

Hydrocarbon and Water Desorption from Oxide Surfaces using Molecular Dynamics

Jason P. Koski
J. Matthew D. Lane

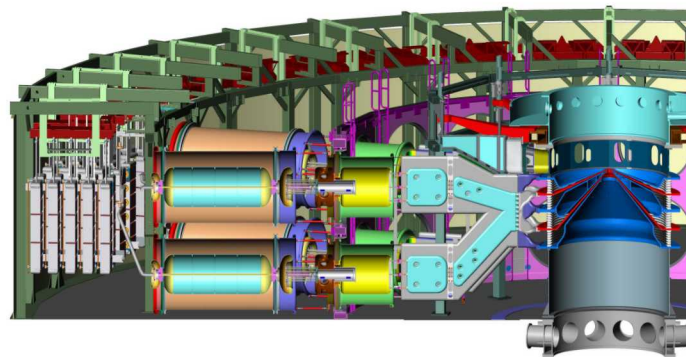
June 19th, 2019

Motivation

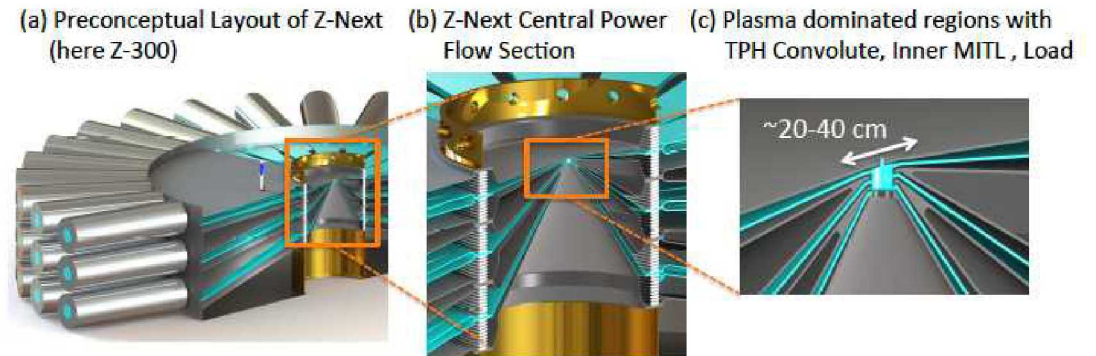
Sandia is the nation's leading laboratory for developing advanced **pulsed power technologies**

- Nuclear weapon physics
- Inertial confinement fusion

Pulsed power machines are unique environments for extreme environment research



Z



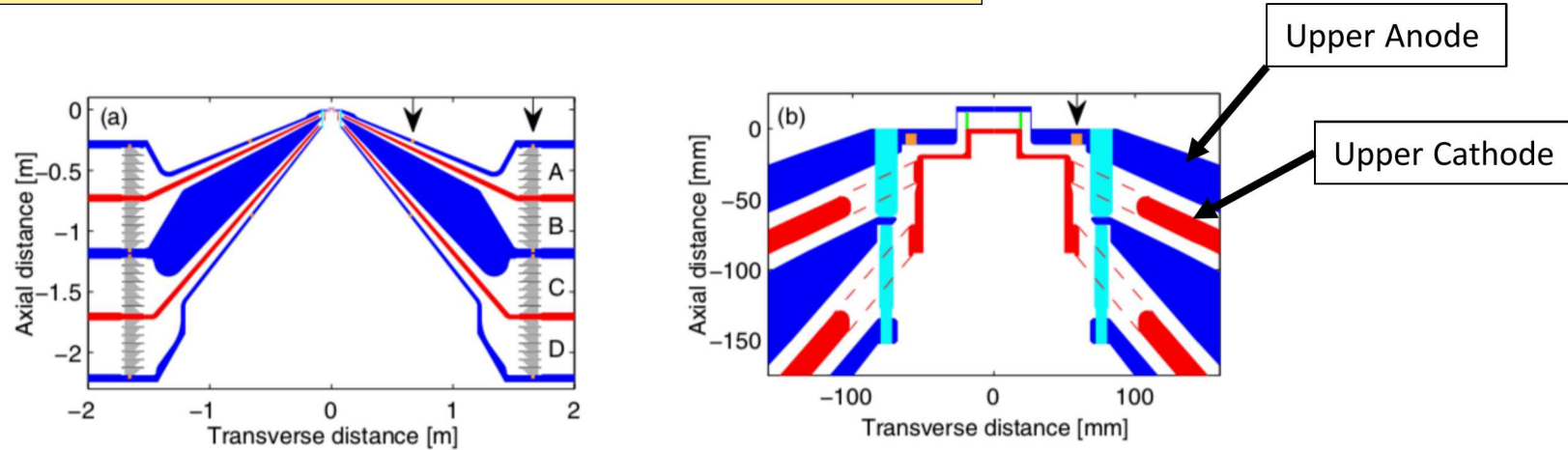
Z-Next

We want to confidently scale-up and design Next-Generation Pulsed Power Machines

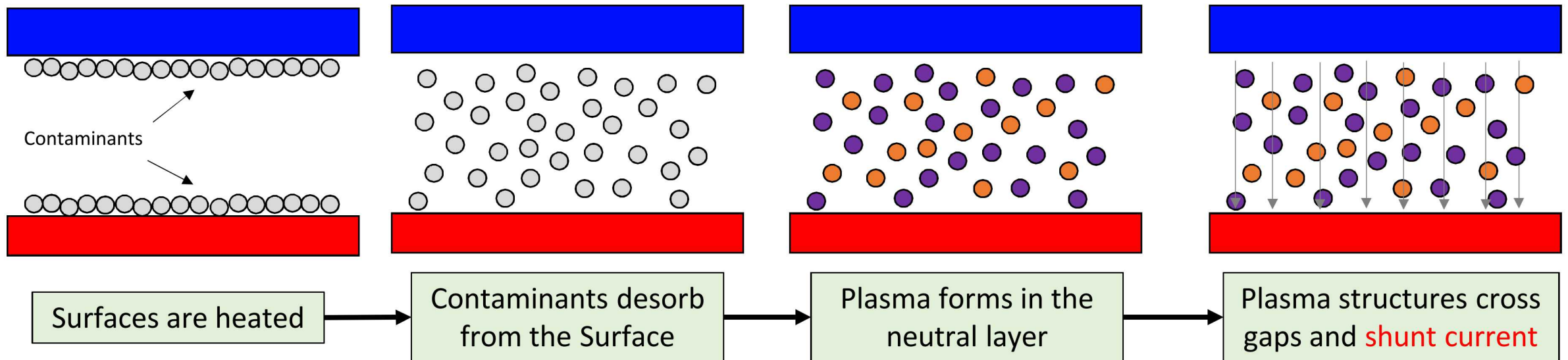
Power flow and current loss need to be addressed for scale-up design

- Current loss is observed from **plasma formation**

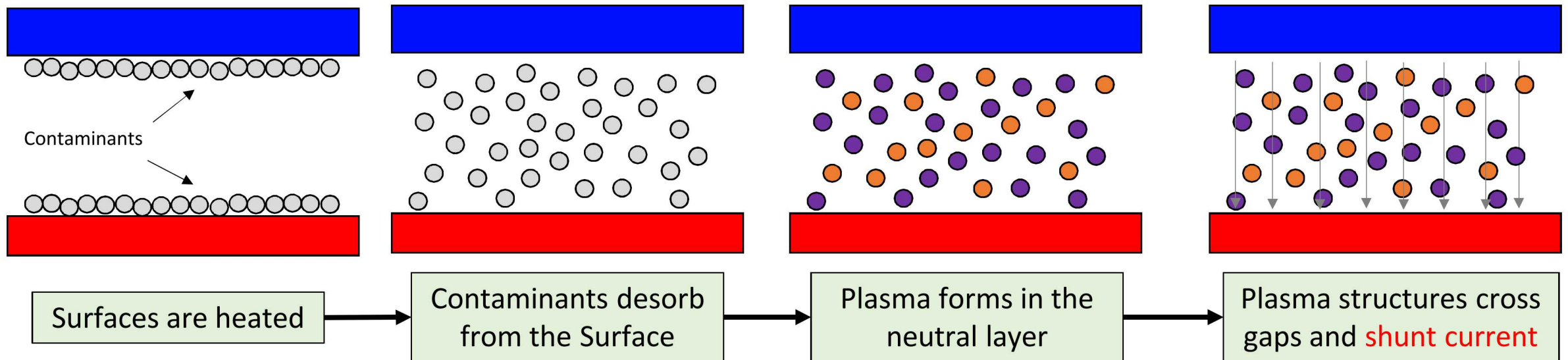
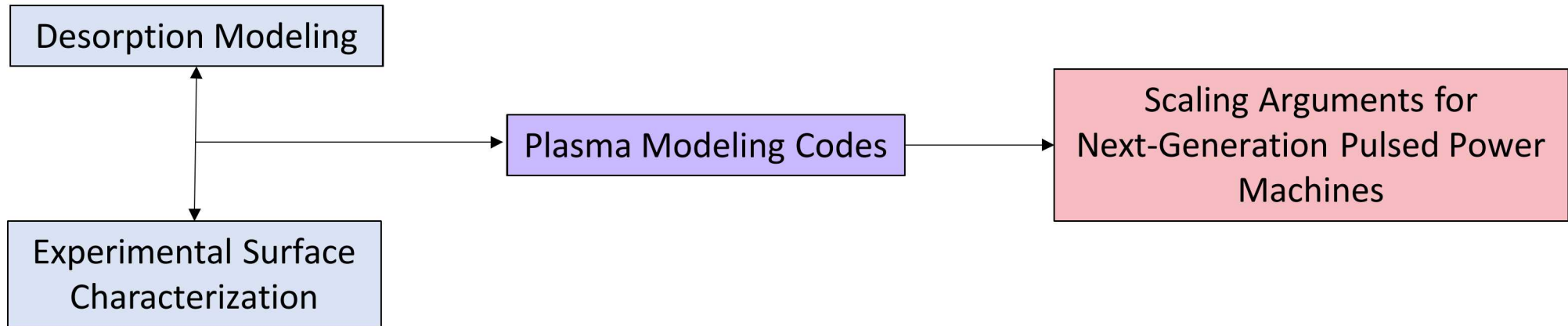
Current Understanding of Plasma Formation on Z



