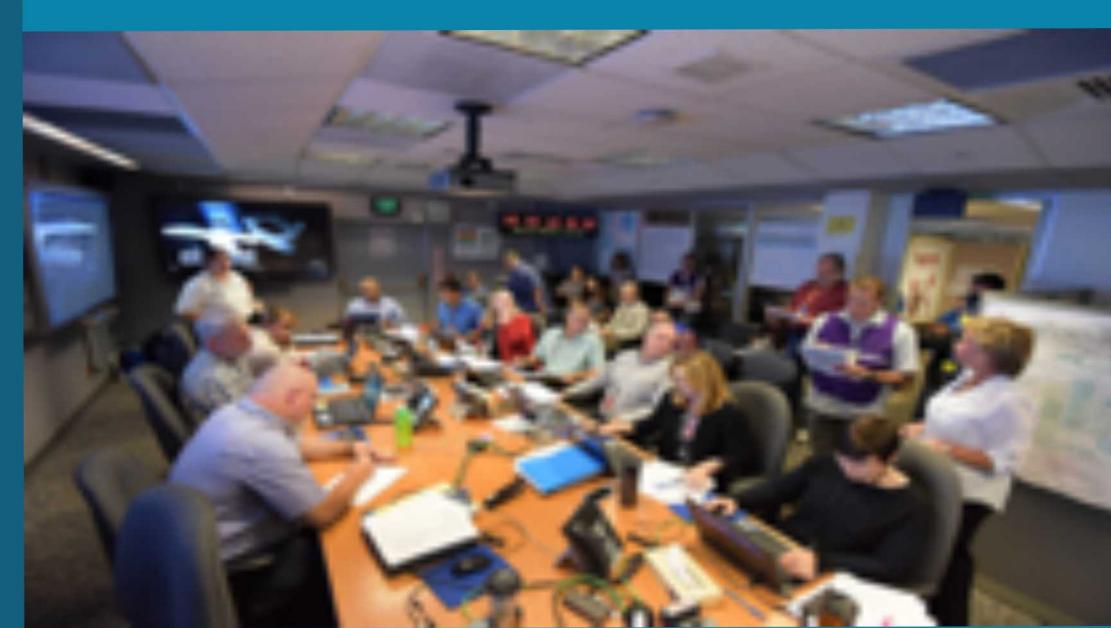
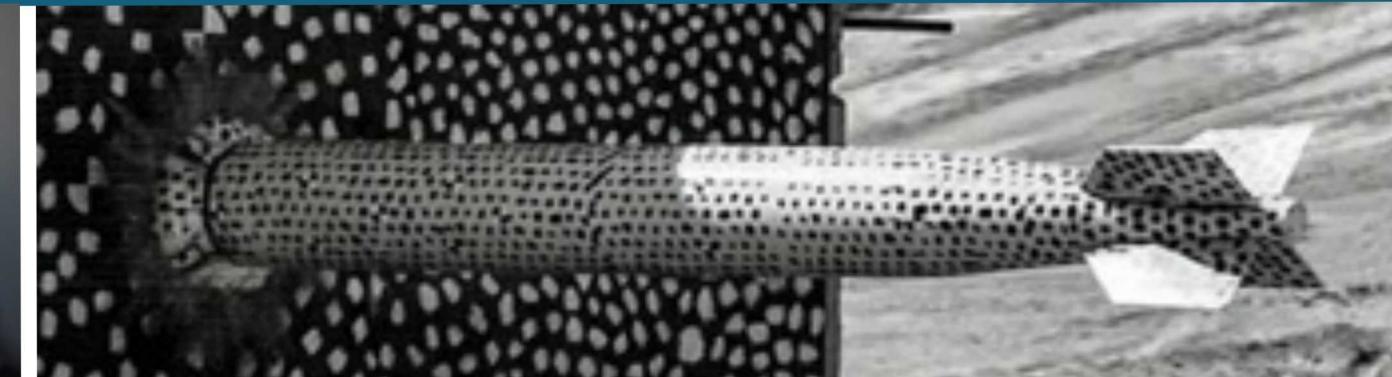
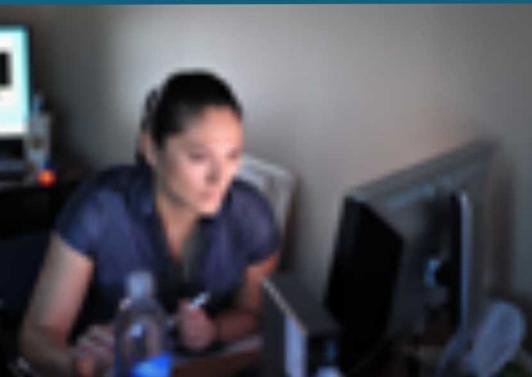


Sandia  
National  
Laboratories

# CONSTRUCTING AND ACCESSING TABULATED CHEMISTRY FOR FIRE SCENARIOS



SAND#



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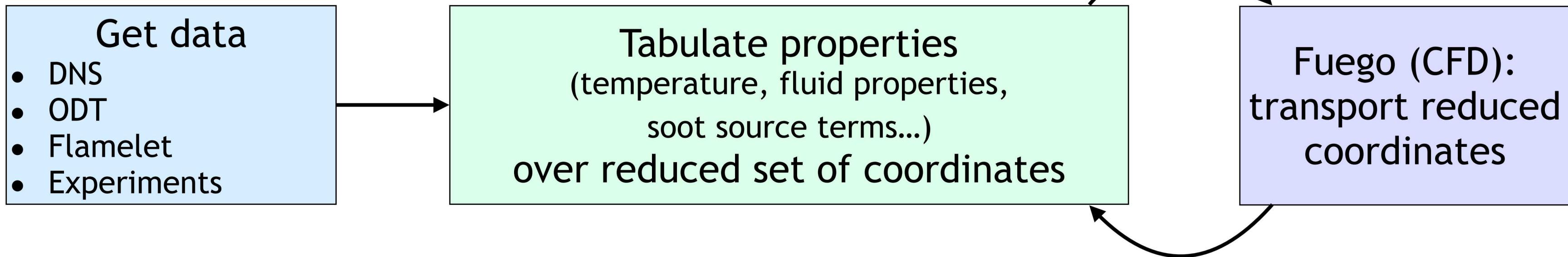
# Non-adiabatic flamelet chemistry tabulation with LES/RANS enables simulation of sooting, turbulent fires at engineering scales of interest



SIERRA/Fuego

- Tabulation techniques aid in making fire simulations computationally feasible
- We were seeing over-predictions in soot and unstable simulations in some cases...
- Want to explore different ways of constructing/accessing chemistry tables

## How chemistry tabulation works:



## Options for the reduced set of coordinates: (for strongly sooting and radiating fires)

1 dimension: mixture fraction ( $z$ )

Equilibrium, Burke-Schumann

*composition*

2 dimensions:  $z$ , scalar dissipation rate ( $\chi$ )

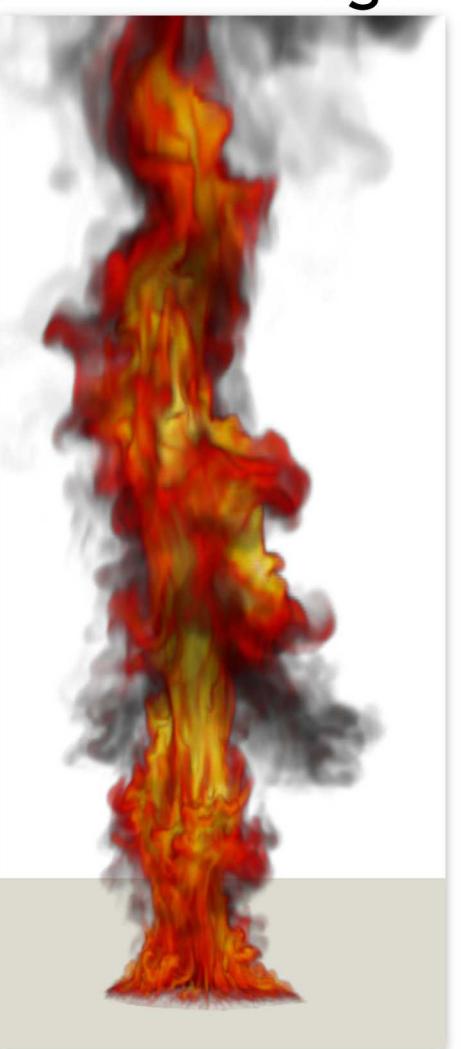
Steady Laminar Flamelet Model (SLFM)

*composition, strain*

*composition, strain, heat loss*

3 dimensions:  $z$ ,  $\chi$ , enthalpy ( $h$ ) or enthalpy deficit ( $\gamma = h - h_{ad}$ )

Non-adiabatic Flamelet Model



SNL's Thermal  
Test Complex



# Non-adiabatic flamelet chemistry tabulation with LES/RANS enables simulation of sooting, turbulent fires at engineering scales of interest



Options for the reduced set of coordinates: (for strongly sooting and radiating fires)

1 dimension: mixture fraction ( $z$ )  
Equilibrium, Burke-Schumann

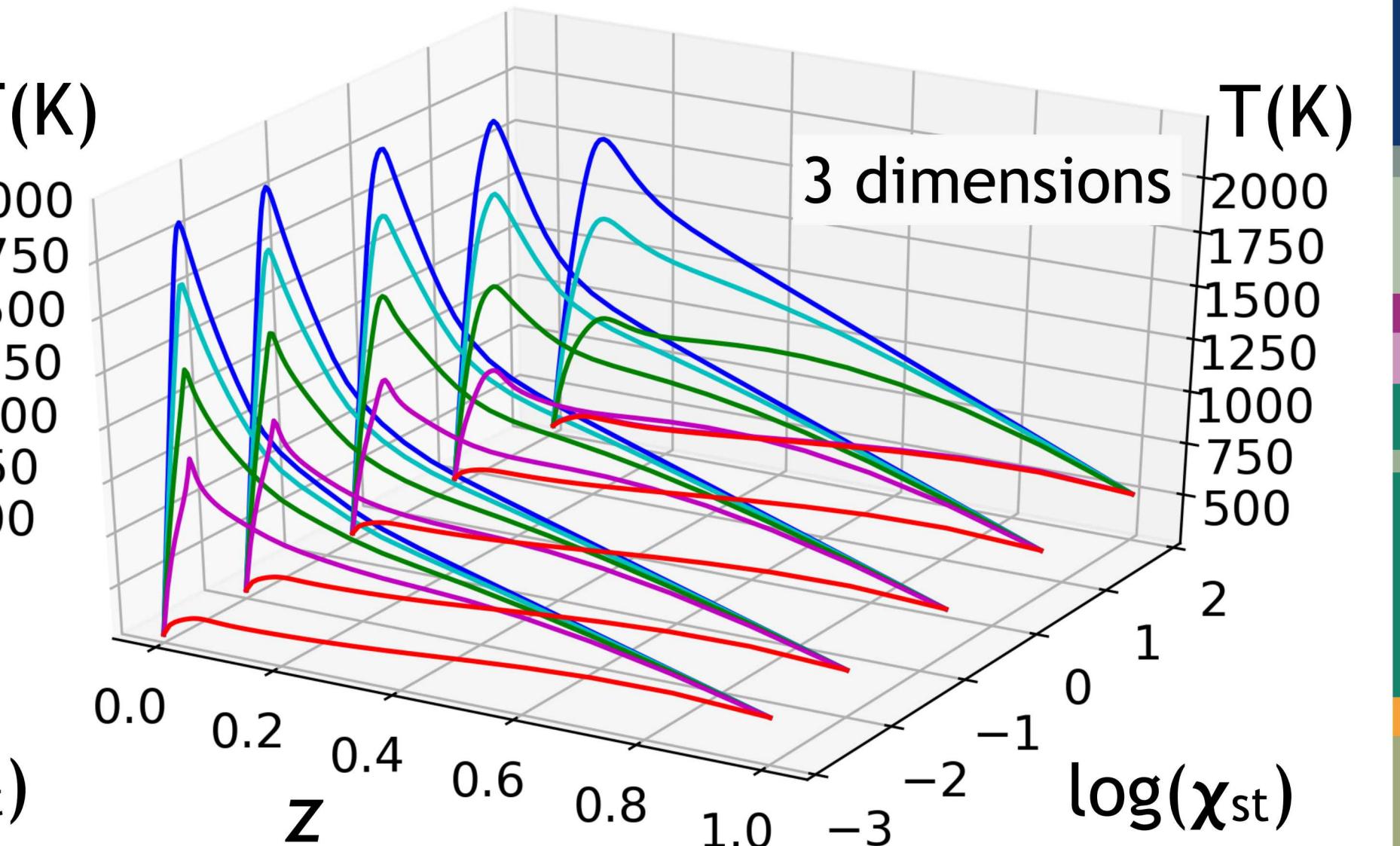
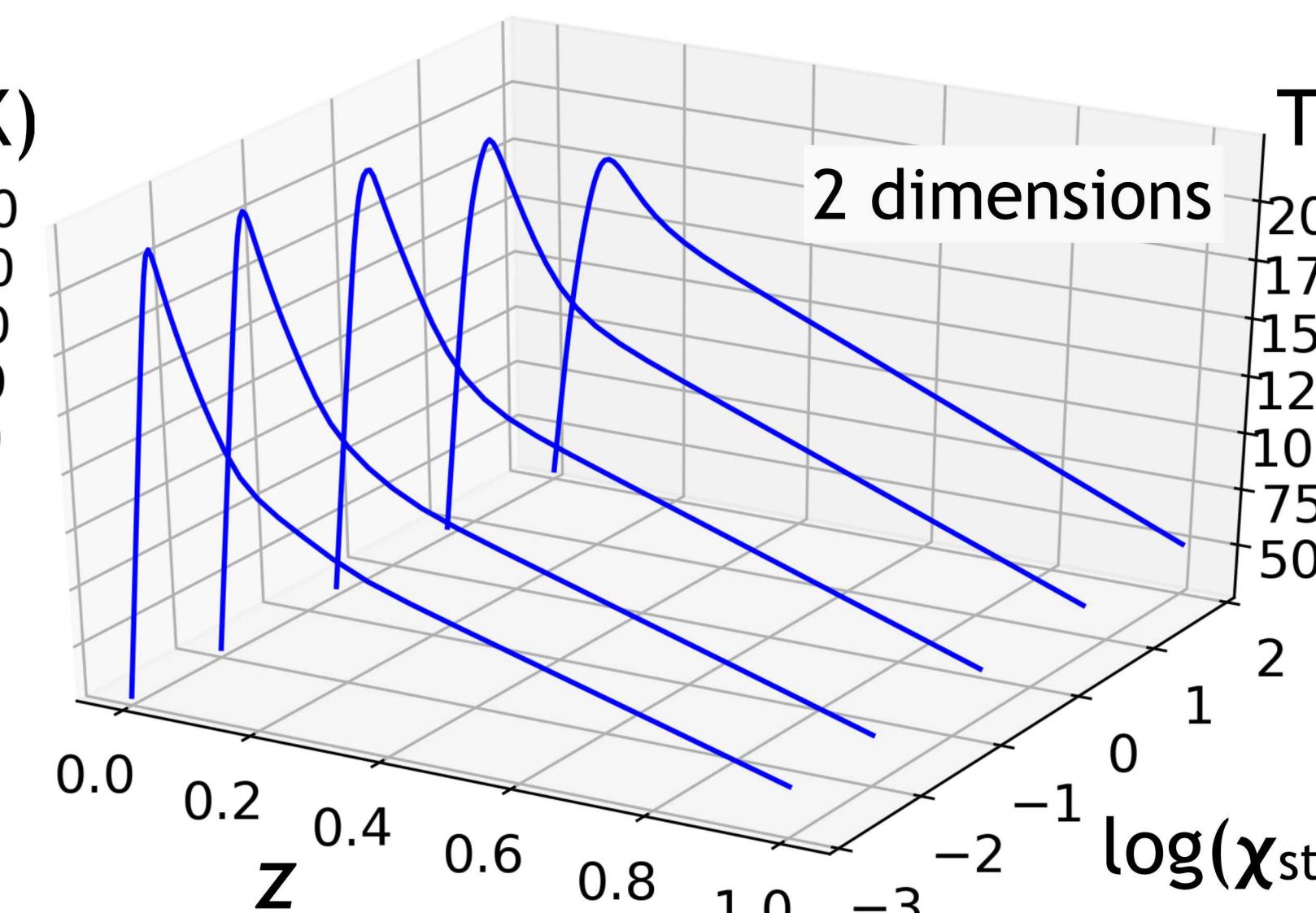
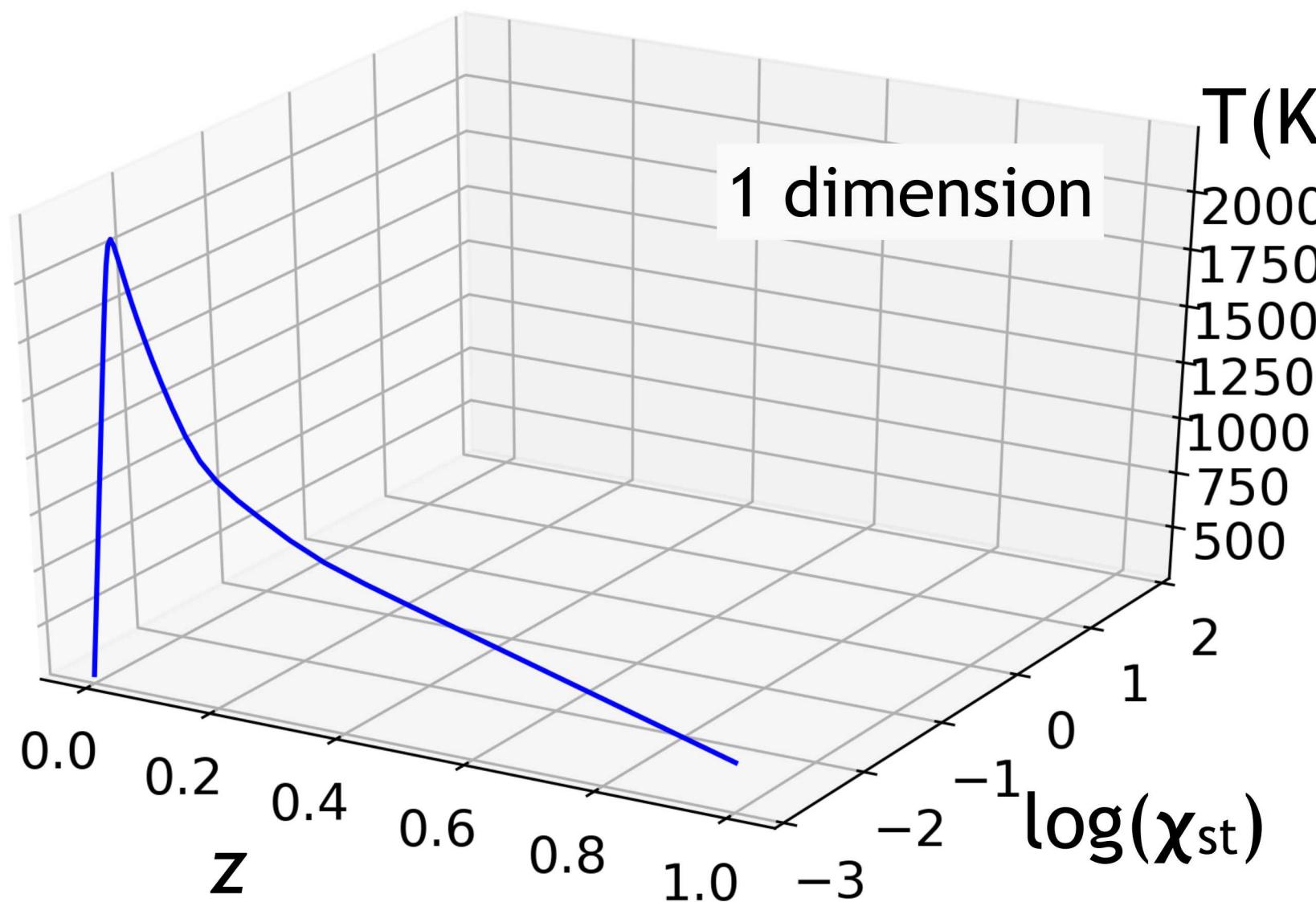
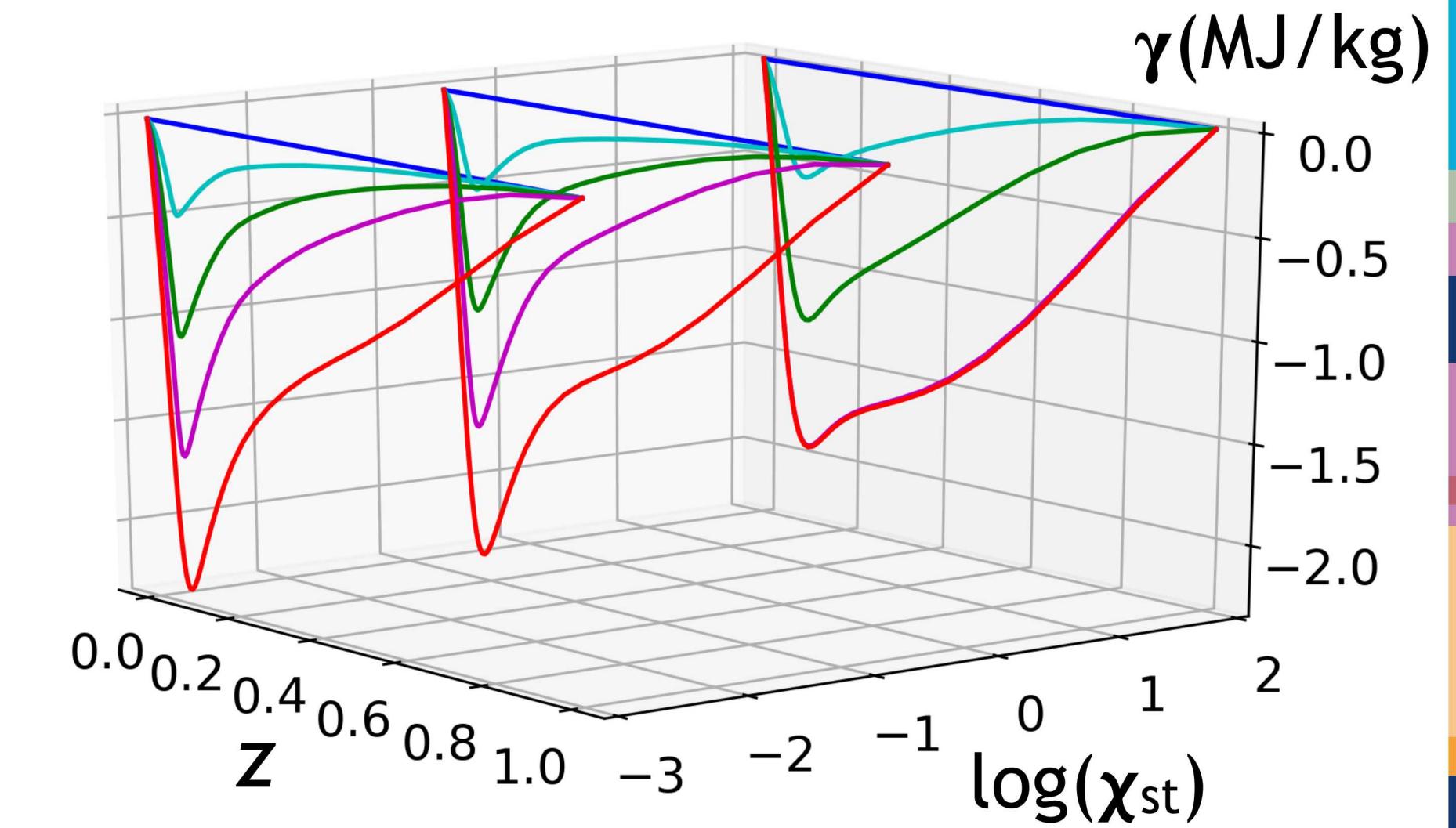
2 dimensions:  $z$ , scalar dissipation rate ( $\chi$ )  
Steady Laminar Flamelet Model (SLFM)

