

Solar Thermochemical Fuels

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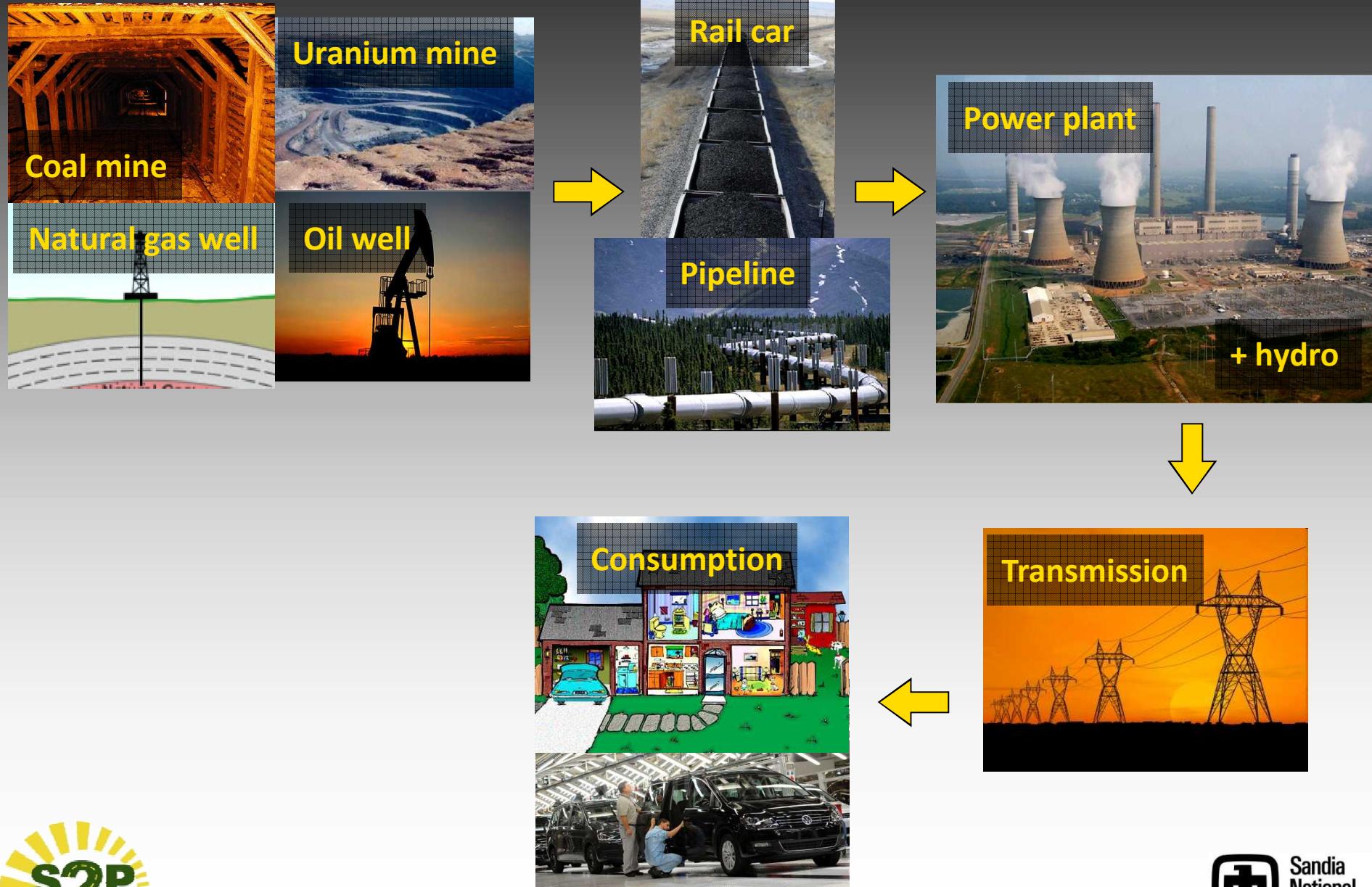
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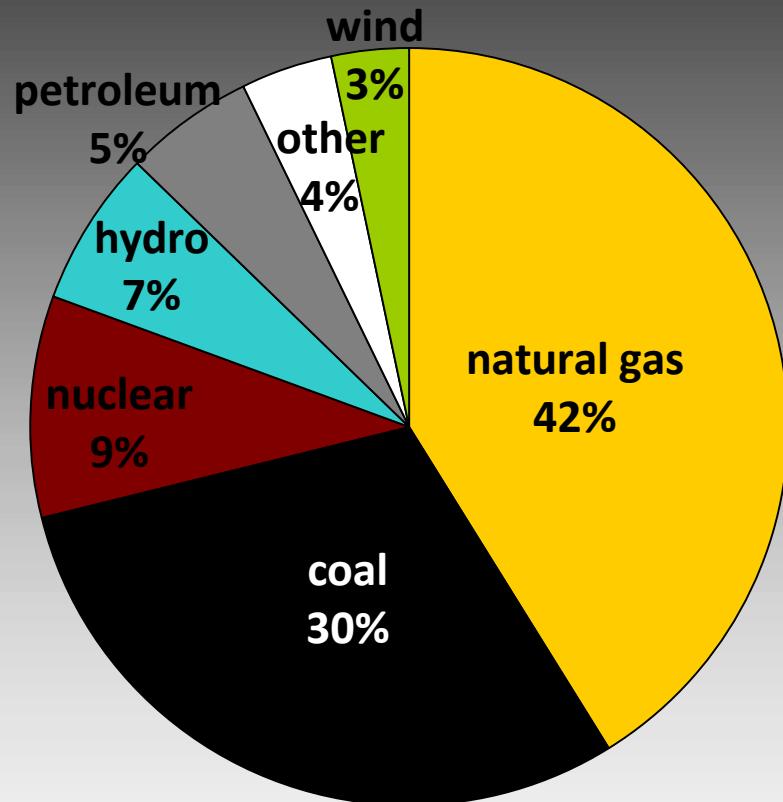
Outline

- The role of fuels in today's energy landscape
- Concentrated solar power and solar fuels
- Packed bed particle reactor for solar fuel production
- Final thoughts

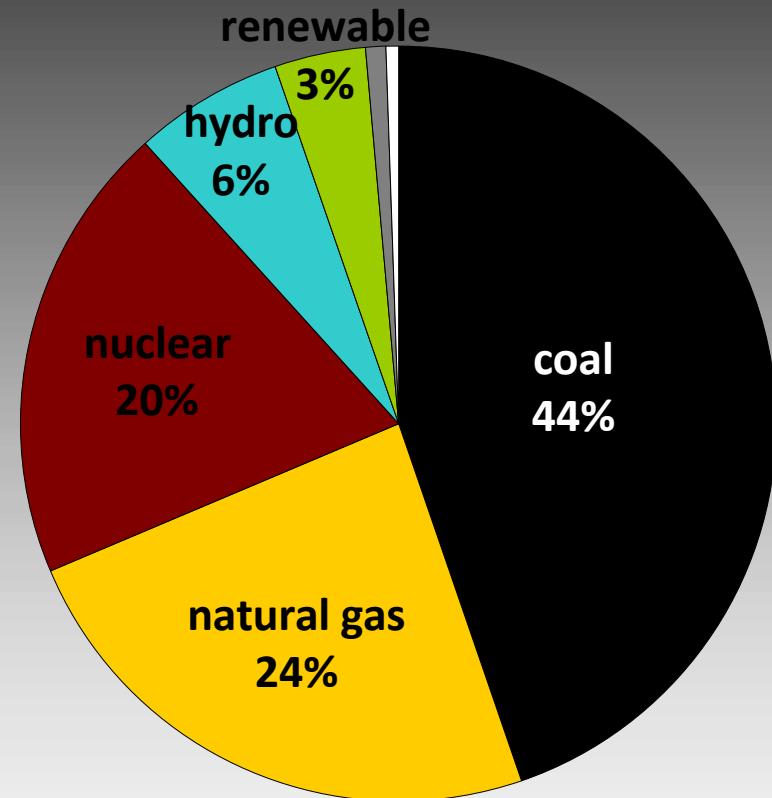
The 19th & 20th Century US Electricity Paradigm



US Electricity Sources: Mostly Fuels

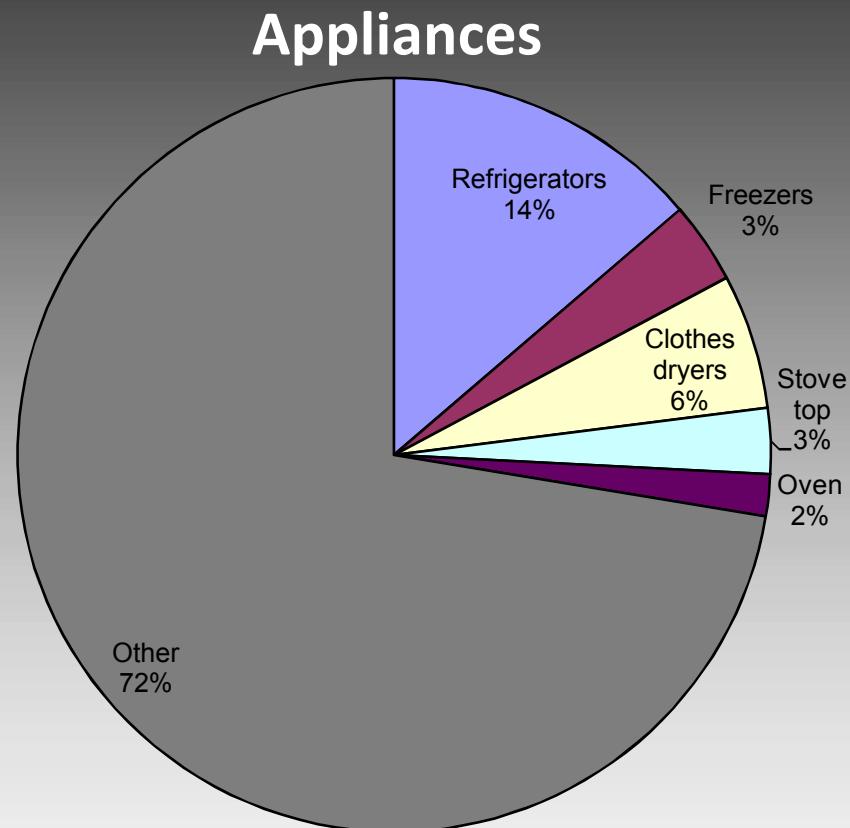
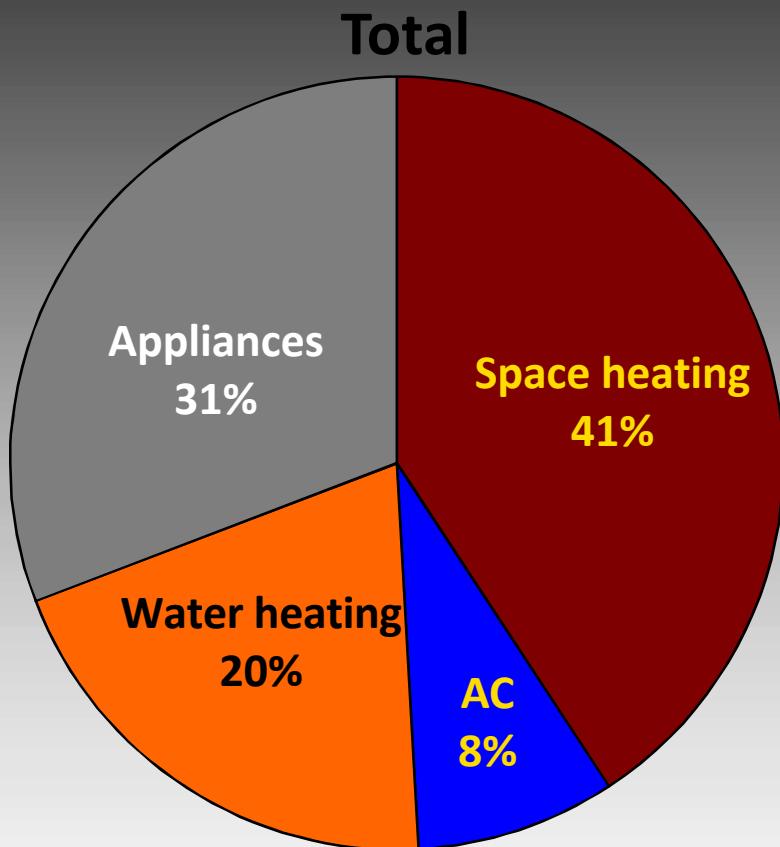


