

1 Preparation of Illite Coated Geomaterial Microfluidic Surfaces: Effect of
2 Salinity and Heat Treatment

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12 **1 Abstract**

13 Unique characteristics of clay (e.g., high surface area, deficiency in positive charges) make any
14 clay abundant shales a good source of adsorbed gas. However, the presence of clay in porous
15 media can also affect shale rock's producibility. The clay-water interaction can cause significant
16 swelling and fines migration in the formation and impair the overall hydrocarbon recovery from
17 shale.

18 Geomaterial micromodels, developed by functionalizing traditional glass or PDMS surfaces with
19 geomaterials (e.g., calcite, Quartz, clay), can represent the physicochemical properties of the
20 natural porous media and have been used during the last few years to understand and evaluate the
21 solid-fluid physicochemical interactions. This study focuses on developing a clay-coated
22 geomaterial surface and investigates the effect of base fluid's salinity on clay adsorption to the
23 glass surface. Glass capillary tubes and straight channel borosilicate glass micromodels are
24 coated with Illite clay to represent the pore-scale clay chemistry of Caney Shale, a Mississippian
25 unconventional play in Southern Oklahoma, USA. 10 wt.% of Illite clay slurries made with
26 brines of four different salinities are used to coat the glass-capillary tubes to understand the
27 effect of salinity in clay adsorption on the glass surface and overall coating quality. To achieve a
28 stable coating and evaluate the impact of heat treatment on coating's stability, straight channel
29 glass flow cells coated with Illite clay are heat-treated at low (25 °C) and high temperature (125
30 °C), and the results are compared with an untreated coated surface. Flooding tests were carried
31 out with brines of different salinities on the coated surface to evaluate the stability of the coating.
32 The experimental results indicated a strong relationship between the brine's salinity and the
33 adsorption of clay particles on the glass surface. An increase in brine concentration resulted in
34 improved adsorption of clay particles on the glass surface. Experiments involving heat treating

35 the glass surface following the coating demonstrated significant improvement in the stability of
36 the coating.

37 **2 Introduction**

38 Clay minerals account for, on average, 60 wt.% of most shales (Shaw and Weaver, 1965). It is
39 generally agreed that the presence of clay in a shale formation can significantly affect fluid flow
40 through the ultra-low permeability porous media. This may lead to a severe reduction in the
41 production rate even after hydraulic fracturing (Rahman et al., 2007). This is mainly due to the
42 swelling induced in clay as a result of the interaction between injected water and clay minerals,
43 resulting in reduced pore space and permeability.

44 Different clay minerals have different levels of swelling potential depending on their structural
45 composition and cation exchange capacity (CEC) (Muhammed et al., 2021). Smectite having a
46 larger surface area and higher CEC than other common clay minerals, such as Kaolinite and
47 Illite, demonstrate greater affinity to adsorb water into the formation, followed by significant
48 swelling (Murray, 2006; Rogala et al., 2013). Kaolinite is a 1:1 silicate mineral where one
49 tetrahedral unit is linked through an oxygen atom with another octahedral unit. Because each
50 tetrahedron-octahedron layer (T-O) in Kaolinite is connected with Van der Waals force and a
51 strong hydrogen bond, Kaolinite is a non-swelling clay. In contrast, Illite is a 2:1 clay mineral
52 where one octahedral sheet is squeezed between two tetrahedral units (T-O-T). Illite has
53 potassium ions fitted into the interlayer region, preventing water encroachment into the region.
54 This is why Illite is less sensitive to swelling. However, in the case of Smectite, each T-O-T
55 layer is connected with another T-O-T layer with a weak Van der Waals force. Therefore, water
56 can easily encroach between the layers, making Smectite a highly expandable clay (Grim, 1953;
57 Liu and Lu, 2006).

58 Clay swelling increases with the decrease in brine salinity as the double-layer spacing between
59 the clay molecules expands when they encounter brines of less ionic strength. Montmorillonite
60 clay is reported to be swelled by 30% in diameter once 5000 mg/L NaCl brine is replaced by
61 pure water (Zhuang et al., 2018). Fang et al. (2017) studied the sensitivity of clay-containing
62 core samples to brines of different salinities. They observed a significant swelling-induced
63 permeability reduction in the porous media once the injection fluid was changed from formation
64 water with 9662.9 mg/L salinity to pure water.

65 Fines migration is another phenomenon that can significantly affect shales' productivity.
66 Detachment of the fines from the surface can be induced by hydrodynamic and colloidal forces.
67 Hydrodynamic forces depend on parameters such as fluid velocity, flow dimension, and particle
68 size. A sensitivity study conducted by Tangparitkul et al. (2020) revealed that, under the
69 influence of effective stress, particle size and fluid velocity are the dominant parameters that
70 affect the hydrodynamic forces and control the fines migration.

71 In the presence of swelling clay (e.g., smectite), the salinity of brines may also influence the
72 hydrodynamic forces and cause fines migration. Exposure to brines of salinity less than the
73 critical salt concentration (CSC) may cause the clayey formation to swell and reduce the
74 dimension of the flow channel. Narrowed pore space creates obstruction in the fluid flow, exerts
75 fluid force on the pore wall, and promotes particle detachment (Song and Kovscek, 2016;
76 Tangparitkul et al., 2020; Wilson et al., 2014).

77 Conversely, colloidal forces are sourced from the net effect of London-van der Waals attractive
78 (vdW) forces and electric double layer (EDL) repulsive forces between the clay particles and
79 rock surfaces. The van der Waals forces retain the clay particles on the grain surface, while EDL

80 forces are responsible for the detachment and migration of the particles in the porous media
81 (Israelachvili, 2011; Khilar and Fogler, 1998; Tchistiakov, 2000).

82 In the presence of high salinity formation brine, clay particles are attached to the pore wall
83 mainly by the influence of the vdW forces between clay particles and the pore surface. As the
84 brine salinity starts to decrease due to the injection of low salinity brines or freshwater, the net
85 forces binding the clay particles to the pore wall start to diminish, and when the salinity is below
86 CSC, the repulsive EDL forces start to dominate the colloidal force, and the fines get detached
87 from the surface (Mohan and Fogler, 1997; Muneer et al., 2020). Khilar and Fogler (1984)
88 reported a significant reduction in the permeability of Berea sandstone due to the release of clay
89 particles from the grain surface when the salinity of permeating fluid was below the critical level.
90 Permeability reduction due to the release of the clay particles upon exposure to low salinity
91 injection fluids was also confirmed by many other researchers (Cihan et al., 2022; Han et al.,
92 2020; Sarkar and Sharma, 1990; Song and Kovscek, 2016; Zeinijahromi et al., 2011).

93 Pang and Liu (2013) measured the permeability loss in sand-pack filled with unconsolidated
94 sand when steam and condensate of low salinity and high temperature were injected into the
95 porous media. Their experimental results revealed an irreversible reduction of permeability up to
96 43.52% due to particle migration and hydrothermal reactions caused by steam and its condensate
97 with formation minerals.

98 Wilson et al. (2014) critically reviewed the clay mineralogy of sandstone reservoirs in the North
99 Sea and reported the breakup of Kaolinite aggregates and mobilization of Illite clay particles
100 during fluid injection as the probable cause of formation damage in the North Sea sandstones.

101 In addition to the ionic effects of brines, the hydrodynamic forces exerted by the injection fluid
102 can further aid the detachment of clay particles from the surface. However, Ochi and Vernoux
103 (1998) observed that chemical effects resulting from the non-compatibility between injected
104 fluid and clay in the sandstone formation caused more reduction in the formation permeability
105 compared to hydrodynamic effects of flow.

106 Clay swelling can also cause surface roughening and alters the wettability of the pores in favor of
107 additional oil recovery during low salinity water flooding (Marhaendrajana et al., 2018). Ridwan
108 et al. (2020) explored the implications of surface roughening and pore size alteration generated
109 from the swelling of the Kaolinite, Montmorillonite, and Muscovite clays at various brine
110 conditions. Low salinity brines with monovalent ions significantly reduced the pore size and
111 resulted in lower recovery for the high clay content cores. However, when the clay content was
112 low, the monovalent ions actually promoted oil recovery. They attributed this effect to the
113 change in wettability due to surface roughening from clay swelling. When the clay content was
114 high, the effect of pore size alteration took over the effect of wettability alteration and reduced
115 oil recovery.

116 Different laboratory tests, such as dispersion test, immersion test, bulk hardness test, etc., are
117 developed to study the effects of rock-fluid interactions (Stephens et al., 2009). However, these
118 tests are designed to assess rock samples' stability upon exposure to different fluids by
119 immersing them in the fluids (Gomez and He, 2012) or flowing the fluids through them (Sayegh
120 et al., 1990; Somerton and Radke, 1983). Since rock samples are usually composed of more than
121 one mineral (Quartz, calcite, clay, etc.), these tests can not recognize the potential clay-fluid
122 interaction and its impact on formation damage. Moreover, these test results do not reflect the in-

123 situ behavior of clay upon exposure to any fluids, nor do they provide any pore-scale
124 visualizations of the rock-fluid interaction.

125 Geomaterial functionalized microfluidic chip, developed by coating traditional micromodels, a
126 substrate usually made with glass, Quartz, or any transparent materials that facilitates visual
127 observation of flow network, with any geomaterials, is an excellent tool that can be facilitated
128 with the required level of surface heterogeneity and surface chemistry to represent the pore-scale
129 flow dynamics. They also provide the ability to mimic specific surface mineralogy of any rock
130 and facilitate visual observation of the surface's behavior upon exposure to various fluids.
131 Besides, the micromodel flow networks are highly customizable (Campbell and Orr, 1985) and
132 provide easy and accurate control of fluid flow (Karadimitriou and Hassanzadeh, 2012).

133 Geomaterial micromodels have been used in the last few years to mimic porous media and study
134 various fundamental and applied aspects of multiphase flow such as wettability alteration
135 (Grattoni and Dawe, 2003; Khajepour et al., 2014; Laroche et al., 1999; Saadat et al., 2021;
136 Yekeen et al., 2020), interfacial tension (Mackay et al., 1998; Xu et al., 2022), capillary pressure
137 (Ghazanfari et al., 2007; Smith et al., 2005), and formation damage (Mohammadalinejad et al.,
138 2019; Onaka and Sato, 2021; Sharifipour et al., 2019).

139 Researchers have also used micromodels to explore the mechanisms of different enhanced oil
140 recovery (EOR) methods (Gaol et al., 2021; Mehdizad et al., 2022; Seyyedi et al., 2018; Su et al.,
141 2022; Sun et al., 2021). Low salinity water flooding (LSWF) is one of the EOR methods we
142 observed been investigated the most using geomaterial micromodels.

143 Song and Kovscek (2015, 2016) functionalized glass micromodels with clay minerals to study
144 the effect of pore-scale fines migration and formation damage in the low salinity oil recovery

145 process. Amirian et al. (2017) also performed a detailed study on pore-scale displacement
146 process during LSWF. Their study incorporated two-dimensional clay-coated oil-wet and water-
147 wet micromodels to visually study the role of wettability alteration, snap-off, and fines migration
148 in the dynamic displacement of oil during flooding.

