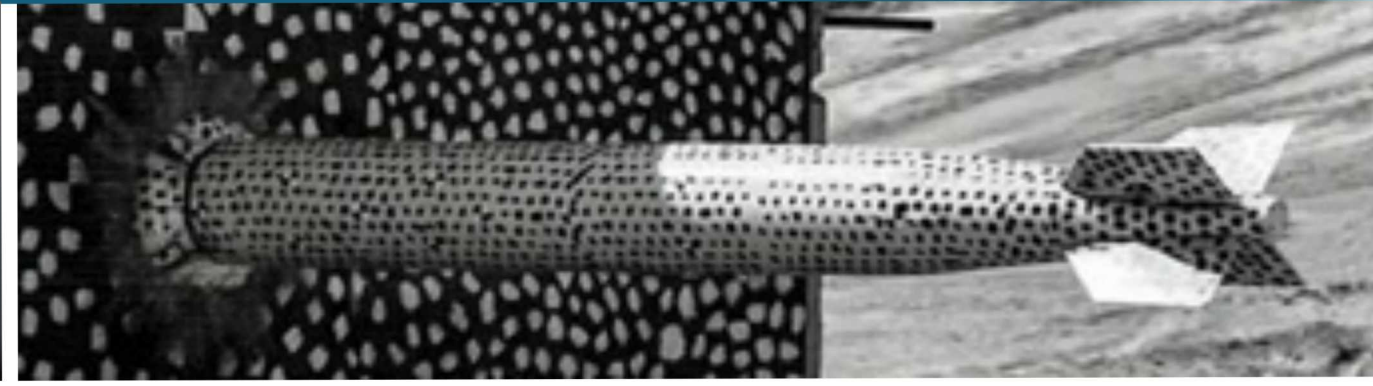
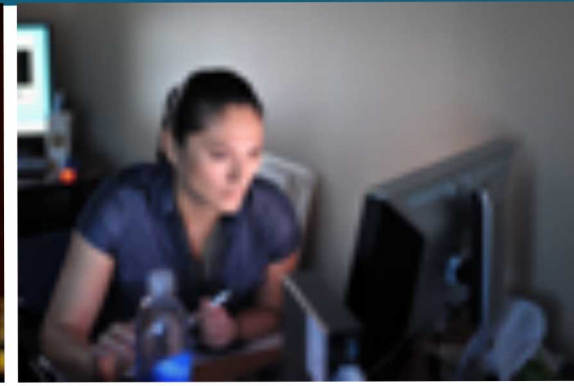
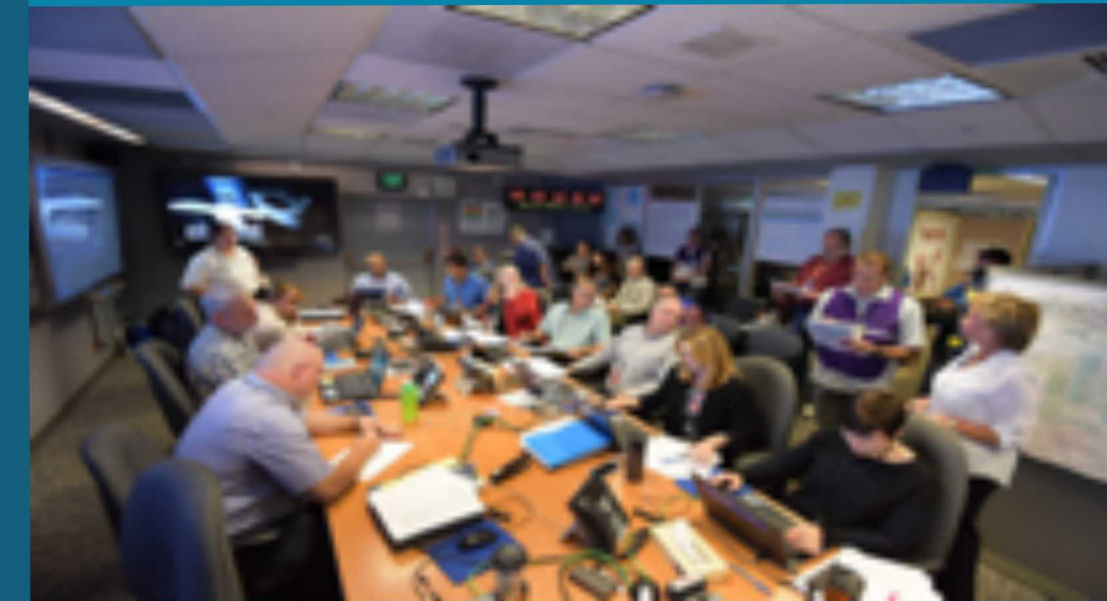




CONSTRUCTING AND ACCESSING TABULATED CHEMISTRY FOR FIRE SCENARIOS

SAND#



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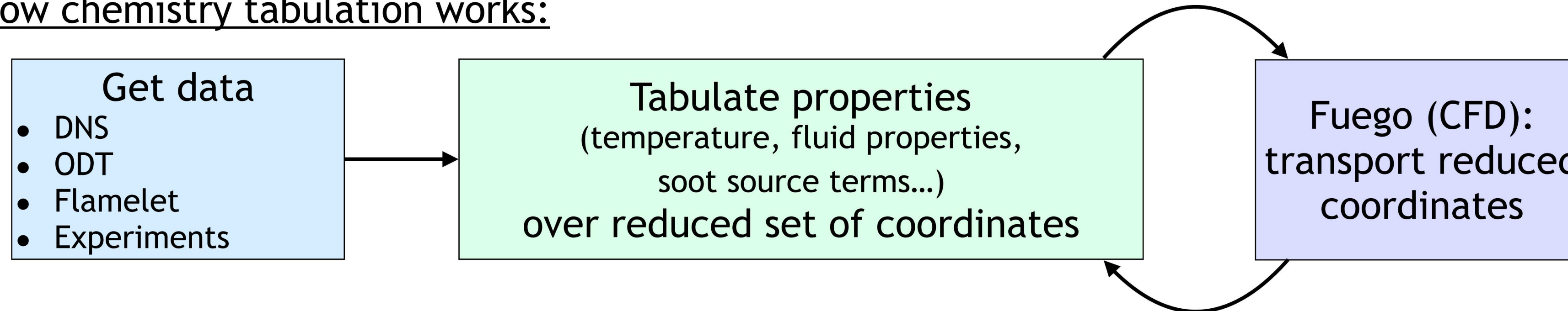
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Non-adiabatic flamelet chemistry tabulation with LES/RANS enables simulation of sooting, turbulent fires at engineering scales of interest



- Tabulation techniques aid in making fire simulations computationally feasible
- We were seeing over-predictions in soot and unstable simulations in some cases...
- Want to explore different ways of constructing/accessing chemistry tables

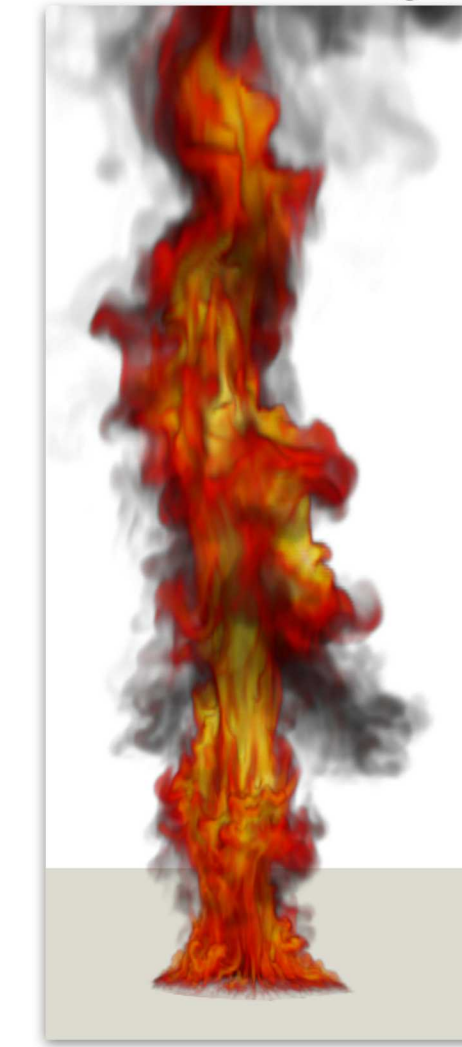
How chemistry tabulation works:



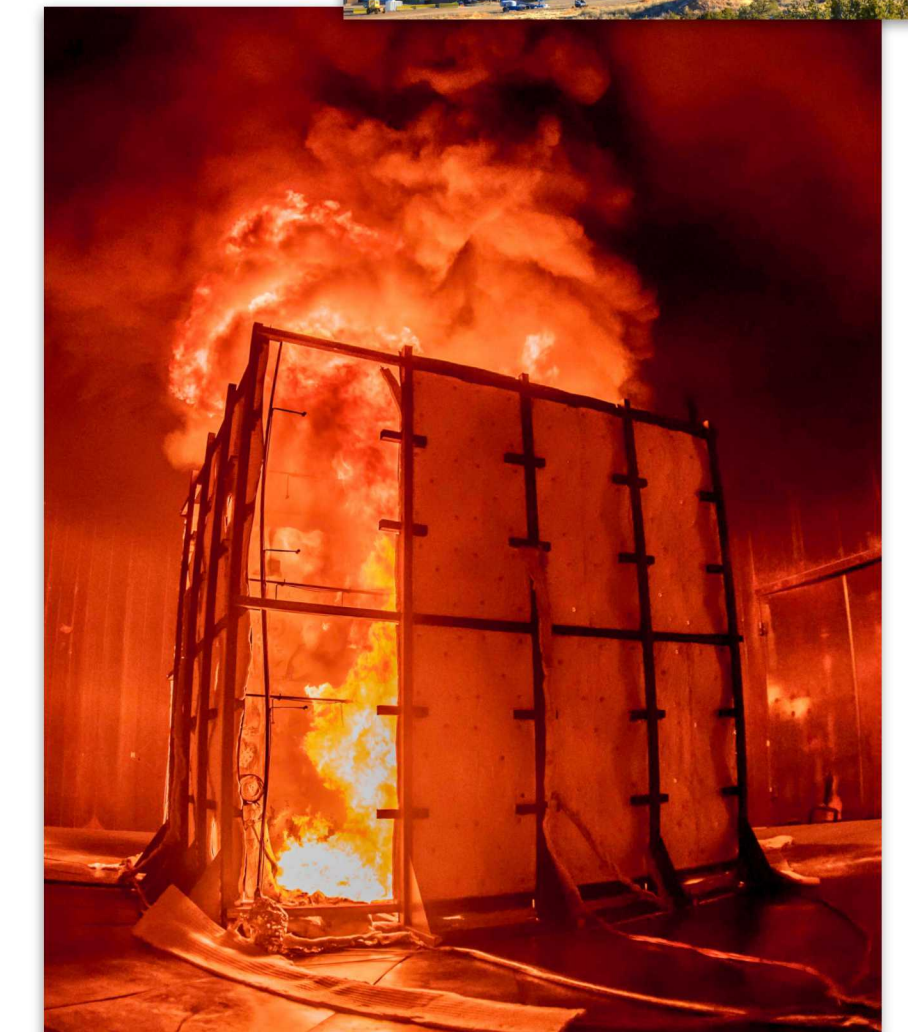
Options for the reduced set of coordinates: (for strongly sooting and radiating fires)

- composition*
- 1 dimension: mixture fraction (z)
Equilibrium, Burke-Schumann
- composition, strain*
- 2 dimensions: z , scalar dissipation rate (χ)
Steady Laminar Flamelet Model (SLFM)
- composition, strain, heat loss*
- 3 dimensions: z , χ , enthalpy (h) or enthalpy deficit ($\gamma = h - h_{ad}$)
Non-adiabatic Flamelet Model

SIERRA/Fuego



SNL's Thermal Test Complex



Non-adiabatic flamelet chemistry tabulation with LES/RANS enables simulation of sooting, turbulent fires at engineering scales of interest



Options for the reduced set of coordinates: (for strongly sooting and radiating fires)

1 dimension: mixture fraction (z)

Equilibrium, Burke-Schumann

2 dimensions: z , scalar dissipation rate (χ)

Steady Laminar Flamelet Model (SLFM)

