



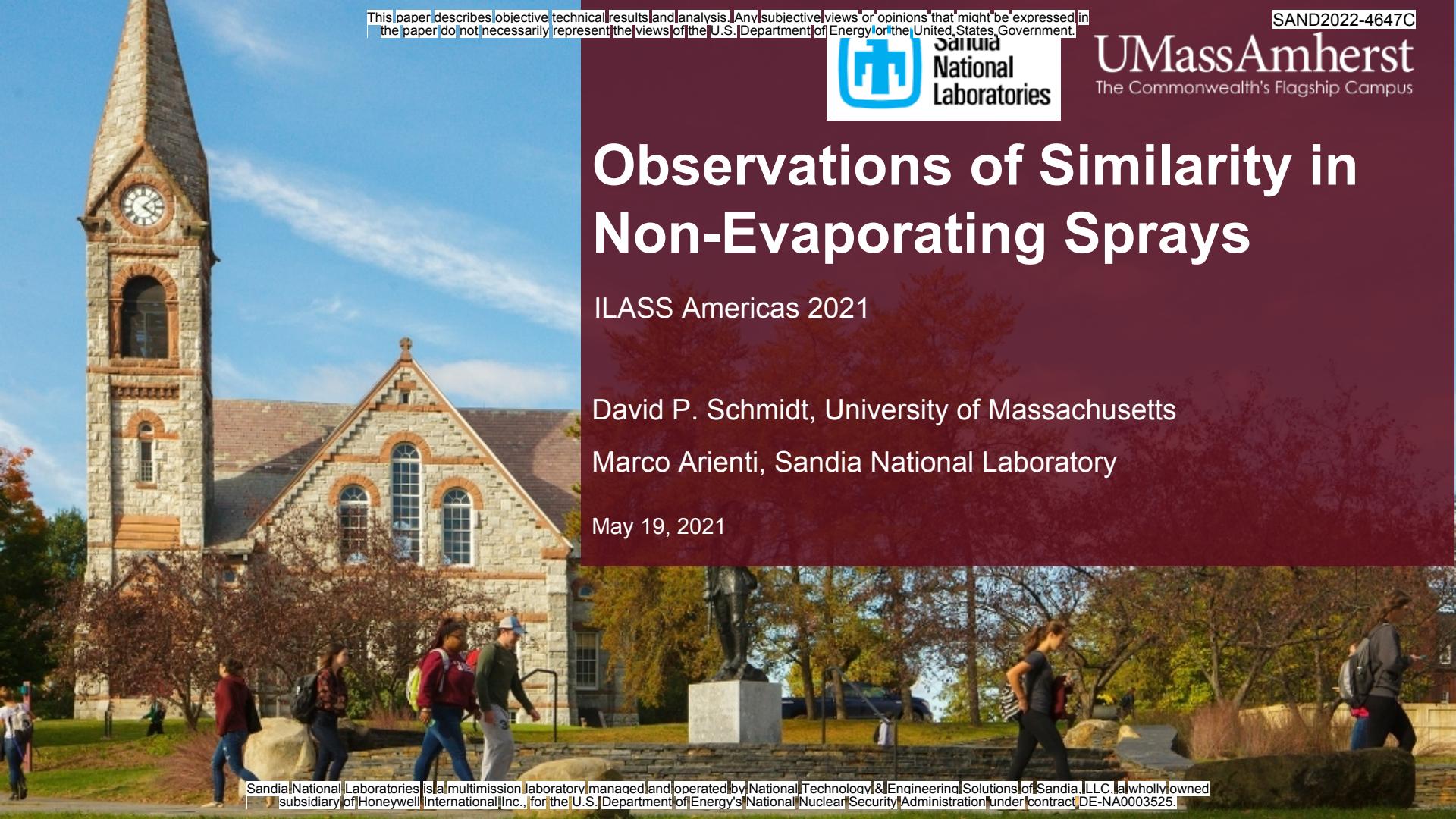
Observations of Similarity in Non-Evaporating Sprays

