

Transport in Fractured Rock



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Outline

- **Fracture transport processes (from perspective of tracer testing)**
- **Three conceptual models**
 - Single Porosity
 - Double Porosity
 - Multi-porosity (multirate)
- **Field Examples**
 - Aspo TRUE tracer tests
 - Imaging fracture filling



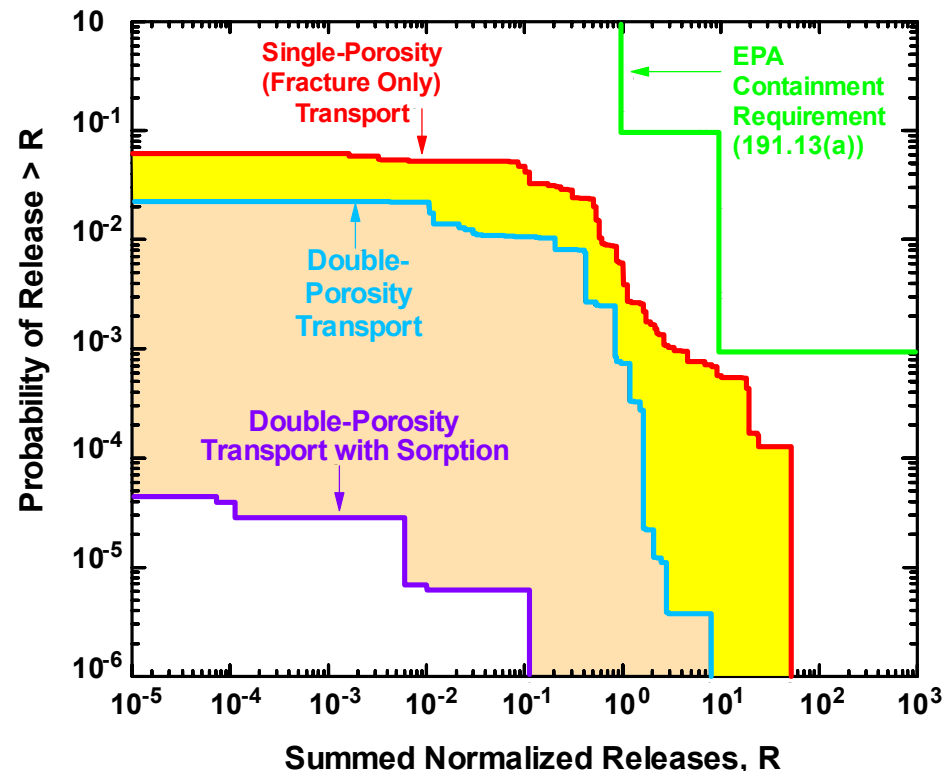
Motivation: WIPP Example

Probabilistic Systems Analysis is used to predict the future performance of the repository – incorporate uncertainty in multiple processes and parameters

Regulations are written to incorporate uncertainty

Mass transfer processes make a huge difference in predicted repository performance

Other situations: hydrothermal mineralization, partitioning tracer tests for DNAPL, groundwater-surface water coupling with bank storage, etc.



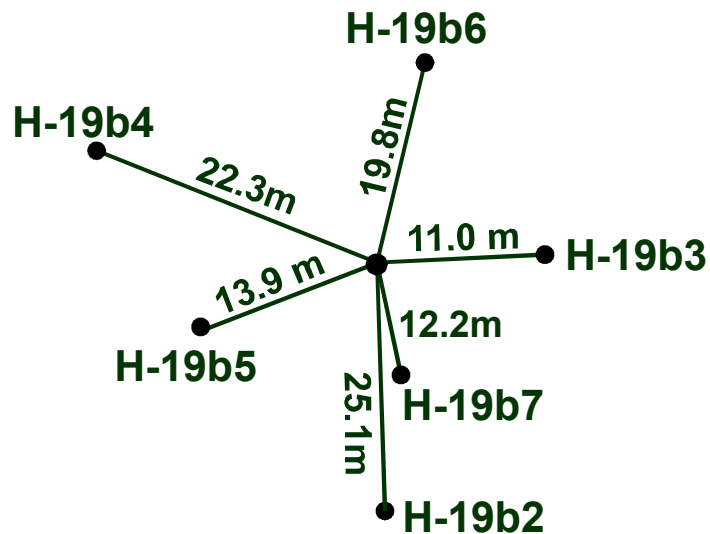
Tracer Testing

- **Inject a solute into the aquifer that does not occur locally in significant amounts**
 - **Naturally Occurring: Iodine, Chlorine, Deuterium**
 - **Synthetic: Radionuclides, Chloro/Flouorobenzoic acids, polystyrene spheres**
- **Extract that solute in a pumping well**
- **Examine the concentration as a function of time (breakthrough curve) to gain insight into aquifer properties**
 - **Dispersion, porosity, diffusion, sorption**

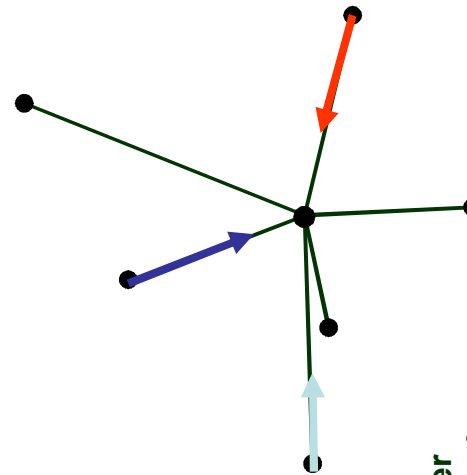


Tracer Testing

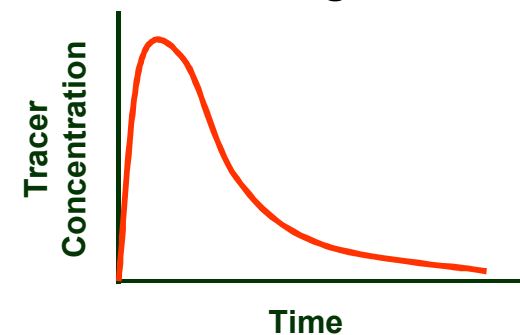
Convergent Flow Tests



Central pumping well with tracer injections at surrounding wells

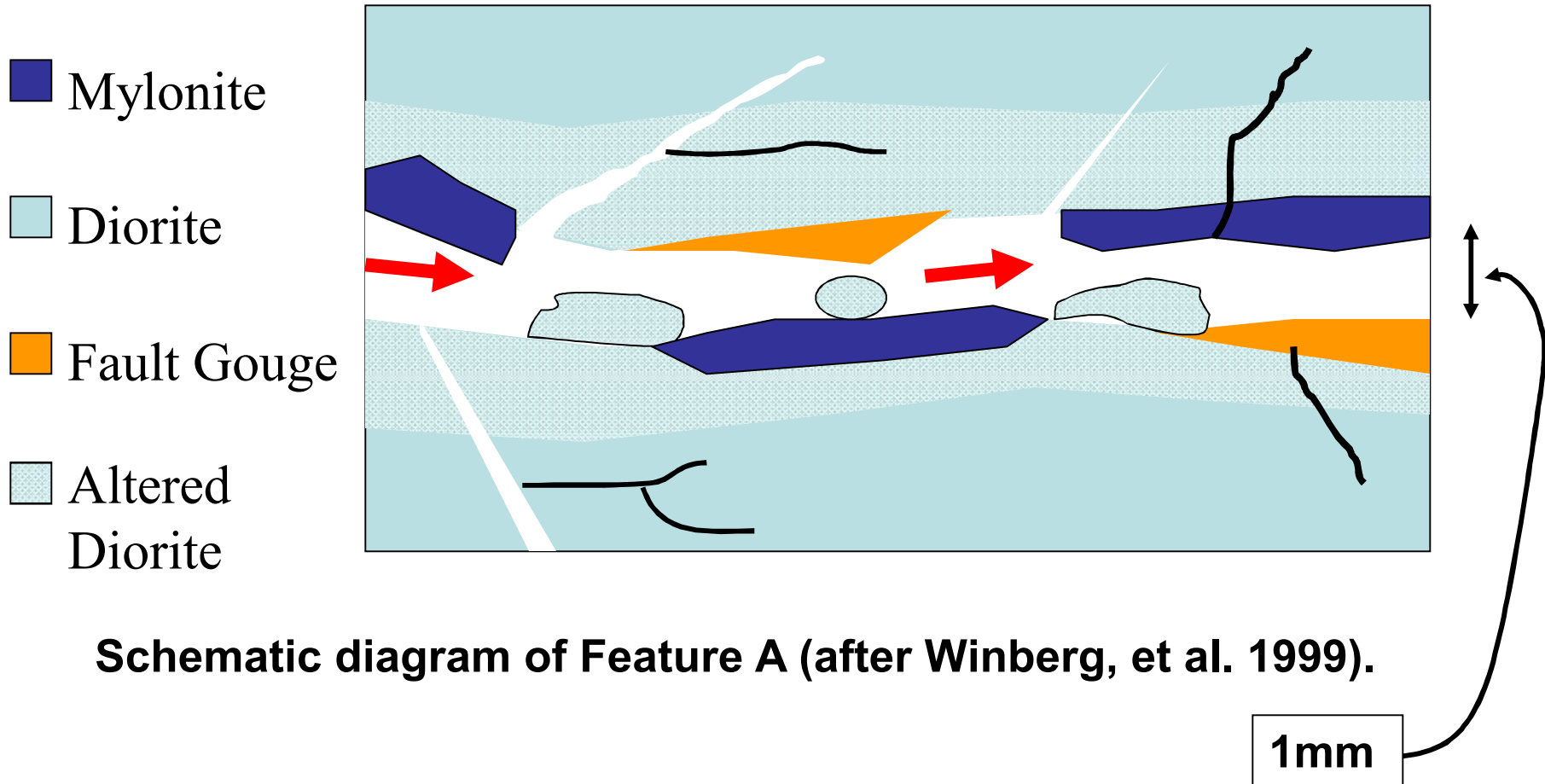


Breakthrough Curve



Injection phase of Culebra H-19 hydropad tracer testing at WIPP Site, SE New Mexico

Conceptual Model: Fractured Granite

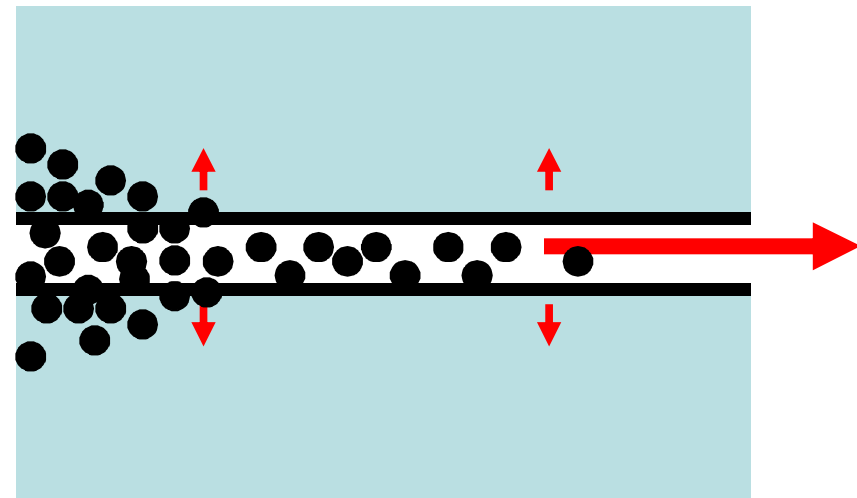


Transport Processes

- **Processes acting in a single fracture:**
 - Dispersion (velocity variation along different flowpaths due to physical heterogeneity in fracture)
 - Diffusion (movement of solute due to concentration gradient – from fracture to matrix and back)
 - Sorption (attachment of solute to fracture walls and matrix pore spaces)

Conceptually, there are two domains in the rock:

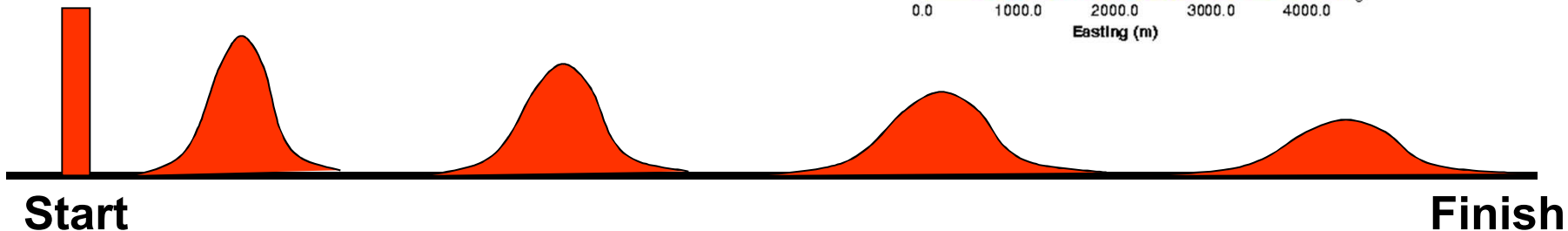
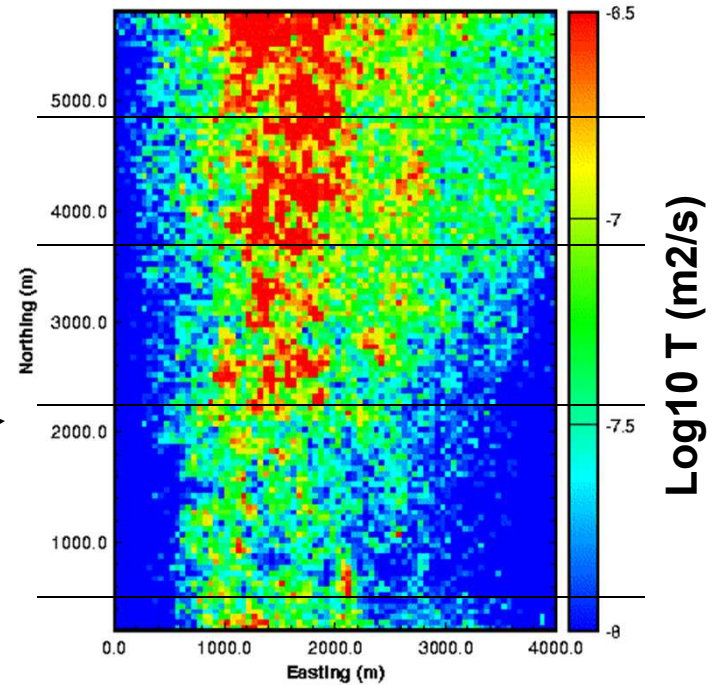
- 1) *Advective, mobile, fracture*
- 2) *Diffusive, stagnant, matrix*



Dispersion

- Physical process of solute moving at different velocities along different flowpaths

