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A numerical study of the length-scale dependence of pool fire behavior using large eddy simulation

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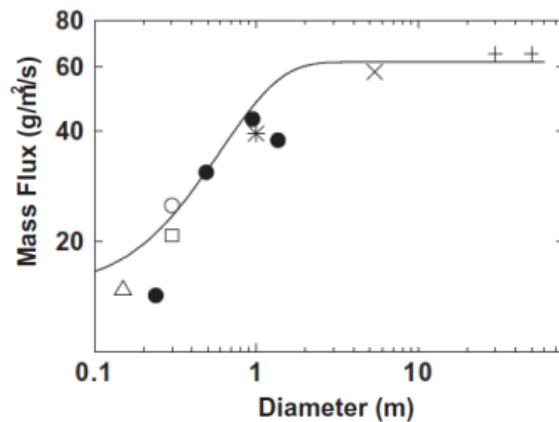
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Motivation

- Heat flux to the pool surface and vaporization rate is observed to increase for medium diameters and level off for large diameters.
 - This is associated with increasing radiation heat flux followed by optically thick conditions where radiative flux to the pool surface is constant W.R.T. pool diameter.
- Experimentally studying the how flame interior radiative heat transfer evolves with changing pool diameter is difficult for large sooting flames.





Model formulation: governing equations

continuity
$$\int \frac{\partial \bar{\rho}}{\partial t} dV + \int \bar{\rho} \tilde{u}_j n_j dS = - \int S_{Y_{\text{soot}}} dV$$

momentum
$$\int \frac{\partial \bar{\rho} \tilde{u}_i}{\partial t} dV + \int \bar{\rho} \tilde{u}_i \tilde{u}_j n_j dS = \int (\tilde{\sigma}_{ij} - \tau_{ij}^{sgs}) n_j dS + \int (\bar{p} - p_o) g_i dV$$

Mixture fraction
$$\int \frac{\partial \bar{\rho} \tilde{Z}}{\partial t} dV + \int \bar{\rho} \tilde{u}_j \tilde{Z} n_j dS = \int \left(\frac{\bar{\mu}}{Sc} \frac{\partial \tilde{Z}}{\partial x_j} - \tau_{Z,j}^{sgs} \right) n_j dS - \int S_{Y_{\text{soot}}} dV$$

enthalpy
$$\int \frac{\partial \bar{\rho} \tilde{h}}{\partial t} dV + \int \bar{\rho} \tilde{u}_j \tilde{h} n_j dS = \int \left(\frac{\bar{\mu}}{Pr} \frac{\partial \tilde{h}}{\partial x_j} - \tau_{h,j}^{sgs} \right) n_j dS - \int S_h dV$$

Soot mass
$$\int \frac{\partial \bar{\rho} \tilde{Y}_{\text{soot}}}{\partial t} dV + \int \bar{\rho} \tilde{u}_j \tilde{Y}_{\text{soot}} n_j dS = \int \left(\frac{\bar{\mu}}{Pr} \frac{\partial \tilde{Y}_{\text{soot}}}{\partial x_j} - \tau_{Y_{\text{soot},j}}^{sgs} \right) n_j dS + \int S_{Y_{\text{soot}}} dV$$

Soot particle concentration
$$\int \frac{\partial \bar{\rho} \tilde{N}_{\text{soot}}}{\partial t} dV + \int \bar{\rho} \tilde{u}_j \tilde{N}_{\text{soot}} n_j dS = \int \left(\frac{\bar{\mu}}{Pr} \frac{\partial \tilde{N}_{\text{soot}}}{\partial x_j} - \tau_{N_{\text{soot},j}}^{sgs} \right) n_j dS + \int S_{N_{\text{soot}}} dV$$

- The enthalpy source term, S_h , includes radiative terms from gas and soot.
- Source terms for soot mass and particle concentration have the following form:

$$S_{N_{\text{soot}}} = S_{\text{nucleation}} - S_{\text{coagulation}} \tilde{Y}_{\text{soot}}^{1/6} \tilde{N}_{\text{soot}}^{11/6}$$

$$S_{Y_{\text{soot}}} = W_{\text{soot}} S_{\text{nucleation}} + [S_{\text{surface growth}} - S_{\text{ox}, \text{O}_2} - S_{\text{ox}, \text{OH}}] \tilde{Y}_{\text{soot}}^{2/3} \tilde{N}_{\text{soot}}^{1/3}$$

- $S_{\text{nucleation}}$, $S_{\text{coagulation}}$, *etc.* are computed based on the Aksit-Moss soot model.
- These terms depend on a number of species concentrations which are computed from a flamelet model.



Model formulation: Flamelet equations

- flamelet equation solution parametrizes $\phi = \{Y_i, T\}$ in terms of 3 variables:

$$\phi = \phi(Z, \chi, \gamma)$$

$$\chi = 2D_Z |\nabla Z|^2$$

$$\gamma = h - h_c$$

$$\frac{\partial Y_i}{\partial t} = \frac{\chi}{2} \frac{\partial^2 Y_i}{\partial Z^2} + \frac{\omega_i}{\rho}$$

$$\frac{\partial T}{\partial t} = -\frac{1}{\rho c_p} \sum_{i=1}^{n_s} \omega_i h_i - \left(\frac{\partial^2 T}{\partial Z^2} + \frac{\partial T}{\partial Z} \frac{\partial c_p}{\partial Z} + \frac{\partial T}{\partial Z} \sum_{i=1}^{n_s} \frac{c_{p,i}}{c_p} \frac{\partial Y_i}{\partial Z} \right) + S_T(Z, T, \chi)$$

Implicitly depends on γ

- Convolution of ϕ with a presumed PDF provides an interface between filtered values of Z, χ, γ and flamelet solutions.

Scalar variance:
determined from
turbulence model

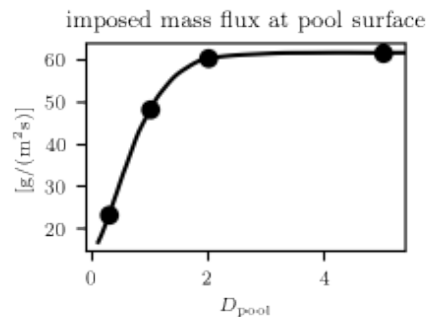
Presumed mixture
fraction PDF

$$\tilde{\phi}(\tilde{Z}, \tilde{Z}''^2, \tilde{\chi}, \tilde{\gamma}) = \int_0^1 \phi(Z, \chi, \gamma) P_Z(Z | \tilde{Z}, \tilde{Z}''^2) dZ, \tilde{\gamma} = \gamma, \tilde{\chi} = \chi$$

