

Correlating Ignition Properties with Critical Species Concentrations

Zachary Buras, Nils Hansen, Dario Lopez Pintor, Leonid Sheps and Craig Taatjes



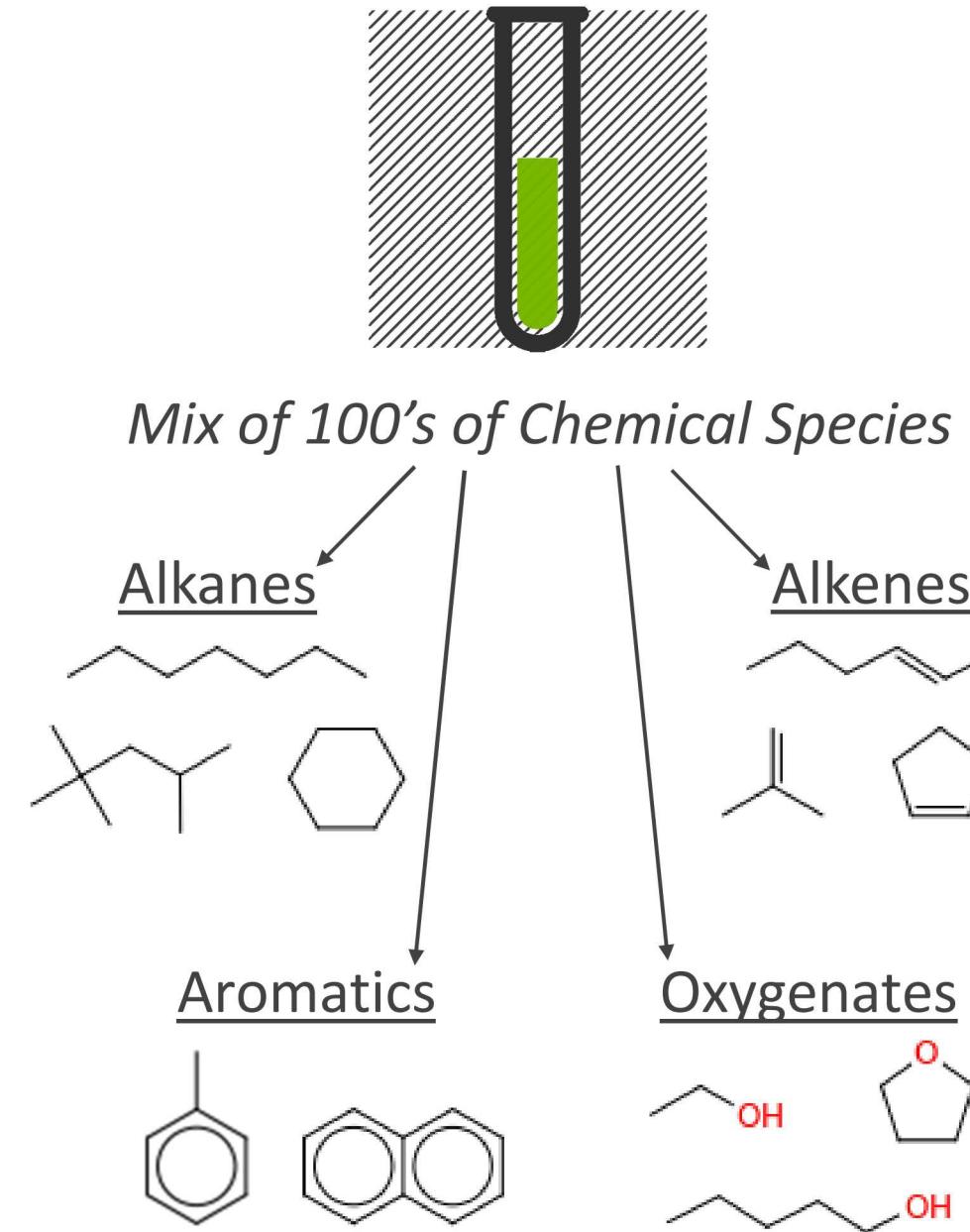
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Vision for an Ideal Fuel Screening Platform

Realistic Candidate Fuel

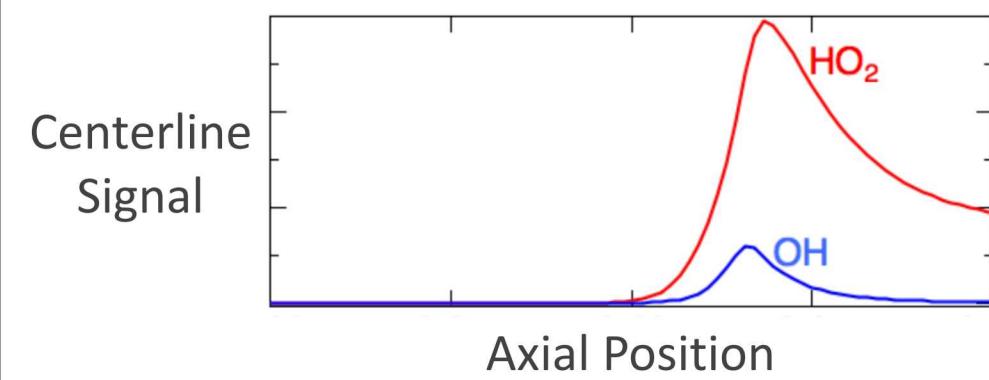
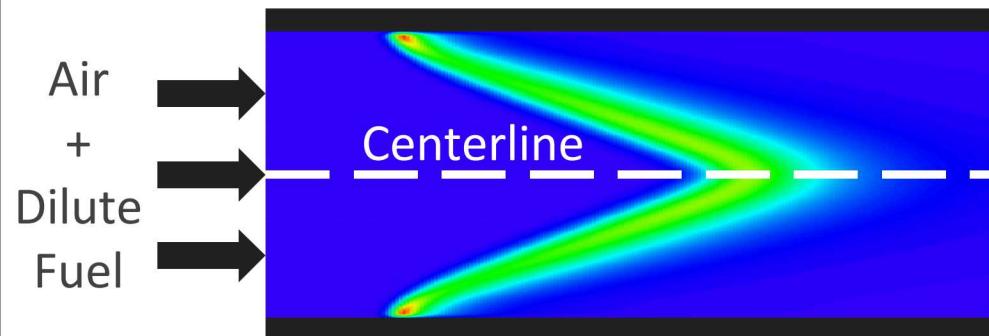


Ideal Screening Platform:

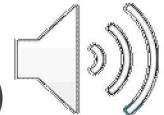
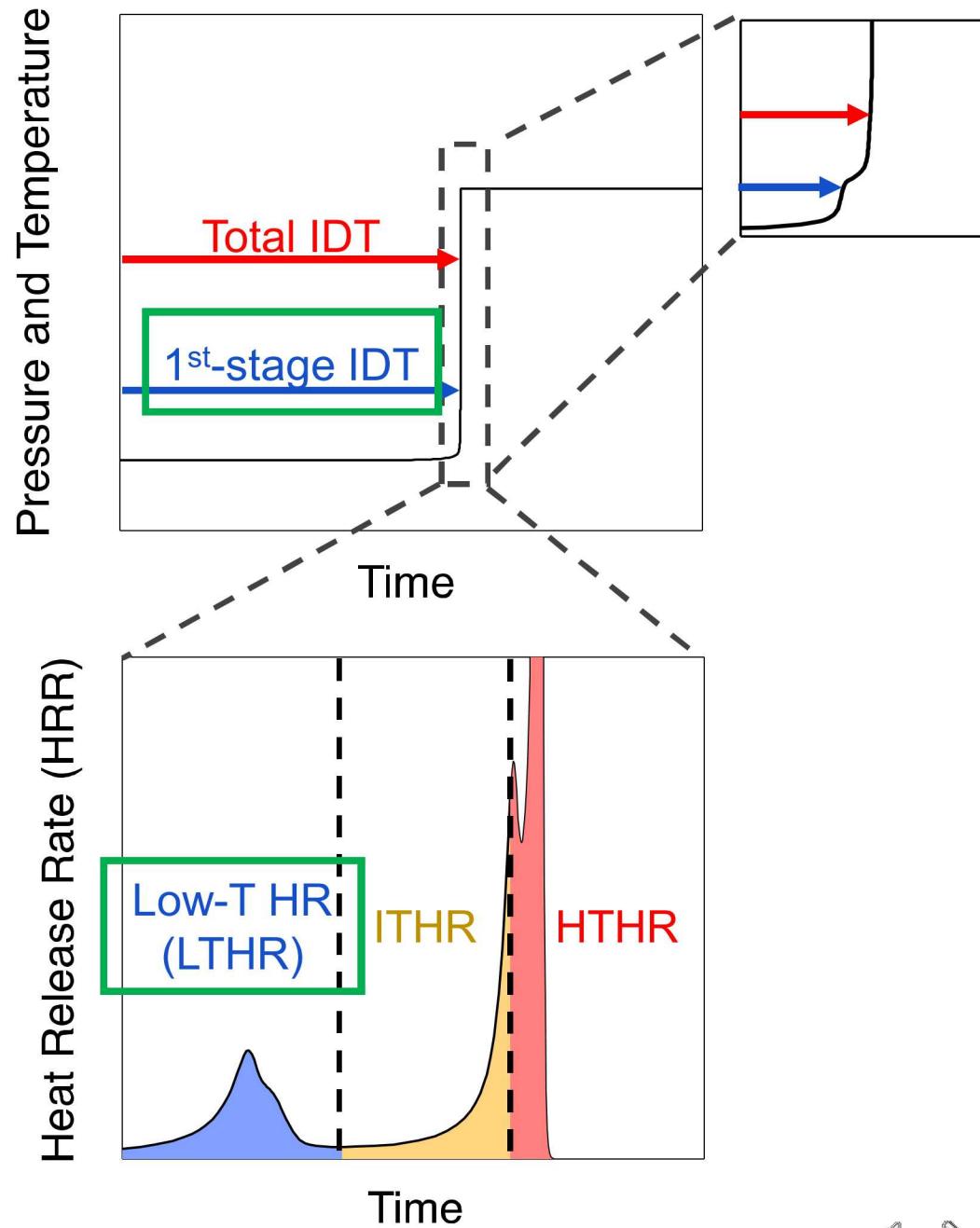
1. General ✓
2. Small Fuel Quantities ✓