Flowpaths in a heterogeneous fracture plane



Analogy: a 10k running race



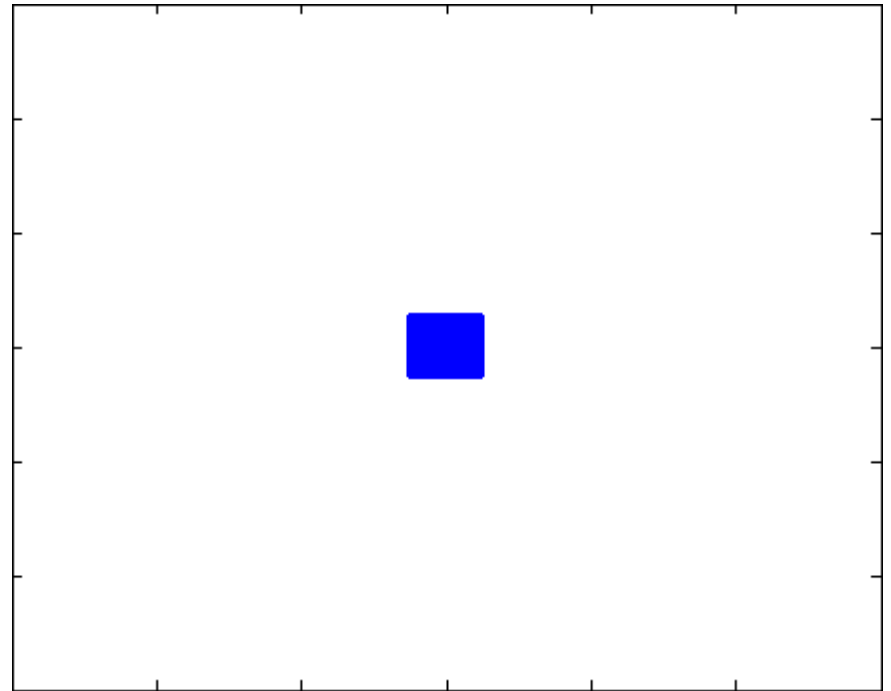
Diffusion

- **Spreading of a solute due to a concentration gradient**

Fick's 1st law: Flux of solute is proportional to concentration gradient

$$F = -D \frac{\partial C}{\partial x}$$

D is a function of the material(s) through which the solute is diffusing

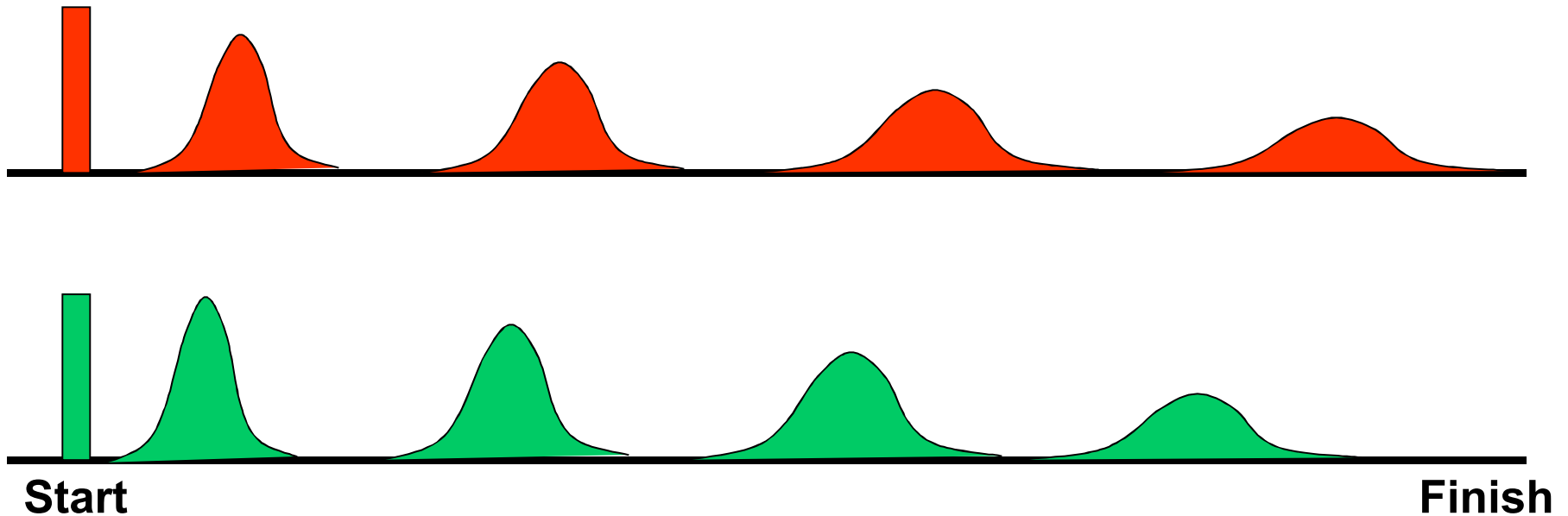


Analogy: Drop of dye in an aquarium



Sorption

- Adherence of solute onto a surface (fracture or pore)



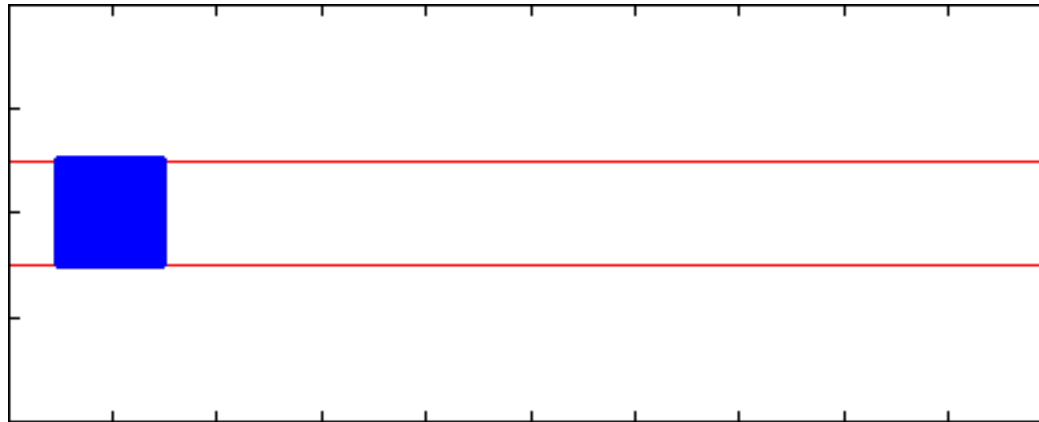
Analogy: A 10k running race with faulty shoe laces



Dispersive Transport

Simple particle tracking model showing solute transport in a single fracture with matrix on top and bottom

Hydrodynamic dispersion is active, but no mass-transfer with matrix



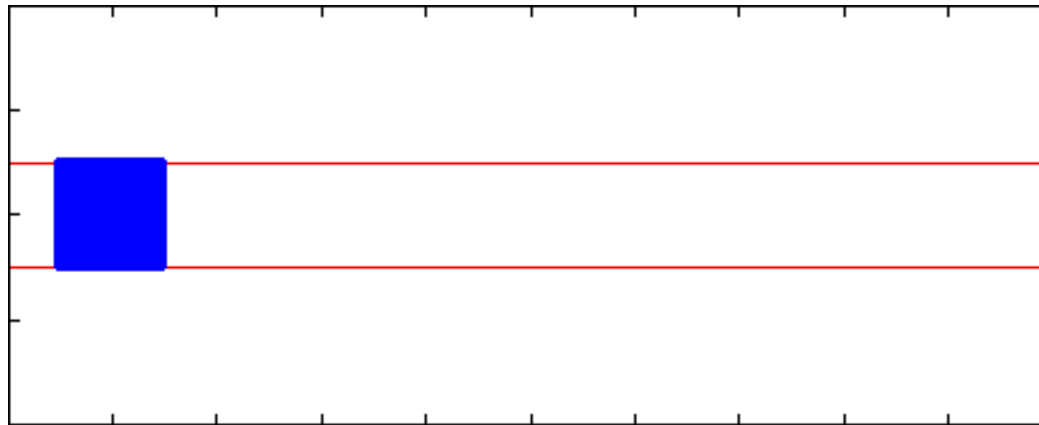
Also referred to as “single-porosity” transport



Dispersion and Diffusion

Simple particle tracking model showing solute transport in a single fracture with matrix on top and bottom

Hydrodynamic dispersion and mass-transfer are active

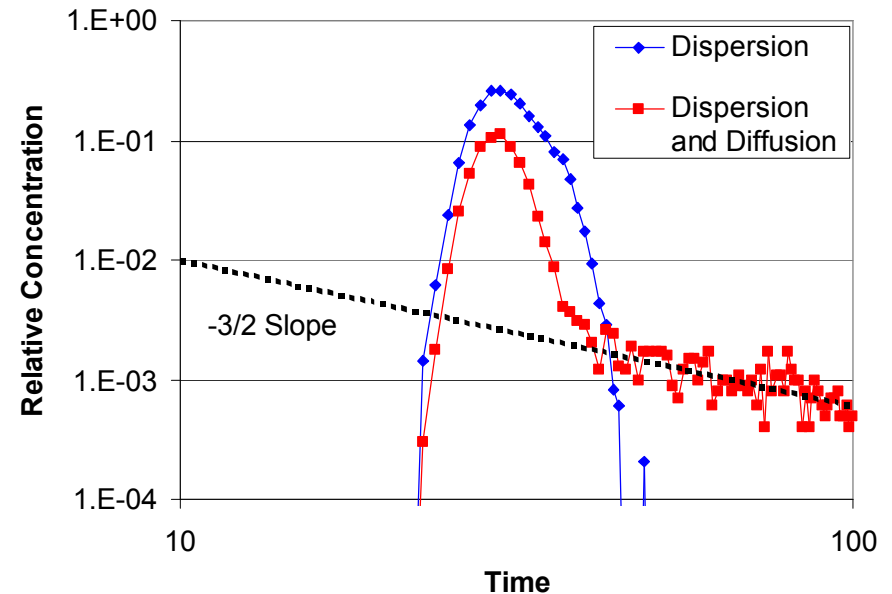
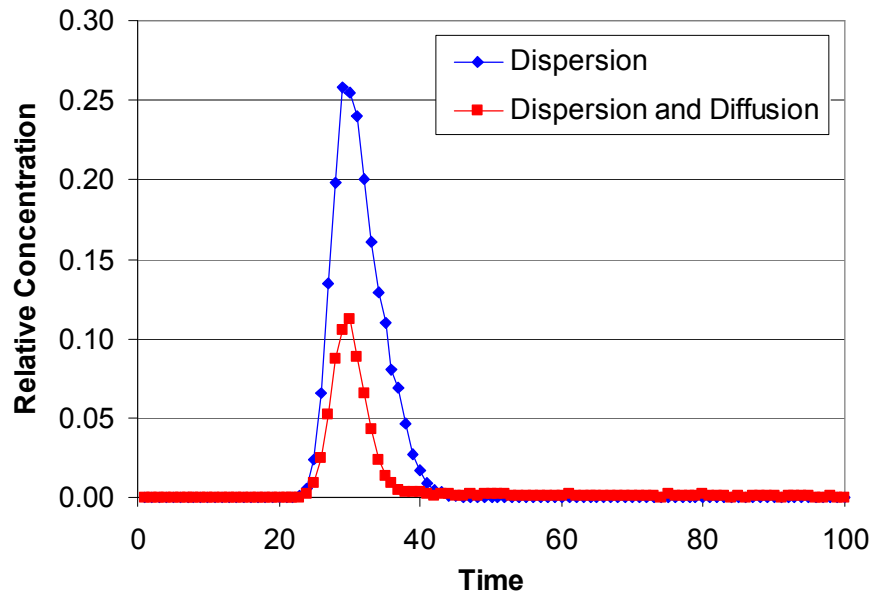


Also referred to as “dual-porosity” transport



Breakthrough Curves

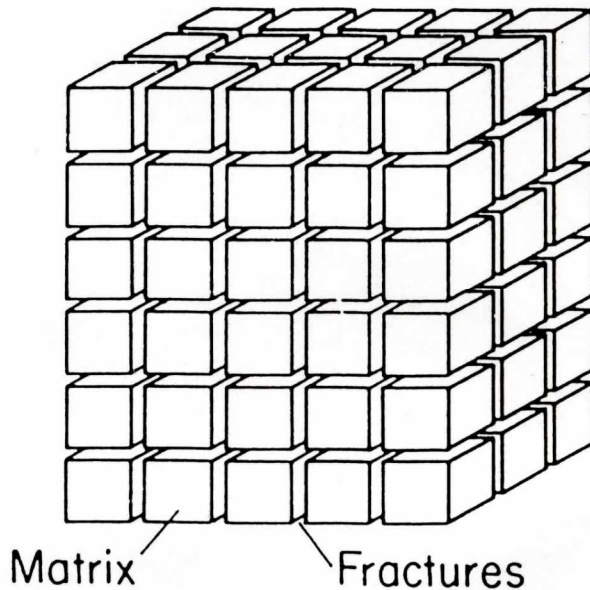
The breakthrough curve is the plot of the concentration as a function of time at a downgradient location (e.g., pumping well).



- *To characterize tailing behavior, examine results in log-log space*
- *-3/2 slope is characteristic of diffusion into an infinite medium*



Traditional Dual Porosity Model



The classic dual-porosity representation of a fractured medium is the “sugar-cube” model

To match an observed breakthrough curve that does not have a $-3/2$ slope, the amount of dispersion and the matrix block size are adjusted

The Real World



Large blocks: bigger capacity, less surface area per aquifer volume, slower diffusion rate

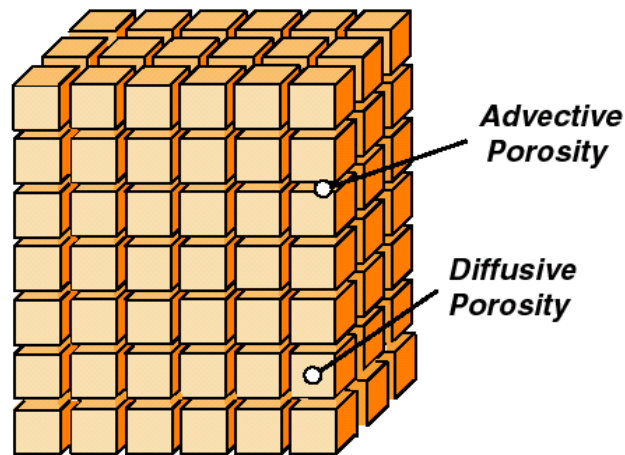
Small blocks: small capacity, more surface area per aquifer volume, faster diffusion rate