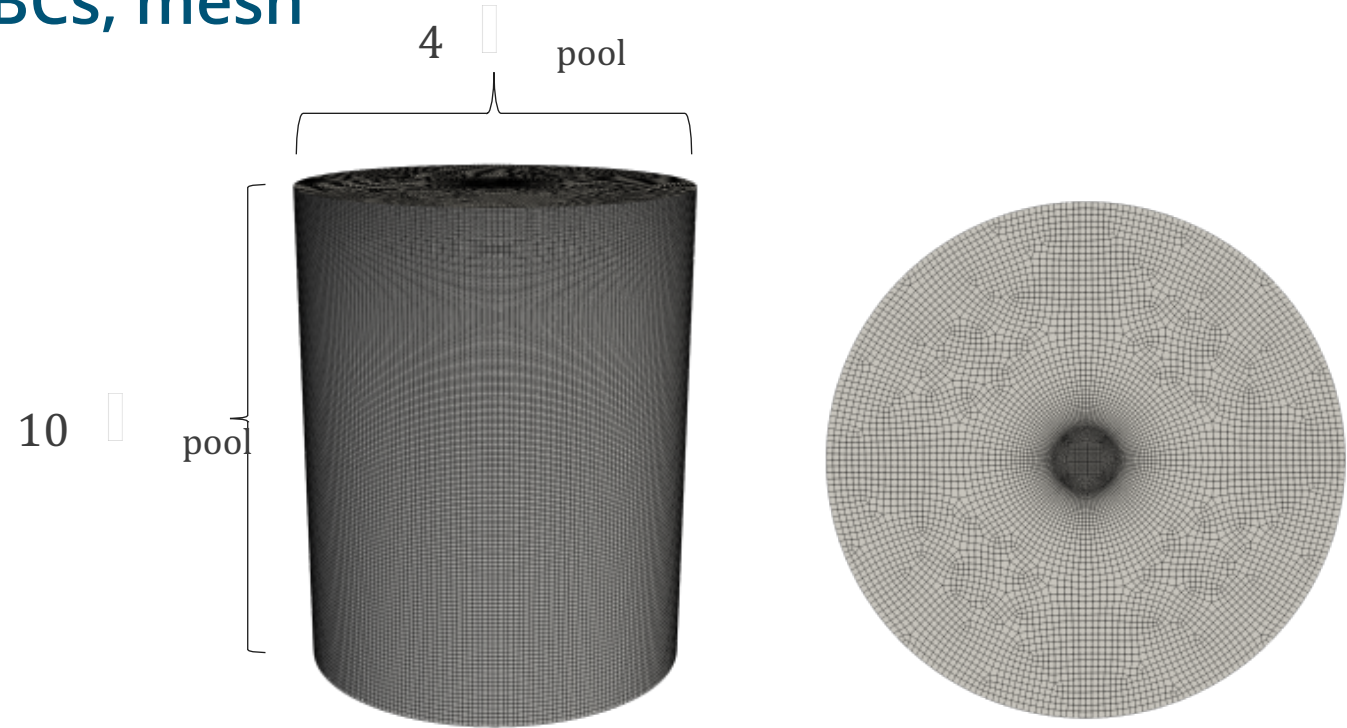


Computational setup; ICs, BCs, mesh

- 4 pool fire diameters considered: 0.3, 1, 2, and 5 meters.
- Cylindrical Domain:
 - 4 pool diameters wide
 - 10 pool diameters high
- BCs at pool surface:
 - $T_{\text{pool}} = 300 \text{ K}$
 - Mass flux set based on empirical correlation (Ditch *et al.* [1]).



- Domain initially consists of air ($Z = 0$) at 300 K.



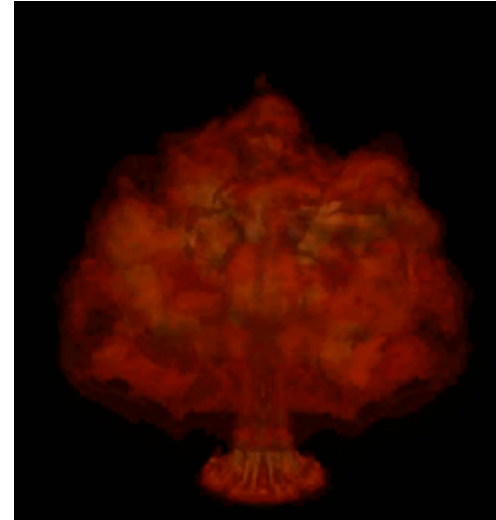
	0.3 m	1 m	2 m	5 m
Pool mass flux $[\text{g}/\text{m}^2\text{s}]$	23.46	48.15	60.35	61.64
Mesh resolution	0.3 cm	1 cm	2 cm	2.5 cm



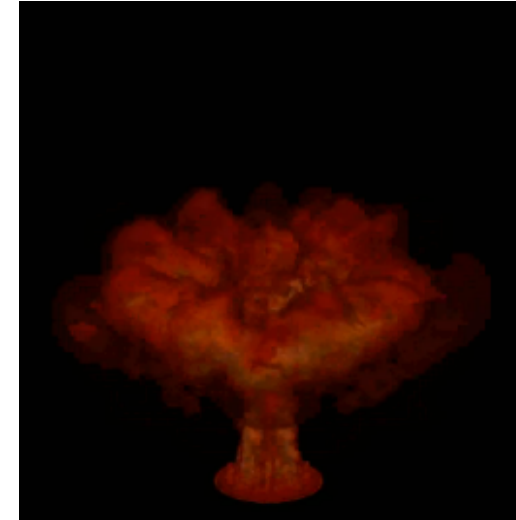
Results

- Animation playback speed is scaled by $D_{\text{pool}}^{1/2}$.
- Calculations for each pool size are run out for at least 10 puff cycles.

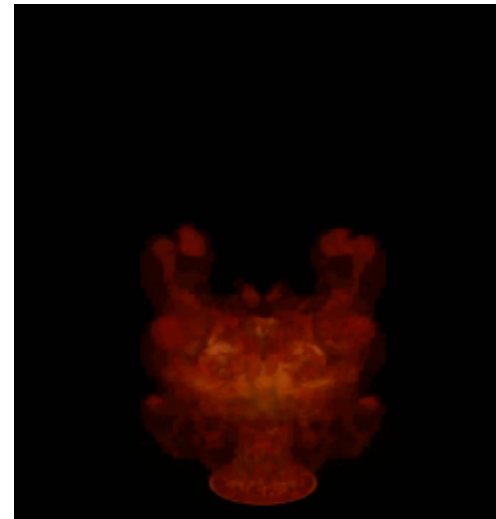
$D_{\text{pool}} = 0.3 \text{ m}$



$D_{\text{pool}} = 1 \text{ m}$



$D_{\text{pool}} = 2 \text{ m}$



$D_{\text{pool}} = 5 \text{ m}$



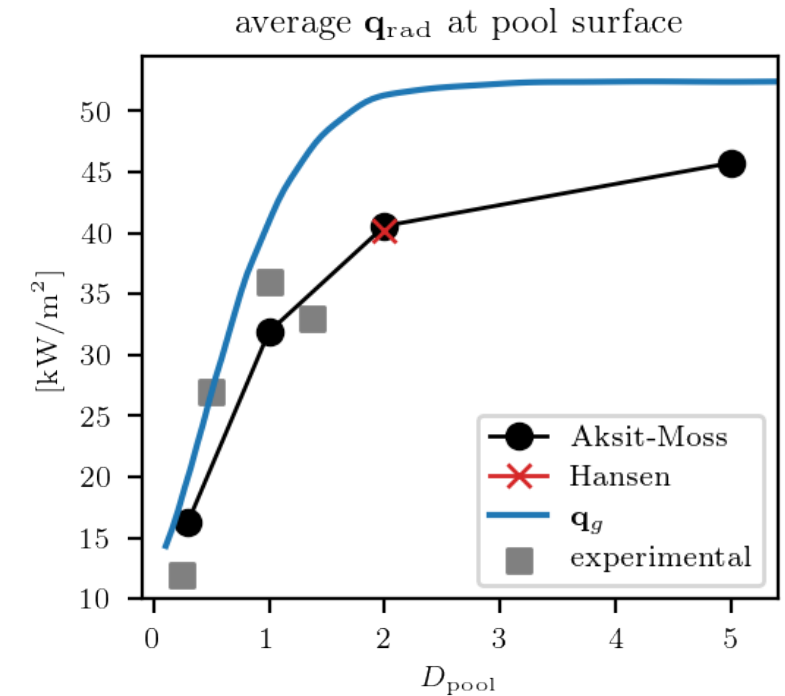
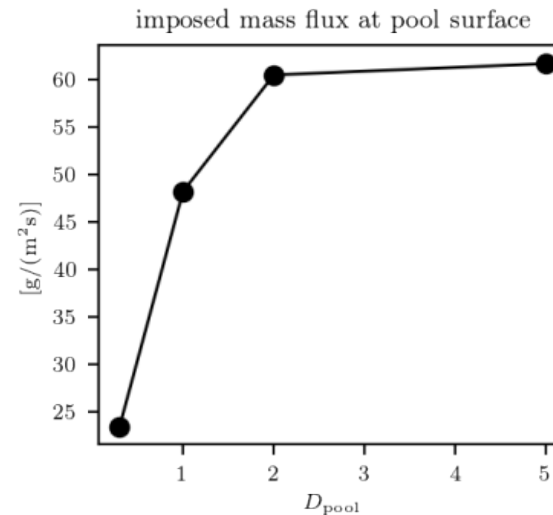


Radiative heat fluxes at pool surface

- Computed radiative heat fluxes agree with measured values .
- Discrepancy between \mathbf{q}_{rad} and \mathbf{q}_g due to
 - Decoupled \mathbf{q}_{rad} and \dot{N}_{pool} .
 - Non-negligible convective heat flux for small D_{pool} .

