

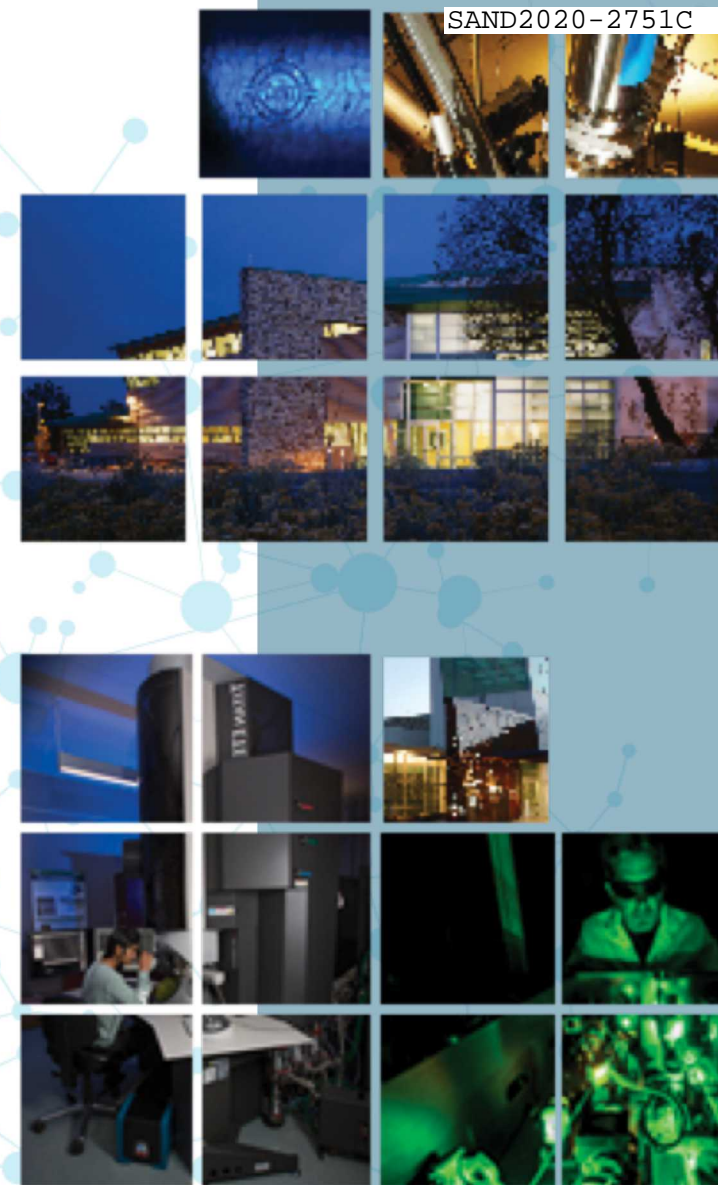
# Flow-Arrest Transition in (Frictional) Granular Materials

Ishan Srivastava



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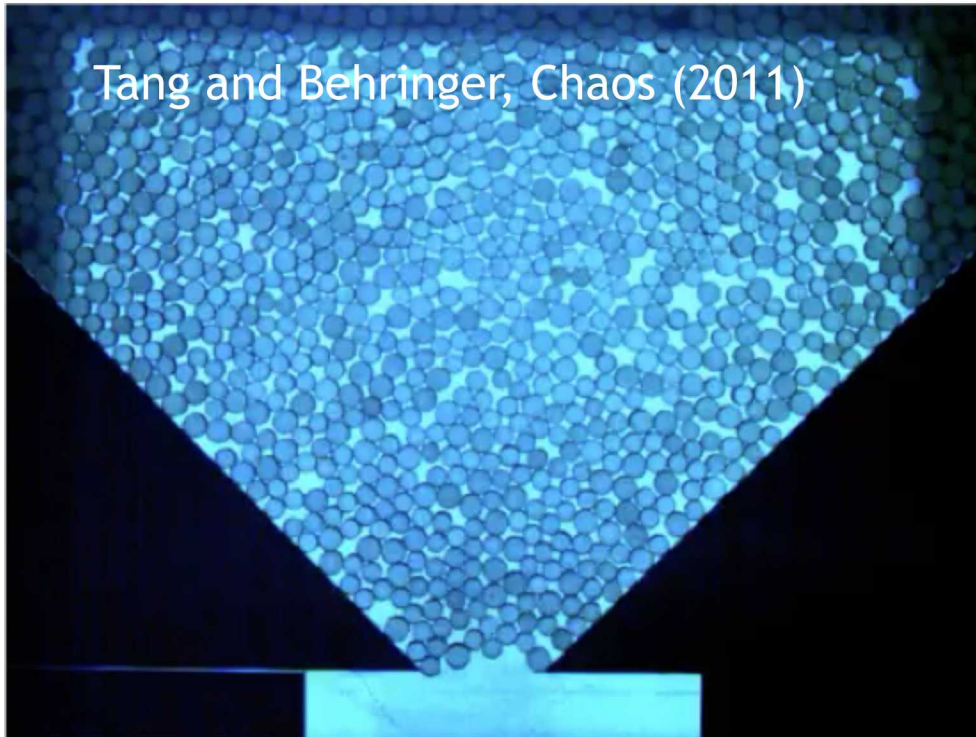
SAND2020-2751C



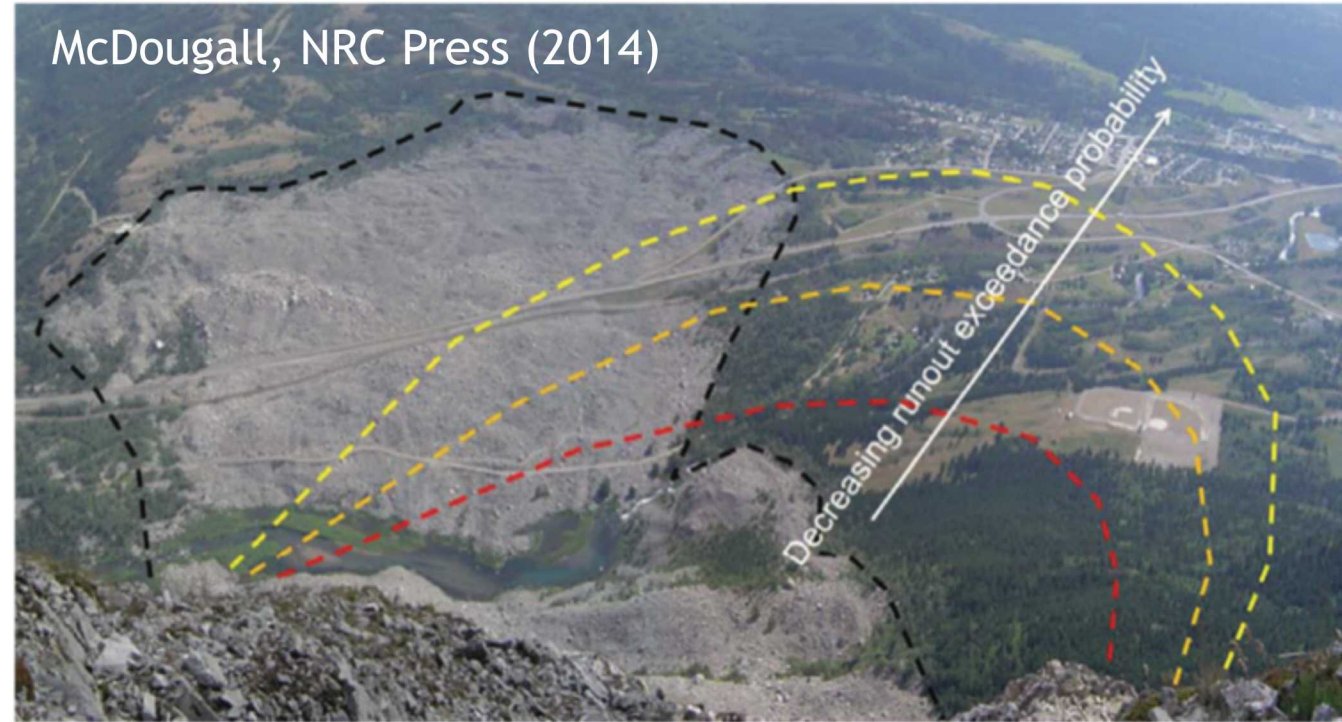
This work was performed, in part, at the Center for Integrated Nanotechnologies, an Office of Science User Facility operated for the U.S. Department of Energy (DOE) Office of Science.

# Flow-Arrest Transition in Granular Materials

clogging in hopper

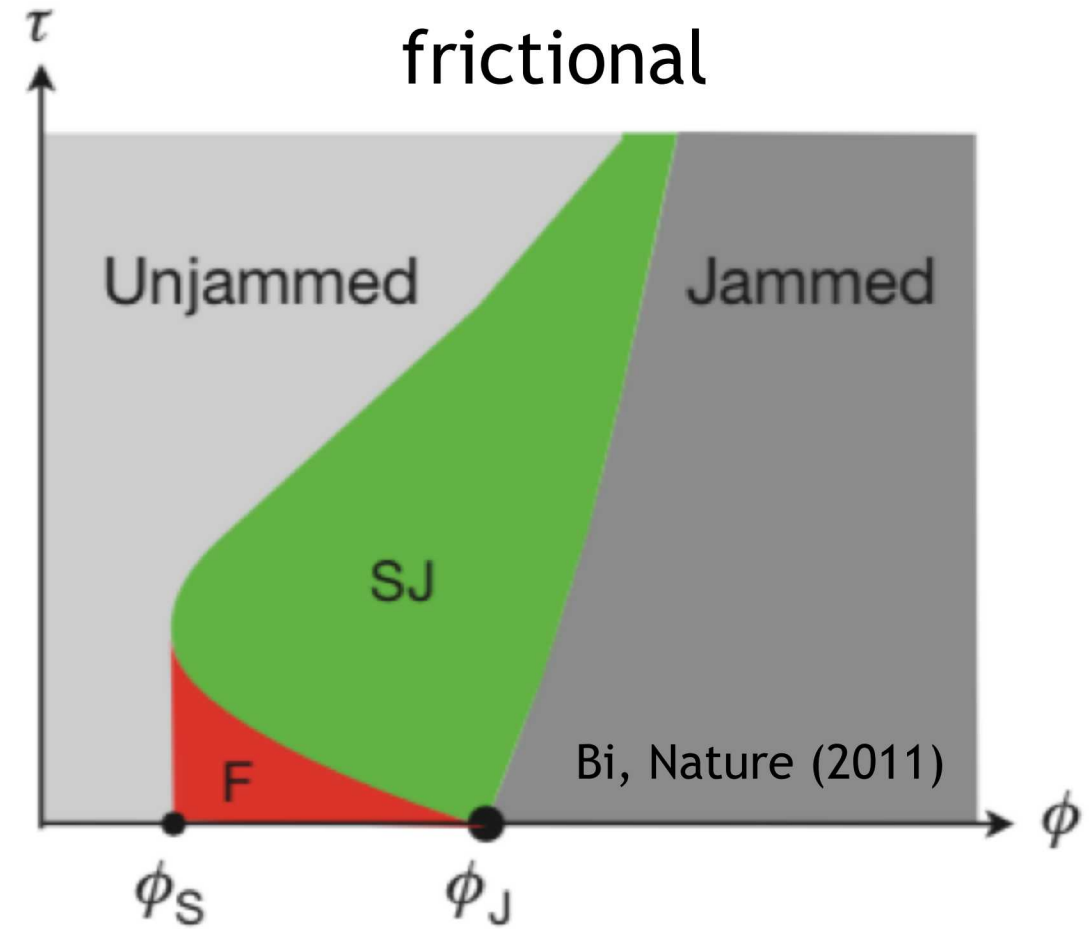
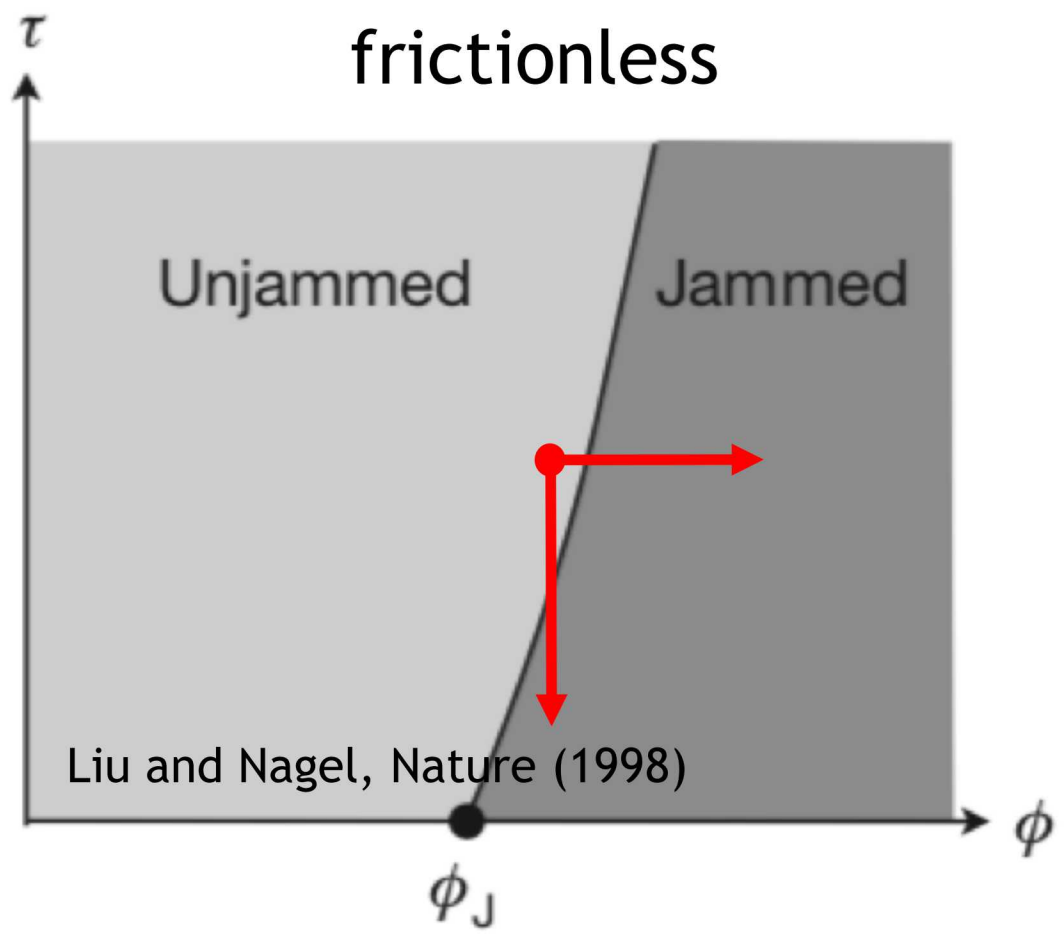


landslide runout probability



1. Will the flow arrest?
2. When will the flow arrest?
3. If it flows, how does it flow?

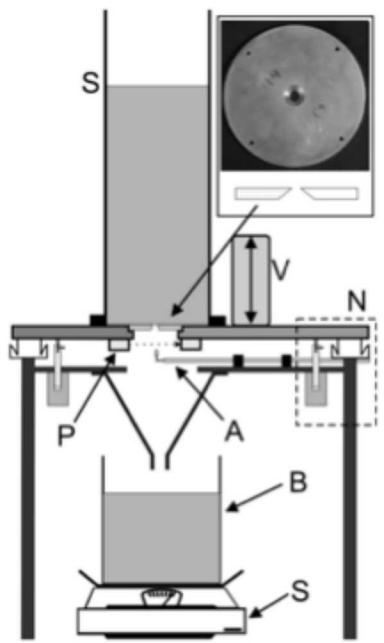
# Will Flowing Granular Material Arrest (Jam)?



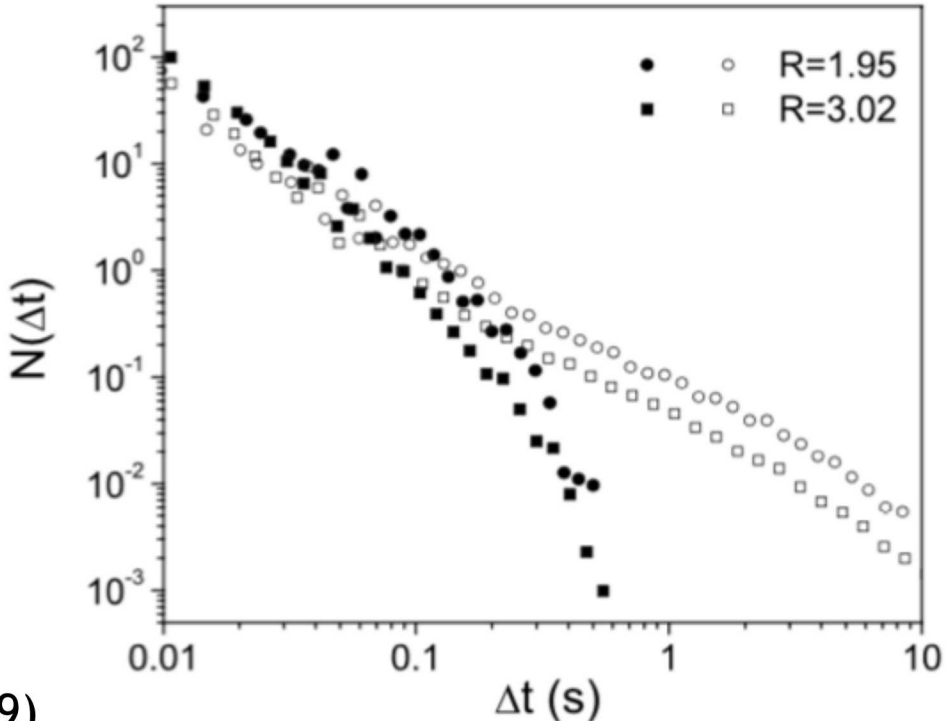
what is the phase diagram under controlled pressure conditions?