Solute accesses all blocks simultaneously

Cemented breccia zone at Yucca Mountain, Nevada

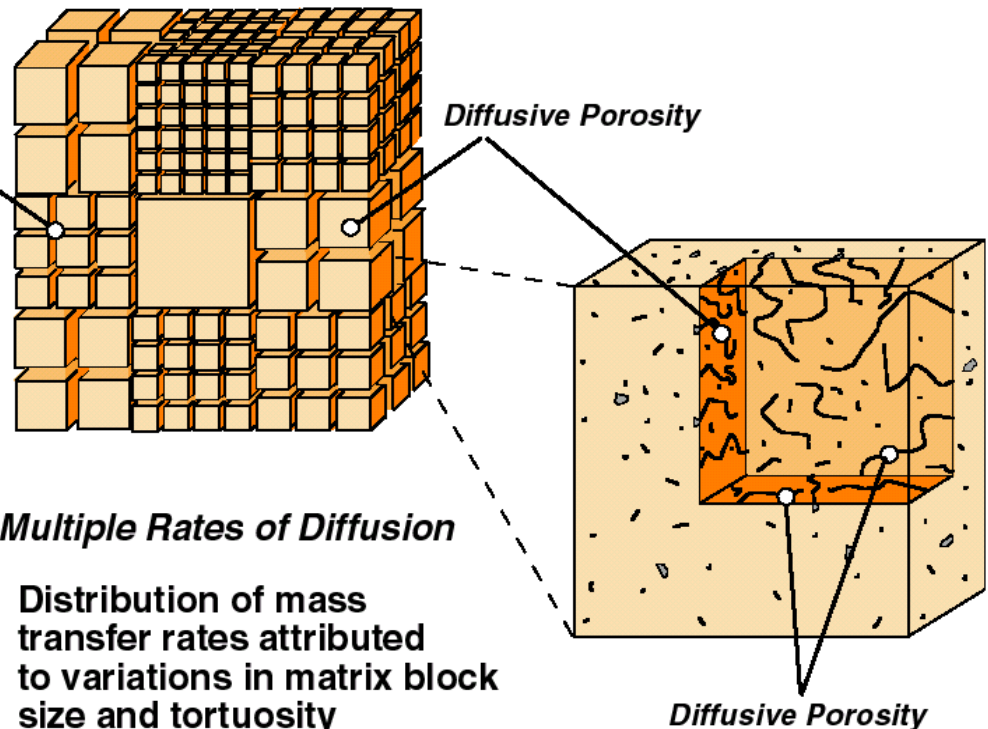
Multi-Porosity Model

Conventional Single Rate Diffusion



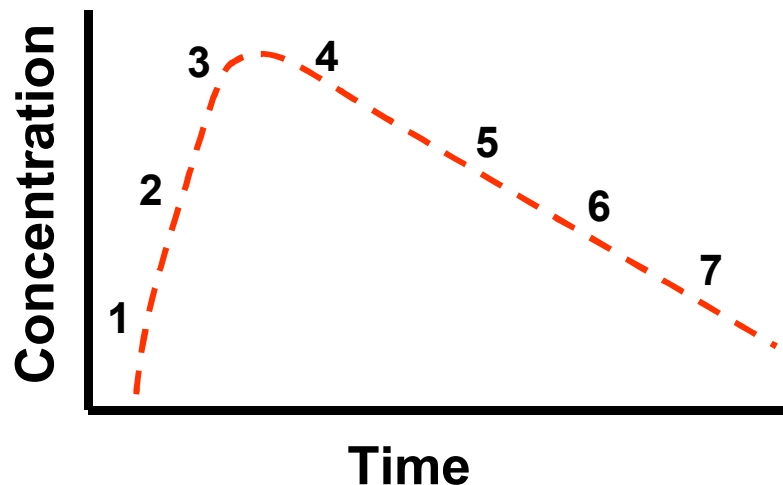
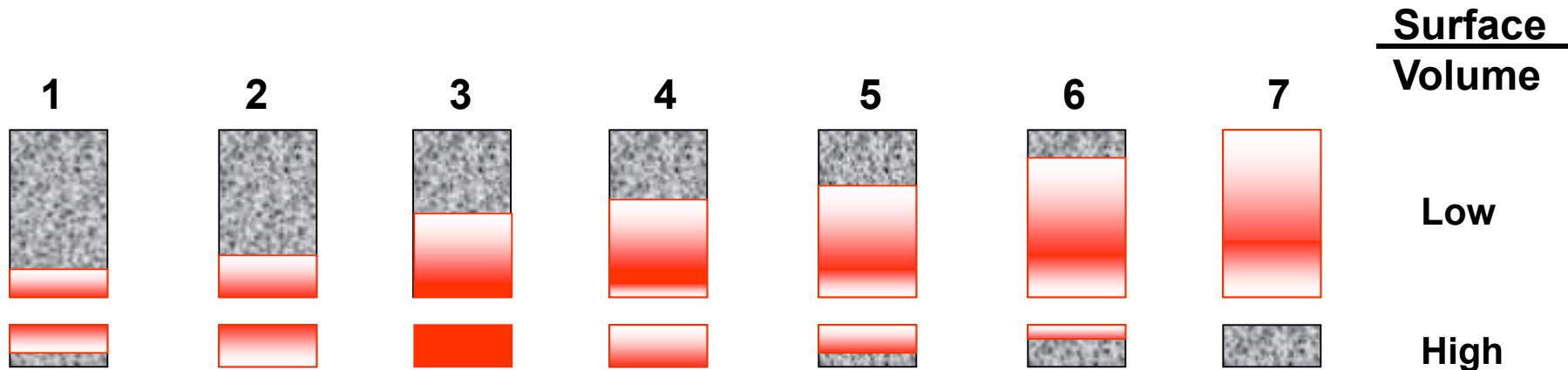
- **Constant Matrix Block Size**
Surface area for diffusion and diffusion distance
- **Constant tortuosity**
Tortuous nature of "matrix" pores

Multirate Diffusion



- **Multiple Rates of Diffusion**
Distribution of mass transfer rates attributed to variations in matrix block size and tortuosity

Matrix Block Size



**Slower mass transfer
from matrix results in
shallower (longer) tail**

**Different rates of mass
transfer create different
slopes in late time tail**

Transport Equation

Solute transport equation for advection and dispersion in one dimension (x direction) and allowing for mass-transfer through diffusion and/or sorption:

$$\frac{1}{R_m} \frac{\partial}{\partial x} \left(D \frac{\partial c}{\partial x} - v c \right) = \frac{\partial c}{\partial t} + \Gamma(x, t)$$

c = solute concentration in the advective domain M/L^3

v = average advective velocity (L/t)

$D = \alpha_l v + D^*$ = hydrodynamic dispersion (L^2/t)

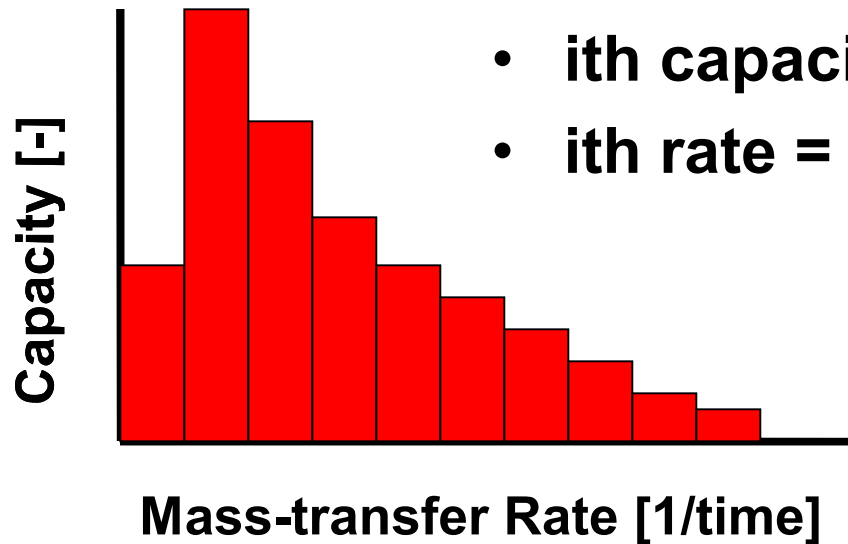
R_m = retardation coefficient in the (mobile) advective domain (-)

$\Gamma(x, t)$ = source/sink for mass transfer with diffusive domain (M/L^3t)



Model Parameters (mass-transfer)

Parameterize the capacity of the matrix to uptake solute with a log-normal distribution of mass transfer rate coefficients



- i th capacity = $b(i)$
- i th rate = $\alpha(i)$

$$\beta_{tot} = \sum_{i=1}^N b(i) = \frac{\phi_{im} R_{im}}{\phi_m R_m}$$

$$\alpha_i = \frac{D_{aq} \tau}{l^2 R_{im}}$$

Log-normal distribution of rate coefficients is defined by mean (μ) and standard deviation (σ)

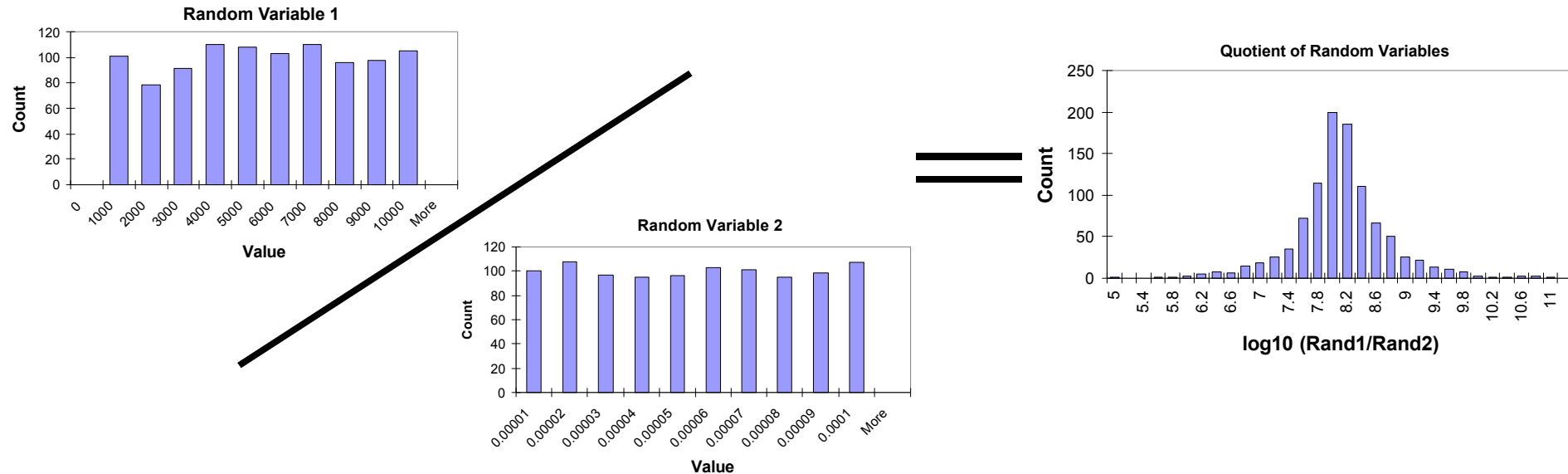
$$\mu = \frac{1}{N} \sum_{i=1}^N \log(\alpha(i))$$

$$\sigma = \sqrt{\frac{1}{N} \sum_{i=1}^N (\log(\alpha(i)) - \mu)^2}$$



Log-Normal Distribution?

Products and Quotients of random variables are log-normally distributed



Random variables: fracture spacing, matrix block size, porosity, diffusion coefficient, tortuosity, sorption site distribution, etc.

$$\alpha_i = \frac{D_{aq}\tau}{l^2 R_{im}}$$



Model Parameters (sorption)

Mobile zone retardation factor:

$$R_m = 1 + \frac{\rho_b K_{d,m} f_m}{\phi_m}$$

Immobile zone retardation factor:

$$R_{im} = 1 + \frac{\rho_b K_{d,im} f_{im}}{\phi_{im}}$$

ρ_b = bulk density (M/L³)

ϕ_m = mobile zone porosity (-)

ϕ_{im} = immobile zone porosity (-)

K_d = distribution coefficient (L³/M)

f_m = mass fraction of sorbed phase in equilibrium with mobile zone (-)

f_{im} = mass fraction of sorbed phase in equilibrium with immobile zone (-)

$$f_m + f_{im} = 1.0$$

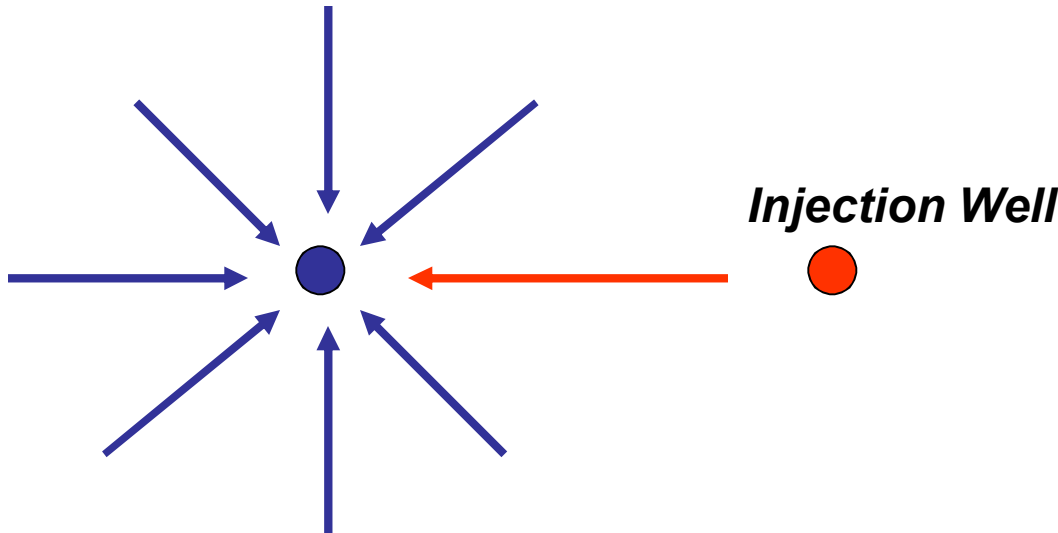


Model Parameters (advective)

V_x = 1-D velocity along transport pathway

α_L = longitudinal dispersivity

dilute = dilution factor (not all water coming out of the pumping well has tracer)



$$dilute = \frac{Q_{pump}}{Q_{inject}}$$

$$dilute = \frac{Q_{pump}}{Q_{inject}} \cdot \frac{1}{RMF}$$

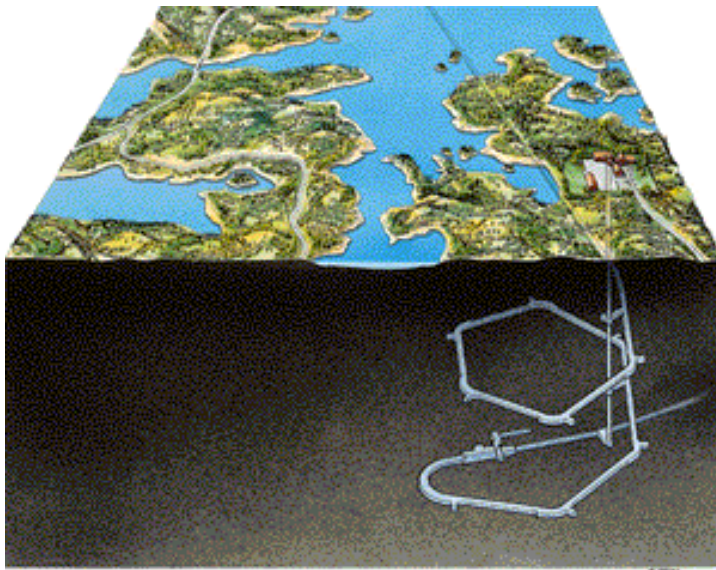
Model Parameters

- **Advective**
 - Velocity (V_x)
 - Dilution Factor (dilute)
 - Dispersivity (α_L)
- **Mass-Transfer**
 - Total Capacity (β_{tot})
 - Mean of lognormal distribution of rates (μ)
 - Standard deviation of lognormal distribution of rates (σ)
 - Mobile zone retardation factor (R_m)



Application to Granitic Rocks

- **Aspo Task Force**
 - 10 nuclear waste organizations from 8 countries
 - Tracer experiments conducted at Aspo underground research laboratory in Sweden

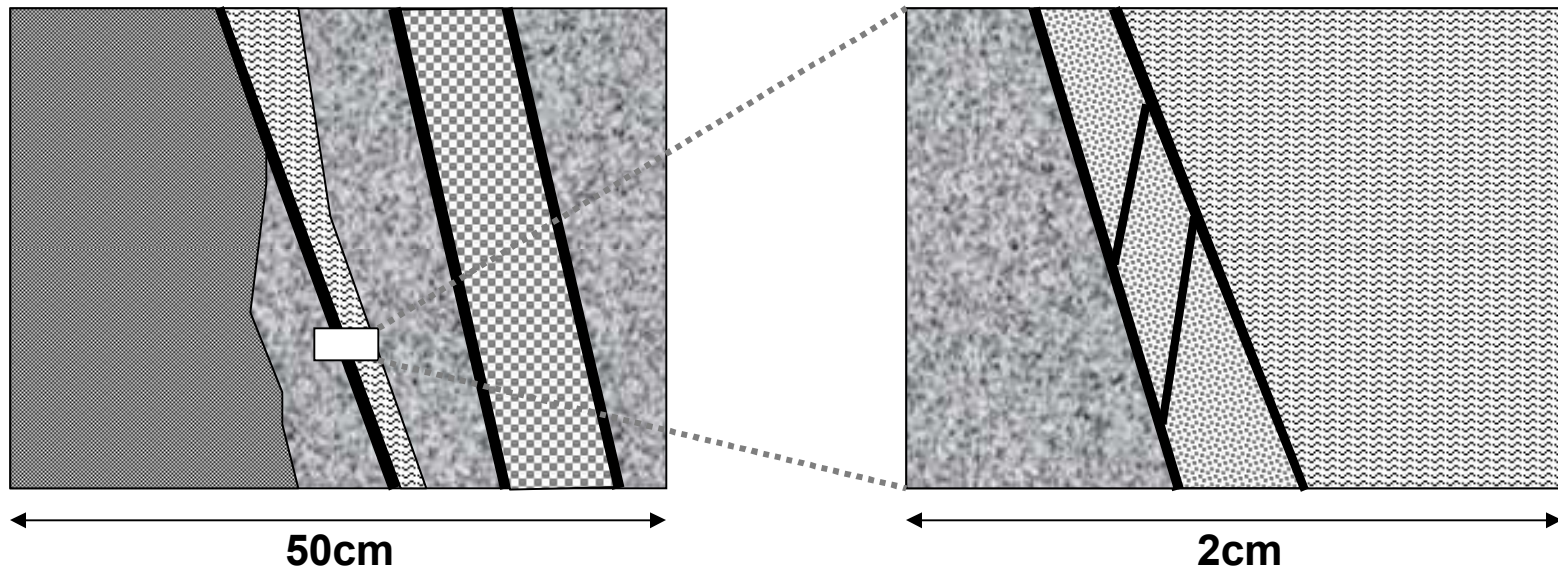


The Äspö Task Force on Modelling of Groundwater Flow and Transport of Solutes



Conceptual Model: Feature A

- Precambrian granites experienced episodic ductile and brittle deformation with hydrothermal mineralization