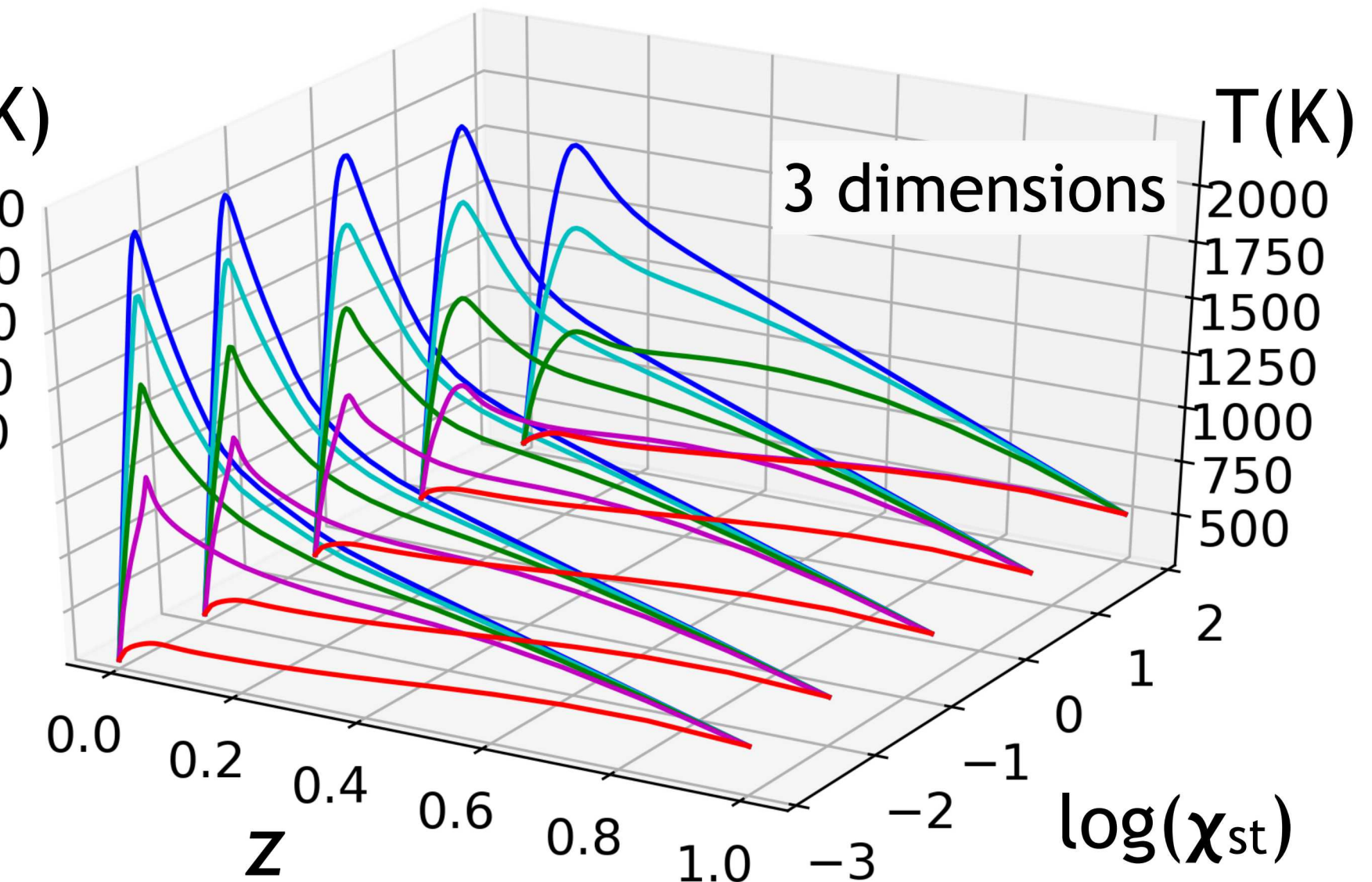
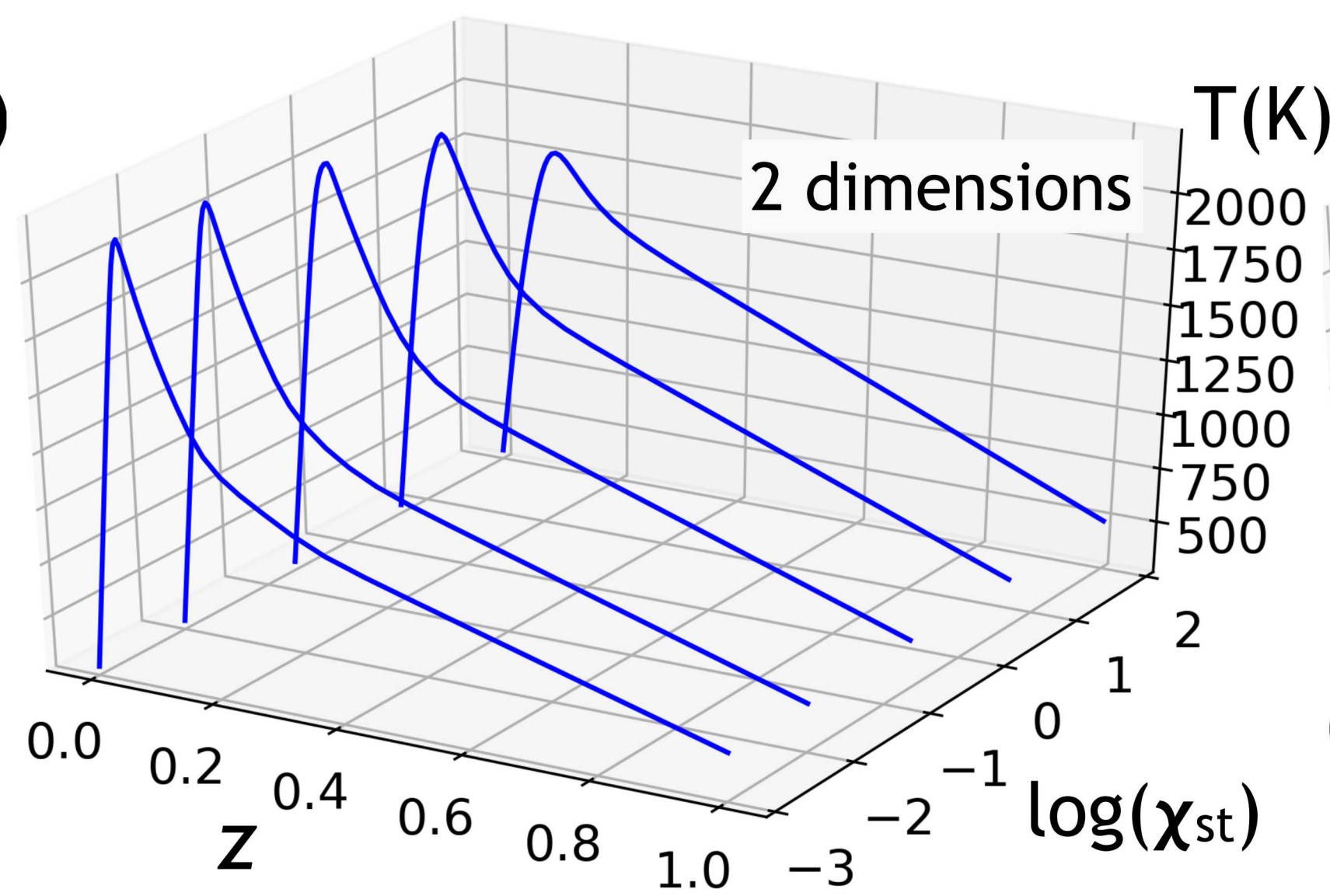
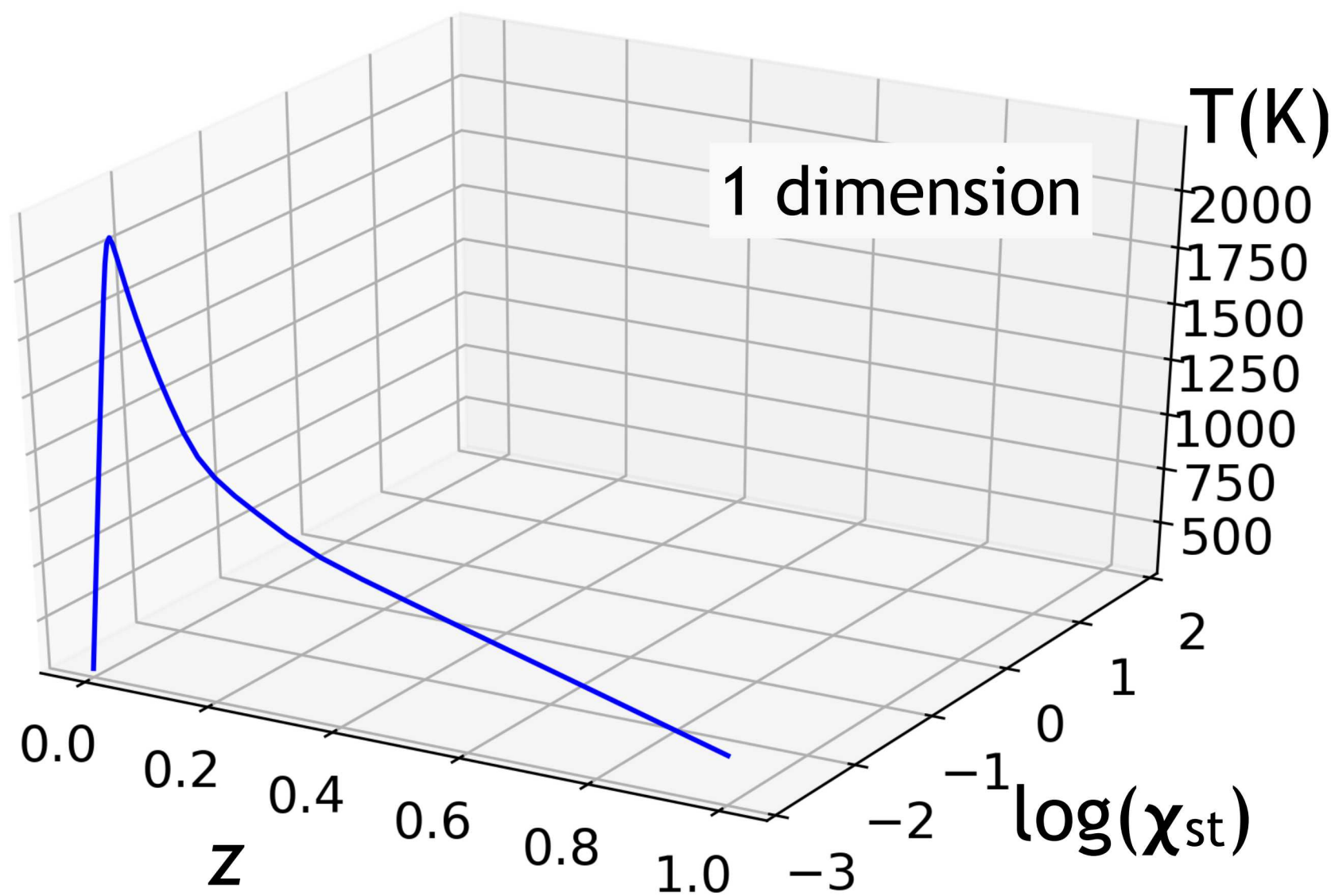
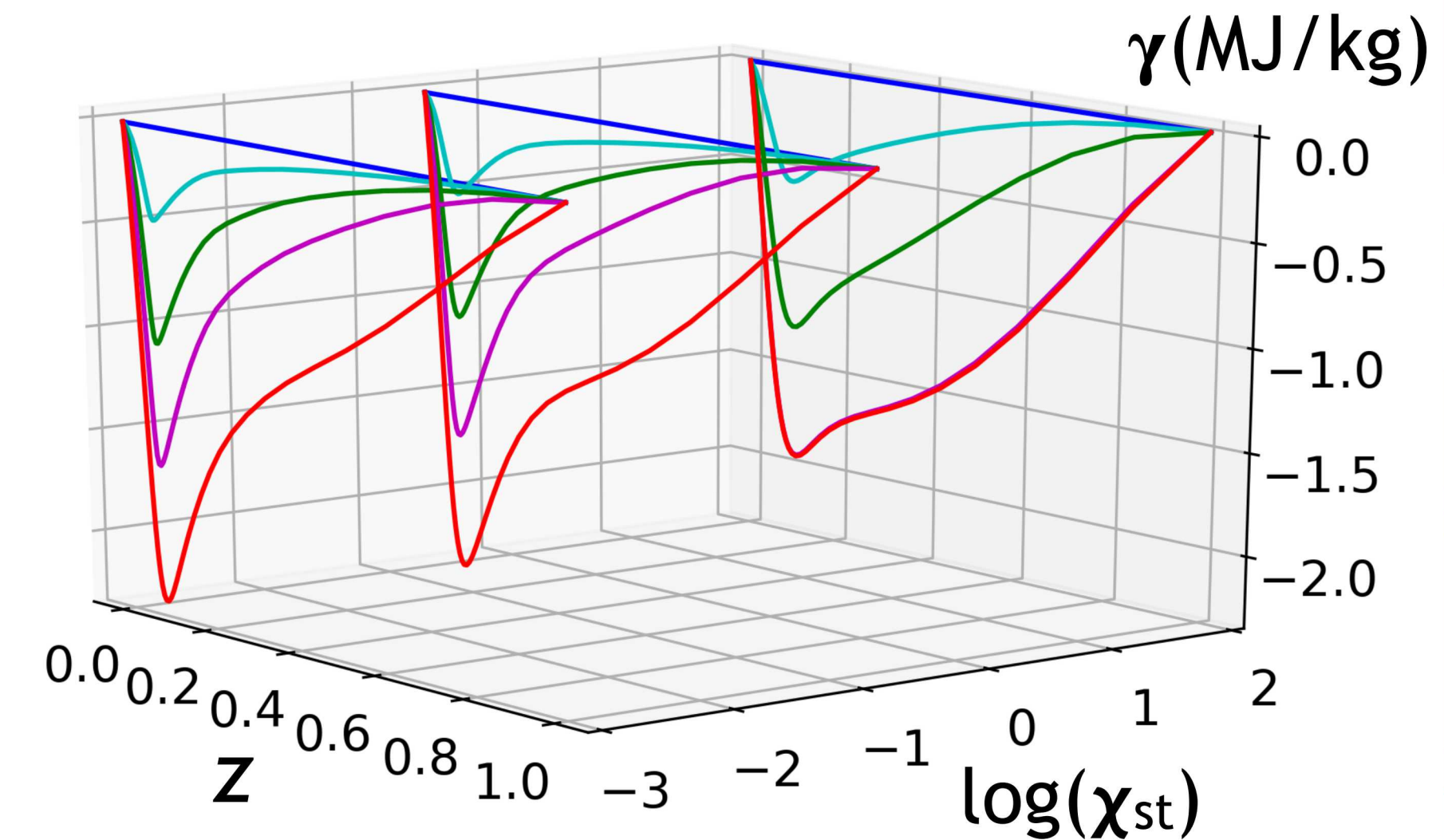
3 dimensions: z , χ , enthalpy deficit ($\gamma = h - h_{ad}$)

