\text{NH}_3$  as a function of reacted nitrogen in a temperature stepping reduction experiment (20 bar, 100%  $\text{H}_2$ , 8<sup>th</sup> cycle)



- Selectivity continuously calculated (summed) over entire run – i.e. not the instantaneous value



Conversion of bulk N to  $\text{NH}_3$  and  $\text{N}_2$  increases with T and P

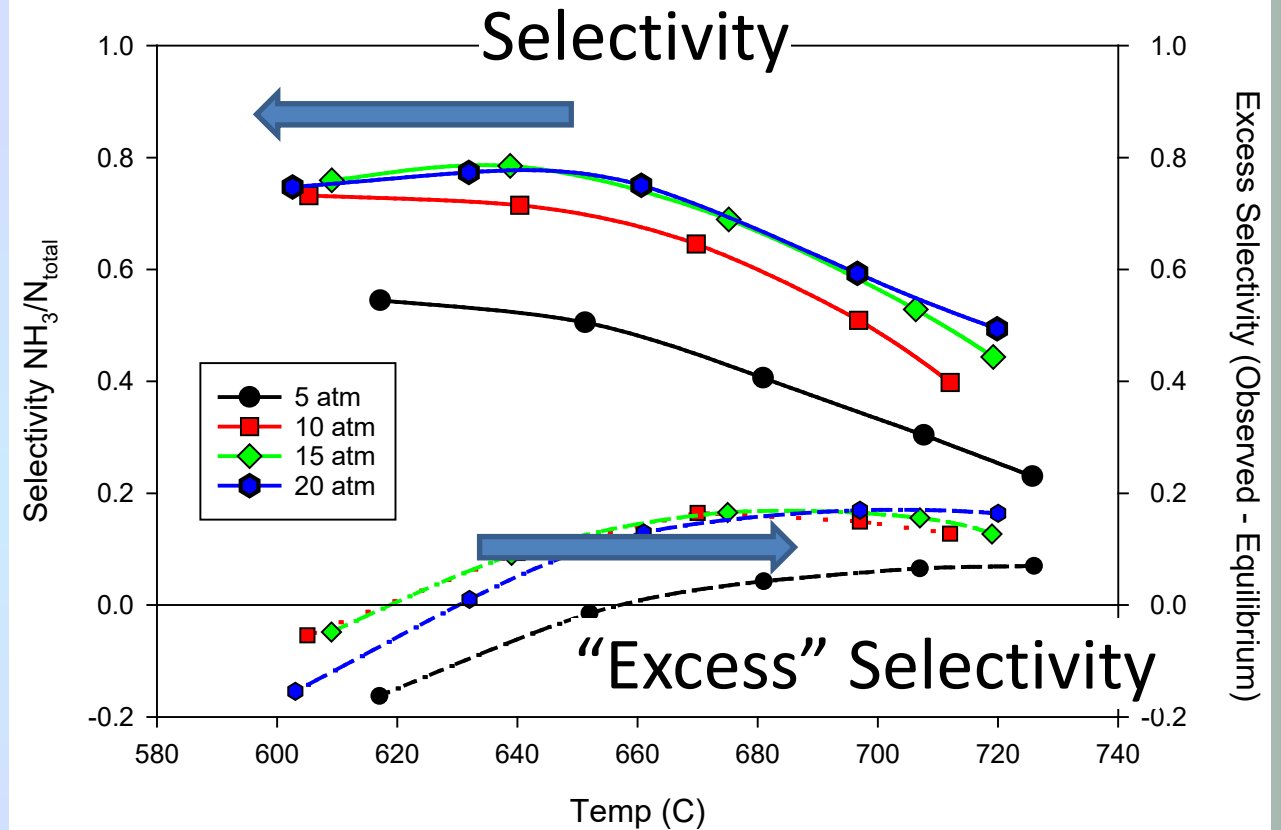
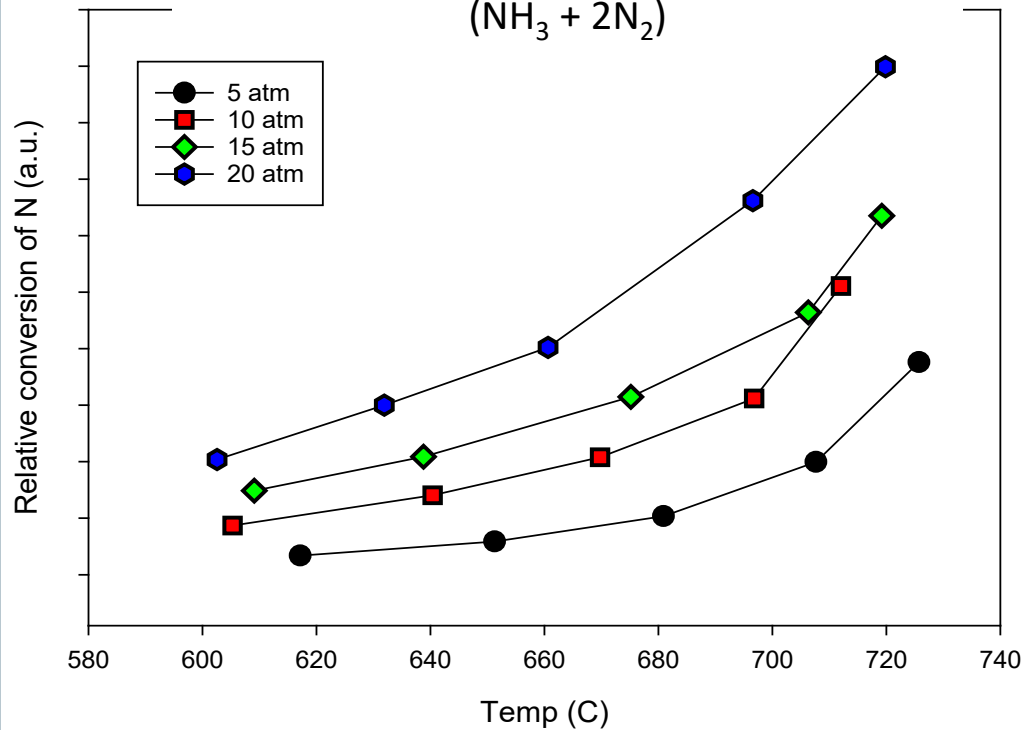
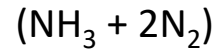