After Mazurek, et al., 2003, Jour. Contaminant Hydrology

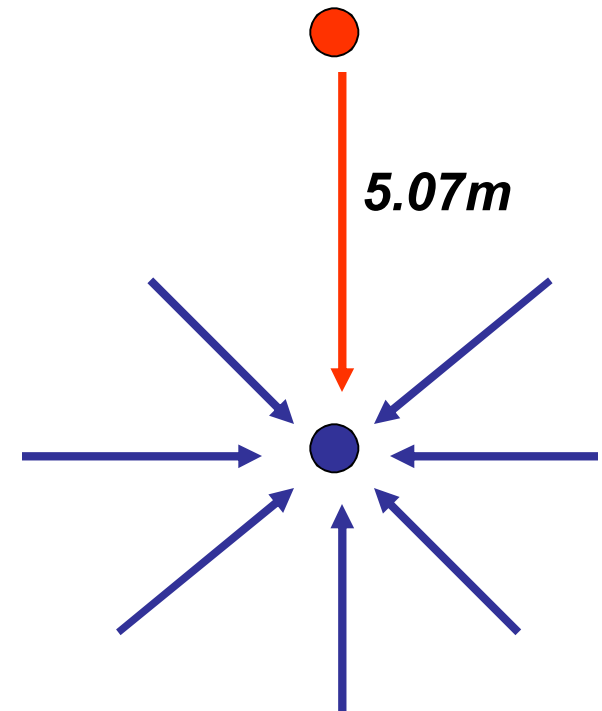
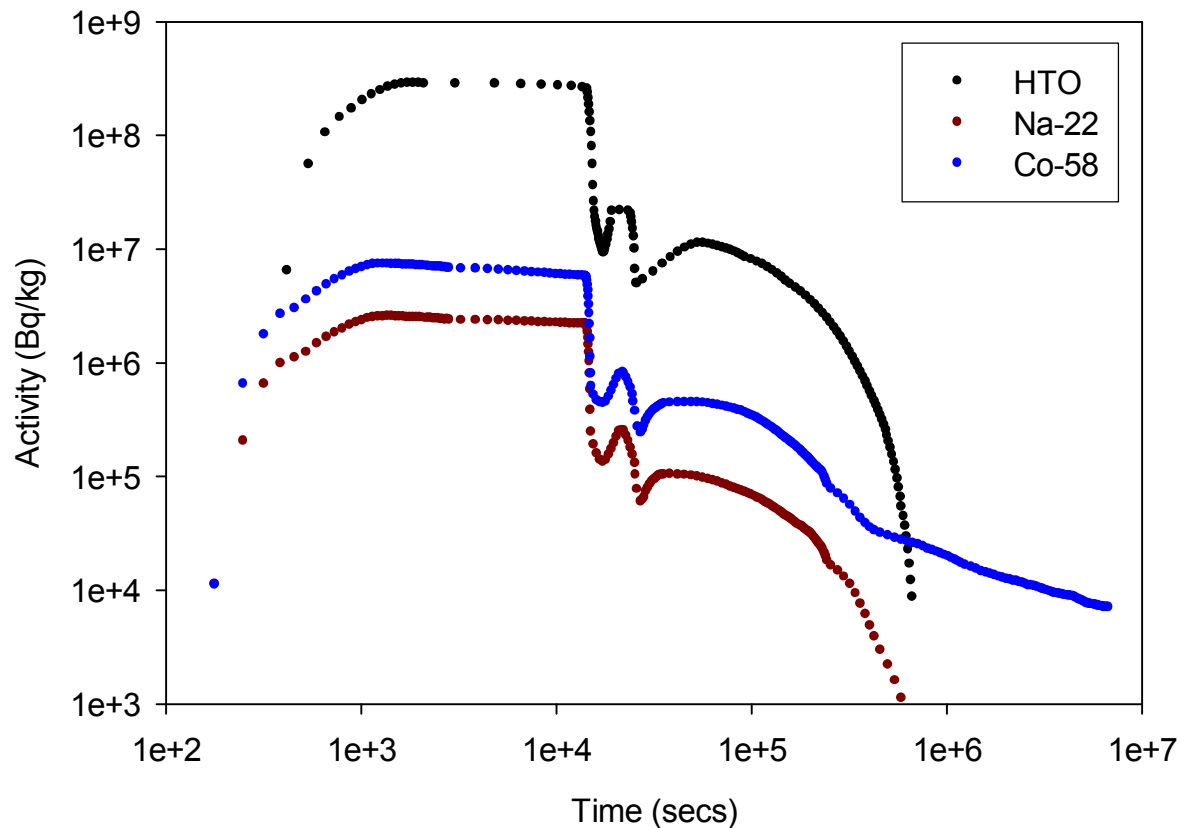
Experimental Setup

- Tracer testing in a single fracture zone (“Feature A”)
- Convergent flow system to a pumping well
- Injection well is 5 m from pumping well
- Multiple radionuclides with different levels of sorption
 - Tritiated water (HTO) *Non-sorbing*
 - Uranine
 - Na22 *Weakly to moderately sorbing*
 - Sr85
 - Rb86 *Strongly sorbing*
 - Co58



STT-1b Tracer Tests

Injection histories for three tracers – *Not a square wave*



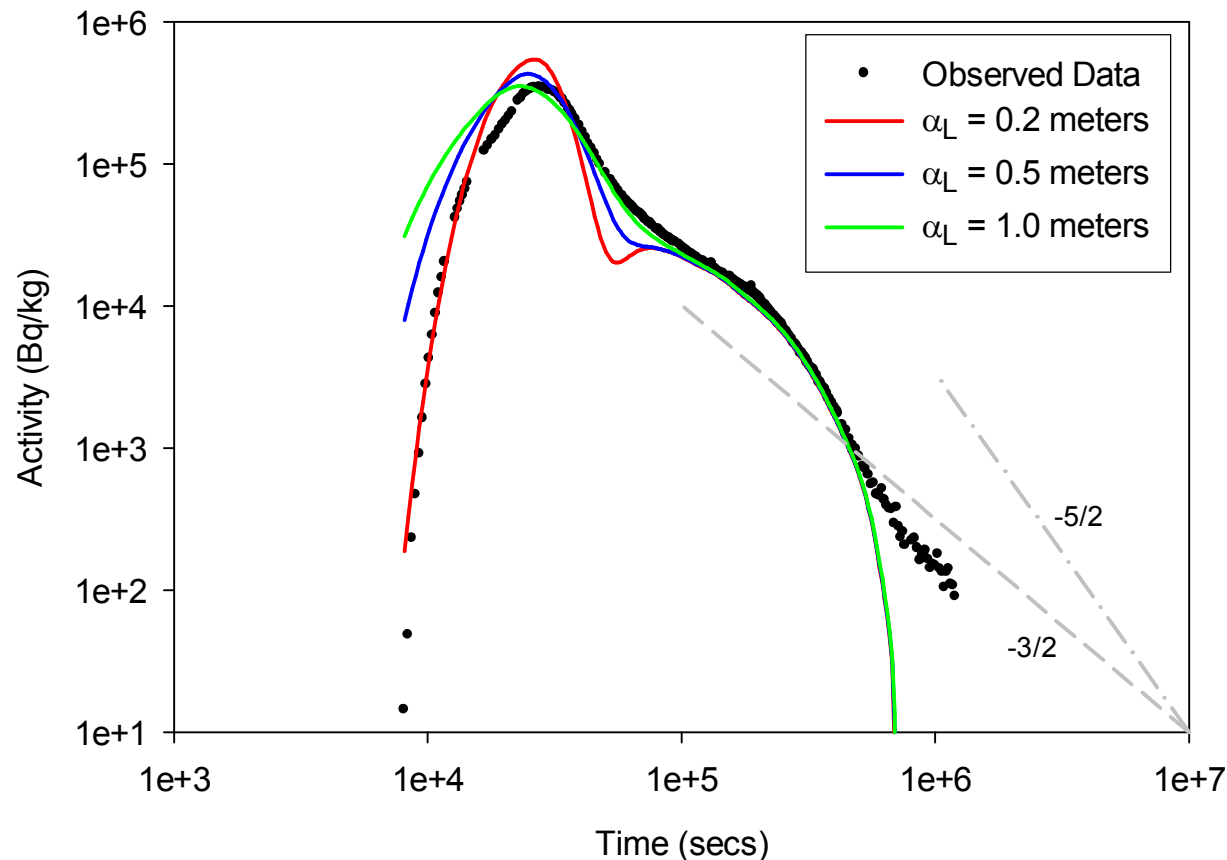
Modeling Approach

- **Start with modeling HTO as it is part of the water molecule and is non-sorbing**
 - Define all advective parameters from HTO data
- **Can breakthrough curves be modeled without mass transfer?**
- **Can breakthrough curves be modeled with a single rate of mass transfer?**
 - Predict other tracers using HTO parameters and laboratory data
- **Does consideration of multiple rates of mass transfer improve the models?**
- **Consistency with geologic conceptual model**



Single Porosity Model

Different values of dispersivity (4, 10 and 20 percent of transport distance) change fit to advective portion of breakthrough curve, but don't match late time data



Late-time data have a slope steeper than $-3/2$ (infinite capacity).

Late-time slope is closer to $-5/2$

Model fit with:

$$V_x = 2.76E-04 \text{ m/s}$$

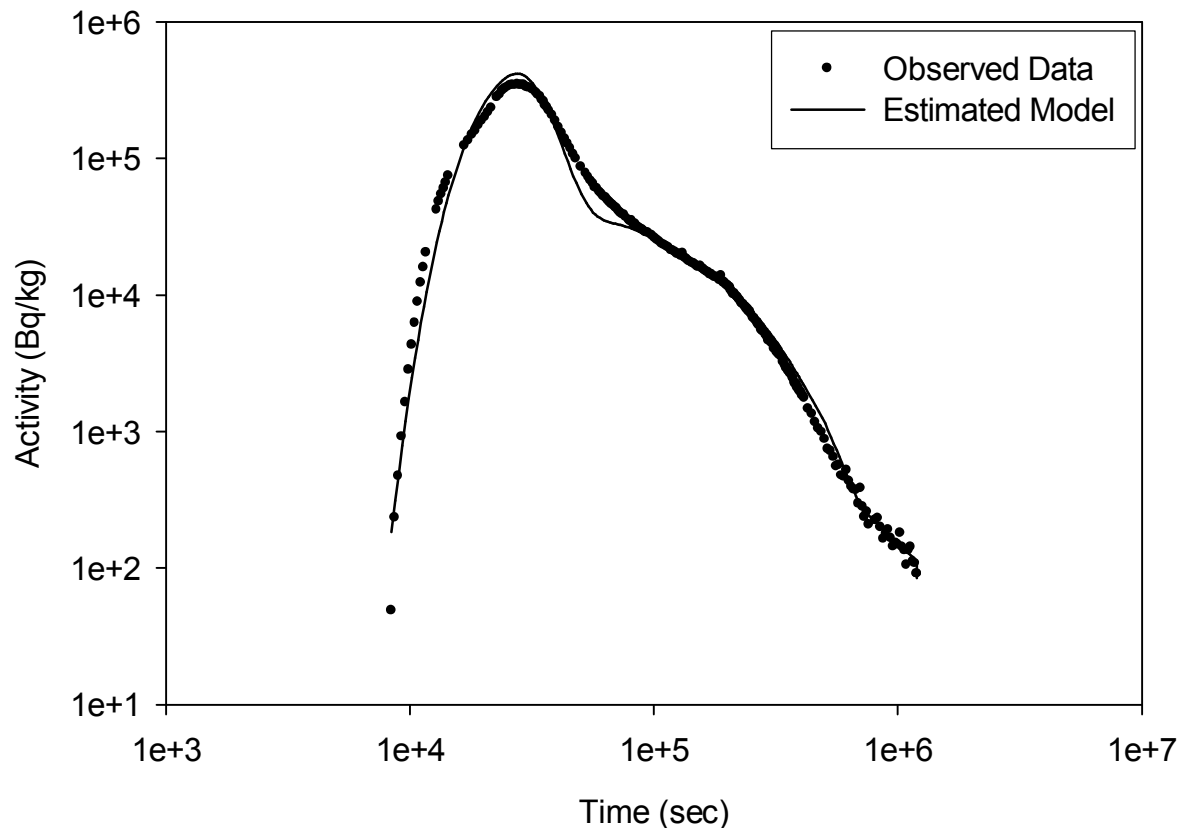
$$dilute = 427$$

$$\alpha_L = 0.2 \text{ m}$$

Single-Rate Mass-Transfer

Adding a single-rate of mass-transfer between the fracture and the matrix allows the model to fit the late time data

Also smoothes out misfits near peak and after peak



Model fit with:

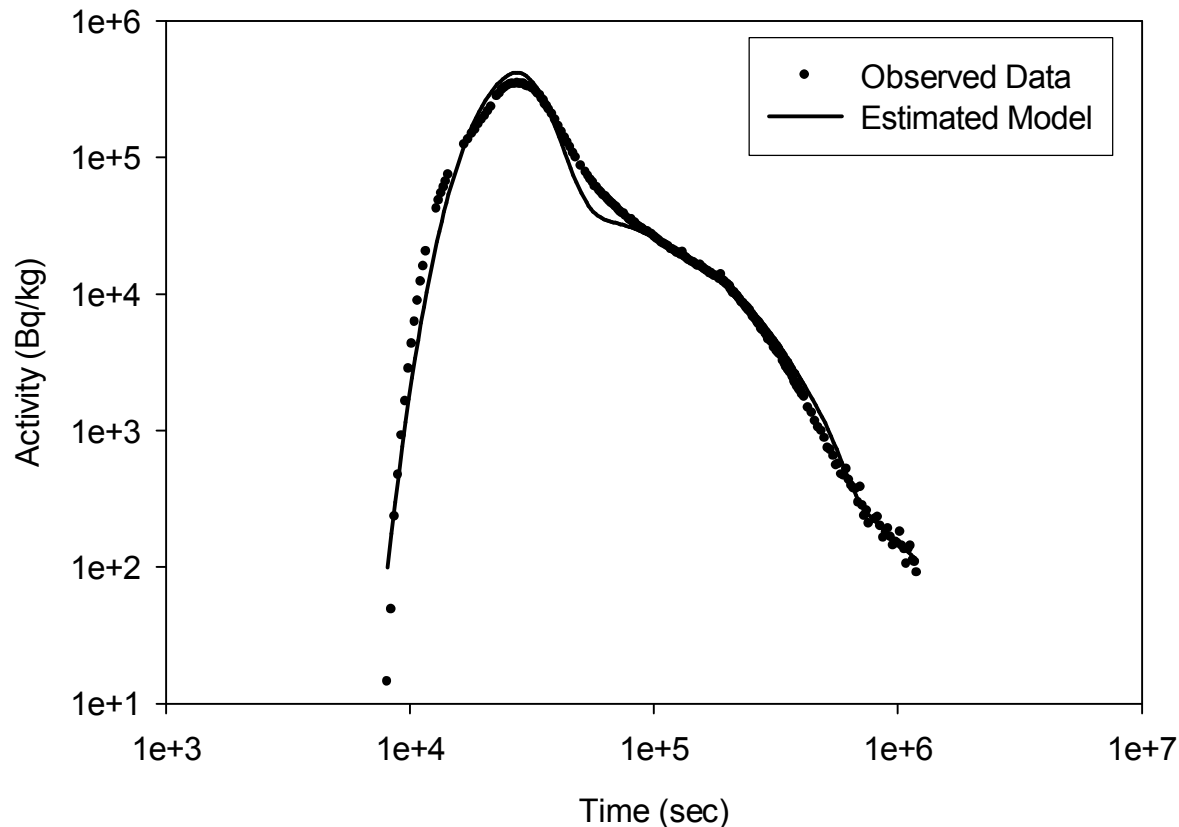
$$\beta_{tot} = 5.6$$

$$\mu = -16.0 \text{ 1/s}$$

Multirate Mass Transfer

Estimating: V_x , $dilute$, α_L , β_{tot} , μ , σ

Multi-Porosity Transport



Model fit with:

$$\beta_{tot} = 6.3$$

$$\mu = -16.3 \text{ 1/s}$$

$$\sigma = 0.4$$

Comparing Results

Parameters	Single-Rate	Multirate
V_x (m/s)	2.76E-04	2.76E-04
<i>dilute</i>	426.7	426.7
α_L (m)	0.2	0.2
B_{tot} (-)	5.6	6.3
μ (1/sec)	-16.0	-16.3
σ (1/sec)	0.0	0.4
<i>RMSE</i>	0.26	0.26