United States 2010
nameplate capacity



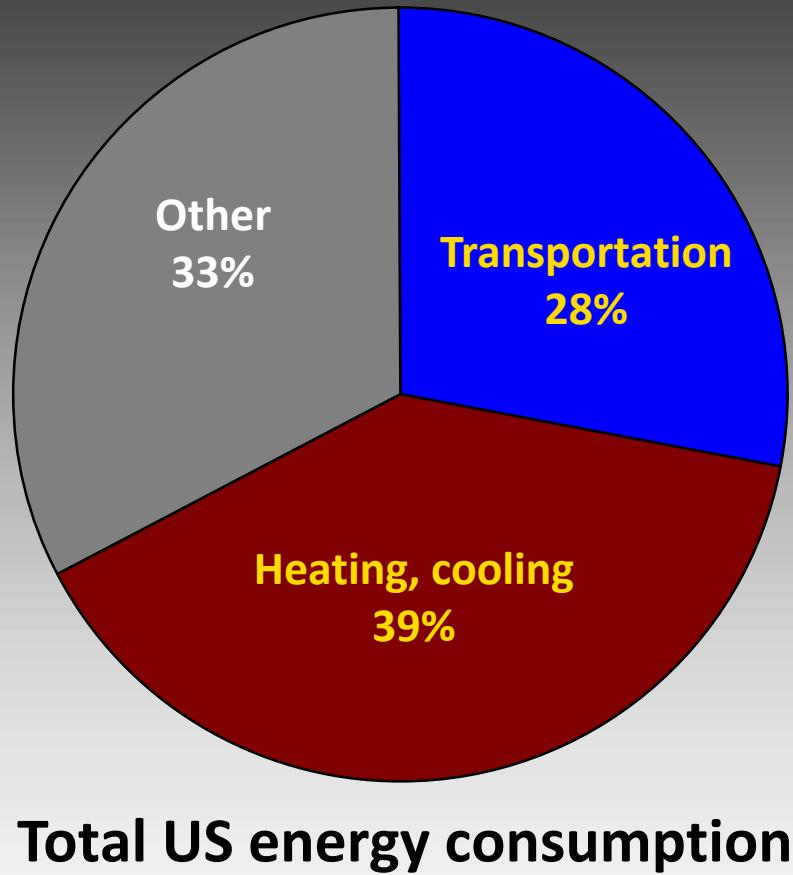
United States 2010
net generation

Residential Energy Needs: Mostly Heating and Cooling



US residential energy consumption: 78% heating and cooling

US Energy Needs: Mostly Heating, Cooling, and Fuels



Why Fuels? Energy and Transport Efficiency

Energy efficiency

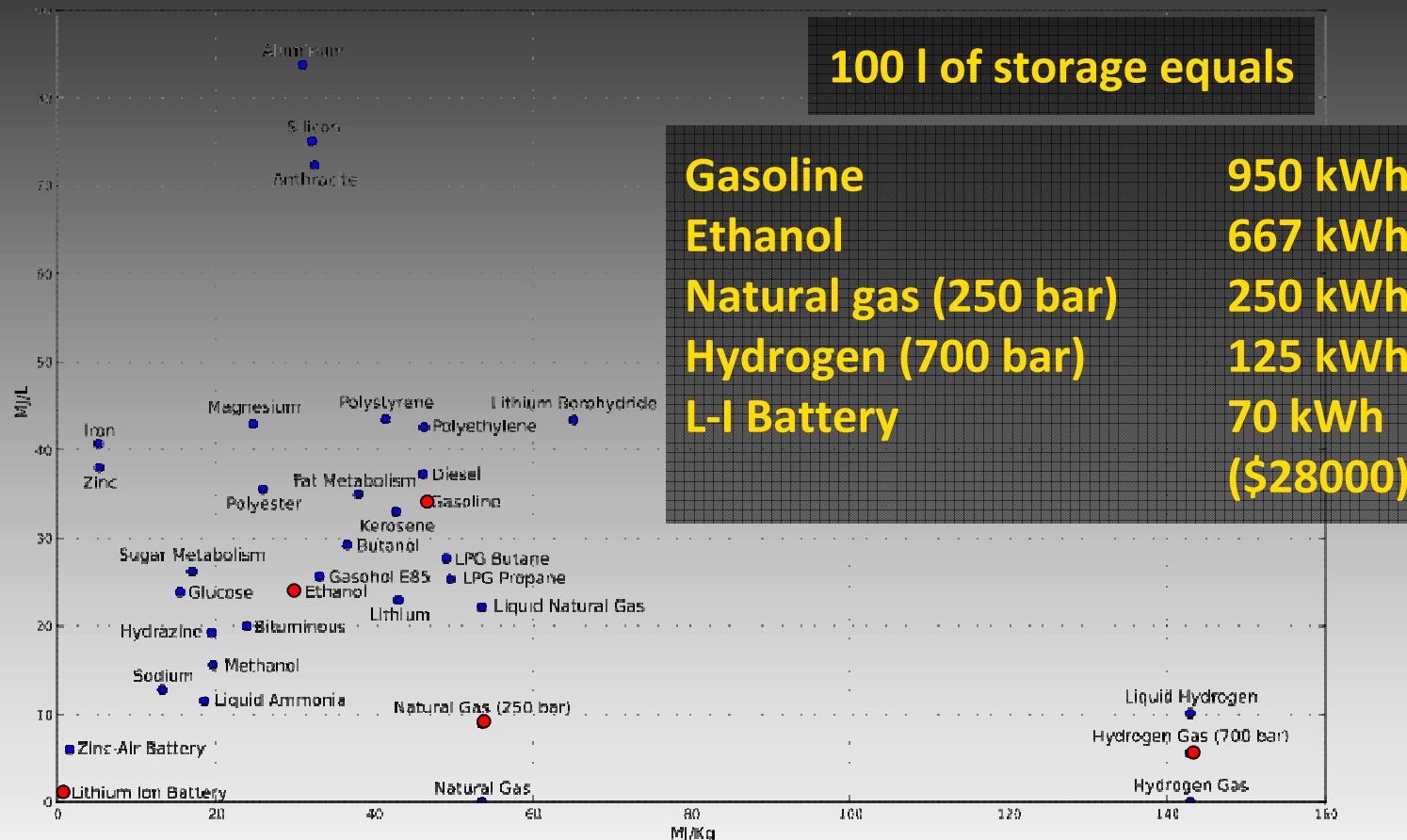
Conventional thermal	35%
Combined cycle	60%
Cogeneration/Micro CHP	80%
Trigeneration	>85%

Transport losses

Oil pipeline	0.8%
Natural gas pipeline	3%
Electricity T&D	9%

Most efficient approach: Deliver fuel close to point of use

Why Fuels? Storage



Days of power reserve from a comparatively small tank

So, Why Fuels?

- Good fit for energy end-use: in transportation, heating, cooling
- Fuels can be transported efficiently
- Efficient when used locally (cogeneration/trigeneration)
- Fuels are easy (and inexpensive) to store

Concentrated Solar Power: Full Solar Spectrum Use



Parabolic trough



Power tower



Parabolic dish

Why Solar Thermochemical Fuels?