Non-adiabatic Flamelet Model

composition

composition, strain

composition, strain, heat loss

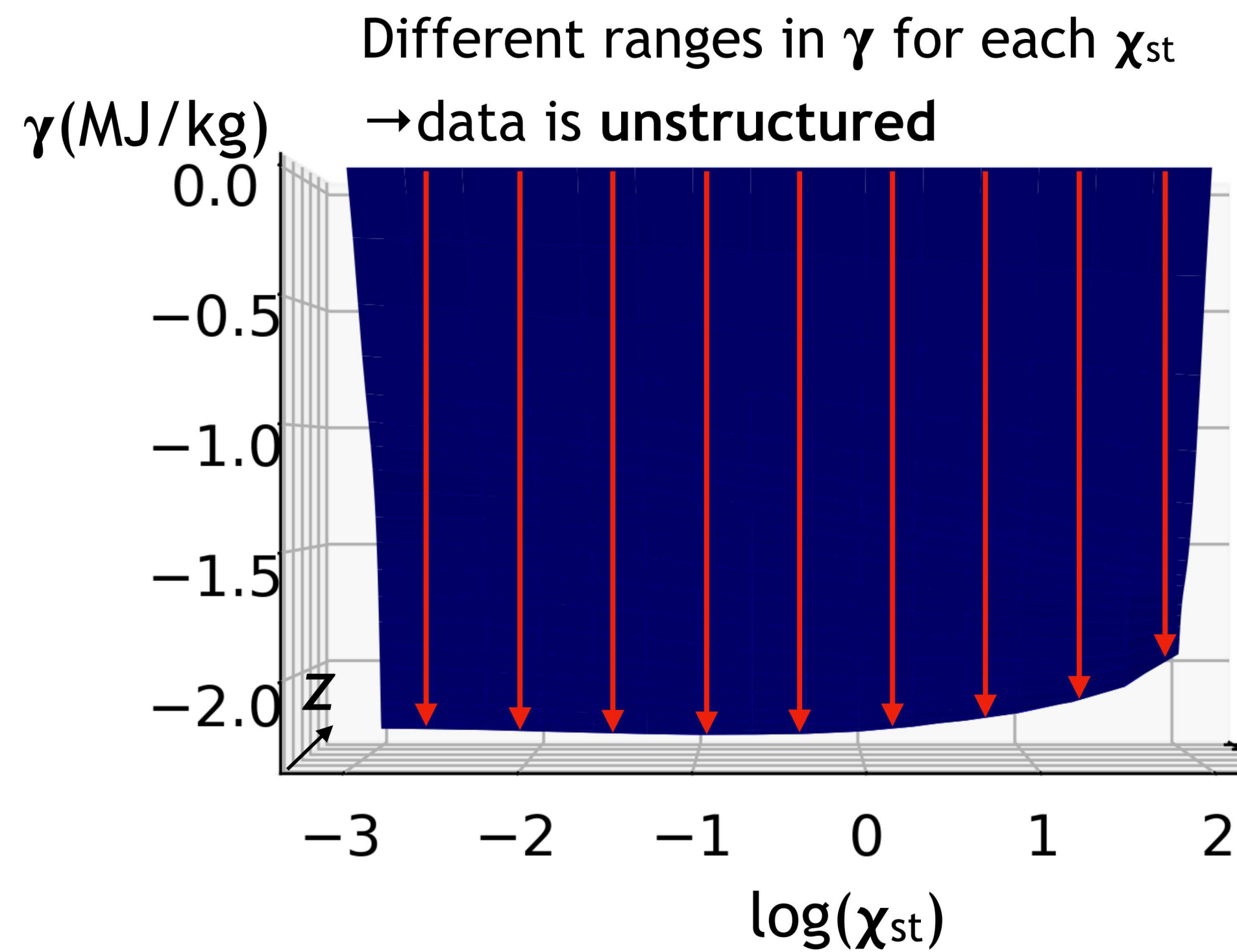




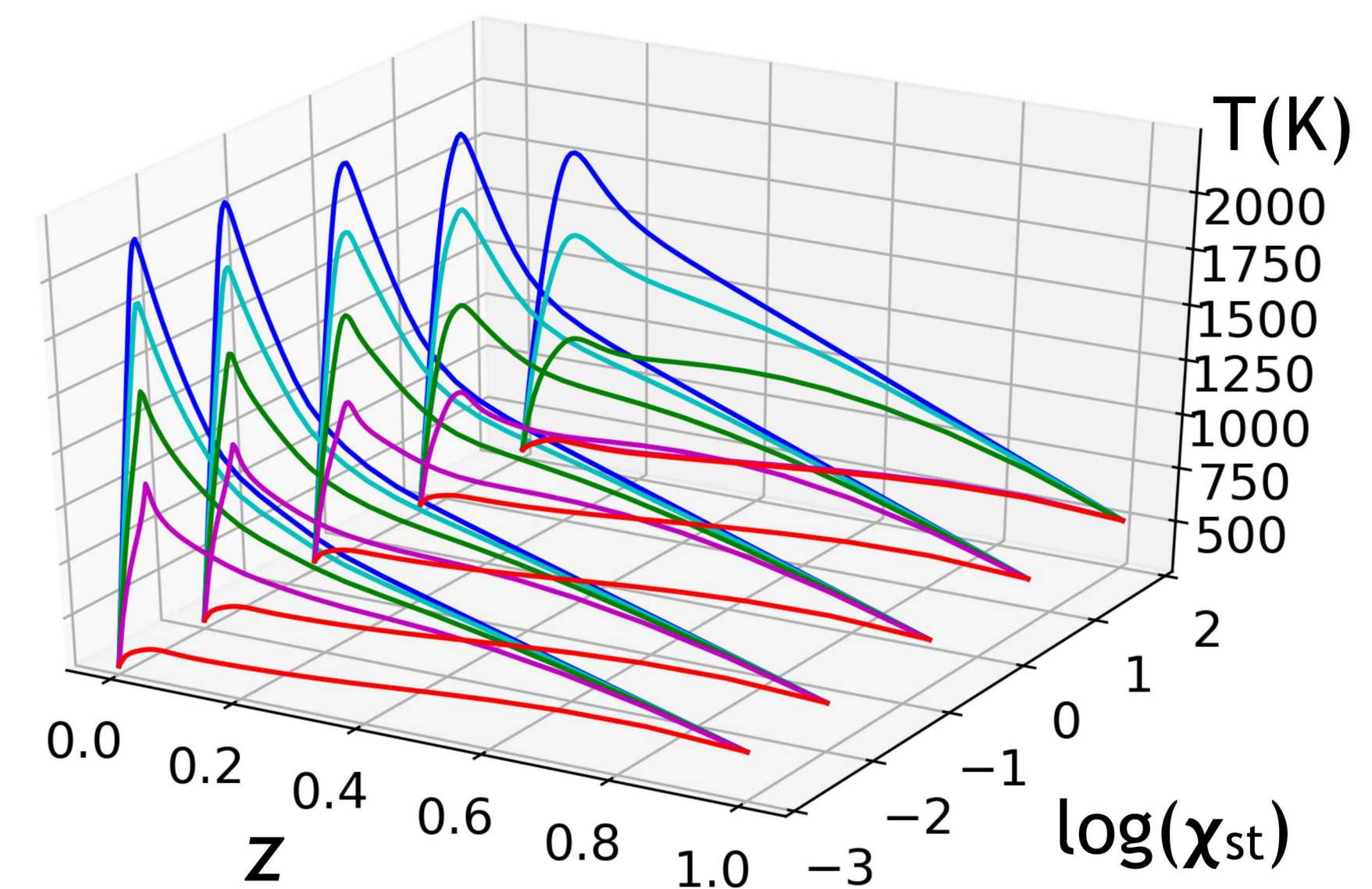
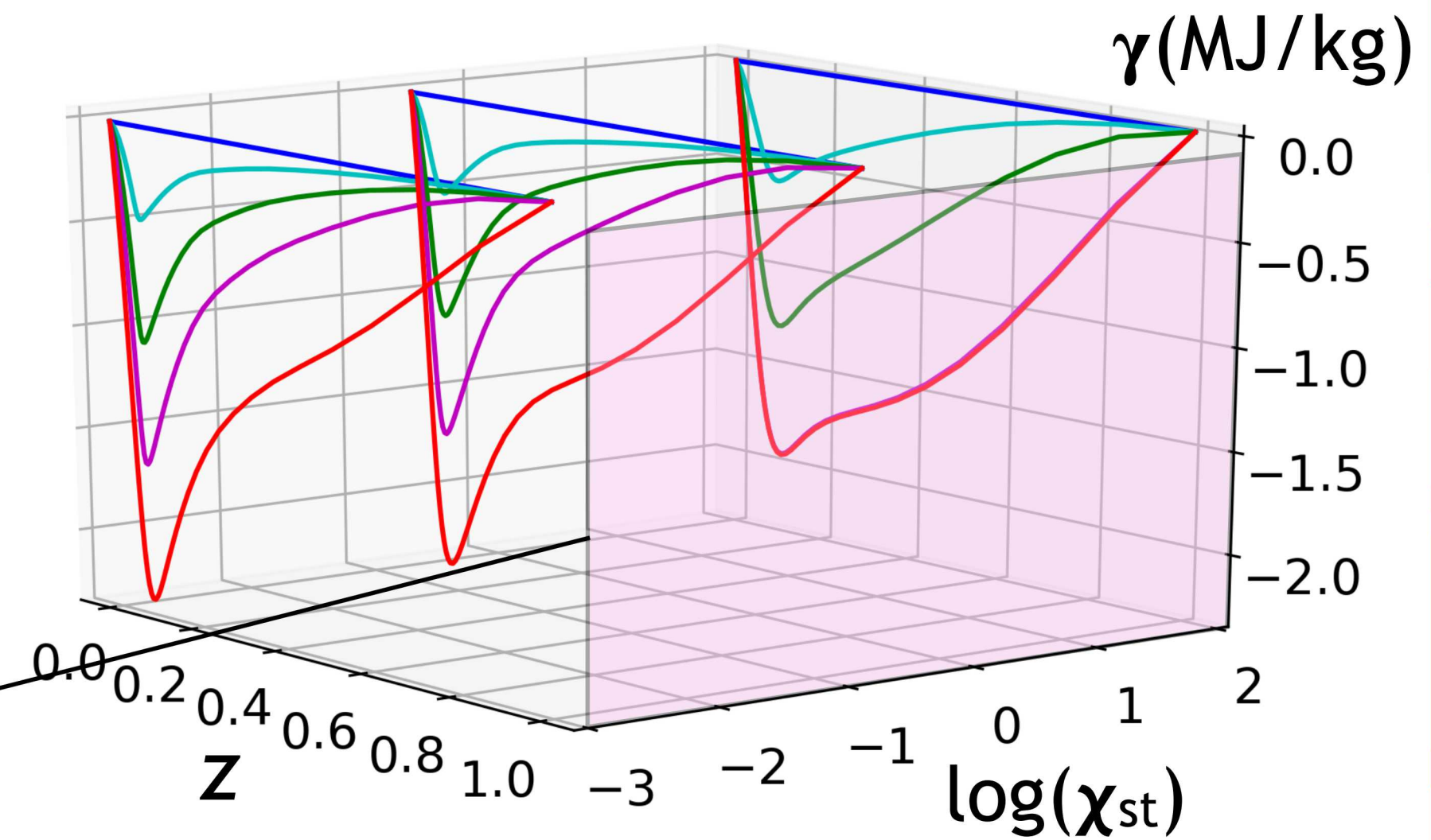
Unstructured non-adiabatic
flamelet data over (z, χ, γ)

Interpolation onto structured grid (for speed)

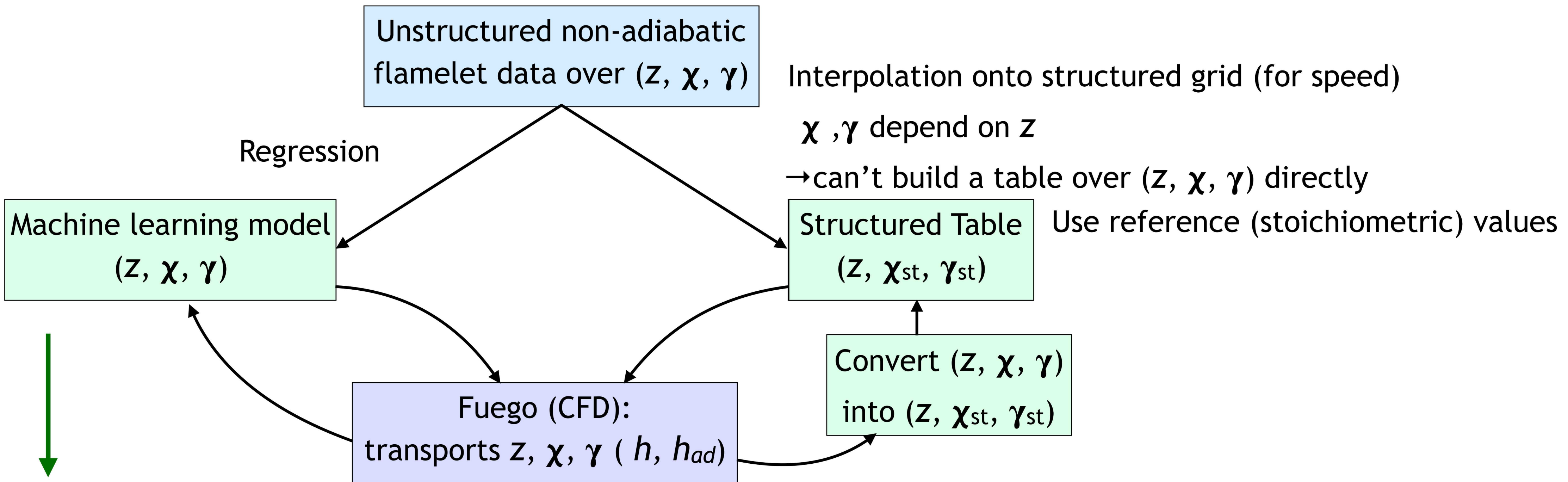
Structured Table



Viewing
this plane



There are challenges in constructing and accessing tabulated/modeled chemistry



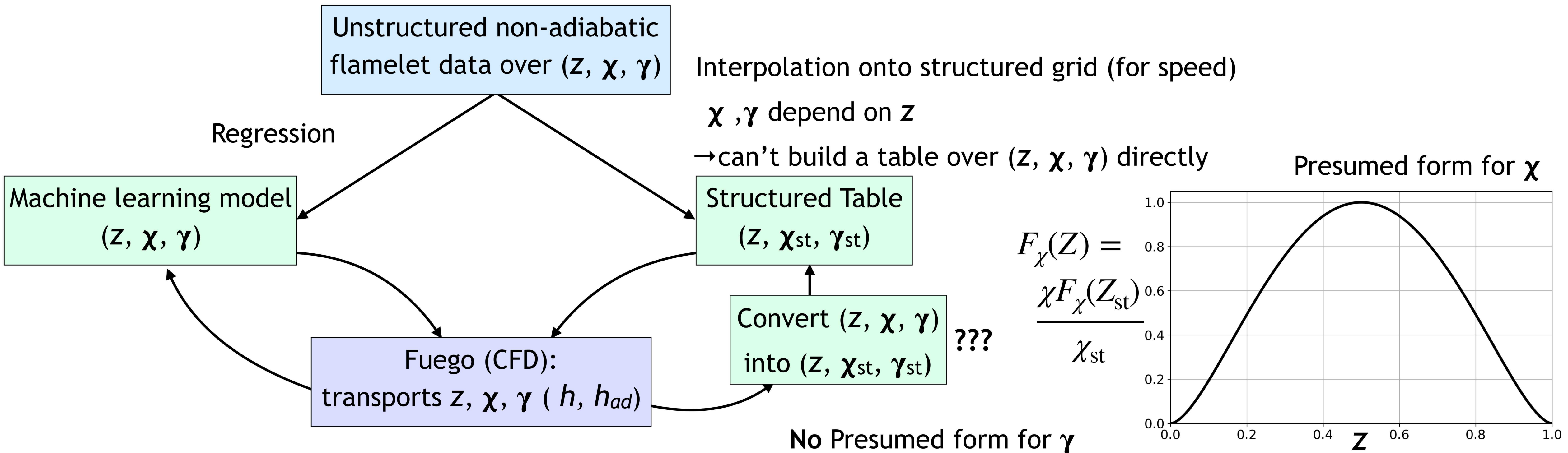
Advantages:

- Simulation variables are the model inputs
- Smaller memory requirements
- Higher dimensional models

Disadvantages:

- Challenges associated with finding “optimal” networks
- Difficult to determine error bounds
- More expensive to query a neural network than interpolant

There are challenges in constructing and accessing tabulated/modeled chemistry

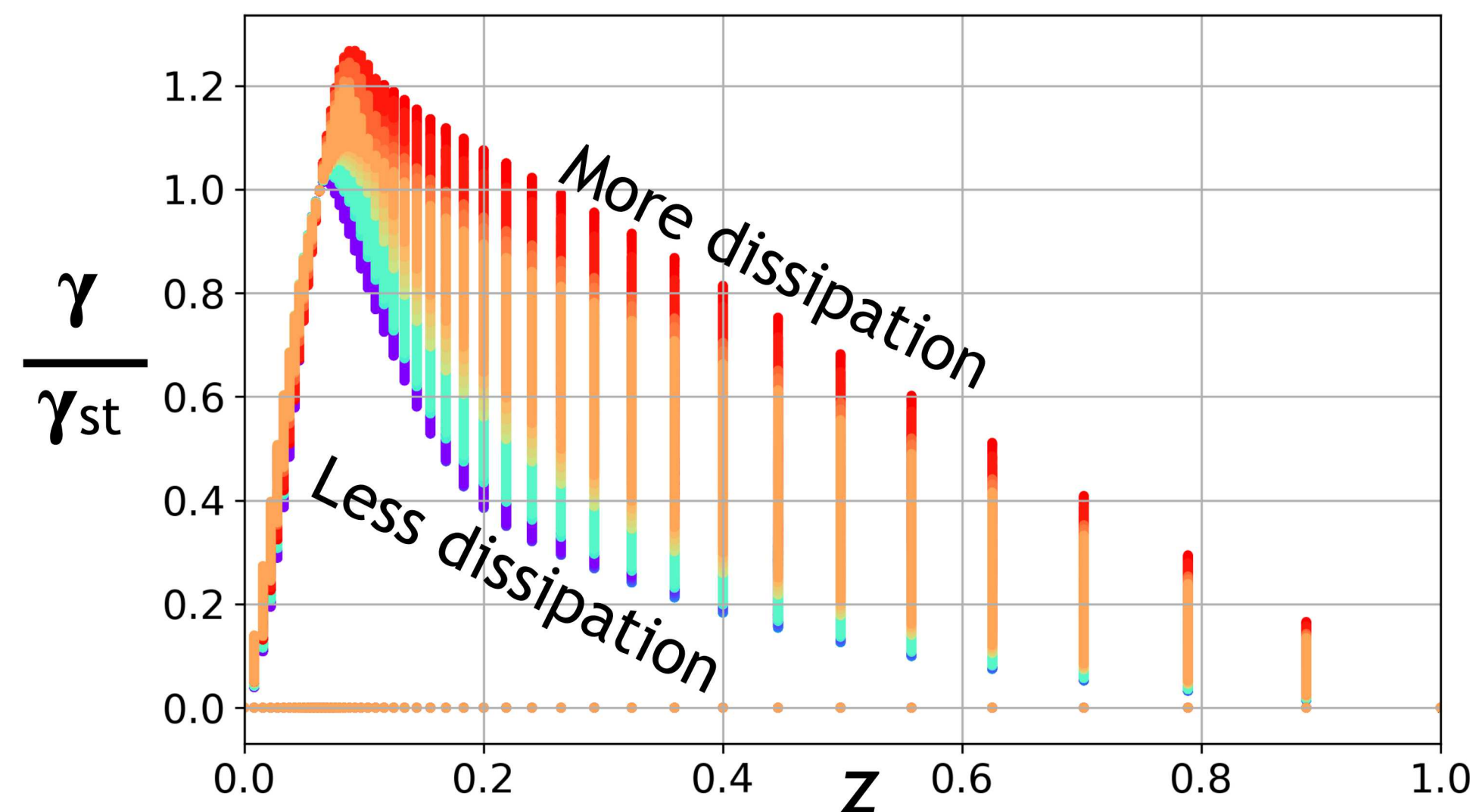


Consistent Enthalpy Reconstruction (CER)

- Find the correct γ_{st} in the table using a (Newton-based) root finding method

$$\gamma_{table}(Z, \chi_{st}, \gamma_{st}) = \gamma_{CFD}$$

- Requires have γ in the property table
- More accurate
- More expensive



Approximate Enthalpy Reconstruction (AER)