Advective-dispersive parameters are held constant for both models

Multi-porosity model has additional parameter, but no better fit to data!

$$RMSE = \sqrt{\frac{1}{N} \sum_1^N (\log_{10}(C_{obs}) - \log_{10}(C_{est}))^2}$$

Predict Other Tracer Tests

Advective parameters: V_x , *dilute* and α_L are fixed for all tracers

Additionally, β_{tot} , the ratio between porosities is known

$$\beta_{tot} = \frac{\phi_{im} R_{im}}{\phi_m R_m}$$

The diffusion rate coefficient is a function of the ability of the tracer to diffuse into and adsorb to the matrix

$$\mu = \frac{D_{aq} \tau}{l^2 R_{im}}$$

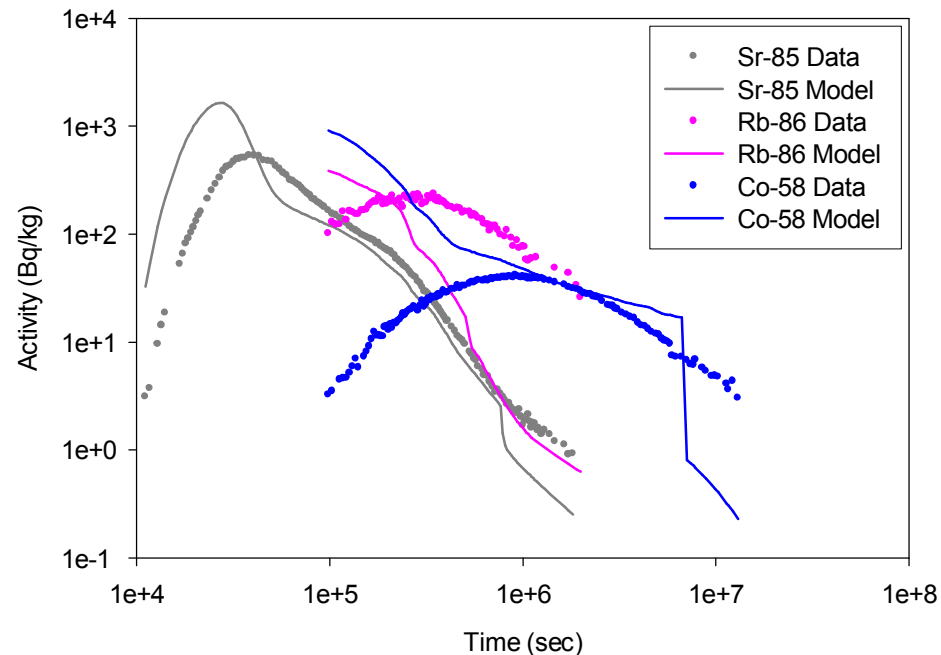
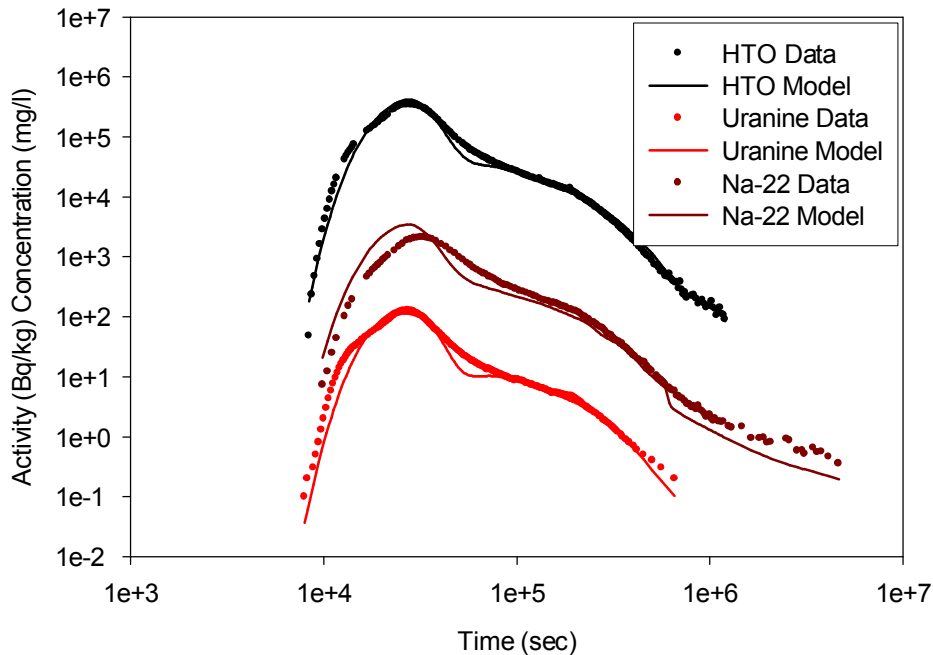
The capacity coefficient is a function of the sorption properties of the fracture wall and matrix

$$\beta_{tot} = \frac{\phi_{im} R_{im}}{\phi_m R_m}$$



Prediction Results

Combining HTO results with laboratory data



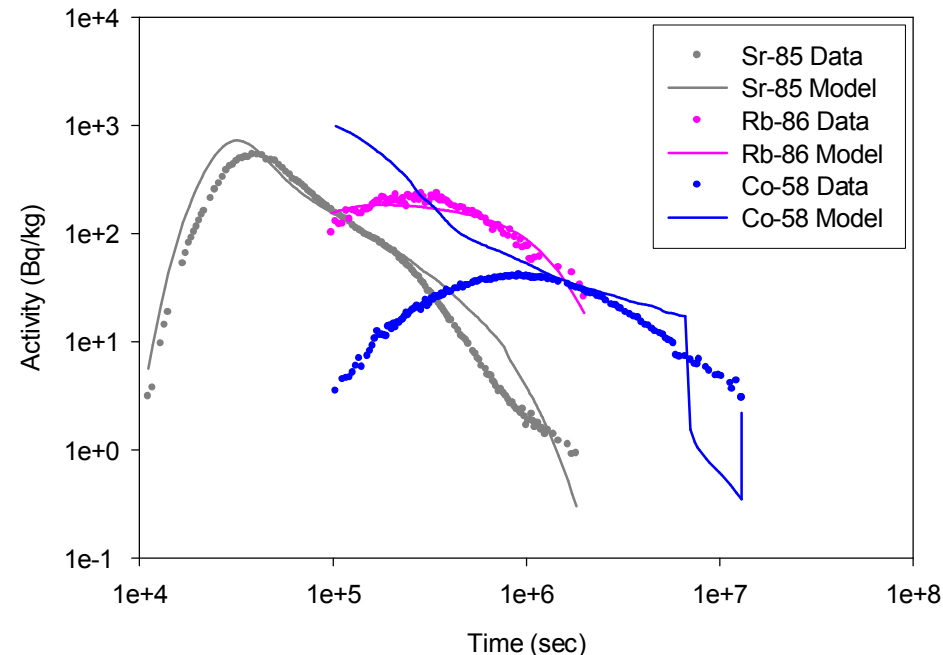
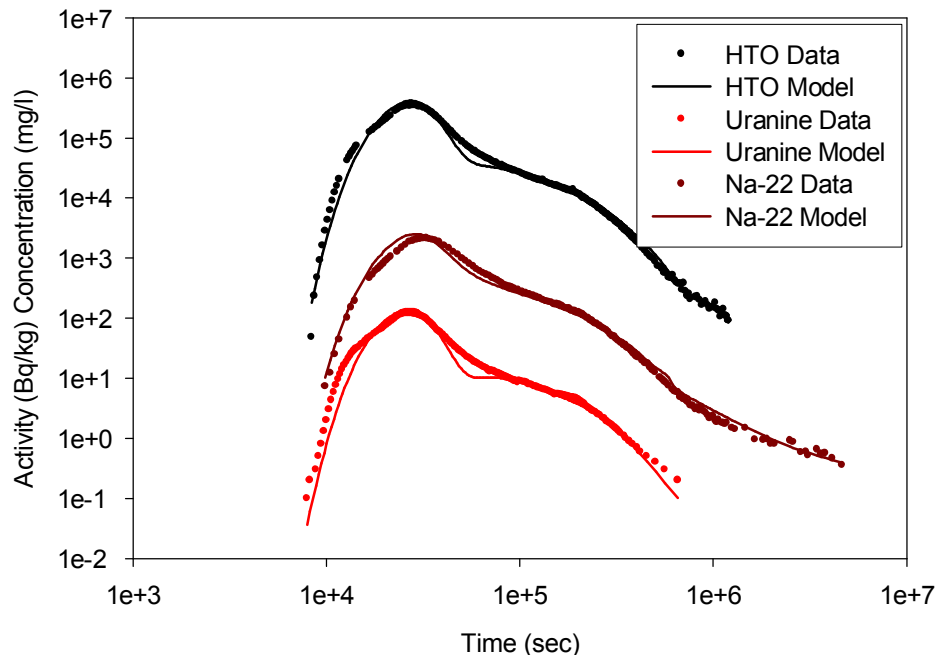
Results are OK for tracers without sorption, but are not accurate for tracers with significant sorption

Wrong parameters (lab data are incorrect)? and/or Wrong processes (Single-rate model is incorrect)?



Single-Rate Estimation Results

Estimating two parameters: mass-transfer rate coefficient, μ , and total capacity, β_{tot}



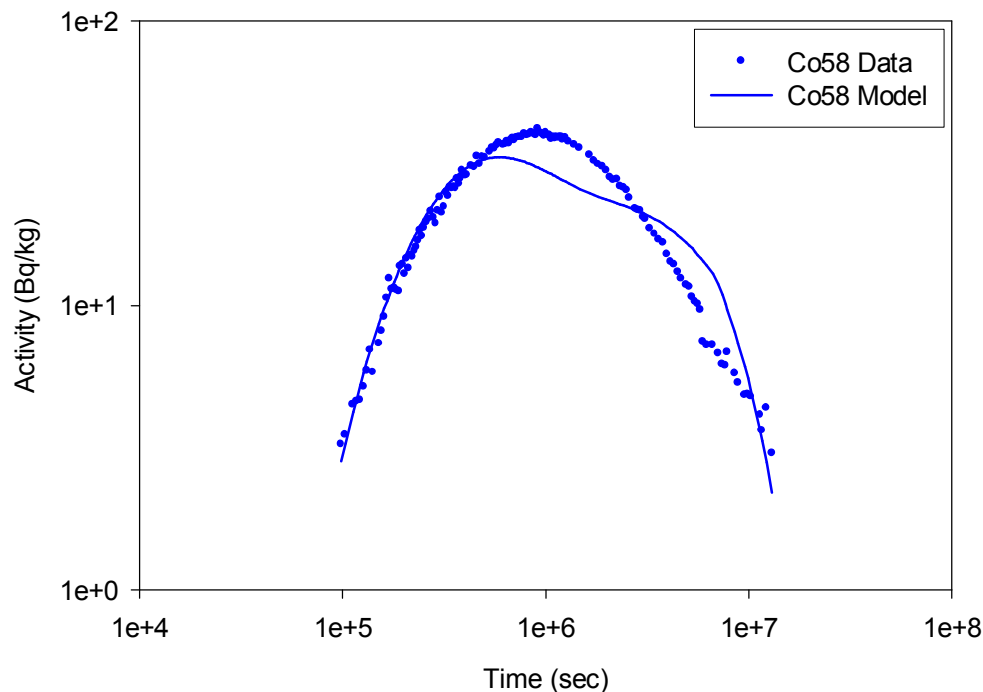
Estimations are considerably closer to observed data than were predictions, especially for more strongly sorbing tracers

Co-58 is still a problem



Sandia National Laboratories

Revised Co58 Estimation



Two parameter estimations of Co58 results start with activities much higher than observed

Results are indicative of non-equilibrium sorption

Estimate 3 parameters, include *dilute*, to account for less than expected mass recovery

$$dilute = \frac{Q_{pump}}{Q_{inject}} \cdot \frac{1}{RMF}$$



Comparing Single-Rate Models

K_d Values are taken from batch testing in the laboratory for predictions

K_d Values are obtained from estimates of β_{tot} from estimating tracer test breakthrough curves

Tracer	Laboratory Kd	Tracer Test Kd
HTO	0.0E+00	0.0E+00
Uranine	0.0E+00	-6.1E-05
Na22	7.0E-06	1.3E-04
Sr85	2.4E-05	1.3E-05
Rb86	3.0E-03	4.4E-04
Co58	1.7E-02	2.6E-03

