

# MFIX-Exa



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Research & Innovation Center

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# Disclaimer

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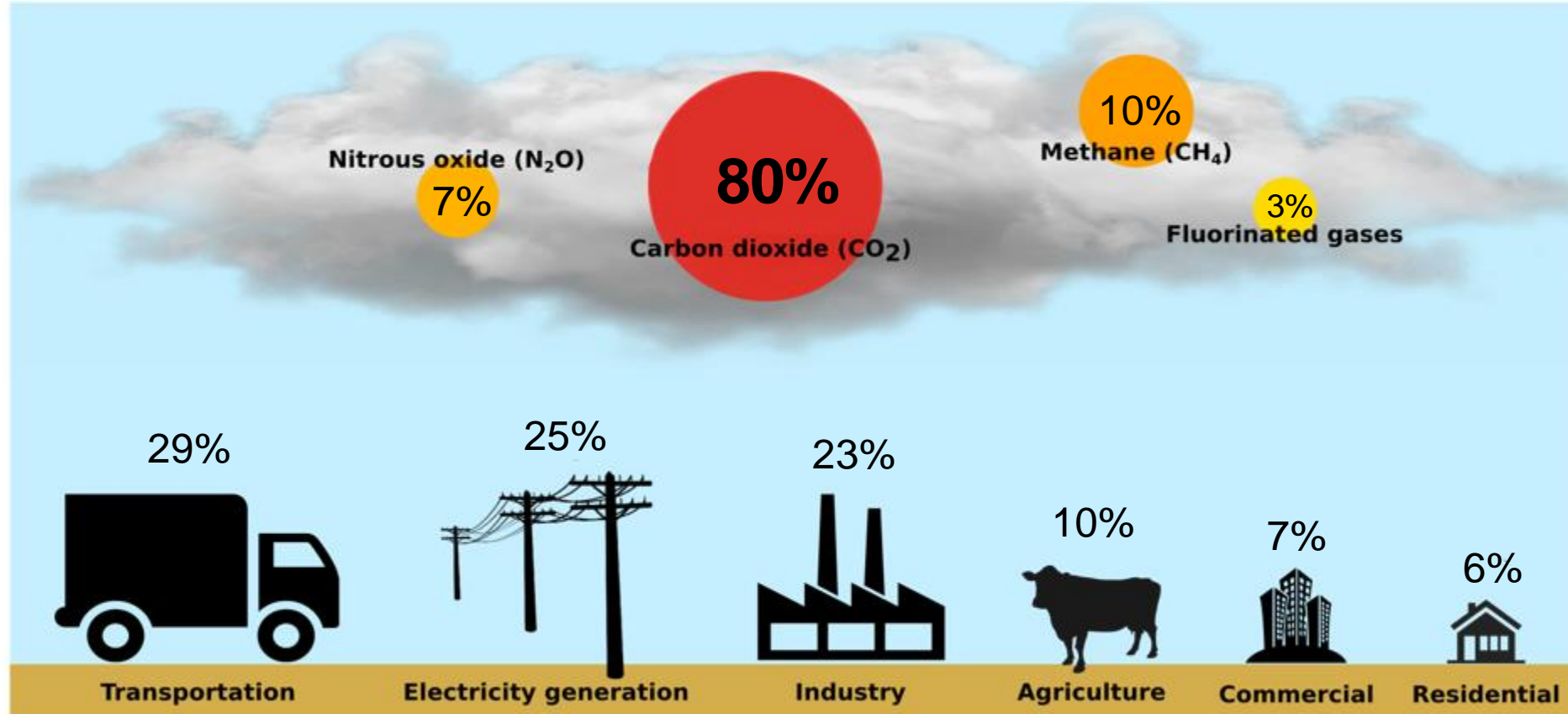
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<sup>2</sup>NETL Support Contractor, 3610 Collins Ferry Road, Morgantown, WV 26507, USA

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# Electricity Generation is a Major Source of CO<sub>2</sub>

Total U.S. greenhouse gas emissions by economic sector in 2019



Source:

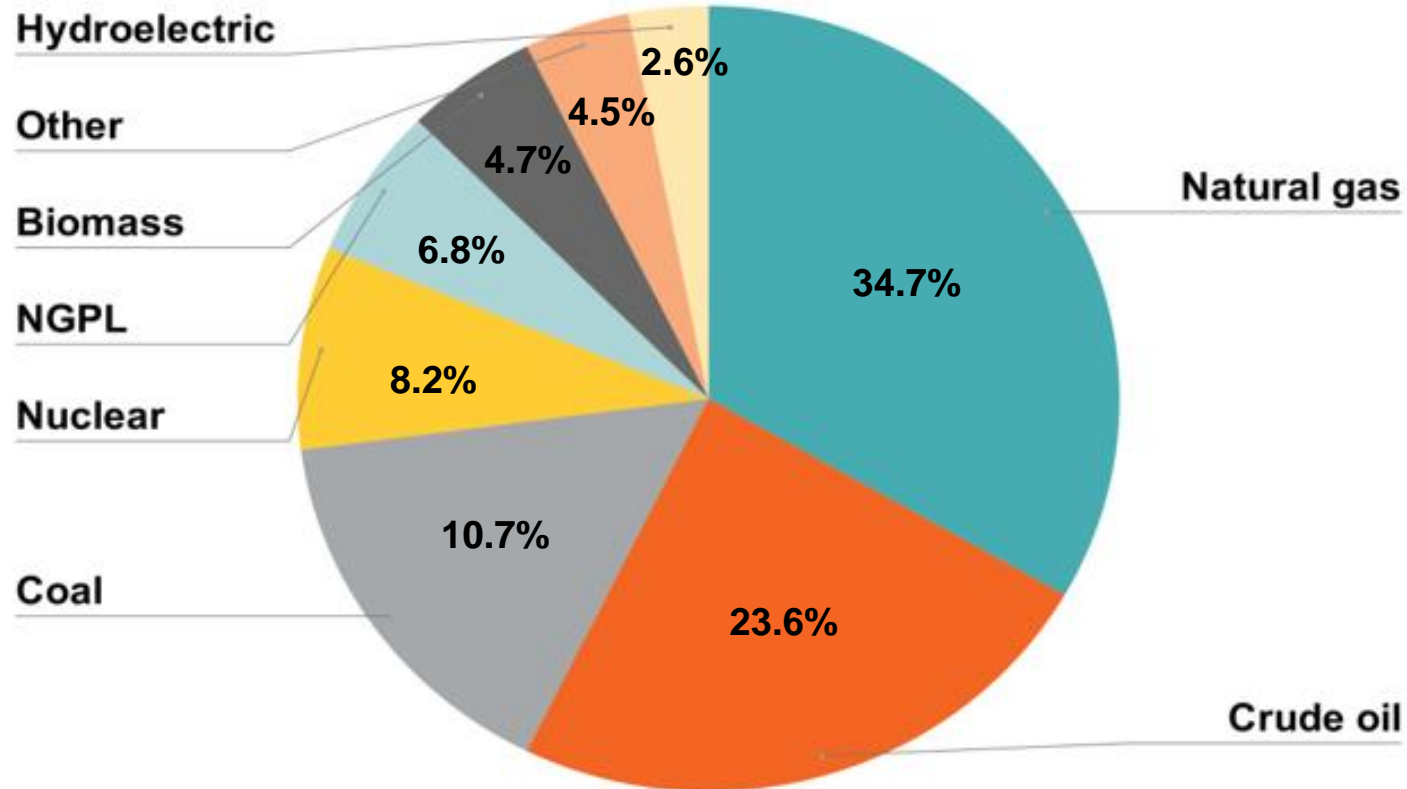
EPA - United States Environmental Protection Agency: Greenhouse Gas Inventory Data Explorer

