



16th International Conference on Greenhouse Gas Control Technologies, GHGT-16

23rd -27th October 2022, Lyon, France

Oxygen Solubility in Aqueous Amine Solvents with Common Additives Used for CO₂ Chemical Absorption

Thomas B. Jorgensen^{a,b}, Jesse Thompson^{a,b,*}, Moushumi Sarma^a,

Keemia Abad^{a,b}, Kunlei Liu^c

^aUniversity of Kentucky, Center for Applied Energy Research, Lexington, KY, United States

^bUniversity of Kentucky, Department of Chemistry, Lexington, KY, United States

^cUniversity of Kentucky Department of Mechanical Engineering, Lexington, KY, United States

Abstract

Major sources of anthropogenic CO₂ are power generation and transportation industries where researcher continue to explore CO₂ emission mitigation strategies as applied to these CO₂ sources through carbon capture, utilization, and sequestration (CCUS). The most mature CO₂ capture technology is post-combustion carbon capture (PCCC) using aqueous amine solutions/solvents, however solvent degradation and regeneration costs are slowing the widespread adoption of PCCC. Solvent degradation of the aqueous amine solutions is mainly caused from the temperature gradient between the absorber and stripper columns and common flue gas components such as SO_x, NO_x, and oxygen (O₂). The two main classifications of solvent degradation are thermal degradation, occurring when the amine reacts with itself at elevated temperatures and anaerobic conditions and oxidative degradation. Oxidative degradation reactions can occur from oxygen mass transfer and free radical oxidation. Metals, such as iron from the corrosion of steel structures used in industrial applications such as PCCC, can help to catalyze these reactions. Various oxidative degradation studies have shown how O₂ concentrations in flue gas and, to a lesser extent, temperature influence the extent of oxidative degradation.

Accurately measuring the O₂ solubility, commonly referred to as dissolved oxygen (DO), in a quick, continuous, and efficient manner in aqueous amine solvents should contribute to determine the effectiveness of mitigation strategies for oxidative degradation. Knowing that commercial PCCC amine solvents contain components beyond water, amine, carbonate species and CO₂, this investigation was conducted to determine the oxygen solubility changes of common aqueous amines solutions with commonly used and published solvent additives. The impact of carbon loadings with and without the additives was also examined. A commercial dissolved oxygen probe was used to measure the DO concentrations and compared them against standard Winkler Method titration values. The results show that antifoam shows minimal change in [DO]. MBT yielded lower DO values, and NaVO₃ showed a higher DO concentration due to interferences. These results indicate that most common amine solvent additives should be expected to minimally impact oxygen solubility and amine oxidative degradation.

Keywords: CO₂ capture; Dissolved oxygen; Oxidative degradation; Winkler Method

* Corresponding author. Email address: jesse.thompson@uky.edu

1. Introduction

The increase in atmospheric CO₂ from anthropogenic sources in the past few decades raises global concerns about effects of climate change. [1] One research field, carbon capture, utilization, and sequestration (CCUS), attempts to discover a cost-effective and viable option for combating global climate change by removing atmospheric CO₂ and then sequestering or utilizing it. [2] The most researched CCUS technique, amine scrubbing post-combustion decarbonization, separates and captures CO₂ from a combustion process's flue gas producing a pure CO₂ stream. While the amine scrubbing process is well known, understanding the amine's solvent degradation and regeneration energy still challenges researchers.

Aqueous amine solvents can be a significant portion of the operating cost of CO₂ capture systems, with some costing over \$40 per kg. If you consider a \$40 per kg amine solvent that degrades at 0.5 kg per CO₂ ton captured, [3] this solvent will cost \$20 per ton of CO₂ captured in terms of solvent replacement from degradation. If this solvent is used at a plant that captures 1 million CO₂ tons per year, then the solvent replacement will cost \$20 million per year. This significant operating cost makes understanding and mitigating solvent degradation a key priority.

Typically, two mechanisms are used to describe degradation including from flue gas contaminants such as O₂ or SO_x and NO_x, and the variable heat gradients in the process. [4] In thermal degradation, a carbamate utilizes the stripper's high temperature and pressure atmosphere to react with itself forming product favored compounds. The other mechanism, known as oxidative degradation, involves O₂ or trace NO_x and SO_x gases becoming radicals through dissolved metal catalysis.