3 dimensions:  $z$ ,  $\chi$ , enthalpy deficit ( $\gamma = h - h_{ad}$ )  
Non-adiabatic Flamelet Model

*composition*

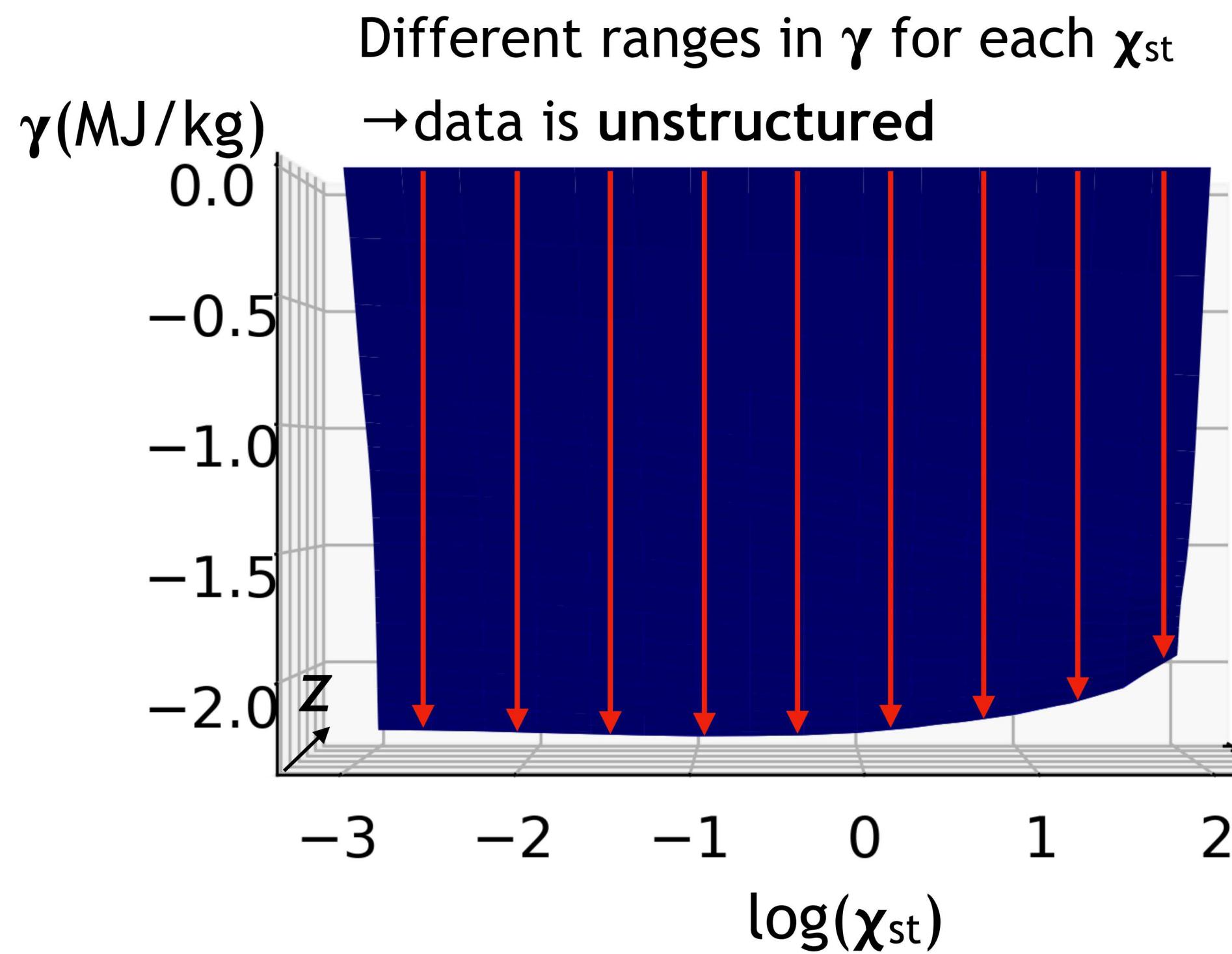
*composition, strain*

*composition, strain, heat loss*



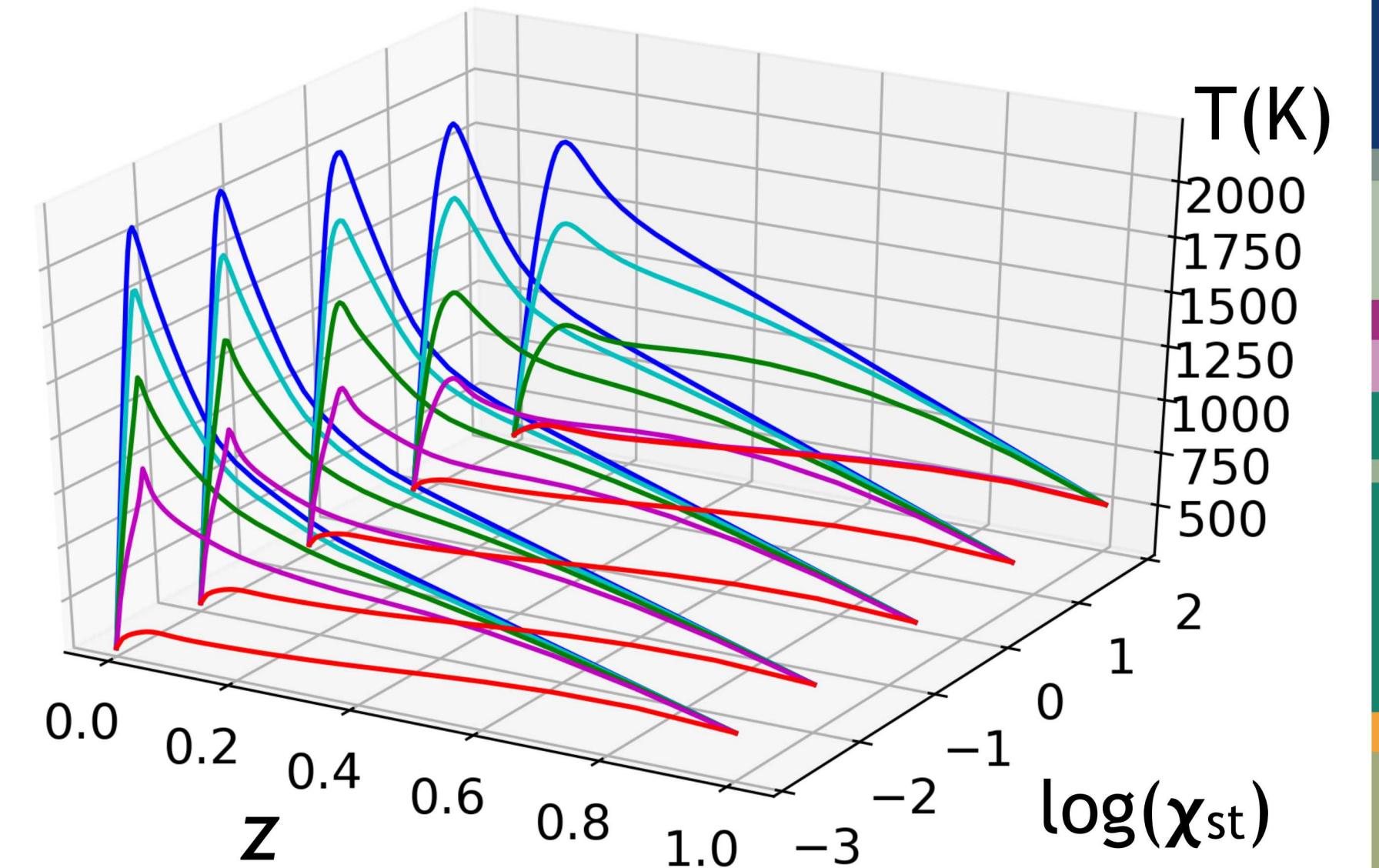
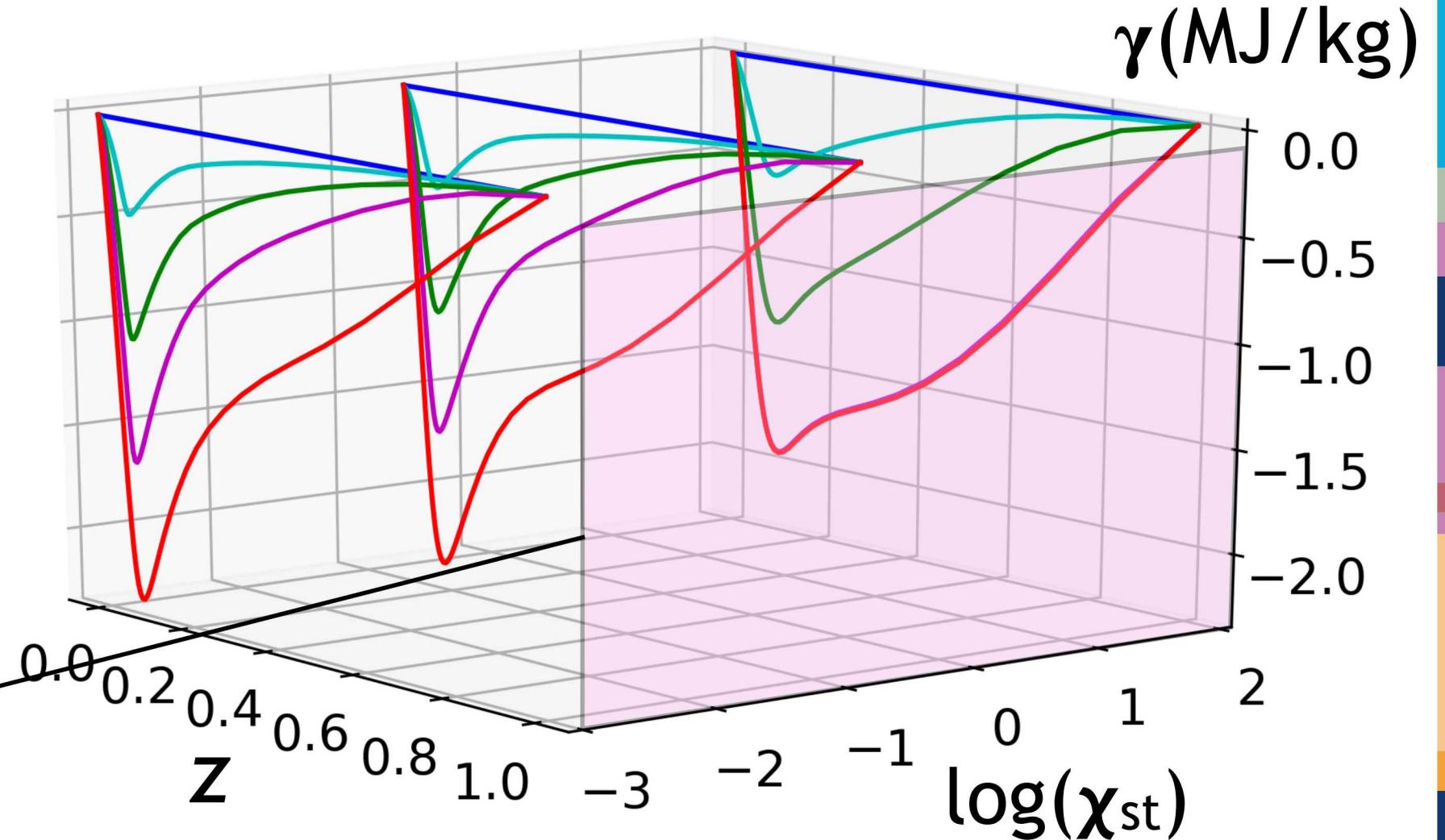
Unstructured non-adiabatic  
flamelet data over  $(z, \chi, \gamma)$