Our Idea:

Measure Universal Oxidation Species
(e.g., OH & HO₂)
in a High-P Flow Reactor

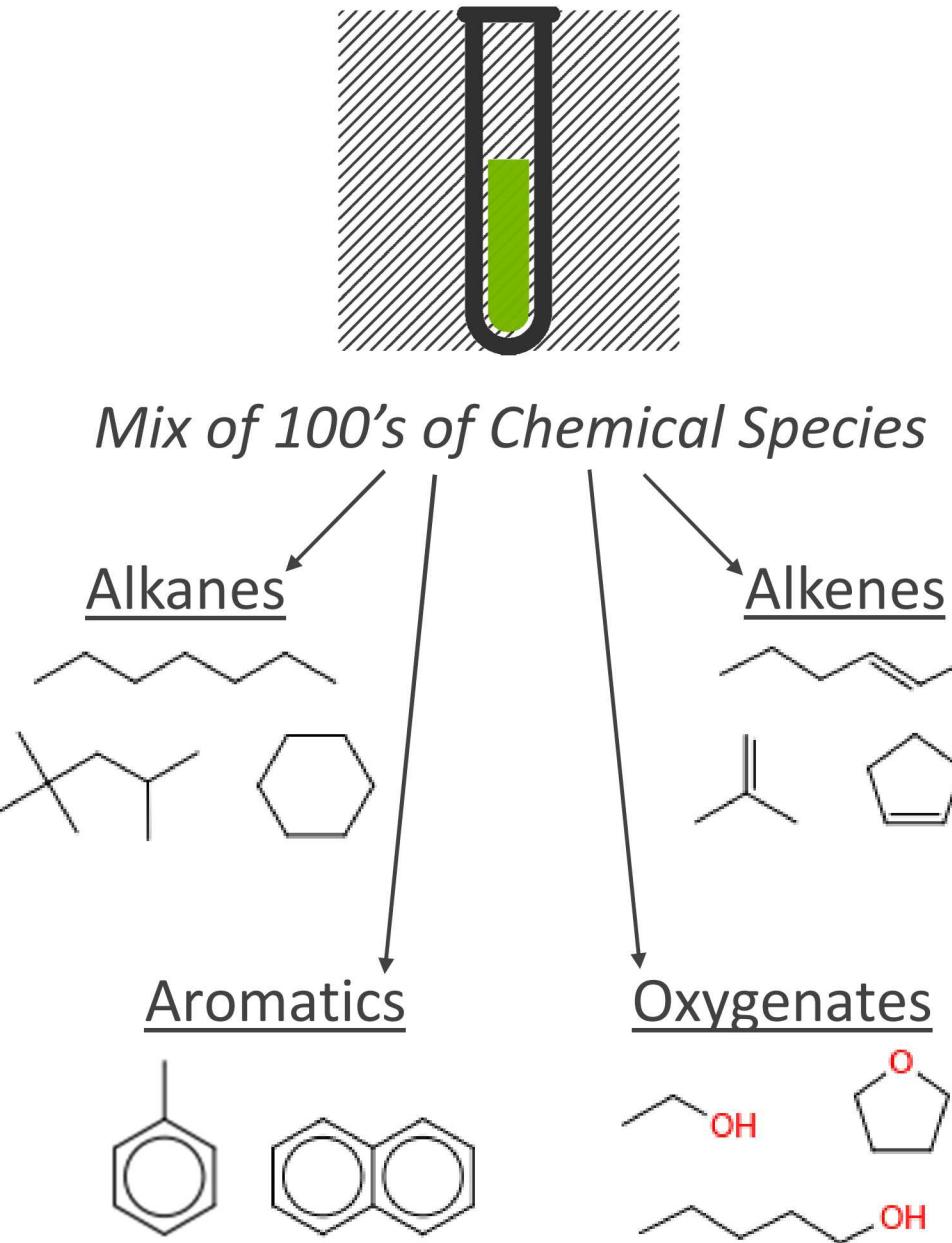


Ignition Properties



Vision for an Ideal Fuel Screening Platform

Realistic Candidate Fuel

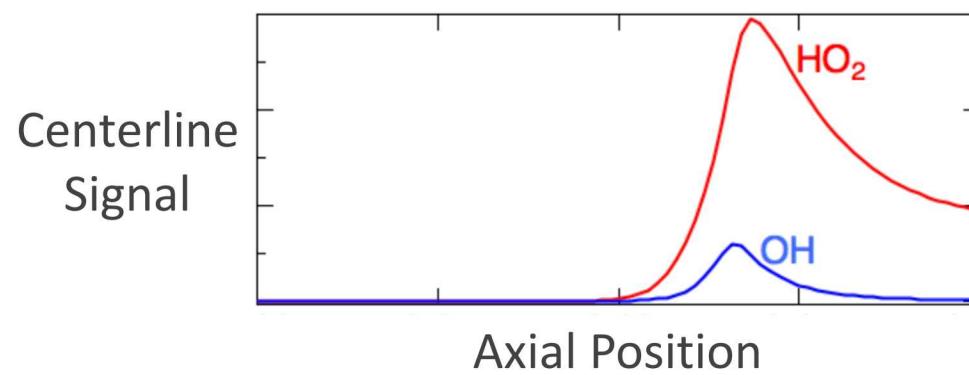
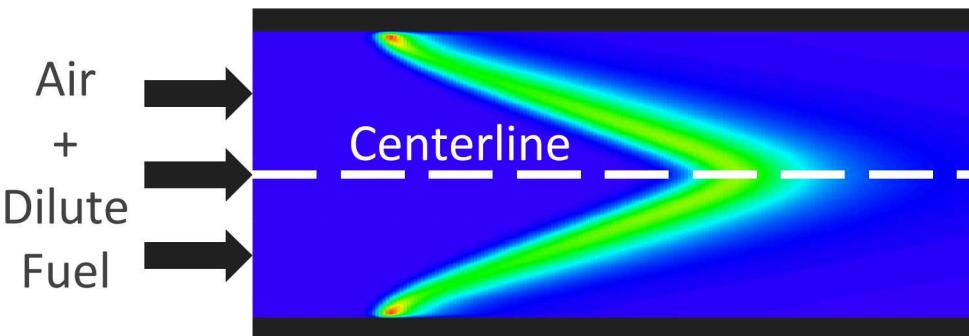


Ideal Screening Platform:

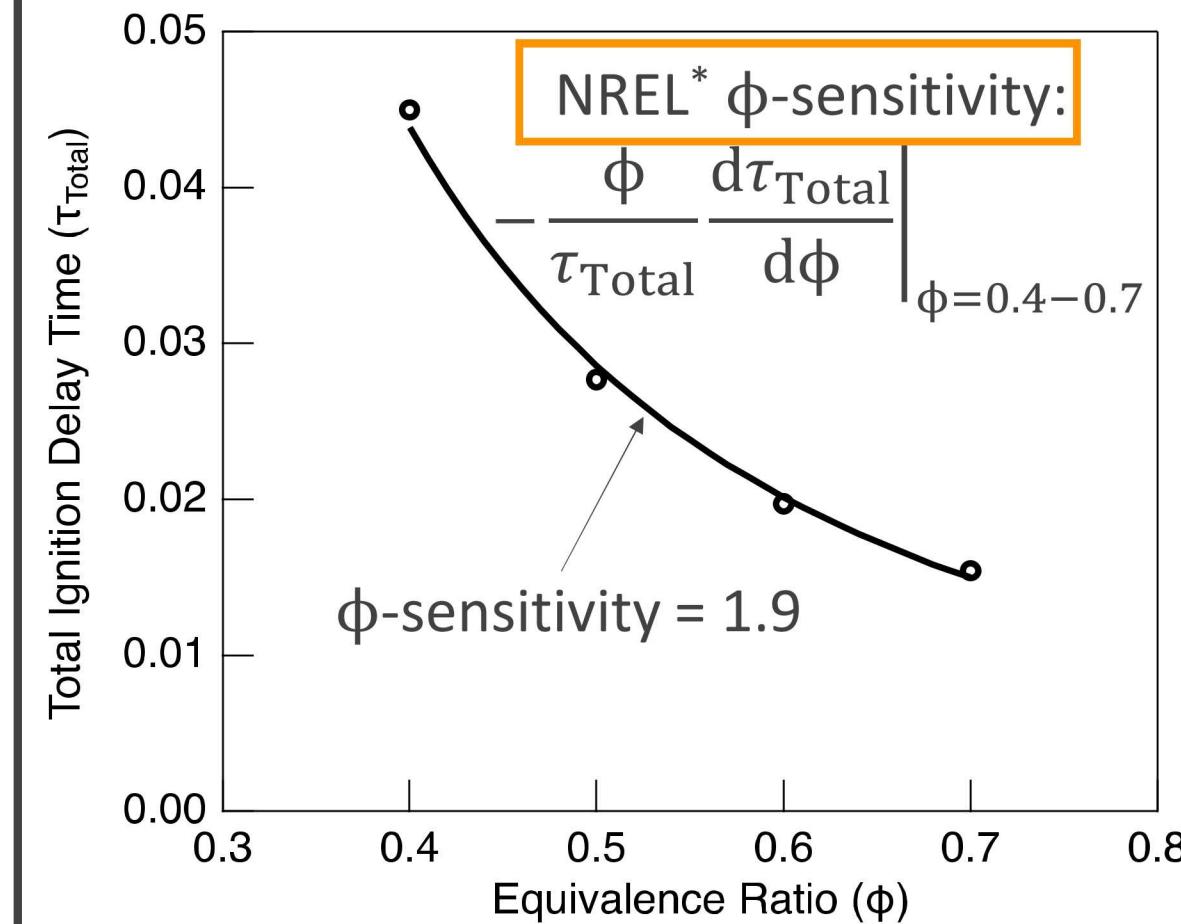
1. General ✓
2. Small Fuel Quantities ✓

Our Idea:

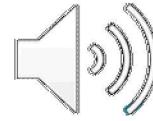
Measure Universal Oxidation Species
(e.g., OH & HO₂)
in a High-P Flow Reactor



Ignition Properties



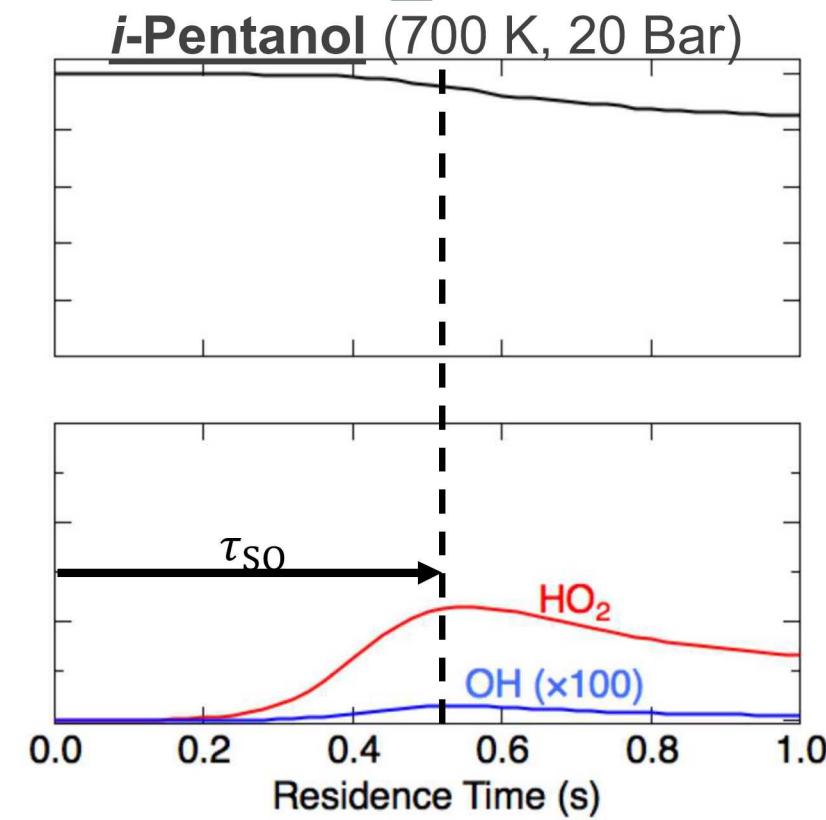
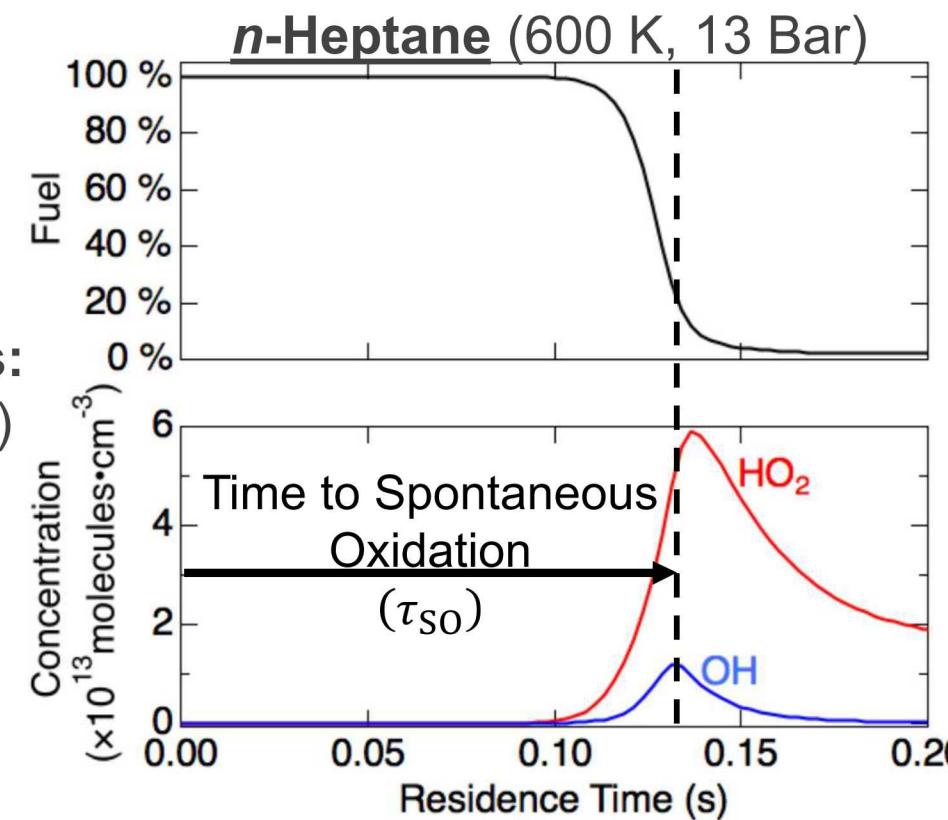
φ-sensitivity too complicated to be correlated with OH/HO₂ from dilute fuel measurements alone



Simulations of Expected OH/HO₂ Profiles

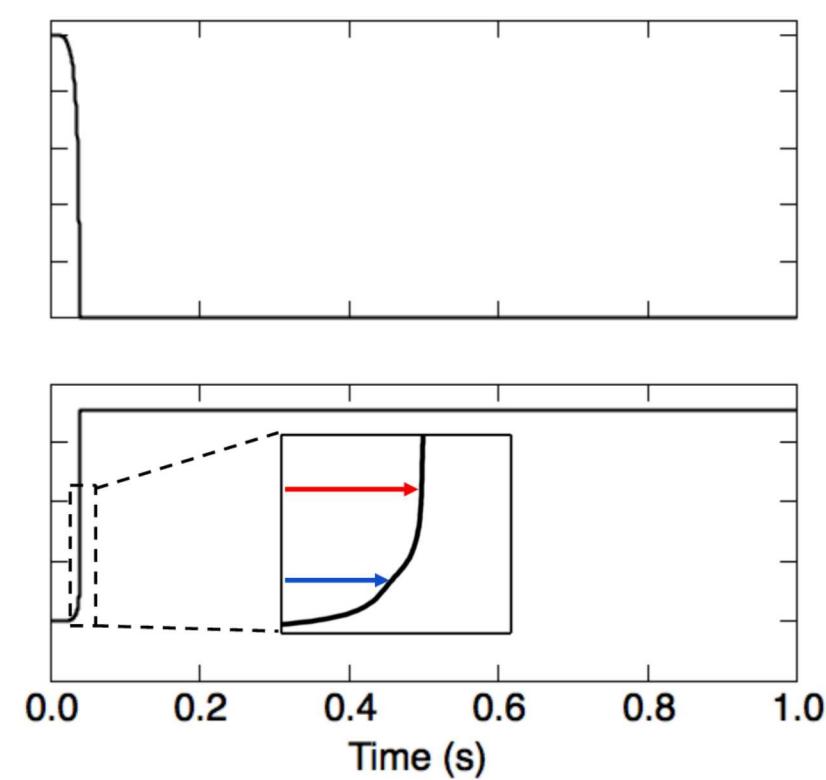
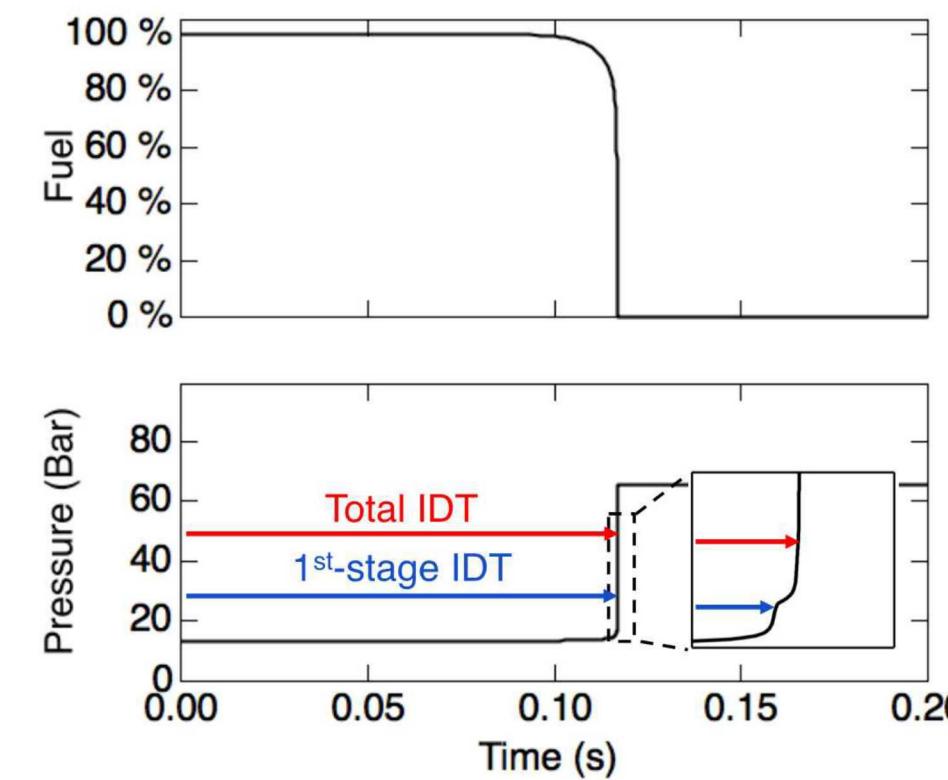
Flow Reactor Simulations:

(~1 Torr of Fuel, $\phi \approx 0.001$)



Ignition Simulations:

($\Phi = 1.0$)



For *n*-heptane:

- $\tau_{SO} \approx 1^{\text{st}}$ -Stage IDT
- Peak [OH] $\approx 10^{13}$ cm $^{-3}$

For *i*-pentanol:

- $\tau_{SO} \gg 1^{\text{st}}$ -Stage IDT
- Peak [OH] $\approx 10^{10}$ cm $^{-3}$

Is this a general trend among all fuels?

- To answer, simulated ~14k perturbed mechanisms for a diversity of fuels from 600-700 K and 10-40 bar



Perturbing Mechanisms to Generate Dataset

"Real" Fuels with Validated Chemical Mechanisms

Class	Fuel
Alkanes	Pentane isomers
	<i>n</i> -Heptane
	<i>i</i> -Octane
	Cyclohexane
	Methylcyclohexane
Alkenes/Aromatics	Butene isomers
	Hexene isomers
	Butylbenzene
	1-Butanol
Oxygenates	<i>i</i> -Pentanol
	Dimethyl Ether (DME)
	Dimethoxy Methane (DMM)
	Tetrahydrofuran (THF)
	Methyl Decanoate
Blends	Binary/Ternary/Quaternary Blends
	of <i>n</i> -Heptane/ <i>i</i> -Octane/Ethanol/Toluene

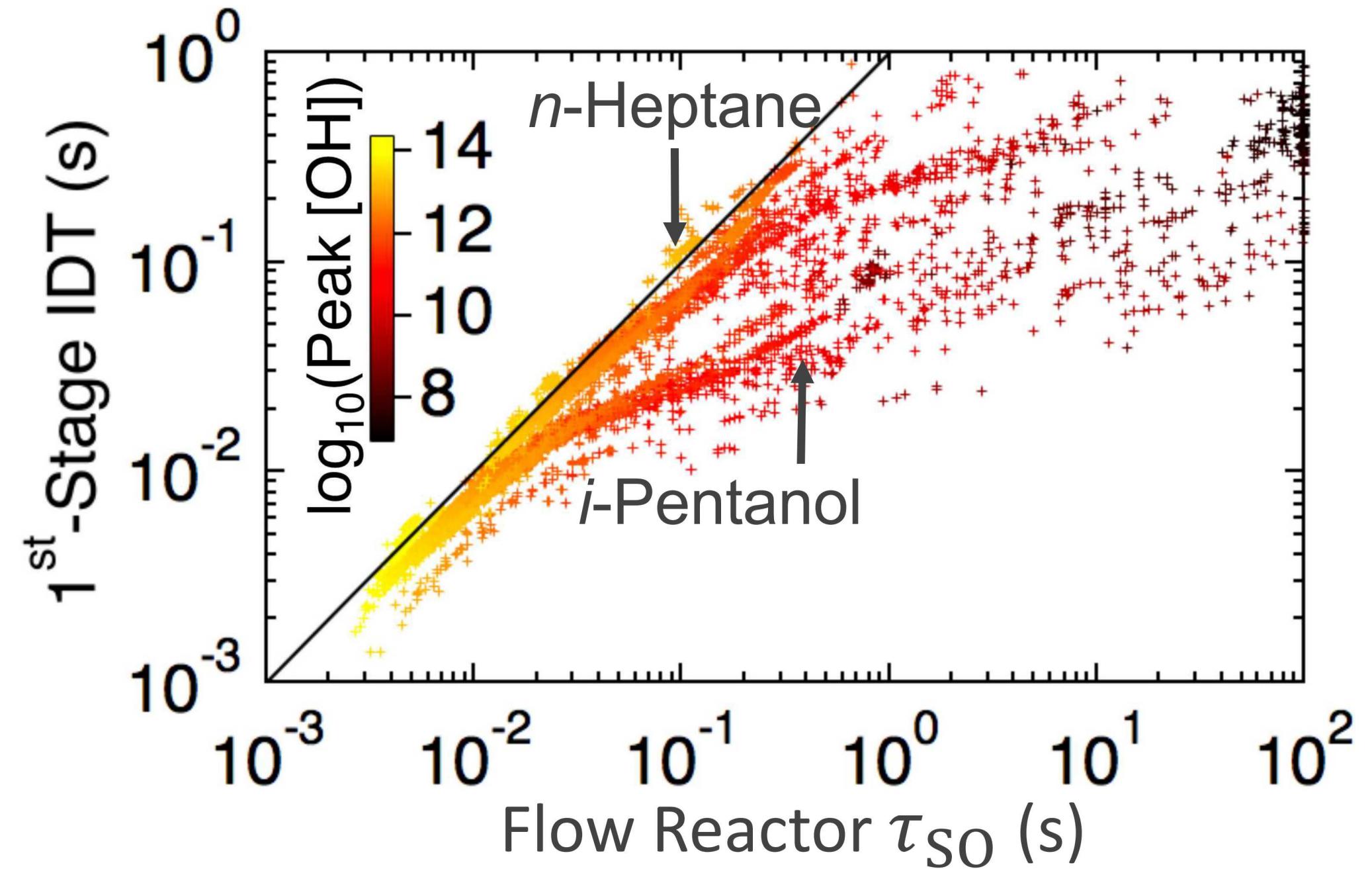
"Hypothetical" Fuels with Perturbed Chemical Mechanisms

1. Sensitive Reaction $\text{ch3och2o2} \rightleftharpoons \text{ch2och2o2h}$ A-factor Multiplied by 0.5 ×
2. Sensitive Reaction $\text{ch3och2o2} \rightleftharpoons \text{ch2och2o2h}$ A-factor Multiplied by 2.0 ×
3. Sensitive Reaction $\text{ho2ch2ocho} \rightleftharpoons \text{och2ocho+oh}$ A-factor Multiplied by 0.5 ×
4. Sensitive Reaction $\text{ho2ch2ocho} \rightleftharpoons \text{och2ocho+oh}$ A-factor Multiplied by 2.0 ×
5. Sensitive Reaction $\text{o2ch2och2o2h} \rightleftharpoons \text{ho2ch2ocho+oh}$ A-factor Multiplied by 0.5 ×
6. Sensitive Reaction $\text{o2ch2och2o2h} \rightleftharpoons \text{ho2ch2ocho+oh}$ A-factor Multiplied by 2.0 ×
7. Sensitive Reaction $\text{ho2+oh} \rightleftharpoons \text{h2o+o2}$ A-factor Multiplied by 0.5 ×
8. Sensitive Reaction $\text{ho2+oh} \rightleftharpoons \text{h2o+o2}$ A-factor Multiplied by 2.0 ×

~10 Validated Chemical Mechanisms → ~14,000 Hypothetical Fuel Mechanisms



Qualitative Trend between τ_{SO} and 1st-Stage IDT

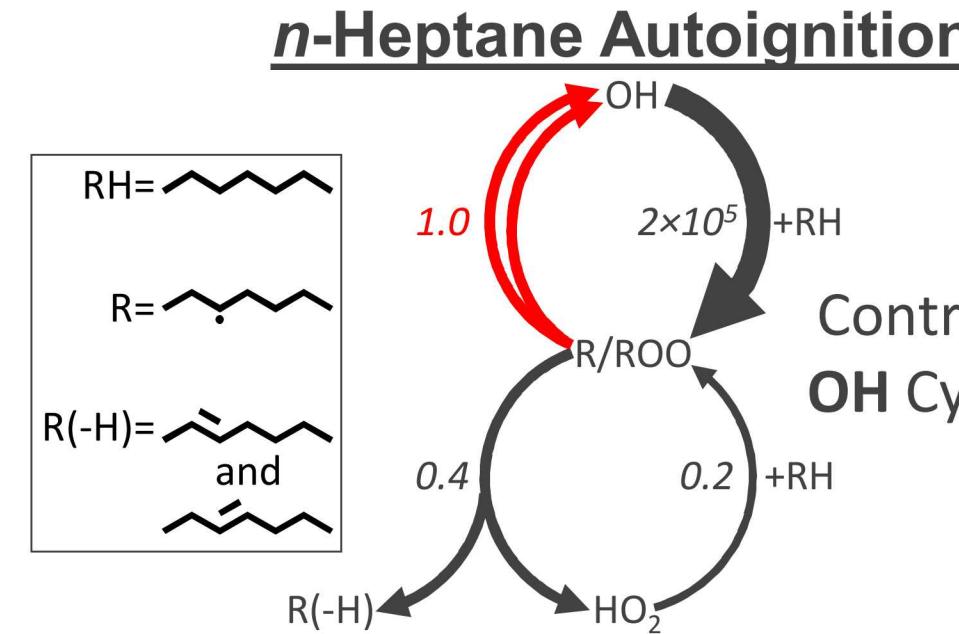


Why are some fuels affected by dilution (e.g., *i*-pentanol) and others are not (e.g., *n*-heptane)?

