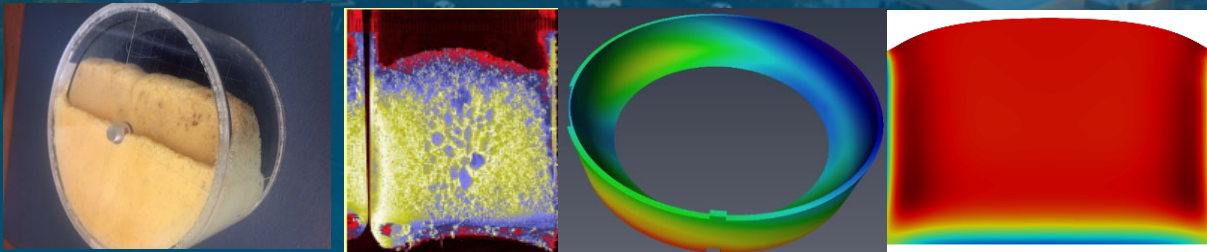
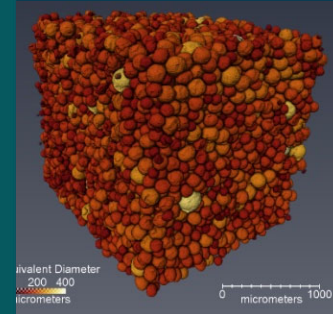
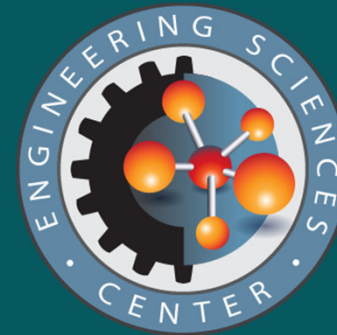


# Multiphysics Modeling of Chemically Blown Polyurethane Foams During Manufacturing



SAND2022-????

PRESENTED BY

Rekha Rao, Sandia National Laboratories  
Albuquerque, NM

For: Christine Roberts, Melissa Soehnel, Judy Brown, Kevin Long, David Noble (SNL), James Tinsley (KCNSC)



Sandia National Laboratories is a multimission laboratory managed and operated by National Technology & Engineering Solutions of Sandia, LLC, a wholly owned subsidiary of Honeywell International Inc., for the U.S. Department of Energy's National Nuclear Security Administration under contract DE-NA0003525.

# Cradle-to-Grave Model of PMDI Foam



**Overarching Goal:** A computational model for foaming, vitrification, cure, aging to help us design molds and determine how inhomogeneities effect the structural response of the final part, including long term shape stability



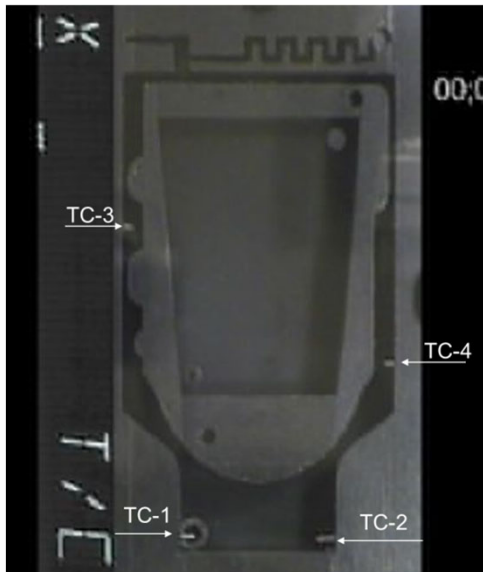
Injection,  
foaming and  
initial curing  
at lower T



Run 030110-PMDI-4 60°C  
Free Rise  
Sandia National Labs



Oven time  
at higher T  
to make  
sure it is  
fully cured



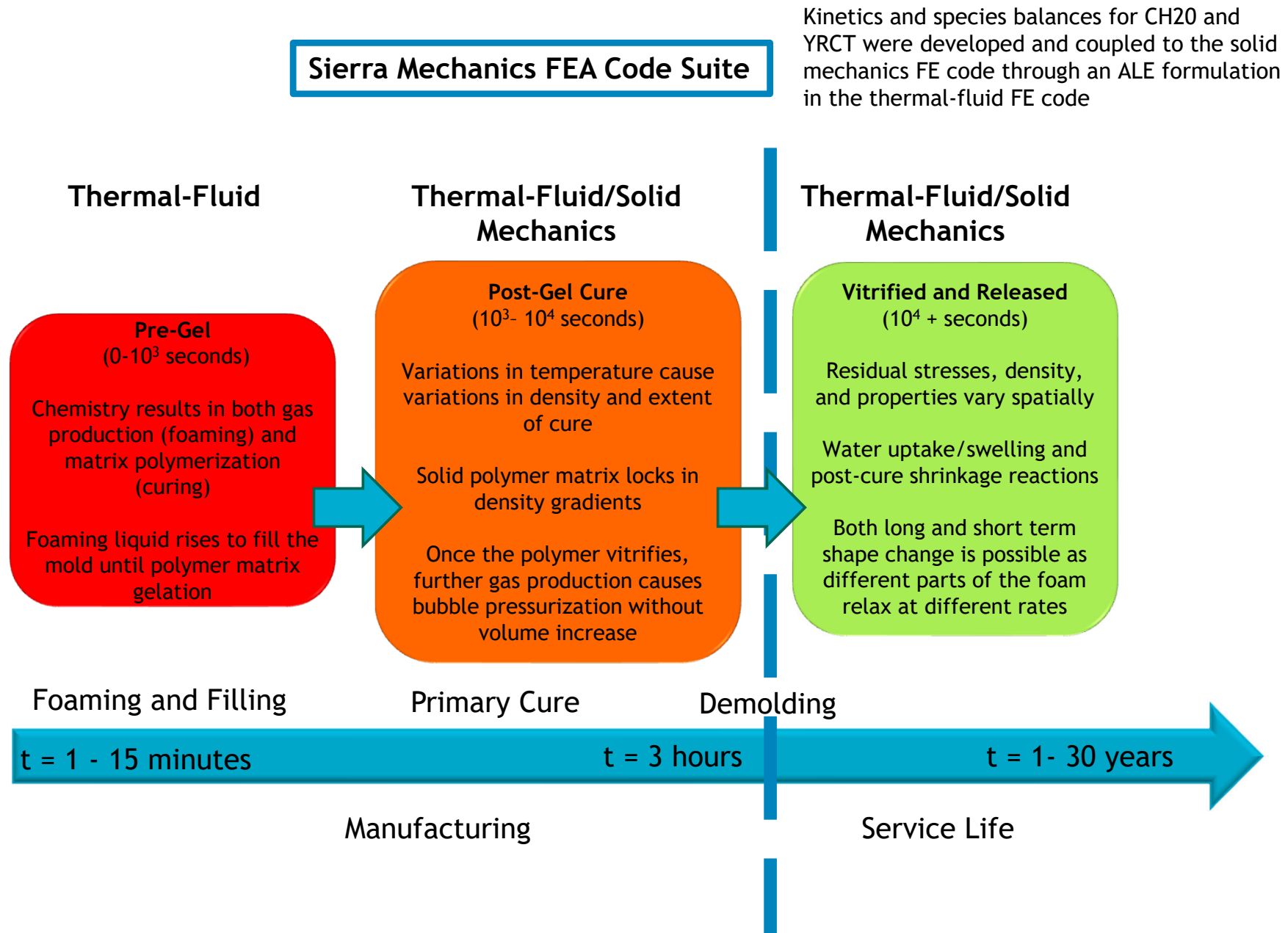
Remove  
from mold –  
predict cure  
and thermal  
stresses



Predict  
shape and  
size over  
years



# Cradle-to-Grave Modeling of Foam Parts



# Why Are Polyurethane Structural Foams Difficult?



Polyurethane (PMDI) is used as an encapsulant for electronic components, to mitigate against shock and vibration, and for light-weight structural parts.

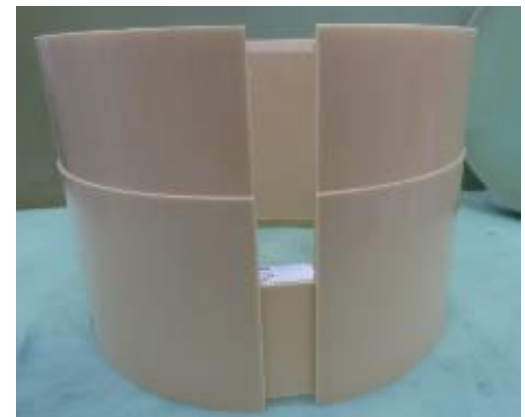
High-fidelity cradle-to-grave foam models for structural polyurethane for part design.

- Filling profile for vent and gate locations
- Density and density gradient predictions for initializing structural mold, including pressurization and compressibility effects
- Polymerization chemistry for gelation and vitrification
- Manufacturing stresses
- Dimensional stability during manufacturing and aging

**Customer asked us to “use” the model to support mold design – while the model was still under development.**



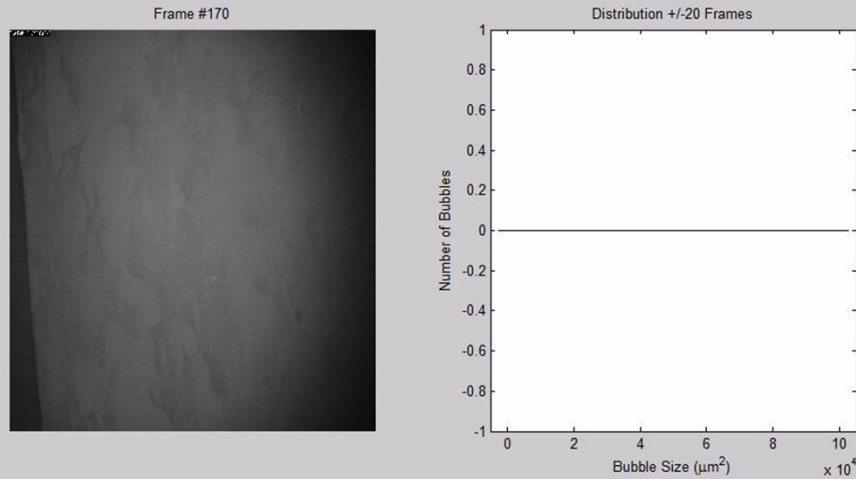
PMDI has a short pot-life: models can help reduce defects and improve filling process



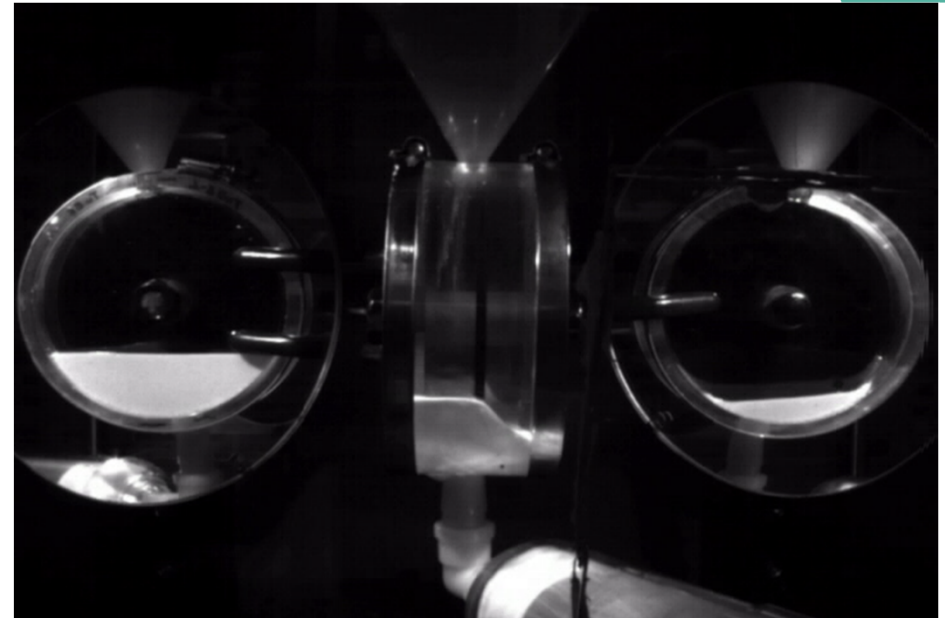
Support A-4 PMDI Structural Part



# Foam Filling is Complex



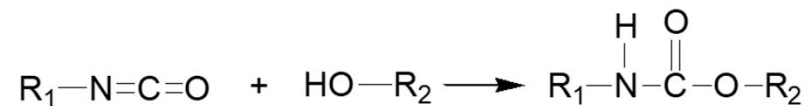
Foam front moving past camera, with bubble sizes at transparent wall determined with image processing.



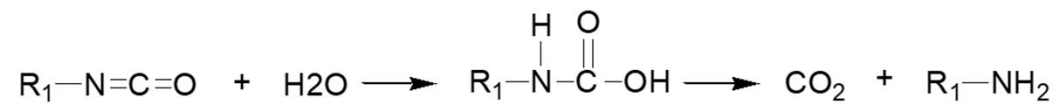
3 views of foam filling with several plates spaced unevenly. Vent location is critical to keep from trapping air.

- Gas generation drives the foam expansion, changing the material from a viscous liquid to a multiphase material.
- Continuous phase is time- and temperature-dependent and eventually vitrifies to a solid.