149 A similar study was performed by Mohammadi and Mahani (2020) for carbonates (Mohammadi
150 and Mahani, 2020) and Shahmohammadi et al. (2021) for sandstones to investigate the low
151 salinity oil recovery process. Mohammadi and Mahani (2020) postulated the presence of an
152 initial water film (connate water) in facilitating the diffusive transportation of low salinity brine
153 and enhancing the potential of LSWF for carbonates, while Shahmohammadi et al. (2021)
154 reported a critical brine salinity below which polar components of oil start to break and
155 formulate emulsion in aqueous phase aiding in oil recovery during LSWF for sandstones. Shaik
156 et al. (2022) coated straight channel glass micromodels with CaCO_3 to transform the internal
157 glass surfaces to carbonate using the layer-by-layer deposition method. The calcite-coated
158 micromodel was used to investigate the effect of brine composition (e.g., salinity and ionic
159 strength) in altering the wettability of calcite surfaces.

160 Solid-fluid physiochemical interaction is another area proven to be advantageous studying with
161 geomaterial micromodels. Porter et al. (2015) investigated the advantages of using real rock
162 micromodels to study the fracture-matrix interactions at a temperature and pressure consistent
163 with the reservoir conditions. They developed a micromodel fabrication method that works well
164 for both real rock and synthetic (e.g., glass, PDMS) micromodels.

165 Oh et al. (2017) investigated the interactions of a synthetic PbCl_2 solution and Uranium (U)
166 containing groundwater with shale and granite surfaces using the micromodels they developed
167 by placing thin sections of the respective rocks in a PDMS micromodel. While studying the

168 sorption of Pb and U onto the thin section, they stated that microfluidic tests are capable of
169 mimicking mineral-fluid interactions in porous media, and micro X-ray fluorescence (μ -XRF)
170 can be coupled with the microfluidic system to analyze the mineral surface after the interactions
171 with fluid.

172 Siadatifar et al. (2021) prepared sandstone and carbonate representing geomaterials to visualize
173 the fluid-fluid and solid-fluid interaction during LSWF. Jahanbakhsh et al. (2020), while
174 reviewing the advancement in the fabrication method of micromodels and imaging techniques,
175 reported that materials used for micromodel preparation could not fully capture the subsurface
176 rock-fluid interactions. Hence, they emphasized functionalizing micromodel surfaces with
177 geomaterials to replicate the surface mineralogy and wettability of the porous medium.

178 Two different methods have been used so far to functionalize the traditional glass or PDMS
179 micromodels with clay minerals: physical adsorption by flowing clay slurry through the flow
180 network (Amirian et al., 2017; Song and Kovscek, 2015) and a layer by layer deposition of
181 polyelectrolyte and clay (Pan et al., 2019; Zhang et al., 2018). Song and Kovscek (2015, 2016)
182 functionalized a silicon microfluidic chip with Kaolinite clay by injecting a clay solution of 1
183 wt.% of Kaolinite in 15,000 ppm brine to understand the effect of low salinity water flooding in
184 sandstone reservoirs. After coating, to create an immobile clay surface and study the wettability
185 alteration due to clay adsorption, they heat treated the surface at 120 °C for 25 minutes. A similar
186 approach was adopted by Amirian et al.(2017) to develop Kaolinite (Amirian et al., 2017) and by
187 Amirian and Haghghi (2018) to develop Illite coated geomaterial surfaces to understand the
188 effect of clay type and water composition on low salinity water flooding. They used a 20 wt.% of
189 clay slurry in 30,000 ppm NaCl brine, and instead of heat drying the coated surface, they air-

190 dried it for two hours by placing it on a hot plate set at 80 °C to ensure the reversibility of the
191 coating.

192 Barnaji et al. (2016), instead of using any brine for base fluid, used a suspension of 10 wt.% of
193 clay in distilled water to coat glass micromodels with Kaolinite and Na-Bentonite clays and dried
194 the micromodels by placing them in an oven at 120 °C for 1 hour. Na-Bentonite was also used by
195 Sharifipour et al. (2019) to coat glass micromodels and study pore-scale swelling behavior of the
196 clay. For the coating purposes, they prepared two different clay slurries: one with 45000 ppm
197 NaCl and 11800 ppm CaCl₂, and the other one with 1000 ppm NaCl. Following the coating, they
198 heated the micromodels at 150 °C for water evaporation.

199 Mehdizad et al. (2022) etched the heterogeneous pattern of a real sandstone rock on the glass
200 micromodel to represent the physical rock network of sandstone and then coated it with Na-
201 Bentonite clay to study the recovery mechanisms in water-wet and oil-wet clay-rich
202 heterogeneous micromodels. 5 wt.% clay slurries prepared with 57000 ppm NaCl brine were
203 injected into the micromodel. During injection, the micromodel was placed in an ultrasonic bath
204 to avoid clay flocculation and ensure homogenous deposition. The clay-saturated micromodel
205 was then heated to 140 °C for water evaporation.

206 Shahmohammadi et al. (2021), to study the interactions between crude oil, brine, and clay,
207 developed Montmorillonite coated micromodels. To fabricate the micromodel, they first laser
208 engraved a graphic pattern onto a glass plate. Afterward, a new glass plate was fused with the
209 engraved one at a temperature of 710 °C to create the flow channel. A 41,600 ppm brine
210 containing components such as NaCl, KCl, MgCl₂.6H₂O, CaCl₂.2H₂O, Na₂SO₄, NaHCO₃ at
211 varying concentrations was used as the base fluid for the clay slurry. The slurry was prepared by

212 dissolving 60g of Montmorillonite clay in one liter of brine. Following the coating, they heat-
213 treated the micromodel at a temperature of 120 °C for 1 hour.

214 Bartels et al. (2017) employed a new deposition method to prepare clay-coated glass
215 micromodels. Instead of using brine to prepare the clay slurry, they used Isopropyl Alcohol
216 (IPA). 60g of Montmorillonite clay was mixed with per liter of IPA to prepare the suspension.
217 IPA was chosen to facilitate rapid drying of the micromodel. The drying was achieved by placing
218 the clay-saturated micromodel in a vacuum oven at 60 °C. Their slurry preparation method was
219 derived from the method developed by Mahani et al.(2015), who used deionized water to prepare
220 the Na-Montmorillonite clay suspensions. The suspensions had a varying range (100-500 mg/L)
221 of clay concentration. Following the coating, they vacuum dried the glass slide in desiccators for
222 5 to 10 minutes.

223 The use of deionized water in preparing the clay slurry is also prevalent in the work of Lebedeva
224 and Fogden (2010). They coated a flat glass substrate with Kaolinite clay to investigate the
225 adhesion of oil to Kaolinite. The slurry was prepared by dissolving 10g of Kaolinite clay in 50g
226 of deionized water. The solution was heated at 85 °C until the final concentration reached 7 wt.
227 %. Immediately after the glass slides were coated with clay, the substrate was swept by a heat
228 gun at 120 °C to immobilize the clay particles.

229 A similar approach was taken by Bondino et al. (2013) and Kashiri et al. (2021) to prepare
230 Kaolinite coated glass micromodel and study the effect of clay on oil recovery and fines
231 migration during low salinity water flooding. While the former prepared a 0.31 wt.% of clay
232 solution in deionized water and dried the coated substrate in an oven at 80 °C for three days
233 followed by heating with a heat gun for 1 minute, the latter used 5 wt. % of clay solution and air-
234 dried the substrate at 80 °C for 2 hours to prevent irreversible clay coating. Table 1 summarizes

235 the specifications of the clay slurries and the drying treatments employed by the researchers
 236 mentioned in this study to prepare the clay-coated micromodels.

237

238 *Table 1: Summary of selected studies on preparing clay-coated micromodels*

Reference	Clay mineral	Clay concentration	Base fluid	Drying temperature	Drying duration
Song and Kovscek (2015, 2016)	Kaolinite	1 wt. %	15,000 ppm NaCl brine	120 °C	25 minutes
Amirian and Haghghi (2018); Amirian et al. (2017)	Kaolinite, Illite	20 wt. %	30,000 ppm NaCl brine	80 °C	2 hours
Barnaji et al. (2016)	Kaolinite, Na-Bentonite	10 wt.%	distilled water	120 °C	1 hour
Sharifipour et al. (2019)	Na-Bentonite	Not reported	45,000 ppm NaCl and 11,800 ppm CaCl ₂ ; 1000 ppm NaCl	150 °C	Not reported
Mehdizad et al. (2022)	Na-Bentonite	5 wt.%	57,000 ppm NaCl brine	140 °C	Not reported
Shahmohammadi et al. (2021)	Montmorillonite	6 wt. %	41,600 ppm brine containing NaCl, KCL, MgCl ₂ .6H ₂ O, CaCl ₂ .2H ₂ O, Na ₂ SO ₄ , NaHCO ₃	120 °C	1 hour
Bartels et al. (2017)	Montmorillonite	6 wt.%	IPA	60 °C	Not reported
Mahani et al. (2015)	Na-Bentonite	100-500 mg/L	Deionized water	Not reported	5 to 10 minutes

Lebedeva and Fogden (2010)	Kaolinite	7 wt. %	Deionized water	120 °C	Not reported
Bondino et al. (2013)	Kaolinite	0.31 wt.%	Deionized water	80 °C	3 days +1 minute
Kashiri et al. (2021)	Kaolinite	5 wt. %	Deionized water	80 °C	2 hours

239

240 As it can be seen, there is not a good agreement between the works of literature on the
 241 specification (e.g., salinity) of base fluid used to make the clay suspension. The post-coating
 242 treatments (e.g., the temperature and duration of drying) also vary widely in the literature.
 243 However, as per the DLVO theory, the presence or absence of cations in the carrier fluid is
 244 critical for the attachment or detachment of clay particles from the rock surface as it controls the
 245 colloidal forces acting between the particles and the solid surface (Berg et al., 2010; Schembre et
 246 al., 2006). The temperature and duration of drying are also equally important to achieve
 247 sufficient stability of the coating. For a successful preparation of the geomaterial model, the heat
 248 treatment should not make the clay particles completely immobile. Having a stable coating
 249 without compromising the natural mobility of the clay particles will make the geomaterial
 250 surface a close representative of the clay-rich rock surface. Given the rise in the application of
 251 clay-coated geomaterial surfaces, it is therefore imperative to evaluate the effect of base fluid's
 252 salinity on clay adsorption and post-coating treatment on the stability of the coated surface to
 253 reach a consensus over the solution preparation and drying procedures for a stable clay coating.

254 In this study, glass capillary tubes are coated with Illite clay slurries made with brines of four
 255 different salinities to investigate the effect of salinity on clay adsorption to the glass surface. The
 256 best performing clay-brine combination is then used to coat straight channel resealable
 257 borosilicate glass micromodels. Once a uniform coating is obtained, the micromodels are dried at

258 different temperatures. The treated surfaces are then exposed to brines of different salinities to
259 assess the effect of heat treatment on the stability of the adsorbed clay particles.