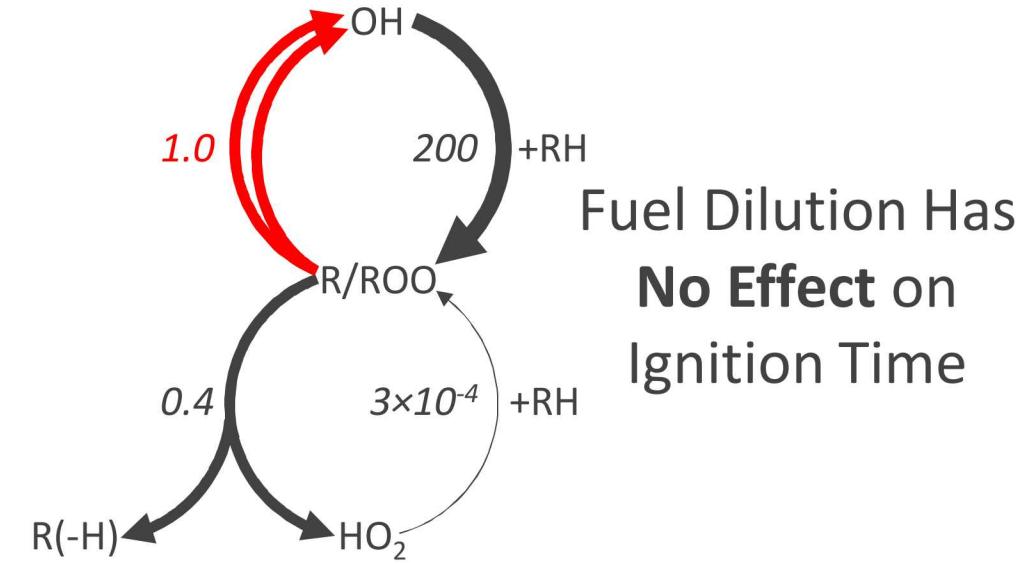


Mechanistic Effect of Fuel Dilution

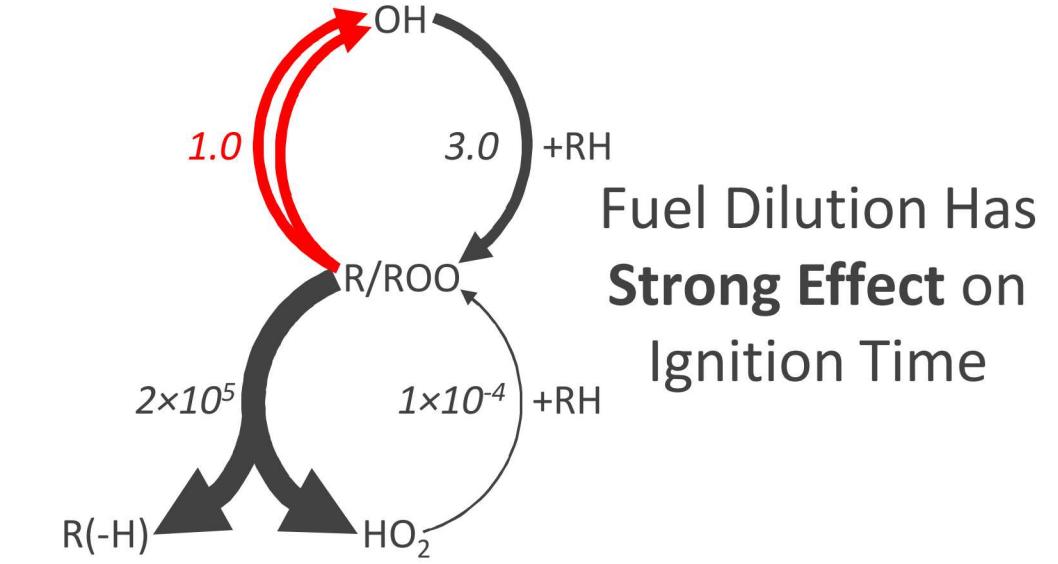
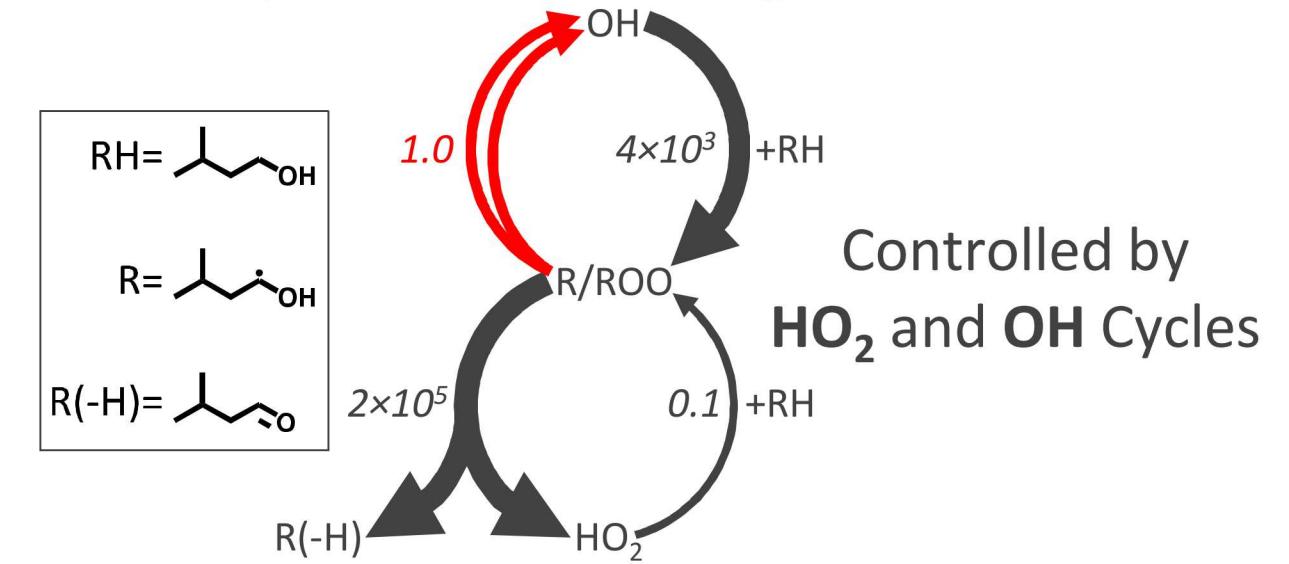
$\phi = 1.0$ in air:



$\phi \approx 0.001$
([Fuel] ≈ 1 Torr):

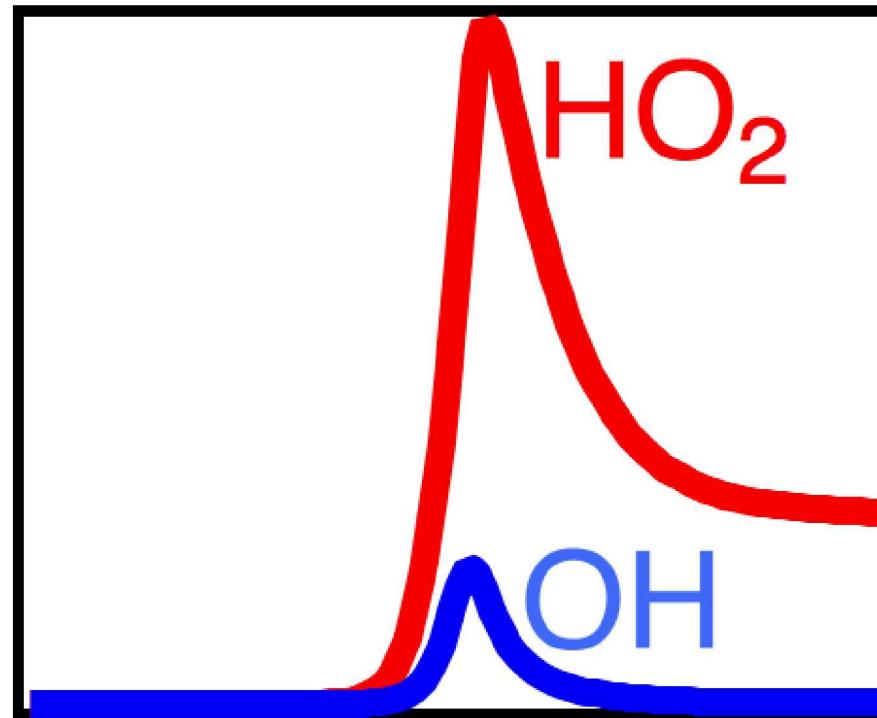


i-Pentanol Autoignition



Correlation from Polynomial Chaos Expansion (PCE) with Regularization

Inputs (\underline{x})



Flow Reactor Residence Time

$$\underline{x} = \begin{bmatrix} \tau_{SO} \\ \text{Max OH} \\ \text{Max HO}_2 \\ \text{Max OH Slope} \\ \text{Max HO}_2 \text{ Slope} \\ T \\ P \end{bmatrix} = \begin{bmatrix} x_1 \\ x_2 \\ x_3 \\ x_4 \\ x_5 \\ x_6 \\ x_7 \end{bmatrix}$$

