

1      CHAPTER X COOKOFF REACTION VIOLENCE

2

3

4

5

6

7

8      Michael L. Hobbs<sup>a</sup>, Jonathan Baker<sup>b</sup>, Malcolm D. Cook<sup>c</sup>, Michael J.  
9      Kaneshige<sup>a</sup>, Shane C. Schumacher<sup>a</sup>, and Christopher Stennett<sup>d</sup>

10     <sup>a</sup>Sandia National Laboratories, Albuquerque NM USA; <sup>b</sup>AWE, Aldermaston,  
11     Reading, UK; <sup>c</sup>Syanco Ltd. West Malling, Kent UK; <sup>d</sup>Centre for Defence  
12     Chemistry, Cranfield University, Defence Academy of the UK, Shrivenham,  
13     Wiltshire, UK

14     \*corresponding author, mlhobbs@sandia.gov

15

16

17

18      X INTRODUCTION

19      Cookoff refers to exposure of an explosive to an abnormally high temperature  
20      such as fire resulting in thermal ignition and a violent response with varying  
21      degrees of damage. Predicting when the explosive thermal ignites is a  
22      relatively straight forward problem if data is available, however, predicting the  
23      resulting violence is a major unsolved problem. The One-Dimensional-  
24      Thermal-Violence (ODTV) experiment was designed to provide quantitative  
25      violence response resulting from cookoff of explosives.

26      The ODTV experiment provides ignition time and wall velocity after 1 mm  
27      of lateral strain. We have determined that the wall velocity at this strain level  
28      correlates strongly with the number of fragments recovered after thermal  
29      ignition. In the current work, we present a model for both pre-ignition and  
30      post-ignition response of the ODTV experiment using an HMX-based  
31      explosive with a formulation of HMX/NC/K10 (91/1/8 by mass) with the most  
32      reactive components during pre-ignition being HMX (1,3,5,7-tetranitro-1,3,5,7-  
33      tetrazocane) and NC (nitrocellulose). A thermal model describes the spatial  
34      and temporal evolution of the energetic material up to ignition. Post ignition  
35      violence is evaluated following ignition.

36

37

38 **X.1 Universal cookoff model and micromechanics pressurization model**

39 Thermal ignition of the HMX-based explosives is modelled by solving the  
40 conductive energy equation in Table 1 that includes a volumetric source for  
41 three reactions that describe desorption of moisture, decomposition of HMX  
42 into equilibrium products, and decomposition of the nitrocellulose into  
43 equilibrium products. A modified Arrhenius rate is used to describe diffusion-  
44 limited moisture desorption and decomposition of the HMX and NC.  
45 Decomposition rates for the HMX and NC components are assumed to be  
46 autocatalytic.

47 Modified Arrhenius reaction rates are given in Table 1. Each reaction uses  
48 distributed activation energies with pressure dependent HMX and NC reaction  
49 rates. Autocatalysis is implemented via the distributed activation energy and  
50 pressure rather than concentrations. More information about this form of  
51 reaction rate has been published.<sup>2</sup> Latent effects for the  $\beta$ - $\delta$  phase change  
52 and HMX melting are accounted for using an effective capacitance method.  
53 Pressure is determined using a gas equation of state with an analytical  
54 expression for deformation of spherical defects caused by internal gas  
55 generation balanced by material strength of the confining explosive<sup>3</sup>. Details  
56 regarding this micromechanics pressurization model (MMP) can be found  
57 elsewhere<sup>2</sup>. The MMP parameters used for the HMX-based explosive include  
58 bulk modulus ( $1.14 \times 10^{10}$  Pa), Young's modulus ( $9.56 \times 10^9$  Pa), Poisson's ratio  
59 (0.36), distance between nucleation sites (0.000226 m), pore failure pressure  
60 ( $5 \times 10^6$  Pa), and volumetric expansion coefficient (0.000131 K<sup>-1</sup>).

61 The thermal model assumptions include 1) HMX and NC decompose into  
62 equilibrium products, 2) the conductive energy equation adequately describes  
63 volumetric energy sources from the chemical reactions, 3) energy transport is  
64 primarily by conduction rather than internal convection or radiation, 4)  
65 moisture evolves by diffusion-limited desorption rather than evaporation, 5)  
66 HMX and NC decomposition is autocatalytic where decomposition rates  
67 accelerate with respect to reaction extent by using a distributed activation  
68 energy, 6) reaction rates depend on confinement, 7) reaction rates are slower  
69 when the explosive is vented and faster when the explosive is sealed, 8)  
70 reaction rates are pressure-dependent using pressure build-up within the the  
71 explosive as well as the confinement, 9) the reaction rate accelerate by a  
72 factor of 10 as HMX melts between 529 and 531 K, 10) decomposition gases  
73 accumulate within defects or pockets within the explosive, 11) the defects  
74 change volume due to decomposition and mechanical strain caused by  
75 thermal expansion or compressibility, and 12) initially the explosive is  
76 impermeable to decomposition gases, but becomes permeable as the internal  
77 pore pressure exceeds 5 MPa.

78

79

Table X.1 Thermal model with nomenclature/parameters in Table 2.