ILASS Americas 2021

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May 19, 2021

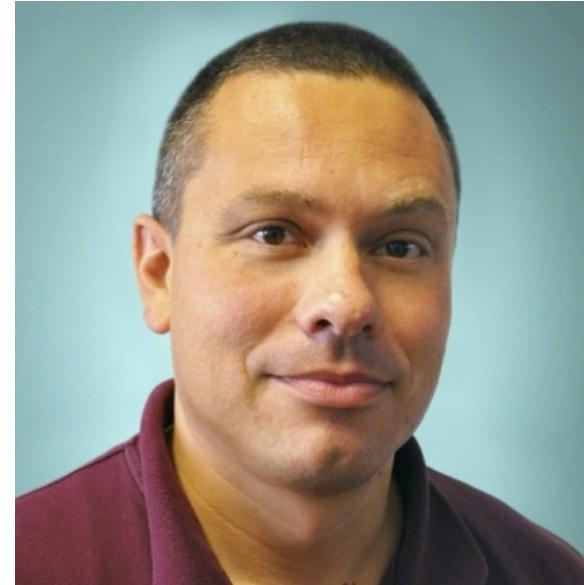


Your Friendly, Yet Remote Authors:

UMassAmherst



Prof. David P. Schmidt



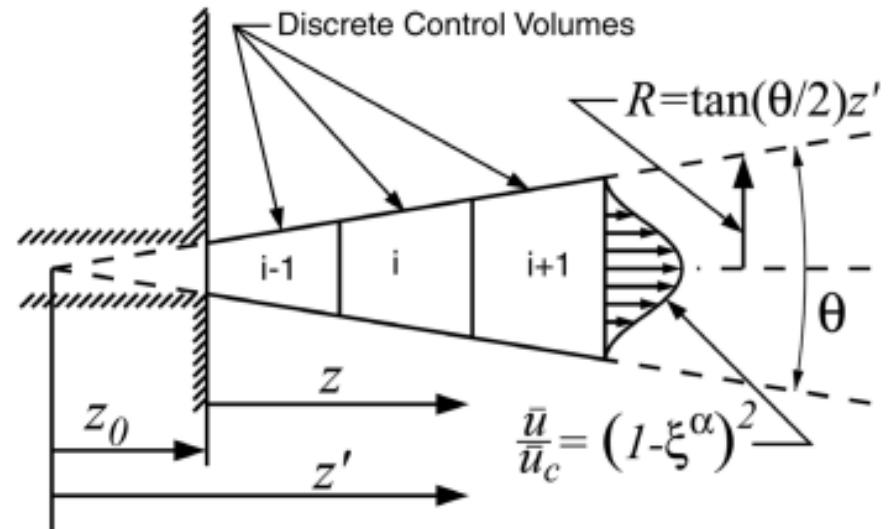
Dr. Marco Arienti

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- Some aging may have occurred since these photos were taken. It couldn't be helped.

Overview

- Examination of a 1-D model reveals a mathematical surprise
- Comparison to DNS for reality check
- Plaintive whine for experimental data



From Musculus & Kattke, 2009

Motivation

- The yield of what you get/what it costs you is excellent
- Basic physics are much more accessible than CFD
- Basis for a CFD model (ELMO)



Homer Simpson image used with permission of the producer's nephew

Assumptions



- Liquid and gas share so much interfacial area, that they move at the same velocity
- Liquid volume fraction and velocity both share the same radial profile (unity Schmidt number)
- Constant densities
- Non-evaporating
- Constant spray angle

Equations for Mass and Momentum



- Overbars indicate time and radial average

$$\beta = \frac{1}{\bar{X}_f \bar{u}} \int X_f u dA$$

- Beta is a parameter representing the correlation of LVF and velocity

$$m_{f,i}^{t+1} = m_{f,i}^t + \rho_f \left[(\beta \bar{X}_f \bar{u} A)_{i-1}^t - (\beta \bar{X}_f \bar{u} A)_i^t \right] \Delta t \quad (11)$$