Value that is minimized in order to fit a **parsimonious** function to data

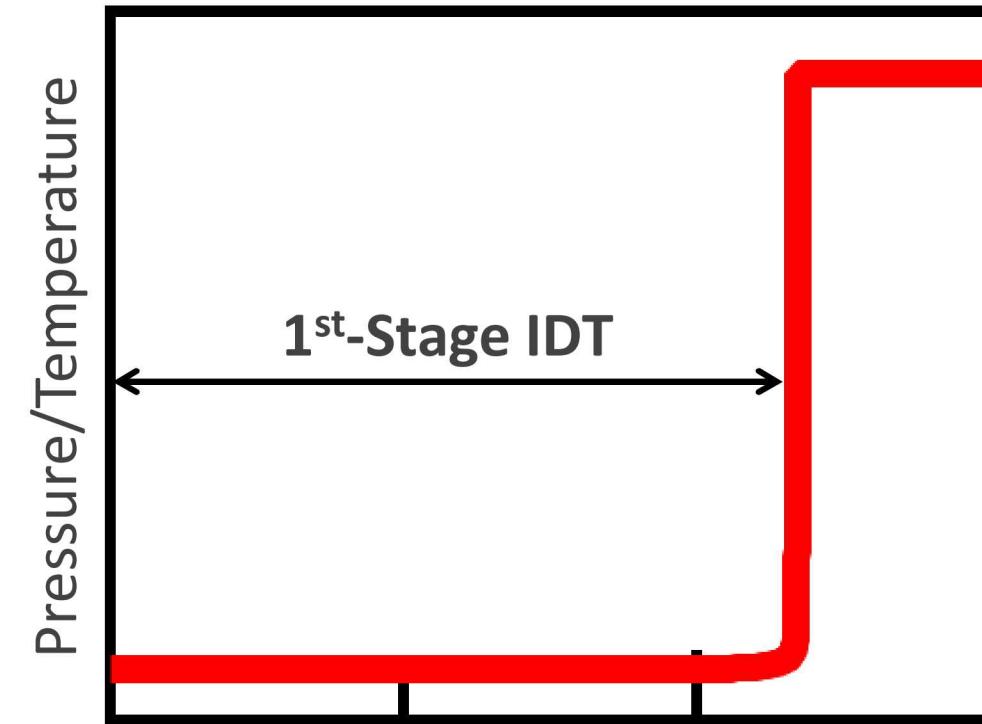
Fitting Function ($\underline{w} \cdot f(\underline{x})$)

Fitting weights: Polynomial Order ≤ 2 :

$$\underline{w} = \begin{bmatrix} w_1 \\ w_2 \\ w_3 \\ w_4 \\ w_5 \\ \dots \\ w_{35} \\ w_{36} \end{bmatrix}$$

$$f(\underline{x}) = \begin{bmatrix} 1 \\ x_1 \\ x_1^2 \\ x_1 x_2 \\ x_1 x_3 \\ \dots \\ x_6 x_7 \\ x_7^2 \end{bmatrix}$$

Target (y)



Time

Objective Function (L)

$$L = |y - \underline{w} \cdot f(\underline{x})| + \lambda |\underline{w}|_1$$

Difference between polynomial fit and data

Regularization term to prevent overfitting (λ is adjustable parameter)

$$\begin{aligned} y &= \text{1st-Stage IDT} \\ &\text{or} \\ y &= \text{LTHR} \\ &\text{or} \\ y &= \phi\text{-Sensitivity} \end{aligned}$$

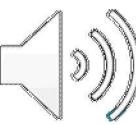
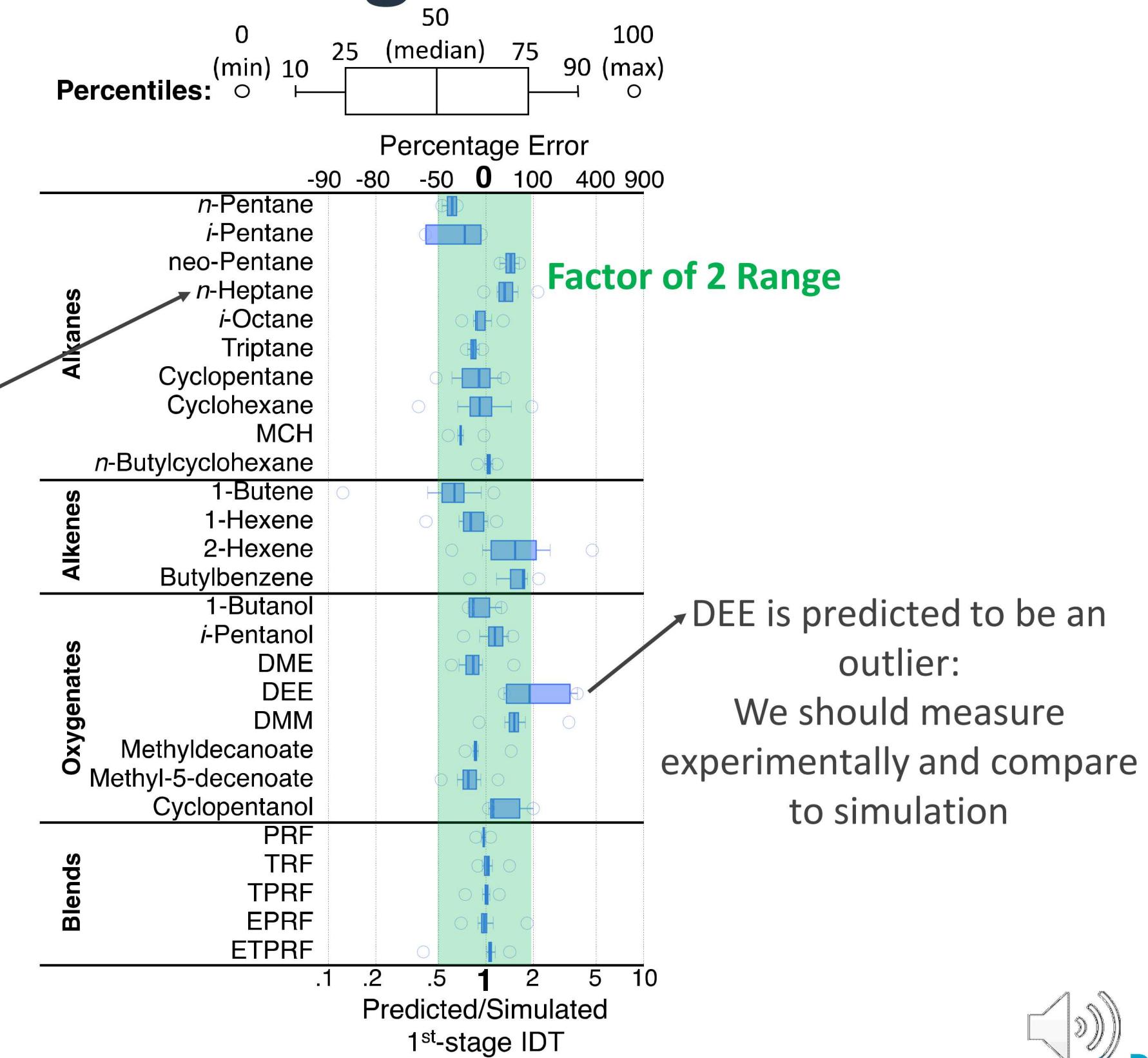
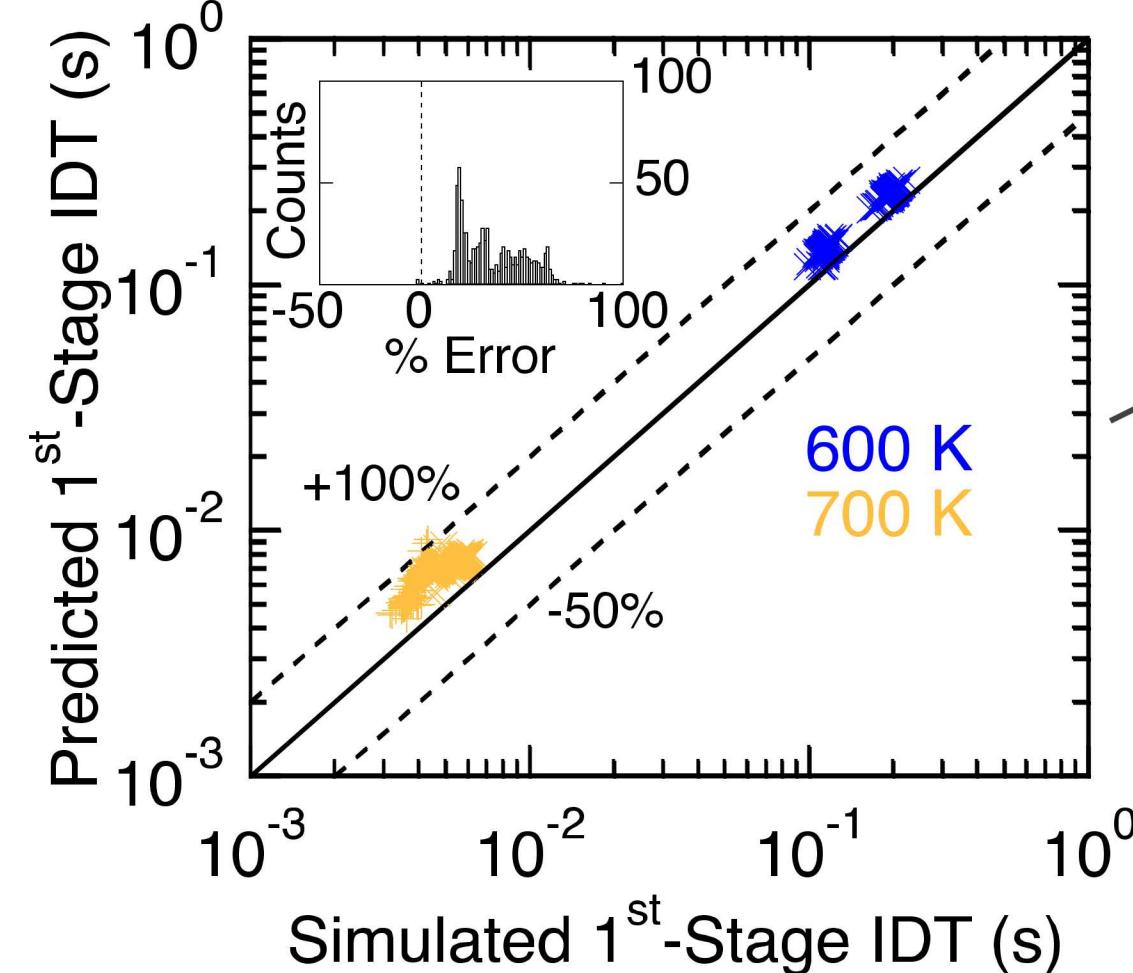