Previously studied mitigation methods for solvent degradation include thermal reclaiming, electrolysis, and ion exchange resins which help maximize the solvent's lifetime. [5] Some recently developed strategies such as N₂ purging [6] or with additive usage [7] show promise but are unproven for long-term treatment. Researchers seem preferential to these proactive strategies because they can stop degradation from occurring. Before deciding if the proactive strategies are effective and viable options, a reliable quantification method is needed. Since oxidative degradation starts with oxygen dissolving into the amine solvent and causing oxidation, accurately measuring dissolved oxygen (DO) can help to quantify the potential for oxidation within the solvent system.

According to ASTM D888[8], three standard analytical methods measure DO in water: a colorimetric titration known as the Winkler method, a polarographic DO electrochemical probe, and luminescence probe. The Winkler method determines O₂ solubility by using redox and acid-base reactions [9] whereas the polarographic probe determines DO by contact with an electrode through an oxygen permeable membrane. The luminescence probe uses dyes to determine DO and is sensitive to light [10] and was not used in this study. The Winkler method and the electrochemical probe are standardized for natural waters and therefore are unverified for aqueous amine solvents which have high pH (typically 10 to 12) depending on carbon loading and concentration.

With an understanding of the standard analytical methods for measuring DO, a commercially available DO electrochemical probe was validated with calculations determined from a modified Winkler method titration. The probe provided consistent and reliable results compared to the modified Winkler method indicating that this type of probe can be used to quantify oxidation in CCUS.

Nomenclature

DO	Dissolved Oxygen
CCUS	Carbon Capture, Utilization, and Sequestration
PCCC	Post Combustion Carbon Capture
HSS	Heat Stable Salts
EDA	1,2 -ethyldiamine

HDA	1,6 – hexadamine
A2P	1-amino-2-propanol
2A1P	2-amino-1-propanol
DEA	diethanolamine
DMEA	dimethylethanolamine
MDEA	Methyldiethanolamine
NMEA	N-methyl-ethanolamine
2EAE	N-ethylamino-ethanol
MEA	ethanolamine
PZ	piperazine

2. Materials and Methods

2.1. Materials

Sigma Aldrich - 1,2-ethyldiamine (EDA), 2-amino-1-propanol (2A1P), Methyldiethanolamine (MDEA), N-methyl-ethanolamine (NMEA), N-(ethylamine)-ethanol (2EAE). TCI America - 1,6-hexadamine (HDA), Acros Organics - 1-amino-2-propanol (A2P), Diethanolamine (DEA), Dimethylethanolamine (DMEA), Piperazine (PZ). Alfa Aesar - Monoethanolamine (MEA).

VWR - Manganese (II) sulfate (MnSO_4) ACS reagent (98%), Potassium iodide (KI) ACS reagent (99%), Sodium thiosulfate pentahydrate ($\text{Na}_2\text{S}_2\text{O}_3 \cdot 5\text{H}_2\text{O}$) ACS reagent (99%). J.T. Baker's - Potassium iodate (KIO_3) ACS reagent (99.4% - 100.4%). Fisher Scientific - Potassium hydroxide (KOH) ACS reagent (88.5%), potato starch, and concentrated sulfuric acid (H_2SO_4), Acros Organics - sodium azide (NaN_3) (99%), Pharma-AAPER's - Chloroform (CCl_4). Pure CO_2 gas obtained from American Welding and Gas.

2.2. Sample Preparation

The aqueous amines solvents, listed in **Fig. 1**, were prepared as described by Jorgensen *et al.* [11]

