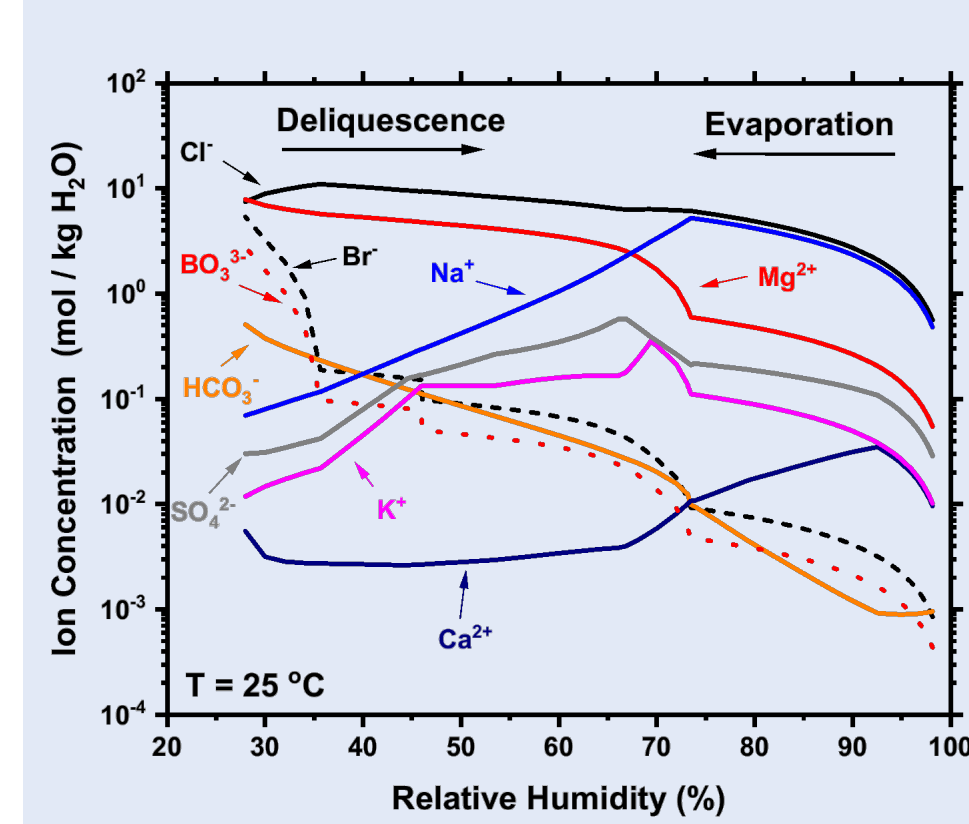




# Towards Understanding the Controlling Nature of Crack Tip Chemistry on the Stress Corrosion Cracking of Austenitic Stainless Steels

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## MgCl<sub>2</sub> Brine Dominant at Low Relative Humidities

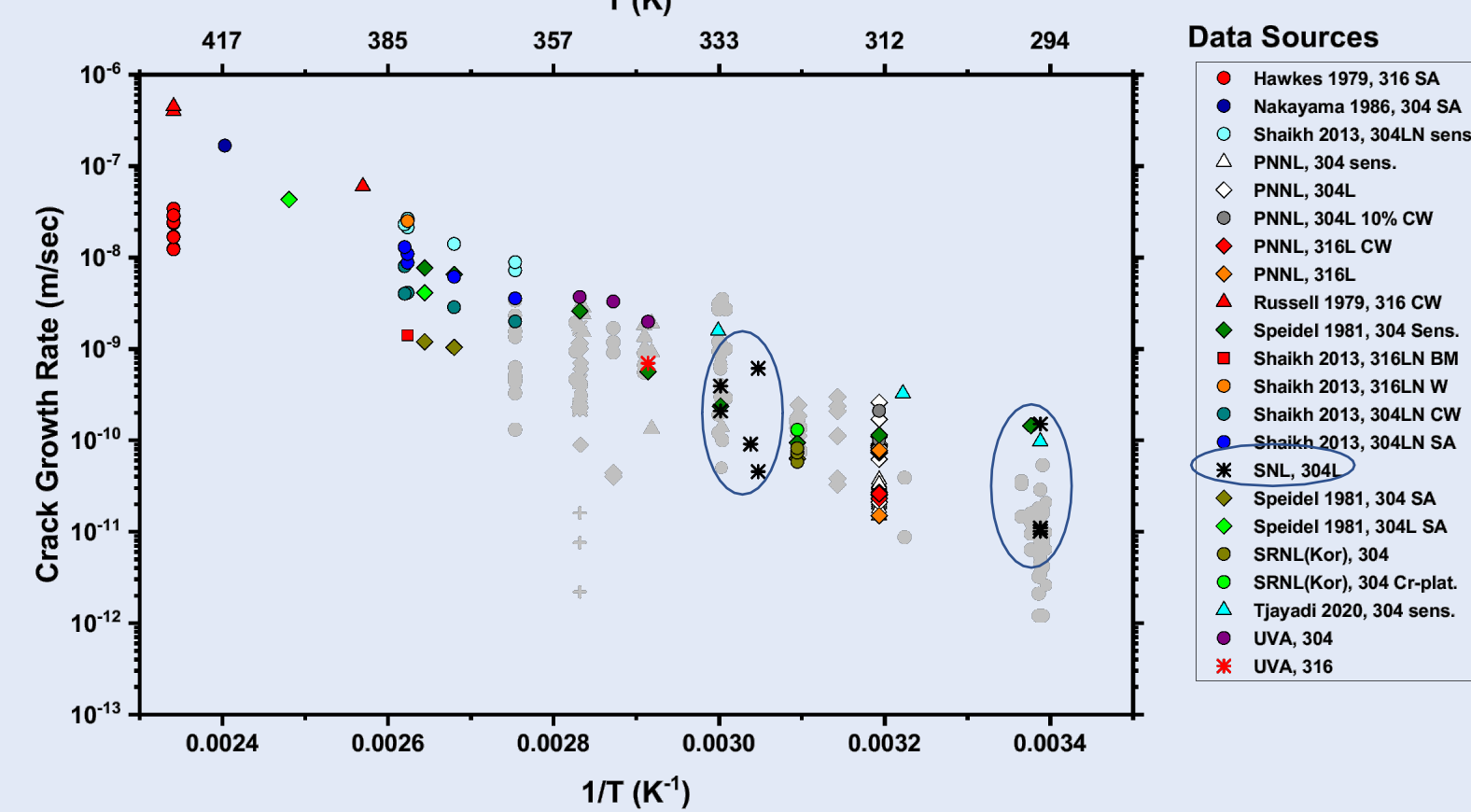


- For Spent Nuclear Fuel canisters, as radioactive materials decay, a decrease in temperature and increase in relative humidity occurs
- In a sea salt environment, concentrated chlorides (MgCl<sub>2</sub> dominant < 75 % RH) will be the first deliquesced salts on the canister surface [1]