# When will Flowing Granular Material Arrest?

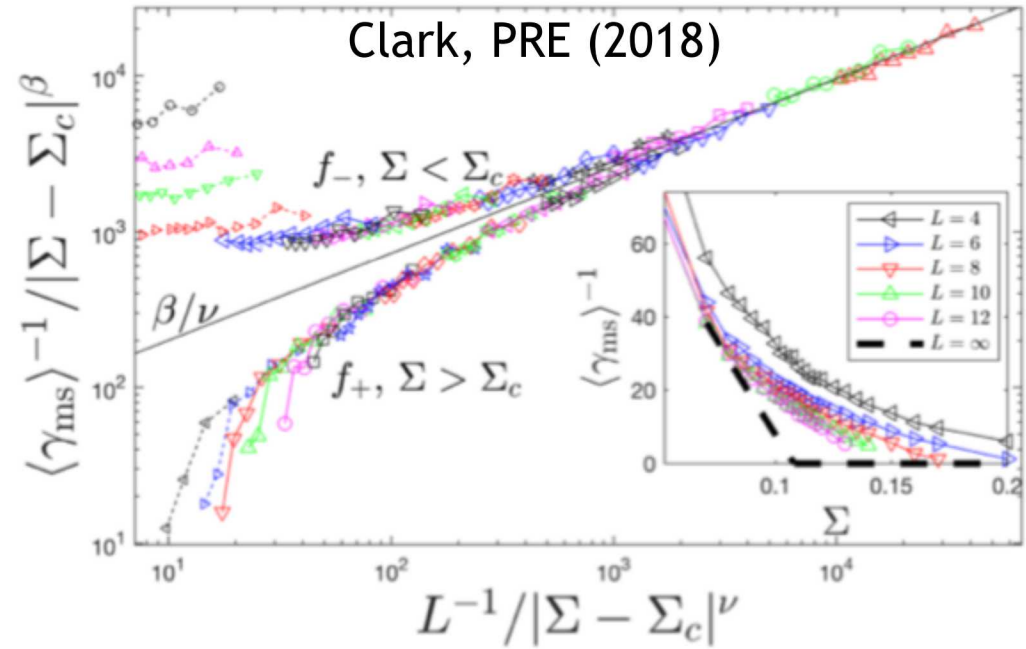
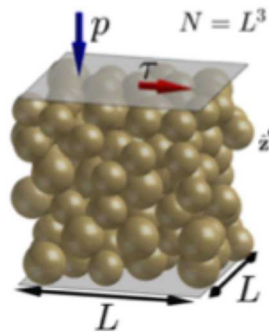
distribution of clog times in silo discharge



Mankoc, PRE (2009)



diverging shear-jamming strain near yield stress



need a better characterization of transients before arrest

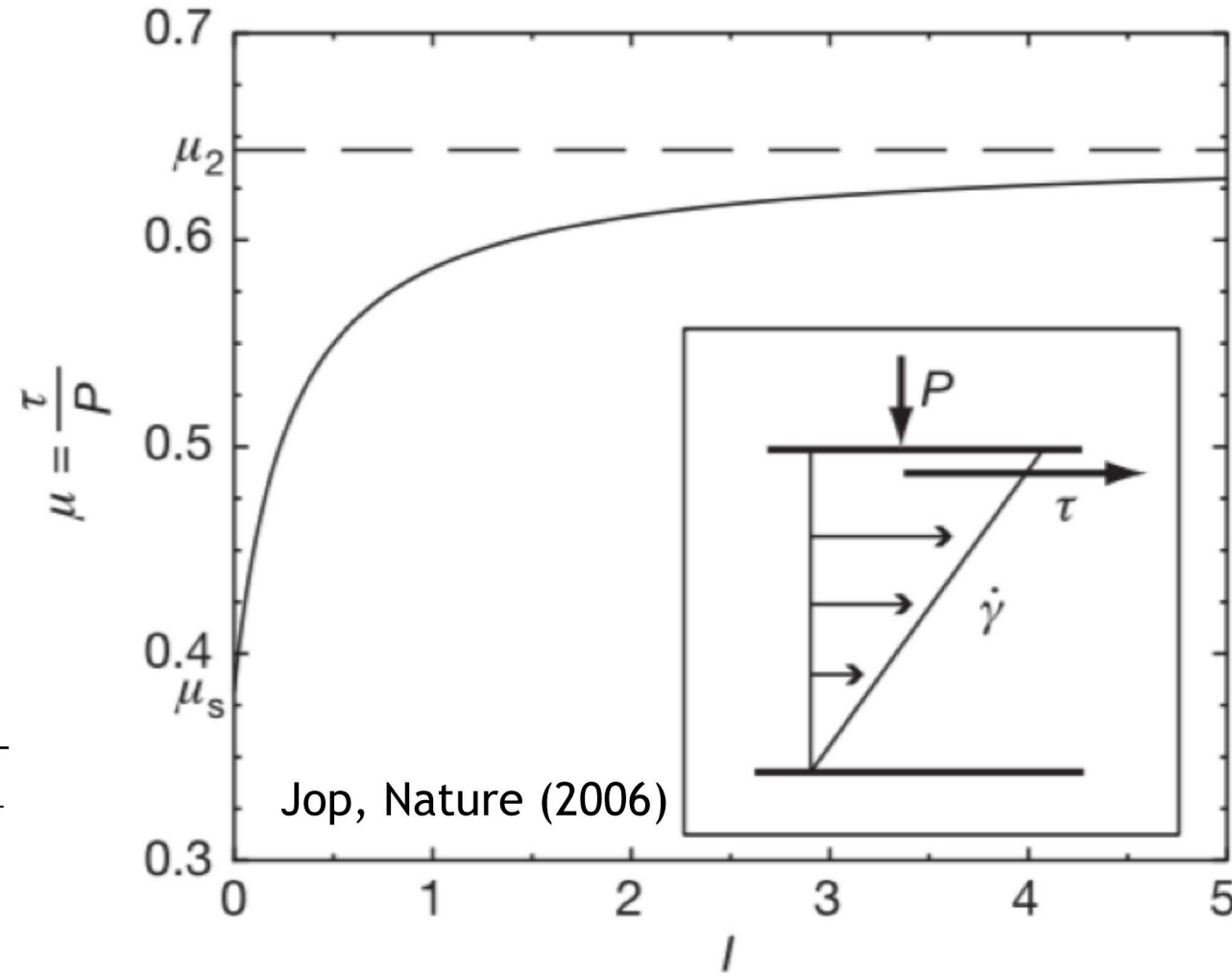
# When it does Flow, how does it Flow? (Rheology)

inertial granular rheology

**inertial Number:**  $I = \dot{\gamma} d \sqrt{\frac{\rho}{P}}$   
(d : diameter  
 $\rho$ : density)

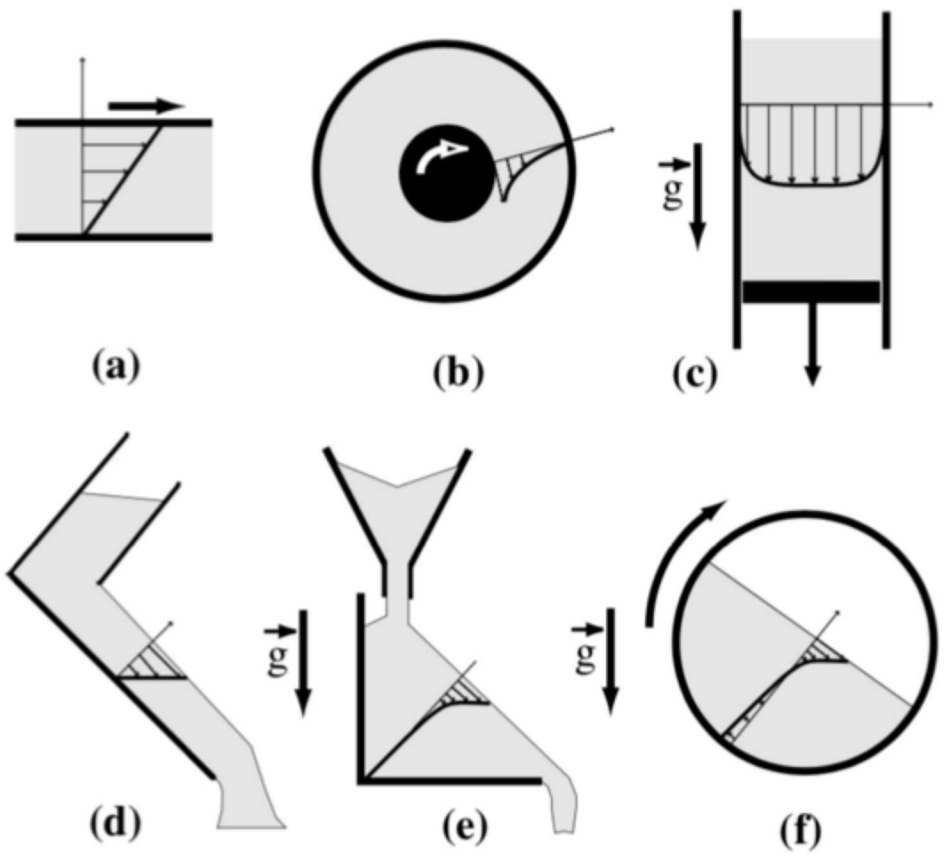
**stress ratio:**  $\mu = \frac{\tau}{P}$

**inertial rheology:**  $\mu(I) = \mu_s + \frac{\mu_s - \mu_s}{I_0/I + 1}$   
(monotonic, yield  
criterion)

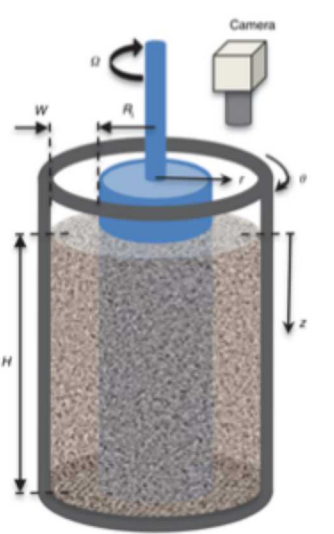


assumes co-directionality of stress and strain rate

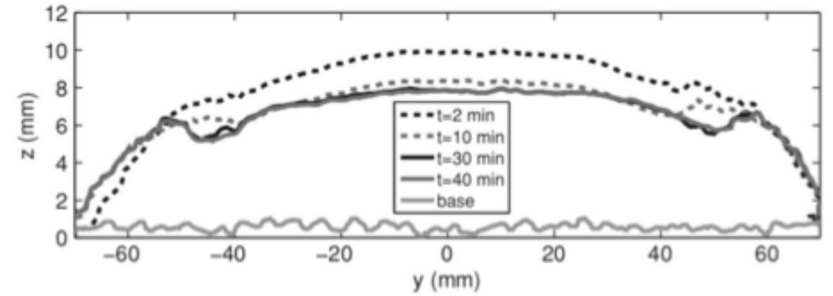
# Features of 3D Granular Flows



GDR MiDi, EPJ (2004)

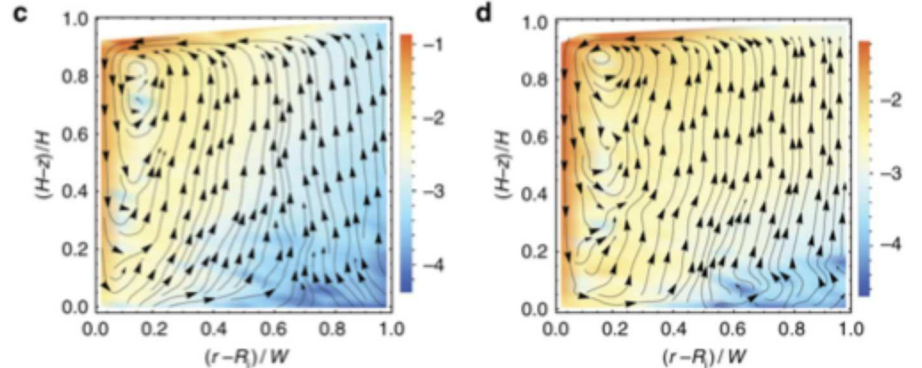


free surface flows



Takagi, PRE (2011)

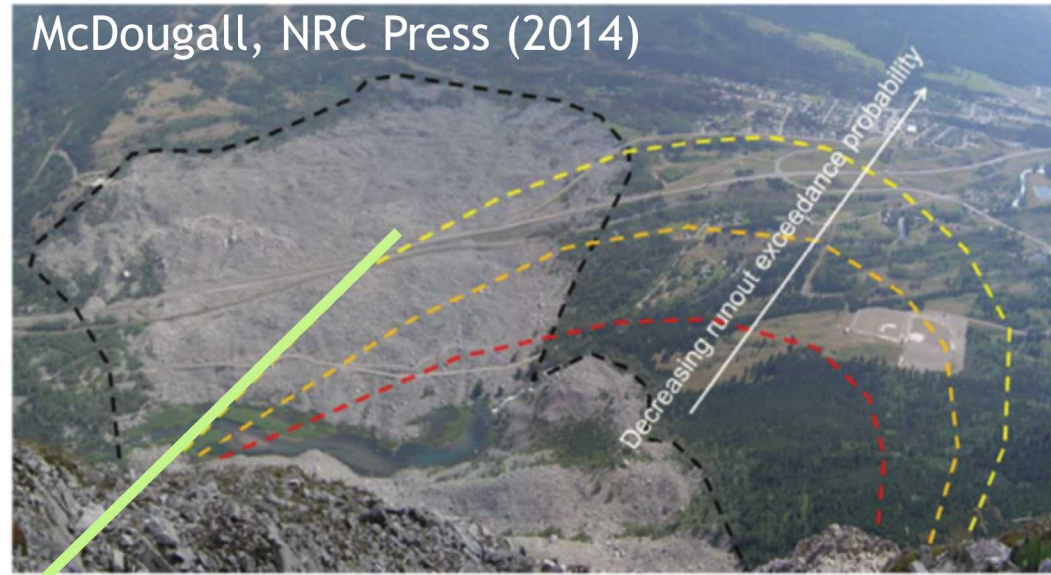
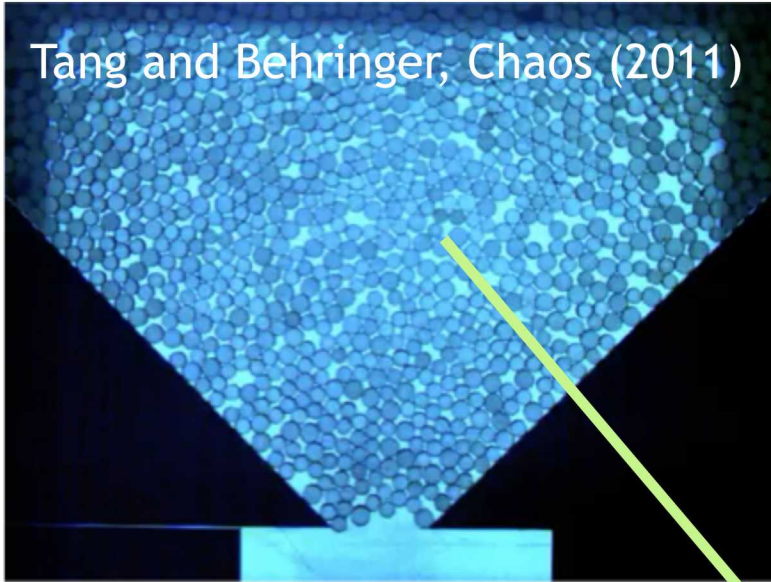
dilation driven vortex flows



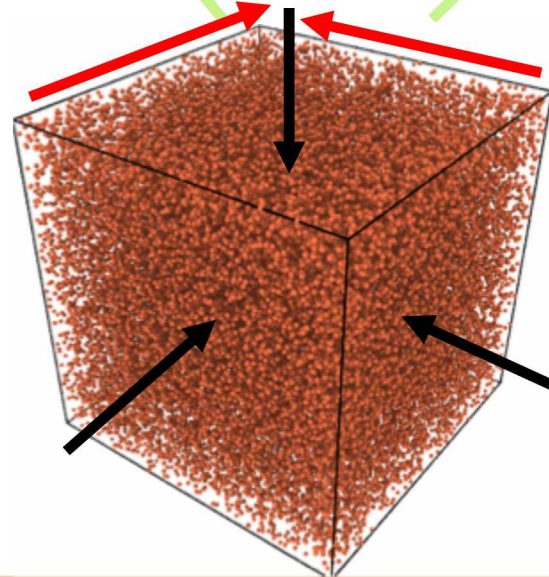
Krishnaraj, Nat. Comm. (2016)

$\mu(I)$  rheology does not completely characterize 3D granular flows

# Flow-Arrest Transition: Problem Statement



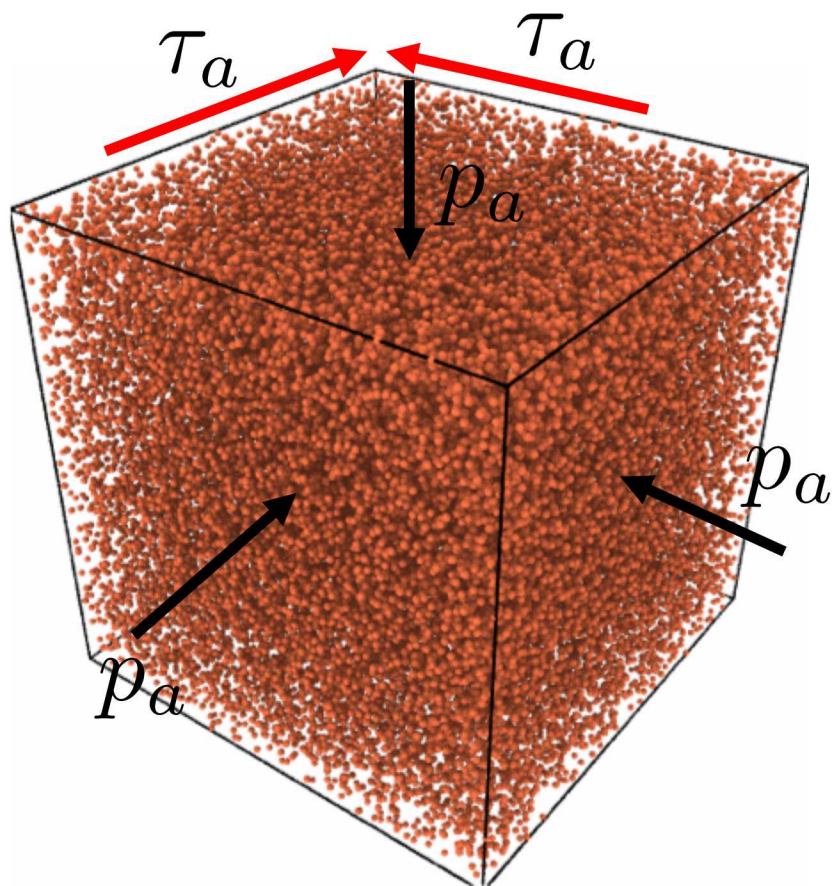
representative  
volume element  
under shear &  
pressure



under prescribed shear and pressure:

1. Will the flow arrest?
2. When will the flow arrest?
3. If it flows, how does it flow?

# DEM Simulation Protocol



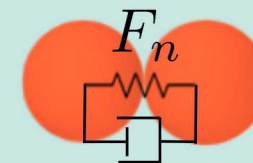
$$\boldsymbol{\sigma}_a = p_a \mathbf{I} + \begin{bmatrix} 0 & \tau_a & 0 \\ \tau_a & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix}$$

Parinello-Rahman dynamics  
(isenthalpic-isotension ensemble in MD)

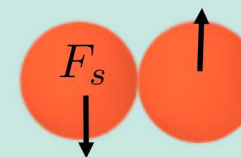
- fully periodic: **no boundary effects**
- uniform surface traction
- homogenous deformation/flow
- no shear bands

## contact mechanics

### Hookean contacts

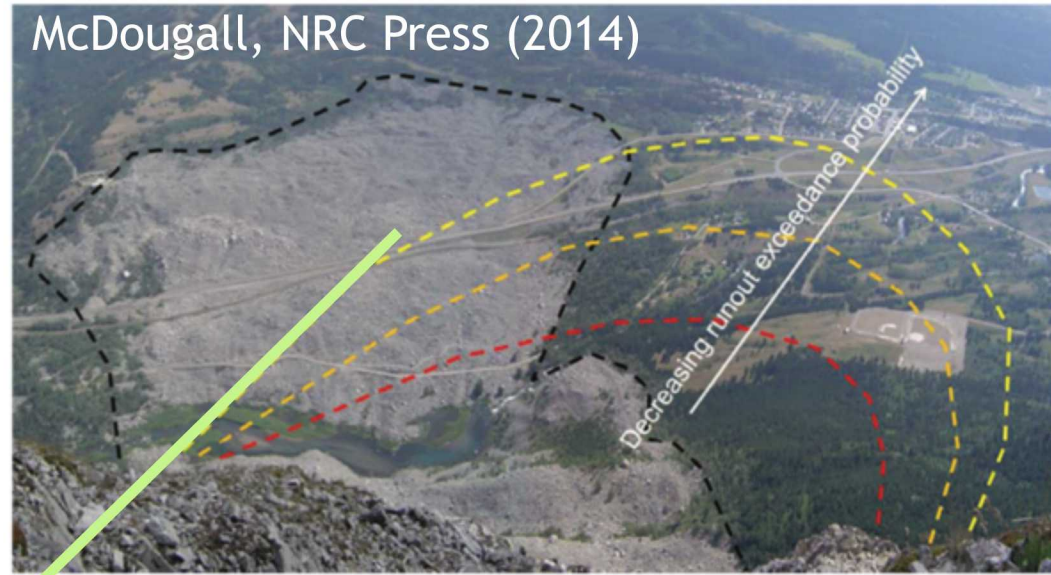
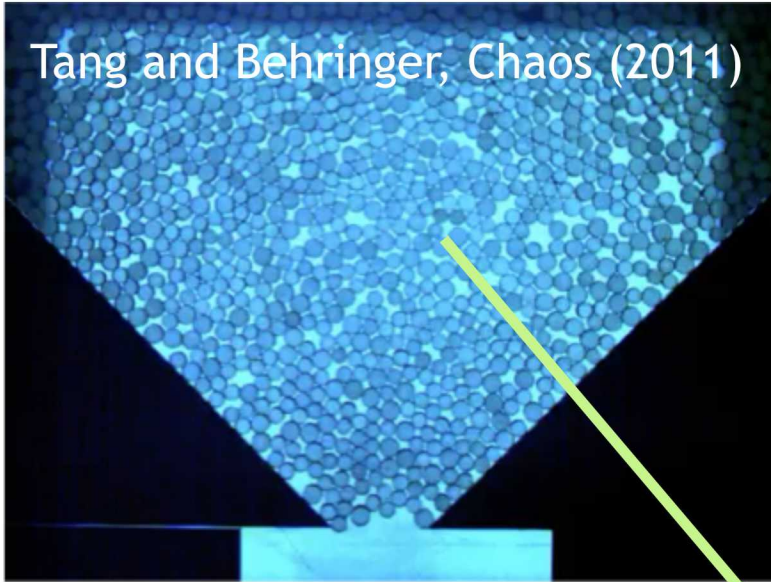


### Coulomb surface friction

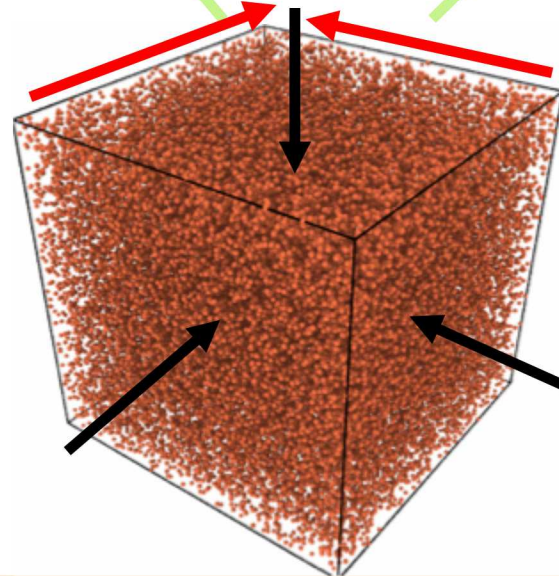


$$\|F_s\| < \mu_s \|F_n\|$$

# Flow-Arrest Transition: Problem Statement



representative  
volume element  
under shear &  
pressure

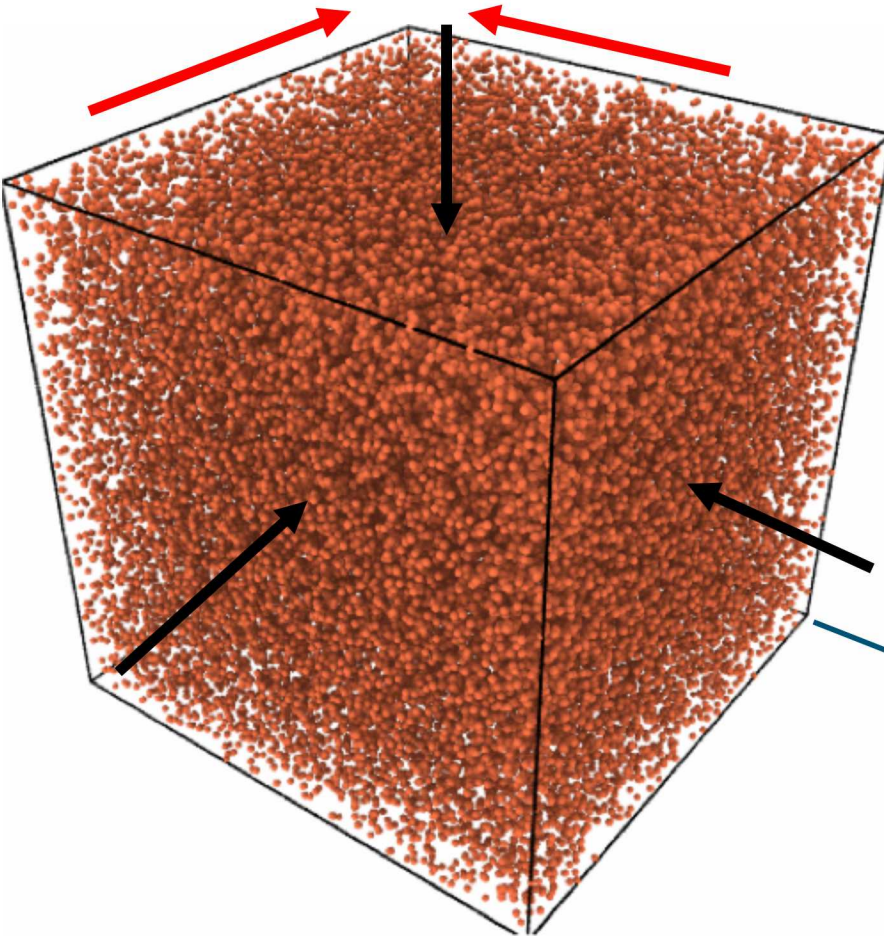


under prescribed shear and pressure:

1. Will the flow arrest?
2. When will the flow arrest?
3. If it flows, how does it flow?

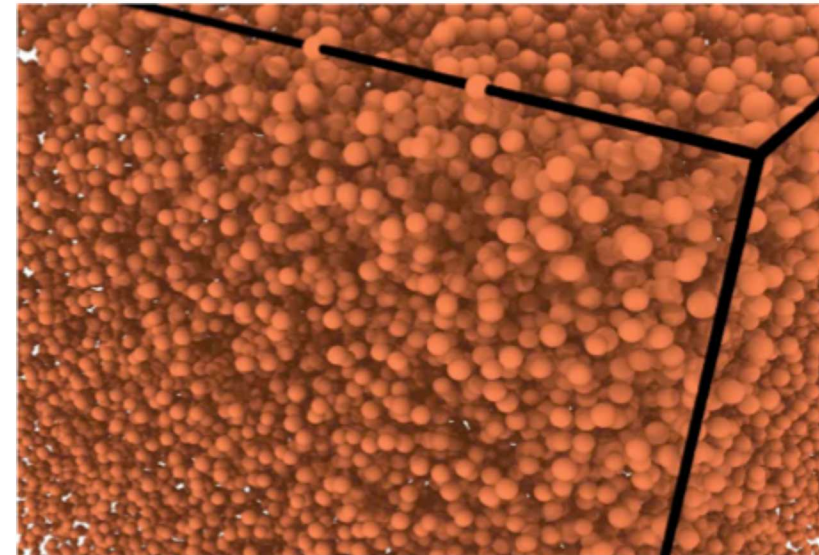
# Granular Flow vs. Arrest

initial dilute system:  $\phi = 0.05$

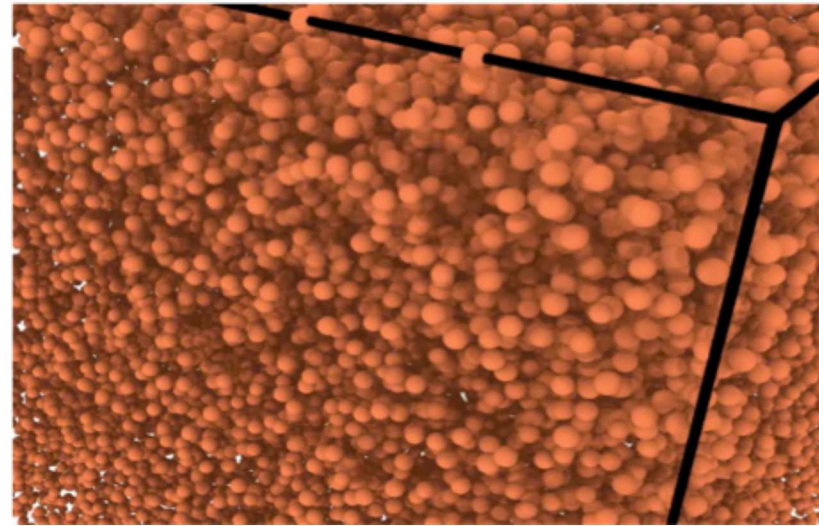


$$\sigma_a = p_a \mathbf{I} + \begin{bmatrix} 0 & \tau_a & 0 \\ \tau_a & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix}$$