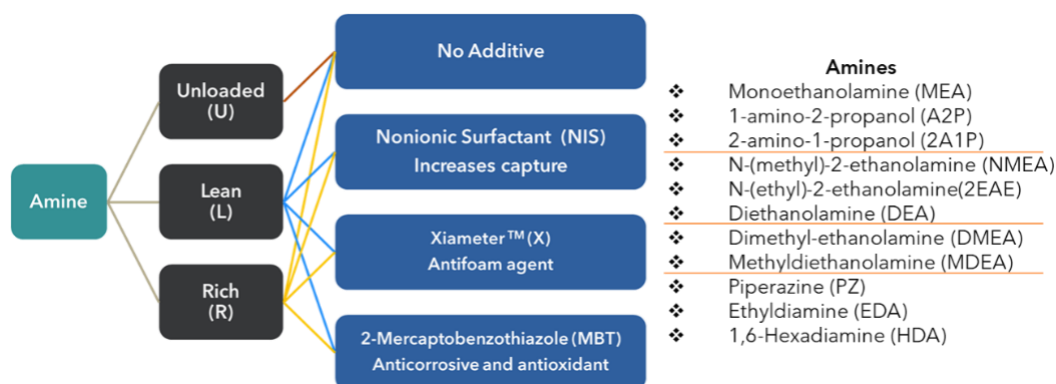


Fig. 1: Sample preparation flow chart and the amine solvents used for this work. The lines separate the amine list by structure. Primary, secondary, and tertiary amine solvents were prepared at 5M, diamines were prepared at 2.5M.

2.3. Electrochemical Dissolved Oxygen Probe

Electrochemical DO probes measure the signal produced by the oxygen reduction to hydroxide at a gold cathode separated from a solution by an oxygen permeable membrane. The current and O_2 partial pressure are proportional, and the converted current will readout a concentration. This study used a Thermo Scientific Orion Versa Star RDO/Dissolved Oxygen Temperature Module Dissolved Oxygen probe that is recommended for natural water ecosystems. A 10% random sampling of the DO probe's measurements in aqueous amine solvents were verified by triplicated Winkler method titrations. The DO probe calibration was conducted weekly by a two-point calibration using water saturated ambient air and zero oxygen standard (Ricca Chemical Co.) as recommended by the manufacturer. Deionized water and 5 wt.% sodium sulfite check standard solutions at 25°C and atmospheric conditions were used to verify calibration.

A water bath maintained at 25°C or 40°C target temperatures with a magnetic stir plate allowed the aqueous amine samples to continuously stir and remain open to ambient air. The measured DO concentration started with placing the DO probe into the aqueous amine samples. The probe equilibrated with the sample for, at minimum, five minutes ensuring the oxygen permeable membrane contacted the solution with no bubbles to provide stable readings.

2.4. Winkler Method

The redox reactions that comprise the traditional Winkler method (**Fig. 2**) start by manganese (II) hydroxide reacting with DO forming manganese (IV) oxide (equation 1). Next, add in potassium iodide under basic conditions which oxidizes iodide to iodine (equation 2). After, acidify the reaction and produce triiodide and a red-brown color (equation 3). A dark blue color appears with starch indicator and when titrated with thiosulfate reduces triiodide to iodide and a colorless solution (equation 4).

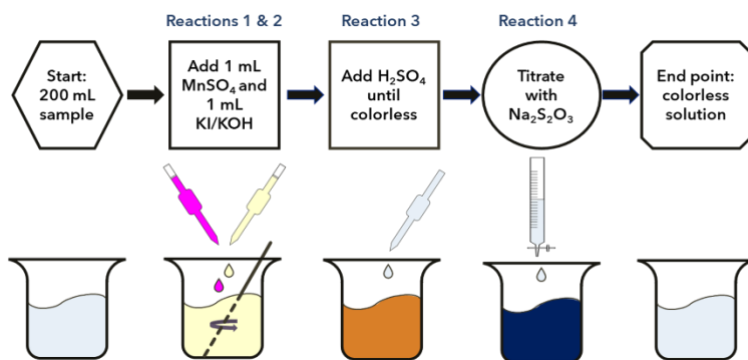


Fig 2. Diagram for the traditional Winkler method steps

Typically, an aqueous amine solvent's pH is between 9 and 11, and the exothermic reaction from adding acid to decrease the pH can increase the reaction temperature above iodine's boiling point and evaporating it. The decrease in iodine's concentration directly correlates to the calculated DO concentration. A backwards titration, proposed by

Wang *et al.* [12], allows iodine to stay in solution. The backwards titration adds in thiosulfate before the acid and where triiodide reduces to iodide a colorless solution with starch added in. When titrated with iodate, iodide oxides back to iodine (equation 5). Then using equation 6 DO mg L⁻¹ can be calculated.



$$[\text{O}_2] = \frac{8000}{V_{\text{Sam}}} \left([\text{Na}_2\text{S}_2\text{O}_3] \times V_{\text{Na}_2\text{S}_2\text{O}_3} - 6 \times [\text{KIO}_3] \times V_{\text{KIO}_3} \right) \quad (6)$$

Following the method outlined in Jorgensen *et al.* [11] this study performed the traditional Winkler method for deionized water equilibrated with ambient air and the modified Winkler method for the aqueous amine solvents.

