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# CODE-VERIFICATION TECHNIQUES FOR HYPERSONIC REACTING FLOWS IN THERMOCHEMICAL NONEQUILIBRIUM

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# Outline

- Introduction
- Governing Equations
- Verification Techniques for Spatial Accuracy
- Spatial-Discretization Verification Results
- Verification Techniques for Thermochemical Source Term
- Thermochemical-Source-Term Verification Results
- Summary

# Outline

- Introduction
  - Hypersonic Flow
  - Sandia Parallel Aerodynamics and Reentry Code (**SPARC**)
  - Verification and Validation
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## Hypersonic Flow

## Hypersonic flows and underlying aerothermochemical phenomena

- Important in design & analysis of vehicles exiting/reentering atmosphere
- High flow velocities and stagnation enthalpies
  - Induce chemical reactions
  - Excite thermal energy modes
- Aerodynamic and thermochemical models require full coupling

## Sandia Parallel Aerodynamics and Reentry Code (SPARC)

Sandia Parallel Aerodynamics and Reentry Code (SPARC)

- Under development at Sandia National Laboratories
- Compressible computational fluids dynamics code
- Models transonic and hypersonic reacting turbulent flows
- Solves transient heat equation and equations associated with decomposing and non-decomposing ablators
- One- and two-way couplings between fluid-dynamics and ablation solvers

## Verification and Validation

Credibility of computational physics codes requires verification and validation.

- **Validation** assesses how well models represent physical phenomena
  - Computational results are compared with experimental results
  - Assess suitability of models, model error, and bounds of validity
- **Verification** assesses accuracy of numerical solutions against expectations
  - *Solution verification* estimates numerical error for particular solution
  - *Code verification* verifies correctness of numerical-method implementation

## Code Verification

Code verification is focus of this work

- Governing equations are numerically discretized
  - Discretization error is introduced in solution
- Seek to verify discretization error decreases with refinement of discretization
  - Should decrease at an expected rate
- Use manufactured and exact solutions to compute error

# Code Verification

Code verification demonstrated in many computational physics disciplines

- Fluid dynamics
- Multiphase flows
- Fluid-structure interaction
- Solid mechanics
- Electrodynamics
- Radiation hydrodynamics
- Heat transfer
- Electromagnetism

Code-verification techniques for hypersonic flows have been presented

- Single-species perfect gas
- Multi-species gas in thermal equilibrium

We present code-verification techniques for hypersonic reacting flows in thermochemical **nonequilibrium** and demonstrate effectiveness

- Spatial discretization
- Thermochemical source term

# Outline

- Introduction
- Governing Equations
  - Conserved Quantities
  - Vibrational Energy
  - Translational–Vibrational Energy Exchange
  - Chemical Kinetics
  - Scope of Code Verification
- Verification Techniques for Spatial Accuracy
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Governing Equations:  $n_s$  Species in Vibrational Nonequilibrium

Conservation of mass, momentum, and energy:

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} \mathbf{0} \\ p \mathbf{I} \\ p \mathbf{v}^T \\ \mathbf{0} \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \boldsymbol{\tau} \\ (\boldsymbol{\tau} \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

$$\mathbf{S}(\mathbf{U}) = \begin{Bmatrix} \dot{\mathbf{w}} \\ \mathbf{0} \\ \mathbf{0} \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, \quad \begin{aligned} \rho &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \rho &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R} T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

Governing Equations:  $n_s$  Species in Vibrational Nonequilibrium

Conservation of mass, momentum, and energy:

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

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Multiple species

$$\begin{aligned} \boldsymbol{\rho} &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \mathbf{S}(\mathbf{U}) &= \begin{Bmatrix} \dot{\mathbf{w}} \\ 0 \\ 0 \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, & \boldsymbol{\rho} &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ & & p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R} T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ & & & & Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

# Governing Equations: $n_s$ Species in Vibrational Nonequilibrium

Conservation of mass, momentum, and energy:

Local time derivative

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} 0 \\ p \mathbf{I} \\ p \mathbf{v}^T \\ 0 \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \tau \\ (\tau \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

$$\mathbf{S}(\mathbf{U}) = \begin{Bmatrix} \dot{\mathbf{w}} \\ 0 \\ 0 \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, \quad \begin{aligned} \rho &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \rho &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R} T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

# Governing Equations: $n_s$ Species in Vibrational Nonequilibrium

Conservation of mass, momentum, and energy:

Convective flux gradient

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} 0 \\ p \mathbf{I} \\ p \mathbf{v}^T \\ 0 \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \tau \\ (\tau \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

$$\mathbf{S}(\mathbf{U}) = \begin{Bmatrix} \dot{\mathbf{w}} \\ 0 \\ 0 \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, \quad \begin{aligned} \rho &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \rho &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R} T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

Governing Equations:  $n_s$  Species in Vibrational Nonequilibrium

Conservation of mass, momentum, and energy:

Pressure flux gradient

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} \mathbf{0} \\ p \mathbf{I} \\ p \mathbf{v}^T \\ \mathbf{0} \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \tau \\ (\tau \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

$$\mathbf{S}(\mathbf{U}) = \begin{Bmatrix} \dot{\mathbf{w}} \\ \mathbf{0} \\ \mathbf{0} \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, \quad \begin{aligned} \rho &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \rho &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R} T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

Governing Equations:  $n_s$  Species in Vibrational Nonequilibrium

Conservation of mass, momentum, and energy:

Diffusive flux gradient

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} 0 \\ p \mathbf{I} \\ p \mathbf{v}^T \\ 0 \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \boldsymbol{\tau} \\ (\boldsymbol{\tau} \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

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$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

Governing Equations:  $n_s$  Species in Vibrational Nonequilibrium

Conservation of mass, momentum, and energy:

Thermochemical source term

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} 0 \\ p \mathbf{I} \\ p \mathbf{v}^T \\ 0 \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \tau \\ (\tau \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

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$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

# Vibrational Energy

Mixture vibrational energy per mass:

$$e_v = \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s},$$

where

$$e_{v_s} = \begin{cases} \sum_{m=1}^{n_{v_s}} e_{v_{s,m}}(T_v) & \text{for molecules,} \\ 0 & \text{for atoms,} \end{cases}$$

and

$$e_{v_{s,m}}(T') = \frac{\bar{R}}{M_s} \frac{\theta_{v_{s,m}}}{\exp(\theta_{v_{s,m}}/T') - 1}$$

$n_{v_s}$ : number of vibrational modes of species  $s$  ( $n_{v_s} = 0$  for atoms)

$\theta_{v_{s,m}}$ : characteristic vibrational temperature of mode  $m$  of species  $s$

# Translational–Vibrational Energy Exchange

Landau–Teller model:

$$Q_{t-v} = \sum_{s=1}^{n_s} \rho_s \sum_{m=1}^{n_{v_s}} \frac{e_{v_{s,m}}(T) - e_{v_{s,m}}(T_v)}{\langle \tau_{s,m} \rangle}$$

Translational–vibrational energy relaxation time for mode  $m$  of species  $s$ :

$$\langle \tau_{s,m} \rangle = \left( \sum_{s'=1}^{n_s} \frac{y_{s'}}{\tau_{s,m,s'}} \right)^{-1} + \left[ \left( N_A \sum_{s'=1}^{n_s} \frac{\rho_{s'}}{M_{s'}} \right) \sigma_{v_s} \sqrt{\frac{8 \bar{R} T}{\pi M_s}} \right]^{-1},$$

where

$$y_s = \frac{\rho_s/M_s}{\sum_{s'=1}^{n_s} \rho_{s'}/M_{s'}}, \quad \tau_{s,m,s'} = \frac{\exp [a_{s,m,s'} (T^{-1/3} - b_{s,m,s'}) - 18.42]}{p'}, \quad \sigma_{v_s} = \sigma'_{v_s} \left( \frac{50,000 \text{ K}}{T} \right)^2$$

$p'$ : pressure in atmospheres.

$a_{s,m,s'}$  and  $b_{s,m,s'}$ : vibrational constants for mode  $m$  of species  $s$  with colliding species  $s'$

$N_A$ : Avogadro constant

$\sigma_{v_s}$ : collision-limiting vibrational cross section

$\sigma'_{v_s}$ : collision-limiting vibrational cross section at 50,000 K.

# Chemical Kinetics

Mass production rate per volume for species  $s$ :

$$\dot{w}_s = M_s \sum_{r=1}^{n_r} (\beta_{s,r} - \alpha_{s,r}) (R_{f_r} - R_{b_r})$$

Forward and backward reaction rates for reaction  $r$ :

$$R_{f_r} = \gamma k_{f_r} \prod_{s=1}^{n_s} \left( \frac{1}{\gamma} \frac{\rho_s}{M_s} \right)^{\alpha_{s,r}} \quad \text{and} \quad R_{b_r} = \gamma k_{b_r} \prod_{s=1}^{n_s} \left( \frac{1}{\gamma} \frac{\rho_s}{M_s} \right)^{\beta_{s,r}}$$

Forward and backward reaction rate coefficients:

$$k_{f_r}(T_c) = C_{f_r} T_c^{\eta_r} \exp(-\theta_r/T_c) \quad \text{and} \quad k_{b_r}(T) = \frac{k_{f_r}(T)}{K_{e_r}(T)}$$

Equilibrium constant for reaction  $r$ :

$$K_{e_r}(T) = \exp \left[ A_{1_r} \left( \frac{T}{10000} \right) + A_{2_r} + A_{3_r} \ln \left( \frac{10000}{T} \right) + A_{4_r} \frac{10000}{T} + A_{5_r} \left( \frac{10000}{T} \right)^2 \right]$$

$\alpha_{s,r}$  and  $\beta_{s,r}$ : stoichiometric coefficients for species  $s$  in reaction  $r$

$\gamma$ : unit conversion factor

$C_{f_r}$ ,  $\eta_r$ ,  $A_{i_r}$ : empirical parameters

$\theta_r$ : activation energy of reaction  $r$ , divided by Boltzmann constant

$T_c$ : rate-controlling temperature ( $T_c = \sqrt{TT_v}$  for dissociation,  $T_c = T$  for exchange)