Interpolation onto structured grid (for speed)

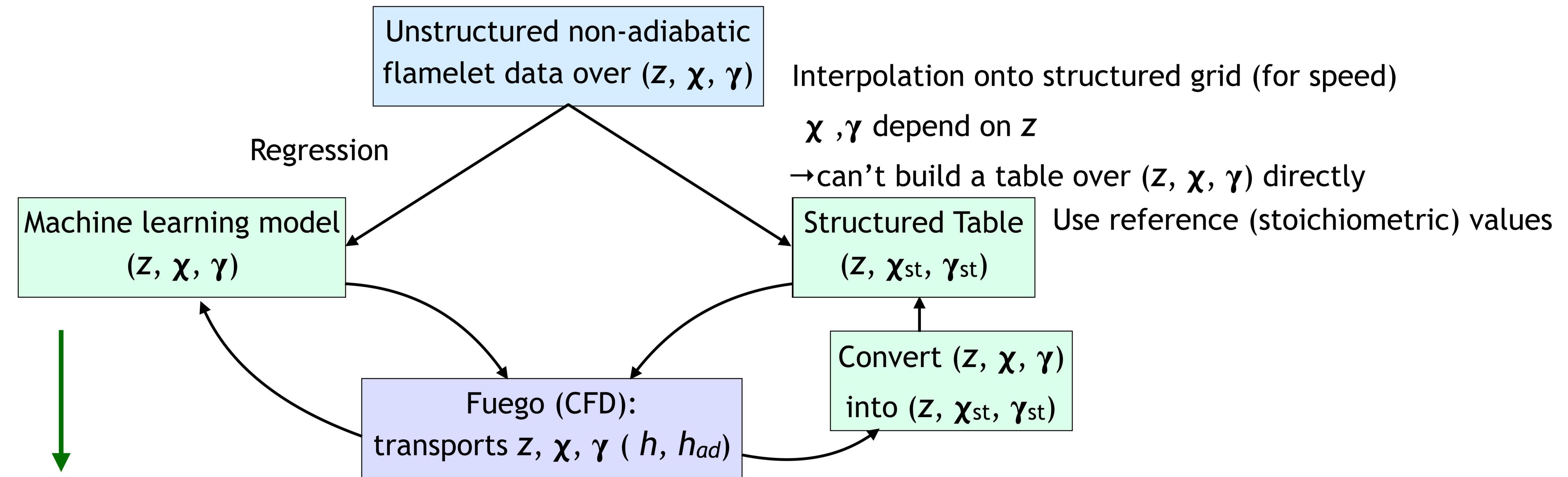


Structured Table

Viewing  
this plane



# There are challenges in constructing and accessing tabulated/modeled chemistry



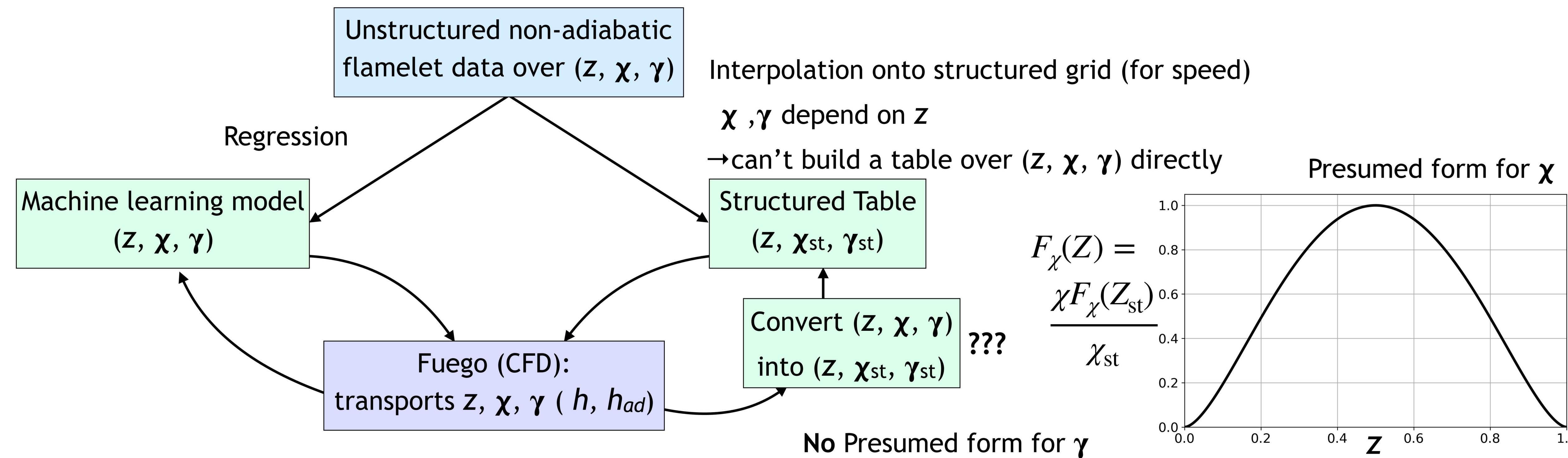
## Advantages:

- Simulation variables are the model inputs
- Smaller memory requirements
- Higher dimensional models

## Disadvantages:

- Challenges associated with finding “optimal” networks
- Difficult to determine error bounds
- More expensive to query a neural network than interpolant

# There are challenges in constructing and accessing tabulated/modeled chemistry

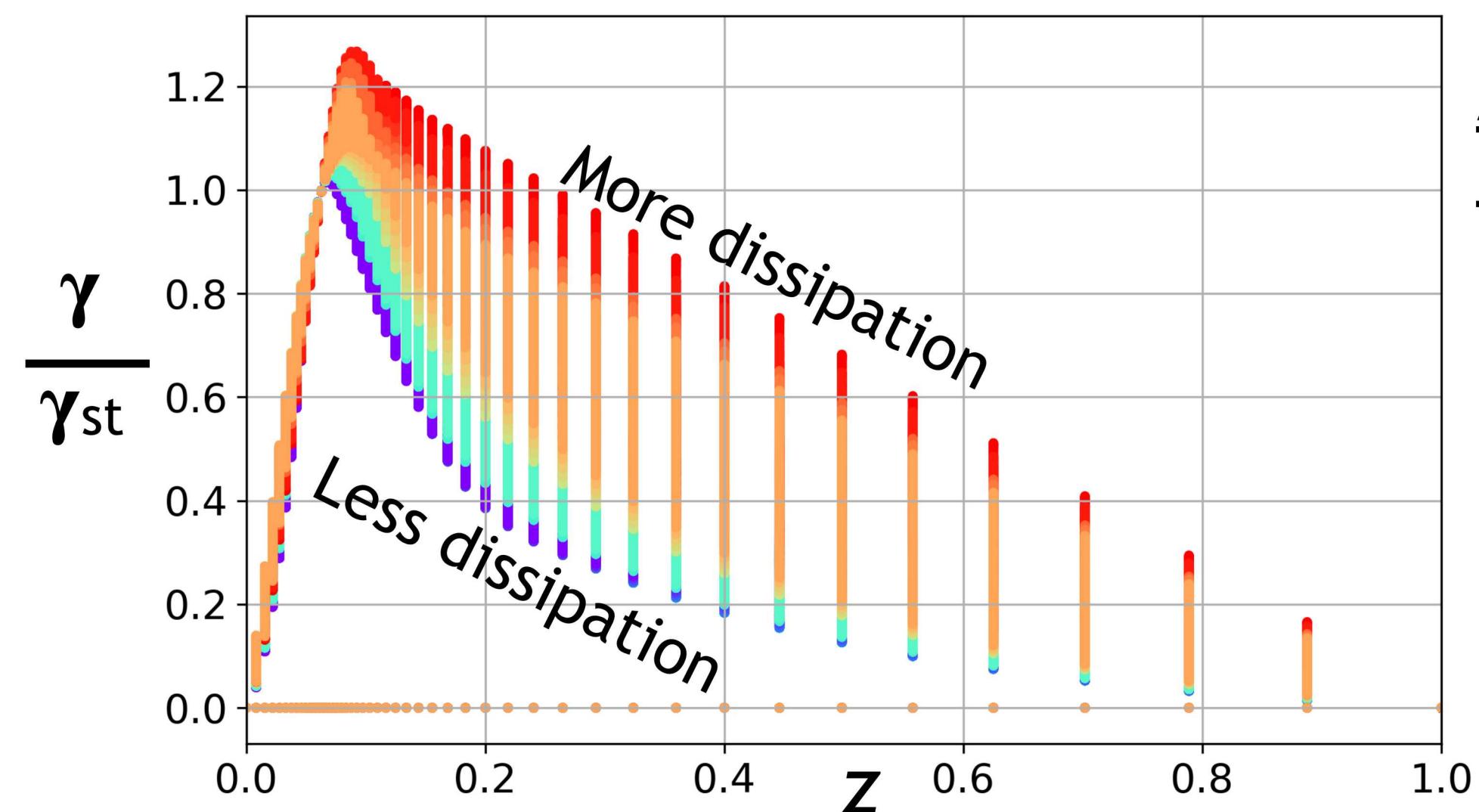


## Consistent Enthalpy Reconstruction (CER)

- Find the correct  $\gamma_{st}$  in the table using a (Newton-based) root finding method

$$\gamma_{table}(Z, \chi_{st}, \gamma_{st}) = \gamma_{CFD}$$

- Requires have  $\gamma$  in the property table
- More accurate
- More expensive

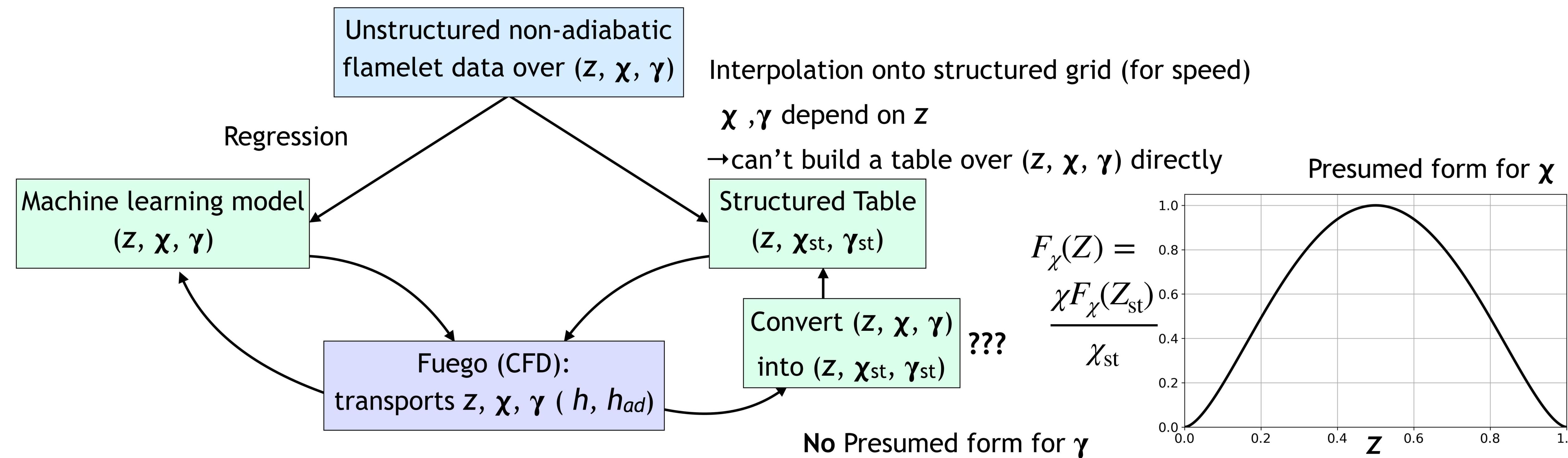


## Approximate Enthalpy Reconstruction (AER)

Presume a functional form for  $\gamma(z; \gamma_{st})$

$$\gamma = F_\gamma(Z) \gamma_{st}$$

# There are challenges in constructing and accessing tabulated/modeled chemistry

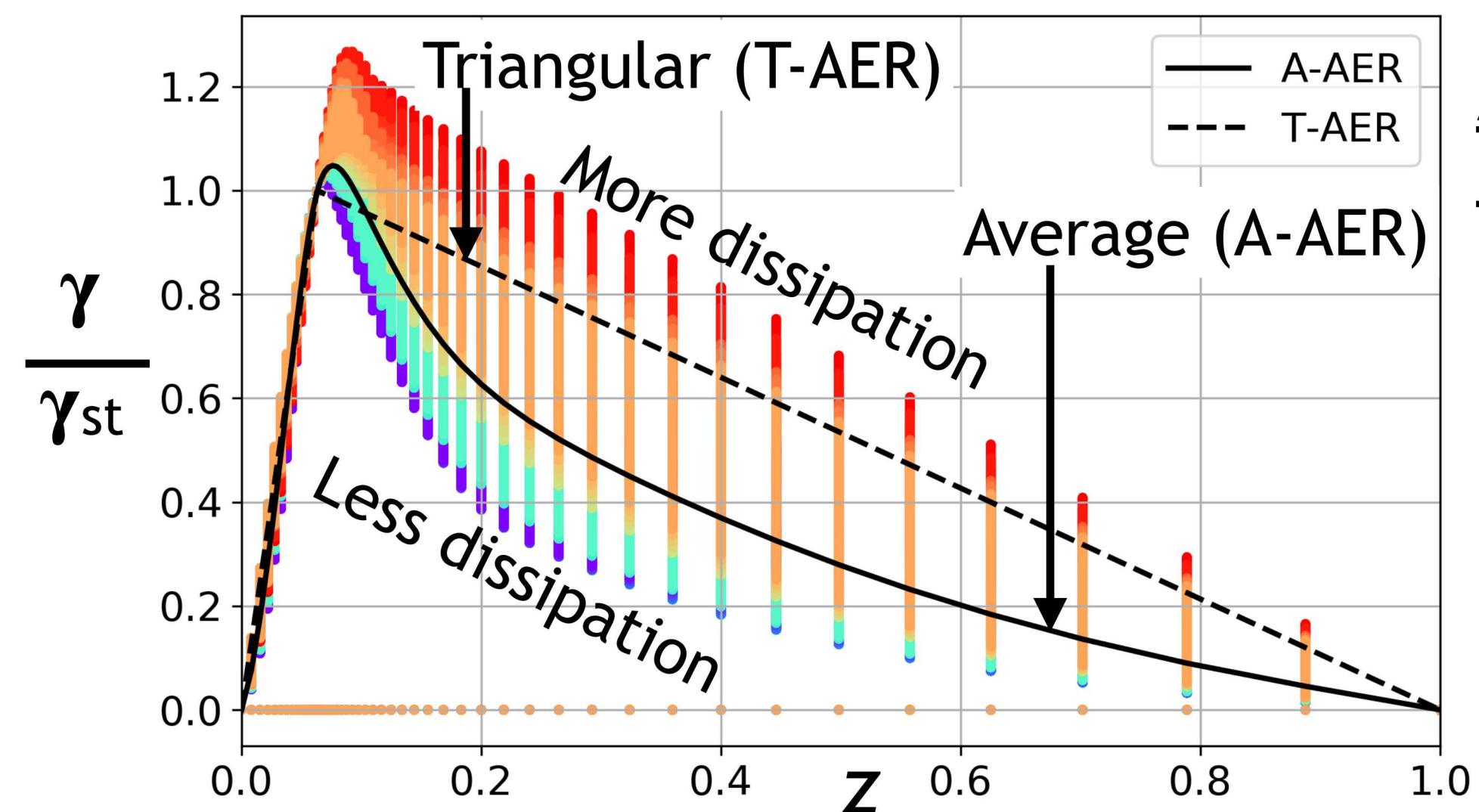


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## Approximate Enthalpy Reconstruction (AER)

