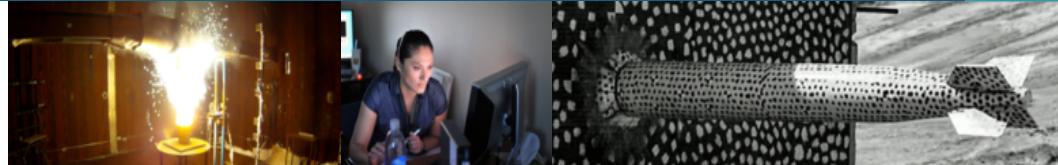
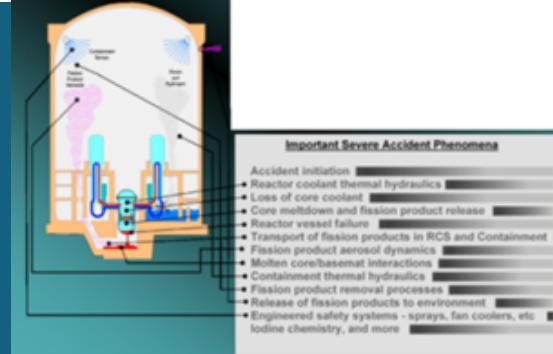




Sandia  
National  
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# MELCOR Validation Study of the Sodium Pool Fire Model with Comparison to SPHINCS



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## Technical Meeting on State-of-the-art Thermal Hydraulics of Fast Reactors

Sep 26-30, 2022

**The SNL work is supported by the DOE Work Package: RD-21SN040307**

SAND2022-XXXXC



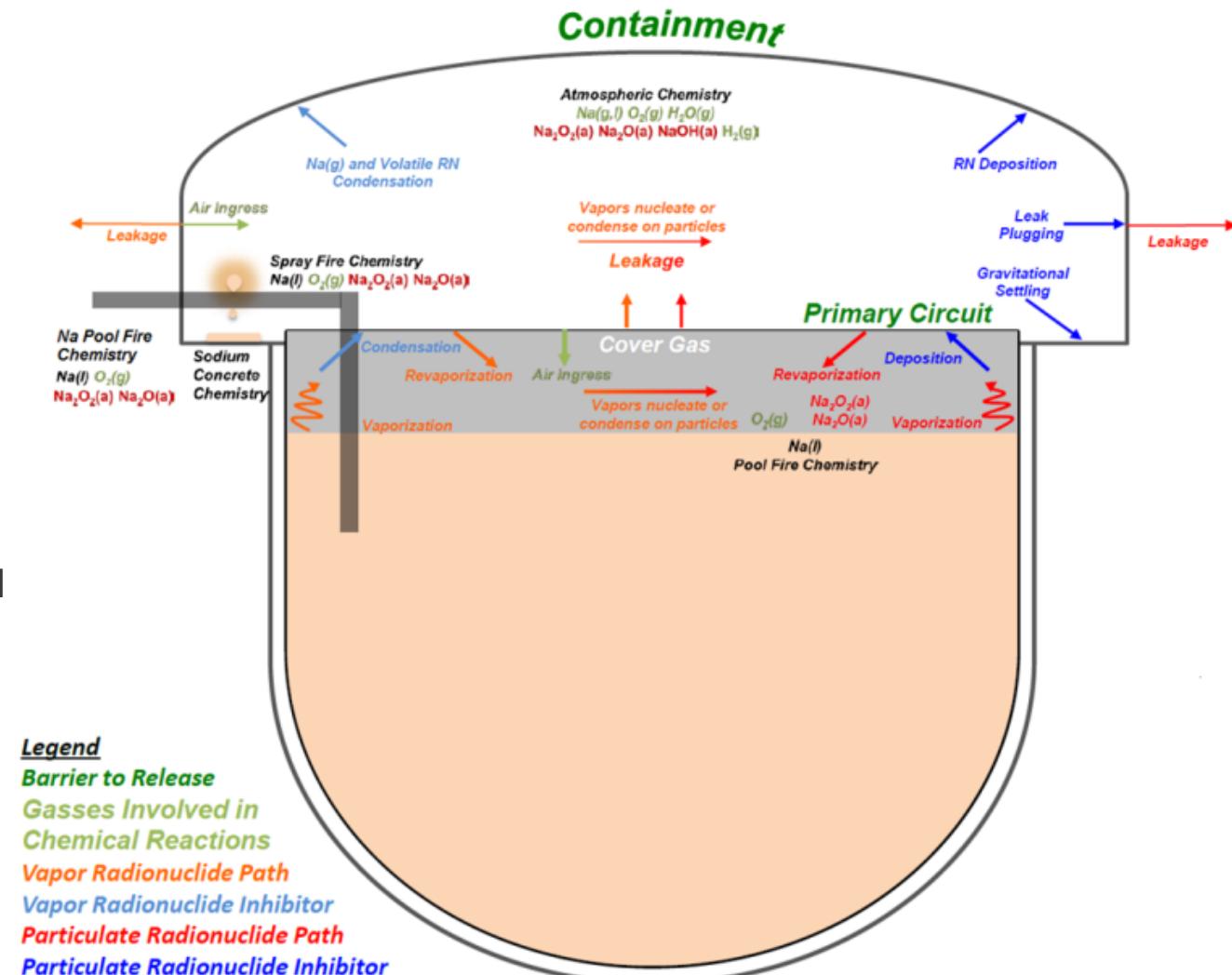
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# Current Sodium Fire Models in



