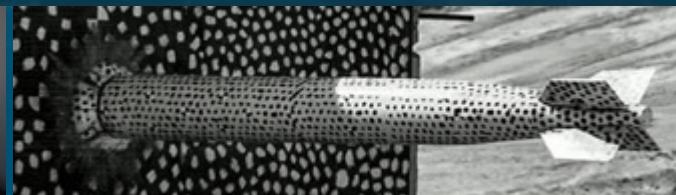
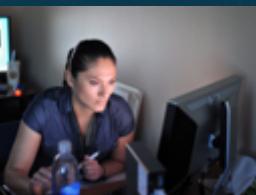


# MELCOR for High Temperature Gas-cooled and Fluoride High Temperature Reactor Modeling



## MELCOR Workshop June 13-11, 2021

*PRESENTED BY*

Brad Beeny



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# MELCOR HTGR and FHR Modeling and Development Thermal Hydraulics – Theory

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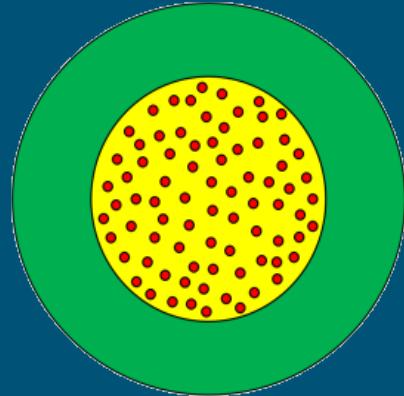


COR thermal hydraulics theory – generally applicable to both HTGRs and FHRs

- COR components and materials
  - Specialized MX and RF components for HTGR/FHR cores
  - Interpretation of FU for HTGR/FHR fuel elements
  - Specification of materials
  - Elements of best practice for components, materials, and nodalization
- Conduction
  - Intracell (between components within a COR cell)
  - Intercell (between components in adjacent COR cells)
  - Boundary (between COR and core boundary HS)
- Convection and flow
- Point Reactor Kinetics
- Oxidation (HTGR)
- Control volume hydrodynamics working fluid
- Other references

## ...COR Components and Materials...

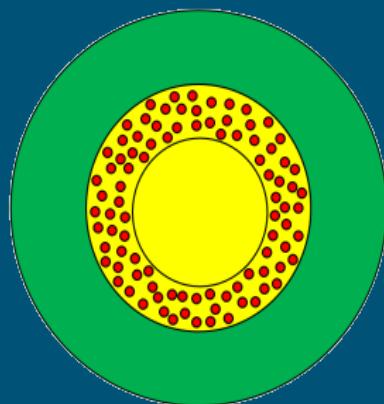
Conventional  
Pebble Fuel  
Element  
(HTGR/PBR)



TRISO

Fuel (FU)

Annular Pebble  
Fuel Element  
(FHR)



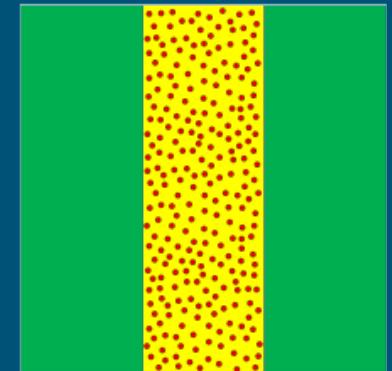
GRAPHITE

Fuel Extra Material (FUXM)

GRAPHITE

Matrix (MX)

Prismatic Fuel  
Element  
(HTGR/PMR)



## COR Components – Matrix (MX)



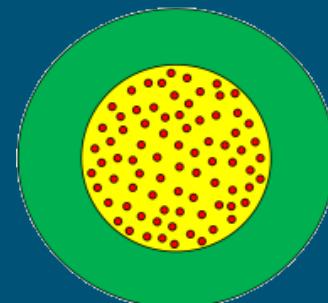
Matrix (MX) component is non-supporting, one-sided, and “thick” for purposes of heat transfer calculations

- Allocate material mass, component surface area, and other geometry
- Ties in to diffusional fission product release model
- Generally participates in conduction, convection, radiation, and oxidation

