

Anoxic Corrosion of Steel and Lead in Na - Cl \pm Mg -Dominated Brines

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Purpose and Scope

- Determine the extent to which Fe and Pb consume CO_2 and H_2S
- Potential for Fe and Pb to support MgO as engineered barrier
- Determine what corrosion products are likely to form
- Kinetics of Fe and Pb corrosion
- Potential for passivation of metal surfaces.
- Competition of CO_2 and H_2S in corrosion



Previous Work

- **Telander and Westerman (1993, 1997)**
 - Investigated gas generation (H_2) due to corrosion of steels immersed in/or hanging above brine with overpressures of different gases (H_2 , N_2 , CO_2 , H_2S)
 - Corrosion independent of H_2 overpressure
 - N_2 overpressure results in Fe-Mg hydroxide
 - CO_2 overpressure passivates with coating of Fe-Mg- CO_3
 - Addition of H_2S de-passivates CO_3 , H_2S alone passivates with FeS layer.
- **Molecke et al. (1993)**
 - Carbon steels and Pb exposed to Brine A in boreholes
 - No control of gas phases present (no *CPR gases, likely oxic conditions)
 - Significant corrosion seen (corrosion products not analyzed)
- **Wang (2001)**
 - Exposed steel coupons to ERDA-6 and G-Seep equilibrated with brucite
 - Produced green rust $[Fe(II),Fe(III)]hydroxide$

*Cellulose, plastic, and rubber materials



Experimental Setup

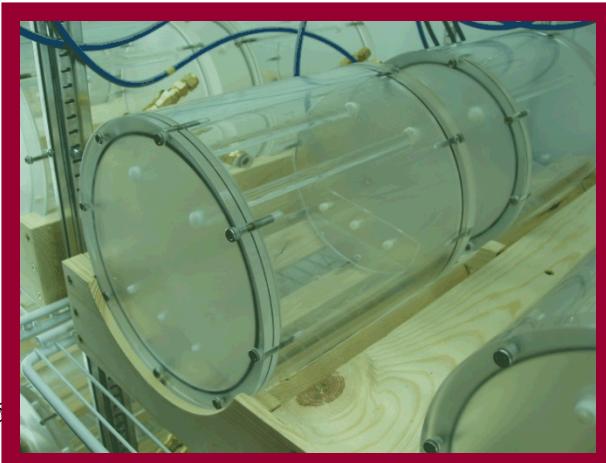
- **WIPP-relevant environmental conditions**
 - Temperature: 26°C
 - Relative humidity: approx. 72%
 - Atmosphere:
 - N₂, N₂ + CO₂, N₂ + H₂S, or N₂ + CO₂ + H₂S
 - Anoxic: < 1 ppm O₂
 - Brine compositions:
 - ERDA-6 ± organics (EDTA, citrate, acetate, oxalate)
 - GWB ± organics (EDTA, citrate, acetate, oxalate)
- **Materials:**
 - Iron – ASTM A1008 carbon steel
 - Lead – QQ-L-171e Grade C chemical Pb
- **Experiments are being performed in a flow-through system designed to maintain above environmental conditions**



Mixed-Flow Gas Control System (MFGCS)

- **Designed to maintain desired environmental conditions in a flowing-gas setup**
- **Continuous monitoring of gas flow rates and compositions with data acquisition software**
 - Alarms if gas flow rates/compositions or RH outside accepted tolerances
 - Logs monitoring data to hard drive
 - Monitors supply gas pressures

Mixed Flow Gas Control System (MFGCS)





Test Matrix (CO₂)

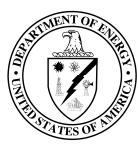
- Two material types
 - Carbon steel (A1008) and lead (QQ-L-171e)
- Four brine compositions
 - ERDA-6 with or without organics, GWB with or without organics
- Four atmospheres
 - N₂, N₂ + CO₂ (350 ppm, 1500 ppm, or 3500 ppm)
- Four time segments
 - 6, 12, 18 and 24 months
- Three sample positions
 - Atmospheric
 - Partially submerged
 - Fully submerged
- Three replicates for each sample
- Total of 432 samples for each metal type
- No experiments involving H₂S are currently underway





