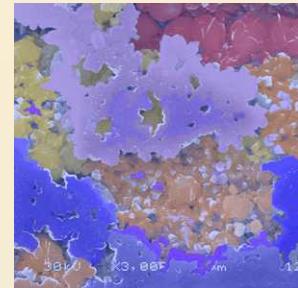
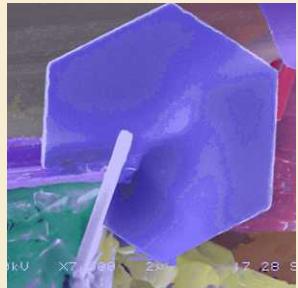


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## Speciation and Solubility of Aluminum in High Ionic Strength Solutions at Elevated Temperatures to 250 °C

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*This research is funded by the Salt Research and Development (Salt R&D) programs administered by the Office of Nuclear Energy (NE) of the U.S. Department of Energy.*



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# Outline of Presentation

- Introduction
  - Importance of Studying Aqueous Chemistry/Geochemistry of Aluminum at Elevated Temperatures
  - Speciation of Aluminum at 25°C and 150°C
  - The Pitzer Activity Coefficient Model
- Objectives of This Work
- Results
  - log K
  - Binary Interaction Parameters for  $\text{Na}^+ - \text{Al}(\text{OH})_4^-$
- Model Verification/Validation
- Summary

# INTRODUCTION: Aluminum

- Aluminum is the third most abundant element in the earth's crust, forming numerous minerals.
- Borosilicate glasses in which aluminum is a major component, are strong candidate waste forms for immobilization of high level nuclear waste (HLW).
- Sodalite,  $\text{Na}_8(\text{Al}_6\text{Si}_6\text{O}_{24})(\text{OH, Cl, I})_2$ , is a candidate waste form for electrorefinery contaminated salt wastes and radioactive iodine waste.
- Hanford and Savannah River Tank wastes have significant inventories of aluminum and silica.
- Solutions associated with geological repositories such as those in salt formations and deep boreholes are of high ionic strengths.

