

Why Low Humidity is Detrimental to Stainless Steel in Marine Atmospheres

E.J. Schindelholz¹, J. Srinivasan¹, A.M. Parey^{1,2}, A.W. Knight², R.F. Schaller², and J.S. Locke¹

¹Fontana Corrosion Center, The Ohio State University, Columbus, OH

²Sandia National Laboratories, Albuquerque, NM

Acknowledgements

Sandia

Charles Bryan (geochemistry, UFD)

Carlos Jove-Colon (geochemistry)

Tony Ohlhausen (surface science)

Philip Noel (tomography)

Remi Dengreville (modeling)

Ryan Katona, PhD student (now
postdoc)

Chris Alexander, postdoc (now USF)

Hai-Duy Nguyen, UNM undergrad intern

Nicholas Kemp, UNM undergrad intern

Jacob Carpenter, UNM undergrad intern

TJ Montoya, UNM undergrad intern

Jason Taylor, technologist

OSU

Jerry Frankel

Tim Weirich, MS student (now Battelle)

UVA

Rob Kelly

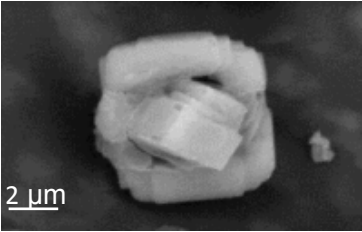
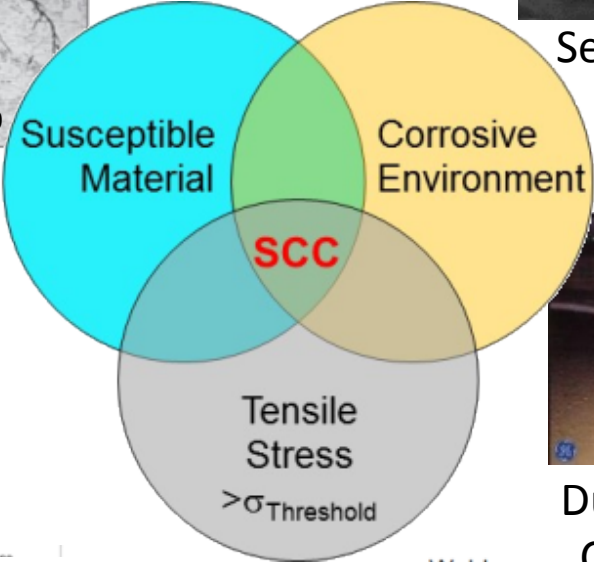
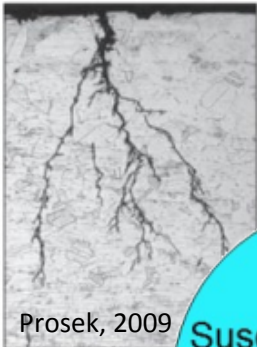
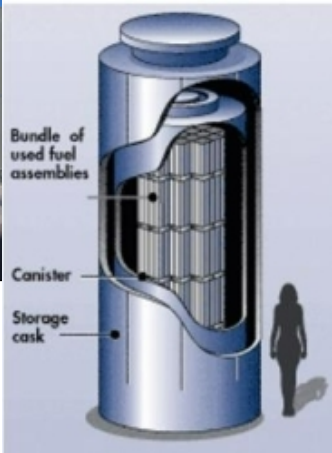
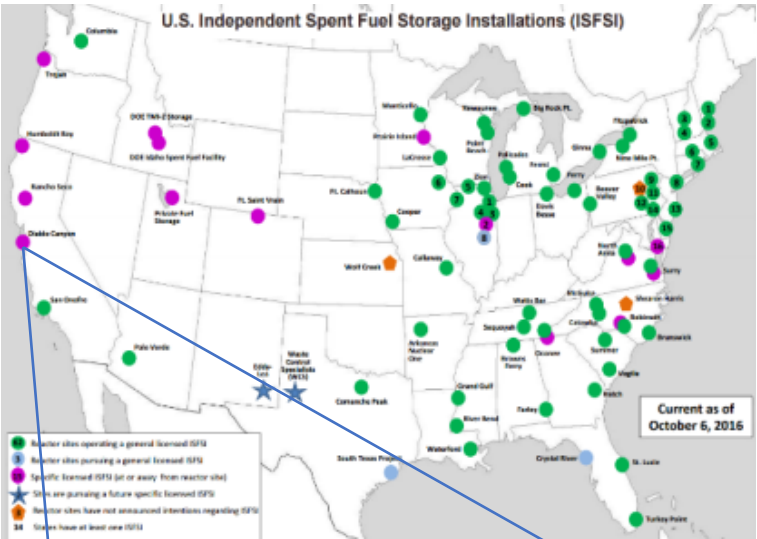


U.S. DEPARTMENT OF
ENERGY

Office of
NUCLEAR ENERGY



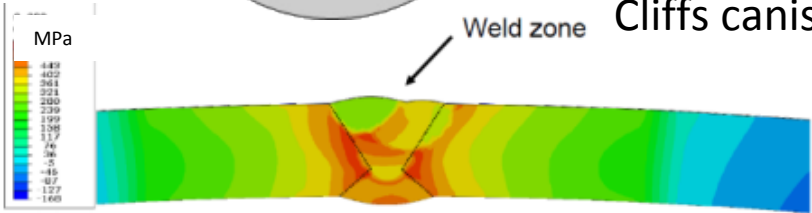
Motivation: SCC Risk of Spent Fuel Dry Storage Canisters