Sample Analysis

- Weight loss after removal of corrosion products
- Characterization of coupon surfaces
 - Before and after removal of corrosion products
 - SEM
- Characterization of corrosion products
 - XRD
 - SEM with EDS and EBSD
- Solution chemistry
 - pH
 - Major element concentrations
- Sample loading/unloading is being done in a VAC environmental glove box (<1 ppm O₂)



Typical Appearance of Steel Coupons

Coupon 135

6 month exposure, 350 ppm CO₂, ERDA-6 w/ organics



Before

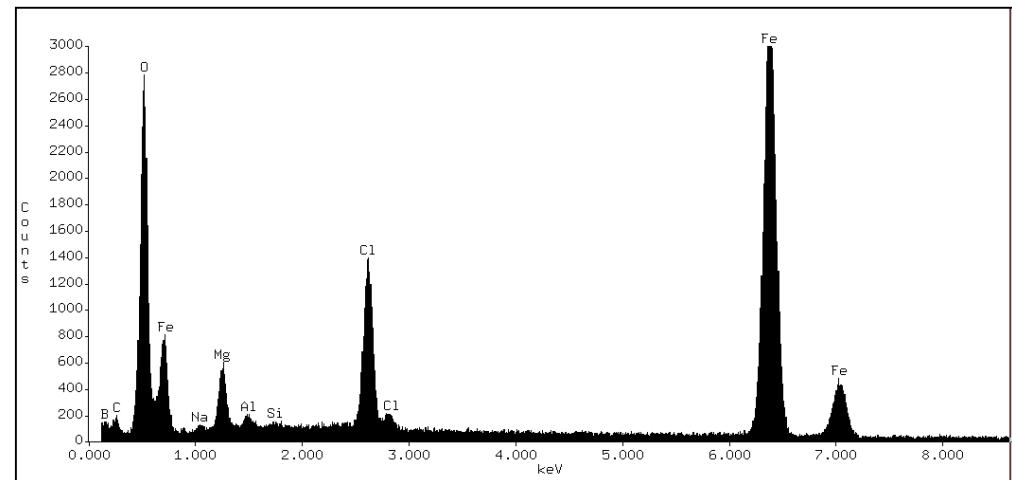
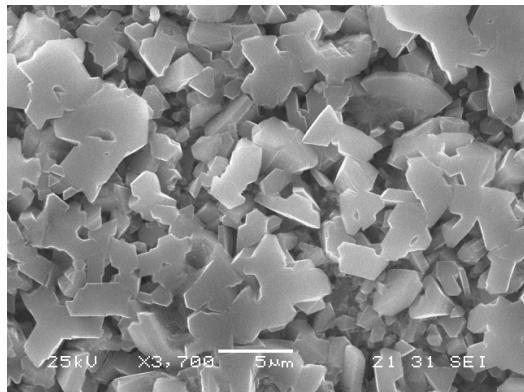


After

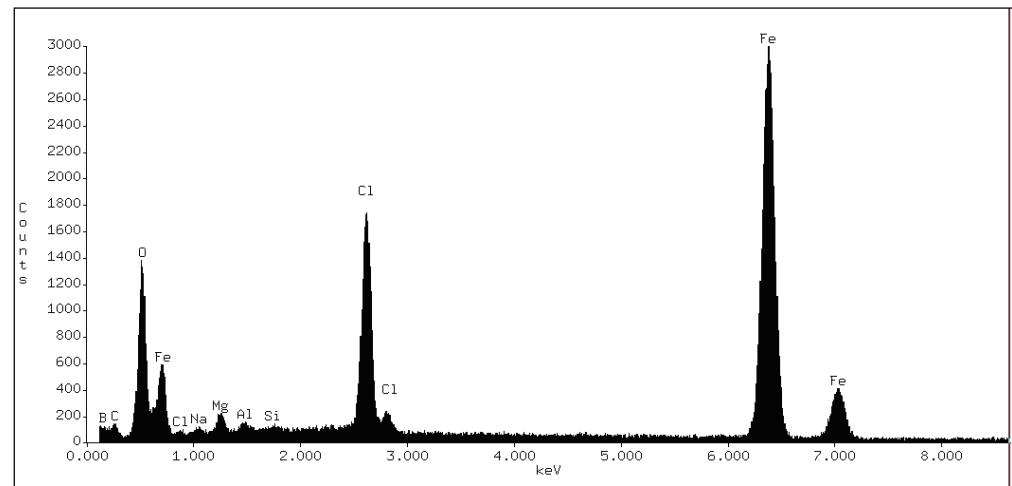
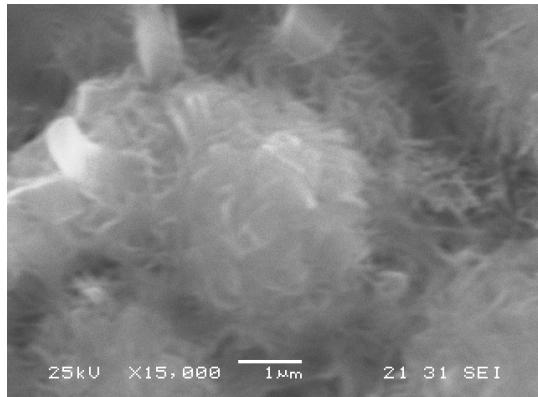
EDS of Fe Corrosion Products

