

Growth and Lipid Measurements Towards Modeling of *Dunaliella salina*

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Problem

Why biofuels?

- Current sources of energy are in decline, harmful to the environment, and often obtained from foreign suppliers.
- To reduce green house gasses, climate change and our dependence on foreign oil we need alternative clean and domestic energy sources.
- Algae-based biofuels are a promising component to a long-term renewable energy solution.

Why Algae?

- Algae can be engineered or stressed to produce large quantities of oil with favorable characteristics for biodiesel.
- Algae can be grown in waste/brackish/sea water, reducing the impact on fresh water supplies.
- Algae mitigate atmospheric CO₂.
- Algae can be grown on non-arable land, decreasing the impact on the food supply.
- Algae growth and harvesting still require much optimization to reduce the cost of oil production and improve efficiency.

• How can we easily optimize algae growth and lipid production for different environmental conditions?

• What bioreactor designs yield the best growth efficiencies?

• What types of algae works best a different times of years or different locations?

Need a realistic model

- We need to be able to optimize algae growth and lipid production in large commercial scale systems.
- It is too time consuming and expensive to test various solutions on a commercial scale.
- A computational model facilitates faster and cheaper optimization.
- However, the necessary data are lacking to create the needed constitutive relations for algae growth and lipid production.

Approach

Multi-factorial Measurements

- Measure effect of light intensity, temperature and salinity on growth multiple key marine algal species
- Use in-situ measurement methods and parallel growth to reduce time needed

Constitutive Relations

- Determine relationships between environmental variables and growth
- Apply to algae growth model

Photobioreactor Models

- Develop model for closed photobioreactor systems
- Expand model for marine algal species with salinity dependence
- Add lipid production to model

Measurement Techniques

Algae Selection:

- Marine, triacylglycerol (TAG) producing, readily available
- Dunaliella salina*, *Chlorella sorokiniana*, *Nannochloropsis oculata*, *Nitzschia frustulum*

Factors:

- Sample 4 salinities, 3 light intensities, 4 temperatures

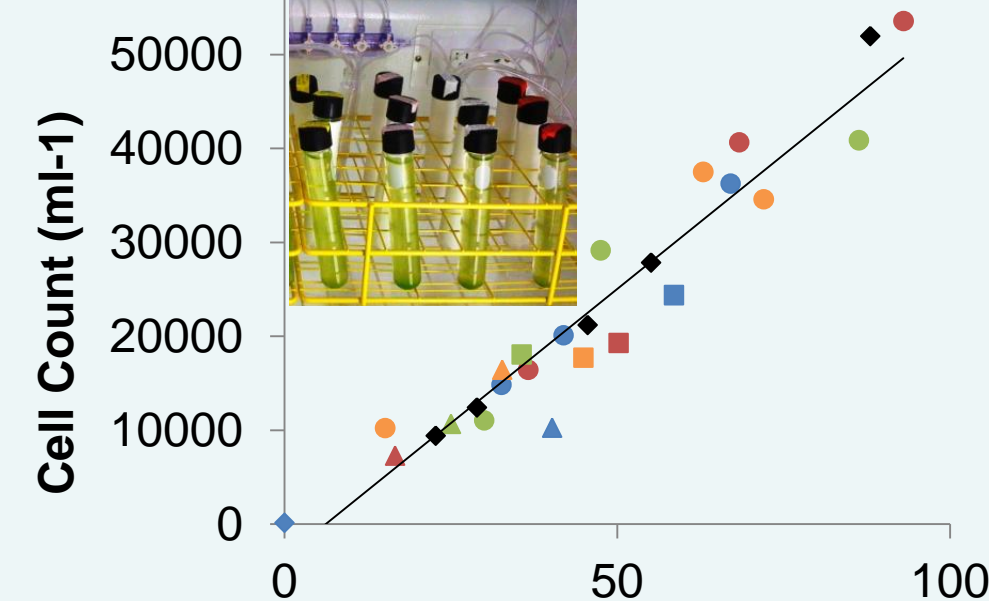
Growth:

- Measure chlorophyll a fluorescence
- Excite at ~440 nm, emit at ~670 nm
- Calibrate chlorophyll fluorescence with known standards of chlorophyll concentration
- Calibrate chlorophyll concentration with cell counter for each algae species

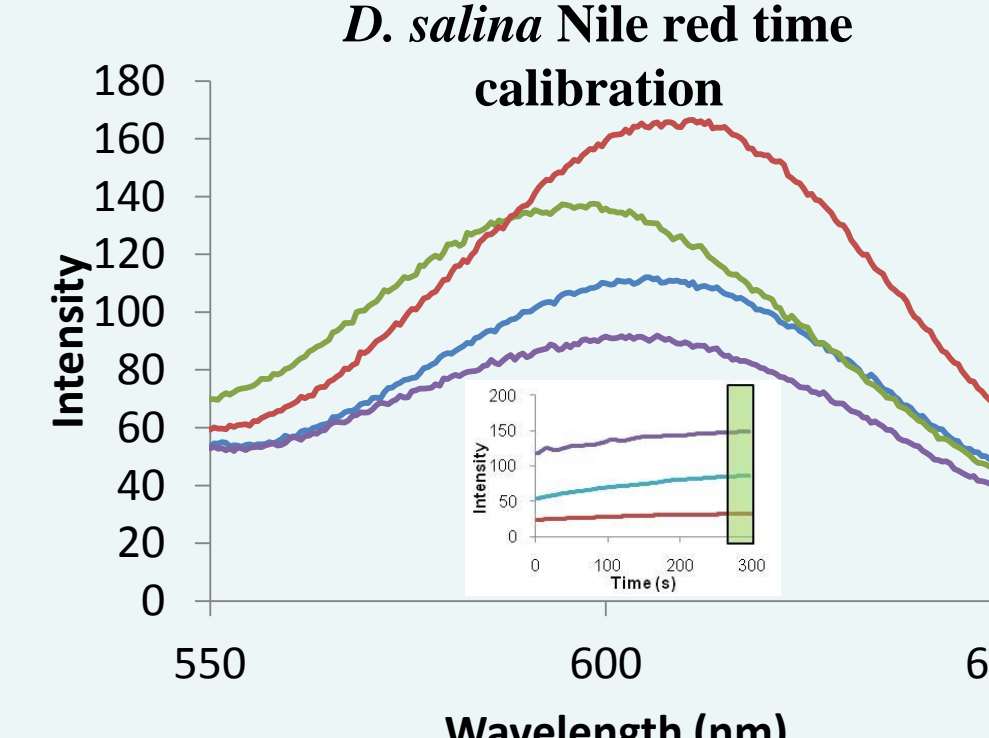
Lipids:

- Use Nile-red-stained lipid fluorescence
- Excite at ~530 nm, emit at ~600 nm
- Calibrate for cell penetration time period for each algae species

Fluorescence calibration



D. salina Nile red time calibration



EFDC and Water Quality Model

- Modified version of the Environmental Protection Agency's Environmental Fluid Dynamics code and U. S. Army Corp of Engineer's water-quality model.
- Models algae growth based on constitutive relations

B – biomass concentration (gC/m³)
 P – production rate (1/d)
 B_M – metabolism rate (1/d)
 P_R – predation rate (1/d)
 f – growth limiting constitutive relations (non-negative, less than or equal to 1)

$$\frac{\partial}{\partial t} B(\mathbf{x}, t) = (P - B_M - P_R) B(\mathbf{x}, t) + \frac{B_L}{V}$$
$$P = \mu_{opt} \cdot [f_1(N) f_2(I) f_3(T) f_5(S)]$$