3. Results and Discussion

3.1. Challenges with the Winkler Method

Wang *et al.* [12] presented MEA's DO concentrations to model oxidative degradation. The one important aspect of this work related to O₂ solubility when adding sulfuric acid and its exothermic reaction causing iodine to evaporate (at ~30°C). [8] The authors explained that adding excess thiosulfate and performing a backwards titration using KIO₃ as the titrant will overcome iodine evaporation. To reproduce the backwards titration described by them, **Fig. 3** describes the challenges the modified Winkler method gave and our recommendations to use this method in amine solvents.

With an unloaded 5M amine solution, five replicated titrations using the modified Winkler method as Wang *et al.* [12] resulted in negative or low values that ranged between -9.60 mg L⁻¹ and 3.20 mg L⁻¹. The negative calculated results indicated lower-than-expected iodate or iodine concentration due to temperature reaching above 40°C.

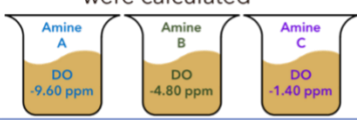


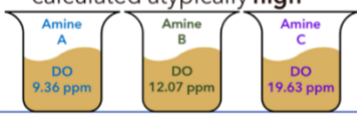


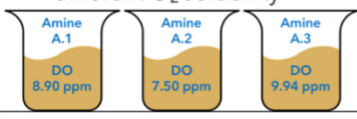
Winkler Method Challenges	Our Recommendation	Why
Negative O₂ concentrations were calculated 	Monitor temperature and keep sample in an ice bath 	Acid-base exothermic reaction can vaporizes I₂ $T_{\text{vap}} = 30^\circ\text{C}$ 
O₂ concentrations were calculated atypically high 	Prepare S₂O₃²⁻ 12 to 15 hours before use 	S₂O₃²⁻ oxidizes to SO₄²⁻ at ambient conditions $\text{S}_2\text{O}_3^{2-} + 3\text{O}=\text{O} + \text{H}_2\text{O} \rightarrow 2\text{SO}_4^{2-} + 2\text{OH}^-$ 
Replicated samples calculated different O₂ solubility 	Standardize S₂O₃²⁻ and IO₃⁻ before use $[\text{O}_2] = \frac{250 \times \text{mw}_{\text{O}_2}}{V_{\text{sample}}} \left([\text{S}_2\text{O}_3^{2-}] \times V_{\text{S}_2\text{O}_3^{2-}} - 6 \times [\text{IO}_3^-] \times V_{\text{IO}_3^-} \right)$	[S₂O₃²⁻] and [IO₃⁻] impact the calculation

Fig 3: The challenges and recommendations when performing the modified Winkler Method.

Next, five titrations with unloaded 5M amine were performed with the reaction flask placed in an ice bath to manage the reaction temperature. These five samples resulted in high calculated O_2 solubility values that ranged between 9.36 mg L^{-1} and 19.63 mg L^{-1} with a $12.67 \pm 4.10 \text{ mg L}^{-1}$ average. The high calculated O_2 solubility indicated a higher-than-expected thiosulfate concentration. Upon further investigation, thiosulfate oxidizes in the presence of O_2 is producing SO_4^{2-} (equation 7). [8, 13] Therefore, to overcome thiosulfate oxidizing to sulfate, the thiosulfate solution was prepared 12 to 15 hours before use.



Using both the ice bath and thiosulfate preparation modifications, an additional five titrations with unloaded 5M amine resulted in reasonable calculated O_2 solubility that ranged between 6.72 mg L^{-1} and 9.94 mg L^{-1} and an average of $8.32 \pm 1.12 \text{ mg L}^{-1}$. The same five samples measured with the electrochemical DO probe resulted in a $6.93 \pm 0.27 \text{ mg L}^{-1}$ average. When comparing the two methods' O_2 solubility value, the Winkler method results in a higher O_2 solubility value and a high standard deviation. When looking closer into equation 6 slight deviations in the thiosulfate and iodate concentrations can cause significant change to the calculated O_2 solubility value. Therefore, accurate standardization of the thiosulfate and iodate concentrations can correct the Winkler method deviation and lead to more accurate O_2 solubility calculations.