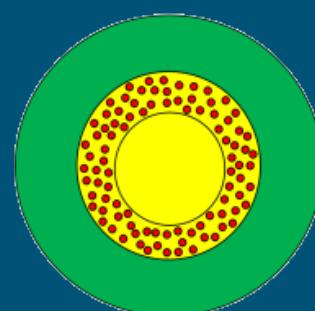
MX participates in intracell conduction (FU/MX) and intercell conduction (MX-MX, MX-RF, MX-SS)

MX is best pictured conceptually as the unfueled (TRISO free) region of a fuel element (green below)

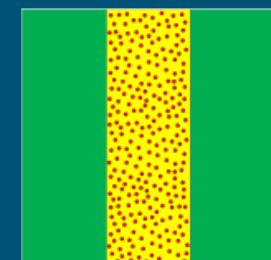
Conventional  
Pebble Fuel  
Element  
(HTGR/PBR)



Annular Pebble  
Fuel Element  
(FHR)



Prismatic Fuel  
Element  
(HTGR/PMR)





Reflector (RF) component is non-supporting, two-sided, and can have multiple orientations

- Radial reflectors (oriented inner/outer)
- Axial reflectors (oriented upper/lower)
- Generally participates in conduction, convection, radiation, and oxidation

RF participates in intercell conduction (RF-RF, RF-MX, RF-SS) and should not be collocated with FU and MX, rather it should be radially adjacent, e.g:

- Radially adjacent central reflector and active fuel region
- Radially adjacent peripheral/outer reflector and active fuel region

Core support logic:

- RF cannot bear the load of FU/MX above, e.g. a bottom reflector cannot “hold up” the active core
- FU/MX cannot bear the load of RF above, e.g. a top reflector cannot be “held up” by the active core
- Utilize SS (e.g. primary material GRAPH) where necessary and preferably in its own COR cells (not mixed with MX or RF)

# COR Components – Fuel (FU) and Extra Material (FUXM)



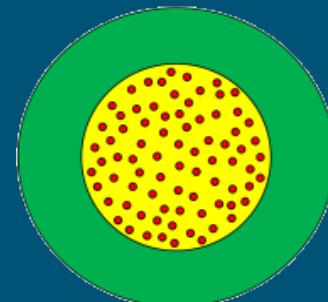
Fuel (FU) component is non-supporting, one-sided, and can include “extra material” (FUXM)

- Generally participates in conduction and radiation
- Ties to diffusional fission product release model and participates in radionuclide transport

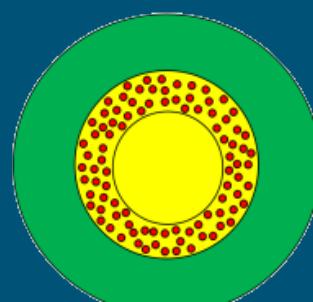
FU/FUXM participates in intracell conduction (FU/MX) and should be collocated with MX (like FU/CL in LWR)

FU/FUXM is best pictured conceptually as the fueled (TRISO laden) region of a fuel element (red/yellow below)

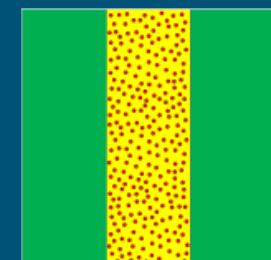
Conventional  
Pebble Fuel  
Element  
(HTGR/PBR)



Annular Pebble  
Fuel Element  
(FHR)



Prismatic Fuel  
Element  
(HTGR/PMR)





Recall “primary materials” are:

- The chief constituent material of a core component,
- Optionally specified by component (COR MELGEN input),
- NOT restricted to conventional built-ins known to MELCOR (MP package),
- Possibly characterized with the new user-defined materials (UDM) capability, and
- Possibly characterized with the new generic oxidation model (GOM) interfaced to UDM so as to:
  - Define oxidation reaction stoichiometry and energetics, or
  - Permit UDM access to built-in MELCOR graphite oxidation models by way of GOM