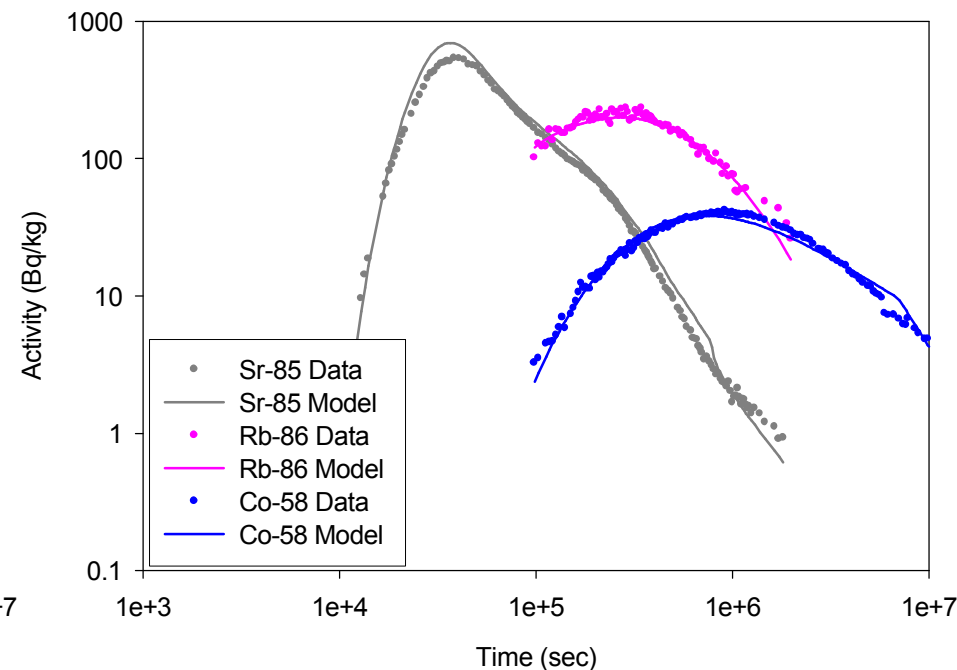
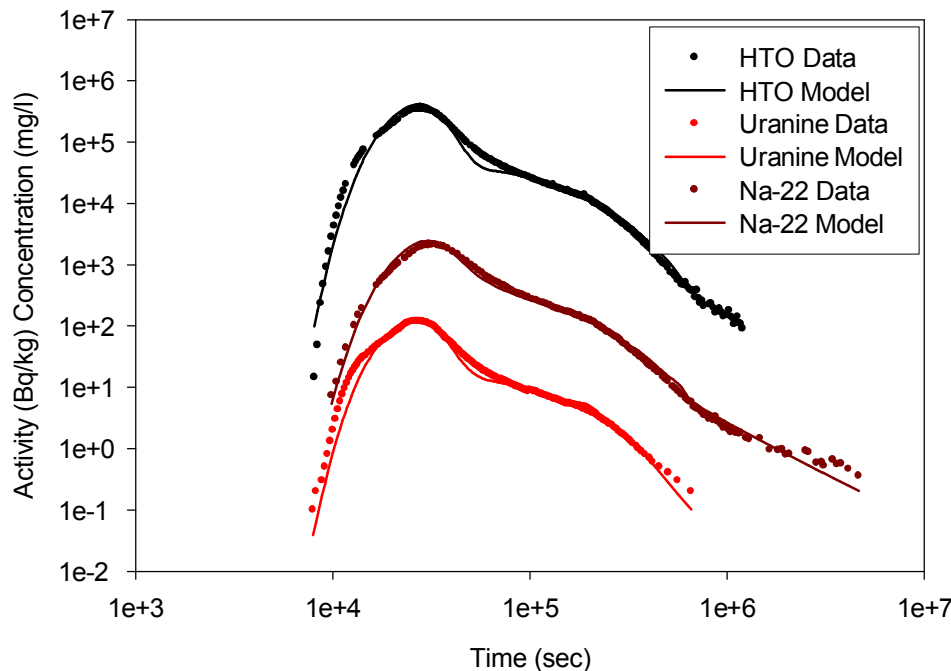
Negative K_d indicates aversion to matrix rock – may be anion exclusion effect

For more strongly sorbing tracers, field estimates are a factor of 2 to 6 lower than lab estimates



Multirate Estimation

Multirate model is used to fit data. μ , σ and β_{tot} are estimated, V_x , *dilute*, and α_L are held constant,



Necessary to also fit *dilute* for Co58 curve

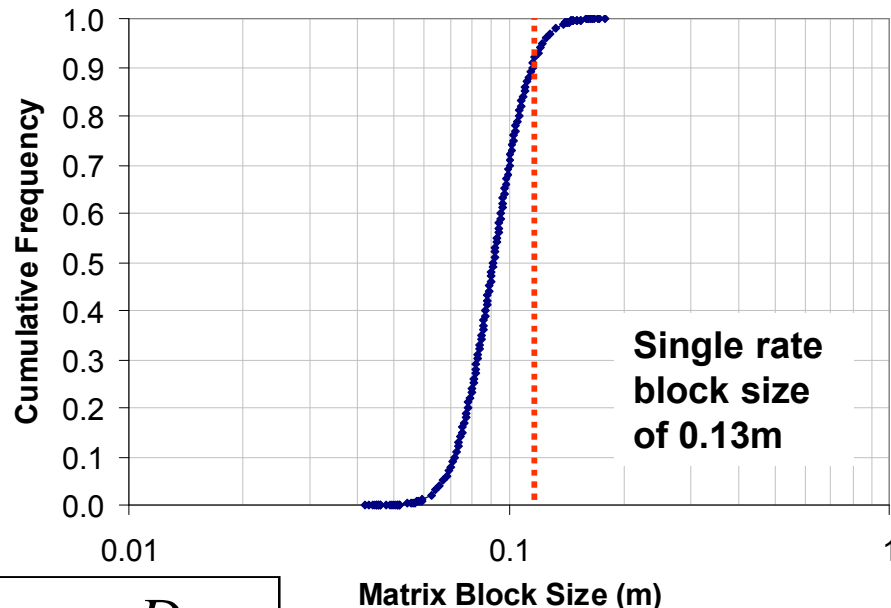
Multirate estimates are better, but are they a significant improvement?

F-test shows all improvements are significant with exception of HTO



Fit to Conceptual Model

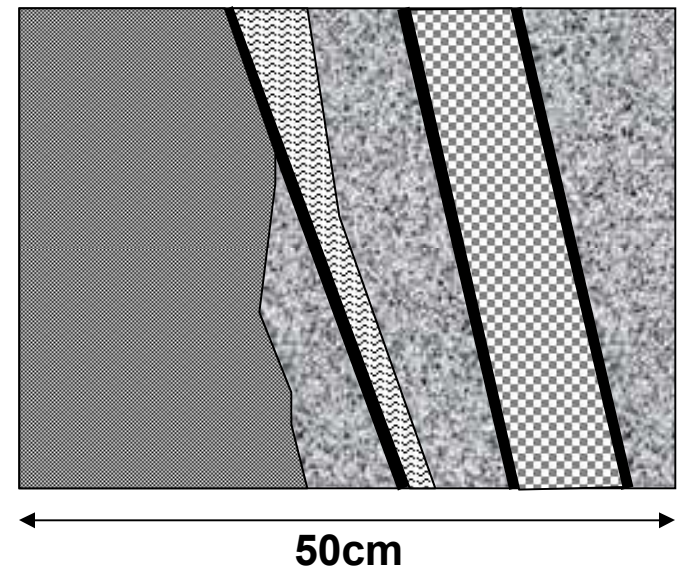
Distribution of mass-transfer rates can be converted to matrix block size distributions



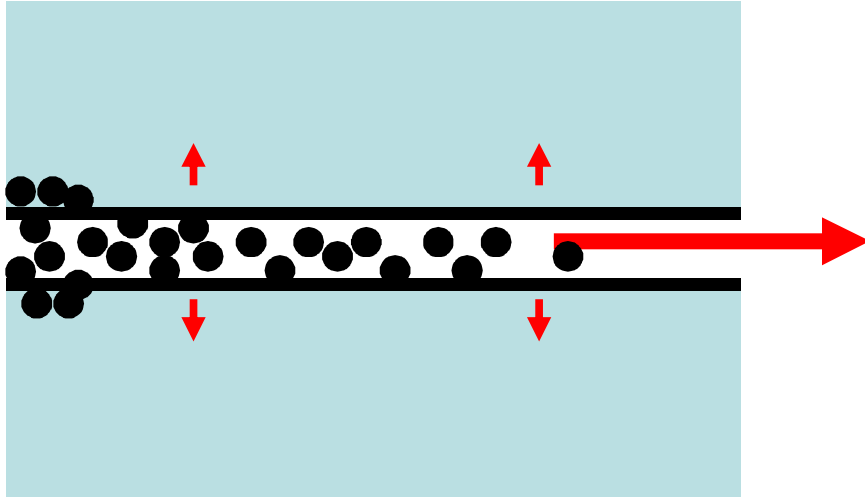
$$\alpha_i = \frac{D_{aq}\tau}{l^2 R_{im}}$$



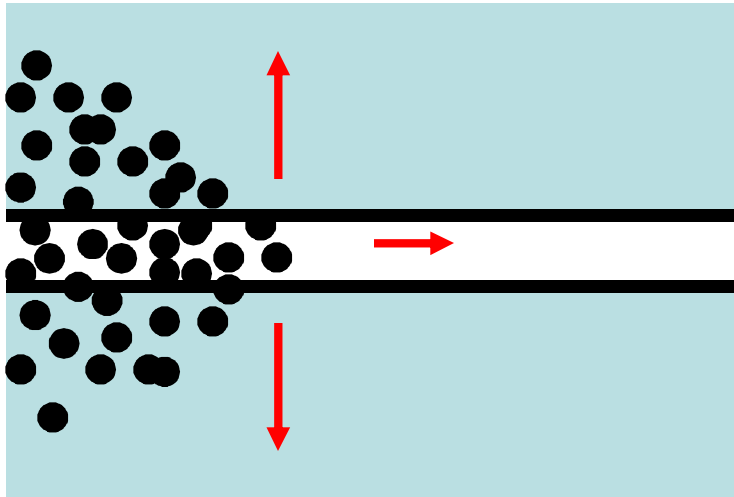
Block size distribution fits conceptual model of materials within Feature A



Tracer Testing: Relative Rates



Advection \gg Diffusion
Low Damkohler Number
Small fraction of matrix
is saturated with solute



Diffusion Rate \gg
Advection
High Damkohler Number
Large Fraction of matrix
is saturated with solute

What Can the Test See?

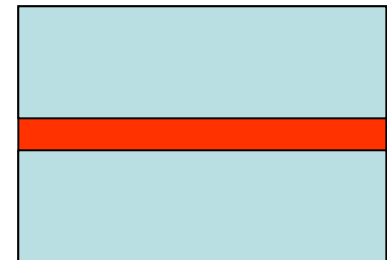
Damkohler number provides ratio of mass-transfer rate to advective rate

$$DaI = 3\alpha_i(1 + \beta_i) \frac{LR_m}{v_x}$$

$DaI \gg 1.0$ indicates local equilibrium behavior



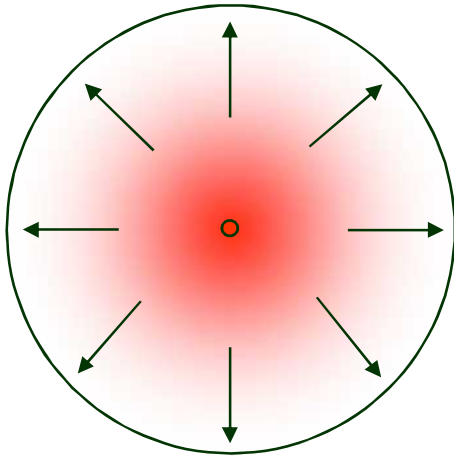
$DaI \ll 1.0$ indicates single porosity transport



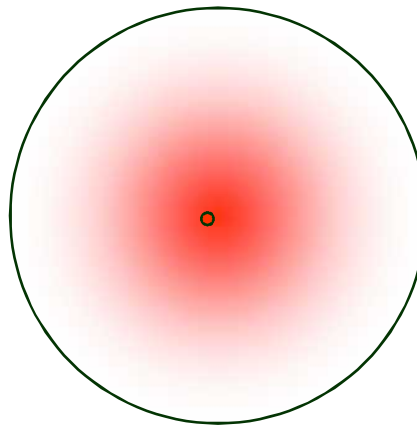
Single-Well Injection-Withdrawal

Single-Well Injection Withdrawal Tests (aka “huff-puff”, “push-pull”)

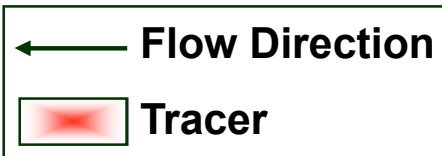
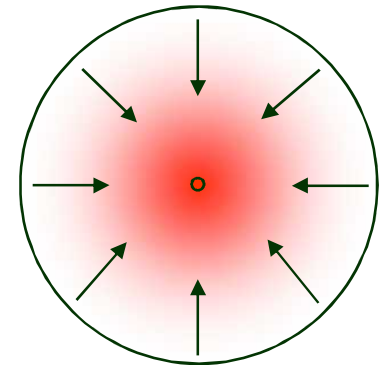
Injection