Sea-salt particle on Diablo Canyon canister



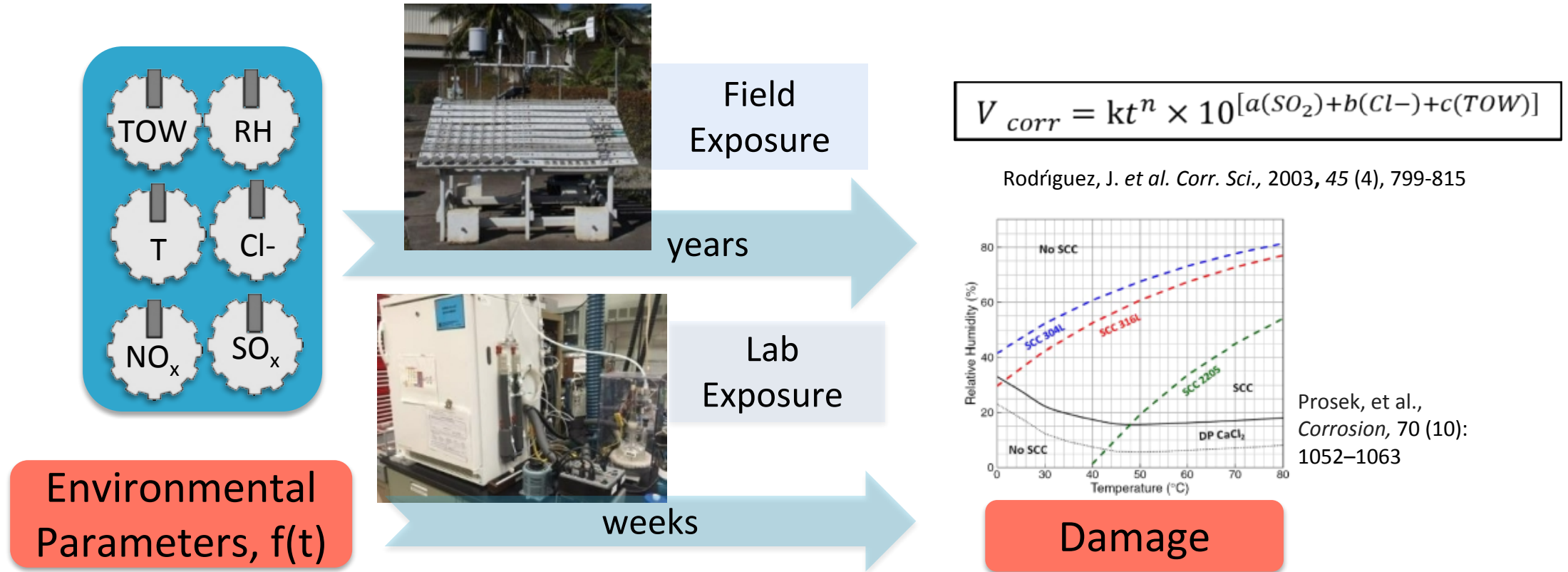
Dust on Calvert Cliffs canister



NRC, 2013

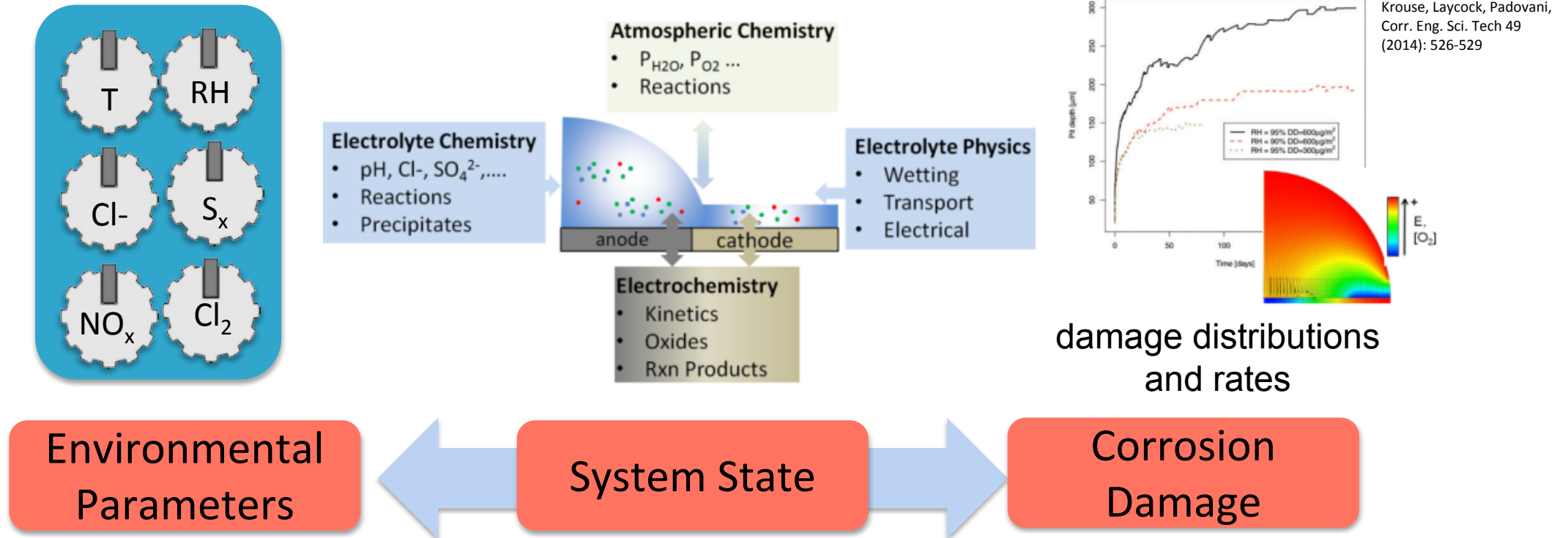
Assessing Risk: Empirical/Probabilistic Approach

At what rate and to what extent will corrosion damage propagate?



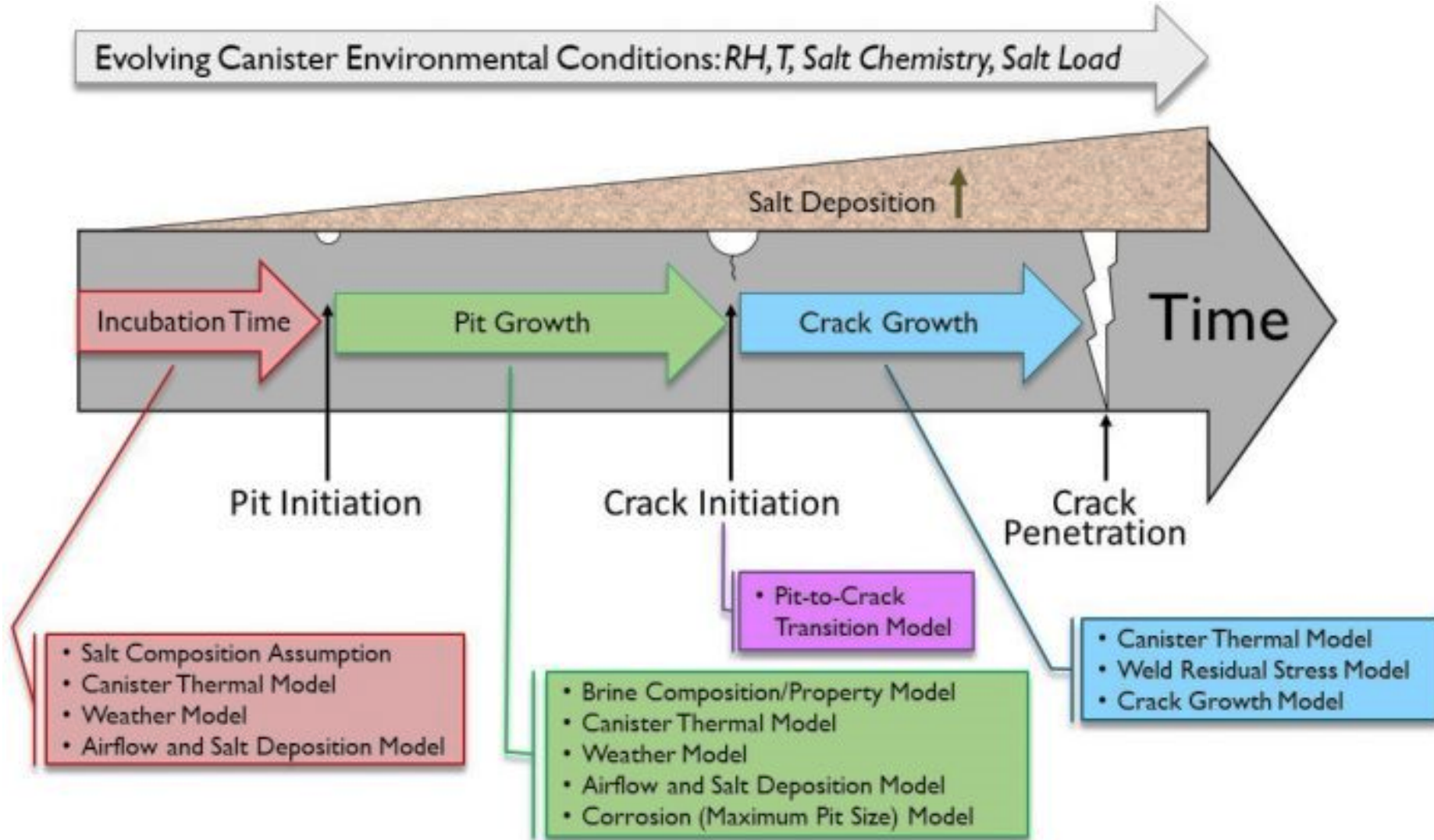
limited prediction capability, mechanistic insight lacking; development of realistic accelerated tests and predictive models is a grand challenge

Opening the Black Box: A Deterministic Approach

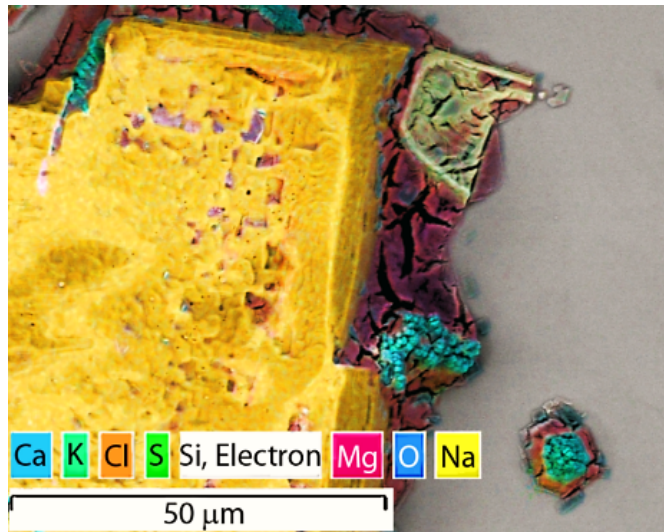


Foundational challenge inhibiting fundamental understanding is the limited ability to directly probe surface environment and corrosion processes

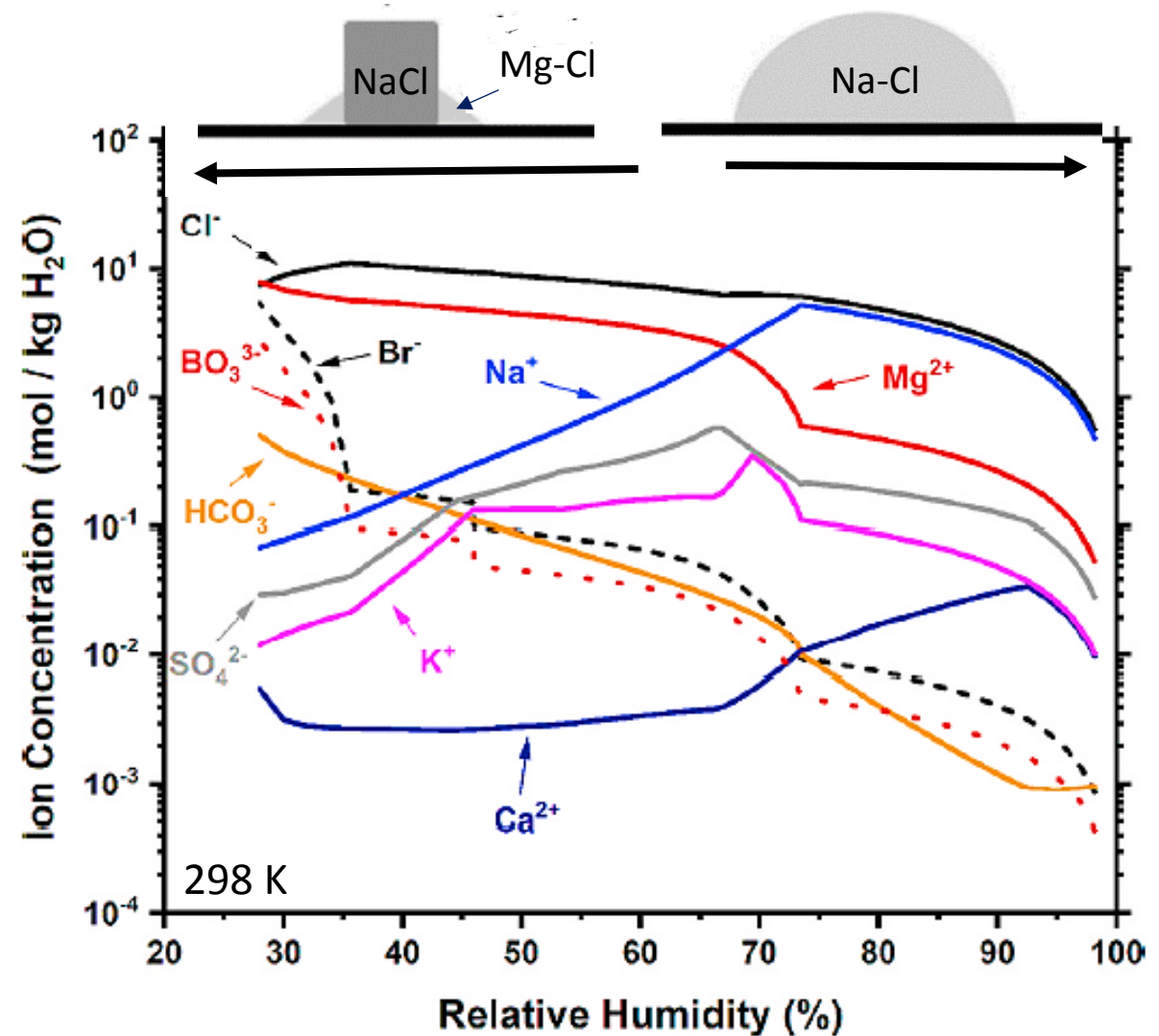
Integrated Deterministic/Probabilistic Model Concept for Canister SCC



