

Memzyme Technology for Cost-Effective CO₂ Separations in Enhanced Oil Recovery

Technology Commercialization Fund Project: TCF-17-13314

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Acknowledgment

Acknowledgment

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Memzyme for Carbon Capture



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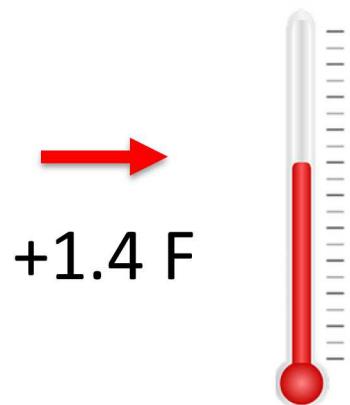
Dr. Ying-Bing Jiang
U. New Mexico
Experimental Lead



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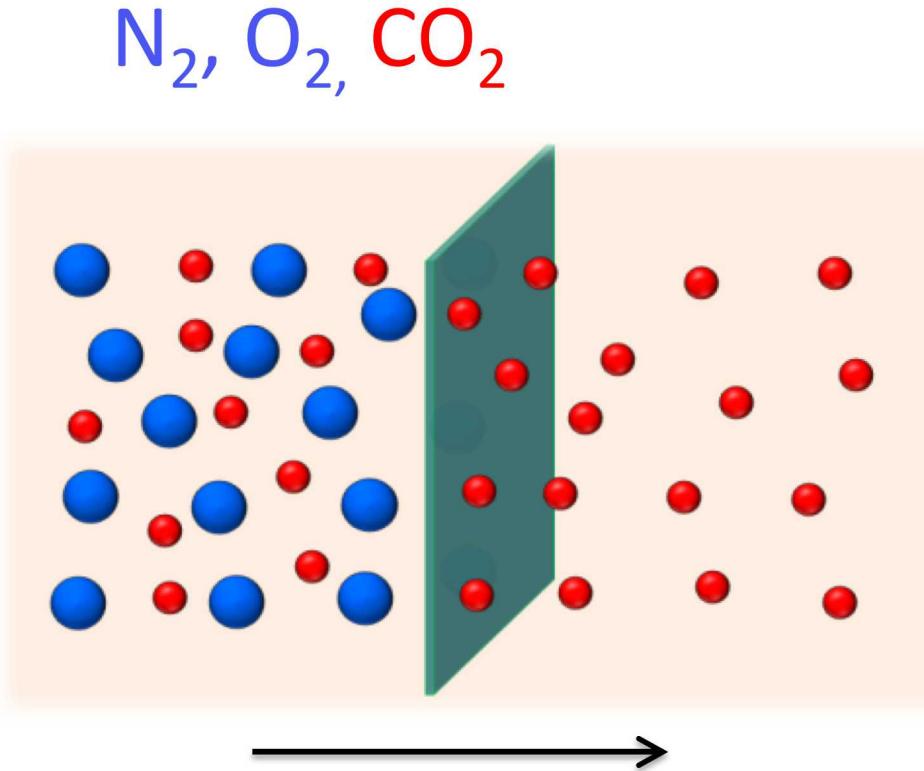


Imagine a future ...