# INTRODUCTION: Aluminum Speciation at 25°C

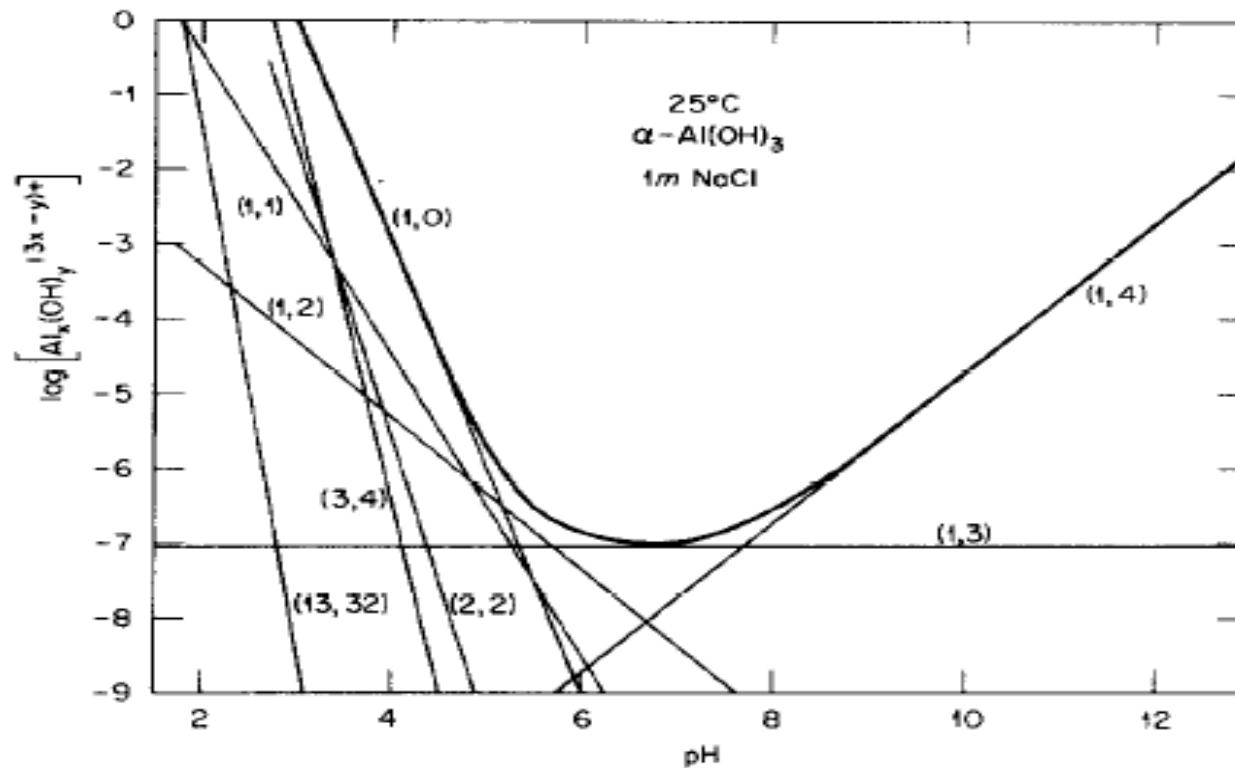
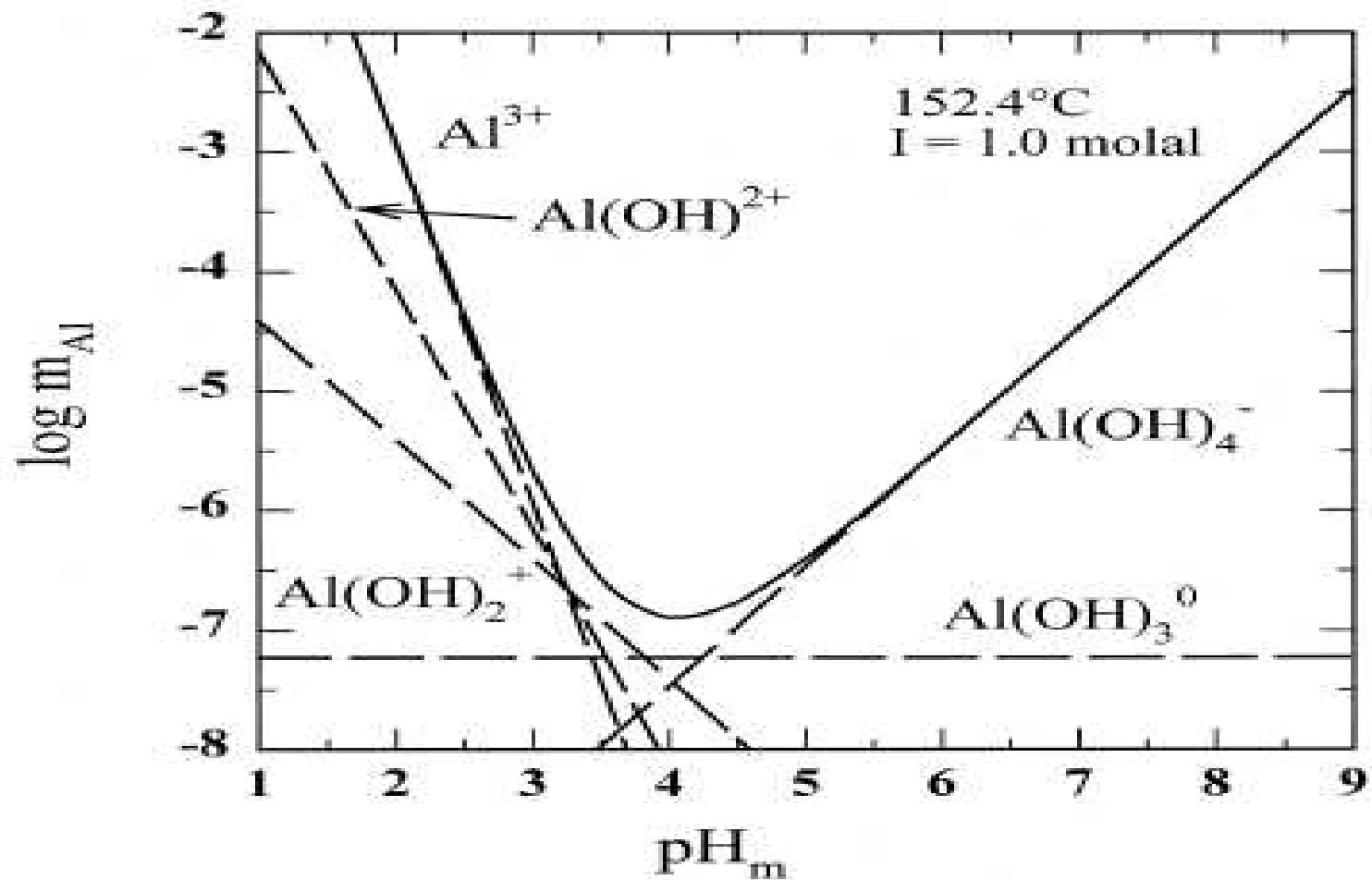