Sea Salt Brine Chemistry and Properties $f(RH, T)$



Schindelholz, E.J., Risteen, B.E., Kelly, R.G., J.
Electrochem. Soc. (2014): C450



Bryan, C.R. and Schindelholz, E.J., SAND 2017-11231

Higher Chloride (lower humidity) Increases Pitting Susceptibility

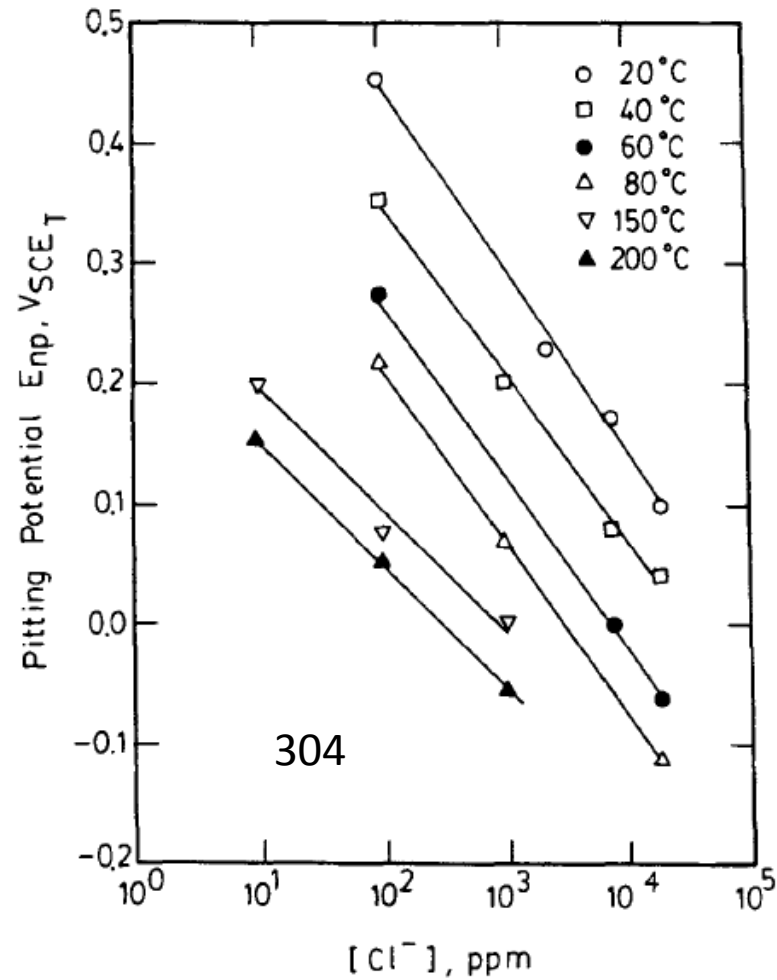
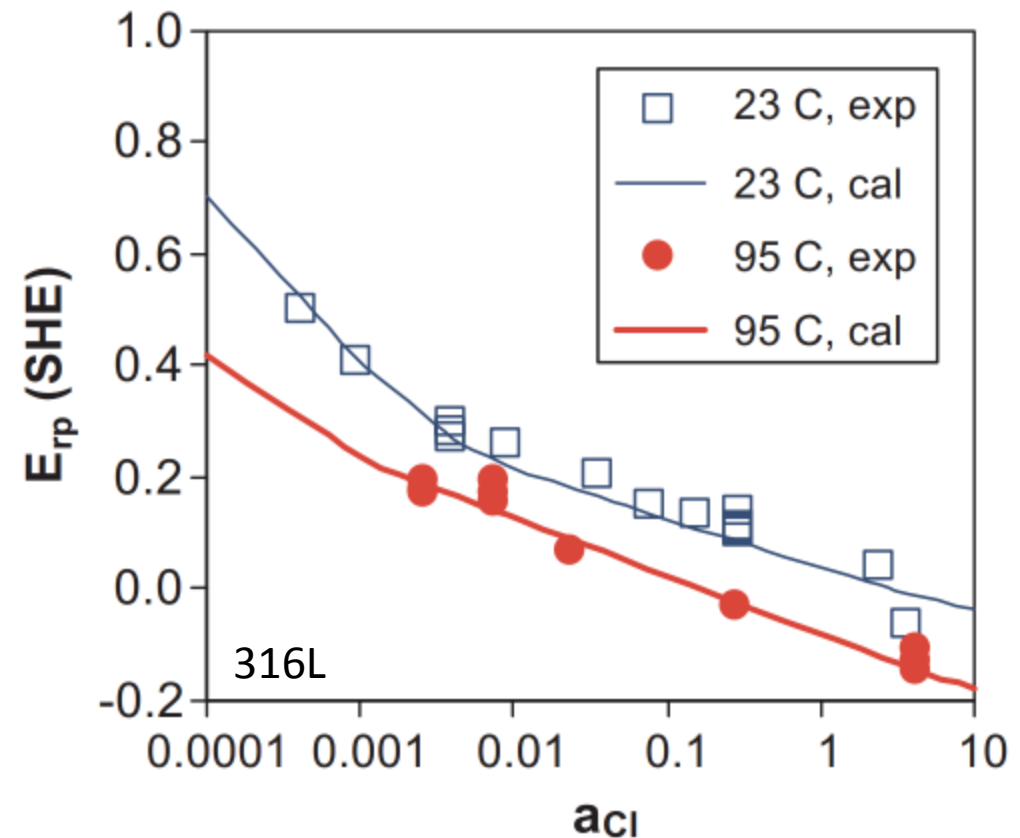


FIGURE 1. Pitting potential vs log Cl^- concentration in aerated solutions at various temperatures.



Lower Humidity (higher chloride) increases SCC Susceptibility

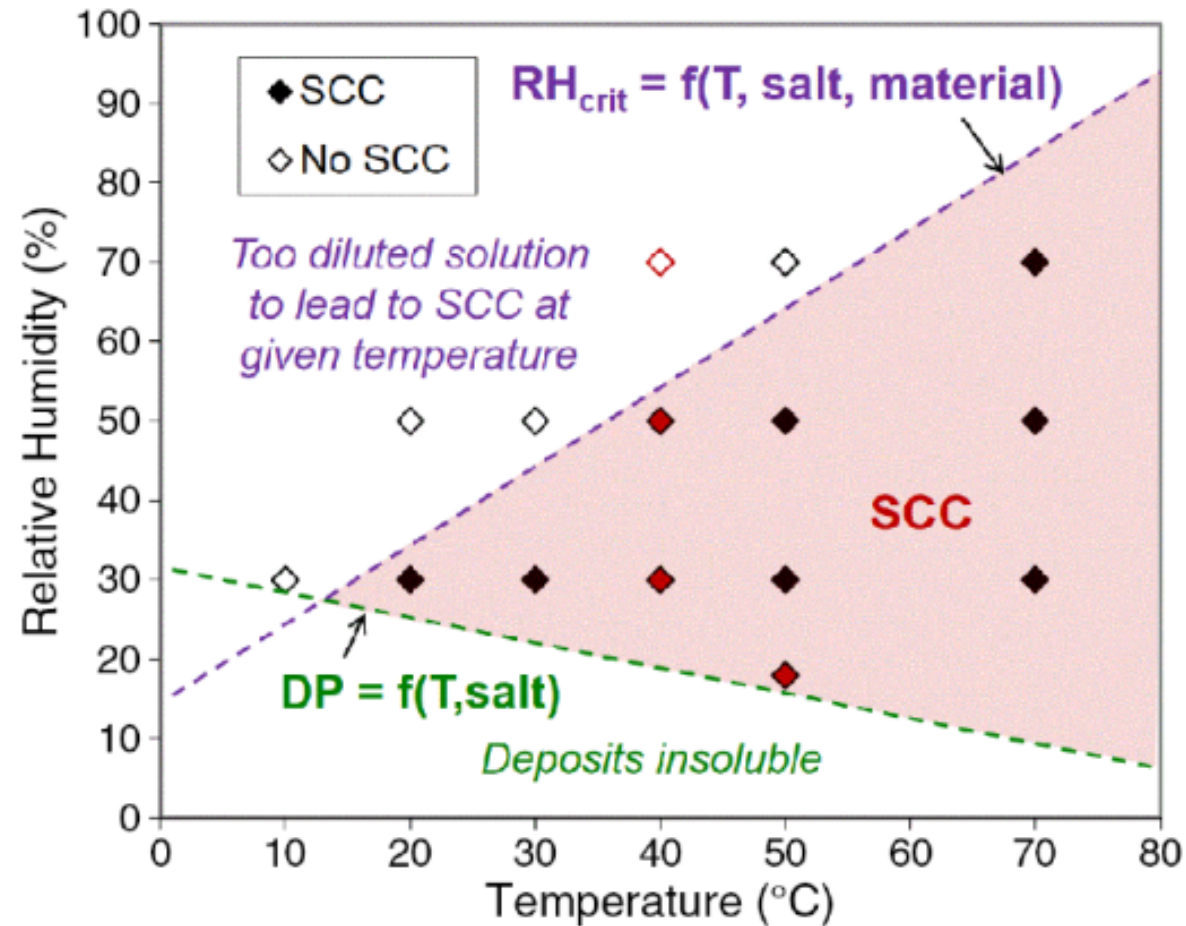
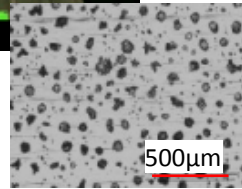
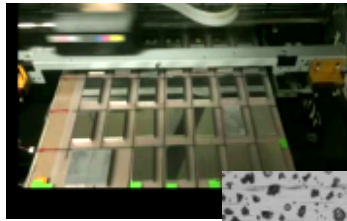