Membrane with unique function

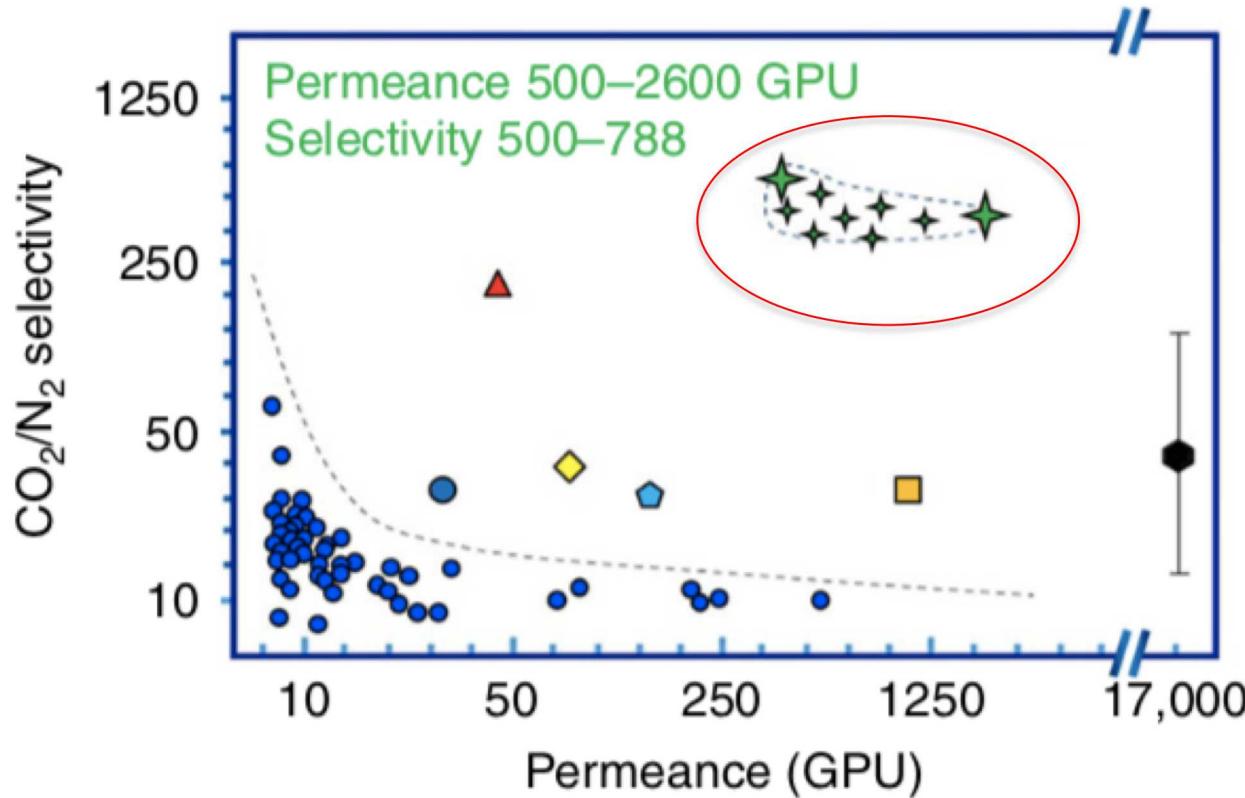


Selective \rightarrow useable CO_2
($>500 \text{ CO}_2/\text{N}_2$)

Rapid \rightarrow less membrane
(2600 GPU)



Membrane with unique function



Green stars: Fu, et al. *Nature Commun.* 9:990 (2018)

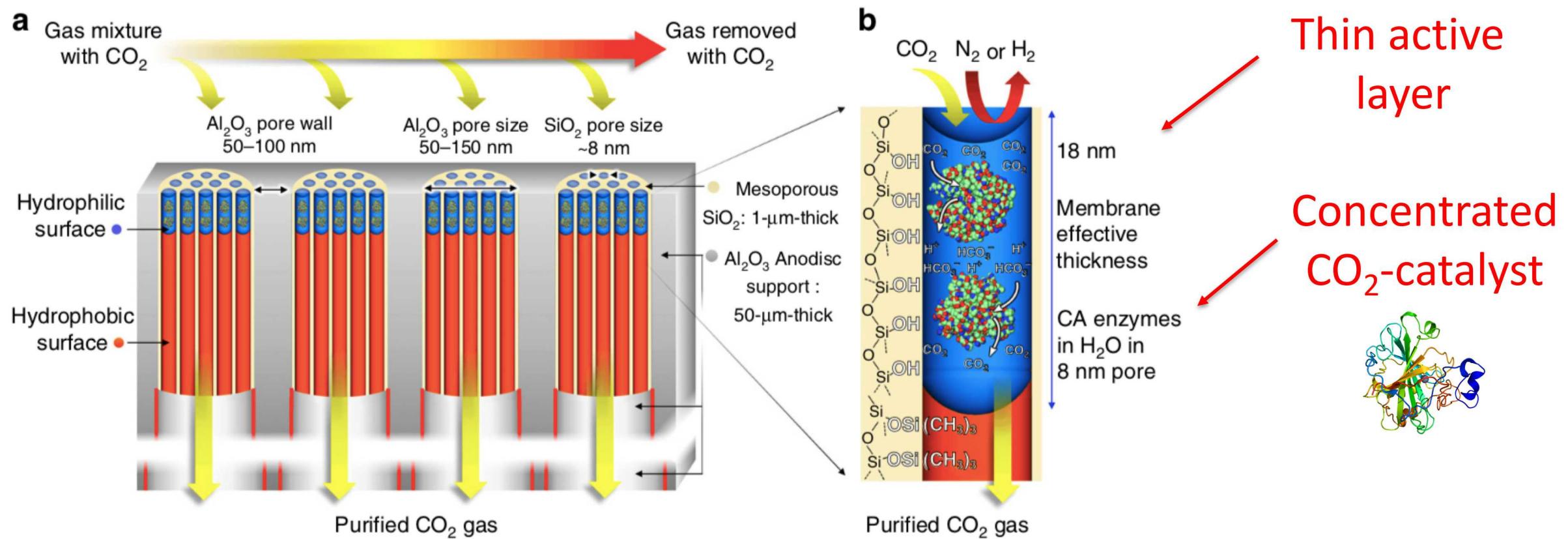
1 GPU = $10^{-6} \text{ cm}^3(\text{STP})/(\text{cm}^2 \text{ s cmHg})$
= $3.35 \times 10^{-10} \text{ mol}/(\text{m}^2 \text{ s Pa})$