Presume a functional form for $\gamma(Z; \gamma_{st})$

$$\gamma = F_{\gamma}(Z) \gamma_{st}$$

There are challenges in constructing and accessing tabulated/modeled chemistry



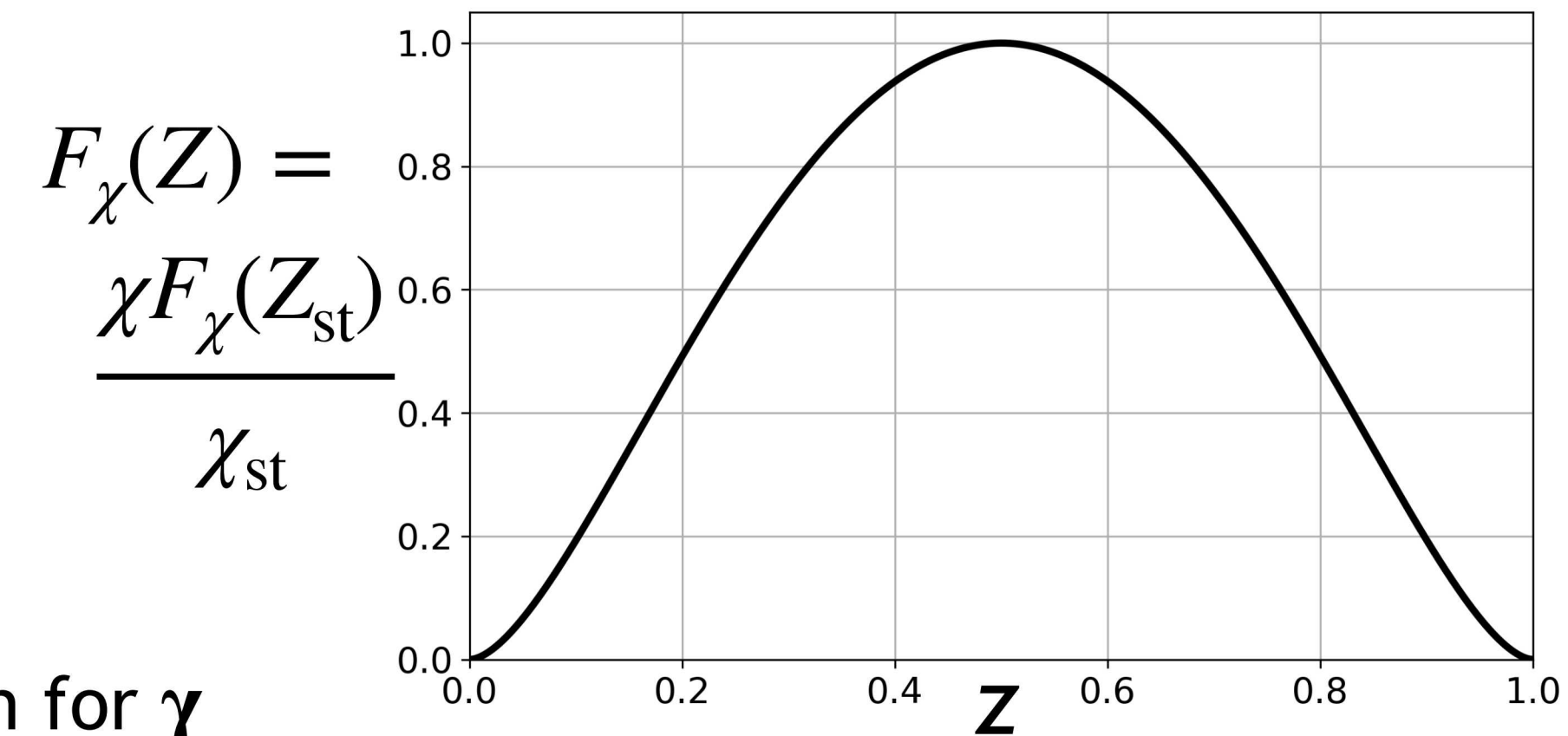
Unstructured non-adiabatic
flamelet data over (Z, χ, γ)

Interpolation onto structured grid (for speed)

χ, γ depend on Z

→ can't build a table over (Z, χ, γ) directly

Presumed form for χ



No Presumed form for γ

Regression

Machine learning model
 (Z, χ, γ)

Structured Table
 $(Z, \chi_{st}, \gamma_{st})$

Convert (Z, χ, γ)
into $(Z, \chi_{st}, \gamma_{st})$???

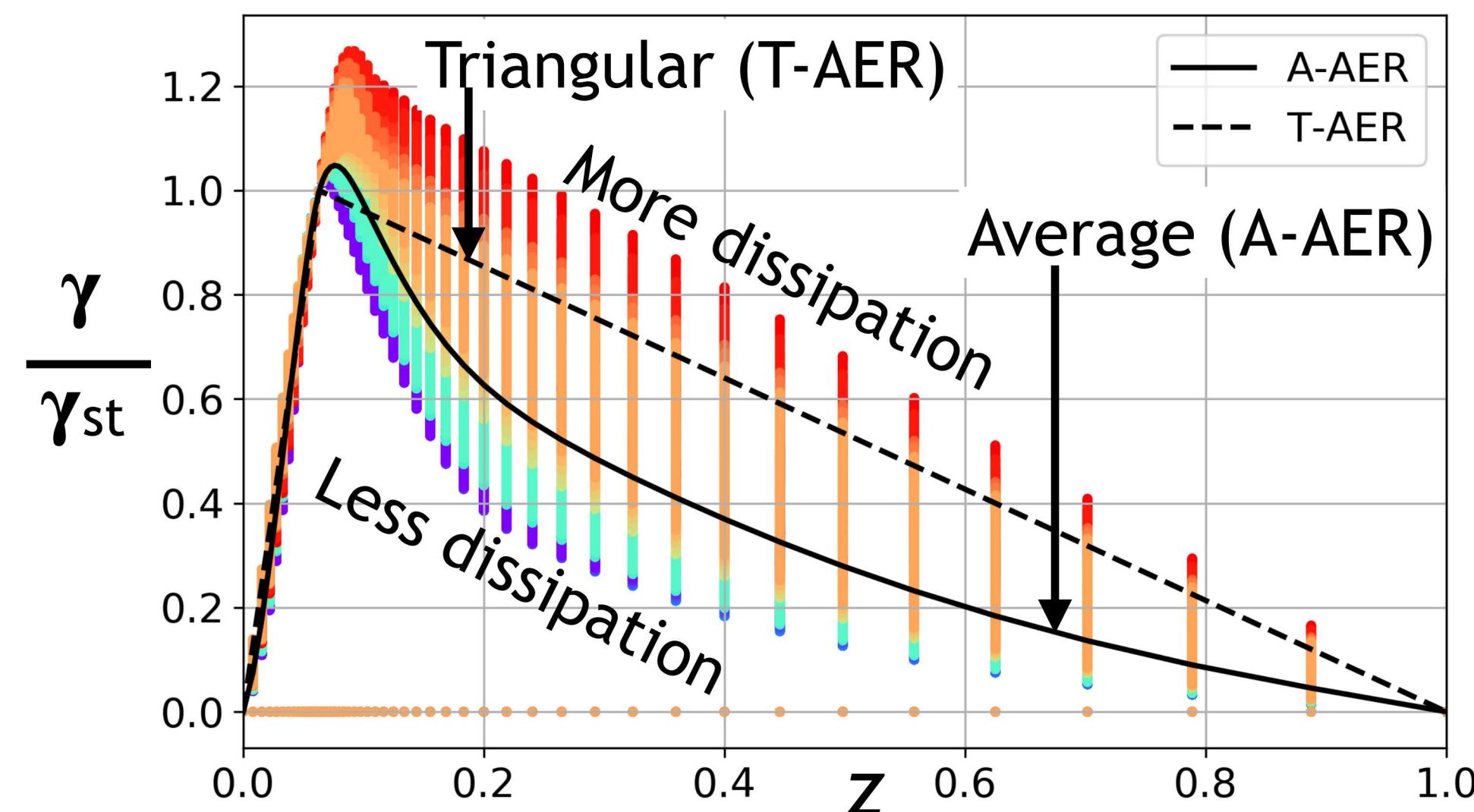
Fuego (CFD):
transports $Z, \chi, \gamma (h, h_{ad})$

Consistent Enthalpy Reconstruction (CER)

- Find the correct γ_{st} in the table using a (Newton-based) root finding method

$$\gamma_{table}(Z, \chi_{st}, \gamma_{st}) = \gamma_{CFD}$$

- Requires have γ in the property table
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Approximate Enthalpy Reconstruction (AER)

Presume a functional form for $\gamma(Z; \gamma_{st})$

$$\gamma = F_{\gamma}(Z) \gamma_{st}$$

The AER methods lead to substantial errors in scenarios with high heat loss



Ethylene laminar coflow, sooting jet steady state

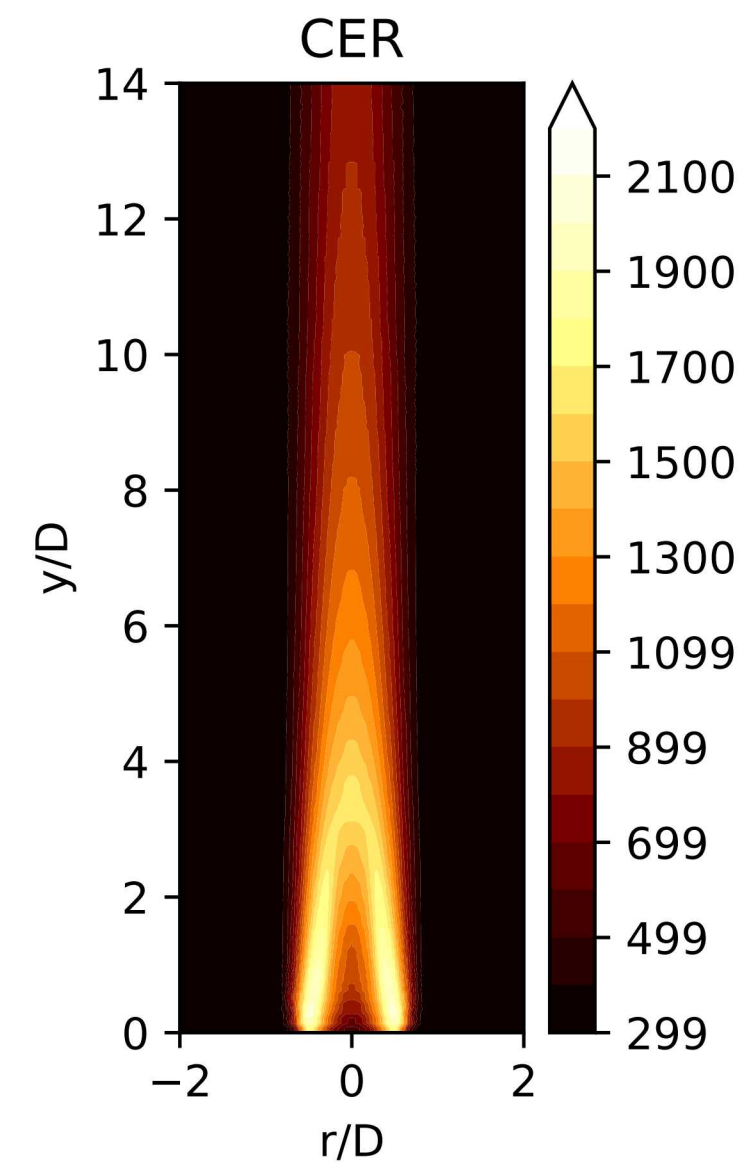
11 mm diameter (D) jet

Simple radiation model ($4\sigma T_{\text{ref}}^4$)

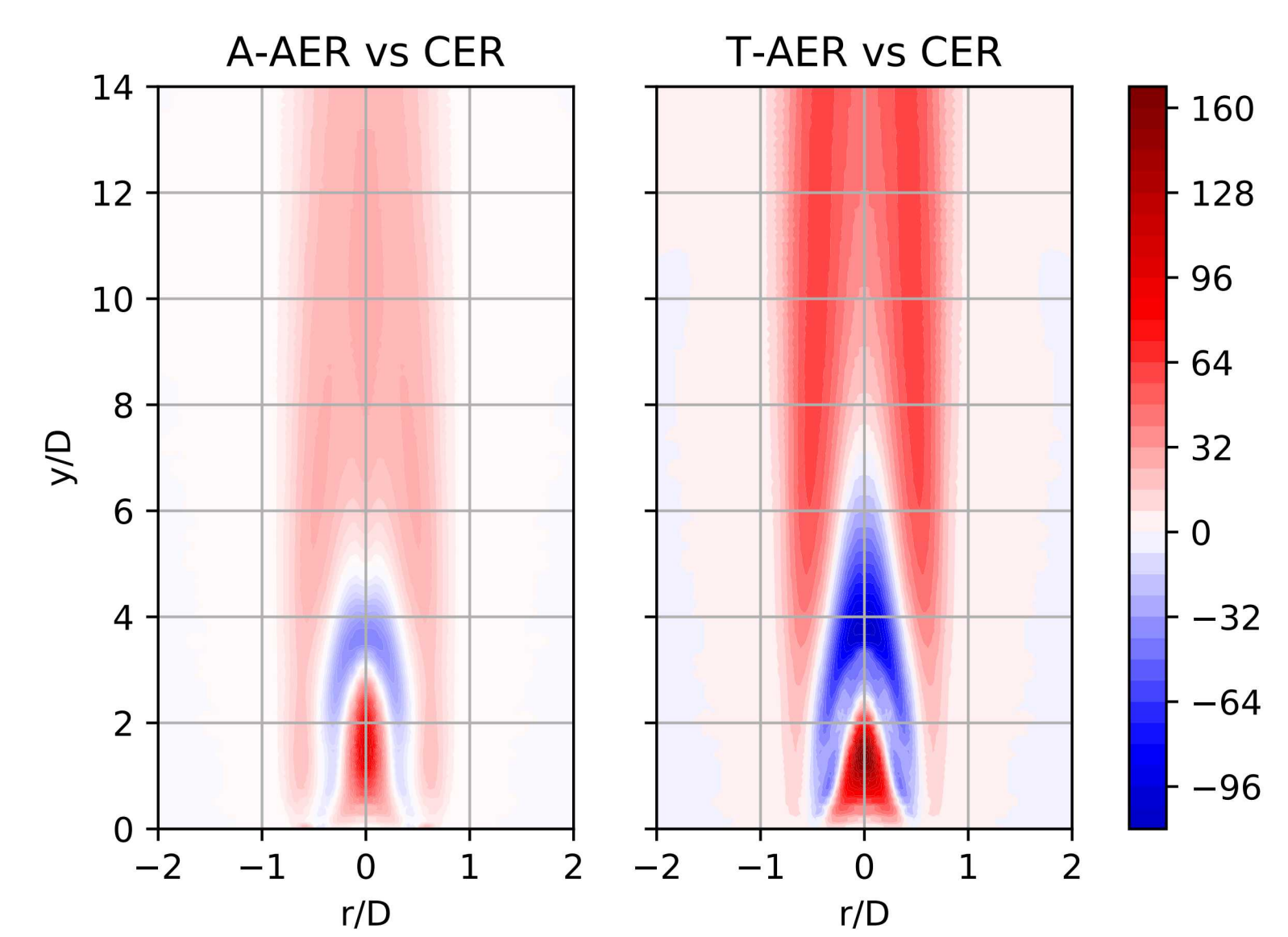
2-equation soot model

- Non-linear trend in temperature errors moving up centerline
 - Largest errors in rich regions near inlet, O(100 K)
- Persistent errors (errors remain in steady state)
- 10% over-prediction in soot for T-AER than CER
 - Emitting more smoke
 - 2% over-prediction in soot for A-AER than CER
- Overall less error in A-AER method compared to T-AER
- Little to no errors in pure streams and near adiabatic
- Observed similar trends in the errors for heptane and for a participating media radiation model
- The CER simulation was 2x slower than the T-AER simulation
 - Currently performing Newton solve for every property table
 - Optimal redesign should result in only 5-10% more time for CER

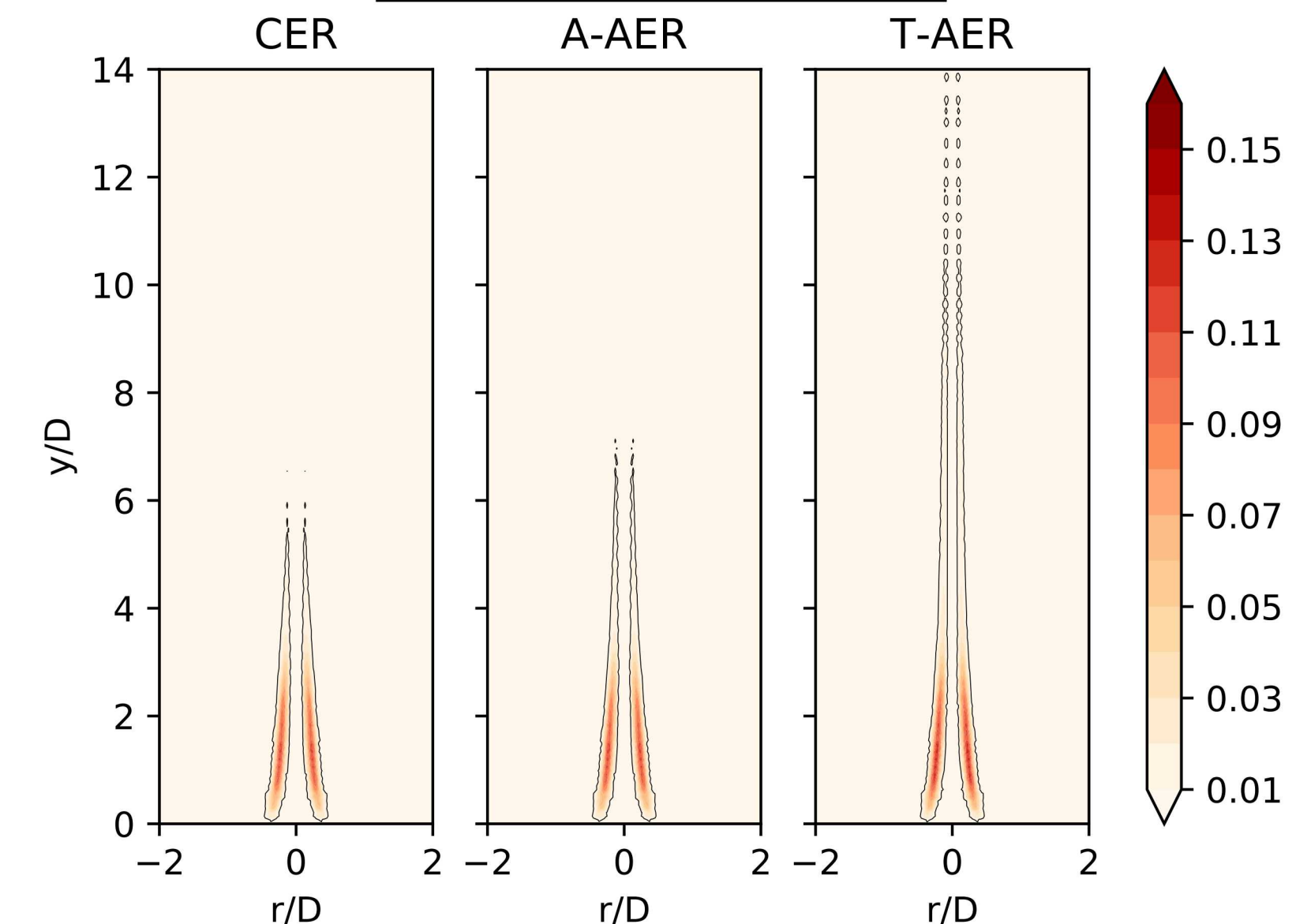
temperature (K)



temperature error (K)



soot mass fraction



Machine learning is a promising alternative to structured chemistry tabulation



Machine learning model
(z, χ, h)