Leave-One-Fuel-Out Tests: 1st-Stage IDT

For Example:

Train on All ~13k Simulations Except *n*-Heptane

Test on ~1k *n*-Heptane Simulations

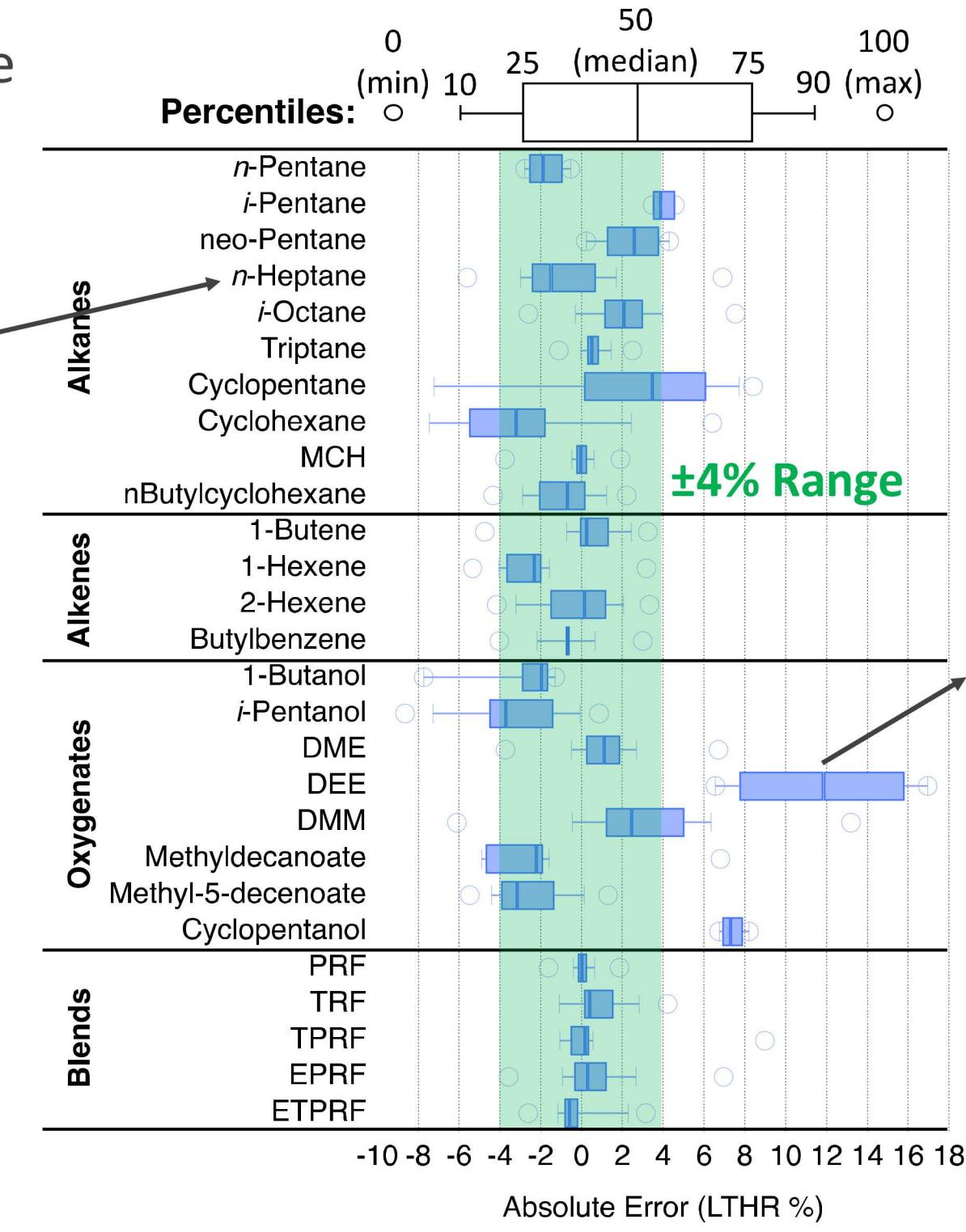
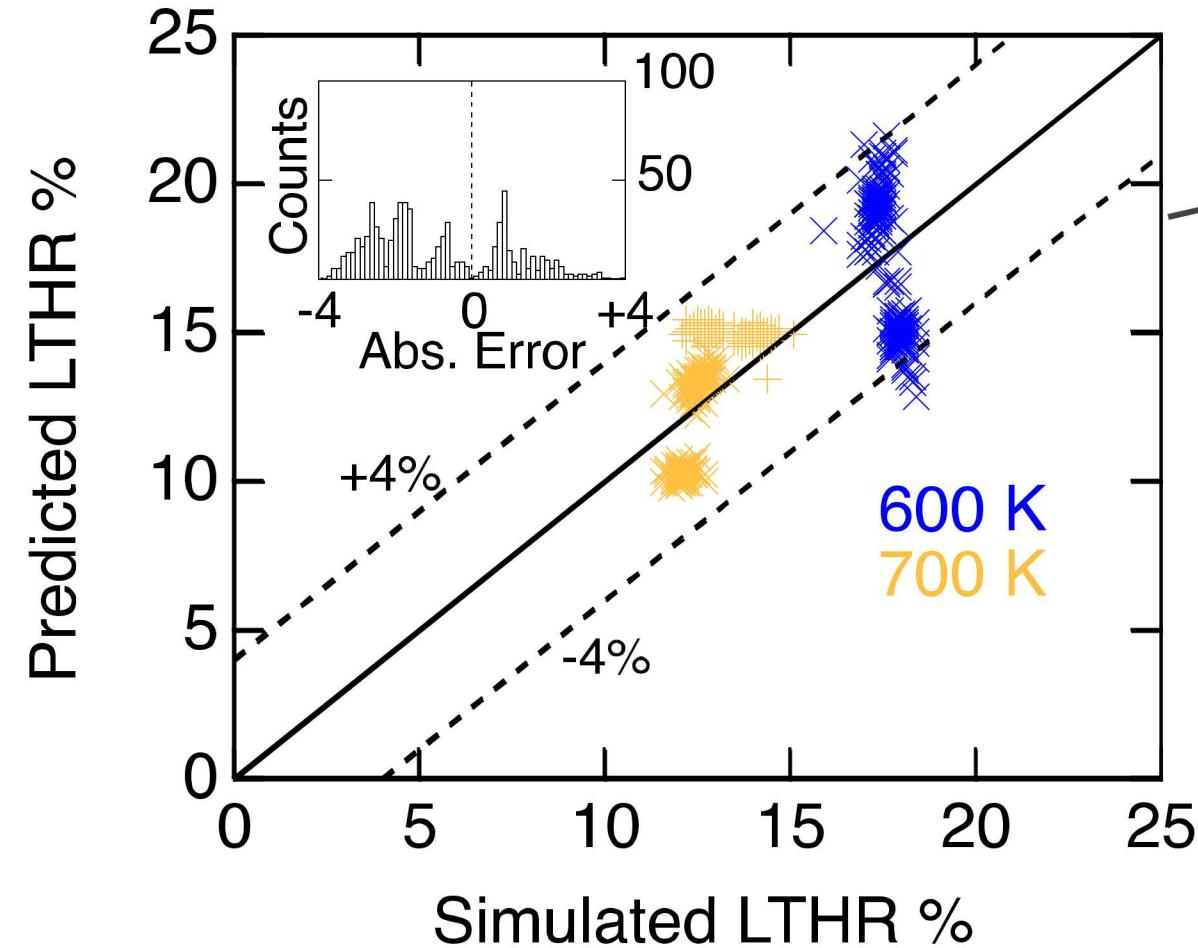


Leave-One-Fuel-Out Tests: LTHR

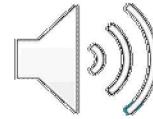
For Example:

Train on All ~13k Simulations Except *n*-Heptane

Test on ~1k *n*-Heptane Simulations:



DEE is predicted to be an outlier:
We should measure experimentally and compare to simulation