- Potential for high efficiency:
 - Use the entire solar spectrum
 - Efficient conversion of solar to chemical energy
 - Production of H₂ and CO avoids reverse water gas shift reaction in hydrocarbon synthesis
- Majority of cycles are two-step metal oxide based
 - Thermal reduction (T>1300°C): $\frac{1}{\delta} \text{MO}_x \rightarrow \frac{1}{\delta} \text{MO}_{x-\delta} + \frac{1}{2} \text{O}_2$
 - Fuel production (T<1200°C):
 $\frac{1}{\delta} \text{MO}_{x-\delta} + \text{H}_2\text{O} \rightarrow \frac{1}{\delta} \text{MO}_x + \text{H}_2$
 $\frac{1}{\delta} \text{MO}_{x-\delta} + \text{CO}_2 \rightarrow \frac{1}{\delta} \text{MO}_x + \text{CO}$

- Key elements: reactive materials and reactors

Comparison of Solar Fuel Technologies

- Molten salt power tower with 65% electrolysis efficiency
 - 11% annual average solar efficiency (solar to H₂)
- Dish-Stirling with electrolysis
 - 16% annual average solar efficiency (solar to H₂)
- PV with electrolysis
 - 10% annual average solar efficiency (solar to H₂)
- Corn ethanol
 - approximately 0.12% annual average solar efficiency (solar to ethanol)

These are the targets that need to be exceeded

System Level View: Many Energy Losses to Consider

Resource efficiency = 95% for Daggett, CA (DNI > 300W/m²)

Operational ~ 94%

Equip. Availability = 97%, Blocking&Shading = 98%, Wind Outage = 99%

Optical ~ 79%

Reflectivity = 93% (two reflections)

Dirt = 95%

Window = 95%

Tracking = 99%

Intercept = 95%

Receiver ~ 82%

Radiation = 82%

Conduction/Convection = 0 %

Solar-to
heat:
~58%

Reactor
→
<60%



H₂
CO

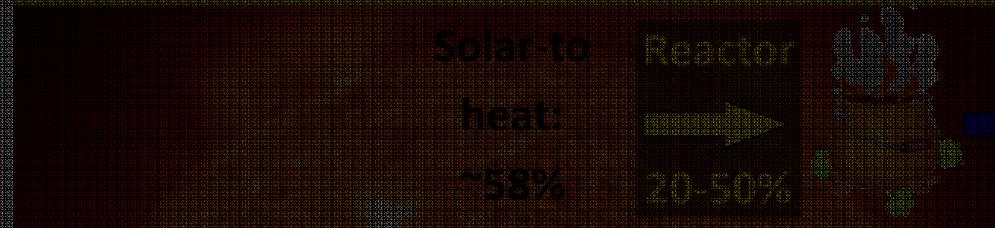
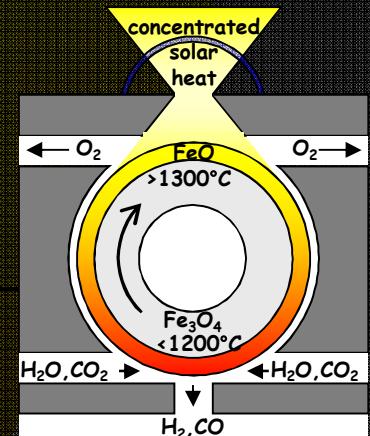
System Level View: Many Energy Losses to Consider

- Lots of places to lose energy
 - Solar collection is mature, improvements will be small

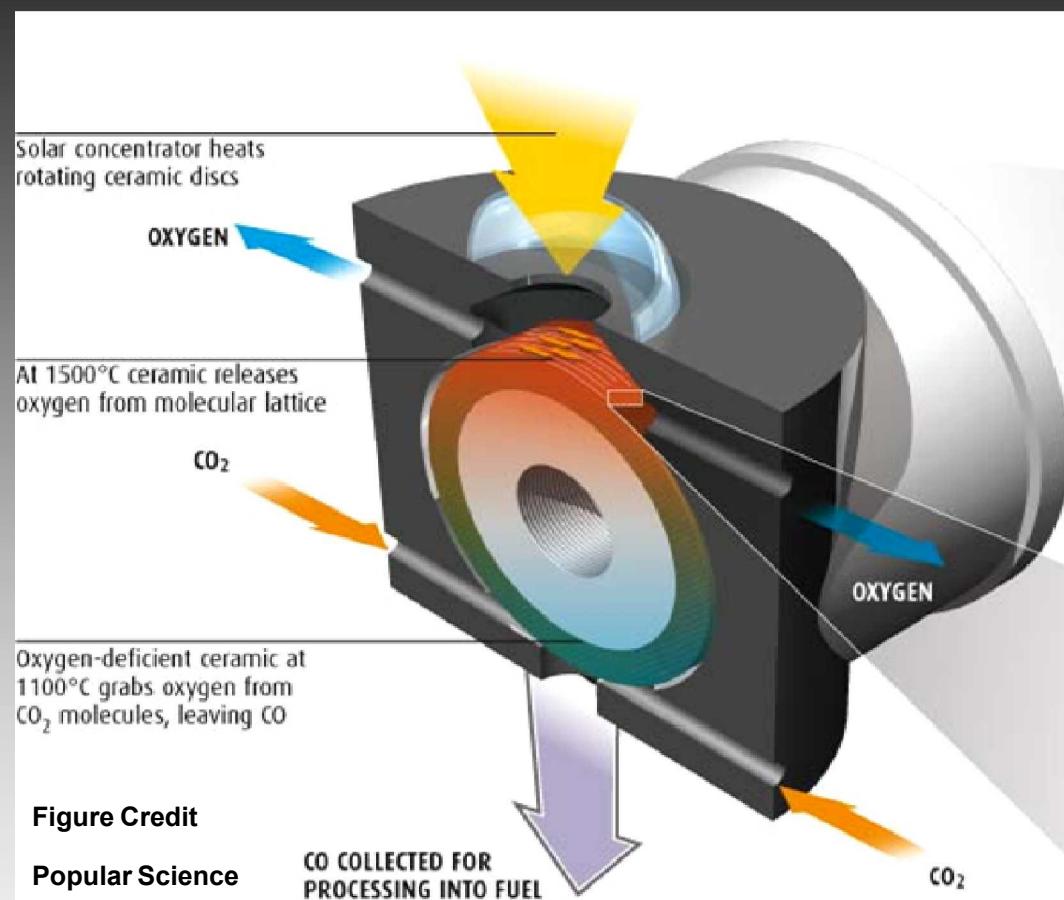
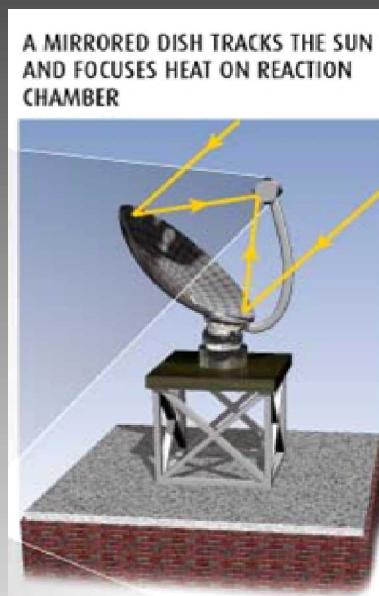
- The **reactor** is the single least efficient component
 - Improve materials
 - Improve reactor: key attributes
 - Reflectivity = 98% (two reflections)
 - DIR = 95%
 - IR = 95%
 - Heat Loss = 99%

- Lessons learned from CR5:
 - Mechanical stability of reactive structures
 - Materials kinetics as source of efficiency limits

Receiver = 82%
Radiation = 82%
Conduction/Convection = 0%



The CR5



Counter-Rotating-Ring Receiver Reactor Recouperator

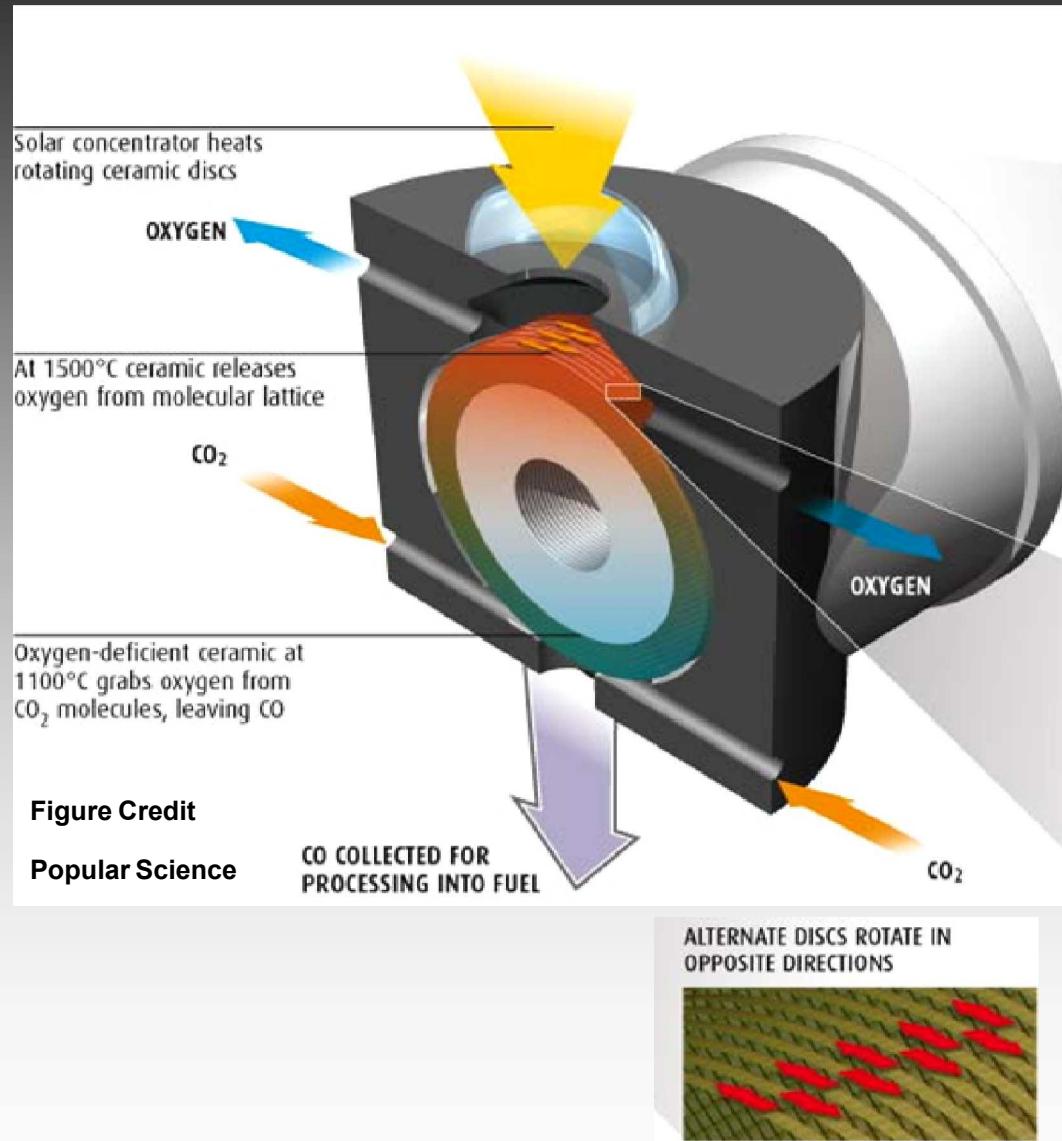


R.B. Diver, J. E. Miller, M. D. Allendorf, N.P. Siegel, R. E. Hogan, J. Solar Energy Engineering (130), 2008



