

# Physical Fluid Dynamics in Reciprocating Engines

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# Fluid mechanics and mixing processes are critical aspects of all reciprocating engine technologies

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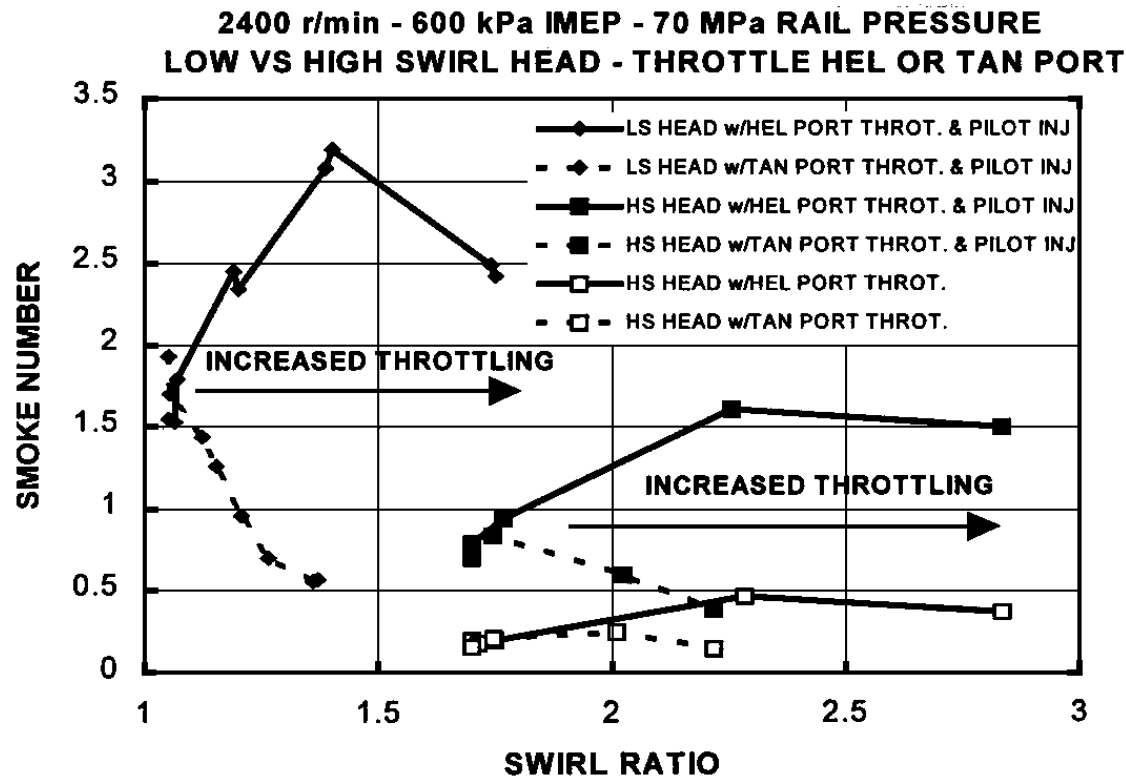
- SI engines:** Breathing efficiency, tumble generation and breakdown, turbulent flame kernel initiation and subsequent propagation
- DISI engines:** + spray/flow interactions, mixture formation processes
- Diesel engines:** + swirl effects, ignition, late-cycle mixing processes for soot and CO burnout
- HCCI/CAI engines:** + mixture stratification, thermal stratification

The subtle interaction of air motion and fuel spray...

...is the cornerstone of development of future ultra-low emissions and high performance diesel engines

*Ricardo Consulting Engineers, 1994*

# Characterization of the flow by global parameters is insufficient



Krieger, et al., SAE 972683

- Gross differences in soot emissions are seen at the same swirl ratio
- Trends observed with changing swirl ratio are opposite

These differences must be associated with differences in the details of the mean flow structure and associated turbulence generation mechanisms

- Building blocks
  - Understanding the momentum equations
  - Conservation of angular momentum
  - Rotational kinetic energy
- Mean flow examples
  - Tumble and swirl flows
  - Squish-swirl interaction
  - Spray-swirl interaction
- Turbulence
  - Identifying the sources
  - Close-up of swirl effects
  - Examples



# Understanding the mean momentum equations is key to understanding the flow development

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## Radial-momentum

$$\frac{\overline{D}\langle U_r \rangle}{\overline{D}t} - \frac{\langle U_\theta \rangle^2}{r} = -\frac{1}{\rho} \frac{\partial \langle P \rangle}{\partial r} - \left( \frac{1}{r} \frac{\partial (r \langle u_r'^2 \rangle)}{\partial r} + \frac{1}{r} \frac{\partial \langle u_r' u_\theta' \rangle}{\partial \theta} + \frac{\partial \langle u_r' u_z' \rangle}{\partial z} - \frac{\langle u_\theta'^2 \rangle}{r} \right)$$

but  $\langle U_\theta \rangle^2 + \langle u_\theta'^2 \rangle = \langle U_\theta^2 \rangle$

$$\frac{\overline{D}\langle U_r \rangle}{\overline{D}t} - \frac{\langle U_\theta^2 \rangle}{r} = -\frac{1}{\rho} \frac{\partial \langle P \rangle}{\partial r} - \left( \frac{1}{r} \frac{\partial (r \langle u_r'^2 \rangle)}{\partial r} + \frac{1}{r} \frac{\partial \langle u_r' u_\theta' \rangle}{\partial \theta} + \frac{\partial \langle u_r' u_z' \rangle}{\partial z} \right)$$

neglecting turbulent diffusion

Radial Acceleration	=	Centripetal Forces	$\Leftrightarrow$	Pressure Forces
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# Understanding the mean momentum equations is key to understanding the flow development

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## Tangential-momentum

$$\frac{\overline{D}\langle U_\theta \rangle}{\overline{D}t} + \frac{\langle U_r \rangle \langle U_\theta \rangle}{r} = -\frac{1}{\rho} \frac{1}{r} \frac{\partial \langle P \rangle}{\partial \theta} - \left( \frac{1}{r} \frac{\partial (r \langle u'_r u'_\theta \rangle)}{\partial r} + \frac{1}{r} \frac{\partial \langle u'^2_\theta \rangle}{\partial \theta} + \frac{\partial \langle u'_\theta u'_z \rangle}{\partial z} + \frac{\langle u'_r u'_\theta \rangle}{r} \right)$$

but we can simplify greatly by writing in terms of  $\langle rU_\theta \rangle$ :

$$\frac{\overline{D}\langle rU_\theta \rangle}{\overline{D}t} = -\frac{1}{\rho} \frac{\partial \langle P \rangle}{\partial \theta} - \left( \frac{1}{r} \frac{\partial (r^2 \langle u'_r u'_\theta \rangle)}{\partial r} + \frac{1}{r} \frac{\partial (r \langle u'^2_\theta \rangle)}{\partial \theta} + \frac{\partial (r \langle u'_\theta u'_z \rangle)}{\partial z} \right)$$

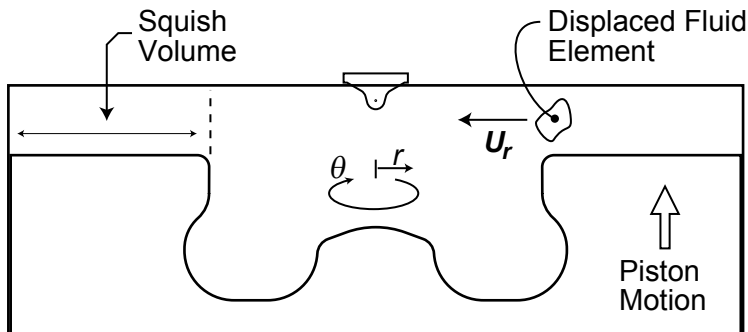
neglecting turbulent diffusion and tangential pressure gradients,