- Momentum should, strictly, have a triple correlation

$$M_i^{t+1} = M_i^t + \left[(\beta \bar{\rho} \bar{u}^2 A)_{i-1}^t - (\beta \bar{\rho} \bar{u}^2 A)_i^t \right] \Delta t \quad (12)$$

Surprising result



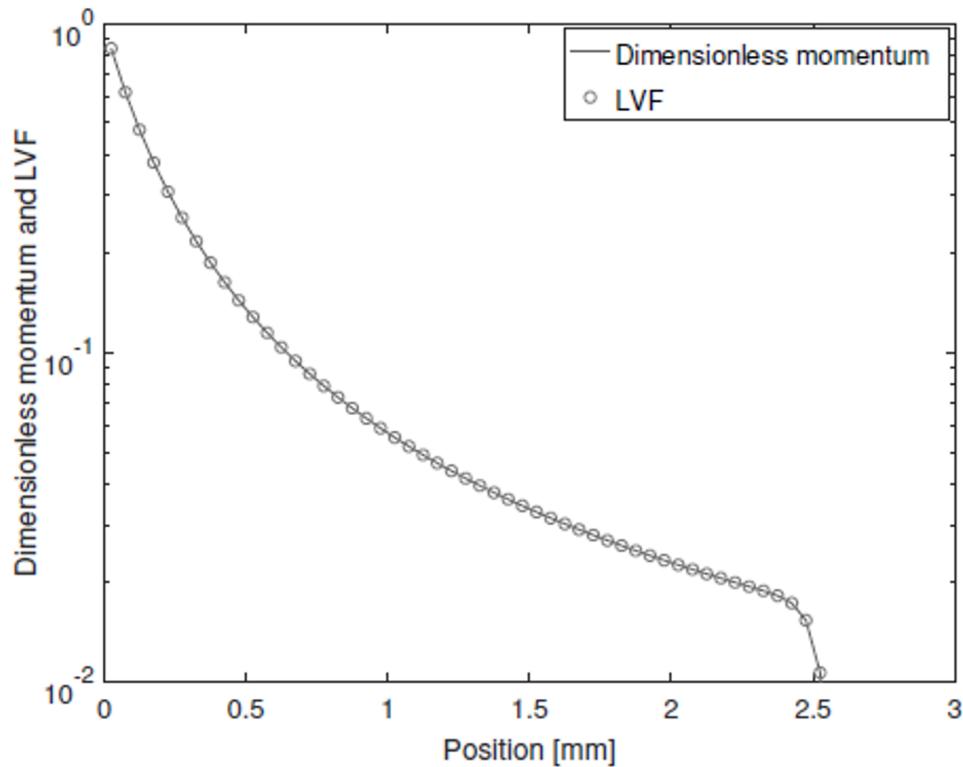
- Change variable to replace velocity with dimensionless *two-phase* momentum
- Take limit as time step and cell size go to zero
- Two-phase momentum is proven equal to LVF via similarity
- True for all times and axial distances