FIG. 1. Molal concentrations of aluminum hydroxyl species in equilibrium with  $\alpha\text{-Al(OH)}_3$  (gibbsite) in 1 molal NaCl solution at 25°C and 1 bar. The straight lines represent the concentrations of individual species  $(x, y)$ , indicating the stoichiometries of species of the type  $Al_x(OH)_y^{3x-y}$ . The heavy curve is the total concentration of all aqueous aluminum species in equilibrium with gibbsite at these conditions. This figure is taken from HITCH et al. (1980).

# INTRODUCTION: Aluminum Speciation at 150°C

From Palmer et al. (2001)



# INTRODUCTION: Activity Coefficient

## Models—low to moderate ionic strength

- Davies Equation:

$$\log \gamma_i = -A_\gamma z_i^2 \left( \frac{\sqrt{I_m}}{1 + \sqrt{I_m}} + 0.3I_m \right)$$

- Extended Debye-Hückel (or WATEQ Debye-Hückel) Equation:

$$\log \gamma_i = -A_\gamma z_i^2 \times \frac{\sqrt{I_m}}{1 + B_{DH} a_i^0 \sqrt{I_m}} - b_i I_m$$

- B dot Equation:

$$\log \gamma_i = -A_\gamma z_i^2 \times \frac{\sqrt{I_m}}{1 + B_{DH} a_i^0 \sqrt{I_m}} + \dot{B} I_m$$

# INTRODUCTION: Activity Coefficient Model—up to ~3.5 m



- Brønsted-Guggenheim-Scatchard Specific Ion Interaction Theory (SIT) Model

$$\log \gamma_i = -A_\gamma z_i^2 \times \frac{\sqrt{I_m}}{1 + 1.5\sqrt{I_m}} + \sum_k \varepsilon(i, k) m_k$$

# INTRODUCTION: Activity Coefficient Model—to high ionic strength, up to saturation of most salts

- Pitzer Model, using mean activity coefficient for NaCl as an example:

$$\ln \gamma_{\pm} = -A_{\phi} \left[ \frac{\sqrt{I_m}}{1+1.2\sqrt{I_m}} + \frac{2}{1.2} \ln(1+1.2\sqrt{I_m}) \right] + m \left\{ 2\beta^{(0)} + \frac{2\beta^{(1)}}{\alpha^2 \times I_m} \left[ 1 - (1 + \alpha\sqrt{I_m} - \frac{\alpha^2 I_m}{2}) e^{-\alpha\sqrt{I_m}} \right] \right\} + \frac{3m^2}{2} C^{\phi}$$

# Pitzer Model for $\text{Na}^+ - \text{Al}(\text{OH})_4^-$ interaction



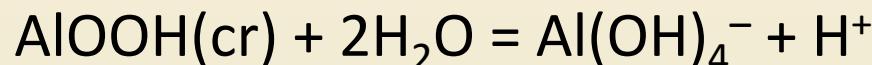
- Wesolowski (1992) recommended two sets of Pitzer parameters for  $\text{Na}^+ - \text{Al}(\text{OH})_4^-$  interaction.
- One set at 25°C was calculated based on the equations of Pitzer and Mayorga (1973).
  - This set of Pitzer parameters was successfully adopted in the Al-Si high ionic strength model to 100°C to model solubilities of zeolite A (Xiong, 2013), assuming they are constant over 25°C-100°C.
- The other set at 0°C-100°C was calculated based on the equations of Simonson et al. (1989).
  - This set was used by Königsberger et al. (2006).