260 In the following sections, the method used for clay coating on a glass surface that includes
261 several cycles of continuous injection and withdrawal of clay solution is described. Scanning
262 electron microscopy (SEM) and Energy-dispersive X-ray spectroscopy (EDS) data of the clay-
263 coated surfaces after each experiment are used to demonstrate the clay coating density, coverage,
264 and chemistry. The effect of heat treatment on the stability of the coated surfaces is also
265 discussed.

266 Experiments with brines of different salinities as the base fluid for clay slurry indicated a strong
267 relationship between the brine's salinity and clay particles' adsorption on the glass surface. An
268 increase in brine concentration resulted in improved adsorption of Illite clay particles on the
269 glass surface. Experiments involving heat treating the coated glass surfaces also demonstrated a
270 significant effect of temperature on the coating stability.

271 **3 Materials and methods**

272 **3.1 Clay minerals**

273 Illite (IMt-1) from Silver Hill's Cambrian Shales, Jefferson Canyon, Montana, USA, obtained
274 from the source clays repository of the Clay Minerals Society was used to coat the glass capillary
275 tubes. Prior to coating, the clay chips were powdered in a ball mill for less than five minutes. To
276 avoid trace contamination of Fe or Al, a Tungsten canister and balls were used to grind the clay
277 chips. To coat the straight channel glass micromodels, Illite clay powder (IMC) was purchased
278 from Lotioncrafter.

279 Illite, $(K, H_3O)(Al, Mg, Fe)_2(Si, Al)_4O_{10}[(OH)_2, H_2O]$, is a 2:1 clay mineral where one octahedral
280 Alumina sheet is sandwiched between two tetrahedral Silica sheets. They have potassium ions
281 between each Tetrahedral-Octahedral-Tetrahedral (TOT) sequence making them less vulnerable
282 to water encroachment. The Illite IMt-1 sample had already been characterized by Köster (1996).
283 He identified the chemical composition of the clay sample by X-Ray diffraction analysis of
284 various size fractions of the clay sample (Köster, 1996) . Table 2 shows the elemental
285 compositional result obtained from the EDS elemental analysis of the Illite powders.

286 Table 2: Major components of the Illite clay (IMt-1 and IMC) as observed in EDS elemental map

Element	Mass Norm. %	
	IMt-1	IMC
Oxygen	46.50	51.80
Silicon	23.00	12.38
Aluminum	14.62	7.73
Potassium	7.80	2.60
Iron	5.23	3.14
Magnesium	1.58	1.50
Calcium	0.72	20.36
Titanium	0.37	0.34
Sodium	0.06	0.17
Zinc	0.03	0.01
Phosphorus	0.02	0

287
288 Clay minerals usually possess two different charges, one on the basal faces that arises from the
289 isomorphic substitution in the structural layers and exhibits permanent negative charges. The
290 other one is called the edge charge resulting from the protonation or deprotonation of the Si-OH
291 group depending on the pH and the ionic strength of the solution (Środoń, 1999). However, Illite
292 is less complicated in charge heterogeneity than Kaolinite and Smectite. The permanent negative
293 charge in the faces of Illite clay owing to the isomorphic substitution, is mostly balanced by the

294 interlayer potassium ion and thus does not contribute much to the electrostatic interaction
295 between clay particles and the glass surface (Kumari and Mohan, 2021).

296 Nevertheless, in this study, instead of the surface charge of basal planes or edges, the net surface
297 charge of Illite clay particles is used to explain the electrostatic interaction between the clay
298 particles and the glass surface. In the alkaline pH condition and salinity range (0 to 30,000 ppm
299 NaCl) of the clay solutions used in this study, the net surface charge of Illite is negative (Shehata
300 and Nasr-El-Din, 2015).

301 **3.2 Test Fluids**

302 Clay slurries prepared with NaCl brines of different concentrations are specified in table 3. The
303 brines were prepared by dissolving NaCl powder purchased from Sigma Aldrich in deionized
304 water (18.2 MΩ-cm).

305 Table 3: Basic properties of the clay solutions

Illite clay slurry	Base fluid	NaCl concentration, ppm	Dynamic viscosity of clay slurry, cP	Density of clay slurry, g/cm³	pH of clay slurry
01	DI water	0	0.5	1.5	8
02	Brine 1	5000	1.1	1.6	8.5
03	Brine 2	10000	1.2	1.65	8
04	Brine 3	30000	1.5	1.75	8.4

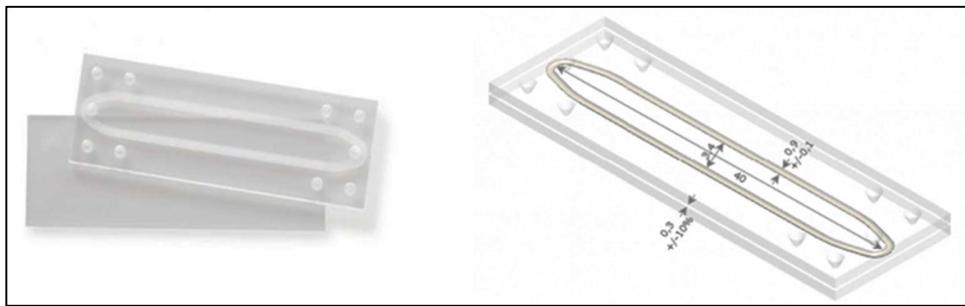
306 **3.3 Solid substrates**

307 Two different glass substrates were used for the coating purpose: capillary tubes and straight
308 channel resealable flow cells. Glass capillary tubes purchased from DWK Life Sciences Kimble
309 (catalog no. 34505-99) were used to develop the coating procedure and study the effect of base
310 fluid's salinity on the adsorption of clay particles to the glass surface. The capillary tubes are

311 made of borosilicate glass, 90 mm long, and have an outer diameter of 1.2-1.5 mm and a wall
312 thickness of 0.2 mm.

313 Straight channel resealable flow cells, purchased from Micronit Micro Technologies B.V, were
314 used to prepare the geomaterial surfaces and study the effect of heat treatment on the stability of
315 the clay coating (Fig. 1). Flow cells are composed of two separate layers. The bottom layer is a
316 700 μ m thick plain glass slide, whereas the top layer is a 1100 μ m thick glass slide with inlet and
317 outlet ports enclosed by an elastomer. When the bottom and top layers are installed in the chip
318 holder, the elastomer seals the top and bottom layer and defines the flow path. The flow path is
319 about 40 mm long and has a hydraulic radius of 1.5 mm. One of the major advantages of these
320 flow cells is that they are resealable, meaning that the top and bottom layer can be separated, and
321 the surface can directly be used for microscopic analysis. Unlike the traditional microfluidic
322 chips, those specially designed resealable flow cells do not have any flow network etched on
323 them as the elastomer defines the flow path. Since no etching was involved, we believe the glass
324 surfaces are molecularly smooth.

325 Moreover, for all the experiments same surfaces were used, i.e., surface roughness was not a
326 varying parameter among the experiments. The only parameter that has been changed is the
327 salinity of the clay solution so that any improvement in the clay coating can primarily be
328 attributed to the base fluid salinity. Before coating, the substrates were treated with Nitrogen
329 plasma to remove any organic contamination from the surface and improve the hydrophilicity
330 (Shaik et al., 2020).



331

332 Figure 1: (left) Top and bottom part of resealable straight channel flow cell; (right) connected
333 flow path with dimensions (Courtesy: Micronit Microfluidics).

334 **3.4 Experimental procedure**

335 **3.4.1 Solution preparation**

336 10 wt.% Illite clay slurries prepared in NaCl brines of different salinities were used to coat the
337 glass capillary tubes and the resealable glass micromodels. The concentration of clay was
338 selected based on several trial experiments to avoid the clogging of the channels and have
339 sufficient clay particles to be adsorbed on the surface. The primary reason for using NaCl brine
340 as the base fluid is to represent the subsurface reservoir environment and prevent in situ fines
341 migration and clay swelling caused by freshwater interaction with clay.

342 Slurries prepared with brines of four different salinities were used to evaluate the effect of
343 salinity on clay adsorption to the glass surface. The properties of the brines are listed in table 4.
344 As the brine salinity increases, the clay particles are more prone to aggregating and settling down
345 due to the decrease in the double layer repulsive forces. Therefore, to keep the particles dispersed
346 in the solution, the clay slurries were vigorously stirred with a magnetic stirrer for 30 minutes,
347 followed by ultrasonication using Branson 2800 Ultrasonic Cleaner for 1 hour and immediately
348 injected into the capillary tubes.

349 Table 4: Specifications of the brines used to study the stability of the coating after each heat
 350 treatment

Brine concentration, ppm	Dynamic viscosity at 25°C, cP	Surface tension, N/m	Capillary number	Flow rate, $\mu\text{L}/\text{min}$	Micromodel volume, μL	Pore volumes injected
30000	0.948	0.072	1×10^{-6}	32.19	300	37.73
10000	0.909	0.072	1×10^{-6}	33.58	300	39.39
5000	0.893	0.072	1×10^{-6}	34.18	300	40.11
0	0.892	0.072	1×10^{-6}	34.22	300	40.16

351

352 **3.4.2 Clay coating**

353 There have been mainly two mechanisms behind glass surface getting coated with geomaterials:
 354 physical adsorption (Amirian et al., 2017; Song and Kovscek, 2015) and a layer by layer
 355 deposition of the minerals on the substrate surface (Shaik et al., 2020; Zhang et al., 2018). In the
 356 former method, the mineral slurry is flowed through the substrate surface, while in the latter
 357 case, a polyelectrolyte is used to link between the solid substrate and the coating minerals.
 358 Because in the latter case the deposition is governed by electrostatic attraction between the glass
 359 surface, polyelectrolyte, and minerals, the coating is more stable than that can be achieved from
 360 mere physical adsorption. Despite this fact, in this study, the former method is used to develop
 361 the coated surface to achieve the following objectives: to avoid using any synthetic materials
 362 except the clay; to replicate the subsurface porous environment as much as possible; and to study
 363 the effect of salinity on physical adsorption to the glass surface. The coating procedure
 364 developed by Song et al. (2015) was used with a few modifications to improve the coating
 365 density and stability (Song and Kovscek, 2015).

366 Herein, a 10 wt.% clay slurry prepared in NaCl solution of 30,000 ppm is used to coat the glass
 367 capillary tubes. Since physical adsorption is driven by the Van der Waals attractive forces

368 between the glass surface and clay particles, 100 cycles of clay solution infusion and withdrawal
369 were performed to increase the contact of clay particles with the glass surface. Each cycle was
370 composed of three steps: infusion-delay-withdrawal. Fluids were infused at a velocity of 26.5
371 meters/hour and withdrew at 2.65 meters/hour using a Harvard Advanced Programmable Syringe
372 Pump (PHD Ultra). A delay of 2 minutes between infusion and withdrawal was maintained to
373 allow sufficient time for the clay particles to get adsorbed. Instead of infusing air through the
374 tubes to displace the clay slurry after each injection, the clay slurry was withdrawn by creating a
375 vacuum at the outlet to avoid air channeling inside the flow network and completely displace the
376 clay slurry. The clay solutions were required to be ultrasonicated every ten cycles to keep the
377 particles dispersed in the solution. The flow rates were selected based on several trial tests to
378 deliver the clay slurry evenly into the flow volume and displace the fluid carrying unadsorbed
379 and loosely attached particles without affecting the coating. The process flow diagram for Illite
380 clay coating on glass capillary tubes is shown in figure 2. Following the coating, the capillary
381 tubes were air-dried at 25 °C for 1 hour.