# Scope of Code Verification

Conservation of mass, momentum, and energy:

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} \mathbf{0} \\ p \mathbf{I} \\ p \mathbf{v}^T \\ \mathbf{0} \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \boldsymbol{\tau} \\ (\boldsymbol{\tau} \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

$$\mathbf{S}(\mathbf{U}) = \begin{Bmatrix} \dot{\mathbf{w}} \\ \mathbf{0} \\ 0 \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, \quad \begin{aligned} \rho &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \rho &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R}T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

# Scope of Code Verification

Conservation of mass, momentum, and energy:

Non-diffusive flux gradients

Thermochemical source term

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} 0 \\ p \mathbf{I} \\ p \mathbf{v}^T \\ 0 \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \tau \\ (\tau \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

$$\mathbf{S}(\mathbf{U}) = \begin{Bmatrix} \dot{\mathbf{w}} \\ 0 \\ 0 \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, \quad \begin{aligned} \rho &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \rho &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R} T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

$$E = \frac{|\mathbf{v}|^2}{2} + \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} (c_{v_s} T + e_{v_s} + h_s^o)$$

# Scope of Code Verification

Conservation of mass, momentum, and energy:

Non-diffusive flux gradients

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

Spatial discretization

$$\mathbf{U} = \begin{Bmatrix} \rho \\ \rho \mathbf{v} \\ \rho E \\ \rho e_v \end{Bmatrix}, \quad \mathbf{F}_c(\mathbf{U}) = \begin{Bmatrix} \rho \mathbf{v}^T \\ \rho \mathbf{v} \mathbf{v}^T \\ \rho E \mathbf{v}^T \\ \rho e_v \mathbf{v}^T \end{Bmatrix}, \quad \mathbf{F}_p(\mathbf{U}) = \begin{Bmatrix} \mathbf{0} \\ p \mathbf{I} \\ p \mathbf{v}^T \\ \mathbf{0} \end{Bmatrix}, \quad \mathbf{F}_d(\mathbf{U}) = \begin{Bmatrix} -\mathbf{J} \\ \tau \\ (\tau \mathbf{v} - \mathbf{q} - \mathbf{q}_v - \mathbf{J}^T \mathbf{h})^T \\ (-\mathbf{q}_v - \mathbf{J}^T \mathbf{e}_v)^T \end{Bmatrix},$$

$$\mathbf{S}(\mathbf{U}) = \begin{Bmatrix} \dot{\mathbf{w}} \\ \mathbf{0} \\ \mathbf{0} \\ Q_{t-v} + \mathbf{e}_v^T \dot{\mathbf{w}} \end{Bmatrix}, \quad \begin{aligned} \rho &= \{\rho_1, \dots, \rho_{n_s}\}^T, & \dot{\mathbf{w}} &= \{\dot{w}_1, \dots, \dot{w}_{n_s}\}^T: \text{mass production rates per volume,} \\ \rho &= \sum_{s=1}^{n_s} \rho_s, & e_v &= \sum_{s=1}^{n_s} \frac{\rho_s}{\rho} e_{v_s}: \text{mixture vibrational energy per mass,} \\ p &= \sum_{s=1}^{n_s} \frac{\rho_s}{M_s} \bar{R} T, & \mathbf{e}_v &= \{e_{v_1}, \dots, e_{v_{n_s}}\}^T: \text{vibrational energies per mass,} \\ Q_{t-v} &: \text{translational-vibrational energy exchange,} \end{aligned}$$

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# Scope of Code Verification

Conservation of mass, momentum, and energy:

Thermochemical source term

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}_c(\mathbf{U}) = -\nabla \cdot \mathbf{F}_p(\mathbf{U}) + \nabla \cdot \mathbf{F}_d(\mathbf{U}) + \mathbf{S}(\mathbf{U}),$$

where

Implementation

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# Outline

- Introduction
- Governing Equations
- Verification Techniques for Spatial Accuracy
  - Spatial Accuracy
  - Solutions
  - Error Norms
- Spatial-Discretization Verification Results
- Verification Techniques for Thermochemical Source Term
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### Spatial Accuracy (Steady State)

## Governing equations

$$\mathbf{r}(\mathbf{U}; \boldsymbol{\mu}) = \mathbf{0}$$

## Discretized equations

$$\tilde{\mathbf{r}}(\tilde{\mathbf{U}}; \boldsymbol{\mu}) = 0$$

For  $\tilde{p}$ <sup>th</sup>-order-accurate discretization, error is

$$\mathbf{e}(\mathbf{x}) = \tilde{\mathbf{U}}(\mathbf{x}) - \mathbf{U}(\mathbf{x}) = \mathbf{C}(\mathbf{x})h^{\tilde{p}(\mathbf{x})} + \mathcal{O}(h^{\tilde{p}(\mathbf{x})+1})$$

*h*: relative characterization of cell sizes

- Between meshes, with respect to one dimension
- Individual cell sizes may be non-uniform functions of  $h$
- Sufficiently fine meshes  $\rightarrow$  asymptotic region ( $h^{\tilde{p}(\mathbf{x})+1} \ll h^{\tilde{p}(\mathbf{x})}$ )

$$\mathbf{e}(\mathbf{x}) \approx \mathbf{C}(\mathbf{x})h^{\tilde{p}(\mathbf{x})}$$

**C(x):** function of derivative(s) of the state vector **U** at **x**

- Approximately constant between meshes in asymptotic region

## Order of Accuracy

Observed accuracy  $\tilde{p}(\mathbf{x})$  computed using 2 meshes:

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Coarser mesh ( $h$ )

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Coarser mesh ( $h$ )

$$e_1(\mathbf{x}) = C(\mathbf{x})h^{\tilde{p}(\mathbf{x})}$$

Finer mesh ( $h/q$ )  
( $q$ -times as fine in each dimension)

$$e_2(\mathbf{x}) = C(\mathbf{x})(h/q)^{\tilde{p}(\mathbf{x})}$$

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$\tilde{p}(\mathbf{x})$  is computed by

$$\tilde{p}(\mathbf{x}) = \frac{\log |e_1(\mathbf{x})/e_2(\mathbf{x})|}{\log q} = \log_q |e_1(\mathbf{x})/e_2(\mathbf{x})|$$

# Solutions

Need solution to compute error

# Solutions

## Exact Solutions

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  - Maximum error
  - Catches localized deviations (expected and **unexpected**)
- Without discontinuities, both norms should yield same  $p$

# Outline

- Introduction
- Governing Equations
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  - Single-Species Inviscid Flow in Thermochemical Equilibrium
  - Five-Species Inviscid Flow in Chemical Nonequilibrium
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## 1D Supersonic Flow using a Manufactured Solution

- One-dimensional domain:  $x \in [0, 1]$  m
- Boundary conditions:
  - Supersonic inflow ( $x = 0$  m)
  - Supersonic outflow ( $x = 1$  m)
- 5 uniform meshes: 50, 100, 200, 400, 800 elements
- Solution consists of small, smooth perturbations to uniform flow:

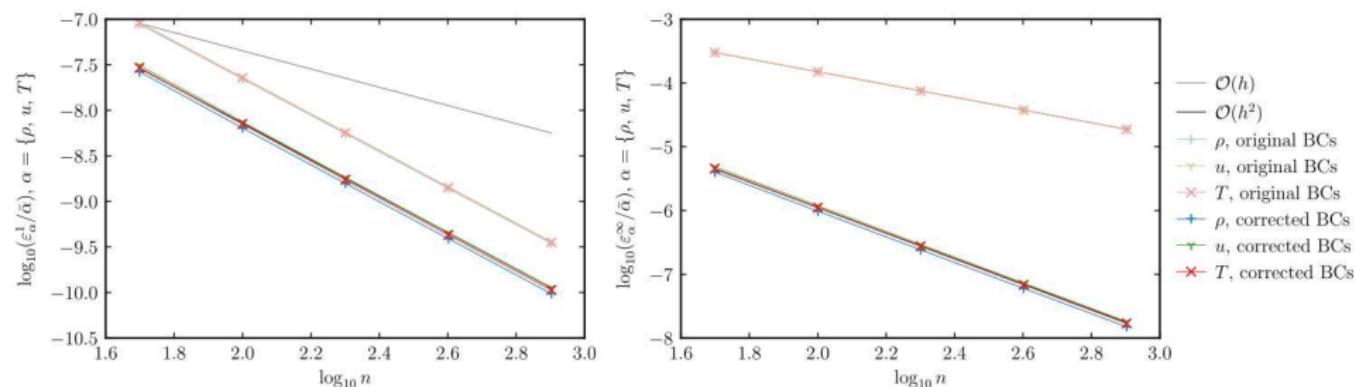
$$\rho(x) = \bar{\rho} [1 - \epsilon \sin(\pi x)],$$

$$u(x) = \bar{u} [1 - \epsilon \sin(\pi x)],$$

$$T(x) = \bar{T} [1 + \epsilon \sin(\pi x)],$$

$$\bar{\rho} = 1 \text{ kg/m}^3, \bar{T} = 300 \text{ K}, \bar{M} = 2.5, \epsilon = 0.05$$

## 1D Supersonic Flow using a Manufactured Solution



## First-order accurate

## Second-order accurate

Mesh	Original boundary conditions			Corrected boundary conditions		
	$\rho$	$u$	$T$	$\rho$	$u$	$T$
1–2	1.0008	1.0008	1.0008	2.0313	2.0362	2.0351
2–3	1.0002	1.0002	1.0002	2.0157	2.0184	2.0178
3–4	1.0001	1.0001	1.0000	2.0079	2.0093	2.0090
4–5	<b>1.0000</b>	<b>1.0000</b>	<b>1.0000</b>	<b>2.0040</b>	<b>2.0047</b>	<b>2.0045</b>

Observed accuracy  $p$  using  $L^{\infty}$ -norms of the error

## 2D Supersonic Flow using a Manufactured Solution

- Two-dimensional domain:  $(x, y) \in [0, 1] \text{ m} \times [0, 1] \text{ m}$
- Boundary conditions:
  - Supersonic inflow ( $x = 0 \text{ m}$ )
  - Supersonic outflow ( $x = 1 \text{ m}$ )
  - Slip wall (tangent flow) ( $y = 0 \text{ m}$  &  $y = 1 \text{ m}$ )
- 5 nonuniform meshes:  $25 \times 25 \rightarrow 400 \times 400$
- Solution consists of small, smooth perturbations to uniform flow:

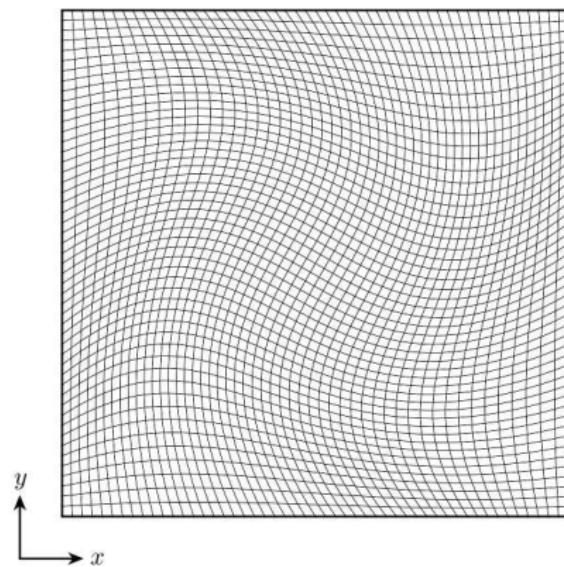
$$\rho(x, y) = \bar{\rho} [1 - \epsilon \sin(\frac{5}{4}\pi x) (\sin(\pi y) + \cos(\pi y))],$$

$$u(x, y) = \bar{u} [1 + \epsilon \sin(\frac{1}{4}\pi x) (\sin(\pi y) + \cos(\pi y))],$$

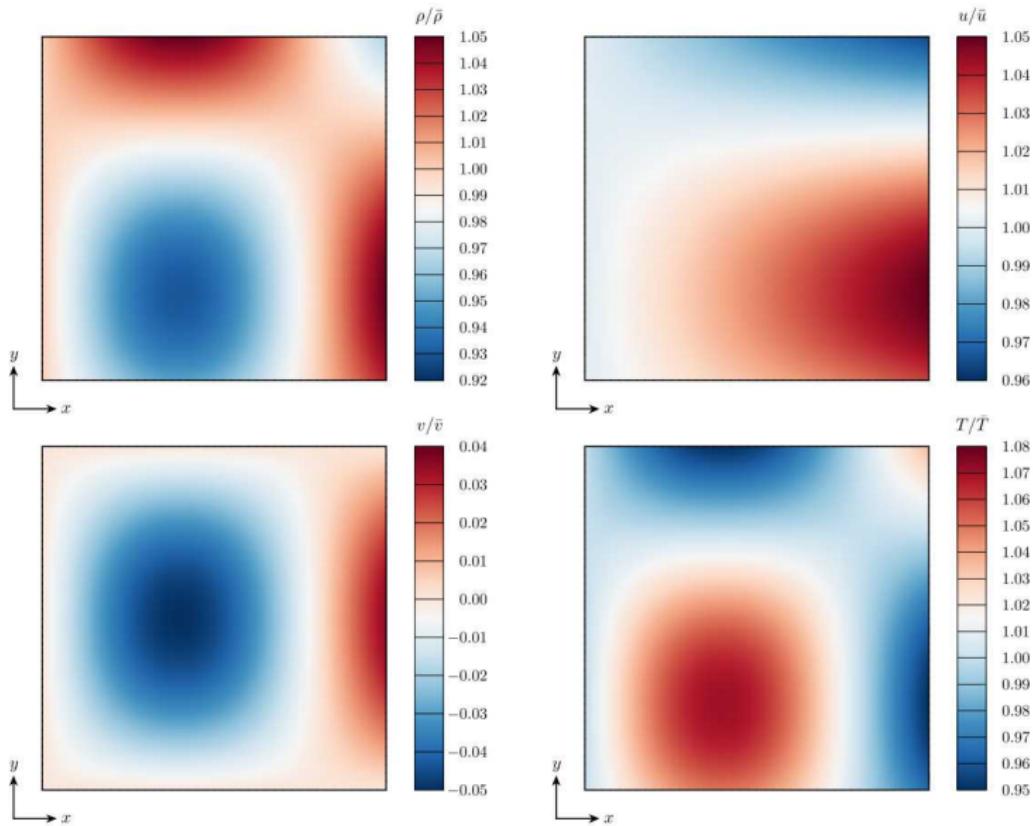
$$v(x, y) = \bar{v} [-\epsilon \sin(\frac{5}{4}\pi x) (\sin(\pi y) + \cos(\pi y))],$$

$$T(x, y) = \bar{T} [1 + \epsilon \sin(\frac{5}{4}\pi x) (\sin(\pi y) + \cos(\pi y))],$$

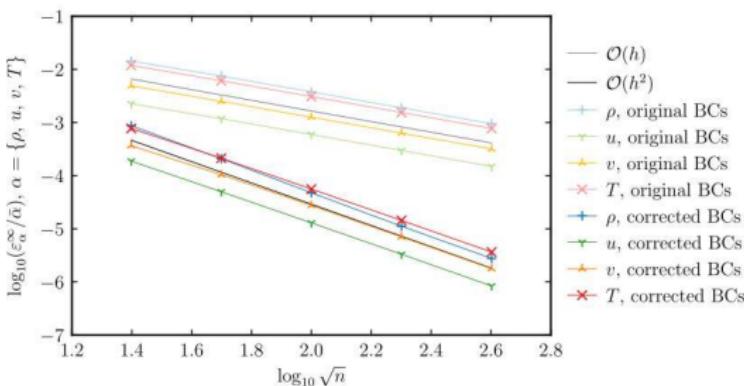
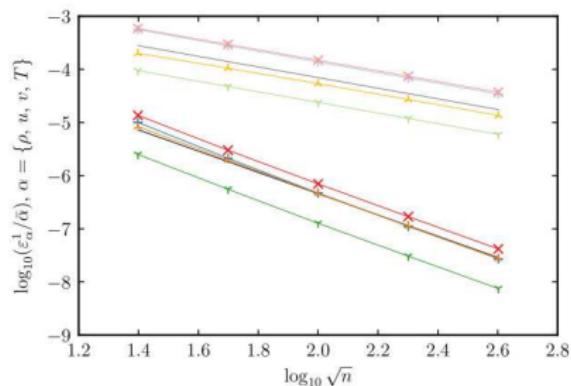
$$\bar{\rho} = 1 \text{ kg/m}^3, \bar{T} = 300 \text{ K}, \bar{M} = 2.5, \epsilon = 0.05$$



## 2D Supersonic Flow using a Manufactured Solution



## 2D Supersonic Flow using a Manufactured Solution



## First-order accurate

## Second-order accurate

Mesh	Original boundary conditions				Corrected boundary conditions			
	$\rho$	$u$	$v$	$T$	$\rho$	$u$	$v$	$T$
1–2	0.9420	0.9409	0.9721	0.9628	2.0623	1.9188	1.8174	1.8598
2–3	0.9850	0.9902	0.9910	0.9874	2.1304	1.9450	1.9221	1.9280
3–4	0.9960	1.0002	0.9924	0.9952	2.0902	1.9603	1.9671	1.9586
4–5	0.9989	1.0009	0.9959	0.9984	2.0128	1.9823	1.9860	1.9809

Observed accuracy  $p$  using  $L^\infty$ -norms of the error

## 2D Supersonic Flow using an Exact Solution

- Two-dimensional domain:  $(r, \theta) \in [1, 1.384] \times [0, 90]^\circ$
- Boundary conditions:
  - Supersonic inflow ( $\theta = 90^\circ$ )
  - Supersonic outflow ( $\theta = 0^\circ$ )
  - Slip wall (tangent flow) ( $r = 1$  &  $r = 1.384$ )
- 6 meshes:  $32 \times 8 \rightarrow 1024 \times 256$
- Solution is steady isentropic vortex:

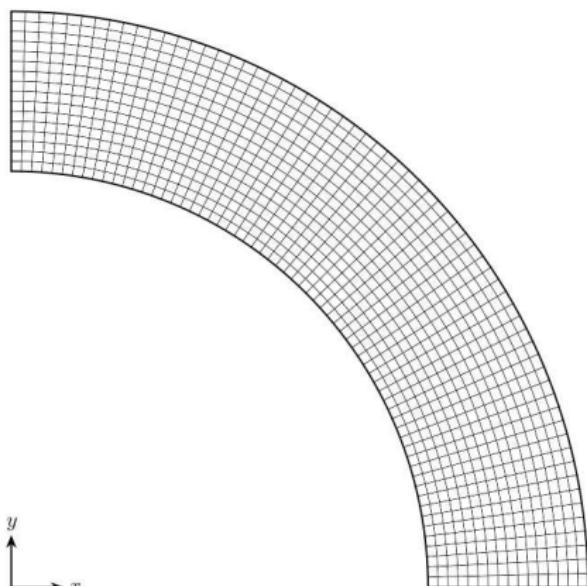
$$\rho(r) = \rho_i \left[ 1 + \frac{\gamma - 1}{2} M_i^2 \left( 1 - \left( \frac{r_i}{r} \right)^2 \right) \right]^{\frac{1}{\gamma-1}},$$