Energy equation	$\rho C_p \frac{\partial T}{\partial t} = \nabla \cdot (k \nabla T) + h_{r1}r_1 + h_{r2}r_2 + h_{r3}r_3$	(1)
Mechanism (3 reactions)	$M \xrightarrow{1} G_M; H \xrightarrow{2} 10 G_H + 1.6 C; N \xrightarrow{3} 8.75 G_N + 2.25 C$	(2)
Rate 1 (diffusion)	$r_1 = A_1 \exp\left(\frac{-(E_1 + \xi_1 \sigma_1)}{RT}\right) [M]$	(3)
Rate 2 (autocatalytic)	$r_2 = A_2 \left(\frac{p}{p_0}\right)^n \lambda T^m \exp(-(E_2 + \xi_2 \sigma_2)/RT) [H]$	(4)
Rate 3 (autocatalytic)	$r_3 = A_3 \left(\frac{p}{p_0}\right)^n T^m \exp(-(E_3 + \xi_3 \sigma_3)/RT) [N]$	(5)
Distribution function*	$\xi_1 = \text{inv}([M]/[M]_o), \xi_2 = \text{inv}([H]/[H]_o), \xi_3 = \text{inv}([N]/[N]_o)$	(6)
Pressure	$P = z \rho R T / M_w$	(7)

Table 2. Nomenclature and model parameters

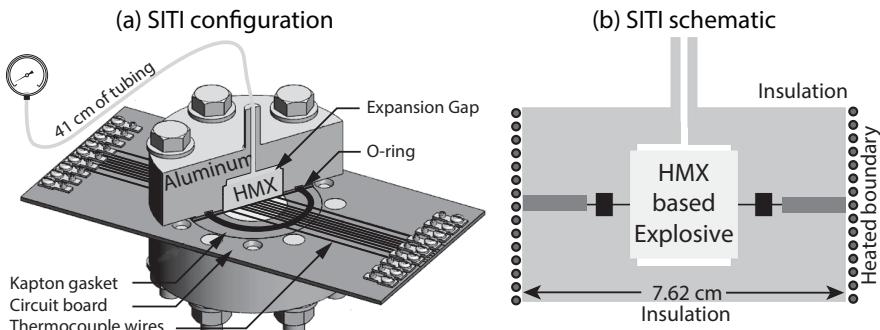
Symbols	Description	Value	Units
$\ln(A_1), \ln(A_2), \ln(A_3)$	Natural logarithm of the pre-exponential factors	35, 35, 35	$\ln(s^{-1})$
B	Binder	Binder is considered inert	None
$[B]$	Binder concentration	Constant: $(1-\omega_M)(\omega_B) \times \rho_{bo}/M_{wB}$ or 0.6826	$\text{kmol m}^{-3}$
C	Carbon	See Eq. (2)	None
$[C]$	Carbon concentration	Initially 0	$\text{Kmol m}^{-3}$
$C_p$	Specific heat <sup>1</sup> with linear interp. and constant extrap.	990 (300 K) 1188 (339 K) 1216 (349 K)	$\text{J kg}^{-1} \text{K}^{-1}$
$E_1/R, E_2/R, E_3/R$	Activation energy divided by R	25000, 15405, 15400	K
$\sigma_1/R, \sigma_2/R, \sigma_3/R$	Standard deviation of activation energy divided by R	2500, -1000, 500	K
$G_H, G_M, G_N$	HMX gas, desorbed moisture gas, and nitrocellulose gas	See Eq. (2)	None
$[G_H], [G_M], [G_N]$	Concentration of $G_H, G_M, G_N$	Initially 0	$\text{kmol m}^{-3}$
H	HMX	Used in Eq. (2) and as subscript	None
$[H]$	Conc. of HMX	Initially $(1-\omega_M) \times \rho_{bo}/M_{wH}$ or 5.5024	$\text{kmol m}^{-3}$
$h_{fi}$ ( $i = M, G_M, H, G_H, C, N, G_N$ )	Heat for formation for $i^{th}$ species	$-285.8 \times 10^6, -241.8 \times 10^6, 75 \times 10^6, -175 \times 10^6, -650 \times 10^6, -265 \times 10^6$	$\text{J kmol}^{-1}$
$h_{latent,\beta-\delta}$	Latent enthalpy for $\beta-\delta$ phase change	33000	$\text{J kg}^{-1}$
$h_{latent,m}$	Latent enthalpy for HMX melt	236000	$\text{J kg}^{-1}$
$h_{ri}$ ( $i = 1, 2, 3$ )	Heat of reaction for $i^{th}$ reaction (Hess's law)	$h_{r1} = (h_{fG_M} - h_{fH}) = +44$ (endo) $h_{r2} = (10h_{fG} + 1.6h_{fC} - h_{fH}) = -1825$ (exo) $h_{r3} = (8.75h_{fG} + 2.25h_{fC} - h_{fN}) = -1670$ (exo)	$\text{J kmol}^{-1}$
i	$i^{th}$ species or $i^{th}$ reaction	M, $G_M$ , H, $G_H$ , C, N, $G_N$ , 1, 2, 3	None
inv	Inverse of the standard normal distribution	Function (see Microsoft Excel NORMINV)	None
k	Thermal cond. <sup>1</sup> (linear interp. and constant extrap.)	0.31 (300 K), 0.37 (320 K)	$\text{W m}^{-1} \text{K}^{-1}$