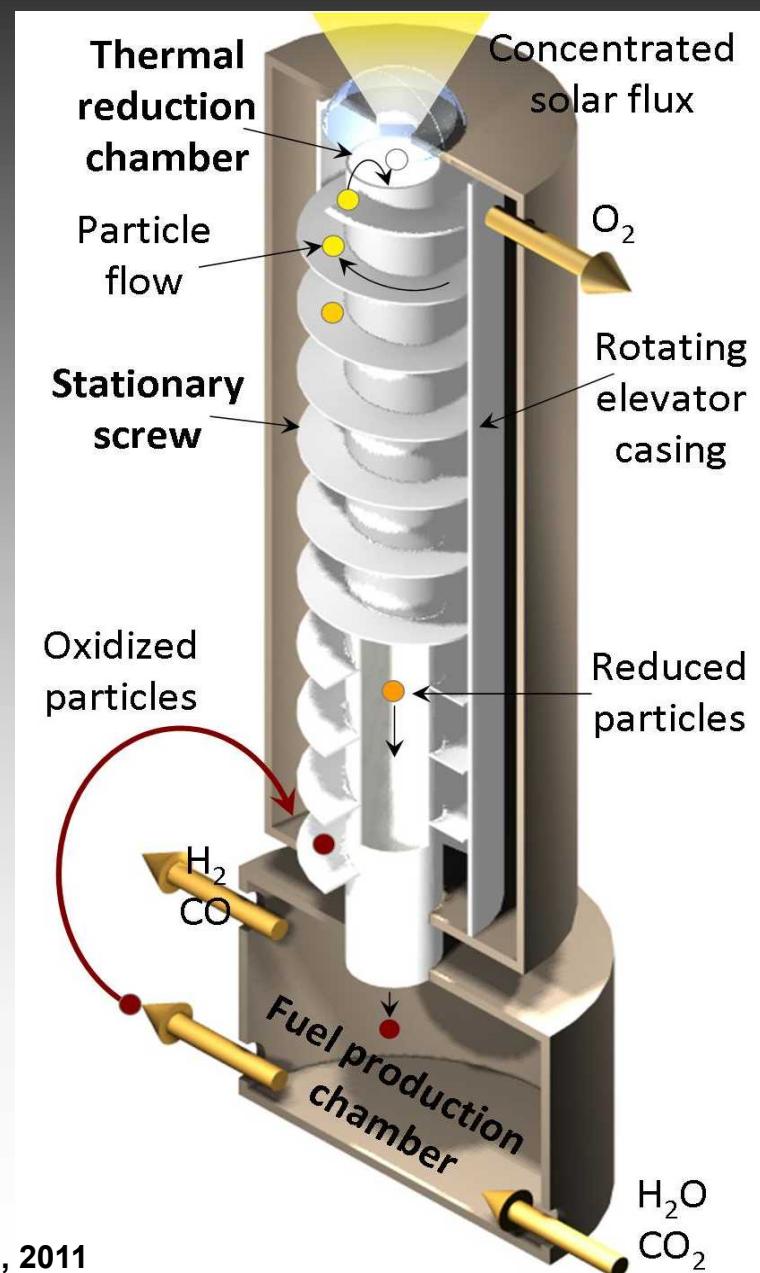
Desirable Reactor Attributes: Efficiency Driven

- Direct solar absorption by the working material
- Sensible energy recovery between T_H and T_L
- Continuous on-sun operation
- Pressure, temperature and product separation
- Lessons learned:
 - Reactive structures durability
 - Material kinetics limitations



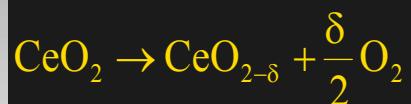
Packed Bed Particle Reactor

- Direct solar absorption by the working material
- Sensible energy recovery between T_H and T_L
- Continuous on-sun operation
- Pressure, temperature and product separation
- Pros:
 - Small reactive particles ($\sim 100\text{mm}$)
 - Only particles are thermally cycled
 - Independent component optimization
 - Easy material replacement
- Cons:
 - Particle conveyance
 - Beam-down optics



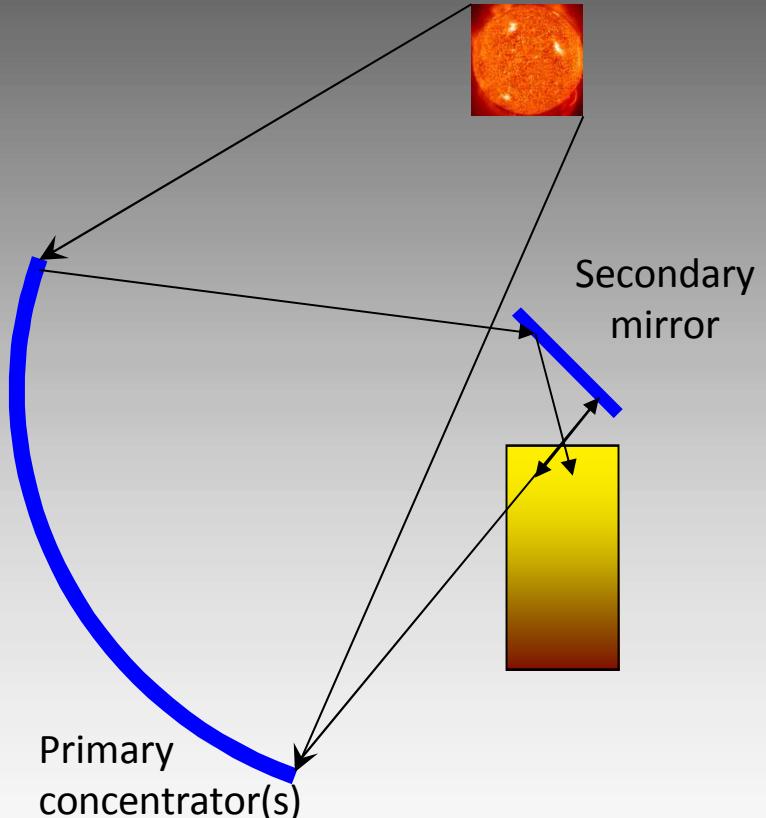
Solar Efficiency: An All Inclusive Metric

- ***Collection losses
(concentrator, re-radiation)***
- **Metal oxide heating**
- **Metal oxide thermal reduction**
- **Feedstock heating (steam)**
- **Pumping**
- **Electrical/mechanical**



**Solar is the *only*
primary energy used**

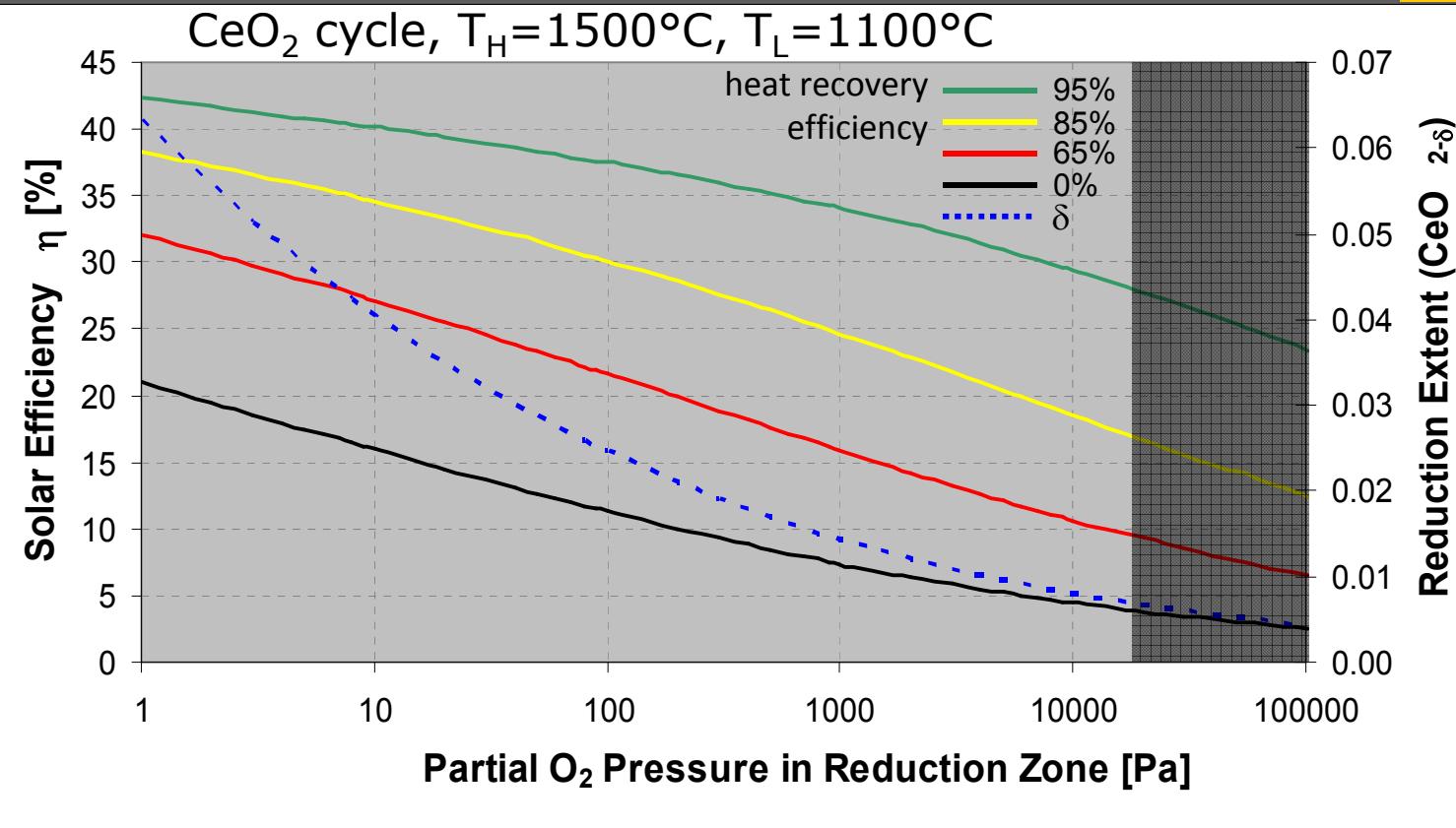
$$\eta = \frac{\dot{n}_{H_2/CO} \cdot HHV_{H_2/CO}}{P_S}$$