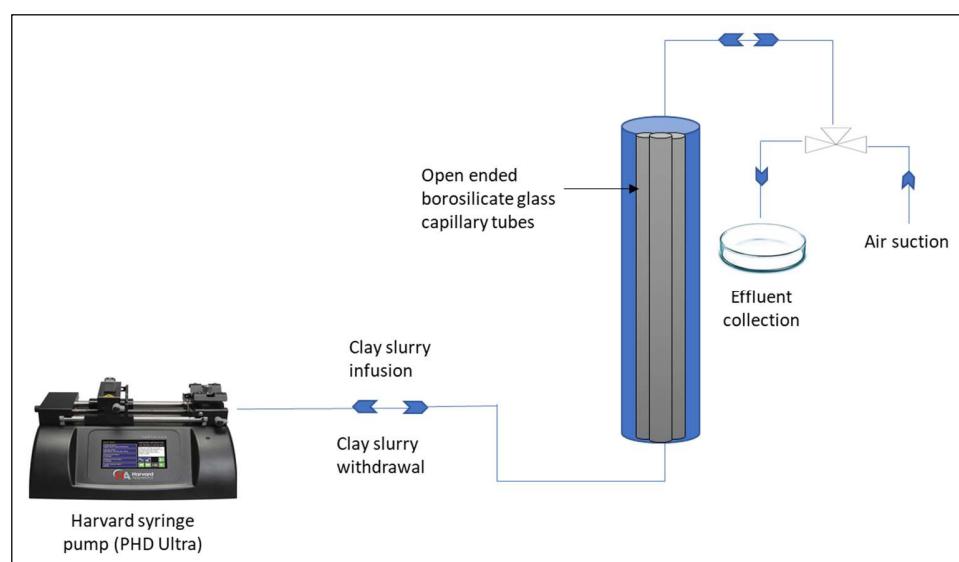
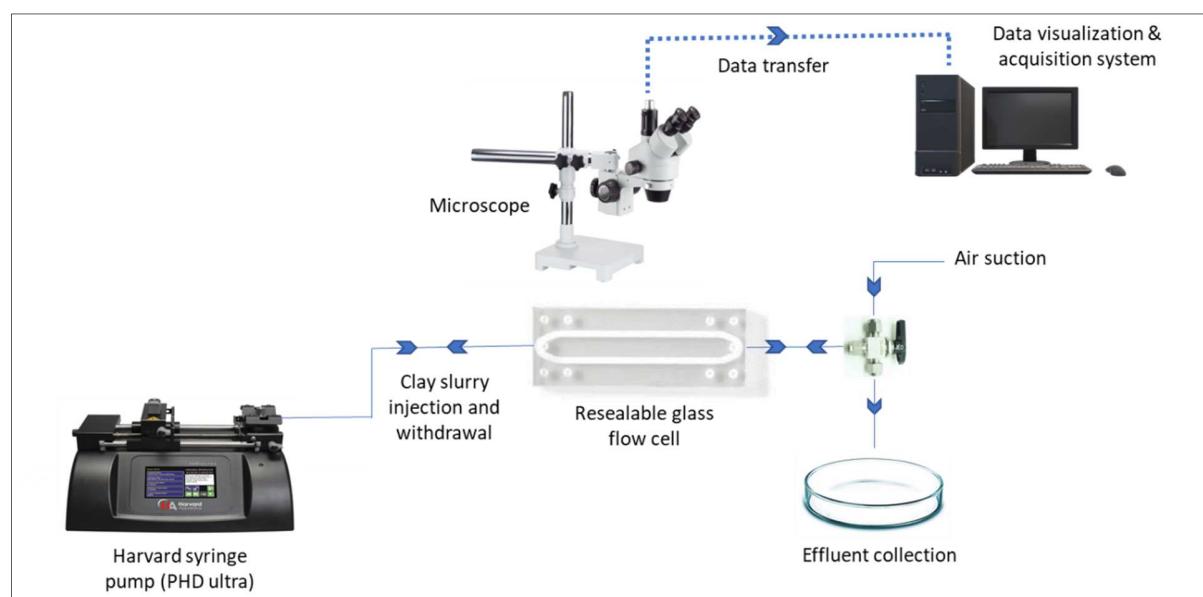


Figure 2: Process flow diagram for Illite clay coating on glass capillary tubes.

384 A very similar procedure was used to coat the resealable glass micromodels (Fig. 3). However,
385 unlike the capillary tubes, the resealable flow cells had the facility to visualize the surface after
386 each coating cycle, and only three cycles were observed to be sufficient to coat the glass surface
387 uniformly; hence, the remaining cycles were not performed.

388 After drying, the capillary tubes were carefully broken into small pieces by gently pressing them
389 with a tweezer to expose the coated surfaces for microscopic characterization. Coating coverage
390 and uniformity were evaluated by AmScope 10X LED optical microscope, morphology by FEI
391 Quanta 600 field-emission gun Environmental Scanning Electron Microscope (SEM), and
392 elemental atomic percentages by Bruker Energy-Dispersive X-ray Spectroscope (SEM-EDS).

393



394
395 Figure 3: Process flow diagram for Illite clay coating on resealable glass micromodels

396 **3.4.3 Evaluating effect of salinity**

397 To evaluate the effect of base fluids salinity on the adsorption of Illite particles to the glass
398 surface, four different clay slurries were prepared: three with NaCl brines of three different

399 salinities: 30,000 ppm, 10,000 ppm, and 5000 ppm and one with deionized water (DIW). The
400 deionized water represented the base fluid with no salinity. Following the coating, the surfaces
401 were air-dried at 25°C for one hour and afterward characterized with the bright-field optical
402 microscope, scanning electron microscope, and Energy-Dispersive X-ray Spectroscopy. The
403 optical images of the coated surfaces were analyzed with Fiji, a distribution of ImageJ software
404 to approximate the coating density.

405 **3.4.4 Heat treatment and coating stability analysis**

406 After the clay coating, the surface needs to be dried to make the particles adhered to it so as to
407 achieve the stability of the coating. For this purpose, the previous researchers have applied
408 different techniques that include heat drying the coated surface in an oven or with heat gun, air
409 drying, hot air drying at different temperatures, and for different time intervals (Amirian et al.,
410 2017; Bondino et al., 2013; Lebedeva and Fogden, 2010; Song and Kovscek, 2015).

411 In this study, the effect of heat treatment on the stability of the coating is evaluated. For this
412 purpose, straight channel resealable glass micromodels are coated with 10 wt.% Illite clay slurry
413 prepared in 30000 ppm NaCl solution. Two different post-coating treatments were used to dry
414 the coated micromodels. The first treatment involved drying the coated surface with air at room
415 temperature (25 °C) for 1 hour, while in the second method, the clay-coated surfaces were air-
416 dried gradually up to 125 °C for 25 minutes.

417 The release of clay particles from the clay-coated surface could be due to the instability of the
418 coating or the sensitivity of the clay particles to the fluid flowing on it. While the former one
419 depends on how firmly clay particles are attached to the substrate surface, the latter one is a
420 function of salinity or the number of counterions present in the fluid.

421 Prior to evaluating the stability of the coating, it is therefore, crucial to distinguish the release of
422 clay particles owing to clay-brine interaction from that due to the instability of coating. Since
423 the clay particles were already in contact with 30,000 ppm NaCl brine as the clay slurry was
424 prepared with it, 30,000 ppm NaCl brine could be considered, in this case, as the formation
425 water. Thus, the coating can be considered stable if the 30,000 ppm NaCl brine flooding for a
426 sufficient period of time does not cause a significant release of clay particles from the glass
427 surface. Any fluid having salinity less than this may cause the release of clay particles, and the
428 effect is expected to increase as the salinity of the injection fluid gets decreased. Having said
429 that, none of the fluids should completely remove the coating if the coating is indeed stable.

430 To evaluate the sensitivity of the coated surface to the fluid flowing on it, the micromodels were
431 exposed to flooding of base brine (30000 ppm) and the brine of reduced salinity (10,000 ppm)
432 and DI water for six hours. After each flooding, vacuum suction was employed to take away
433 loosely attached clay particles and brine. The fluid flow was conducted at the rates specified in
434 Table 4. These flow rates were chosen to maintain a low capillary number (1×10^{-6}) so that the
435 release of clay particles during the flow is driven by clay-fluid interaction, not by viscous force.
436 Afterward, the surfaces were dried in the oven at 100 °C for 30 minutes to get away with any
437 water left on the glass surface.

438 **3.4.5 Microscopic characterization of coating stability**

439 Following oven-drying, the brine exposed resealable chips were disintegrated. Then, the bottom
440 wall was evaluated with optical and SEM microscopy to observe the coating state after each
441 flooding. It should be noted that the bottom wall of the flow cell had a slightly higher coating
442 density than the top one, hence used for the microscopic analysis. This might be due to the effect

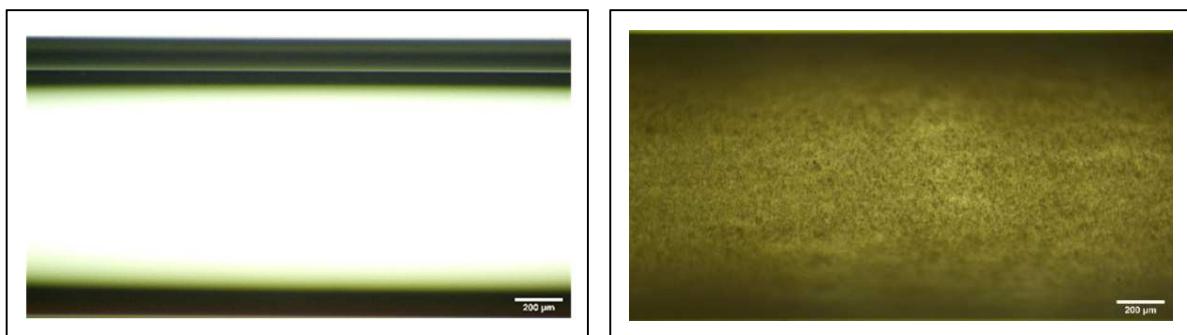
443 of gravity that led to the increased deposition of clay particles on the bottom wall. This
444 observation was consistent with the findings of Zhang et al. (2019) [49].