COR\_FUM, COR\_MXM, and COR\_RFU cards specify FUXM, MX, and RF material names

Recall COR\_NMAT specifies component-wise mass of UDM’s when leveraged as primary materials



FU uses  $\text{UO}_2$  (modify in MP as necessary, e.g. to UCO) and is collocated in COR cells with MX

FUXM is a part of FU and uses either GRAPH (built-in or MP redefinition) or some UDM

- COR\_FUM for FUXM material name/mnemonic
- COR\_KFU has a slot for extra material mass specification by COR cell

MX \*\*\*MUST USE\*\*\* UDM/GOM, COR\_MXM, and COR\_NMAT (invoking MX) to either:

- Template (copy) built-in GRAPH and access built-in graphite oxidation models, or
- Define a new material dissimilar to built-in GRAPH along with a user-specified oxidation model

RF uses either GRAPH (built-in or MP redefinition) or some UDM

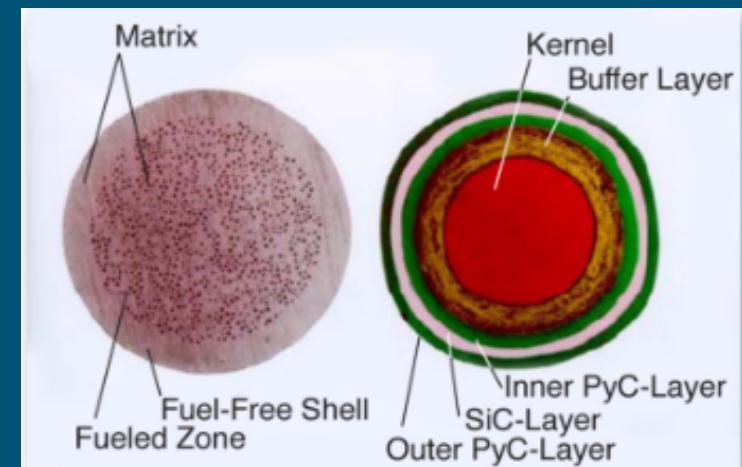
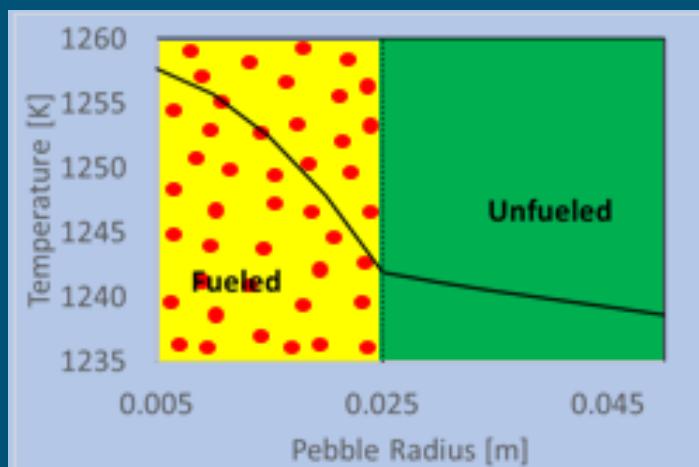
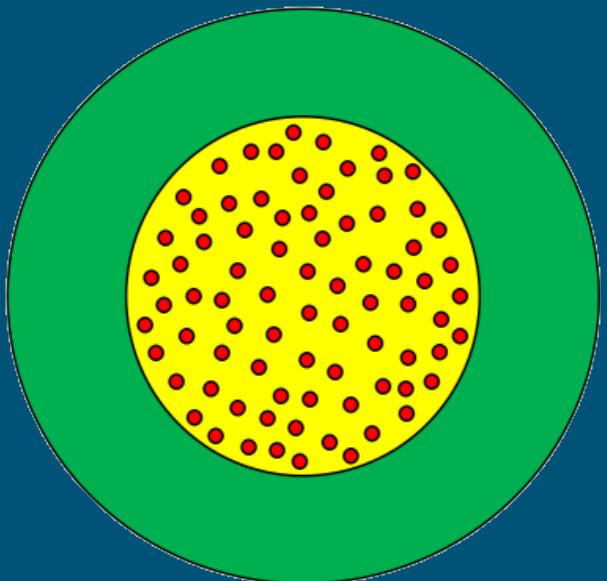
- COR\_RFU for RF material name/mnemonic
- COR\_KRF for material mass specification by COR cell
- COR\_RFG to define orientation (cylindrical inner/outer, plate upper/lower)