Packed Bed Reactor Performance Model

All mechanical work included, excess waste heat not included

$$\eta = \frac{\dot{n}_{H_2/CO} \cdot HHV_{H_2/CO}}{P_S}$$

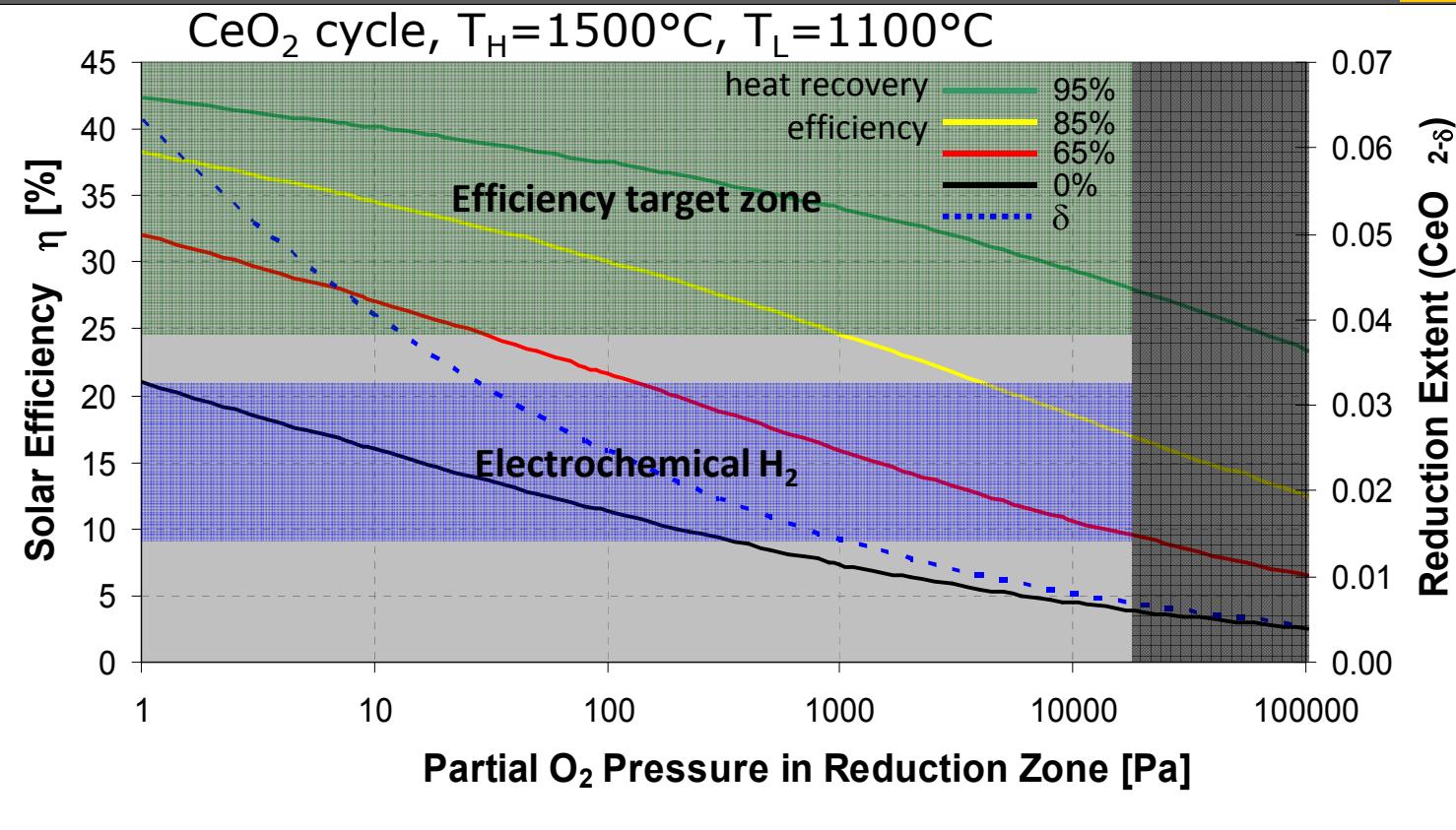


Most important: Oxide chemistry, heat recovery, pressure (p_{O₂})

Packed Bed Reactor Performance Model

All mechanical work included, excess waste heat not included

$$\eta = \frac{\dot{n}_{H_2/CO} \cdot HHV_{H_2/CO}}{P_S}$$



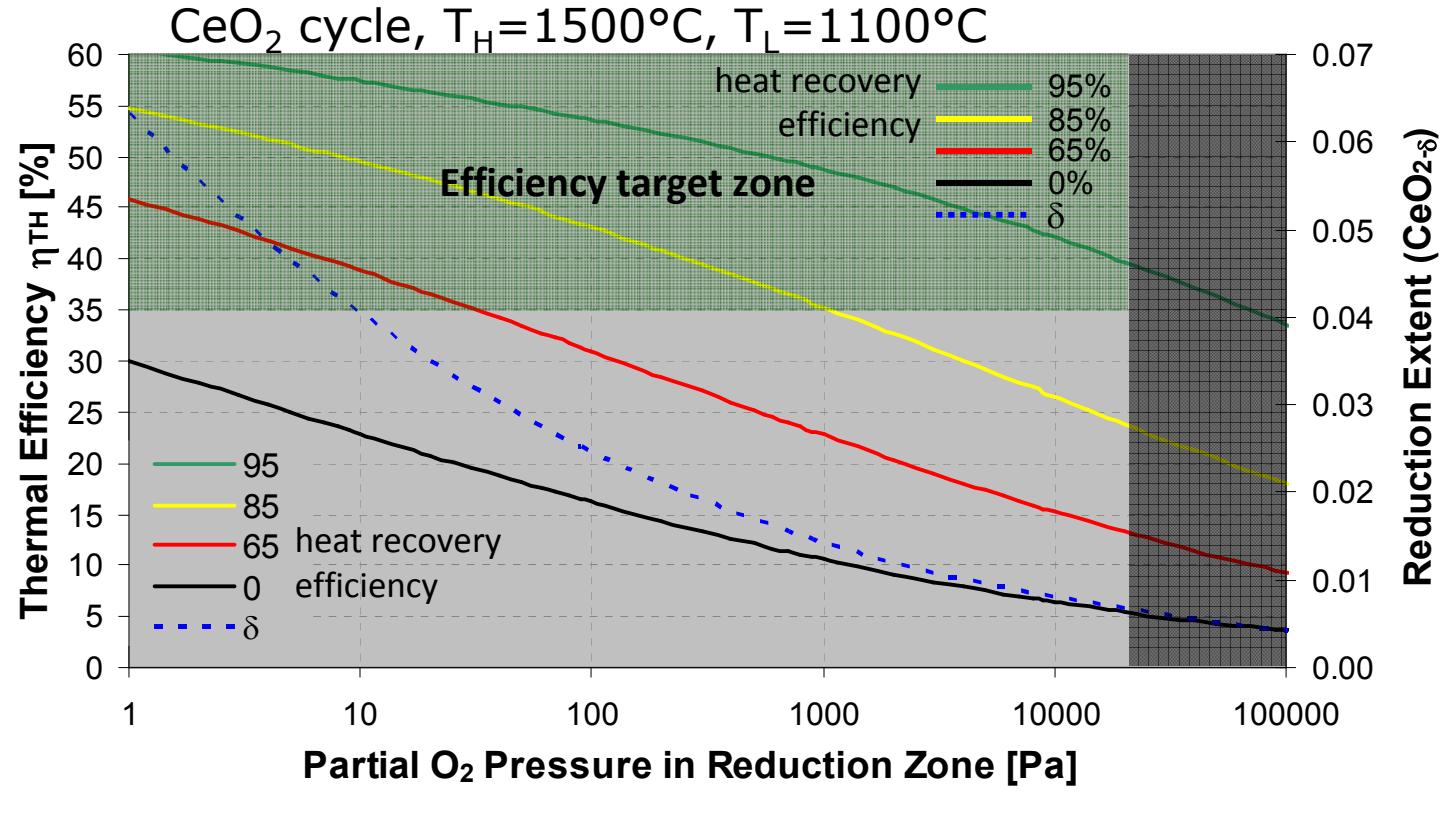
Most important: Oxide chemistry, heat recovery, pressure (p_{O₂})

Performance Model Predicts High Thermal Efficiency

Collection losses excluded

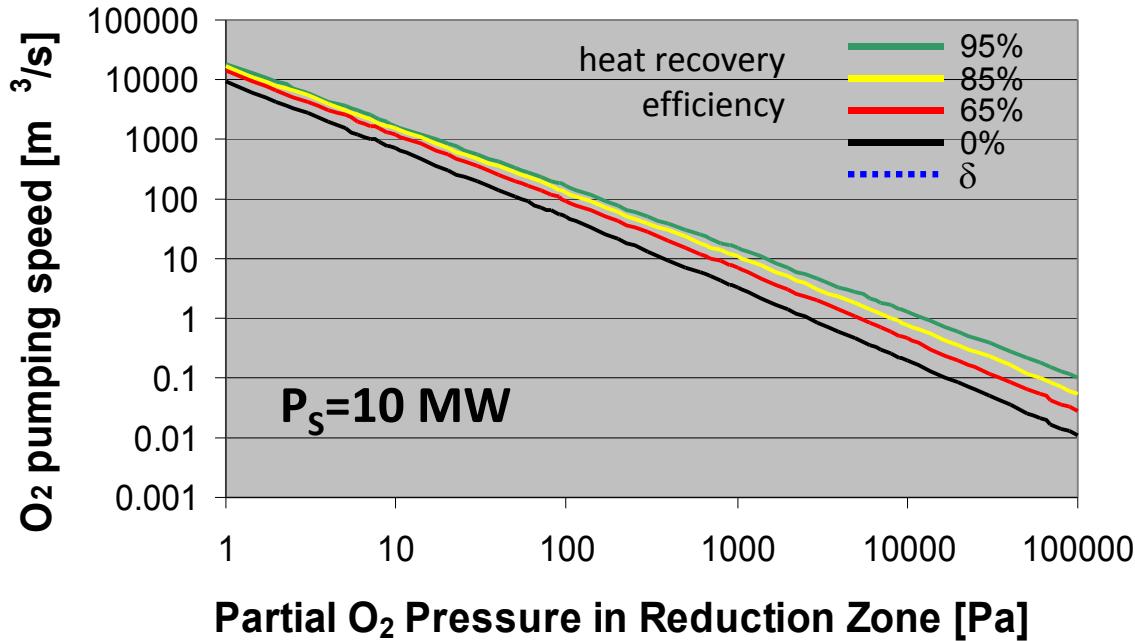
All mechanical work included, excess waste heat not included

$$\eta_{TH} = \frac{\dot{n}_{H_2/CO} \cdot HHV_{H_2/CO}}{P_{TH}}$$

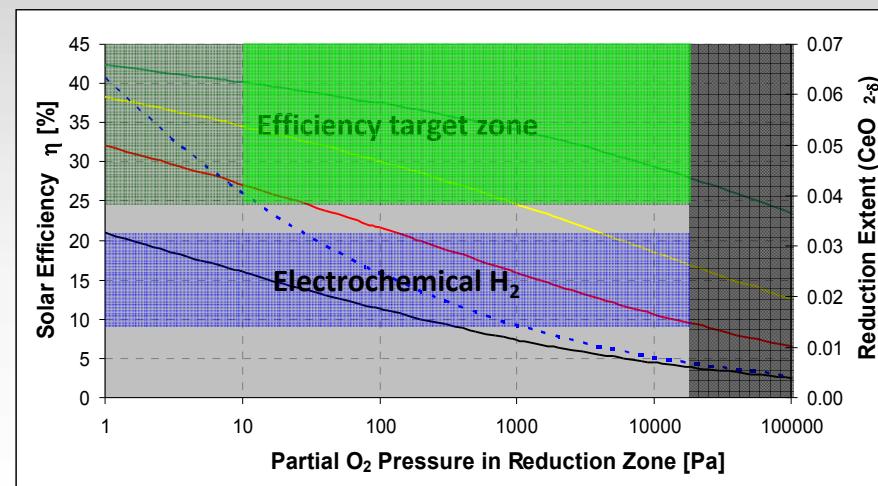


- Thermal Efficiency > 50% possible even with CeO₂
- Great materials and efficient reactors needed for success