445 Confocal laser scanning microscopy was used to develop 3D reconstructed images of the mineral
446 coatings on the glass surface following each stability test. The surfaces were excited with 488 nm
447 laser lines, and no fluorescent dyes were added to the samples as the clay particles were auto-
448 fluorescent. Each of the surfaces was divided into a number of slices based on the focus planes,
449 and 2D images taken under the bright-field mode from each of the slices were stacked together to
450 make 3-D reconstructed images of the optical section of the sample. The 3D images provided
451 insights into the effectiveness of heat treatment on the stability of the coating.

452 **4 Results and discussions**

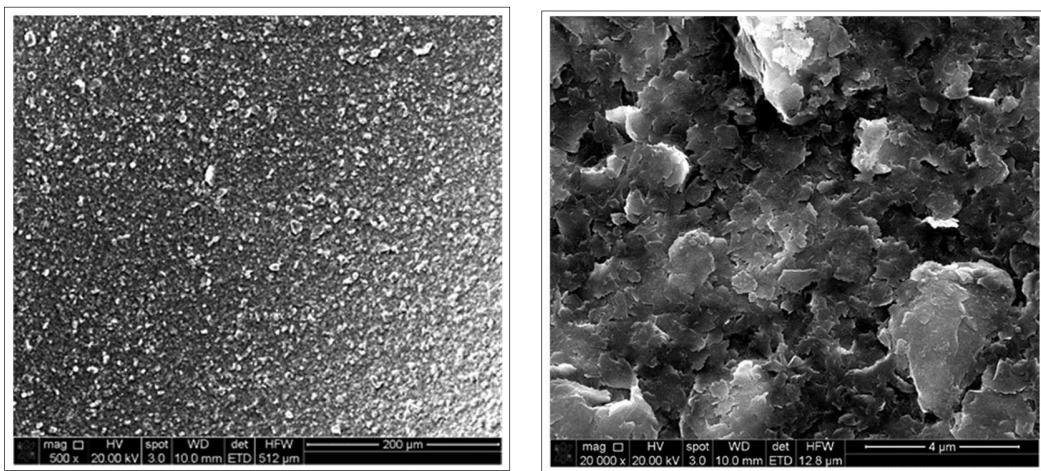
453 **4.1 Functionalizing glass capillary tubes with Illite clay**

454 Figure 4 shows bright-field microscopic images of the uncoated glass capillary tube surface and
455 the surface coated with 10 wt.% Illite clay slurry prepared in 30,000 ppm NaCl brine. With this
456 combination of the solution, a nearly uniform distribution of clay particles was observed on the
457 glass surface, indicating the efficacy of the developed coating procedure.

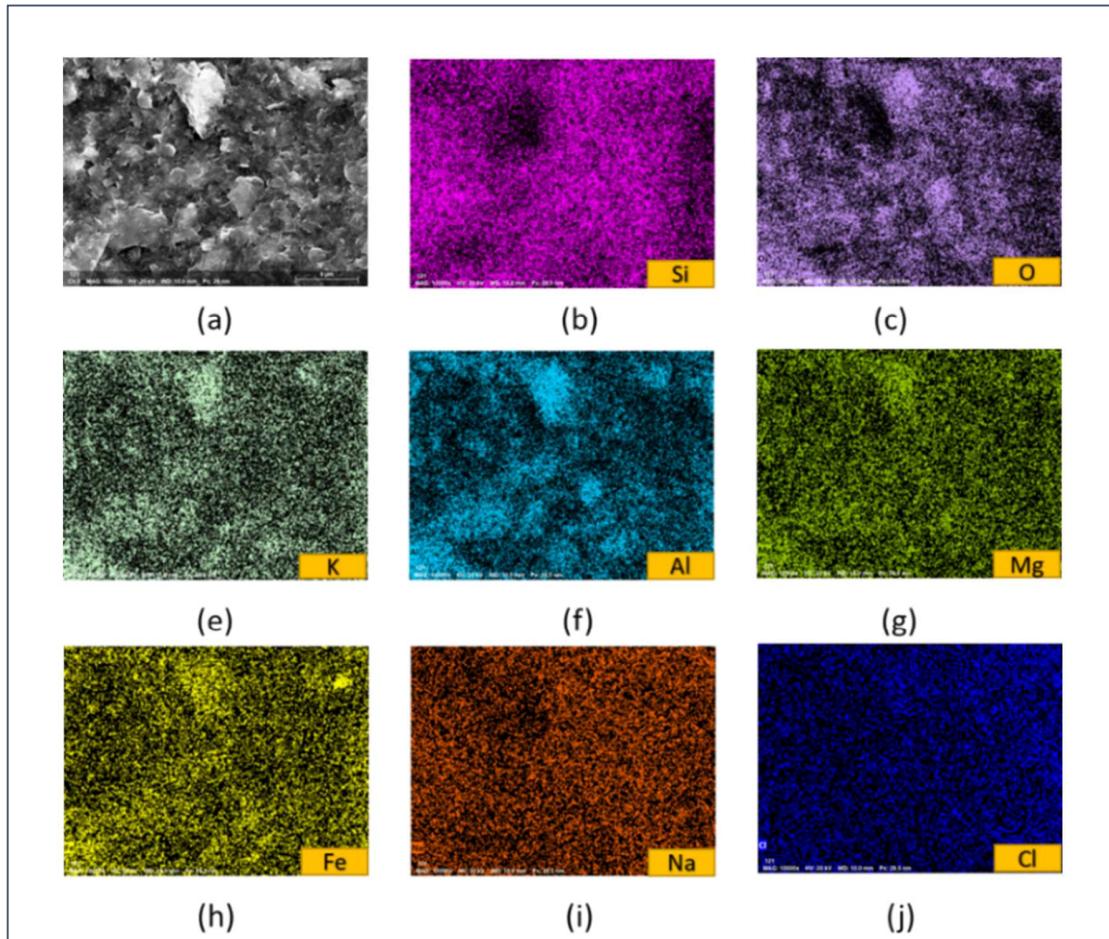


458
459 Figure 4: Microscopic image of the uncoated (left) and Illite-coated (right) glass capillary tube
460 surfaces.

461 Figure 5 shows the Scanning Electron Microscopic (SEM) image of the coated surface at
462 different magnifications. SEM-EDS elemental map of the coated surface is shown in figure 6.
463 Oxygen, Silicon, Aluminum, Potassium, Iron, and Magnesium were the major chemical elements
464 present in the Illite clay (IMt-1) used to coat the glass capillary tubes (Table 2). EDS elemental
465 map indicates the presence of those components on the coated surface as well.



466
467 Figure 5: SEM image of the Illite-coated capillary tube surface at two different magnifications.



468

469 Figure 6: (a) SEM image and (b-j) EDS elemental map of the Illite coated glass capillary tube
 470 surface.

471

472 Table 5 shows the contribution of different components of the clay slurry on the coated surface
 473 as evidenced from the EDS elemental map. Even though, the clay slurry was prepared by
 474 dissolving Illite clay in high salinity NaCl brines, the marginal contribution of both Na and Cl on
 475 the elemental map indicates that only the clay particles were adsorbed on the glass surface.

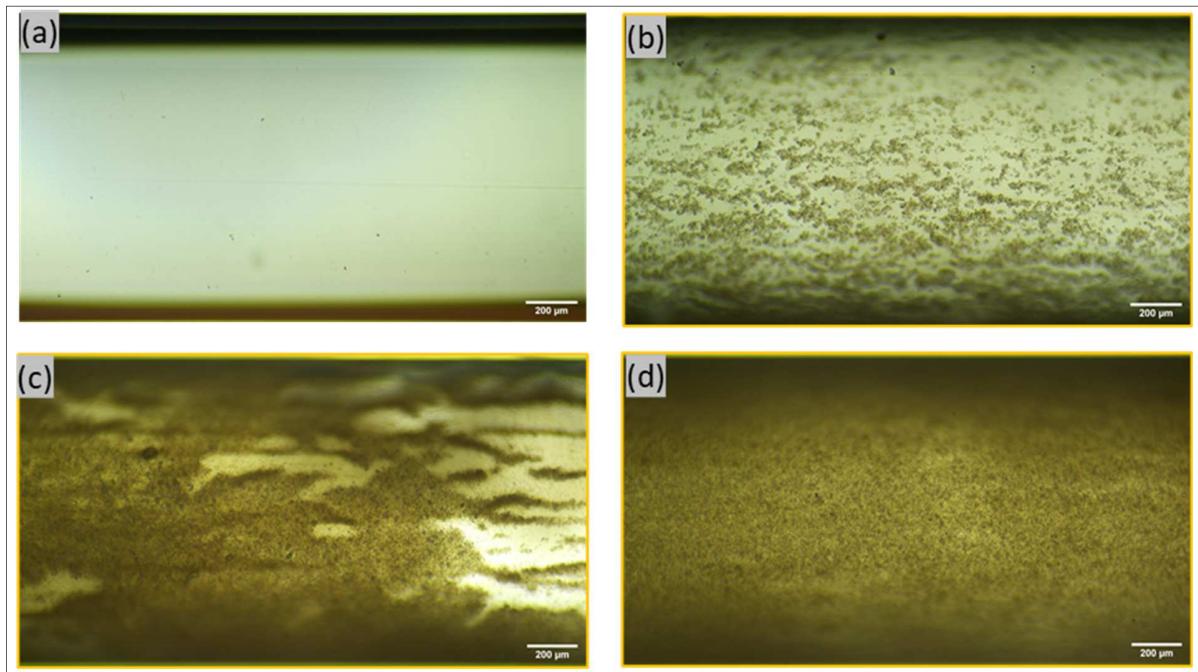
476 Table 5: Contribution of different components of clay slurry on the coated surface as evidenced
 477 from EDS elemental analysis

Element	Mass, [%]	Mass Norm., [%]	Atom, [%]
Carbon	4.77	7.48	12.57
Oxygen	26.50	41.56	52.43
Sodium	0.72	1.13	0.99

Magnesium	0.56	0.87	0.73
Aluminium	5.30	8.31	6.22
Silicon	20.70	32.47	23.33
Chlorine	0.18	0.29	0.16
Potassium	2.96	4.64	2.40
Calcium	0.01	0.02	0.01
Iron	2.06	3.23	1.17
Total	63.75	100.00	100.00