<https://cfpub.epa.gov/ghgdata/inventoryexplorer/>



# Electricity is Mainly Generated from Fossil Fuels

U.S. primary energy production by major sources in 2020



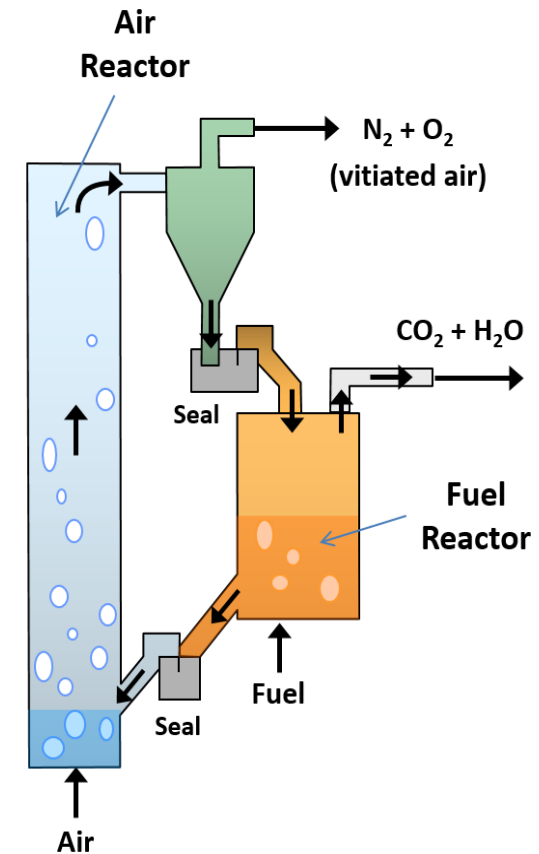
Source:  
EIA - United States Energy Information Administration  
<https://www.eia.gov/energyexplained/us-energy-facts/>

# Numerical Simulations are Necessary for Industrial-Scale CLR Design

NETL's 50 kW hot flow chemical looping reactor (CLR)

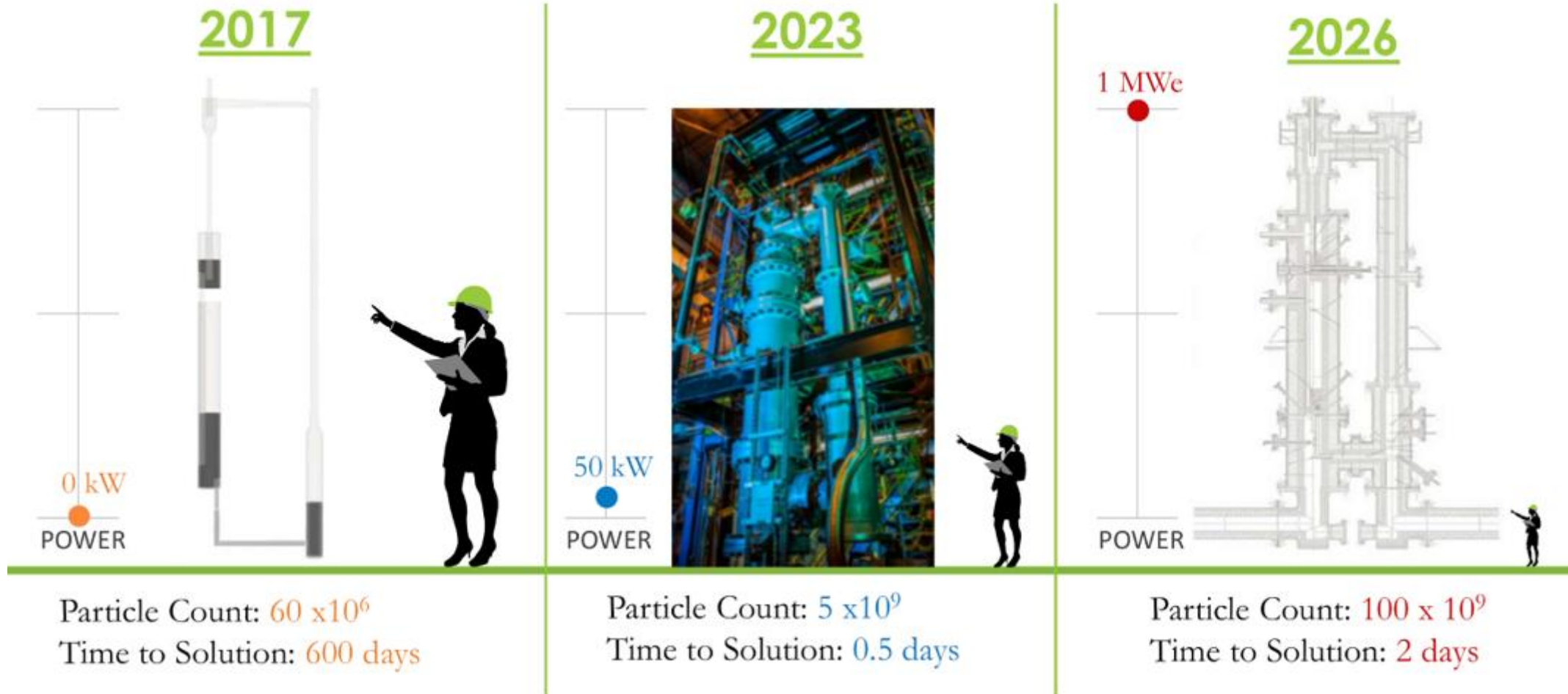


Chemical looping combustion



# Objective: CLRs to be Operative by 2026

The 2023 and 2026 values are rough estimates.



