

# Optical Fiber-based Corrosion Sensor with Fe/SiO<sub>2</sub> Composite Coating



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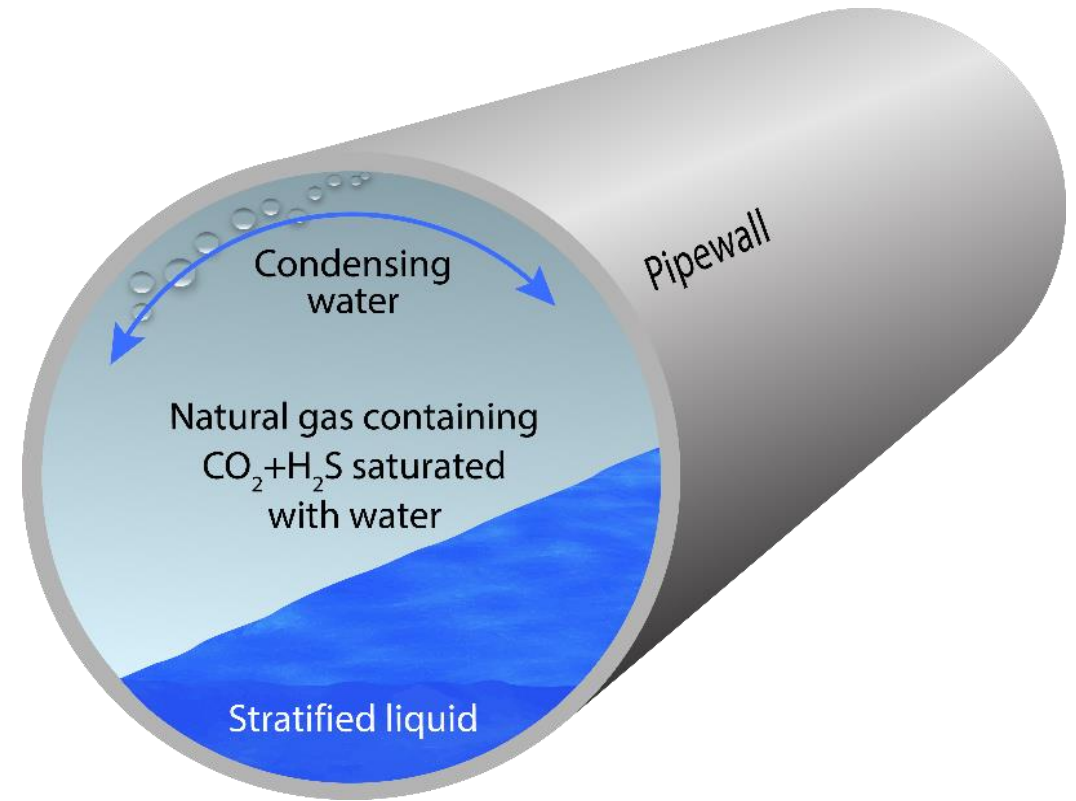
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- Research Background
- Experimental Procedure
- Results and Discussion
- Conclusions
- Acknowledgment and Disclaimer

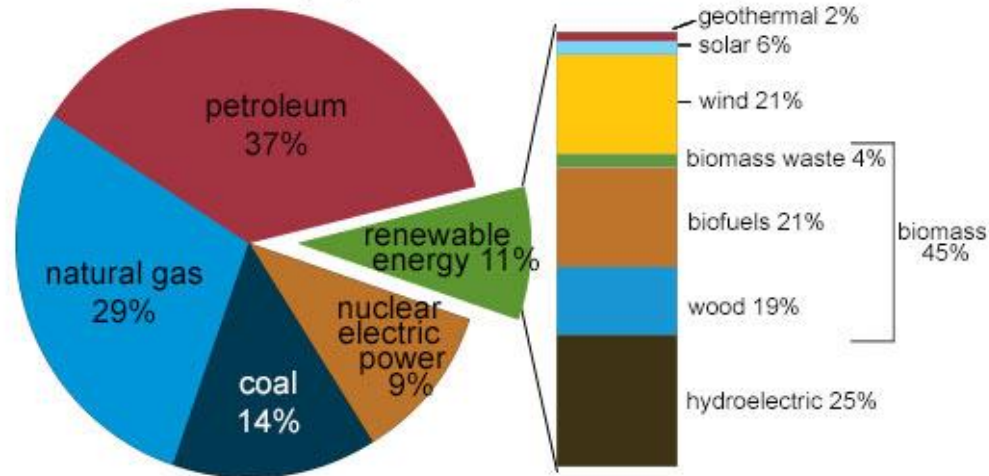




# Corrosion in Oil and Natural Gas Industry

## U.S. energy consumption by energy source, 2017

Total = 97.7 quadrillion  
British thermal units (Btu)



Note: Sum of components may not equal 100% because of independent rounding.  
Source: U.S. Energy Information Administration, *Monthly Energy Review*, Table 1.3 and 10.1, April 2018, preliminary data

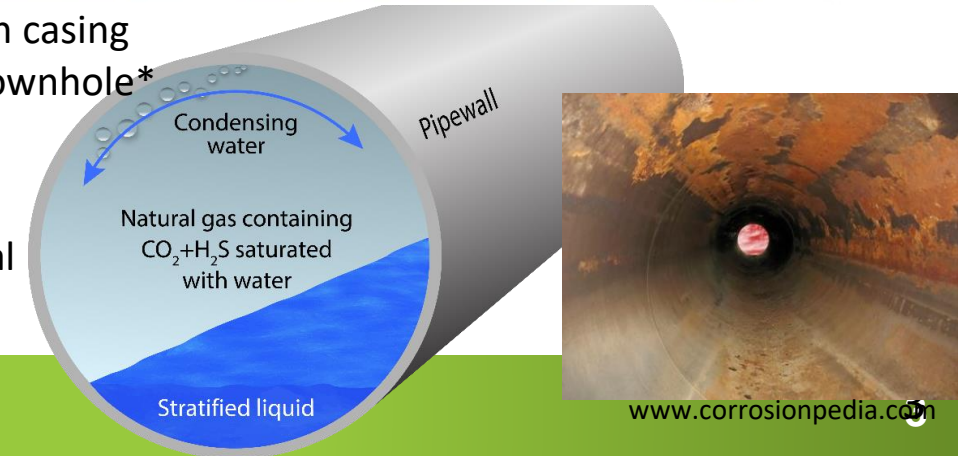


- \$1.4 billion annually: direct corrosion costs in domestic oil and gas exploration and production in the U.S.
- \$589 million: surface piping and facility costs
- \$463 million: downhole tubing expenses
- \$320 million: capital expenditures related to corrosion.
- **25~30% can be saved** with optimal corrosion management.