$\lambda$	Rate acceleration factor for HMX melt.	Variable used to accelerate HMX decomposition rates when HMX melts. Transition occurs between 529 K and 531 K with $\lambda$ changing from 1 to 10.	None
$m$	Steric factors	-2	None
[M]	Adsorbed moisture concentration	Initially $\omega_M \times \rho_{bo} / M_{wM}$ or 0.5	kmol m <sup>-3</sup>
[M <sub>g</sub> ]	Desorbed moisture concentration	Initially 0	kmol m <sup>-3</sup>
$M_{wi}$ ( $i = M, G_M, H, G_H, C, N, G_N$ )	Molecular weight of $i^{th}$ species	18, 18, 296.2, 27.6, 12, 297.1, 30.87	kg kmol <sup>-1</sup>
N	Nitrocellulose	Used in Eq. (2) and as subscript	None
[N]	Concentration of N	Initially $(1 - \omega_M) \times \rho_{bo} / M_{wN}$ or 0.0603	
n	Pressure exponent	0.49	None
P	Absolute pressure	Initially $P_o$	MPa
$P_o$	Initial pressure	0.083 (NM), 0.1 (CA and UK)	MPa
$P_{fail}$	Pore failure pressure	5	MPa
$\rho$	Density	Field variable	kg m <sup>-3</sup>
$\rho_{bo}$	Initial bulk density	1800	kg m <sup>-3</sup>
$\rho_c$	Condensed density	Field variable	kg m <sup>-3</sup>
$\rho_{co}$	Initial condensed density	1841	kg m <sup>-3</sup>
R	Gas constant	8314	m <sup>3</sup> Pa K <sup>-1</sup> kmol <sup>-1</sup>
[S]	Solid concentration	Initially 0	kmol/m <sup>3</sup>
$S_f$	Solid fraction	$S_f = (M_{wM}[M] + M_{wW}[W] + M_{wS}[S] +) / \rho_{bo}$	kg kg <sup>-1</sup>
t	Time	Global variable	s
T	Temperature	Field variable	K
[W]	Waste concentration	Initially $\omega_{waste} \times \rho_{bo} / M_{ww}$ or 4.07	kmol m <sup>-3</sup>
$T_o$	Initial temperature	ODTV: 296 ODTX: 300 (guess) SITI: 297	K
$V_{ex}$	Extra gas volume ( <i>i.e.</i> , expansion slot, pressure tube, etc)	ODTV: $4 \times 10^{-6}$ ODTX: $0.07 \times 10^{-6}$ SITI: $1.3 \times 10^{-6}$	m <sup>3</sup>
$V_o$	Initial volume of explosive	ODTV: $14.1 \times 10^{-6}$ ODTX: $1.1 \times 10^{-6}$ SITI: $12.87 \times 10^{-6}$	m <sup>3</sup>
$\omega_B$	Initial mass fraction of inert binder	$(1 - \omega_M) \times 0.08 = 0.0796$	kg kg <sup>-1</sup>
$\omega_H$	Initial mass fraction of H	$(1 - \omega_M) \times 0.91 = 0.90545$	kg kg <sup>-1</sup>
$\omega_M$	Initial mass fraction of adsorbed water	0.005	kg kg <sup>-1</sup>
$\omega_N$	Initial mass fraction of N	$(1 - \omega_M) \times 0.01 = 0.00995$	kg kg <sup>-1</sup>
$\xi$	inv: inverse of the standard normal distribution	Field variable	None
$\xi_1, \xi_2, \xi_3$	inv for 1 <sup>st</sup> , 2 <sup>nd</sup> , and 3 <sup>rd</sup> reaction	Field variable	None
z	Gas compressibility	1 for ideal gas	None

84 **X.2 Calibration of thermal model using SITI data**

85 Sandia Instrumented Thermal Ignition (SITI) experiment (see Figure X.1) was  
86 used to determine the thermal conductivity and reaction parameters for the  
87 thermal model described in Table 1 using measured temperatures presented  
88 in Figure X.2.

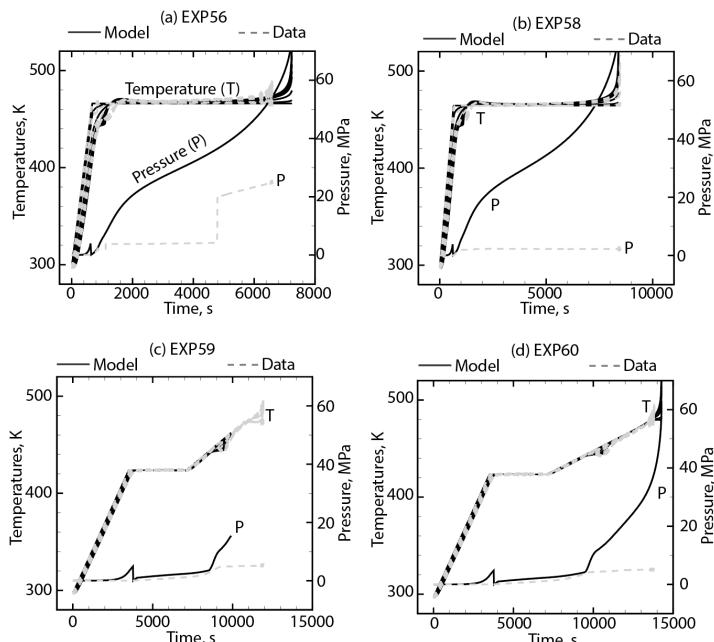
89



90

91 **Figure X.1 SITI (a) configuration and (b) schematic.**

92



93

94 **Figure X.2 SITI measured and predicted radial temperatures for SITI**  
95 **experiments with an average mass of 23.5 g and density of 1829 g/m<sup>3</sup>.**

