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# New MELCOR Models Homologous Pumps



PRESENTED BY

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## Homologous Pump Model Overview

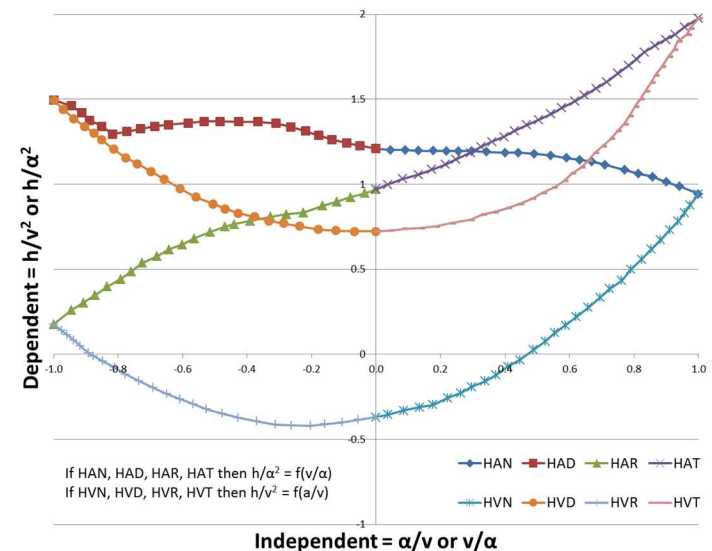
- ◆ More mechanistic centrifugal pump model than previously available
- ◆ Model integrated into FL package, predicts the pump momentum source as a function of impeller speed, capacity (volumetric flow)
- ◆ Model computes:
  - Pressure head (hydraulic power = head x flow)
  - Hydraulic torque (brake power = hydraulic torque x speed)
  - Pump dissipation energy and pump efficiency
  - Pump speed via torque-inertia equation (also user-defined, optional trips)
  - Two-phase degradation effects
- ◆ For pump performance modeling, predict head and torque given speed and flow using built-in or user-defined data in a specialized “homologous” form

# Homologous Pump Theory

- ◆ Pump performance model - homologous and polar homologous
  - Inputs: Impeller speed,  $\omega$ , and pump volumetric flow (capacity),  $Q$
  - Outputs: Pump head ( $H$ ), hydraulic torque ( $T$ ) exerted by fluid on impeller
  - Two-phase head/torque degradation via two-phase multiplier approach
  - Also a “universal correlation” option requiring less information from user
- ◆ Semi-implicit treatment of pump head in phasic velocity equations
- ◆ Pump speed control and the torque-inertia equation (TIE)
  - User controls and/or TIE can govern speed at different problem times
  - Pump trips available to arbitrarily model start-up, steady run, coast-down
- ◆ Other features
  - Friction torque generally modeled as a polynomial in  $\omega/\omega_R$
  - Pump inertia generally modeled as a polynomial in  $\omega/\omega_R$
  - Pump energy dissipation and efficiency