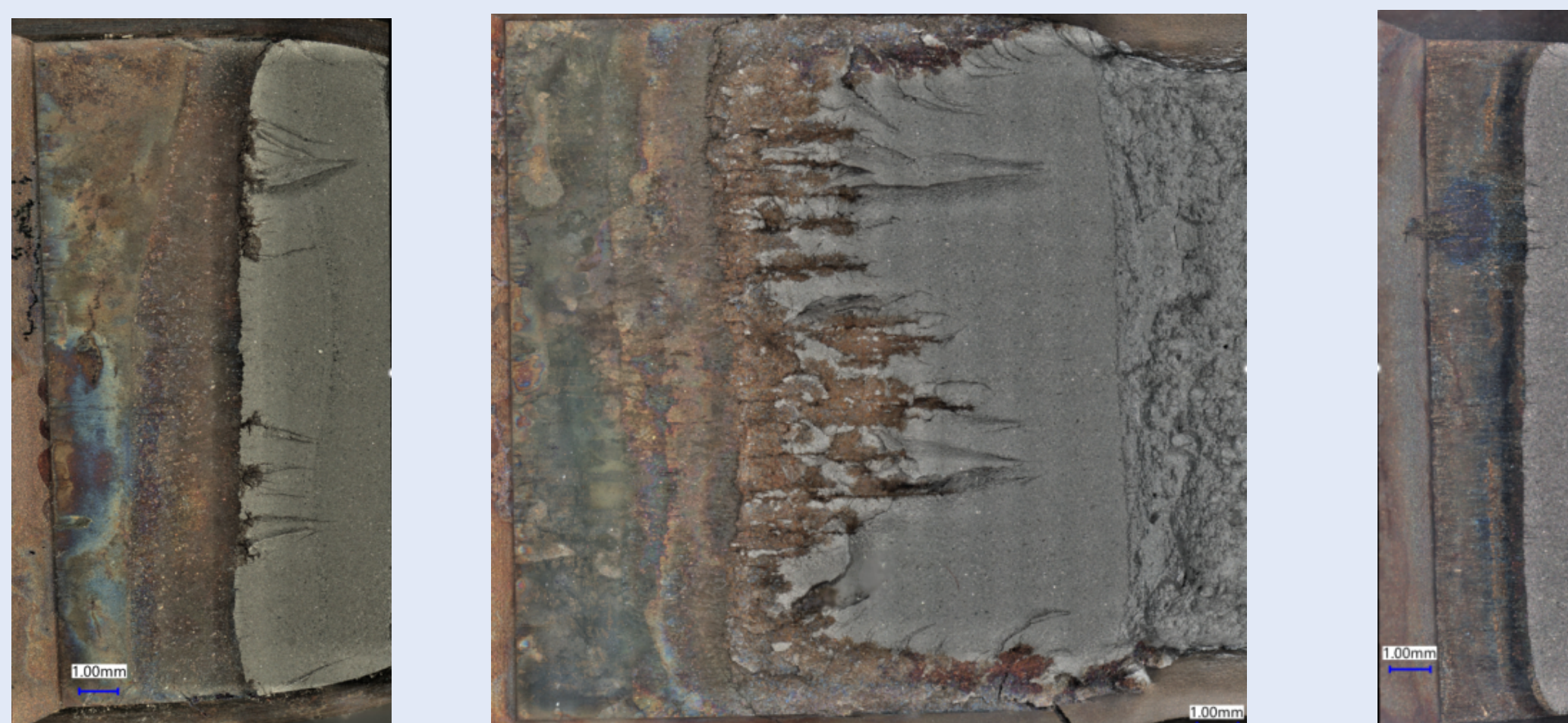
- Goal: Explore the similitude of stress corrosion cracking of SS304 in concentrated chloride environments

## Austenitic SS304L Exhibits Solution-Dependent Fracture Morphology

- SS304L, under the same loading protocol and maximum stress intensity, exposed to saturated MgCl<sub>2</sub> and NaCl
- SNL measured crack growth rates within literature scatter [2]



- Solution composition, material lot, direction, and temperature influence fracture morphology

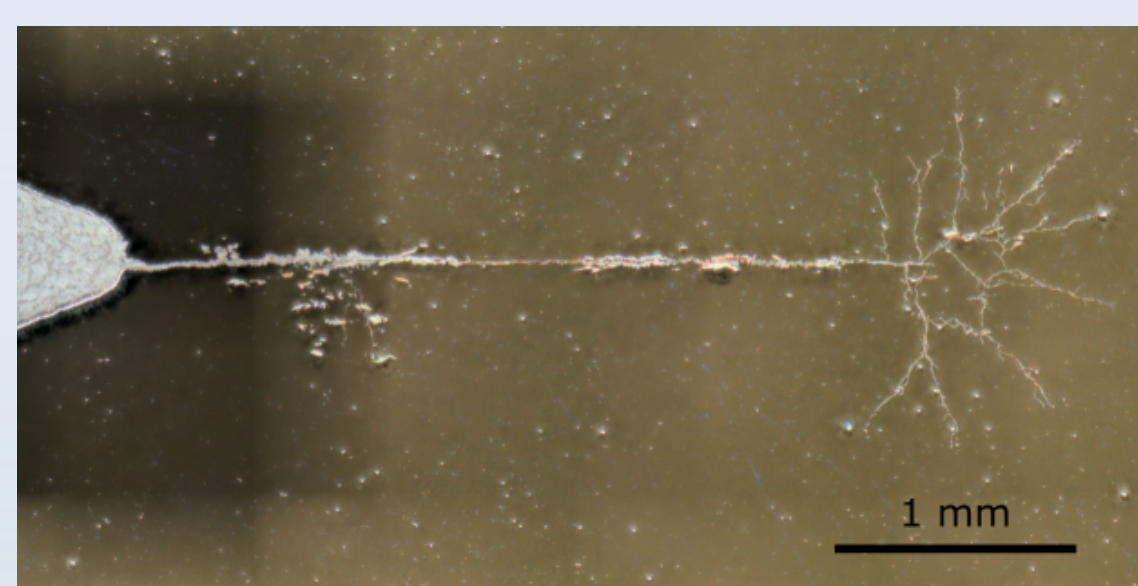
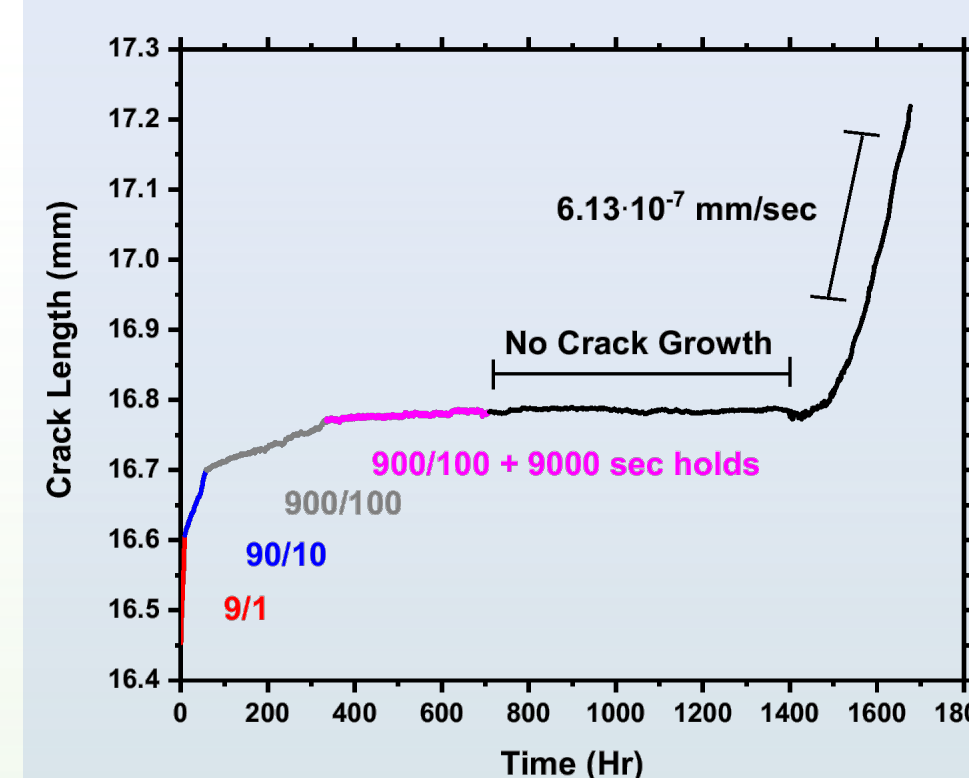