## Fluid phase

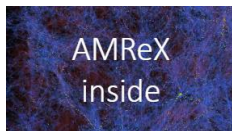
- *Particle-unresolved multi-component low-Mach number* formulation
- *Embedded boundaries*
- *Finite volumes* in space, *Godunov scheme* for time integration
- Conservation of mass
- *Navier-Stokes momentum equation* in convective form
- Conservation of species mass
- Conservation of energy
- *Incompressibility* or *ideal gas equation of state*

## Solid phase: particles

- *Soft-sphere spring-dashpot* model
- *Forward Euler* time integration with *subcycling*
- Conservation of mass
- Conservation of *linear momentum*
- Conservation of *angular momentum*
- Conservation of species mass
- Conservation of energy

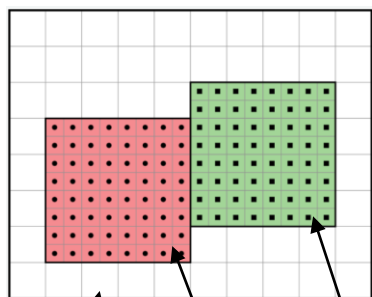


# Hybrid Parallelism



## Levels, Grids and Tiling

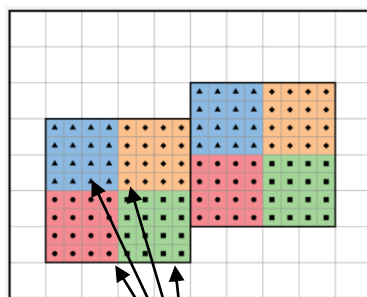
Without tiling



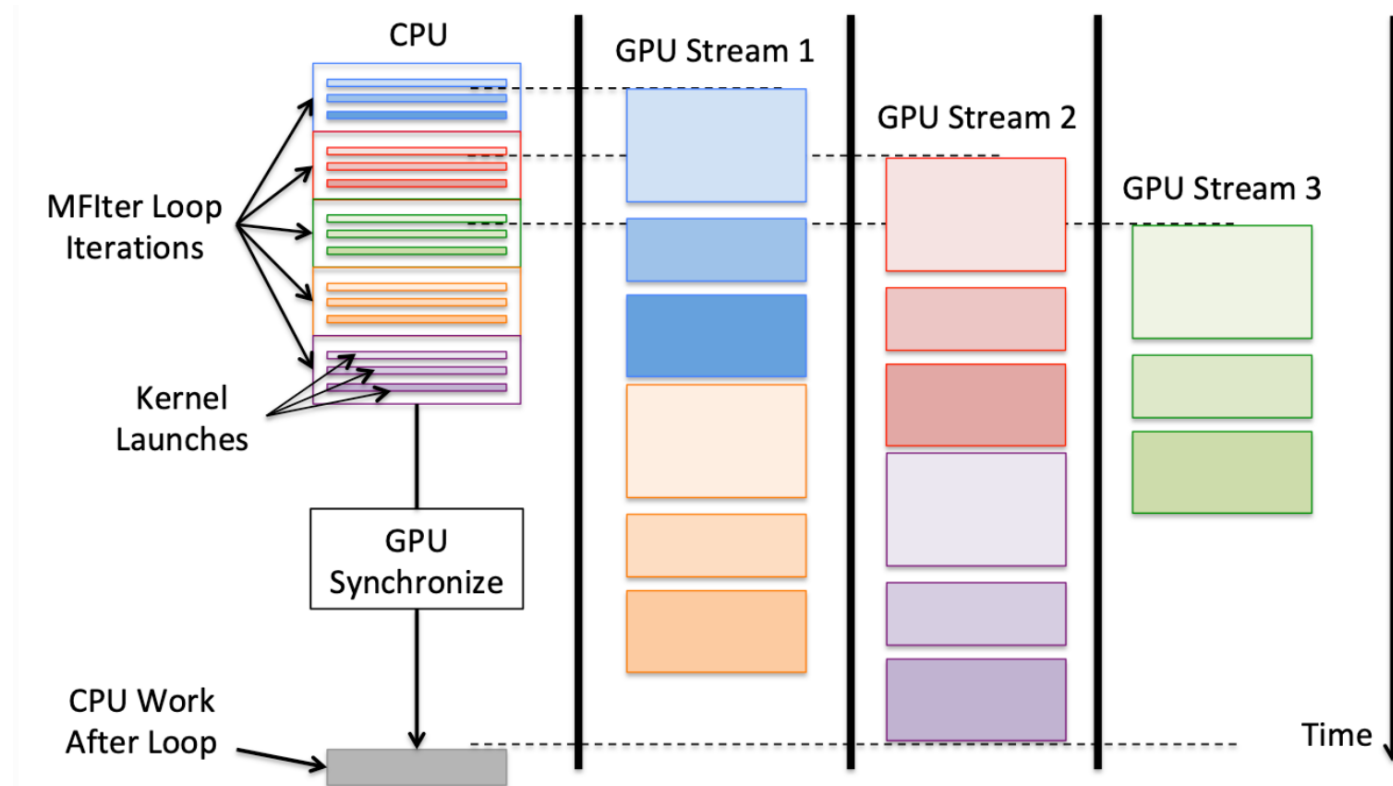
Level 0

Level 1 = {Grid 0, Grid 1}

With tiling



Tiles

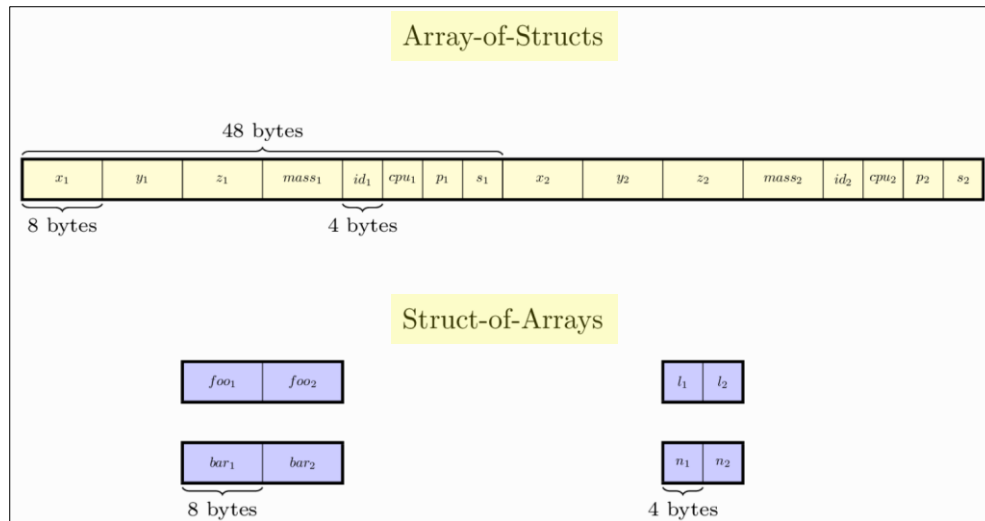


Images source: AMReX online documentation

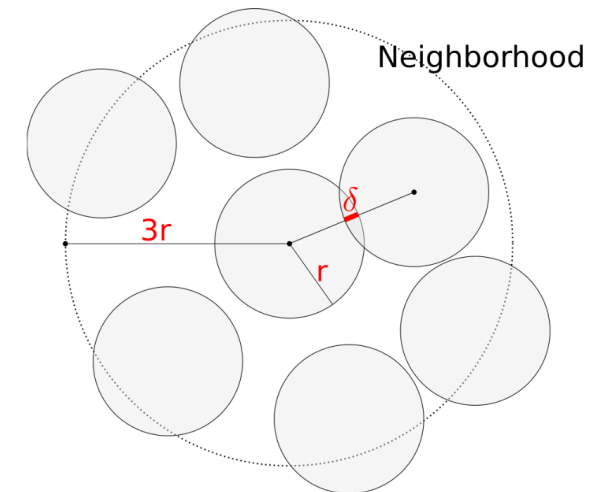
# Improve Coalescence + Reduce Communication