Angular momentum is conserved

$$\langle U_\theta \rangle = \frac{r_0 \langle U_\theta \rangle_0}{r}$$

# The squish/swirl interaction

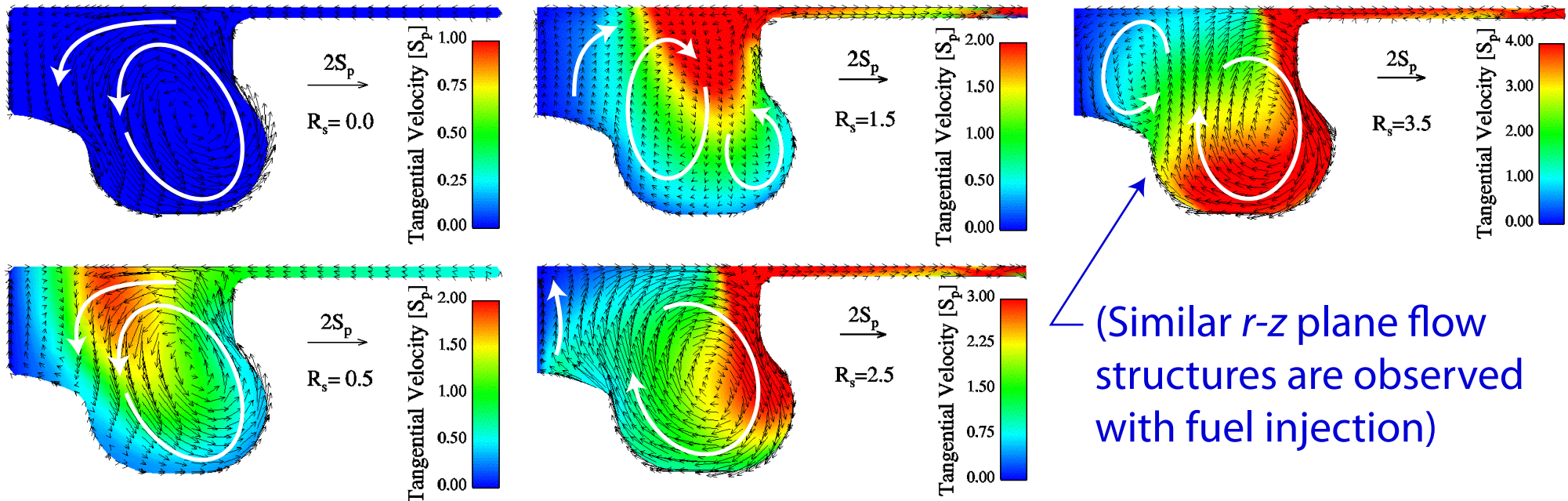
The dominant factor affecting the inward penetration of a fluid element is centrifugal force...



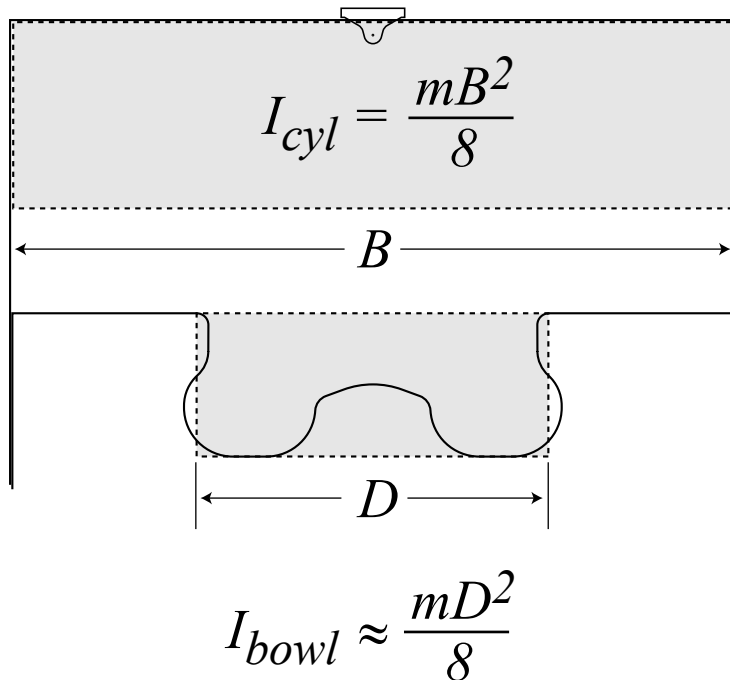
$$\frac{\overline{D}\langle rU_\theta \rangle}{\overline{D}t} = 0 \Rightarrow \langle U_\theta \rangle = \frac{r_0 \langle U_\theta \rangle_0}{r} \quad (\theta\text{-mom})$$

$$\frac{\overline{D}\langle U_r \rangle}{\overline{D}t} = -\frac{1}{\rho} \frac{\partial \langle P \rangle}{\partial r} + \frac{\langle U_\theta^2 \rangle}{r} \quad (r\text{-mom})$$

Near-TDC Flow Structure:



# Squish-swirl interaction also changes the rotational kinetic energy of the flow



Compressing the flow into the bowl and conserving angular momentum

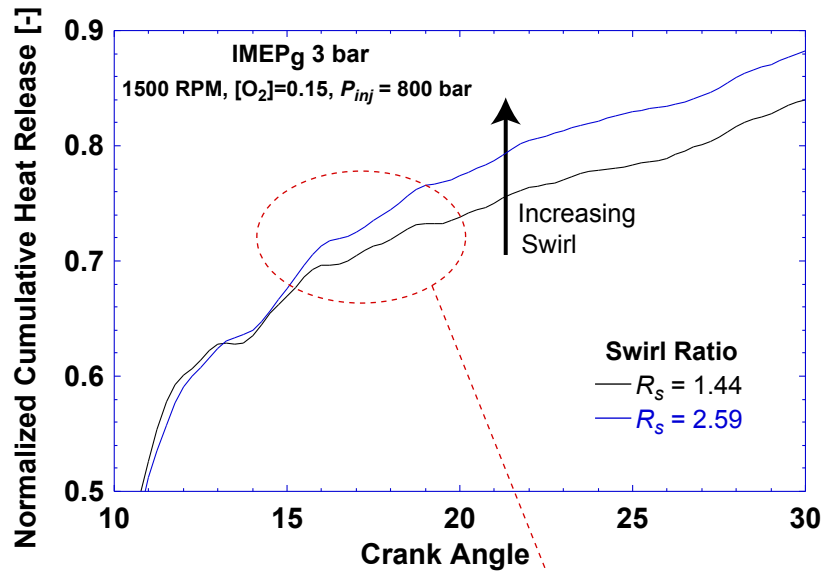
$$\frac{\Omega_{bowl}}{\Omega_{cyl}} \approx \frac{I_{cyl}}{I_{bowl}} \approx \frac{B^2}{D^2}$$

The kinetic energy ratio is

$$\frac{K.E._{bowl}}{K.E._{cyl}} = \frac{I_{bowl} \Omega_{bowl}^2}{I_{cyl} \Omega_{cyl}^2} \approx \frac{B^2}{D^2}$$