**Two key reactions:** Isocyanate reaction with polyols and water



Urethane formation,  
crosslinking



Foaming reaction yields  
CO<sub>2</sub> and amine

# Equations of Motion Include Evolving Material Models



Momentum equation and continuity have variable density, shear viscosity, and bulk viscosity

$$\rho \frac{\partial \mathbf{v}}{\partial t} = -\rho \mathbf{v} \cdot \nabla \mathbf{v} - \nabla p + \nabla \cdot (\mu_f (\nabla \mathbf{v} + \nabla \mathbf{v}^t)) - \nabla \cdot \lambda (\nabla \cdot \mathbf{v}) \mathbf{I} + \rho \mathbf{g}$$

$$\frac{D\rho_f}{Dt} + \rho_f \nabla \cdot \mathbf{v} = 0$$

Energy equation has variable heat capacity and thermal conductivity including a source term for heat of reaction for foaming and curing reactions

$$\rho C_{pf} \frac{\partial T}{\partial t} + \rho C_{pf} \mathbf{v} \cdot \nabla T = \nabla \cdot (k \nabla T) + \rho \phi_e \Delta H_{rxn} \frac{\partial \xi}{\partial t}$$

Extent of reaction equation for polymerization: condensation chemistry

$$\frac{\partial \xi}{\partial t} = \left( \frac{1}{(1+wa)^\beta} \right) \left( k_0 \exp\left(-\frac{E}{RT}\right) \right) (b + \xi^m)(1-\xi)^n$$

Molar concentration equations for water and carbon dioxide

$$\frac{dC_{H_2O}}{dt} = -k_{H_2O} C_{H_2O}^n$$

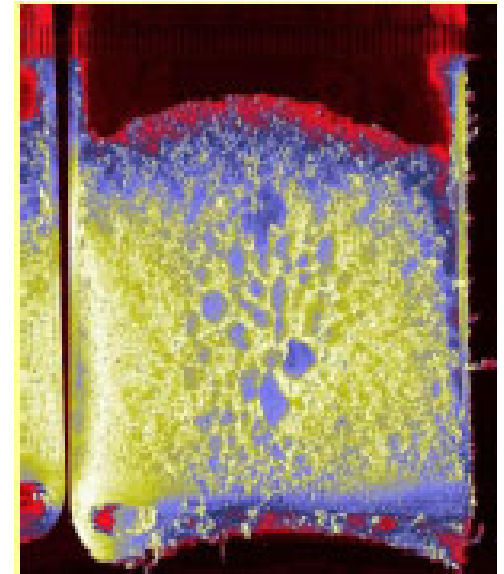
$$C_{H_2O} = \frac{\rho_{foam} x_{H_2O}}{M_{H_2O}}$$

$$\frac{dC_{CO_2}}{dt} = +k_{H_2O} C_{H_2O}^n$$

$$C_{CO_2} = \frac{\rho_{foam} x_{CO_2}}{M_{CO_2}}$$

$$k_{H_2O} = A_{H_2O} \exp(-E_{H_2O} / RT)$$

Rao et al., "Polyurethane kinetics for foaming and polymerization", *AIChE Journal*, 2017



NMR imaging shows coarse microstructure (Altobelli, 2006)

# Complex Material Models Vary with Cure, Temperature, and Gas Fraction



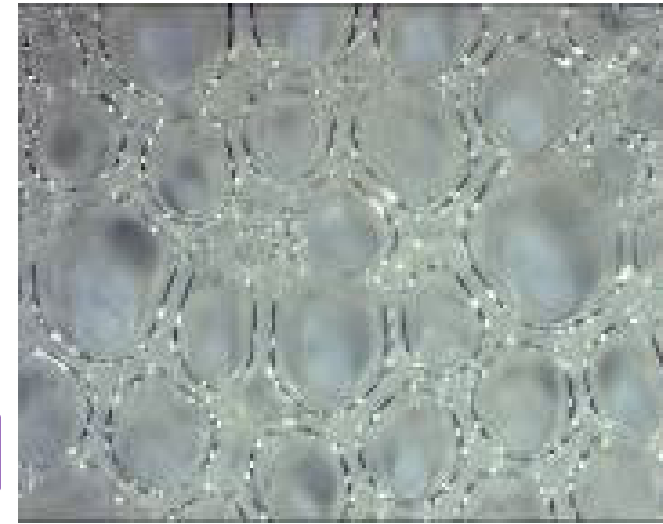
Foaming reaction predicts moles of gas from which we can calculate density

$$\rho_{gas} = \frac{PM_{CO_2}}{RT}$$

$$v = \frac{V_{gas}}{V_{liq}} = \frac{M_{CO_2} C_{CO_2}}{\rho_{gas}} \quad \phi_v = \frac{v}{1+v}$$

$$\rho_{foam} = \rho_{gas} \phi_v + \rho_{liq} (1 - \phi_v)$$

Compressibility built into this model via the ideal gas law for gas density



Foam is a collection of bubbles in curing polymer

Thermal properties depend on gas volume fraction and polymer properties

$$k = \frac{2}{3} \left( \frac{\rho}{\rho_e} \right) k_e + \left( 1 - \frac{\rho}{\rho_e} \right) k_v$$

$$C_{pf} = C_{pl} \phi_l + C_{pv} \phi_v + C_{pe} \phi_e$$

Shear and bulk viscosity depends on gas volume fraction, temperature and degree of cure

- Experiments to determine foaming and curing kinetics as well as parameters for model

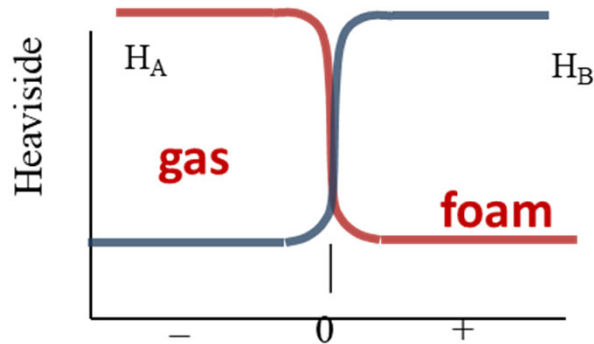
$$\mu = \mu_0 \exp\left(\frac{\phi_v}{1-\phi_v}\right) \quad \mu_0 = \mu_0^0 \exp\left(\frac{E_\mu}{RT}\right) \left(\frac{\xi_c^p - \xi^p}{\xi_c^p}\right)^{-q}$$

$$\lambda = \frac{4}{3} \mu_0 \frac{(\phi_v - 1)}{\phi_v}$$

M. Mooney, *J. Colloid Sci.*, **6**, 162-170 (1951).

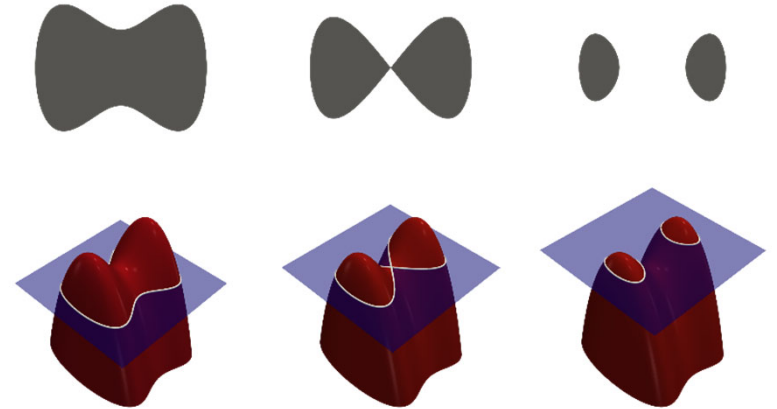
Gibson, L. J.; M. F. Ashby. Cambridge University Press, Cambridge, UK, 1990

# Coupled Finite Element Method/Level Set to Solve Foam Dynamics



$$\frac{\partial \phi}{\partial t} + v \cdot \nabla \phi = 0$$

$$H(\phi) = \frac{1}{2} \left( 1 + \frac{\phi}{\alpha} + \frac{\sin(\frac{\pi \phi}{\alpha})}{\pi} \right), \quad -\alpha < \phi < \alpha$$



Nicoguardo [CC BY 4.0  
(<https://creativecommons.org/licenses/by/4.0/>), from Wikimedia Commons]

- Level set advects with the fluid velocity
- Renormalize periodically to maintain the distance function using a mass conserving Huygens algorithm
- Properties vary with the level set based on the level set and modulated using the Heaviside

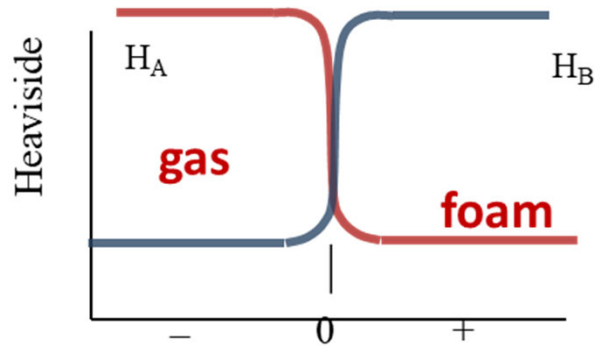
$$\eta(\phi) = (\eta_{gas} - \eta_{foam})H(\phi) + \eta_{foam}$$

$$\kappa(\phi) = (\kappa_{gas} - \kappa_{foam})H(\phi) + \kappa_{foam}$$

$$\rho(\phi) = (\rho_{gas} - \rho_{foam})H(\phi) + \rho_{foam}$$



# Coupled Finite Element Method/Level Set to Solve Foam Dynamics



$$\frac{\partial \phi}{\partial t} + \mathbf{v} \cdot \nabla \phi = 0$$

- Momentum and Continuity shown for an example. Energy is similar

$$\rho(\phi) \left( \frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v} \right) = -\nabla P + \nabla \cdot (\eta(\phi) (\nabla \mathbf{v} + \nabla \mathbf{v}^t)) - \left( \frac{2}{3} \eta(\phi) - \kappa(\phi) \right) (\nabla \cdot \mathbf{v}) \underline{\underline{\mathbf{I}}} + \rho(\phi) \mathbf{g}$$

$$\frac{\partial \rho(\phi)}{\partial t} + \nabla \cdot \rho(\phi) \mathbf{v} = 0$$

- Reactions equations use equation averaging and a Heaviside directly on the equations

$$\frac{dC_{H_2O}}{dt} = -(k_{H_2O} C_{H_2O}^n) H_B$$

$$\frac{dC_{CO_2}}{dt} = +(k_{H_2O} C_{H_2O}^n) H_B$$

- Equations discretized with bilinear FEM, pressure stabilized and upwinded
- Equations solved in a segregated manner with momentum and pressure in one block, level set in another, and energy and reactions in the third
- Each block solved with Krylov-based iterative solvers

# Simulations & Experiments

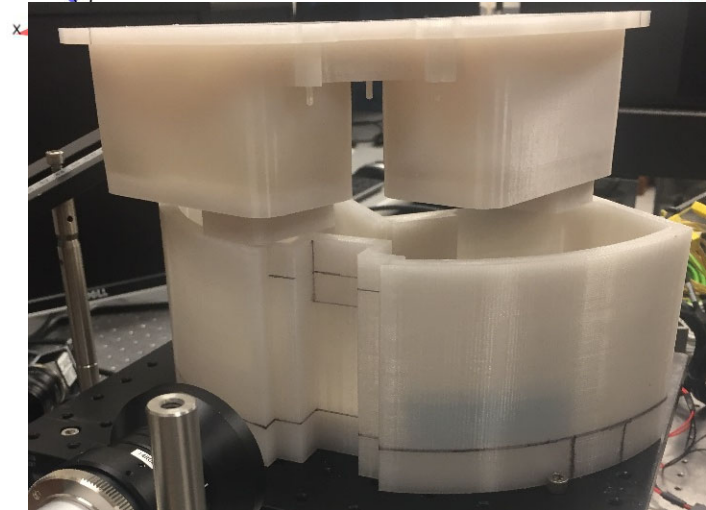
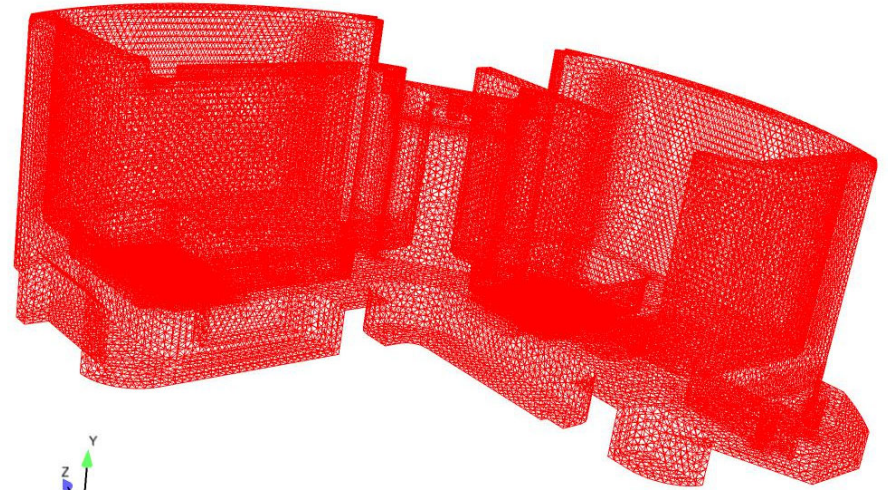


## Simulations

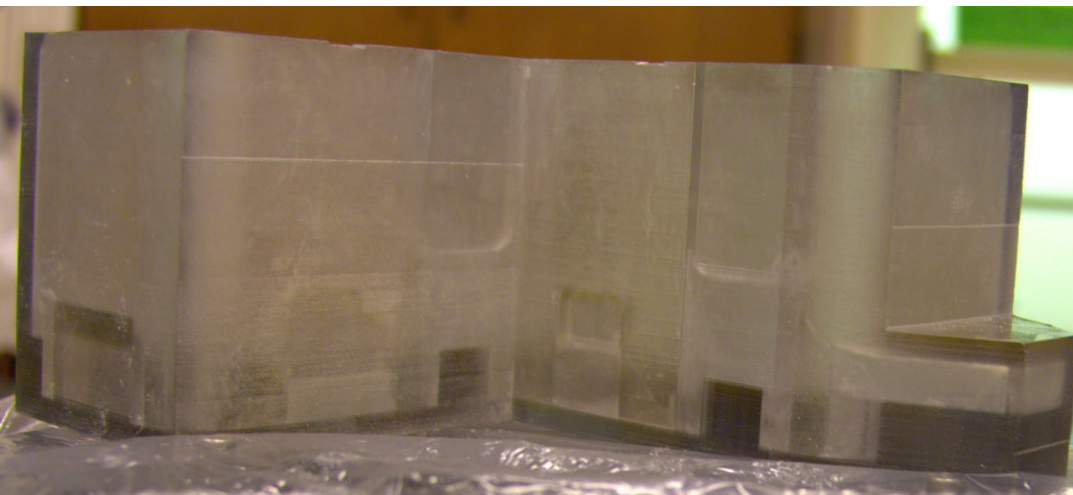
- Flat configuration
- 5° tilt
- 20° tilt
- 20° tilt toward the shelf feature
- Study of vent locations