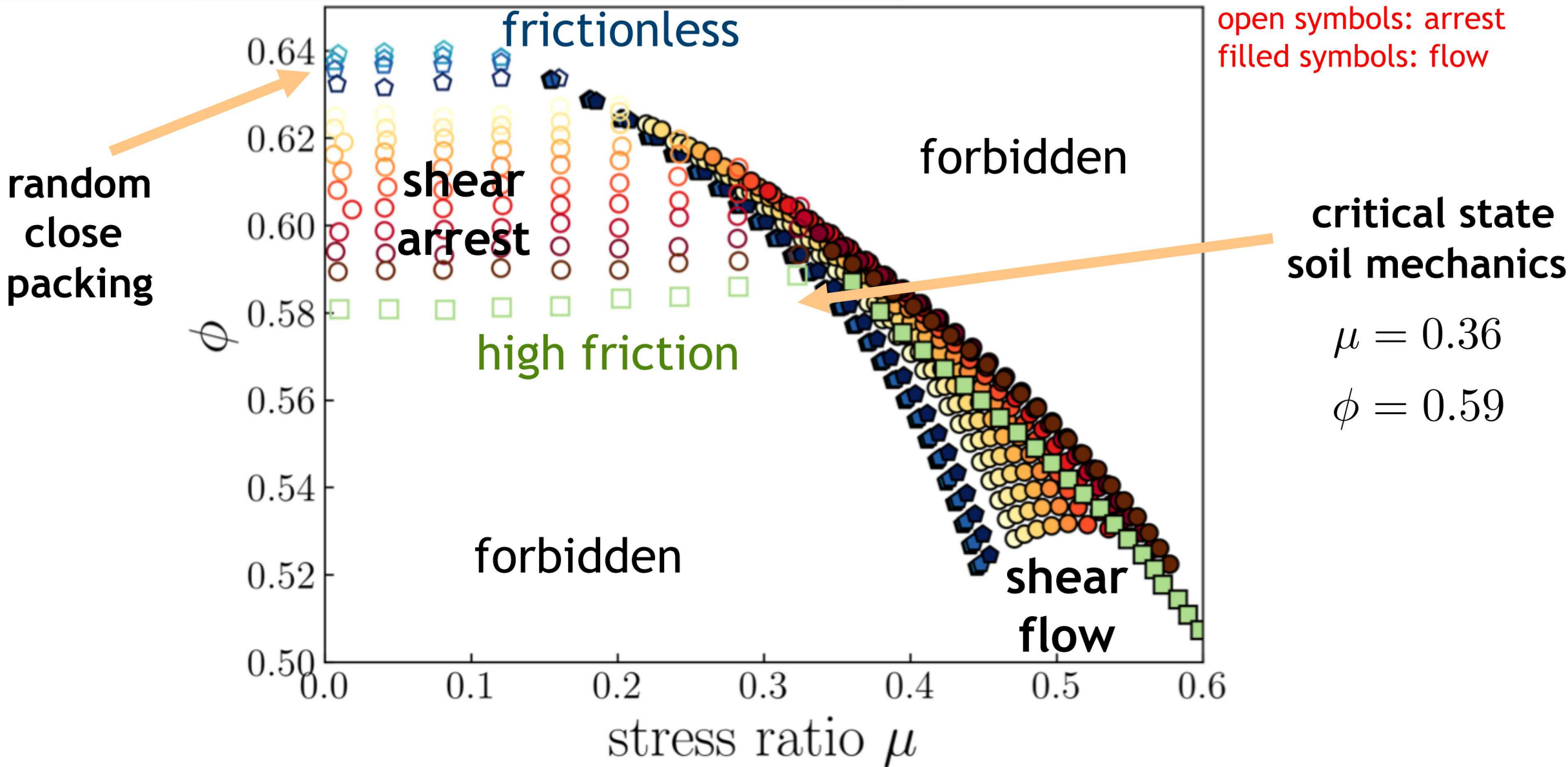
steady flow



shear arrest



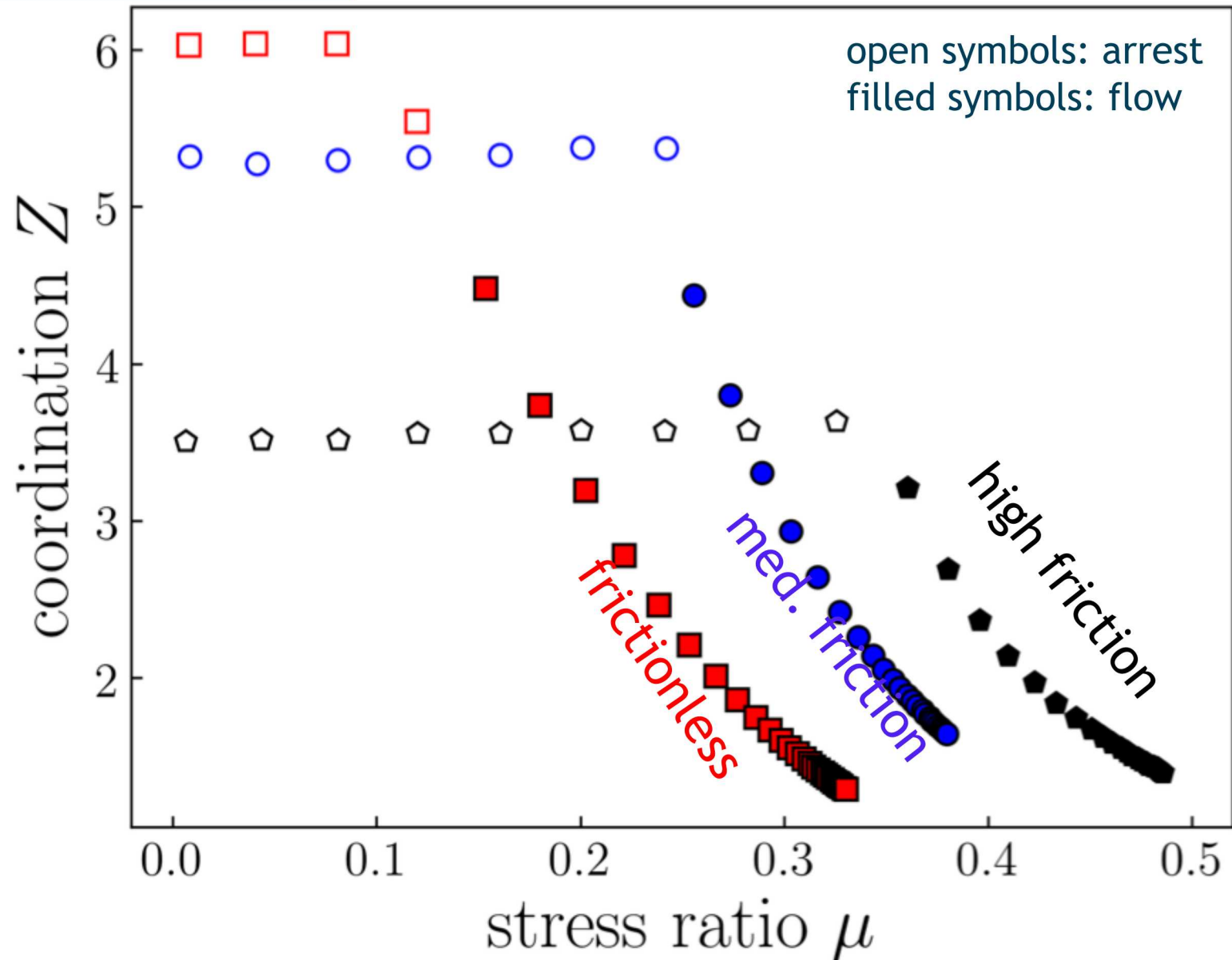
# Flow-Arrest Phase Diagram



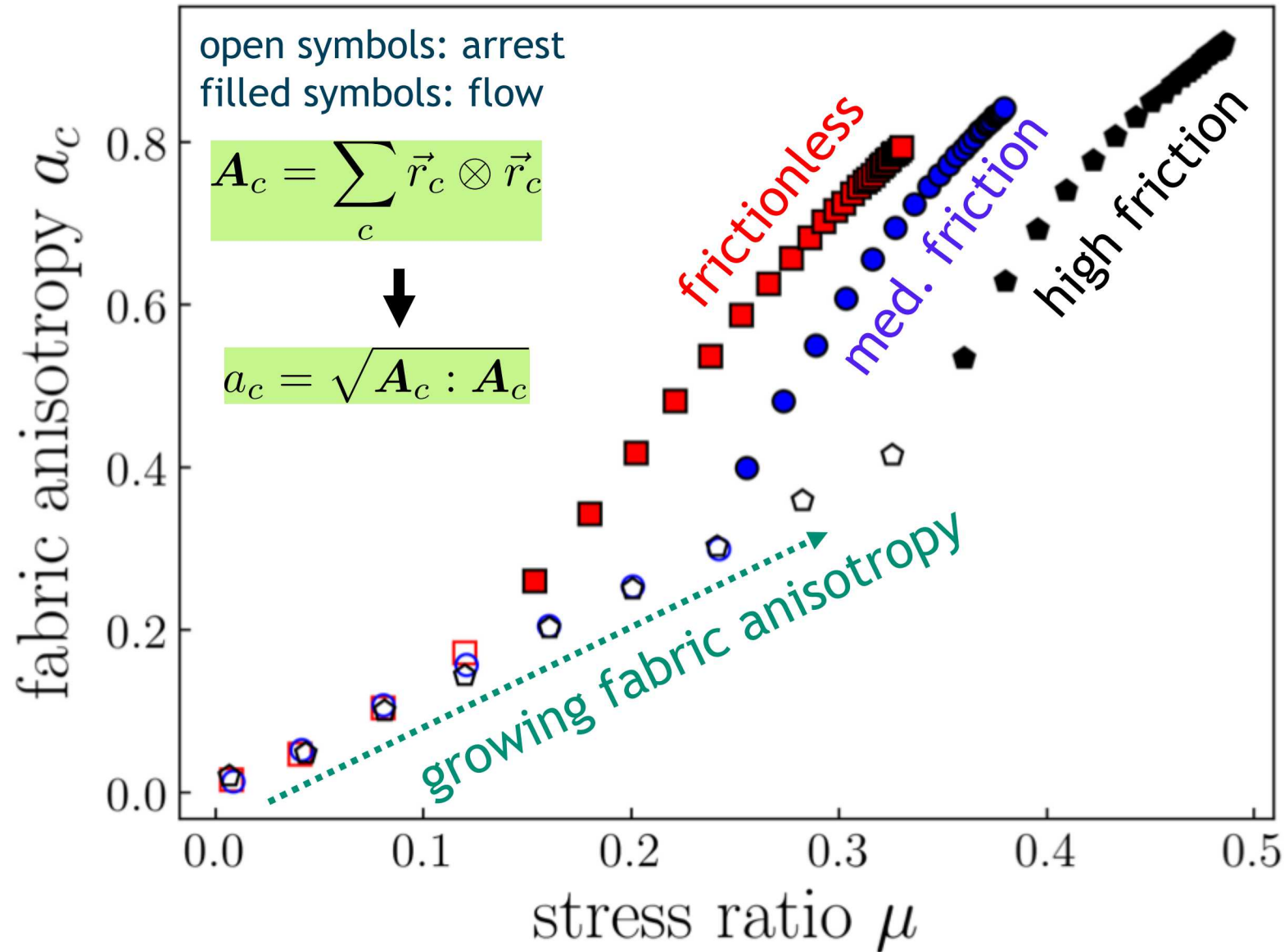
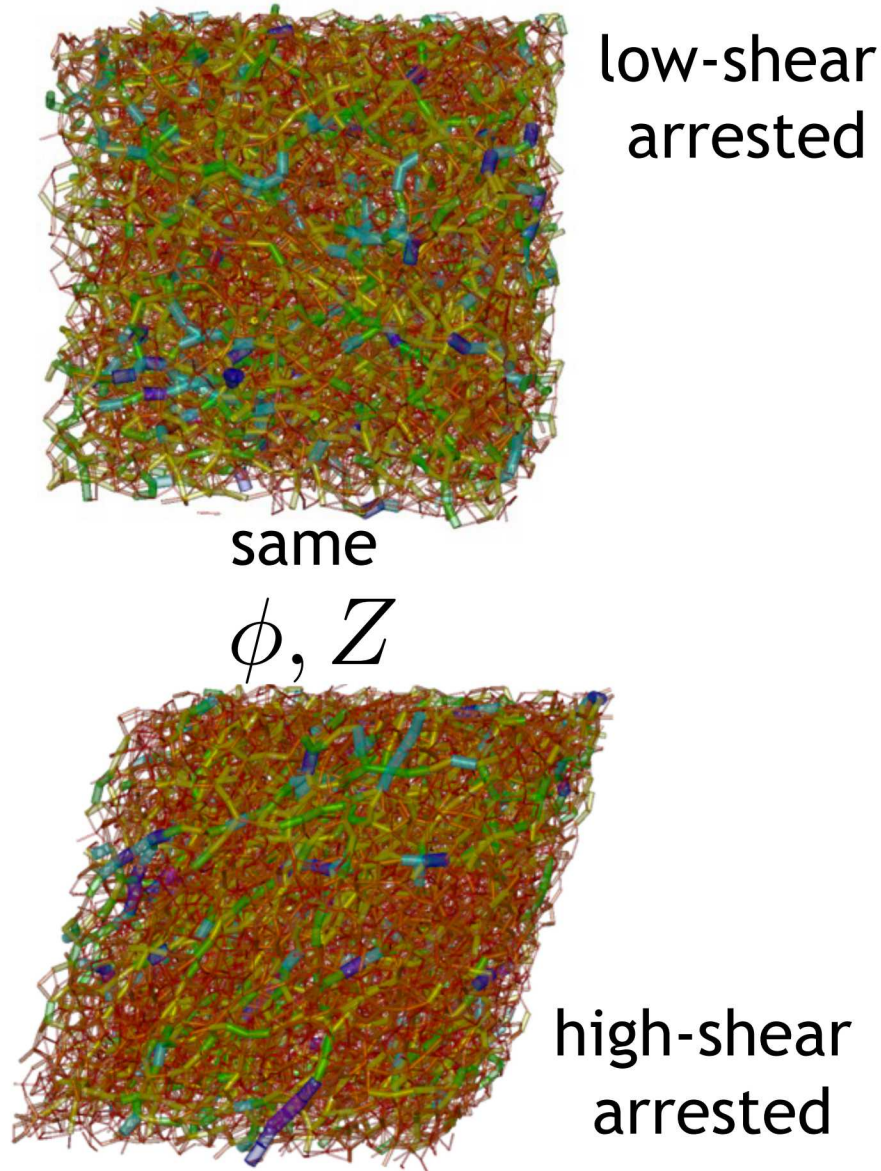
# Coordination at Flow-Arrest Transition

well-defined  
coordination at arrest  
for every friction

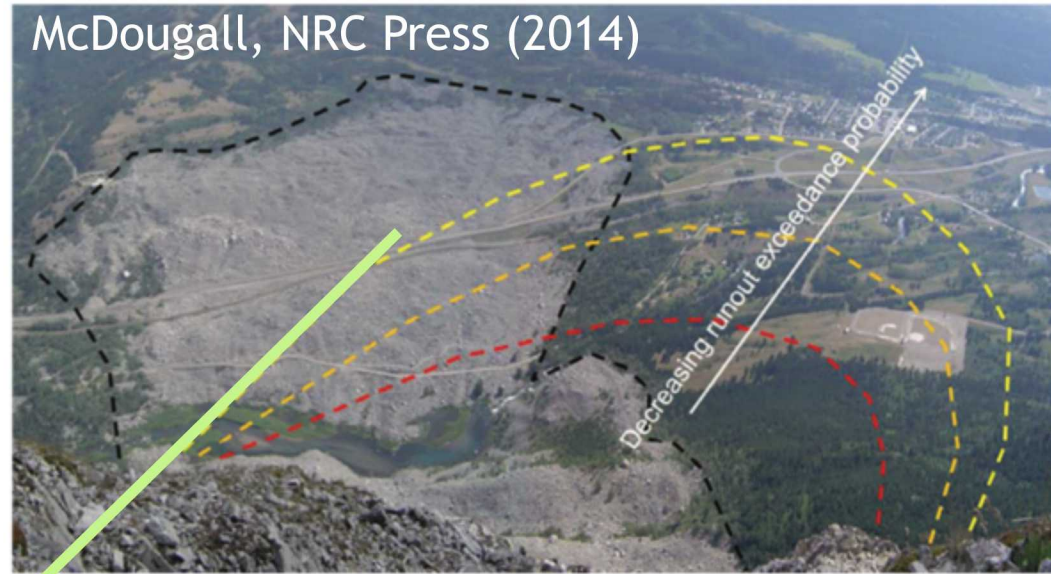
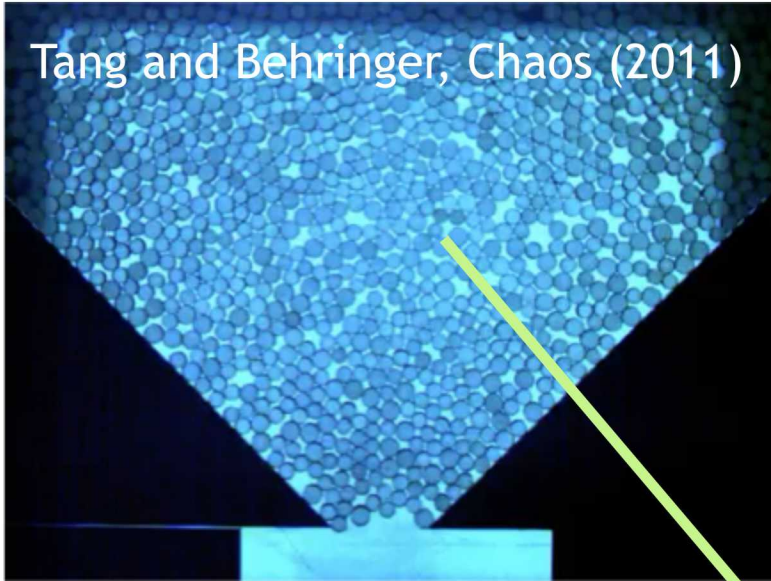
low coordination  
for high shear flows



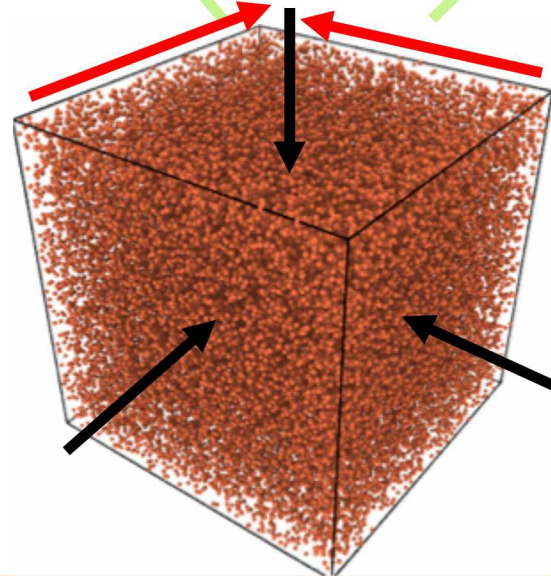
# Granular Fabric at Flow-Arrest: Stress-Dependent



# Flow-Arrest Transition: Problem Statement



representative  
volume element  
under shear &  
pressure

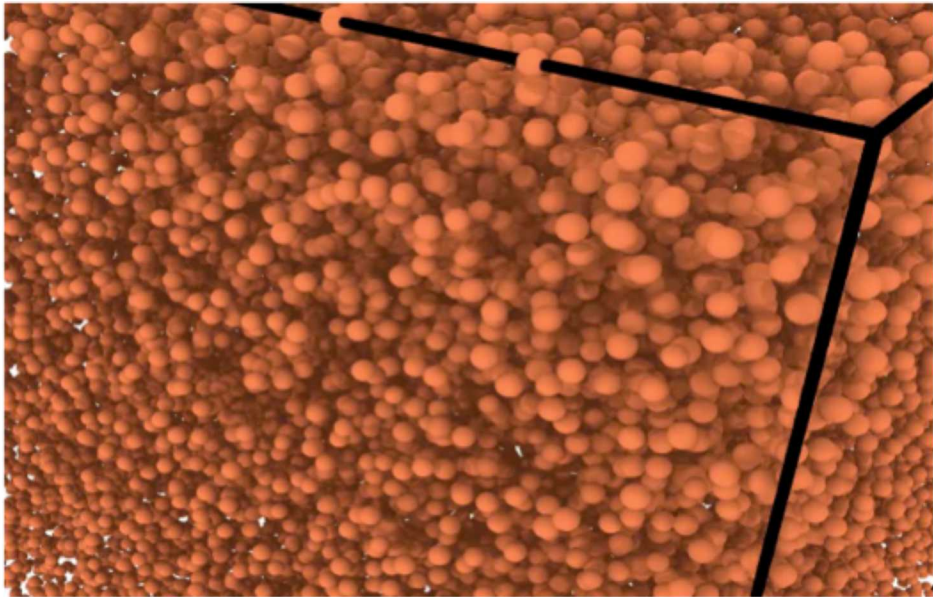


under prescribed shear and pressure:

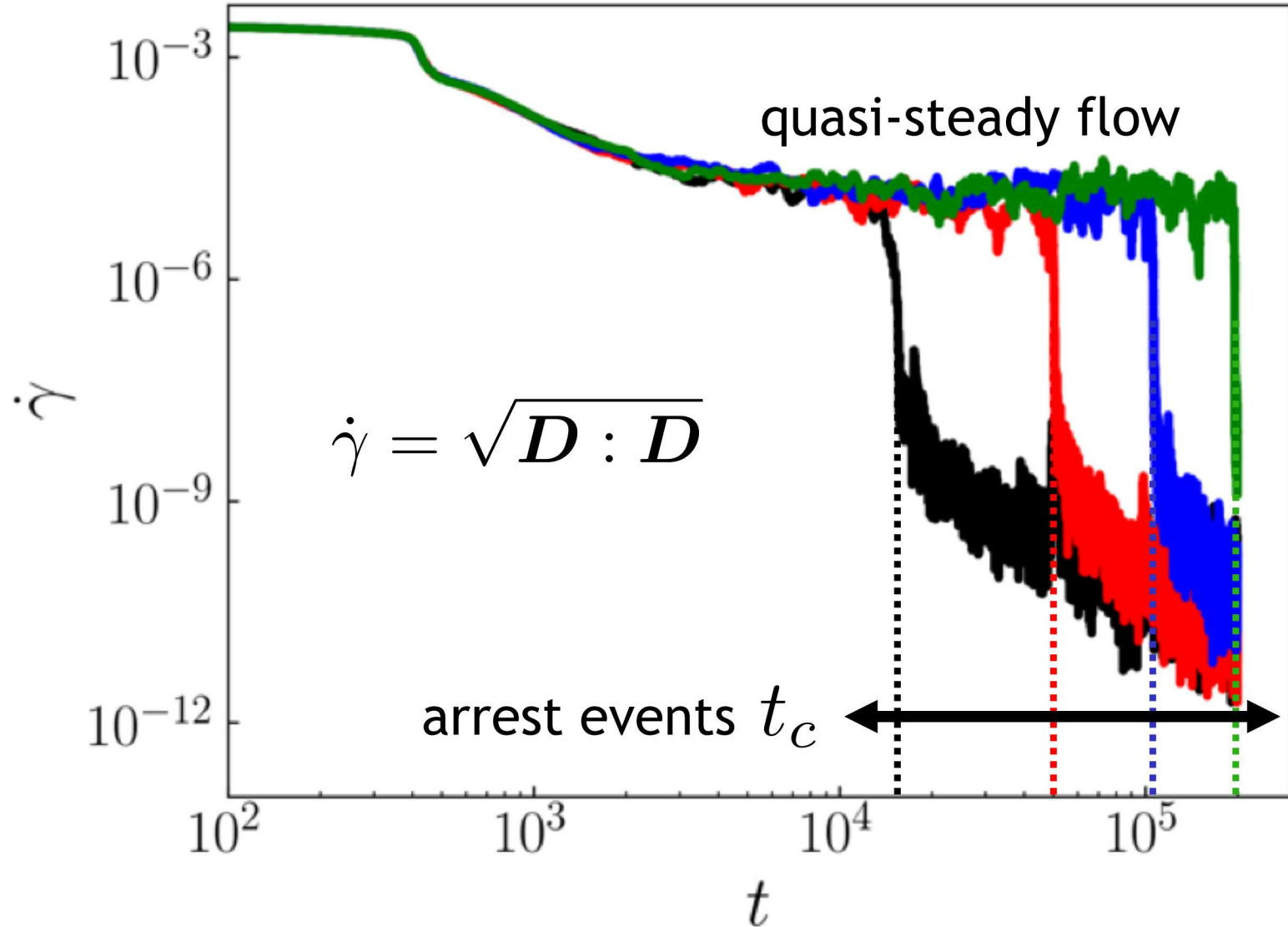
1. Will the flow arrest?
2. When will the flow arrest?
3. If it flows, how does it flow?