$\text{NH}_3$  production demonstrated at slightly higher T and much lower P ( $\sim 650^{\circ}\text{C}$ ,  $\sim 20$  bar) compared to H-B ( $\sim 450^{\circ}\text{C}$ ,  $\sim 200$  bar)





## Normalized N Conversion

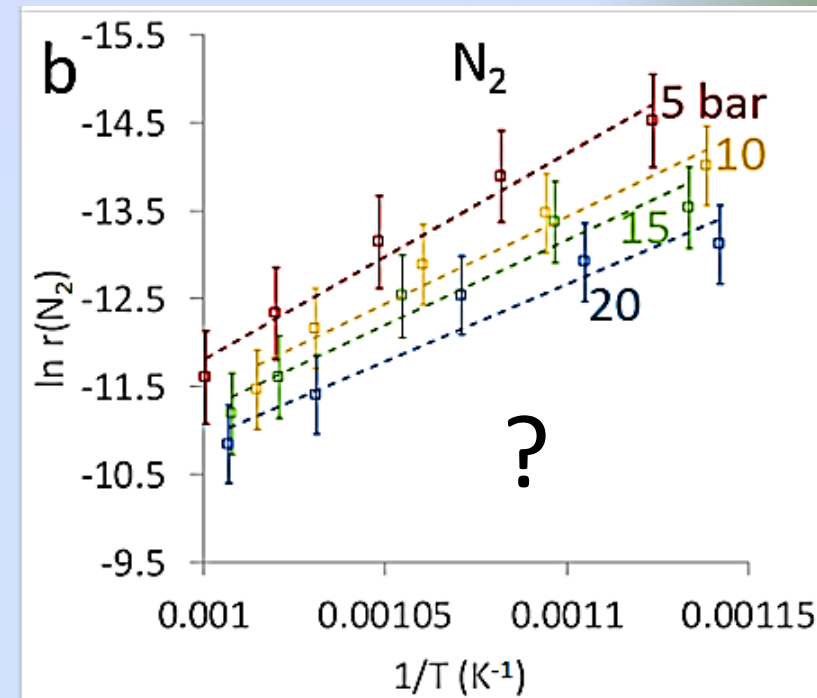
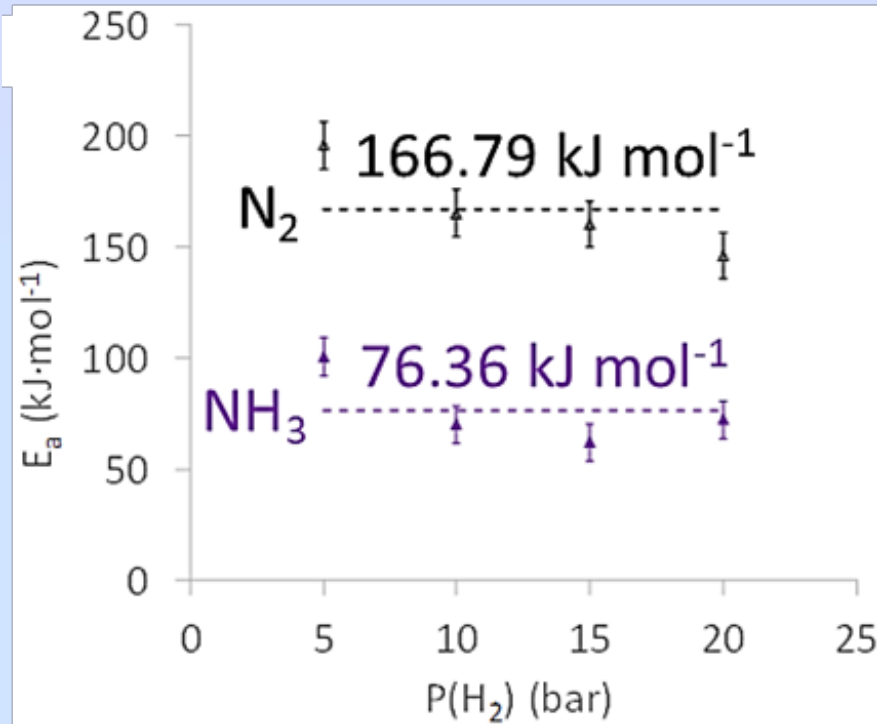
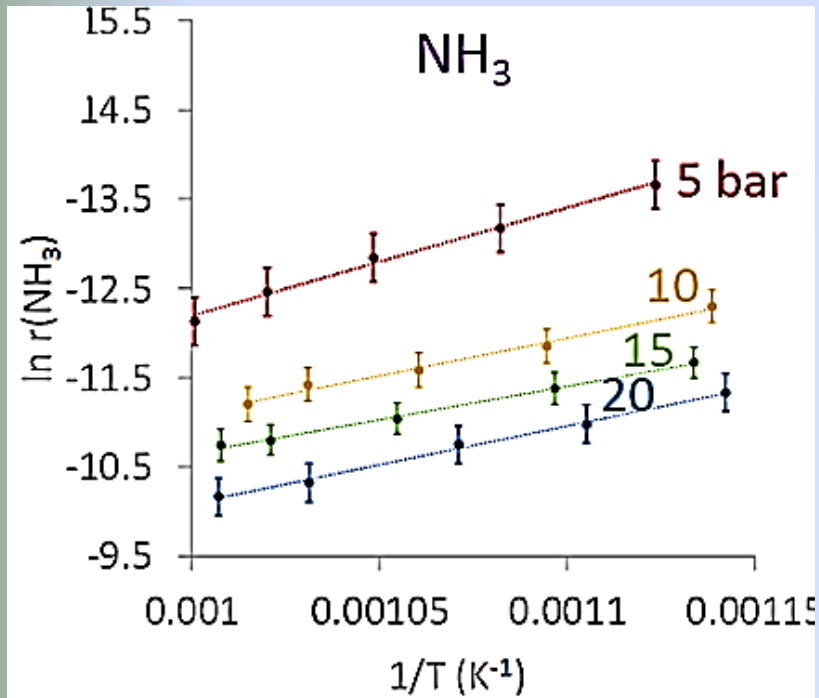