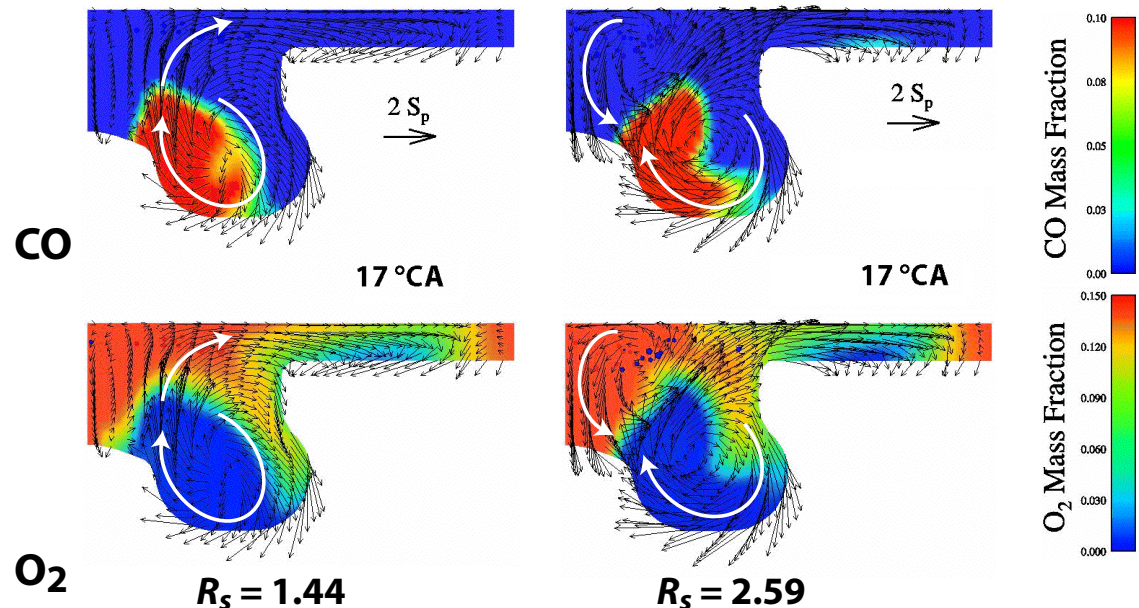
- For typical conservation efficiencies of angular momentum ( $\approx 60\%$ ) and  $B/D \approx 2$ , a 40–50% increase in rotational kinetic energy is expected.
- The source of this increased energy is work done by the piston.

# Flow structures formed by a similar “spray–swirl” interaction can enhance mixing rates during combustion



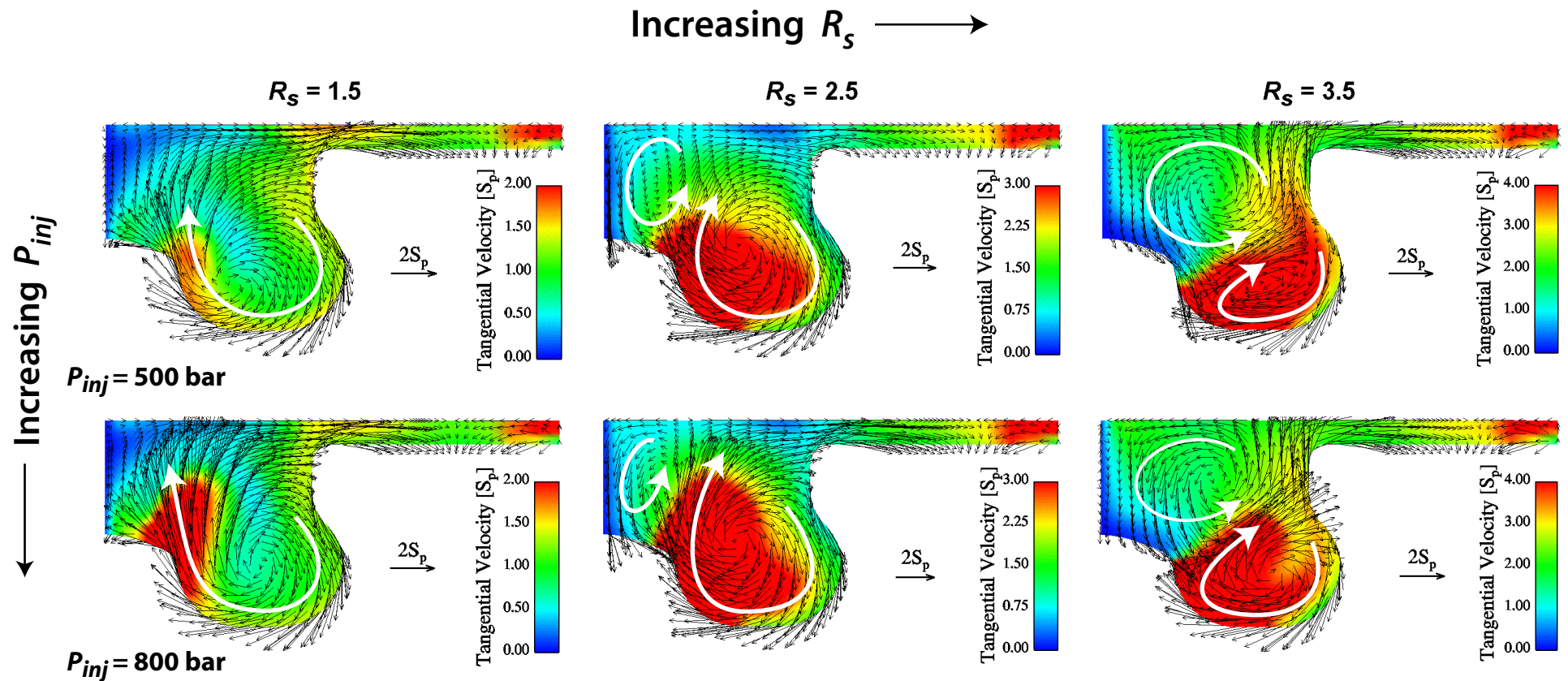
Increased swirl increases the late-cycle rate of heat release

Numerical simulations indicate that the increased heat release due to beneficial flow structures formed with higher swirl levels



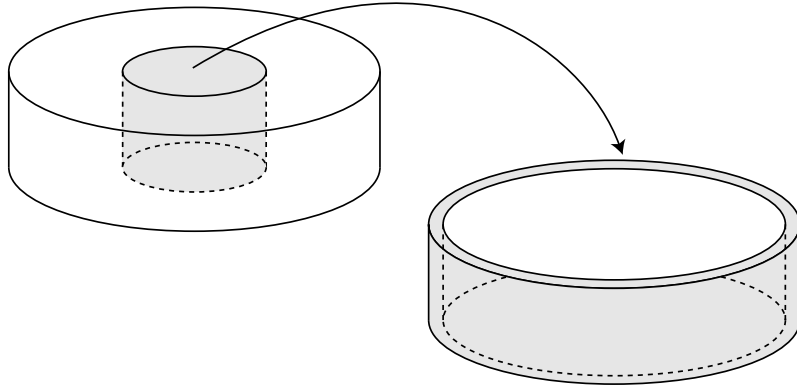


# These structures are also formed from the displacement of high angular momentum ( $\Omega$ ) fluid



- High swirl limits inward penetration of high- $\Omega$  fluid, and promotes its rapid return towards larger radii: Bowl vortex is smaller and lower in the bowl
- Higher  $P_{inj}$  promotes inward and upward penetration of high- $\Omega$  fluid: Bowl vortex is larger and higher in the bowl
- Flow structures are under the designer's control via  $R_s$ ,  $P_{inj}$ , bowl geometry and spray targeting — Speed and load effects follow inductively

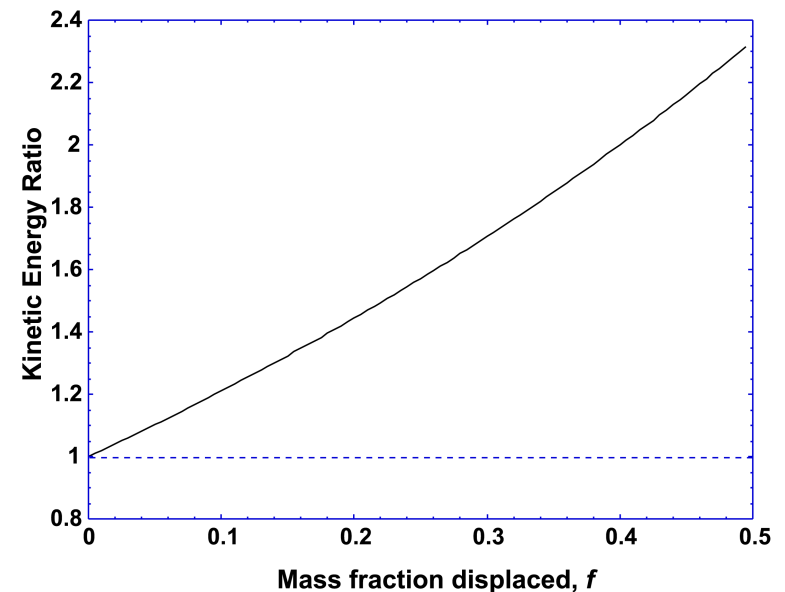
# Displacement of angular momentum can lead to an increase in the bulk rotational kinetic energy