$$\mathbf{q}_g = \dot{N}_{\text{pool}} \Delta h_g$$

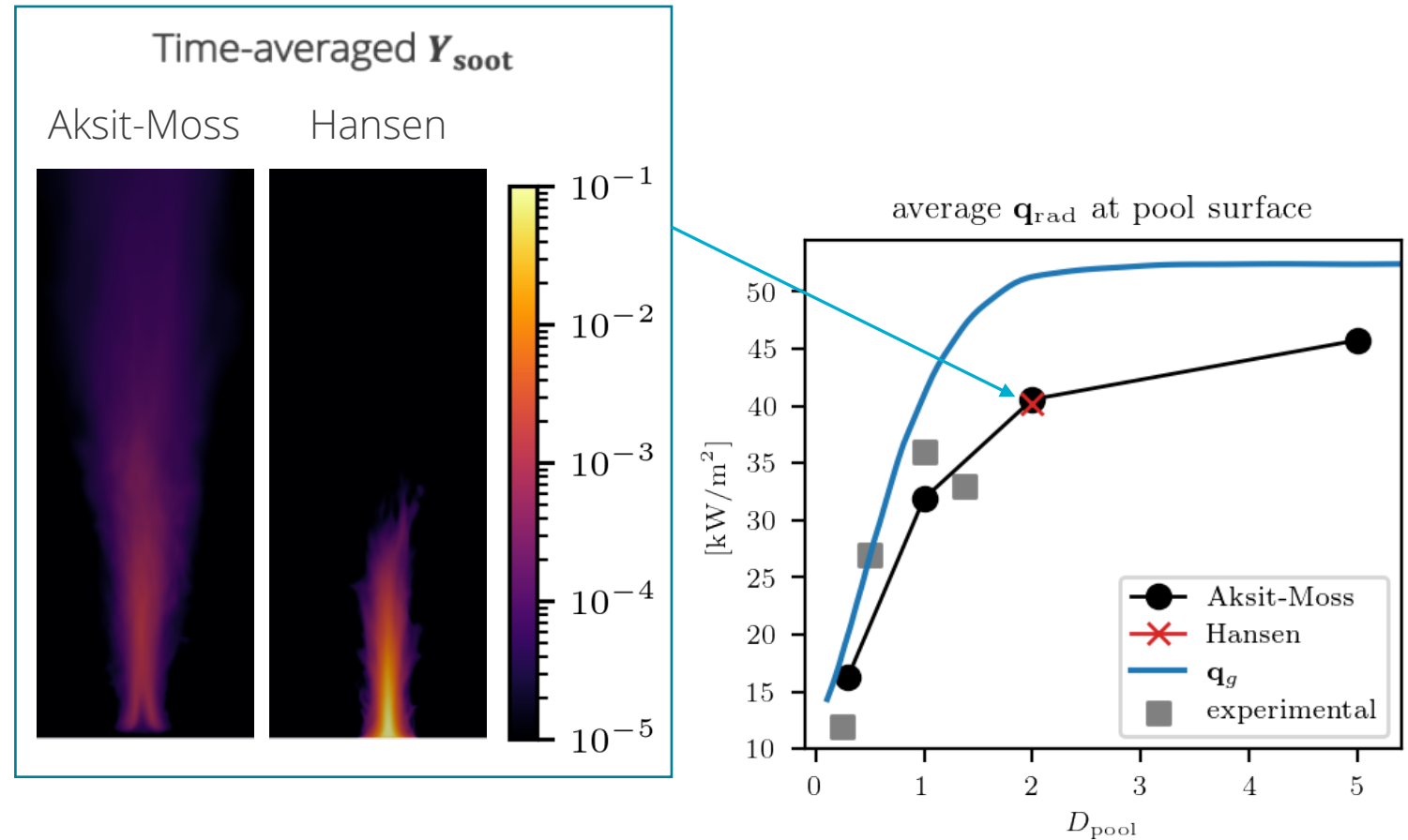
$$\Delta h_g = L_v(T_b) + \int_{T_0}^{T_b} C_p(T) dT$$





Radiative heat fluxes at pool surface

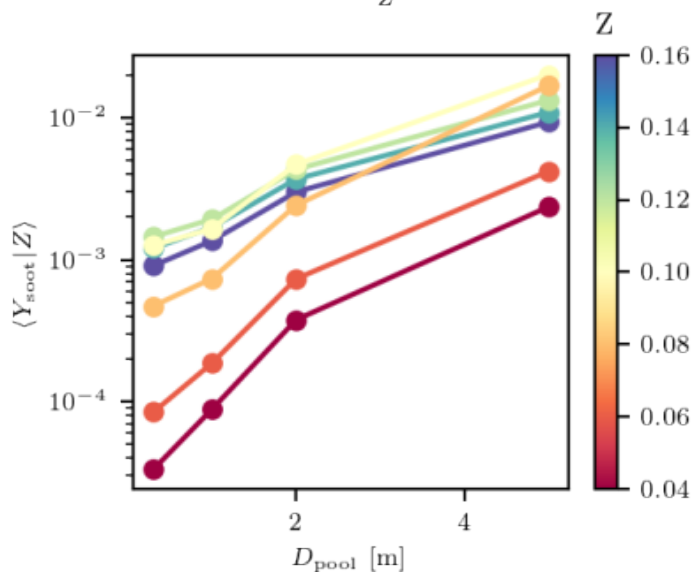
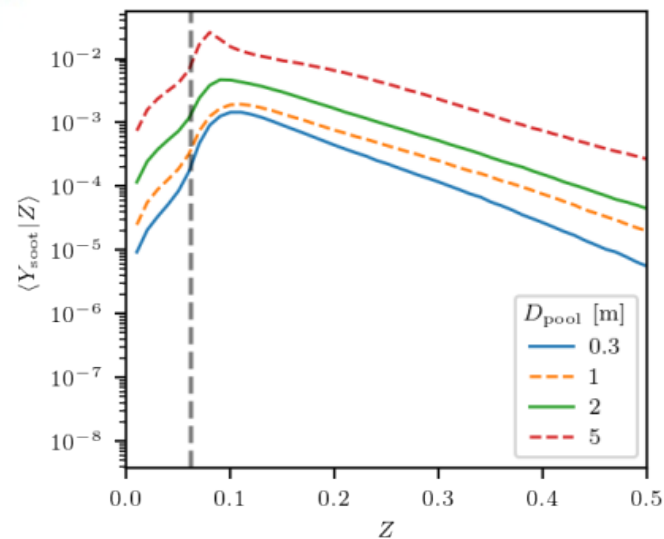
- Comparison of simulations using different soot models indicate $\mathbf{q_{rad}}$ at pool surface is insensitive to $\mathbf{Y_{soot}}$ if $\mathbf{Y_{soot}}$ is sufficiently large.



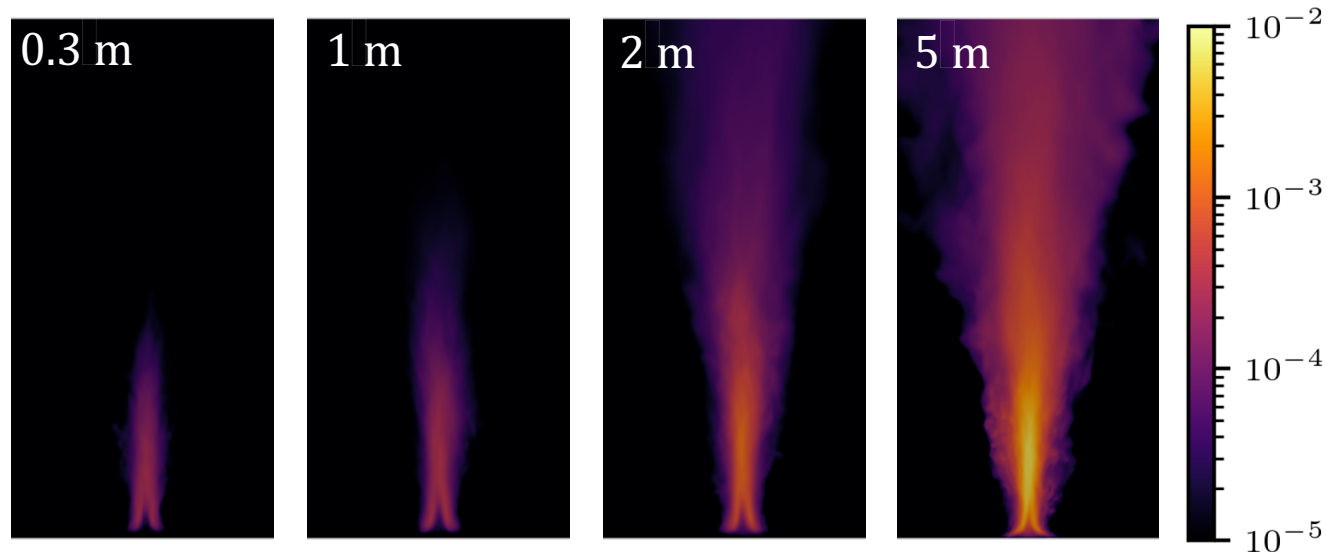


Soot concentration dependence on D_{pool}

- Trends of $\langle Y_{\text{soot}}|Z \rangle$ reflect those for time-averaged Y_{soot} .
- For fixed Z , computed $\langle Y_{\text{soot}}|Z \rangle$ grows approximately exponentially W.R.T D_{pool} for $D_{\text{pool}} \leq 2$ m.
 - This behavior should become asymptotic for sufficiently large D_{pool} .