# Objectives of This Work

- The need to obtain Pitzer parameters for  $\text{Na}^+ - \text{Al}(\text{OH})_4^-$  interaction to higher temperatures:
  - The peak temperatures in the near field for geological repositories for HLW/used nuclear fuel in salt formations are up to 200°C or slightly higher.
  - The peak temperatures in the near field for deep boreholes for HLW/used nuclear fuel are expected to be higher than 200°C.
- The first objective of this work is to evaluate Pitzer binary interaction parameters for  $\text{Na}^+ - \text{Al}(\text{OH})_4^-$  as a function of temperature to 250°C.
- The second objective is to evaluate the temperature dependence of the psi parameters,  $\Psi_{\text{Na-Al(OH)4-OH}}$ .

# Experimental Data Used for Evaluation

- Equilibrium quotients for the following reaction in NaCl solutions up to 5.0 m from Palmer et al. (2001) are used for evaluation of binary parameters for  $\text{Na}^+ - \text{Al(OH)}_4^-$  up to 250°C:



$$Q_{\text{S4}} = [\text{Al(OH)}_4^-][\text{H}^+]$$

- Boehmite ( $\text{AlOOH(cr)}$ ) solubility data in NaOH solutions to 170°C from Russell et al. (1955) are used for evaluation of  $\Psi_{\text{Na-Al(OH)}_4\text{-OH}}$ .

# Auxiliary Data

- Binary interaction parameters for  $\text{H}^+ - \text{Cl}^-$  valid to 375°C from Holmes et al. (1987)
- Binary interaction parameters for  $\text{Na}^+ - \text{Cl}^-$  valid to 300°C from Pitzer et al. (1984)
- Binary interaction parameters for  $\text{Na}^+ - \text{OH}^-$  valid to 350°C from Pabalan and Pitzer (1987)
- Modeling platform: EQ3/6 Version 8.0a (Wolery et al., 2010; Xiong, 2011) with data0.ypf (Wolery, and Jarek. 2003)