FIGURE 14. Schematic presentation of RH limits for SCC initiation.

Pitting Kinetics and Damage Distributions: Baseline Data

Salt Load
120 grit finish 304H SS
coupons



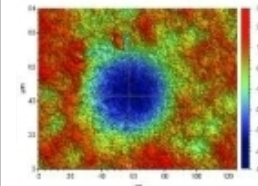
300µg/cm²
ASTM D-1141
sea salt

Expose

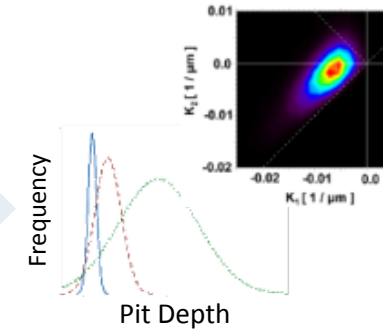
RH %	Temperature (°C)			
76	35			
70	35			
65	35			
60	35			
55	35	40		
50	35	40		
45	35	40	45	
40	35	40	45	
35	35	40	45	50
30	35	40	45	50

Duration: 1 week to 2 years

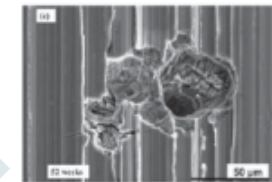
Post-Exposure Analysis



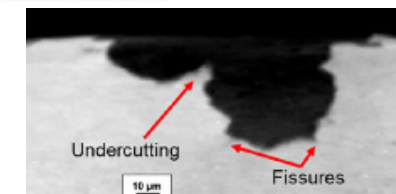
Profilometry



Pit Size and Shape
Distributions

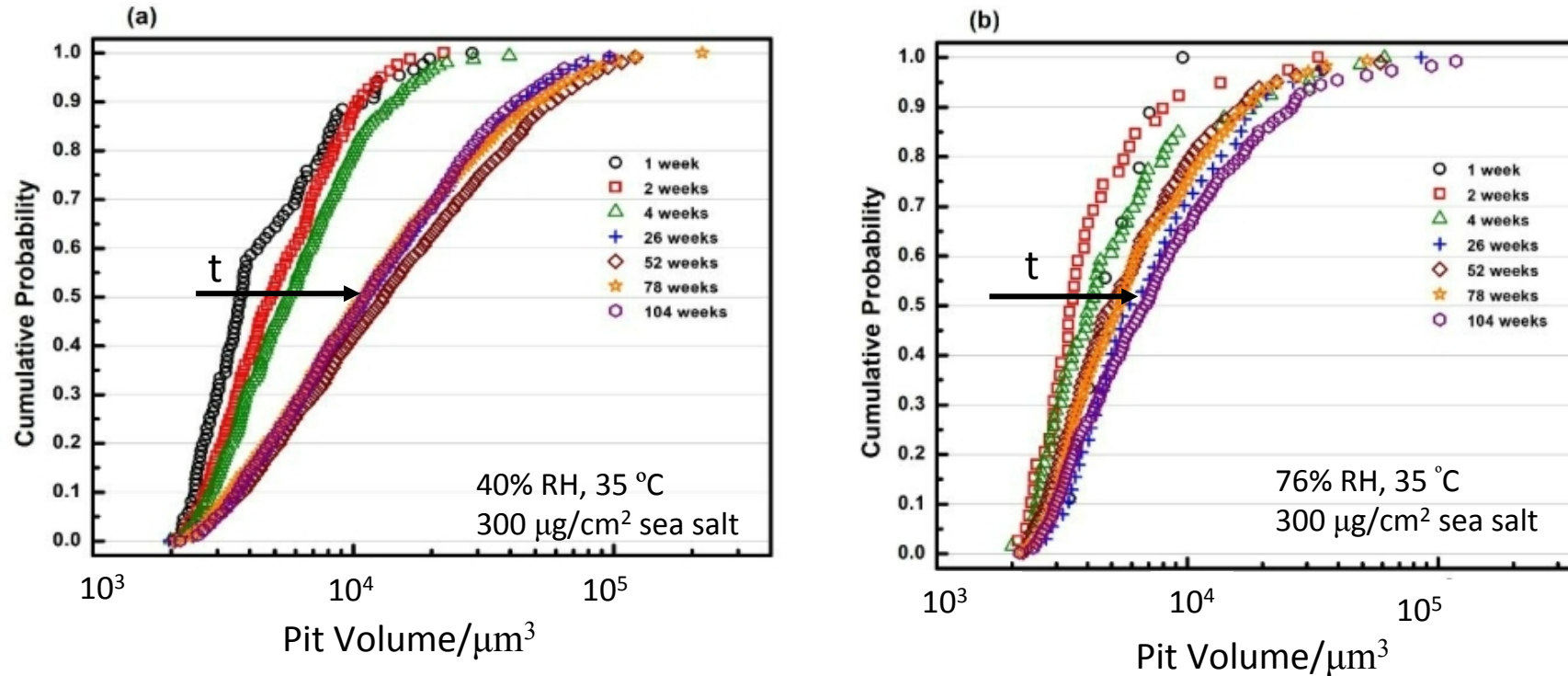


FIB/SEM



Tomography

Pit size and frequency on 304H reach limiting values; 40% RH produces larger pits



What about other RH, T, salt loads, alloy, material conditions?.....Fluctuating RH, salt loads?.....

Maximum Pit Size Model: Deterministic Approach

Electrochemical model for predicting maximum pit size possible for a given material and environmental condition

Model Inputs:

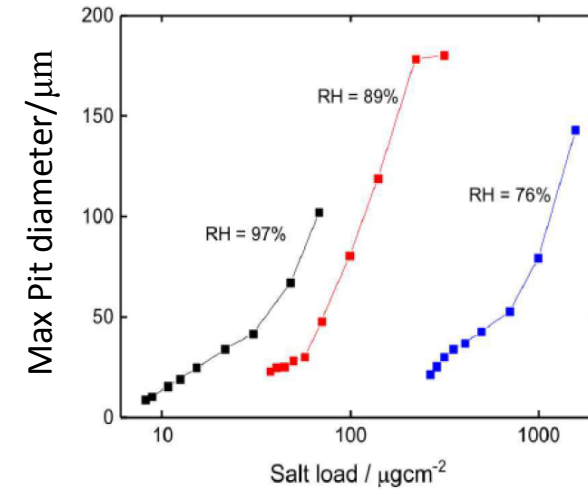
salt chemistry, salt load, RH, T, alloy

Challenge:

Information on electrochemical parameters lacking for expected canister brine conditions

Assumptions:

1. Continuous and uniform brine film
2. Hemispherical pits
3. Cathodic and anodic kinetics are time independent (fixed electrolyte conditions)

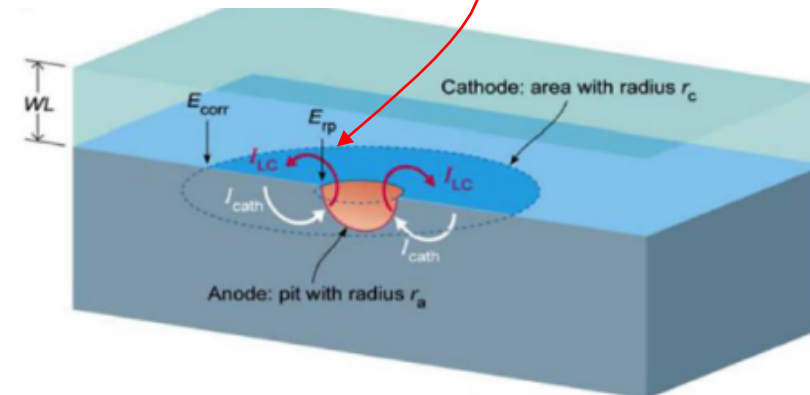


Conceptual schematic

$$\ln I_{c,max} = \frac{4\pi k W_L \Delta E_{max}}{I_{c,max}} + \ln \left[\frac{\pi e r_a^2 \int_{E_{corr}}^{E_{rp}} (I_c - I_p) dE}{\Delta E_{max}} \right]$$