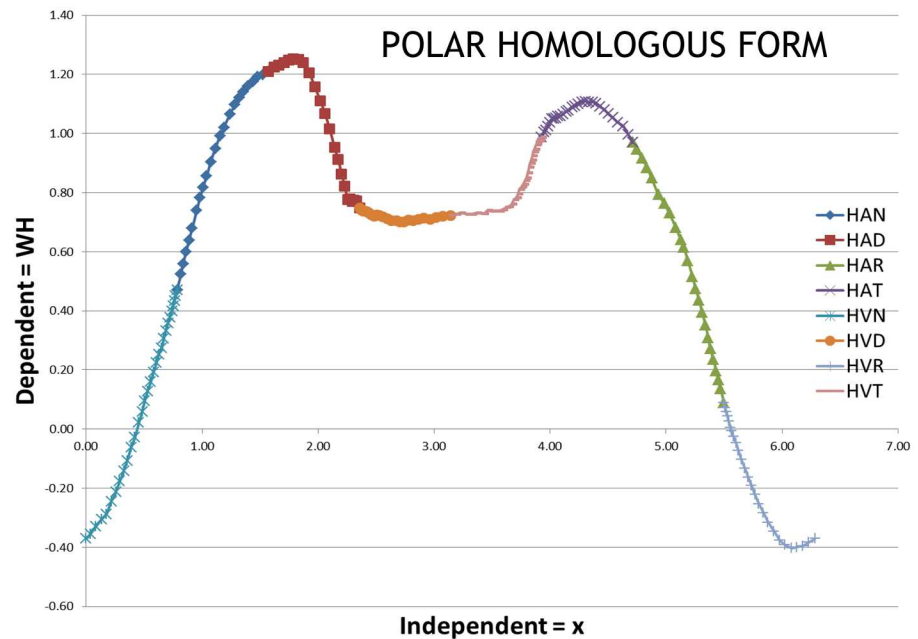
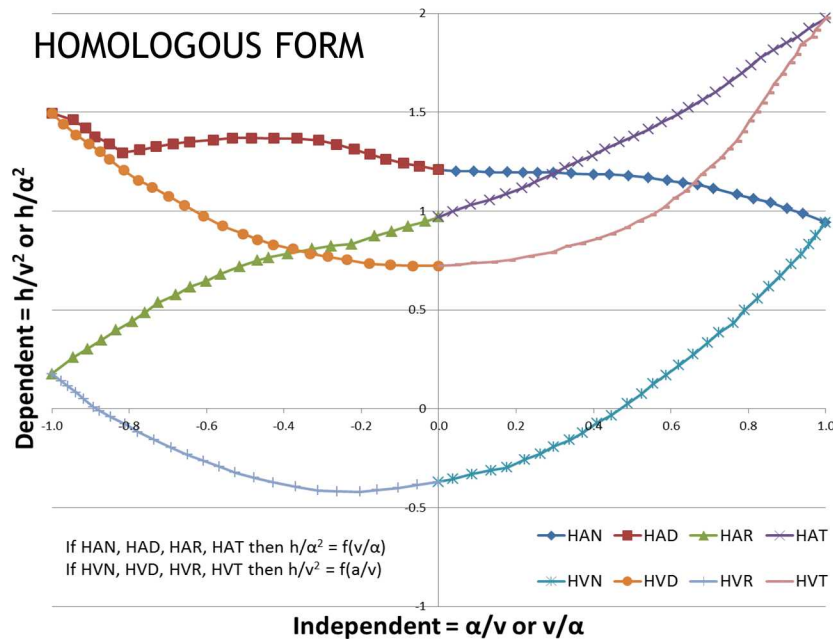
# Homologous Pump Theory Pump Performance Model

- ◆ Non-dimensional speed ( $v = \omega/\omega_R$ ), flow ( $\alpha = Q/Q_R$ ) with “rated” conditions
- ◆ Non-dimensional head ( $h = H/H_R$ ), torque ( $\tau = T/T_R$ ) with “rated” conditions
- ◆ Construct a plot covering the entire domain of pump operation
  - Four quadrants (normal, turbine, dissipation, reversal modes)
  - Two pieces per quadrant for a total of eight octants
  - Indep. var's  $v/\alpha$  or  $\alpha/v$ 
    - If  $|v/\alpha| \leq 1$ , then use  $v/\alpha$
    - If  $|v/\alpha| > 1$ , then  $|\alpha/v| < 1$  and use  $\alpha/v$
    - Independent variable bounded on  $[-1, 1]$
  - Dep var's for single/two-phase head/torque
    - If  $x$  is  $v/\alpha$ , dependent variable is  $h/\alpha^2$  or  $\tau/\alpha^2$
    - If  $x$  is  $\alpha/v$ , dependent variable is  $h/v^2$  or  $\tau/v^2$



# Homologous Pump Theory Pump Performance Model

User gives homologous data, code converts to “polar homologous”



Practical difficulties with interpolation

- Which ind/dep variable forms apply
- Independent variable crosses zero

- Positive definite indep. var domain  $[0, 2\pi]$
- Single, non-overlapping curve
- Simply convert ind/dep variable space