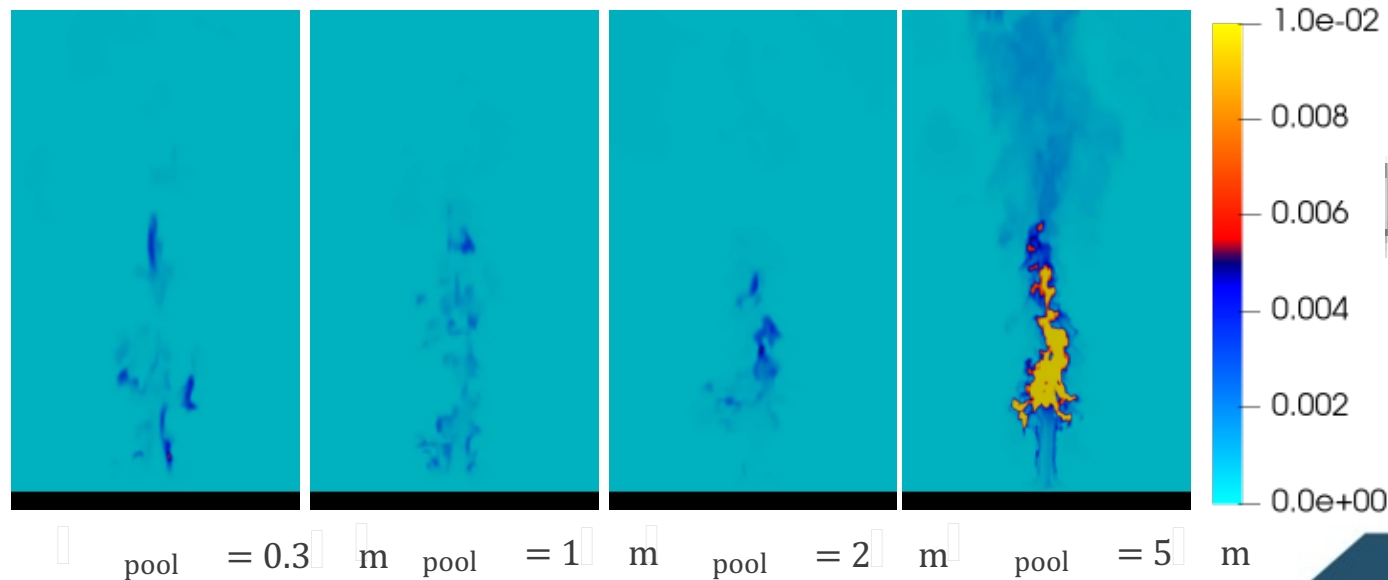
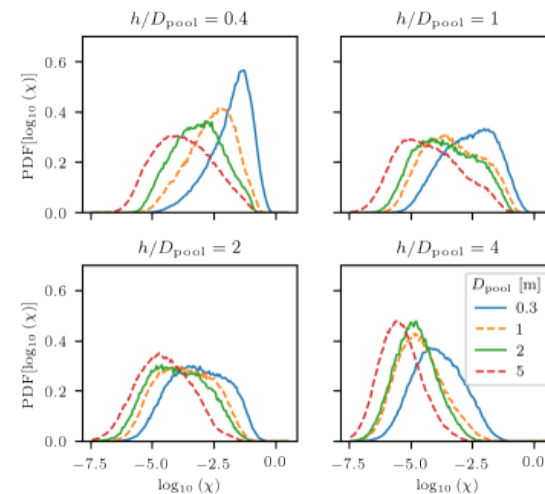
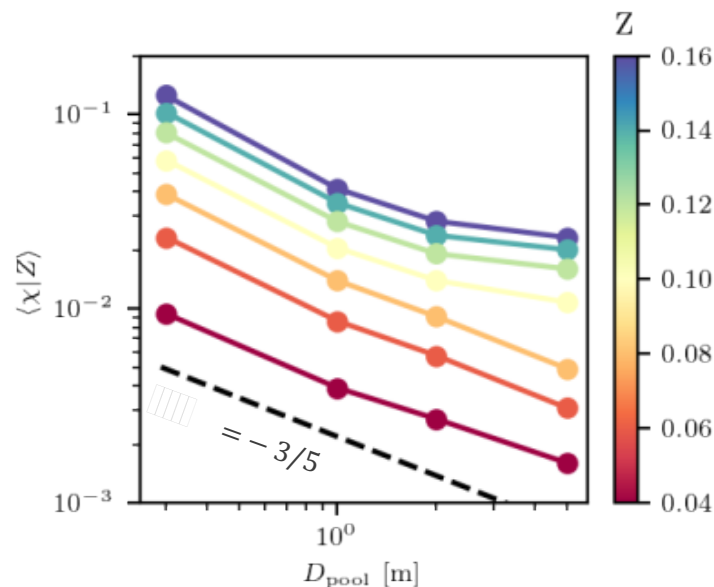
Time averaged Y_{soot}





Small-scale mixing dependence on D_{pool}

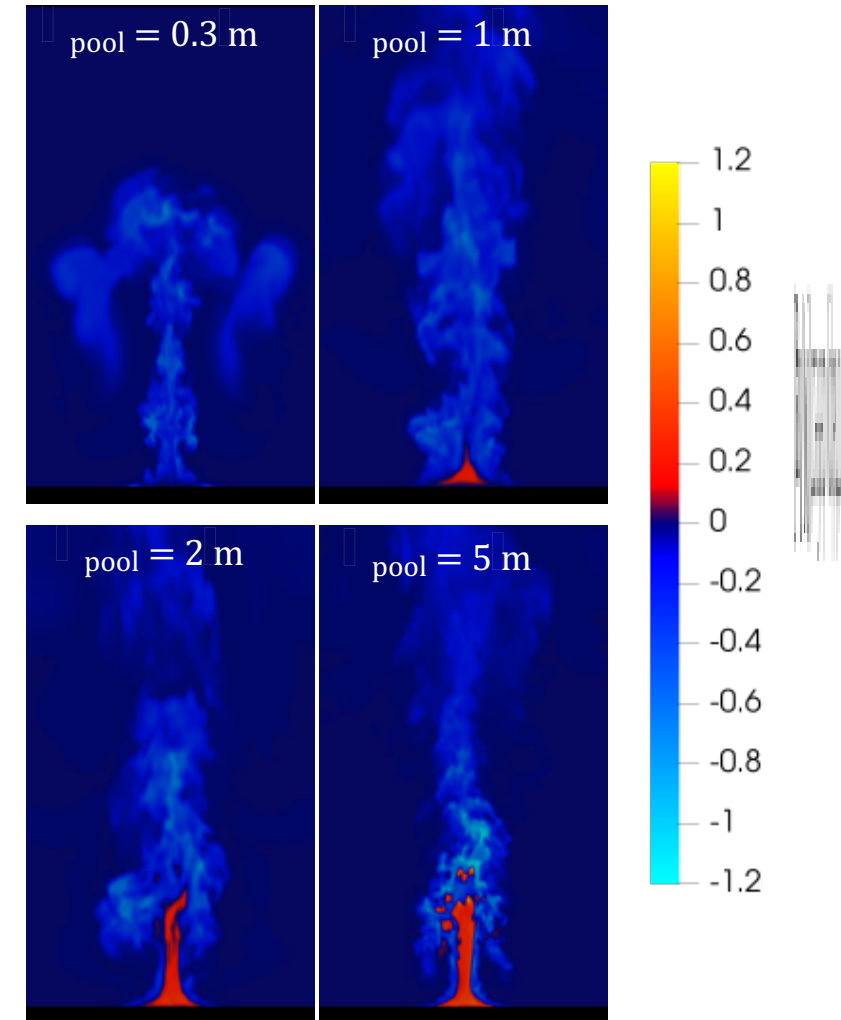
- Scalar dissipation rate decreases with increasing D_{pool}
 - What this indicates:
As D_{pool} is increased, the proportion of the volume that scalar gradients are created is reduced with increasing D_{pool} .
- This results in large, fuel-rich regions where soot formation is controlled by reaction kinetics for large enough D_{pool} .