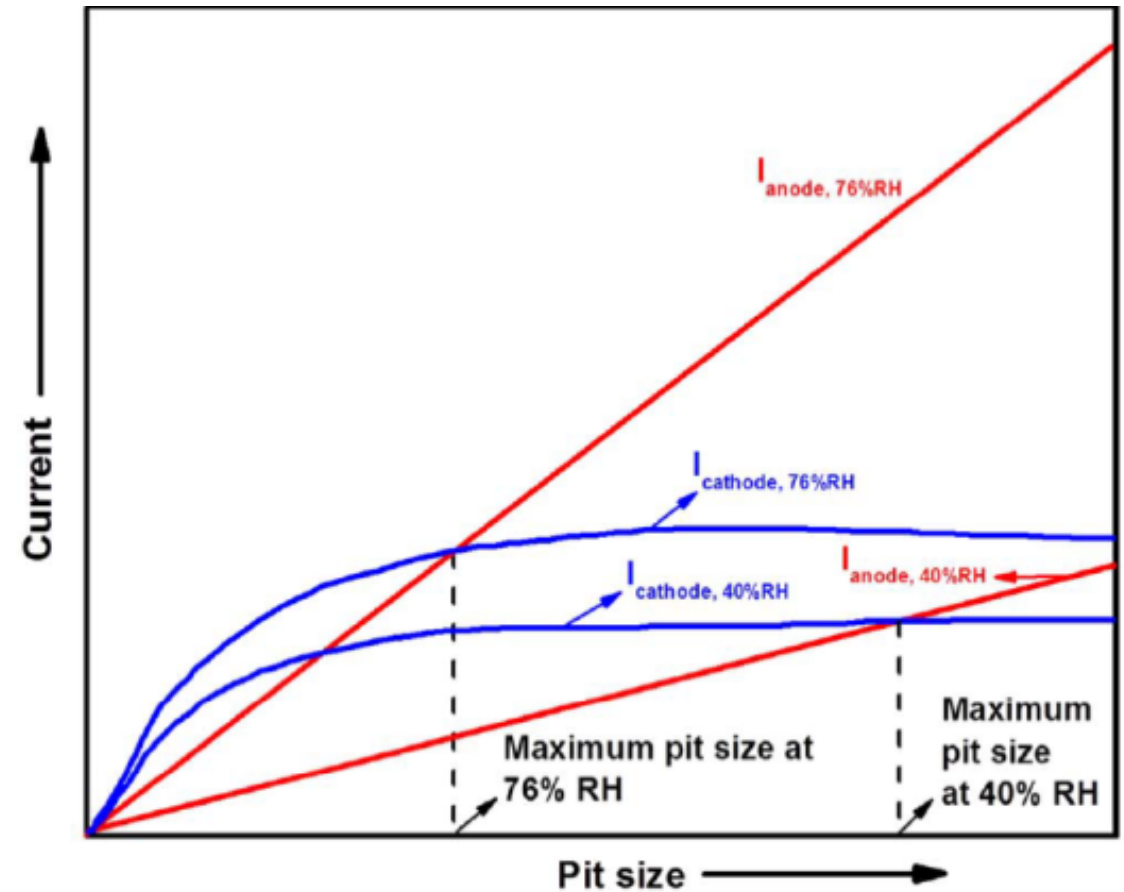
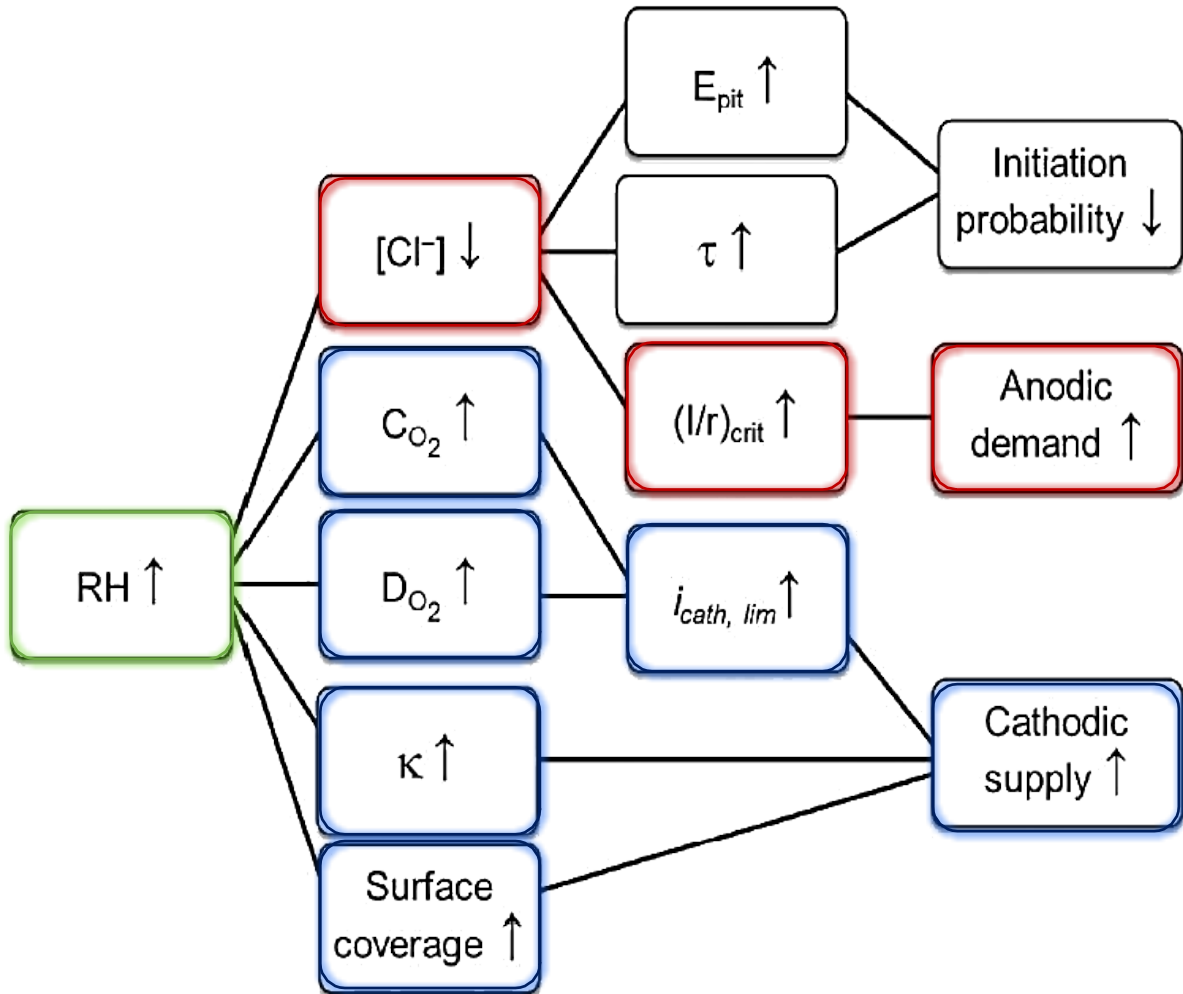
Labels for the equation components:

- Max. cathode current (points to $I_{c,max}$)
- Brine conductivity (points to k)
- Brine layer thickness (points to W_L)
- Cathodic Kinetics (points to the integral term)

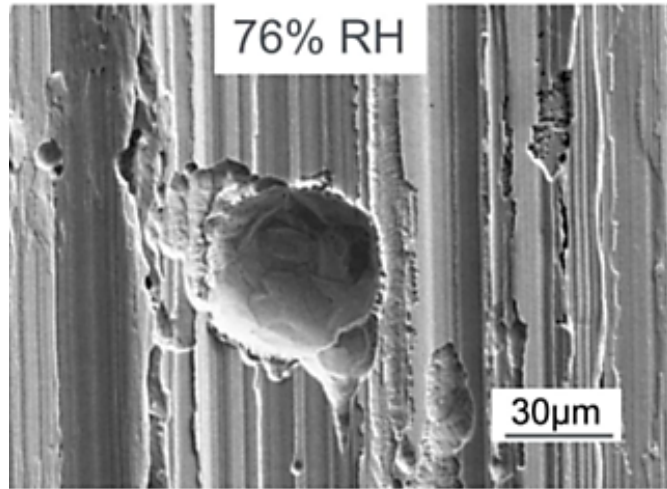


Several Humidity-Dependent Brine Characteristics

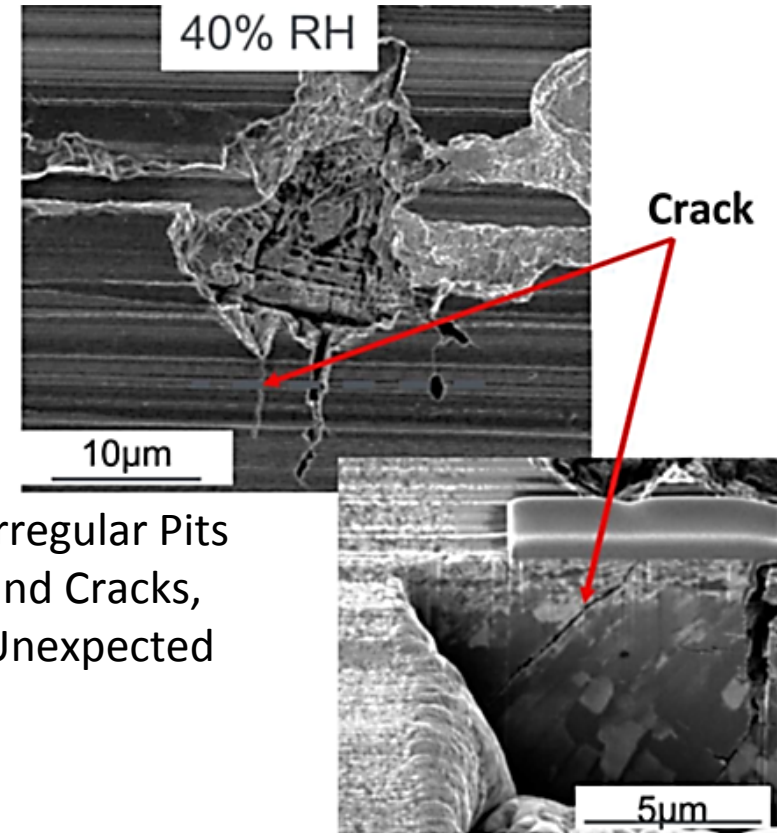
Control Pit Growth



Something Unexpected: Pit Morphology f(RH)