## Homologous Pump Theory Pump Performance Model

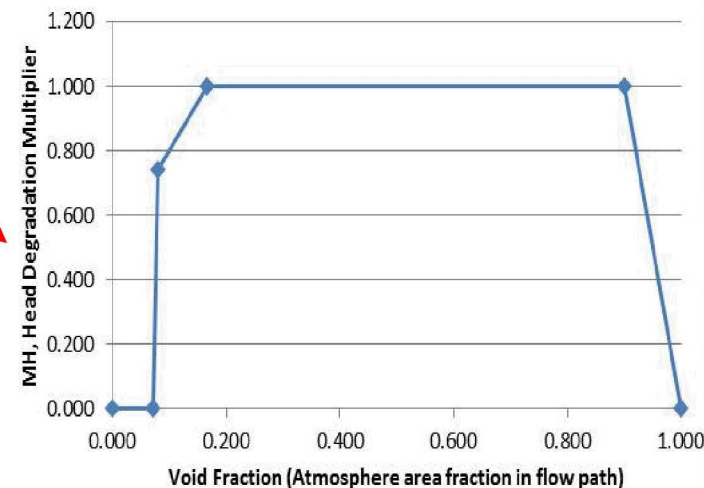
- ◆ Two-phase effects from two-phase head/torque curves and multipliers
- ◆ “Fully-degraded” curves for worst performance in two-phase conditions
- ◆ Use void-fraction-dependent “degradation multipliers”
- ◆ Overall equals single phase head/torque less a two-phase term