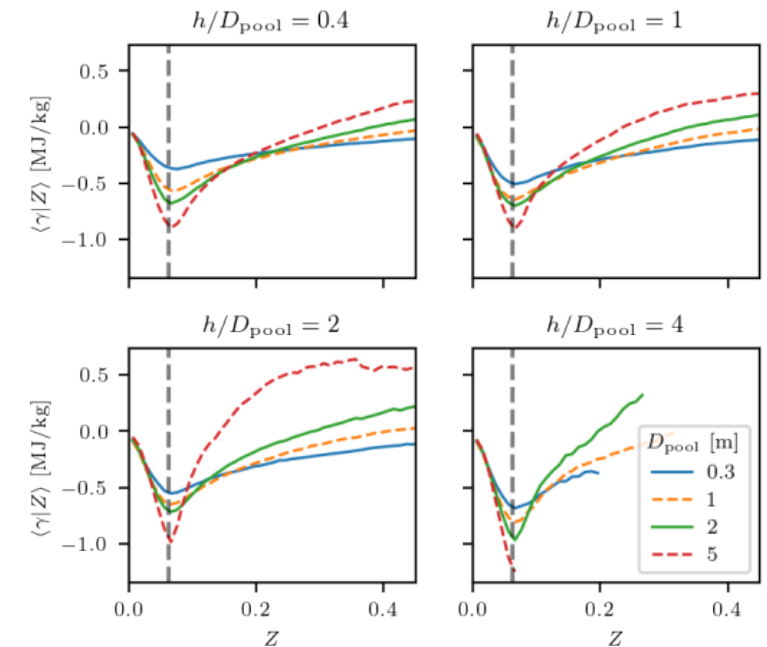
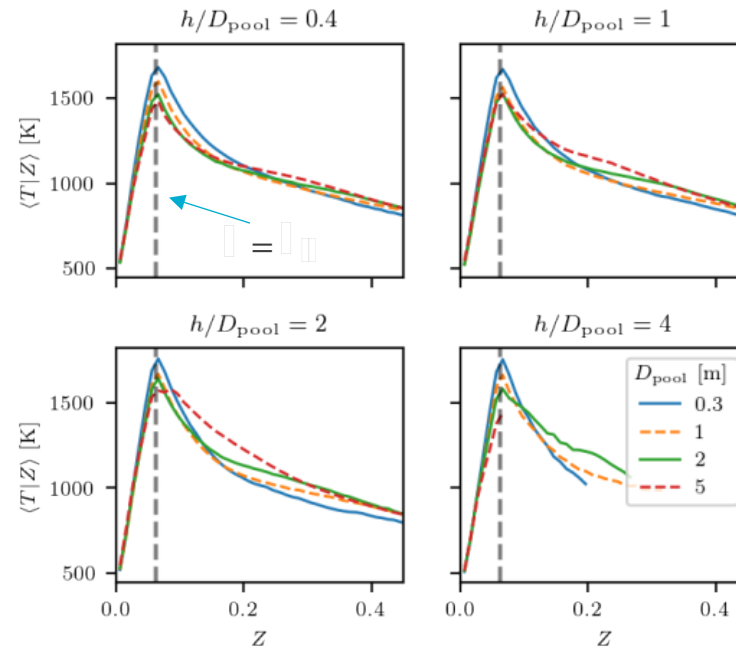
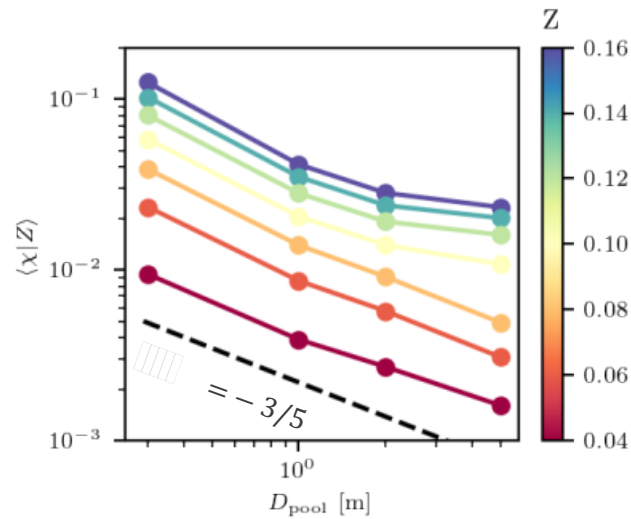
Magnitude of enthalpy defect grows with D_{pool}

- Enthalpy defect = $h - h_{ad}$.
- Sufficiently-large fires exhibit super-adiabatic regions.
 - These regions appear within the interior of the fire.
 - If the fire is large enough, transient superadiabatic regions appear in the upper portion of the flame.





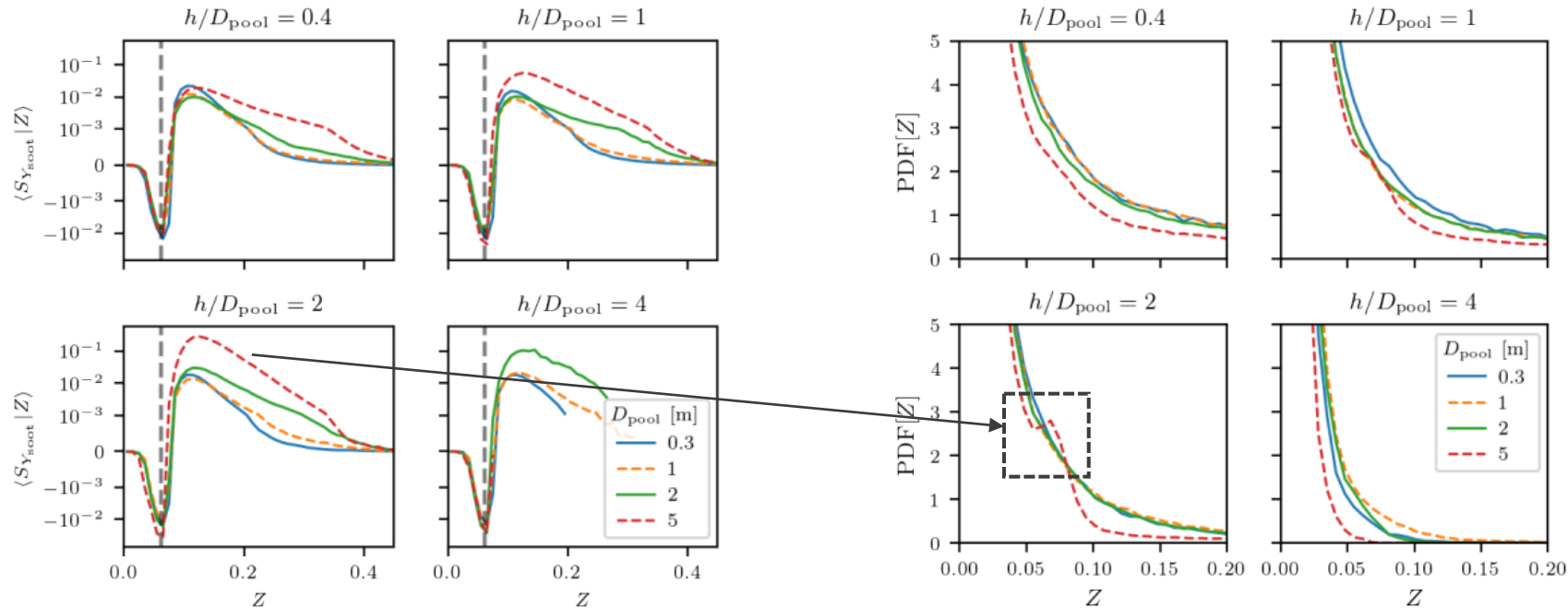
Magnitude of enthalpy defect grows with D_{pool}



- As D_{pool} increases, χ decreases \rightarrow slower mixing .
- Consequently,
 - Lifetime of fuel-rich regions increases allowing for more soot formation
 - Radiation distributes energy from hot regions ($Z \approx Z_{st}$) to cooler sooty, fuel-rich regions.
 - Less mixing of super- and subadiabatic regions.