### General guidelines:

- Use RF only in cells that comprise reflectors (besides SS graphite in cells for core support)
- Use FU and MX only in active core cells
- Use SS for actual core support structures
- Use SS on an as-needed basis to hold up FU/MX and/or RF and avoid support logic issues
- Component collocation:
  - Always collocate FU and MX,
  - Never collocate FU/MX and RF,
  - Never collocate FU/MX with SS, and
  - Avoid collocating RF and SS in an attempt to alleviate support logic issues

## ...Core Conduction...





### Intracell conduction between collocated FU and MX

- Account for FU conduction resistance and non-negligible MX conduction resistance
- Modify the FU-to-MX conductance in terms of its serial/parallel resistance combinations

$$q_{FU-to-MX} = h_{FU,MX} A_{FU} (T_{FU} - T_{MX})$$

$$\frac{1}{h_{FU,MX}} = \frac{1}{h_{FU}} + \frac{1}{\frac{1}{\frac{1}{h_{gap}} + \frac{1}{h_{CF}}} + h_{rad}} + \frac{1}{h_{MX}} \quad , \quad \text{for } \frac{1}{h_{MX}} = \begin{cases} k_{MX}a/fR_{MX,i}, & \text{PMR} \\ k_{MX}a/fR_{MX,i}^2, & \text{PBR} \end{cases}$$

$$a = \begin{cases} \left( \ln \left( \frac{R_{MX,o}}{R_{MX,i}} \right) \right)^{-1}, & \text{PMR} \\ \left( \frac{1}{R_{MX,i}} - \frac{1}{R_{MX,o}} \right)^{-1}, & \text{PBR} \end{cases}$$

$$\frac{1}{h_{FU}} = \begin{cases} \frac{R_{FU}}{4k_{FU}}, & \text{PMR} \\ \frac{R_{FU}}{5k_{FU}}, & \text{PBR} \end{cases}$$

$$f = \begin{cases} \left( \frac{1}{2} \right) \left( \frac{2R_{MX,o}^2 \ln \left( \frac{R_{MX,o}}{R_{MX,i}} \right) - (R_{MX,o}^2 - R_{MX,i}^2)}{(R_{MX,o}^2 - R_{MX,i}^2) \ln \left( \frac{R_{MX,o}}{R_{MX,i}} \right)} \right), & \text{PMR} \\ \frac{1}{R_{mx,i}} - \left( \frac{3/2}{\frac{1}{R_{mx,i}} - \frac{1}{R_{mx,o}}} \right) \left( \frac{R_{mx,o}^2 - R_{mx,i}^2}{R_{mx,o}^3 - R_{mx,i}^3} \right), & \text{PBR} \end{cases}$$



Intercell conduction (allows: MX-MX, MX-RF, RF-SS, MX-SS ; disallows: FU-FU for PBR)

- General equation (axial or radial):

$$q_{i,j} = K_{eff} (T_i - T_j)$$

- Effective conductivity  $K_{eff}$ :

$$K_{eff} = \frac{1}{1/K_i + 1/K_j} \quad ; \quad K_i = \frac{k_i A_i}{\Delta x_i}$$

- For RF and SS

- Conductivity  $k_i$  comes from solid thermal conductivity data
  - Conduction areas and lengths are derived from notions of cell volumes, lengths, boundary areas, etc.