Fuel injection transports entrained low momentum fluid to the bowl periphery, high momentum fluid is displaced inward

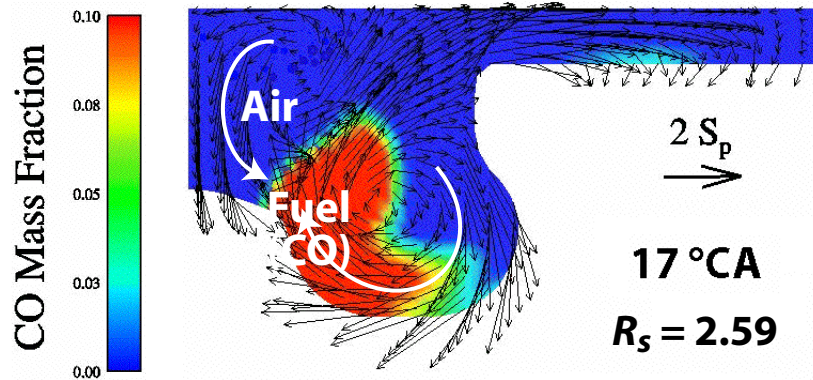
An idealized 2-zone analysis, conserving total angular momentum, suggests that the increase in rotational kinetic energy may be significant

The source of this additional rotational energy is the kinetic energy of the fuel spray



Kinetic energy of the fuel spray can be stored in the bulk rotational motion for later release

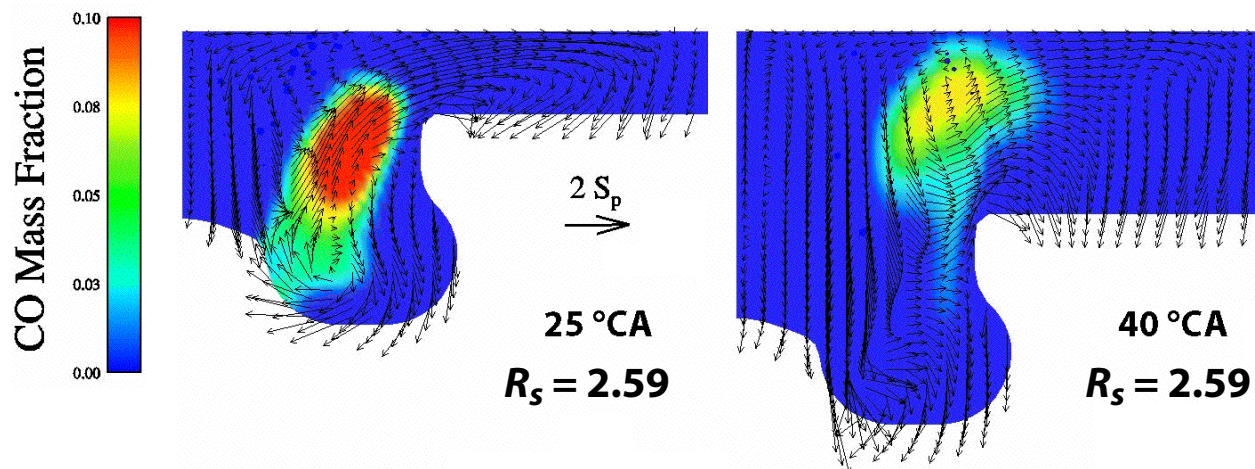
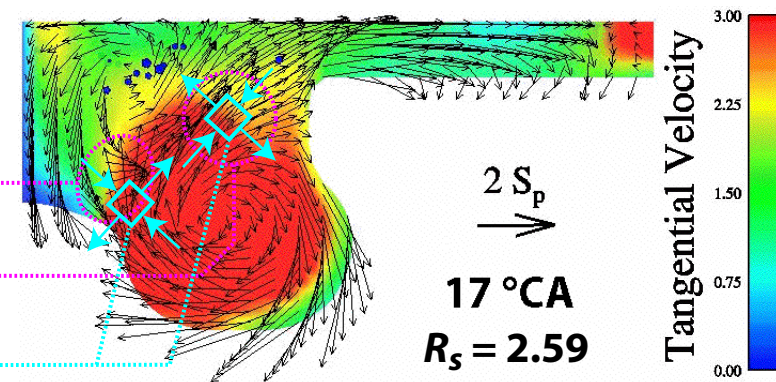
# These structures form an effective mixing *system*



- Counter-rotating vortices transport unburned fuel and fresh air to a common interface

- These vortices also generate high levels of flow turbulence at the interface via:

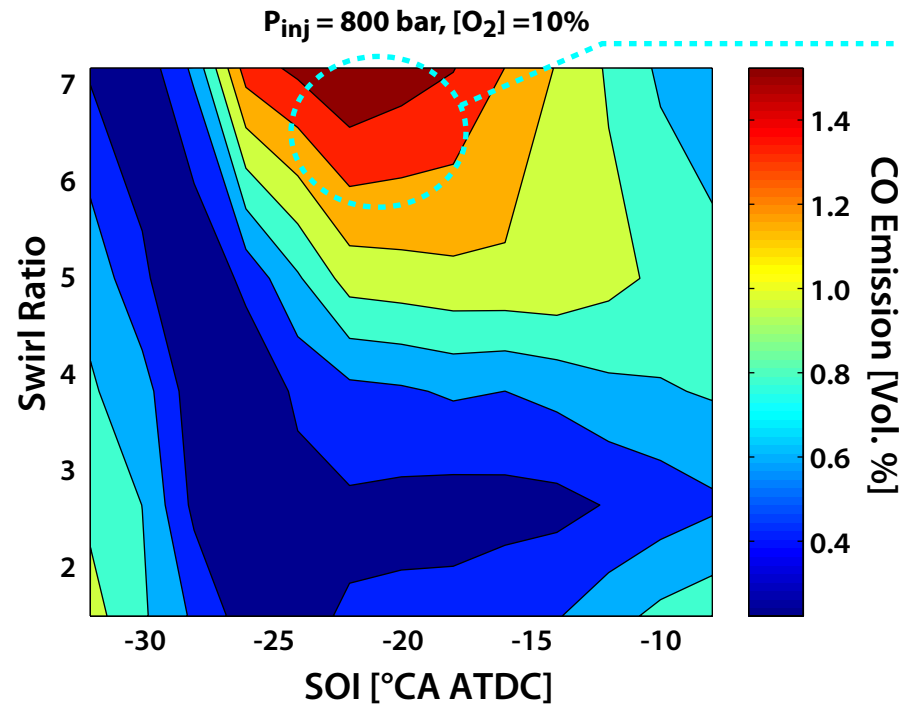
- High shear ( + swirl velocity gradients)
- Negative swirl velocity gradients
- High rates of  $r$ - $z$  plane deformation



- Late in the cycle, these structures transport remaining unburned fuel (CO, soot) into the squish volume... *Careful!*