AoS → SoA

ParticleContainer<NStructReal, NStructInt, NArrayReal, NArrayInt>



“Halving” the neighborlist



Take advantage of particle-particle mutual interaction:

*if particle “i” **is** in particle “j” neighborhood,  
then particle “j” **is not** in particle “i” neighborhood*

Images source: AMReX online documentation

# Improve Coalescence + Reduce Communication

## Real domain extents

lower bound ( $m$ ): (0, 0, 0)

upper bound ( $m$ ): (0.64, 0.16, 0.16)

## Computational domain

number of cells: (256, 64, 64)

## Embedded boundaries

geometry: cylinder

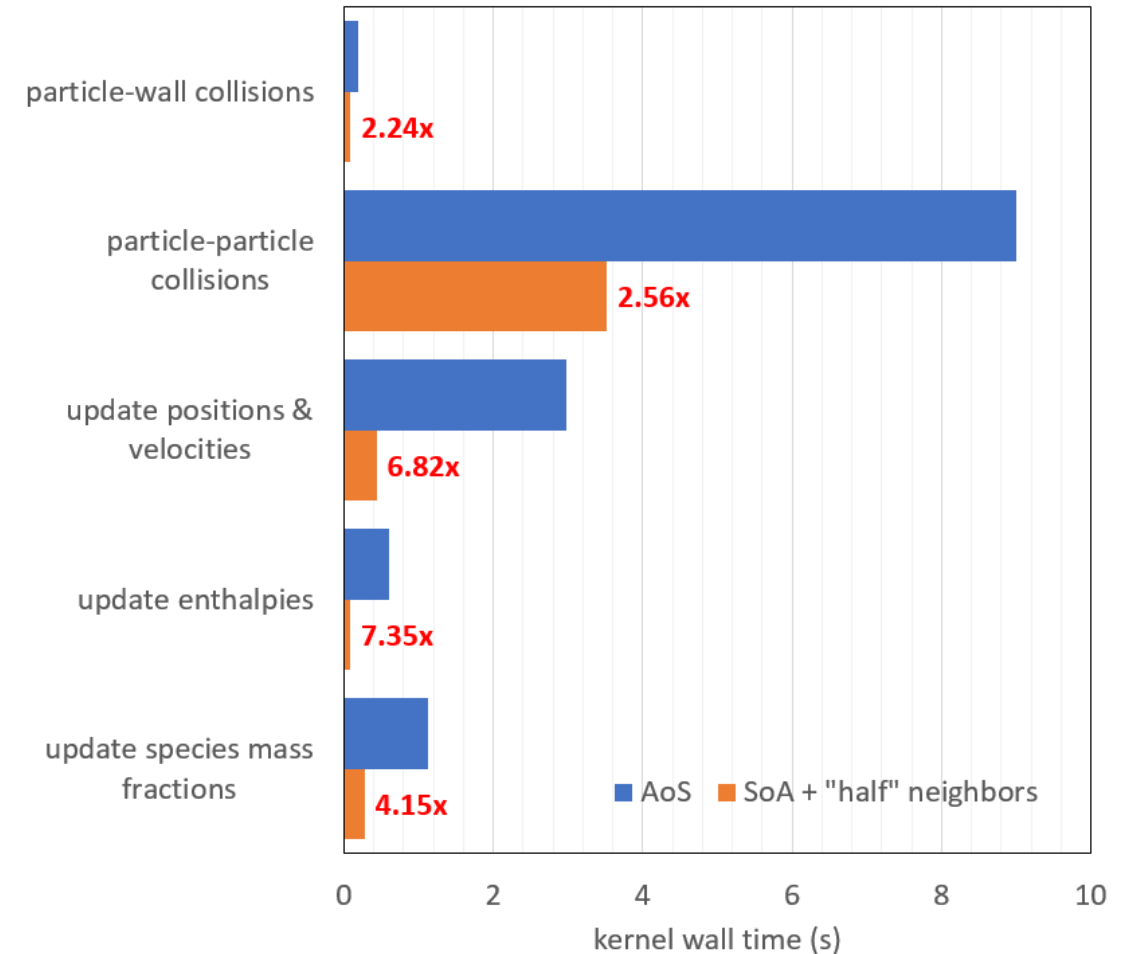
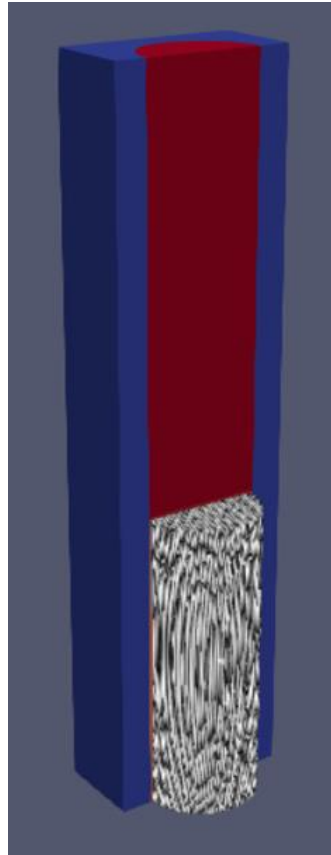
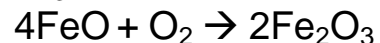
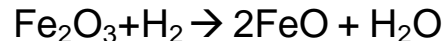
cylinder radius ( $m$ ): 0.1016

cylinder center ( $m$ ): (0.64, 0.16, 0.16)