Hemispherical Pits, Assumed

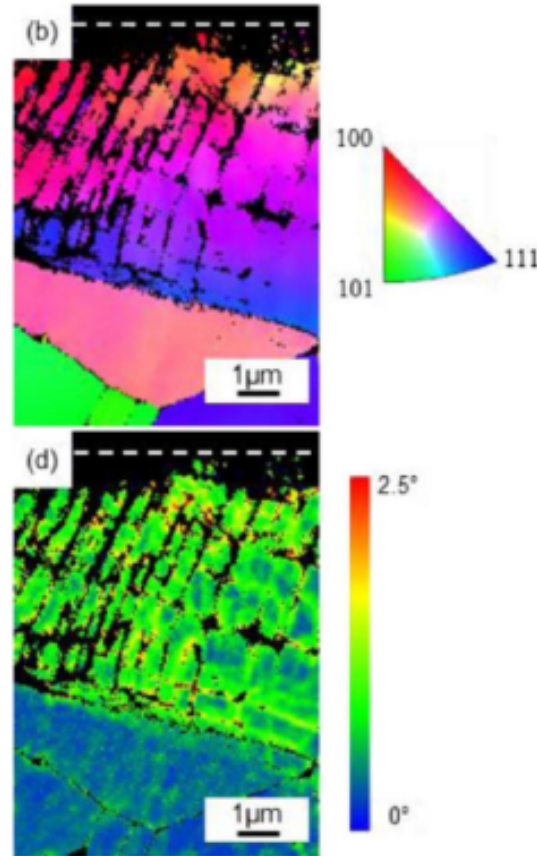


Irregular Pits and Cracks, Unexpected

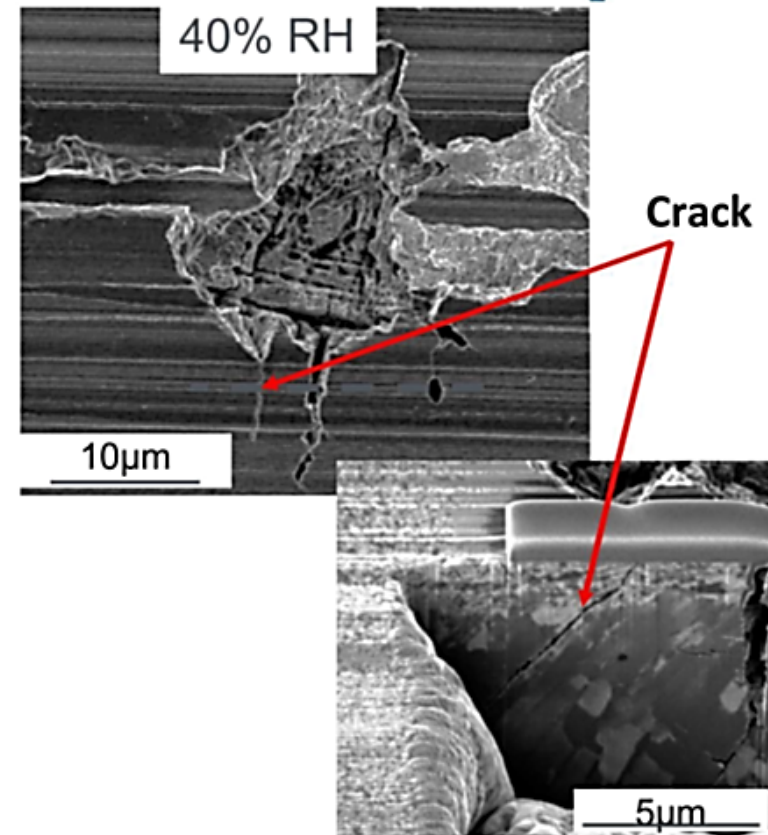
cross-section
through cracked
region

What is going on here?

Low Humidity (40% RH) Produces Irregular Pits Reflective of Surface Condition



EBSD maps of cross-section
through 304 SS coupon surface



Irregular Pit Morphology at Low RH Near Critical Pit Stability?