$$WH_{overall} = WH - MH * (WH - WH2)$$

$$WT_{overall} = WT - MT * (WT - WT2)$$

Subtract part of the  
difference between  
single/two phase

e.g. Semiscale MH

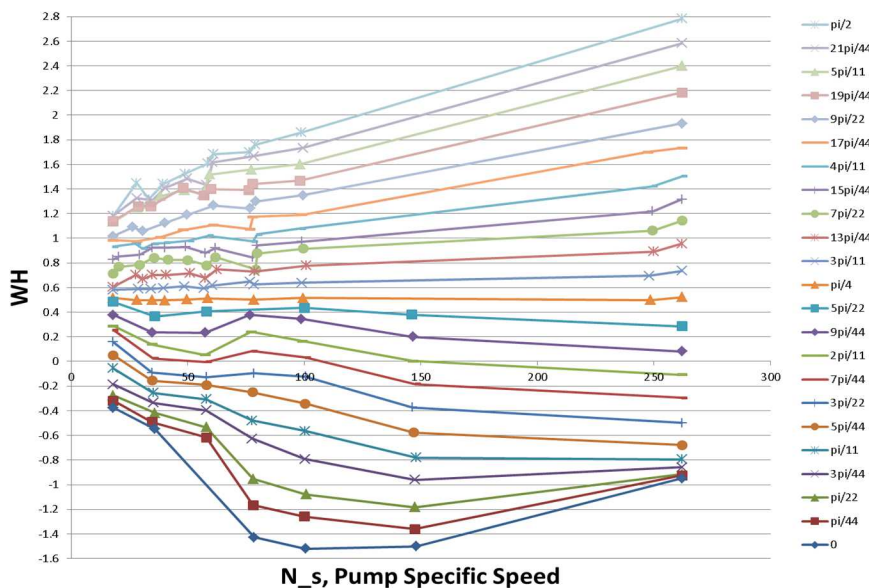


# Homologous Pump Theory Pump Performance Model

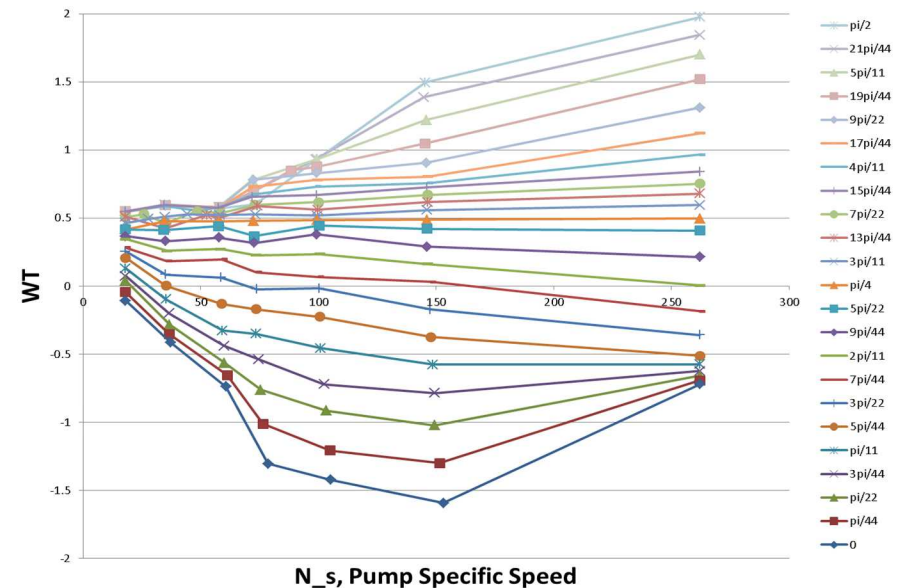
- ◆ Universal correlation uses  $\omega$  and  $Q$  to find  $H$  and  $T$  via data interpolation
- ◆ Use a data set compiled from several pump experiments
  - User gives pump specific speed, defined from rated quantities as:
  - Use  $N_s$ ,  $\omega$ , and  $Q$  to interpolate  $H$  and  $T$  functions
  - Valid for “normal”, single-phase operation

$$N_s = \frac{\omega_R \sqrt{Q_R}}{H_R^{3/4}}$$

$X=f(\omega, Q)$



$X=f(\omega, Q)$



# Homologous Pump Theory, Semi-Implicit Head Treatment

$$\begin{aligned}
 & \left( 1 + \frac{K_{j,\varphi}^* \Delta t}{2L_j} |v_{j,\varphi}^{n-} + v'_{j,\varphi}| + \frac{\alpha_{j,-\varphi} f_{2,j} L_{2,j} \Delta t}{\rho_{j,\varphi} L_j} \right) v_{j,\varphi}^n - \frac{\alpha_{j,-\varphi} f_{2,j} L_{2,j} \Delta t}{\rho_{j,\varphi} L_j} v_{j,-\varphi}^n + \sum_{s,\psi} C(j, \varphi : s, \psi) v_{s,\psi}^n \\
 & = v_{j,\varphi}^{o+} + \frac{K_{j,\varphi}^* \Delta t}{2L_j} |v'_{j,\varphi}| v_{j,\varphi}^{n-} + \frac{\Delta t}{\rho_{j,\varphi} L_j} (\hat{P}_i + \Delta P_j - \hat{P}_k) + (\rho g \Delta z)_{j,\varphi}^o + \frac{\partial(\rho g \Delta z)_{j,\varphi}}{\partial M_{i,P}} (\hat{M}_{i,P}^o - M_{i,P}^{o+}) + \frac{\partial(\rho g \Delta z)_{j,\varphi}}{\partial M_{k,P}} (\hat{M}_{k,P}^o - M_{k,P}^{o+})
 \end{aligned}$$

**Phasic Velocity Equation, FP j**

Explicit pressure head term, expand for semi-implicit treatment (new-time velocity factors into new-time head):

$$\Delta P_j = \Delta P_j^{n-1} + \left( \frac{d\Delta P}{dQ} \right)^{n-1} (Q_j^n - Q_j^{n-}) \left\{ \begin{array}{ll} \left( \frac{d\Delta P}{dQ} \right)^{n-1} = \rho_m g \left( \frac{dH}{dQ} \right)^{n-1} & Q_j = Af(V_{j,P} + V_{j,A}) \\ \Delta P_j^{n-1} = \rho_m g H_j^{n-1} & H_j^n = H_j^{n-1} + \left( \frac{dH}{dQ} \right)^{n-1} (Q_j^n - Q_j^{n-}) \end{array} \right.$$

**Final expanded term:**

$$\Delta P_j = \rho_m g H_j^{n-1} - \rho_m g Af \left( \frac{dH}{dQ} \right)^{n-1} (V_{j,P}^{n-}) - \rho_m g Af \left( \frac{dH}{dQ} \right)^{n-1} (V_{j,A}^{n-}) + \rho_m g Af \left( \frac{dH}{dQ} \right)^{n-1} (V_{j,\varphi}^n) + \rho_m g Af \left( \frac{dH}{dQ} \right)^{n-1} (V_{j,-\varphi}^n)$$