- For MX ONLY

- Conductivity  $k_i$  comes from effective conductivity models
  - Conduction areas and lengths are similarly defined
  - Cell MX component “height fraction” derived from volume ratio force to unity (no artificial degradation of radial heat transfer)

→ best practice COR SC1507 set  $> 0.0$  (real kind)



PBR effective conductivity model (pebble bed conduction) applied to MX component exclusively

- Zehner-Schlunder-Bauer with Breitbach-Barthels modification to the radiation term
- Accounts for conduction through pebbles and through fluid plus radiation

$$k_{\text{eff}} = (1 - \sqrt{1 - \varepsilon}) \varepsilon 4\sigma T^3 D_p + (1 - \sqrt{1 - \varepsilon}) k_f + \sqrt{1 - \varepsilon} k_c$$

$$\Lambda_s = \frac{k_s}{4\sigma T^3 D_p}$$

$$\varepsilon = 4\sigma \text{ 끝 } \text{ 끝 }$$

$$k_c = \frac{2}{N} \left\{ \frac{B \left( 1 + \frac{1}{\Lambda_s \left( \frac{2}{\varepsilon_r} - 1 \right)} - \lambda \right)}{N^2 \frac{1}{k_f}} \ln \left( \frac{\lambda_p + \lambda_r}{B} \right) + \frac{B+1}{2B} \left( \frac{\frac{4\sigma T^3 D_p}{2} - B k_f}{\frac{2}{\varepsilon_r} - 1} \right) - \frac{B-1}{N} k_f \right\}$$

$$B = C \left( \frac{1 - \varepsilon}{\varepsilon} \right)^m$$

$$C = 1.25$$

$$m = 10/9$$

$$\lambda = k_f/k_s$$

$$\lambda_p = k_s/k_f$$

$$\lambda_r = k_r/k_f$$

\* Same correlation with zeroed radiation components for FHR with FLiBe working fluid

$$N = 1 + \frac{1}{\left( \frac{2}{\varepsilon_r} - 1 \right) \Lambda_s} - \lambda B$$



PMR effective conductivity model (continuous solid with pores) applied to MX component exclusively

- Tanaka-Chisaka
- Accounts for solid conduction, pore conduction, and pore radiation
- A radiation term is incorporated into the pore (gas) conduction term
- After obtaining an effective PMR fuel element (hex block) conductivity, a parallel gap conductance term is added

$$k_{eff} = k_s \left[ A + (1-A) \frac{\ln(1 + 2B(k_{por}/k_s - 1))}{2B(1 - k_s/k_{por})} \right]$$

$$k_{rad} = 4\epsilon_r \sigma T^3 D$$

$$k_{por} = k_{s,por} + k_{rad}$$

$$k_{er} = \left( \frac{1}{h_{gap} D_{blk}} + \frac{1}{k_{eff}} \right)^{-1}$$

$k_{eff}$  = effective conductivity [W/m-K]

$A$  =  $2(1-\epsilon)/(2+\epsilon)$

$B$  =  $(1-\epsilon)/3$

$k_s$  = thermal conductivity of solid (continuous) material [W/m-K]

$k_{por}$  = thermal conductivity of pores (discontinuous) material [W/m-K]

$\epsilon$  = porosity

$h_{gap}$  = Gap heat transfer coefficient (W/m<sup>2</sup>-K)

$D_{blk}$  = Effective radial diameter of a block (m)

## COR Conduction – Boundary



Boundary conduction occurs between COR components in the outermost ring and radial boundary HS's

Governed by a contact resistance consisting of a gap component and a thermal diffusion component