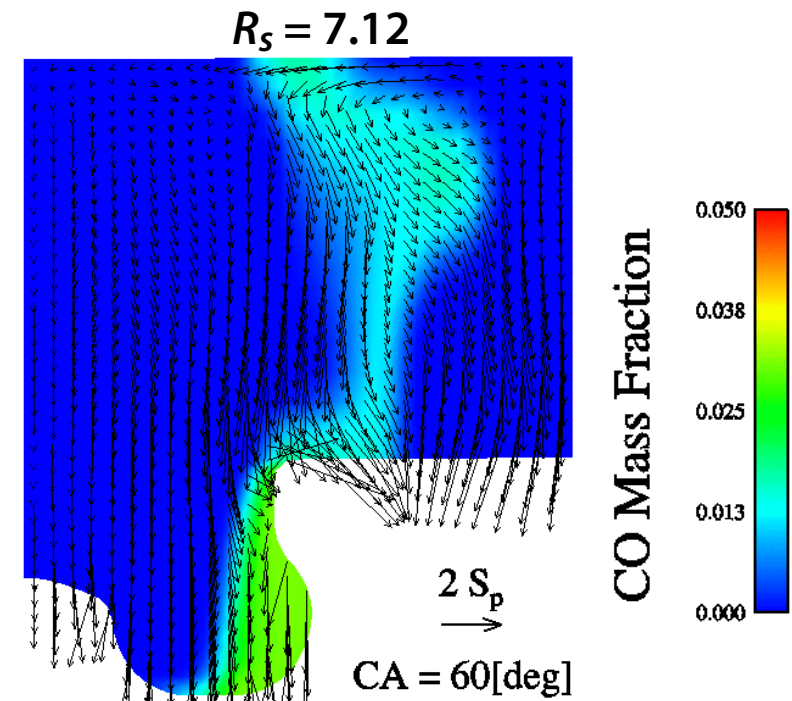


# These structures can inhibit mixing when swirl is excessive

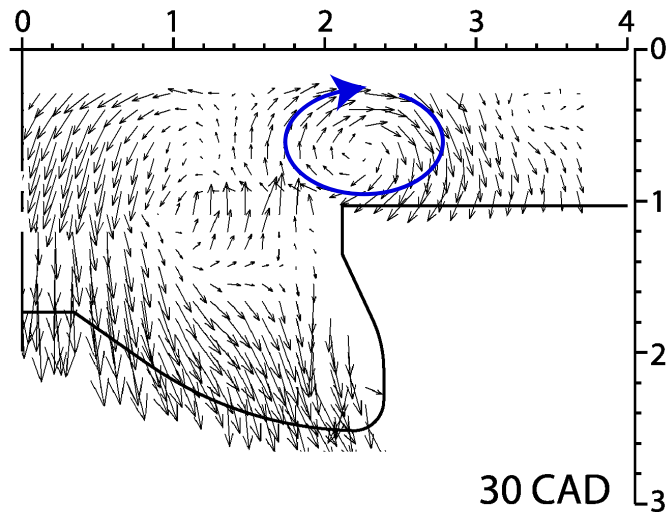


Very high CO emissions are observed at high swirl ratio (similar to MK system swirl)

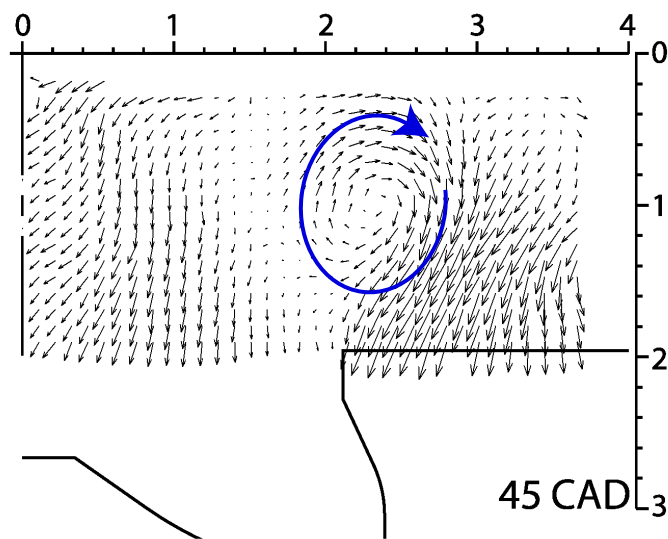
- Simulations point to CO trapped by high centrifugal forces in the periphery of the bowl as a major source of CO emissions
- This phenomenon may be a cause of the need to reduce swirl at high engine speeds



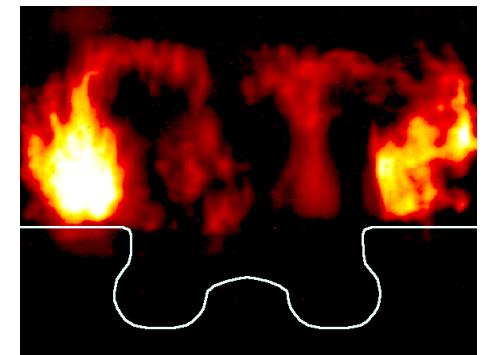
# Detrimental flow structures can also form in the squish volume



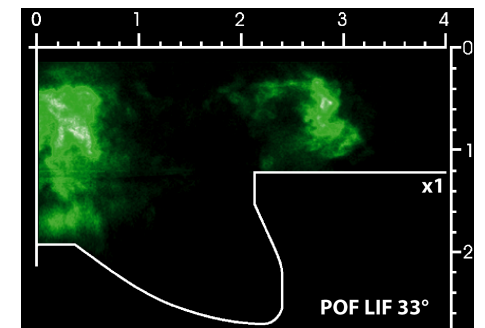
MK-like combustion  
15% O<sub>2</sub>, SOI = -4°  
1200 rpm, 4 bar gIMEP



- Fluid exiting the bowl can trigger formation of a toroidal vortex above the bowl lip
- The vortex is stable and long-lived
- It also forms when no heat release occurs (motored operation) but its formation is delayed
- It impedes mixing in at least two possible ways:
  - It forms a barrier that prevents mixing of fluid exiting the bowl with fluid in the squish volume
  - It may trap soot/partially-burned fuel within the vortex



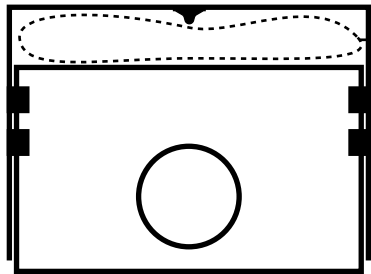
Conventional combustion  
20% EGR, 2000 rpm, 5 bar gIMEP



Low-temperature combustion  
56% EGR, 1200 rpm, 4 bar gIMEP

# Our understanding of engine turbulence is largely empirical

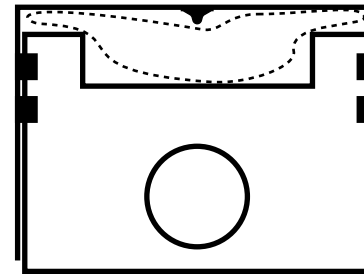
Pancake:



$u' \approx 0.5S_p$   
Approximately Homogeneous  
Little effect of swirl

Increasing  
 $A_{squish}$

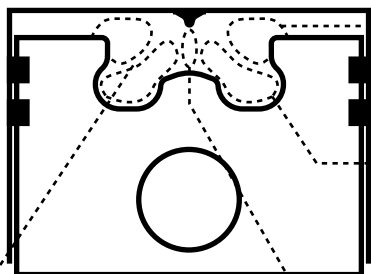
Open cylindrical bowl:



No swirl  
 $u' \approx 0.5-0.6S_p$   
Swirl  
 $u' \approx 0.7S_p$   
No significant inhomogeneity



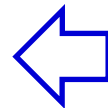
Re-entrant:



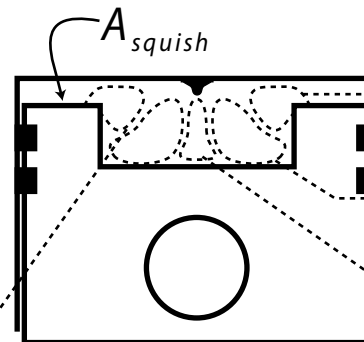
Swirl  
Largest  $u'$  near  $-10^\circ$   
 $u'_\theta > u'_r$   
 $u' \approx 0.5-1.8S_p$   
(Increases with swirl or  $A_{squish}$ )

Generally less homogeneous than cylindrical

Modeling studies often predict a local maximum



Deep cylindrical bowl:



Swirl  
 $u' \approx 1.2S_p$   
 $u' \approx 0.7-0.8S_p$   
 $u' \approx 1.1S_p$   
Increased centerline turbulence often attributed to swirl center precession