- Conversion increases with T
- $\text{NH}_3$  selectivity decreases with increasing T but exceeds expectation

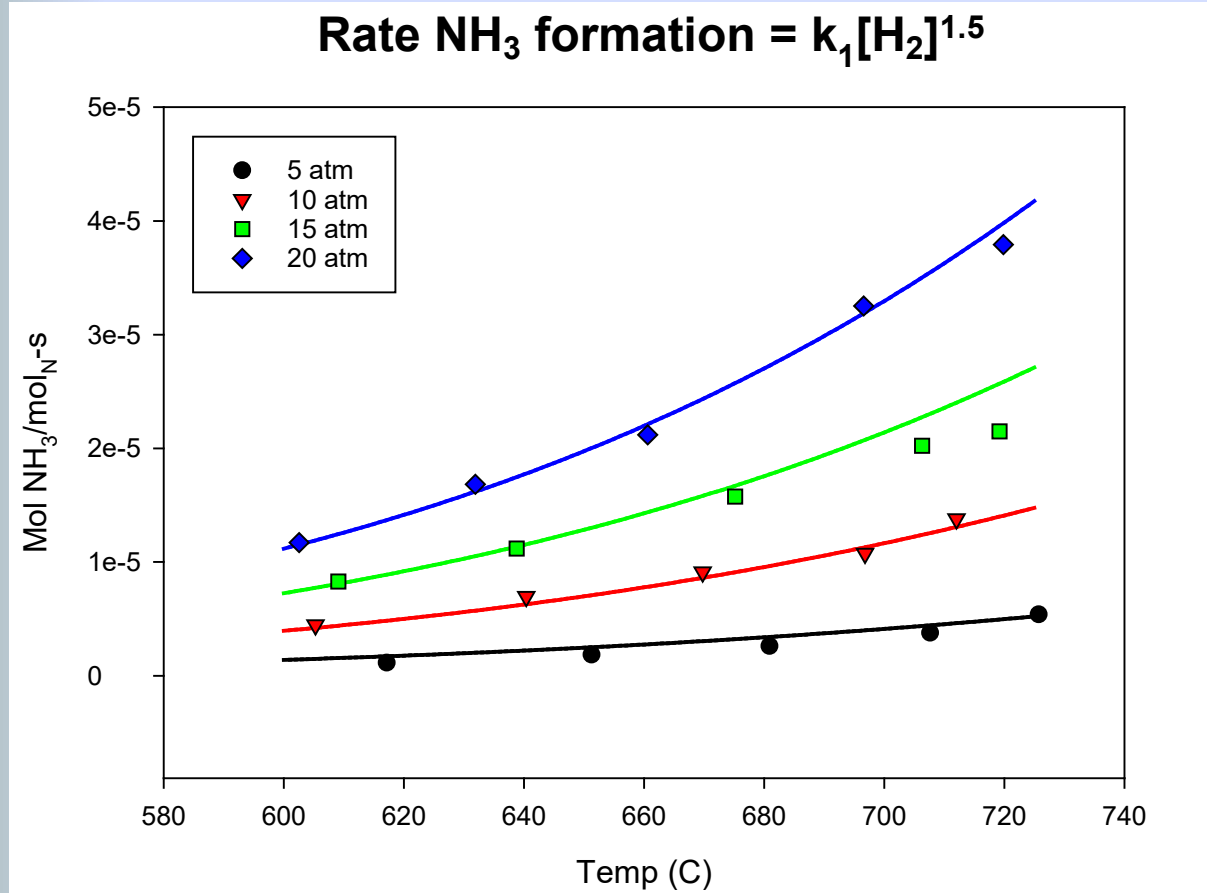
~650 °C Balances Rate and Selectivity



### Activation energies of $N_2$ and $NH_3$



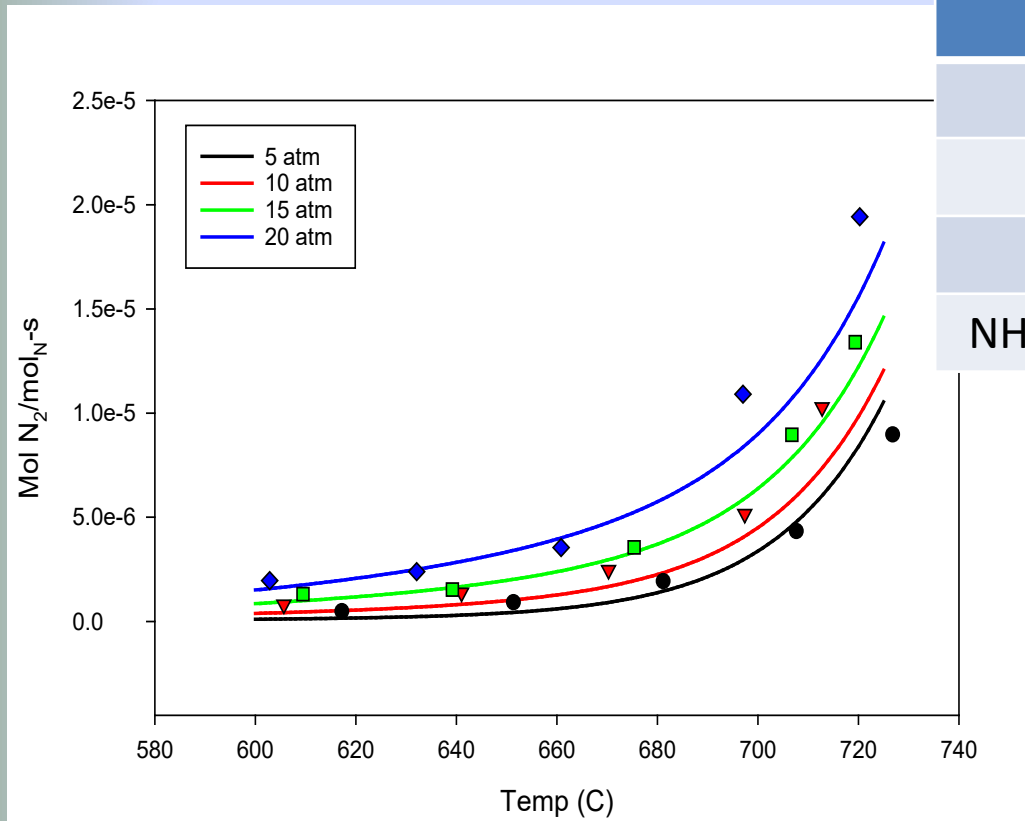
- Use caution comparing catalytic vs bulk reaction, but ...
- $E_a$  ranges from 40 (HB) -120 kJ/mol for a variety of heterogeneous (HB) catalysts
- $E_a = 54$  kJ/mol reported for Cs-promoted  $Co_3Mo_3N$ ,  $T = 320-440$  °C,  $P = 50$  bar