## Experiments

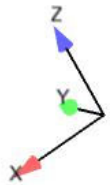
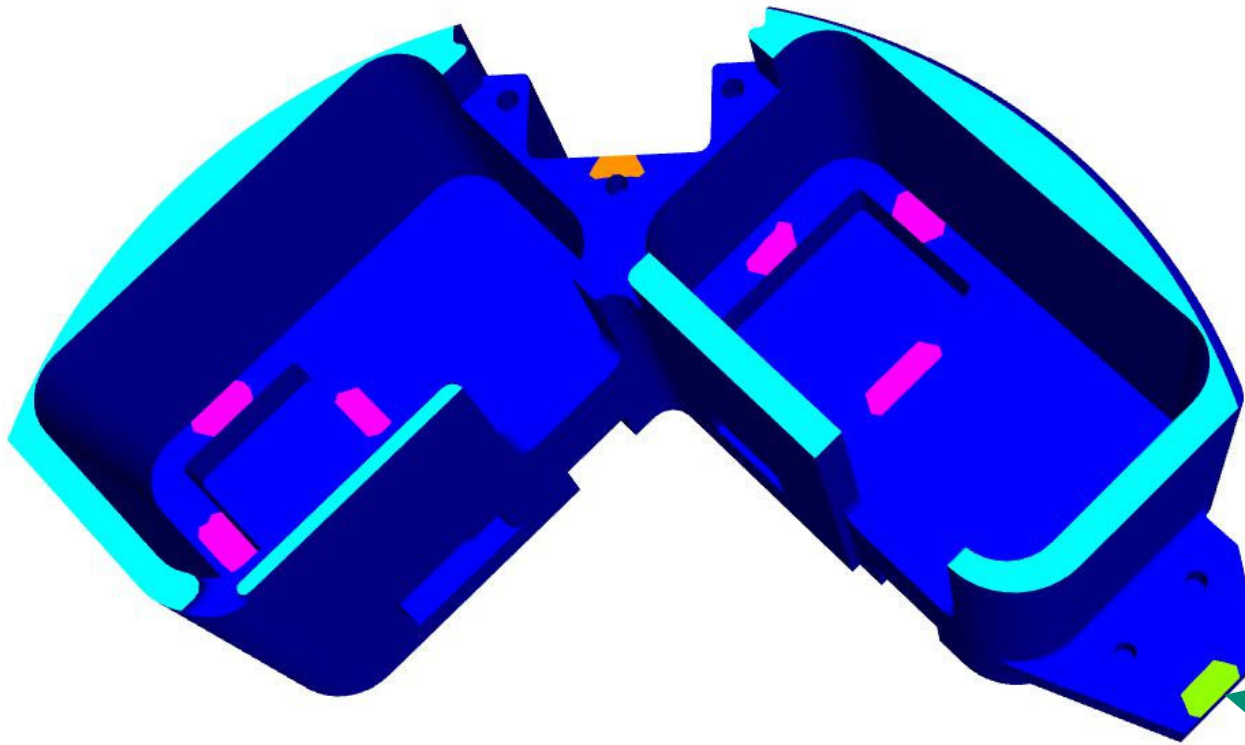
- Flow visualization experiments
- Additive manufacture mold



Goal: Use foaming and filling modeling and flow visualization experiments to develop confidence in foam model



# These Vent Locations Seem Representative of a Foaming Process



Simulation tests the idea of adding a vent on the shelf feature



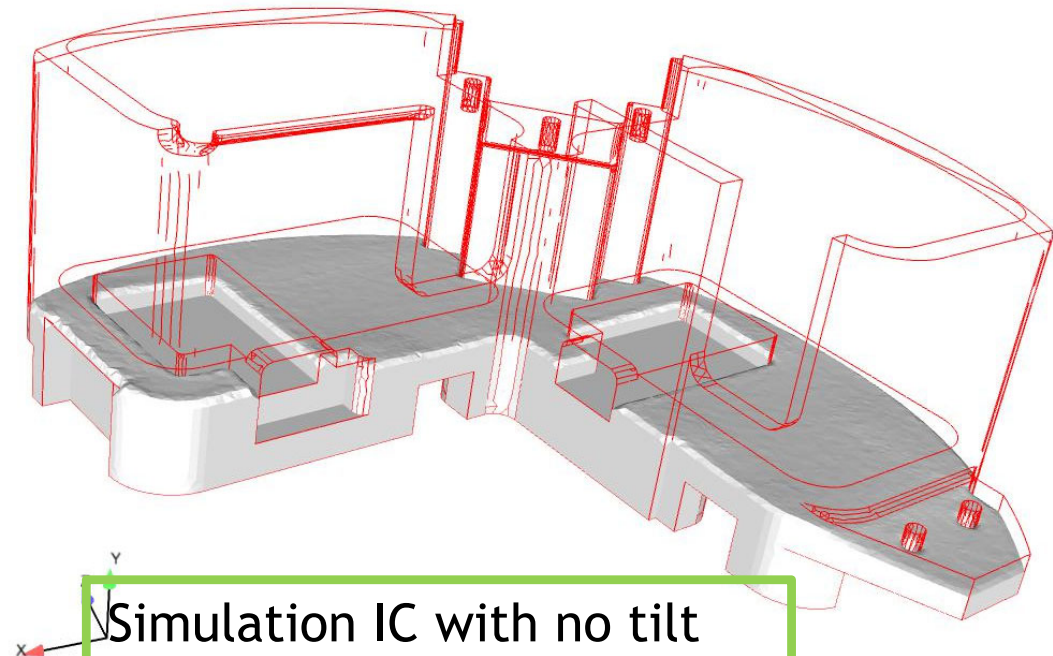
# Initial Conditions for Model: Experiments Show Shelf Starts Well-Filled



Flow visualization study using opaque mold to determine filling of shelf supports use of flat initial condition

*Flow visualization verifies initial condition:*

- *Foam levels well and flows to fill she area*
- *Simulation initial condition of a flat interface seems fairly accurate*



Simulation IC with no tilt

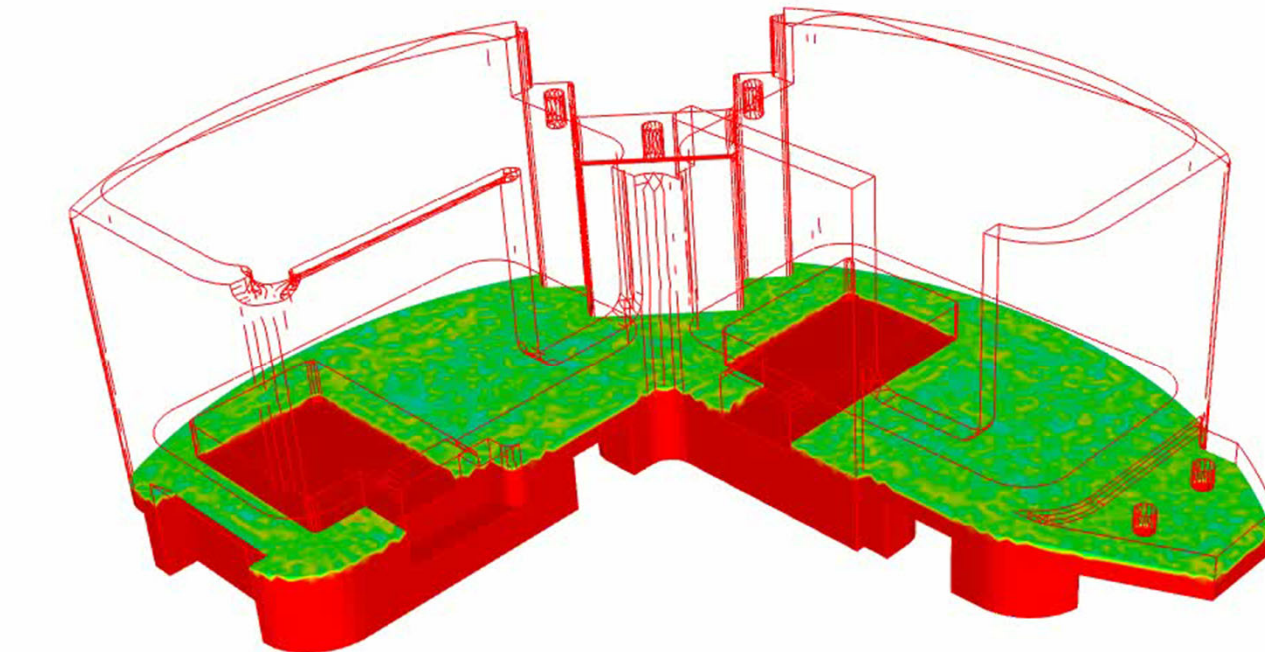
- Shelf is half-filled at start of the simulation



# Foam Filling and Curing for Flat Configuration



Time = 5.00



Base Case:

- Look at issues for filling the mold when it is flat on the table
- Model shows density evolution and filling profile over time

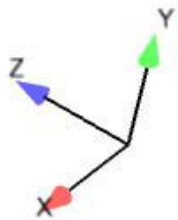
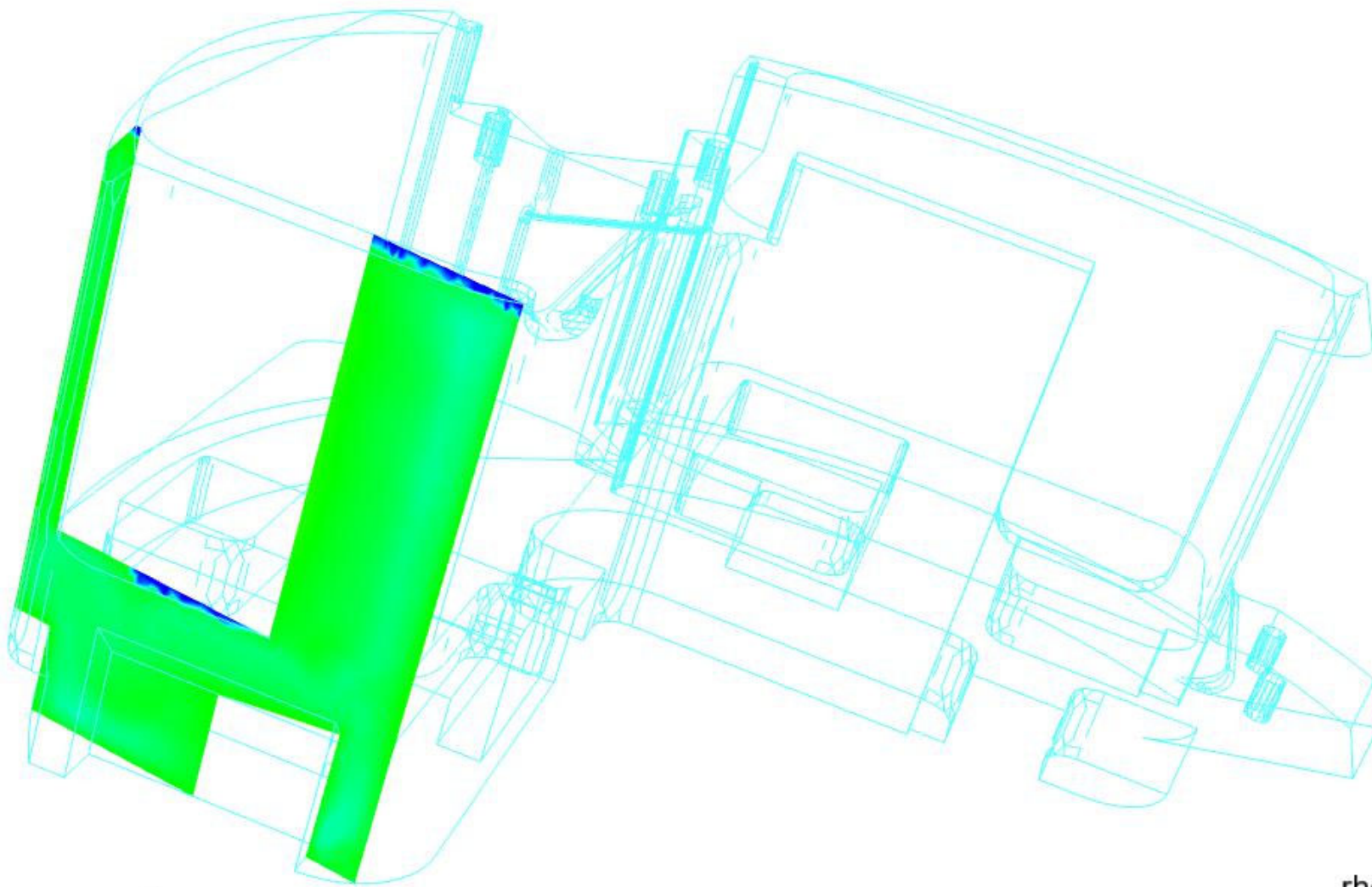
rho

1.000e+00  
7.625e-01  
5.250e-01  
2.875e-01  
5.000e-02





time=82.7s  
voids = 3.6%



rho

4.300e-01  
3.850e-01  
3.400e-01  
2.950e-01  
2.500e-01



Density Variations at Different Locations: Flat  
Mold with Shelf Vent

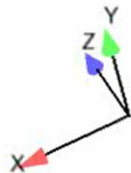
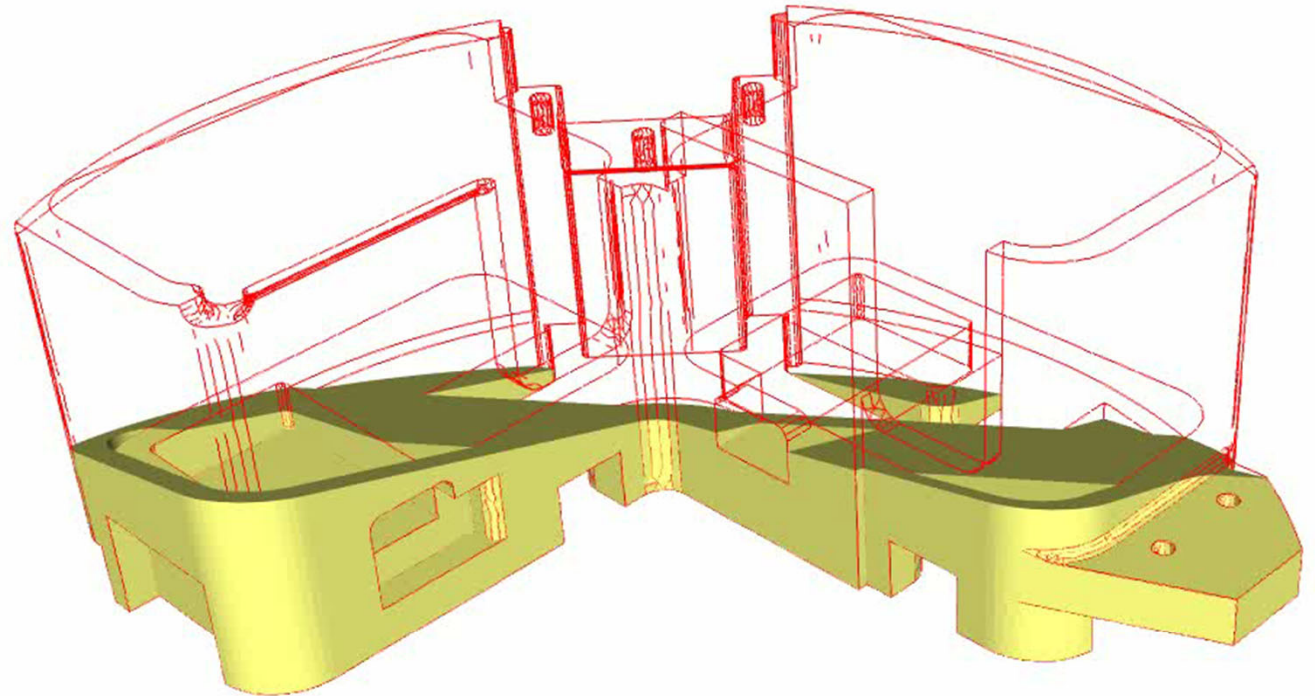
# Dynamics of Filling with 20° Tilt Angle