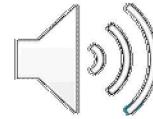
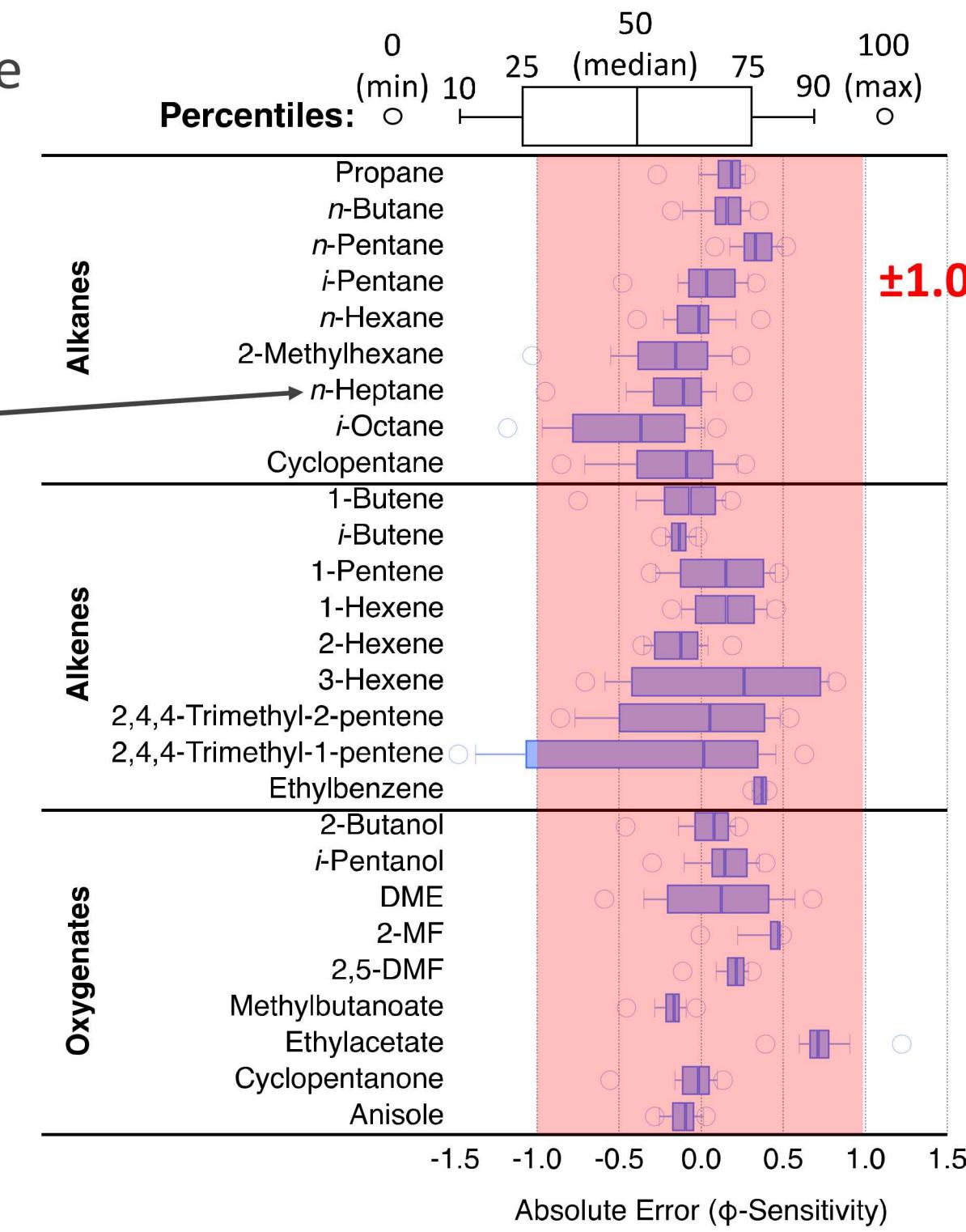
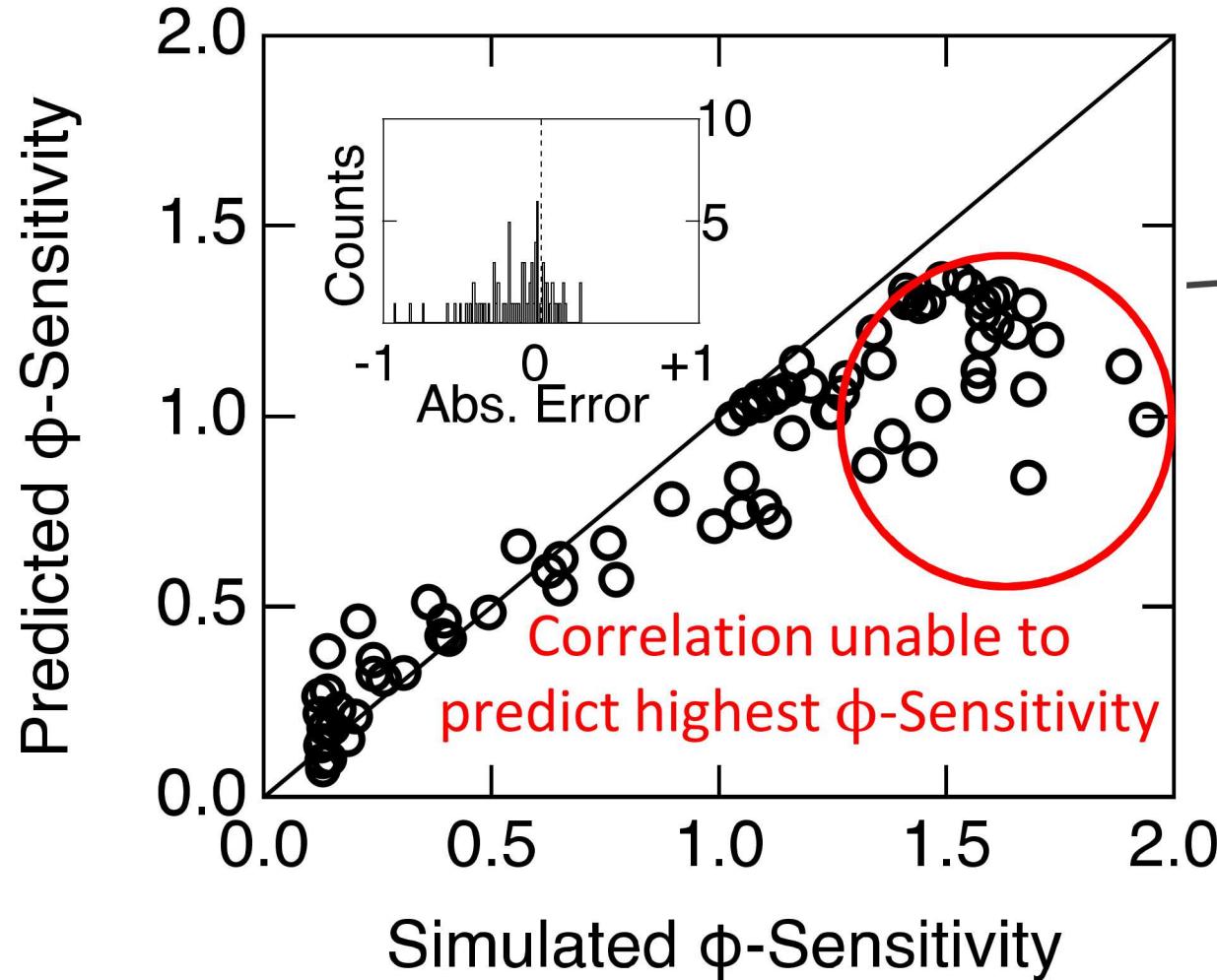


Leave-One-Fuel-Out Tests: ϕ -sensitivity

For Example (smaller dataset):

Train on All ~1.8k Simulations Except *n*-Heptane

Test on ~80 *n*-Heptane Simulations:



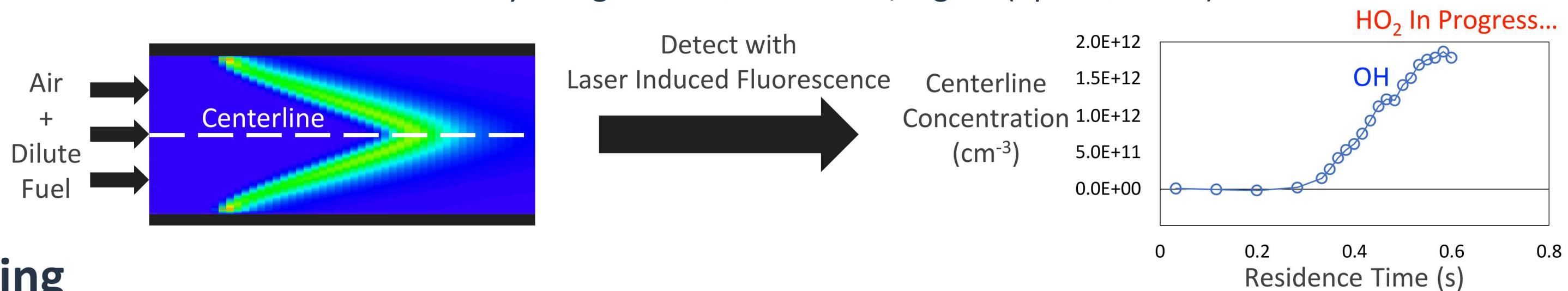
Conclusions

Used PCE to find correlations between OH/HO₂ profiles simulated in a high-P flow reactor with dilute fuel and:

1. 1st-Stage IDT → Correlation predicts values within a factor of 2
2. LTHR % → Correlation predicts absolute values within 4%
3. ϕ -Sensitivity → Correlation does not predict (interesting) high values
→ A different experiment that can measure intermediate-T chemistry might be more suitable

Next Steps

Experimental measurements of OH currently being conducted in a new, high-P (up to 100 bar) laminar flow reactor:



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