Coupon 104

Green Corrosion Product



Hazy Corrosion Product



Typical Appearance of Steel Coupons

Coupon 327

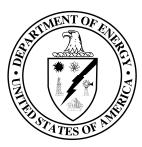
6 month exposure, 1500 ppm CO₂, ERDA-6 w/ organics



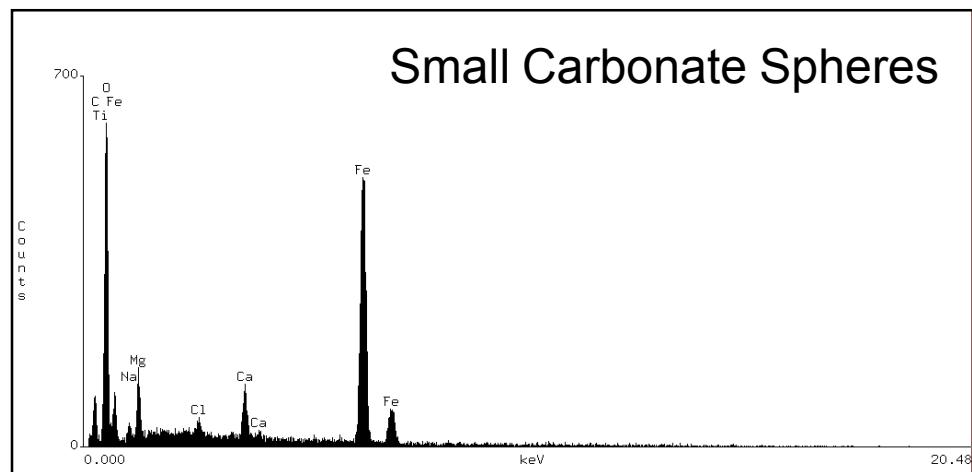
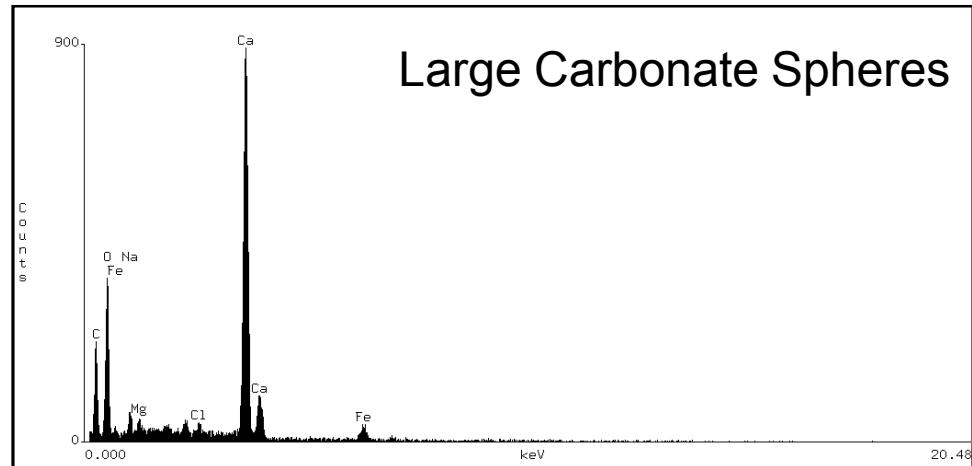
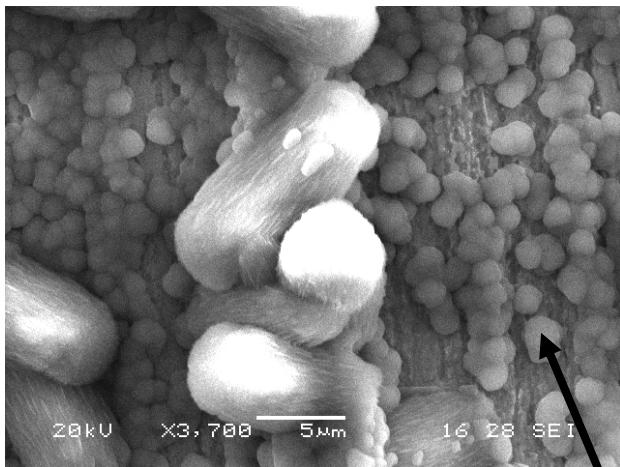
Before