Time = 5.000000

Foam Using a 20° Tilt Angle forward similar to legacy process

- Initial condition has a tilt forward for foam position and a flat interface
- Gravity vector is also tilted

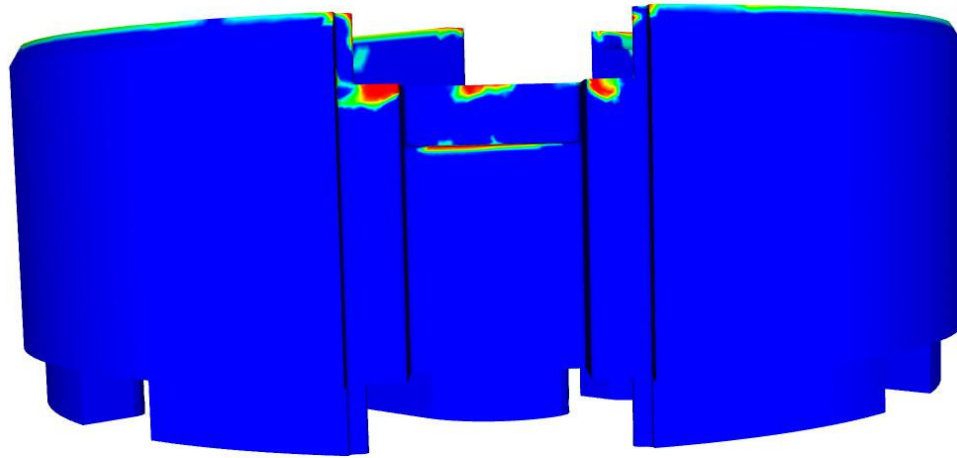


# Density Variations: Back View



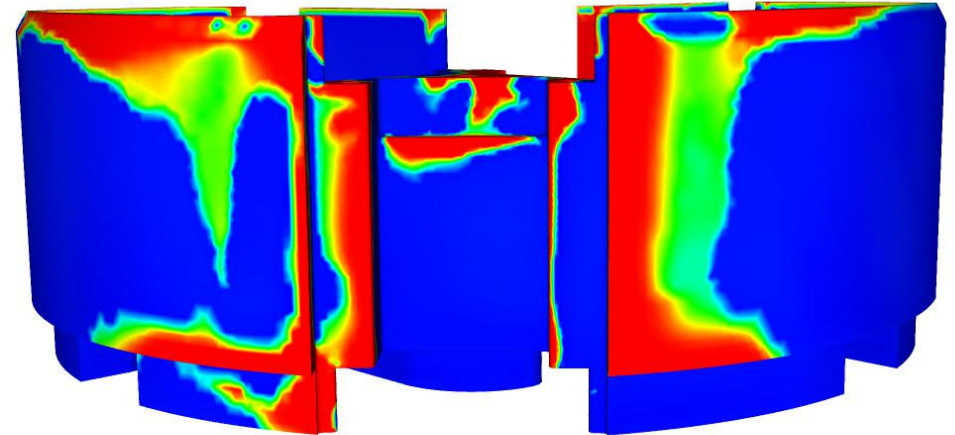
Time = 82.737

FLAT FILL



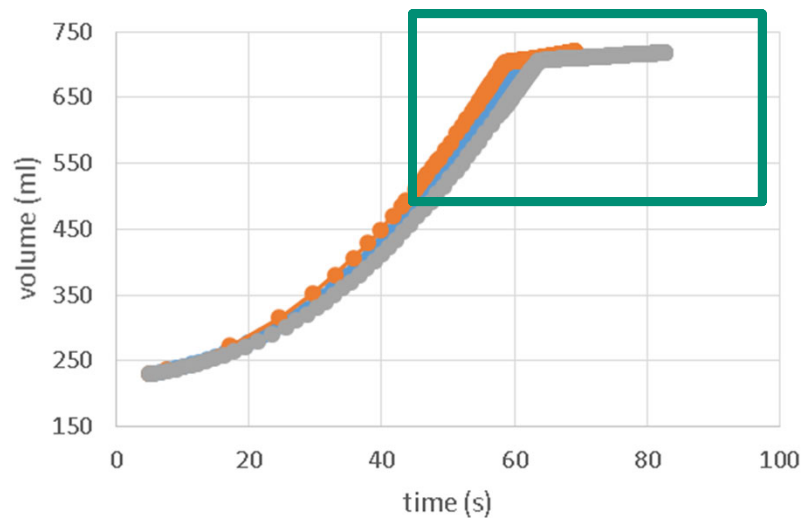
Time = 71.091

TILT 20 DEGREES FILL



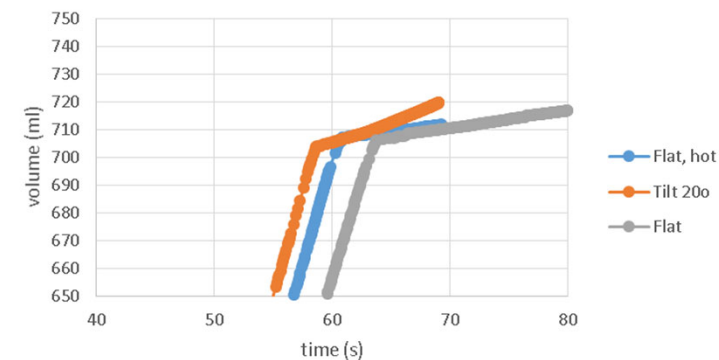
- Forward tilt moves defects to the back part of the mold
- Tilt fills faster than flat

Volume versus time



density\_var  
1.034e-01  
7.758e-02  
5.172e-02

Volume versus time



density\_var  
1.034e-01  
7.758e-02  
5.172e-02  
2.586e-02  
1.154e-11



# Computational Models of Foam



FLAT FILL

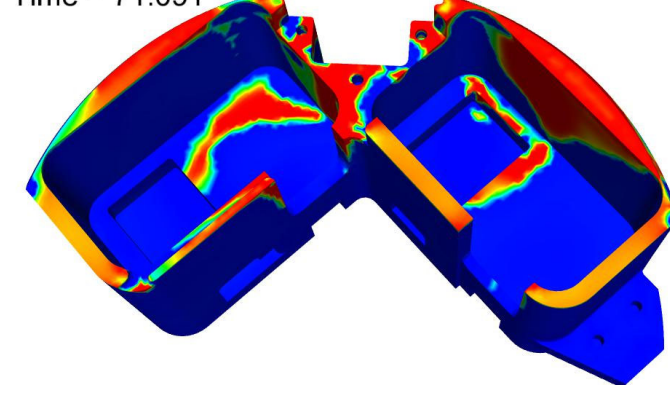
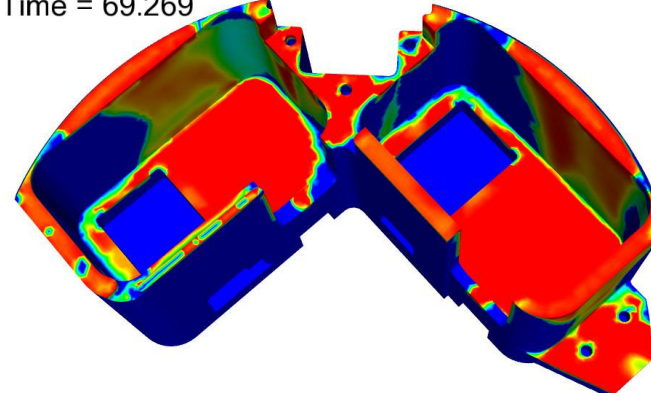
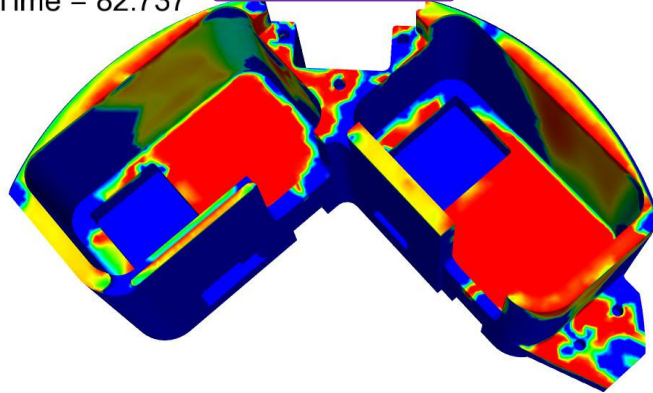
FLAT HOT

20° Tilt

Time = 82.737

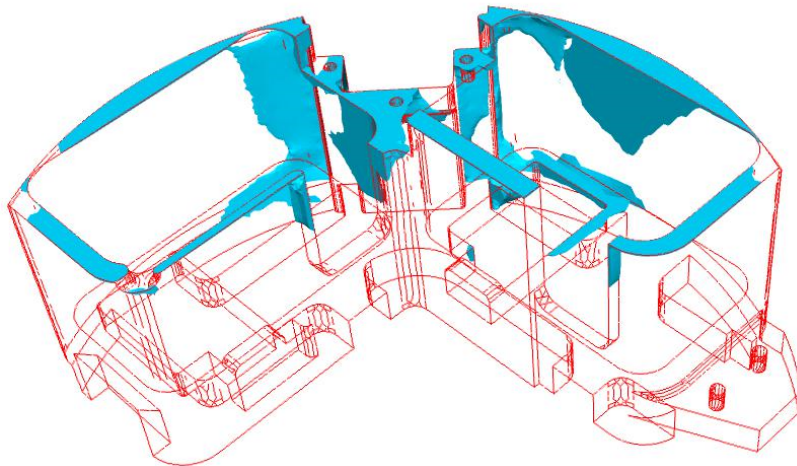
Time = 69.269

Time = 71.091



Density variations for three cases of interest

Time = 75.2433



Foam filling for 20° tilt: the angled fill reduces voids on the new shelf

Case	Flat	Flat Hot	20° Tilt
Max. Time (s)	83s	70s	71s
Voids	3.6%	4.4%	2.9%
Density variation	2.8	2.9	3.6

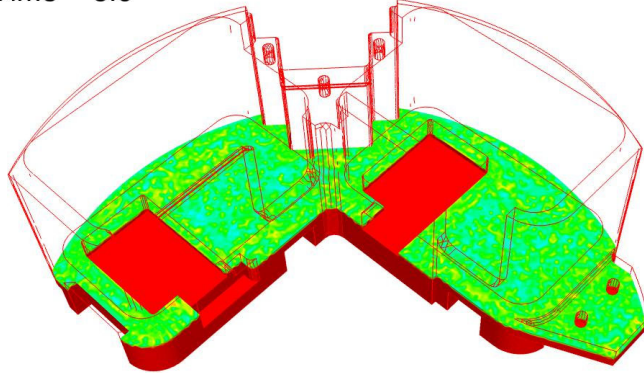
All cases fill well!

- Model over-predicts voids, but predictions are small
- Density variation greater with tilt

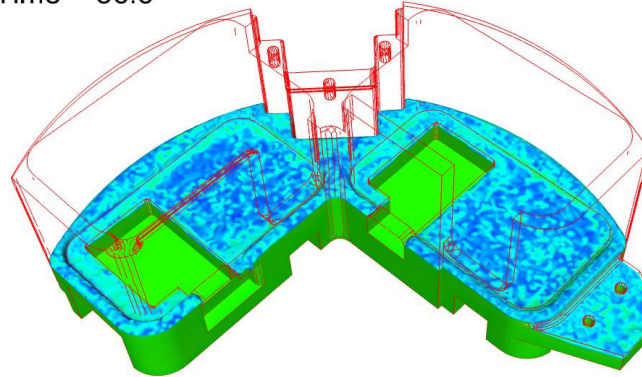
# Computational Models of Foam



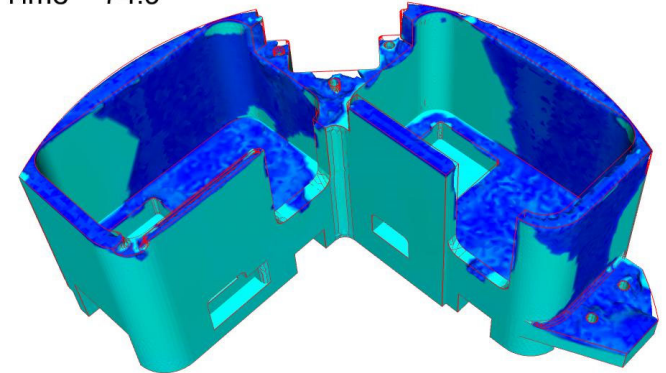
Time = 5.0



Time = 36.6



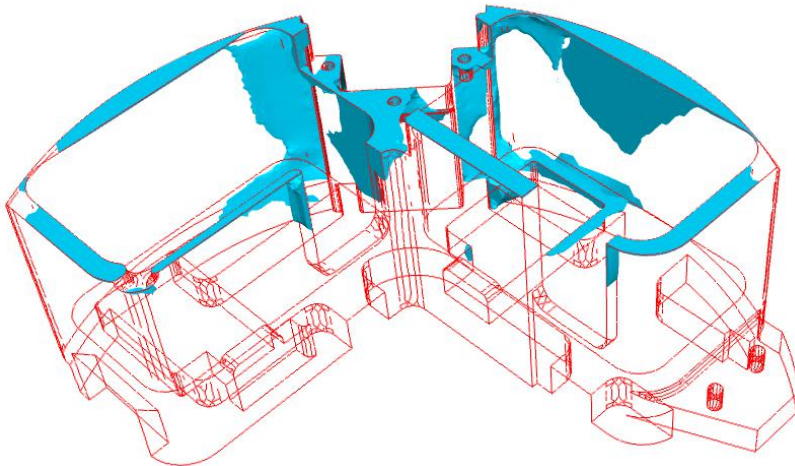
Time = 74.9



Evolution of density for flat mold with vent on the shelf feature

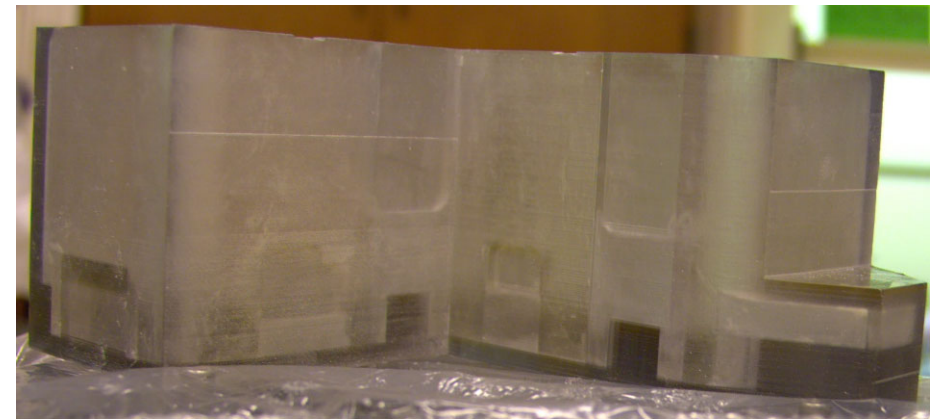
rho  
1.000e+00  
7.750e-01  
5.500e-01  
3.250e-01  
1.000e-01