M. R. GOMEZ *et al.* PHYS. REV. ACCEL. BEAMS **20**, 010401 (2017)



Motivation



Desorption Modeling

Goal:

Confidently **scale-up and design** Next-Generation Pulsed Power Machines

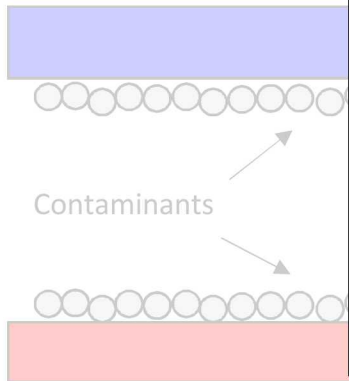
Problem:

Power flow and current loss need to be addressed for scale-up design

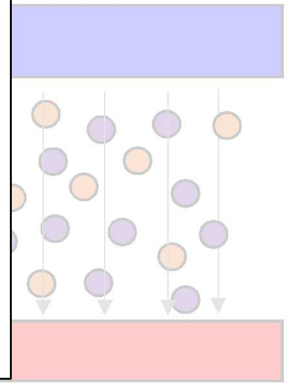
- Current loss is observed from **plasma formation**

Approach:

Use **molecular dynamics** to predict hydrocarbon and hydrocarbon/water mixture **desorption composition** and **rates** to inform plasma models/codes



or
Power



Surfaces are heated

Contaminants desorb
from the Surface

Plasma forms in the
neutral layer

Plasma structures cross
gaps and **shunt current**

Details of Desorption Modeling

Desorption Modeling

ClayFF (substrate) with SPC (water):

$$E_{\text{total}} = E_{\text{Coul}} + E_{\text{VDW}} + E_{\text{bond}} + E_{\text{angle}} + E_{\text{torsion}}$$

$$E_{\text{Coul}} = \frac{e^2}{4\pi\epsilon_0} \sum_{i \neq j} \frac{q_i q_j}{r_{ij}}$$

$$E_{\text{VDW}} = \sum_{i \neq j} D_{o,ij} \left[\left(\frac{R_{o,ij}}{r_{ij}} \right)^{12} - 2 \left(\frac{R_{o,ij}}{r_{ij}} \right)^6 \right]$$

$$E_{\text{bond stretch } ij} = k_1 (r_{ij} - r_o)^2$$

$$E_{\text{angle bend } ijk} = k_2 (\theta_{ijk} - \theta_o)^2$$

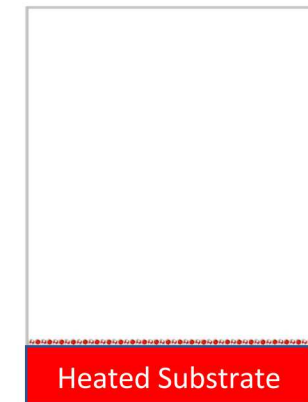
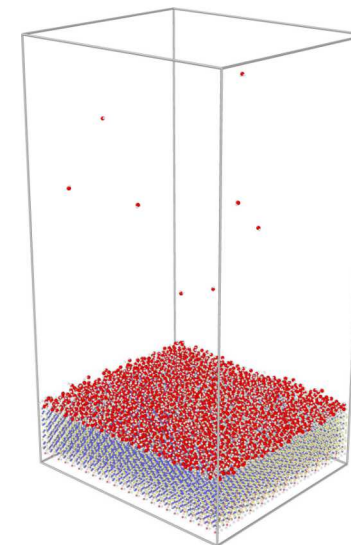
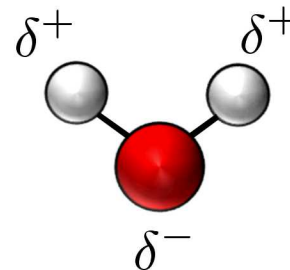
$$E_{\text{torsion}} = \sum_{n=1,5} A_n \cos^{n-1}(\phi)$$

- ClayFF does well with water binding energies with metal oxides.
- SPC Water

Lane, Leung, Thompson, and Cuneo, *J. Phys. Cond. Matt.*, 2018

Initial desorption studies of focused on **Water**:

- Composition
- Coverage
- Electrode Temperature



Temperature ramp from
300K to 1300K

Details of Desorption Modeling

Desorption Modeling

ClayFF with SPC with OPLS (hydrocarbons):

$$E_{\text{total}} = E_{\text{Coul}} + E_{\text{VDW}} + E_{\text{bond}} + E_{\text{angle}} + E_{\text{torsion}}$$

$$E_{\text{Coul}} = \frac{e^2}{4\pi\epsilon_0} \sum_{i \neq j} \frac{q_i q_j}{r_{ij}}$$

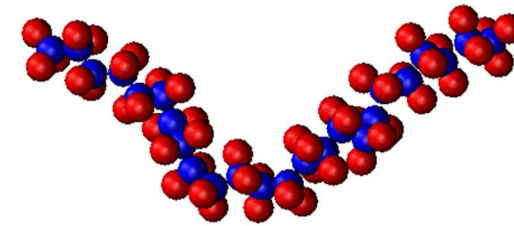
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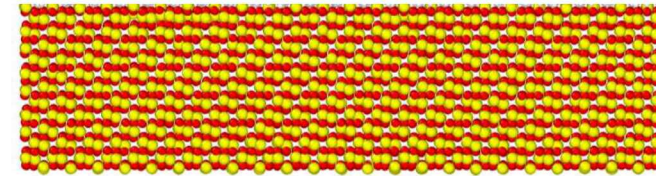
$$E_{\text{torsion}} = \sum_{n=1,5} A_n \cos^{n-1}(\phi)$$

- ClayFF does well with water binding energies with metal oxides.
- SPC Water
- **OPLS Hydrocarbons**



Hydrocarbon (ex. C₂₄H₅₀)

α -Fe₂O₃ hematite (0001)



Side view of substrate

New Study focusing on:

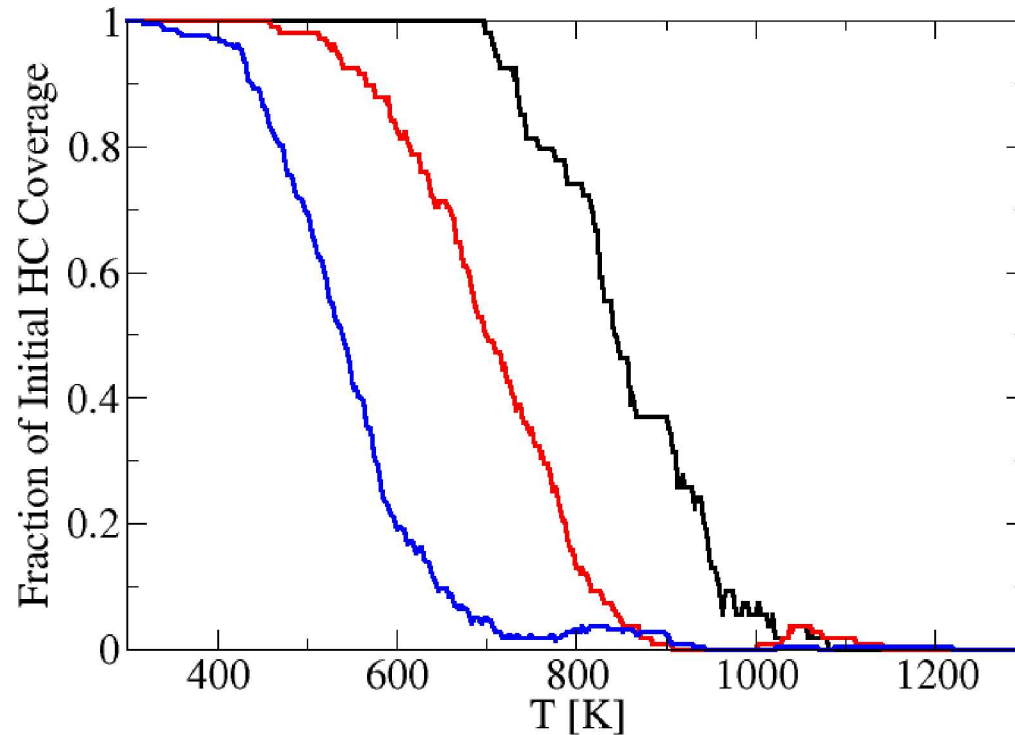
- Chain length
- Chain architecture
- Mixtures