After



EDS of carbonate Corrosion Products



Typical Appearance of Lead Coupons

Coupon L451

6 month exposure, 3500 ppm CO₂, ERDA-6 w/ organics



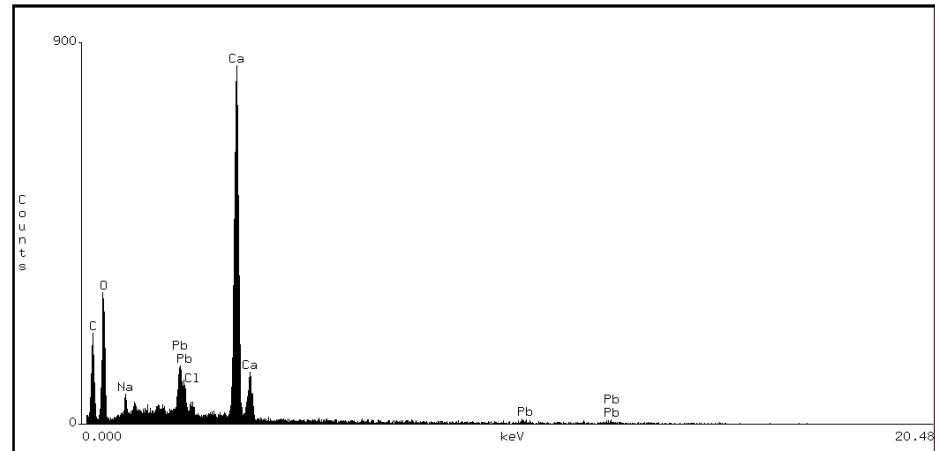
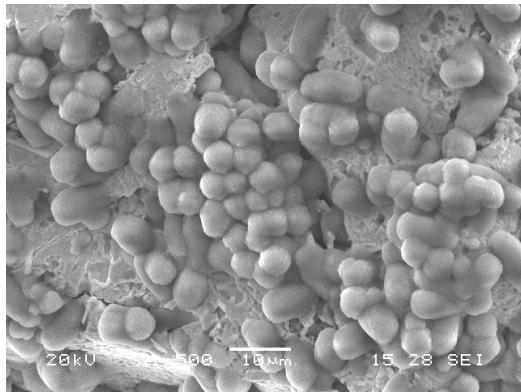
Before