$$q_{C-HS} = \frac{T_C - T_{HS}}{R}$$

$$R = R_{gap} + R_{dif}$$

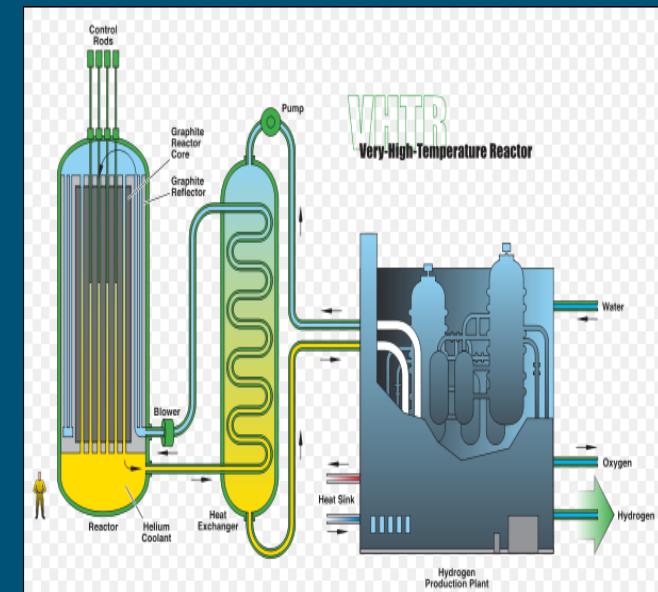
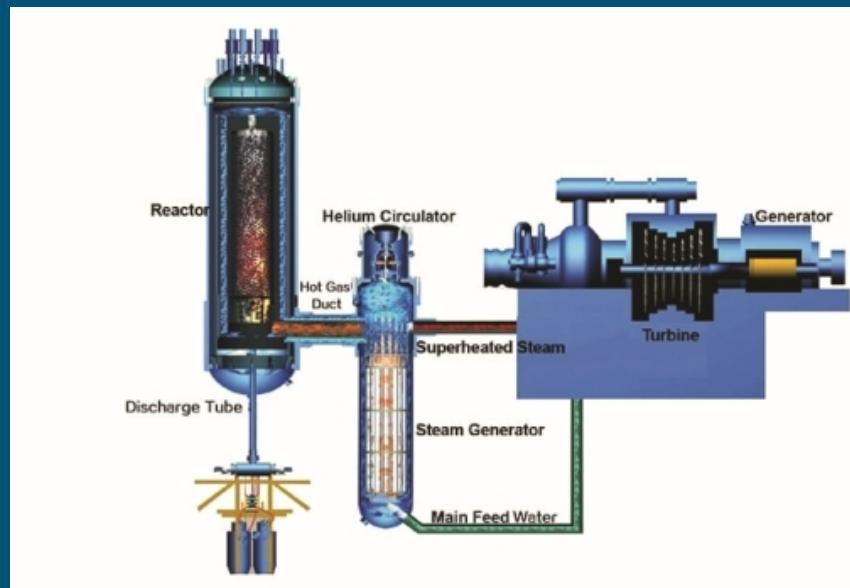
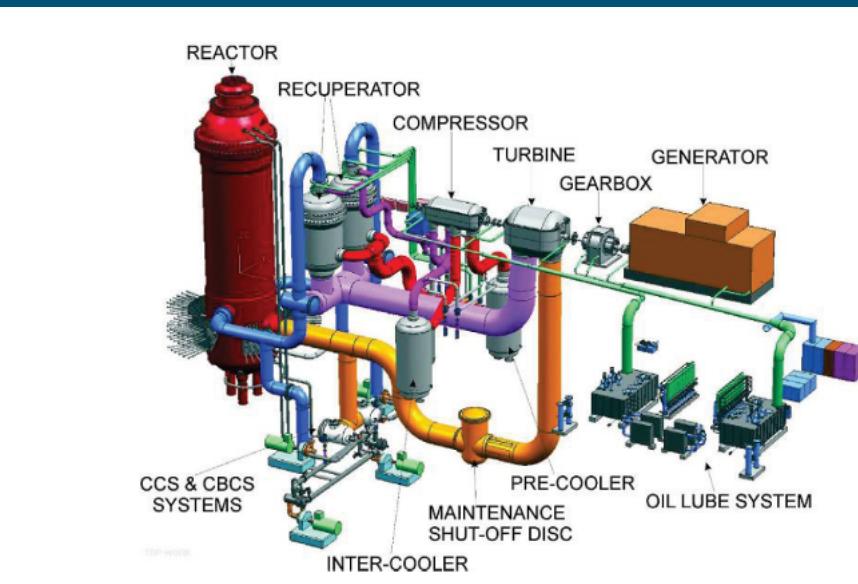
$$R_{gap} = \Delta r_{gap} / k_{gap}$$

$$R_{dif} = \sqrt{\frac{\pi \Delta t}{(k \rho c_p)_{HS}}}$$

Thermal diffusion resistance mitigates oscillations due to explicit COR/HS coupling