Homogeneity decreases with increasing swirl or  $A_{squish}$

# The angular momentum distribution can also profoundly impact the turbulence field

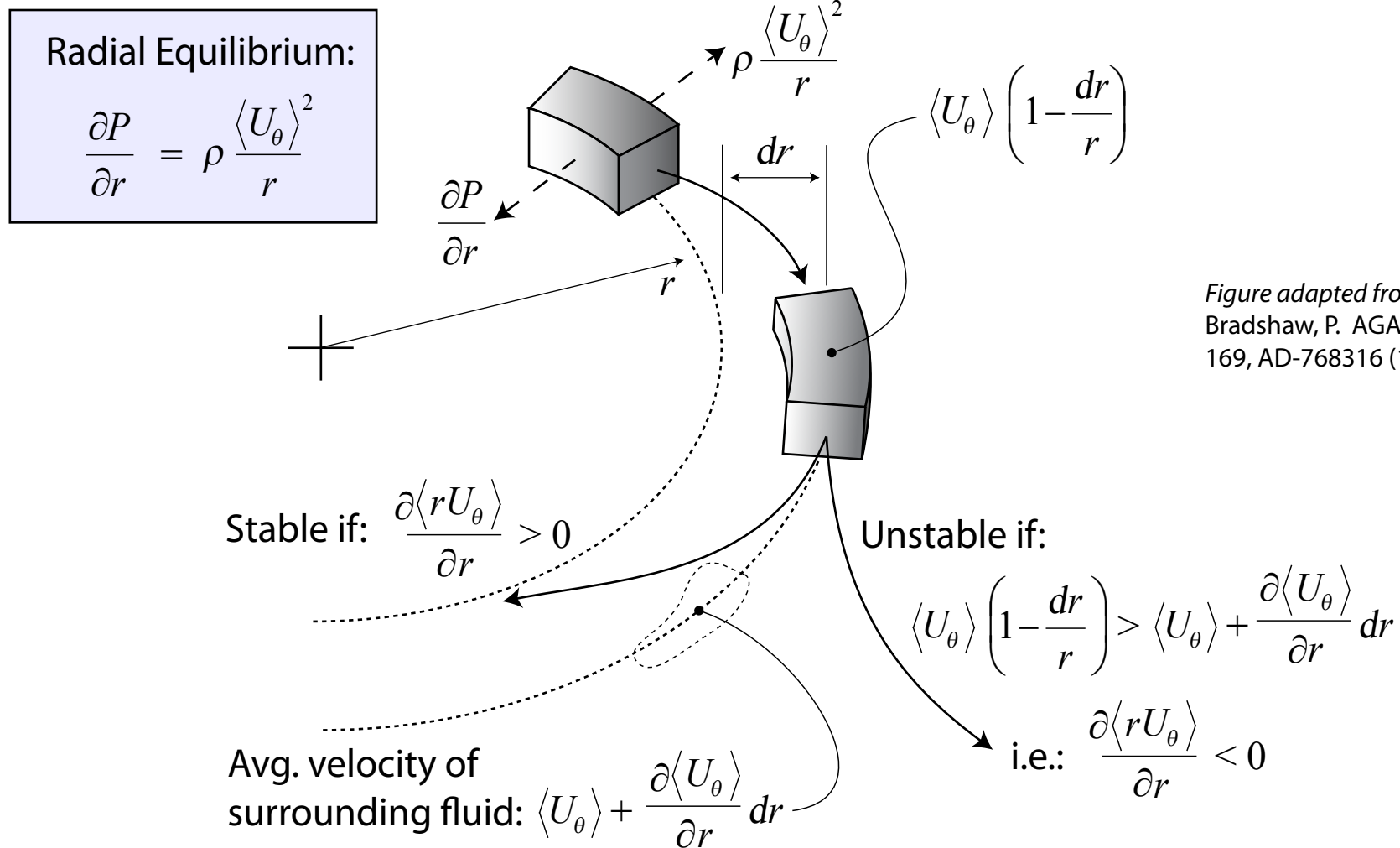
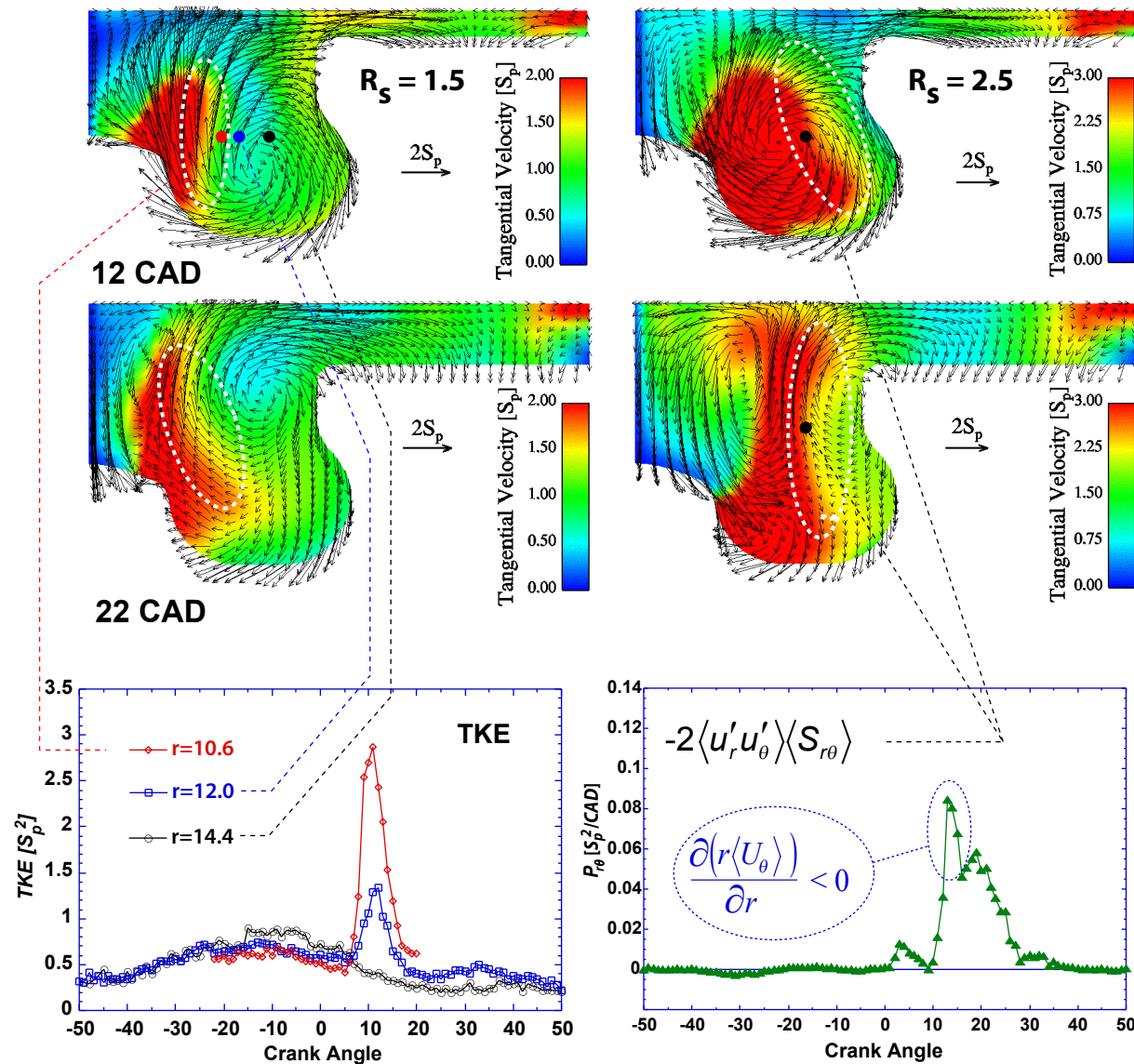


Figure adapted from:  
Bradshaw, P. AGARDograph  
169, AD-768316 (1973)

A swirling flow characterized by a negative mean radial gradient in angular momentum is inherently unstable

Any perturbation of a fluid element will be amplified

# Negative mean radial gradients of angular momentum are not just an academic curiosity



- At low swirl ratios, measured turbulence energy increases by an order of magnitude as the negative momentum gradient region is approached
- With higher swirl, we measure the negative momentum gradient directly—along with increased production & turbulence energy