Time = 75.2433



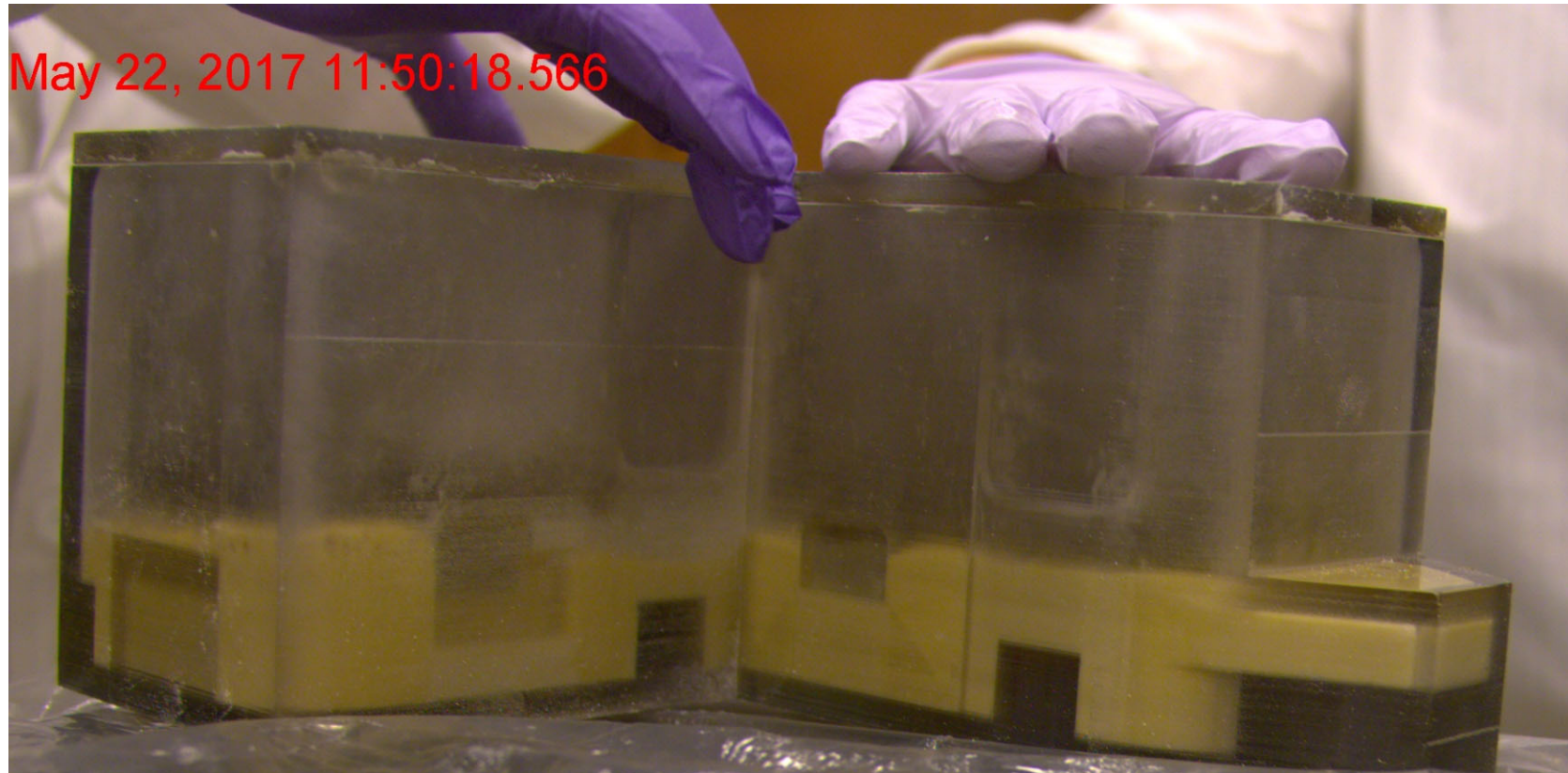
Flow visualization study supports computational conclusions

Foam filling for 20° tilt: the angled fill reduces voids on the new shelf





# Validation Experiment: 5 Degree Tilt: Foam Fills Shelf and Levels Quickly



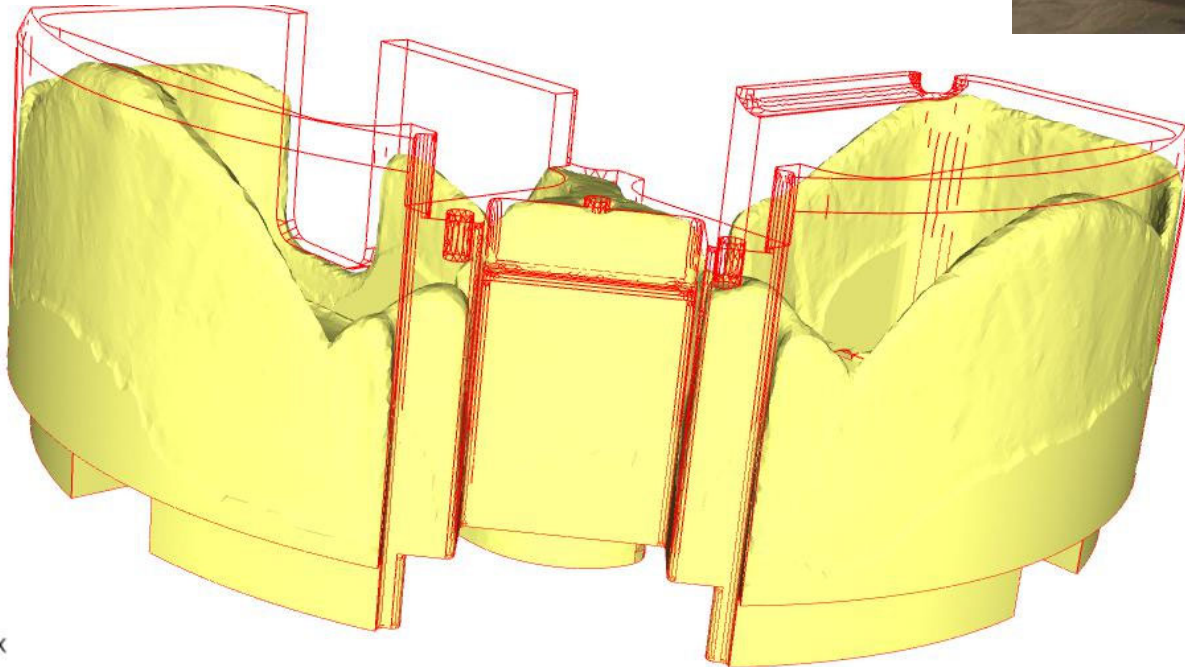
- New experiment using clear mold
- Room temperature mix of foam, which heats up to 24°C
- Mold stays roughly 22°C
- 5 degree tilt towards the front of the mold

# Experimental Conditions: Back of Mold



Run model with similar initial conditions:

- 240g material
- 4 degree tilt
- Room temperature mold and foam



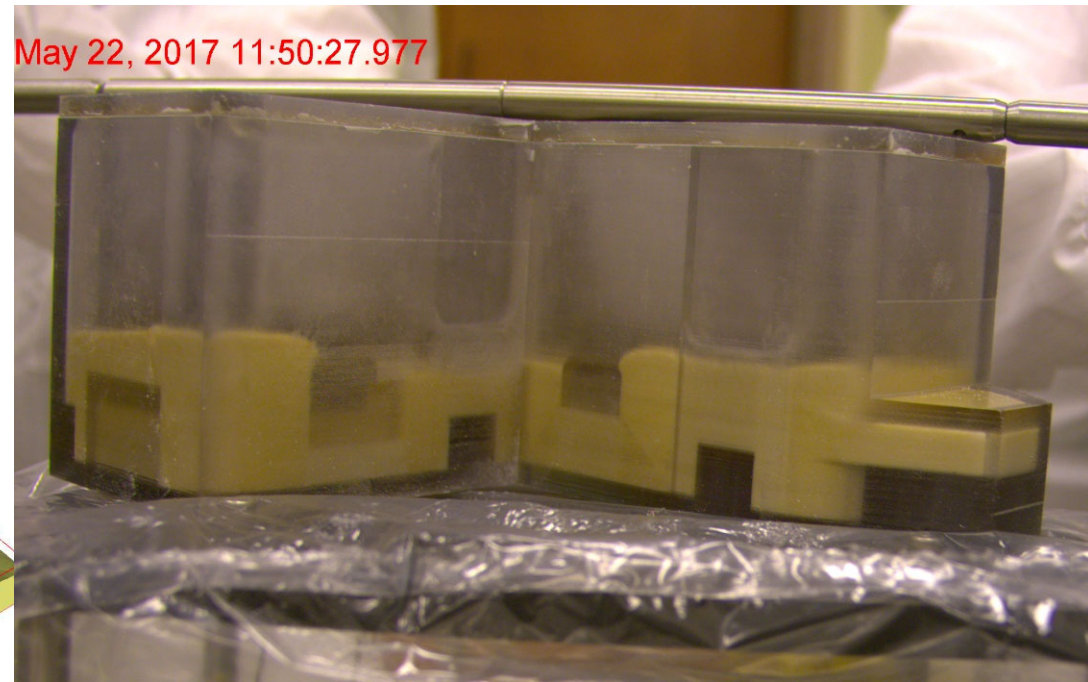
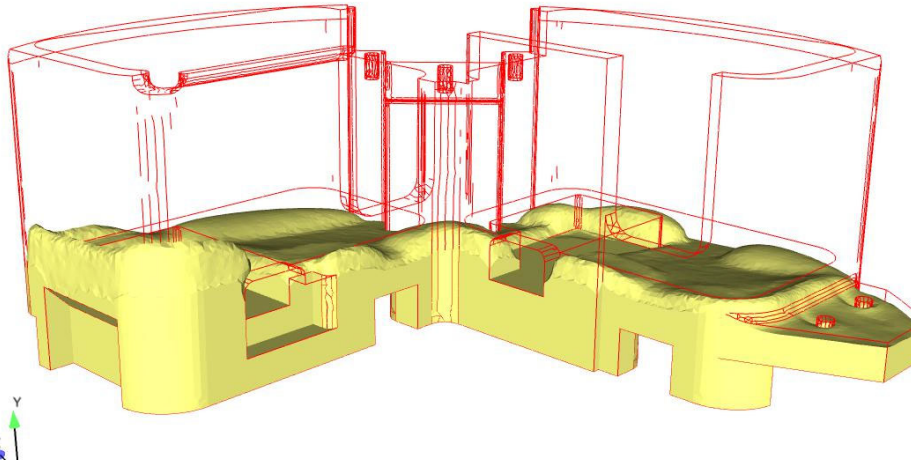
Shape of the model interface matches well with shape of experiment thought model fills back feature faster