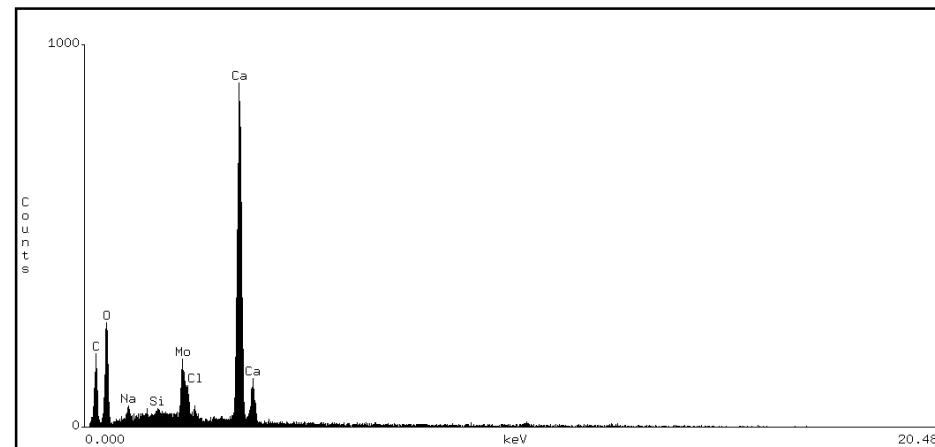
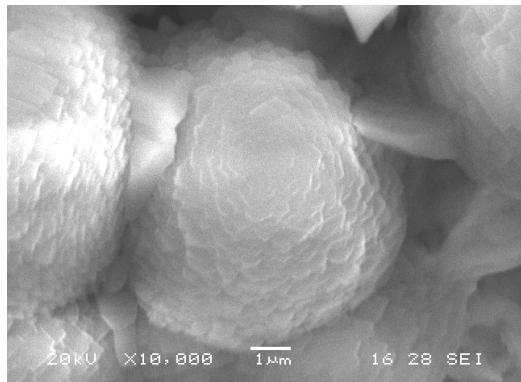
After

EDS of Pb Corrosion Products

Coupon L451



Coupon L313



Weight Loss Determination

- Coupon placed in cleaning solution for 2 minutes**

Material	Chemical	Time	Temp.	Source ¹
Iron (Fe)	concentrated HCl + 50 g/L SnCl_2 + 20 g/L SbCl_3	25 min max.	Cold	A
	500 mL conc. hydrochloric acid (HCl) 3.5 g hexamethylene tetramine Reagent water to make 1000 mL	10 min	20 to 25 °C	B
Lead (Pb)	250 g ammonium acetate ($\text{CH}_3\text{COONH}_4$) Reagent water to make 1000 mL	5 min	60 to 70 °C	B

¹Source: A, NACE Standard TM0169-2000; B, ASTM G 1 – 03.

- After 2 minutes, removed, scrubbed, rinsed in DI water followed by ethanol**
- Coupon weighed**
- Repeat process for 5 to 10 cycles**