Behavior of mixture fraction distribution



- $\text{PDF}[Z]$ shifts towards lower values of Z as D_{pool} increases
 - This occurs because total soot production increases W.R.T D_{pool}
- Local max. in $\text{PDF}[Z]$ occurs for $D_{\text{pool}} = 5$ m over a certain range of heights.
 - under rich conditions ($Z > Z_{st}$) soot formation dominates soot oxidation, so a net removal of gaseous fuel occurs which decreases Z , and
 - for lean conditions ($Z < Z_{st}$), soot oxidation is dominant so that mass originating from the fuel is readded to the gas phase which increases Z .



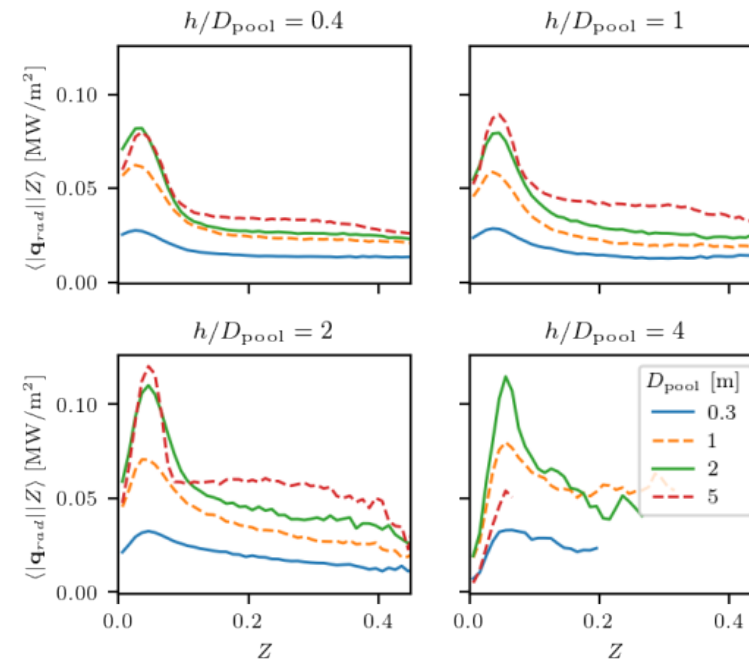
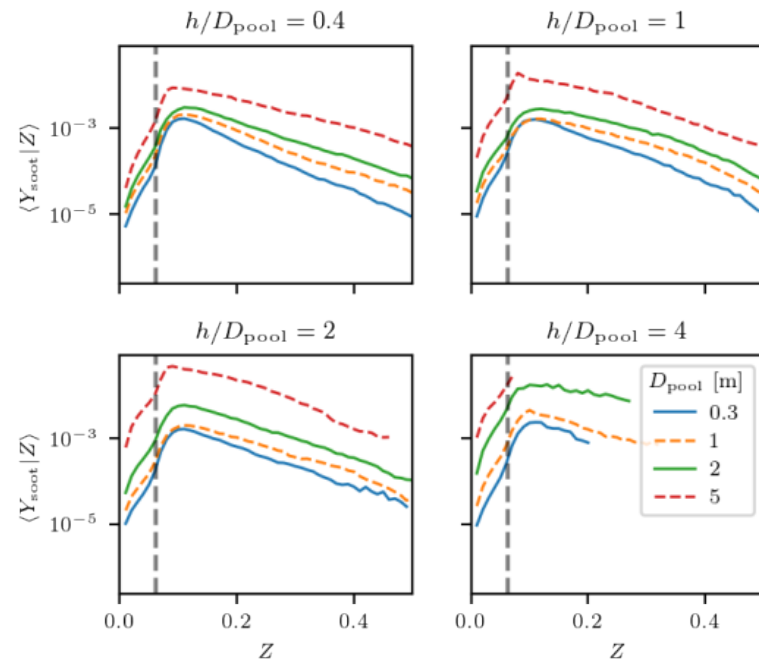
Summary and conclusions



Questions?

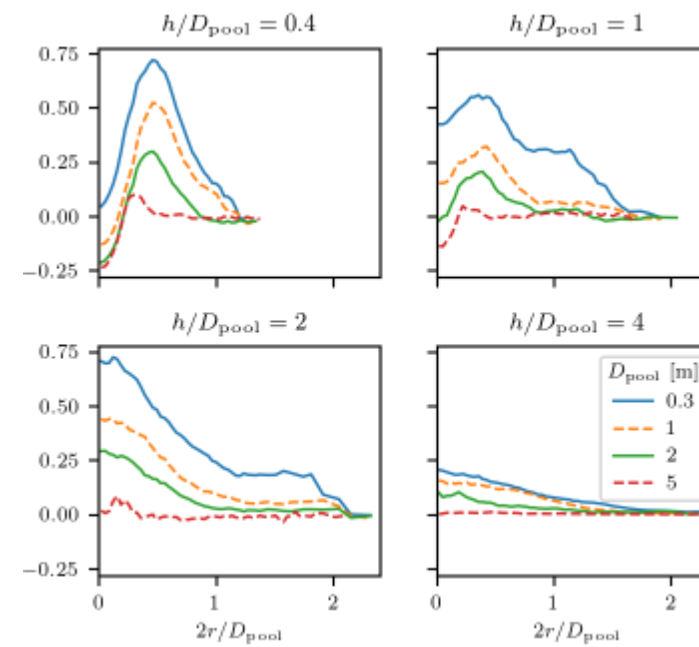
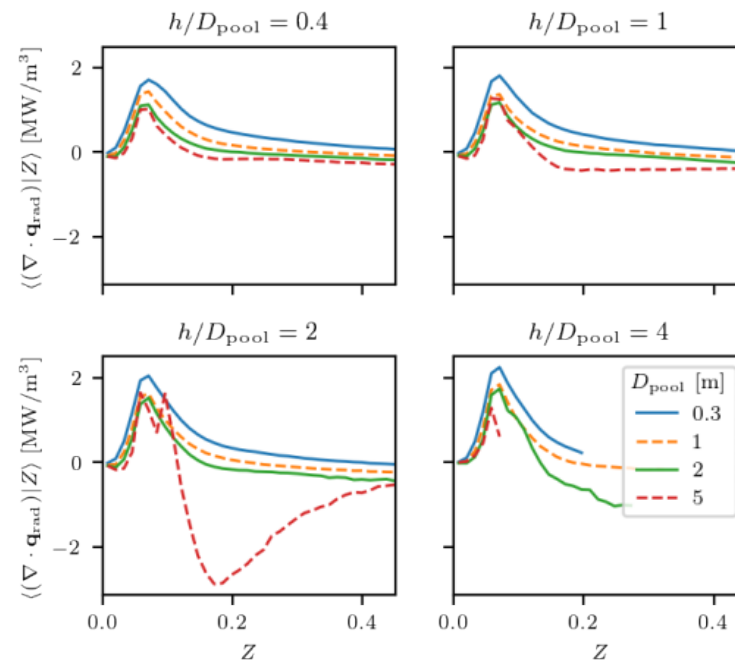