96 The SITI experiment confines two 2.54 cm diameter by 1.27 cm tall  
97 cylinders of HMX-based explosive in aluminum with nine type K 127  $\mu\text{m}$   
98 (0.005 in.) diameter thermocouples located at radial positions in mm of 0,  
99 1.70, 2.55, 3.40, 4.25, 5.11, 5.96, 8.81, and 11.7 and placed between the two  
00 explosive cylinders. The outer surface of the 7.62 cm diameter by 4.58 cm tall  
01 aluminum confinement is heated using rope heaters controlled by a  
02 thermocouple on the lateral surface (e.g., see Figure X.1a and Figure X.1b).  
03 Figure X.2 shows the external aluminum temperature measured for four SITI  
04 experiments. Two expansion gaps that are above and below the explosive are  
05 also machined into the confining aluminum. Each expansion gap has a  
06 diameter of 2.22 cm and is 0.16 cm tall.

07 Four SITI experiments were used to both parameterize and validate the  
08 reaction model: A) Exp56, B) Exp58, C) Exp59, and D) Exp60 with measured  
09 internal and boundary temperatures shown in Figure X.2 as dashed light gray  
10 lines. Exp56 was heated from 297 K to 466 K in 673 s and held until ignition.  
11 Exp58 was heated from 297 K to 464.33 K in 654 s and held until ignition.  
12 Exp59 was heated from 297 K to 423.75 K in 3500 s and held at 423.75 K  
13 until 7100 s, and then ramped to 473.34 K at 11930 s wherein the explosive  
14 thermally ignited. Exp60 was heated from 297 K to 423.35 K in 3500 s and  
15 held at 423.35 K until 7100 s, and then ramped to 479.36 K at 13826 s  
16 wherein the explosive thermally ignited. The predicted (solid black lines) and  
17 measured (dashed grey lines) radial temperatures and pressure are shown for  
18 each of the SITI experiments in Figure X.2

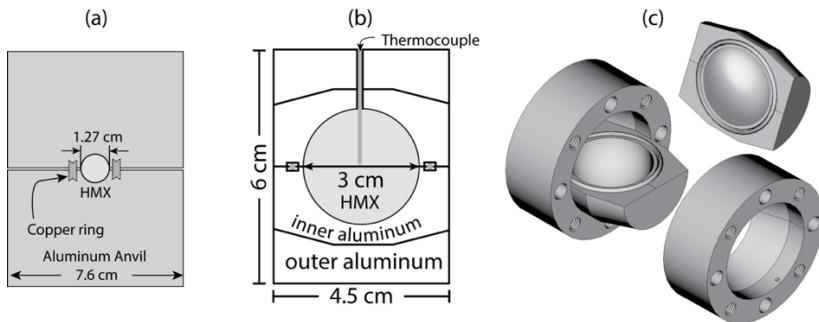
19 Exp58 in Figure X.2b was used to obtain the kinetic parameters for the  
20 model since this experiment clearly shows the  $\beta$ - $\delta$  phase change as well as a  
21 thermal excursion between 1000 and 2000 s. The other three SITI  
22 experiments (Exp56, Exp59, and Exp60) were used for validation. The  
23 measured and predicted (in parentheses with percent error) ignition times for  
24 these three experiments were 6603 s (7192 s, +9%), 11930 s (9926 s, -17%),  
25 and 12700 s (14200 s, +12%). These are reasonable predictions especially  
26 for high-density plastic bonded explosives that are at 98% of the theoretical  
27 maximum density (98%TMD). Lower density explosives are usually easier to  
28 predict since the decomposition gases are not retained within the explosive.

29 All SITI predictions were made assuming that the high-density HMX-based  
30 explosive was initially impermeable. A simple damage model was used to  
31 transition closed pores (impermeable) to open pores (permeable). The  
32 damage model determines when a pore fails, and thus allowing the pore gas  
33 to be part of the open pore network which includes the gases in the expansion  
34 gap. A maximum pore pressure of 5 MPa was chosen for the HMX-based  
35 explosive based on the work of others<sup>2</sup>. The predicted pressures show a spike  
36 when the internal pressures reach 5 MPa followed by a sudden decrease in  
37 pressure as the internal pressures are relieved as shown in the pressure  
38 predictions in Figure X.2. The measured pressures are from the pressure  
39 transducer that does not measure internal pressure build-up. In fact, the

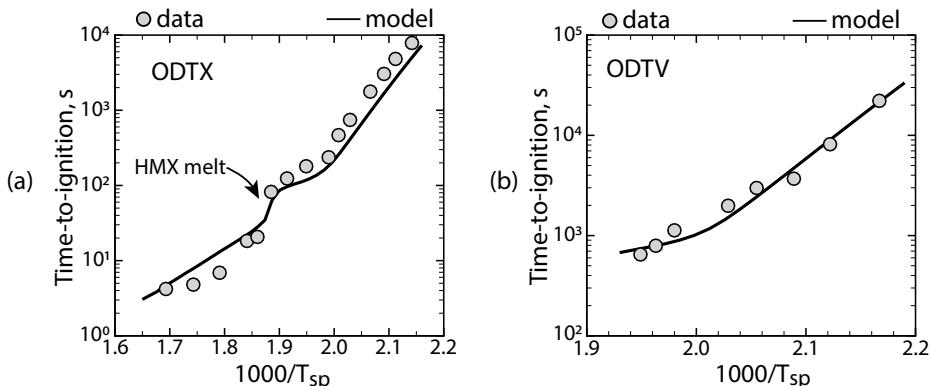
.40 simple pore damage model might not capture more complex damage that  
.41 may result from heterogeneous cracking.