Red triangle: Trachtenberg, et al. DOE Project DE-FC26-07NT43084, Carbozyme (2011)

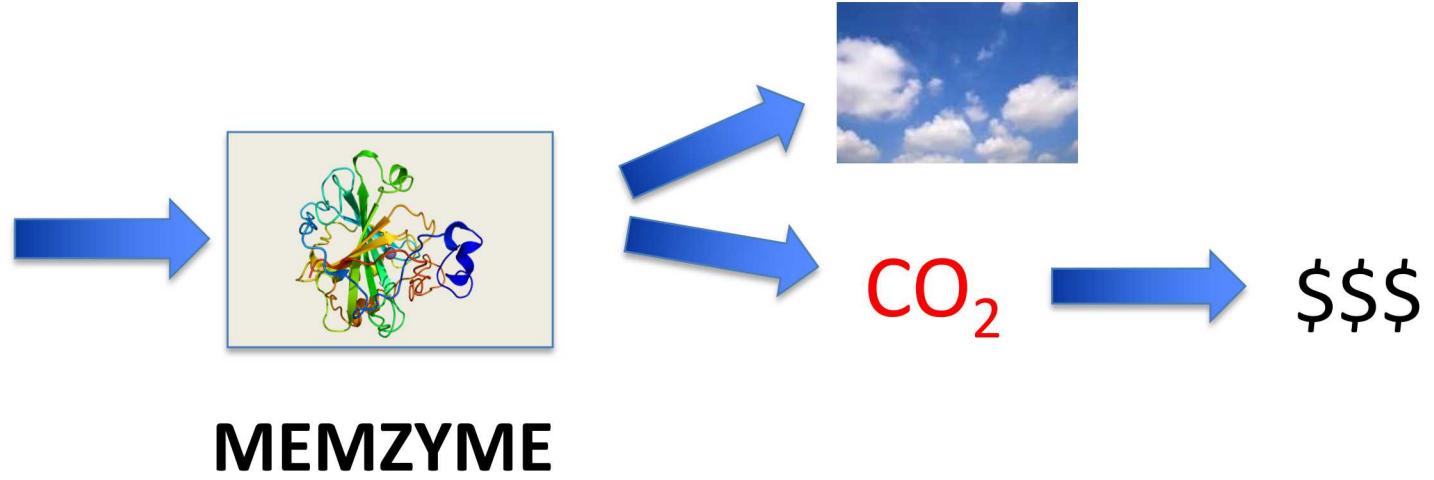
Black hexagon: -43 C, Zhou, et al. *Angew. Chem. Int. Ed.* 53:3492 (2014)

Others: see references in Fu, et al.