$$u_r(r) = 0,$$

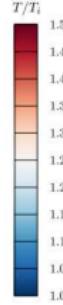
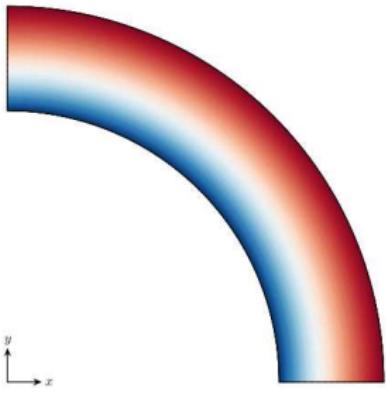
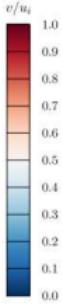
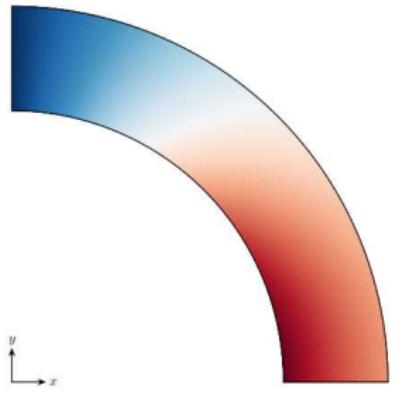
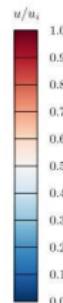
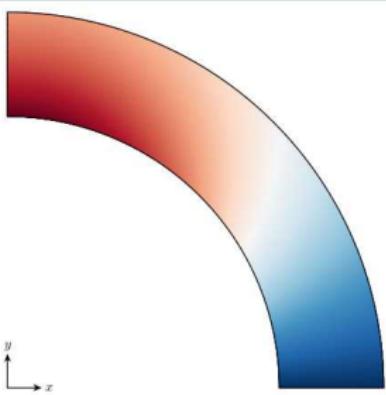
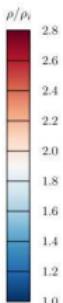
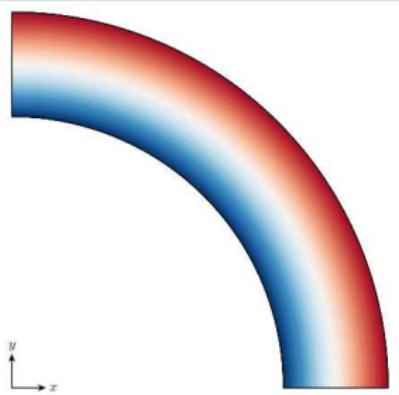
$$u_\theta(r) = -a_i M_i \frac{r_i}{r},$$

$$T(r) = T_i \left[ 1 + \frac{\gamma - 1}{2} M_i^2 \left( 1 - \left( \frac{r_i}{r} \right)^2 \right) \right],$$

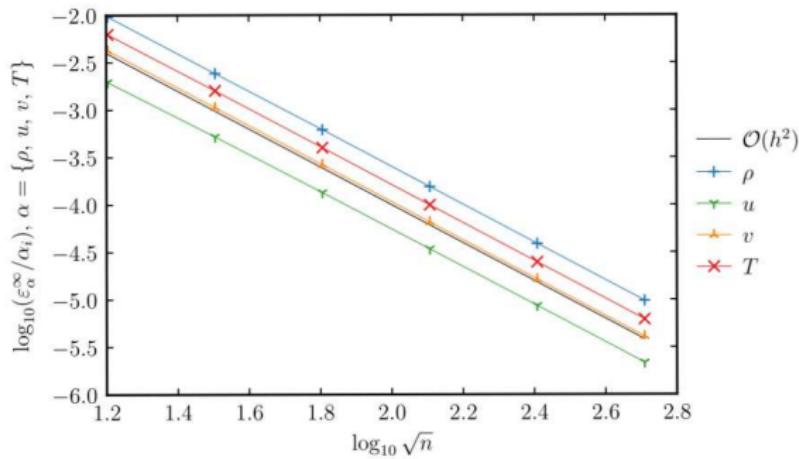
$$\rho_i = 1, a_i = 1, M_i = 2.25, T_i = 1/(\gamma R)$$



## 2D Supersonic Flow using an Exact Solution



## 2D Supersonic Flow using an Exact Solution



Mesh	$\rho$	$u$	$v$	$T$
1–2	1.9896	1.9119	1.9943	1.9699
2–3	1.9735	1.9589	2.0070	1.9979
3–4	1.9954	1.9760	2.0099	2.0076
4–5	1.9972	1.9879	2.0054	2.0044
5–6	<b>1.9986</b>	<b>1.9940</b>	<b>2.0029</b>	<b>2.0025</b>

Observed accuracy  $p$  using  $L^\infty$ -norms of the error

# 3D Supersonic Flow using a Manufactured Solution

- Three-dimensional domain:  $(x, y, z) \in [0, 1] \text{ m} \times [0, 1] \text{ m} \times [0, 1] \text{ m}$
- Boundary conditions:
  - Supersonic inflow ( $x = 0 \text{ m}$ )
  - Supersonic outflow ( $x = 1 \text{ m}$ )
  - Slip wall (tangent flow)  
( $y = 0 \text{ m}$ ,  $y = 1 \text{ m}$ ,  $z = 0 \text{ m}$ ,  $z = 1 \text{ m}$ )

- 5 nonuniform meshes:  
 $25 \times 25 \times 25 \rightarrow 400 \times 400 \times 400$
- Solution consists of small, smooth perturbations to uniform flow:

$$\rho(x, y, z) = \bar{\rho}[1 - \epsilon \sin(\frac{5}{4}\pi x)(\sin(\pi y) + \cos(\pi y))(\sin(\pi z) + \cos(\pi z))],$$

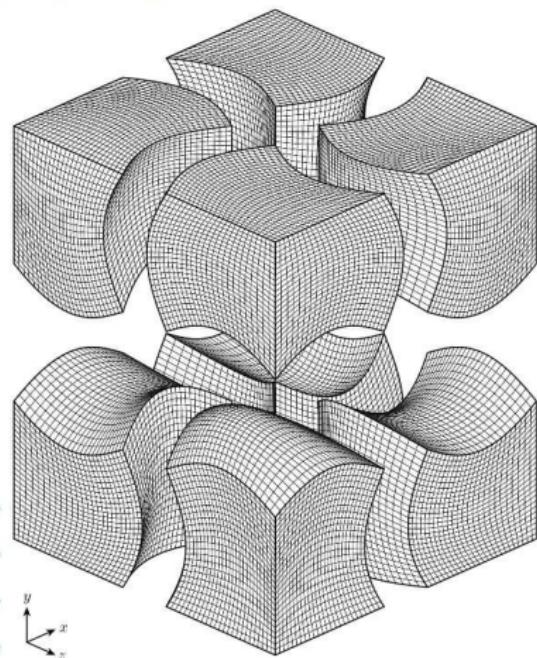
$$u(x, y, z) = \bar{u}[1 + \epsilon \sin(\frac{1}{4}\pi x)(\sin(\pi y) + \cos(\pi y))(\sin(\pi z) + \cos(\pi z))],$$

$$v(x, y, z) = \bar{v}[-\epsilon \sin(\frac{5}{4}\pi x)(\sin(\pi y) + \cos(\pi y))(\sin(\pi z) + \cos(\pi z))],$$

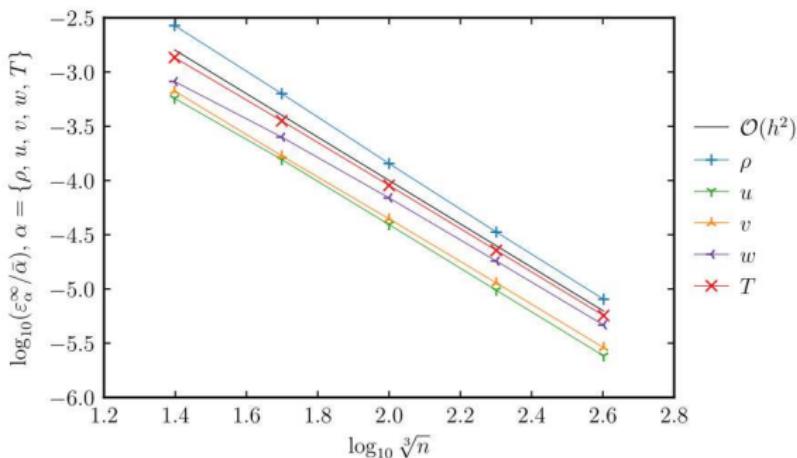
$$w(x, y, z) = \bar{w}[-\epsilon \sin(\frac{5}{4}\pi x)(\sin(\pi y) + \cos(\pi y))(\sin(\pi z) + \cos(\pi z))],$$

$$T(x, y, z) = \bar{T}[1 + \epsilon \sin(\frac{5}{4}\pi x)(\sin(\pi y) + \cos(\pi y))(\sin(\pi z) + \cos(\pi z))],$$

$$\bar{\rho} = 1 \text{ kg/m}^3, \bar{T} = 300 \text{ K}, \bar{M} = 2.5, \epsilon = 0.05$$



## 3D Supersonic Flow using a Manufactured Solution



Mesh	$\rho$	$u$	$v$	$w$	$T$
1–2	2.0849	1.8731	1.9841	1.7039	1.9404
2–3	2.1406	1.9923	1.9295	1.8621	1.9774
3–4	2.0990	2.0115	1.9623	1.9349	1.9922
4–5	2.0585	2.0100	1.9820	1.9571	1.9964

Observed accuracy  $p$  using  $L^\infty$ -norms of the error

## Five-Species Air Model

5 species:  $\text{N}_2$ ,  $\text{O}_2$ ,  $\text{NO}$ ,  $\text{N}$ , and  $\text{O}$ 

17 reactions:

$r$	Reaction	Type of Reaction
1–5	$\text{N}_2 + \mathcal{M} \rightleftharpoons \text{N} + \text{N} + \mathcal{M}, \quad \mathcal{M} = \{\text{N}_2, \text{O}_2, \text{NO}, \text{N}, \text{O}\}$	Dissociation
6–10	$\text{O}_2 + \mathcal{M} \rightleftharpoons \text{O} + \text{O} + \mathcal{M}, \quad \mathcal{M} = \{\text{N}_2, \text{O}_2, \text{NO}, \text{N}, \text{O}\}$	Dissociation
11–15	$\text{NO} + \mathcal{M} \rightleftharpoons \text{N} + \text{O} + \mathcal{M}, \quad \mathcal{M} = \{\text{N}_2, \text{O}_2, \text{NO}, \text{N}, \text{O}\}$	Dissociation
16	$\text{N}_2 + \text{O} \rightleftharpoons \text{N} + \text{NO}$	Exchange
17	$\text{NO} + \text{O} \rightleftharpoons \text{N} + \text{O}_2$	Exchange