5 M MgCl<sub>2</sub>  
25 °C

5 M MgCl<sub>2</sub>  
55 °C

5 M NaCl  
60 °C

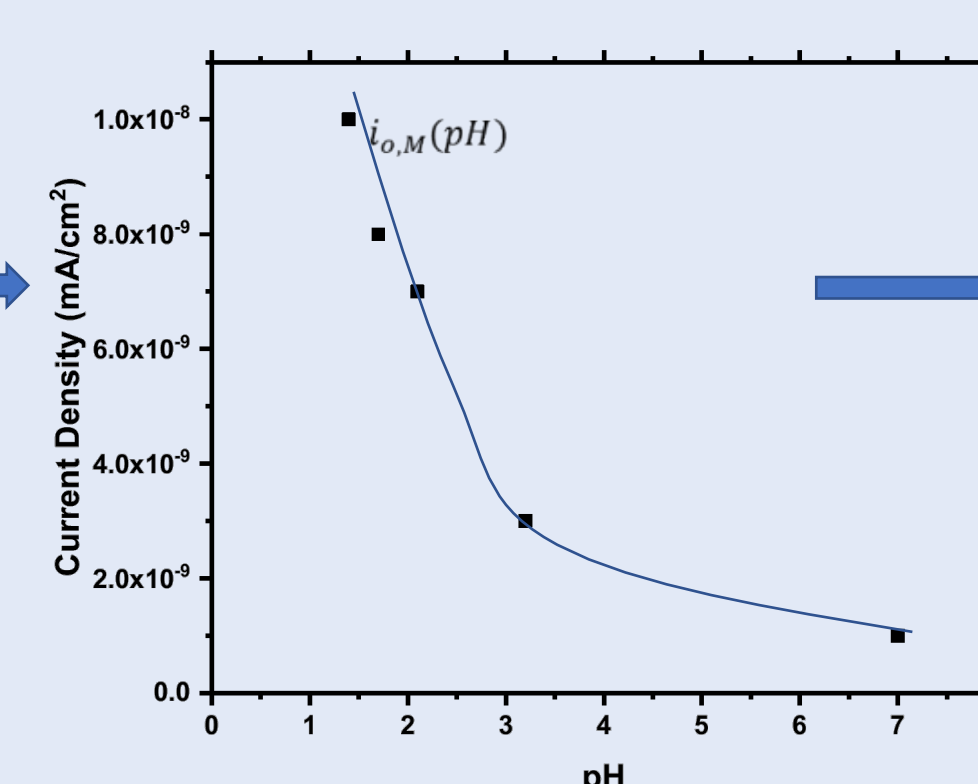
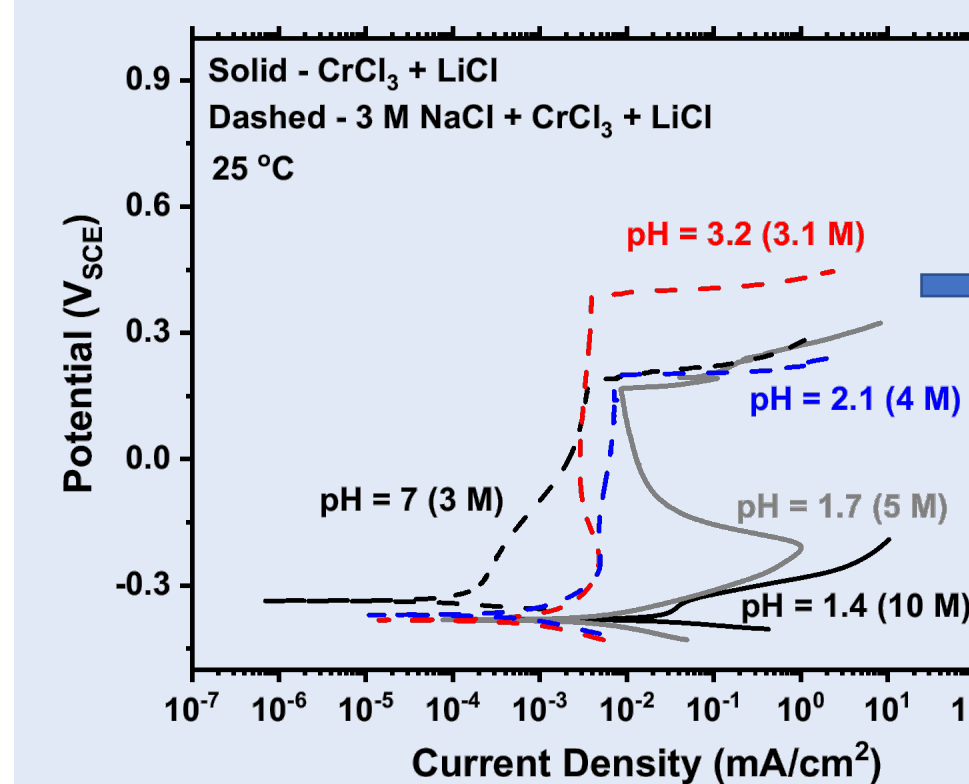
- Significant crack branching in MgCl<sub>2</sub> solutions at 55 °C may influence mechanical driving force and cracking kinetics



Could differences in crack tip electrochemistry be causing the differences in cracking morphology?

## Creation of Reactive Transport Model to Predict Crack Tip Electrochemistry

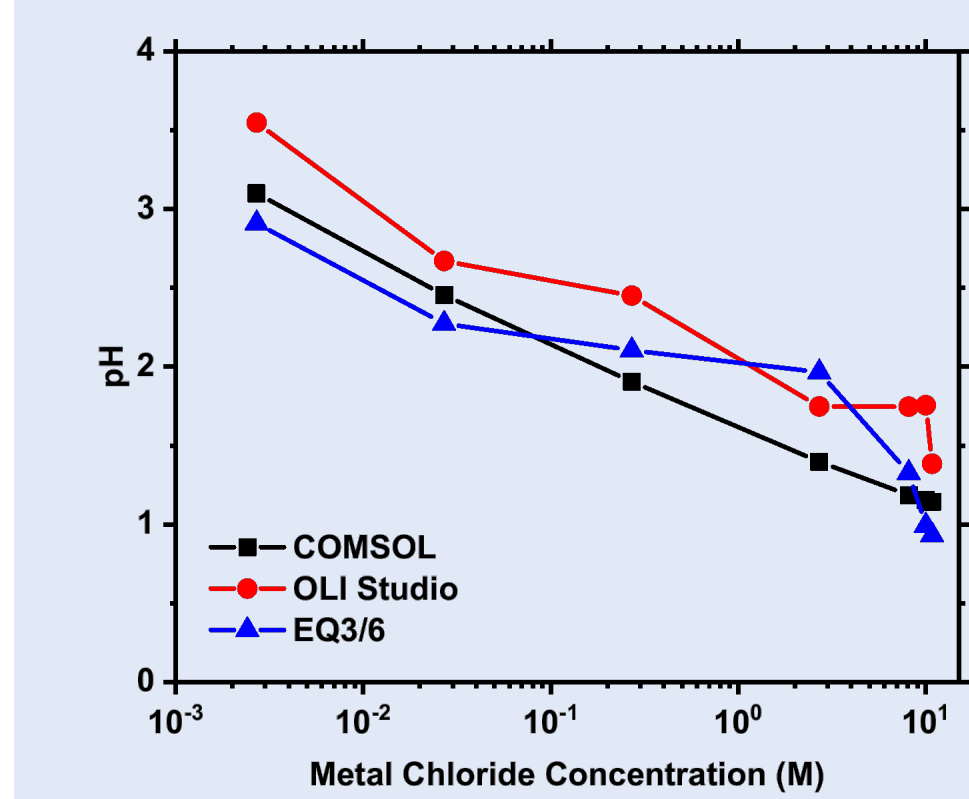
Measurement of crack tip boundary conditions in deaerated solutions as a function of pH