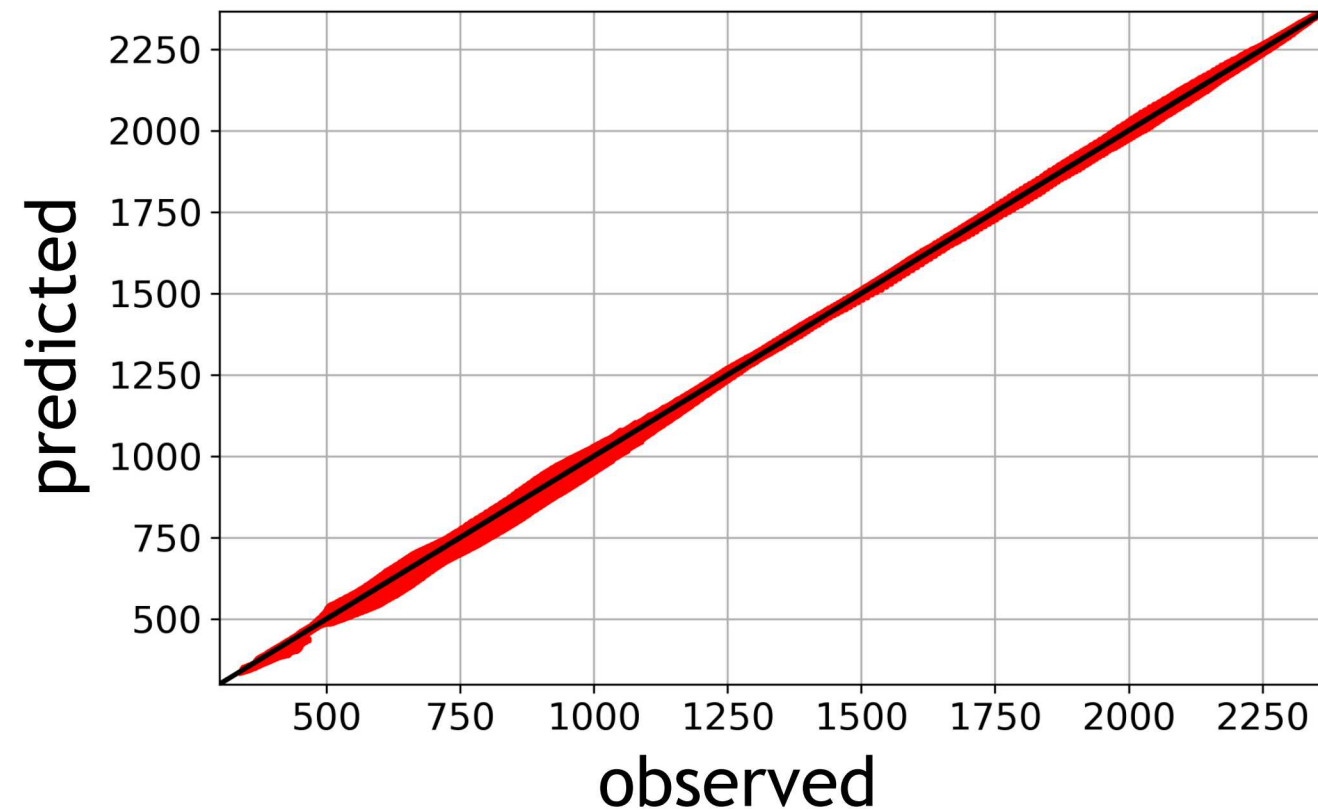
Unstructured (T, ρ)
ethylene flamelet data

Structured Table (CER, AER)
($z, \chi_{st}, \gamma_{st}$)

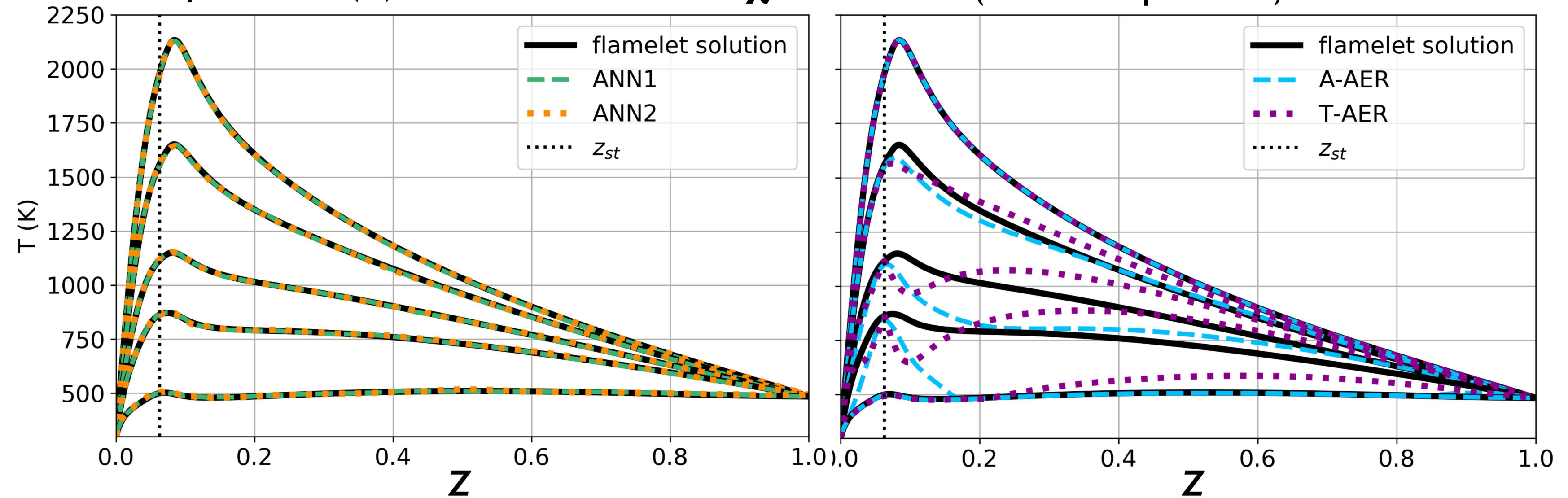
ANN1: trained on whole
unstructured flamelet dataset

ANN2: trained on every
other point in dataset

Temperature parity plot (ANN2)



Temperature (K) reconstructions for $\chi_{st} = 11 \text{ s}^{-1}$ (selected profiles)



- The ANNs have **more** error than CER, but **less** error than AER methods
- ANNs trained on coarsened datasets show good accuracy
- ANNs are only 1 MB compared to 28 MB for a structured table build using (T, ρ, γ)
 - Structured tables can reach around a few GB large for actual turbulent simulations

Conclusions

- AER methods lead to substantial errors in scenarios with high heat loss
 - Up to 10% over-prediction in steady state soot mass fraction for T-AER compared to CER for the laminar sooting ethylene jet flame studied here
 - Improved approximations can be constructed (A-AER), but are not generally accurate
- The CER method offers more accuracy for high heat loss scenarios
 - Should only be 5-10% more expensive than AER when optimized
- Replacing structured tabulation with ANNs shows promise
 - May dramatically reduce memory ~30x
 - May enable higher dimensional models
 - Shows accuracy between AER and CER

Future Work

- Explore optimal ANNs and run *in situ* for flame calculations
- Study optimized interpolants to improve CER
- Perform more detailed cost analysis between CER and ANN approaches
- Test in turbulent simulations at scale

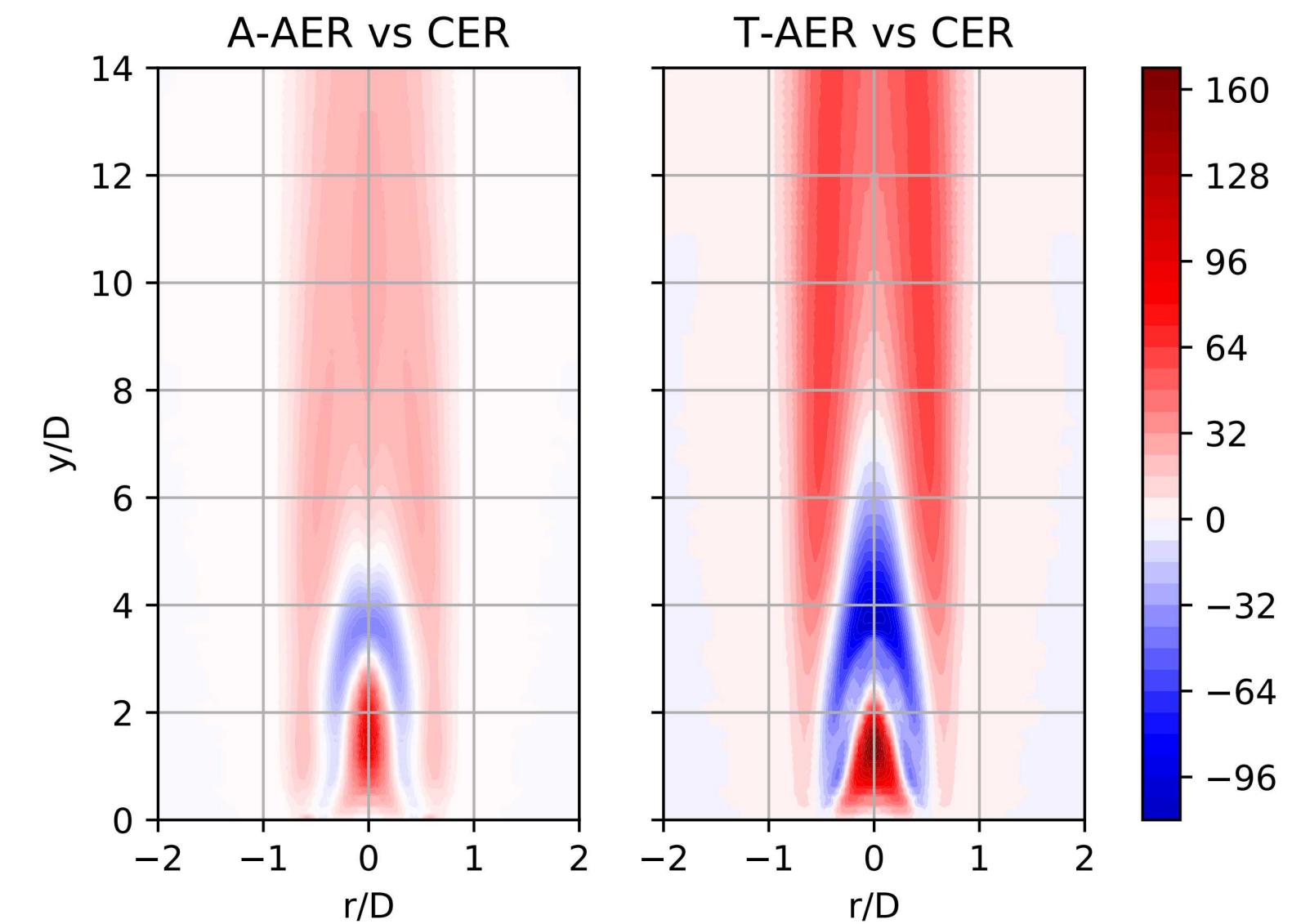
Acknowledgements

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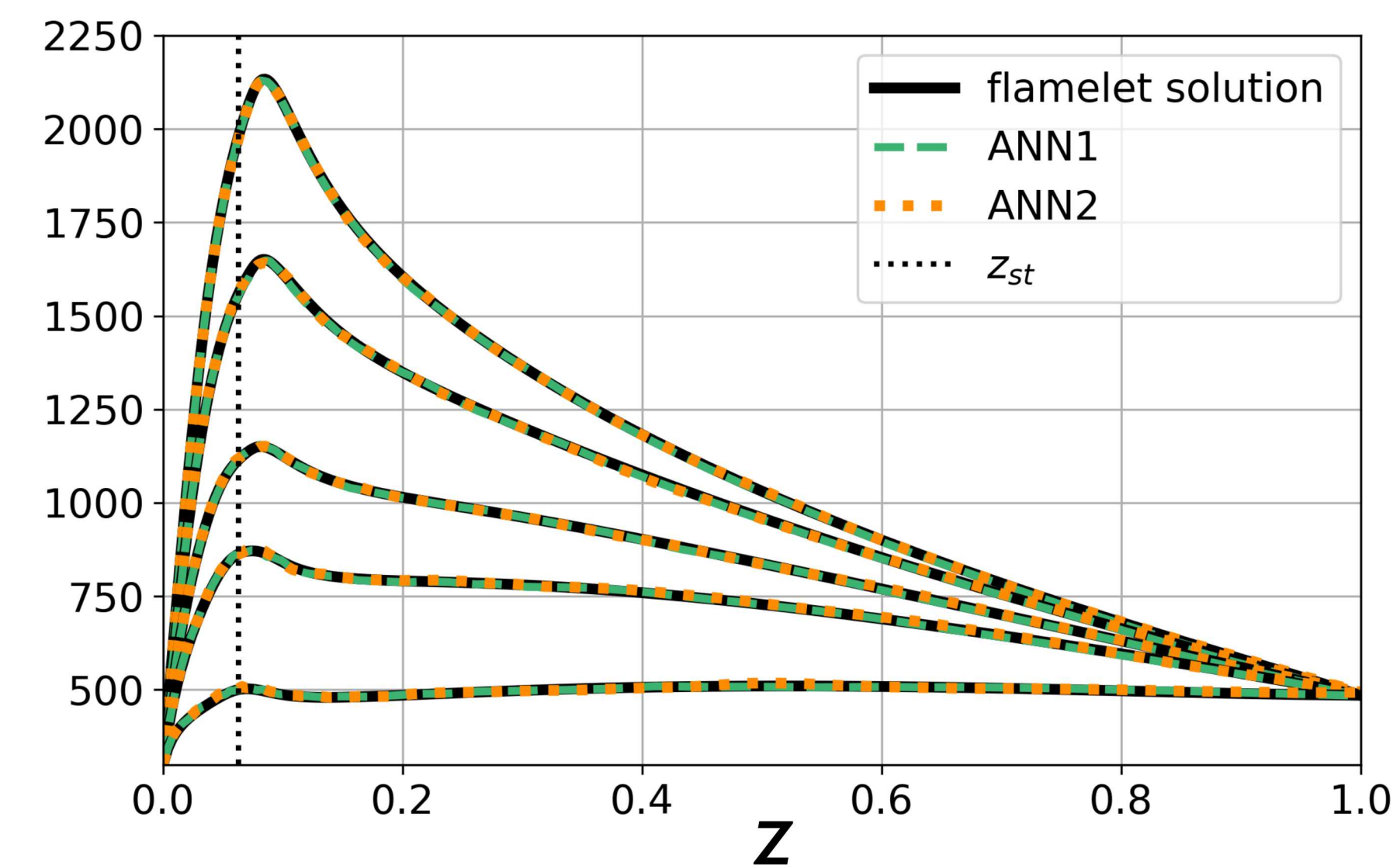
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Research Staff (SNL)
Research Staff (SNL)
Research Staff (SNL)
Professor of Chemical Engineering (Univ. Of Utah)



temperature error (K)