## Solid particles

initial volume fraction = 60%

## Chemical reactions



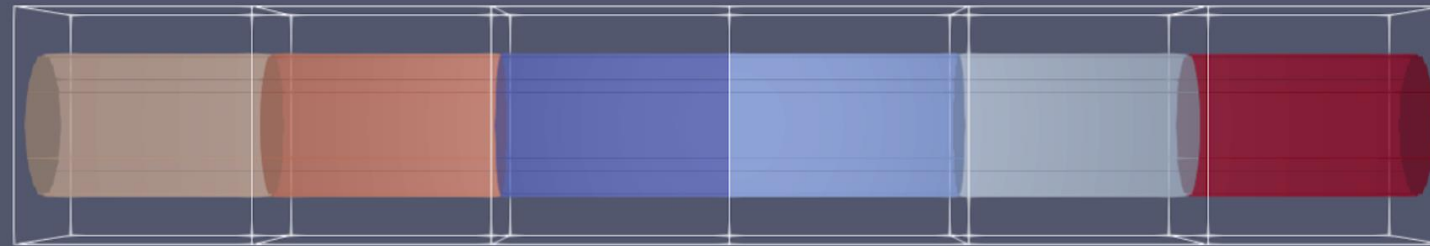
# Dual Grids Load Balancing

Fluid Grids: one grid per GPU

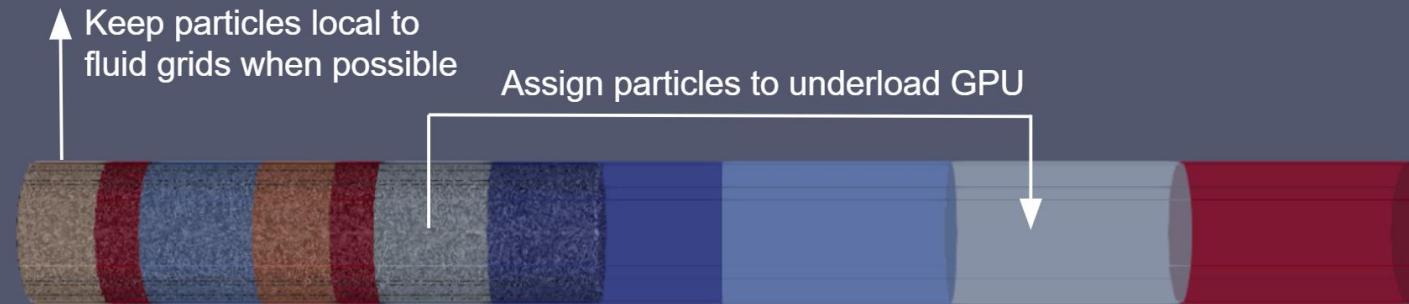
Particle Grids:

- balance particle counts among GPUs.
- minimize the communication between particle and fluid grids.

Fluid grids



Particles grids



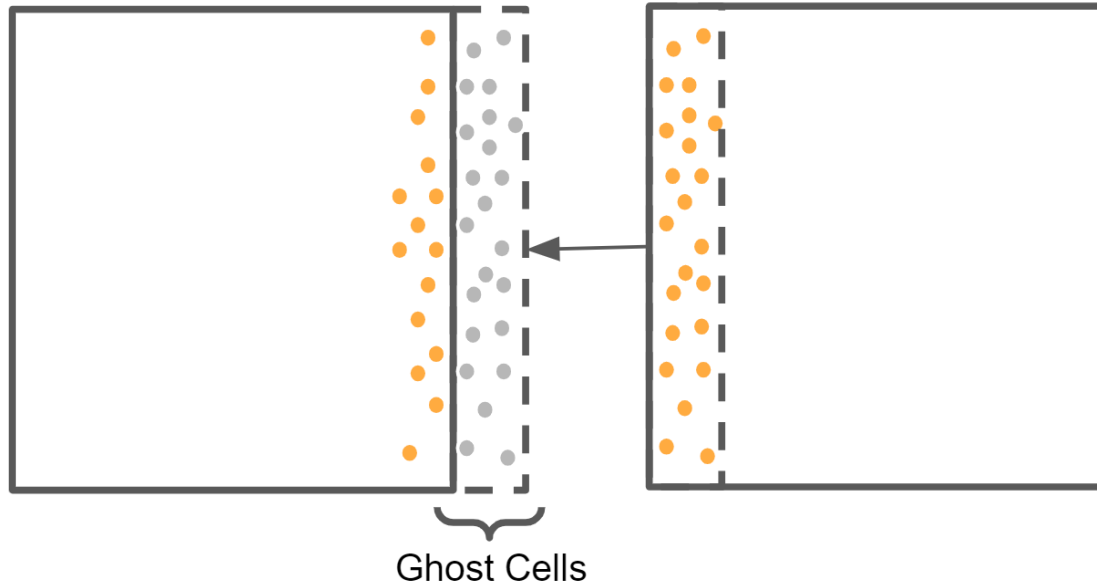
Load Balance Example. Each color represents a GPU.

Courtesy of Hengjie Wang



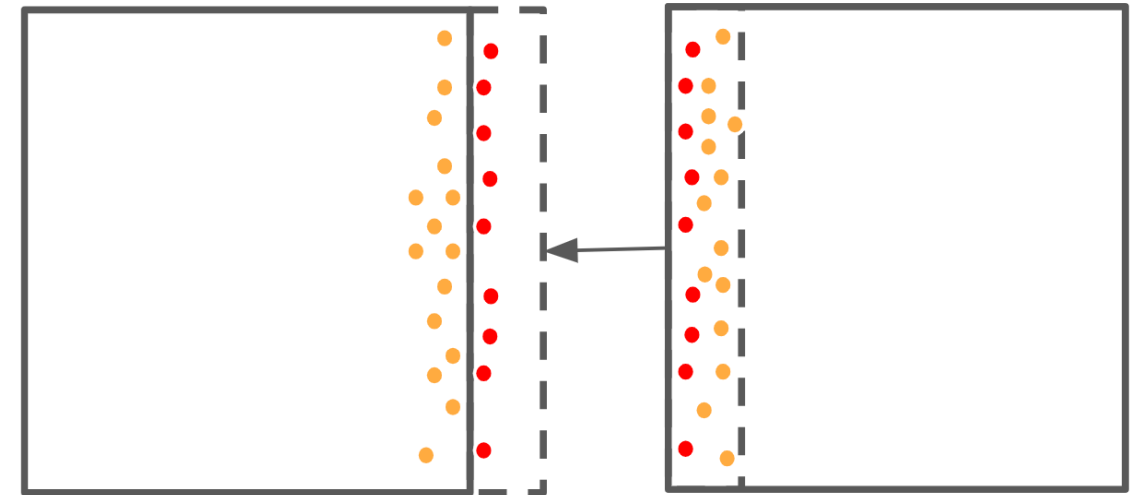
# Reduce Particle Communication

- We need to communicate particles in the ghost regions.
- Only the neighbor particles are used in the computation in the destination grid.
- Reduce particle variables used in communication.



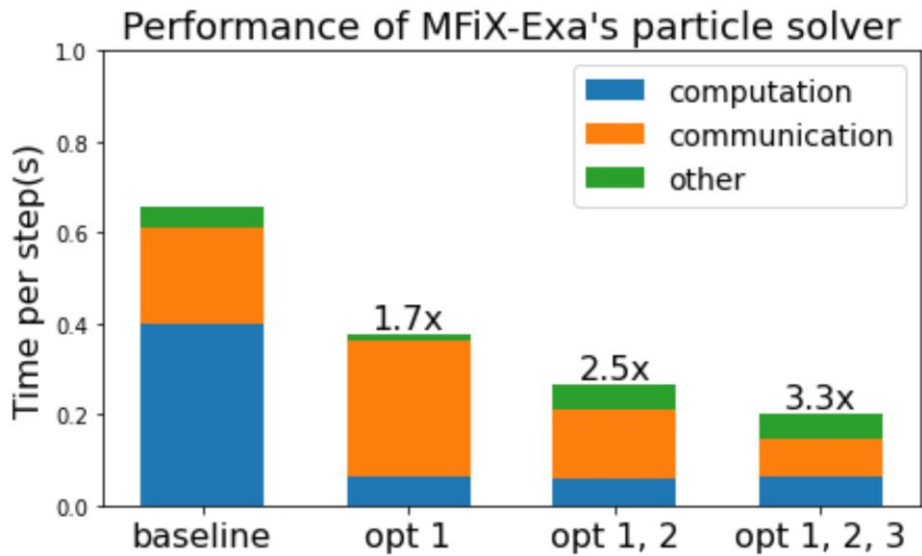
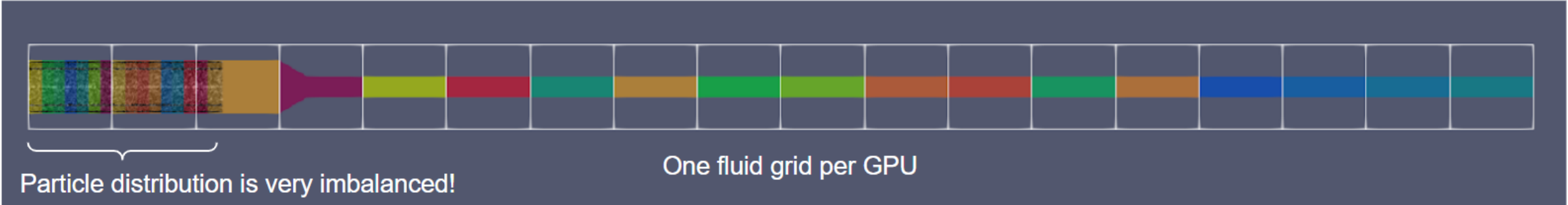
Transfer all the particles in the ghost region