Table 1: Modified Winkler method calculated DO values compared to electrochemical probe measurements after last modification

Sample	Winkler Method (mg L^{-1})	Electrochemical Probe (mg L^{-1})	Variance
1	6.06	6.63	
2	6.30	7.18	
3	5.54	7.20	
4	6.15	6.68	
5	6.75	6.96	
Average	6.16 ± 0.44	6.93 ± 0.27	-0.77

Finally, five unloaded amine samples were titrated with thiosulfate and iodate standardized from an adapted ASTM-1510 [14] producing a $6.16 \pm 0.44 \text{ mg L}^{-1}$ calculated O_2 solubility average with a range of 5.54 mg L^{-1} and 6.75 mg L^{-1} . Comparing the calculated modified Winkler method O_2 solubility with the measured electrochemical DO probe an observed difference of 0.77 mg L^{-1} as shown in **Table 1**.

3.2. Validation

With the modified Winkler method and the electrochemical DO probe giving comparable results for a single sample, the DO for a 5M monoethanolamine (MEA) solvent at unloaded ($C/N = 0$), lean loaded ($C/N = 0.20$), and rich loaded ($C/N = 0.40$) conditions were calculated using the modified Winkler method titration and measured with the electrochemical probe. The results, shown in **Fig. 4**, determine the titration calculated the O_2 solubility are in good agreement, with the probe showing only slightly higher values. One possible reason for this is the thiosulfate being added into the solution may have absorbed some O_2 from the air and resulting in a slightly higher calculated DO concentrations.

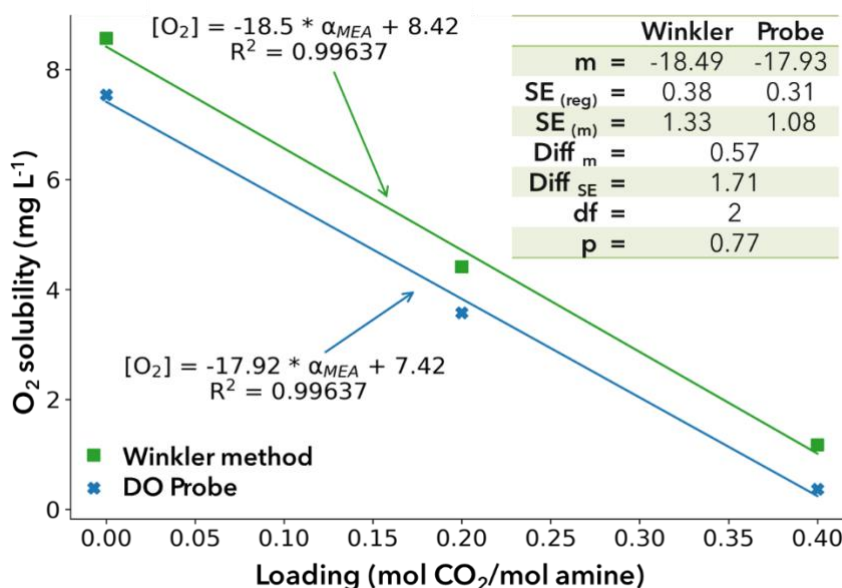


Fig 4: The O₂ solubility vs Loading for 5M MEA at unloaded, lean loaded, and rich loaded conditions

To further validate the electrochemical probe, eleven aqueous amine solvents at typical loadings found in carbon capture were prepared with and without four additives typically found in commercial application solvents. These amines were chosen based on structure (primary, secondary, tertiary, and diamines) and are solvents typically discussed in literature. Commercial amine solvents will contain additives to increase performance, or inhibit a technical challenge caused by the solvent or process. Common additives include a non-ionic surfactant (NIS), XiameterTM (X) and 2-mercaptobenzothiazole (MBT). A 10% random sampling of the prepared solutions had the measured O₂ solubility by probe and compare to the calculated titration values.