Stored mean flow energy can be released to turbulence very effectively by forming negative  $\Omega$  gradients

# RANS equations describing the production\* of $k$ can help us understand turbulence generation by swirl

Production by  
anisotropic stresses

$$\frac{\bar{D}k}{\bar{D}t} = -\underbrace{\langle u_i u'_j \rangle \langle S_{ij} \rangle}_{\text{Production by anisotropic stresses}} - \varepsilon + \text{Diffusion}$$

Production by  
isotropic stresses

$$-\left( \langle u'_i u'_j \rangle - \frac{2}{3} k \delta_{ij} \right) \langle S_{ij} \rangle$$

Vertical, diametral plane  
"squish" generated turbulence

$$-\langle u'_r u'_z \rangle \left( \frac{\partial \langle U_r \rangle}{\partial z} + \frac{\partial \langle U_z \rangle}{\partial r} \right)$$

Additional terms  
exist that are  
not considered  
here

Horizontal plane  
"swirl" generated turbulence

$$-\langle u'_r u'_\theta \rangle \left( \frac{1}{r} \frac{\partial (r \langle U_\theta \rangle)}{\partial r} - \frac{2 \langle U_\theta \rangle}{r} \right)$$

Dominant shear related  
production term in  
swirl-supported diesels

$$-\frac{2}{3} k (\nabla \cdot \langle \mathbf{U} \rangle)$$

$$\nabla \cdot \langle \mathbf{U} \rangle \approx -\frac{1}{\rho} \frac{\partial \rho}{\partial t}$$

$$\approx \frac{1}{V} \frac{\partial V}{\partial t} \approx \frac{1}{P^{1/\gamma}} \frac{\partial P^{1/\gamma}}{\partial t}$$

Independent of  
flow structure

$$-\frac{2}{3} k (\nabla \cdot \langle \mathbf{U} \rangle)$$

$$-\frac{2}{3} k \left( \underbrace{\frac{\partial \langle U_r \rangle}{\partial r}}_{\langle u'^2_r \rangle} + \underbrace{\frac{1}{r} \frac{\partial \langle U_\theta \rangle}{\partial \theta}}_{\langle u'^2_\theta \rangle} + \underbrace{\frac{\langle U_r \rangle}{r}}_{\langle u'^2_r \rangle} + \frac{\partial \langle U_z \rangle}{\partial z} \right)$$

Often determines normal stress anisotropy

\* The redistributive terms associated with convection of the normal stresses in a curvilinear coordinate system are included here

# A closer examination of the swirl related production

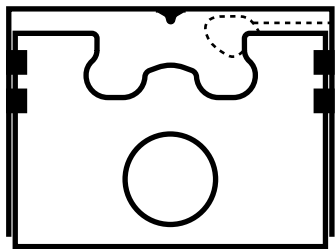
$$-\langle u'_r u'_\theta \rangle \left( \underbrace{\frac{1}{r} \frac{\partial(r\langle U_\theta \rangle)}{\partial r}}_{\langle u'^2_\theta \rangle \text{ (+)}} - \underbrace{\frac{2\langle U_\theta \rangle}{r}}_{\langle u'^2_r \rangle \text{ (-)}} \right)$$

- For positive  $\frac{\partial(r\langle U_\theta \rangle)}{\partial r}$  and  $\langle U_\theta \rangle$ , the two terms are of opposite sign. **If  $\langle u'_r u'_\theta \rangle < 0$ , then  $\langle u'^2_\theta \rangle$  can be expected to dominate**

- For solid-body flow ( $\langle U_\theta \rangle \propto r$ ), the production is zero

Swirl generally tends to redistribute energy

- When  $\frac{\partial(r\langle U_\theta \rangle)}{\partial r} < 0$ , both terms are sources of turbulence, **provided  $\langle u'_r u'_\theta \rangle > 0$**

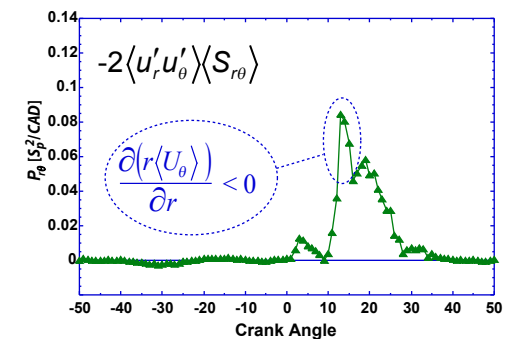


Largest  $u'$   
near  $-10^\circ$   
 $u'_\theta > u'_r$

For an axially-uniform, axisymmetric flow on circular streamlines:

$$\langle u'_r u'_\theta \rangle \propto -\langle u'^2_r \rangle \frac{1}{r} \frac{\partial(r\langle U_\theta \rangle)}{\partial r} + \langle u'^2_\theta \rangle \frac{2\langle U_\theta \rangle}{r}$$

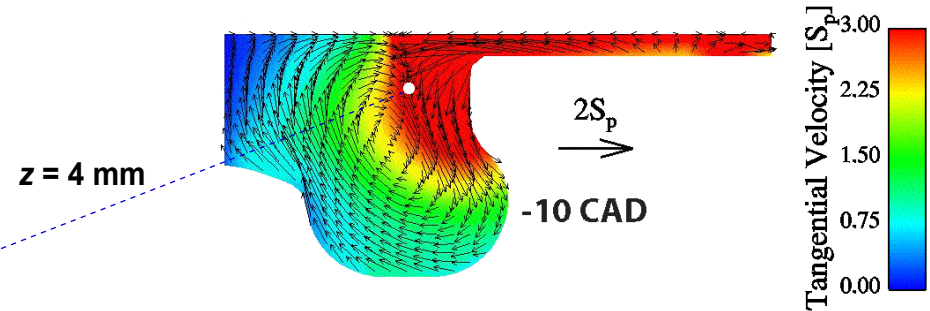
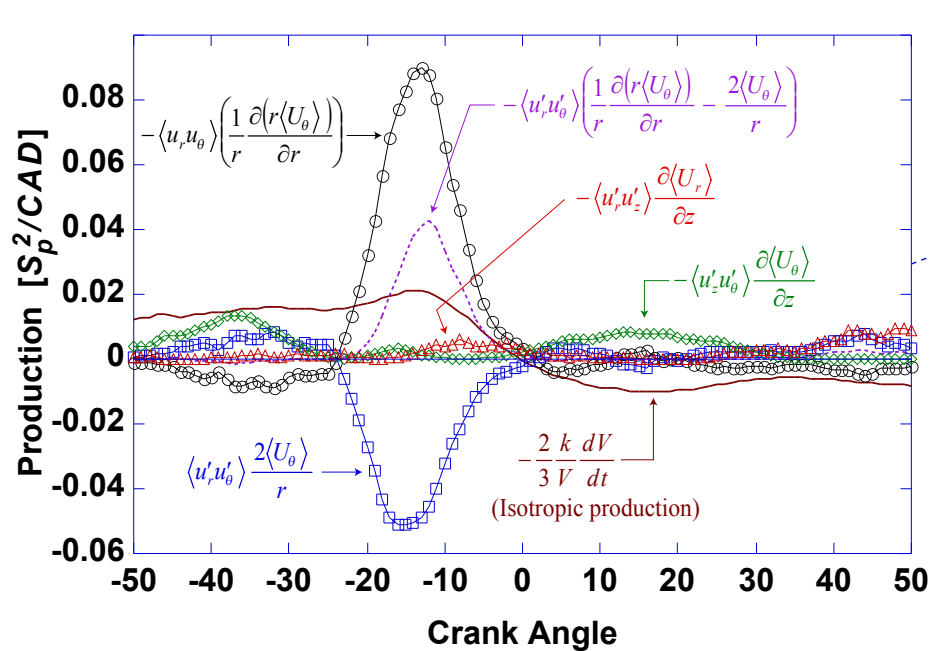
(Assumes shear stress is proportional to its production)