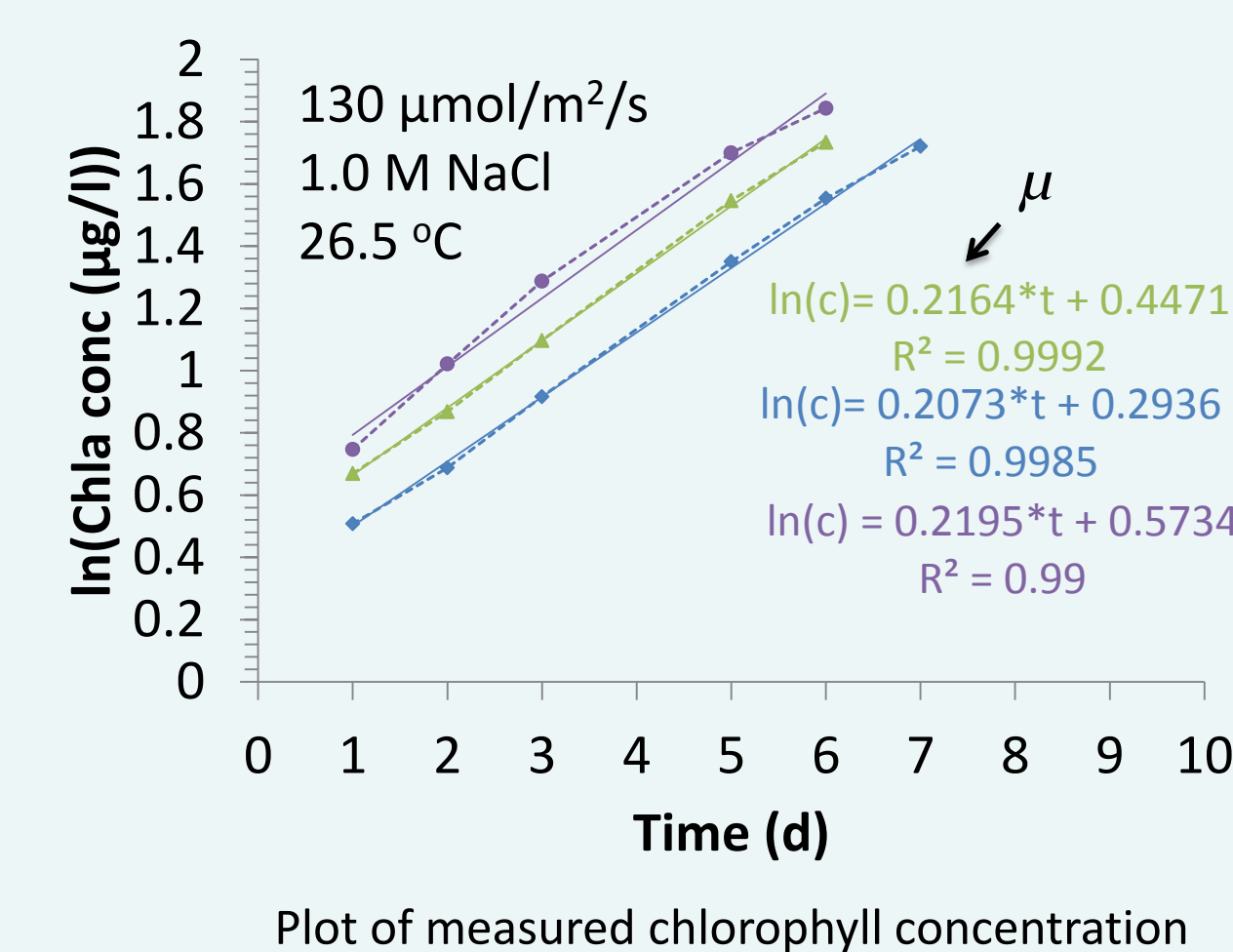
- Tracks nutrients, salinity, temperature, light, CO₂ and O₂ concentrations
- Allows for sources and sinks of parameters
- Currently assuming no settling (well mixed)

Results

Growth Measurements

- Measured growth at 23.5, 26.5, 29.5, and 31.5 °C for 3 light intensities (50, 130, 280 µmol/m²/s) and 4 salinities (1, 1.5, 2, 2.5 M NaCl) in parallel
- Bubble air into samples
- Light/dark cycle = 16:8
- Measured in triplicate and averaged
- Calculate specific growth rate, μ , by fitting data to exponential growth curve:

$$C_{Chla} = C_0 e^{\mu t}$$
$$\ln(C_{Chla}) = \mu t + \ln(C_0)$$



Constitutive Relation Determination

Salinity:

- Bell curve with different above and below optimum decay coefficients and non-zero asymptote

$$ksal_1 = 0.0001 \text{ (ppt NaCl)}^{-2}$$
$$ksal_2 = 0.0002 \text{ (ppt NaCl)}^{-2}$$
$$S_{opt} = 90 \text{ ppt NaCl (1.01 M)}$$
$$f_{sal} = 0.6$$
$$f(S) = \frac{\mu(S)}{\mu_{opt}} = \begin{cases} \left(f_{sal} \exp(-ksal_1 (S - S_{opt})^2) + (1 - f_{sal}) \right) & \text{when } S \leq S_{opt} \\ \left(f_{sal} \exp(-ksal_2 (S - S_{opt})^2) + (1 - f_{sal}) \right) & \text{when } S > S_{opt} \end{cases}$$

Light Intensity:

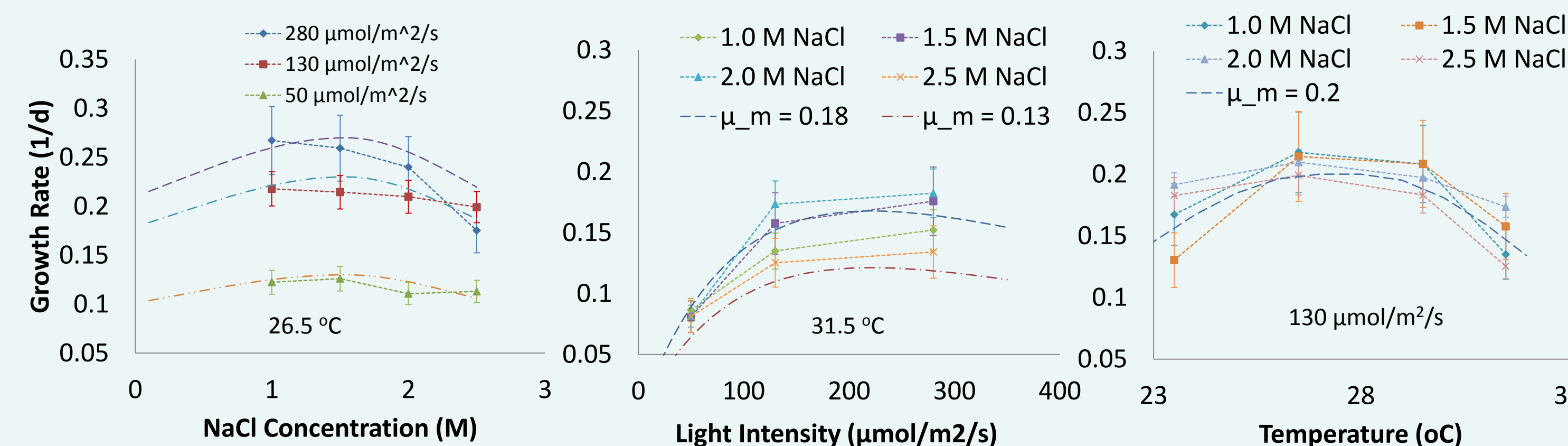
- Steele's equation for light intensity constitutive relation including light extinction

$$I_{opt} = 150 \text{ µmol/m}^2/\text{s}$$
$$FD = \frac{1}{2} \text{ (from 16:8 light/dark cycle)}$$
$$f(I_0) = \frac{\mu(I_0)}{\mu_{opt}} = \frac{2.718 \cdot FD}{Kess \cdot \Delta z} (e^{-\alpha_b} - e^{-\alpha_r})$$
$$\alpha_b = \frac{I_0}{FD \cdot I_{opt}} e^{-Kess(H_T + \Delta z)}, \quad \alpha_r = \frac{I_0}{FD \cdot I_{opt}} e^{-Kess \cdot H_T}$$
$$Kess = K_{e_b} + K_{e_{chl}} \frac{B}{CChl}$$

Temperature:

- Gaussian curve with differing above and below optimum decay coefficients and a range of optimal temperature.