Temperature (K) reconstructions for $\chi_{st} = 11 \text{ s}^{-1}$



Supplemental Slides

A transient non-adiabatic flamelet approach enables a large enough range of states accessed in sooting, turbulent fire simulations

$$\frac{\partial Y_i}{\partial t} = \frac{\chi}{2} \frac{\partial^2 Y_i}{\partial Z^2} + \frac{\omega_i}{\rho}$$

$$\frac{\partial T}{\partial t} = \frac{\chi}{2} \frac{\partial^2 T}{\partial Z^2} - \frac{1}{\rho c_p} \sum_{i=1}^n \omega_i h_i - \frac{H \chi_{\max}}{\rho c_p} \frac{1 - Z_{\text{st}}}{Z_{\text{st}}} \frac{T - T_{\infty}}{T_{\max} - T_{\infty}}$$

adiabatic formulation

non-adiabatic formulation

provide cooling for flames with higher mixing rates

related to heat released, hydrocarbons $O(10^7 \text{ J/m}^3)$

more uniform heat loss during transient heat-loss driven extinction

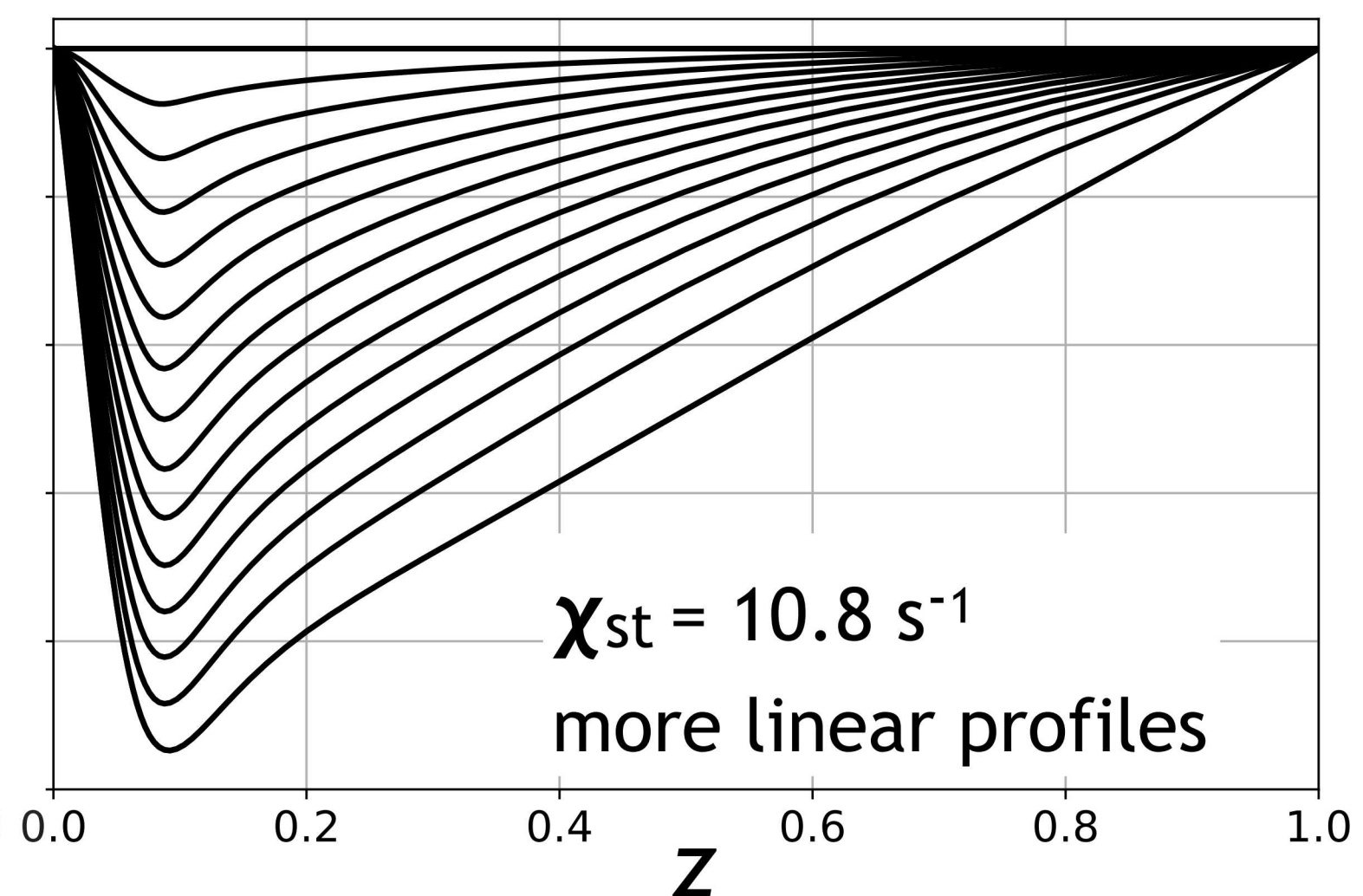
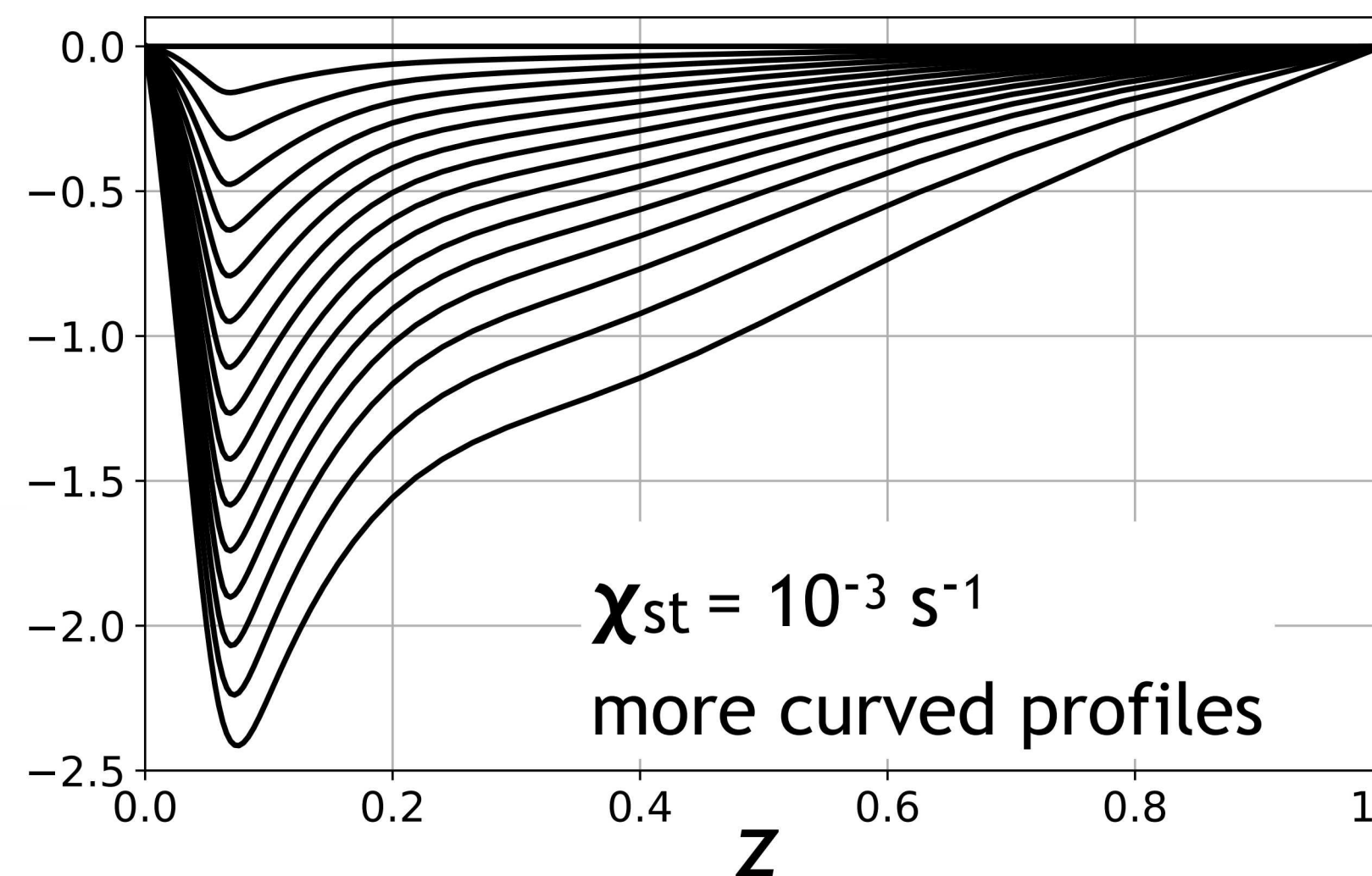
linear background temperature

avoid increase in stoichiometric enthalpy from reactant mixing

Integrate equations until T comes within 5% of $\max(T_{\infty})$

Solved using Spitfire
(soon to be open-sourced)

γ (MJ/kg)



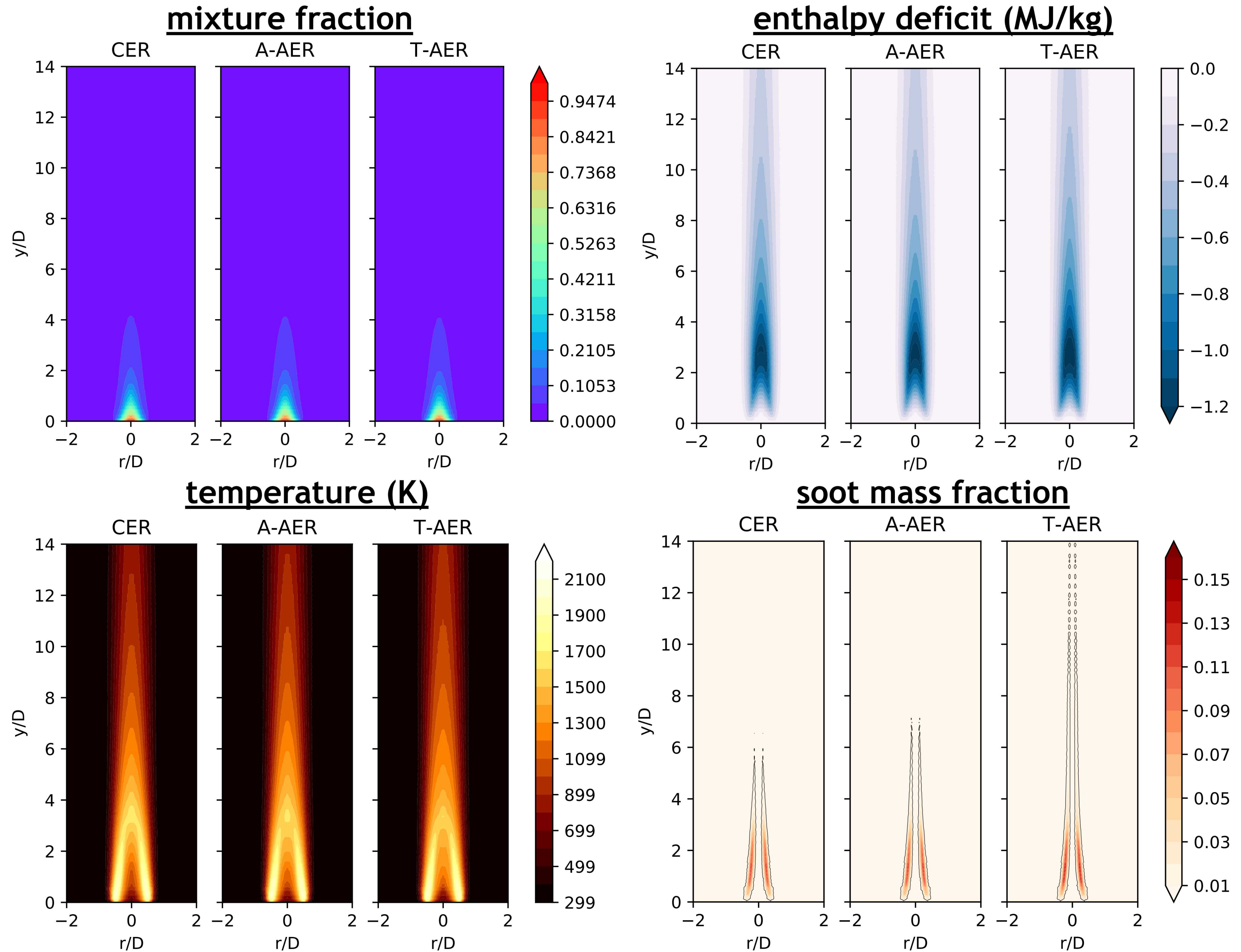
Qualitative differences are observed between the methods for a steady laminar ethylene sooting jet flame



Steady state profiles for an ethylene laminar coflow, sooting jet with 11 mm diameter (D)

Simple radiation ($4\sigma T_{\text{ref}}^4$)

- Largest qualitative difference in soot mass fraction
- T-AER has the largest areas of heat loss for a given contour