Corroded production casing  
pipe sample from downhole\*

## Top-of-line corrosion in Natural gas transmission pipeline

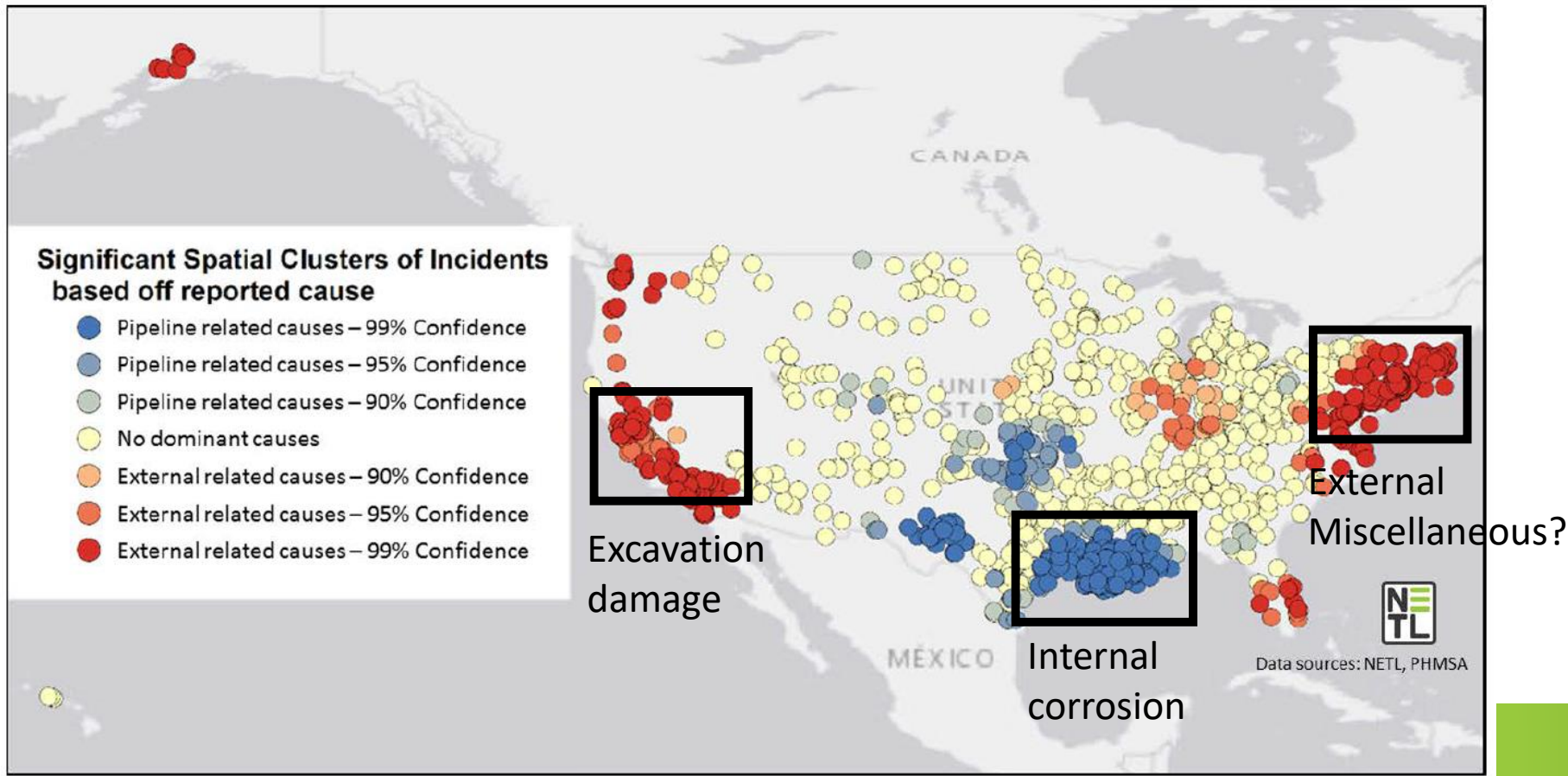


Koch, G. H., Brongers, Michiel, P. H., Thompson, N. G., Virmani, Y. P. and Payer, J. H., "Corrosion costs and preventive strategies in the United States" (2002).

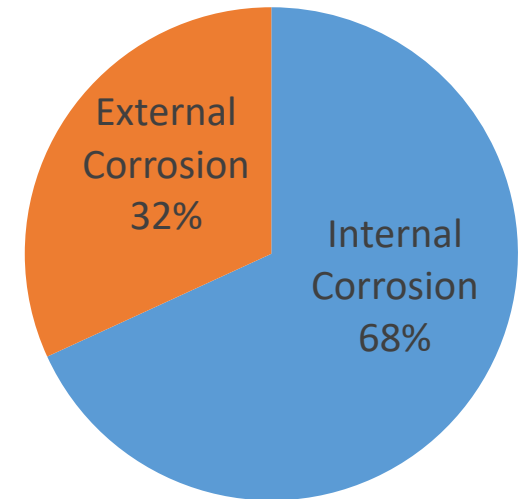
\* University of North Dakota Energy & Environmental Research Center.

# Corrosion in Natural Gas Pipelines

- 528,000 km of Natural Gas Transmission & Gathering Pipelines in U.S.
- ~ \$4.5 billion Corrosion-related Annual Cost to monitor, replace, and maintain these assets.



**2010-2016  
Transmission Pipelines**



# Corrosion is an electrochemical process that causes mass loss and structural deterioration

Dissolution of CO<sub>2</sub>: CO<sub>2</sub>(g) ↔ CO<sub>2</sub>(aq)

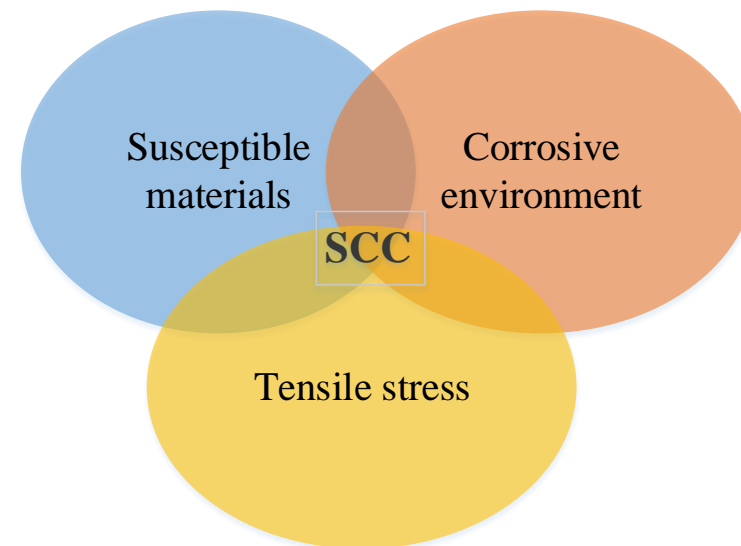
Hydration of CO<sub>2</sub>: CO<sub>2</sub>(aq) + H<sub>2</sub>O(l) ↔ H<sub>2</sub>CO<sub>3</sub>(aq)