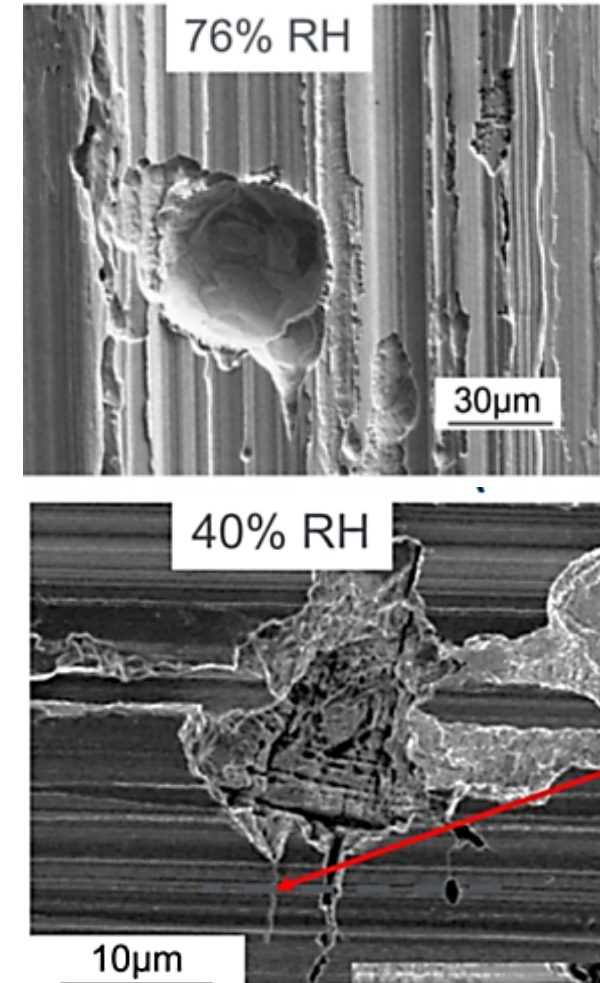
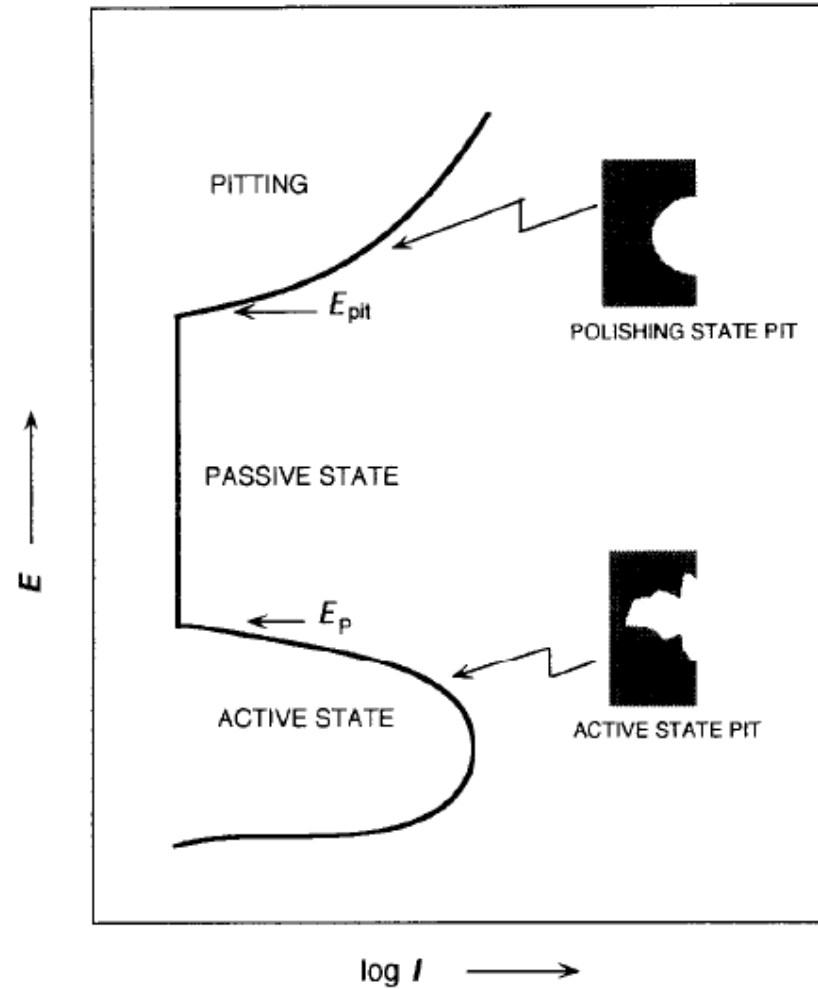
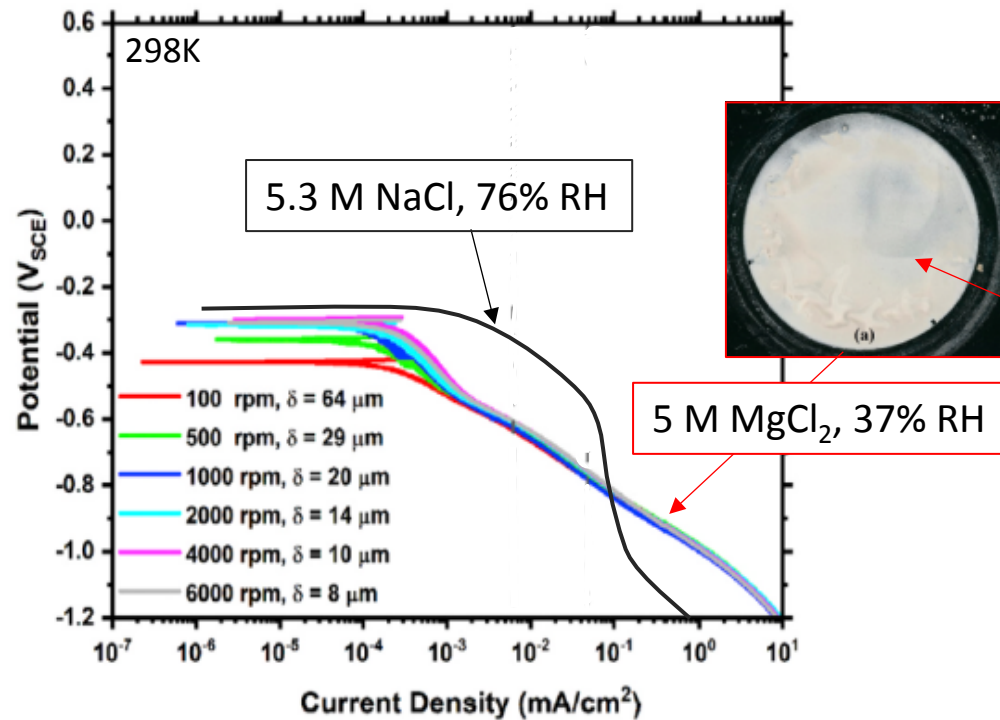
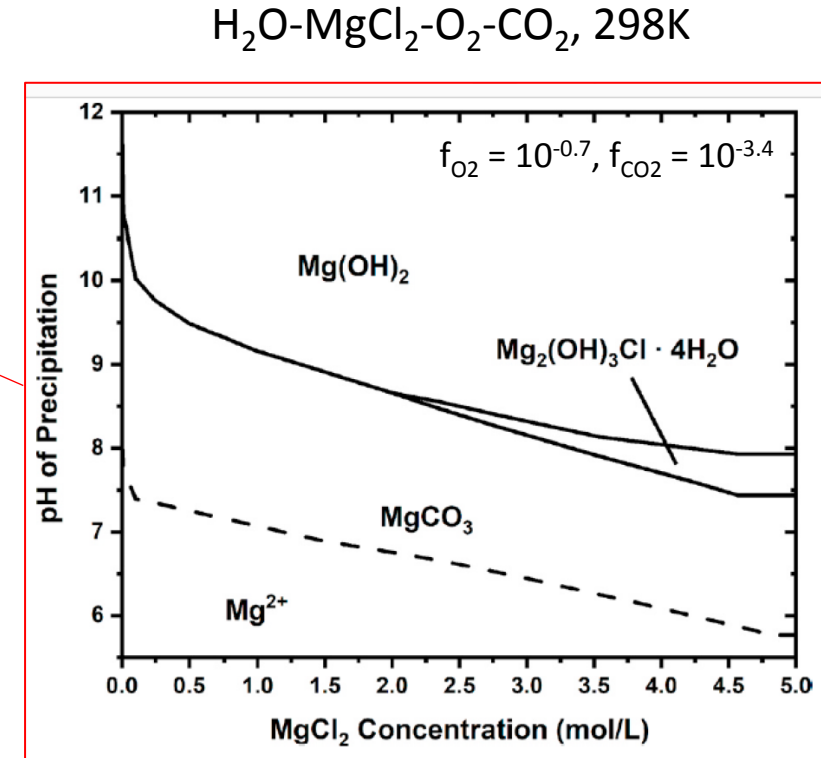


Fig. 1. Anodic polarization curve of metal showing potential regions for polishing state and active state pitting. E =electrode potential; I =metal dissolution current; E_{pit} =the pitting potential; E_p =the passivation-depassivation potential.

Precipitation of Mg Species May Limit Cathodic Supply and Promote HER in Low Humidity Brines

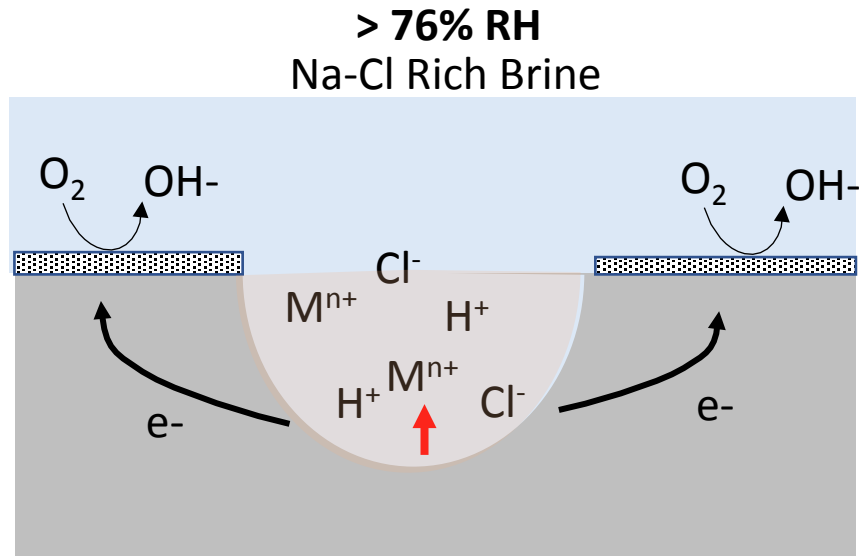


HER Dominates Cathodic
Polarization Behavior in MgCl₂

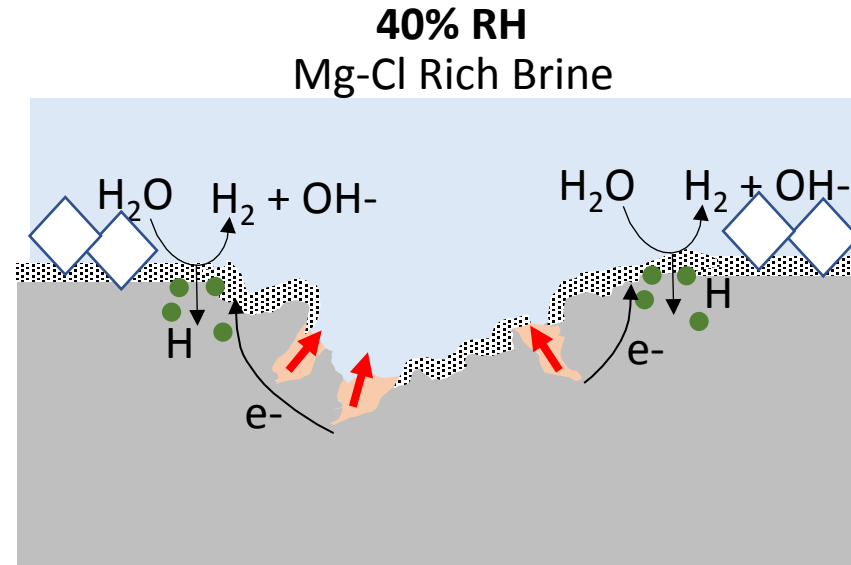


Mg precipitates buffer pH and
promote HER

To What Extent does Low RH Sea Salt Brine Diminish Cathode Power and Embrittle Pit Area?