Under U.S. DOE  
Advanced Reactor  
Technologies – Fast  
Reactor Program

- Most sodium fire models from CONTAIN-LMR had been implemented:
  - Most input parameters for the models are constant
  - Original spray fire model enhanced to include an upward spray sub-model
  - Atmospheric chemistry model assumes the water vapor as an ideal gas
  - CF input approach improves the model flexibility and allows sensitivity studies
    - Added CF capability to input key fire model parameters.
- Previous validation works include benchmarks using ABCOVE AB5 and AB1 tests and comparison to CONTAIN-LMR results



Sodium concrete  
chemistry (SLAM) has  
NOT yet been  
implemented into

Figure adapted from ANL-ART-3

# Model improvements under Civil Nuclear Energy Research and Development Working Group Efforts between Sandia National Labs (SNL) and Japan Atomic Energy Agency (JAEA)



A Collaborated Research was identified to improve the MELCOR pool fire model using F series pool fire experiments from JAEA

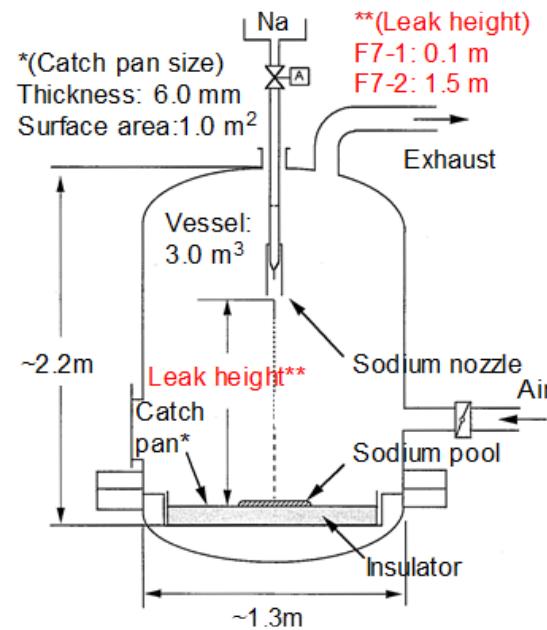
## Current Sodium Pool Fire Model in MELCOR

Parameter	Description
FO2	Fraction of the oxygen consumed that reacts to form monoxide. The value 1.0-FO2 is the remaining oxygen fraction for the reaction to form peroxide.
FHEAT	Fraction of the sensible heat from the reactions to be added to the pool. The balance will go to the atmosphere.
FNA2O	Fraction of the Na <sub>2</sub> O remaining in the pool. The balance will be applied to the atmosphere as aerosols.
FNA2O2	Fraction of the Na <sub>2</sub> O <sub>2</sub> remaining in the pool. The balance will be applied to the atmosphere as aerosols.
TOFF	Model deactivation time. This is useful for modeling experiments.
DAB	Oxygen diffusion coefficient model switch. The default diffusion correlation will be used if a real value of greater than or equal to 0.0 is specified.