Presume a functional form for  $\gamma(z; \gamma_{st})$

$$\gamma = F_\gamma(Z) \gamma_{st}$$

# The AER methods lead to substantial errors in scenarios with high heat loss



Ethylene laminar coflow, sooting jet steady state

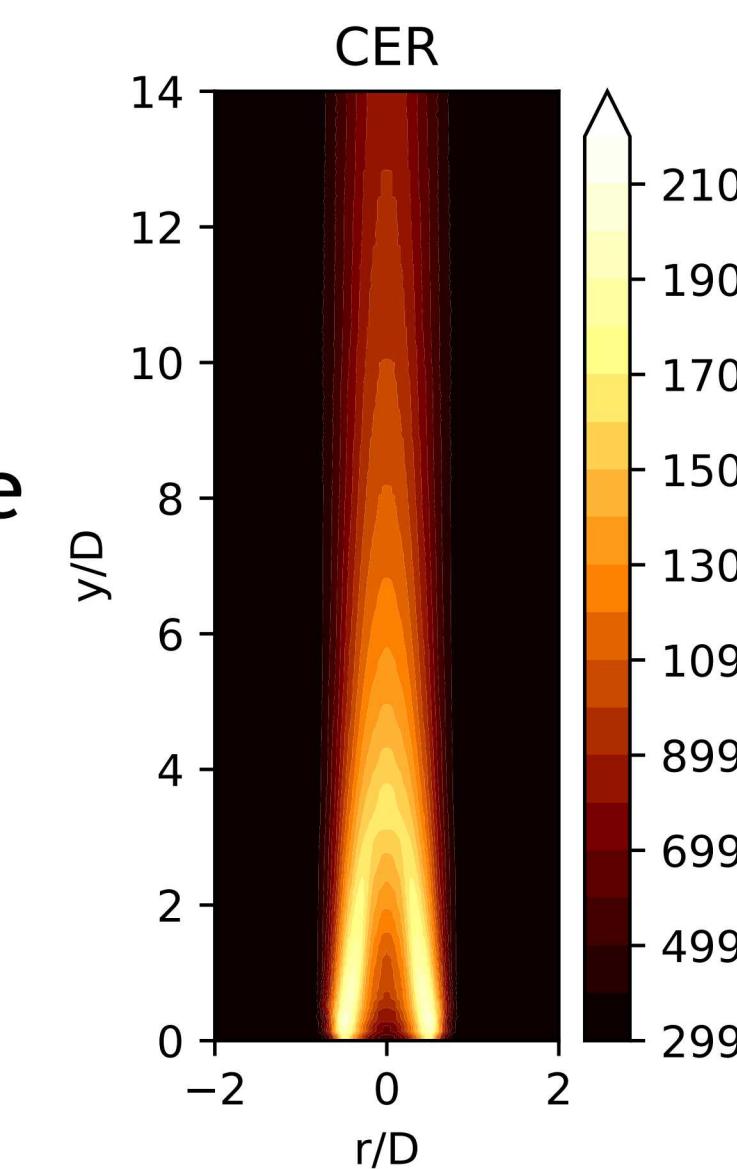
11 mm diameter (D) jet

Simple radiation model ( $4\sigma T_{\text{ref}}^4$ )

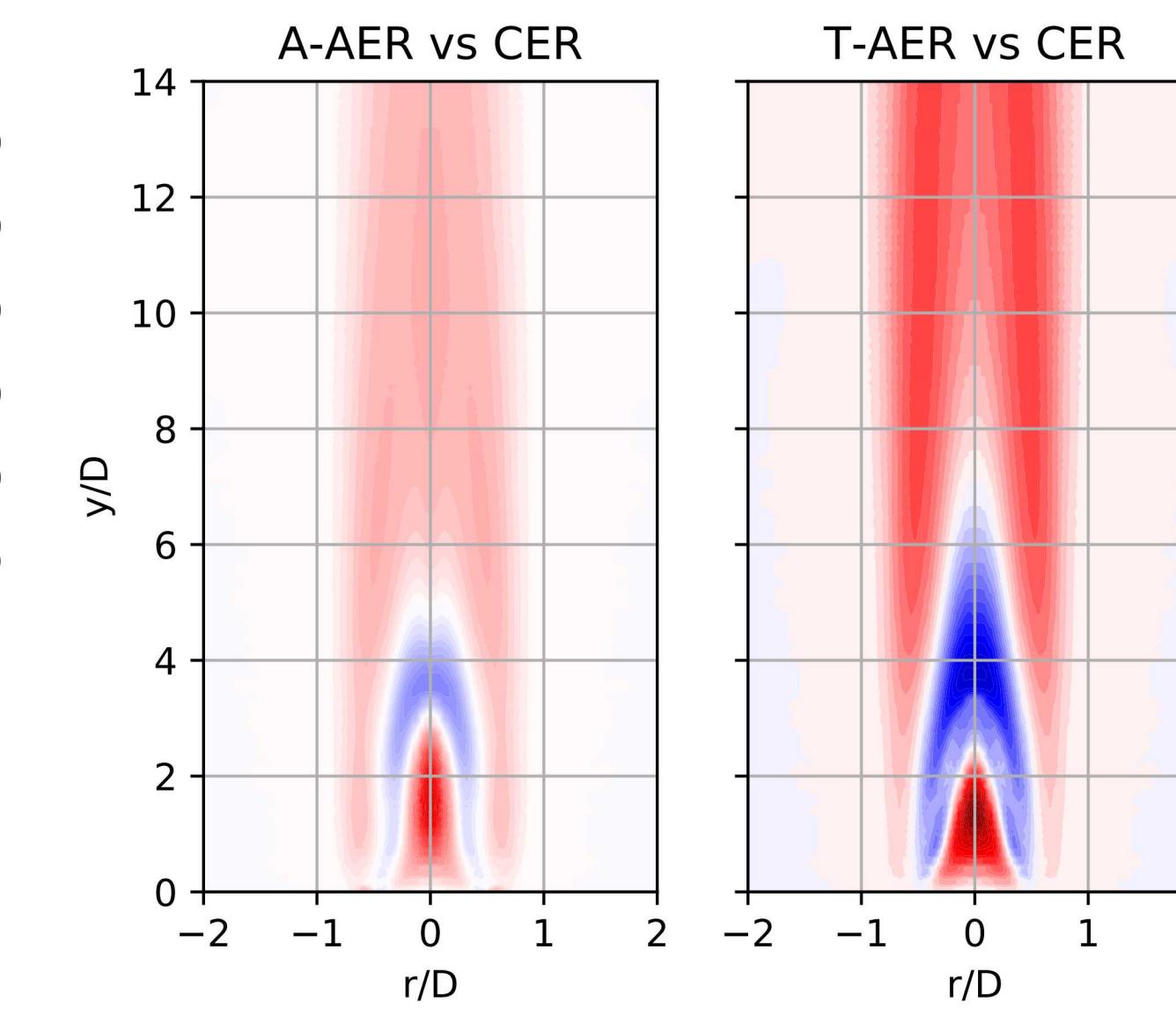
2-equation soot model

- Non-linear trend in temperature errors moving up centerline
  - Largest errors in rich regions near inlet,  $O(100 \text{ K})$
- Persistent errors (errors remain in steady state)
- 10% over-prediction in soot for T-AER than CER
  - Emitting more smoke
  - 2% over-prediction in soot for A-AER than CER
- Overall less error in A-AER method compared to T-AER
- Little to no errors in pure streams and near adiabatic
- Observed similar trends in the errors for heptane and for a participating media radiation model
- The CER simulation was 2x slower than the T-AER simulation
  - Currently performing Newton solve for every property table
  - Optimal redesign should result in only 5-10% more time for CER

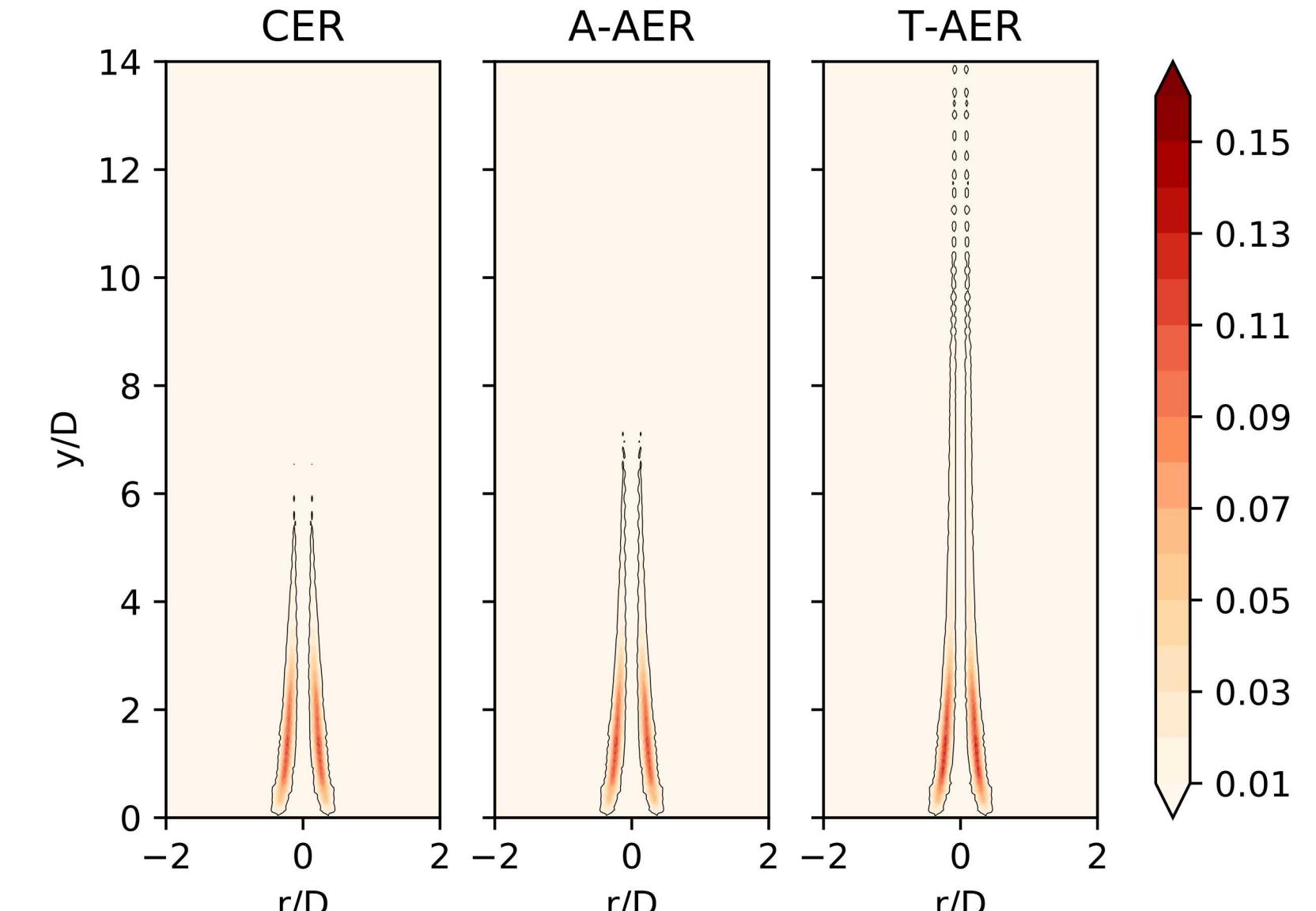
temperature (K)



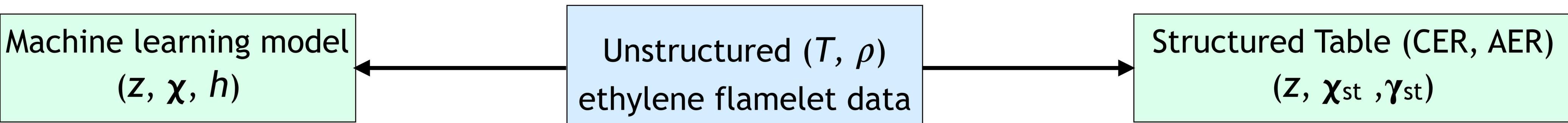
temperature error (K)



soot mass fraction

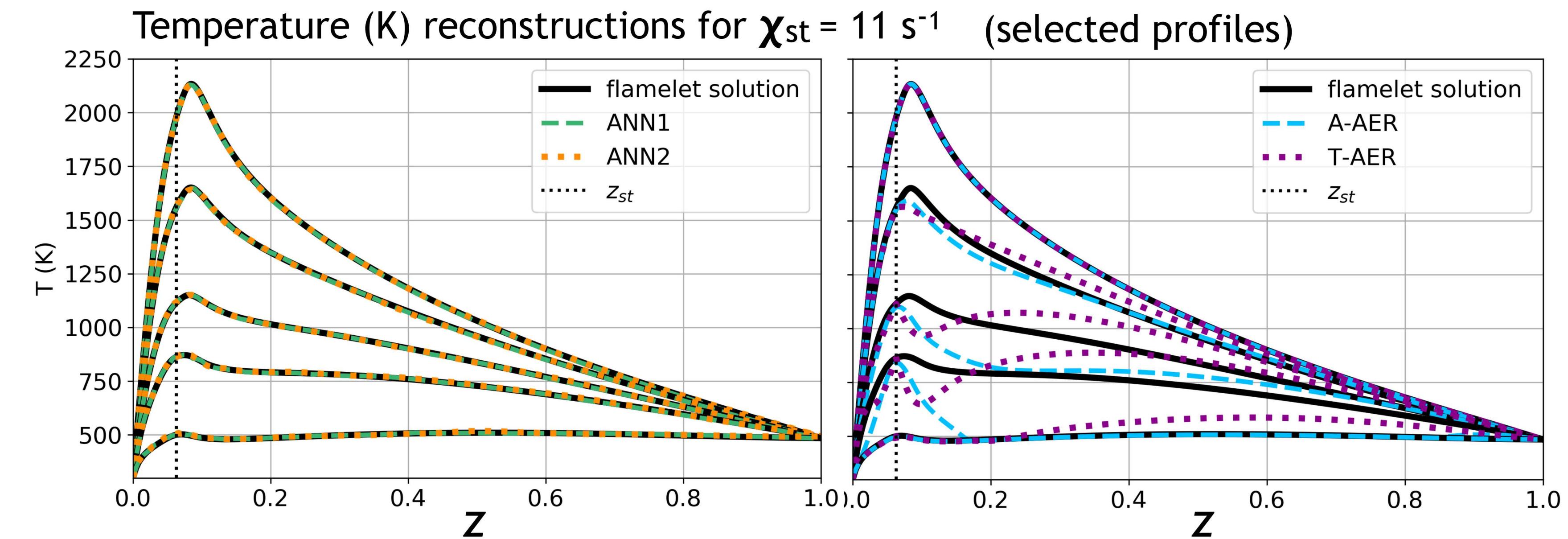
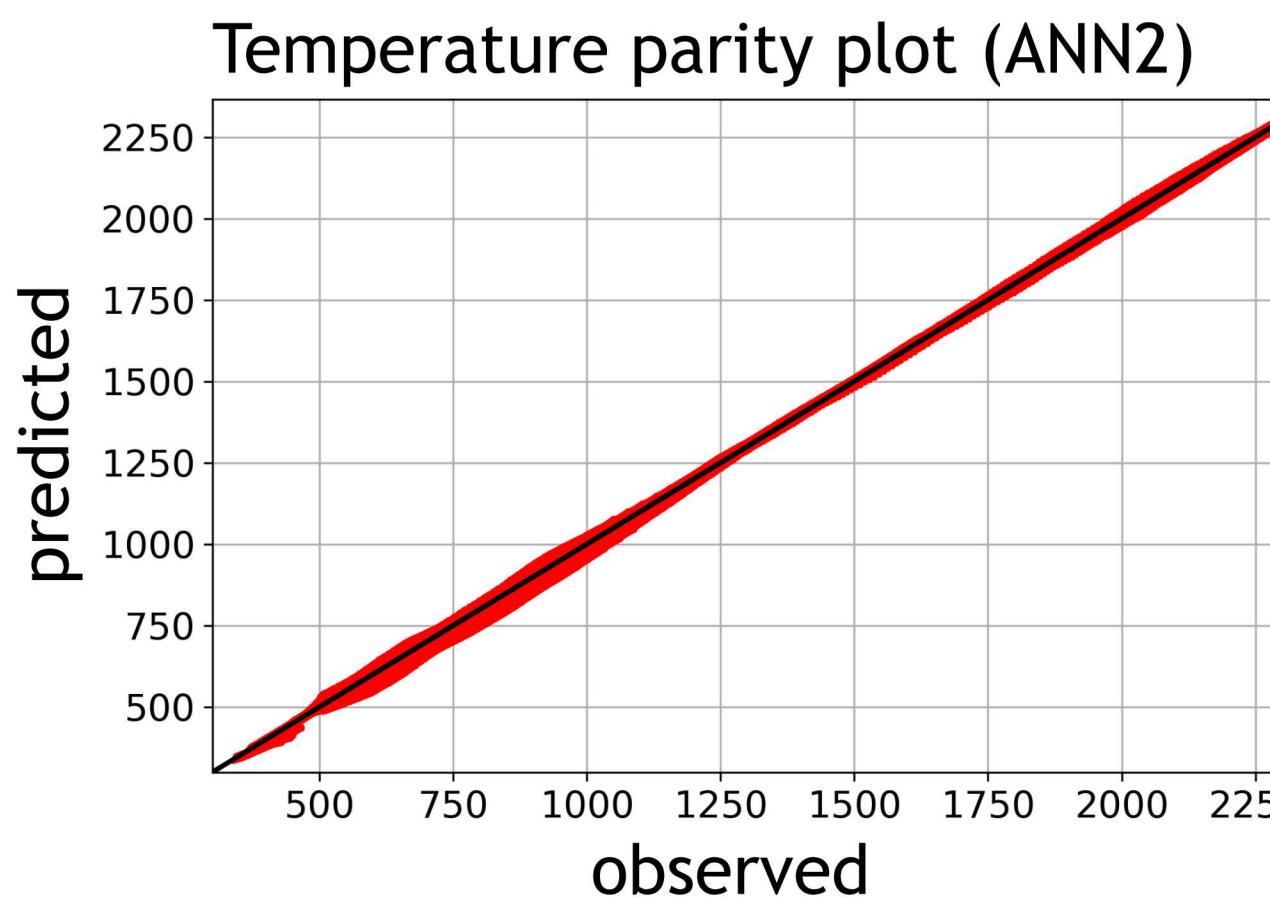