Chain Length Effect

Ramp Rate: 2000K/ns

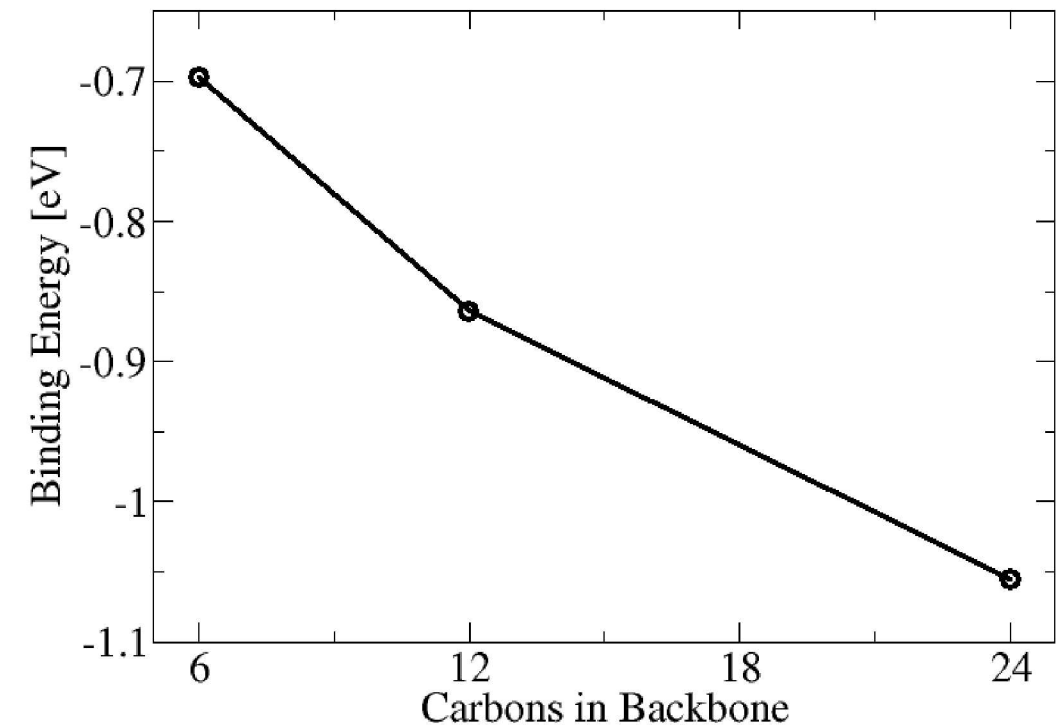
1296 Carbons Initially on Surface

- $n_{\text{chains}} = \{54 \text{ C}_{24}\text{H}_{50}, 108 \text{ C}_{12}\text{H}_{26}, 216 \text{ C}_6\text{H}_{14}\}$



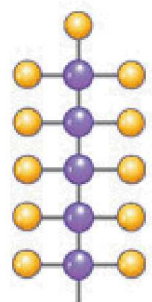
Instantaneous energy difference
between initial and final state

Binding/Desorption energy vs Chain Length

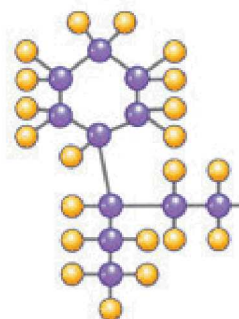


Longer chains more strongly adsorbed to surface due to increased vDW interactions

Chain Architecture Effect

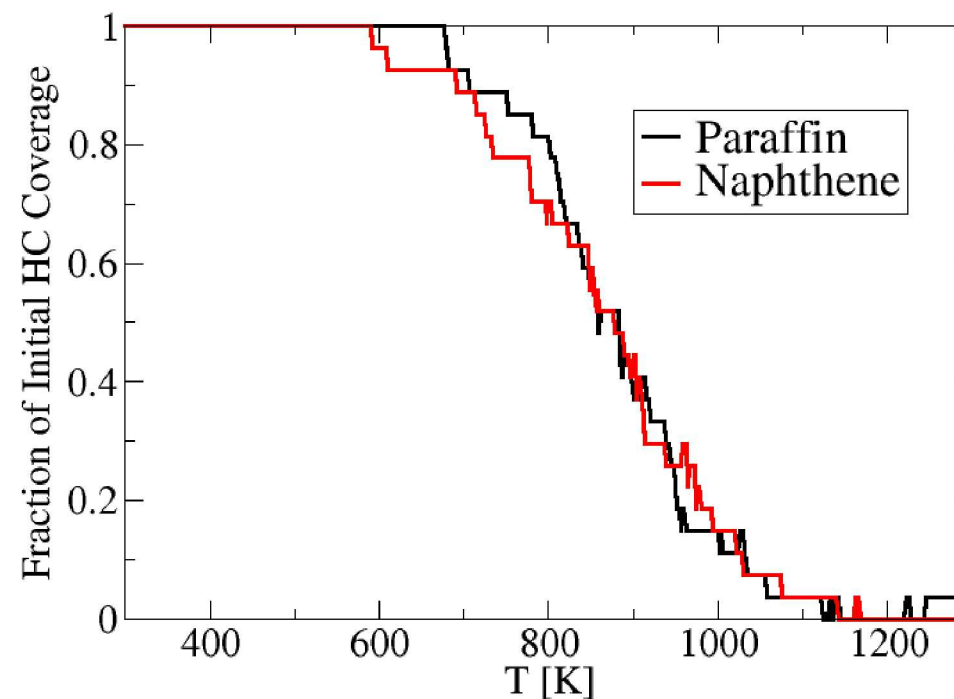


Paraffin



Naphthene

More realistic representation of
mineral oil found in Z-machine



Ramp Rate: 2000K/ns

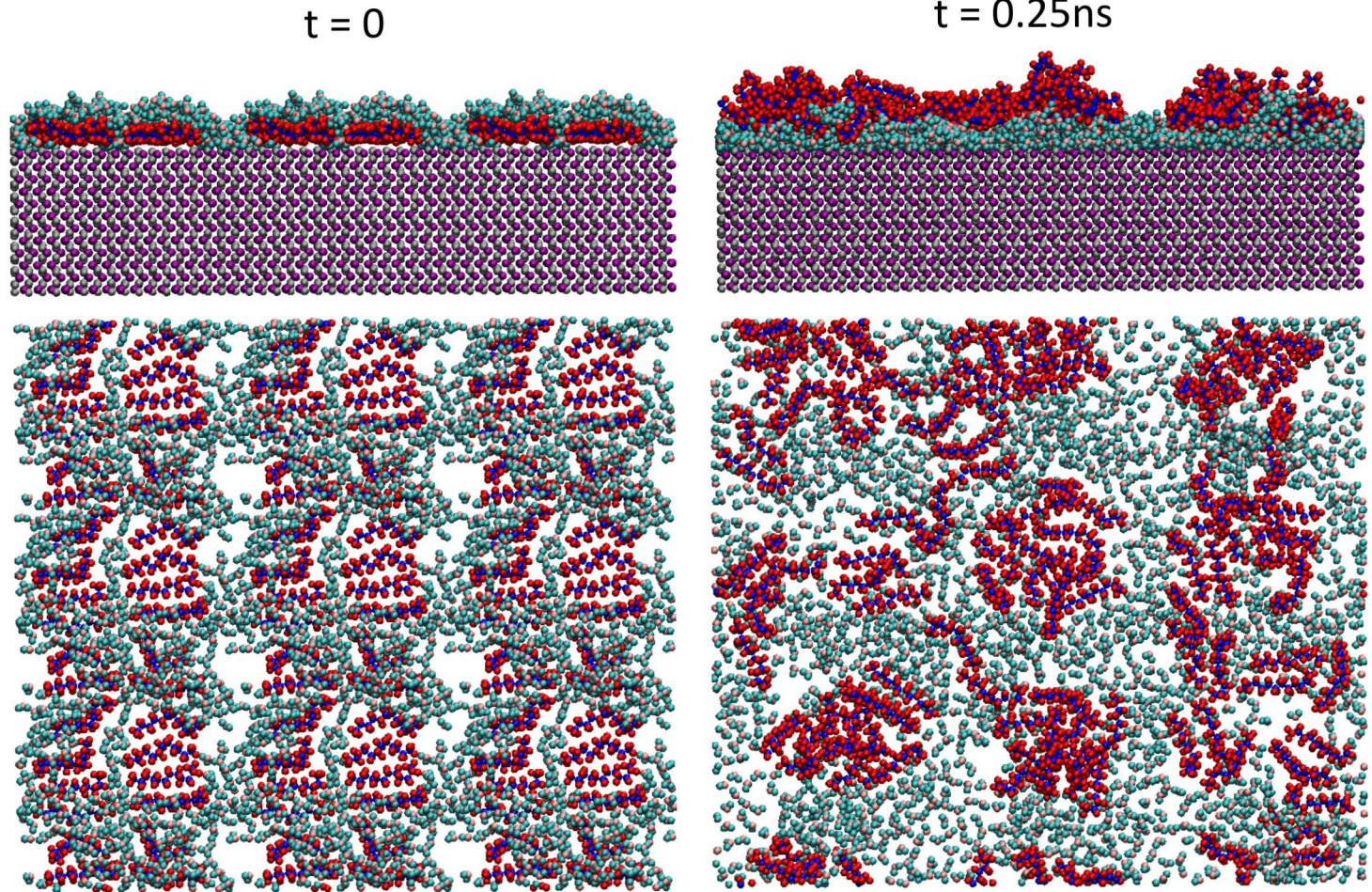
648 Carbons Initially on Surface

- $n_{\text{chains}} = \{27 \text{ C}_{24}\text{H}_{50} \text{ paraffin chains}, 27 \text{ C}_{24}\text{H}_{48} \text{ naphthene chains}\}$