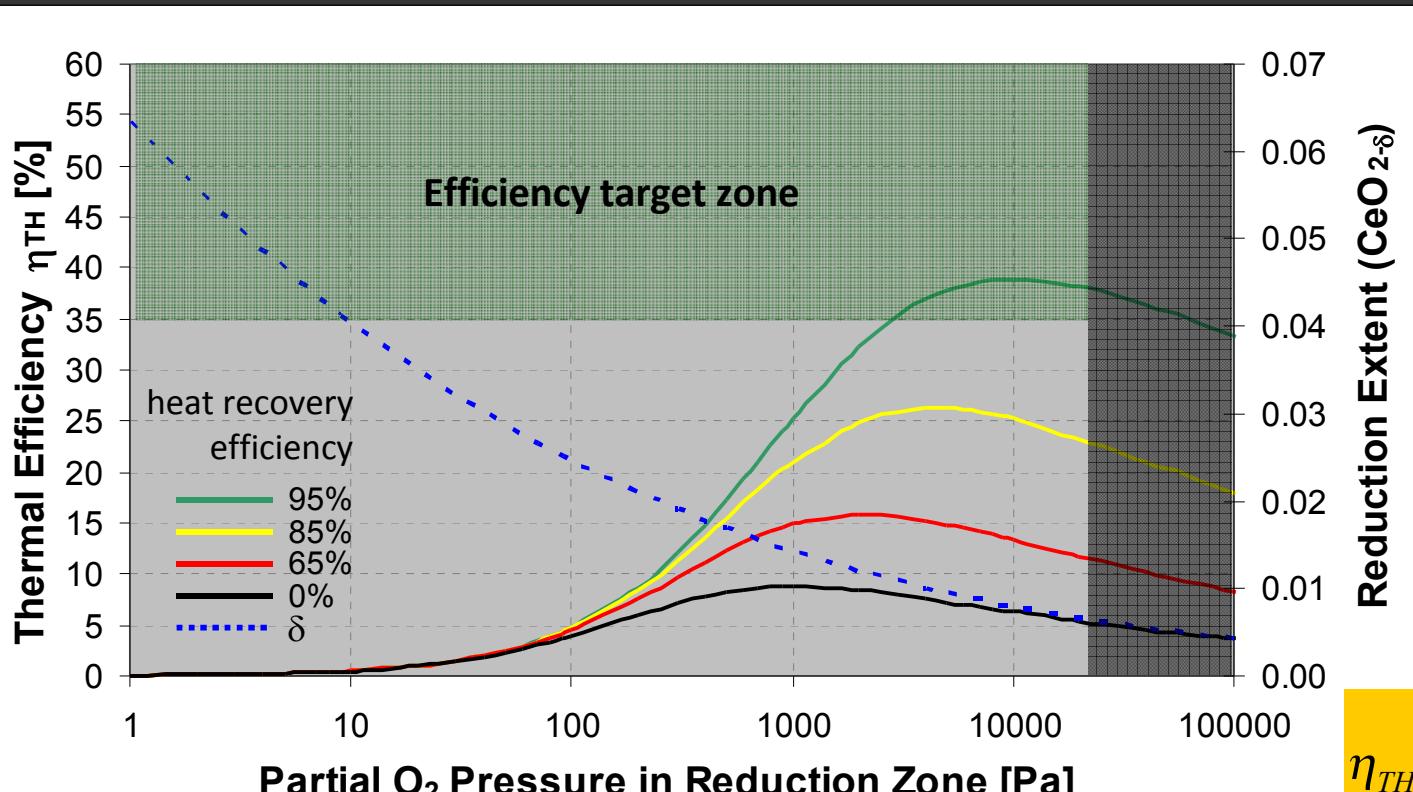
Low Pressure Limit: Pumping Speed



Pump size, not efficiency
may limit p_{O_2}

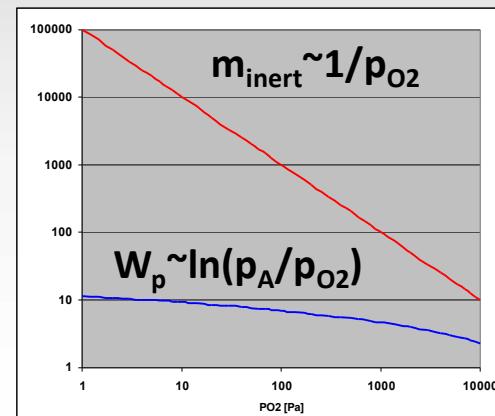


Inert Sweep Limit: Efficiency



$$\eta_{TH} = \frac{\dot{n}_{H_2/CO} \cdot HHV_{H_2/CO}}{P_{TH}}$$

Inert gas production and heating limit efficiency



Weakly Coupled Design and Operational Flexibility

Independent component optimization allows a design point efficiency choice

Identify working oxide



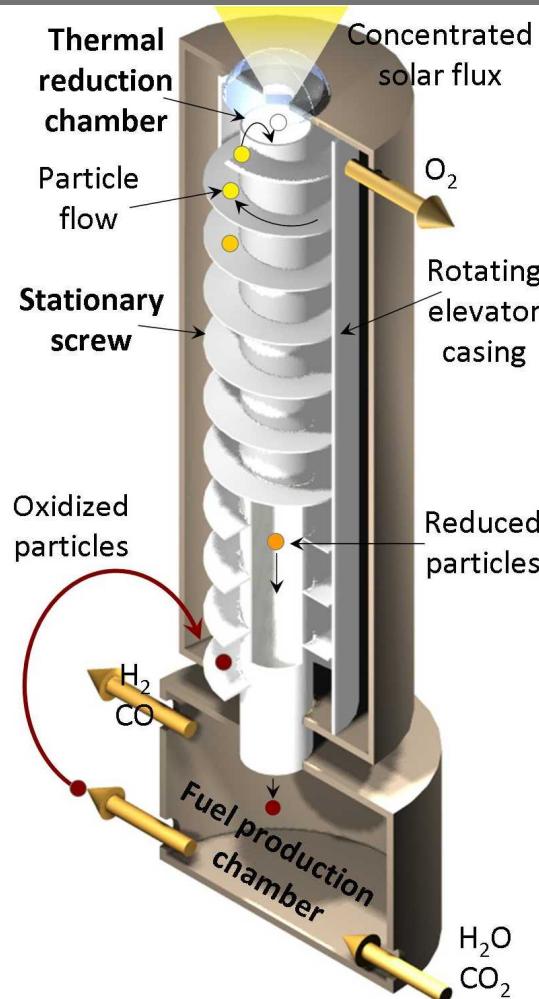
Set T_H , residence time, p_{O_2}



Set η_{HR} (size exchanger)



Set T_L , residence time



Weakly Coupled Design and Operational Flexibility

Independent component optimization allows a design point efficiency choice

Operational flexibility allows design point efficiency for $\delta P_s \sim 33\%$

Identify working oxide



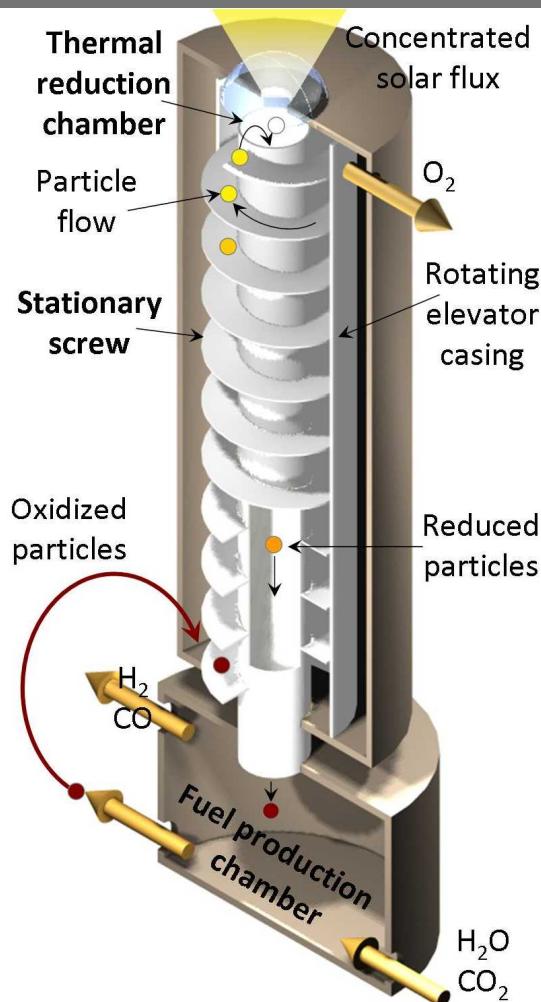
Set T_H , residence time, p_{O_2}



Set η_{HR} (size exchanger)



Set T_L , residence time



Low P_s

Decrease oxide flow to maintain $T_H \rightarrow$ increases $\eta_{HR} \rightarrow \eta$ is unchanged

High P_s

Increase oxide flow to maintain $T_H \rightarrow$ decreases $\eta_{HR} \rightarrow \eta$ is unchanged