$$i_{act,M}(pH) = i_{o,M}(pH) \cdot 10^{\frac{\eta_M}{AM}}$$

$$i_M(pH) = \frac{i_{act,M}(pH)}{1 + i_{act,M}(pH)}$$

COMSOL pH calculated with [H<sup>+</sup>] agrees with activity-based pH



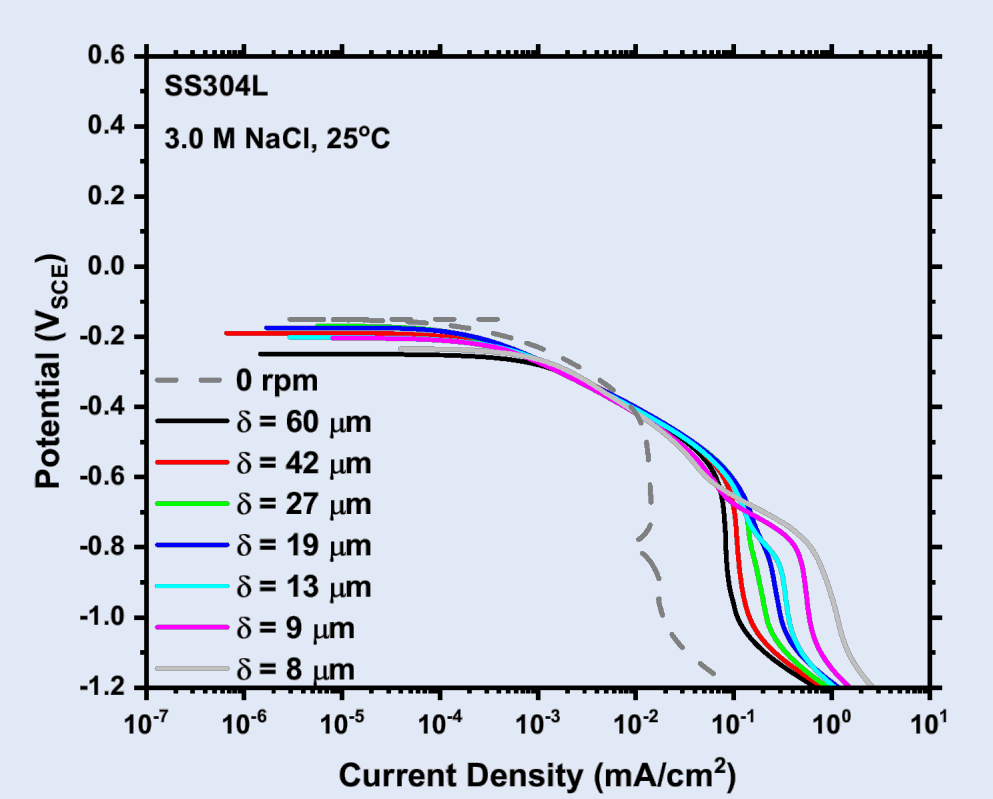
Metal Hydrolysis  
Water Ionization  
Metal Formation