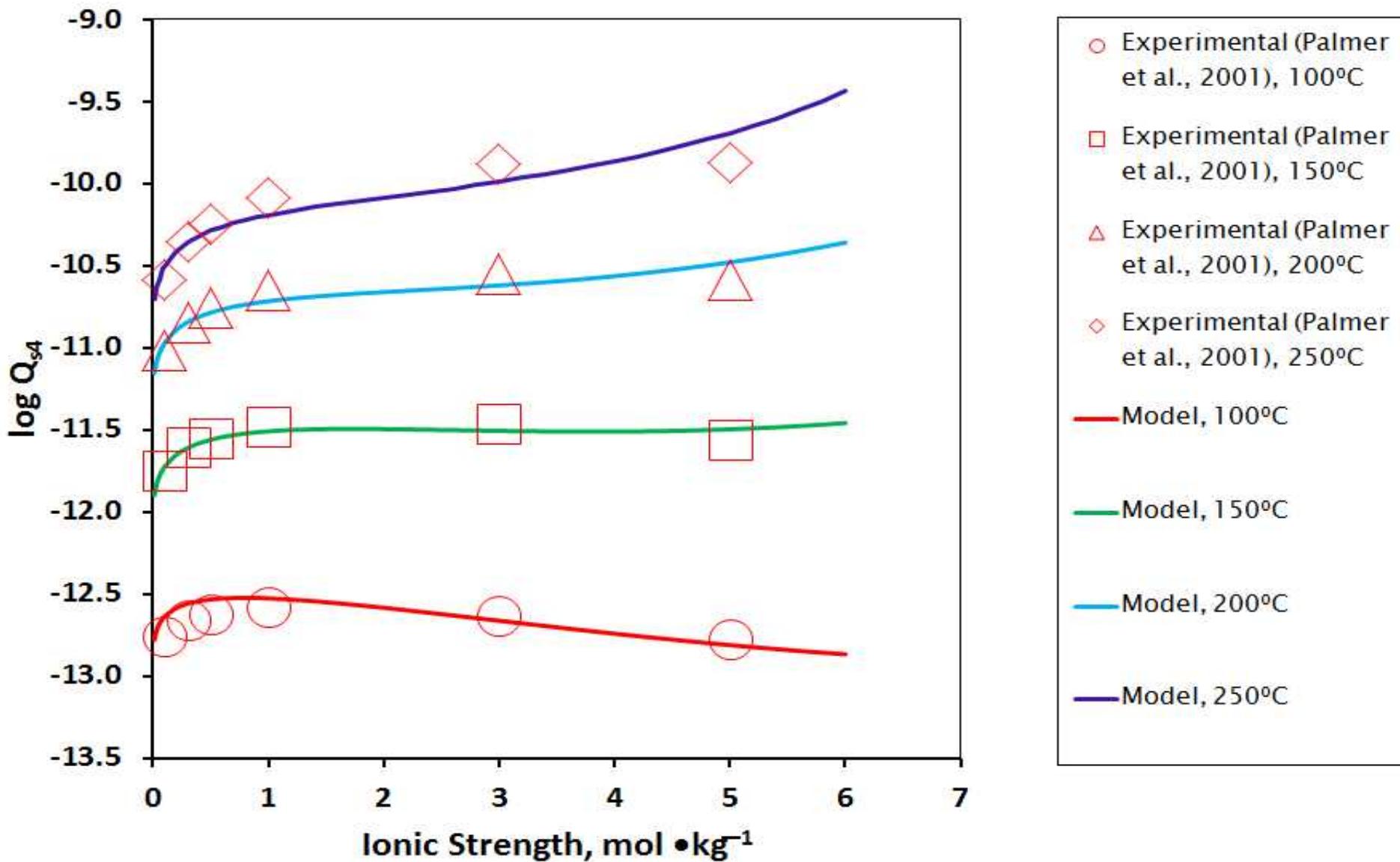
# Modeling Results

- $\log K_{s4}$ 
  - $T = 100^\circ\text{C}$ ,  $\log K_{s4} = -12.89$
  - $T = 150^\circ\text{C}$ ,  $\log K_{s4} = -12.03$
  - $T = 200^\circ\text{C}$ ,  $\log K_{s4} = -11.34$
  - $T = 250^\circ\text{C}$ ,  $\log K_{s4} = -10.98$
- Pitzer Parameters for  $\text{Na}^+ - \text{Al}(\text{OH})_4^-$ 
  - $\beta^{(0)} = 0.051$  from Wesolowski (1992), constant
  - $T = 100^\circ\text{C}$ ,  $\beta^{(1)} = 0.330$ ,  $C^\phi = -0.00550$
  - $T = 150^\circ\text{C}$ ,  $\beta^{(1)} = 0.376$ ,  $C^\phi = -0.00834$
  - $T = 200^\circ\text{C}$ ,  $\beta^{(1)} = -0.223$ ,  $C^\phi = 0.00745$
  - $T = 250^\circ\text{C}$ ,  $\beta^{(1)} = -0.720$ ,  $C^\phi = 0.00673$