Using the Control Function input capability to enhance models with code modification for the proposed models:

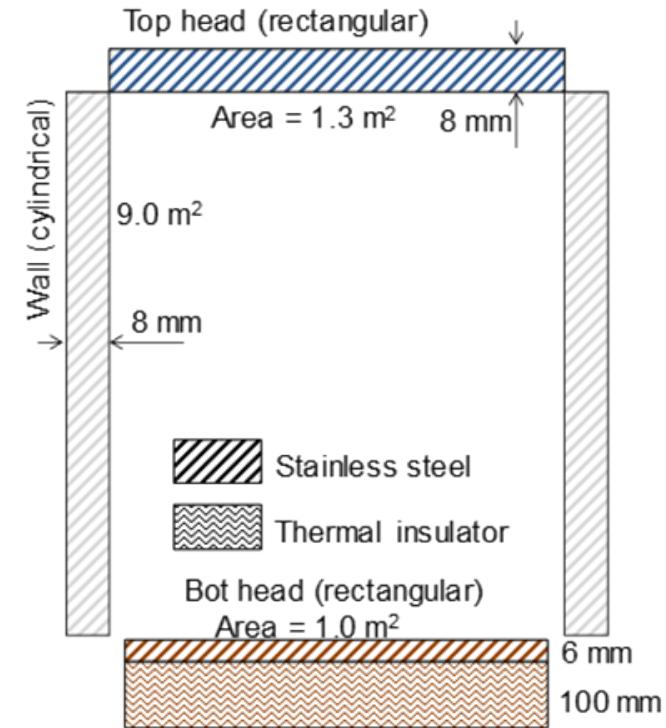
- **Highlighted** input parameters were enhanced last 2 years
  - DAB (FY2020)
    - Account the effect of oxide layer buildup
  - FNA2Ox (FY2021)
    - Allows better prediction of the suspended sodium aerosols
- FO2 is being enhanced in this year
- Other enhancement were made
  - Pool-Pan heat transfer – enhanced with pool radius functionality
  - Liquid sodium spreading
    - Viscosity dependent spreading