# Machine learning is a promising alternative to structured chemistry tabulation



ANN1: trained on whole unstructured flamelet dataset

ANN2: trained on every other point in dataset



- The ANNs have **more** error than CER, but **less** error than AER methods
- ANNs trained on coarsened datasets show good accuracy
- ANNs are only 1 MB compared to 28 MB for a structured table build using  $(T, \rho, \gamma)$
- Structured tables can reach around a few GB large for actual turbulent simulations

# Conclusions

- AER methods lead to substantial errors in scenarios with high heat loss
  - Up to 10% over-prediction in steady state soot mass fraction for T-AER compared to CER for the laminar sooting ethylene jet flame studied here
  - Improved approximations can be constructed (A-AER), but are not generally accurate
- The CER method offers more accuracy for high heat loss scenarios
  - Should only be 5-10% more expensive than AER when optimized
- Replacing structured tabulation with ANNs shows promise
  - May dramatically reduce memory  $\sim 30x$
  - May enable higher dimensional models
  - Shows accuracy between AER and CER

## Future Work

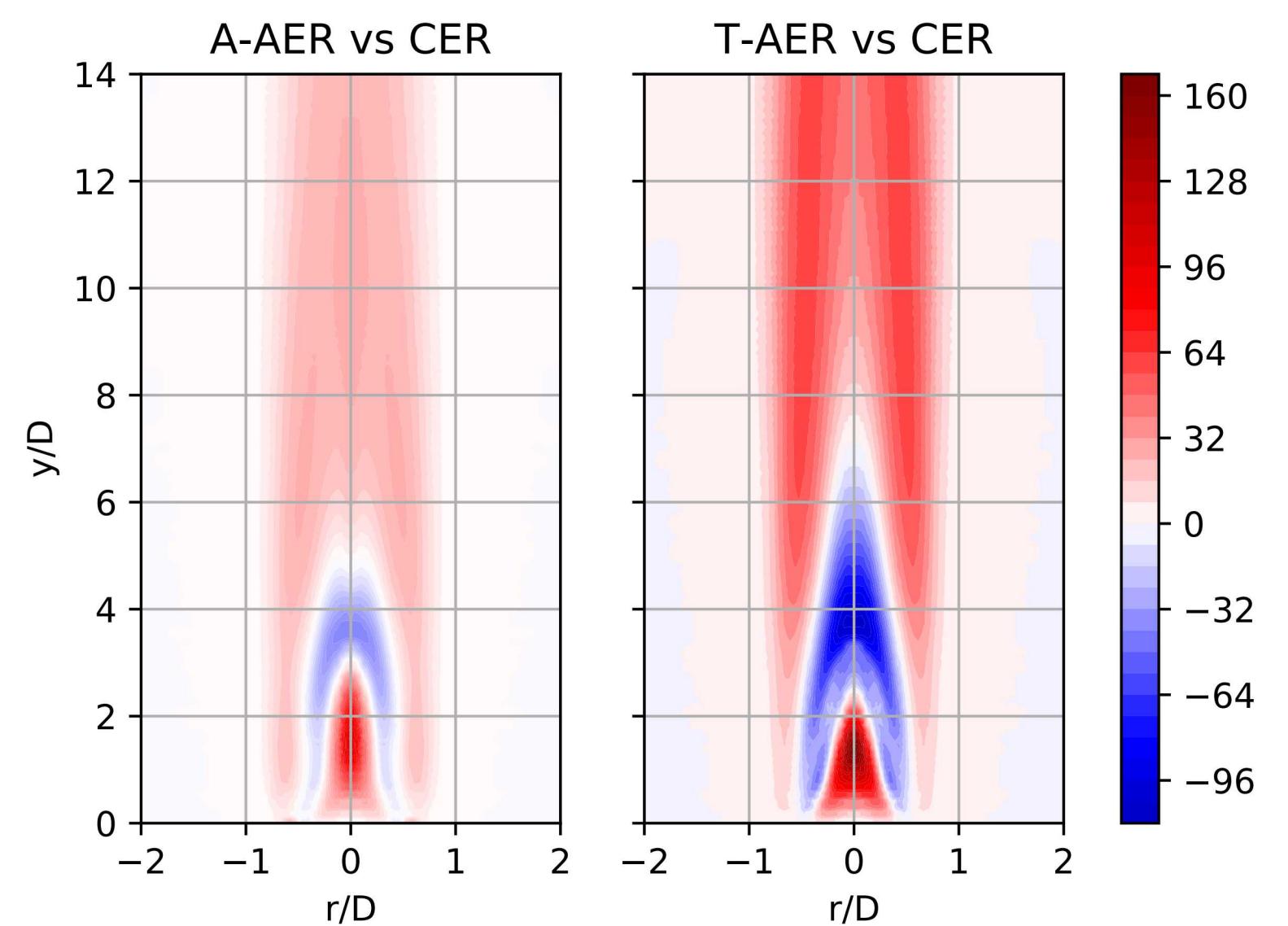
- Explore optimal ANNs and run *in situ* for flame calculations
- Study optimized interpolants to improve CER
- Perform more detailed cost analysis between CER and ANN approaches
- Test in turbulent simulations at scale

## Acknowledgements

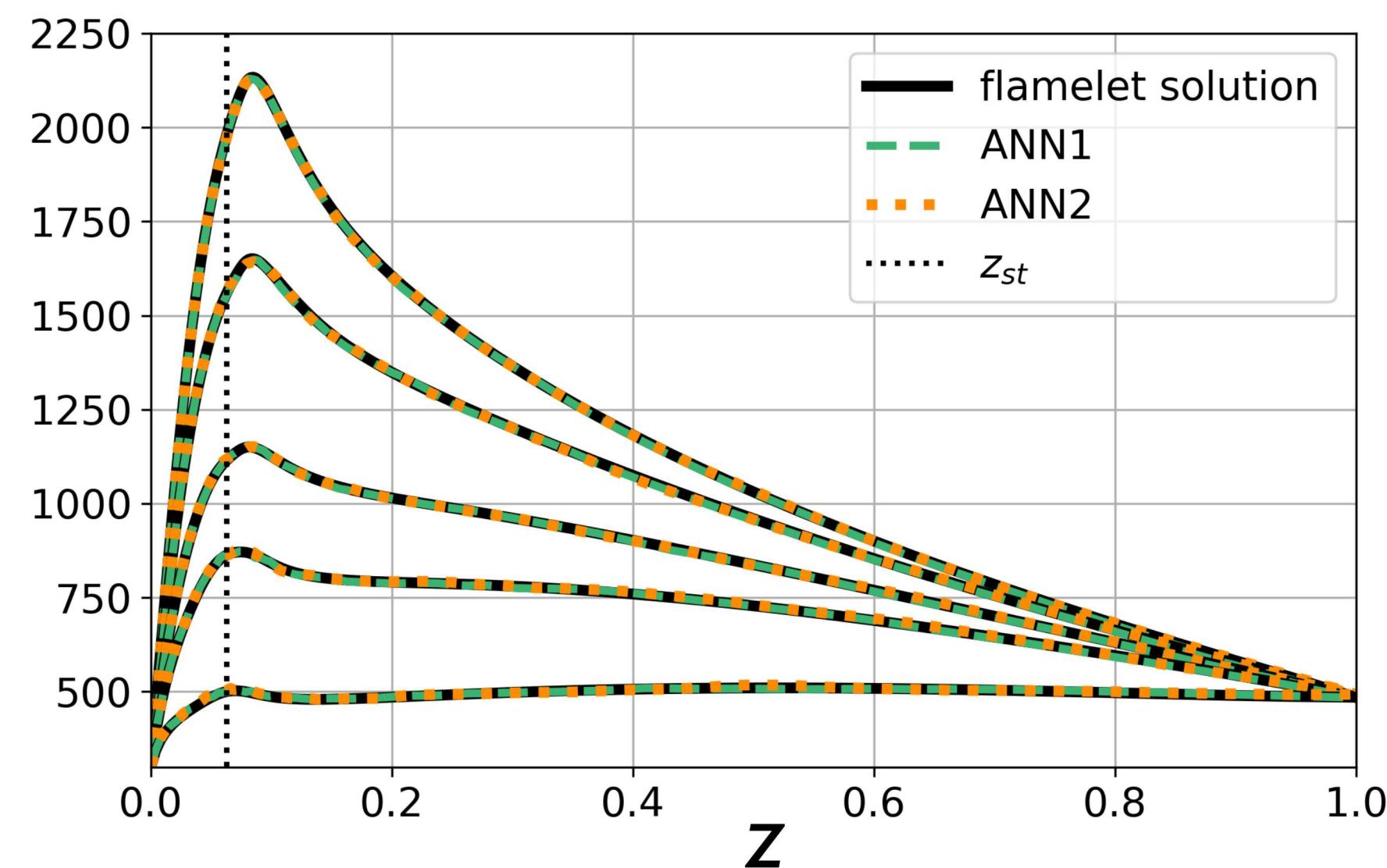
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Professor of Chemical Engineering (Univ. Of Utah)

## temperature error (K)



## Temperature (K) reconstructions for $\chi_{st} = 11 \text{ s}^{-1}$





## Supplemental Slides

# A transient non-adiabatic flamelet approach enables a large enough range of states accessed in sooting, turbulent fire simulations



$$\frac{\partial Y_i}{\partial t} = \frac{\chi}{2} \frac{\partial^2 Y_i}{\partial Z^2} + \frac{\omega_i}{\rho}$$

adiabatic formulation

provide cooling for flames with higher mixing rates

more uniform heat loss during transient heat-loss driven extinction

linear background temperature

avoid increase in stoichiometric enthalpy from reactant mixing

$$\frac{\partial T}{\partial t} = \frac{\chi}{2} \frac{\partial^2 T}{\partial Z^2} - \frac{1}{\rho c_p} \sum_{i=1}^n \omega_i h_i - \frac{H \chi_{\max}}{\rho c_p} \frac{1 - Z_{\text{st}}}{Z_{\text{st}}} \frac{T - T_{\infty}}{T_{\max} - T_{\infty}}$$

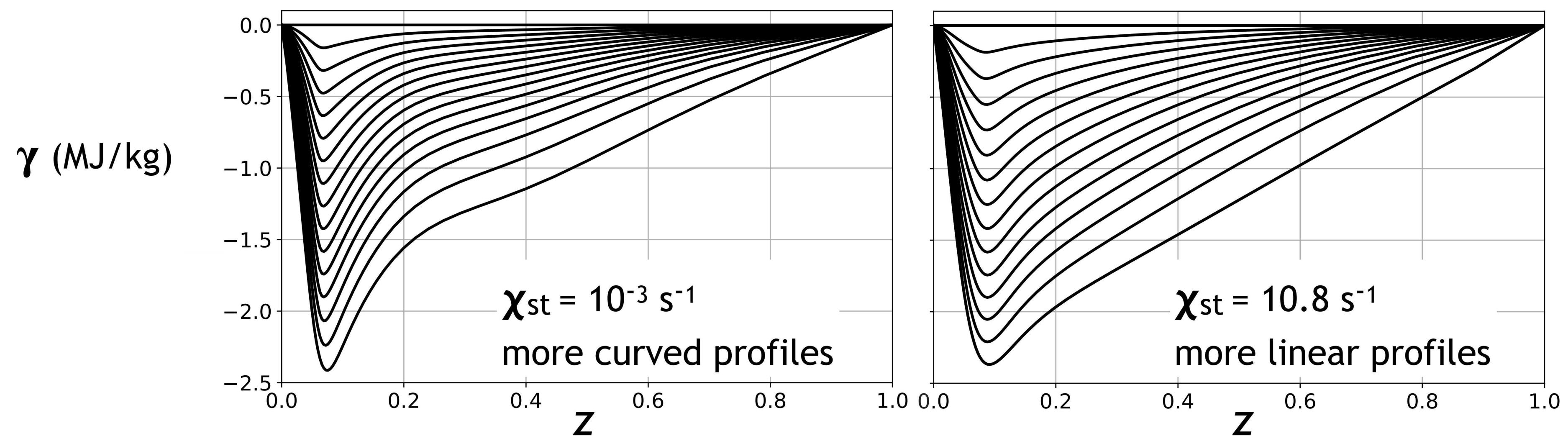
related to heat released, hydrocarbons  $O(10^7 \text{ J/m}^3)$

non-adiabatic formulation

↑

Integrate equations until  $T$  comes within 5% of  $\max(T_{\infty})$

Solved using Spitfire  
(soon to be open-sourced)