Soot concentration and radiative heat flux vs. mixture fraction



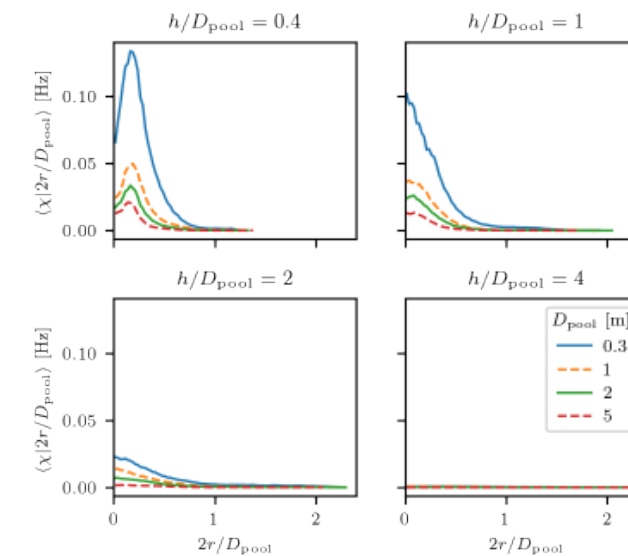
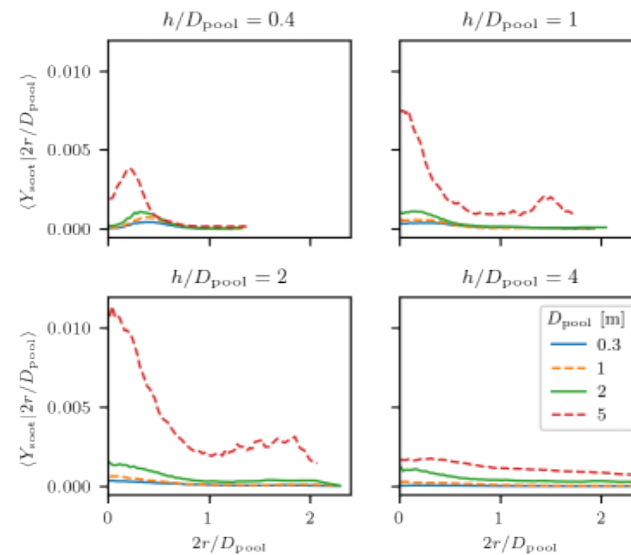
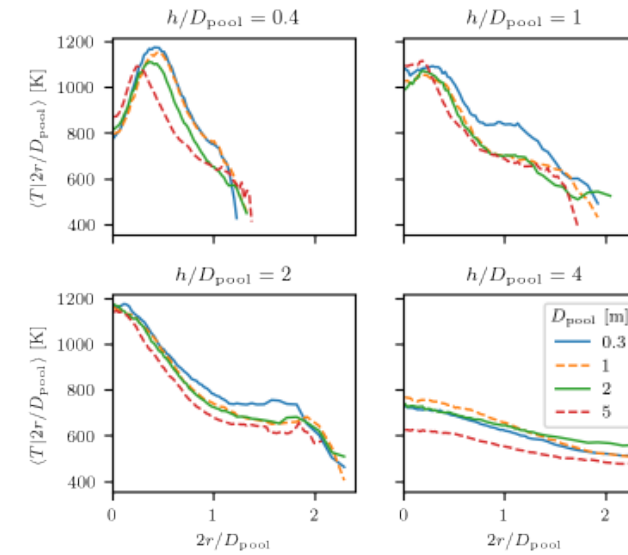
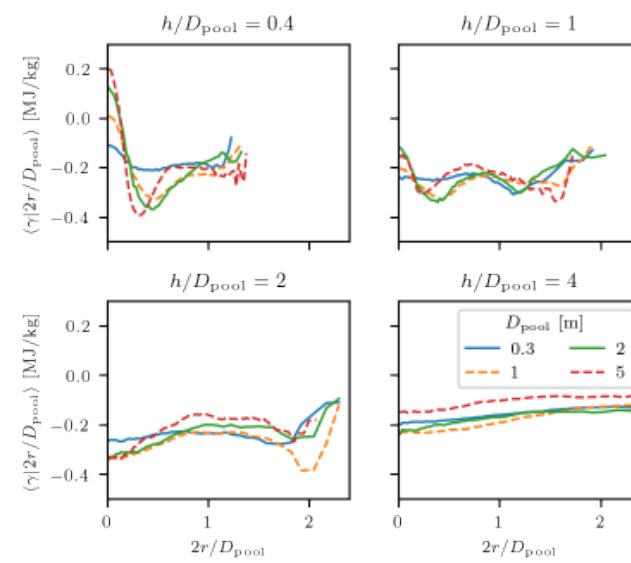


Divergence of radiative heat flux





Enthalpy defect, temperature, soot concentration, and scalar dissipation rate

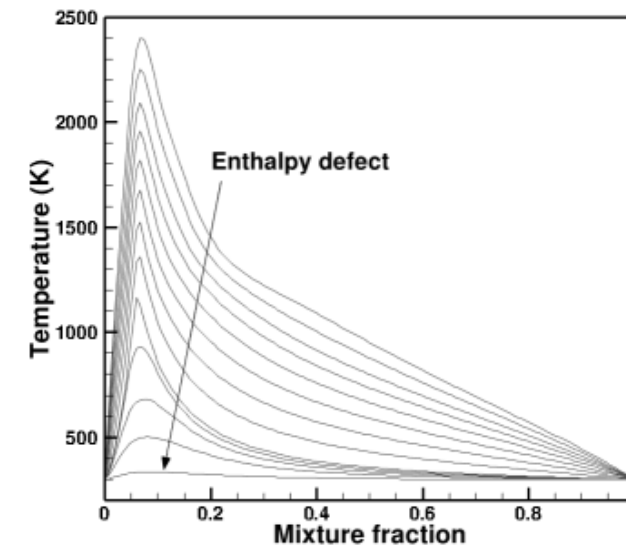
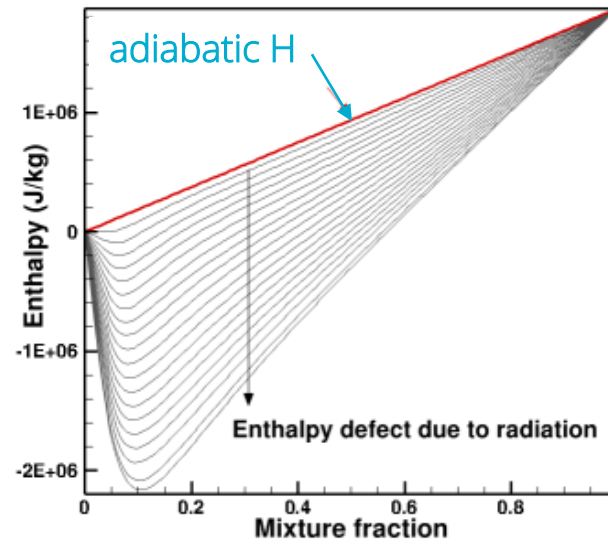
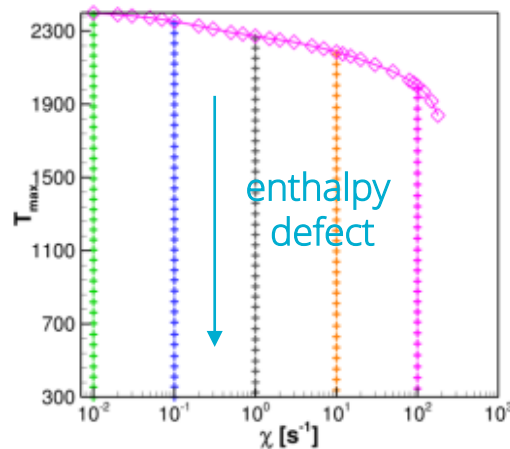




Non-Adiabatic Flamelets



- To allow for radiative quenching and generalize to other heat losses, a new heat-loss term is proposed:
 - Proportional to χ for complete cooling $\frac{\partial H}{\partial t} + \frac{\chi}{2} \frac{\partial^2 H}{\partial Z^2} = h_0 \chi \left[\frac{T(H, Z) - T_\infty}{T_{max} - T_\infty} \right]$
 - Linear in temperature temperature: better off-stoich coverage
- With the larger sink term, flame cools down to ambient T
- This is 'cooled product', not reactants mixing
- Enthalpy defect γ is introduced $\tilde{\gamma} = \tilde{H} - \widetilde{H}_{ad}$ $\widetilde{H}_{ad} = H(0) + [H(1) - H(0)] \tilde{Z}$