Passive, HER, ORR

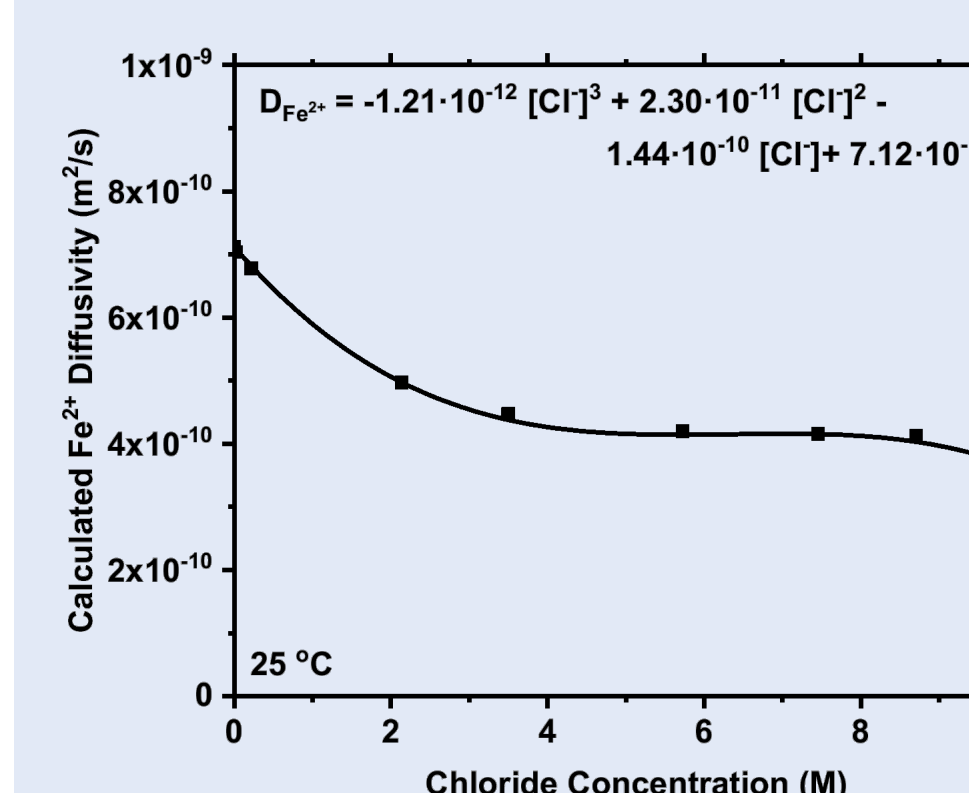
Passive, HER, ORR

Active, HER, ORR

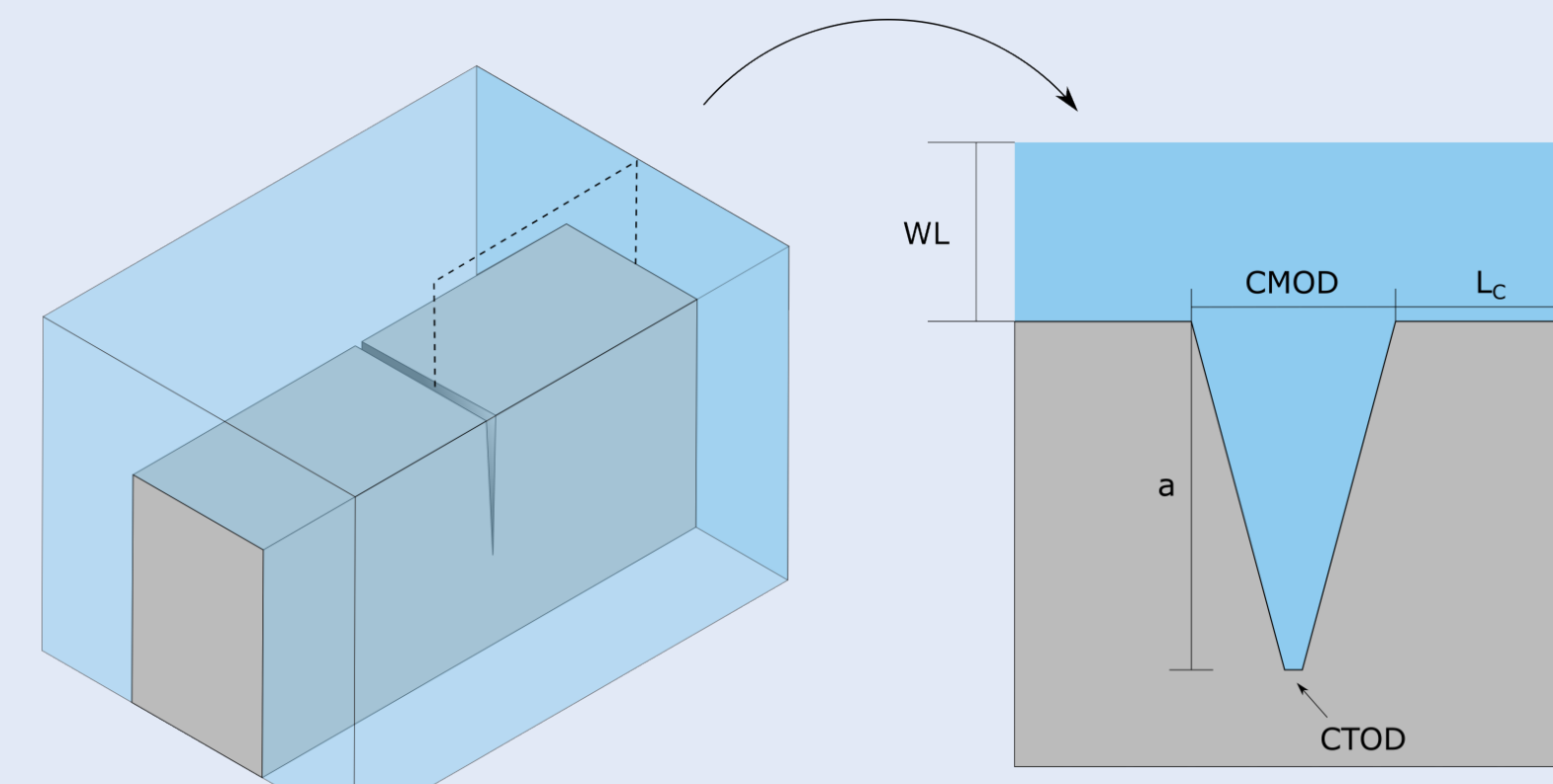
Diffusion limited ORR with O<sub>2</sub> flux at air/solution boundary [3]



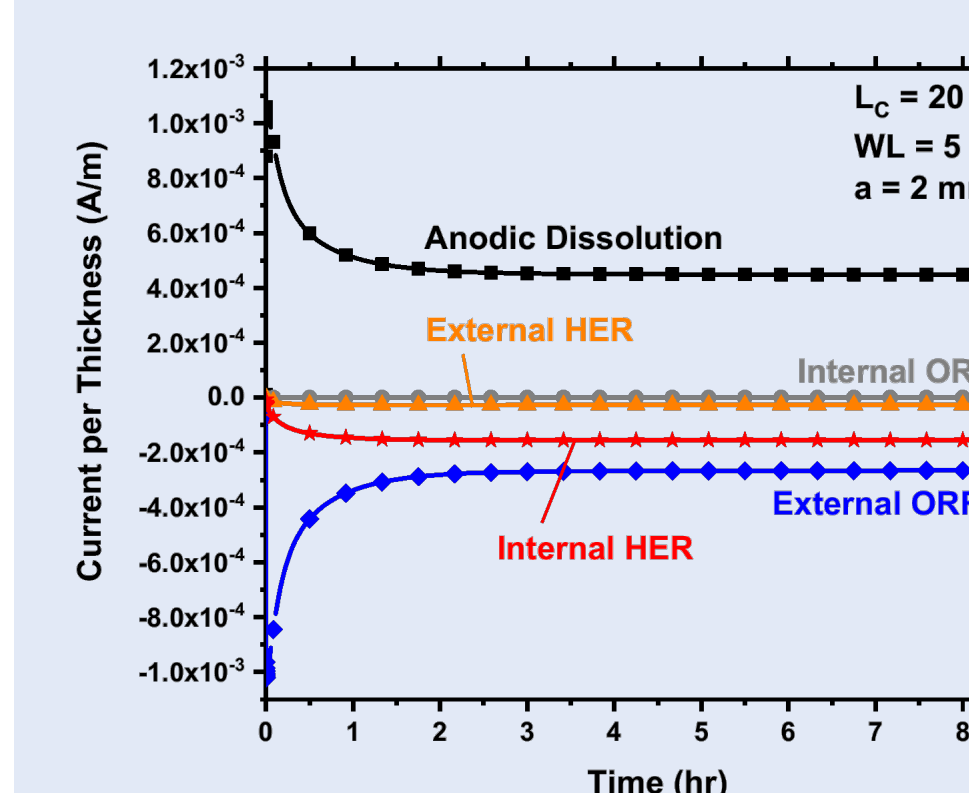
Incorporation of concentration dependent diffusivities



2D crack tip geometries based on stress intensity (load) [4]