~ 0.2% of CO<sub>2</sub>(aq) and quite slow

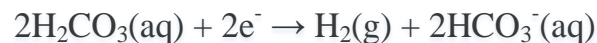
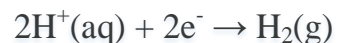
Dissociation of H<sub>2</sub>CO<sub>3</sub>(aq):

H<sub>2</sub>CO<sub>3</sub>(aq) ↔ H<sup>+</sup>(aq) + HCO<sub>3</sub><sup>-</sup>(aq),  $pK_1=6.35$  at 25 °C

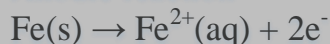
HCO<sub>3</sub><sup>-</sup>(aq) ↔ H<sup>+</sup>(aq) + CO<sub>3</sub><sup>2-</sup>(aq),  $pK_2=10.33$  at 25 °C



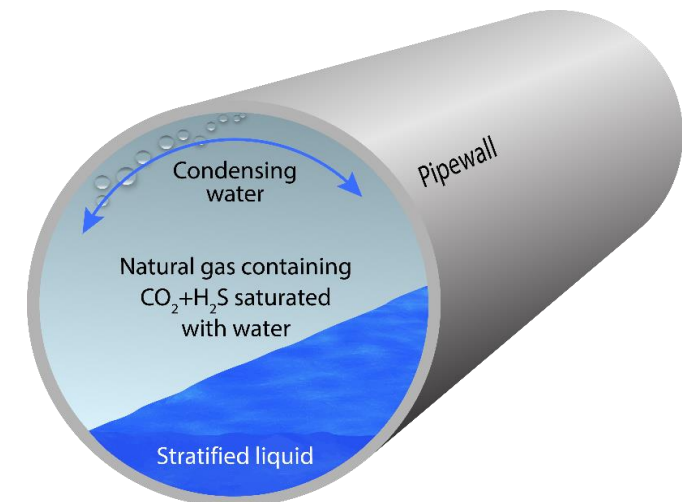
Cathodic reaction



Anodic reaction



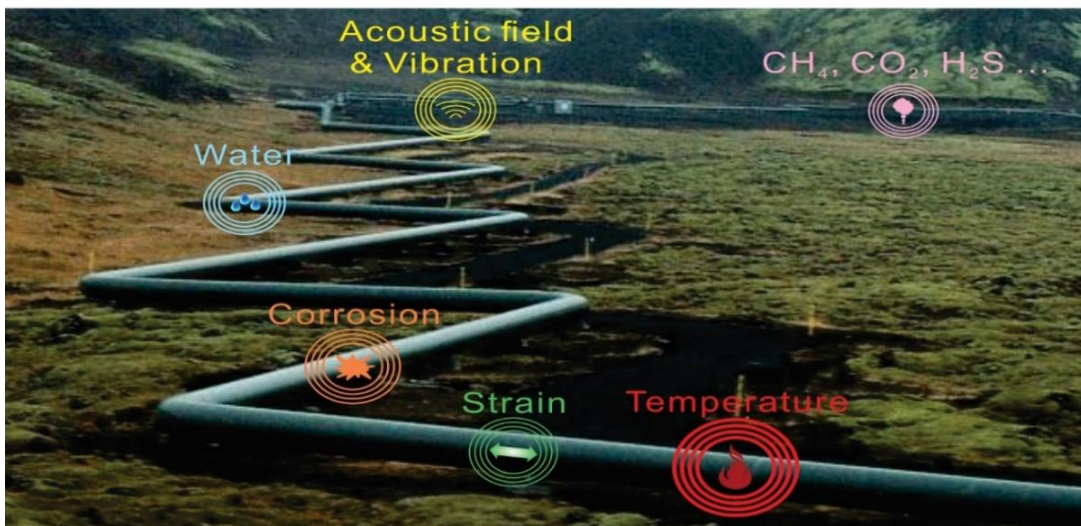
Iron or Steel



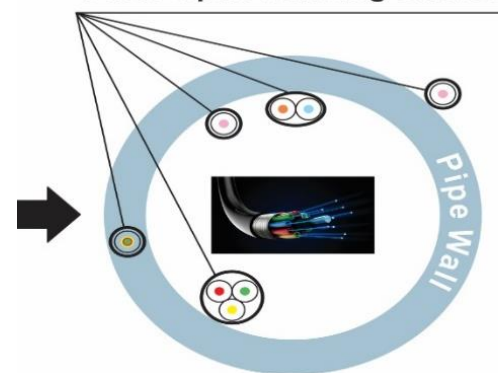


# Optical Fiber Sensor Platform

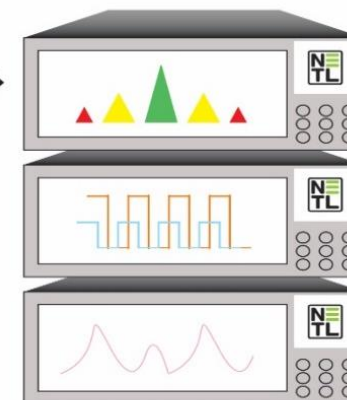
## Pipeline Integrated with Distributed Optical Fiber >100 km



## Fiber Optic Sensing Cables



## Distributed Sensor Interrogator (DSI)



## Monitoring and Manage

- > Pipeline Structure Health Monitoring
- > Infrastructure Perimeter Security
- > Hotspot detection
- > Early Corrosion Prediction and Quantification
- > Methane Leakage Alert
- ...

Emphasis Within NETL Research & Innovation Center:

- Optimize Interrogation System (Range, Resolution, Cost)
- Early Corrosion On-Set Detection
- Methane Leak Detection & In-Pipe Gas Composition Monitoring