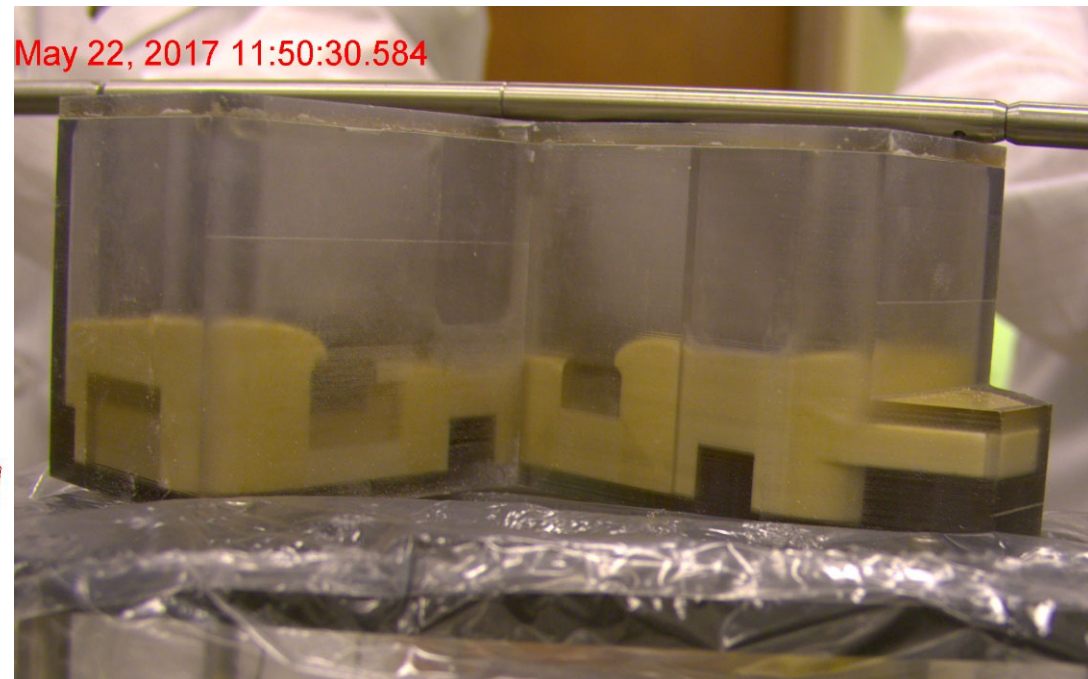
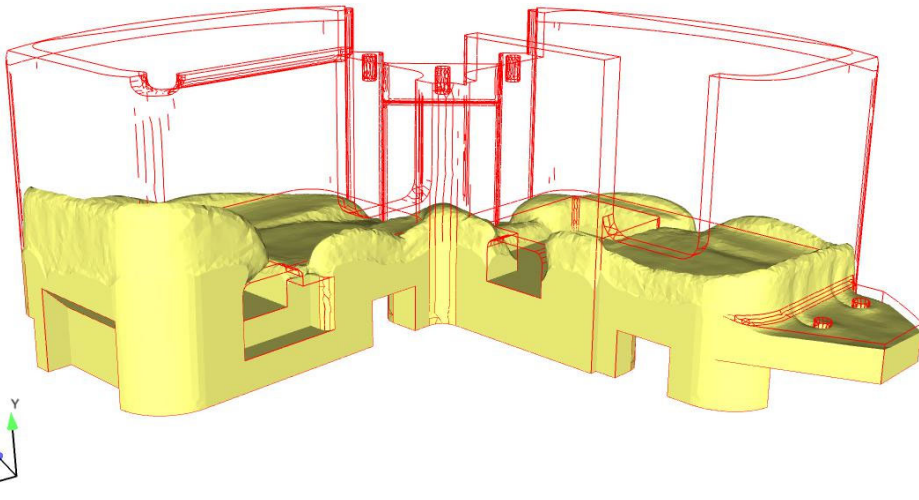
# Compare Mold Front: Early Times



Time = 34.184



Time = 44.617

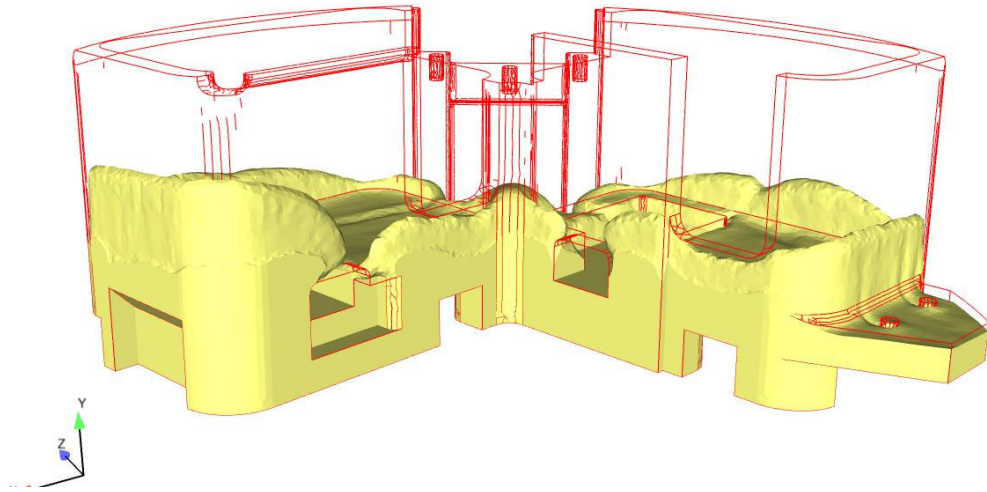




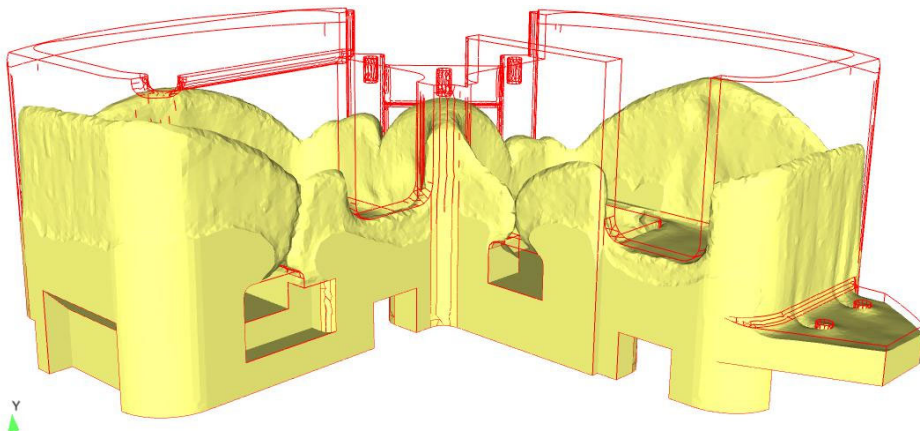
# Compare Mold Front: Moderate Time



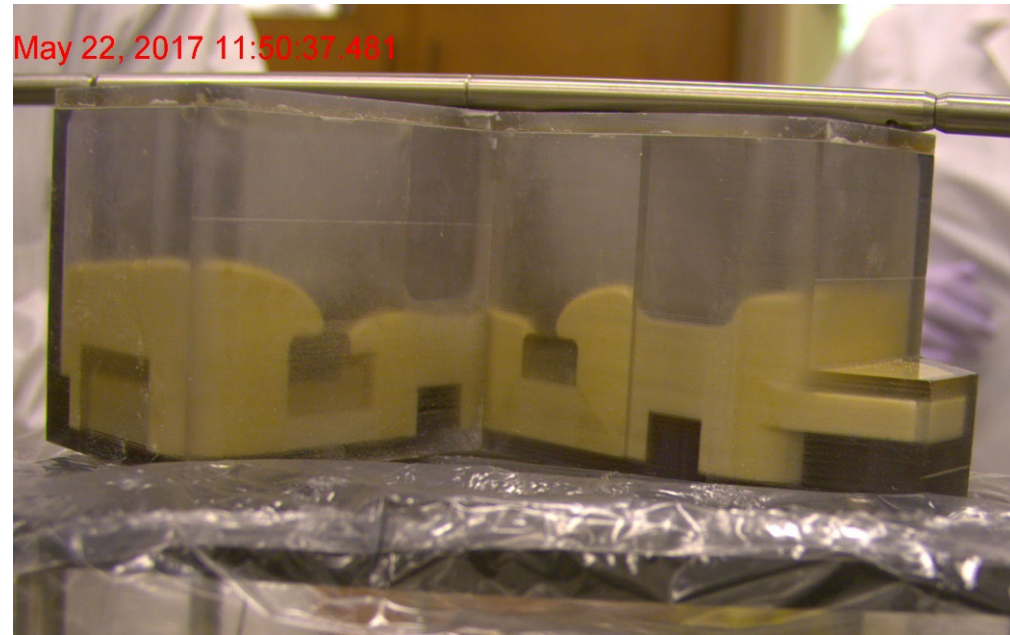
Time = 49.913



Time = 62.538



May 22, 2017 11:50:37.481



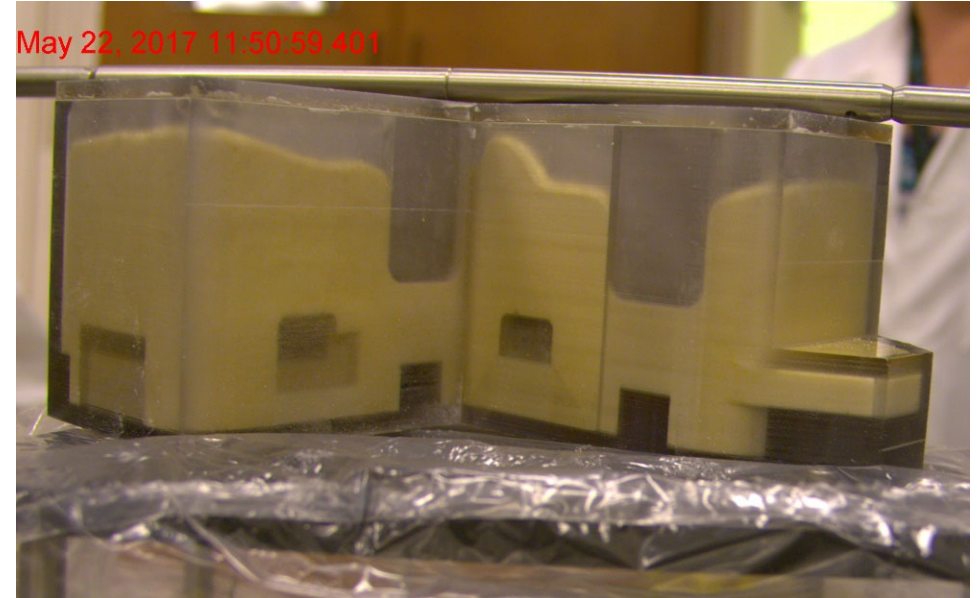
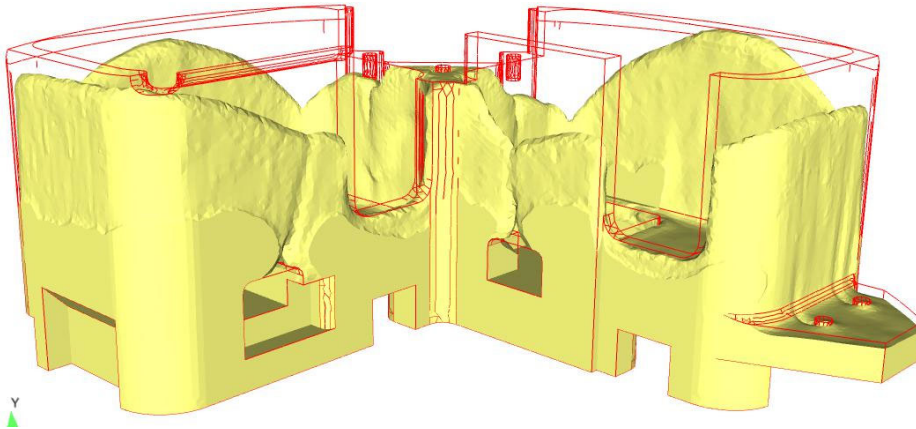
May 22, 2017 11:50:45.296



# Compare Mold Front: Late Time



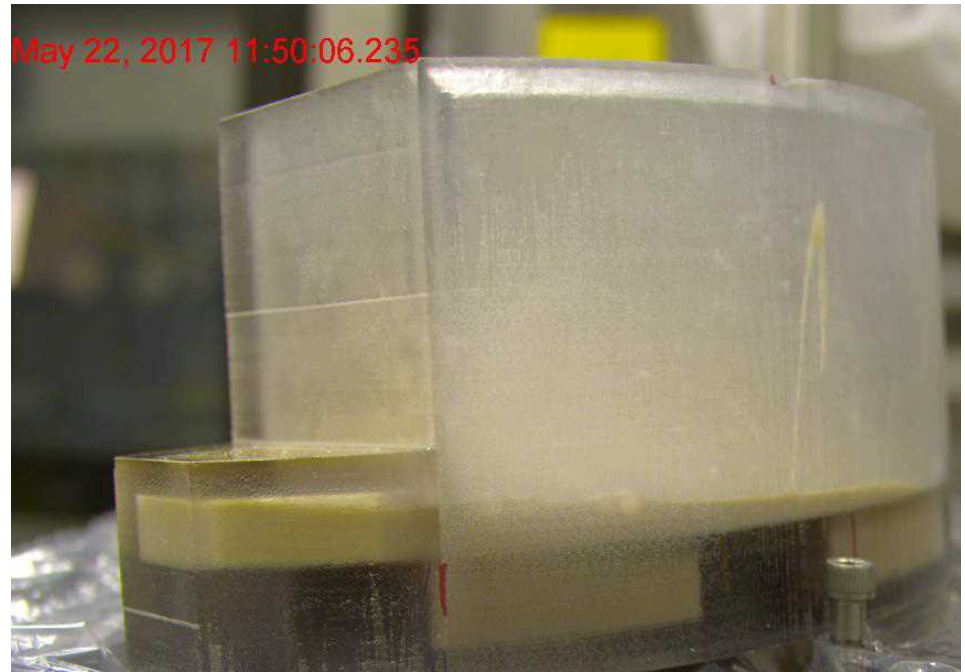
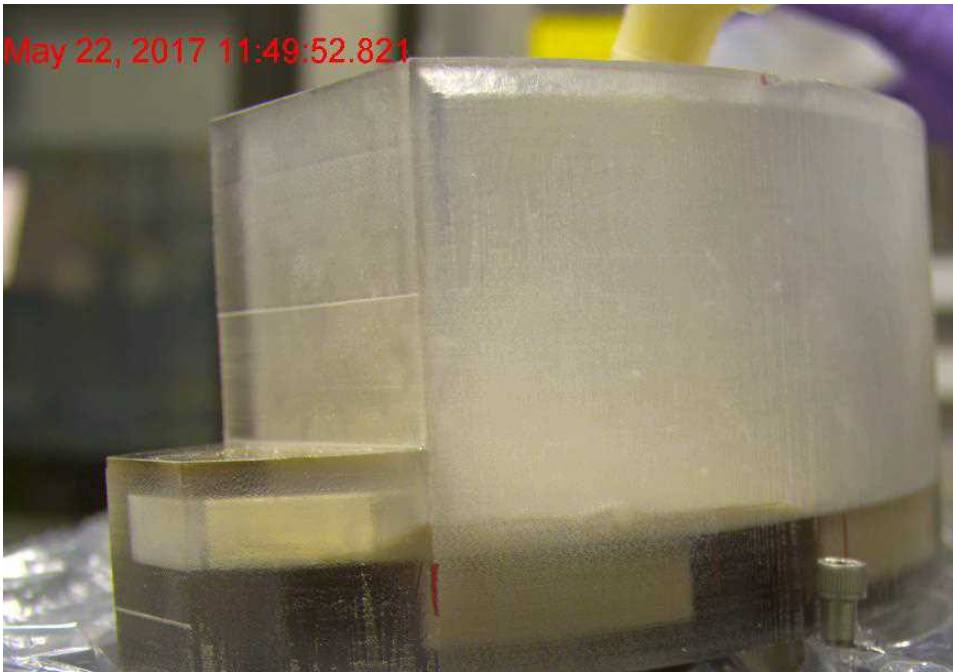
Time = 68.204