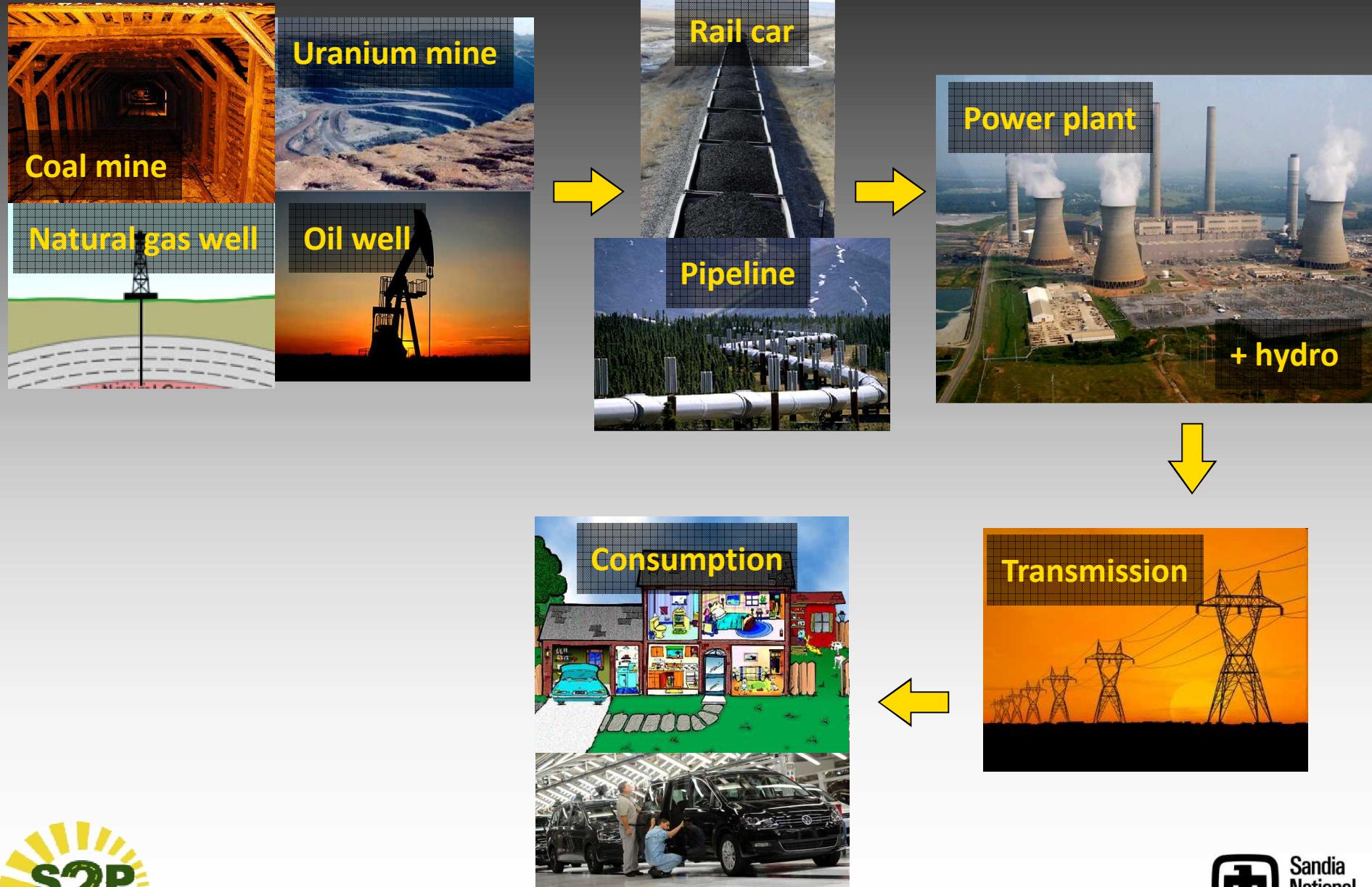
Reduction to Practice

- Demonstrating a good “paper design” is not always easy
- Technical challenges being addressed
 - Reactant properties
 - Material chemical durability
 - Material compatibility

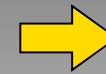
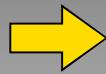
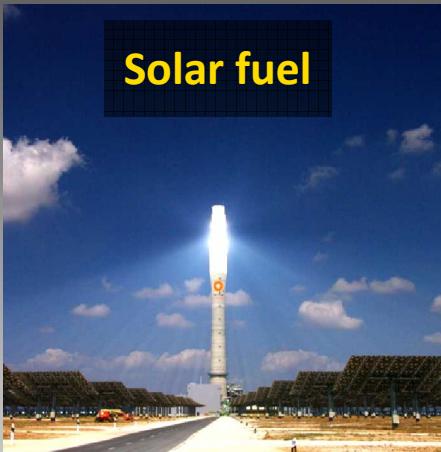
Packed Bed Reactor: Summary and Next Steps

- The packed bed particle reactor embodies all of the efficiency-driven attributes
- It has the potential to exceed considerably electrochemical efficiency for H₂ production
- Lowest p_{O₂} probably limited by pumping speed, not efficiency
- Efficiency through design, independent component optimization, and operational flexibility
- Conveyor/heat exchanger detailed design
- Gradually increasing temperature prototypes

The 19th & 20th Century US Electricity Paradigm



The 21th Century Energy Paradigm?



Local cogeneration
and consumption





Thank you for your attention.

Questions?

SUNSHINE

PETROL



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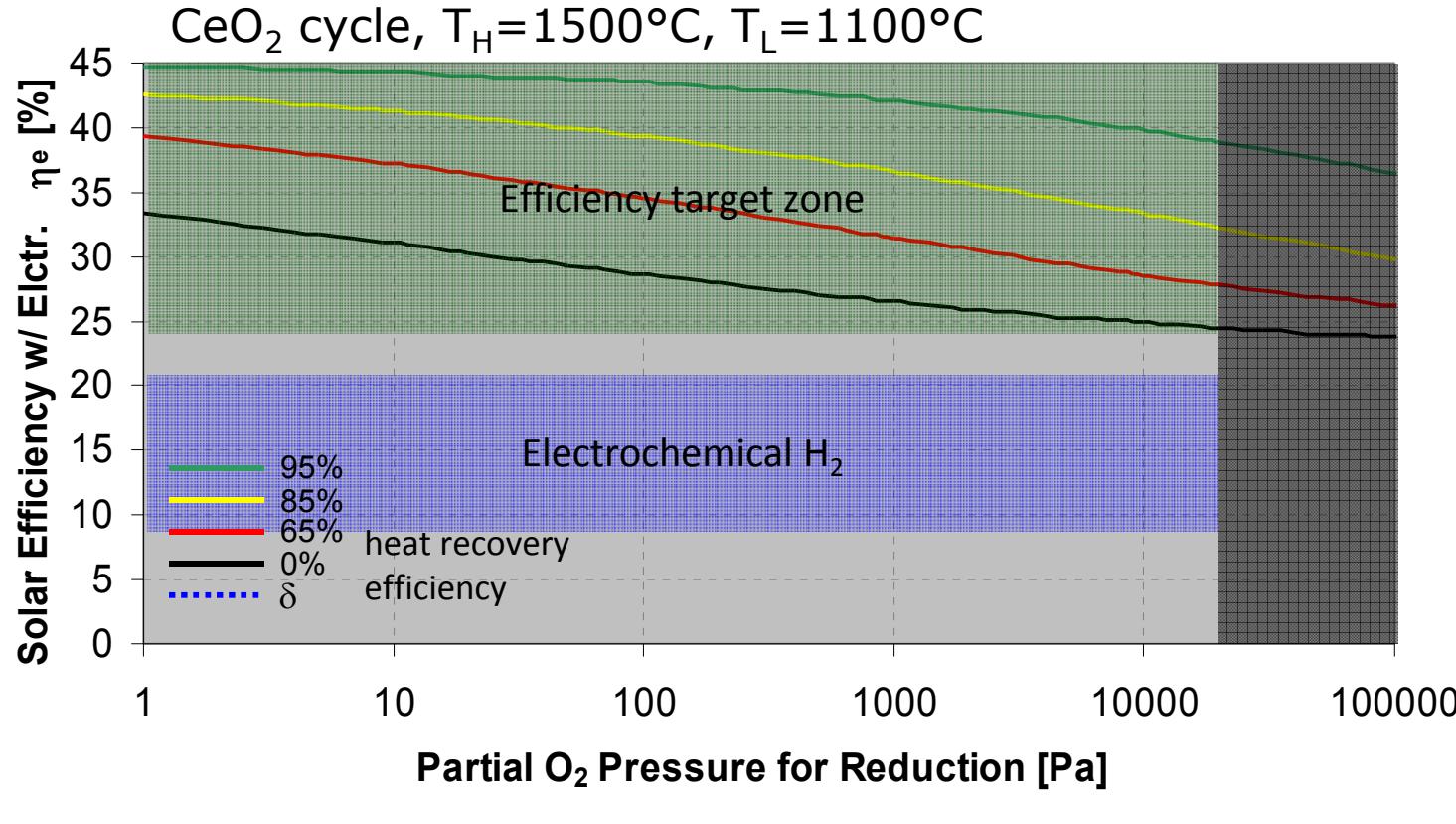