Mixtures: Initialization

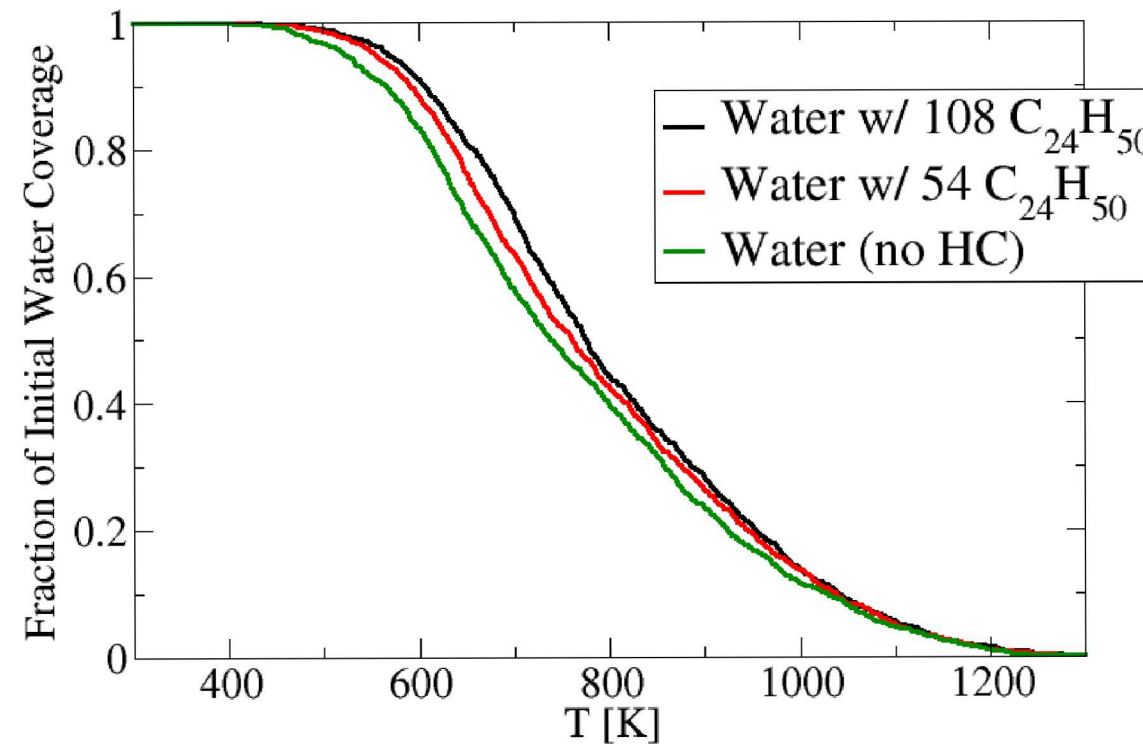
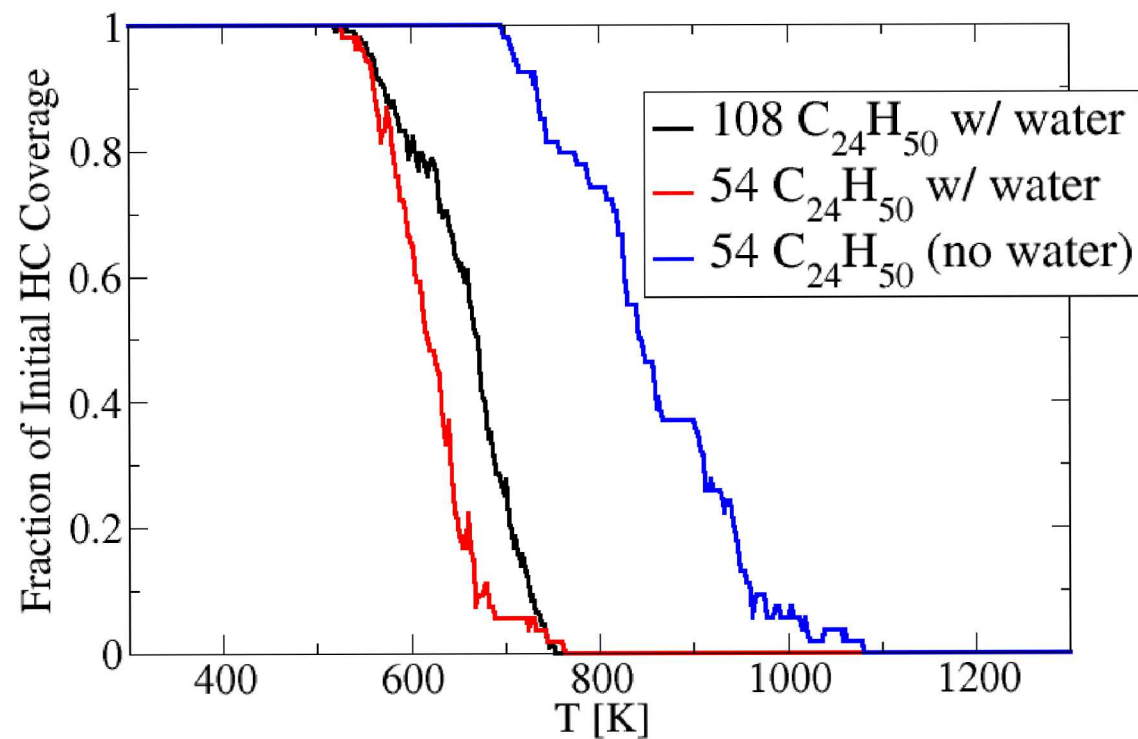
108 $C_{12}H_{26}$ chains (red/blue) / 192 water (pink/cyan) molecule mixture. Water is initially placed on top of the hydrocarbons at $T = 100K$. Simulation is ramped from 100K to 300K over the course of 0.25ns.

- The water moves to the surface causing the **hydrocarbons** to **lift off** the surface and sit atop the water.
- Hydrocarbons begin to phase separate from the water and form **rafts**.
- This simulation indicates the **water's propensity to sit at the surface** compared to the hydrocarbons is very **strong**

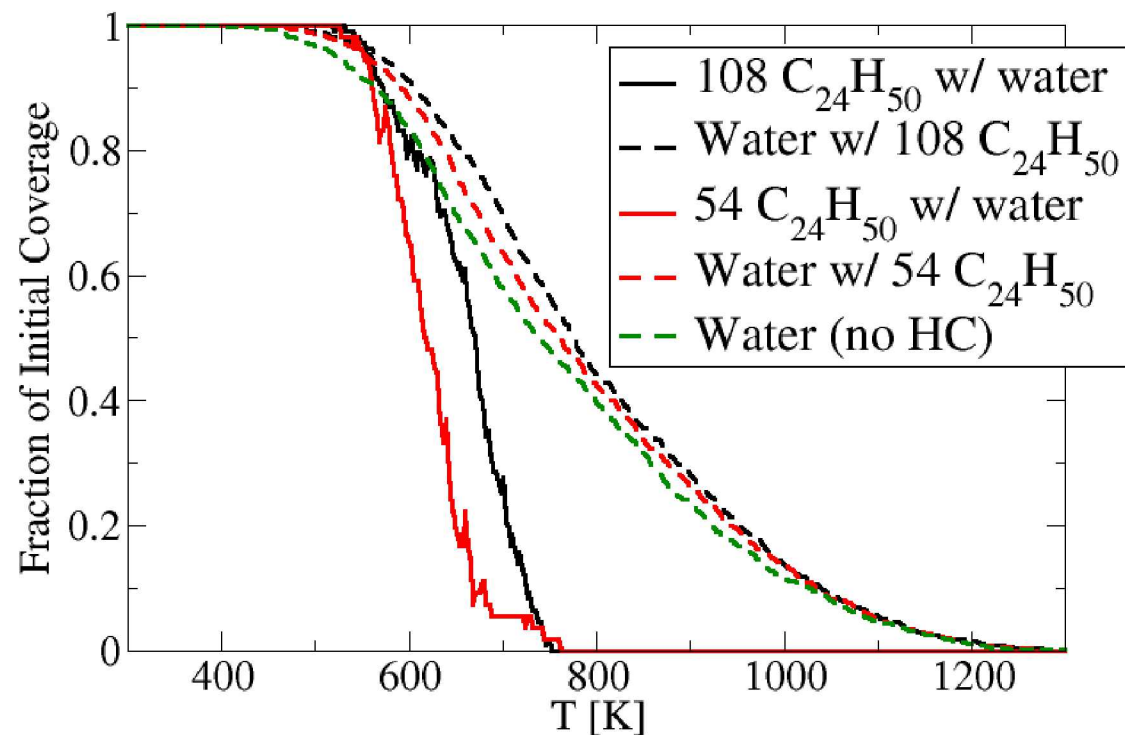


Top Row: Side view of substrate. Bottom Row: Bird's-eye view

Mixtures: Varying hydrocarbon concentration



Mixtures: Varying hydrocarbon concentration



When 50% of water has desorbed:

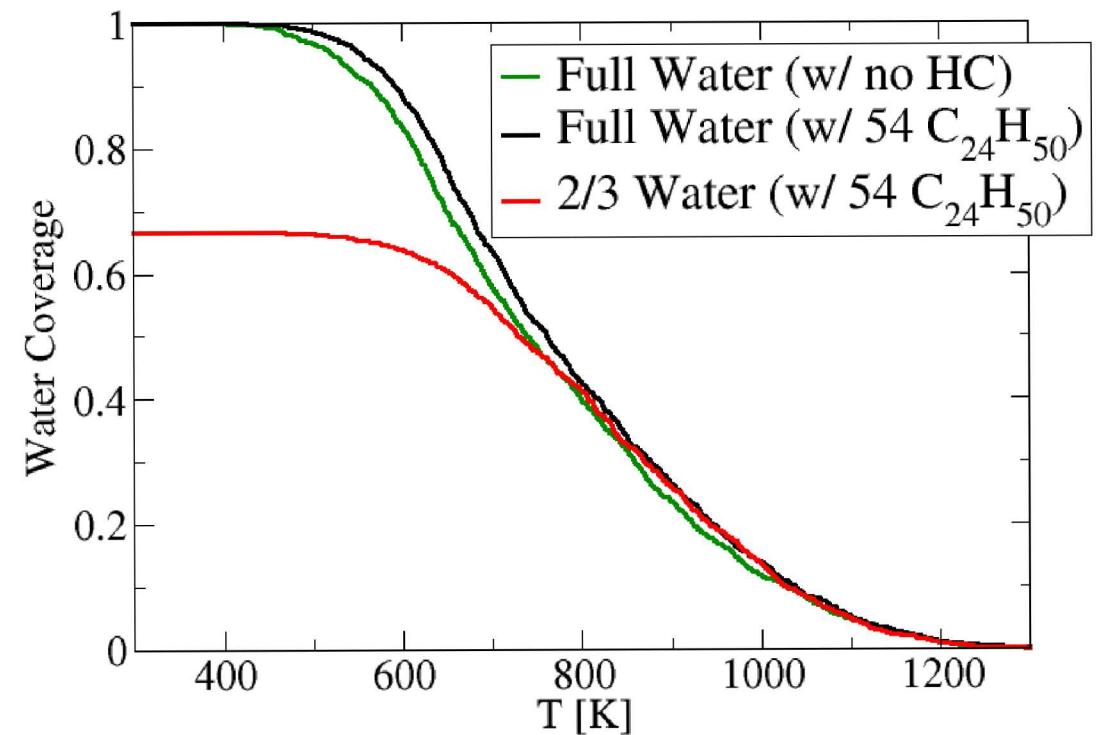
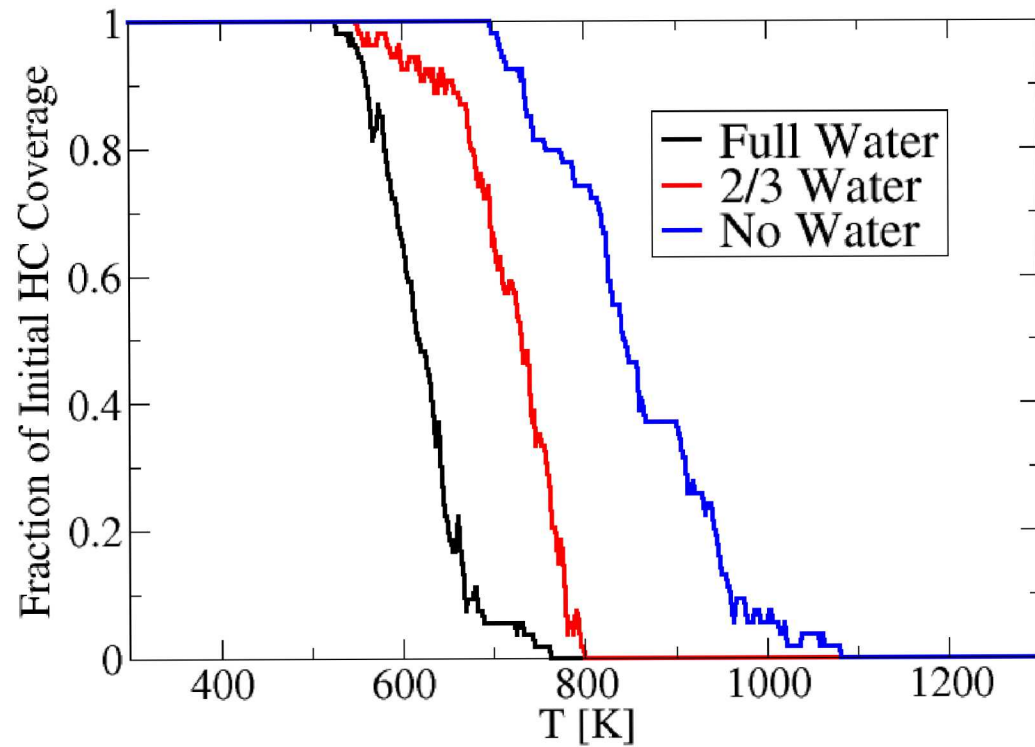
No HC: 738K

“Low” HC concentration: 761K (~3.1% increase)

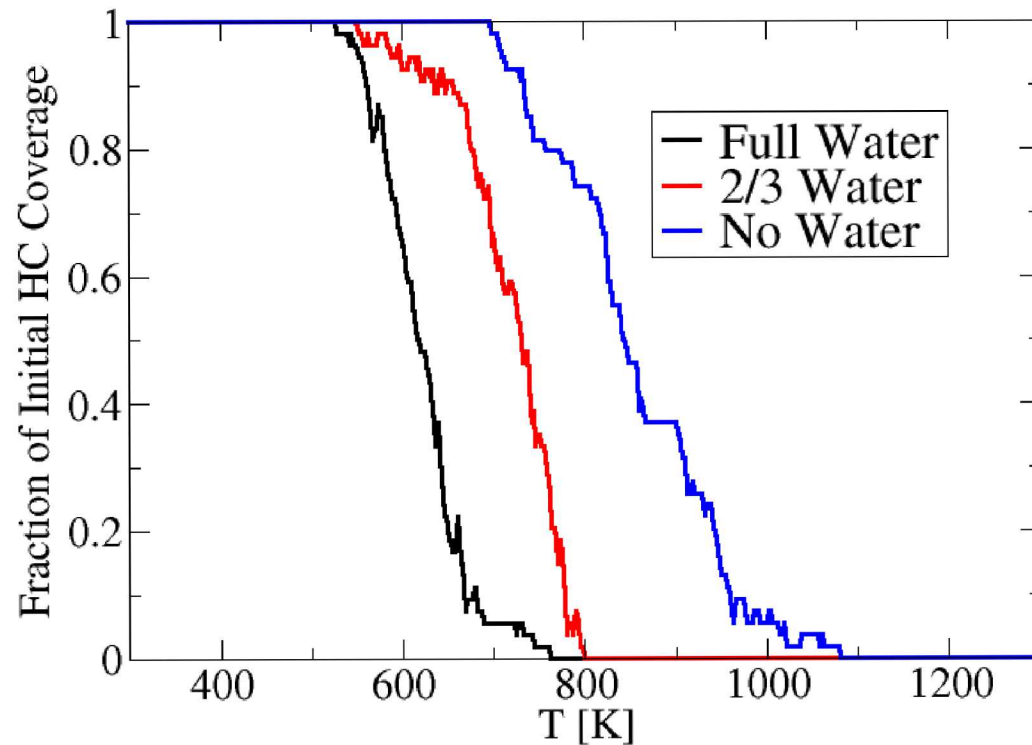
“High” HC concentration: 776K (~5.1% increase)

Increasing the hydrocarbon concentration/coverage on top of the water increases the desorption temperature

Mixtures: Varying water concentration



Mixtures: Varying water concentration



When 50% of hydrocarbon has desorbed:

No water: 843K

2/3 water coverage: 730K (~13.4% decrease)

Full water coverage: 617K (~26.8% decrease)

Increasing the water concentration/coverage on beneath the hydrocarbons decreases the desorption temperature

Conclusions: How Hydrocarbons affect desorption

Chain Length

- Longer hydrocarbons desorb slower than short hydrocarbons
- Supported by longer hydrocarbons having a higher desorption energy