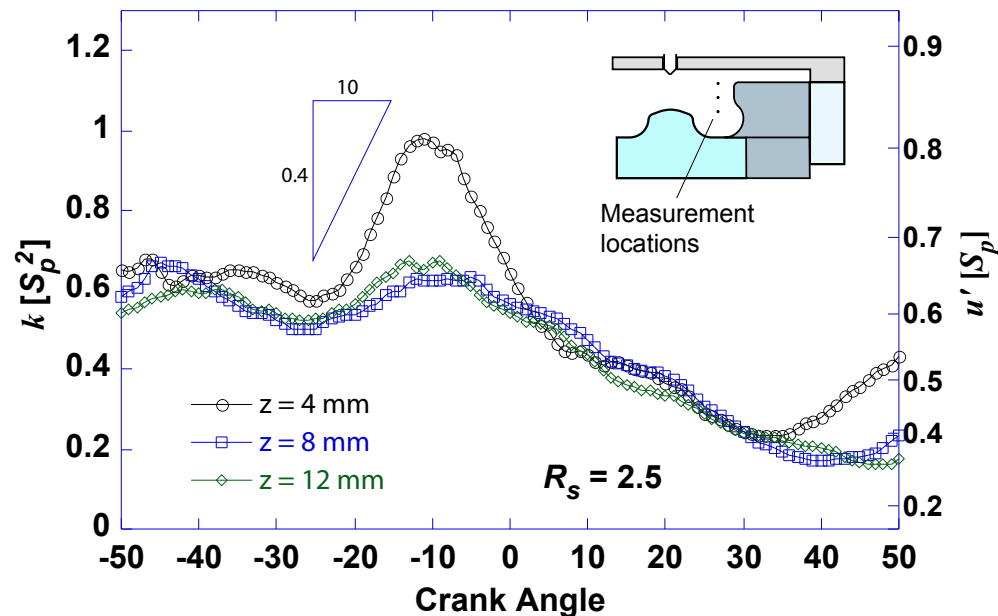
Both terms can be understood in terms of the same momentum conservation principles



# Direct measurements of turbulence production confirm these ideas



- Radial gradients in  $\langle U_\theta \rangle$  dominate production (and anisotropy) near TDC
- Squish generated turbulence is negligible
- Axial gradients in  $\langle U_\theta \rangle$  contribute early in the compression stroke and during expansion
- Over the course of the compression stroke, **bulk compression dominates**—especially lower in the bowl
- During expansion, bulk compression is negative—and typically dominates



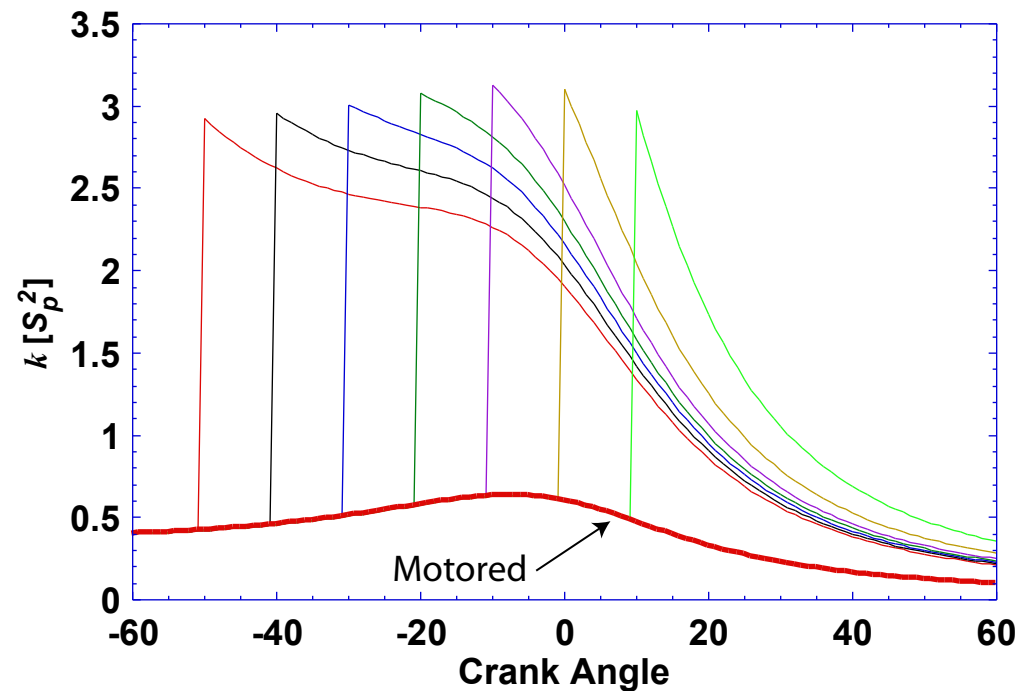
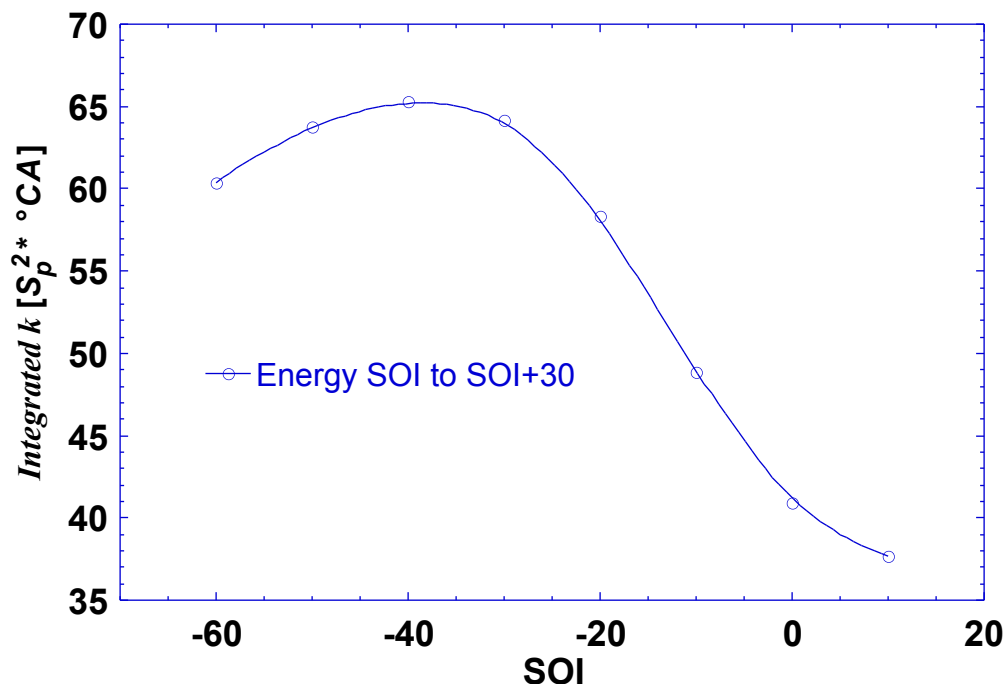


# We can take advantage of production by compression to amplify turbulence 'injected' into the cylinder

For homogeneous turbulence:

$$\frac{dk}{dt} = P - \varepsilon = -\frac{2}{3}k \frac{1}{V} \frac{dV}{dt} - CA \frac{u'^3}{\ell}$$

To explore the influence of compression on the utilization of the turbulence generated by the injection event, we "inject" a fixed quantity of  $k$  at discrete crank angles



We integrate the turbulence energy in the bowl for the first 30  $^\circ CA$  after injection.

The turbulence energy available for mixing is maximized with fuel injection at -30 to -40 CAD

- Many aspects of in-cylinder flows can be readily understood through a relatively simple consideration of the governing equations
- These flows are not necessarily subtle. Several “textbook” flow structures (toroidal vortices, negative radial angular momentum gradients) can be identified.
- In swirling flows, the distribution (and re-distribution) of angular momentum plays a dominant role in determining both the mean flow evolution and the shear generated turbulence.
- Turbulence generation by bulk compression is a dominant, and often overlooked source (and sink) of in-cylinder turbulence.