478 **4.2 Effect of salinity on clay coating**

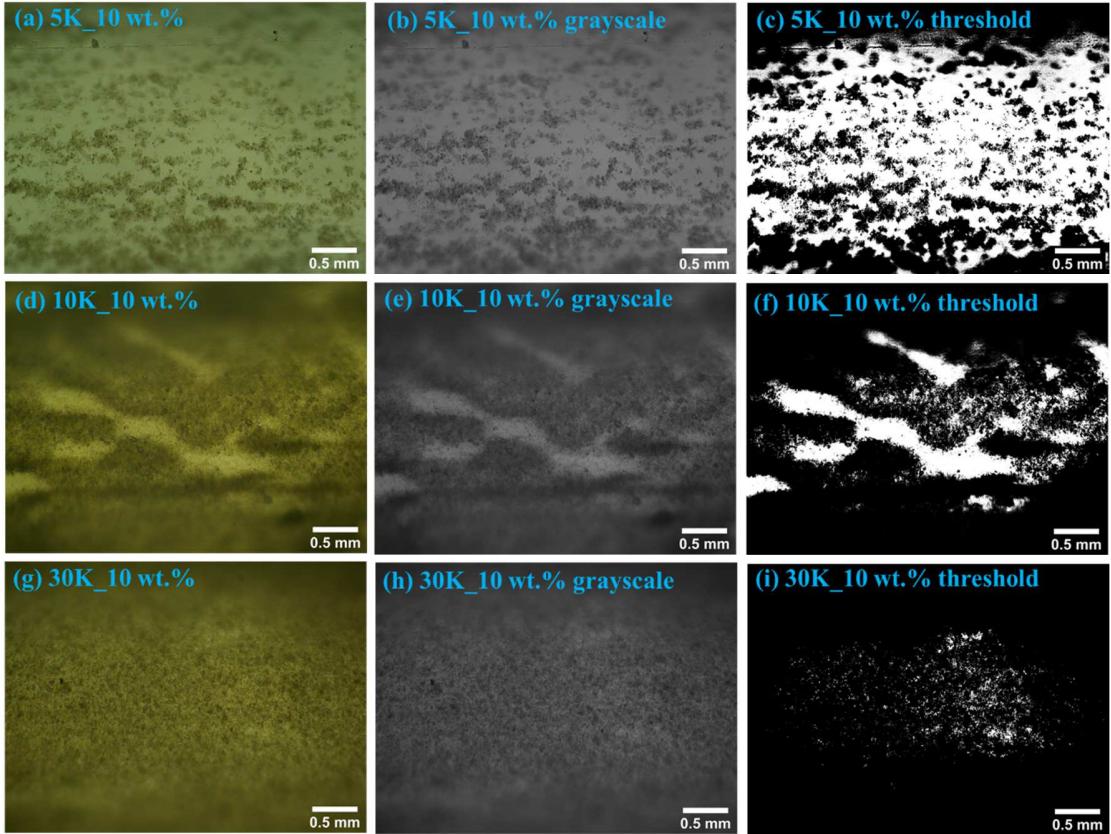
479 Glass capillary tubes coated with 10 wt.% illite clay prepared in NaCl solutions of four different
 480 concentrations (0 ppm, 5000 ppm, 10000 ppm, and 30000 ppm) were created to evaluate the
 481 effect of base fluids salinity on clay adsorption to the glass surface. Figure 7 shows the optical
 482 microscopic images of the surfaces coated with those different clay slurries. It is observed that as
 483 the brine concentration is increased, the coating coverage is improved. When the clay slurry is
 484 created with DI water, there was seemingly no adsorption of the clay particles on the glass
 485 surface. However, with higher concentrations of brine, the number of adsorbed particles
 486 increased, and with 30000 ppm, a quasi-homogeneous coating is observed.



487

488 Figure 7: Glass capillary tubes coated with 10 wt.% Illite clay slurry prepared with: (a) DI water,
 489 (b) 5000 ppm NaCl, (c) 10000 ppm NaCl, and (d) 30000 ppm NaCl. Images are taken after
 490 drying the coated capillary tubes at 25 °C.

491 The coating density approximation (Fig. 8) revealed that, the coating coverage was around 49 %
 492 when the surface was coated with clay in 5000 ppm brine. When the surface was coated with
 493 clay in 10,000 ppm NaCl brine, the coating coverage increased to ~ 85 %. Finally, with 30,000
 494 ppm NaCl, almost 98% coating coverage was obtained.

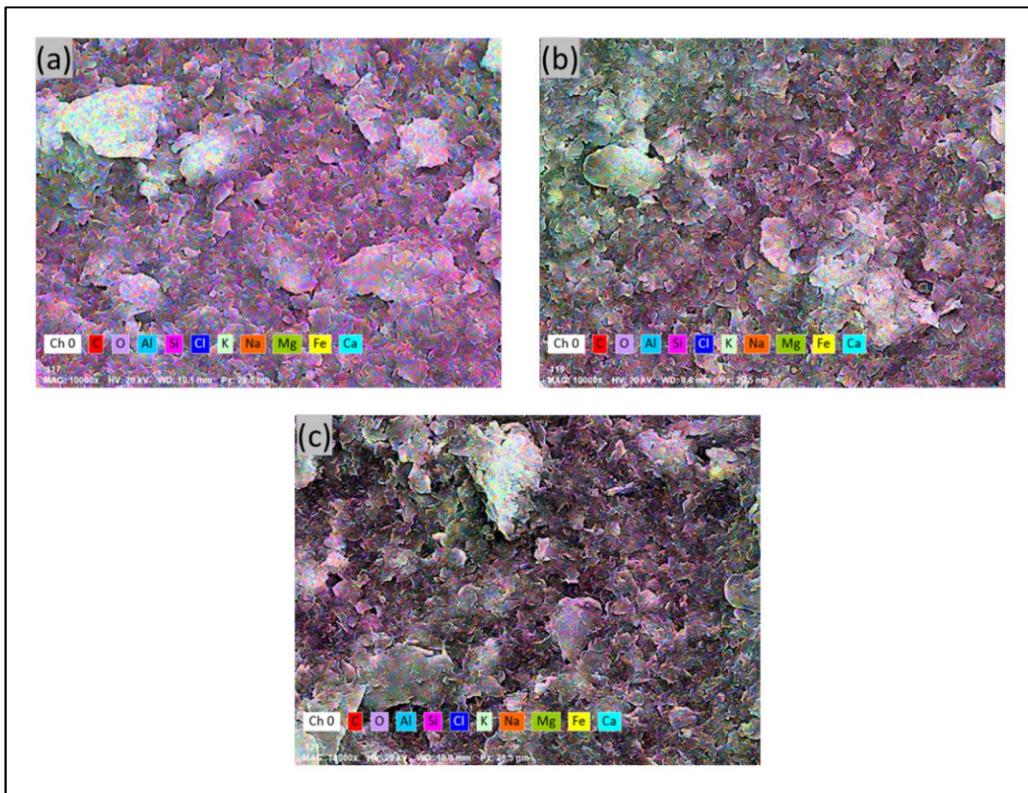


495

496 Figure 8: Coating density approximation with Fiji. High magnification (a, d, g) optical, (b, e, h)
497 8-bit grayscale, and (c, f, i) threshold images of the capillary tube surfaces after coating with clay
498 slurry prepared in (a-c) 5000 ppm, (d-f) 10,000 ppm, and (g-i) 30,000 ppm NaCl brine. The
499 rectangular region is showing the Region of Interest where the coating density is approximated.

500 EDS elemental map (Fig. 9) of the coated surface has also exhibited increased adsorption of clay
501 particles on the glass surface when the slurry is prepared with the high salinity brine. Figure 9 (a)
502 shows that the surface coated with clay slurry prepared in 5000 ppm brine has the elemental map
503 dominated by the presence of silicon (Si). Even though Si is the primary constituent of both the
504 solid substrate and the clay minerals, the significant dominance of silica here indicates the
505 uncoated borosilicate glass surface as the primary source of it. Otherwise, there would also have
506 a significant contribution of other clay components (e.g., Mg, Al, K, Ca, Fe, etc.) on the
507 elemental map similar to figure 9 (b) and figure 9 (c). Increased concentration of brine (10,000
508 ppm and 30,000 ppm) resulted in increased adsorption of clay particles. As a result, the coated

509 surfaces display more distribution of other clay constituents besides Si on the EDS elemental
510 map (Fig. 9 (b) and 9 (c)).



511
512 Figure 9: EDS elemental distribution maps of glass surfaces coated with Illite clay prepared in
513 (a) 5000 ppm, (b) 10000 ppm, and (c) 30000 ppm NaCl solution. The color indexes are showing
514 the presence of different chemical elements on the coated surface. Figure 9 (a) being dominated
515 by purple color indicates less amount of clay adsorption on the glass surface, rendering the
516 surface mostly uncoated. With the increased salinity of brine, a more balanced distribution of
517 clay constituents is displayed in figure 9 (b) and figure 9 (c).

518 This effect of salinity on clay adsorption can be explained with the DLVO theory and attributed
519 to the net effect of electric double layer (EDL) repulsive forces and Van der Waals attractive
520 forces between the clay particles and the glass surface. It is well known that clay particles have a
521 net negative surface charge, and glass surface, due to the dissolution of the silanol group, also
522 exhibits a negative surface charge. However, the surface charge of the clay particles or glass
523 surface might exhibit charge reversal from negative to positive at a high brine concentration or

524 even at a low concentration when the pH is in the acidic region due to the adsorption of H^+ ions
525 on the mineral surface. Since the pH of the clay slurries used in this study is not in the acidic
526 range (Tab. 3), the effect of the H^+ ion may not be applicable here. This leads us to the
527 possibility of charge reversal only due to the effect of high salinity brine.

528 However, for Illite clay particles and Quartz (the primary constituent of glass) to become
529 positively charged at the alkaline pH regions, the brine concentration must be higher than the
530 seawater (Shehata and Nasr-El-Din, 2015). At the alkaline pH region, the ζ -potential values of
531 Illite clay and Quartz in seawater (~38,000 ppm NaCl) are reported to be -5.3 mV and -2.5 mV,
532 respectively. The ζ -potential values get further decreased (increase in the negative value) as the
533 brines get diluted. The maximum brine concentration (30,000 ppm) used in our study is less than
534 the seawater salinity. Therefore, in the attempt to explain the effect of brines salinity on DLVO
535 forces, we assumed that the brine concentrations used in this study are not sufficiently high, and
536 the pH of the solution is not low enough to reverse the surface charge of either the clay particles
537 or the glass surface; hence both of the surfaces behave as negatively charged.