Courtesy of Hengjie Wang



Just transfer the neighbor particles (red)

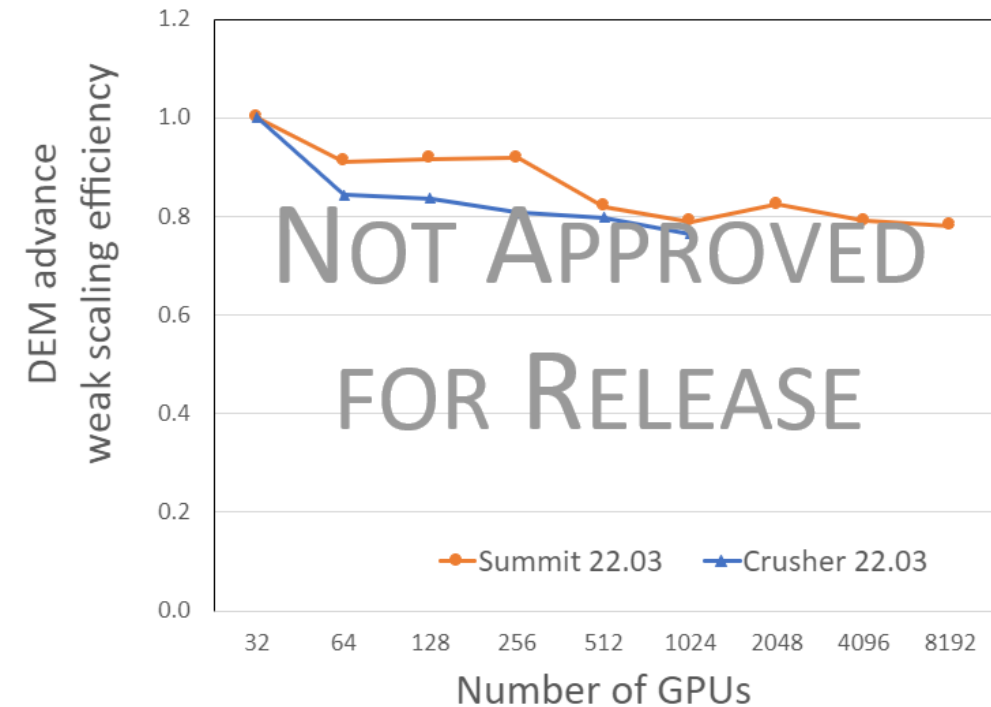
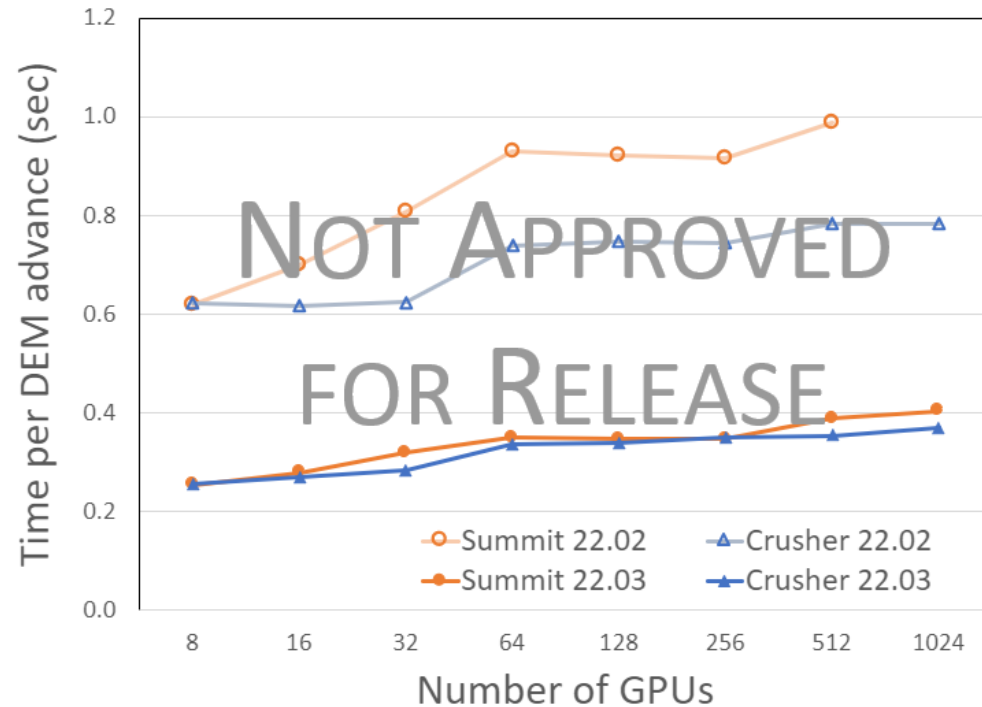
# Performance Evaluation of a Riser with 18 GPUs



Baseline	Use the same grids for fluid and particles
Optimization 1	Use dual grids with load balance
Optimization 2	Only communicate neighbor particles
Optimization 3	Reduce particle variables