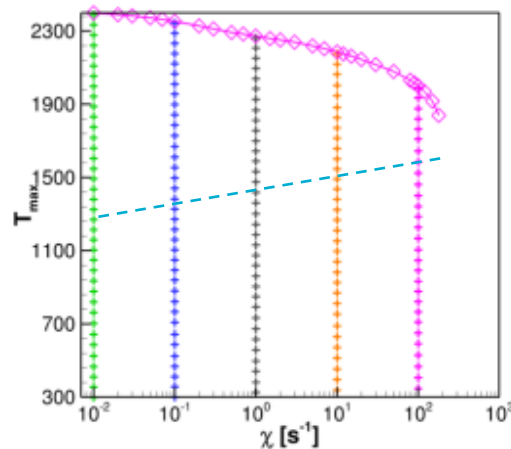


Unsteady flamelet cooling

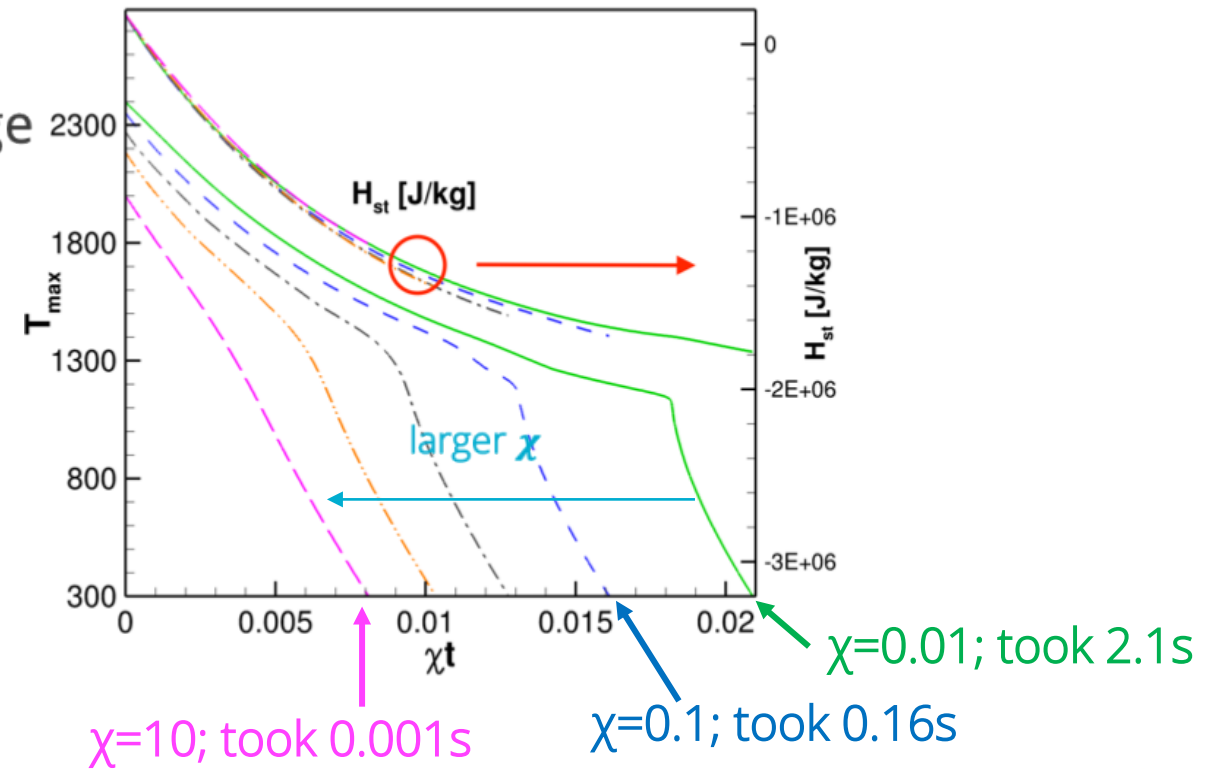
- **Heat loss and heat release both scale by χ .**

- Normalize by $(T_{max} - T_o)$ to retain the same magnitude with time.

- Timescale matches estimated enthalpy response time
- O(0.1-1s) for complete cooling at lower χ range
- Max temp falls faster below unstable middle branch.



$$\frac{\partial H}{\partial t} + \frac{\chi}{2} \frac{\partial^2 H}{\partial Z^2} = h_0 \chi \left[\frac{T(H, Z) - T_\infty}{T_{max} - T_\infty} \right]$$

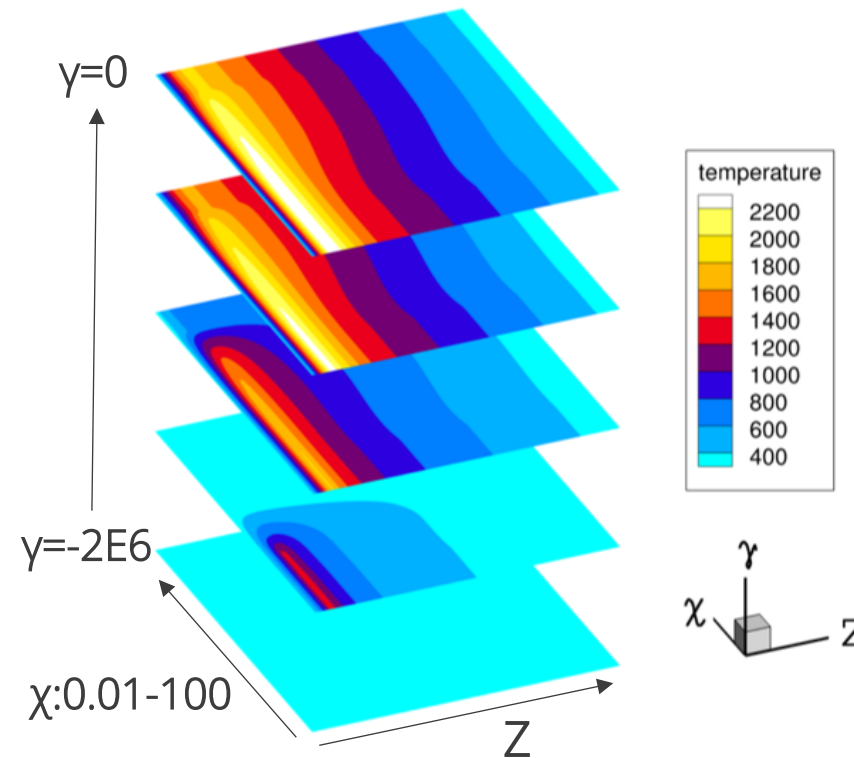
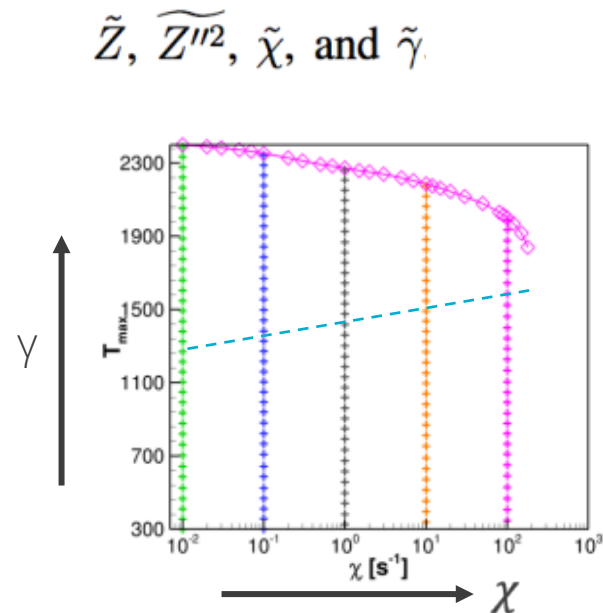




Tabulation

- Tabulation of χ -based enthalpy defect approach is preferred for fire and similar scenarios over progress variable approach.
- Progress variable predicts ignition delay, local quenching/re-ignition for fast mixing.
- No heat losses are associated with progress variable decrement.
- χ is orthogonal to y .

Sub-filter PDF applied to the mixture fraction: results in 4-d table





Tabulation – orthogonal transformation



To generate structured table, presumed form of $\gamma(Z)$: $\gamma = \gamma_o F_\gamma(Z, Z_o) = \begin{cases} \frac{Z}{Z_o} & : Z \leq Z_o \\ \frac{1-Z}{1-Z_o} & : Z > Z_o \end{cases}$

- Extract table location from convolved form, F .
- Store results in B-splines.
- Logarithmic spacing for \widetilde{Z}''^2

$$\gamma_o = \frac{\widetilde{\gamma}}{\int_0^1 F_\gamma(Z, Z_o) p_Z(\widetilde{Z}, \widetilde{Z}''^2) dZ}$$