**New phasic velocity equation:**

$$\begin{aligned}
 & v_{j,\varphi}^n \left( 1 + \left( \frac{K_{j,\varphi}^* \Delta t}{2L_j} \right) |v_{j,\varphi}^{n-} + v'_{j,\varphi}| + \left( \frac{\alpha_{j,-\varphi} f_{2,j} L_{2,j} \Delta t}{\rho_{j,\varphi} L_j} \right) - \zeta \left( \frac{\Delta t}{\rho_{j,\varphi} L_j} \right) \rho_m g Af \left( \frac{dH}{dQ} \right)^{n-1} \right) - v_{j,-\varphi}^n \left( \frac{\alpha_{j,-\varphi} f_{2,j} L_{2,j} \Delta t}{\rho_{j,\varphi} L_j} + \zeta \left( \frac{\Delta t}{\rho_{j,\varphi} L_j} \right) \rho_m g Af \left( \frac{dH}{dQ} \right)^{n-1} \right) \\
 & + \sum_{s,\psi} [C(j, \varphi : s, \psi) v_{s,\psi}^n] = v_{j,\varphi}^{o+} + \left( \frac{K_{j,\varphi}^* \Delta t}{2L_j} \right) (|v'_{j,\varphi}| v_{j,\varphi}^{n-}) + \left( \frac{\Delta t}{\rho_{j,\varphi} L_j} \right) \left( \hat{P}_i + \left( \rho_m g H_j^{n-1} - \zeta \rho_m g Af \left( \frac{dH}{dQ} \right)^{n-1} (V_{j,\varphi}^{n-} + V_{j,-\varphi}^{n-}) \right) - \hat{P}_k \right) \\
 & + (\rho g \Delta z)_{j,\varphi}^o + \frac{\partial(\rho g \Delta z)_{j,\varphi}}{\partial M_{i,P}} (\hat{M}_{i,P}^o - M_{i,P}^{o+}) + \frac{\partial(\rho g \Delta z)_{j,\varphi}}{\partial M_{k,P}} (\hat{M}_{k,P}^o - M_{k,P}^{o+})
 \end{aligned}$$

If  $\zeta = 1$  use semi-implicit formulation

if  $\zeta=0$  revert to fully explicit formulation



- ◆ Derivative  $dH/dQ$  must be evaluated at time level  $n-1$  ( i.e. at  $Q|_{n-1}$  or equivalently at polar homologous variable  $x(\omega|_{n-1}, Q|_{n-1})$  )
- ◆ Recently switched from a Lagrange polynomial approach
- ◆ Use a cubic spline fit to polar homologous head such that, for any given polar homologous independent variable  $x(\omega, Q)$ , can interpolate  $dH/dQ$
- ◆ Calculated once to evaluate the fitting and uses spline fit parameters during the transient

# Homologous Pump Theory Speed Control

## ◆ Three options:

1. Pump speed always under CF/TF control
2. Pump speed always governed by TIE
3. Pump speed under CF/TF control until a pump trip transfers control to TIE

◆ TIE:  $I_p \frac{d\omega}{dt} = \tau_{net} = \tau_{motor} - (\tau_H + \tau_{fr})$

- User-supplied motor and friction torque, hydraulic torque from model
- Net positive torque causes speed increase and vice-versa
- Pump-to-motor connection subject to trip
  - If no trip applies (option 2 above), motor torque always under user control
  - If trip applies (option 3 above), then:
    - OFF state of trip - pump speed under CF/TF control
    - ON-FORWARD state of trip - pump disconnected from motor, thus  $\tau_{motor}$  is zero
    - ON-REVERSE state of trip - pump connected to motor,  $\tau_{motor}$  given by CF/TF

◆ Solve by FE:  $\omega^n = \omega^{n-1} + \frac{\tau_{net}(\omega^{n-1})}{I_p(\omega^{n-1})} \Delta t$  OR BE/FPE:  $\omega^n_{[0]} = \omega^{n-1}$   
 $\omega^n_{[i+1]} = \omega^{n-1} + \frac{\tau_{net}(\omega^n_{[i]})}{I_p(\omega^n_{[i]})} \Delta t$