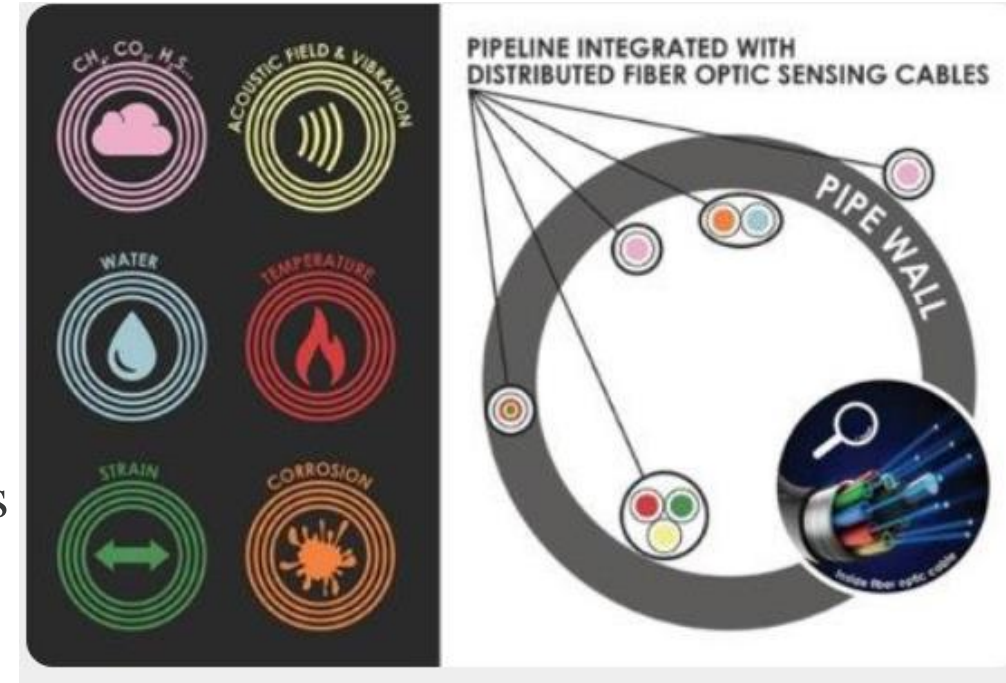
**A Multi-Parameter, Distributed Optical Fiber Sensor Platform Enabling Reliability & Flexibility**

**Target Metrics = >100km Interrogation, <1m Spatial Resolution, Cost ~\$30k (<\$0.30 / m)**

# Optical fiber sensors

- **Advantages of optical fiber sensors (OFS)**

- nondestructive monitoring
- in-situ distributive measurements
- small size, flexibility, geometric versatility, light weight
- inherent immunity to electromagnetic interference (EMI)
- compatibility to optical fiber data communication systems
- improved safety in the presence of flammable gas environments as compared to electrical based sensors
- can be functionalized with specific sensing materials



<http://www.materialsperformance.com/news/2018/09/fiber-optic-sensors-prevent-corrosion-of-natural-gas-pipelines>

# Distributed OFS sensing principle

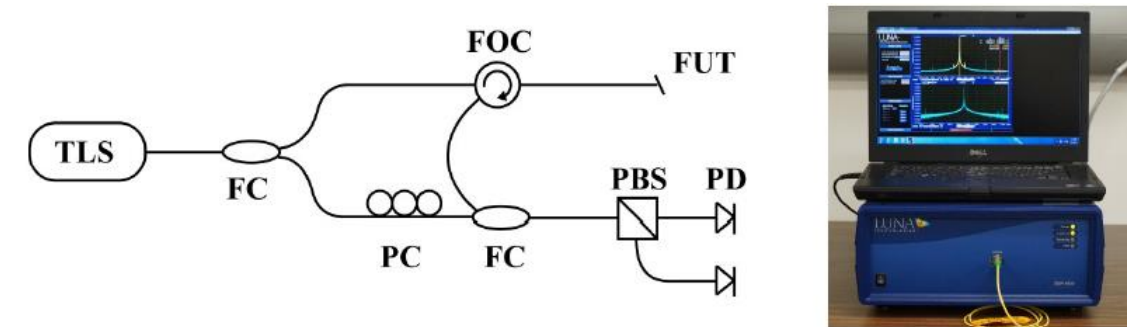
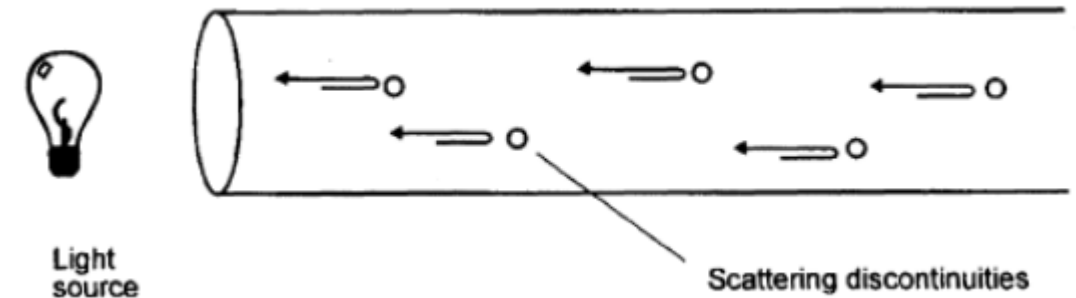
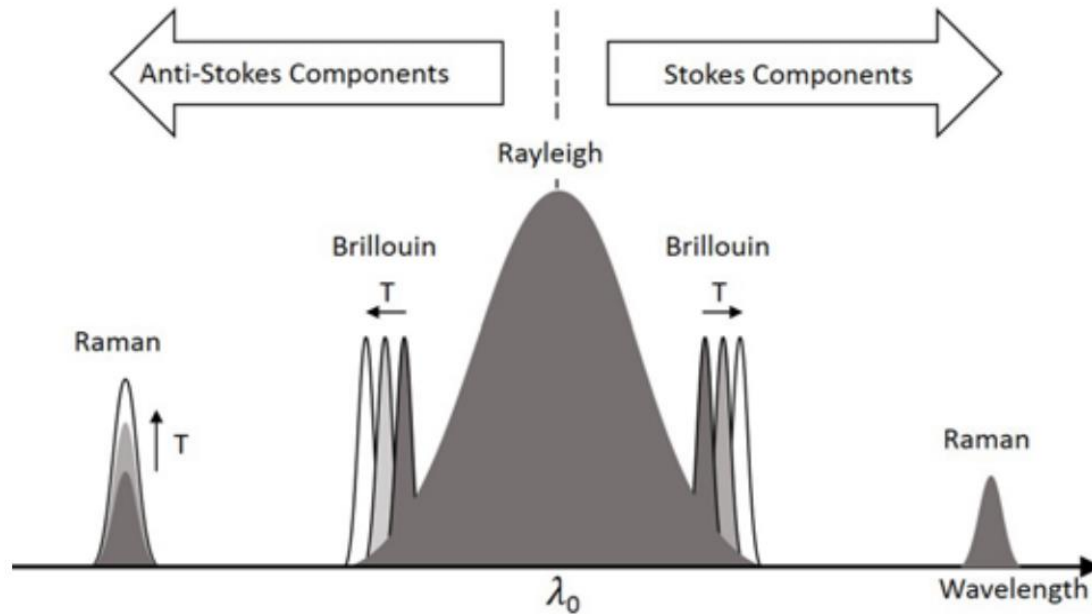


Figure 1 – LUNA OBR 4600 distributed interrogator LEFT: internal components (TLS: tunable laser source, FC: fiber coupler, FOC: fiber optic circulator, PC: polarization controller, PBS: polarizing beamsplitter, PD: photodiode); RIGHT: photo of instrument.