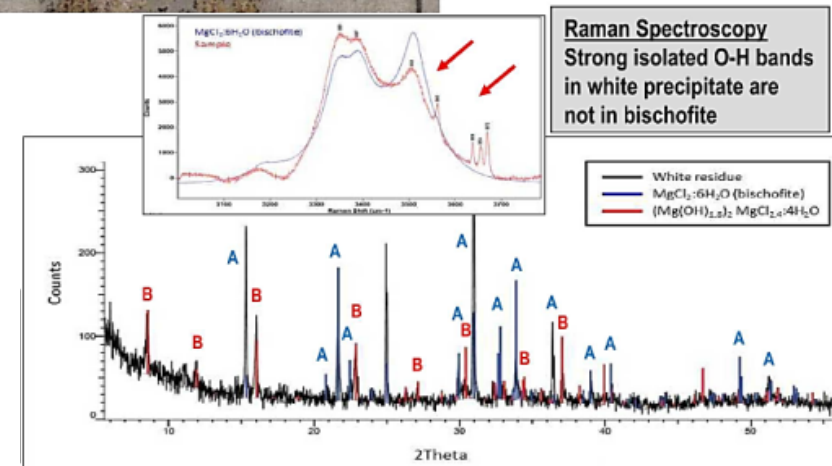
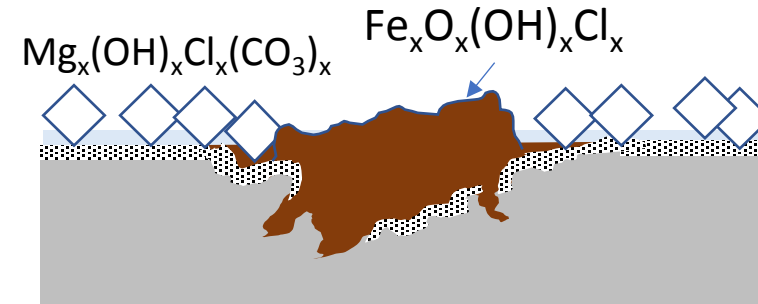
pH at cathode sites increases
with hydroxyl production



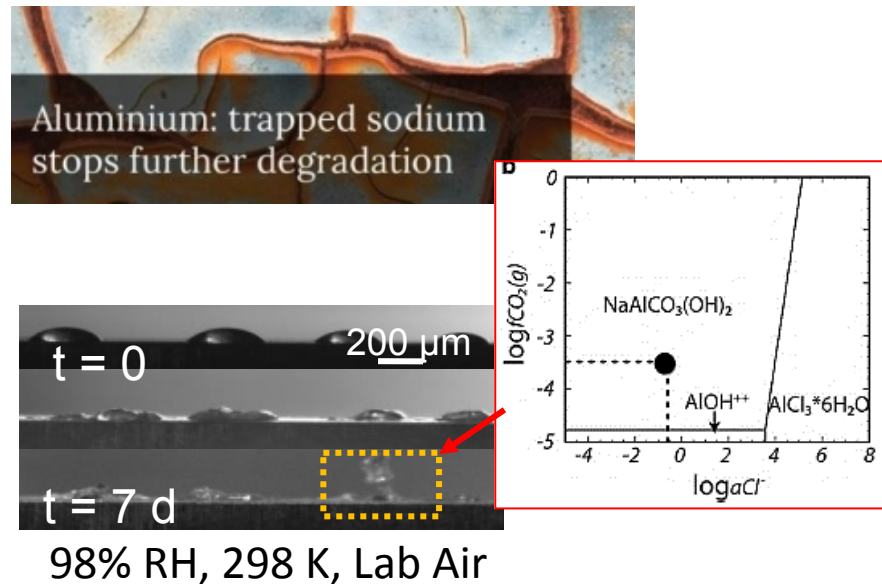
Mg precipitates buffer to neutral
pH and promote HER. H
absorption embrittles area
around pit?

To What Extent do Low Humidity Precipitation Reactions Dry Out Brine and Limit Corrosion?

- Cathodic reactions produce hydroxides promoting Mg precipitates
- Corrosion products sequester Cl- from the brine
- Precipitation removes brine components, reducing brine volume at a given RH

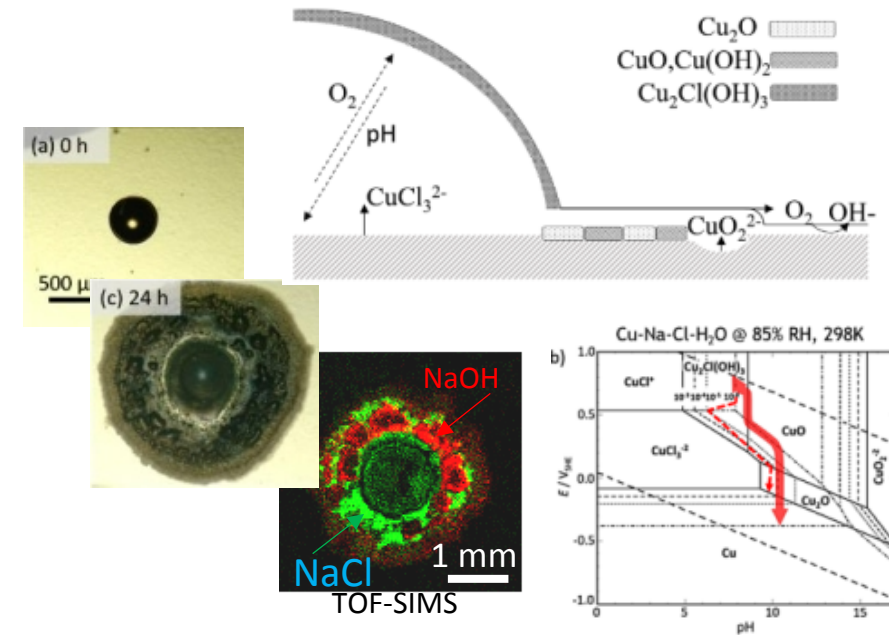


Brine Evolution is a Critical Factor Controlling Corrosion Kinetics and Damage Distributions



Corrosion-induced drying
of NaCl electrolyte stops
aluminum corrosion

Schaller, R.F., Jove-Colon, C., Taylor, J.S.,
Schindelholz, E.J., *Mat. Deg.* 1 (2017): 20



Copper corrodes in alkaline brine
produced by cathodic reactions
outside of salt droplets

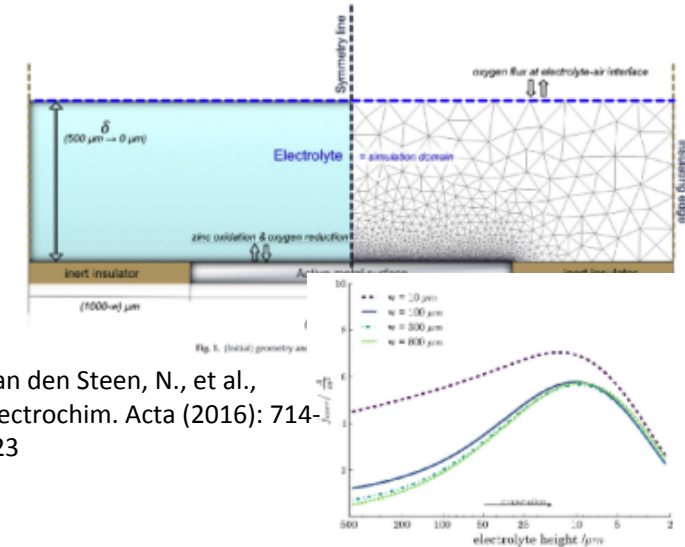
Schindelholz, E.J., Cong, H., Jove-Colon, C., Moffat,
H.K., *Electrochimica Acta* 276 (2018): 194-206.

Broader Implications for Electrochemical Atmospheric Corrosion Models

Variety of Assumptions

- static electrolyte- fixed geometry, chemistry or phases
- electrochemical behavior in bulk electrolyte, “dilute” solutions

Assumptions are largely due to lacking definition of electrolyte and electrochemical kinetics



Van den Steen, N., et al.,
Electrochim. Acta (2016): 714-723

Fig. 13. Corrosion current density for different electrode widths during evaporation ($\delta = 500 \mu\text{m}$, $\text{[Zn}^{2+}]_{\text{init}} = 0.1 \text{ wt\%}$, $h_{\text{air}} = 500 \mu\text{m}$).

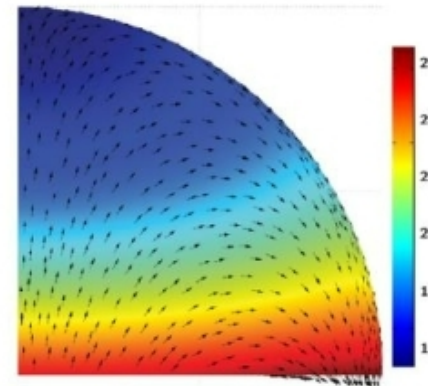
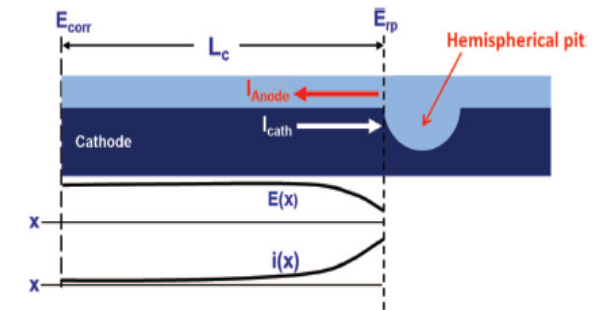


Fig. 10. $(C_{\text{Zn}^{2+}}/C_{\text{Zn}^{2+}}^0)$ of zinc ions and arrow plot of current density vectors showing separation of metal surface into anodic and cathodic regions over time.

Cole, Ivan S., et al., Electrochim. Acta (2011): 1856-1865



Chen, Z. Y., and R. G. Kelly, J. Electrochem. Soc. (2009): C69

Conclusions

Pitting and SCC are promoted by low humidity conditions in the presence of sea salt deposits.

Why?

- Shift in brine conditions – high volume of Na-Cl rich brine at high humidity to low volume of more concentrated Mg-Cl rich brines below ~ 75 % RH
- High [Cl⁻] can promote pitting – anodic processes are well studied
- Concentrated Mg-Cl rich brines lead to irregular/jagged pits and microcracks in rough finish SS 304 that could promote SCC - limit cathode power and support HER?

Elucidating the relationship between evolving brine characteristics and the cathodic processes driving atmospheric corrosion and SCC would further the development of deterministic electrochemical models.