# F7 pool fire experiments/MELCOR Model



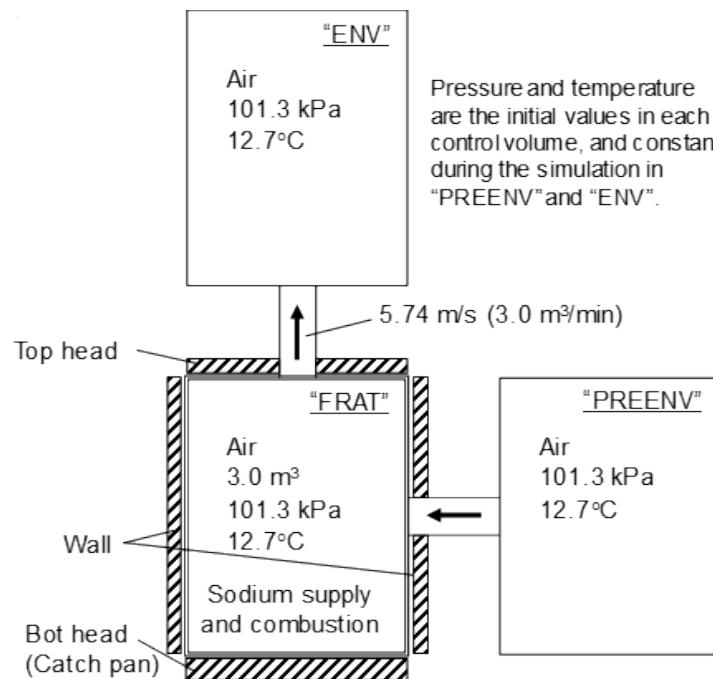
## Test Conditions

Parameter	F7-1	F7-2
Sodium temperature	505°C	
Sodium leak form	Column	
Sodium leak height from catch pan	0.1 m	1.5 m
Sodium leak duration	Approximately 1,500 s	
Average sodium leak rate	3.3 g/s	
Total leak quantity of sodium	4.94 kg	
Oxygen concentration (initial)	20.8%	20.7%
Atmosphere temperature (initial)	12.7°C	19.6°C
Atmosphere relative humidity	49.2%	71.5%
Ventilation flow rate	Approximately 3.0 m <sup>3</sup> /min	



**Measurements (representative)**

- Temperature (gas, sodium pool, catch-pan, vessel wall)
- Concentration (oxygen, aerosol)



## Sodium Fire Models used

- Spray fire
- Pool fire

# Enhancement to MELCOR Pool Fire Model



- Oxidation is limited by diffusion (DAB) through the oxide layer
- Normal pool combustion

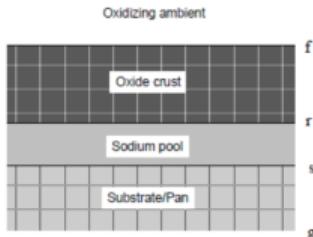
$$m\dot{Y}_{O_2} = A_s H \rho_g Y_{O_2} \quad H = 0.14 D_{\text{diff}} \left( g S_c \frac{\beta}{\nu^2} |T_{\text{surf}} - T_g| \right)^{1/3} \quad D_{\text{diff}} = \frac{6.4312 \times 10^{-5}}{P_g} \left[ \frac{(T_{\text{surf}} + T_g)}{2} \right]^{1.823}$$

- Oxygen diffusion through the oxide layer [Oliver 2010] =DAB: default

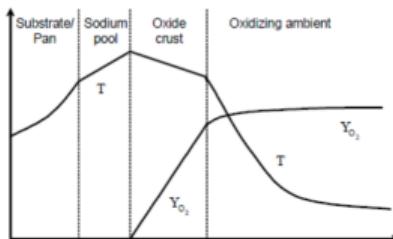
$$m\dot{Y}_{O_2} = A_s \left[ \left( \frac{Sh}{L} \right) \frac{D}{1 + \delta / \Delta_1} \right] \rho_g Y_{O_2, \infty} \quad H^* = \left( \frac{Sh}{L} \right) \frac{D}{1 + \delta / \Delta_1}$$

$$D_{\text{diff}} = \frac{\left( \frac{Sh}{L} \right) \frac{D}{1 + \delta / \Delta_1}}{0.14 \left( g S_c \frac{\beta}{\nu^2} |T_{\text{surf}} - T_g| \right)^{1/3}}$$

$$D_{\text{diff}} = \frac{D}{1 + \delta / \Delta_1}$$



Schematic of the pool layers, temperature Profile (T), and Oxygen Fraction ( $Y_{O_2}$ ) [Olivier 2010]



The oxide layer thickness  $\delta$  is given by the amount of oxide formed in the pool with an assumed porosity function.

[Olivier 2010] Olivier, T.J., et al., Metal Fires and Their Implications for Advanced Reactors Part 3: Experimental and Modeling Results, SAND2010-7113, Sandia National Laboratories, Albuquerque, NM, October 2010.

- Pool oxide fractions (FNA2Ox) – can influence the by-product sodium aerosol distribution

$$FNA2OX = a_1 \cdot \varepsilon^{a_2} + a_3 \cdot \varepsilon + a_4$$

# Non-Sodium pool model enhancement



## Liquid sodium spreading

- The spreading rate was improved using a viscosity dependent model adapted from the ex-vessel corium spreading model in MELCOR

### Adapted corium spreading model:

$$\mu \frac{u}{H^2 R} \propto \rho g H \quad \frac{dR}{dt} = C1 \frac{\rho g}{\mu \pi^3} \frac{V^3}{R^7}$$

$$R(t + \Delta t) = \sqrt[8]{R(t)^8 + C1 \cdot \frac{g}{\mu \pi^3 \rho^2} m^3 \Delta t}$$