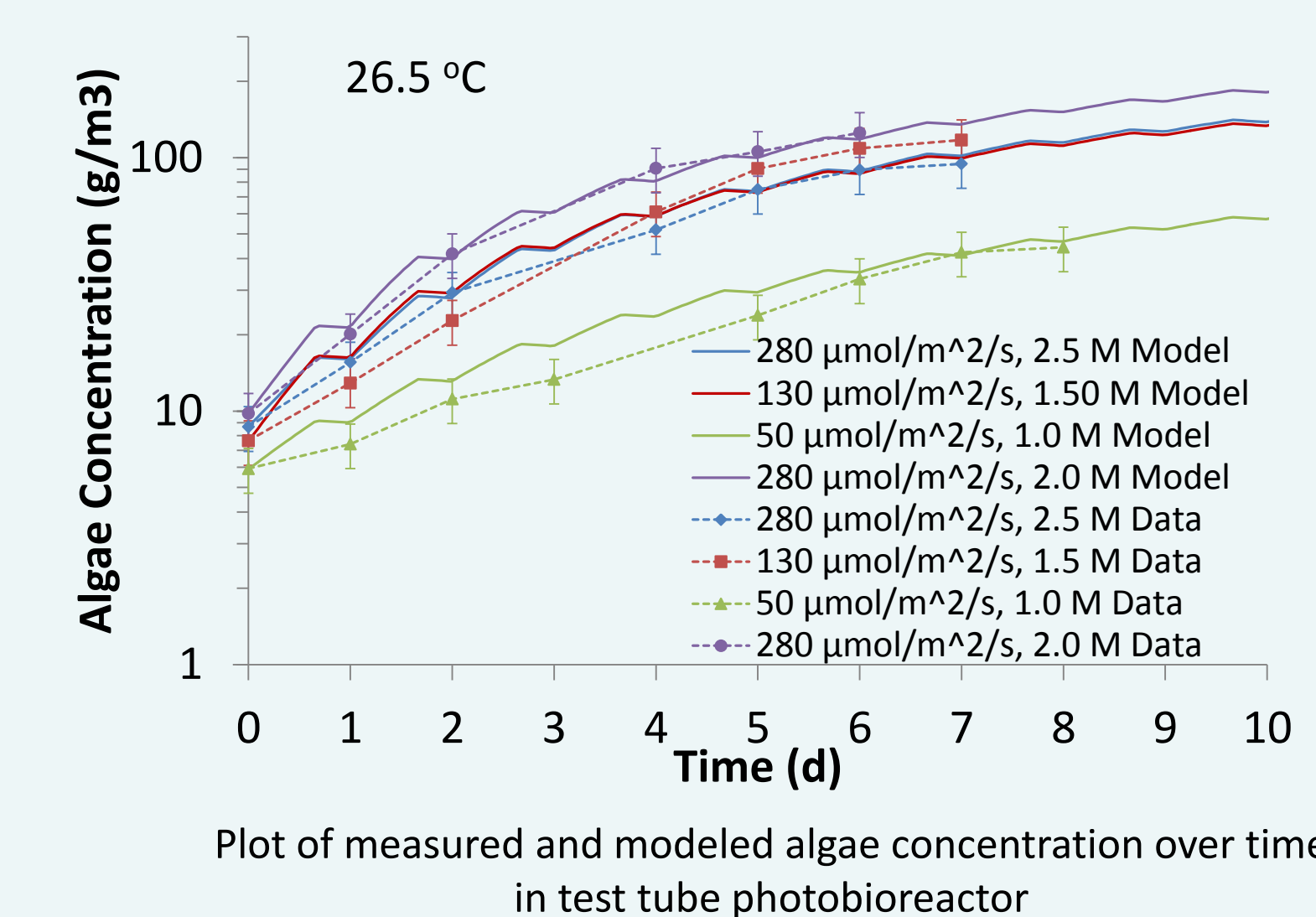
$$k_{T1} = 0.02 \text{ (°C)}^{-2}$$
$$k_{T2} = 0.025 \text{ (°C)}^{-2}$$
$$T_{opt,1} = 27 \text{ °C}$$
$$T_{opt,2} = 28 \text{ °C}$$
$$f(T) = \frac{\mu(T)}{\mu_{opt}} = \begin{cases} \exp(-k_{T1} (T - T_{opt,1})^2) & T \leq T_{opt,1} \\ 1 & T_{opt,1} < T \leq T_{opt,2} \\ \exp(-k_{T2} (T - T_{opt,2})^2) & T > T_{opt,2} \end{cases}$$



Comparisons between measured data and constitutive relations.