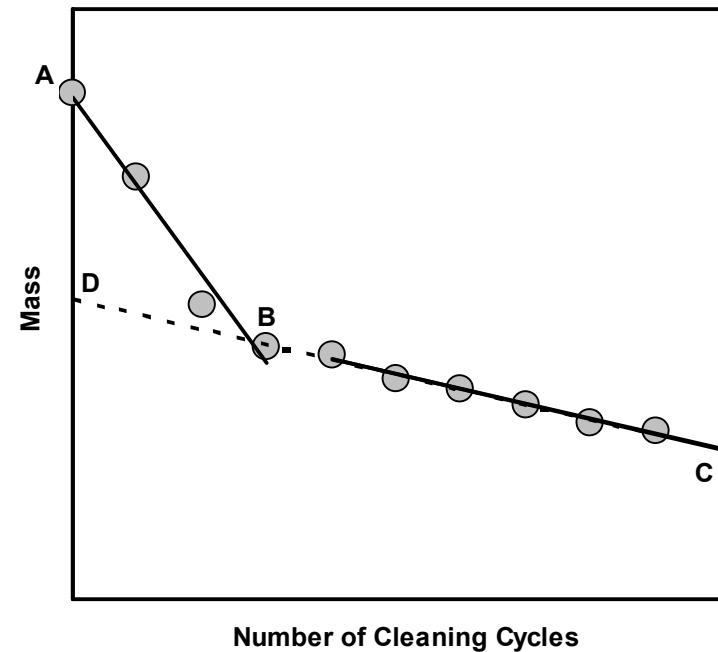


Weight Loss Graphical Analysis

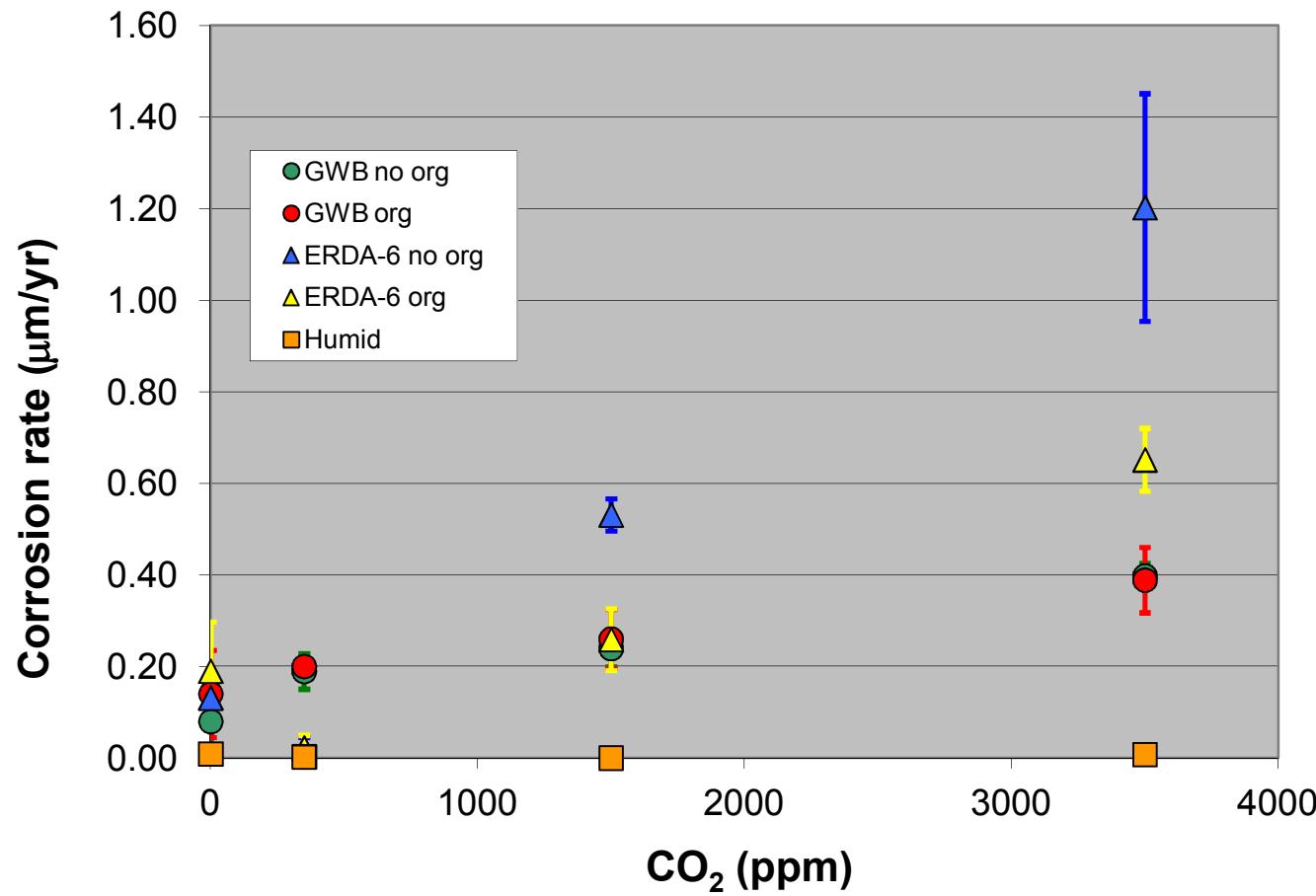
AB – Removal of corrosion product and base metal