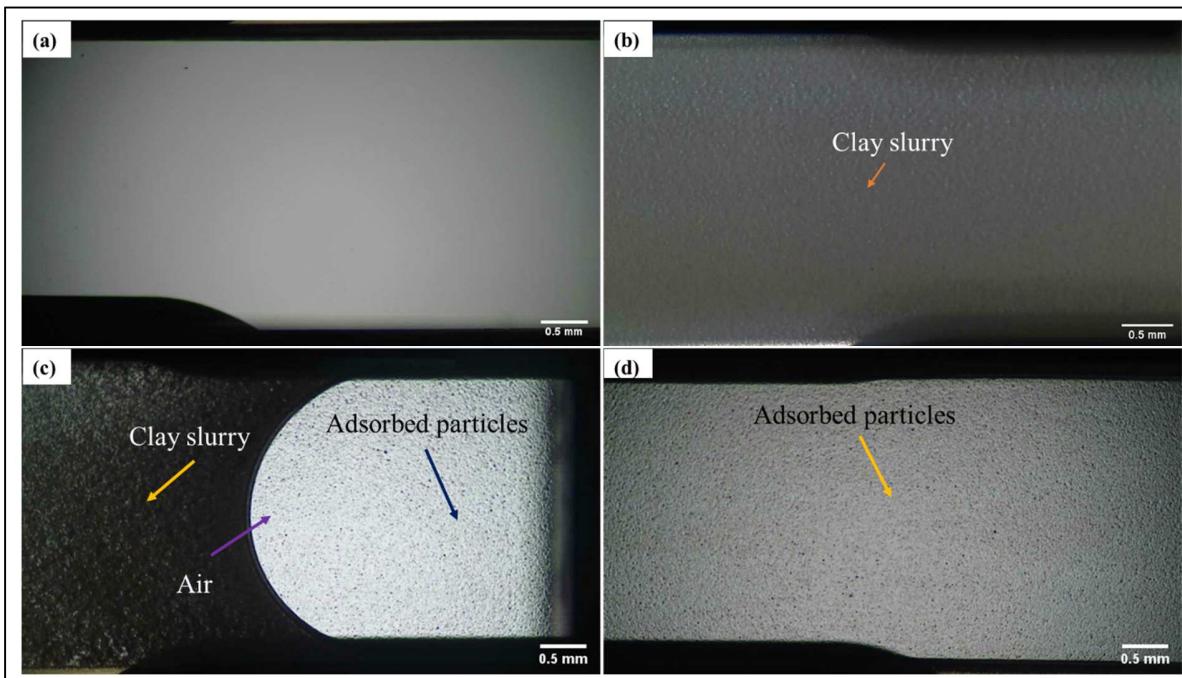
538 The development of a net negative charge on the clay particles' surface would cause an increased
539 concentration of counterions from the surrounding fluid in the interfacial region (electrical
540 double layer). However, in the case of clay solution prepared with deionized water or low
541 salinity brines, the lack of counterions causes expansion of the double layer (increase in Debye
542 Length). Therefore, double layer repulsive forces between the particles and glass surface
543 dominate over the effect of weak Van der Waals attractive forces between the particles and the
544 surface, hence not allowing the particles to get adsorbed on the glass surface.

545 As the brine concentration or the ionic strength of the clay solution increases, increased
546 concentration of counterions from the surrounding fluid suppresses the thickness of the double
547 layer (Debye Length). The extent of the repulsive forces also gets diminished.

548 In simpler words, as the ionic strength increases, the negative surface potential of the clay
549 particles starts to get dropped off by the positive ions. Hence, the effect of electrostatic repulsive
550 forces between the particles negates, and at a certain concentration of brine, Van der Waals
551 attractive forces between the particles and the glass surface become the dominant force driving
552 the adsorption of clay particles to the glass surface. The higher the effect of Van der Waals force,
553 the better the adsorption would be. Therefore, we have seen an increase in the coating density
554 with higher concentrations of brine, and at 30,000 ppm, a complete coverage of glass surface
555 with clay particles was observed.

556 **4.3 Preparing clay-coated micromodel**

557 Figures 10 shows different states of the resealable microfluidic chip surface before and during
558 the coating experiment. As can be deduced from the figures, the microfluidic chip was
559 completely saturated with clay slurry and the vacuum suction of air from the chip outlet resulted
560 in a very effective displacement of clay slurry and uniform distribution of adsorbed particles on
561 the glass surface. Figure 11 shows the high magnification optical microscopic image of the Illite
562 coated micromodel surface.



563
564 Figure 10: Micromodel surface at different states: (a) uncoated surface, (b) completely saturated
565 with clay slurry after infusion, (c) vacuum suction leading to a uniform displacement of clay
566 slurry, and (d) even distribution of adsorbed clay particles on the glass surface after complete
567 withdrawn of the clay slurry.

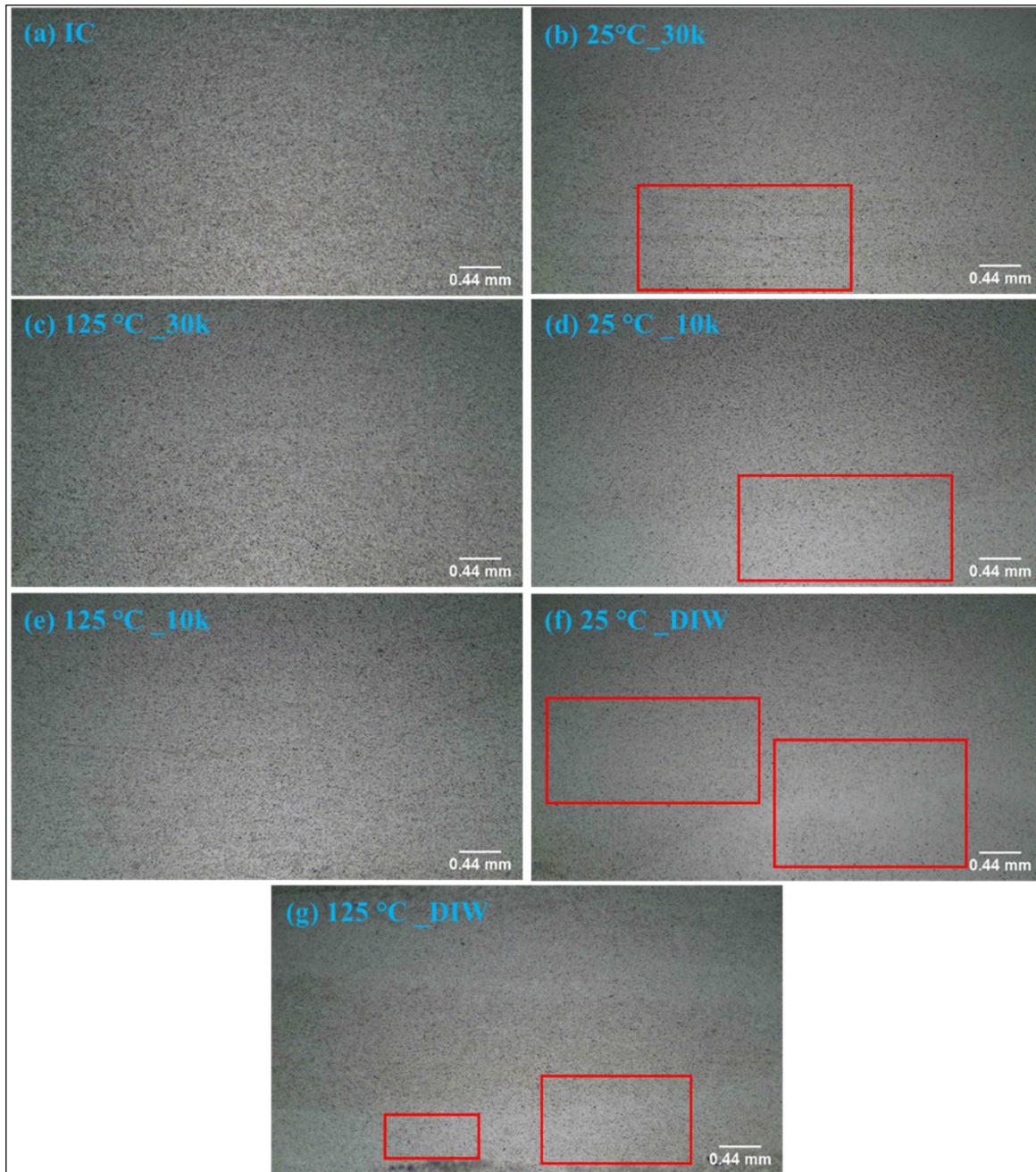


568
569 Figure 11: High magnification image of the dried micromodel surface after Illite-clay coating.
570

571 **4.4 Effect of heat treatment on coating stability**

572 **4.4.1 Stability characterization using optical microscopy**

573 Figure 12 shows the optical microscopic images of the Illite coated surfaces after being exposed
574 to brines of different concentrations and deionized water (diw) for 6 hours. Comparisons
575 between figure 12 (a), 12 (b), and 12 (c) indicate that the surface dried at 125 °C has more
576 similarity in coating appearance with the initial state than the one dried at 25 °C, where the
577 release of clay particles is visually detectable. This implies that drying the clay-coated
578 micromodel at 125 °C temperature improves the stability of the coating.



579

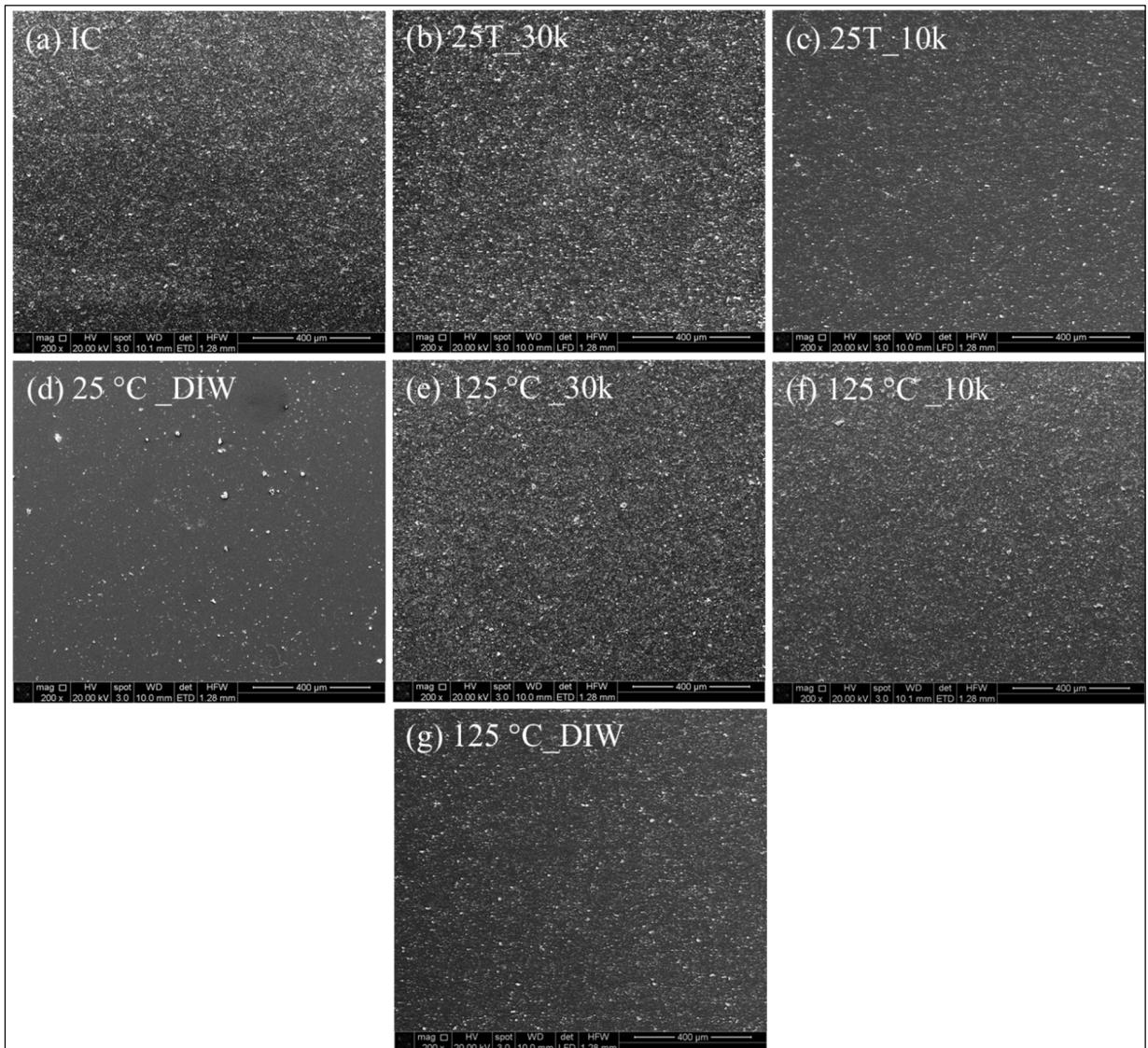
580 Figure 12: Optical microscopic images of the (a) initial state of the Illite-coated micromodel
 581 surface before flooding any fluid, state of the coated surface dried at (b) 25 °C and (c) 125 °C
 582 after exposed to 30,000 (30k) ppm NaCl brine, surface dried at (d) 25 °C and (e) 125 °C
 583 exposed to 10,000 (10k) ppm NaCl, and surface dried at (f) 25 °C and (g) 125 °C exposed to
 584 deionized water (DIW) for 6 hours during the dynamic flooding test. Red rectangles are showing
 585 some of the washout zones in the coated surface from where the clay particles are washed away
 586 or might have migrated to other locations as the surface came in contact with the liquids.