Shape of the model interface matches well with shape of experiment and the time-scale is similar



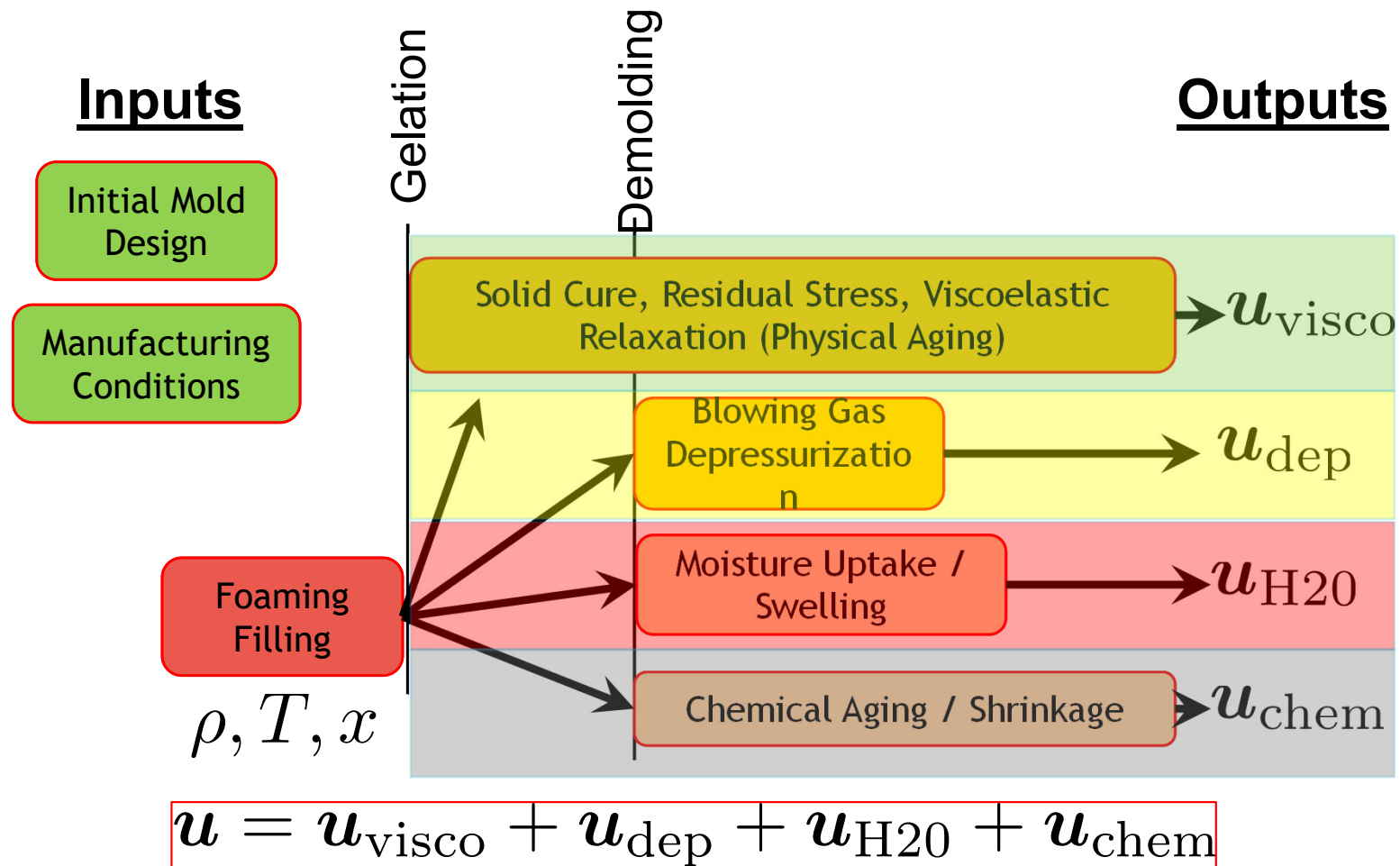
# Shelf Feature Fills Well in Clear Mold



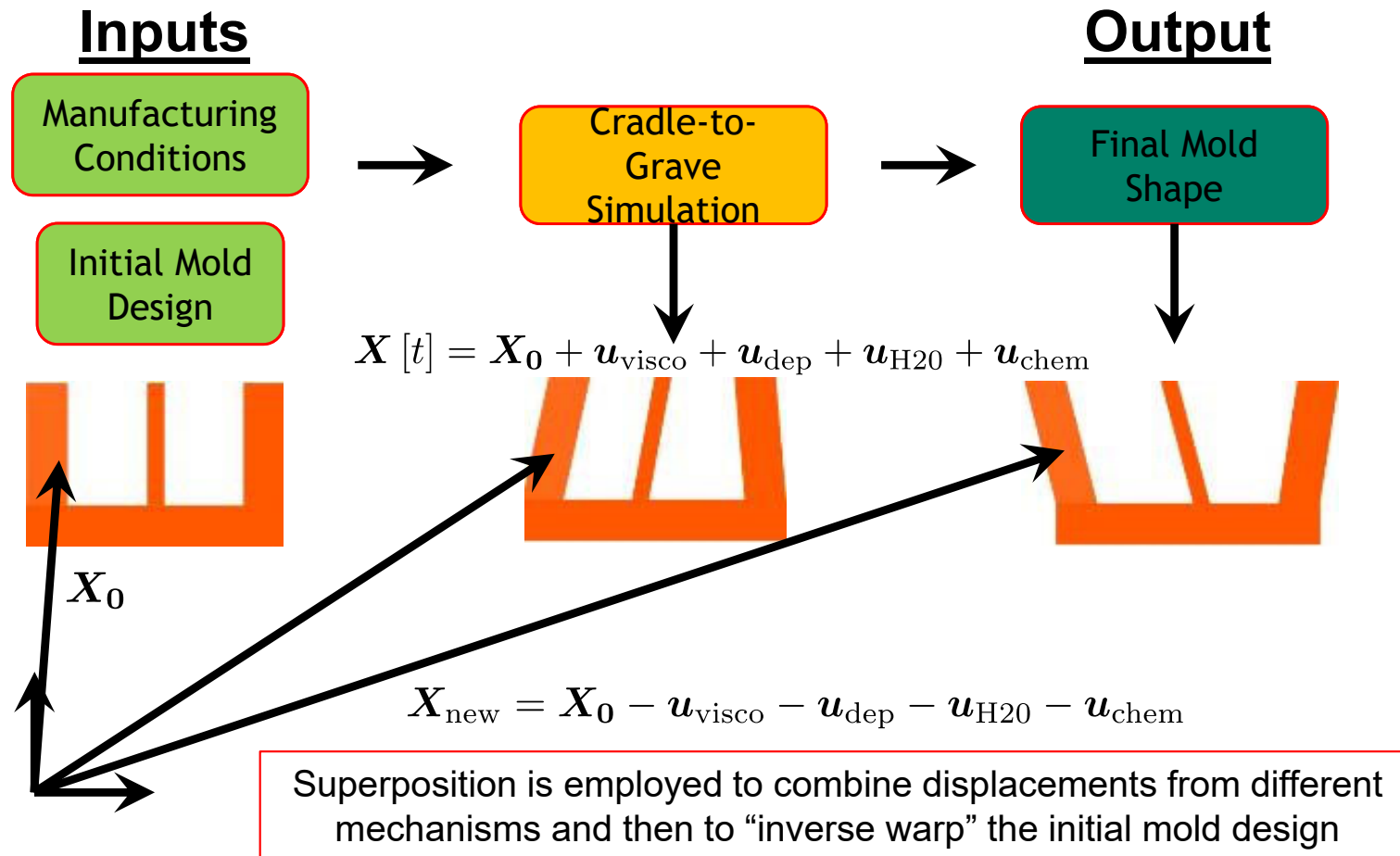
Experiment shows good filling of the shelf feature even at early times giving confidence in the foam model



# Develop an engineering-scale model framework for manufacturing and in-service aging for Rigid PMDI Foams



# A Key Model Target: Inverse mold design for manufacturing/age aware shrinkage mitigation



# Non-Linear Curing Viscoelastic Solid Modeling



## Balance Laws and Solution Fields:

- Mass + Momentum (*Displacements*) ← Lagrangian
- Species Balance (*Chemical Reaction Extent*) ← FEM
- Energy (*Temperature*) ← ALE FEM

## Solid State Non-Linear Viscoelastic (NLVE) Model Initial Conditions

- Initialize *temperature, foam density, and reaction extent* from simulation stage 1
- Directly initialize the stress-free reaction and temperature (expansion free)
- Assume the NLVE viscous stresses are initially zero

## Stress prediction based on the universal curing model developed at SNL

DB Adolf and RS Chambers, "A thermodynamically consistent, nonlinear viscoelastic approach for modelling thermosets during cure," *J. Rheology*, 2007.

Cauchy Stress: SNL Non-linear Viscoelastic Curing Model (Adolf & Chambers 2007)

$$\underline{\underline{\sigma}} = \underline{\underline{\sigma}}[\log \underline{\underline{U}}, T, x, \text{histories}]$$

Logarithmic Strain

Temperature

Extent of matrix cure

### Material and Laboratory Time Relation

$$dt^* = \frac{dt}{a[t]}$$

$$\log a = -\hat{C}_1 \left( \frac{N}{\hat{C}_2 + N} \right)$$

### Density

#### Scaling

$$\psi[\rho_0] = \left( \frac{\rho_0}{\rho_{ref0}} \right)^p \psi[\rho_{ref0}] \quad \text{Free Energy}$$

$$\underline{\underline{\sigma}}[\rho_0] = \left( \frac{\rho_0}{\rho_{ref0}} \right)^p \underline{\underline{\sigma}}[\rho_{ref0}] \quad \text{Cauchy Stress}$$

# Curing NLVE Model Continued



Relaxation behavior and mechanical properties depend on the *temperature, extent of cure, and histories of deformation*

## Material Time Dependencies

Thermal

Pressure

$$N = \left\{ \left[ T(t) - T_{ref} \right] - \int_0^t ds \, f_1(t^* - s^*) \frac{dT}{ds}(s) \right\} + C_3 \left\{ I_1(t)_{ref} - \int_0^t ds \, f_1(t^* - s^*) \frac{dI_1}{ds}(s) \right\} \\ + C_4 \left\{ \int_0^t \int_0^t ds \, du \, f(t^* - s^*, t^* - u^*) \frac{d\varepsilon_{dev}(s)}{ds} : \frac{d\varepsilon_{dev}(u)}{du} \right\} + C_5(x(t)) \left\{ \left[ x(t) - x_{ref} \right] - \int_0^t ds \, f_1(t^* - s^*) \frac{dx}{ds}(s) \right\}$$

Shear Deformation Matrix Cure

## Glass Transition Evolution

$$T_{ref}(x) = T_{ref} - \frac{[C_3\beta_\infty + C_5(x(t))](x(t) - x_{ref})}{(1 + C_3\alpha_\infty)}$$

$$C_5(x(t)) \equiv C_{5a} + C_{5b} x$$

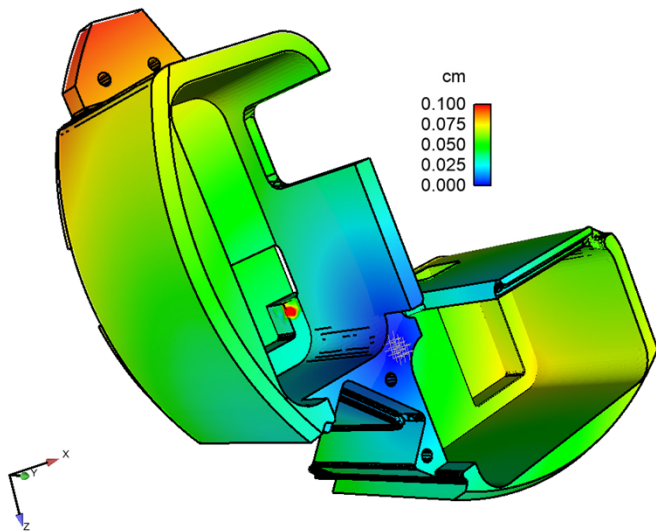
## Shear Modulus

$$G_g(T) = G_{gref} + \frac{\partial G_g}{\partial T}(T - T_{ref}) + \frac{\partial G_g}{\partial x}(x - x_{ref})$$

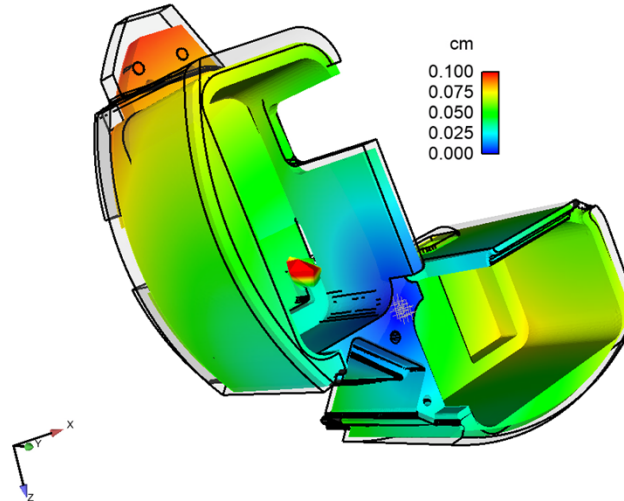
$$G_\infty(T) = \left\{ G_{ref} + \frac{\partial G_\infty}{\partial T}(T - T_{ref}) \right\} \left[ \frac{x^m - x_g^m}{x_{ref}^m - x_g^m} \right]^n$$