BC – Removal of base metal only

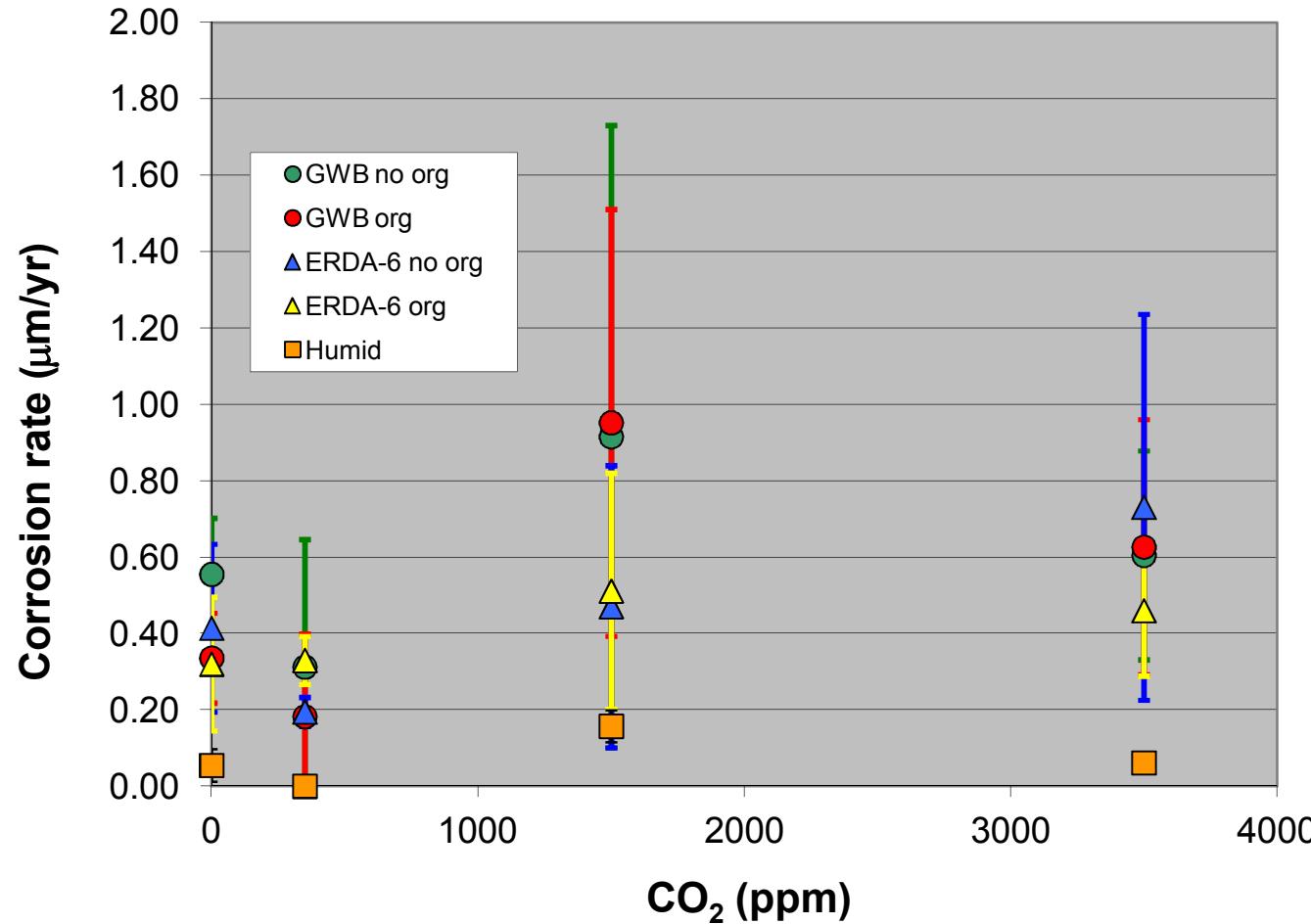
D – Projected final weight



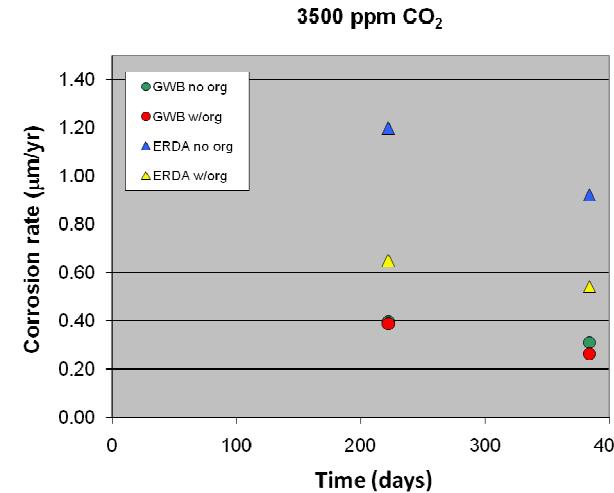
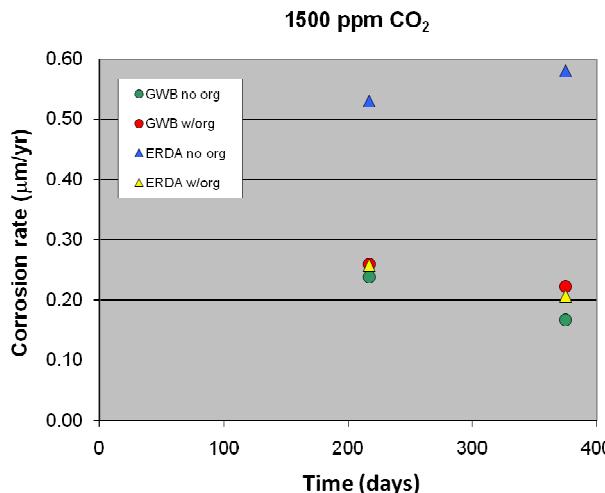
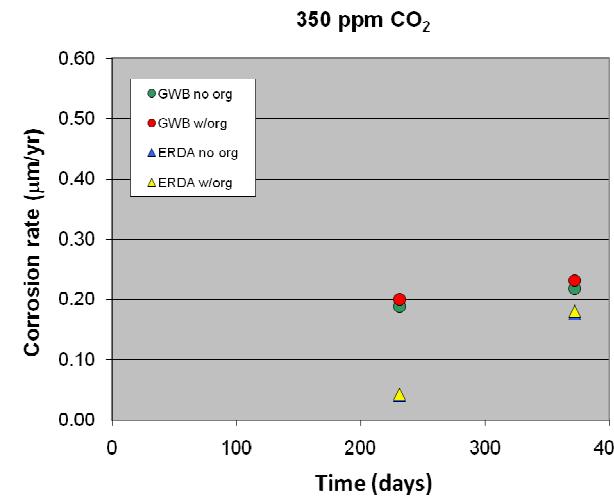
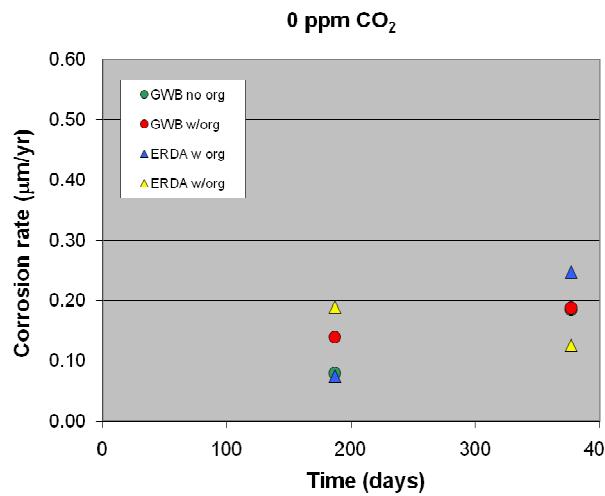
Corrosion Rate for Fe Coupons



Corrosion Rate for Pb Coupons



Corrosion Rate for Fe Coupons





Summary

- **Corrosion of Fe**
 - ERDA-6 is more corrosive than GWB
 - The presence of organics is important only for ERDA-6 (suppresses corrosion)
 - Corrosion increases with CO_2
- **Corrosion of Pb**
 - No clear trends apparent in corrosion rates
 - GWB may be more corrosive than ERDA-6
 - Further data required to support this hypothesis
- **Passivation may be occurring at high P_{CO_2}**



References

Molecke, M.A., N.R. Sorensen, and G.G. Wicks. 1993. *Waste Isolation Pilot Plant Materials Interface Interactions Test: Papers Presented at the Commission of European Communities Workshops on Situ Testing of Radioactive Waste Forms and Engineered Barriers*. SAND93-1055. Albuquerque, NM: Sandia National Laboratories.

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Wang, Z., R.C. Moore, A.R. Felmy, M.J. Mason, and R.K. Kukkadapu. 2001. "A Study of the Corrosion Products of Mild Steel in High Ionic Strength Brines," *Waste Management*. Vol. 21, 335-341.