As a best practice, use boundary conduction (COR\_BCP) to allow energy transfer from the core periphery

## ...Core Convection, Point Kinetics, and Oxidation...





Heat transfer coefficient (Nusselt number) correlations for PBR

MX has a conduction component to its heat transfer resistance (parallel with convection term)

$$Nu = 2.0 + 0.6 \ Re_f^{1/2} \ Pr_f^{1/3}$$

$$Nu = 2.0 + 0.6 \ Gr_f^{1/4} \ Pr_f^{1/3}$$

Isolated spherical particles  
Film temperature to evaluate nondimensional numbers  
Max of forced/free used

$$\frac{1}{h_{MX}} = \begin{cases} \frac{1-f}{k_{MX} \left( a/R_{MX,o} \right)} & , PMR \\ \frac{1-f}{k_{MX} \left( a/R_{MX,o}^2 \right)} & , PBR \end{cases}$$

$$f = \begin{cases} \left( \frac{1}{2} \right) \left( \frac{2R_{MX,o}^2 \ln \left( \frac{R_{MX,o}}{R_{MX,i}} \right) - (R_{MX,o}^2 - R_{MX,i}^2)}{(R_{MX,o}^2 - R_{MX,i}^2) \ln \left( \frac{R_{MX,o}}{R_{MX,i}} \right)} \right) & , PMR \\ \frac{1/R_{mx,i}}{1/R_{mx,i} - 1/R_{mx,o}} - \left( \frac{3/2}{1/R_{mx,i} - 1/R_{mx,o}} \right) \left( \frac{R_{mx,o}^2 - R_{mx,i}^2}{R_{mx,o}^3 - R_{mx,i}^3} \right) & , PBR \end{cases}$$

$$a = \begin{cases} \left( \ln \left( \frac{R_{MX,o}}{R_{MX,i}} \right) \right)^{-1} & , PMR \\ \left( \frac{1}{R_{MX,i}} - \frac{1}{R_{MX,o}} \right)^{-1} & , PBR \end{cases}$$



Flow resistance due to packed bed flow as computed from one of several correlations (CVH SC4413)

- Ergun
- Modified Ergun (rough/smooth)
- Achenbach

Correlation	C <sub>1</sub>	C <sub>2</sub>	C <sub>3</sub>	C <sub>4</sub>
Ergun (original)	3.5	300.	0.0	-
Modified Ergun (smooth)	3.6	360.	0.0	-
Modified Ergun (rough)	8.0	360.	0.0	-
Achenbach	1.75	320.	20.0	0.4

K-loss formulation used in phasic velocity equations (CVH/FL)

$$K^* = K_{empty} + \left[ C_1 + C_2 \frac{1-\varepsilon}{Re} + C_3 \left( \frac{1-\varepsilon}{Re} \right)^{C_4} \right] \frac{(1-\varepsilon)L}{\varepsilon D_p} \quad Re = \frac{\rho \varepsilon v_j D_p}{\mu}$$

COR\_ZP or COR\_CPOR for porosities entering into packed bed K-loss calculations



Standard PRKE's with kinetics data accessible by sensitivity coefficient

Feedback models (Doppler, fuel/moderator density, external CF) and COR\_TAVG for average temperatures

$$\frac{dP}{dt} = \left( \frac{\rho - \beta}{\Lambda} \right) P + \sum_{i=1}^6 \lambda_i Y_i + S_0$$

$P$ = Thermal power due to fission

$$\frac{dY_i}{dt} = \left( \frac{\beta_i}{\Lambda} \right) P - \lambda_i C_i, \quad \text{for } i = 1 \dots 6$$

$Y_i$ = Thermal power due to delayed neutron precursor group  $i$

$S_0$ = Thermal power generation rate due to neutron source

$\rho = \frac{k-1}{k}$ = Reactivity for  $k$  the effective multiplication factor