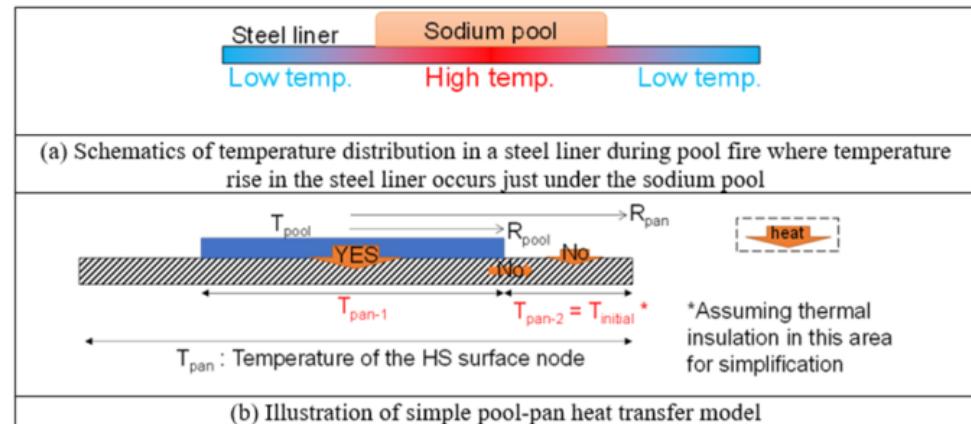
Ramacciotti correlation:

$$\mu = \mu_0 \cdot \exp(2.5 \cdot C \cdot \varepsilon)$$

Solid fraction  $\varepsilon = \frac{\sum m_j / \rho_j}{\sum m_i / \rho_i}$

## Pool-to-pan heat transfer

- Addressing the limitation of 1-dimensional heat structure model in MELCOR
  - A quasi 2-dimensional heat transfer model developed

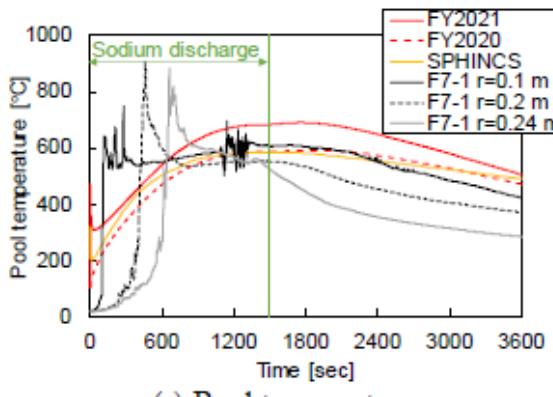


# SPHINCS Sodium Pool Fire Model

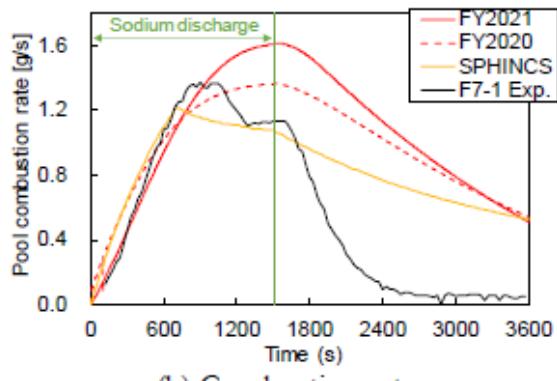


- SPHINCS is developed by JAEA
- Sodium fire analysis code – lumped mass model for control volumes with 1-dimensional flow model network (similar to MELCOR)
- Flame sheet model employed for pool combustion - between
  - pool and flame sheet
  - atmosphere and flame sheet
- Accounts for the oxide layer effect on pool combustion
- Liquid pool spreading is modeled by surface tension and gravitational forces
- SPHINCS has a 2-dimensional heat transfer model between pool and substrate