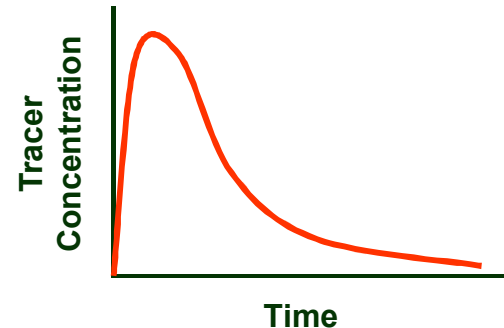
Rest Period



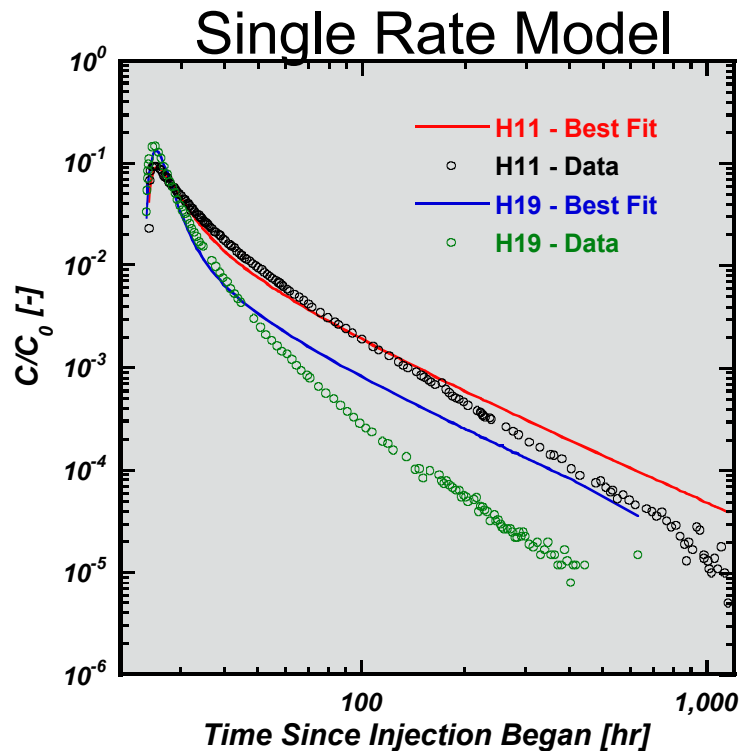
Withdrawal



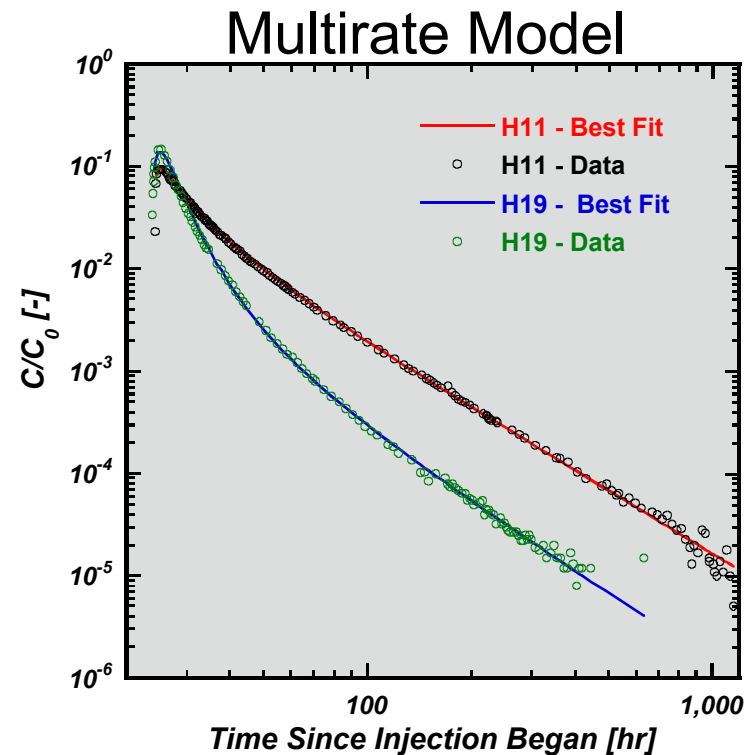
Recovery Curve



WIPP Example: Culebra Tracer Tests



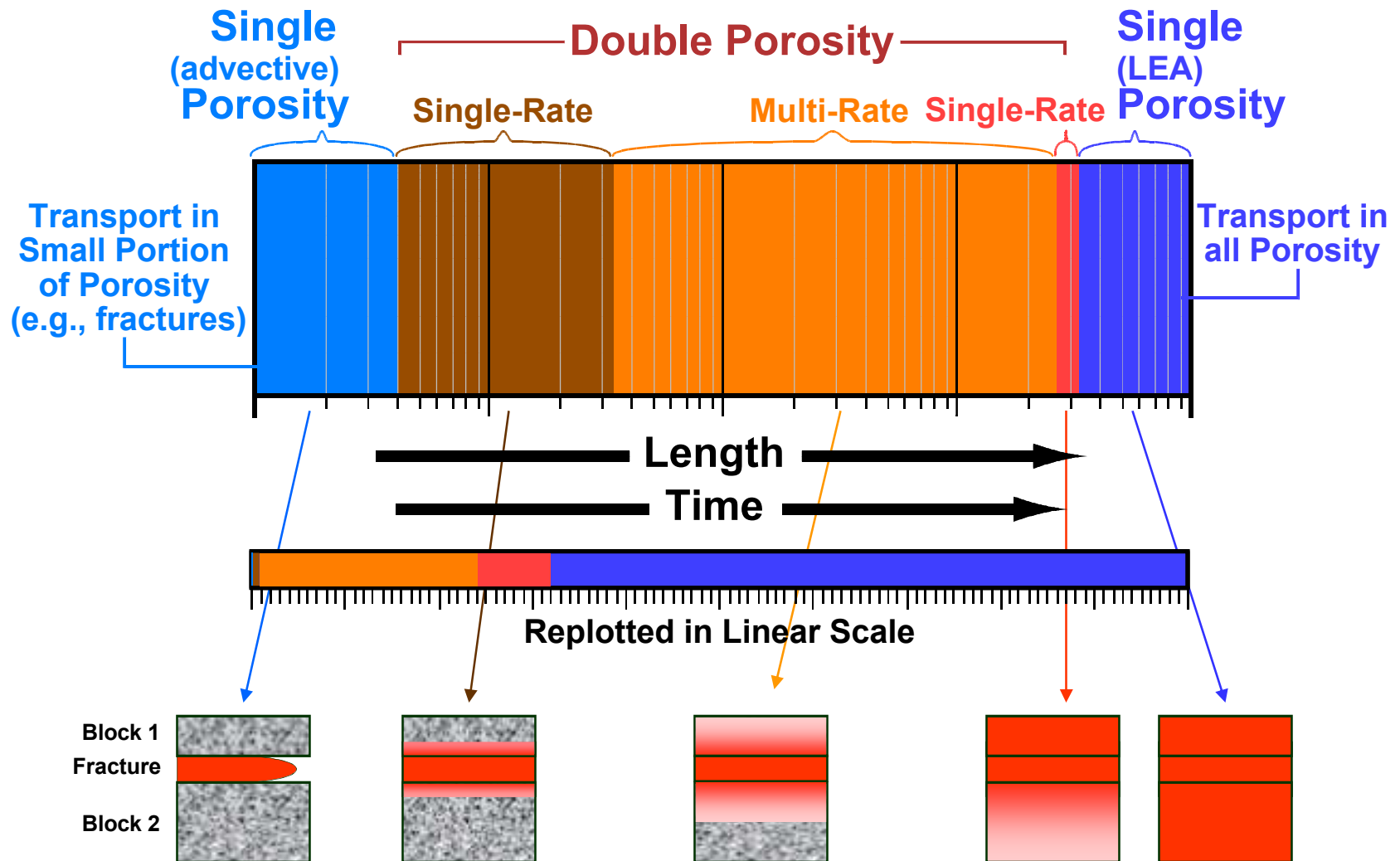
Cannot Capture Tailing Behavior



Provides Excellent Fits Throughout Time Range



Beyond the Tracer Test Scale



Conclusions

- **Signature of mass-transfer processes in tracer test results is unique from dispersive processes**
- **For Aspo tracer test results:**
 - Dispersion alone cannot account for results
 - Single-rate of mass transfer applies to non-sorbing and moderately sorbing tracers
 - K_d values from laboratory are generally too high to predict field results
 - Multiple rate mass transfer model required for strongly-sorbing tracers



Conclusions (Cont.)

- **Aspo tracer test results (Cont.):**
 - **Multirate mass-transfer model provides significantly better fits to tracer data**
 - **Multirate results are consistent with conceptual model of geologic materials within Feature A**



Additional Information

- McKenna, S.A. and J.-O. Selroos, 2004, Constraining Performance Assessment Models with Tracer Test Results: A Comparison of Two Conceptual Models, *Hydrogeology Journal*, 12 (3), pp. 243-256
- Altman, S.J., L.C. Meigs, T. L. Jones and S.A. McKenna, 2002, Controls of Mass-Recovery Rates in Single-Well Injection-Withdrawal Tracer Tests with a Single-Porosity Heterogeneous Conceptualization, *Water Resources Research*, Vol. 38, No. 7,
- Haggerty, R., S. W. Fleming, L.C. Meigs and S.A. McKenna, 2001, Tracer Tests in a Fractured Dolomite. 2. Analysis of Mass Transfer in Single-Well Injection Withdrawal Tests, *Water Resour. Res.*, 37 (5), pp. 1129-1142.
- McKenna, S.A. and L.C. Meigs, and R. Haggerty, 2001, Tracer Tests in a Fractured Dolomite 3. Double Porosity, Multiple-Rate Mass-Transfer Processes in Two-Well Convergent Flow Tests, *Water Resour. Res.*, 37(5), pp. 1143-1154.
- Haggerty, R., S. A. McKenna, and L. C. Meigs, 2000, On the late-time behavior of tracer test breakthrough curves, *Water Resour. Res.*, 36(12), pp. 3467-3479.



BACKUP SLIDES



Quantify Small-Scale Diffusivity

- **Rock samples with fault gouge, altered and unaltered diortie from Kamaishi Mine in northern Japan**
- **What is the variability in diffusivity values in a small sample?**
- **Is there a relationship between porosity and diffusivity?**



Imaging Diffusion

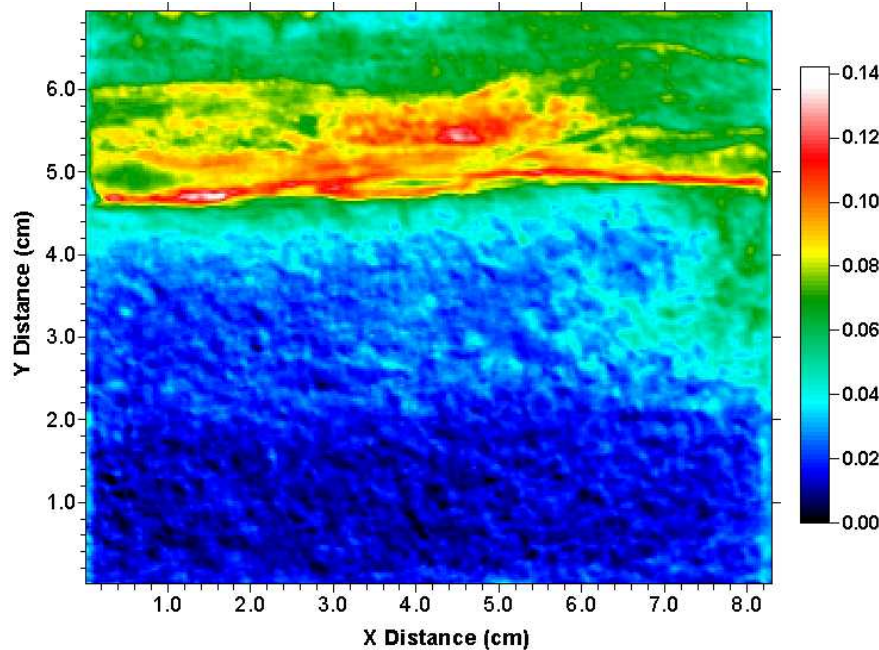
- **X-ray adsorption imaging technique developed at Sandia:**
 - *Tidwell and Glass, 1997; Water Resour. Research*
- **Approach**
 - Sample is placed between X-ray source and film
 - Iodide tracer adsorbs X-rays (linear relation between adsorption and iodide concentration)
 - X-ray film is developed and digitized
 - Difference between dry and saturated images gives porosity



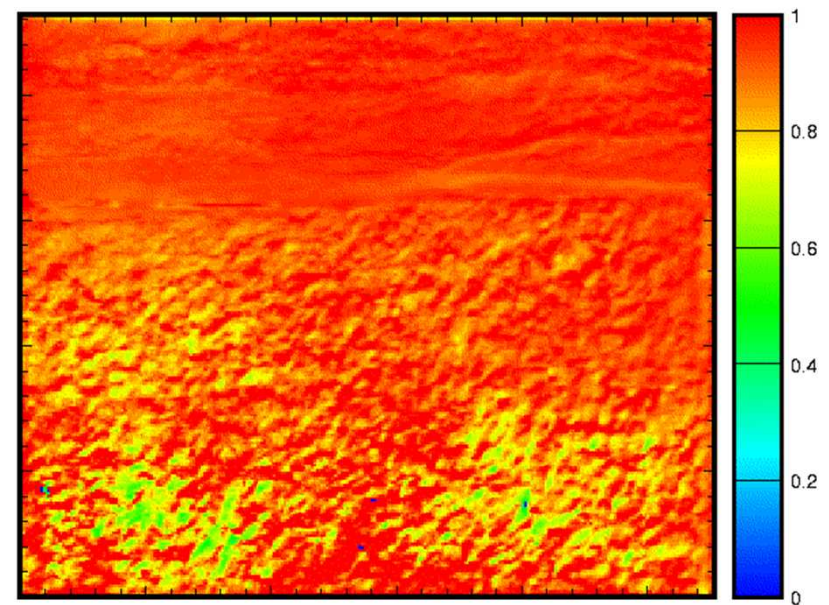
Laboratory Evidence

X-ray Transmission imaging of KI tracer in fracture filling material from granites at the Kamaishi Mine in Japan