.42 **X.3 Validation of thermal model using ODTX and ODTV data**

.43 The schematics and ignition data for the one-dimensional time-to-explosion  
.44 (ODTX) and the one-dimensional thermal violence (ODTV) experiments are  
.45 shown in Figure X.3 and Figure X.4, respectively. The ODTX experiments<sup>4</sup>  
.46 confine a 1.27 cm diameter sphere of explosive within two aluminum anvils  
.47 that have hemispheres machined into each face. The maximum gas pressure  
.48 within the ODTX confinement is 150 MPa. The explosive is sealed by  
.49 plastically deforming a copper O-ring (shown in Figure X.3). Each aluminum  
.50 anvil is held at the set point temperature ( $T_{sp}$ ). At time zero, the hot anvils,  
.51 heated and maintained at various set point temperatures, are brought  
.52 together to hydraulically confine the initially room temperature explosive. The  
.53 primary diagnostic for the ODTX experiment is the time required to reach  
.54 thermal ignition.



.55  
.56 Figure X.3 (a) ODTX configuration, (b) ODTV schematic, (c) ODTV parts.  
.57

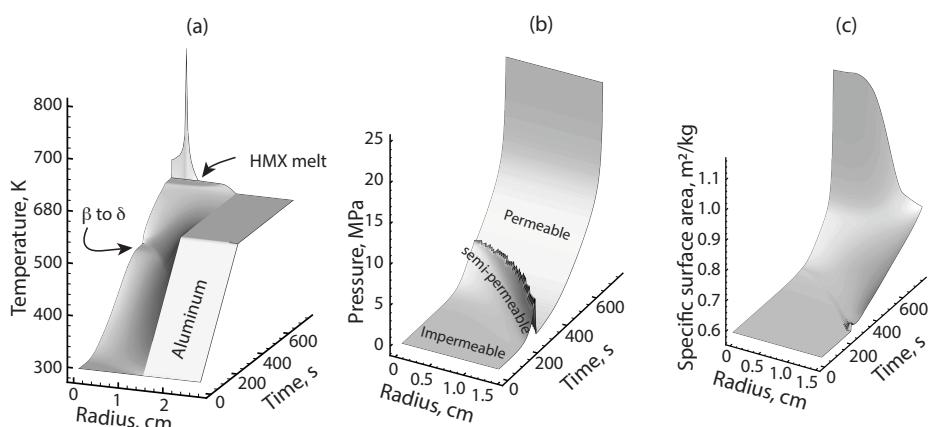


.58  
.59 Figure X.4 Measured (symbol) and predicted (line) ignition data for the (a)  
.60 ODTX experiments<sup>4</sup> and the (b) ODTV experiments<sup>5</sup>.

61 The ODTV experiments<sup>5</sup> restrain a 3 cm diameter sphere of explosive  
62 using a double shell confinement (see Figure X.3b and X.3c). The confining  
63 aluminum is heated using induction heating. At time zero, the aluminum  
64 confinement is ramped from room temperature to the set point temperature in  
65 300 s. The primary diagnostic for the ODTV experiment is ignition time,  
66 temperature measured in the center of the explosive, number of confinement  
67 fragments, and wall velocity using particle Doppler velocimetry (PDV). The  
68 maximum working pressure of the ODTV experiment was not measured and  
69 no limit on pressure was imposed on the ODTV model.

70 Predicted and measured time-to-ignition for both the ODTX and ODTV  
71 experiments for the HMX-based explosive are shown in Figure X.4. The  
72 parameters used to obtain the predictions in Figure X.4 were the same as  
73 used for the SITI predictions in Figure X.2. In the UCM/MMP model, the HMX  
74 reaction rate was increased by a factor of ten at the melting point to cause the  
75 distinct change in slope in the ignition plot as highlighted in Figure X.4(a).

76 The predicted temperature, pressure, and specific surface area for the  
77 ODTV experiment with the external temperature ramped from 296 K to 513 K  
78 in 300 seconds and then held until ignition is presented in Figure X.5. The  
79 temperature plot in Figure X.5(a) shows both the  $\beta$ - $\delta$  polymorphic phase  
80 transition as well as the melting of the HMX. The pressure plot in Figure  
81 X.5(b) shows the transition of the initially closed pore explosive (impermeable  
82 to gases) into an open pore explosive that is permeable to gases. The specific  
83 surface area shown in Figure X.5(c) was calculated with the MMP model and  
84 shows how thermal damage can be calculated for subsequent post ignition  
85 violence calculations. The ignition time for this simulation was 743 s. The  
86 measured ignition time was 648 s.