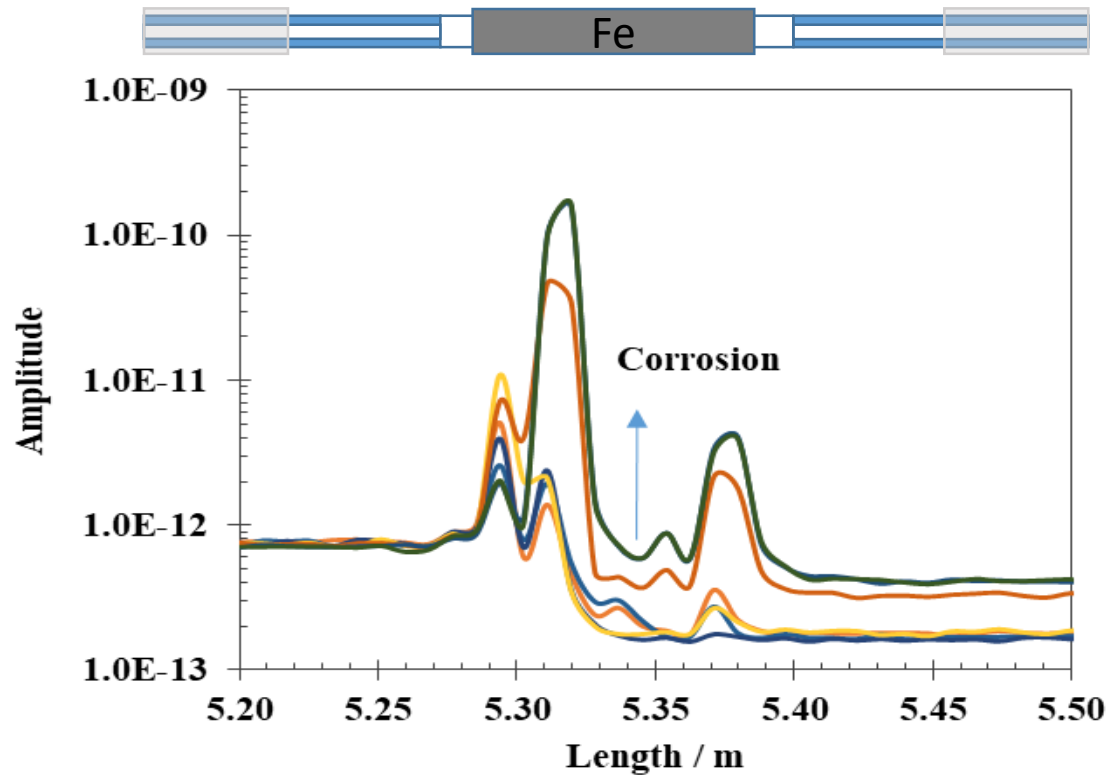
## Optical backscatter reflectometer (OBR)

- Distributed OFS enables continuous real-time monitoring over the whole structure at a reduced cost per length unit.