Hybrid Solar Efficiency: Use Waste Heat

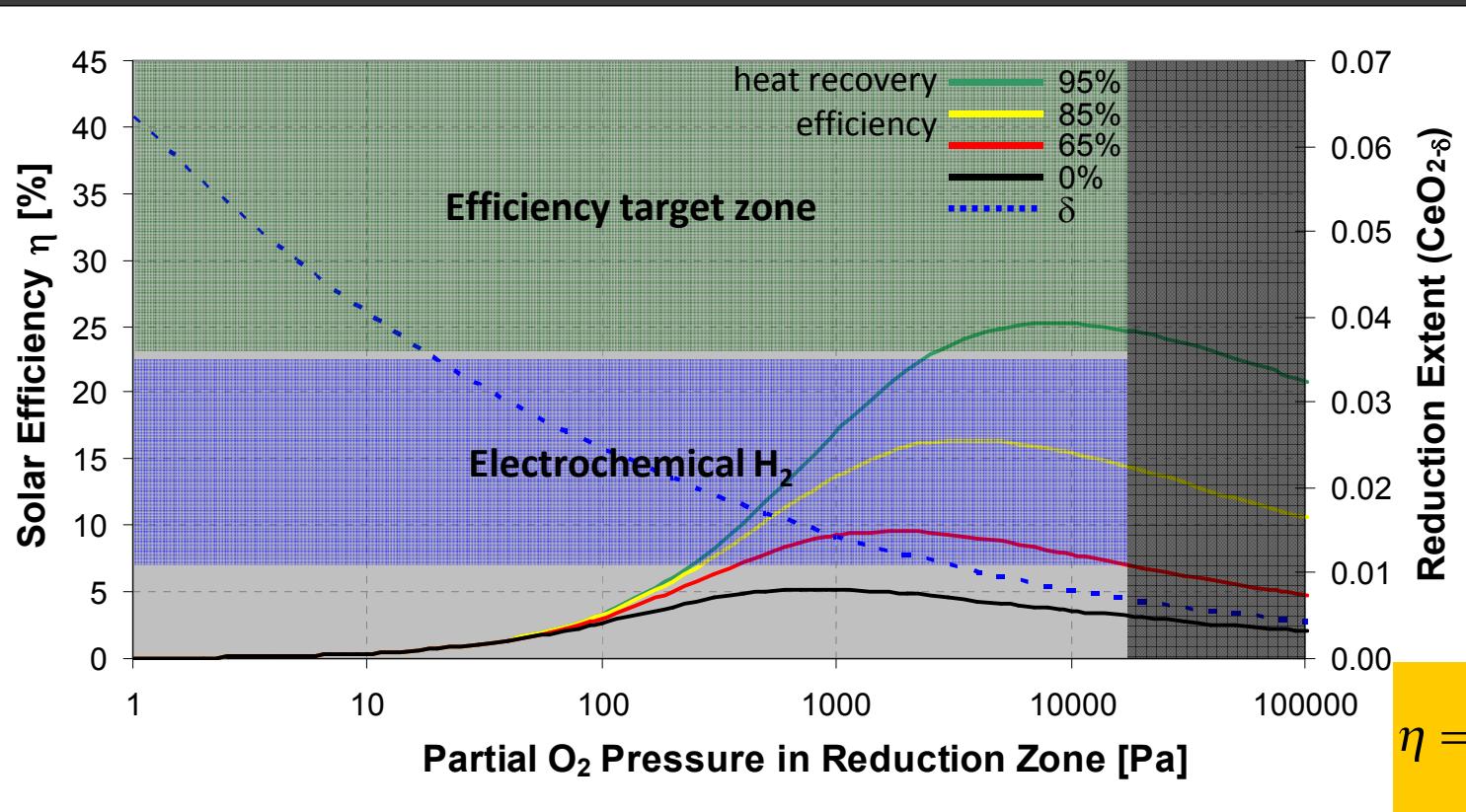
All mechanical work included

Excess waste heat used to produce electricity for electrolysis

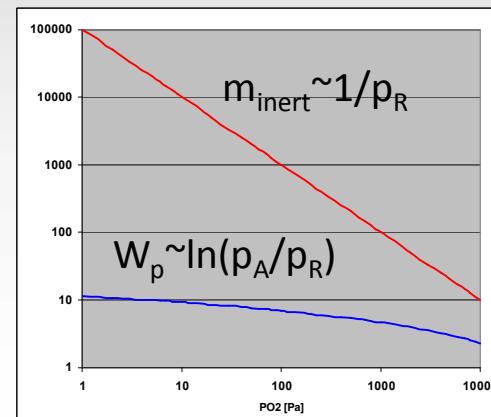
$$\eta = \frac{\dot{n}_{H_2/CO} \cdot HHV_{H_2/CO}}{P_S}$$



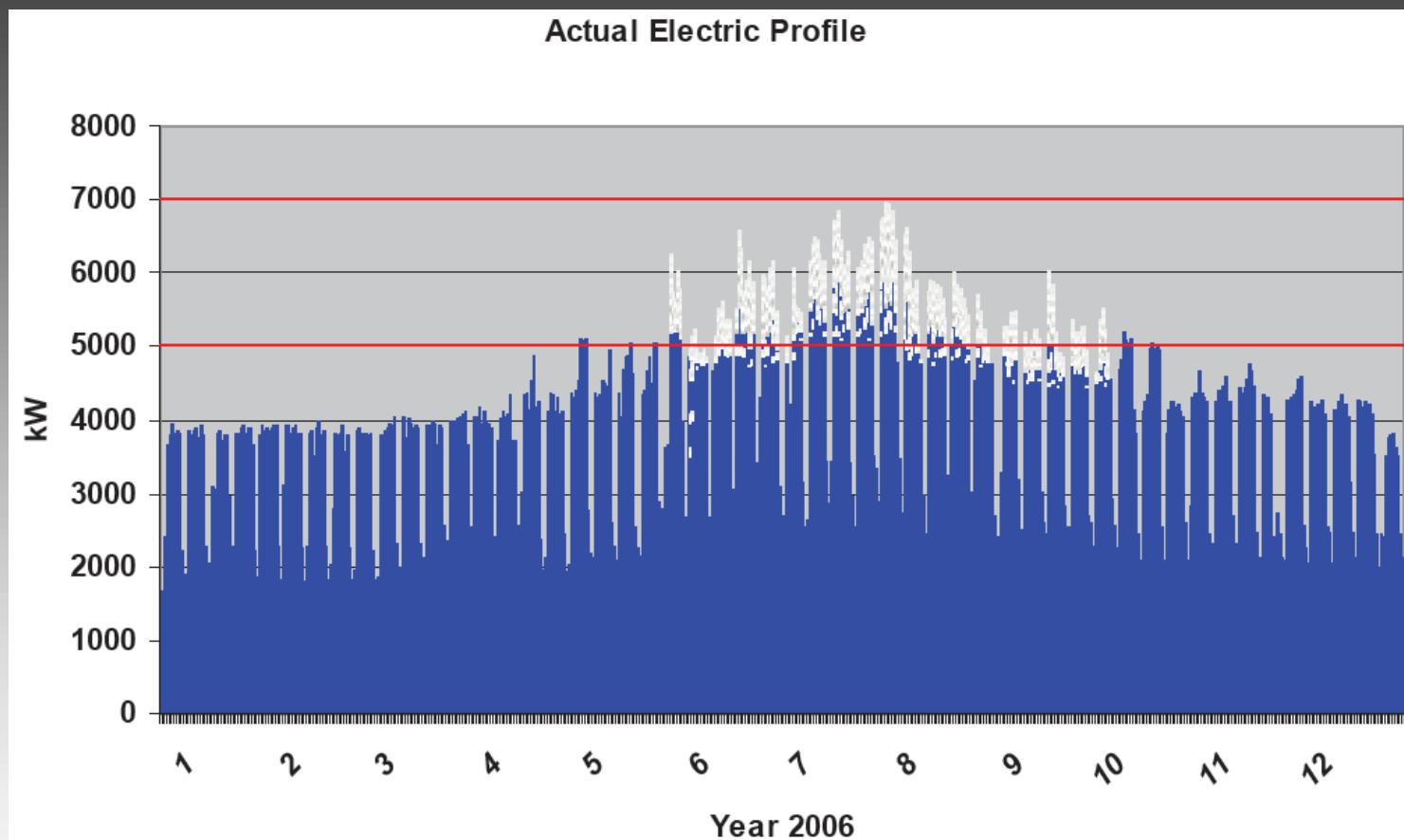
Inert Gas Sweep Limit: Efficiency



Inert gas production and heating limit efficiency



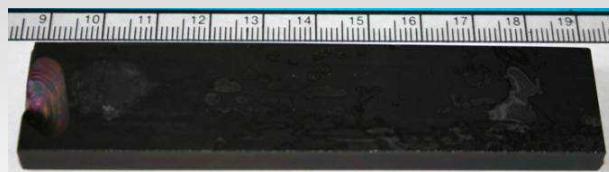
Using Heat for Cooling



Con Edison proposal for New York City steam cooling

Material Compatibility: High T Makes Reactions Easy

- The reactor and reactants should not react... With each other
- Ceria compatibility with
 - Alumina: 1550°C
 - Haynes 214 alloy: 1400°C
 - SiC: 1400°C
- Material strength is a concern
 - Creep in metals
 - Shock resistance in ceramics



CeO₂/SiC Hexoloy, 1400 °C
stagnant air, 3h



CeO₂/Al₂O₃, 1450 °C
stagnant air, 3h



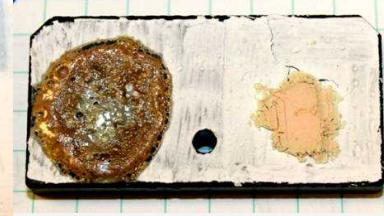
CeO₂/HA214, 1200 °C
10ppm O₂, 2h



CeO₂/HA214, 1400 °C
10ppm O₂, 2h

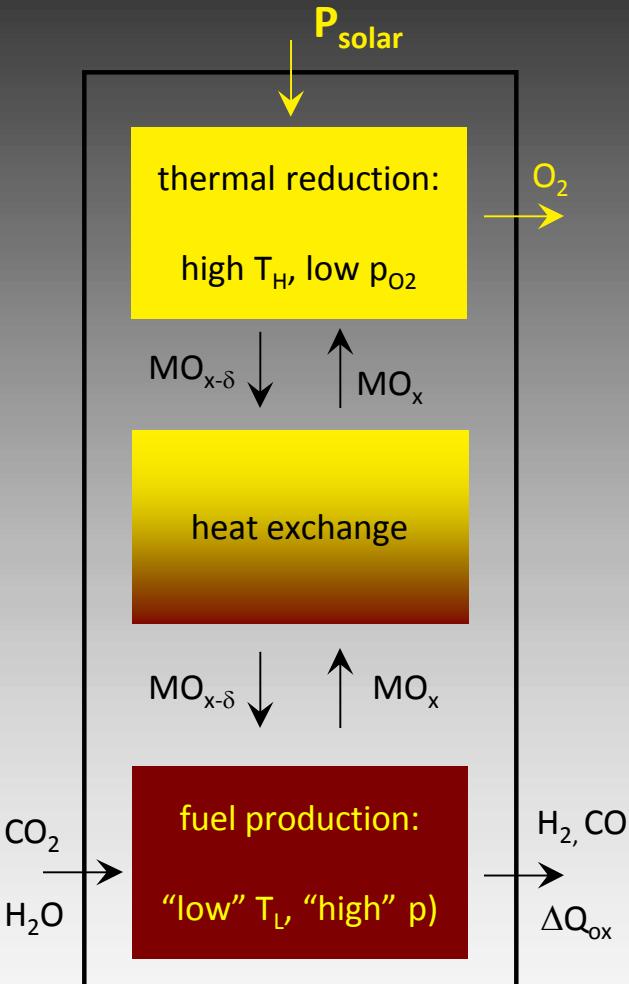


paint CeO₂/Al₂O₃/SiC, 1450 °C
stagnant air, 3h



Desirable Reactor Attributes: Efficiency Driven

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- Sensible energy recovery between T_H and T_L
- Continuous on-sun operation
- Pressure, temperature and product separation



Metal oxide cycle

Packed Bed Particle Reactor

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