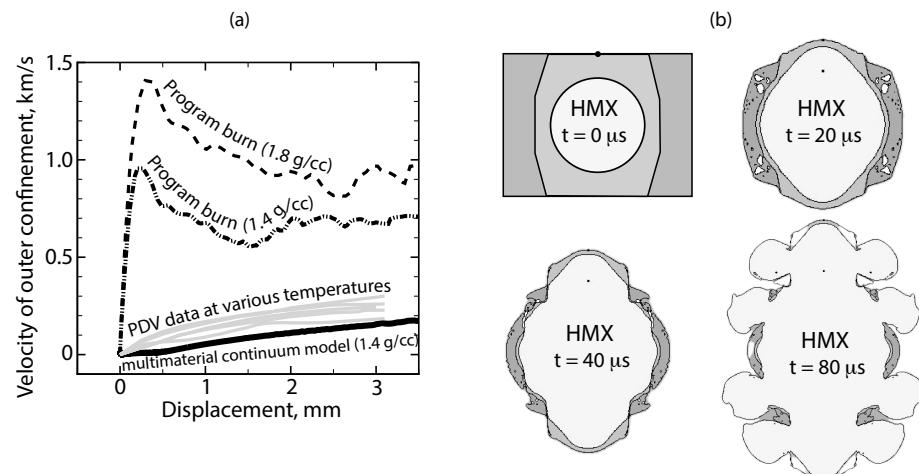
89 Figure X.5 Calculated (a) temperature, (b) pressure, and (c) specific surface  
90 area for the ODTV experiment with the external temperature ramped to 513 K.

## 91 X.4 Determining violence

92 Historically, violence is assessed post-mortem by counting the number of  
93 fragments. In all ODTV experiments shown in Figure X.4(b), the outer  
94 compression rings each produce 8 fragments for a total of 16 fragments  
95 regardless of the external heating rate. Damage occurs as the compression  
96 ring breaks at each of the 8 bolt holes. There are no bolt holes in the  
97 aluminum that surrounds the explosive, and the number of fragments  
98 originating from this confining aluminum defines the overall violence of the  
99 ODTV experiment. The number of inner confinement fragments, some of the  
00 measured velocities at a confinement displacement of 1.5 mm, and set point  
01 temperature for each of the eight ODTV experiments were 4 (240°C), 13  
02 (237°C), 16 (232°C, 180 m/s), 24 (220°C), 21 (213°C, 140 m/s), 21 (205°C,  
03 165 m/s), 31 (198°C, 210 m/s), and 38 (188°C, 205 m/s).

04 The simplest way to determine fragmentation of the confining aluminum in  
05 the ODTV experiment is by using a programmed burn following ignition. A  
06 program burn model assumes that the explosive burns at the detonation  
07 velocity starting at the location determined with the thermal ignition model  
08 which is typically near the center of the explosive (see Figure X.5a). In the  
09 current work, post-ignition calculations were performed by assuming the  
10 density of the explosive was either 1.8 g/cm<sup>3</sup> or 1.4 g/cm<sup>3</sup> with detonation  
11 velocities of 8.5 km/s and 7.2 km/s respectively. The product equation of state  
12 was determined using a JWL equation-of-state.

13 Predicted wall velocities using the two programmed burn models is shown  
14 in Figure X.6(a). The model used a two-dimensional axisymmetric mesh  
15 without bolt holes. A slide surface was used between the inner aluminum



16  
17 Figure X.6 (a) Predicted and measured confinement velocities and (b)  
18 material plots at various times for the programmed burn simulations at 1.8  
19 g/cm<sup>3</sup>.

confinement and the aluminum compression rings. For the aluminum, an elastic perfectly plastic von Mises (EPPVM) yield surface model with a yield strength of 945 MPa and a Poisson ratio of 0.3 were used in the simulations in Figure X.6. A simple Mie-Grüneisen equation of state with typical parameters was used for the aluminum equation-of-state. Fracture was assumed to occur when the aluminum was in tension at -900 MPa (negative sign indicates tension).

Figure X.6(b) shows sliding occurring between the inner confinement and compression rings and fragmentation of the aluminum for the higher density program burn calculation. Fragmentation of the confinement is usually determined by inserting void into computational cells when tension states exceed a critical level. The computed results are best near the onset of containment breakup. However, fragmentation cannot be accurately predicted without resolving the small aluminum grains which are on the order of microns in length. Such resolution is beyond the scope of the current paper.

The outer confinement velocities calculated with the simple programmed burn are much higher than the measurements shown in Figure X.6(a). Even the shape of the program burn velocities is incorrect. A better way to calculate the velocities is to use a multi-material continuum model for the HMX. Predictions from a multi-material model is also shown in Figure X.6(a) as well as Figure X.7(b) with magnitudes and shapes better approximating the measured velocity of the outer confinement. Material plots using the multi-material continuum model are shown in Figure X.7(a).

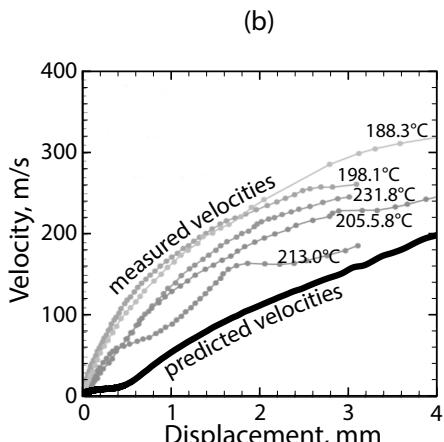
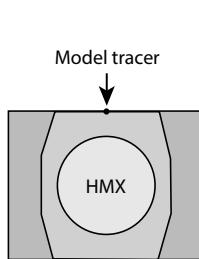


Figure X.7 (a) The ODTV experiment at two times following thermal ignition showing confinement deformation. (b) Measured (lines with symbols) and predicted (thick black line) of the outer confinement velocity at the tracer location shown in (a).