Membrane with unique structure



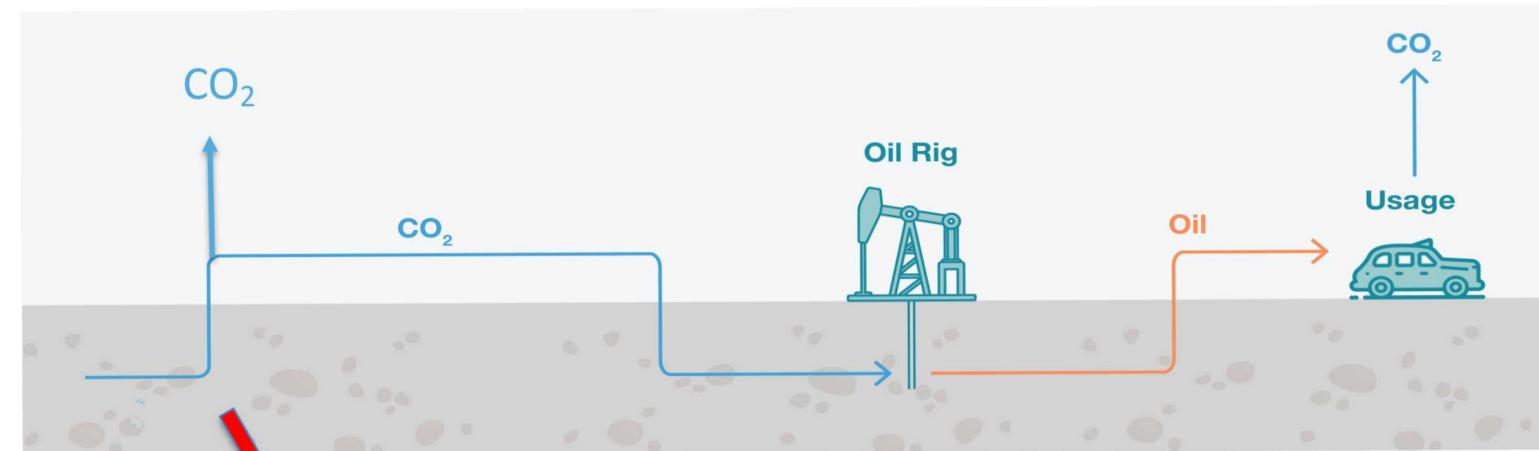
Commercialization Value



At lab-scale, our modular, rechargeable filters separate CO_2 from nitrogen rapidly (2600 GPU) **and** selectively (>500), creating the potential to make carbon capture from power plant emissions profitable while restoring our climate.

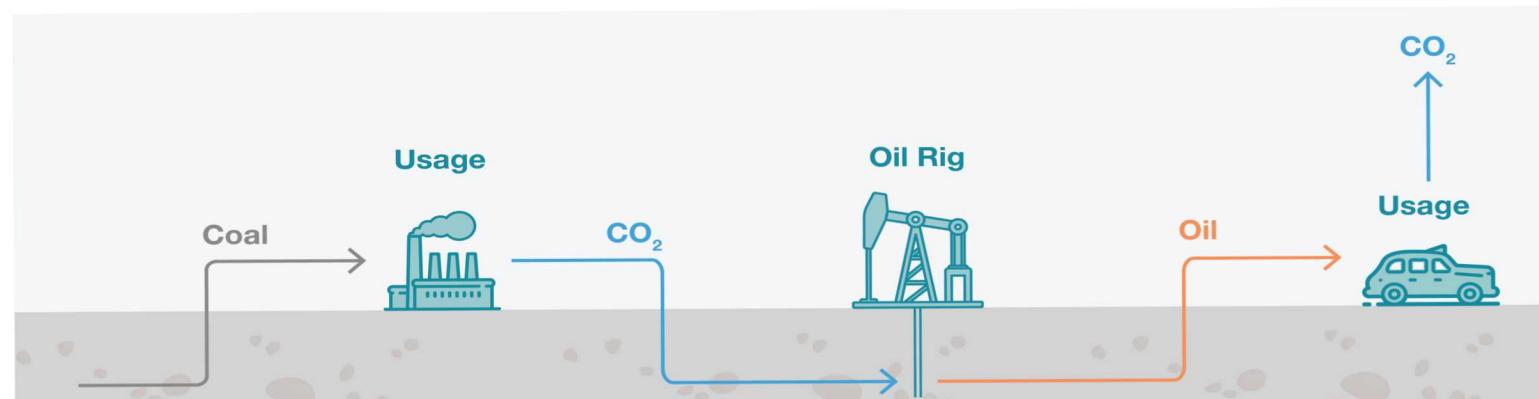
Oil & tax credits drive CO₂ capture

Natural CO₂



tax credit (\$35/t caught & utilized)
(\$50/t caught & stored)