$\beta$ = Delayed neutron fraction

$\Lambda = 1/\nu V \Sigma_f$ = Neutron generation time

$\lambda_i$ = Decay constant of delayed neutron precursor group  $i$



## Steam oxidation

$$R_{OX,steam} = \frac{k_4 P_{H_2O}}{1 + k_5 P_{H_2}^{0.5} + k_6 P_{H_2O}}$$

Reaction	$\Delta H$ (kcal/mol)
$C + H_2O(g) \rightarrow CO(g) + H_2(g)$	+31.14
$CO(g) + H_2O(g) \rightarrow CO_2(g) + H_2(g)$	-9.65

where

$R_{OX,steam}$  = Reaction rate for steam oxidation [1/s]

$P_{H_2O}$  = Partial pressure of  $H_2O$  [Pa]

$P_{H_2}$  = Partial pressure of  $H_2$  [Pa]

$k_i$  = ith reaction coefficient =  $K_i \exp\left(-\frac{E_i}{RT}\right)$

$K_i$  = ith precoefficient

$E_i$  = ith activation energy [J/kmol]

$R$  = Gas constant = 8314 [J/kmol-K]

$T$  = Temperature [K]

	$K_i$	$E_i/R$
$k_4$	$2.646 \times 10^{-4}$ [1/s-Pa]	16455 K
$k_5$	$1.075 \times 10^{-12}$ [1/Pa <sup>1/2</sup> ]	30596 K
$k_6$	$4.887 \times 10^{-21}$ [1/Pa]	20129 K

Includes rate limit due to steam diffusion towards active oxidation surface



## Air oxidation

$$R_{OX} = 1.7804 \times 10^4 \exp\left(-\frac{20129}{T}\right) \left(\frac{P}{0.21228 \times 10^5}\right)^{0.5}$$

where

$R_{OX}$  = Reaction rate [1/s],  
 $T$  = Temperature [K],  
 $P$  = Oxygen partial pressure [Pa].

Reaction	$\Delta H$ (kcal/mol)
1. $C + O_2 \rightarrow CO_2(g)$	-94.03
2. $C + \frac{1}{2}O_2 \rightarrow CO(g)$	-26.62
3. $CO(g) + \frac{1}{2}O_2(g) \rightarrow CO_2(g)$	-67.41
4. $C + CO_2(g) \rightarrow 2CO(g)$	+40.79

Includes rate limit as with steam oxidation

$$f_{CO/CO_2} = 7396 e^{-69604/RT}$$

where

$f_{CO/CO_2}$  = CO/CO<sub>2</sub> mole ratio  
 $R$  = Gas constant = 8.314 [J/mol-K]  
 $T$  = Temperature [K]

Two SC enhancements (catalysis, pore diffusion)  
 → COR SC1014 and SC1015

Empirical CO-to-CO<sub>2</sub> ratio



For PBR, PMR, and FHR, the COR/CVH connections are configured as usual

PBR and PMR working fluid is helium

- Configure initial thermodynamic conditions in CVH
- NCG helium in an “atmosphere-only” scenario
- Require no working fluid EOS library files to access (NCG package facilitates)

FHR working fluid is FLiBe

- Configure initial thermodynamic conditions in CVH
- FLiBe in a “pool-only” scenario
- Require a working fluid EOS library file and a global input record (cover this in subsequent MSR presentations)



Note that the COR thermal hydraulics models used for PBR and/or PMR – the traditional HTGR reactor types – are equally applicable to other reactor types that use a different working fluid but the same fuel elements (e.g. FHR)

Recent useful references on related subject matter:

- SNL's USNRC source term demo calculation for HTGR (PBR) and FHR
- 2021 EMUG presentation on HTGR best practices
- 2022 EMUG and AMUG
- 2022 NURETH-19 materials



COR PBR/PMR thermal hydraulics theory/physics was reviewed in some detail and these concepts are generally applicable to the pebble fueled FHR reactor design

Elements of best practice were discussed

Key takeaways:

- Understand how to configure FU (FUXM), MX, RF, and SS plus how to connect primary materials (including UDMs)
- Understand the specialized MX component
- Understand some basic points about nodalizing a PBR, PMR, or FHR core in view of thermal hydraulics modeling