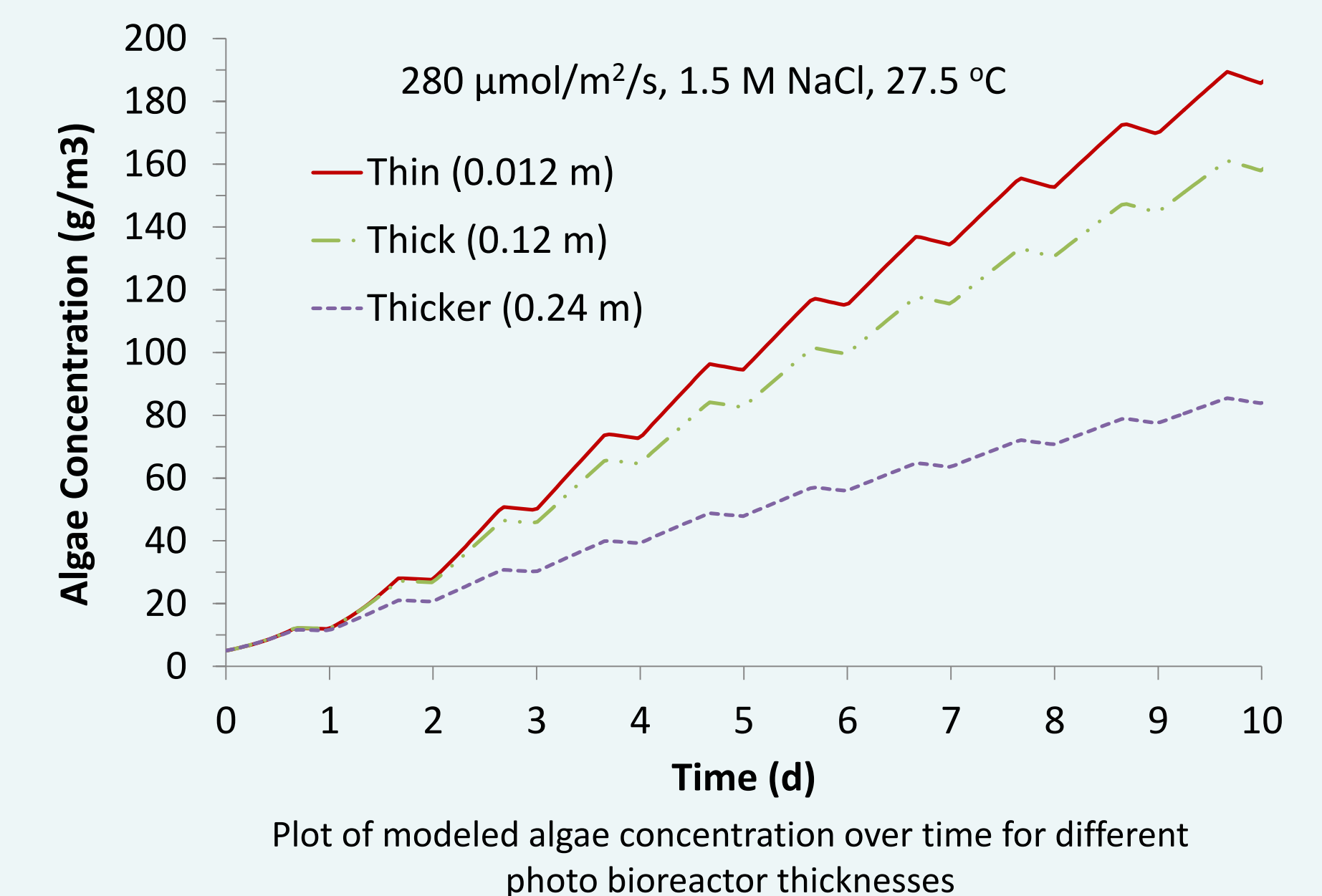