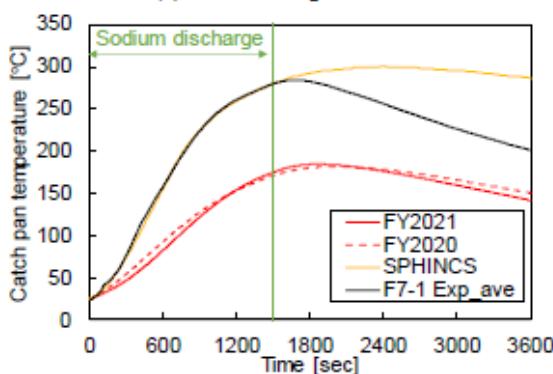
# MELCOR – SPHINCS Comparison on F7-1 Test



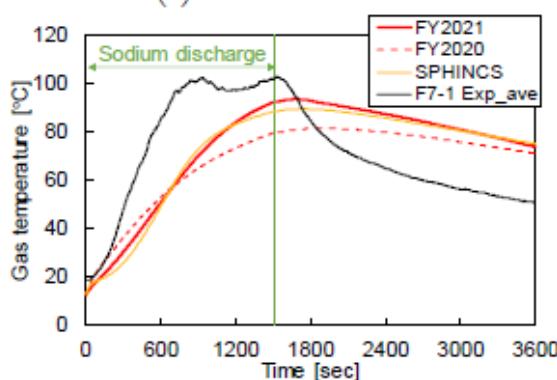
(a) Pool temperature



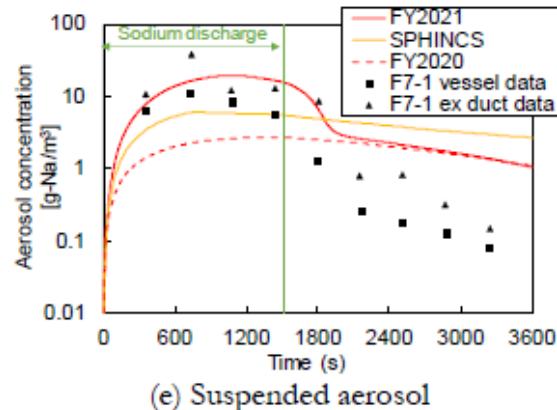
(b) Combustion rate



(c) Catch pan temperature



(d) Gas temperature

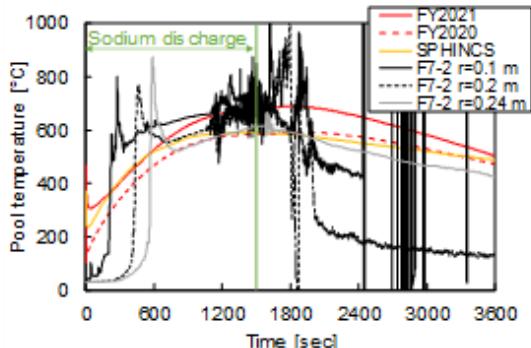


(e) Suspended aerosol

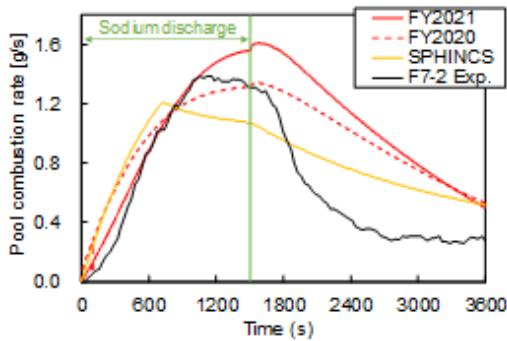
- Results indicate:
  - Similar predictions on pool combustion rate up to 600s
  - Pool temperatures are similar
  - MELCOR underpredicts the catch pan temperature\*
  - MELCOR generally predicted better aerosol concentration

\*The catch pan temperature modeling in MELCOR was not updated from FY2021 to FY2022