$$L^* \equiv \frac{\bar{\rho}\bar{u}}{\rho_l u_{inj}}$$

$$\bar{X}_f = L^*$$

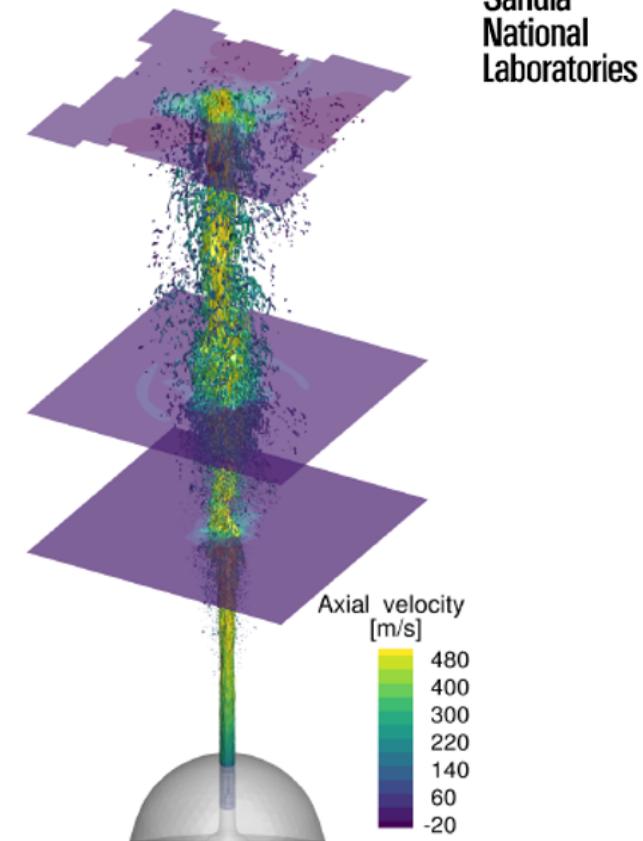
Verification

- Ran publically-available Musculus-Kattke code
- Snapshot at 0.01 ms ASOI



How do we validate this?

- Need both mass based diagnostics for LVF and velocity
- Not usually made for the same spray at the same location
- DNS is our only hope

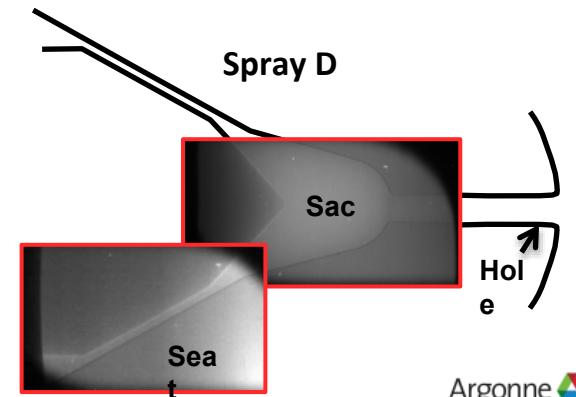


The interface-capturing code

CSLVOF

In collaboration with FSU and the LBNL AMReX co-design center

- Sharp-interface discretization of multi-phase Navier-Stokes eqns. with Moment of Fluid interface representation [1].
 - ✓ Fully compressible formulation [2]
 - ✓ Non-conformal moving wall boundaries
 - ✓ Adaptive Mesh Refinement (AMReX)
 - ✓ Large Eddy Simulation (WALE)
 - ✓ Cavitation [3] and surface evaporation [4]
- Injector surfaces are reconstructed from X ray radiography and converted into level set representation



[1] Jemison, et al., J. Sci. Comput. 54(2-3) (2013) 454-491.

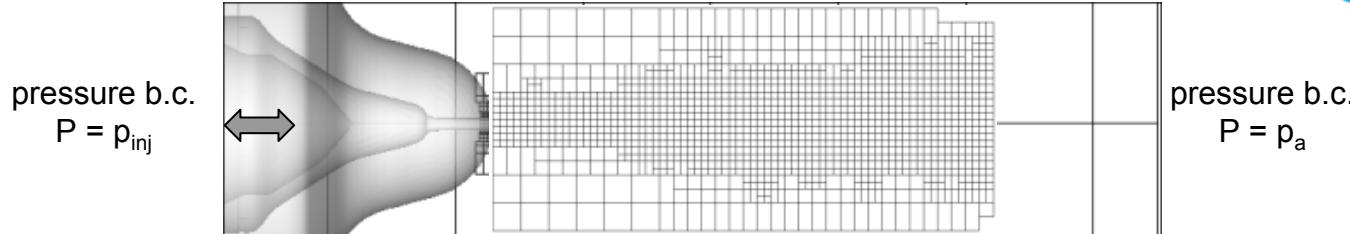
[2] Jemison, Sussman, Arienti, J. Comput. Phys., 279, (2014) 182-217.