# Time to Arrest is Stochastic

shear arrest



four random cases, same stress

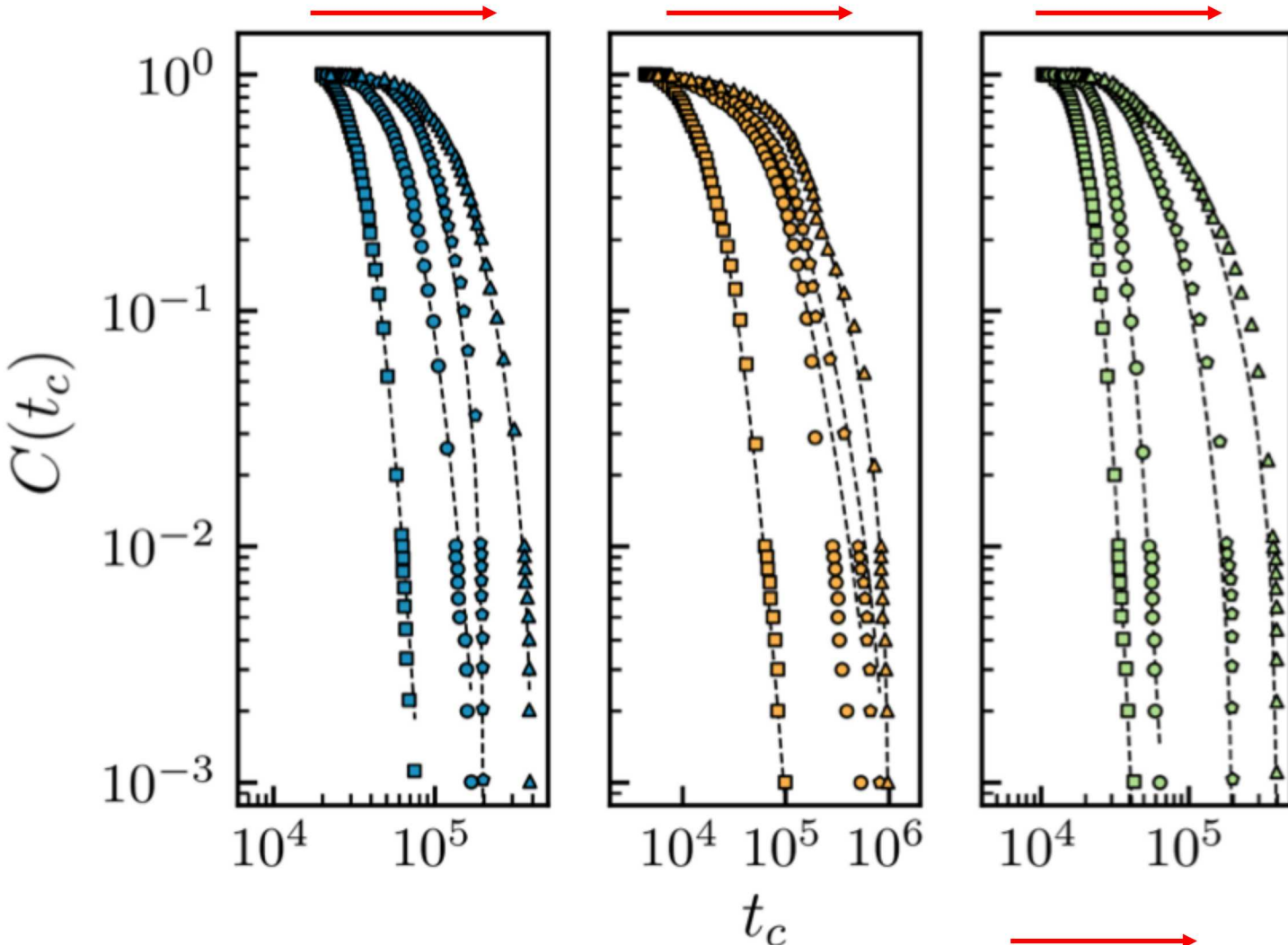


# Time to Arrest: Long-tailed Distributions

long-tailed *log-normal* distribution of arrest times

longer tails at higher stress ratio

frictionless    med. friction    high friction



arrest times:

complementary cumulative distribution

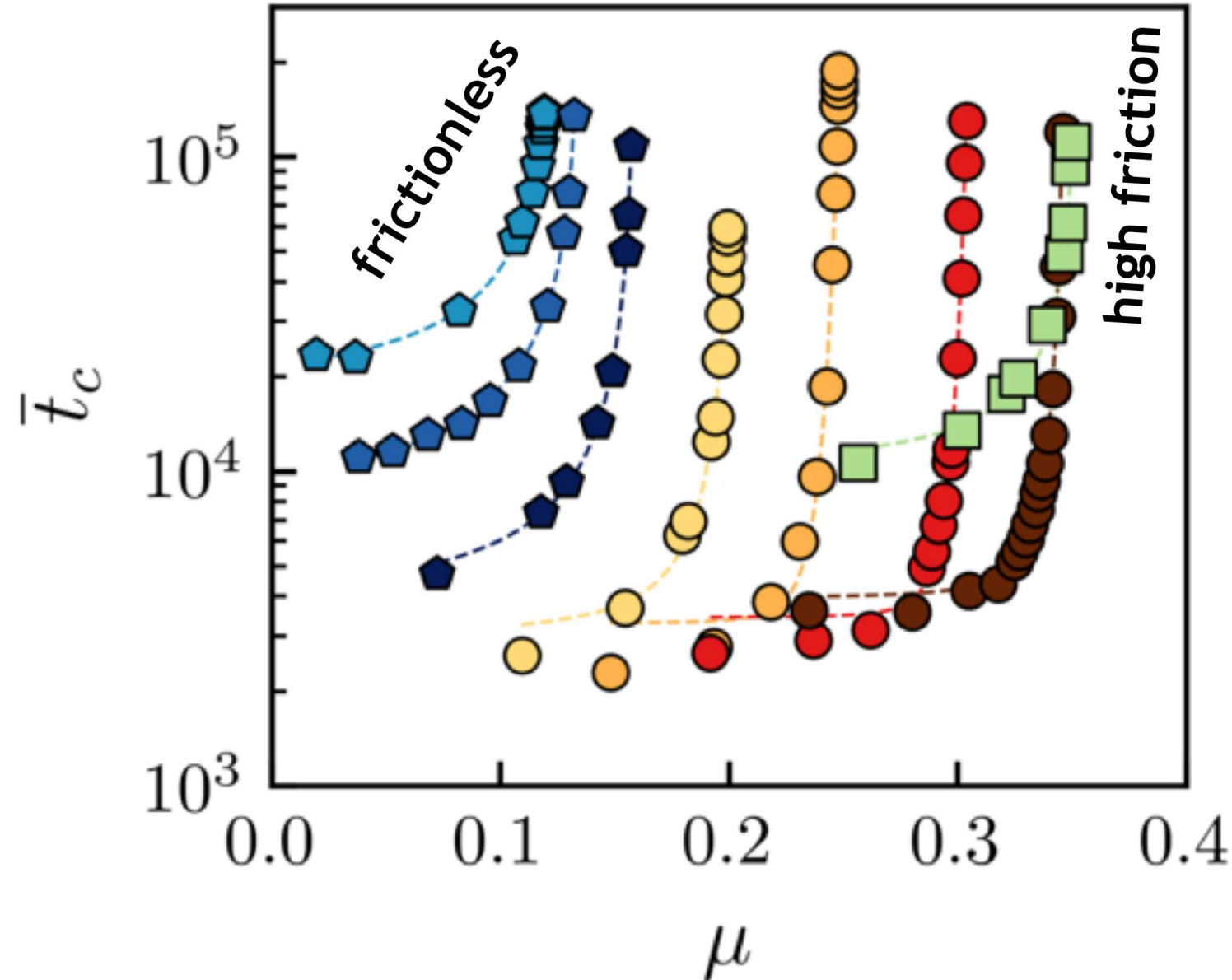
increasing stress ratio  $\mu$

# Divergence of Mean Arrest Times

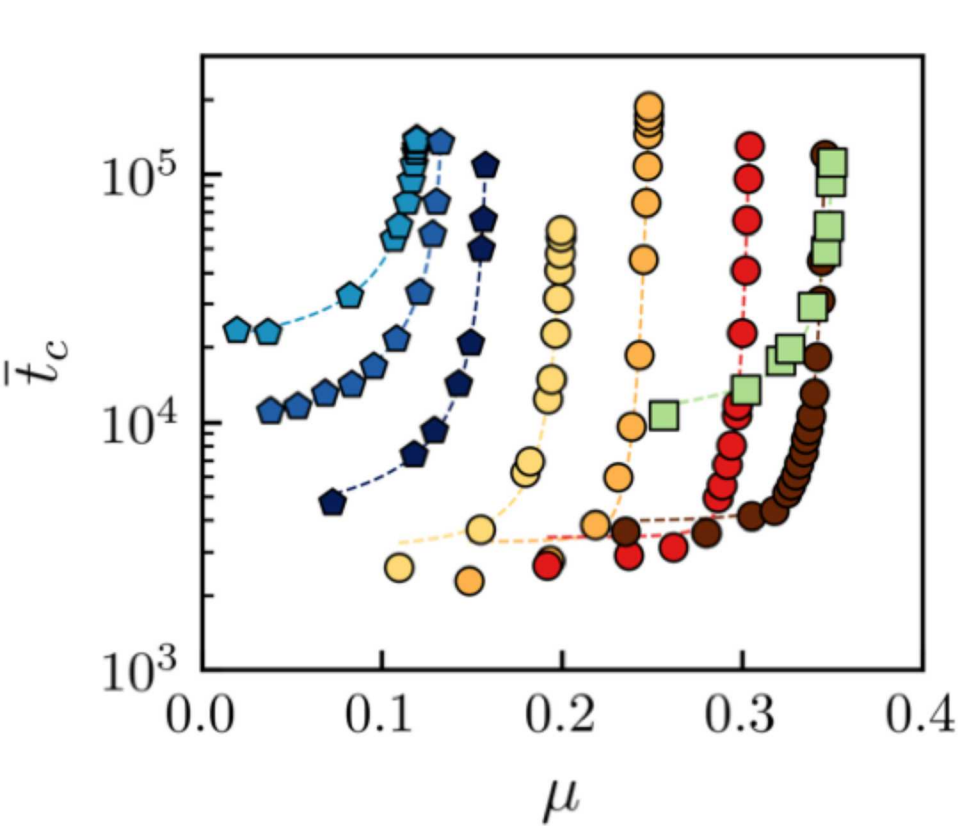
$$\bar{t}_c \sim (\mu_c - \mu)^\alpha$$

power-law divergence of mean arrest times at a critical stress ratio

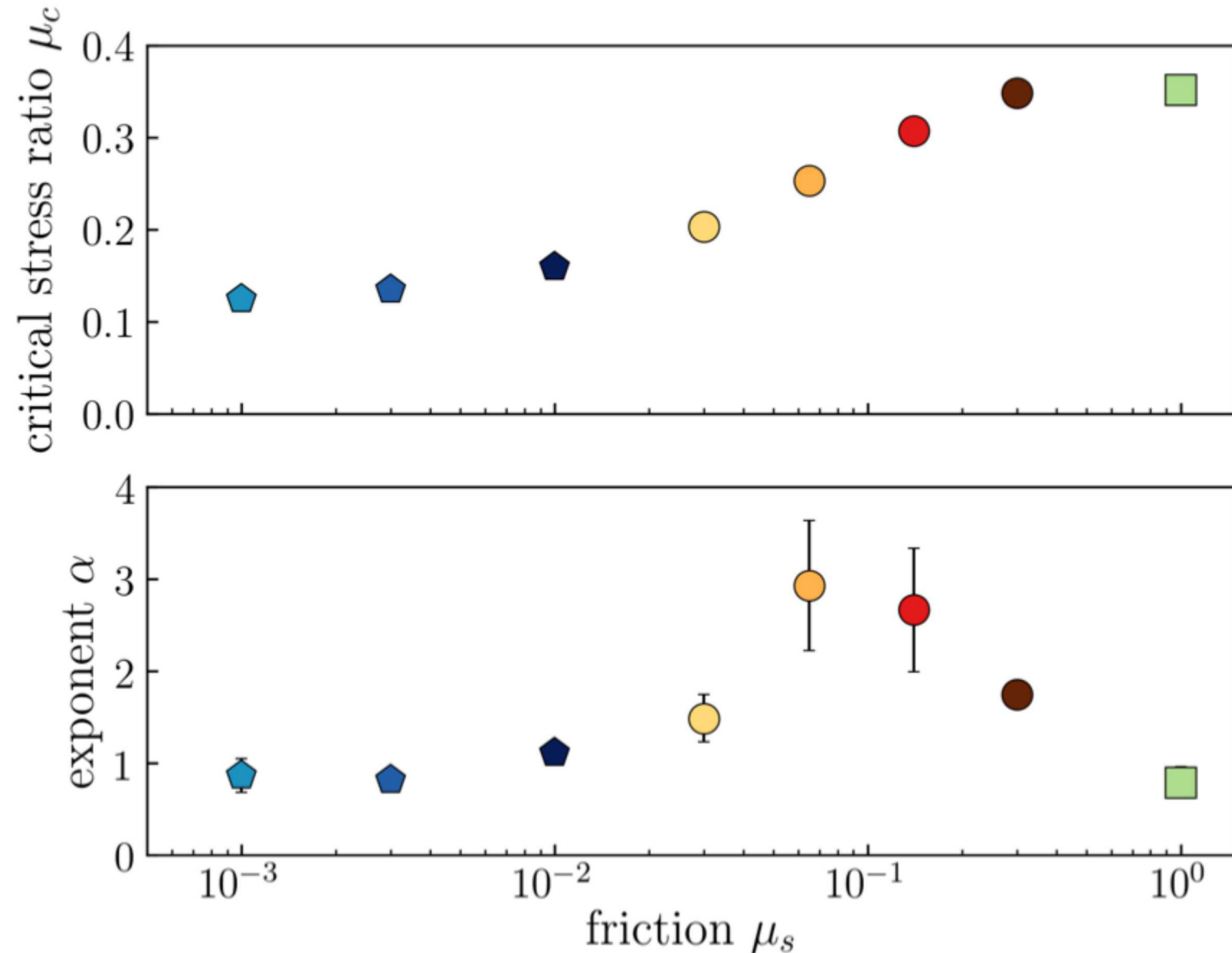
averaged over  $10^3$  simulations  
per data



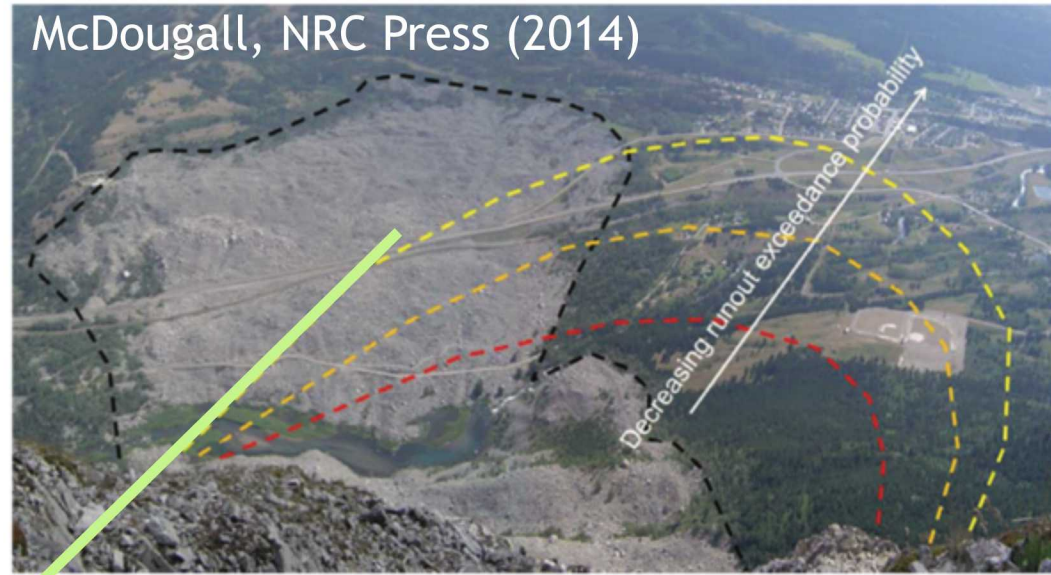
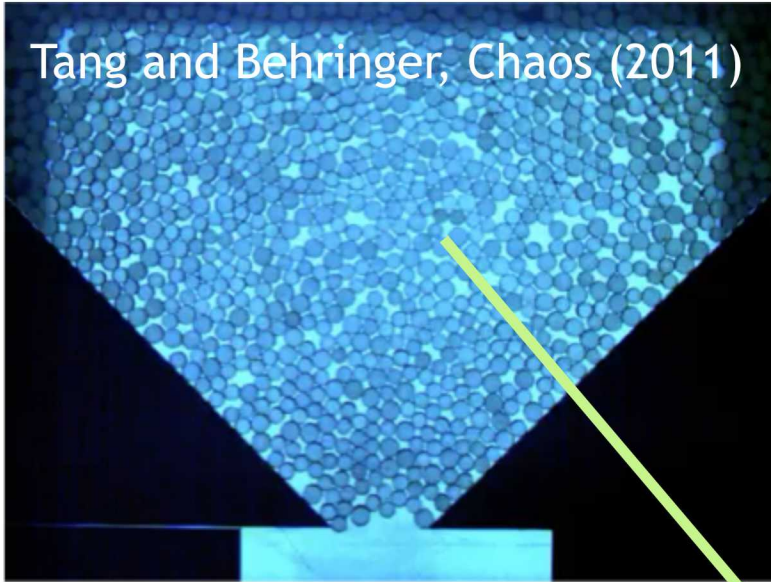
# Power-law Divergence: Critical Exponents