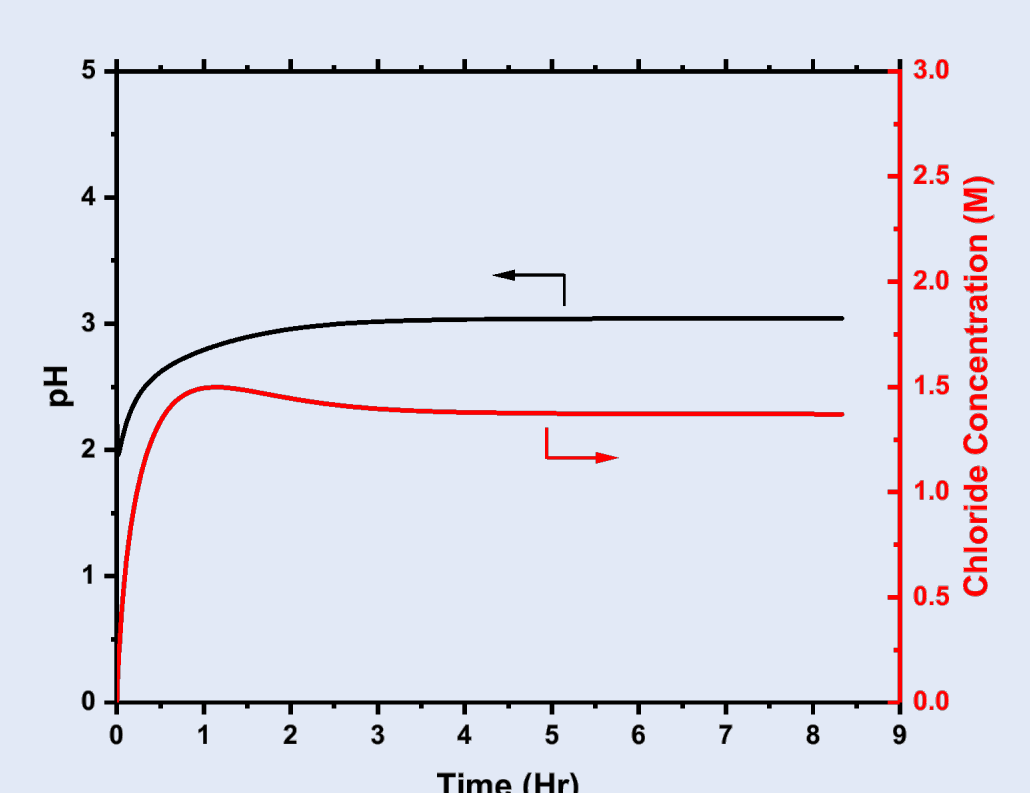


## Local Cathodic Reactions Play Significant Role in Determining Modeled Crack Tip Electrochemistry

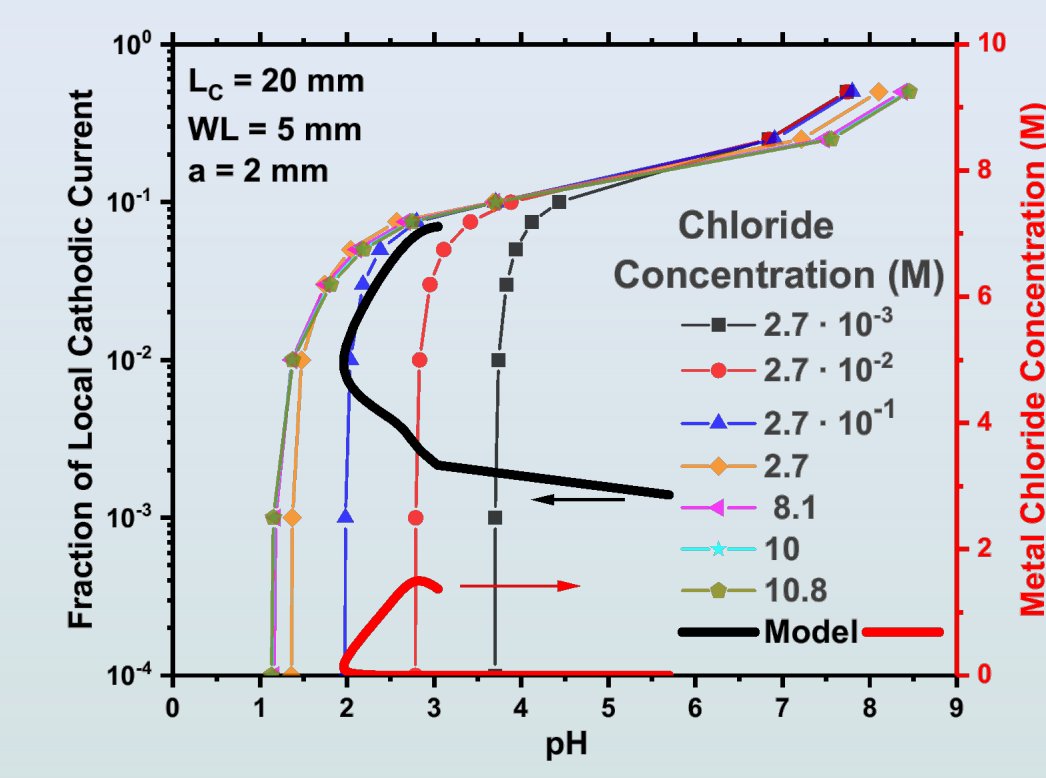
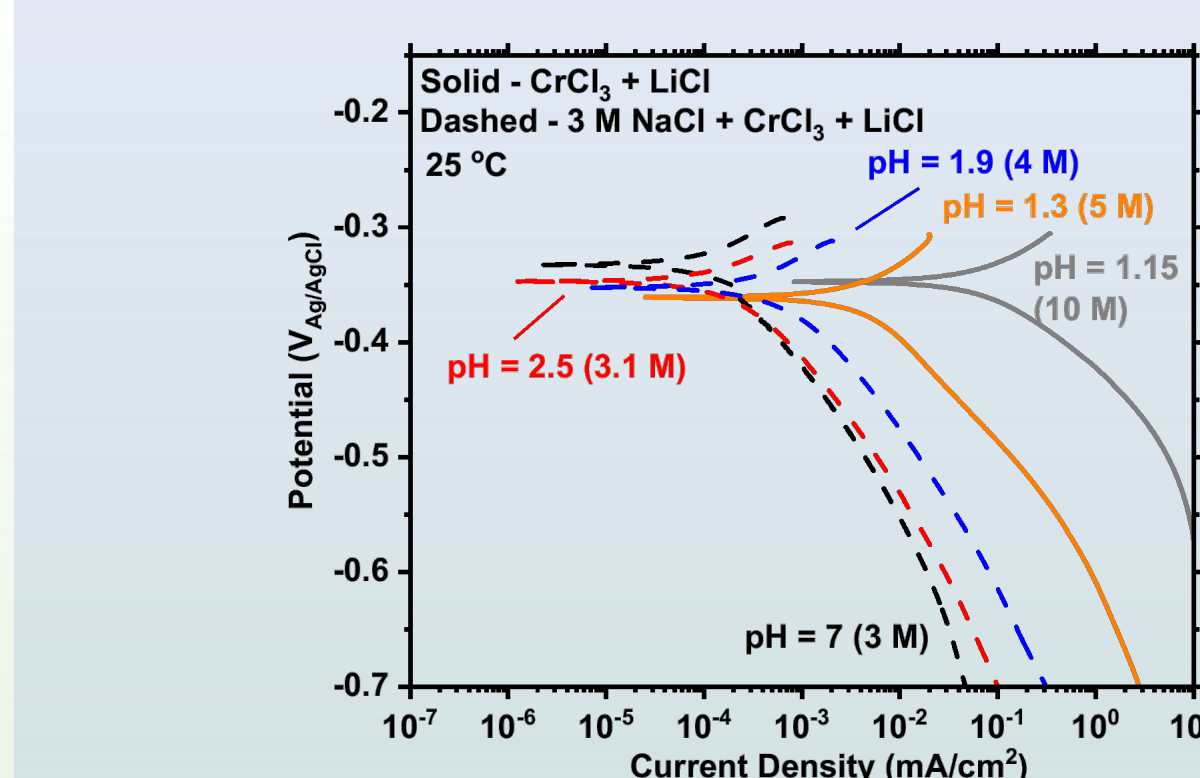