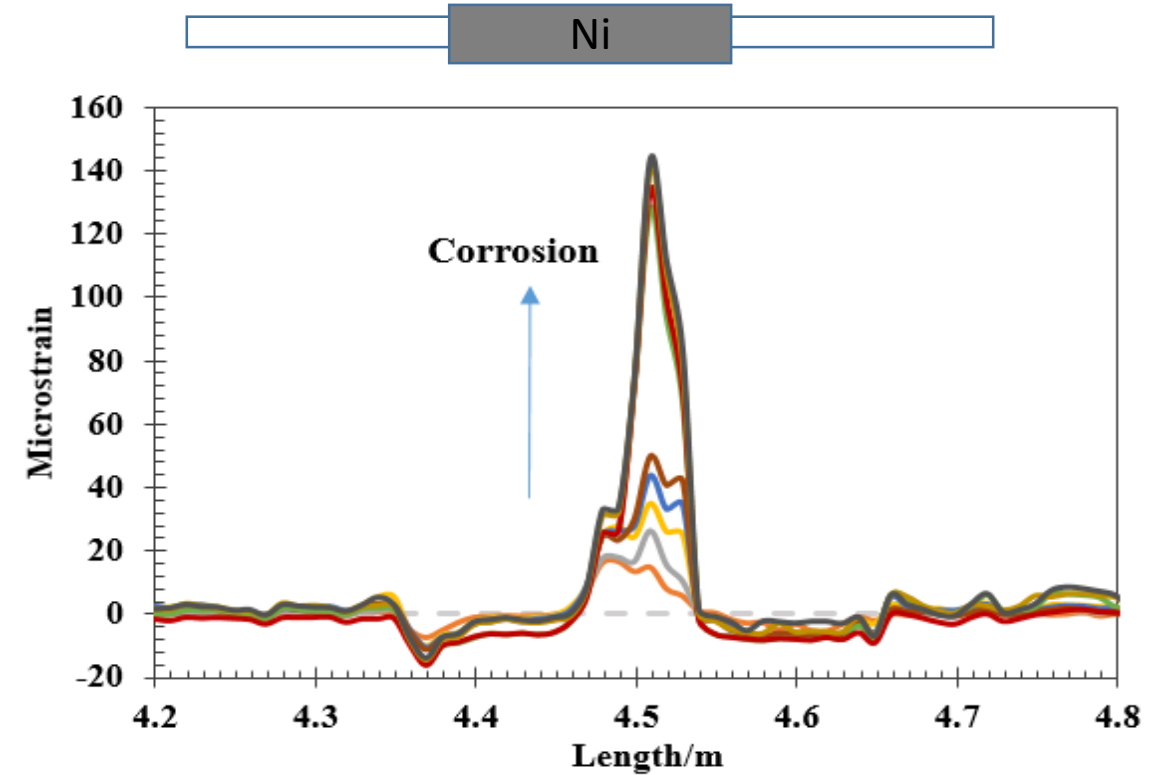
# Corrosion sensors from previous work

Multi-mode Fiber Coreless Fiber Multi-mode Fiber



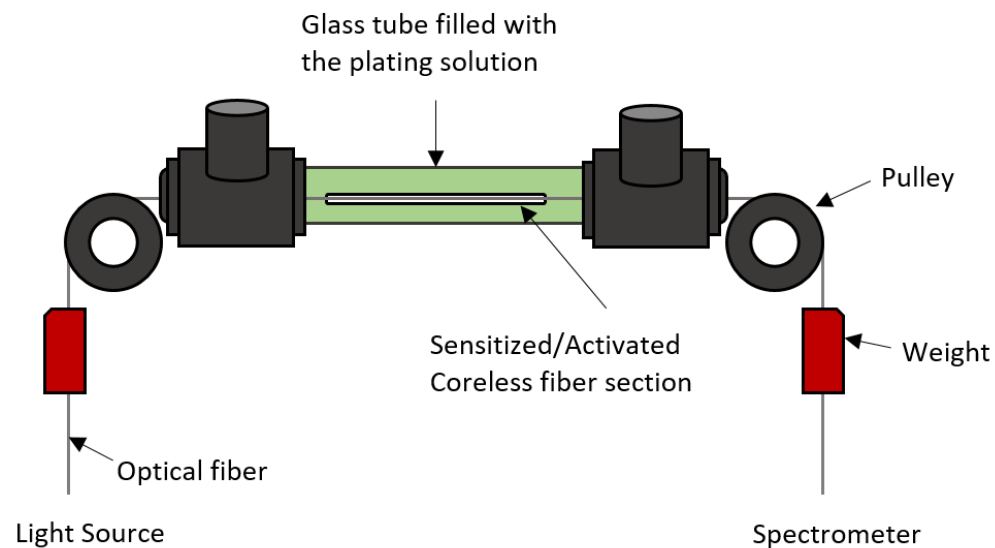
Rayleigh backscattered light increased as corrosion of Fe film proceeded

Single-mode Fiber



Microstrain on the fiber increased with mass loss of coated metallic Ni film.

# Experimental Setup



Transmission measurement during the Fe plating onto and dissolution from the  $\text{SiO}_2$  coated optical fiber.



# Fe/SiO<sub>2</sub> Composite Coating Preparation

TEOS sol-gel for dip coating to form SiO<sub>2</sub> layer

Chemical	Amount	Stir Hot plate T	Dip/travel	Calcination
DI	1mL	60 °C for 3h	~25 travels of coreless fiber	Up, 3h; 600 °C, 2h; Cool, 3h
Ethanol	4.5mL			
TEOS	4.5mL			



Cleaning and Prep

Chemical	Amount	Operation
Acetone	100%	<5min, Sliding
DI water	Rinse	Air dry
NaOH	10M, 50C	<5min, Sliding in PTFE plate
DI water	Rinse	Air dry



Fe Electroless Plating

Chemical	Amount	Operation
FeSO <sub>4</sub> ·7H <sub>2</sub> O	11g/L	Stir, 30mL
C <sub>6</sub> H <sub>5</sub> Na <sub>3</sub> O <sub>7</sub> ·2H <sub>2</sub> O (Sodium Citrate)	57g/L	Stir, 30mL
H <sub>3</sub> BO <sub>3</sub>	10g/L	Stir, 30mL
NaOH	1.2M to pH 9.8@22C	Drops
NaBH <sub>4</sub>	3.0g/L	Added the last



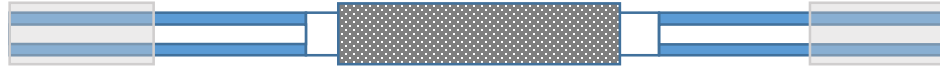
Sensitization & Activation

Chemical	Amount	Operation
SnCl <sub>2</sub>	22.6g/L	Stir, 30mL Immerse, 20min at 50C
HCl, conc.	10mL/L	
PdCl <sub>2</sub>	0.795g/L	Stir, 30mL Immerse, 20min at 50C
HCl, conc.	5mL/L	

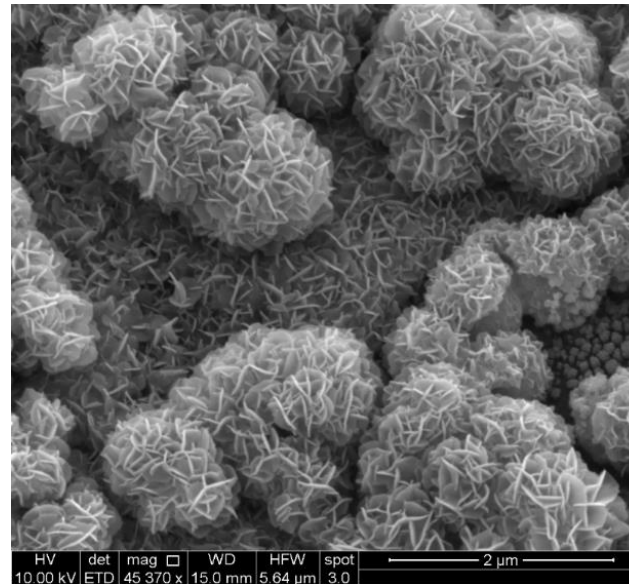
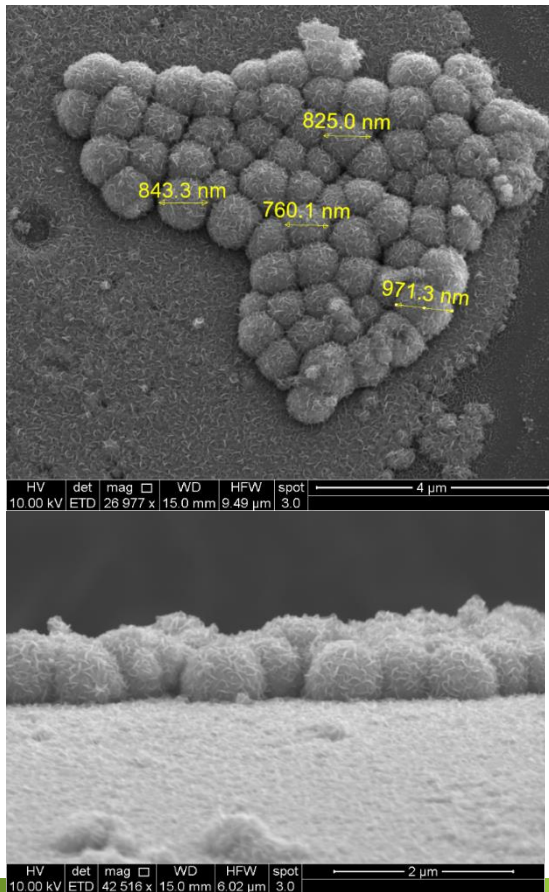
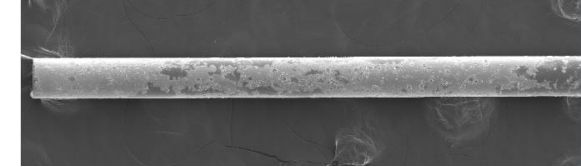