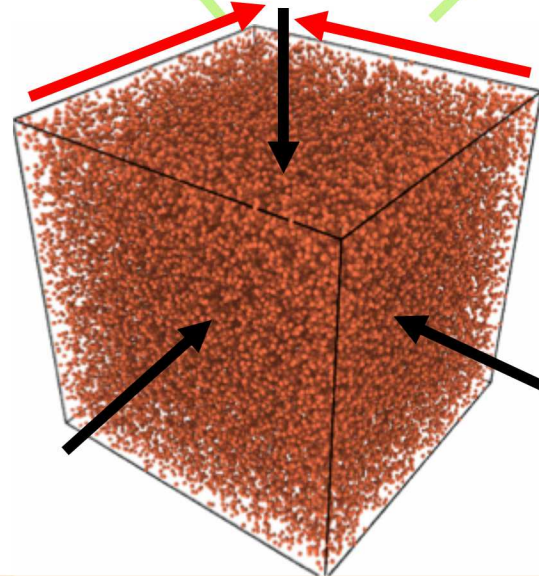
$$\bar{t}_c \sim (\mu_c - \mu)^\alpha$$



# Flow-Arrest Transition: Problem Statement



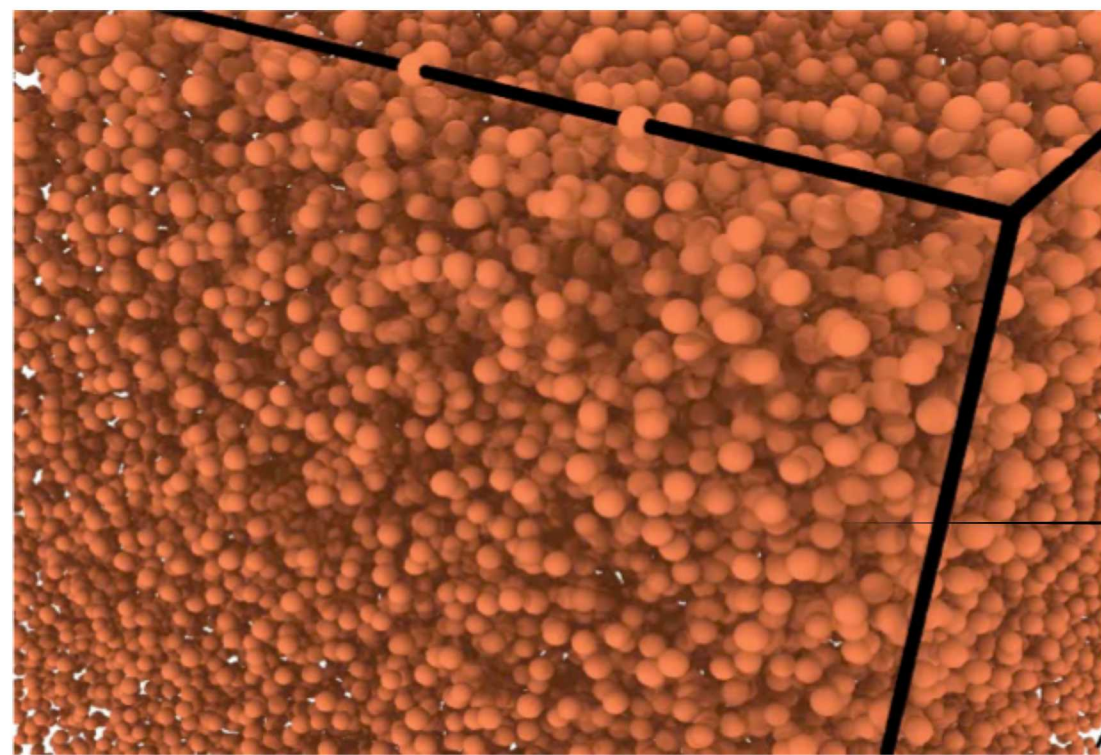
representative  
volume element  
under shear &  
pressure



under prescribed shear and pressure:

1. Will the flow arrest?
2. When will the flow arrest?
3. If it flows, how does it flow?

# Planar Shear Rheology



after appropriate coordinate transformation

vel. gradient

$$\nabla u = \begin{bmatrix} 0 & \dot{\gamma} & 0 \\ 0 & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix}$$

strain rate

$$D = \begin{bmatrix} 0 & \dot{\gamma}/2 & 0 \\ \dot{\gamma}/2 & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix}$$

spin

$$W = \begin{bmatrix} 0 & \dot{\gamma}/2 & 0 \\ -\dot{\gamma}/2 & 0 & 0 \\ 0 & 0 & 0 \end{bmatrix}$$

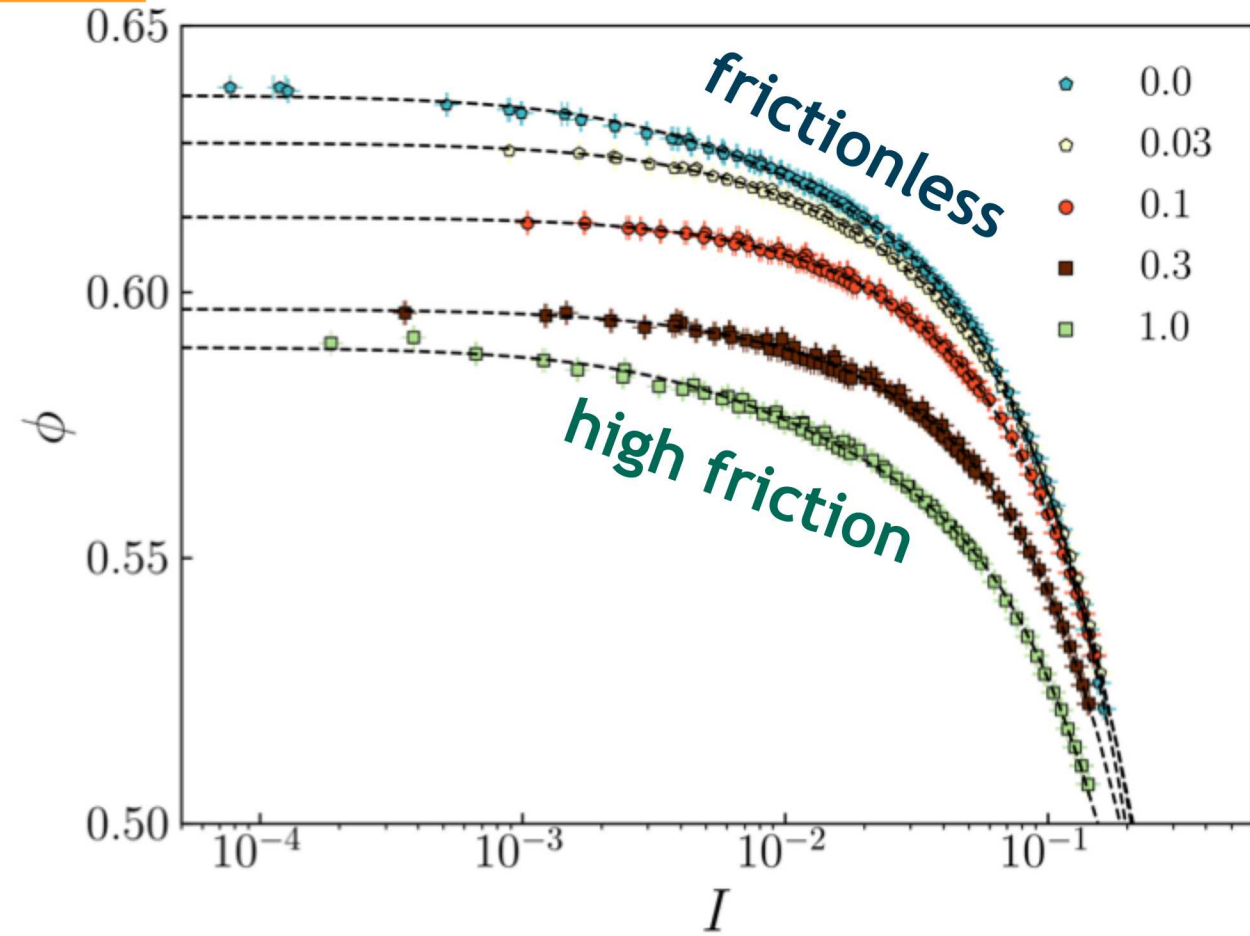
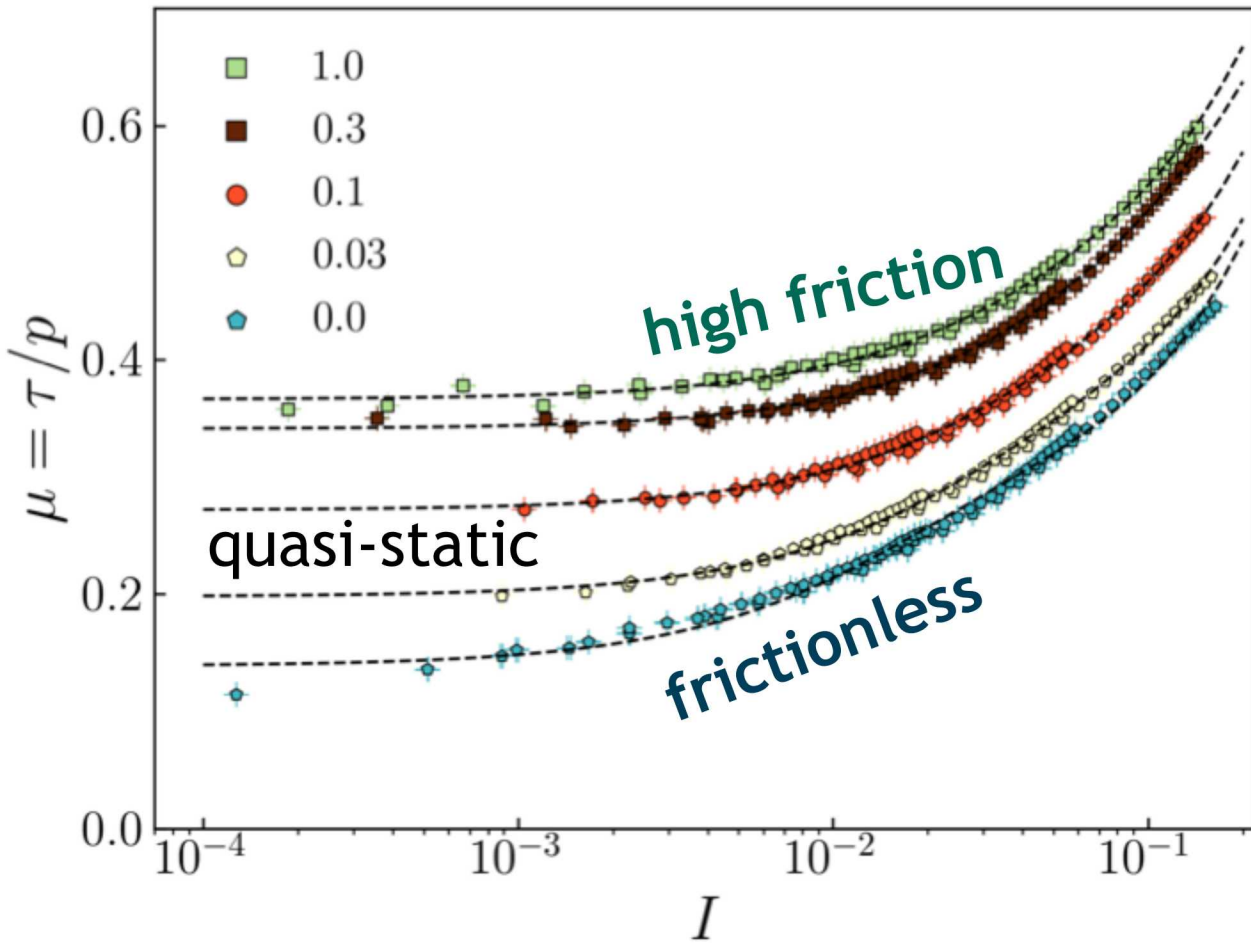
Cauchy stress

$$\sigma = \sum_c \vec{r}_c \otimes \vec{F}_c$$

Rheology:

$$\sigma = \sigma(D)?$$

# Shear $\mu(I)$ and Dilation $\phi(I)$ laws



$$\boldsymbol{\sigma} = -p\mathbf{I} + \boldsymbol{\sigma}_D$$

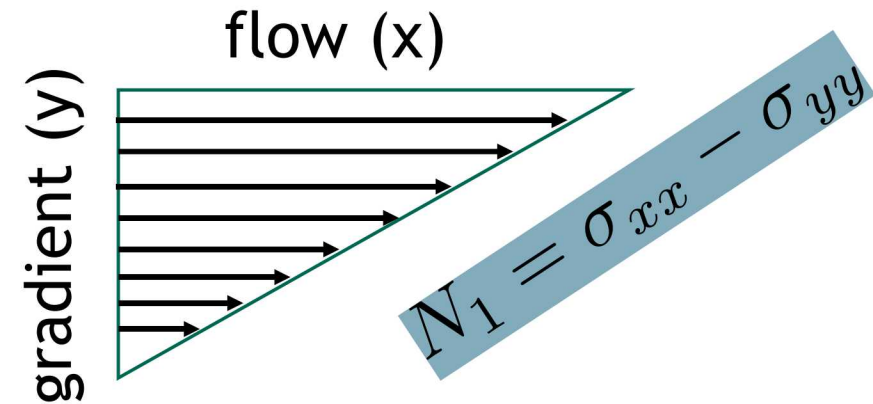
$$\tau = \sqrt{\frac{1}{2}\boldsymbol{\sigma}_D : \boldsymbol{\sigma}_D}$$

$$\mu = \mu_1 + aI + (\mu_0 - \mu_1) e^{-I/b}$$

$$\phi = \phi_1 - pI + (\phi_0 - \phi_1) e^{-I/q}$$

# First Normal Stress Difference

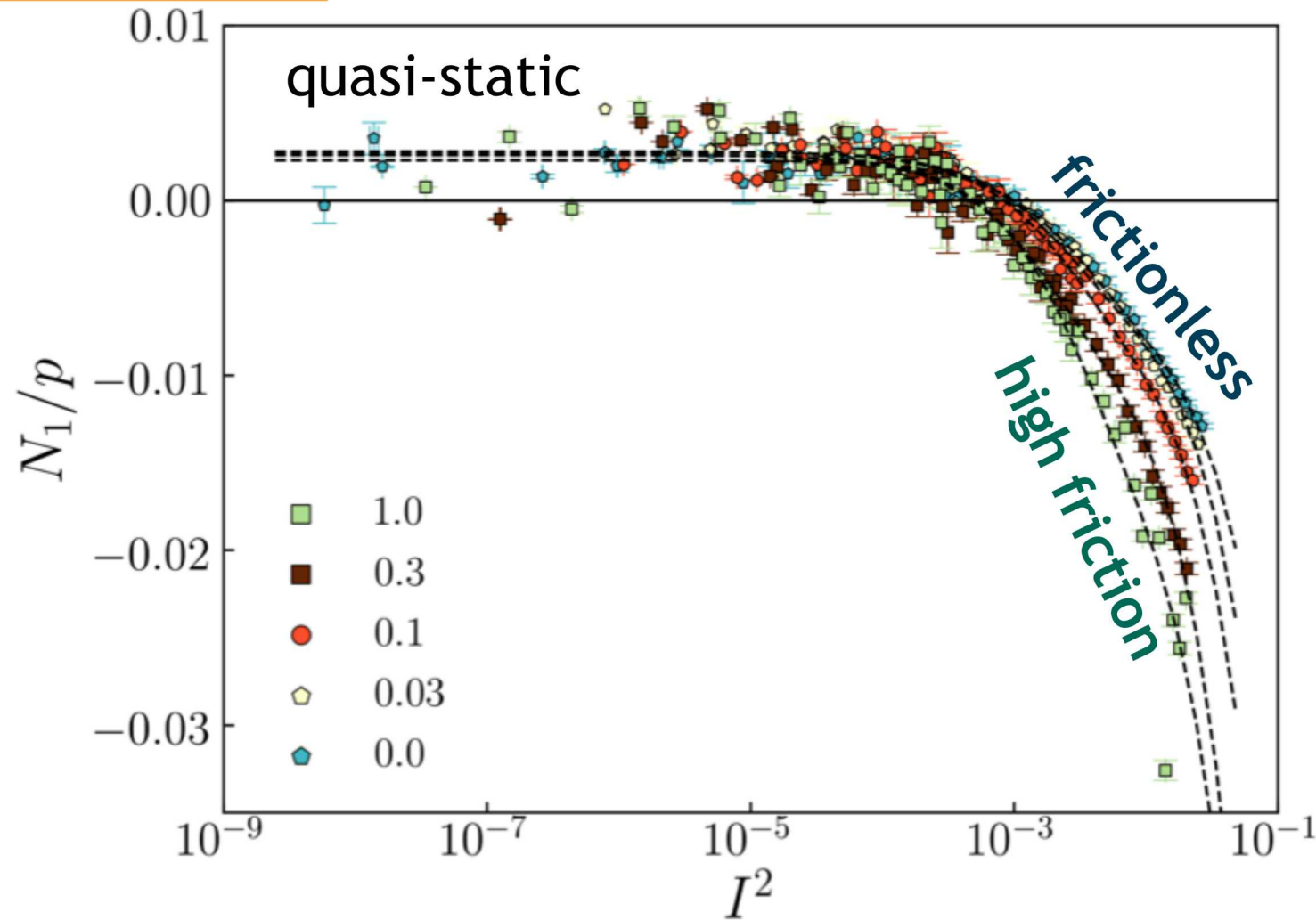
flow plane



$N_1$  is negative in the inertial regime

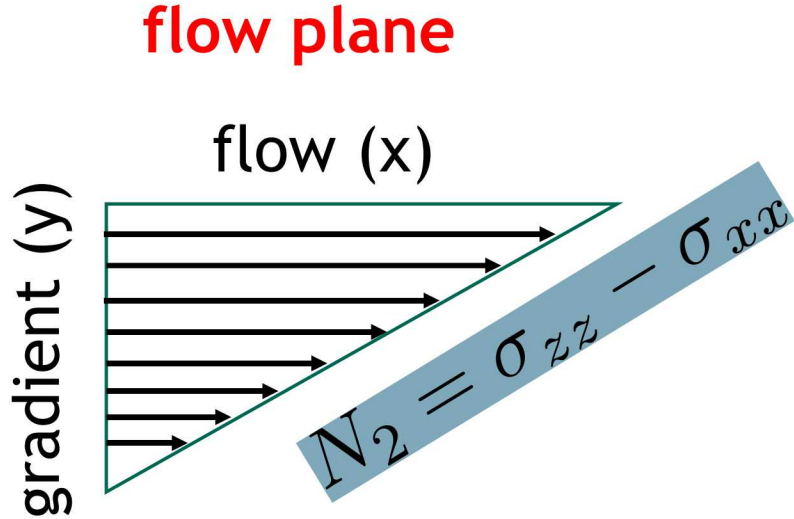
$N_1$  is slightly positive in quasi-static regime