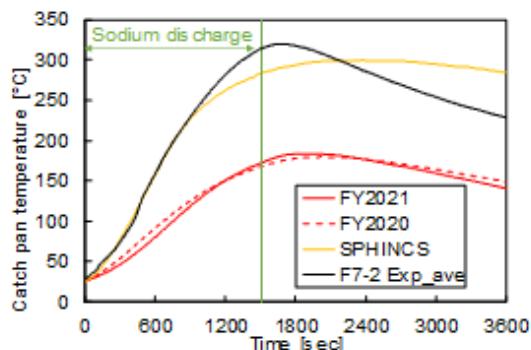
# MELCOR – SPHINCS Comparison on F7-2 Test



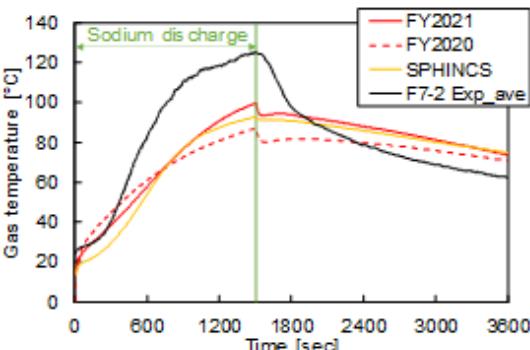
(a) Pool temperature



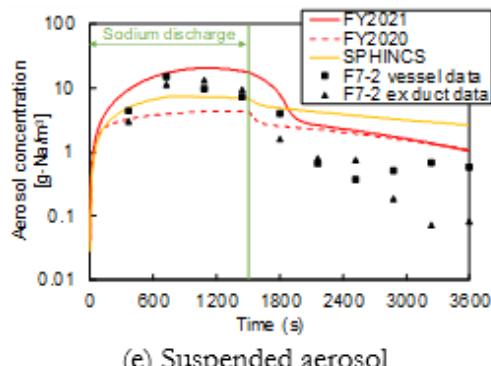
(b) Combustion rate



(c) Catch pan temperature



(d) Gas temperature



(e) Suspended aerosol

- Results indicate:
  - Similar predictions on pool combustion rate up to 1200s
  - Pool temperatures are similar
  - MELCOR underpredicts the catch pan temperature\*
  - MELCOR generally predicted better aerosol concentration

\*The catch pan temperature modeling in MELCOR was not updated from FY2021 to FY2022

# Summary and Conclusion



- This paper presents the progress on sodium fire collaboration between SNL and JAEA
- Validation study including for code-to-code comparison was possible using the JAEA's F7 experimental results
- The code-to-code comparison between MELCOR and SPHINCS demonstrated significant improvement on the agreement on many key parameters



# THANK YOU



# Backups



# DAB in Control Functions

- To model DAB, a control function variable is added to NAC input section

```
!!
! //// add NAC models
!          iactv
NAC_INPUT
!          NaCL1      NaCL2      NaCL3      NaCL4      NaCL5
NAC_RNCLASS H2OA       NA          NAOH       NA2O2      NA2O
!
NAC_SPRAY 1
  !n  CVHNAME      HITE      DME      FNA2O2    SPRDT  SOU-TYPE  MASS-NAME  THERM-NAME
    1  'FRAT'      0.1      0.0045      1.0      -1.      TF      'NA-M'    'NA-T'
!
NAC_PFIRE 1
  !n  CVHNAME      FO2       FHEA      FNA2O    FNA2O2    TOFF      DAB
    1  'FRAT'      0.60      0.6      0.9      0.9      3600.0  'DABOX'  !Pool oxide
                                         ! layer model
!
!      change FNA2O and FNA2O2 from 0.5 to 0.9
!      FO2 = Fraction of O2 that reacts to form monoxide.
!      FHEAT = Fraction of heat from rxn added to pool. Balance goes to atmosphere.
!      FNA2O = Fraction of monoxide that remains in the pool. Balance goes to atmosphere.
!      FNA2O2= Fraction of peroxide that remains in the pool. Balance goes to atmosphere.
```