[3] Arienti et al., Proceedings of the Combustion Institute 2021.

[4] Wenzel and Arienti, Proceedings of the 31st ILASS-Americas, May 2021.

Validation case: Spray D, served cold

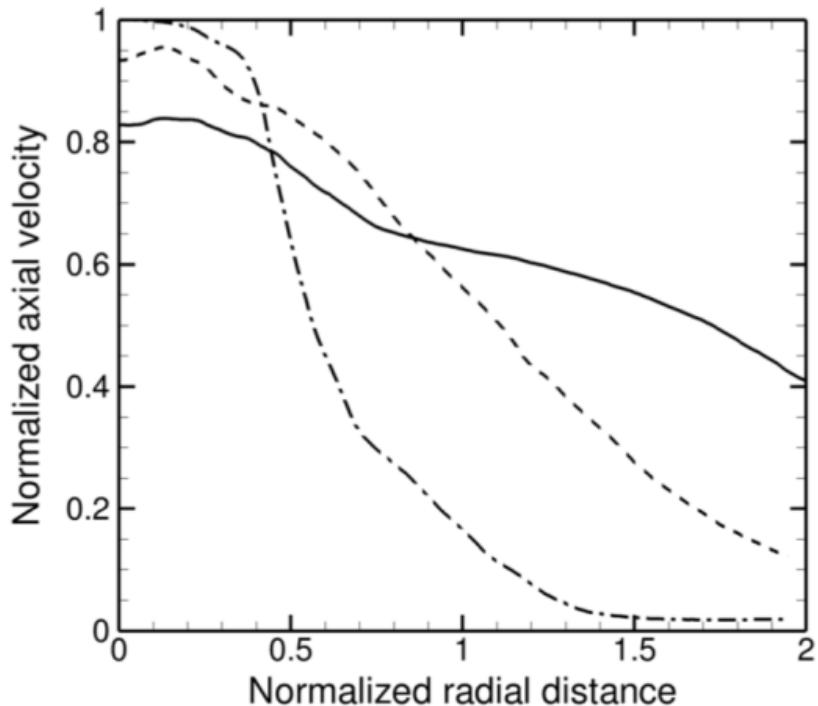
3D domain (3.6 x 3.6 x 15.6 mm) with AMR, Δx min = 2.5 μm



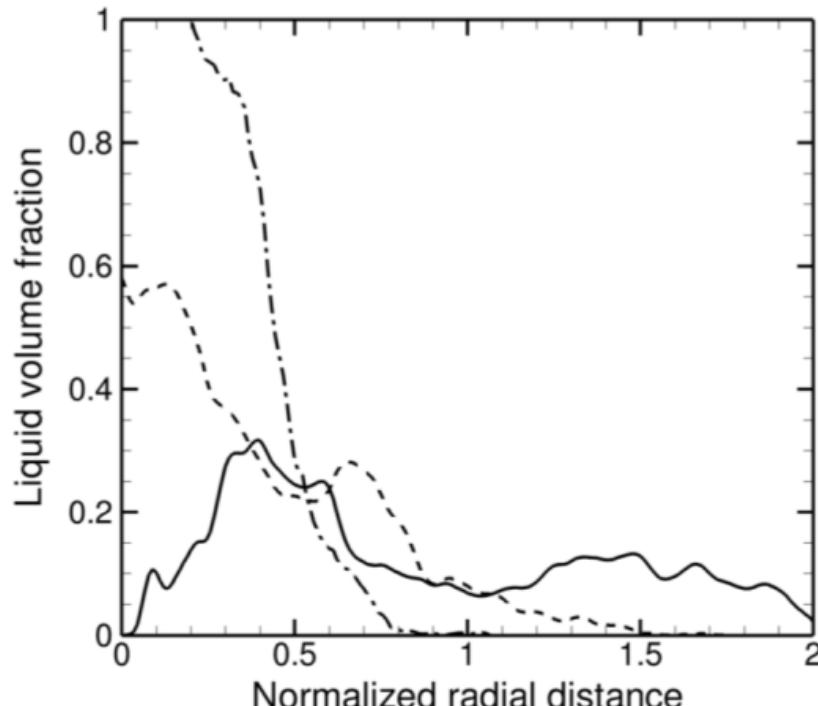
| Geometry | Nominal | SCC Cold Conditions | | External flow (from simulation) | |
|------------------------|-------------------|---------------------|------------------------|---------------------------------|----------------------------|
| Nozzle Outlet Diameter | 186 μm | Fuel | n-dodecane | Mass flow rate | $10.2 \pm 0.4 \text{ g/s}$ |
| Nozzle K-Factor | 1.5 | Injection Pressure | 1000 bar | Momentum flow rate | $5.06 \pm 0.3 \text{ N}$ |
| Nozzle L/D | --- | Fuel Temperature | 300 K | C_v | 0.967 ± 0.026 |
| | | Ambient Temperature | 300 K | C_d | 0.946 ± 0.036 |
| | | Ambient Density | 22.8 kg/m ³ | | |