Chain Architecture

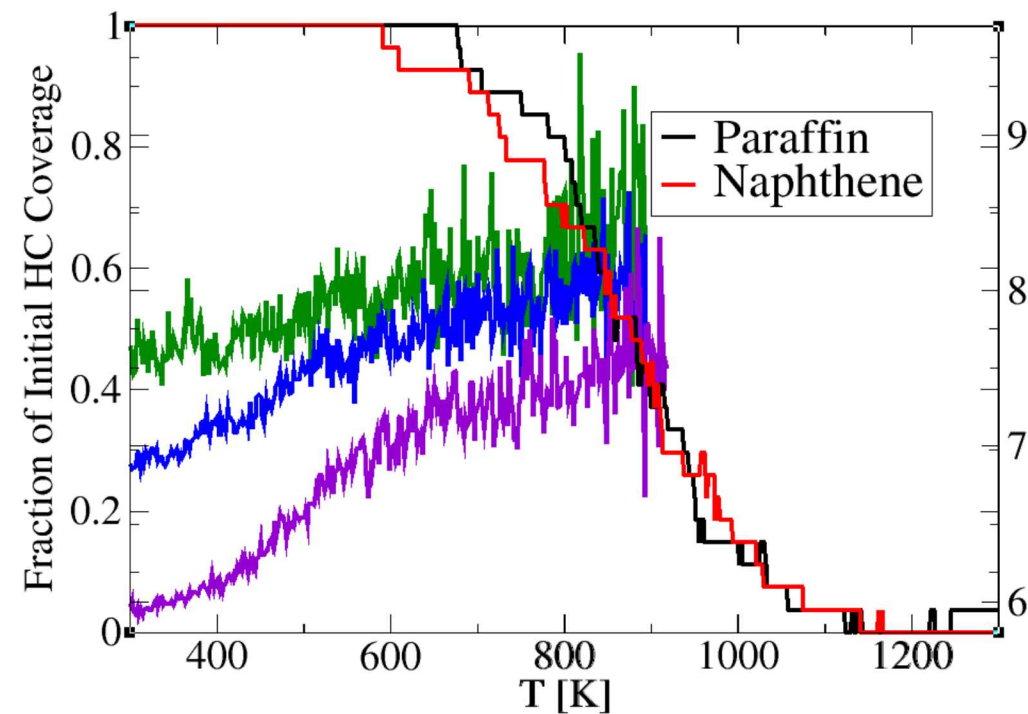
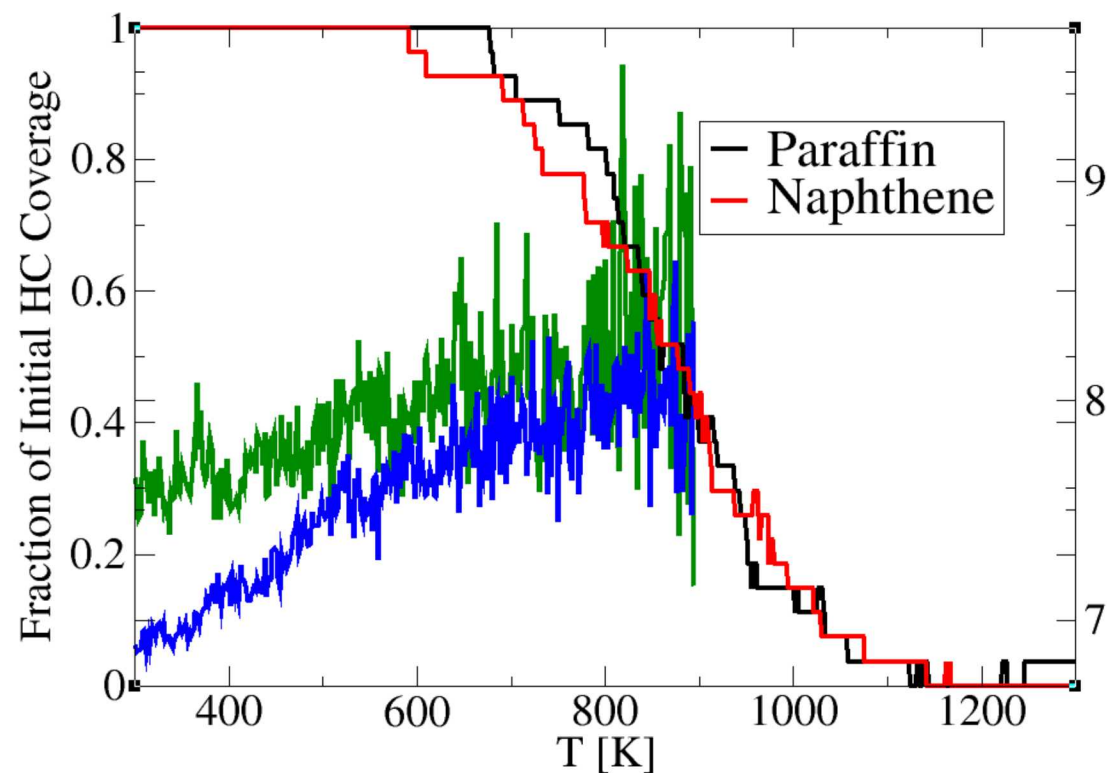
- C24 Naphthene and C24 Paraffin have similar desorption profiles
- Additional statistics and characterization of binding energy are necessary to further conclude any difference in the desorption as a function of chain architecture

Mixtures

- Hydrocarbons are observed to sit on top of water due to water having a higher desorption energy/area than hydrocarbons
- Increasing the hydrocarbon concentration/coverage while keeping the water coverage the same increases the water desorption temperature (~ 3%-5% for coverages tested)
- Increasing the water concentration/coverage while keeping the number of hydrocarbons constant decreases the hydrocarbon desorption temperature (up to ~27% for full water coverage)

Supplementary Slides

Green: Carbons in cyclohexane (naphthene)
 Blue: Carbons in backbone (naphthene)
 Purple: Carbons (paraffin)

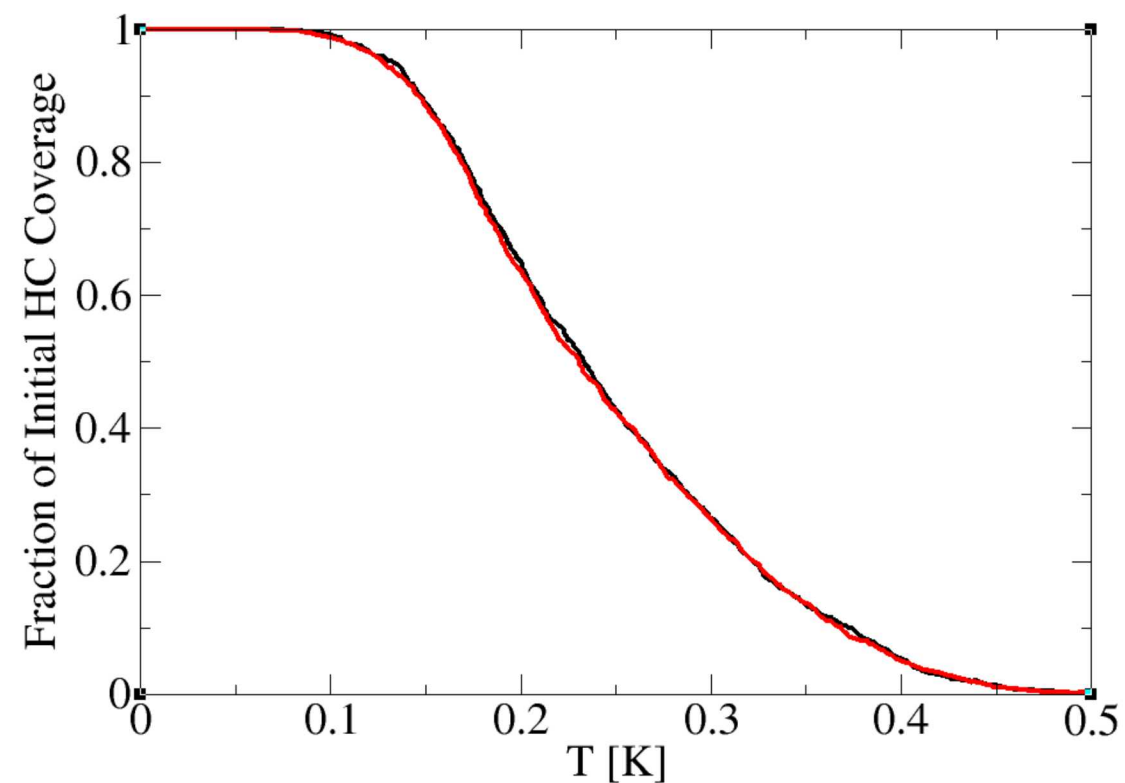


The right y-axis is height in Angstroms. Note the two y-axis are on slightly different scales

Water desorption from full monolayer

Black: Starting from initial ramp (100K to 300K, not equilibrated at 300K, so most chains laying flat)

Red: Equilibrated at 300K initially for > 1ns



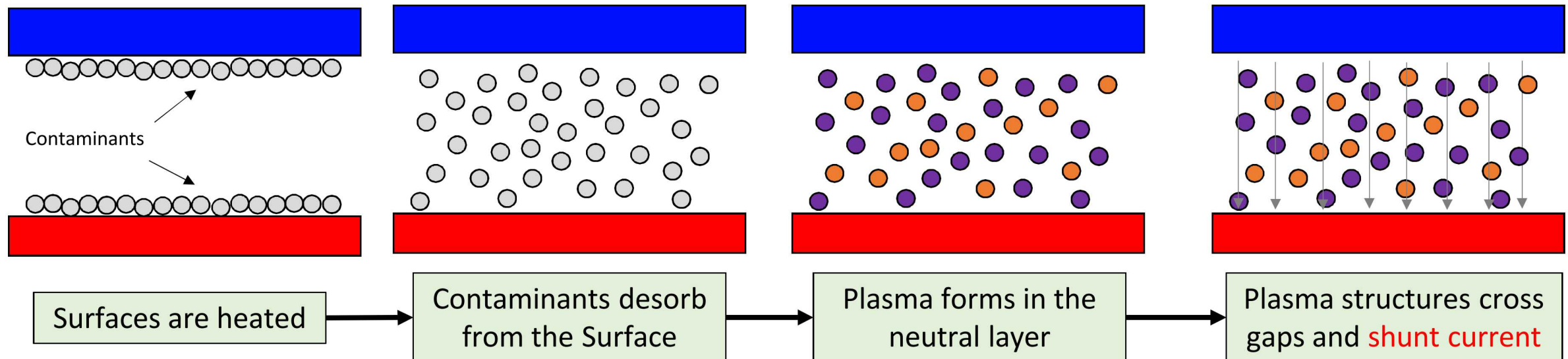
Current Understanding of Plasma Formation on Z

Accurate understanding of contaminant composition and **desorption processes** are necessary to inform plasma codes