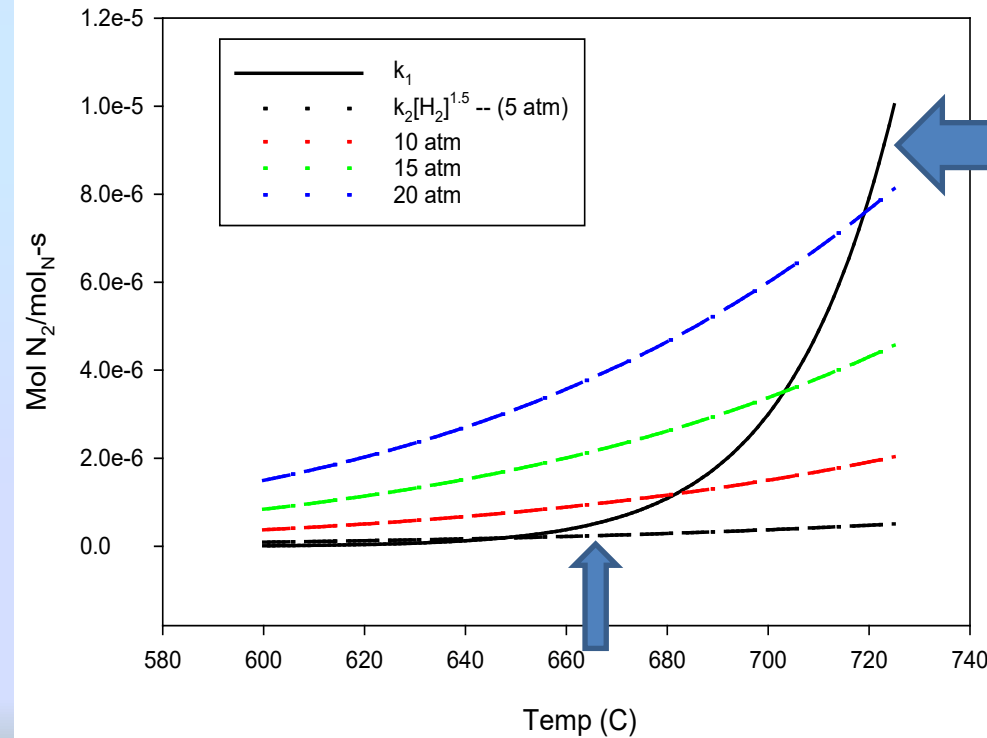
- Simple analysis consistent with multi-step mechanism for  $\text{NH}_3$  formation
- (3/2 order in  $\text{H}_2$ )
- Favorable Energetics

Reaction	A (mol/mol <sub>N</sub> -s)	Ea (kJ/mol)	Order in [H <sub>2</sub> ]
$\text{NH}_3$	0.00463	76.4	3/2
$\text{NH}_3$ thermolysis		≈ 350	





Reaction	A (mol/mol <sub>N</sub> -S)	Ea (kJ/mol)	Order in [H <sub>2</sub> ]
NH <sub>3</sub>	0.00463	76.4	3/2
N <sub>2</sub> (1)	2.59x10 <sup>16</sup>	390	0
N <sub>2</sub> (2)	0.00274	98	≈ 2
NH <sub>3</sub> thermolysis		≈ 350	



0 order in H<sub>2</sub>

**Rate N<sub>2</sub> formation =  $k_1 + k_2[H_2]^2$**   
N<sub>2</sub> rates consistent with multiple pathways



- Ternary nitrides in the family  $A_3B_xN$  ( $A=Co, Ni, Fe$ ;  $B=Mo$ ;  $x=2,3$ ) identified and synthesized
- Experiments with  $Co_3Mo_3N$  in Ammonia Synthesis Reactor demonstrate cyclable  $NH_3$  production from bulk nitride under pure  $H_2$ 
  - Production rates were approx. constant in all the reduction steps with no evident dependence on the consumed solid-state nitrogen up to formation of 661
  - Material can be re-nitridized under pure  $N_2$  (or 10%  $H_2/N_2$ )
  - Bulk N utilization per reduction step averaged between 25 – 40% of the total (2-3 hours)
  - Rate equations and parameters extracted from data.
  - $NH_3$  selectivity exceeds gas phase equilibrium at higher temperatures (in a large excess of  $H_2$ )
  - Selectivity begins to decrease significantly above 650 C,  $N_2$  production rapidly increases above 650 C seemingly due to reaction that is zero order in  $H_2$  (thermal reduction of the nitride?).
- Poised to begin the systematics studies of relationships between materials and reactions



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This work is supported by the U.S. Department of Energy's Office of Energy Efficiency and Renewable Energy (EERE) under the Solar Energy Technologies Office (SETO) Award Number DE-EE0034250.