# Five-Species Inviscid Flow in Chemical Nonequilibrium

- Two-dimensional domain:  $(x, y) \in [0, 1] \text{ m} \times [0, 1] \text{ m}$
- Same boundary conditions
- 7 nonuniform meshes:  $25 \times 25 \rightarrow 1600 \times 1600$
- Solution consists of small, smooth perturbations to uniform flow

$$\rho_{N_2}(x, y) = \bar{\rho}_{N_2} \left[ 1 - \epsilon \sin\left(\frac{5}{4}\pi x\right) (\sin(\pi y) + \cos(\pi y)) \right],$$

$$\rho_{O_2}(x, y) = \bar{\rho}_{O_2} \left[ 1 + \epsilon \sin\left(\frac{3}{4}\pi x\right) (\sin(\pi y) + \cos(\pi y)) \right],$$

$$\rho_{NO}(x, y) = \bar{\rho}_{NO} \left[ 1 + \epsilon \sin(\pi x) (\sin(\pi y)) \right],$$

$$\rho_N(x, y) = \bar{\rho}_N \left[ 1 + \epsilon \sin(\pi x) (\cos(\frac{1}{4}\pi y)) \right],$$

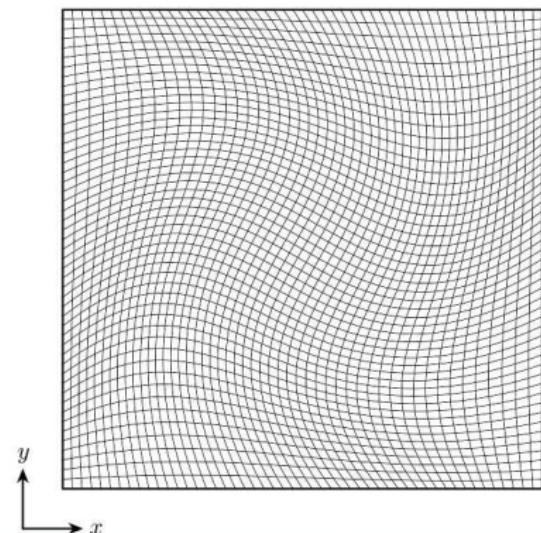
$$\rho_O(x, y) = \bar{\rho}_O \left[ 1 + \epsilon \sin(\pi x) (\sin(\pi y) + \cos(\frac{1}{4}\pi y)) \right],$$

$$u(x, y) = \bar{u} \left[ 1 + \epsilon \sin\left(\frac{1}{4}\pi x\right) (\sin(\pi y) + \cos(\pi y)) \right],$$

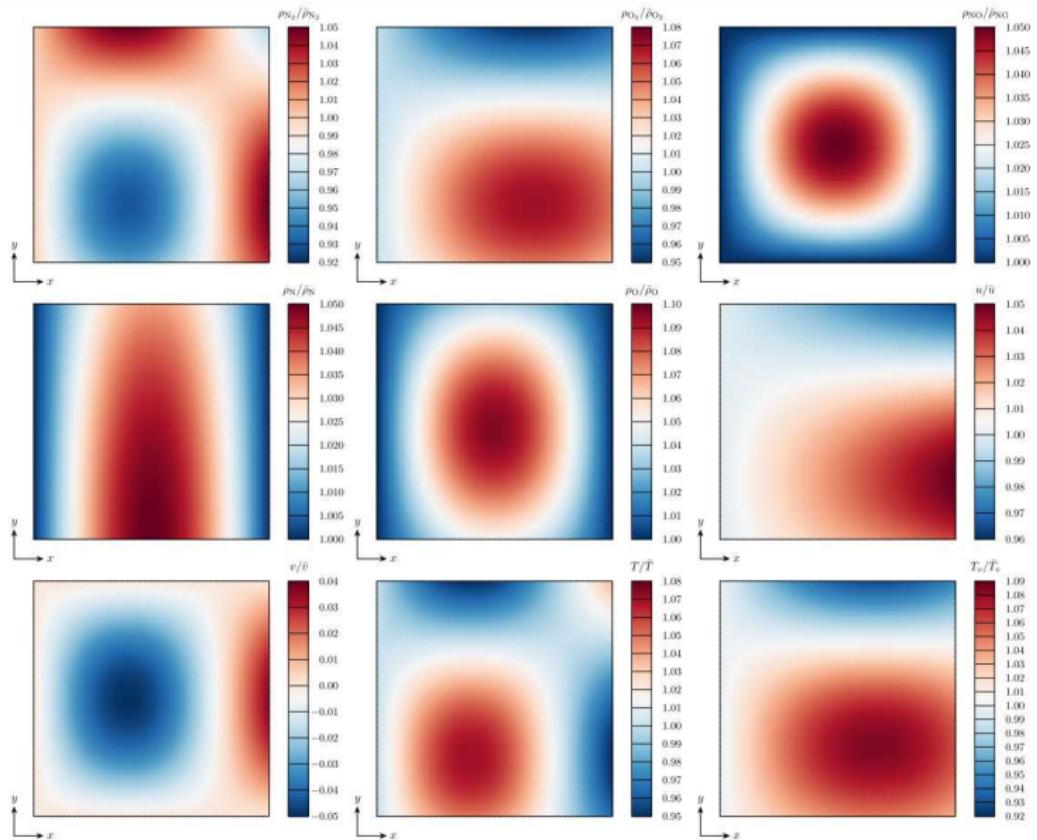
$$v(x, y) = \bar{v} \left[ -\epsilon \sin\left(\frac{5}{4}\pi x\right) (\sin(\pi y)) \right],$$

$$T(x, y) = \bar{T} \left[ 1 + \epsilon \sin\left(\frac{5}{4}\pi x\right) (\sin(\pi y) + \cos(\pi y)) \right],$$

$$T_v(x, y) = \bar{T}_v \left[ 1 + \epsilon \sin\left(\frac{3}{4}\pi x\right) (\sin(\frac{5}{4}\pi y) + \cos(\frac{3}{4}\pi y)) \right]$$

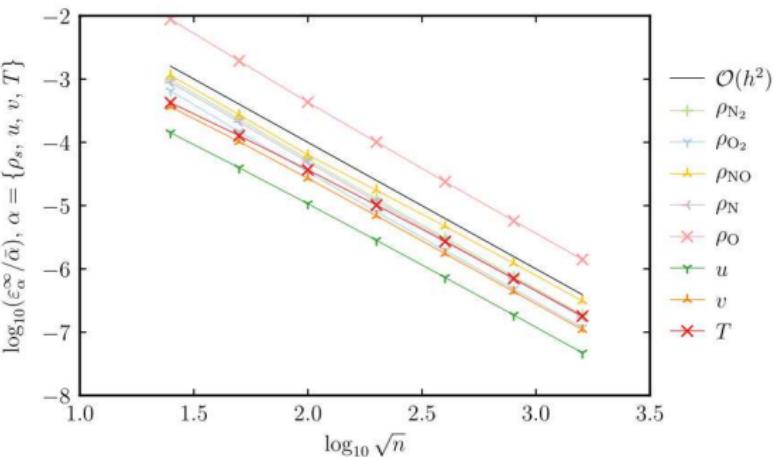


## Five-Species Inviscid Flow in Chemical Nonequilibrium



## 2D Supersonic Flow in Thermal Equilibrium using a Manufactured Solution

Variable	Value	Units
$\bar{\rho}_{N_2}$	0.77	kg/m <sup>3</sup>
$\bar{\rho}_{O_2}$	0.20	kg/m <sup>3</sup>
$\bar{\rho}_{NO}$	0.01	kg/m <sup>3</sup>
$\bar{\rho}_N$	0.01	kg/m <sup>3</sup>
$\bar{\rho}_O$	0.01	kg/m <sup>3</sup>
$\bar{T}$	3500	K
$\bar{M}$	2.5	
$\epsilon$	0.05	

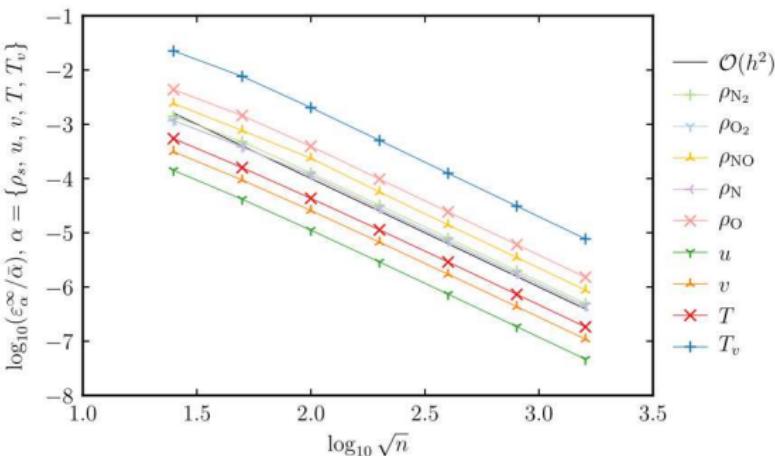


Mesh	$\rho_{N_2}$	$\rho_{O_2}$	$\rho_{NO}$	$\rho_N$	$\rho_O$	$u$	$v$	$T$
1–2	2.0608	2.1382	2.0698	2.0644	2.1885	1.8425	1.8289	1.7351
2–3	2.1161	2.1219	2.1127	2.1072	2.1697	1.8875	1.9220	1.7923
3–4	2.0798	2.0813	1.8555	2.0754	2.0971	1.9200	1.9686	1.8525
4–5	2.0456	2.0458	1.8917	2.0428	2.0806	1.9522	1.9871	1.9079
5–6	2.0243	2.0243	1.9427	2.0228	2.0529	1.9735	1.9939	1.9485
6–7	<b>2.0125</b>	<b>2.0125</b>	<b>1.9790</b>	<b>2.0118</b>	<b>2.0318</b>	<b>1.9865</b>	<b>1.9969</b>	<b>1.9737</b>