# Fe plating on sub-micron SiO<sub>2</sub> spheres

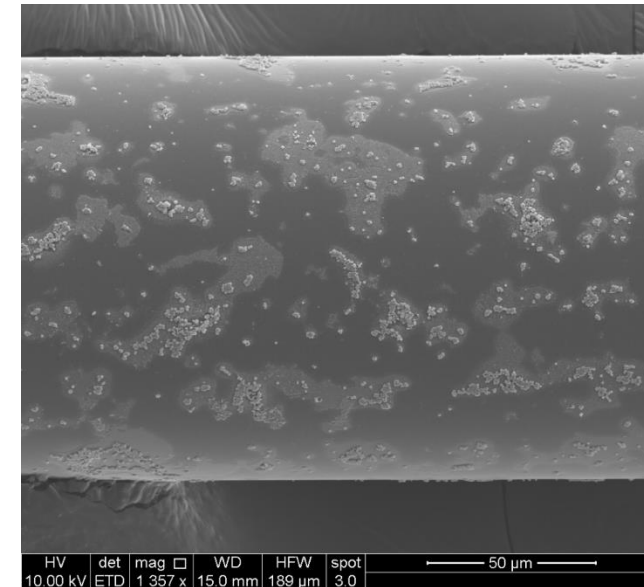
Fe on SiO<sub>2</sub> spheres



Multi-mode Fiber Coreless Fiber Multi-mode Fiber



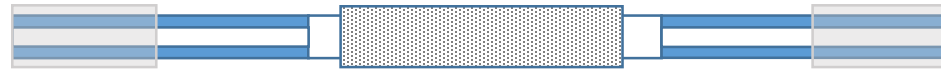
- Fe coated SiO<sub>2</sub> spheres with about hundreds of nm thickness. (~1h)
- Honeycomb-like Fe coating.



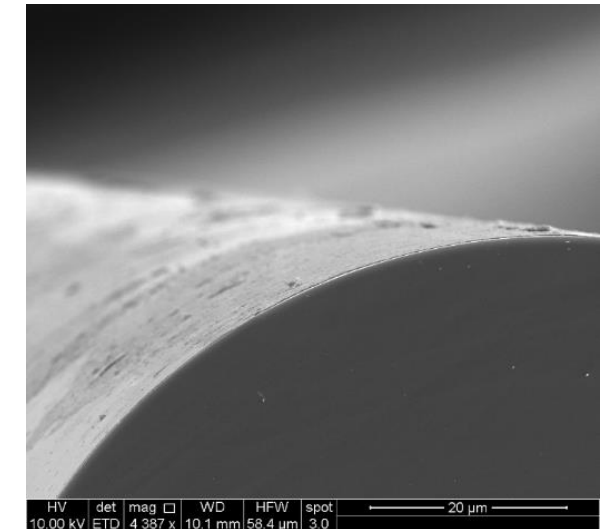
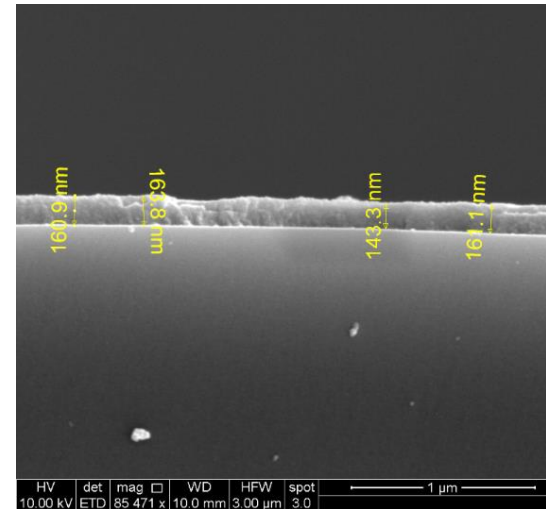
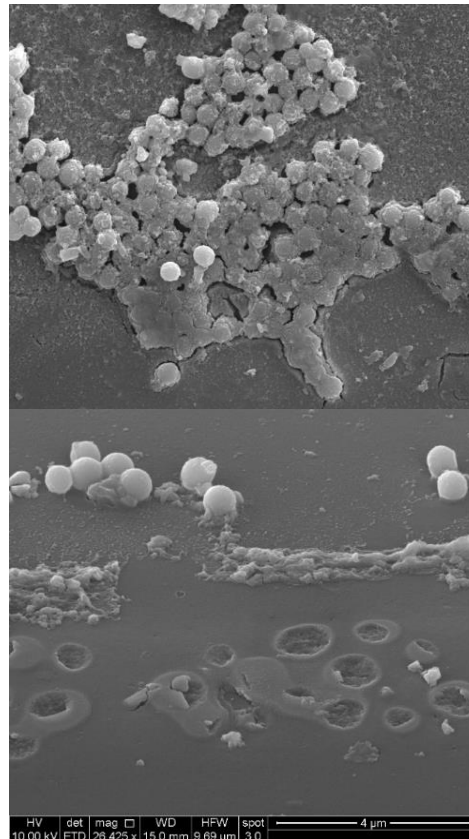
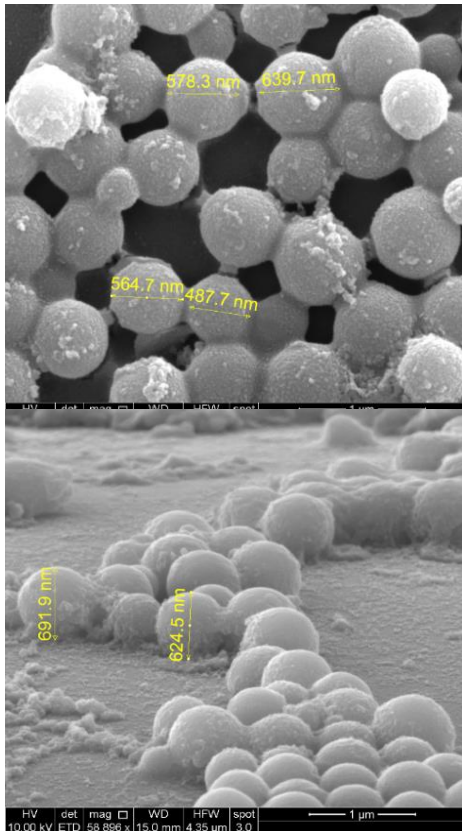
- The patches of Fe coating indicates that SiO<sub>2</sub> spheres/coating facilitated Fe plating.