# Contour Plots of Displacements: Manufacturing + Viscoelasticity

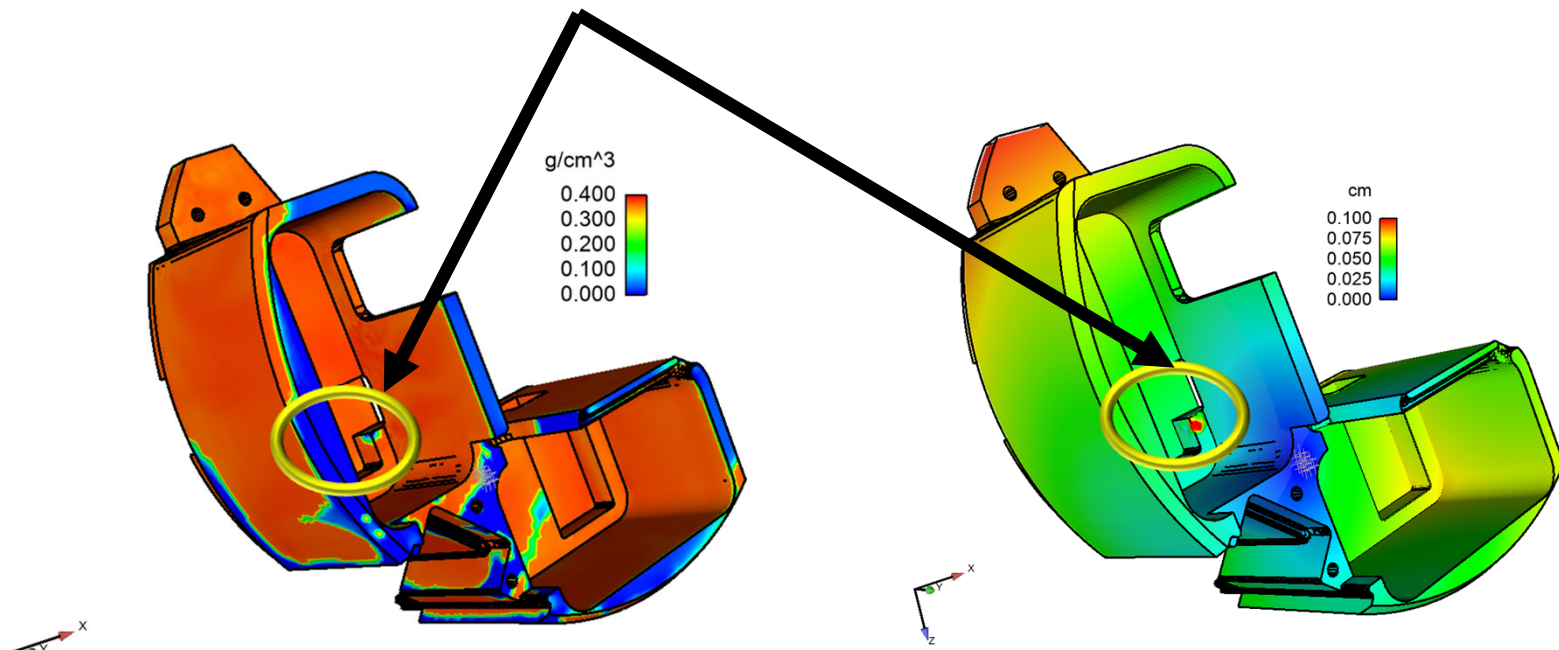


Deformed shape shown to scale



Deformed shape magnified 10x

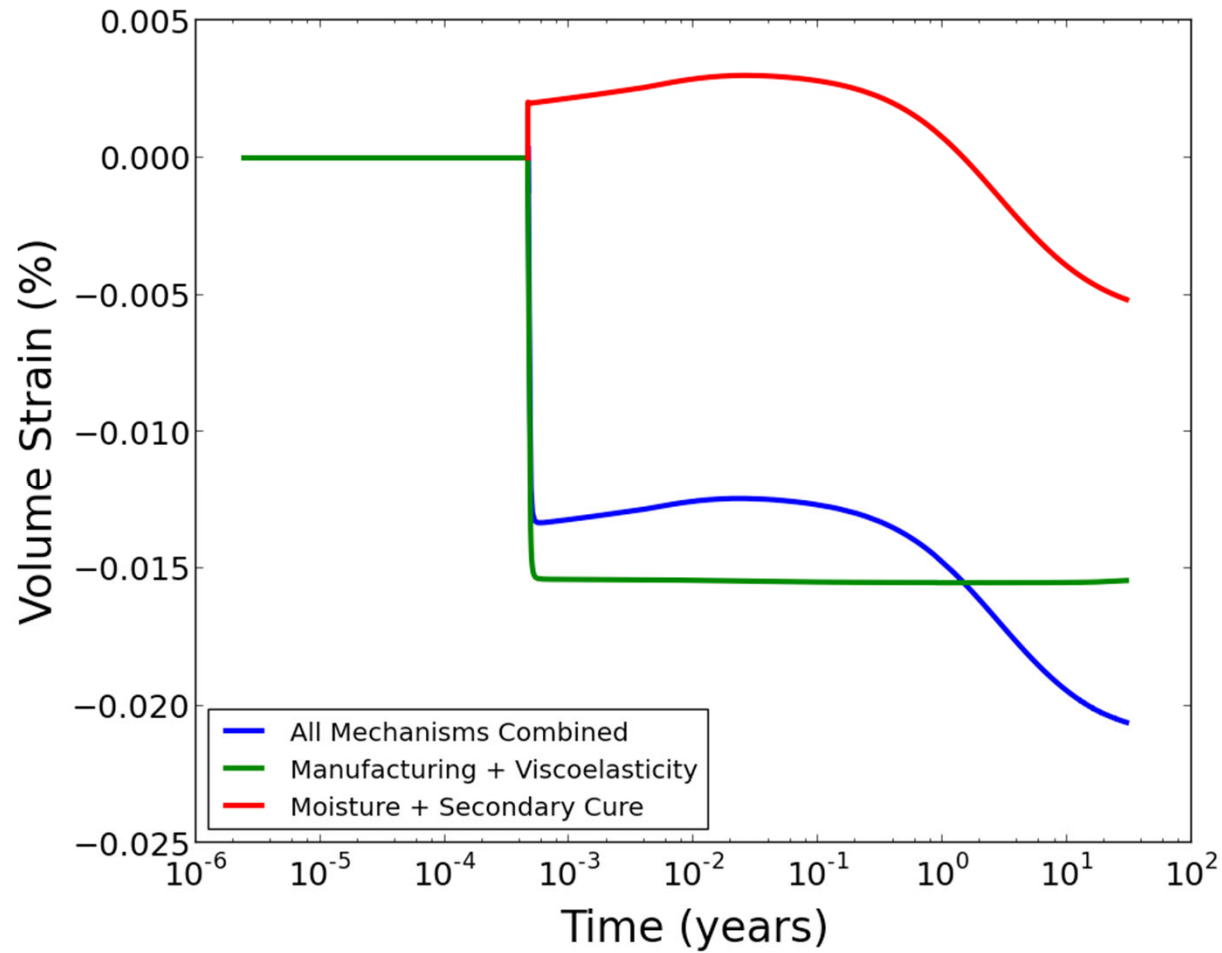
# Poor fill quality leads to large, local deformations



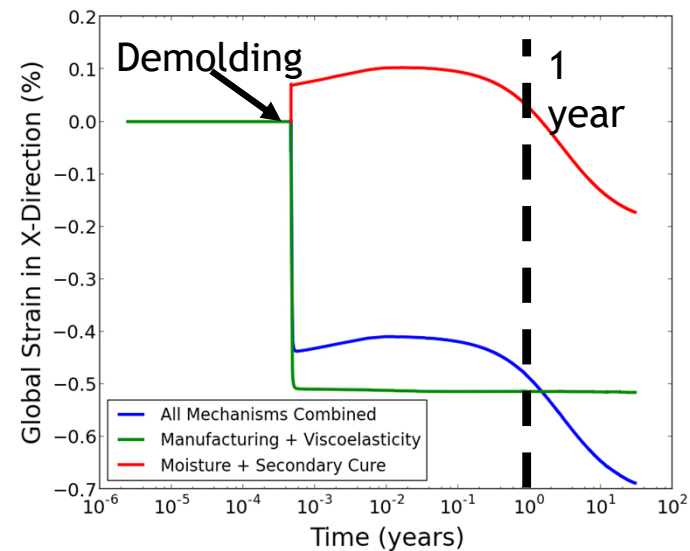
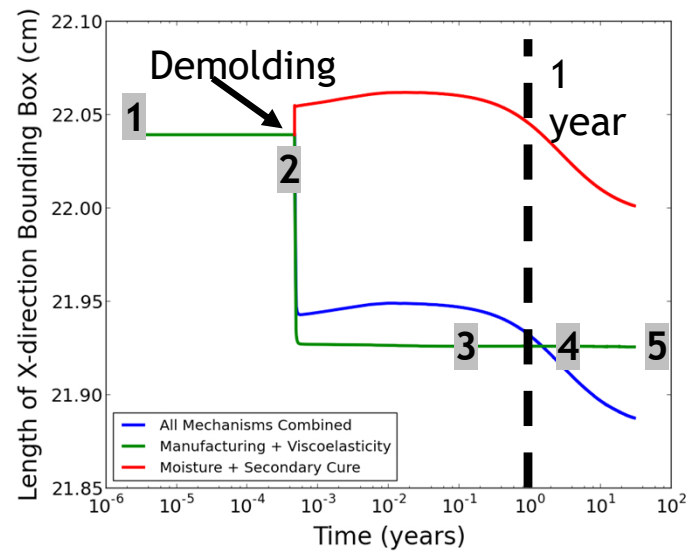
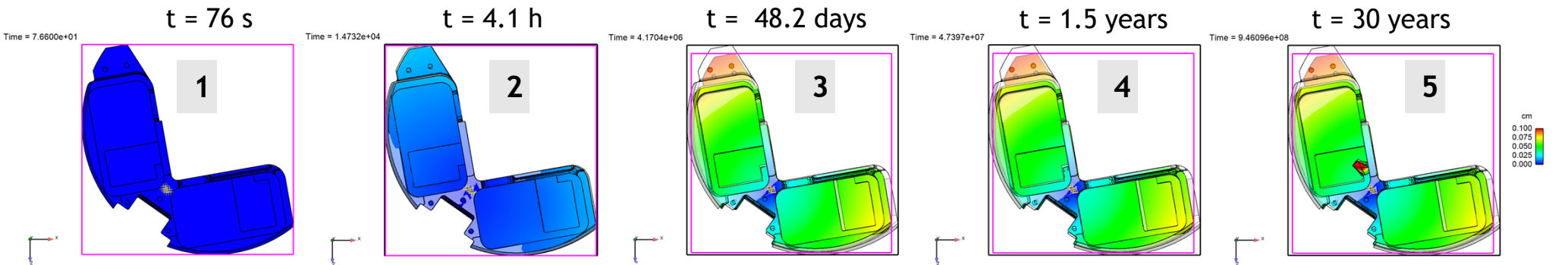
Density of filled part

Displacement from  
Manufacturing +  
Viscoelasticity, Deformed  
shape shown to scale

# Volume Strain as a Function of Time



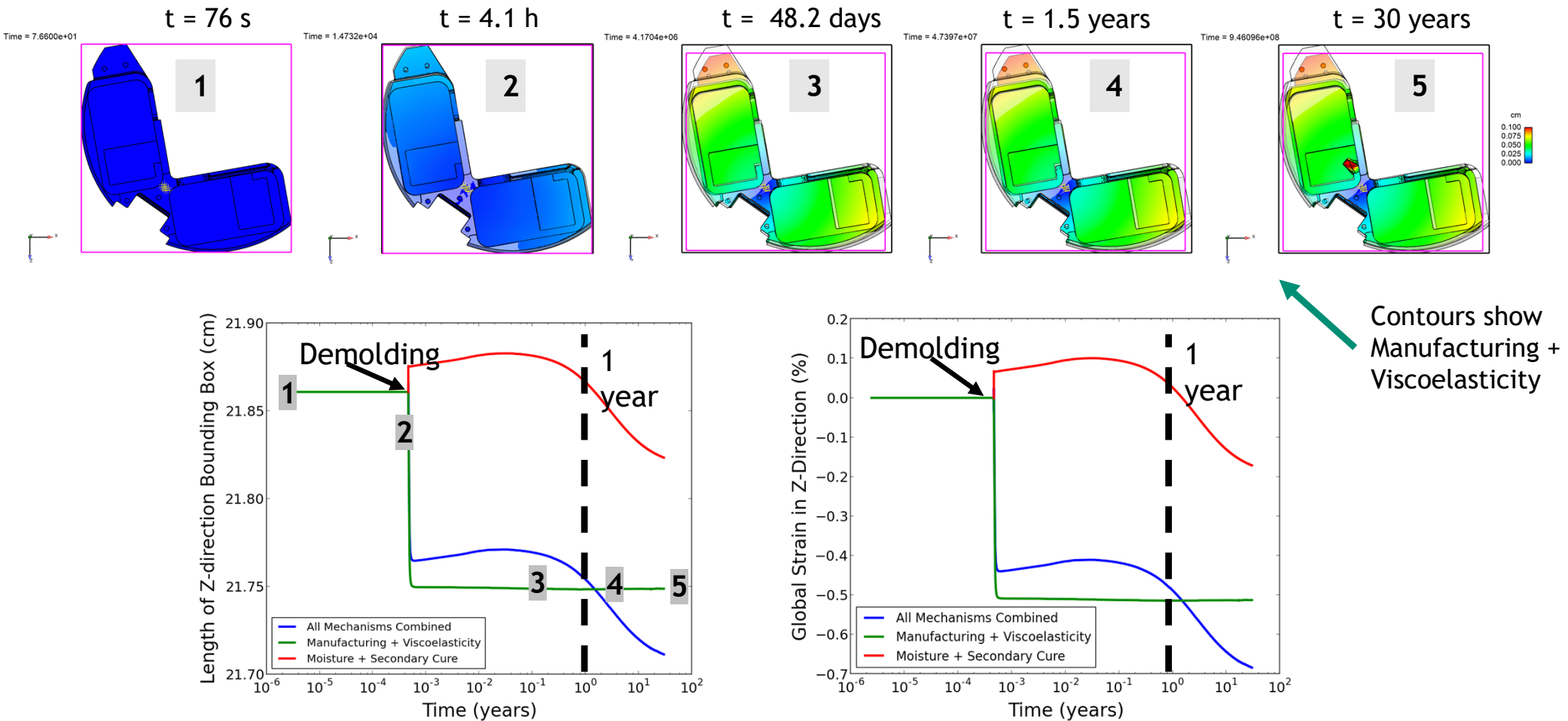
# Change in Bounding Box Length—X Direction



Contours show Manufacturing + Viscoelasticity



# Change in Bounding Box Length—Z Direction



# Conclusions



- All simulations filled fairly well: Complex mold should fill with new shelf!
- Density of the shelf may be lower than nominal density
- Higher temperature increased void size due to ideal gas law, though it filled faster on average
- Vent on shelf did not change void content or density – this is probably due to coarse mesh. In real world, it should help
- Model follows free surface of foam fairly well
- Combination of experimental and computational work led to synergistic breakthroughs creating confidence in mold redesign
- Density and density gradients are still not quantitative and give direction for future work -> bubble-scale modeling
- Multiphysics models allows prediction of shape change during manufacturing and viscoelastic relaxation over 30 years of storage