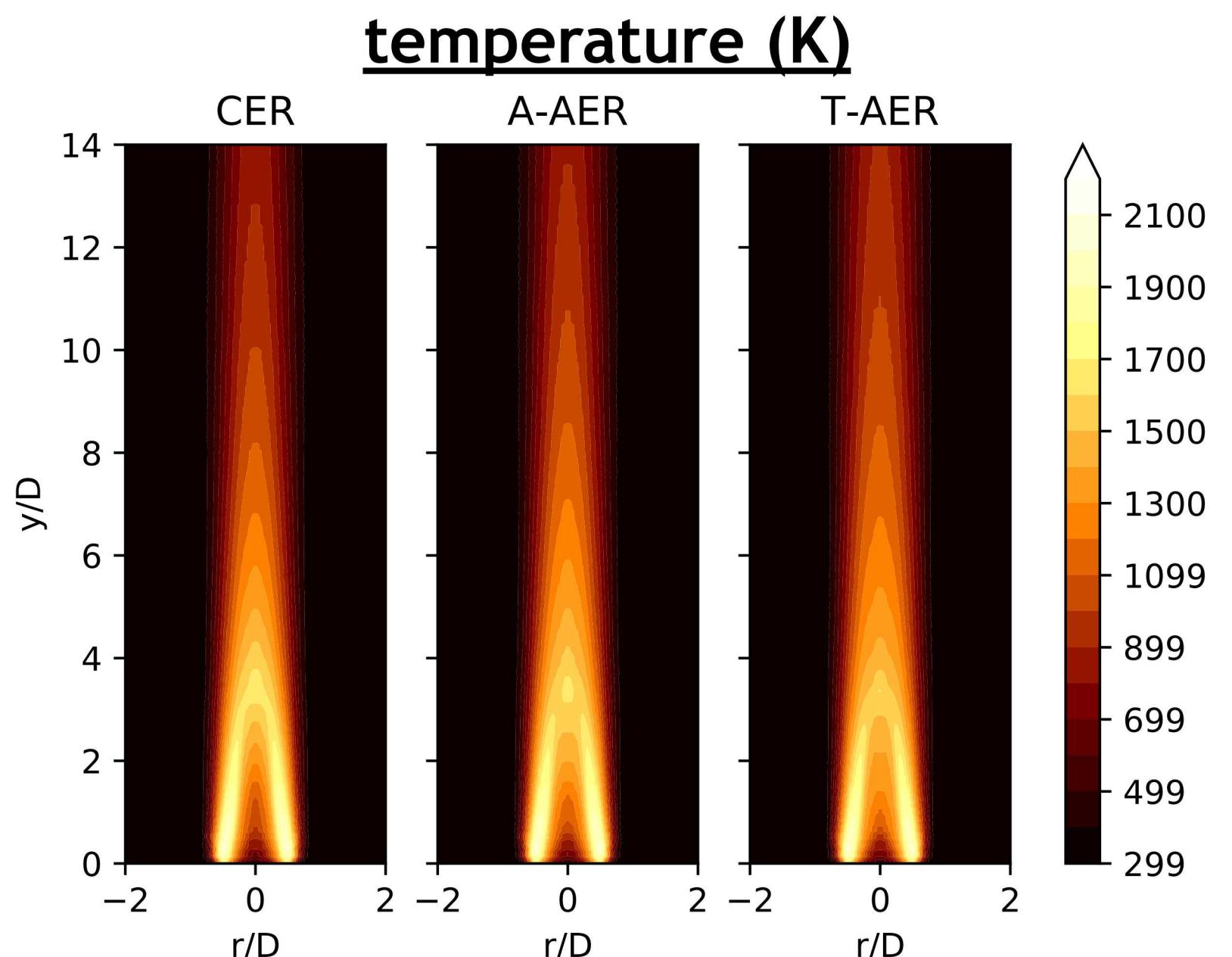
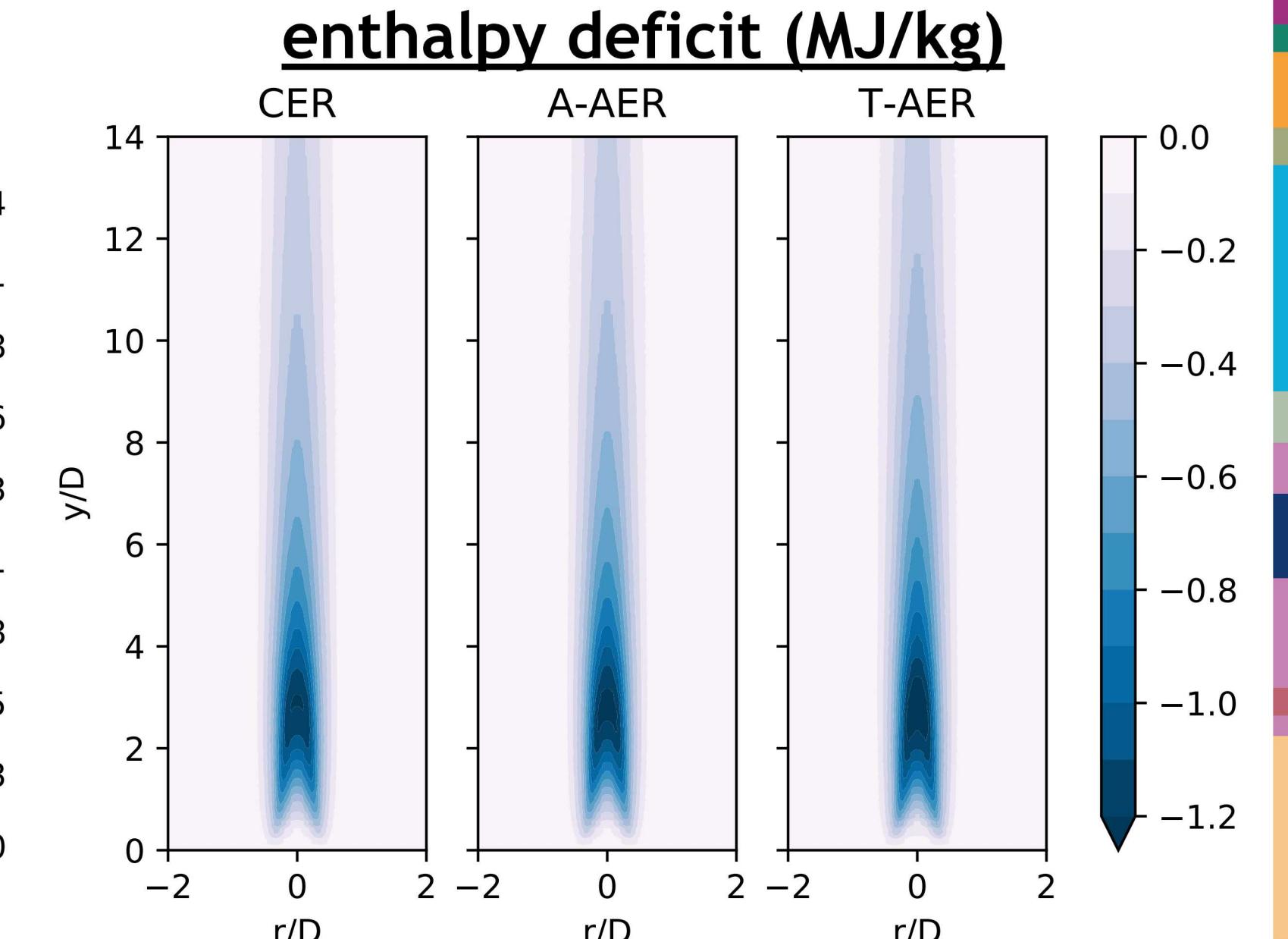
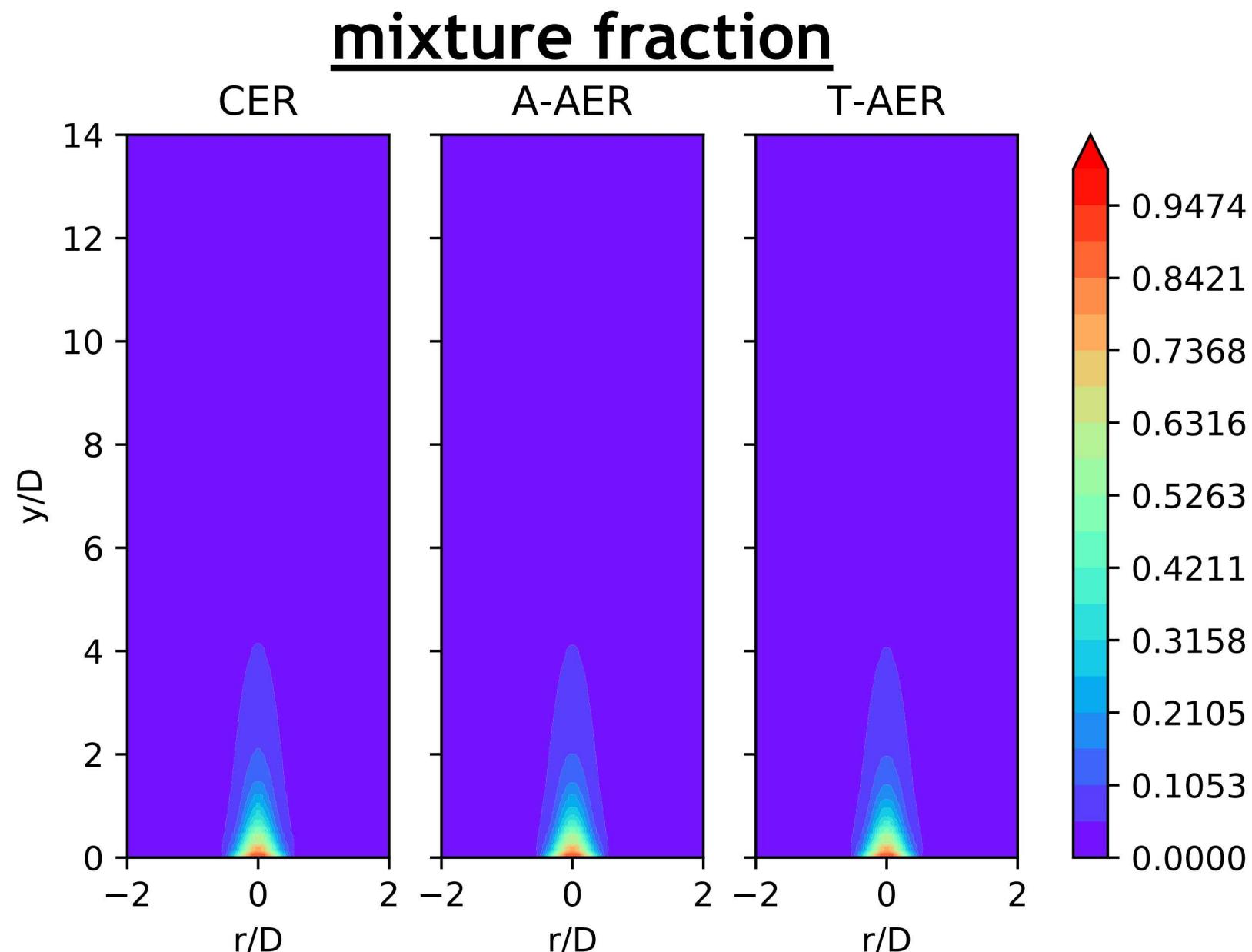


# Qualitative differences are observed between the methods for a steady laminar ethylene sooting jet flame

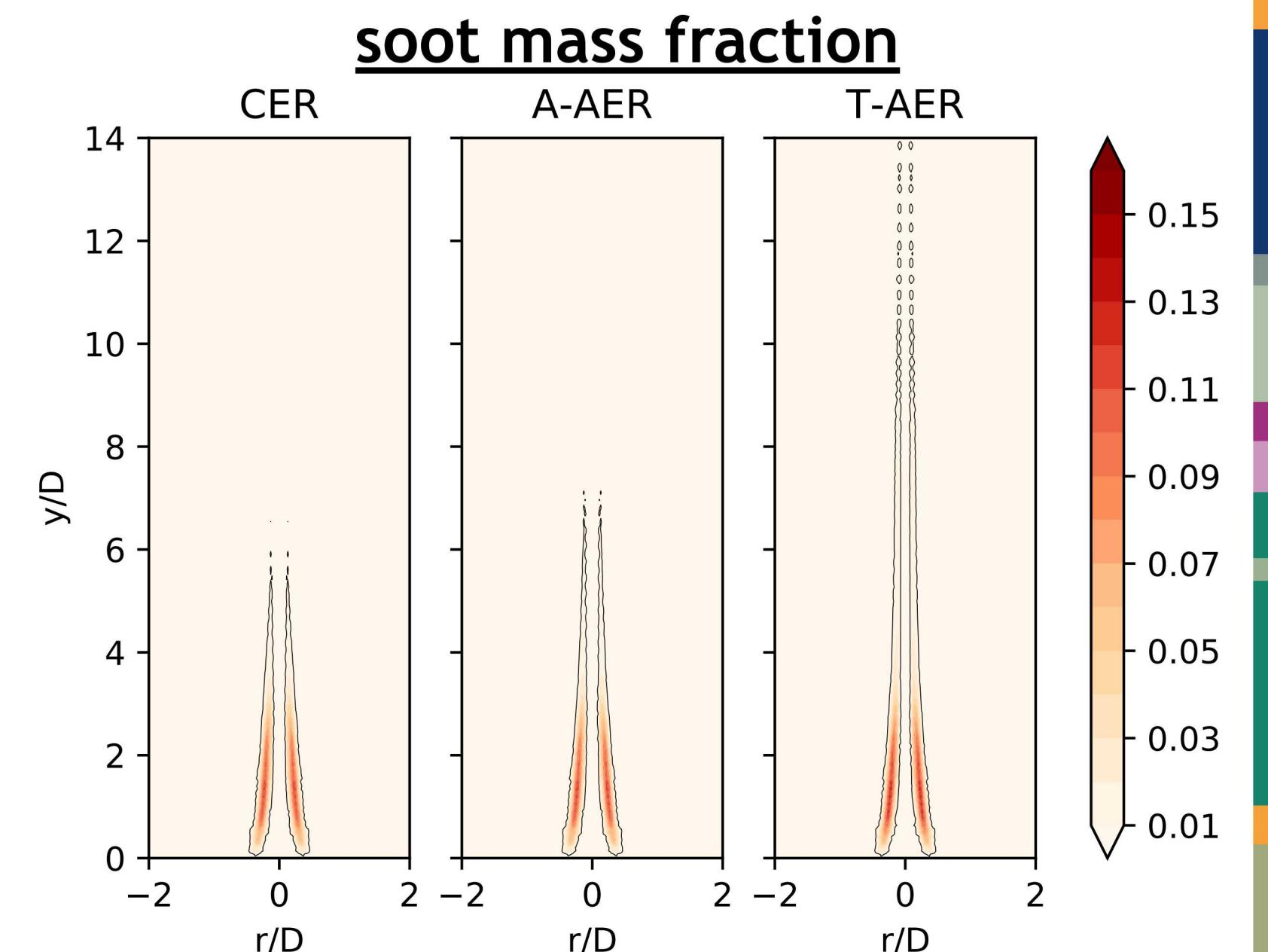


Steady state profiles for an ethylene laminar coflow, sooting jet with 11 mm diameter (D)

Simple radiation ( $4\sigma T_{\text{ref}}^4$ )



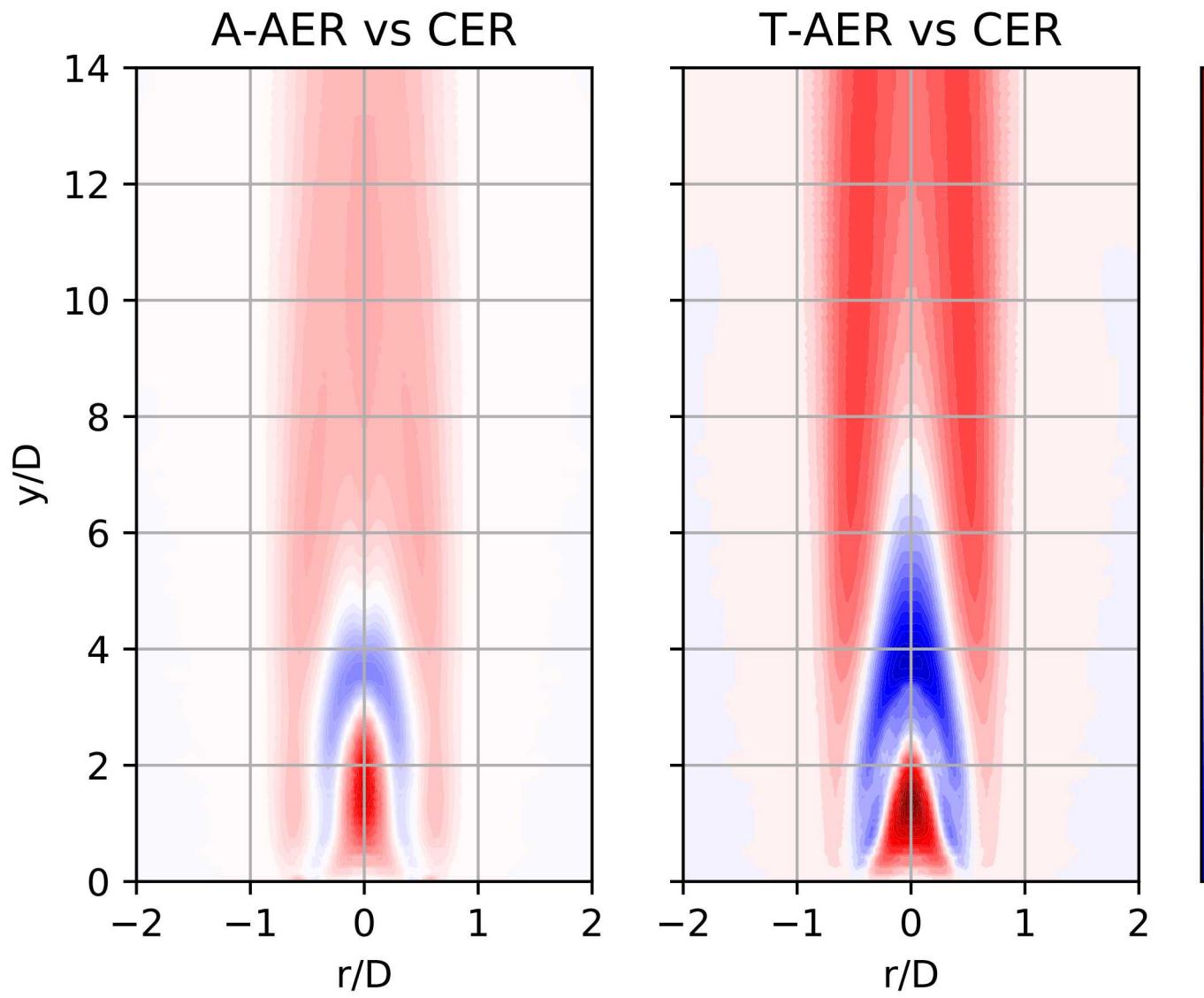
- Largest qualitative difference in soot mass fraction
- T-AER has the largest areas of heat loss for a given contour



# AER methods have less error in scenarios with less heat loss

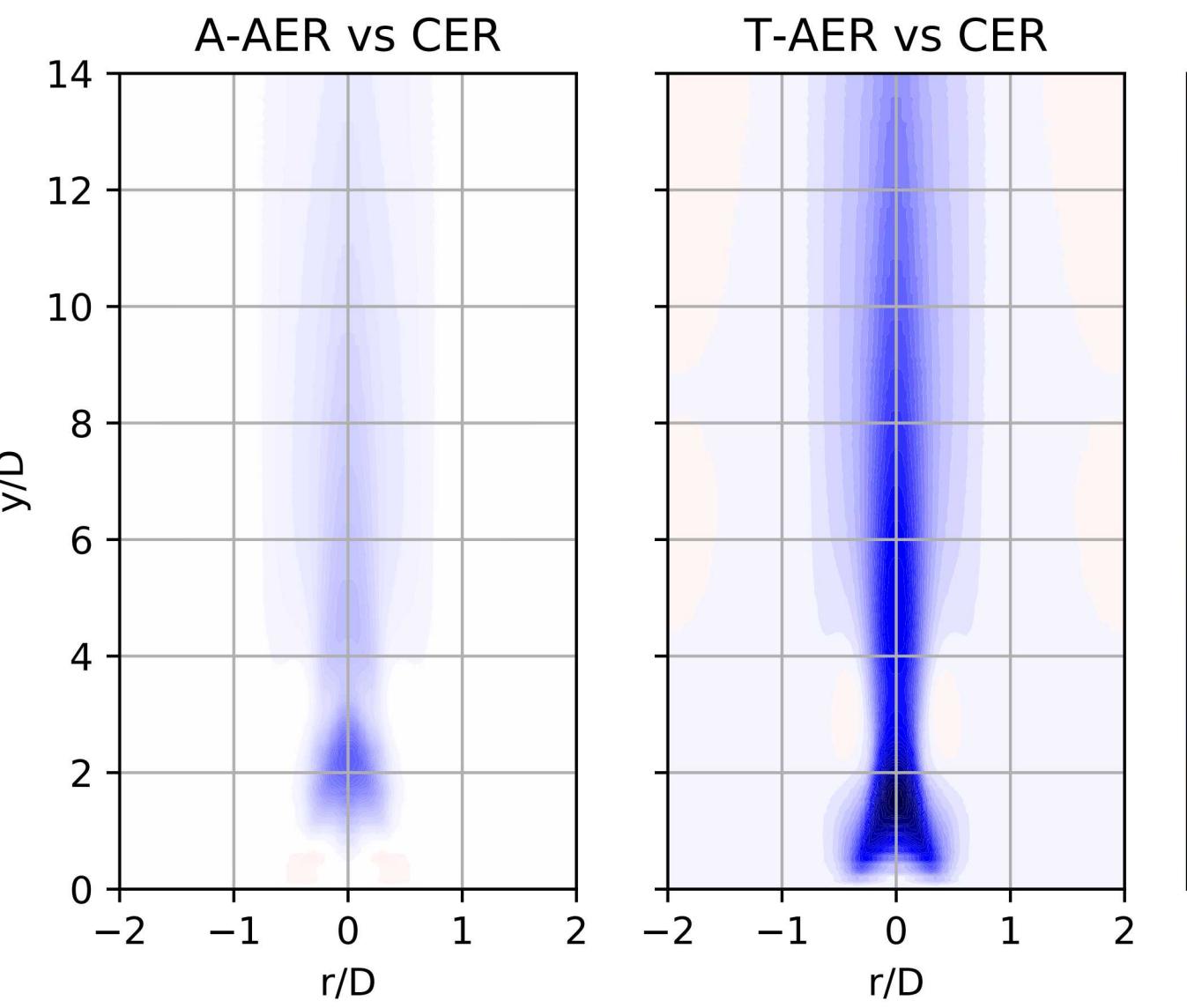


Computed from table queries  
temperature error (K)