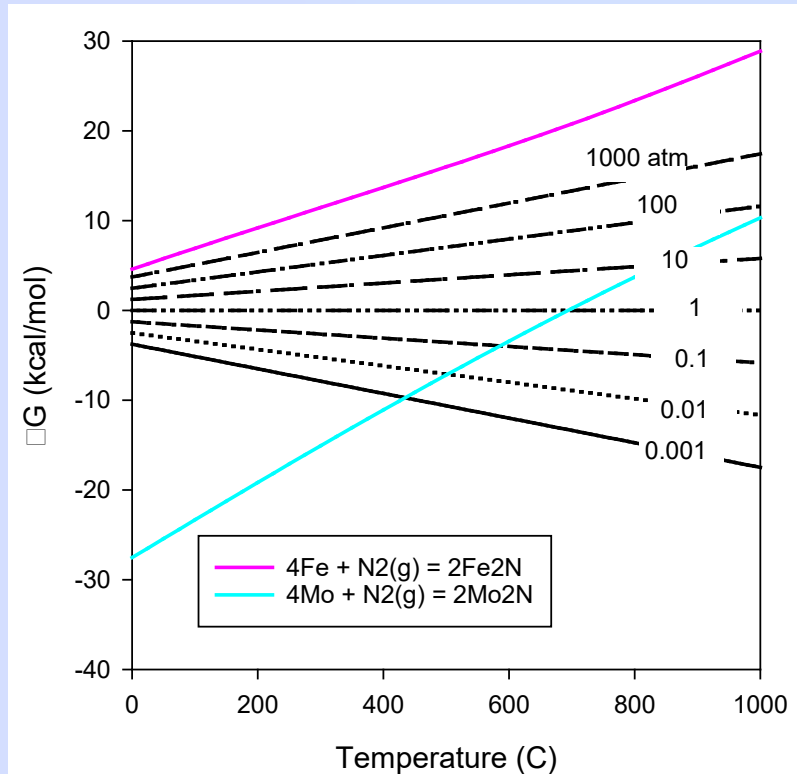






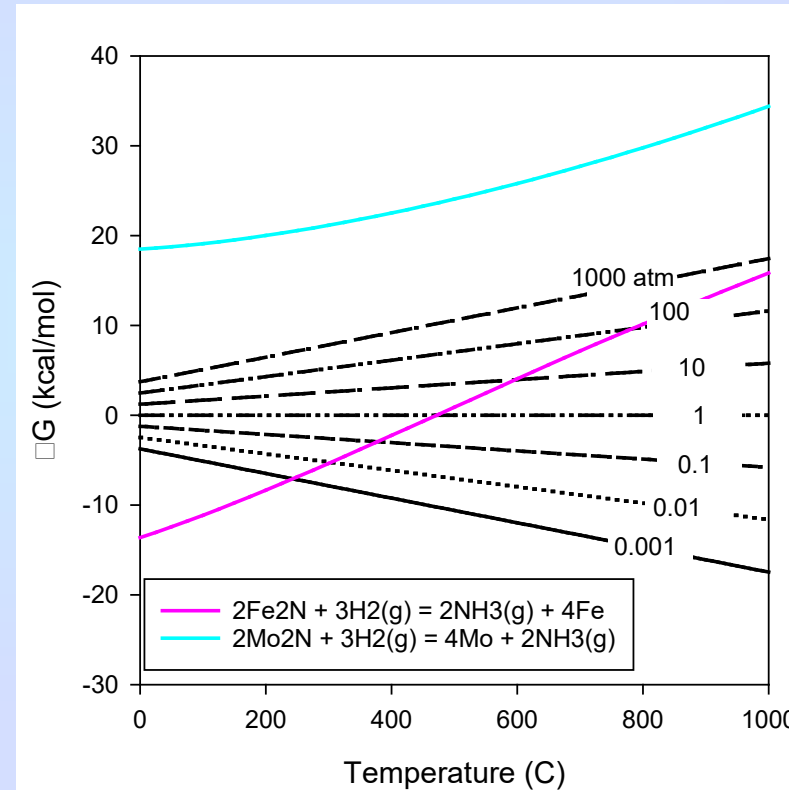
## Why Multiple Metals are Required

### Nitridation



Black lines: Equilibrium  $p\text{N}_2$

### Ammonia Formation



Equilibrium  $p\text{H}_2 = p\text{NH}_3$