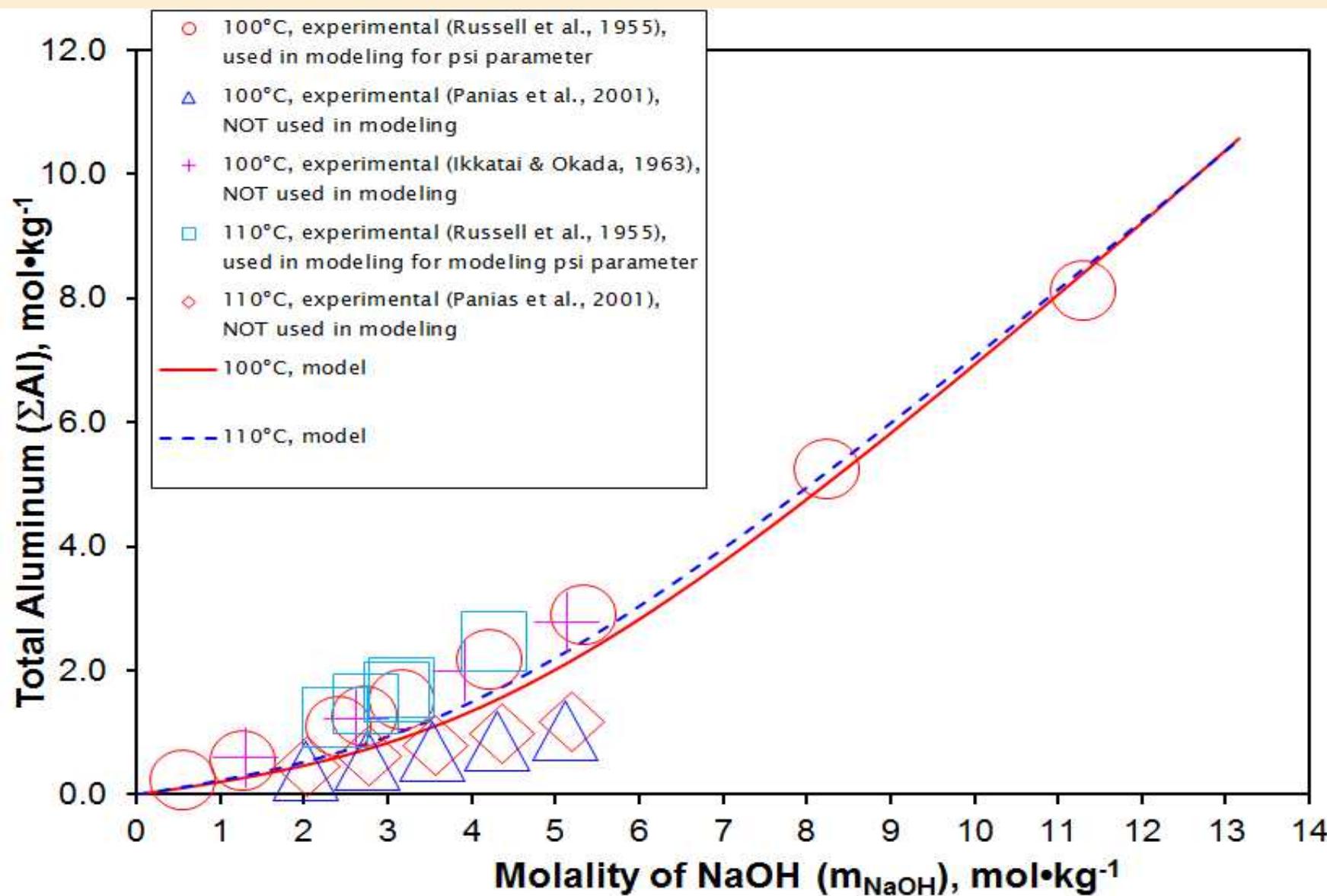
# Modeling Results

- Pitzer Parameters for  $\text{OH}^- - \text{Al}(\text{OH})_4^-$ 
  - $\theta = 0.014$  from Wesolowski (1992), constant
- Pitzer Parameters for  $\text{Na}^+ - \text{OH}^- - \text{Al}(\text{OH})_4^-$ 
  - $T = 100^\circ\text{C}$ ,  $\Psi = 0.129$
  - $T = 110^\circ\text{C}$ ,  $\Psi = 0.139$
  - $T = 120^\circ\text{C}$ ,  $\Psi = 0.135$
  - $T = 130^\circ\text{C}$ ,  $\Psi = 0.132$
  - $T = 140^\circ\text{C}$ ,  $\Psi = 0.128$
  - $T = 150^\circ\text{C}$ ,  $\Psi = 0.125$
  - $T = 160^\circ\text{C}$ ,  $\Psi = 0.122$
  - $T = 170^\circ\text{C}$ ,  $\Psi = 0.119$