Anthro CO₂

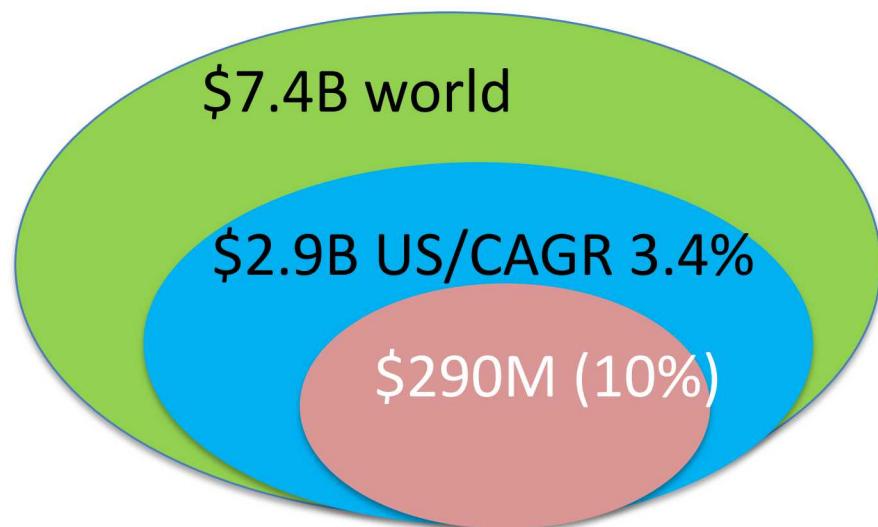


CO₂-enhanced oil recovery (EOR)

CO₂ from coal power plants is marketable

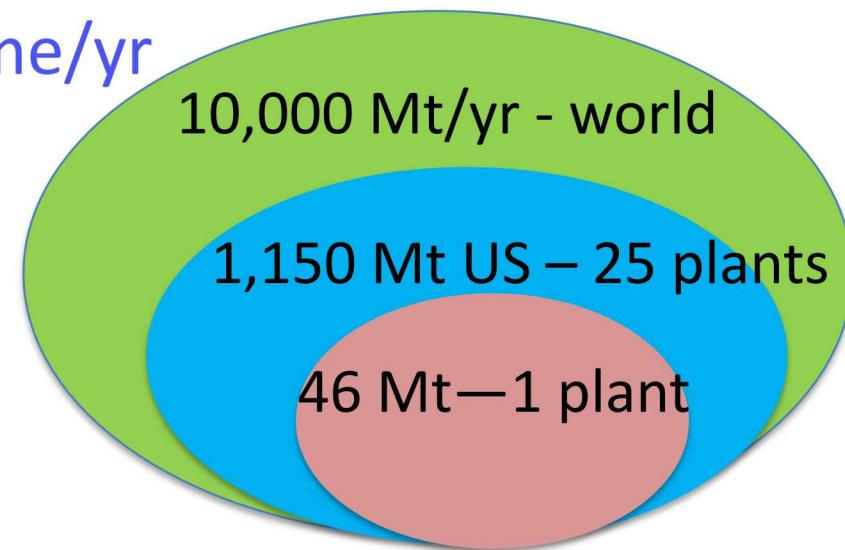
Current CO₂ market

\$/yr



CO₂ available w/capture tech.

Volume/yr



Current capture tech is expensive



Liquid amine absorption
(\$60/t* – credit = \$25/t)

CO₂-EOR
needs <\$20/t at
today's oil prices

*includes all costs, including compression of separated CO₂

Membranes show promise for low-cost CO₂ capture



Membranes (lab scale)	Flux (GPU)	Selectivity (CO ₂ /N ₂)	Capital (\$/m ²)	Cost of Separation* (\$/t CO ₂ , 90%)
Memzyme	2600	500+	Low (~\$50/m ²)	\$18
MTR	1000	50	Low (\$150/m ²)	\$32
UOP	60	30	unknown	>\$35
Air Liquide	70	30	unknown	>\$35

*estimated based on lab-scale performance, membrane fabrication costs, and includes compression

Basic Research Needs for Carbon Capture: Beyond 2020, Appendix A (Fig. 9)
Merkel, T. C., et al. *J. Membr. Sci.* (2010) 359:126

Data taken from reports:

Merkel, T., et al. Membrane process to capture CO₂ from coal-fired power plant flue gas. (NETL, 2009).

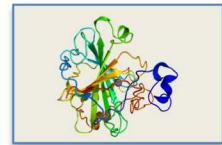
Casillas, C. et al. Pilot testing of a membrane for post-combustion CO₂ capture. In *Proc. 2015 NETL CO₂ Capture Technology*.