Courtesy of Hengjie Wang

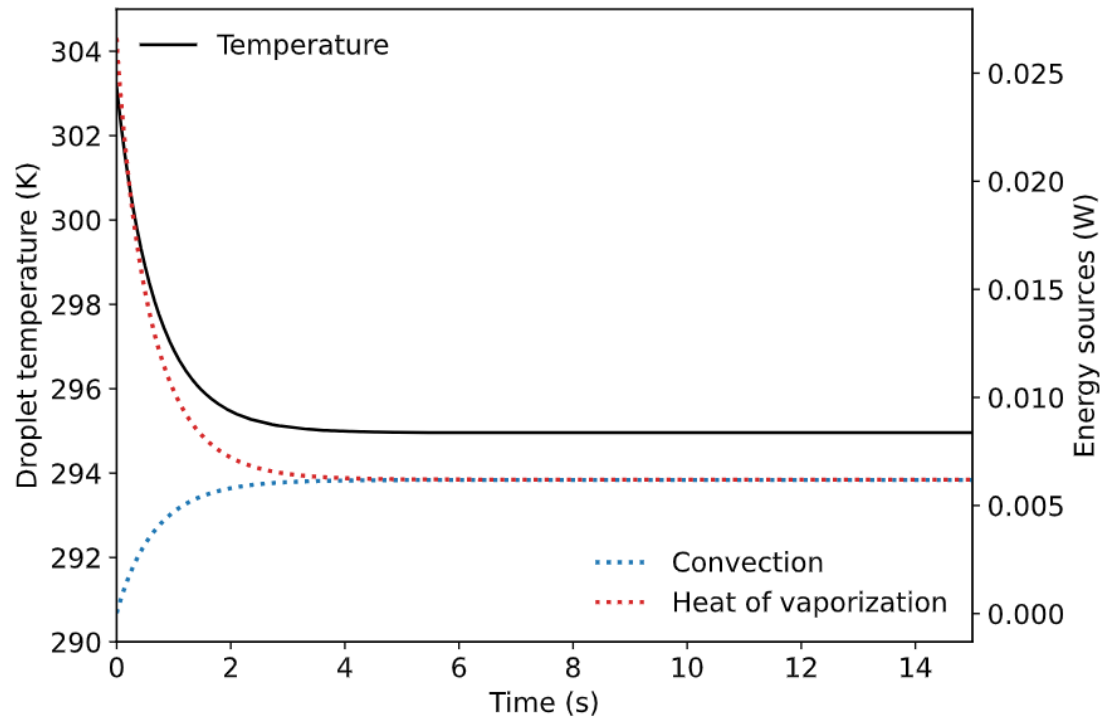
# Scaling on Crusher



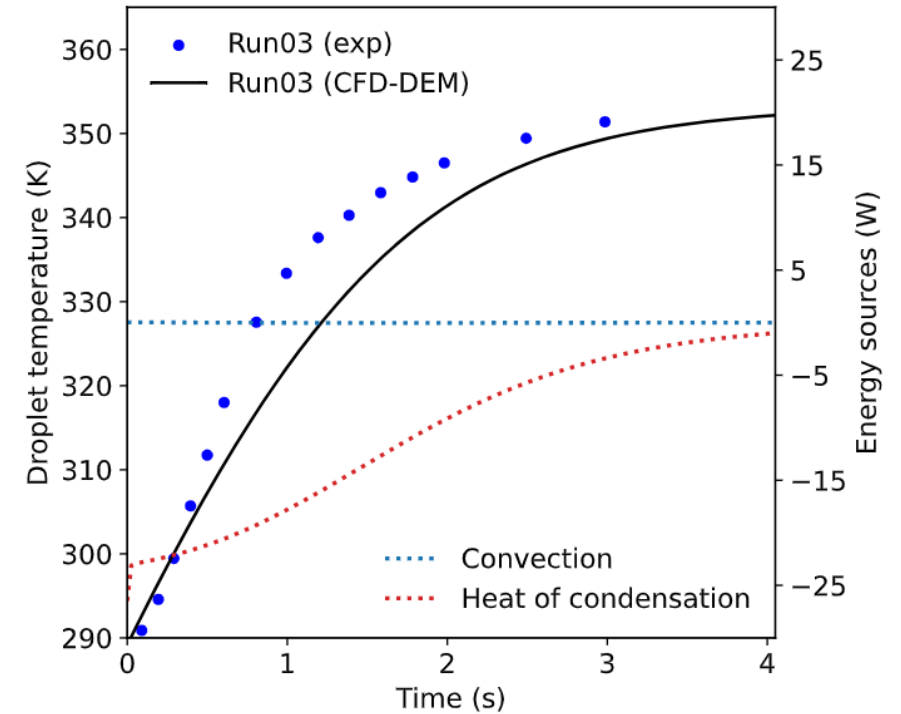
# Numerical Results

Wet-bulb: water droplet in a humidified air stream

## Droplet evaporation



## Water vapor condensation



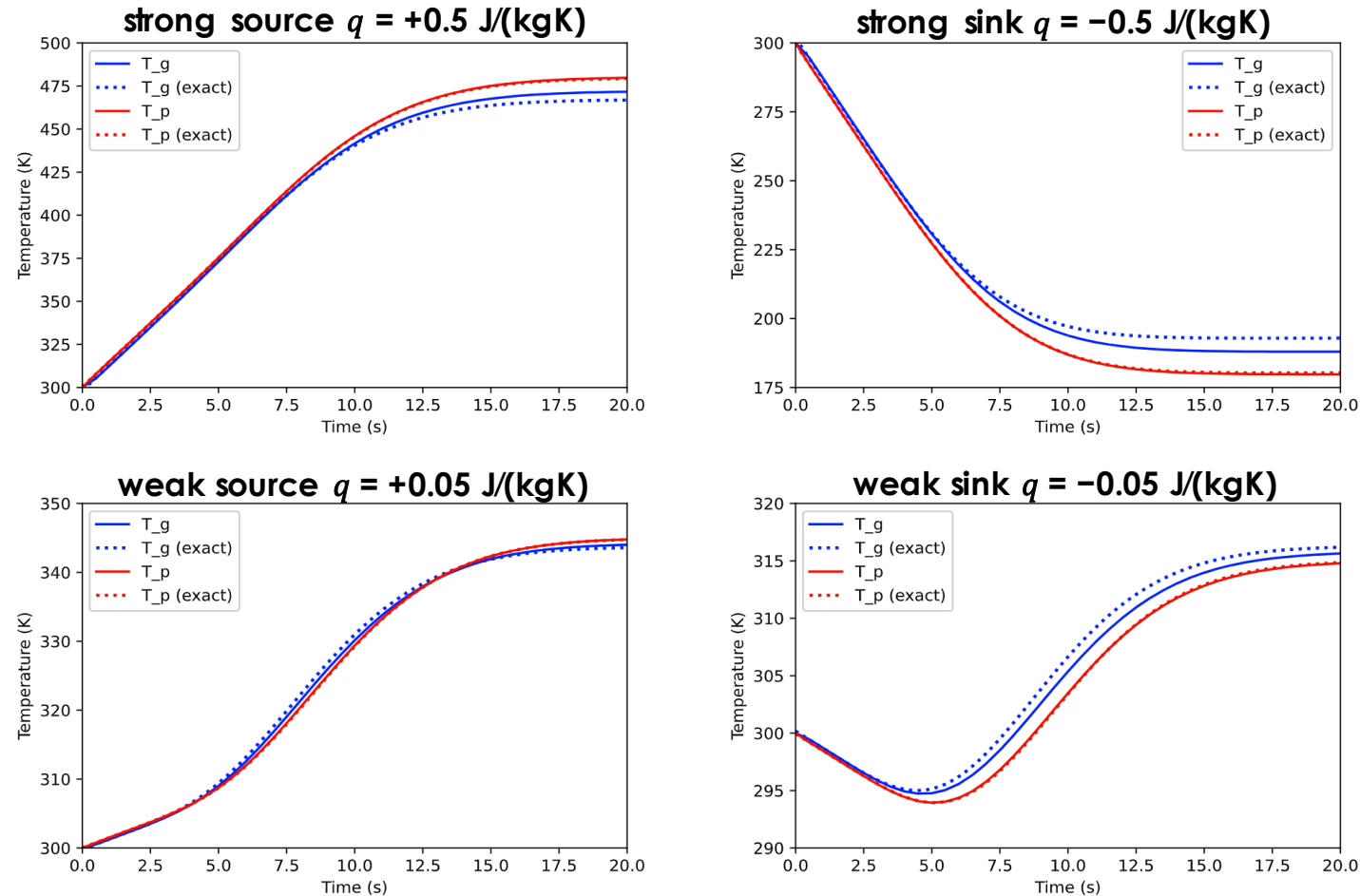
Musser, J., Syamlal, M., Shahn timer, M., Huckaby, D., (2015). **Constitutive equation for heat transfer caused by mass transfer**. *Chemical Engineering Science*