- Time averaged profiles at 7.8, 19, and 58 diameters downstream

Axial w/w_{MAX}

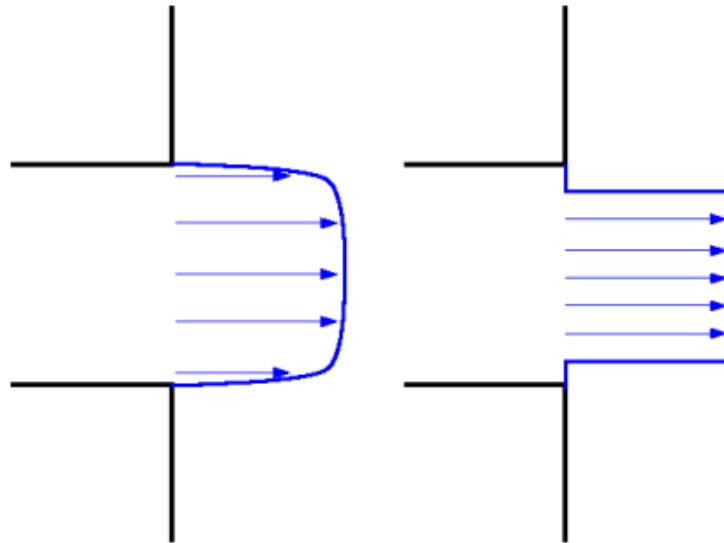


Liquid volume fraction

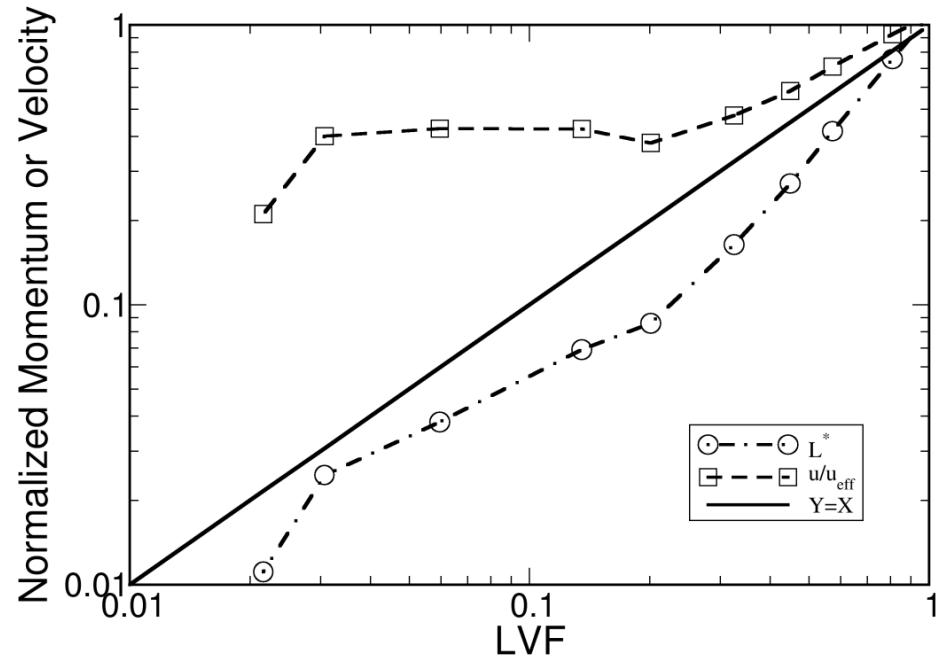
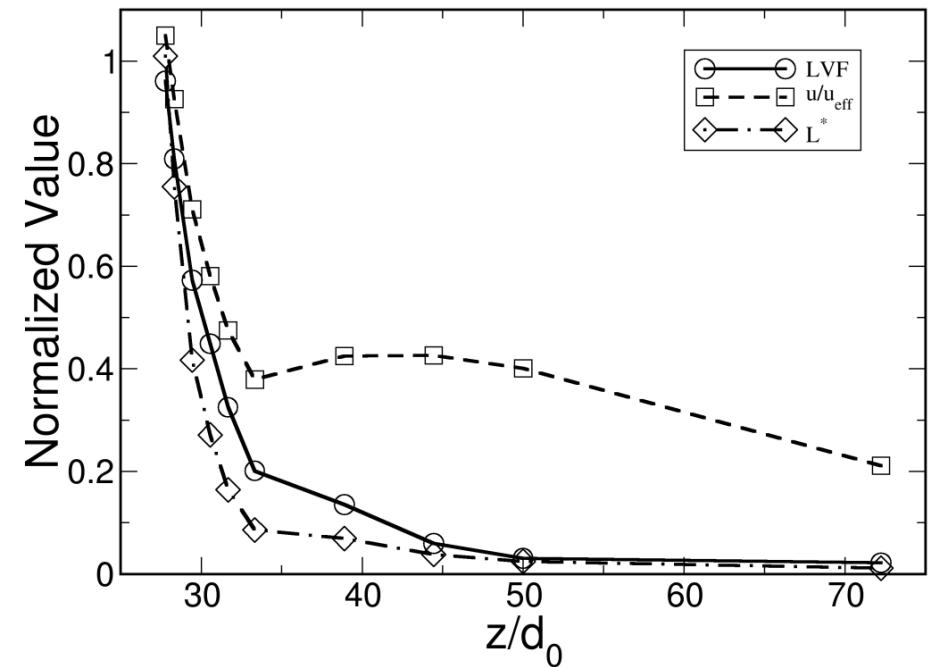


Caveats

- For extracting from DNS, assume half angle of 5.2 degrees
 - Velocity profiles are wider than LVF
- Analysis requires a single uniform orifice exit velocity
 - Use Ca , Cv
- Time averaging is over a relatively short time



Do the Analysis and DNS Agree?



- Transverse integrated, time-averaged results

Conclusions



- Analysis of a 1-D model indicates that two-phase momentum (not just liquid) is similar to LVF
- DNS simulations are supportive, but not conclusive

Future work



- Longer time-averaging
- Investigate transverse profile shapes
- Compare with Kastengren et al.'s assertion that mass-averaged velocity is proportional to transverse integrated mass
- Formalize details of transverse integration area

Acknowledgements



Sandia
National
Laboratories

Support by the Spray Combustion Consortium of automotive industry sponsors, including Convergent Science Inc., Cummins Inc., Ford Motor Co., Hino Motors Ltd., Isuzu Motors Ltd., Groupe Renault, and Toyota Motor Co., is gratefully acknowledged.

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Questions?

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