Vora, S.D. *DOE/NETL Advanced Carbon Dioxide Capture R&D Program: Technology Update* (NETL, 2013).

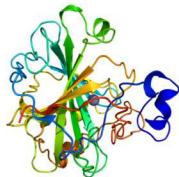
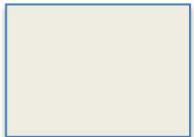
Hasse, et al. CO₂ capture by sub-ambient membrane operation. *Energy Procedia* (2013) 37, 993.



Optimize for
flue gas



Make samples



Make raw mat'l's



Design (IP)



US Patent 9,242,210 (2016)

Memzyme path toward market

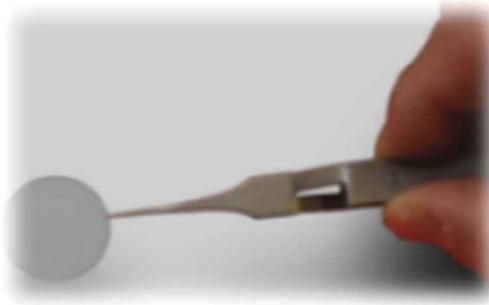
Challenge: Maintain Function in Scalable Format
with Industrial Gases

- Task 1: Make stronger, scalable supporting material
- Task 2: Test compatibility of membrane & support
- Task 3: Optimize active layers (enzymes, buffers)
- Task 4: Optimize selectivity for CO_2 from flue gas

Task 1: Supporting material

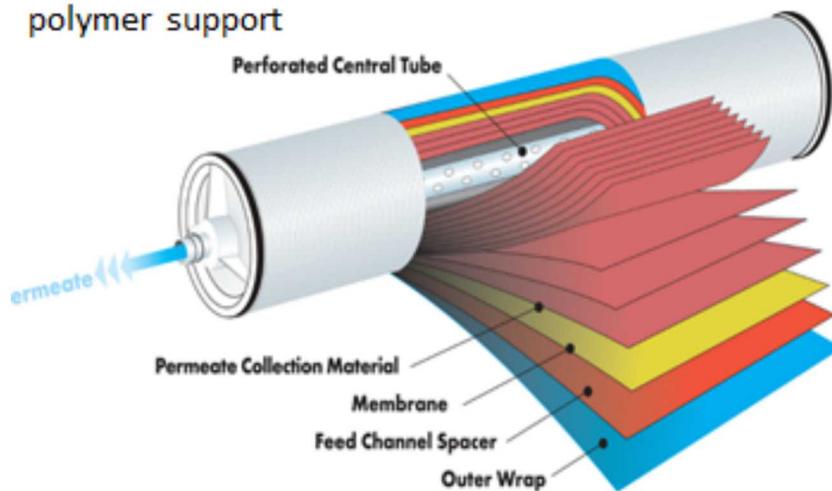
Current lab-scale supports:

Small piece of polymer support and small piece of anodized porous alumina



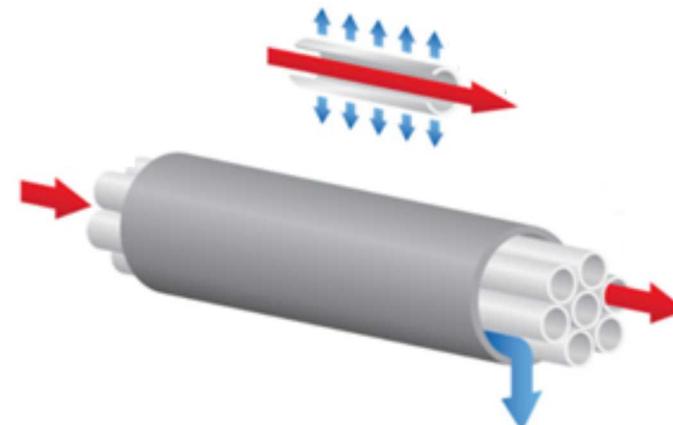
Strategy 1:

Spiral wound by using flexible polymer support

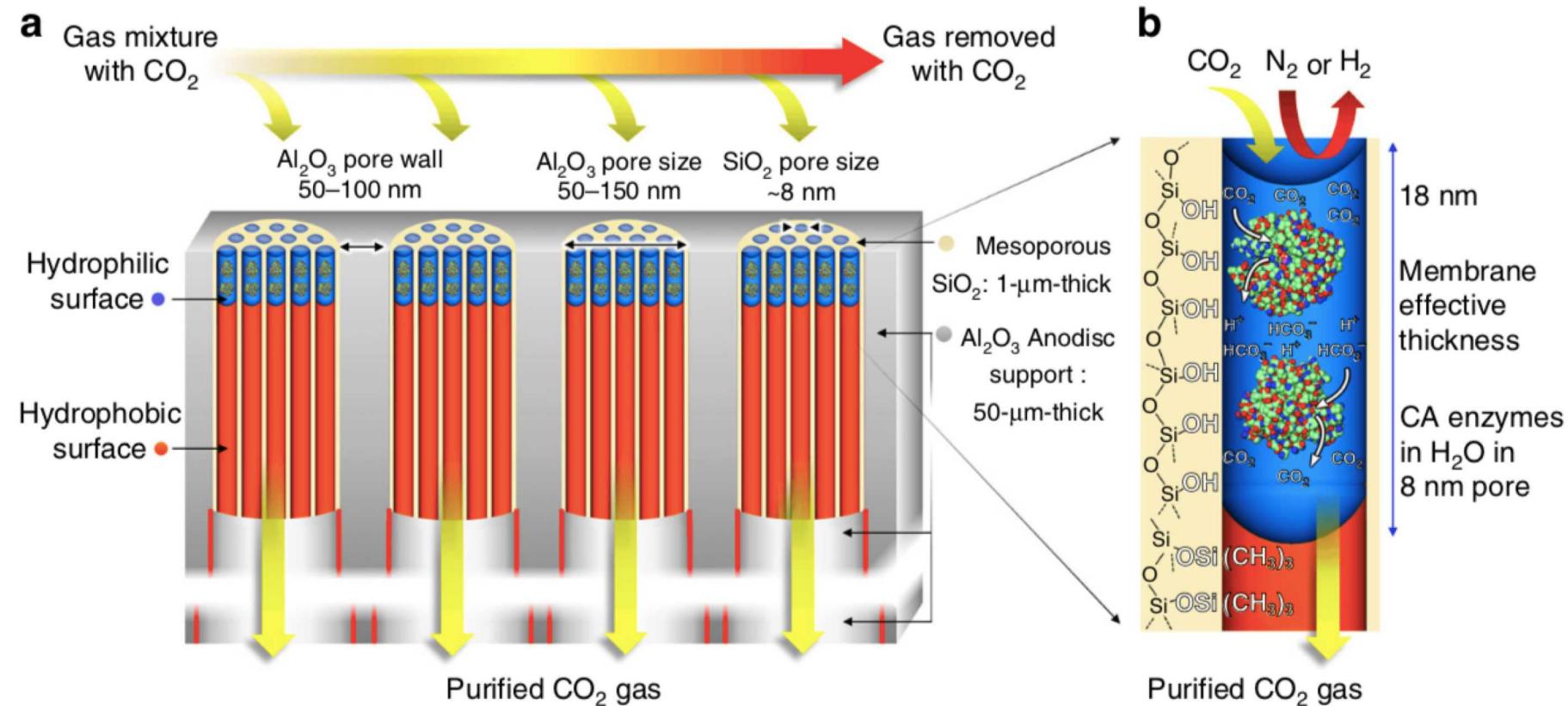


Strategy 2:

parallel tubes by using rigid porous ceramic support



Task 2: Test membrane-support compatibility



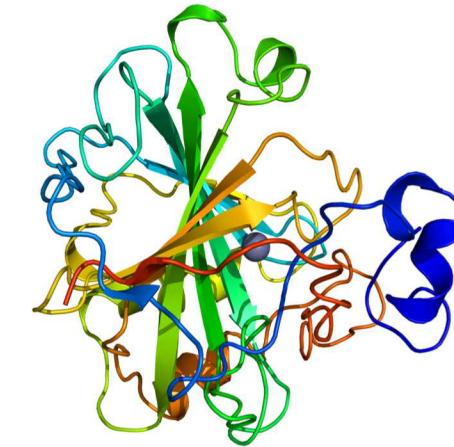
Can the new supporting structure be made compatible with membrane fabrication?