587 Figures 12 (d-g) reveal that, regardless of what temperature was used to dry the coated surface,
588 fluids with salinity less than 30,000 ppm brine caused detachment of the clay particles in both
589 types of surface. This implies that the heat treatment did not make the coating completely
590 immobile. However, the degree of sensitivity of the clay particles with the brines was affected by
591 the heat treatment. Compared to the Illite-coated surfaces dried at 25 °C, the surfaces treated at
592 125 °C temperature retained more particles attached to the surface following the flow of lower
593 salinity brines and deionized water.

594 **4.4.2 Stability characterization using scanning electron microscopy**

595 Similar to optical images, SEM images also exhibit a resemblance in the coating appearance
596 between the initial condition (Figure 13 (a)) and the 125 °C treated surface exposed to 30,000
597 ppm brine flooding (Figure 13 (e)). However, unlike the optical image (Figure 12 (b)), SEM
598 image of the 25 °C treated surface (Figure 13 (b)) shows a relatively denser coating than the
599 initial state (Figure 13 (a)). This might be due to the very small field of view usually associated
600 with SEM images and localized accumulation of clay particles being migrated from another
601 location of the surface. Nevertheless, this also implies that the 25 °C treated surface was more
602 prone to clay detachment than the one treated at 125 °C.

603 The effect of heat treatment is more evident in the SEM images of the coated surfaces exposed to
604 low salinity brines (salinity < 30,000 ppm) and deionized water (Fig. 13 (c), 13 (d), 13 (f), and
605 13 (g)). Even though the release of particles is visible in both types of surfaces, the surface-
606 treated at 25 °C was affected the most.



607

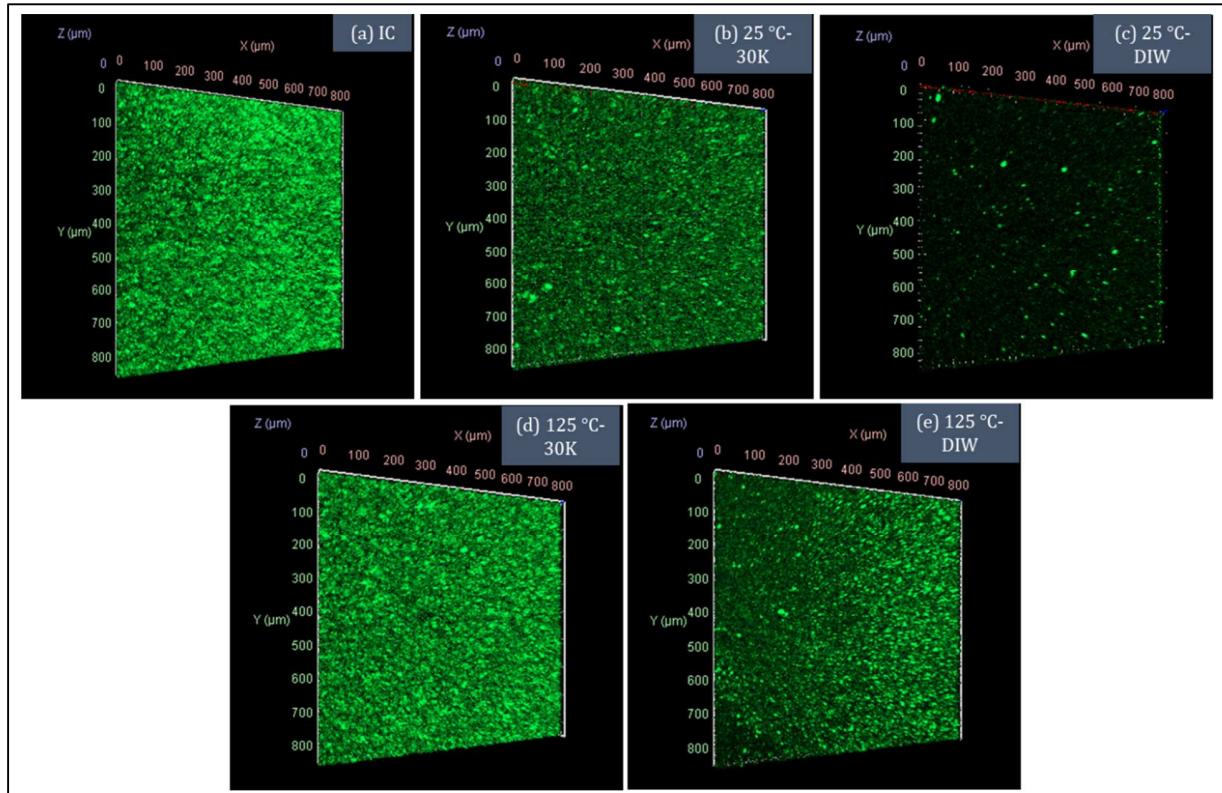
608 Figure 13: SEM images of the coated surfaces after exposed to brines of different concentrations
 609 for 6 hours. Figure 13 (a) shows the initial condition (IC) of the coated surface before flooding
 610 any fluid; (b) state of the coated surface dried at 25 °C after exposed to NaCl brines of 30,000
 611 ppm (30K), (c) 10,000 ppm (10K), and (d) deionized water (DIW) for 6 hours; Figure 13 (e)
 612 shows the state of the coated surface dried at 125 °C after exposed to NaCl brines of 30K ppm,
 613 (f) 10K ppm, and (g) DIW for 6 hours.

614

615 4.4.3 Stability characterization using confocal laser scanning microscopy

616 Confocal laser scanning microscopy (CLSM) was used to further confirm the improved stability
 617 of the coated surface treated at 125 °C. Figure 14 shows the 3D reconstructed images of the
 618 coated surfaces after being exposed to 30,000 ppm NaCl brine and deionized water. The surfaces

619 were excited with 488 nm laser lines. No fluorescent dyes were applied to the auto-fluorescent
 620 clay minerals. Clay particles adsorbed the laser lights and caused the green fluorescence visible
 621 in figure 14.



622
 623 Figure 14: 3D reconstructed images of the mineral coatings over the glass surface showing the
 624 state of coating at different conditions. (a) The initial condition (IC) of the coated surface before
 625 flooding any fluid ; (b-c) state of the coated surface dried at 25 °C after being exposed to 30,000
 626 ppm (30K) NaCl brine and deionized water (DIW) for 6 hours; (d-e) state of the coated surface
 627 dried at 125 °C after being exposed to 30,000 ppm NaCl brine and deionized water for 6 hours.
 628 Each image has the size of 848.53 μm × 848.53 μm × 40.5 μm.

629 Following the 30,000 ppm brine flooding, the surface treated at 125 °C exhibited more similarity
 630 in coating appearance with the initial state of the coating than the one treated at 25 °C. The
 631 surface dried at 25 °C and exposed to 30,000 ppm NaCl flow, displayed fewer green
 632 fluorescence when excited with the laser beams, indicates that a good number of clay particles
 633 have already been washed away from the surface.

634 The effect of heat treatment is more evident in the case of DI water flooding. Coating treated at
635 25 °C experienced wash away of most of the clay particles during the DI water flooding, as it can
636 be deduced from the dearth of green fluorescence in Figure 14 (c). However, even though 125 °C
637 treated surface also experienced some release of clay particles due to DI water flow, thus
638 corroborating the fact that natural mobility of the clay particles was not compromised by the
639 heat-treatment, the 125 °C treated surface had considerably more clay particles remained
640 attached to the surface following the flooding compared to the one treated at 25 °C. These
641 observations are consistent with the findings from optical and SEM image analysis.

642 **5 Conclusion**

643 In this study, Illite-coated surfaces were successfully generated in borosilicate glass capillary
644 tubes and resealable straight channel microfluidic chips made of borosilicate glass. It was
645 observed that vacuum suction of air to displace clay slurry from the flow volume produced a
646 very uniform and even distribution of clay particles on the glass surface. NaCl solution was used
647 as the base fluid to prepare the clay slurry required to inject into the capillary tubes and
648 microfluidic chip. The salinity of the NaCl solution was found to have a significant effect on the
649 adsorption of clay particles to the glass surface. Based on the microscopic characterization and
650 coating density approximation with Fiji, this study has shown that if the salinity or ionic
651 concentration of the base fluid is increased, a more dense and uniform clay coating could be
652 obtained on the glass surface. In this study, the slurry prepared with deionized water rendered no
653 adsorption of clay particles on the surface, whereas with 30,000 ppm NaCl brine a more uniform
654 and dense distribution of clay particles was observed.

655 The micromodel dried at 25 °C performed poorly even when contacted with the high salinity
656 brine. There were considerable detachments of the clay particles from the glass surface at
657 different locations. Deionized water caused the maximum damage as several wash-away zones
658 of the coated layer was seen in the optical, SEM, and CLSM images. In contrast, there were not
659 such detachments of the clay particles from the 25 °C treated glass surface when exposed to the
660 high salinity brine flooding for 6 hours. The temperature was enough to keep the particles firmly
661 attached to the surface without compromising the natural mobility of the clay particles. The
662 particles from a few locations got eventually detached when the surface came in contact with
663 lower salinity brine and deionized water.

664 **6 Acknowledgment**

665 We acknowledge the financial support (Award Number: DE-FE0031776) from the U.S
666 Department of Energy (DOE) and Continental Resources Inc. We thank Dr. Jim Puckette for his
667 help in providing and preparing the clay samples. We also thank Mr. Sushobhan Pradhan and
668 Mr. Brent Johnson for their support during the microscopic analysis.

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