2D MMS,  $n_s = 5$ ,  $T_v = T$ ,  $\dot{\mathbf{w}} \neq \mathbf{0}$ : Observed accuracy  $p$  using  $L^\infty$ -norms of the error

## 2D Hypersonic Flow in Thermal Nonequilibrium using a Manufactured Solution

Variable	Value	Units
$\bar{\rho}_{N_2}$	0.0077	kg/m <sup>3</sup>
$\bar{\rho}_{O_2}$	0.0020	kg/m <sup>3</sup>
$\bar{\rho}_{NO}$	0.0001	kg/m <sup>3</sup>
$\bar{\rho}_N$	0.0001	kg/m <sup>3</sup>
$\bar{\rho}_O$	0.0001	kg/m <sup>3</sup>
$\bar{T}$	5000	K
$\bar{T}_v$	1000	K
$M$	8	
$\epsilon$	0.05	



Mesh	$\rho_{N_2}$	$\rho_{O_2}$	$\rho_{NO}$	$\rho_N$	$\rho_O$	$u$	$v$	$T$	$T_v$
1-2	1.5659	1.6370	1.6555	1.6046	1.5869	1.7742	1.7337	1.7814	1.5545
2-3	1.9067	1.6944	1.6986	1.7598	1.8819	1.8916	1.8701	1.8768	1.9150
3-4	1.9868	2.0475	2.0698	2.0477	2.0110	1.9488	1.9357	1.9349	2.0082
4-5	2.0074	1.9941	2.0138	1.9936	2.0089	1.9752	1.9684	1.9672	2.0168
5-6	2.0062	1.9939	2.0004	1.9935	2.0061	1.9879	1.9843	1.9836	2.0111
6-7	2.0037	1.9965	1.9994	1.9962	1.9955	1.9940	1.9922	1.9918	2.0063

2D MMS,  $n_s = 5$ ,  $T_v \neq T$ ,  $\dot{\mathbf{w}} \neq \mathbf{0}$ : Observed accuracy  $p$  using  $L^\infty$ -norms of the error

# Outline

- Introduction
- Governing Equations
- Verification Techniques for Spatial Accuracy
- Spatial-Discretization Verification Results
- Verification Techniques for Thermochemical Source Term
  - Techniques
  - Distinctive Features
- Thermochemical-Source-Term Verification Results
- Summary

# Verification Techniques for Thermochemical Source Term

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  - For many values of  $\{\boldsymbol{\rho}, T, T_v\}$
  - Compare with independently developed code
- For each query, compute symmetric relative difference

$$\delta_\beta = 2 \left| \frac{\beta_{\text{SPARC}} - \beta'}{\beta_{\text{SPARC}} + \beta'} \right|$$

$$\beta = \left\{ Q_{t-v}, e_{v_{\text{N}_2}}, e_{v_{\text{O}_2}}, e_{v_{\text{NO}}}, \dot{w}_{\text{N}_2}, \dot{w}_{\text{O}_2}, \dot{w}_{\text{NO}}, \dot{w}_{\text{N}}, \dot{w}_{\text{O}} \right\}$$

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- **Wide** condition coverage
  - Comparison is queried for 1000s of conditions, spans extreme ranges
  - Code-to-code comparison typically considers single or few conditions

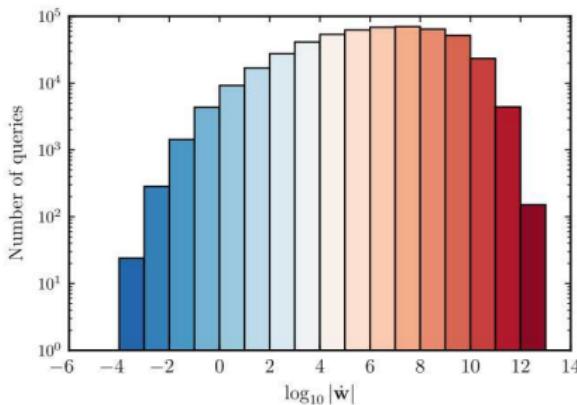
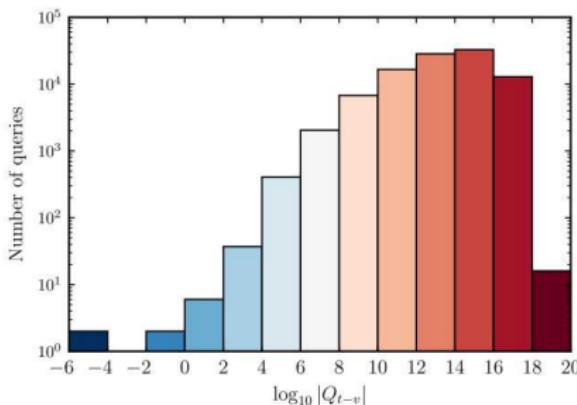
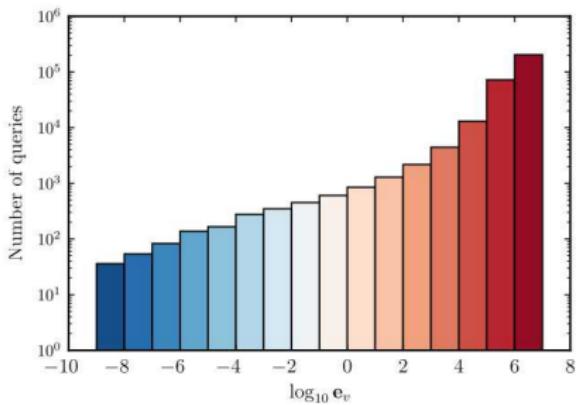
# Outline

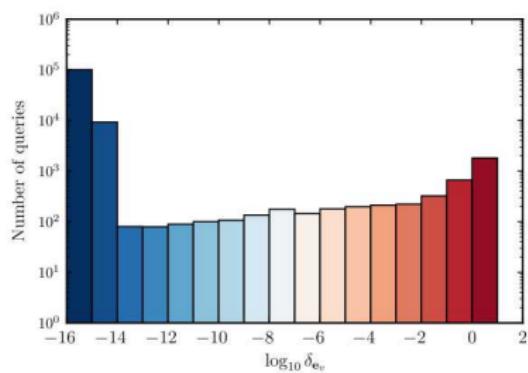
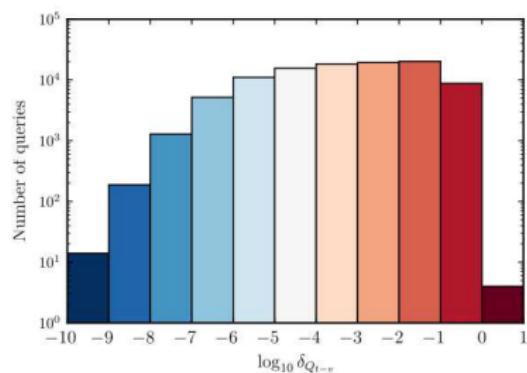
- Introduction
- Governing Equations
- Verification Techniques for Spatial Accuracy
- Spatial-Discretization Verification Results
- Verification Techniques for Thermochemical Source Term
- Thermochemical-Source-Term Verification Results
  - Samples of  $Q_{t-v}(\rho, T, T_v)$ ,  $\mathbf{e}_v(\rho, T, T_v)$ , and  $\dot{\mathbf{w}}(\rho, T, T_v)$
  - Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$
  - Nonzero Relative Differences in  $\dot{\mathbf{w}}$
- Summary

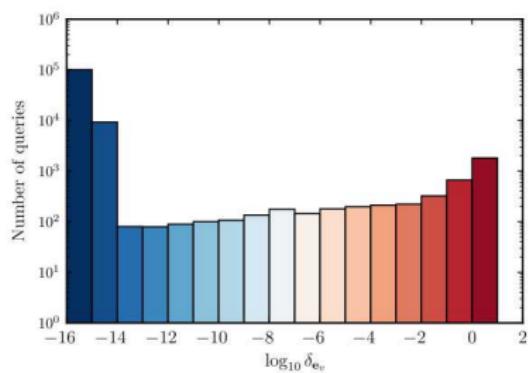
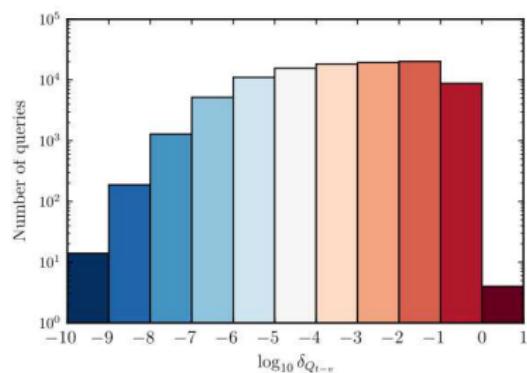
Samples of  $Q_{t-v}(\rho, T, T_v)$ ,  $\mathbf{e}_v(\rho, T, T_v)$ , and  $\dot{\mathbf{w}}(\rho, T, T_v)$ 

Variable	Minimum	Maximum	Units	Spacing
$\rho_{N_2}$	$10^{-6}$	$10^1$	kg/m <sup>3</sup>	Logarithmic
$\rho_{O_2}$	$10^{-6}$	$10^1$	kg/m <sup>3</sup>	Logarithmic
$\rho_{NO}$	$10^{-6}$	$10^1$	kg/m <sup>3</sup>	Logarithmic
$\rho_N$	$10^{-6}$	$10^1$	kg/m <sup>3</sup>	Logarithmic
$\rho_O$	$10^{-6}$	$10^1$	kg/m <sup>3</sup>	Logarithmic
$T$	100	15,000	K	Linear
$T_v$	100	15,000	K	Linear