Porosity



C/Co

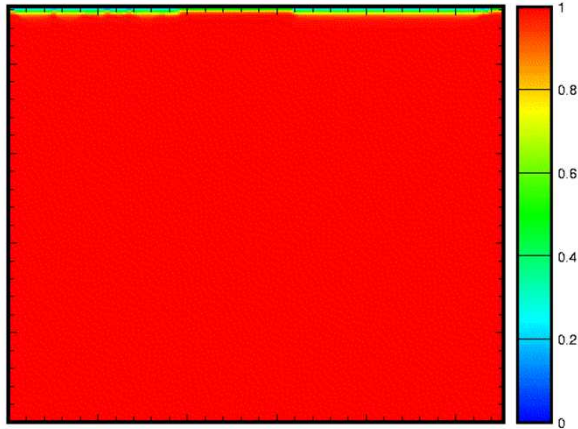


*Images out to 10 days with
log spacing of times*

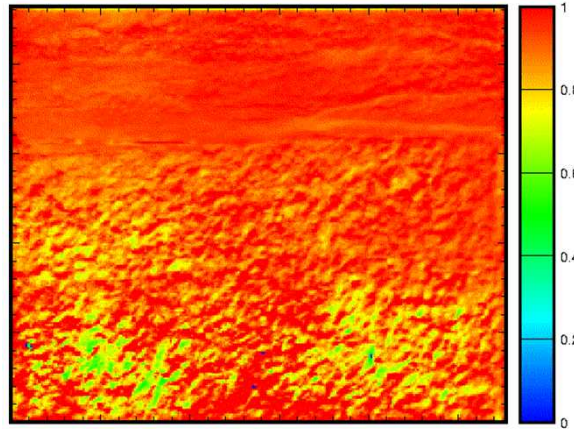


KC1c-FF Results Animations

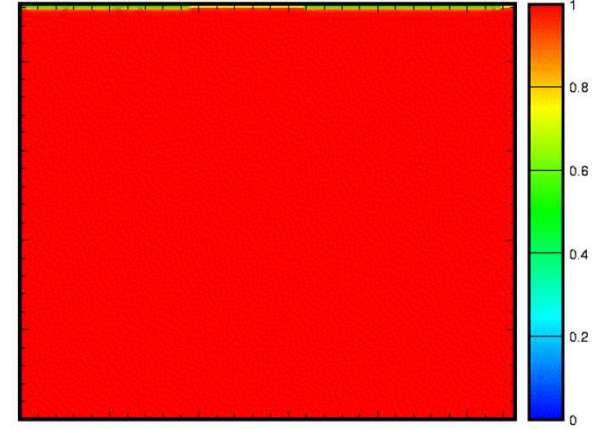
Optimized Porosity Zonation



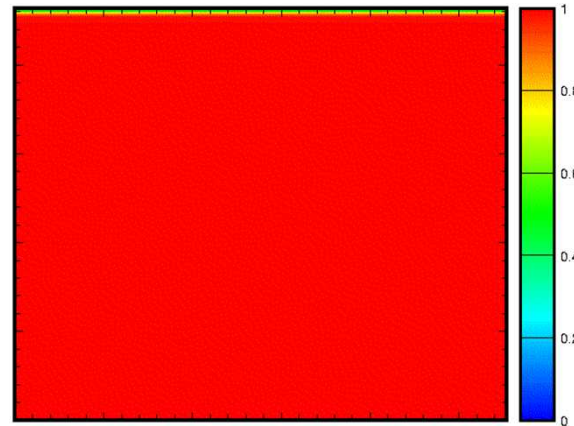
Experimental Data



Initial Porosity Zonation

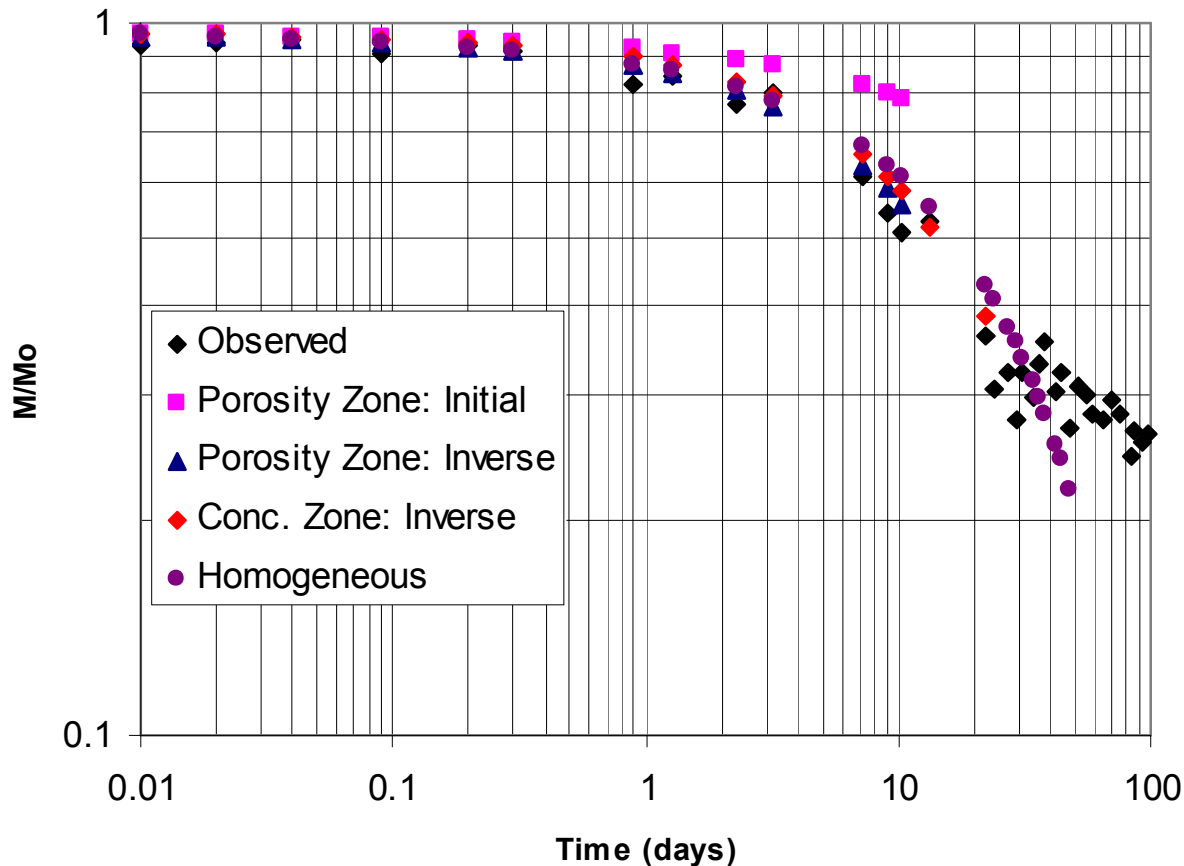


Concentration Zonation



Best fit to observed data is provided by the concentration zonation

KC1c FF Results



All optimized solutions improve on initial estimates

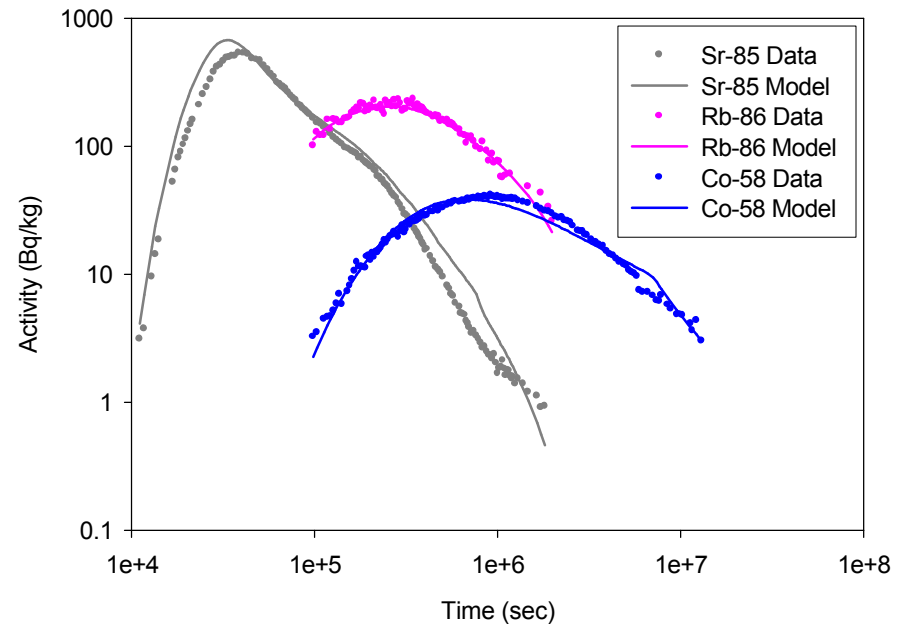
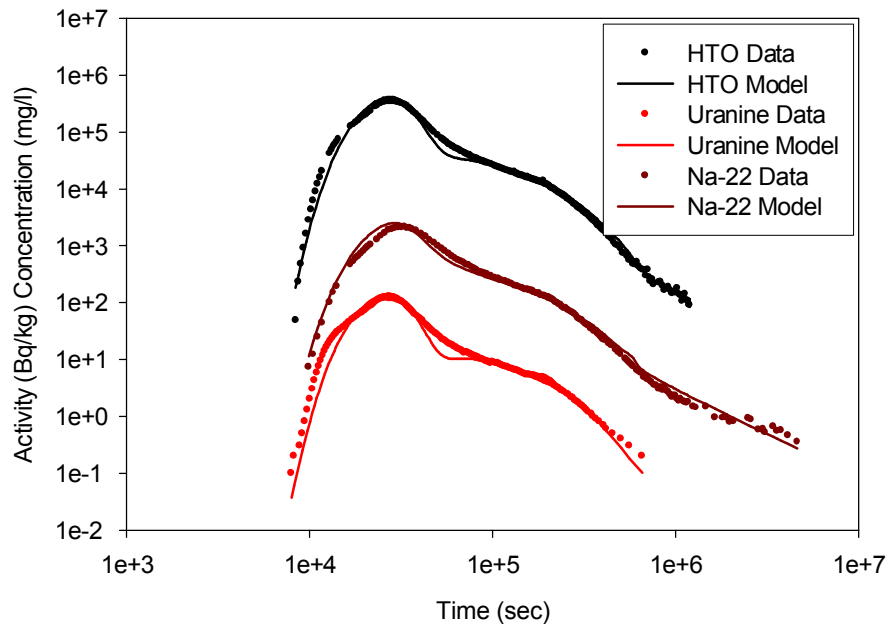
Change in slope of data is noisy, could possible be real due to very low De in low porosity material





Double Porosity Fits

Model fits with single mass-transfer rate and no surface sorption
SPHERICAL FITS

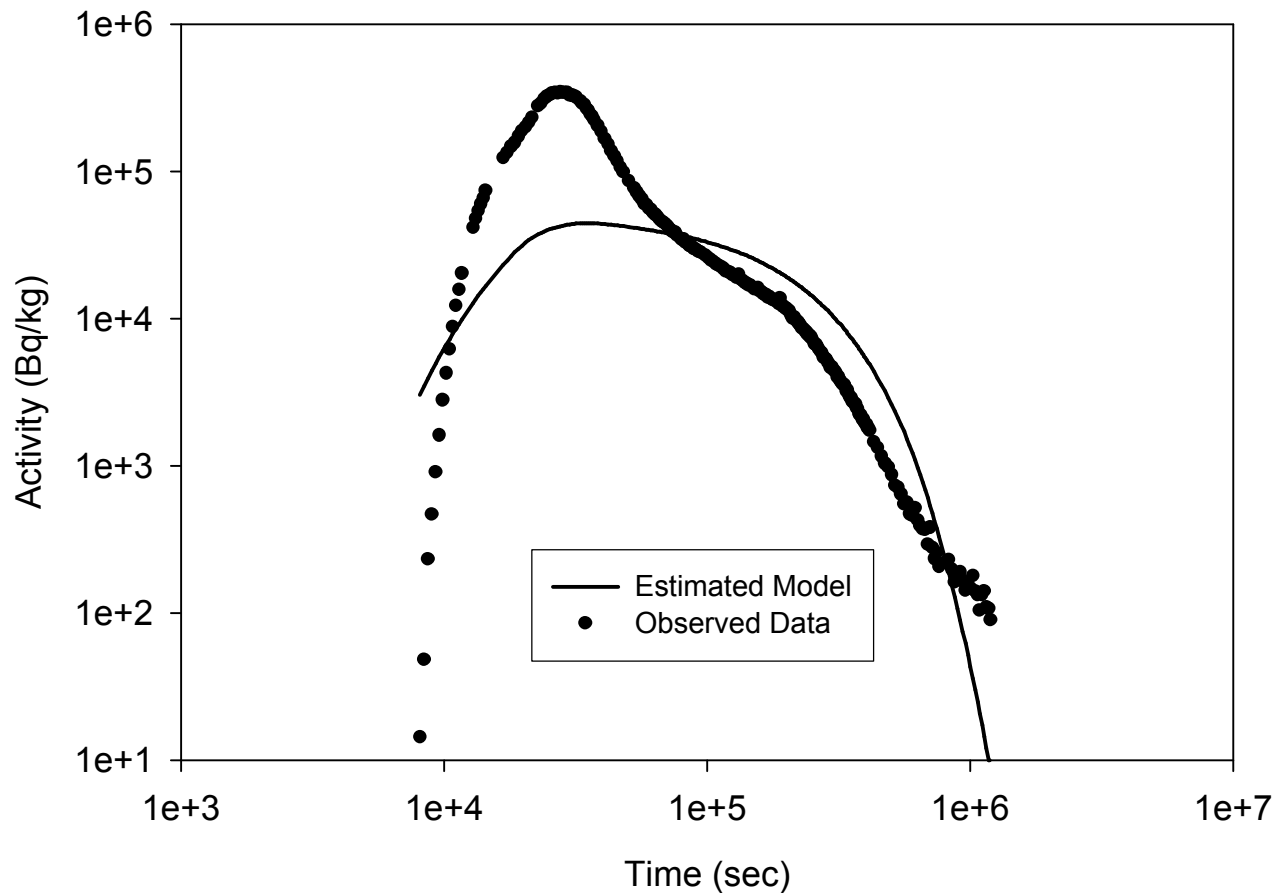


Model has difficulty with Uranine, Sr-85 and Co-58

Single-Porosity Model

Estimating: V_x , $dilute$, α_L

Single Porosity Transport



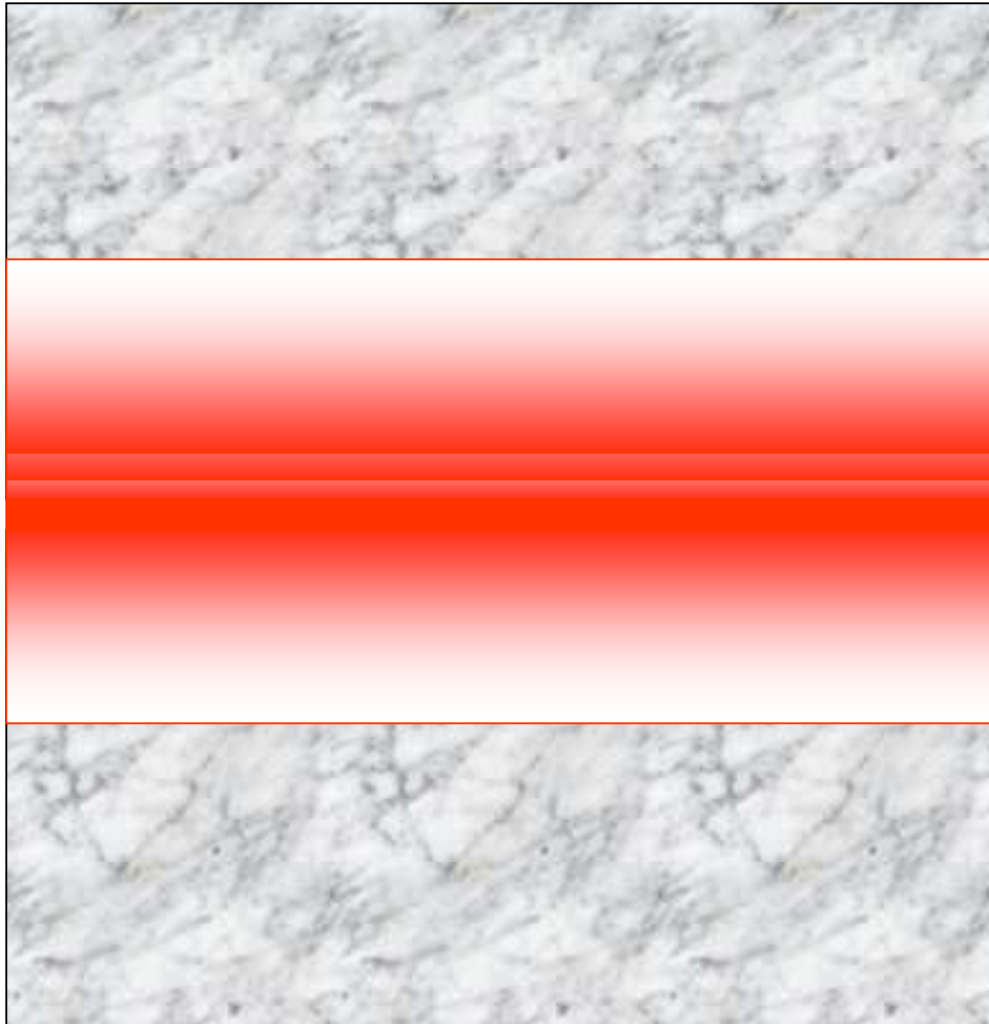
Comparing Results

Parameters	Single Porosity	Multi-Porosity
V_x (m/s)	6.55E-05	2.76E-04
<i>dilute</i>	644.7	426.7
α_L (m)	6.0	0.2
B_{tot} (-)	NA	6.30
μ (1/sec)	NA	-16.3
σ (1/sec)	NA	0.37
<i>RMSE</i>	1.15	0.26

$$RMSE = \sqrt{\frac{1}{N} \sum_1^N (C_{obs} - C_{est})^2}$$



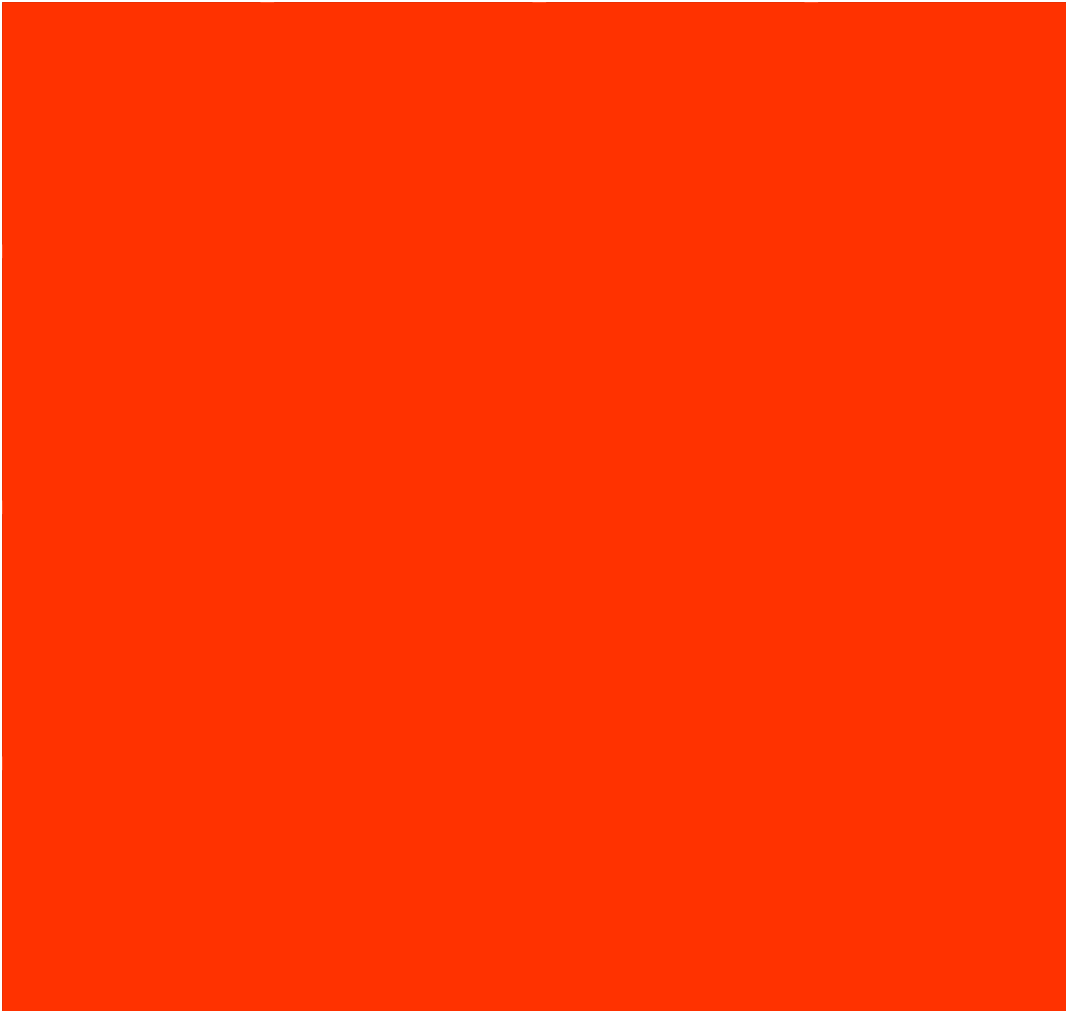
Matrix Block Size



Diffusion into an infinite medium means that the concentration front does not encounter any boundary conditions that limit the rate of diffusion

The fracture surface area to matrix volume ratio is small

Matrix Block Size



Diffusion into a finite medium means that the concentration front does encounter boundary conditions that limit the rate of diffusion

The fracture surface area to matrix volume ratio is relatively larger



Culebra Dolomite