The difference between the electrochemical DO probe and the modified Winkler method or variance for samples without additives, samples with NIS, XiameterTM, and MBT are all within 1 ppm and presented in **Fig. 5**. All samples with XiameterTM measured DO resulted in a higher deviation from the modified Winkler method than NIS and MBT samples, as the probe gave a lower result than the titration. The higher deviation from XiameterTM could be due to the additive properties as it is an antifoam agent, it likely slowed down the decrease in pH during the titration and allowed the thiosulfate to capture more O₂ from the air. The further validation by the modified Winkler method to the electrochemical DO probe values shows confidence in the probe to produce accurate O₂ concentrations in the aqueous amine solvents with CO₂ and additives.

4. Conclusion

This study focused on the lessons learned during the Winkler method's modification with aqueous amine solvent analysis and an electrochemical DO probe's validation for amine scrubbing carbon capture purposes. The modified Winkler's method lessons learned include iodine evaporating at 30°C, thiosulfate oxidizing when exposed to ambient atmosphere, and the importance of accurate thiosulfate and iodate reagent concentrations. In addition to the backwards titration, the temperature sensitivity was aided using an ice bath removing excess heat produced by the acid and base reaction allowing iodine to stay in solution. Thiosulfate oxidizing when exposed to ambient atmosphere was overcome by preparing fresh thiosulfate no more than 12 to 15 hours before each titration. The sensitivity of iodate and thiosulfate concentrations in the modified Winkler method's calculation was solved by standardizing the solutions before use.

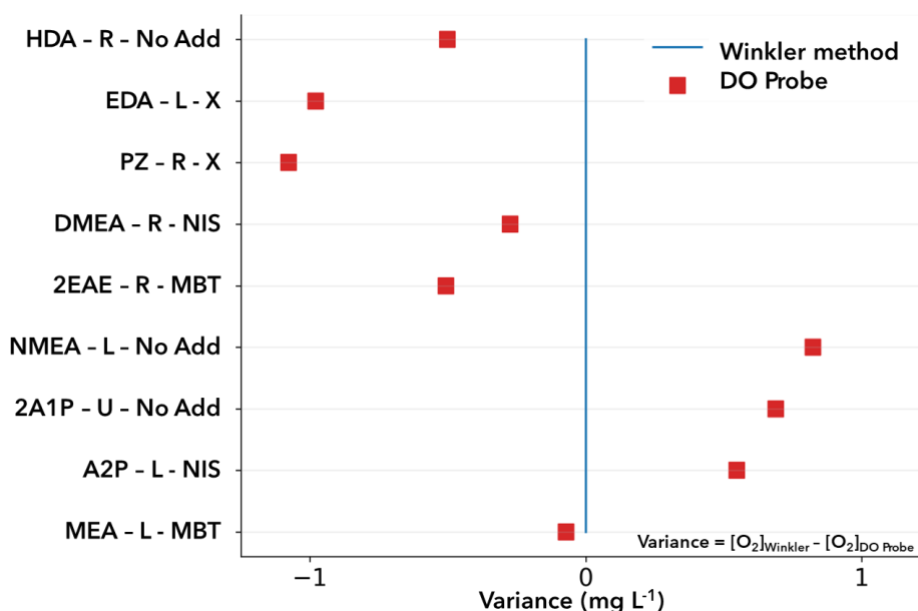


Fig 5: The variance between electrochemical DO probe and modified Winkler method for a random sampling of the samples discussed in Jorgensen *et al.* [11]

The electrochemical DO probe validation included a 5M MEA aqueous amine solvent at different loadings. The measured probe values were compared to the calculated titration values and resulted in similar values thus giving confidence in the probe's measurements. The probe was further tested with a random sample of different amines, at different loadings, with and without common additives used in amine scrubbing carbon capture. The difference between the two methods were within 1 ppm for the different amines, loadings, and additives indicating that the probe can confidently measure commercial amine solvent's oxygen solubility quickly and efficiently.

Acknowledgements

The authors would like to acknowledge the U.S. Department of Energy National Energy Technology Laboratory (U.S. DOE, NETL) for the financial support of this project (DE-FE0031661).