# DAB in Control Functions (continue)



```

!DAB considering oxide layer
CF_ID  'DABOX'  93  FORMULA
!           NUM OF ARGs      FORMULA TEXT
CF_FORMULA      3           MIN(DAB0,AAA/BBB)
!           N   ARG NAME   VALUE
    1   DAB0        CF-VALU(DAB0)      ! Ddiff for no oxide layer
    2   AAA         CF-VALU(AAA)       !
    3   BBB         CF-VALU(BBB)       !
CF_ID  'DAB0'   81  FORMULA !Gas diffusion coefficient (Ddiff for no oxide layer)
!           NUM OF ARGs      FORMULA TEXT
CF_FORMULA      6           A/P*((TPL+TGS)/TWO)^B
!           N   ARG NAME   VALUE
    1   A            6.4312E-05    ! CONSTANT
    2   P            CVH-P('FRAT')  ! Gas pressure
    3   TPL          CVH-TLIQ('FRAT') ! Pool temperature
    4   TGS          CVH-TVAP('FRAT') ! Gas temperature
    5   TWO          2.0           ! CONSTANT
    6   B            1.823         ! CONSTANT
CF_ID  'AAA'    89  FORMULA !DAB_ox-layer = AAA/BBB
!           NUM OF ARGs      FORMULA TEXT
CF_FORMULA      6           (SH/L)*(DAB0/(ONE+DELT/DELL))
!           N   ARG NAME   VALUE
    1   SH           CF-VALU(SH)      ! Sherwood number
    2   L            CF-VALU(DIAM)   ! Pool diameter
    3   DAB0         CF-VALU(DAB0)   ! Ddiff for no oxide layer
    4   ONE          1.0           ! CONSTANT
    5   DELT         CF-VALU(THICKOX) ! Oxide layer thickness
    6   DELL         CF-VALU(DELL)   ! Characteristic length scale

```

# DAB in Control Functions (concluded)



```

CF_ID  'BBB'  92  FORMULA  !DAB_ox-layer = AAA/BBB
!
!           NUM OF ARG'S      FORMULA TEXT
CF_FORMULA      8      A* (G*SC*BET/ (NYU*NYU) *ABS (TPL-TGS) ) ^B
!
!           N   ARG NAME   VALUE
1   A           0.14          ! CONSTANT
2   G           9.8           ! Gravity
3   SC          CF-VALU(SC)  ! Schmidt number,
4   BET          CF-VALU(BET) ! Gas expansion,
5   NYU          CF-VALU(NYU) ! Kinematic viscosity
6   TPL          CVH-TLIQ('FRAT') ! Pool temperature
7   TGS          CVH-TVAP('FRAT') ! Gas temperature
8   B           0.3333333  ! CONSTANT

CF_ID  'THICKOX' 71  FORMULA
CF_FORMULA      7      (X1/D1+X2/D2) / ((one-P)*A)
1   X1          RN1-AML('FRAT',NA2O,TOT)  ! aerosol na2o in pool
2   D1          2280.0                     ! density of na2o
3   X2          RN1-AML('FRAT',NA2O2,TOT) ! aerosol na2o2 in pool
4   D2          2800.0                     ! density of na2o2
5   P           cf-valu('porosity')       ! porosity
6   one          1.0
7   A           CF-VALU(PAREA)          ! pool area

cf_id  'porosity' 70  formula
CF_ULB 3  0.0  0.95
cf_formula      2  P*x
1   P           cf-valu('FSOLID')        ! solid fraction
2   x           1.5                      ! multiplier

cf_id  'Fsolid' 42  formula
cf_formula      4  min(vmax,s/(s+nal/rho))
!
!           N   ARG NAME   VALUE
1   s           cf-valu('Na_Ox_V')    ! total oxide volume
2   nal         cvh-mass('FRAT',POOL) ! pool mass
3   rho         cvh-rho('FRAT',POOL) ! pool density
4   vmax        0.98                  ! max solid fraction allowed

```

$$0.14 \left( g S_c \frac{\beta}{V^2} |T_{\text{surf}} - T_g| \right)^{\frac{1}{3}}$$