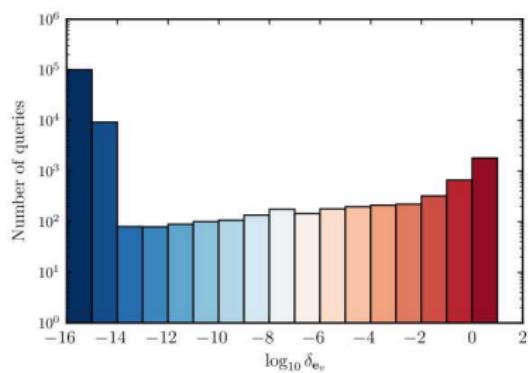
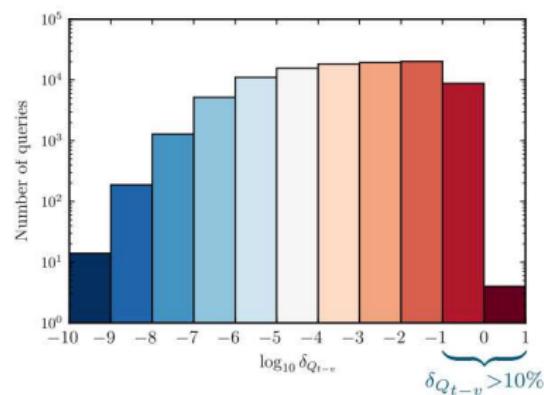
Ranges and spacings for 100,000

Latin hypercube samples of  $\rho$ ,  $T$ , and  $T_v$ 

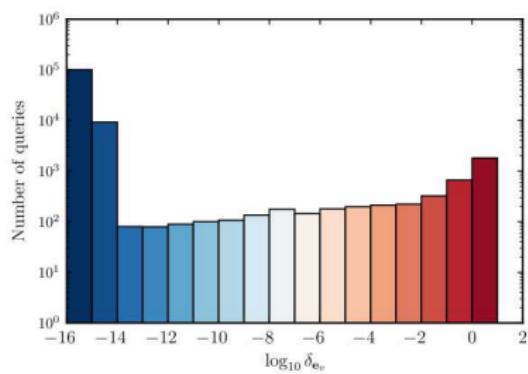
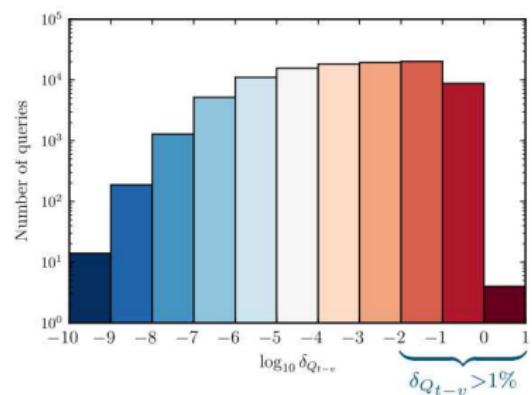
Original Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

Original Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

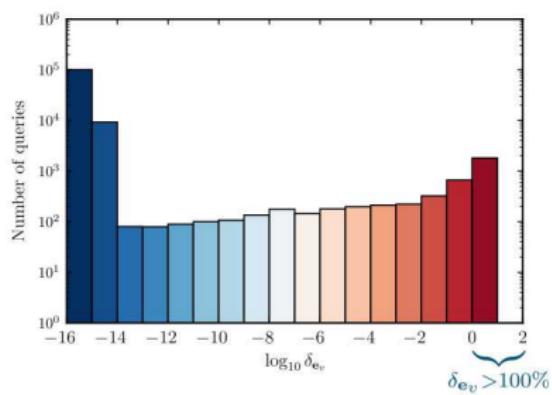
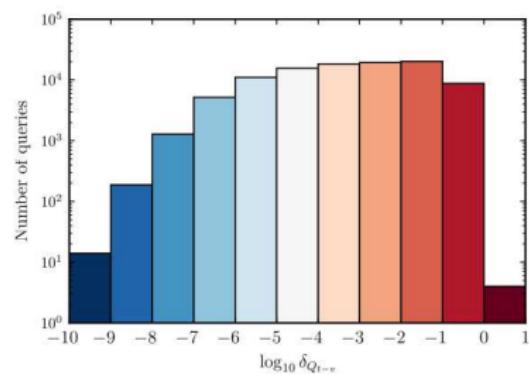
- Relative differences are **not** near machine precision

Original Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

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- $\delta_{Q_{t-v}} > 10\%$  in 8.8% of simulations

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- Relative differences are **not** near machine precision
- $\delta_{Q_{t-v}} > 10\%$  in 8.8% of simulations
- $\delta_{Q_{t-v}} > 1\%$  in 29% of simulations
- $\delta_{\mathbf{e}_v} > 100\%$  for some simulations

# Causes of Large Relative Differences in $Q_{t-v}$ and $\mathbf{e}_v$

Two causes:

## Causes of Large Relative Differences in $Q_{t-v}$ and $\mathbf{e}_v$

Two causes:

- **Incorrect lookup table values** for vibrational constants
  - For N<sub>2</sub> and O<sub>2</sub> when the colliding species is NO
  - Introduced error in  $Q_{t-v}$  for all simulations
  - For high-enthalpy (20 MJ/kg), hypersonic, laminar double-cone flow, 1.4% change in pressure and 2.7% change in heat flux

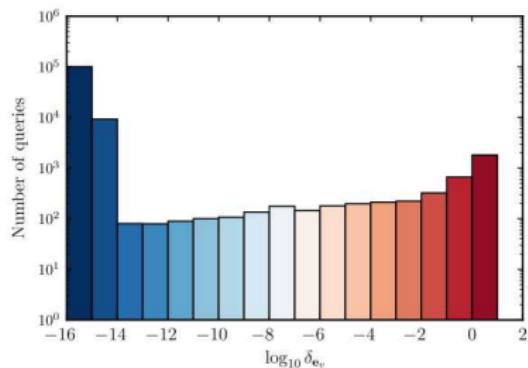
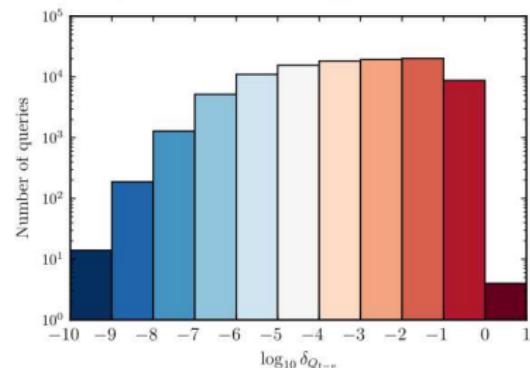
## Causes of Large Relative Differences in $Q_{t-v}$ and $\mathbf{e}_v$

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  - For high-enthalpy (20 MJ/kg), hypersonic, laminar double-cone flow, 1.4% change in pressure and 2.7% change in heat flux
- **Loose convergence criteria** for computing  $T_v$  from  $\rho e_v$ 
  - Unsuitable for low values of  $T_v$
  - Introduced errors in  $Q_{t-v}$  and  $\mathbf{e}_v$  for a few simulations
  - For converged, steady problem, original criteria are acceptable

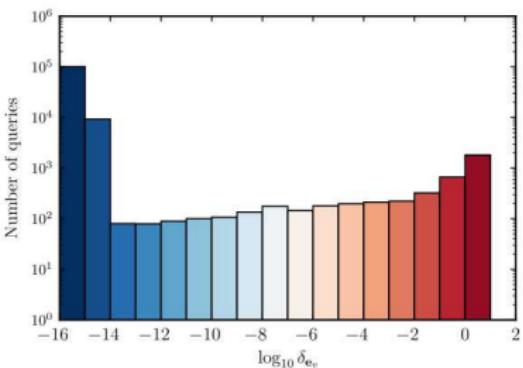
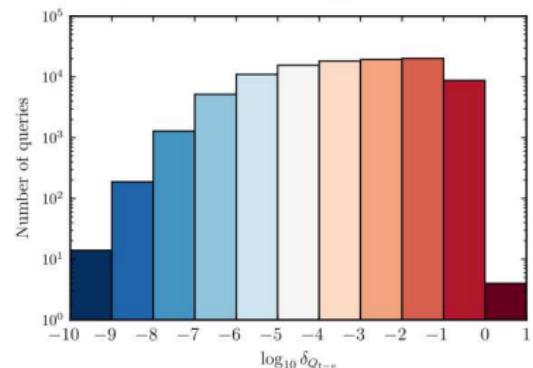
Corrected Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

Original lookup table and convergence criteria

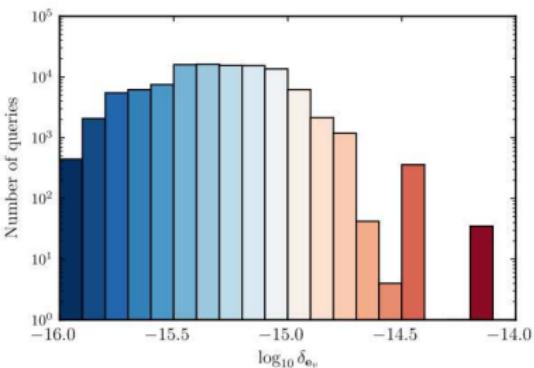
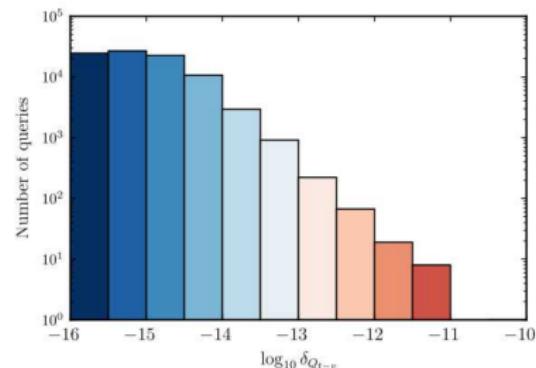