References

- [1] IEA CO₂ Emissions from Fuel Combustion: Overview, IEA, Paris. <https://www.iea.org/reports/co2-emissions-from-fuel-combustion-overview> (accessed October 15, 2021).
- [2] Bui, M.; Adjiman, C. S.; Bardow, A.; Anthony, E. J.; Boston, A.; Brown, S.; Fennell, P. S.; Fuss, S.; Galindo, A.; Hackett, L. A.; Hallett, J. P.; Herzog, H. J.; Jackson, G.; Kemper, J.; Krevor, S.; Maitland, G. C.; Matuszewski, M.; Metcalfe, I. S.; Petit, C.; Puxty, G.; Reimer, J.; Reiner, D. M.; Rubin, E. S.; Scott, S. A.; Shah, N.; Smit, B.; Trusler, J. P. M.; Webley, P.; Wilcox, J.; Mac Dowell, N., Carbon capture and storage (CCS): the way forward. *Energy & Environmental Science* 2018, 11 (5), 1062-1176.
- [3] Saeed, I. M.; Alaba, P.; Mazari, S. A.; Basirun, W. J.; Lee, V. S.; Sabzoi, N., Opportunities and challenges in the development of monoethanolamine and its blends for post-combustion CO₂ capture. *International Journal of Greenhouse Gas Control* 2018, 79, 212-233.

- [4] Bello, A.; Idem, R. O., Pathways for the Formation of Products of the Oxidative Degradation of CO₂-Loaded Concentrated Aqueous Monoethanolamine Solutions during CO₂ Absorption from Flue Gases. *Industrial & Engineering Chemistry Research* 2005, 44 (4), 945-969.
- [5] ElMoudir, W.; Supap, T.; Saiwan, C.; Idem, R.; Tontiwachwuthikul, P., Part 6: Solvent recycling and reclaiming issues. *Carbon Management* 2012, 3 (5), 485-509.
- [6] Chen, C.-I.; Rochelle, G. In *Amine Oxidation by NO₂*, 6th Post-Combustion Capture Conference, Sheffield United Kingdom, October 19-21, 2021; Sheffield United Kingdom, 2021.
- [7] Morken, A. K.; Pedersen, S.; Nesse, S. O.; Flø, N. E.; Johnsen, K.; Feste, J. K.; de Cazenove, T.; Faramarzi, L.; Vernstad, K., CO₂ capture with monoethanolamine: Solvent management and environmental impacts during long term operation at the Technology Centre Mongstad (TCM). *International Journal of Greenhouse Gas Control* 2019, 82, 175-183.
- [8] D888-18, A., *Standard Test Methods for Dissolved Oxygen in Water*. ASTM International: West Conshohocken, PA 2018; Vol. D888-18.
- [9] Winkler, L. W., *Die Bestimmung des im Wasser gelösten Sauerstoffes*. *Berichte der deutschen chemischen Gesellschaft* 1888, 21 (2), 2843-2854.
- [10] Bondyale-Juez, D. R.; Packard, T. T.; Viera-Rodríguez, M. A.; Gómez, M., Respiration: comparison of the Winkler technique, O₂ electrodes, O₂ optodes and the respiratory electron transport system assay. *Marine Biology* 2017, 164 (12), 226.
- [11] Jorgensen, T. B.; Abad, K.; Sarma, M.; Guzman, M. I.; Thompson, J. G.; Liu, K., Research on oxygen solubility in aqueous amine solvents with common additives used for CO₂ chemical absorption. *International Journal of Greenhouse Gas Control* 2022, 116, 103646.
- [12] Wang, M. H.; Ledoux, A.; Estel, L., Oxygen Solubility Measurements in a MEA/H₂O/CO₂ Mixture. *Journal of Chemical & Engineering Data* 2013;58(5):1117-1121.
- [13] Ahmad, N.; Ahmad, F.; Khan, I.; Khan, A., Studies on the Oxidative Removal of Sodium Thiosulfate from Aqueous Solution. *Arabian Journal for Science & Engineering* (Springer Science & Business Media B.V.) 2015, 40 (2), 289-293.
- [14] D1510-19a, A., *Standard Test Method for Carbon Black - Iodine Adsorption Number*. ASTM International: West Conshohocken, PA, 2019; Vol. D1510-19a.