FE= Forward Explicit

BE=Backwards Explicit

## Homologous Pump Theory Other Features

- ◆ Pump friction torque (factors into TIE), generally a polynomial function:

$$\tau_{fr} = \begin{cases} \pm \tau_{frn}, \text{ for } \left| \frac{\omega}{\omega_R} \right| < S_{PF} \\ \pm \left( \tau_{fr0} + \tau_{fr1} \left| \frac{\omega}{\omega_R} \right|^{x1} + \tau_{fr2} \left| \frac{\omega}{\omega_R} \right|^{x2} + \tau_{fr3} \left| \frac{\omega}{\omega_R} \right|^{x3} \right), \text{ for } \left| \frac{\omega}{\omega_R} \right| \geq S_{PF} \end{cases}$$

- ◆ Pump inertia (factors into TIE), generally a polynomial function:

$$I_p = \begin{cases} I_{pn}, \text{ for } \left| \frac{\omega}{\omega_R} \right| < S_{PI} \\ \left( I_{p0} + I_{p1} \left| \frac{\omega}{\omega_R} \right| + I_{p2} \left| \frac{\omega}{\omega_R} \right|^2 + I_{p3} \left| \frac{\omega}{\omega_R} \right|^3 \right), \text{ for } \left| \frac{\omega}{\omega_R} \right| \geq S_{PI} \end{cases}$$

- ◆ Pump energy dissipation and efficiency

- Total power delivered by impeller to fluid (“brake power”) :  $\tau_H * \omega * 2\pi/60$
- Not all brake power translates into “hydraulic power”:  $gH \left( (1 - \alpha_g) \rho_f V_f + \alpha_g \rho_g V_g \right) Af$
- The difference is “dissipation” due to inefficiency:

$$DISS = \tau_H \omega \frac{2\pi}{60} - gH \left( (1 - \alpha_g) \rho_f V_f + \alpha_g \rho_g V_g \right) Af$$

$$EFF = \frac{gH \left( (1 - \alpha_g) \rho_f V_f + \alpha_g \rho_g V_g \right) Af}{\tau_H * \omega * \frac{2\pi}{60}}$$

- Add dissipation as thermal energy to pump discharge CV

## Homologous Pump Theory Other Features

- ♦ Model is implemented through FP, expand existing **FL\_PMP**
- ♦ **FL\_PMP**, field 4, now has two new possibilities for **PTYPE**
  - **HOM** – User specifies a complement of homologous pump data or use built-in
    - New fields 5 and 6 if field 4 sets **PTYPE** to **HOM**
    - Field 5 is **PHSOPT**, set to **ONE** for single-phase, set to **TWO** for two-phase
    - Field 6 is **DATOPT**, set to **USER** for user data, set to **SEMI** or **LOFT** for built-in
  - **UNIV** – User gives specific speed, opts for interpolation of **UNIV** model data
    - New fields 5 and 6 if field 4 sets **PTYPE** to **UNIV**
    - Field 5 is **PHSOPT**, same as above but note if a departure from single phase occurs, the model defaults to **PTYPE** = **HOM** and **DATOPT** = **SEMI**
    - Field 6 is **DATOPT**, pertains to single phase dissipation, normal, and reversal

```
FL_PMP 3 ! N   PNAME   FLNAME   PTYPE   PHSOPT   DATOPT   ITRIP   CF/TFNAME
1 'PUMP_1' 'FL101' HOM     ONE     USER    ON
2 'PUMP_2' 'FL102' HOM     TWO     SEMI    CF 'CF101'
3 'PUMP_3' 'FL103' UNIV    ONE     SEMI    TF 'TF101'
```

! ITRIP is ON, pump not subject to trip  
! Use a built-in Semiscale data, CF trip  
! Use UNIV model, TF trip