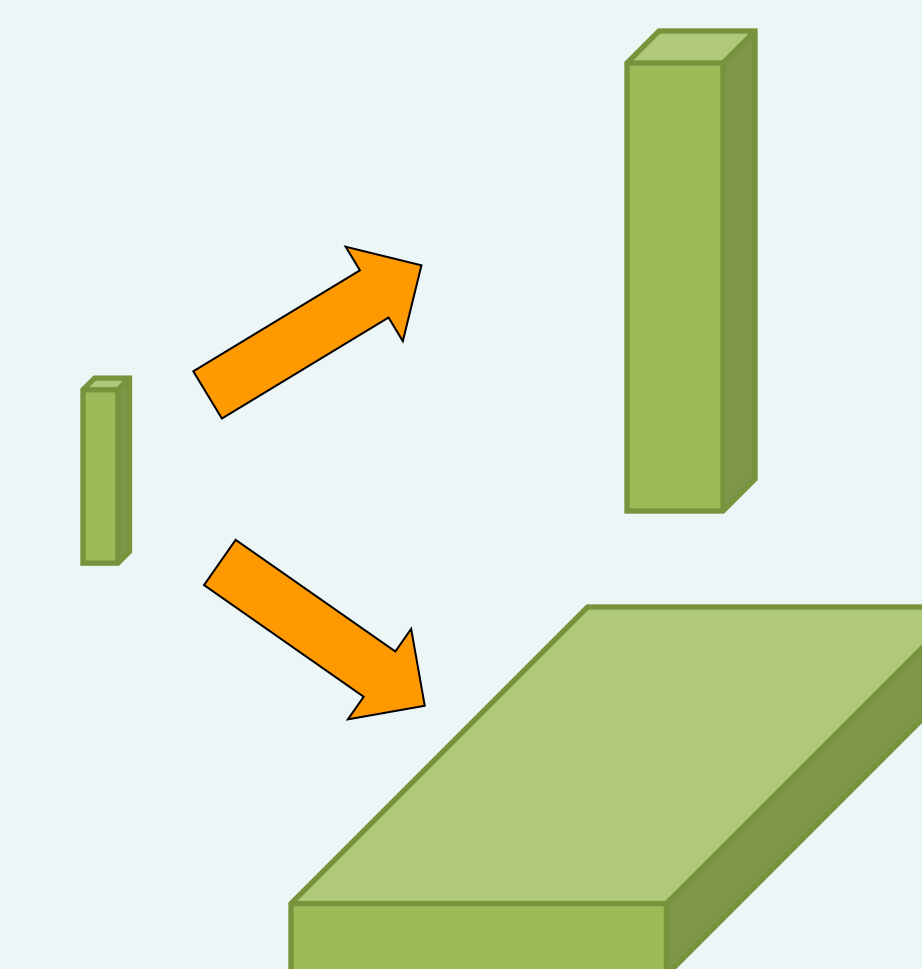
Lab-scale Model and Data Comparison