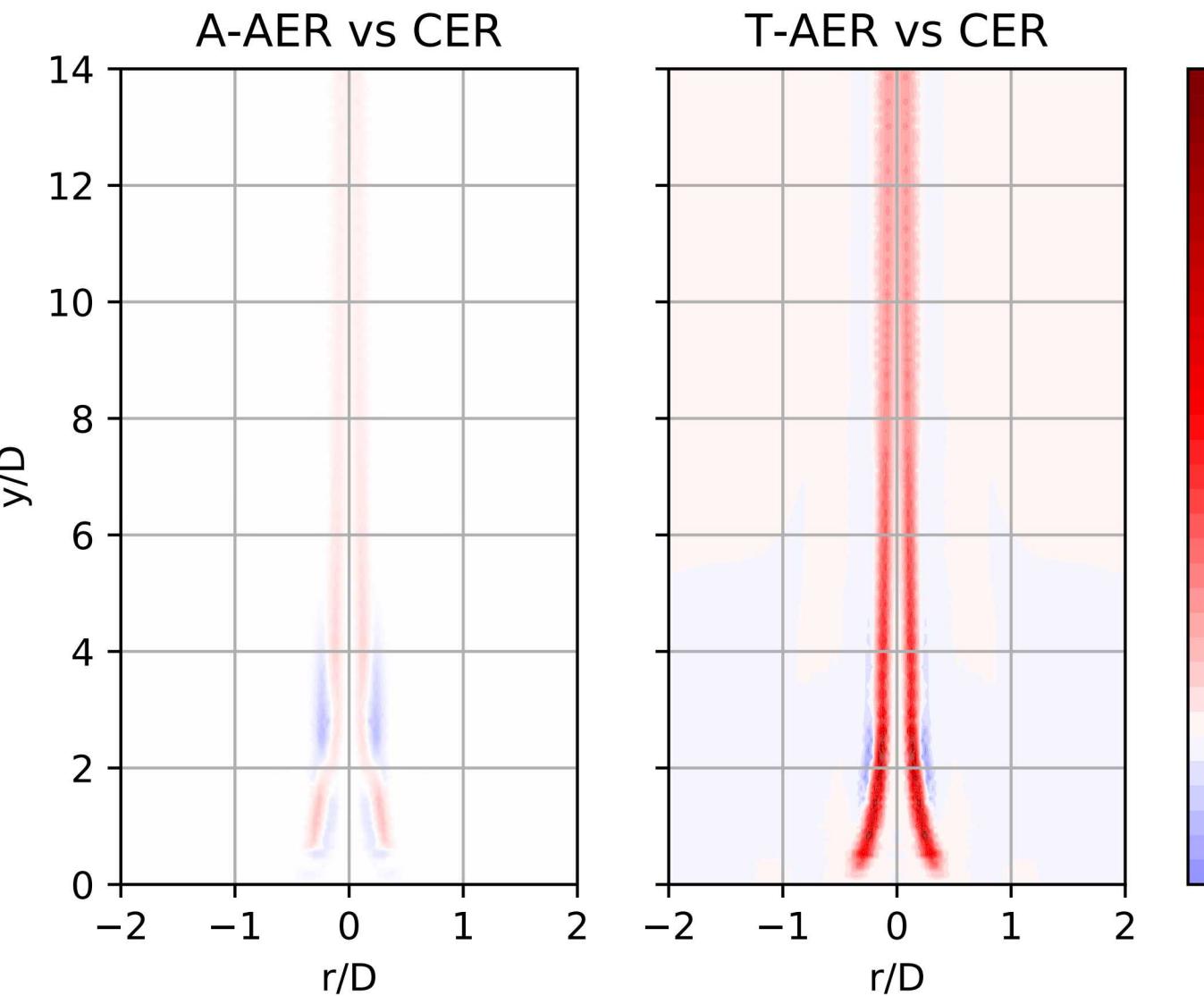


Transported in simulation

enthalpy deficit error (MJ/kg)



soot mass fraction error



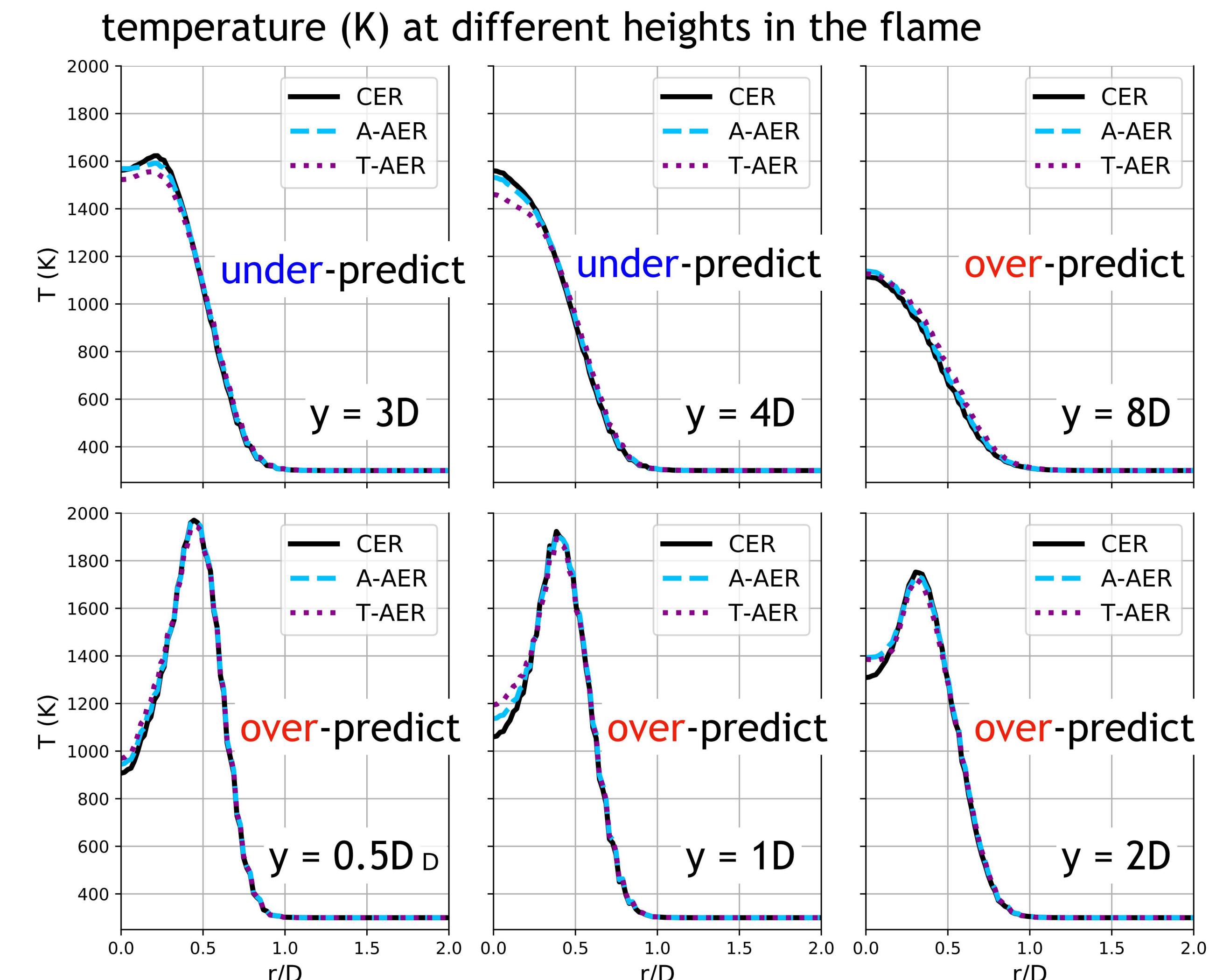
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Steady state profiles for an ethylene laminar coflow, sooting jet with 11 mm diameter (D)

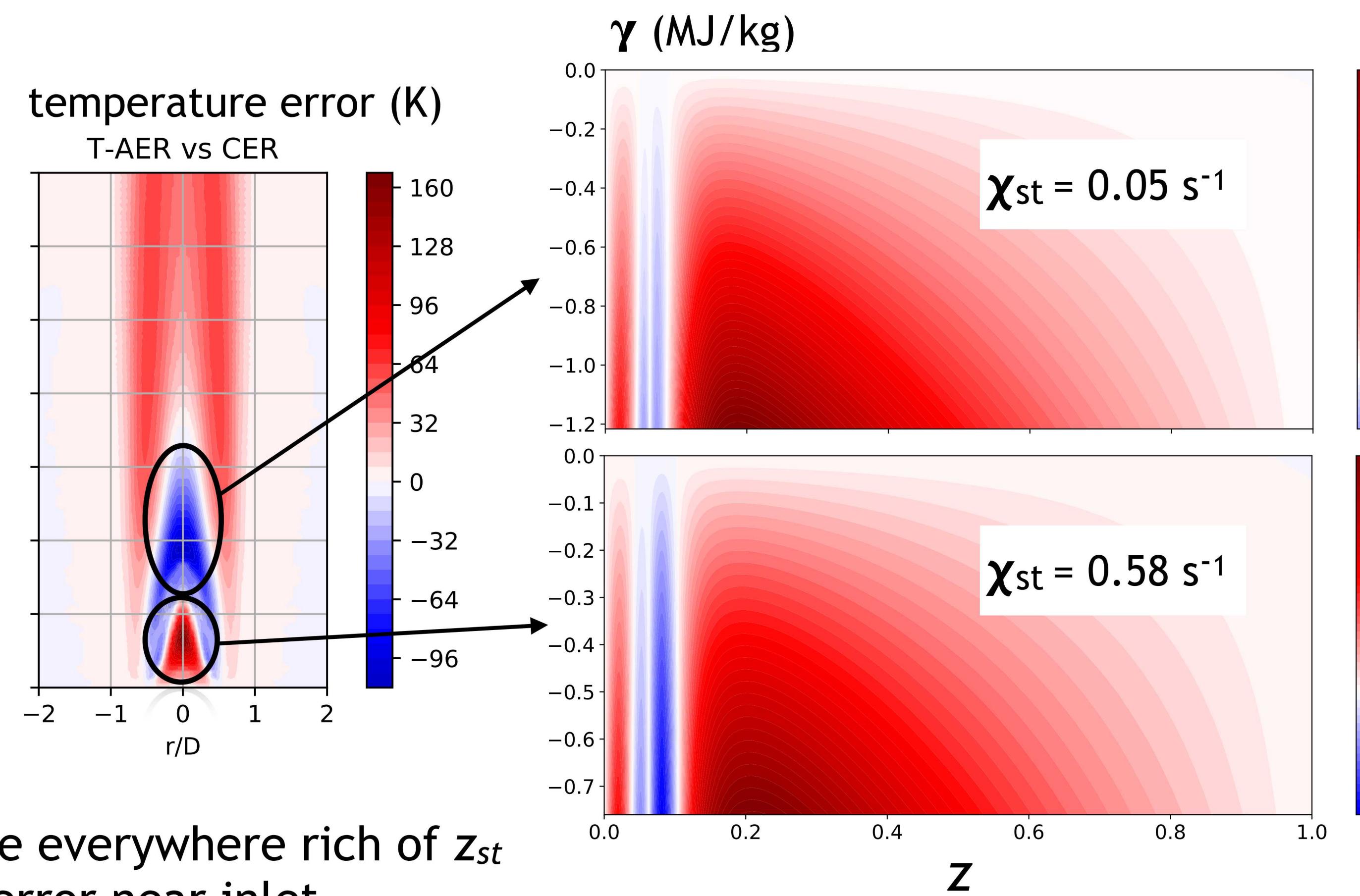
Simple radiation ( $4\sigma T_{\text{ref}}^4$ )

- A-AER results are closer to CER than T-AER results
- AER methods show a non-linear pattern of over-under-predictions in temperature moving up the domain at the centerline



We can explain errors in the steady state profiles through *a priori* error analysis

Under-predicting temperature around  $z_{st}$   
Smaller magnitude of error in this region compared to rich regions at  $0.58 \text{ s}^{-1}$

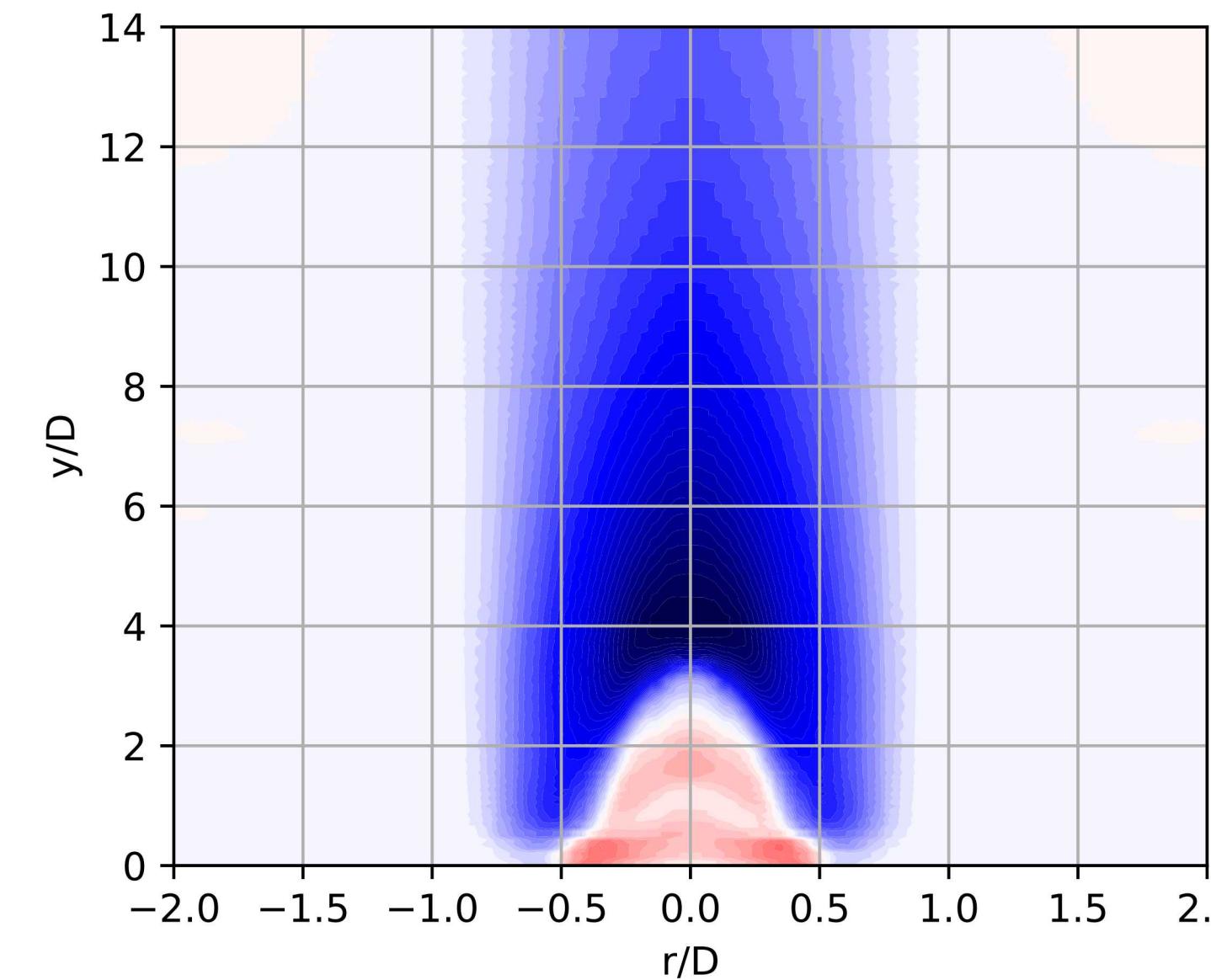


Over-predicting temperature everywhere rich of  $z_{st}$   
Matches observations for T error near inlet