49 The velocity of the inner barrel-shaped containment was calculated using a  
50 generalized continuum mixture theory for the HMX-based material<sup>7</sup>  
51 implemented into a multi-material shock physics research code<sup>8</sup> using typical  
52 properties for the aluminum confinement. This code<sup>8</sup> can determine the  
53 behaviour of the explosive as it transitions from a subsonic deflagration to a  
54 supersonic detonation. Details regarding the multi-material mixture theory are  
55 beyond the scope of the present work and the interested reader is directed to  
56 the appropriate references<sup>7,8</sup>. The multi-material mixture model was initiated  
57 using a 1 mm bubble in the center of the explosive with a pressure and  
58 temperature (4370 MPa, 3540 K).

59 Unfortunately parameterizing the multi-material continuum model is  
60 complex and requires a substantial number of parameters and experiments at  
61 both pristine and heated conditions. However, parameters are available for a  
62 1.4 g/cm<sup>3</sup> granular HMX<sup>8</sup> which is 74% of the theoretical maximum density  
63 (74%TMD). Parameters for the reactive constitutive model are not available  
64 for the higher density HMX-based explosive in the current work which is at 1.8  
65 g/cm<sup>3</sup> (97%TMD). The predicted external velocity calculated with the multi-  
66 material mixture model using 1.4 g/cm<sup>3</sup> HMX is shown in Figure X.7.

67 The discrepancy between the measured and predicted velocities using the  
68 multi-material mixture model is primarily due to the lower density used in the  
69 model where the energy content in the model is crudely, 78% of the  
70 experiment. Another source of discrepancy is the delay in movement of the  
71 confinement that is absent in the data which shows immediate displacement  
72 of the outer surface. The model shows a delay in movement. Future work  
73 should enforce time synchronization between the experiments and the model.

74 Cook et al.<sup>5</sup>, point out that the number of confining vessel fragments  
75 correlate to the measured velocity at a displacement of 1.5 mm. In the current  
76 work, fragmentation is correlated by using a simple model that assumes the  
77 fragmentation is dominated by fracture toughness<sup>6</sup>:

$$78 s = \left( \frac{\sqrt{24}K(1 - \frac{T}{T_m})^n}{\rho c \dot{\epsilon}} \right) \quad (8)$$

79 where s is a characteristic length of the fragment, K is the fracture toughness  
80 ( $20 \times 10^6$  Pa m<sup>0.5</sup>), T is the ODTV set point temperature, T<sub>m</sub> is the melting point  
81 of aluminum (933 K), n is the temperature exponent (-3.5), ρ is density of the  
82 aluminum (2700 kg m<sup>3</sup>), C is the sound speed of the aluminum (3000 m/s),  
83 and  $\dot{\epsilon}$  is the strain rate. For the ODTV experiment, the strain rate can be  
84 approximated by either the measured or calculated confinement velocity  
85 normalized by the displacement at 1.5 mm.

86 Fragmentation is determined in the current work by using the damage  
87 model in Eq. (8), which require continuum strain predictions. The predicted  
88 velocities shown in Figure X.7(b) are not used to predict fragmentation due to  
89 lack of model parameters for the higher density HMX-based material

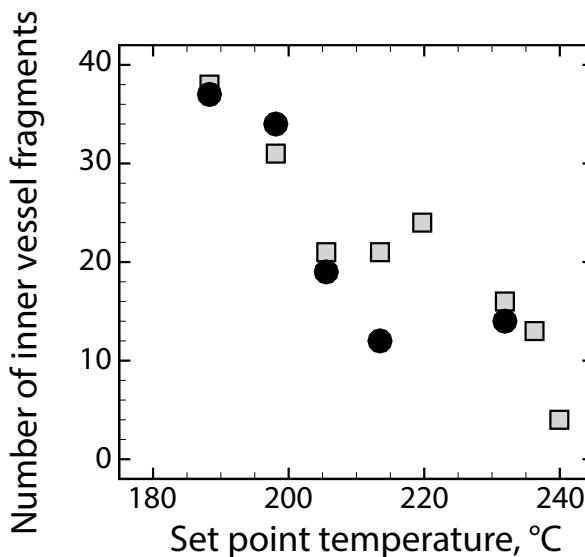
90 discussed in the current work. Instead, the velocity measurements are used  
91 with Eq. (8) to predict the number of fragments.

92 The measured velocity profiles shown in Figure X.7(b) are not distinctly  
93 different at small displacements. Once the displacement reaches about 1.5  
94 mm, the velocity profiles have separated. The number of fragments is  
95 determined by calculating the characteristic dimension,  $S$ , from Eq. (8). The  
96 average fragment volume is then used with the ODTV aluminum volumes to  
97 determine the number of fragments.

98 Number of fragments =  $V_{\text{confinement}}/V_{\text{fragment}}$  (9)

99 where  $V_{\text{fragment}}$  is the volume of the fragments calculated as  $s^3$  and the volume  
00 of the inner confinement ( $V_{\text{confinement}}$ ) is  $34.5 \text{ cm}^3$ . For reference, the volume of  
01 both compression rings is  $67.6 \text{ cm}^3$  and the volume of the explosive is  $14.1 \text{ cm}^3$ .  
02 Other volumes include the O-ring space and the hole drilled for the  
03 internal thermocouple. Figure X.8 shows a comparison of the predicted and  
04 measured number of fragments.