# After Fe dissolution in pH2 (SEM)

SiO<sub>2</sub> spheres

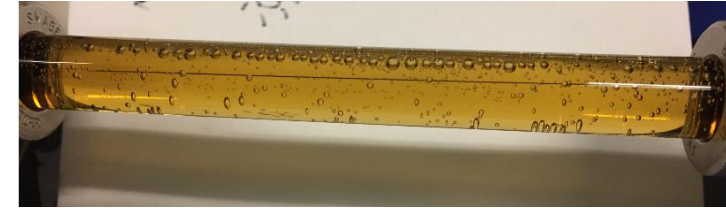
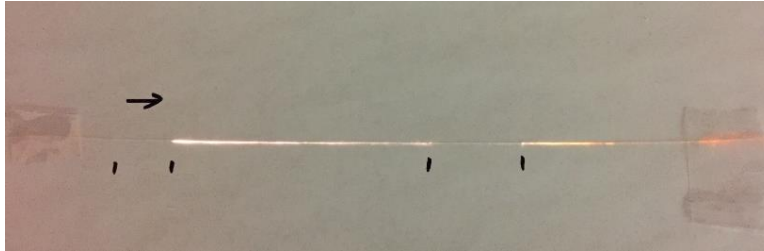


Multi-mode Fiber Coreless Fiber Multi-mode Fiber

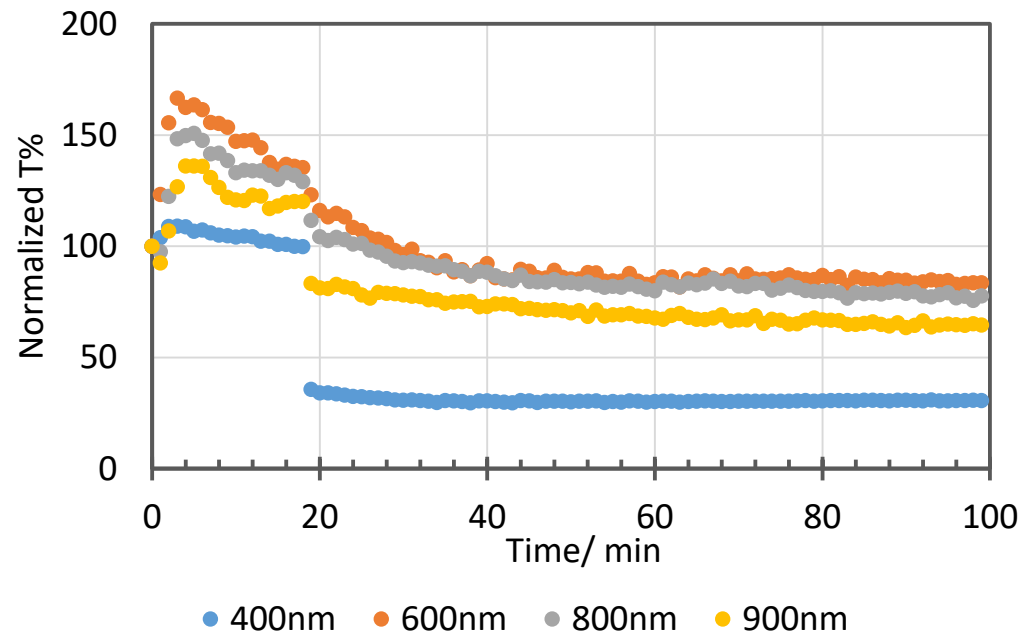


- Fe coating was dissolved in pH 2.
- A ~150nm uniform coating was observed in the cross-section. Porous SiO<sub>2</sub> or residual Fe?

# T% decreased during Fe plating



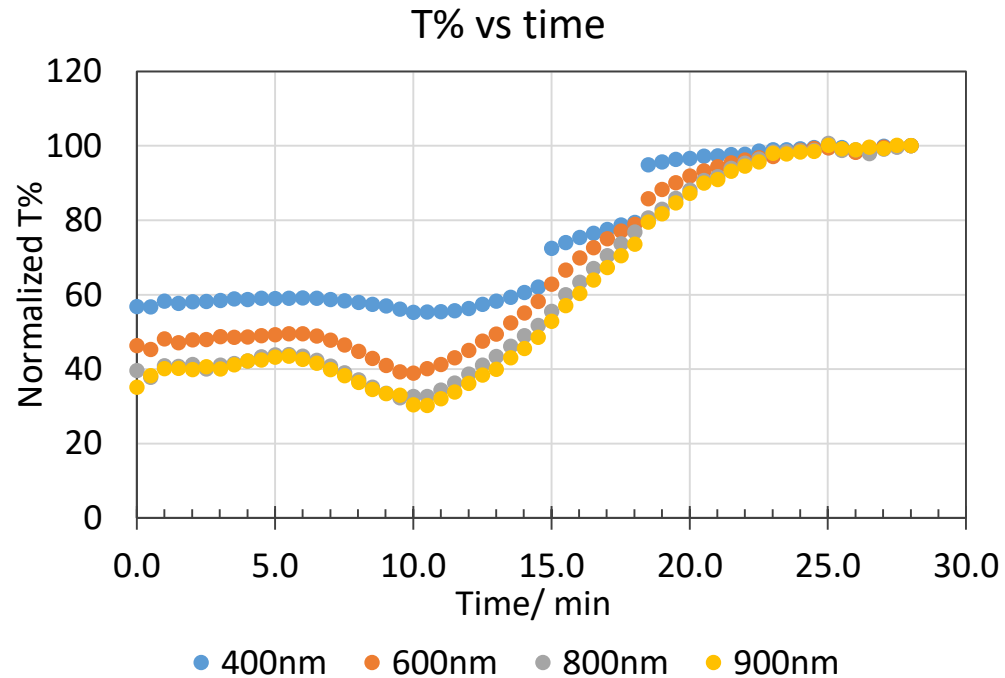
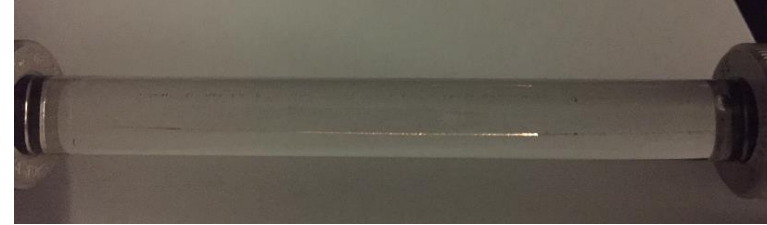
T% vs time



- T% increased in the first 2 mins, probably due to the  $H_2$  gas formation on the surface at the early stage of Fe plating.
- T% then decreased after Fe deposited on the fiber due to Fe light absorption.
- For the wavelengths of 600nm and 800nm, T% became relatively stable after 60min.
- Wavelengths of 400nm and 900nm were affected more by the integration time because of low SNR.



# T% increased during Fe dissolution in pH 2



- T% increased as Fe dissolved, which enables corrosion monitoring.

# Conclusions

- A Fe/SiO<sub>2</sub> composite film was studied as the sensing film where the SiO<sub>2</sub> layer provides roughness/porosity and light coupling and the Fe layer serves as the corrosion sensing element.
- The composite film was prepared through a sol-gel and electroless plating combined process with potential for mass production.
- T% decreased after Fe deposited on the fiber due to light absorption of Fe film.
- T% increased as Fe dissolved, which enables corrosion monitoring using this Fe/SiO<sub>2</sub> coated optical fiber.

# Acknowledgments



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# Disclaimer

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