microstructure-induced anisotropy in flow plane



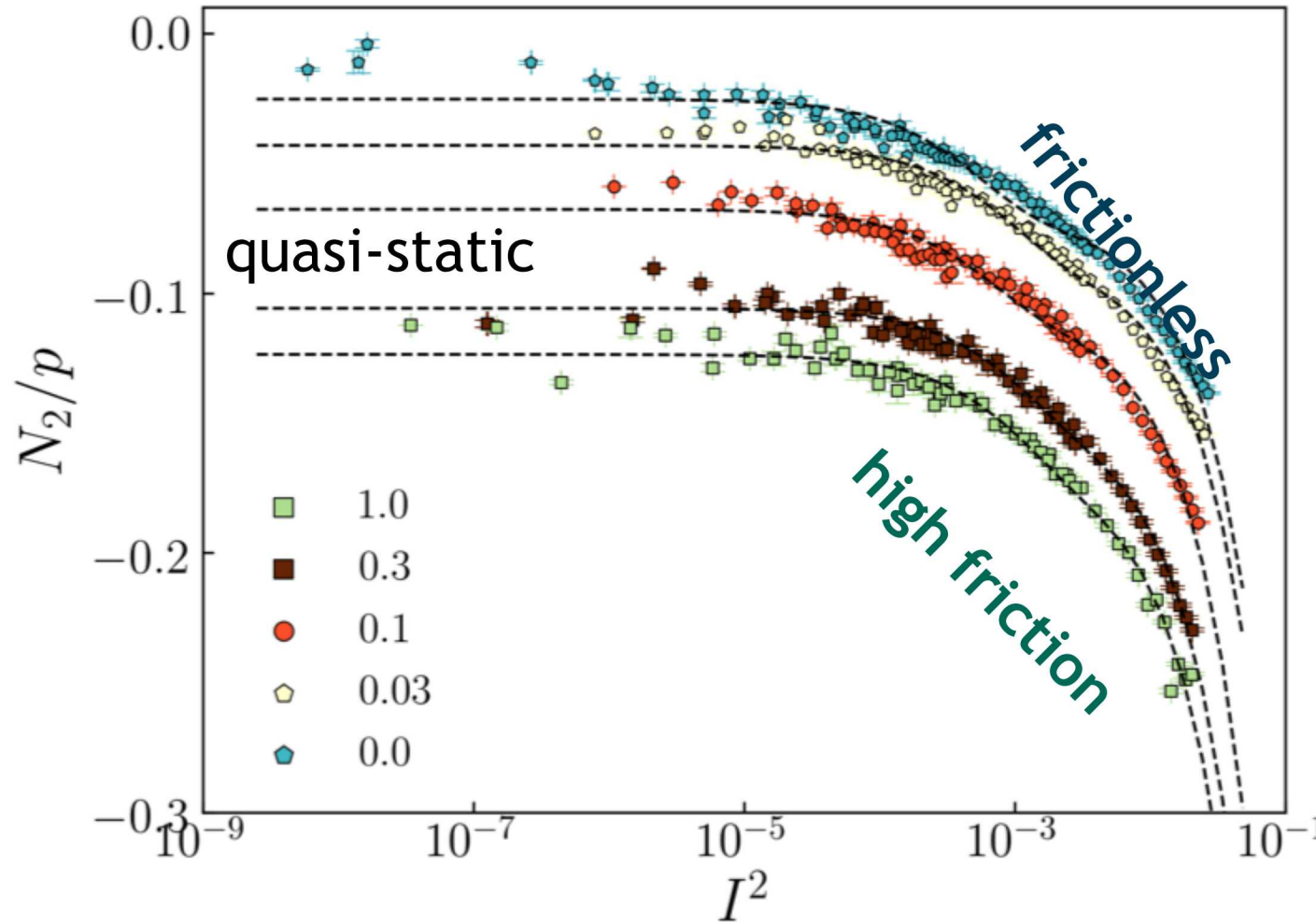
$$\frac{N_1}{p} = \mu_2 - cI^2 + (\mu_2 - \mu_3) e^{-I^2/d}$$

# Second Normal Stress Difference



second normal stress is always negative

frictionless particles show zero normal stress difference at RCP



$$\frac{N_2}{p} = \mu_4 - eI^2 + (\mu_4 - \mu_5) e^{-I^2/f}$$

# 3D Constitutive Model for Granular Rheology

purely dissipative rheological framework: Goddard (1984,1986)

$$\boldsymbol{\sigma} = p\mathbf{I} + \eta_1 \mathbf{D} + \eta_2 \left[ \mathbf{D}^2 - \frac{\text{tr}(\mathbf{D}^2)}{3} \mathbf{I} \right] + \eta_3 \left[ \dot{\mathbf{D}} - \mathbf{W}\mathbf{D} + \mathbf{D}\mathbf{W} \right]$$

hydrostatic

shear

second normal stress diff.

first normal stress diff.

$$+ \kappa_1 \frac{\mathbf{D}}{|\mathbf{D}|} + \kappa_2 \left[ \frac{\mathbf{D}^2}{|\mathbf{D}|^2} - \frac{\text{tr}(\mathbf{D}^2)}{3|\mathbf{D}|^2} \mathbf{I} \right] + \kappa_3 \left[ \frac{\dot{\mathbf{D}} - \mathbf{W}\mathbf{D} + \mathbf{D}\mathbf{W}}{|\dot{\mathbf{D}} - \mathbf{W}\mathbf{D} + \mathbf{D}\mathbf{W}|} \right]$$

shear

second normal stress diff.

first normal stress diff.

(rate-independent)

(rate-independent)

(rate-independent)

# Extensions to Complex Flow Scenarios

$$\begin{aligned} \boldsymbol{\sigma} = & p\mathbf{I} + \eta_1 \mathbf{D} + \eta_2 \left[ \mathbf{D}^2 - \frac{\text{tr}(\mathbf{D}^2)}{3} \mathbf{I} \right] + \eta_3 \left[ \dot{\mathbf{D}} - \mathbf{W}\mathbf{D} + \mathbf{D}\mathbf{W} \right] \\ & + \kappa_1 \frac{\mathbf{D}}{|\mathbf{D}|} + \kappa_2 \left[ \frac{\mathbf{D}^2}{|\mathbf{D}|^2} - \frac{\text{tr}(\mathbf{D}^2)}{3|\mathbf{D}|^2} \mathbf{I} \right] + \kappa_3 \left[ \frac{\dot{\mathbf{D}} - \mathbf{W}\mathbf{D} + \mathbf{D}\mathbf{W}}{|\dot{\mathbf{D}} - \mathbf{W}\mathbf{D} + \mathbf{D}\mathbf{W}|} \right] \end{aligned}$$

$$\eta_{1,2,3} = \eta_{1,2,3} \left( \text{tr}(\mathbf{D}^2), \text{tr}(\mathbf{D}^3) \right)$$

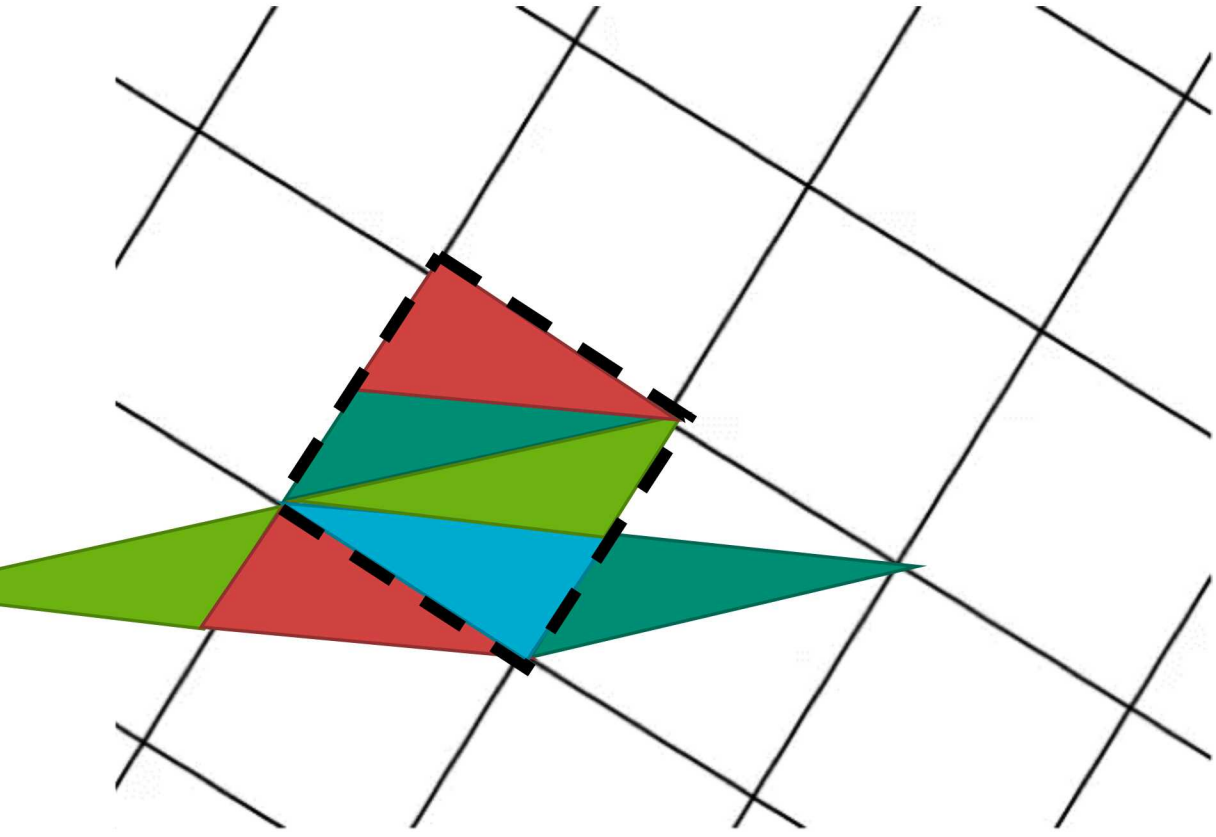
... shear vs. extensional vs. complex flows

$$\kappa_{1,2,3} = \kappa_{1,2,3} \left( \frac{\text{tr}(\mathbf{D}^2)}{|\text{tr}(\mathbf{D}^2)|}, \frac{\text{tr}(\mathbf{D}^3)}{|\text{tr}(\mathbf{D}^3)|} \right)$$

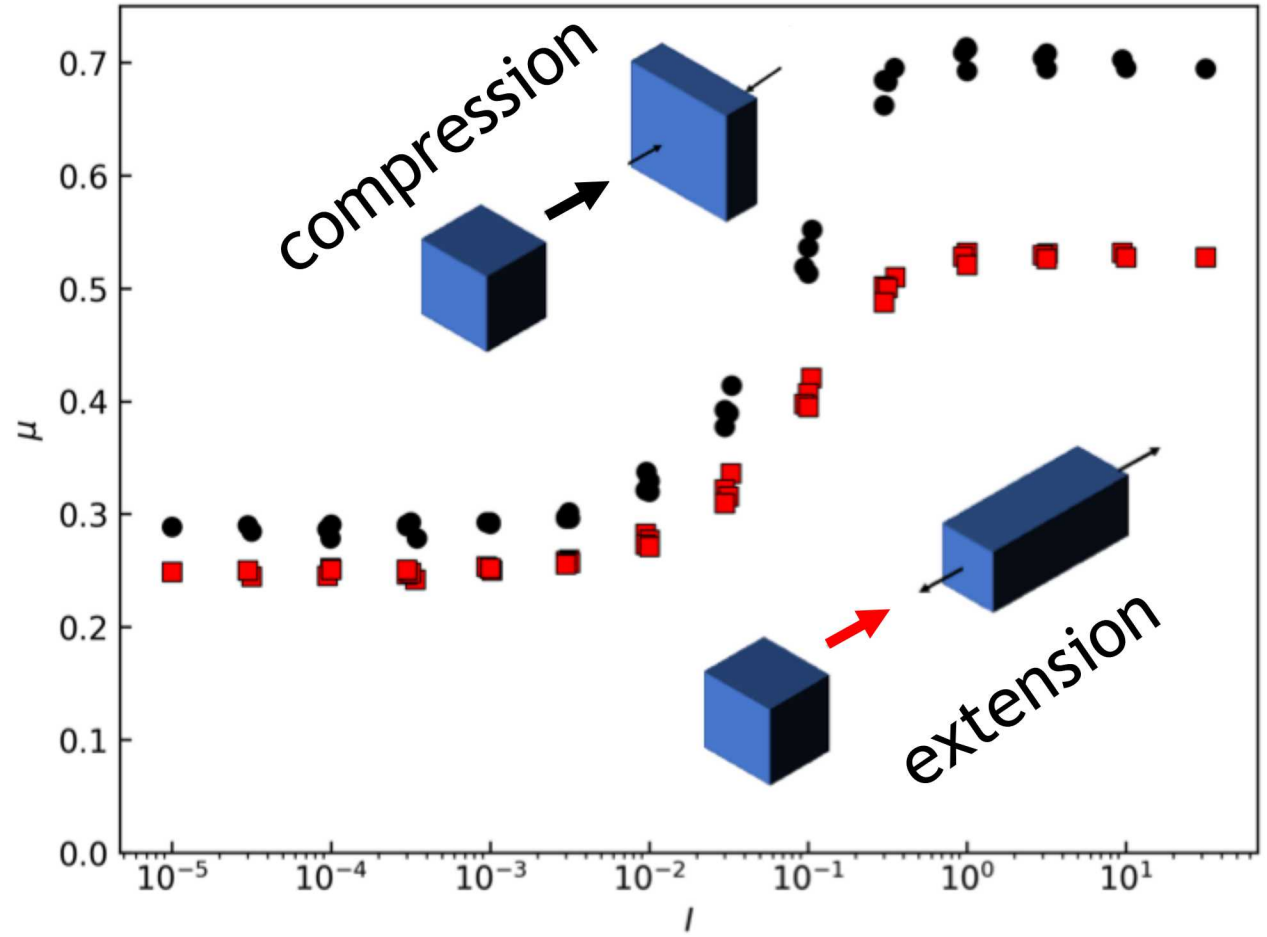
... direction-dependent deformation - soil plasticity (Lode angle)

# Compressional and Extensional Flows

compressional and extensional flows

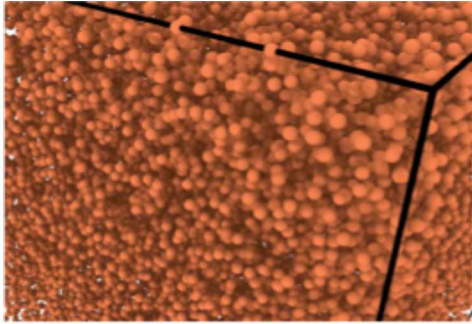


Kraynik-Reinelt boundary conditions

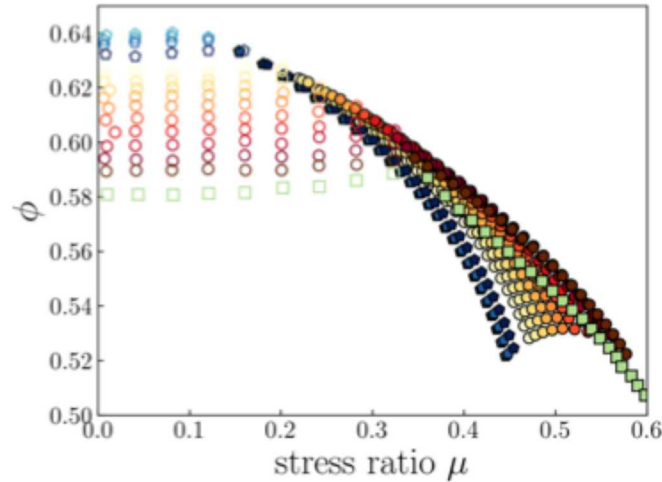


# Conclusions & Outlook

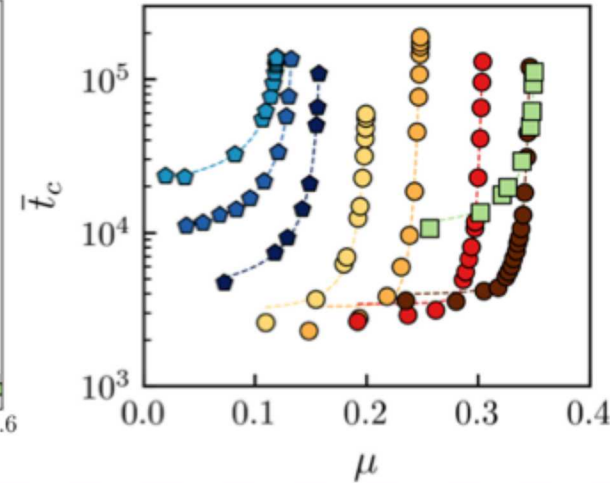
stress-driven  
simulations



**IF:** flow-arrest  
diagram

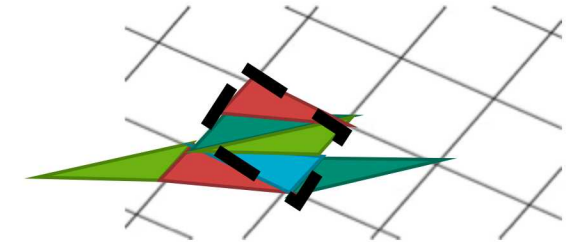


**WHEN:** diverging  
arrest times



**HOW:** beyond  
 $\mu(I)$  rheology

$$\sigma = pI + \eta_1 D + \eta_2 \left[ D^2 - \frac{\text{tr}(D^2)}{3} I \right] + \eta_3 \left[ \dot{D} - WD + DW \right] + \kappa_1 \frac{D}{|D|} + \kappa_2 \left[ \frac{D^2}{|D|^2} - \frac{\text{tr}(D^2)}{3|D|^2} I \right] + \kappa_3 \left[ \frac{\dot{D} - WD + DW}{|\dot{D} - WD + DW|} \right]$$



- are shear-arrested states fragile/stable? mechanical properties?  
à la [Bi, Behringer, Nature (2011)]
- is there a diverging length scale at shear-arrest near critical yield?
- calibrate the constitutive model for complex flow scenarios

CONCLUSIONS

OUTLOOK:

# Acknowledgements

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## Sandia National Laboratories