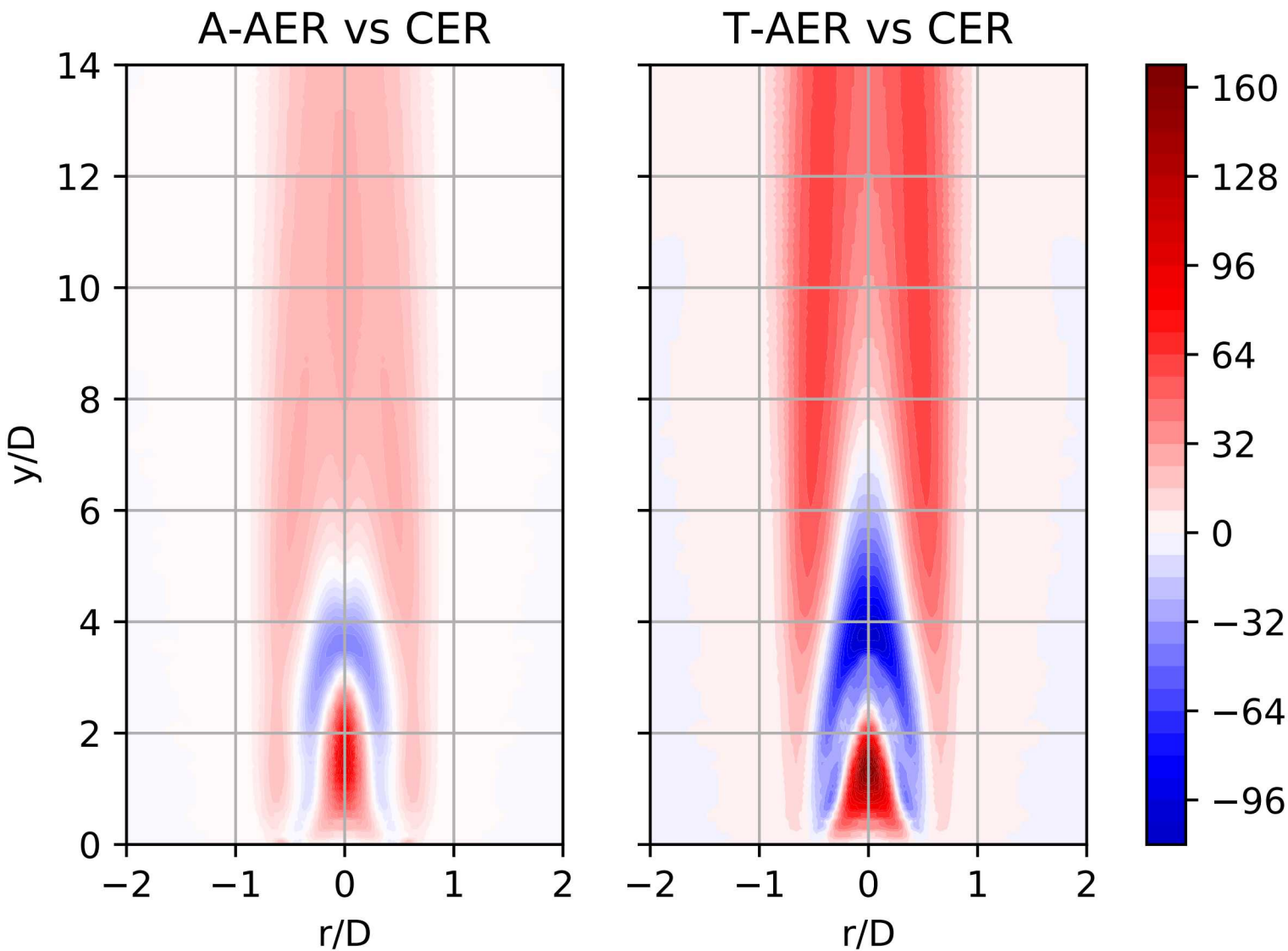


AER methods have less error in scenarios with less heat loss



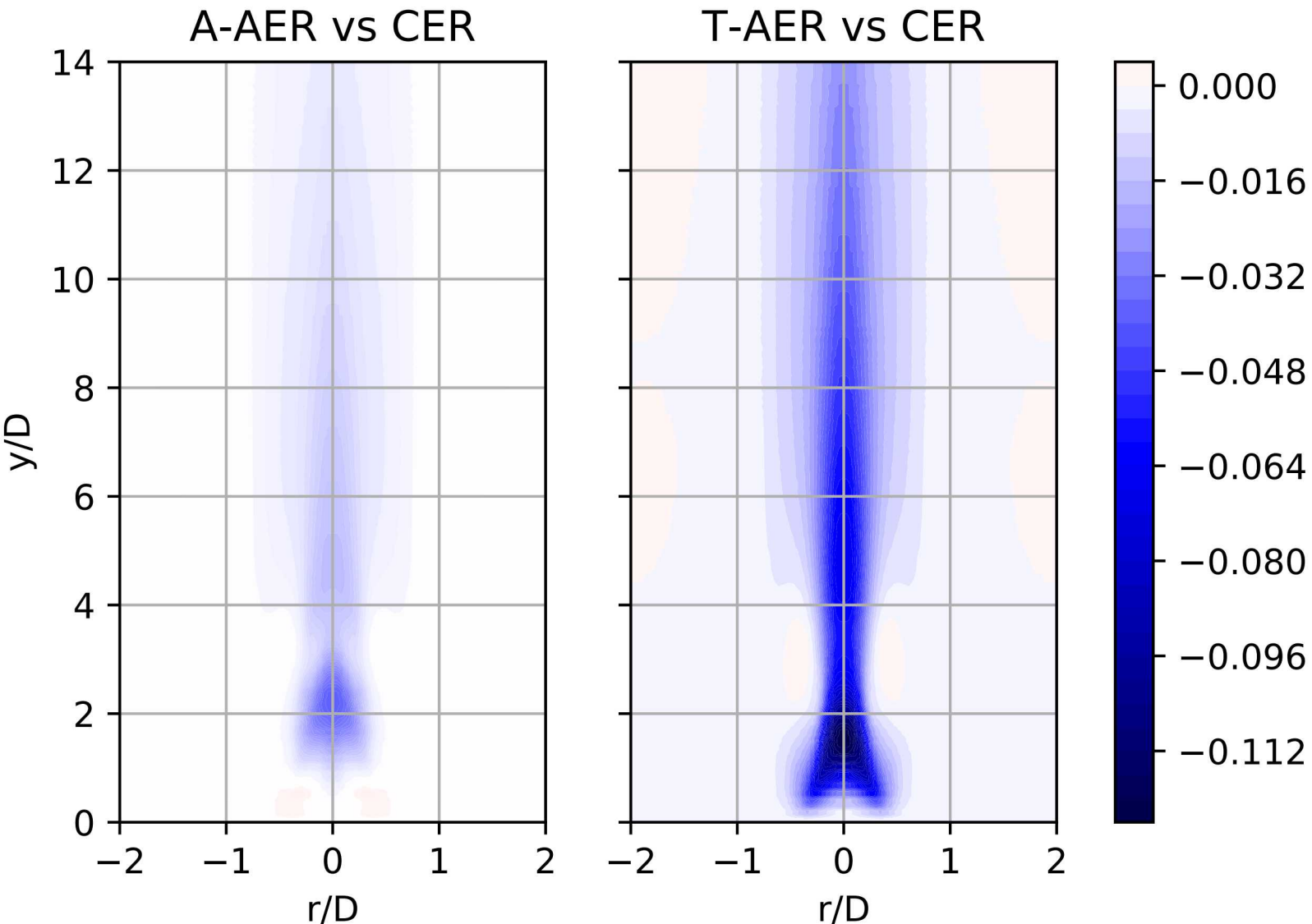
Computed from table queries

temperature error (K)

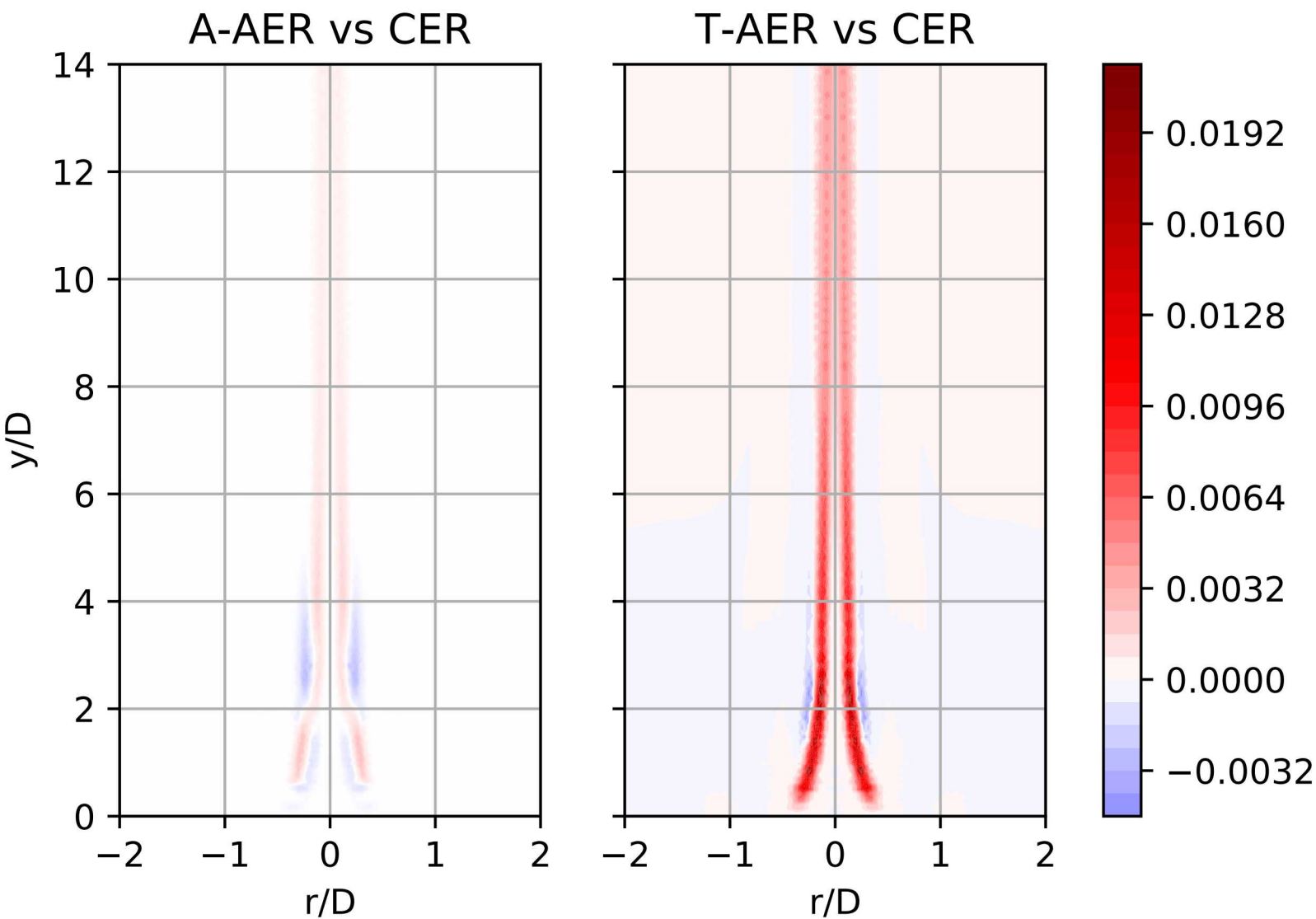


Transported in simulation

enthalpy deficit error (MJ/kg)



soot mass fraction error

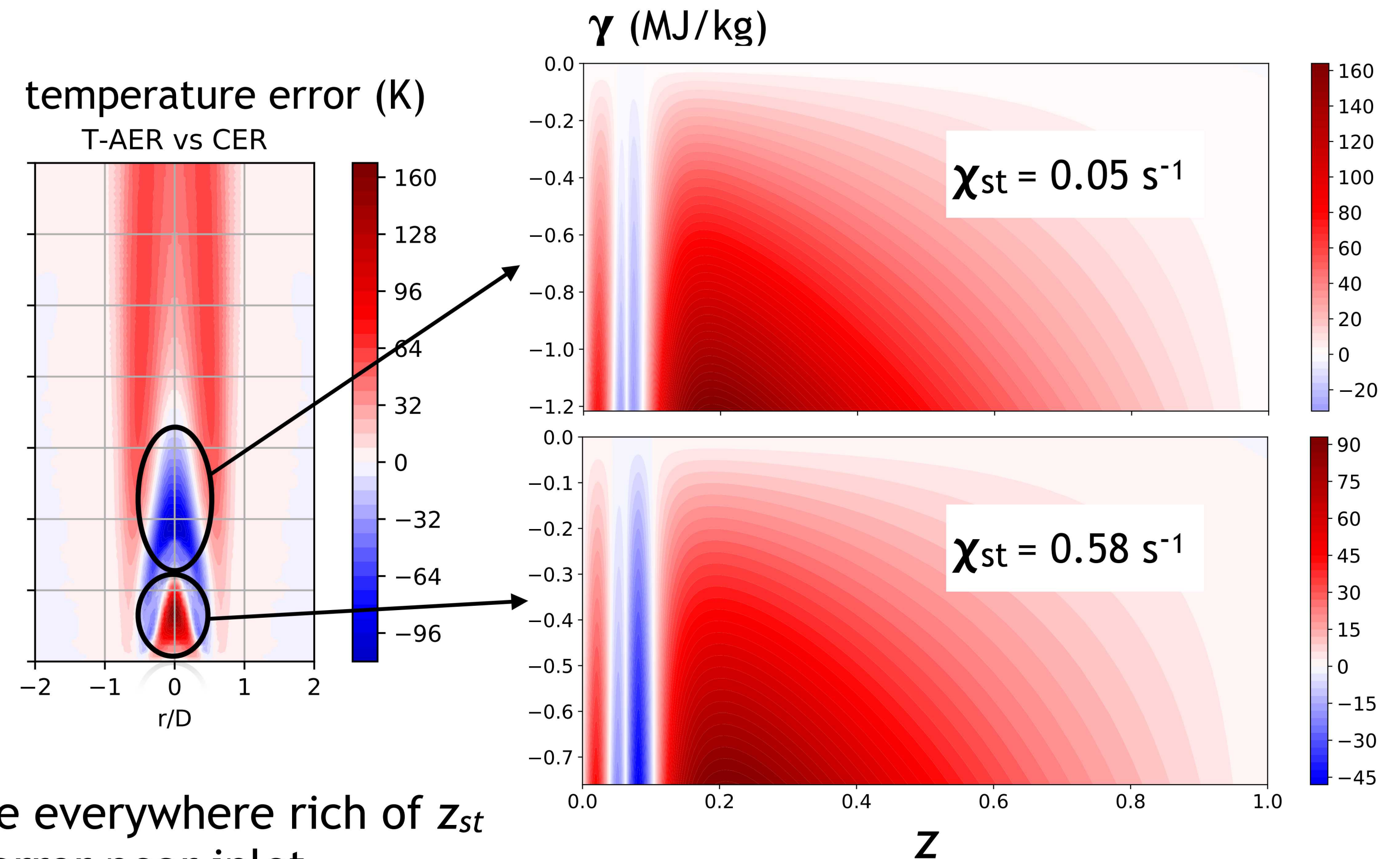


We can explain errors in the steady state profiles through *a priori* error analysis



Under-predicting temperature around z_{st}

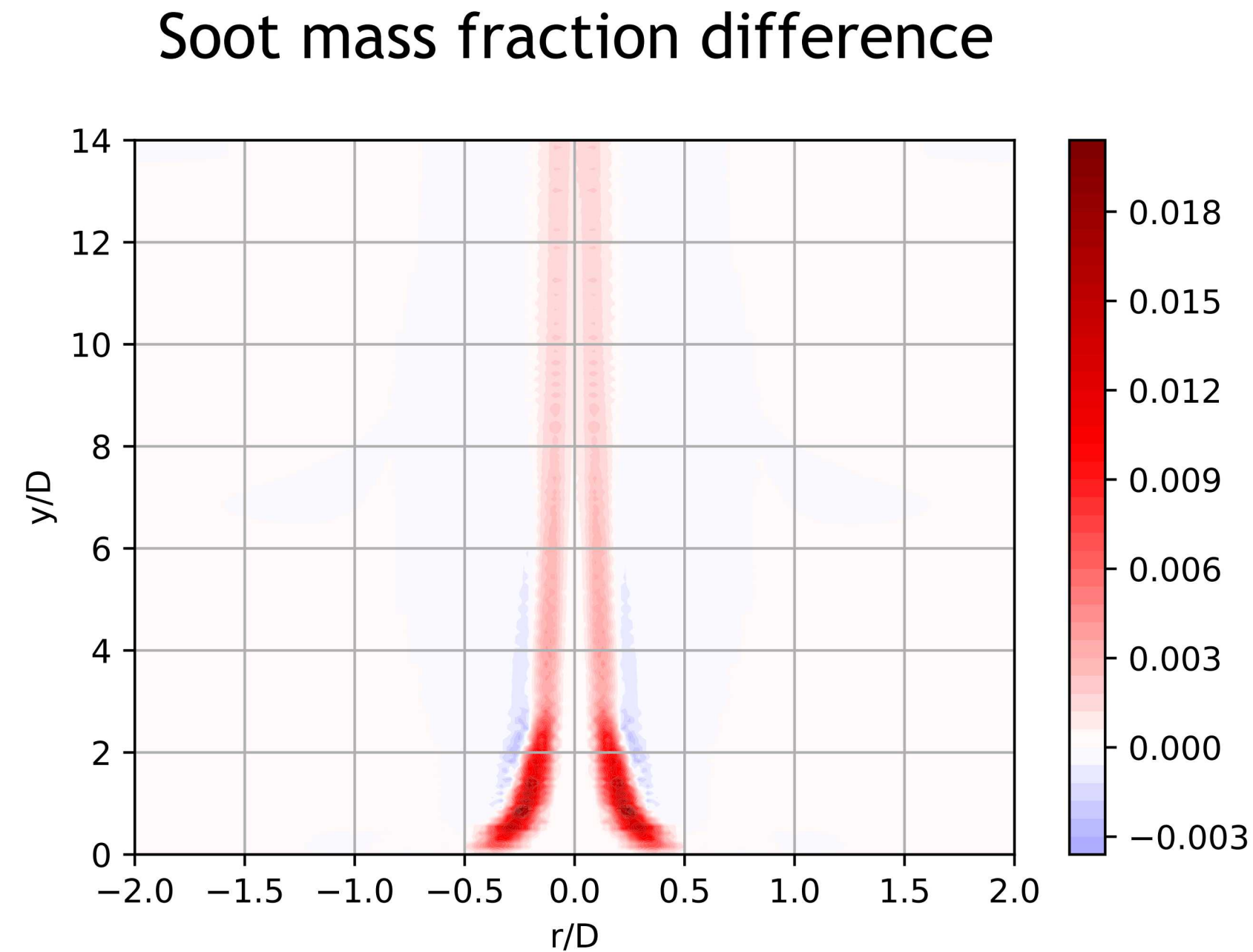
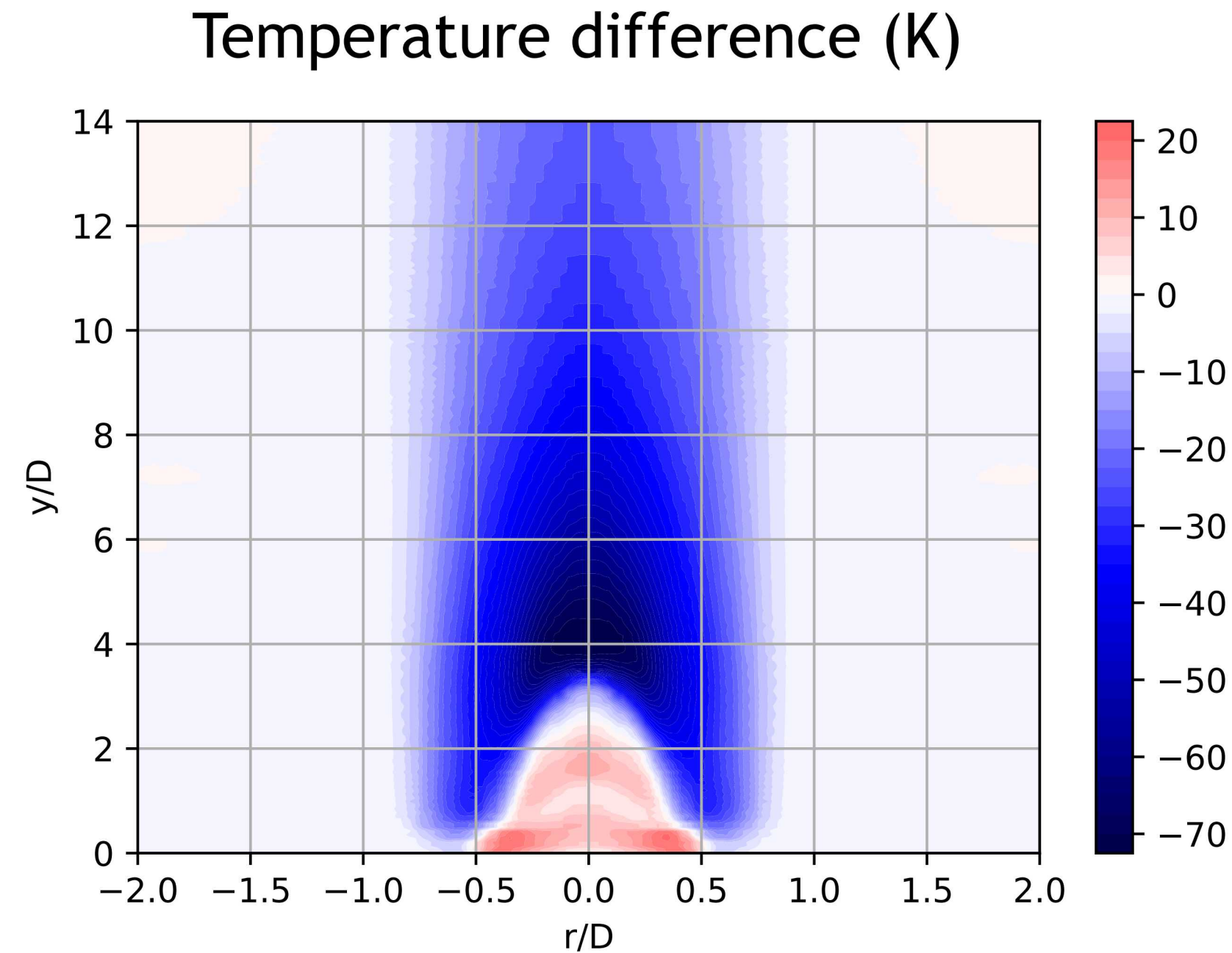
Smaller magnitude of error in this region compared to rich regions at 0.58 s^{-1}