## Homologous Pump User Input

- ◆ New records for rated pump conditions, pump performance model data:
  - **FL\_RPD** – Specify rated pump data, required if **PTYPE** is **HOM** or **UNIV**
    - Pump object number and object name
    - Complement of rated conditions: **OMEGAR**, **SPDRAT**, **QR**, **HR**, **PSHR**, **RHOR**
    - Rated speed, initial-to-rated speed, rated capacity, head, shaft power, density

```
FL_RPD 1 ! N  PNAME  OMEGAR  SPDRAT  QR  HR  PSHR  RHOR
      1 'PUMP1' 3560.0  0.0   0.0114 58.52 1.769E+4 997.95  ! PSHR = (rated hyd torque)*OMEGAR
```

- **FL\_SPH** – Single phase head performance data, required if **PTYPE** is **HOM** and **DATOPT** is **USER**
  - Name TF's for pump data, the two N mode octants are required (other 6 optional)
  - Fields for each octant: **HAN**, **HVN**, **HAD**, **HVD**, **HAT**, **HVT**, **HAR**, **HVR**
  - Use placeholders '-' for excluded octants
  - Also have analogous **FL\_SPT**, **FL\_TPH**, and **FL\_TPT** for single phase torque and two phase head/torque

```
FL_SPH 2 ! N  PNAME  HAN  HVN  HAD  HVD  HAT  HVT  HAR  HVR
      1 'PUMP1' 'HANTF' 'HVNTF' 'HADTF' 'HVDTF' 'HATTF' 'HVTTF' 'HARTF' 'HVRTF'
      2 'PUMP2' 'HANTF' 'HVNTF' 'HADTF' 'HVDTF'  '-'  '-'  '-'  '-'
```



# Homologous Pump User Input

- ◆ New records for friction torque and inertia, numerical treatment:
  - **FL\_PFR** – Specify coefficients, exponents of pump friction torque polynomial
    - Four coefficients, three exponents, one critical speed ratio
    - Recall a constant friction torque is used if below a critical speed ratio

```
FL_PFR 1 ! N  PNAME      TCOEFFC  TCOEFF1  TCOEFF2  TCOEFF3  TEXP1  TEXP2  TEXP3      TFRC  TSPCRT
          1 'PUMP1'  451.0   100.0    50.0    25.0    1.1    2.2    3.3   451.0  0.25
```

- **FL\_PIN** – Specify coefficients of the pump inertia polynomial
  - Four coefficients, one critical speed ratio
  - Recall a constant inertia is used if below a critical speed ratio

```
FL_PIN 1 ! N  PNAME      ICOEFFC  ICOEFF1  ICOEFF2  ICOEFF3  INRC  ISPCRT
          1 'PUMP1'   1.43     1.0     0.5     0.25    1.43   0.25
```

- **FL\_PNT** – Pump numerical treatment (in velocity eqns, for diss. energy)
  - First field is **PNTOPT**, either **SIMP** or **EXP** for semi-implicit or explicit head
  - Second field is **DISOPT**, either **YES** or **NO** to dissipation energy source term

```
FL_PNT 1 ! N  PNAME      PNTOPT  DISOPT
          1 'PUMP1'   SIMP    YES
```

## Homologous Pump User Input

- ◆ New record for pump speed control and motor torque specification
  - **FL\_SMT** – Specify speed control mechanism, motor torque, and CFs/TFs
    - Speed control, third through fifth fields
      - 3rd : **SMTOPT** – **CFTF-ONLY|CFTF-TIE|TIE**
      - 4th : **SFLAG** – **NO|CF|TF** (NO CF/TF control, CF control, or TF control)
      - 5th : ' ', 'CFNAME', 'TFNAME'
    - Motor torque, fifth through seventh fields
      - 6th : **MTFLAG** – **NO|CF|TF** (NO CF/TF control, CF control, or TF control)
      - 7th : ' ', 'CFNAME', 'TFNAME'
    - If no motor torque CF/TF, the constant value is implied by rated conditions

```
FL_SMT 1 ! N  PNAME      SMTOPT  SFLAG  CF/TFNAME  MTFLAG  CF/TFNAME
1 'PUMP1'  CFTF-ONLY  CF      'OMEGA_CF'  CF      'TAUMOT_CF'
2 'PUMP2'  CFTF-TIE    TF      'OMEGA_TF'  NO      ' '
3 'PUMP3'  TIE         NO      ' '         TF      'TAUMOT_TF'
```