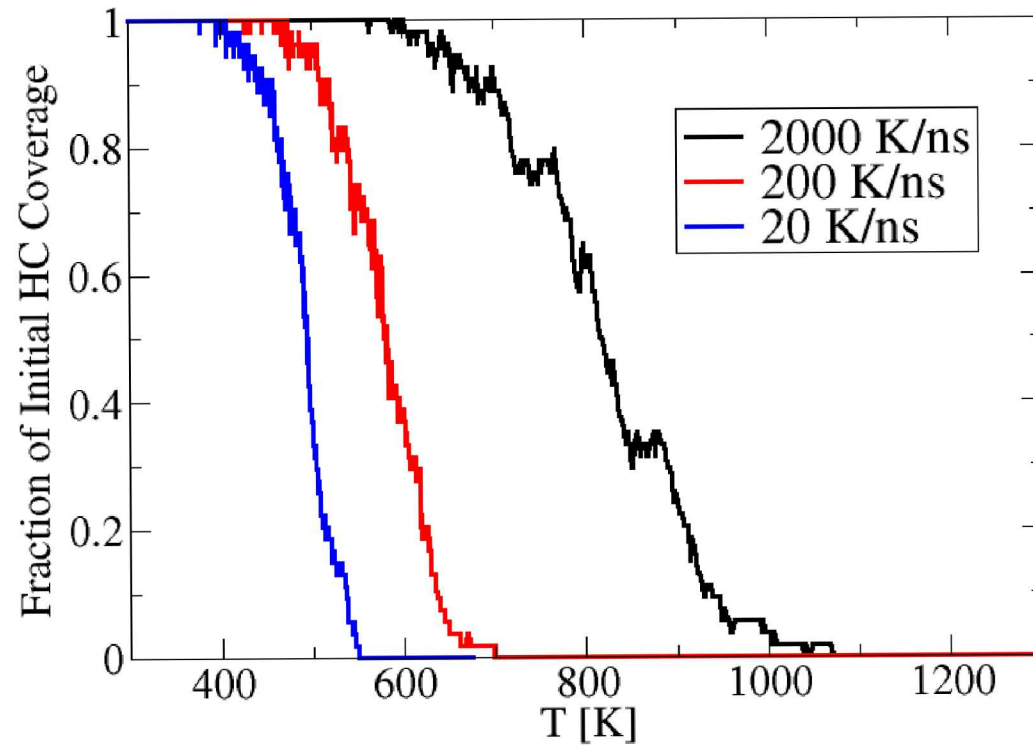
Plasma modeling/codes

- Large investment to predict power flow phenomena
- Rely on **boundary conditions** at electrode boundary

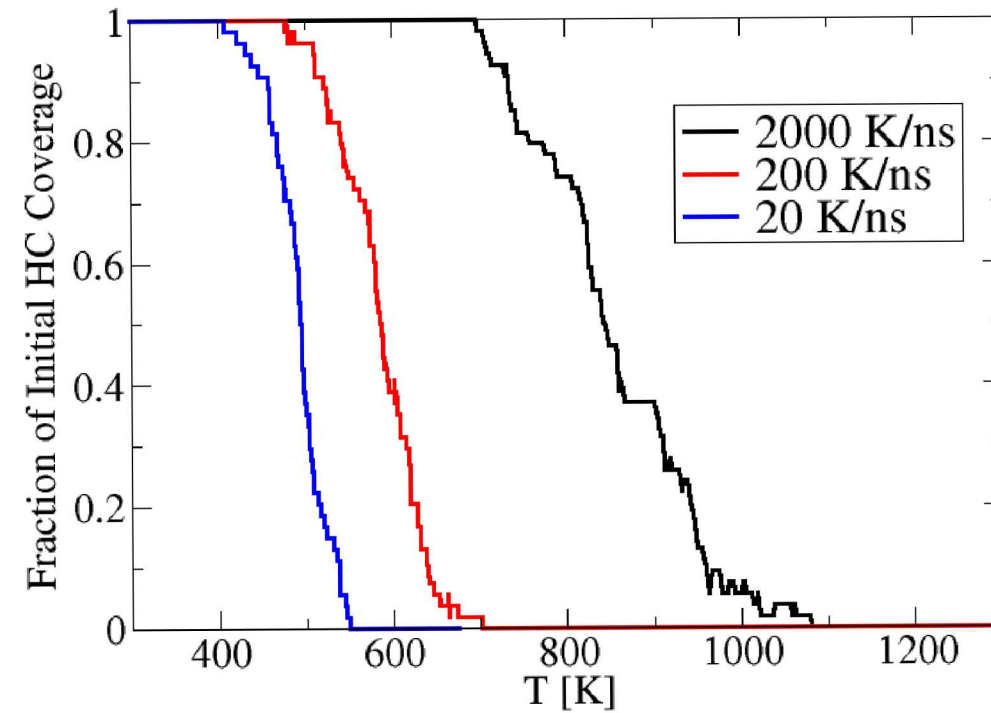
Evidence of hydrocarbons and will affect desorption composition and rates