### Parameters

- WL = 5 mm
- a = 2 mm
- L<sub>c</sub> = 20 mm
- [NaCl] = 3 M
- T = 25 °C

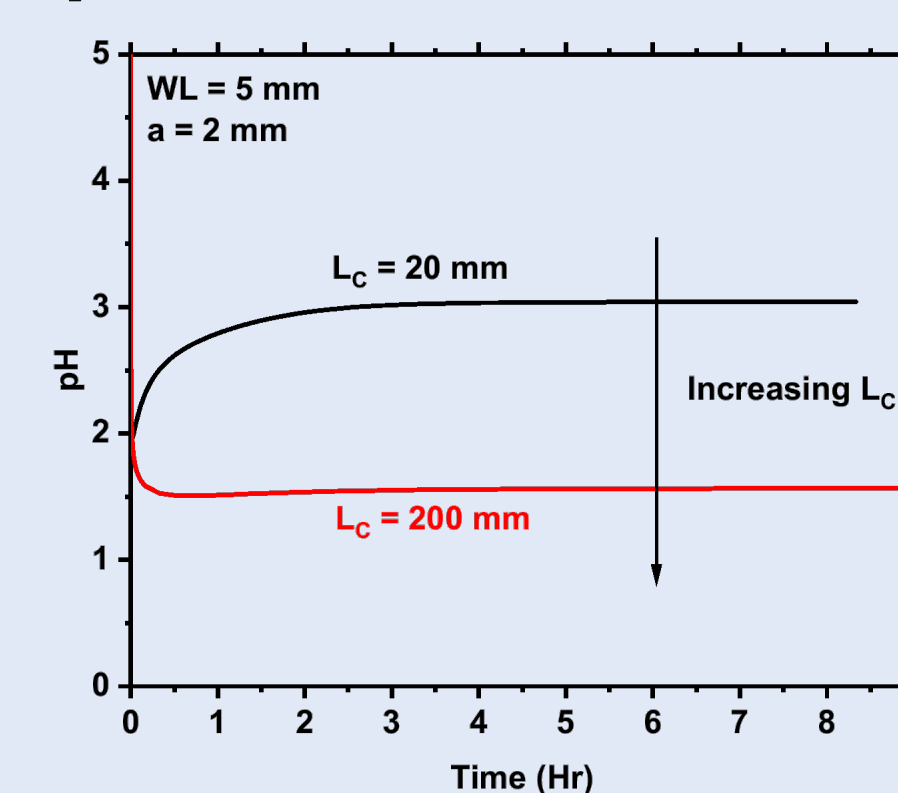


- Majority of cathodic current is external ORR (strong coupling to ext. surface)
- ~10% of total cathodic current is HER local to inside the crack which causes a significant pH rise