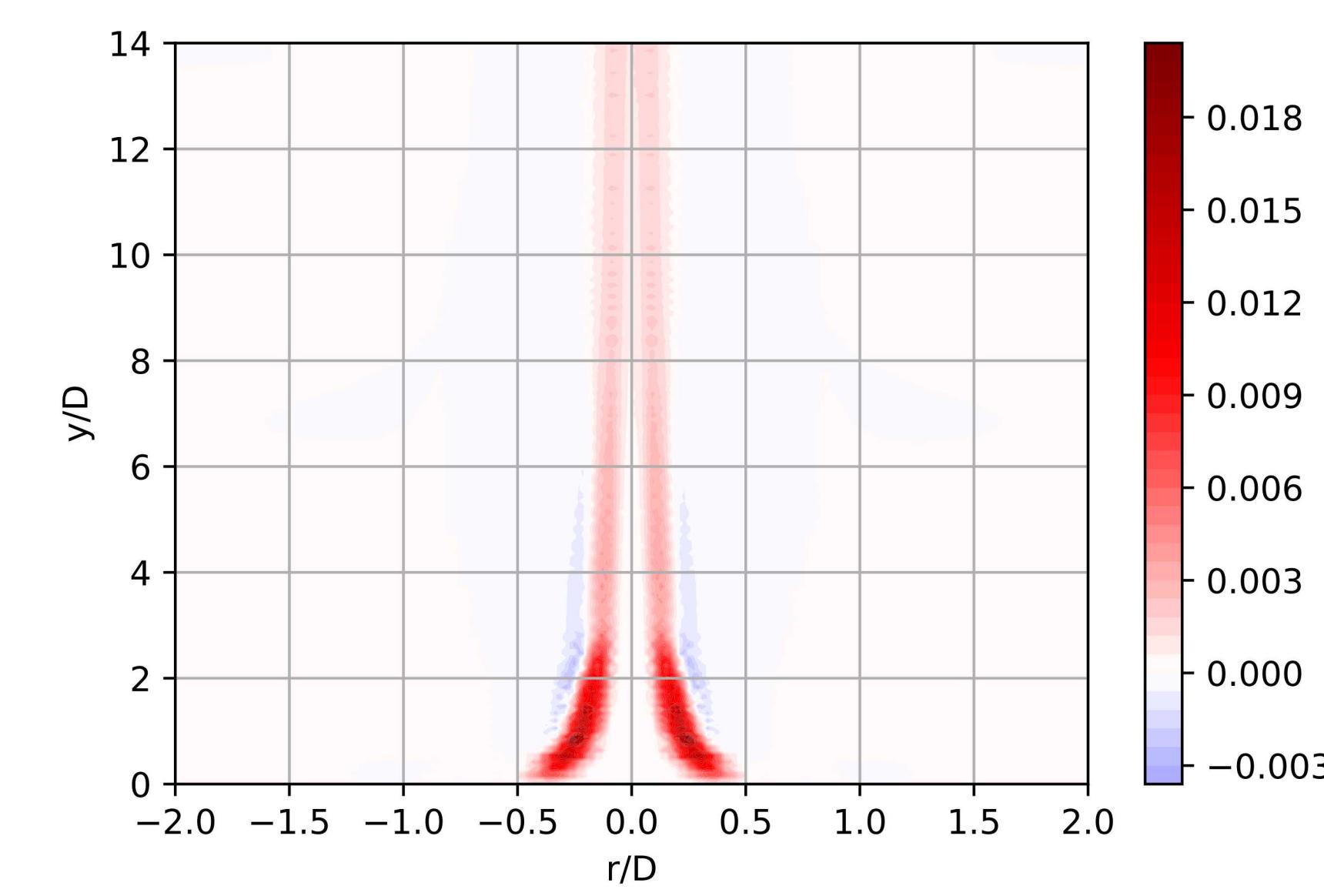
# The analysis remains applicable for radiation modeled with PMR

participating media radiation (PMR) - simple radiation for CER

Temperature difference (K)



Soot mass fraction difference

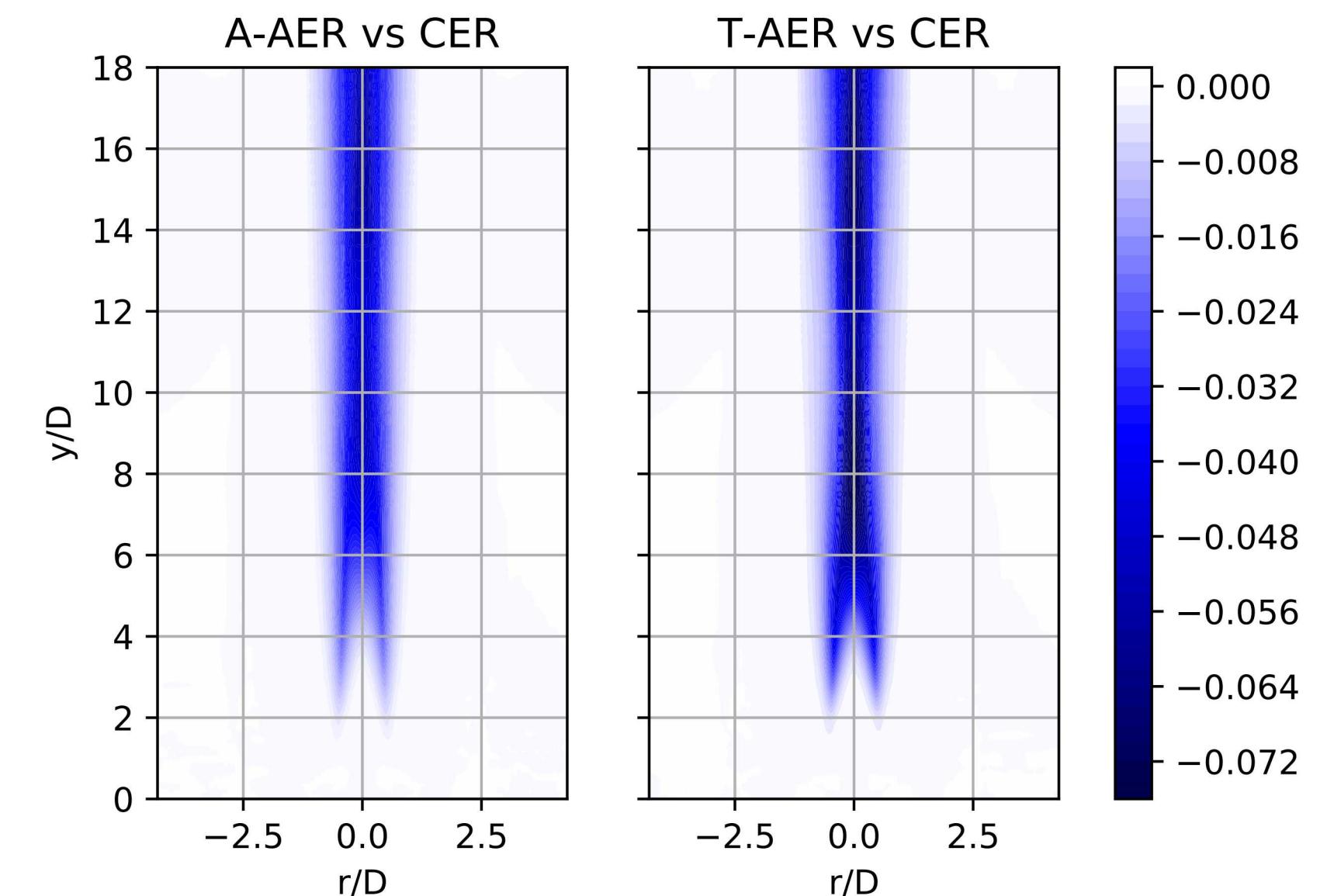


- Near the inlet, the temperature is higher for PMR than SR, which corresponds to a larger soot mass fraction
- At most a 5% difference in temperature, but an 11% higher maximum observed soot mass fraction for PMR compared to simple radiation
  - any differences in temperature can be amplified in the soot production due to sensitivities
  - soot production more coupled to PMR
- PMR changed the overall quantities of the steady state properties compared to simple radiation, but did not change the relative differences between the CER, T-AER, and A-AER

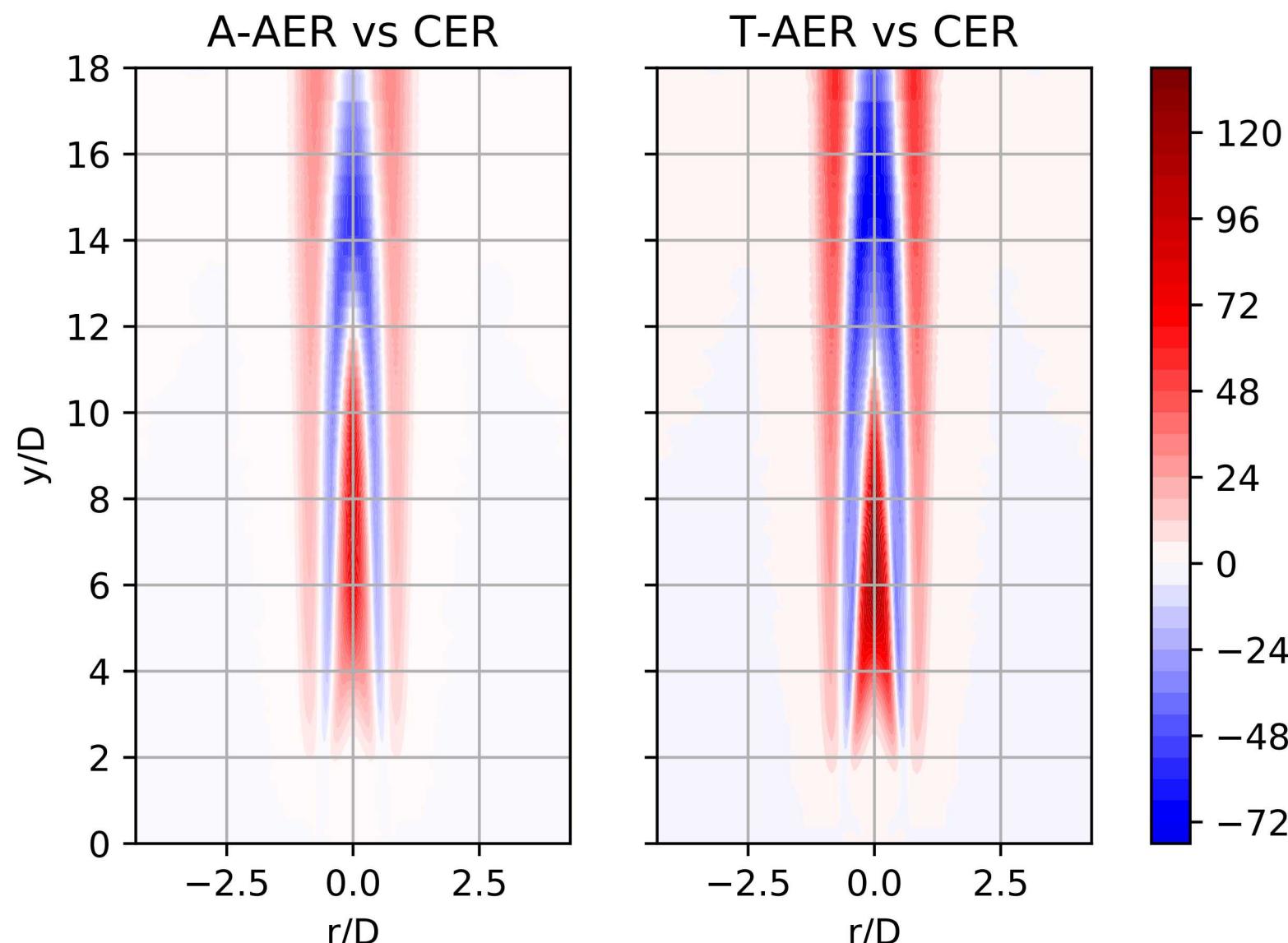
# The analysis remains applicable for heptane

- See same trends in results as saw with ethylene
- However, with heptane there is only about a 5% over-prediction of the maximum soot mass fraction by T-AER compared to CER
- The heptane case also has less heat loss overall compared to ethylene
  - AER methods have less error in scenarios with less heat loss
  - have the benefit of being less expensive in these scenarios

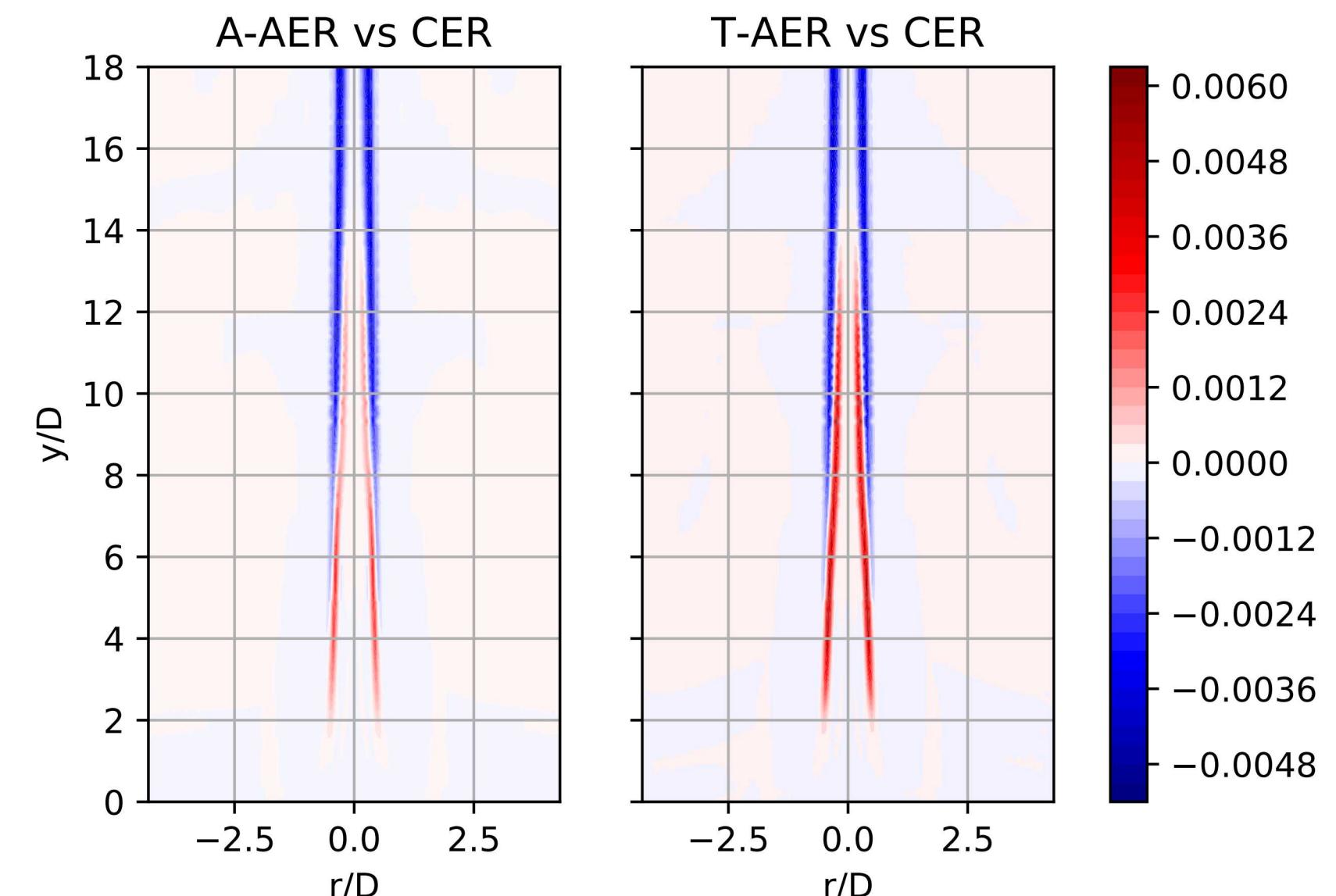
enthalpy deficit error (MJ/kg)



temperature error (K)



soot mass fraction error



# The equations we solve

- Thermochemical states are typically calculated using the steady laminar flamelet model (SLFM)

$$\frac{\partial Y_i}{\partial t} = \frac{\chi}{2} \frac{\partial^2 Y_i}{\partial Z^2} + \frac{\omega_i}{\rho}$$

$$\frac{\partial T}{\partial t} = -\frac{1}{\rho c_p} \sum_{i=1}^n \omega_i h_i + \frac{\chi}{2} \frac{\partial^2 T}{\partial Z^2} + \frac{\chi}{2} \frac{1}{c_p} \frac{\partial T}{\partial Z} \frac{\partial c_p}{\partial Z} + \frac{\chi}{2} \frac{\partial T}{\partial Z} \sum_{i=1}^n \frac{c_{p,i}}{c_p} \frac{\partial Y_i}{\partial Z}$$

classical flamelet equations

variable  $c_p$

distinct  $c_{p,i}$