- Predicted *D. salina* growth in test tube based on constitutive relations (measurement (S, I, T) and literature (M))
- Relations chosen work relatively well, more improvements could be made



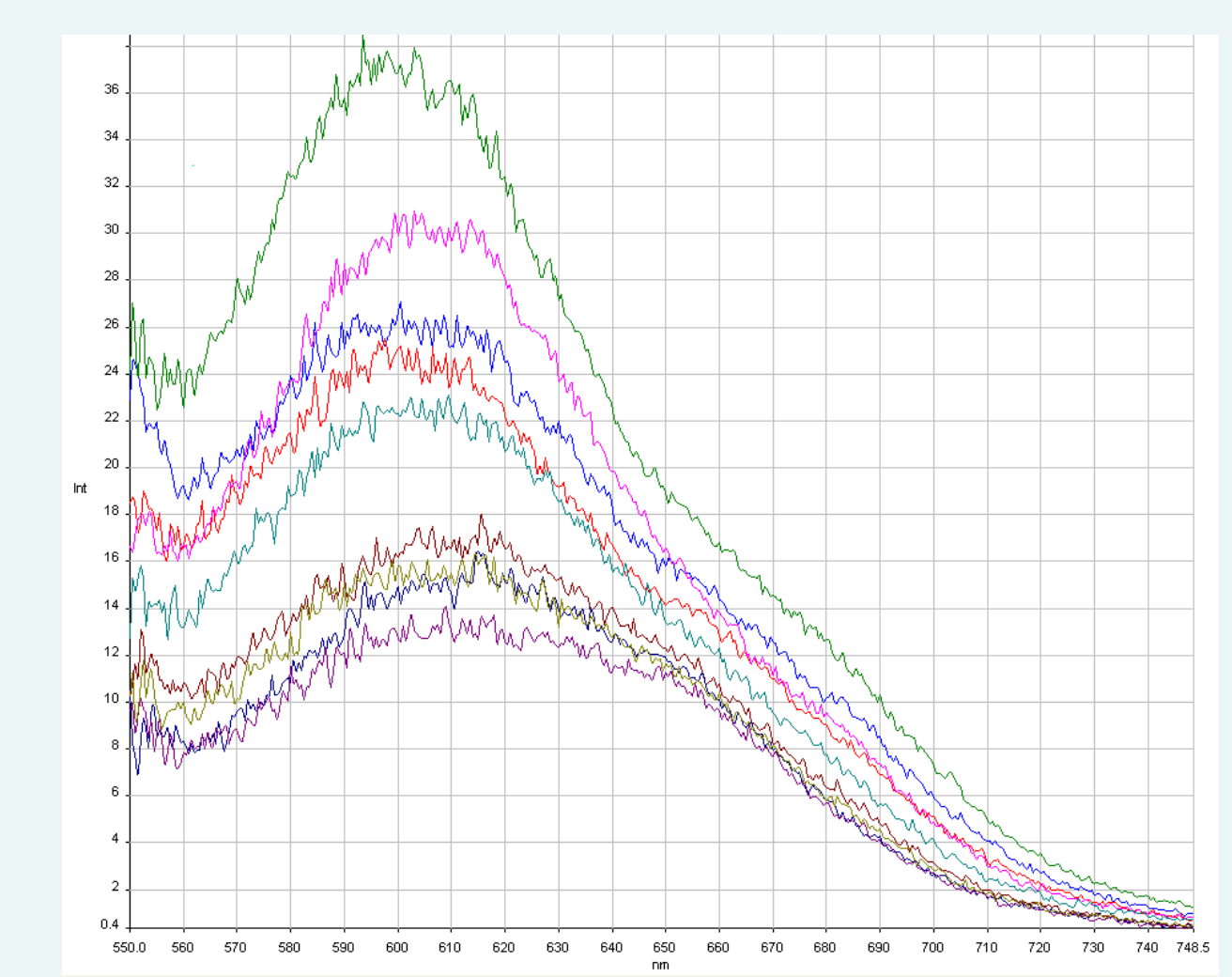
Model Expansion

- Model can be expanded to larger scale bioreactors like open channel raceways, column and flat plate airlift bubble mixing photobioreactors, and closed channel tubular photobioreactors.
- Able to compare various bioreactor geometries
- Model shows dependencies on photobioreactor thickness due to reduced light penetration.



Lipid Measurements

- Lipids were measured later in the exponential growth phase and after.
- No appreciable variations were seen during the growth
- When CO₂ bubbling was stopped, no appreciable difference in lipid quantity was measurable.
- Beta carotene build-up in *Dunaliella salina* caused interference and error with the Nile Red measurements especially at high light conditions.



Nile Red fluorescence measurements for *Dunaliella salina*

Conclusions

- Completed multi-factorial measurements of *D. salina* growth
- Added salinity growth dependence to existing EFDC model
- Created airlift bubble type photobioreactor model (e.g., test tube, column, plate)
- Developed salinity, temperature, and light intensity constitutive relations for *D. salina*
- Modeled *D. salina* in airlift photobioreactor and compared to measurement data
- Modeled effect of photobioreactor thickness
- Knowledge gained will enable computational models to optimize algae growth in real-world conditions with varying temperature, light, and salinity over the course of a day or year.
- Through a validated constitutive growth model, algae performance and production efficiency can be predicted for various growth conditions, including different weather climates and reactor designs.
- The model will enable improved design and algae strain selections.