Over-predicting temperature everywhere rich of z_{st}
Matches observations for T error near inlet

The analysis remains applicable for radiation modeled with PMR

participating media radiation (PMR) - simple radiation for CER



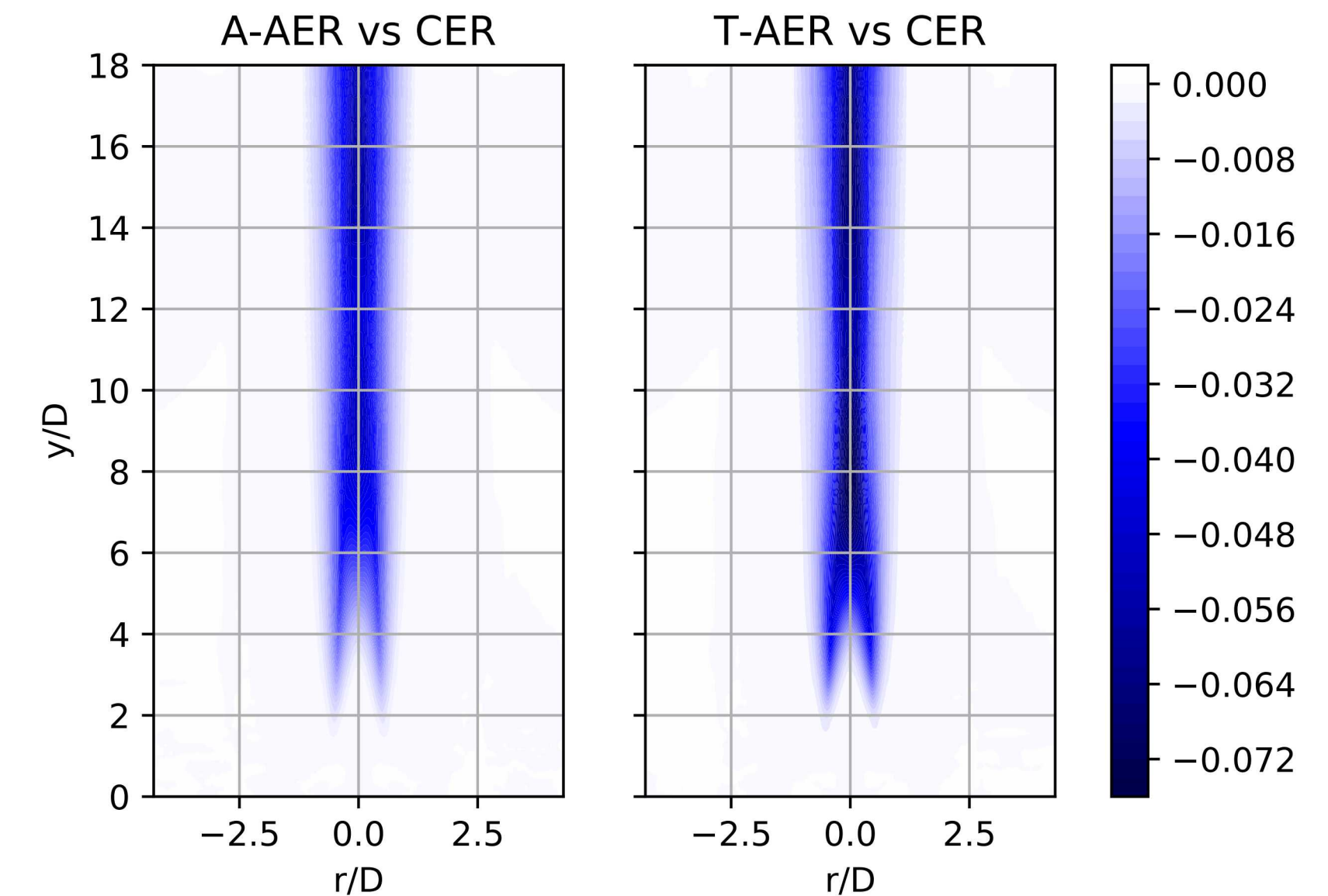
- Near the inlet, the temperature is higher for PMR than SR, which corresponds to a larger soot mass fraction
- At most a 5% difference in temperature, but an 11% higher maximum observed soot mass fraction for PMR compared to simple radiation
 - any differences in temperature can be amplified in the soot production due to sensitivities
 - soot production more coupled to PMR
- PMR changed the overall quantities of the steady state properties compared to simple radiation, but did not change the relative differences between the CER, T-AER, and A-AER

The analysis remains applicable for heptane

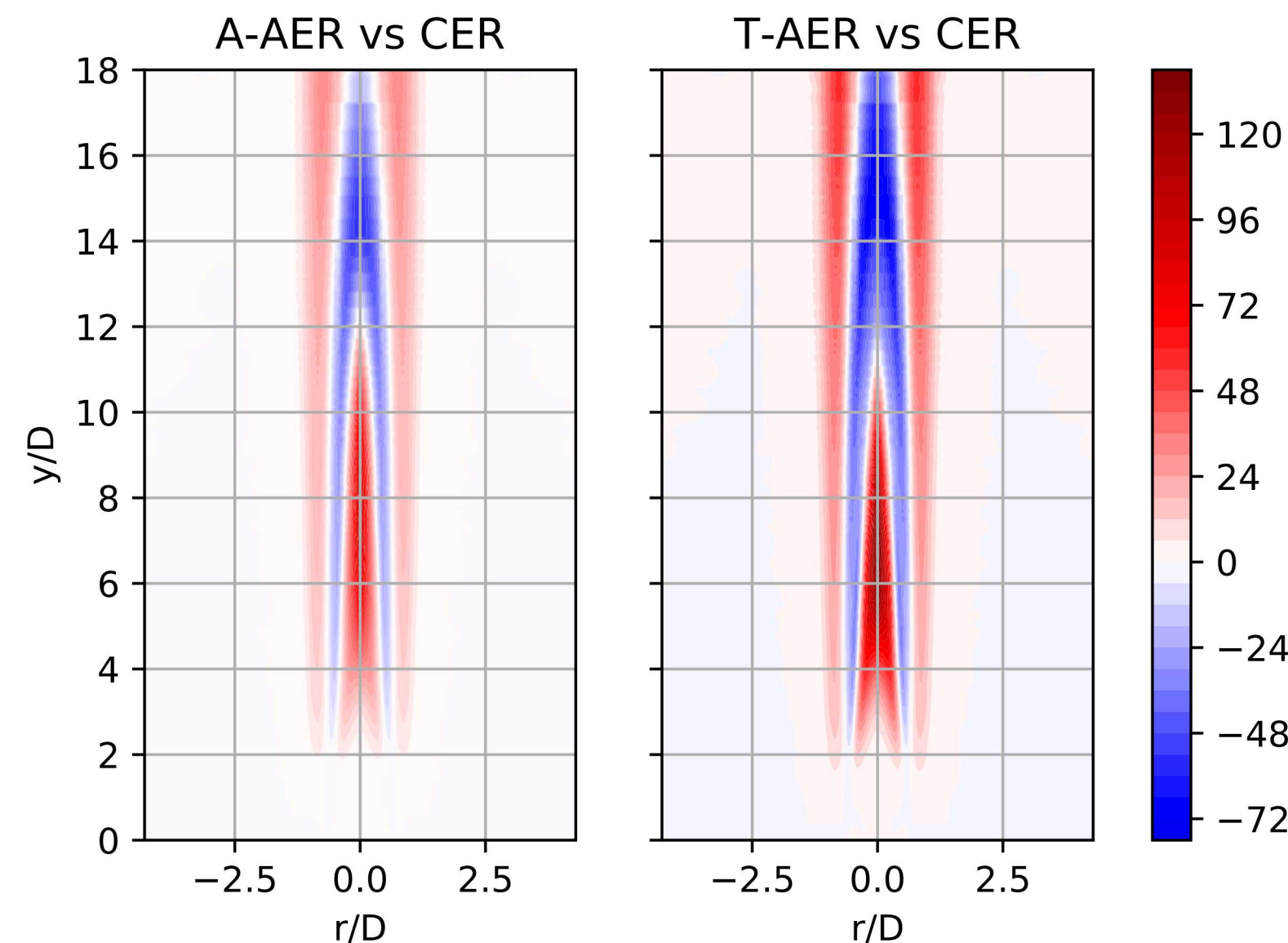


- See same trends in results as saw with ethylene
- However, with heptane there is only about a 5% over-prediction of the maximum soot mass fraction by T-AER compared to CER
- The heptane case also has less heat loss overall compared to ethylene
 - AER methods have less error in scenarios with less heat loss
 - have the benefit of being less expensive in these scenarios

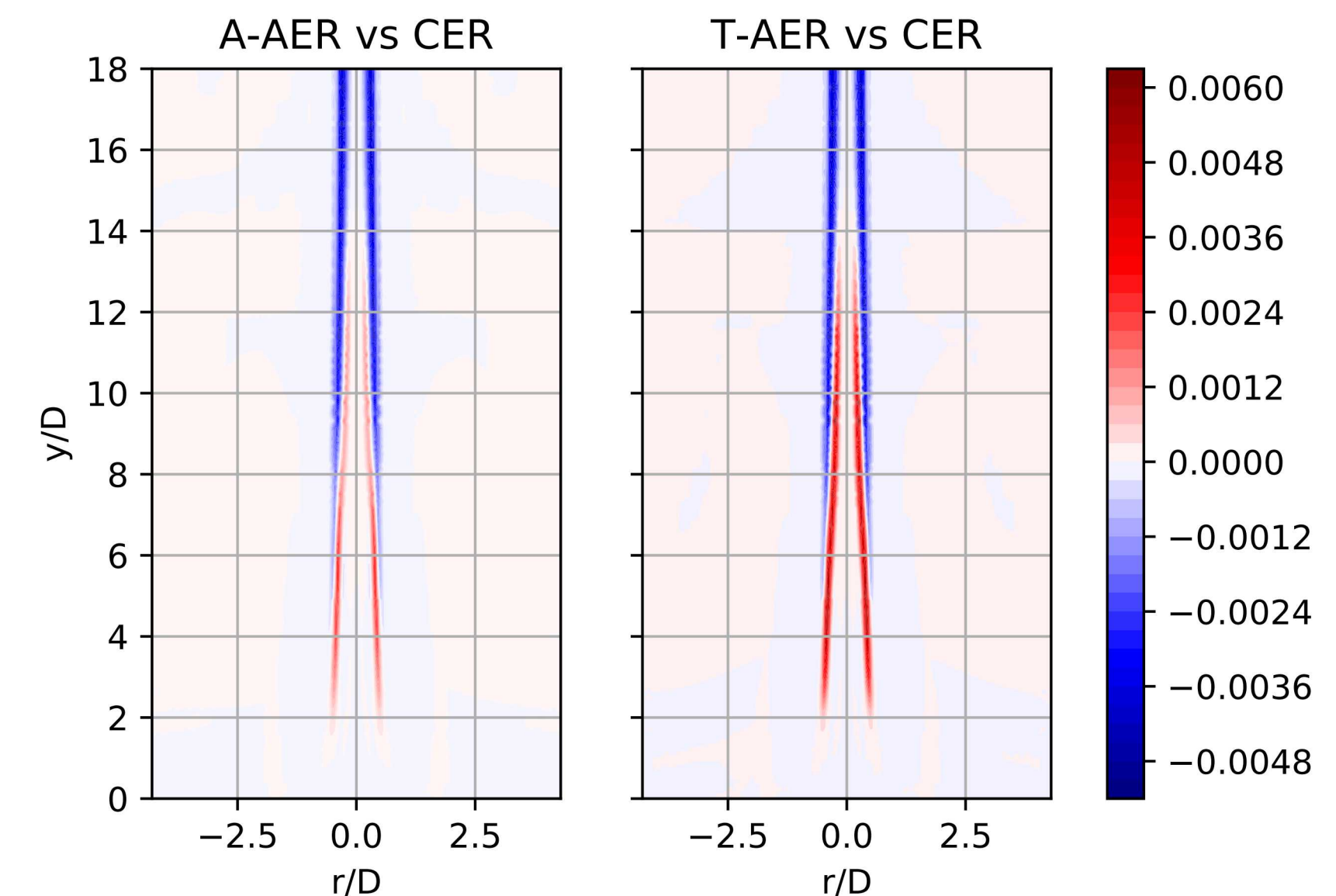
enthalpy deficit error (MJ/kg)



temperature error (K)



soot mass fraction error



The equations we solve



- Thermochemical states are typically calculated using the steady laminar flamelet model (SLFM)

$$\frac{\partial Y_i}{\partial t} = \frac{\chi}{2} \frac{\partial^2 Y_i}{\partial Z^2} + \frac{\omega_i}{\rho}$$

$$\frac{\partial T}{\partial t} = \underbrace{-\frac{1}{\rho c_p} \sum_{i=1}^n \omega_i h_i + \frac{\chi}{2} \frac{\partial^2 T}{\partial Z^2}}_{\text{classical flamelet equations}} + \underbrace{\frac{\chi}{2} \frac{1}{c_p} \frac{\partial T}{\partial Z} \frac{\partial c_p}{\partial Z}}_{\text{variable } c_p} + \underbrace{\frac{\chi}{2} \frac{\partial T}{\partial Z} \sum_{i=1}^n \frac{c_{p,i}}{c_p} \frac{\partial Y_i}{\partial Z}}_{\text{distinct } c_{p,i}}$$