Kulic, E., (1976). **An experimental and theoretical study of simultaneous heat and mass transfer applied to steam dousing**. *Ph.D. thesis. University of Waterloo. Waterloo, Ontario, Canada*



# Numerical Results

## Transient heat conduction in packed beds



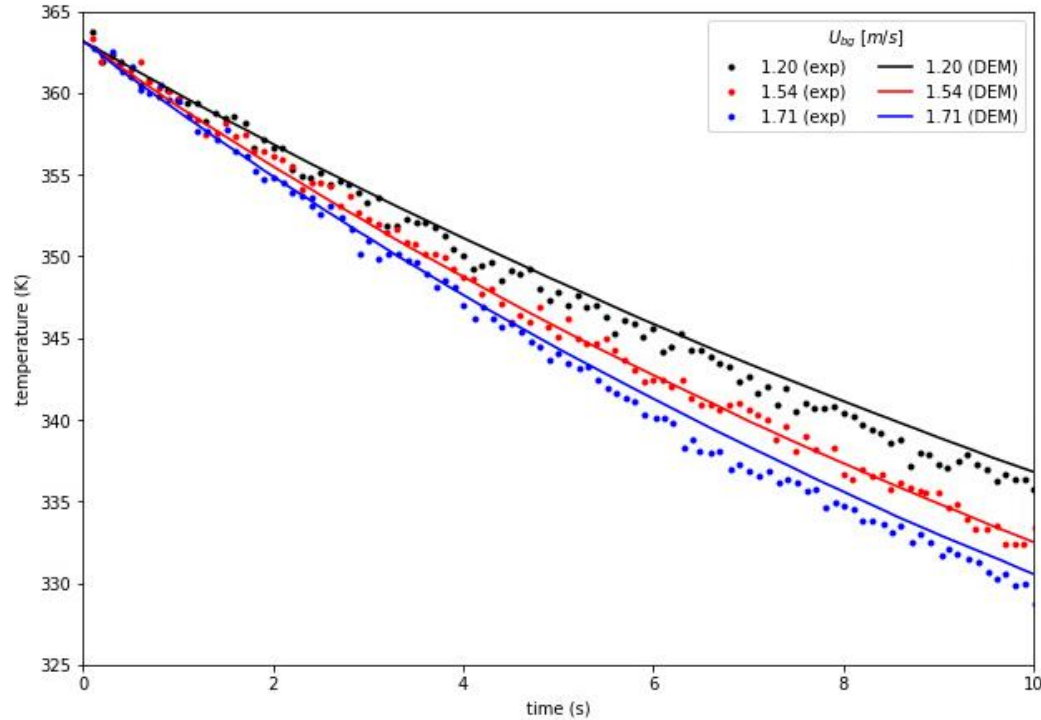
Schumann, T.E.W. (1929). **Heat transfer: a liquid flowing through a porous prism.** *Journal of the Franklin Institute*

Salehi, M.S., Askarishahi, M., Radl, S. (2017). **Analytical solution for thermal transport in packed beds with volumetric heat source.** *Chemical Engineering Journal*

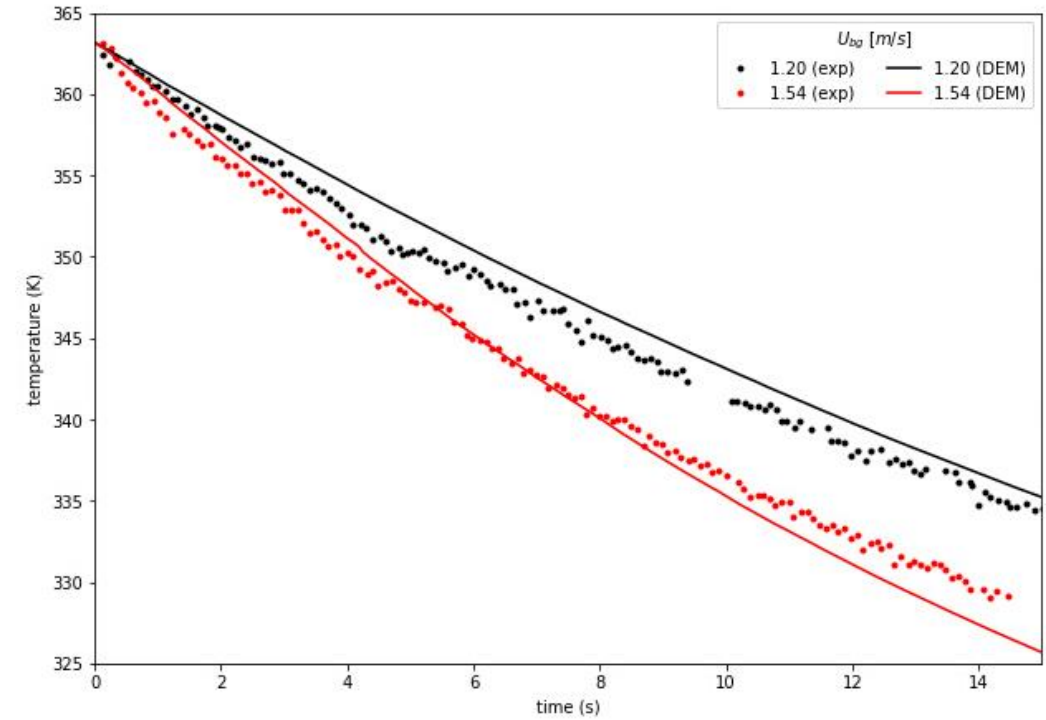
# Numerical Results

## Bench-scale fluidized bed

### Light



### Heavy



Patil, A.V., Peters, E.A.J.F., Sutkar, V.S., Deen, N.G., Kuipers, J.A.M. (2015). **A study of heat transfer in fluidized beds using an integrated dia/piv/ir technique.** *Chemical Engineering Journal*

# THANKS!!

# NETL RESOURCES

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