Task 3: Optimize active layer

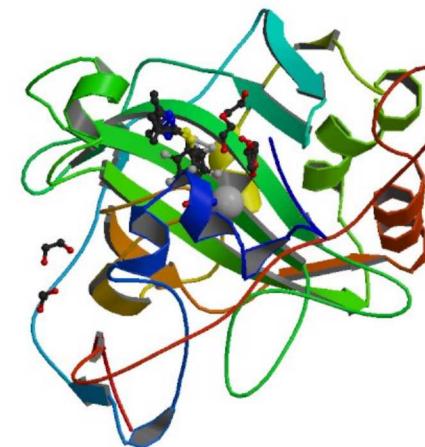


Incorporate variants, modify buffer

What conditions optimize
enzyme lifetime and performance
in nanoconfined membrane?



Bovine C. anhydrase

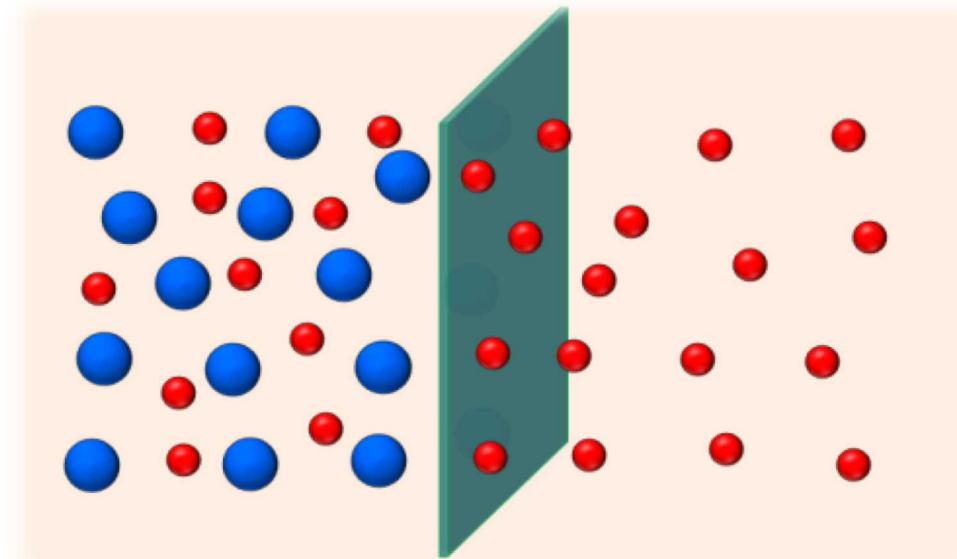


Thermostable, rapid Saz_C.A.
(*Int. J. Mol. Sci.*, 2019 20:1494)

Task 4: Optimize selectivity for flue gas

- CO_2 vs N_2 (15:85)
- CO_2 vs O_2 (15:85)
- CO_2 vs SO_x and NO_x
- CO_2 separation with flue gas (60 °C)

$\text{N}_2, \text{O}_2, \text{CO}_2$



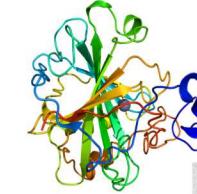
Vary - thickness,

- surface chemistry,
- active layer.

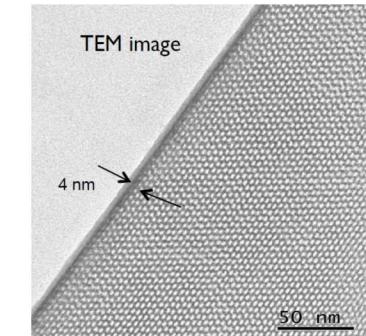
Work flow



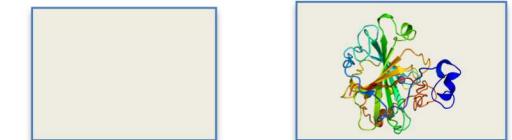
Vary active layer -- enzyme, buffer, storage conditions



Characterize membrane samples (FT-IR, TEM, SEM)



Make samples on support; measure function



TRL 3

TRL 4+

Q1

Q2

Q3

Q4

Q1

Q2

Q3

Q4



Budget

Schedule	Year 1	Year 2
DOE TCF Share	\$150,000	\$150,000
Non-Federal Share	\$150,000	\$150,000



Summary

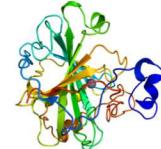
Design
(US Patent)
Start-
up



Make
samples



Make robust,
scalable raw
materials



Scale up



Implement



LDRD (SNL) Private Funds

DOE-TCF

Partnerships

2016

2017

2019

2020

2021

2022

2025