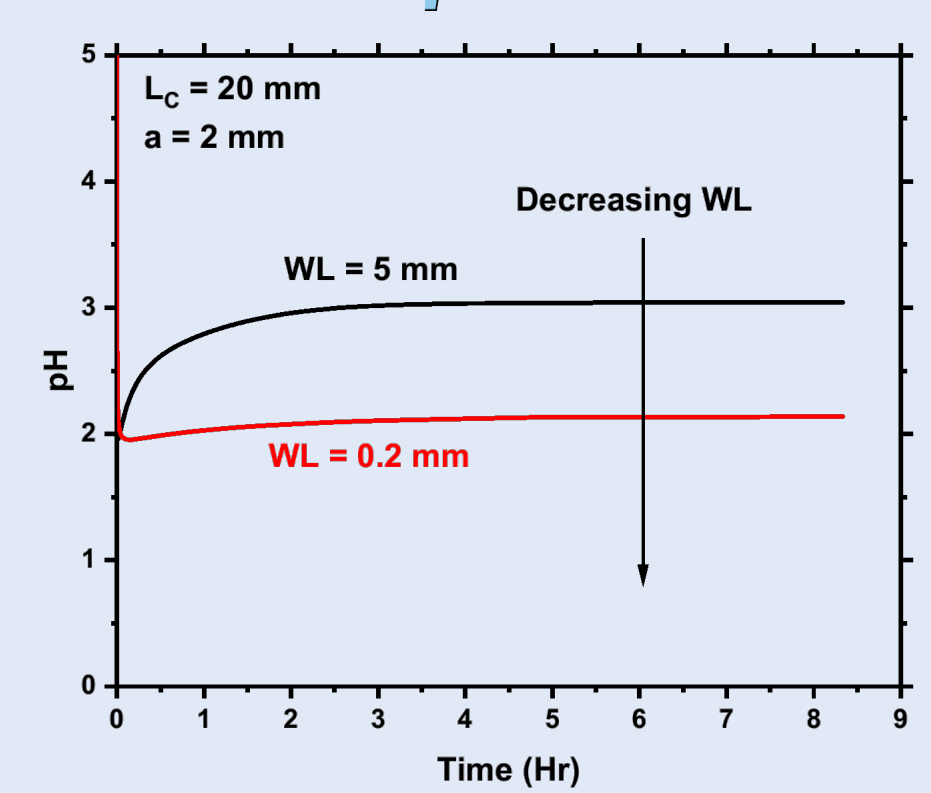


## Model Indicates Electrochemical Similitude is Often not Up-held

Larger Cathode  
Decreases pH

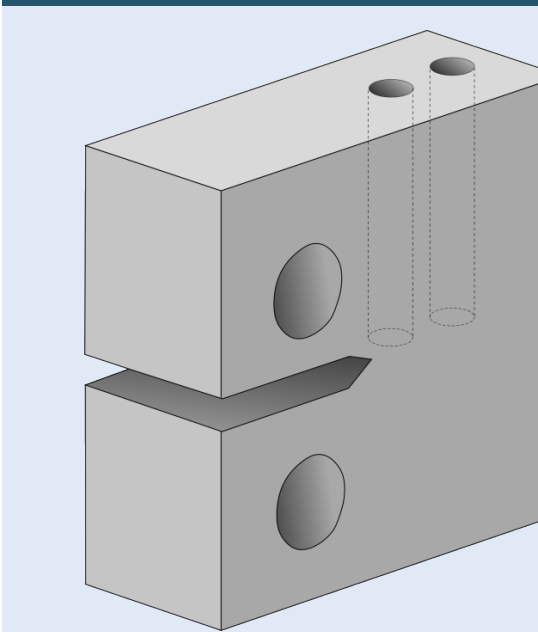


Thinner WL  
Decreases pH

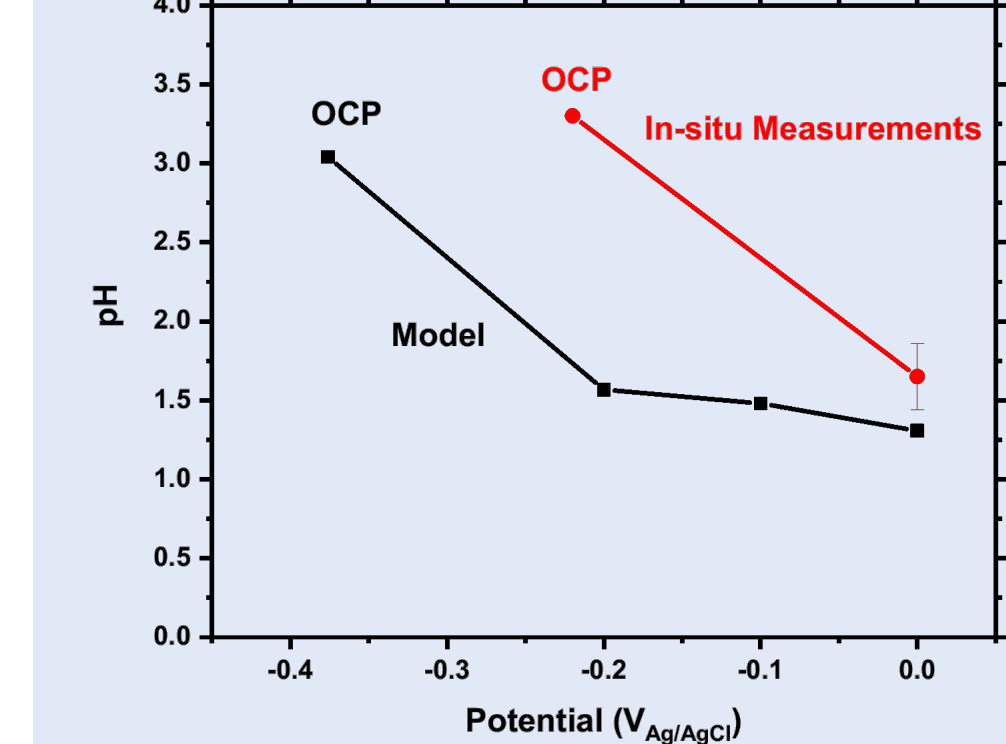
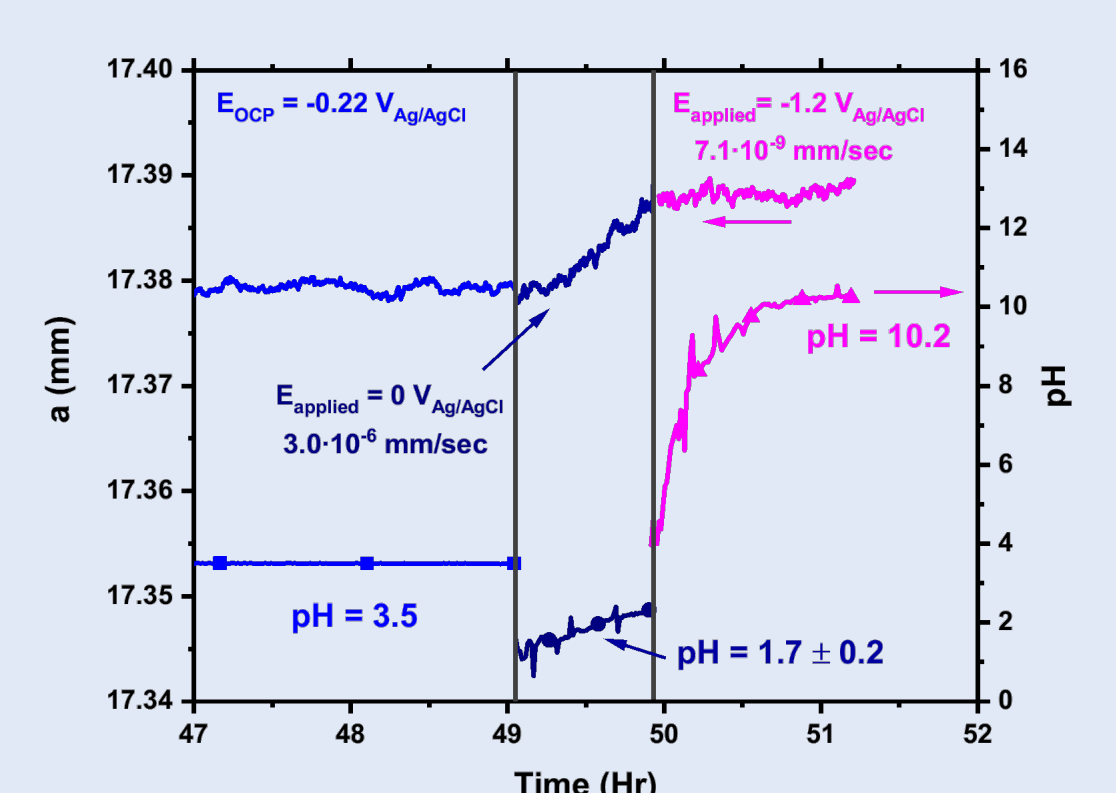
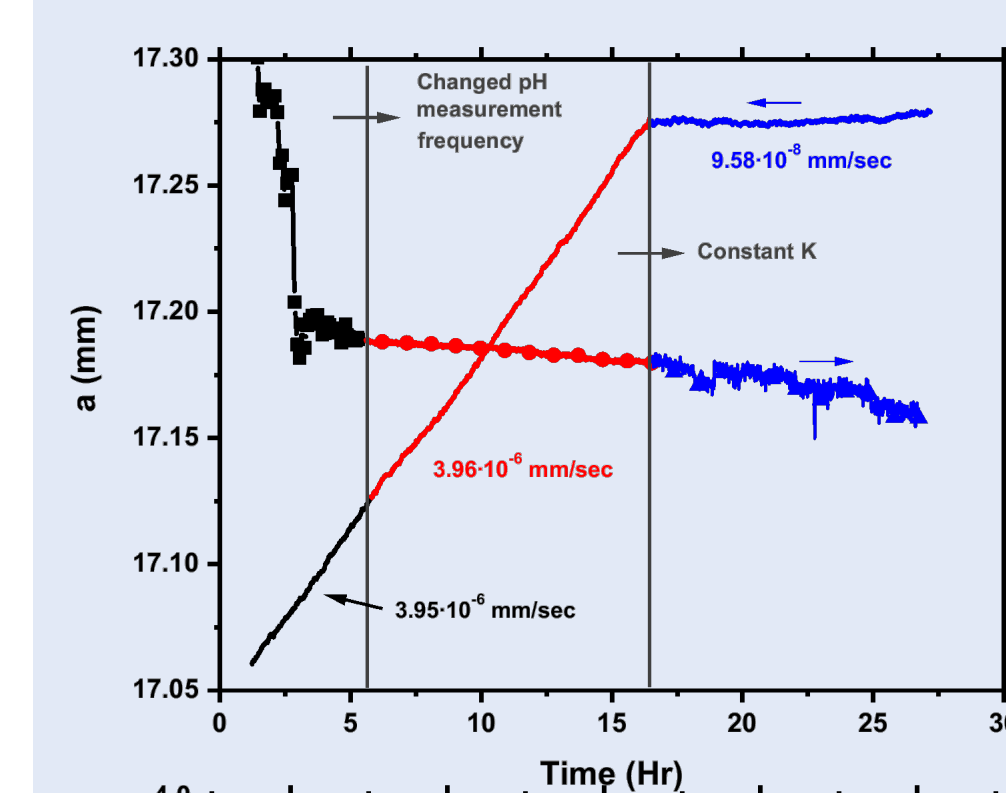


- Increasing cathode length and decreasing WL thickness decrease pH at the crack tip
- Electrochemical similitude not maintained
- Extrapolating crack growth from lab-scale specimens to field-relevant conditions could be problematic

## In-situ Measurements Confirm Polarizations Highly Influences Crack Tip Chemistry



- Holes do not significantly change mechanical driving force
- Confined dimensions do not significantly impact ohmic drop
- Measurement of in-situ crack tip pH and cracking kinetics with DCPD



- pH in SS304L exposed to 3M NaCl ~ 3.5 during constant K
- Anodic polarizations increase CGR and decrease pH
- Same trend present between model and experiments

## Conclusions and Future Exploration of Electrochemical Similitude of SCC

- SS304L exhibits CGR within literature scatter however displays non-uniform crack front
- Newly created model to predict crack tip electrochemical conditions shows significant influence of internal HER
- Model indicates external environment (sample size and WL thickness) highly influence crack tip conditions
- In-situ crack tip measurements show same trend as model
- Future exploration of influence of sample geometry and exploration of NaCl vs. MgCl<sub>2</sub> with model and in-situ crack tip measurements