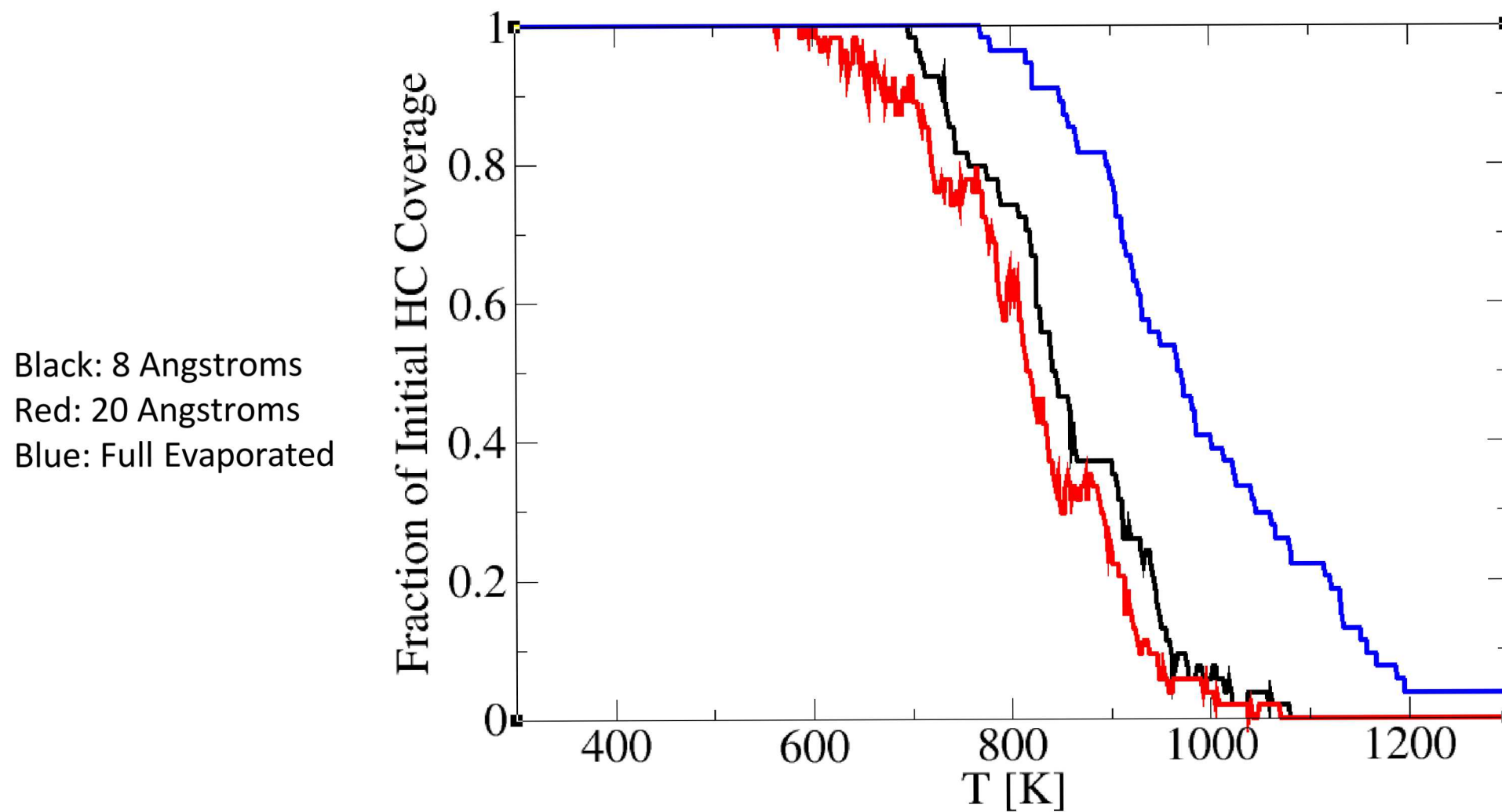


8 Angstroms

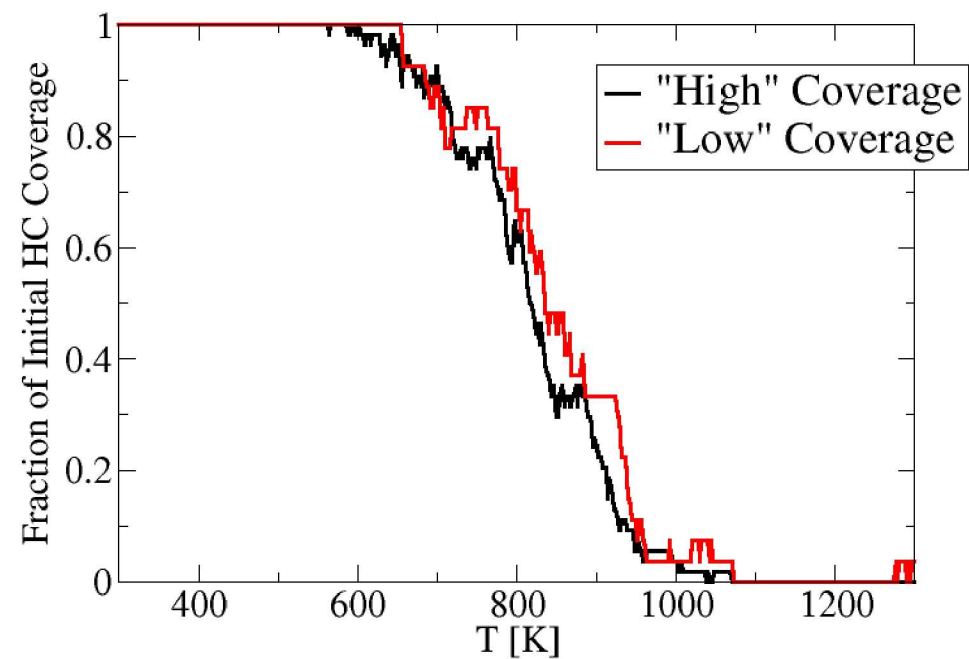


20 Angstroms

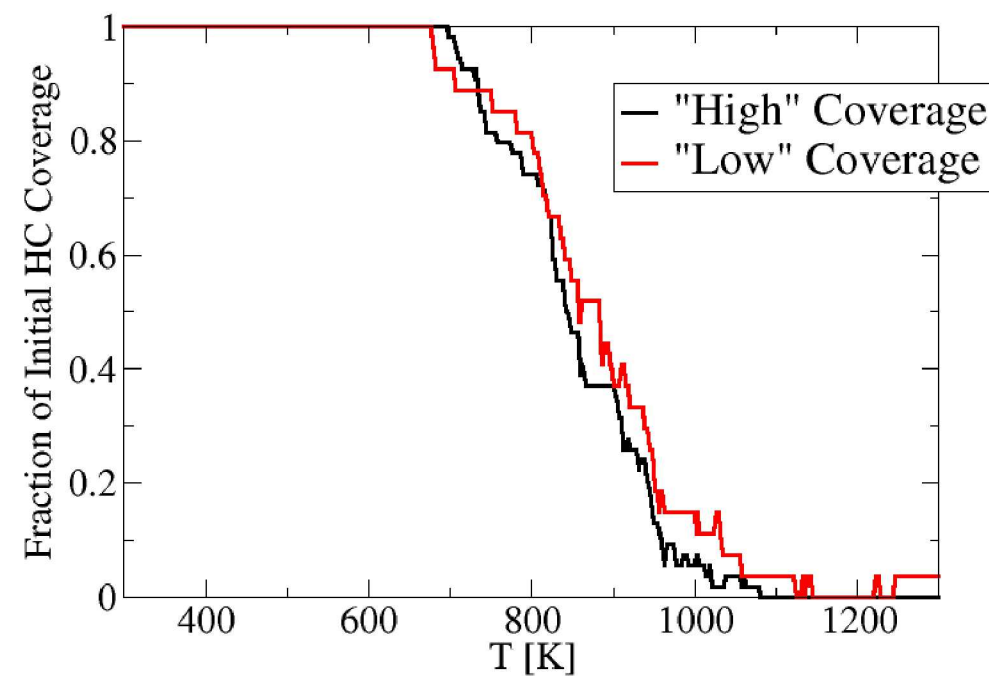


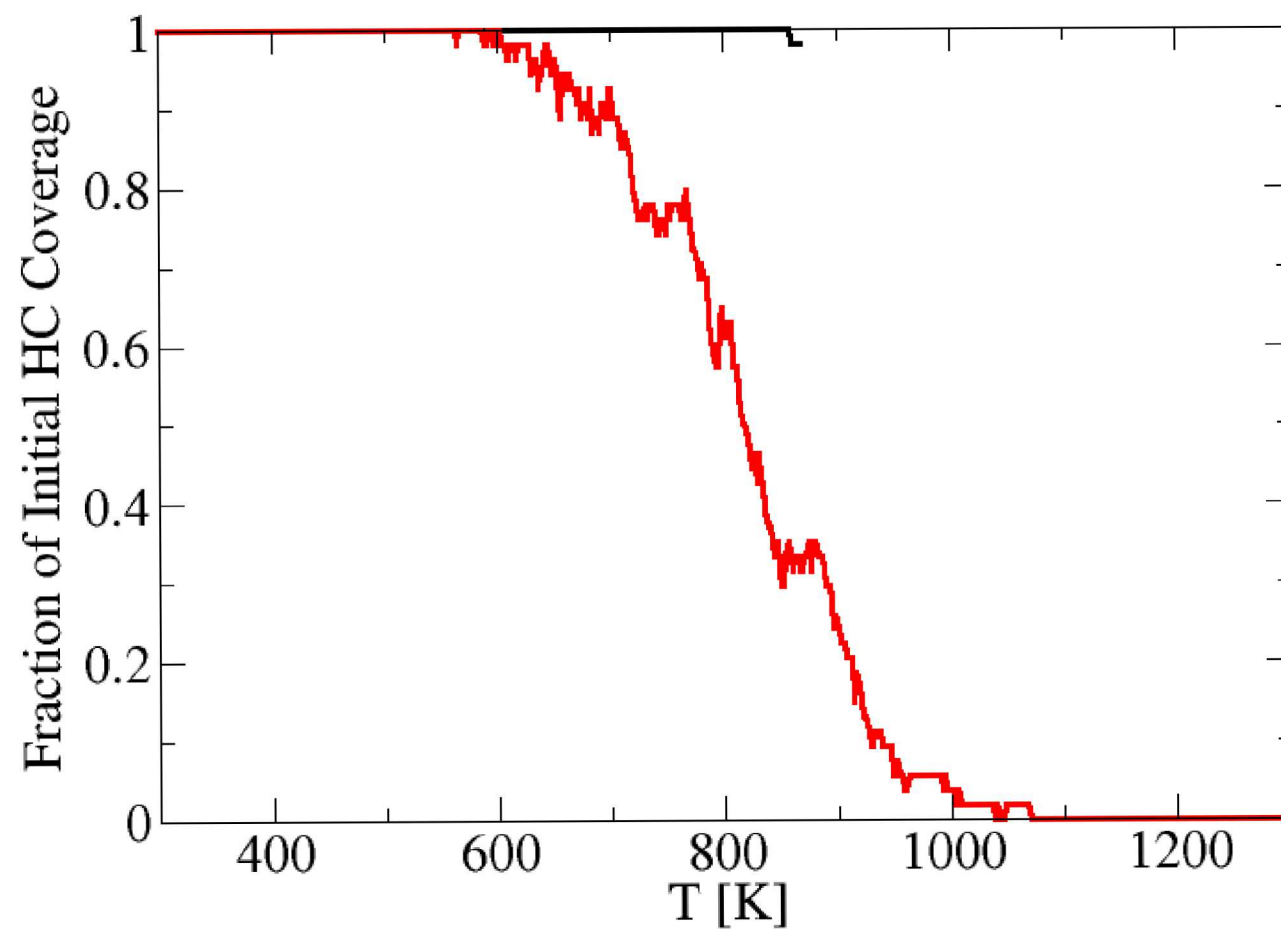


8 Angstroms



20 Angstroms





Binding Energies:

Non-React. ~ -1.055 eV

ReaxFF Oxide \rightarrow React. ~ -1.824 eV

Details of Desorption Modeling

Desorption Modeling

Previous Work (Non-Reactive MD):

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- SPC Water
- **OPLS Hydrocarbons**

Reactive MD (ReaxFF)

$$E_{\text{system}} = E_{\text{bond}} + E_{\text{over}} + E_{\text{under}} + E_{\text{val}} + E_{\text{pen}} + E_{\text{tors}} + E_{\text{conj}} + E_{\text{vdWaals}} + E_{\text{Coulomb}}$$

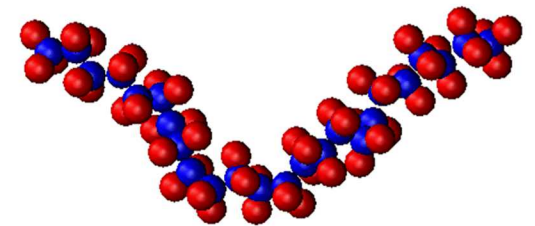
- Allows bond-breaking/reactivity
- “Oxide” force-field (Aryanpour [2010])
- Electrostatic energy

$$E(\mathbf{q}) = \sum_{i=1}^N \left[\chi_i q_i + \eta_i q_i^2 + \text{Tap}(r_{ij}) k_c \frac{q_i q_j}{(r_{ij}^3 + \gamma_{ij}^{-3})^{1/3}} \right]$$

- At each timestep, charges are adjusted to minimize energy

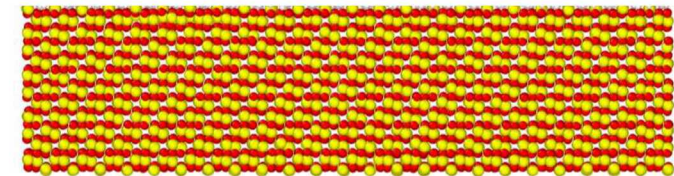
New Study focusing on:

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- Chain architecture
- Mixtures



Hydrocarbon (ex. $\text{C}_{24}\text{H}_{50}$)

$\alpha\text{-Fe}_2\text{O}_3$ hematite (0001)



Side view of substrate