- Gary Grest
- Jeremy Lechman
- Dan Bolintineanu
- Andrew Santos
- Joel Clemmer

## Central New Mexico College

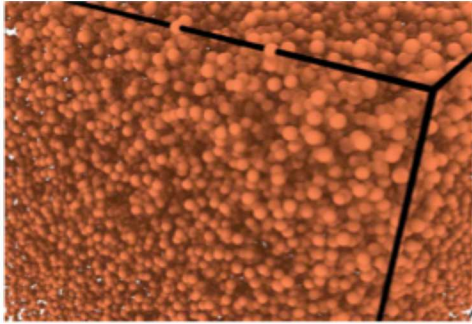
- Leonardo Silbert



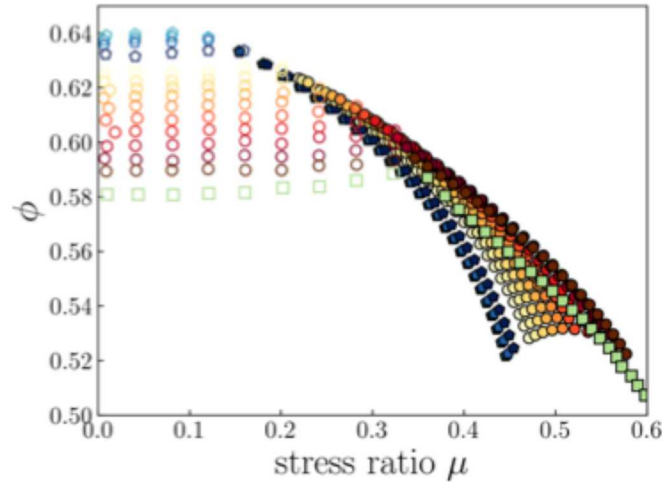
Center for Integrated Nanotechnologies,  
Sandia National Laboratory

# Conclusions & Outlook

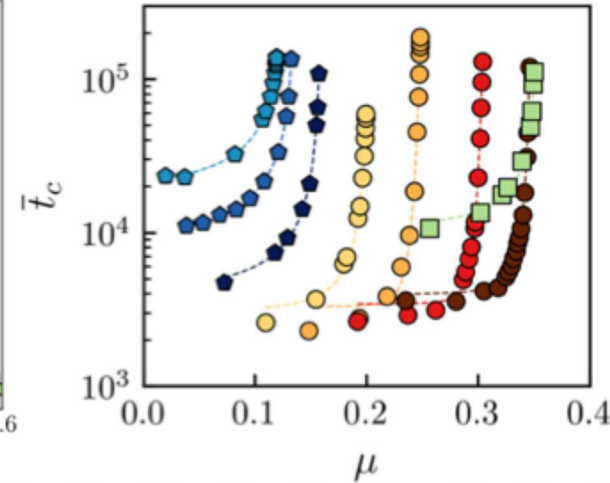
stress-driven simulations



**IF:** flow-arrest diagram

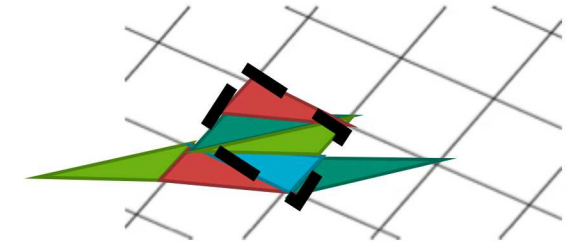


**WHEN:** diverging arrest times



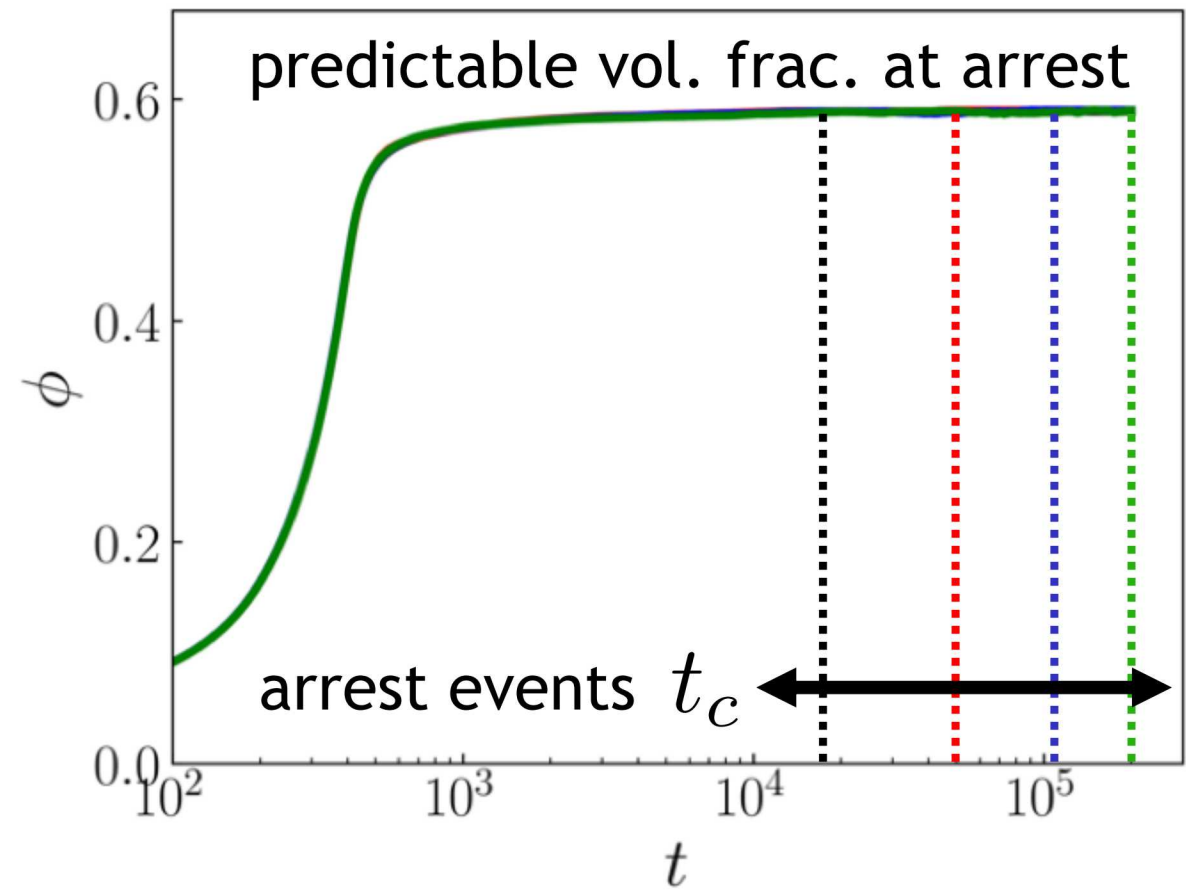
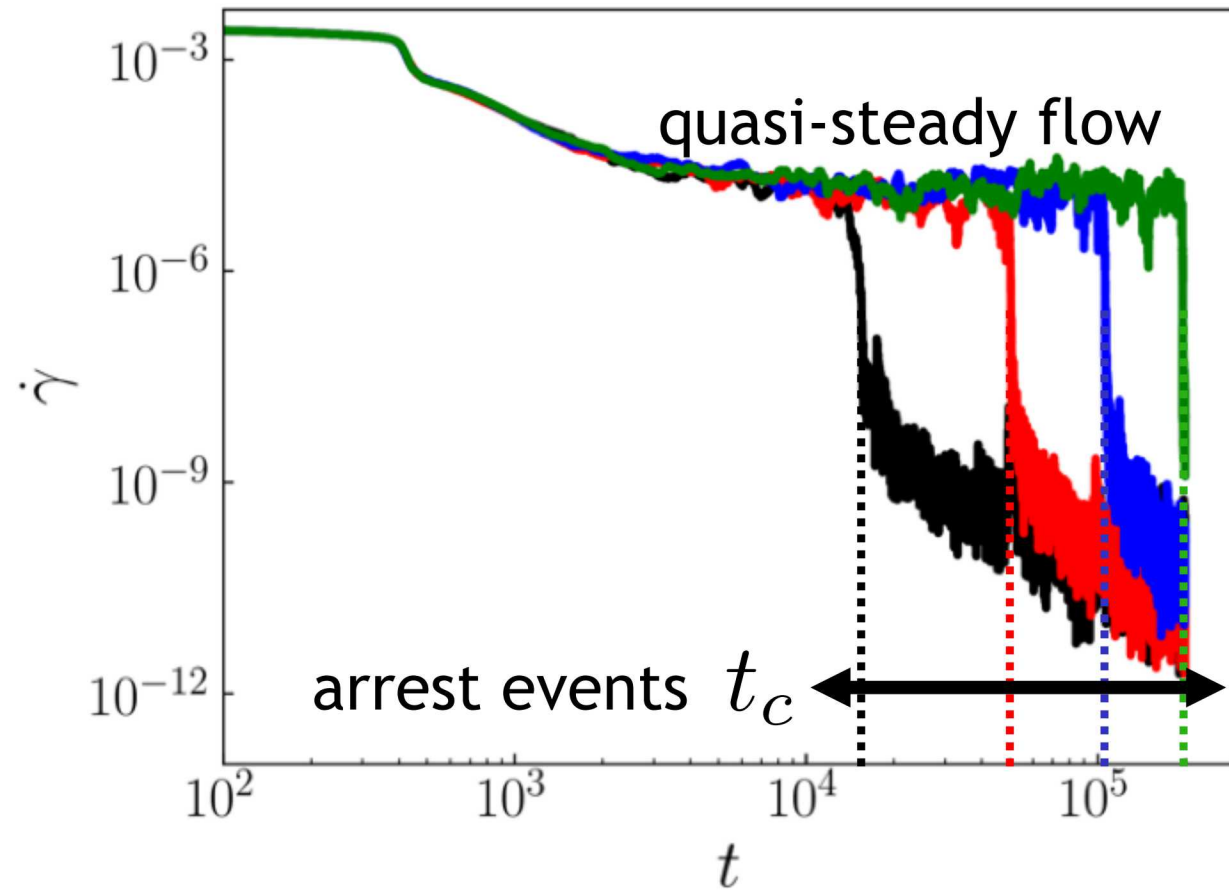
**HOW:** beyond  $\mu(I)$  rheology

$$\sigma = pI + \eta_1 D + \eta_2 \left[ D^2 - \frac{\text{tr}(D^2)}{3} I \right] + \eta_3 \left[ \dot{D} - WD + DW \right] + \kappa_1 \frac{D}{|D|} + \kappa_2 \left[ \frac{D^2}{|D|^2} - \frac{\text{tr}(D^2)}{3|D|^2} I \right] + \kappa_3 \left[ \frac{\dot{D} - WD + DW}{|\dot{D} - WD + DW|} \right]$$



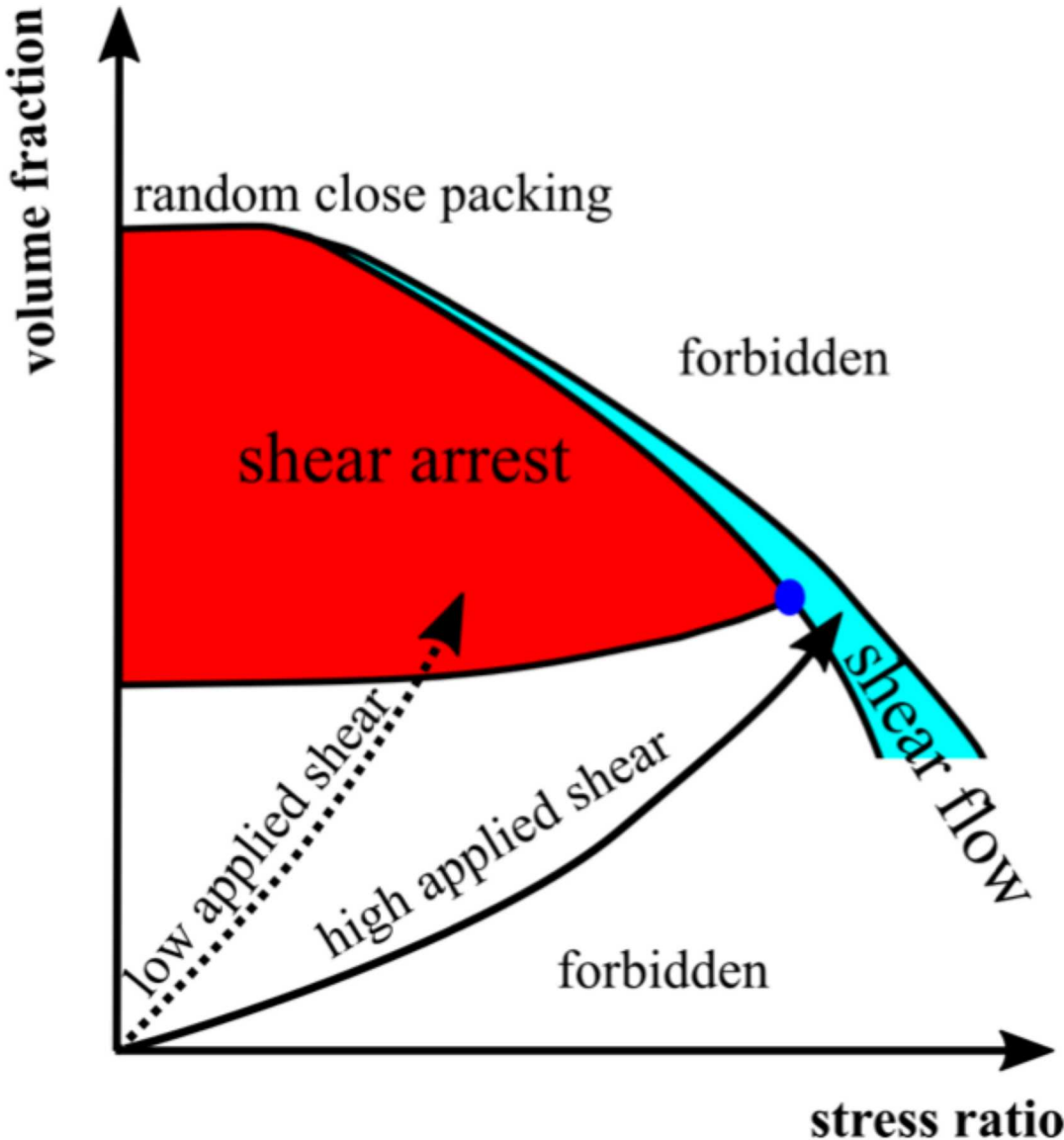
- are shear-arrested states fragile/stable? mechanical properties?  
à la [Bi, Behringer, Nature (2011)]
- is there a diverging length scale at shear-arrest near critical yield?
- calibrate the constitutive model for complex flow scenarios

# Volume Fraction at Arrest is Deterministic

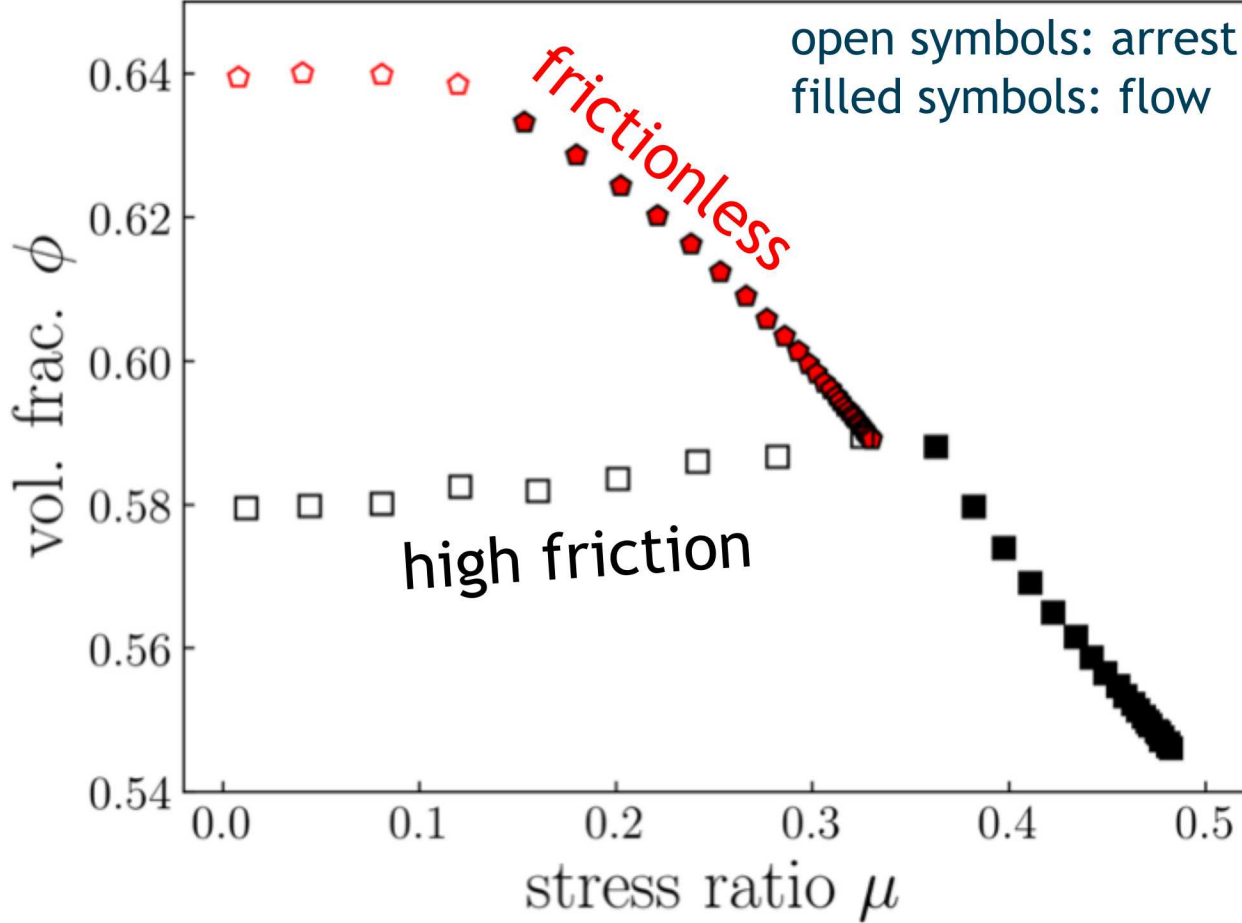


difficult to predict when a flow will arrest,  
but sure of volume fraction & coordination upon arrest

# Paths to Flow or Arrest



well-defined flow & arrest states for every friction



# Stress States at Yielding and Flow

$$\Delta E(t) = \int_{\Gamma} f_i \Delta u_i dS - \int_V \sigma_{ij} \frac{\partial (\Delta u_i)}{\partial x_j} dV$$

change in kinetic energy

boundary traction work

second order work (constitutive)

**Arrest (Jammed):**

$$\int_{\Gamma} f_i \Delta u_i dS = \int_V \sigma_{ij} \frac{\partial (\Delta u_i)}{\partial x_j} dV$$

equilibrium: balance of internal and external stress

**Yielding:**

$$\int_{\Gamma} f_i \Delta u_i dS > \int_V \sigma_{ij} \frac{\partial (\Delta u_i)}{\partial x_j} dV$$

rapid increase in kinetic energy: imbalance of internal and external stresses