05 Generally, the number of fragments decreases as the set point  
06 temperatures increase (see Figure X.8). However, there are several  
07 anomalies in both the predictions and measurements where the number of  
08 fragments increase with increasing temperature. For example, the model  
09 predicts an increase in the number of fragments at  $232^\circ\text{C}$  compared to  $213^\circ\text{C}$ .



11  
12 Figure X.8 Predicted (circles) and measured (squares) fragments of the  
13 barrel-shaped confinement vessel. There were 16 fragments from the  
14 compression rings.

15 This occurs since the model predictions are based on the measured wall  
16 velocity shown in Figure X.7(b) which show higher velocities for 232°C than  
17 for 213°C. The anomaly with the velocity at 232°C could have been caused by  
18 poor alignment of the PDV laser that was aimed too close to the joint at the  
19 mid-plane of the capsule. The PDV may have recorded the motion of several  
20 different surfaces during expansion<sup>5</sup>.

21 Although the agreement between the predicted number and measured  
22 number of fragments is good, the agreement was obtained by judicious  
23 selection of the temperature exponent  $n$  (-3.5) in Eq. (8). To test this model, a  
24 future experiment should include powdered HMX at 1.4 g/cm<sup>3</sup>.

## 25 **X.5 Summary and conclusions**

26 A universal cookoff model coupled to a micromechanics pressurization model  
27 (UCM/MMP) has been parameterized for an HMX-base explosive that also  
28 contains nitrocellulose. The model consists of three reactions that describe  
29 diffusion-limited moisture desorption, HMX decomposition, and nitrocellulose  
30 decomposition. The reaction rates use distributed activation energies. The  
31 HMX reactions were also increased by a factor of ten at the melting point. The  
32 UCM/MMP model was parameterized by using data from the Sandia  
33 Instrumented Thermal Ignition (SITI) experiment. The UCM/MMP model was  
34 validated using data from the one-dimensional time-to-explosion (ODTX) and  
35 one-dimensional thermal violence (ODTV) experiments without using any size  
36 dependent parameters.

37 A single post ignition example calculation for the ODTV experiment was  
38 performed using a continuum mixture model for a lower density HMX material.  
39 Predictions at the higher density were not attempted since model parameters  
40 were not available for the higher density material at elevated temperatures.  
41 Even though the predicted wall velocities were lower than the measured wall  
42 velocities, the predicted trends were similar.

43 Violence was calculated using a damage model that depends on the fracture  
44 toughness, set point temperature, melting temperature, density, sound speed,  
45 and strain rate. Strain rate was determined from the measured wall velocities.  
46 The predicted and measured number of fragments were similar. We  
47 recommend the ODTV experiments be run with pure HMX at density of 1.4  
48 g/cm<sup>3</sup> to check the model. Parameterization of the multiple-material  
49 continuum model should also be done at the higher density and should  
50 include both pristine material and thermally-degraded material.

## 51 **ACKNOWLEDGEMENTS**

52 We would also like to thank Shane Snedigar for running the SITI experiments,  
53 Bill Erikson and Judith Brown for internal review, and Jeremy Lechman for  
54 management support. We would also like to thank AWE reviewers Rodney  
55 Drake and Caroline Handley. We would also like to thank AWE for supplying  
56 the material for the SITI experiments.

57 Sandia National Laboratories is a multimission laboratory managed and  
58 operated by National Technology & Engineering Solutions of Sandia, LLC, a  
59 wholly owned subsidiary of Honeywell International Inc., for the U.S.  
60 Department of Energy's National Nuclear Security Administration under  
61 contract DE-NA0003525. This paper describes objective technical results and  
62 analysis. Any subjective views or opinions that might be expressed in the  
63 paper do not necessarily represent the views of the U.S. Department of  
64 Energy or the United States Government.

65 X REFERENCES

- 66 1. Z. D. Lawless, M. L. Hobbs and M. J. Kaneshige, *Journal of Energetic*  
67 *Materials*, 2020, **38**, 214.
- 68 2. M. L. Hobbs, J. A. Brown, M. J. Kaneshige and C. Aviles-Ramos, *Propellants,*  
69 *Explosives, Pyrotechnics*, 2022, **47**, e202100155.
- 70 3. M. L. Hobbs, M. J. Kaneshige and W. W. Erikson, presented in part at 50th  
71 International Annual Conference of the Fraunhofer ICT, Karlsruhe, June,  
72 2019.
- 73 4. C. M. Tarver and T. D. Tran, *Combustion and Flame*, 2004, **137**, 50.
- 74 5. M. D. Cook, C. Stennett and M. L. Hobbs, presented in part at the 16th  
75 International Detonation Symposium, Cambridge, July, 2018.
- 76 6. M. E. Kipp, D. E. Grady and J. W. Swegle, *International Journal of Impact*  
77 *Engineering*, 1993, **14**, 427.
- 78 7. M. R. Baer and J. W. Nunziato, *International Journal of Multiphase Flow*,  
79 1986, **12**, 861.
- 80 8. S. C. Schumacher and M. R. Baer, *International Journal of Multiphase Flow*,  
81 2021, **144**, 1.