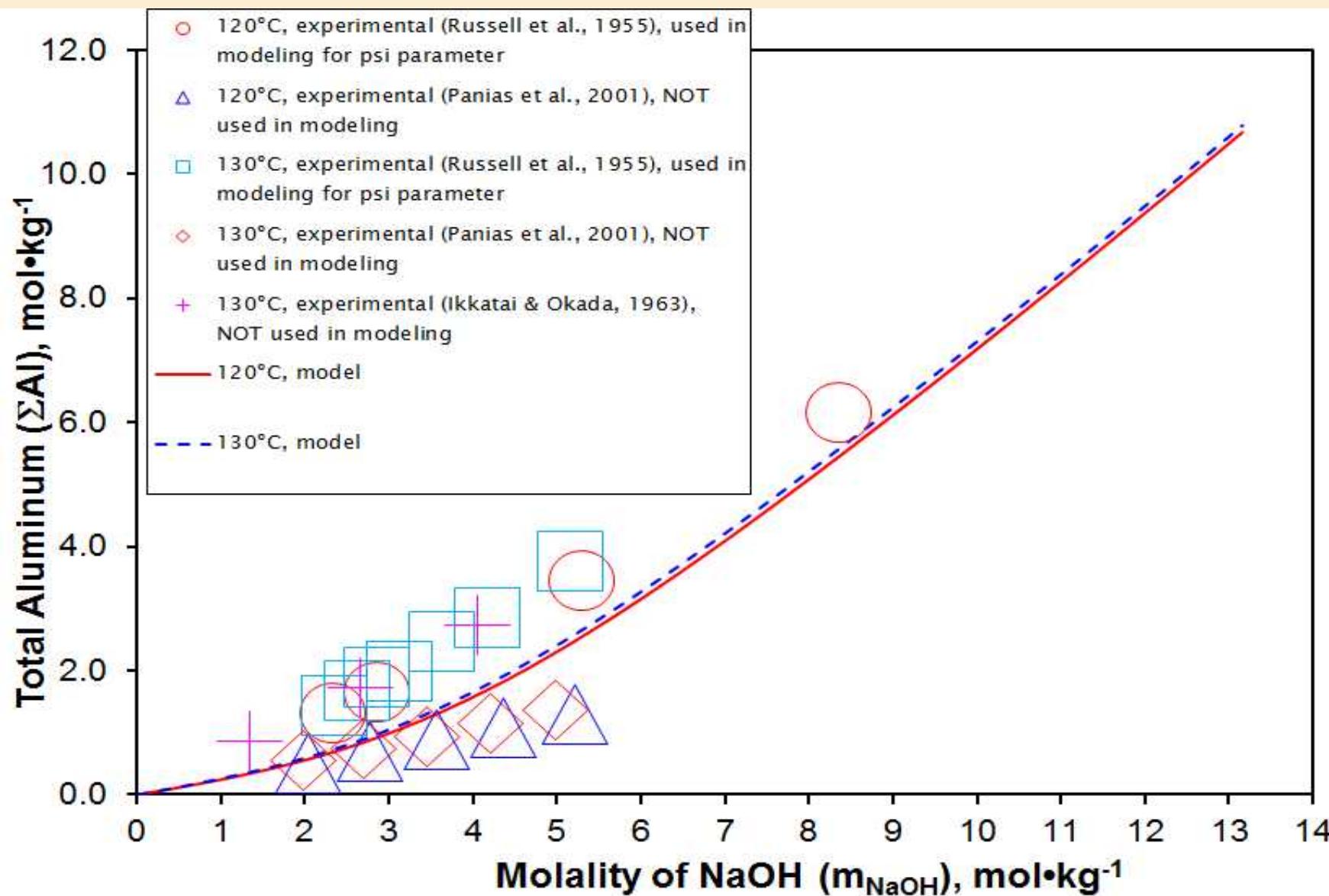
# Model Verification



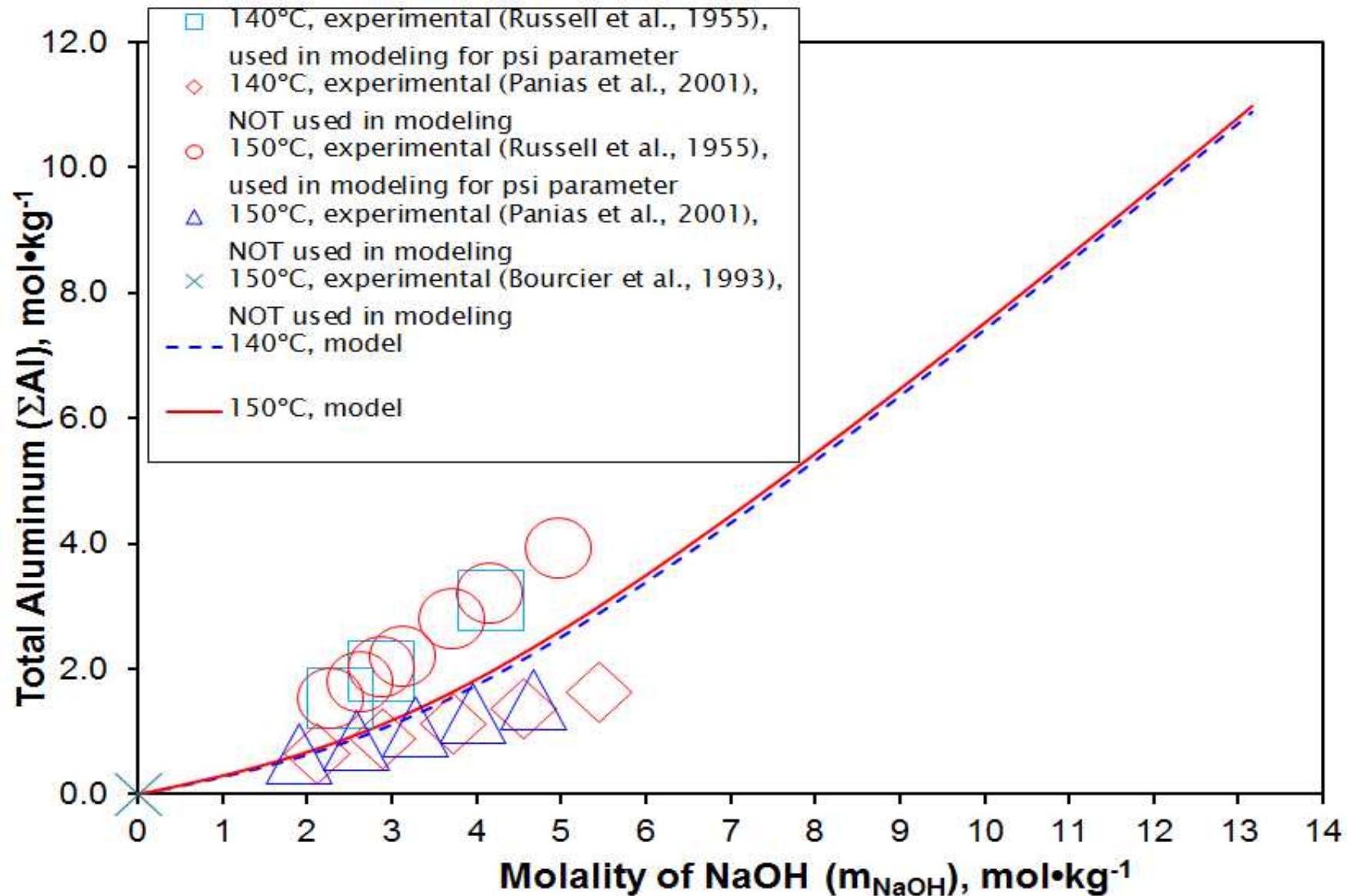
# Model Verification/Validation



# Model Verification/Validation



# Model Verification/Validation



# Summary

- In this study, a Pitzer model for the Na-Cl-OH-Al(OH)<sub>4</sub> system is tentatively established to 250°C to ionic strength of 5.0 m, and to 170°C to ionic strength of 13 m.
- Solubilities of boehmite in NaOH solutions predicted by the model are in good agreement with independent experimental data.

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