Corrected Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

Original lookup table and convergence criteria

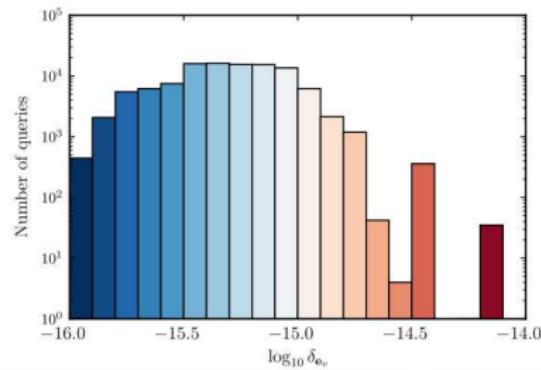
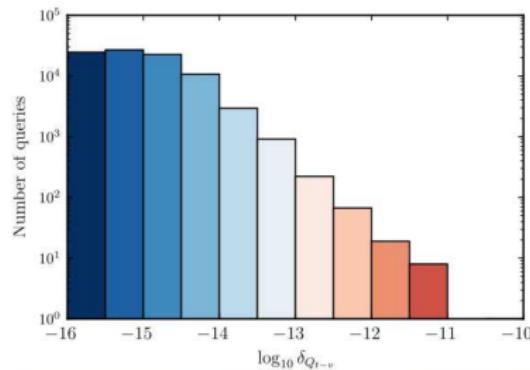


Corrected lookup table and tighter convergence criteria



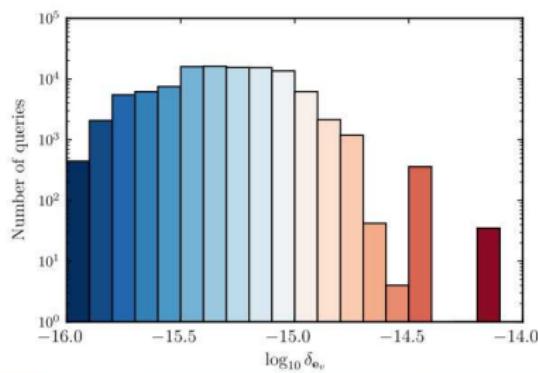
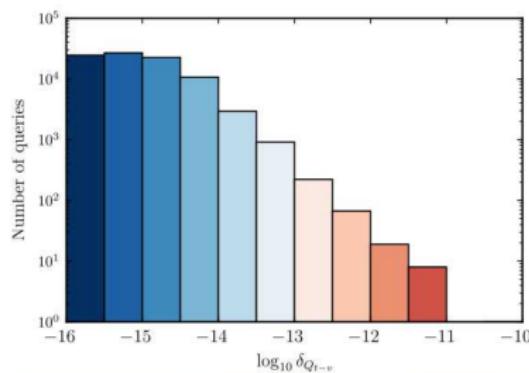
Corrected Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

- Relative differences are consistent with our expectations



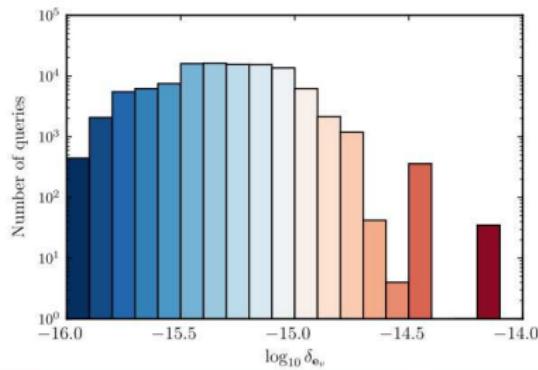
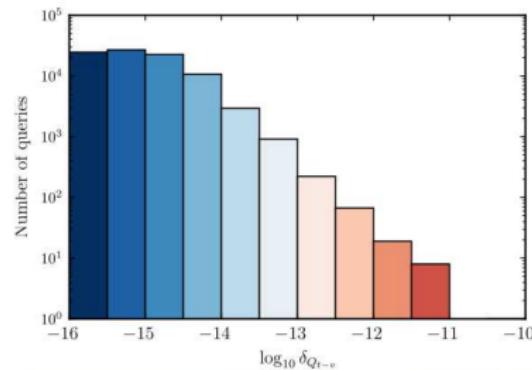
Corrected Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

- Relative differences are consistent with our expectations
- $\delta_{Q_{t-v}} < 10^{-10}$  and  $\delta_{\mathbf{e}_v} < 10^{-14}$  in all simulations



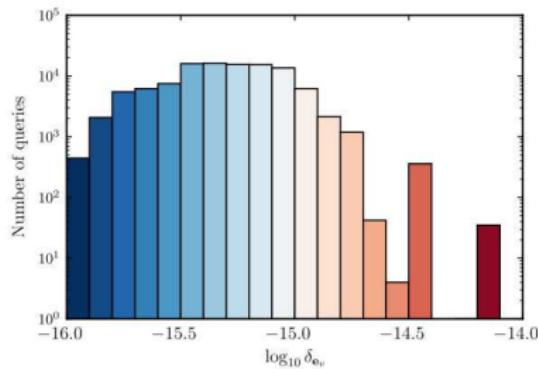
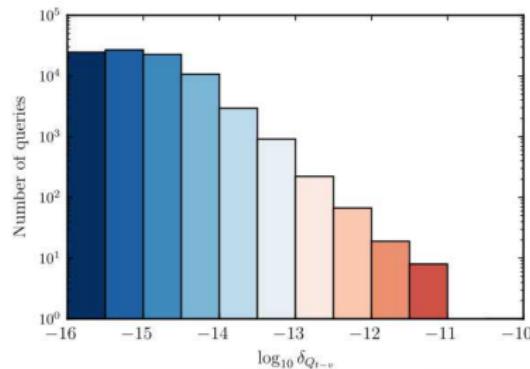
Corrected Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

- Relative differences are consistent with our expectations
- $\delta_{Q_{t-v}} < 10^{-10}$  and  $\delta_{\mathbf{e}_v} < 10^{-14}$  in all simulations
- $\delta_{Q_{t-v}} > 10^{-12}$  in 28/100,000 simulations



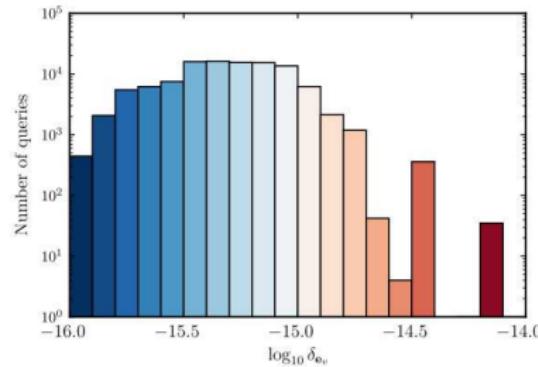
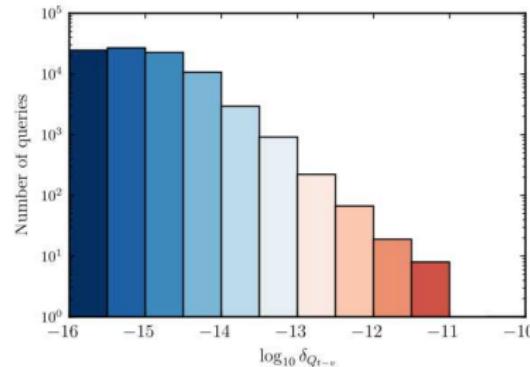
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  - $T$  and  $T_v$  have relative difference less than 0.2%



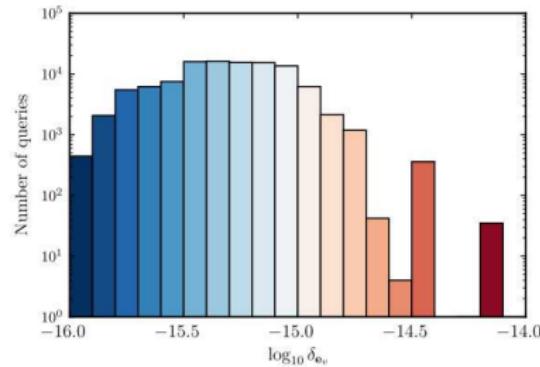
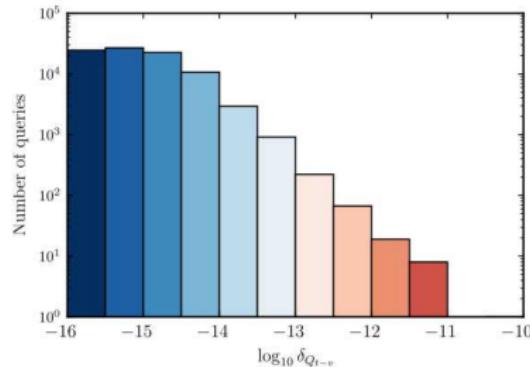
Corrected Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

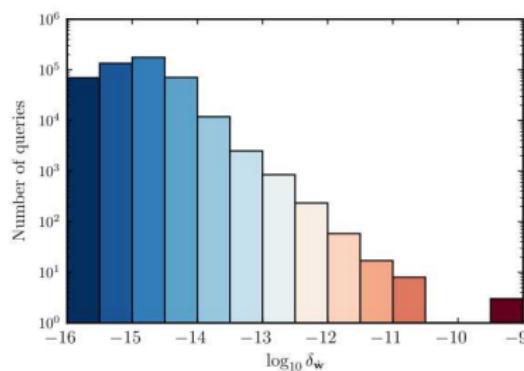
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- $\delta_{Q_{t-v}} > 10^{-12}$  in 28/100,000 simulations
  - $T$  and  $T_v$  have relative difference less than 0.2%
  - In numerator of  $\frac{e_{v_{s,m}}(T) - e_{v_{s,m}}(T_v)}{\langle \tau_{s,m} \rangle}$ ,  $e_{v_{s,m}}(T)$  and  $e_{v_{s,m}}(T_v)$  share many leading digits

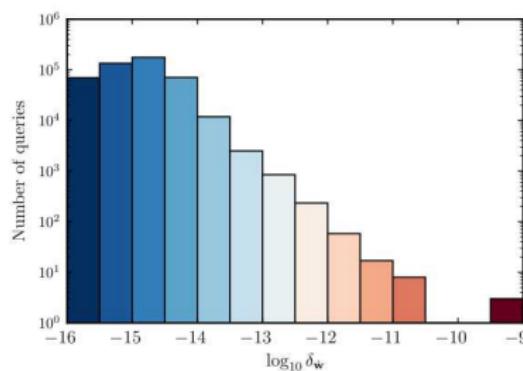


Corrected Nonzero Relative Differences in  $Q_{t-v}$  and  $\mathbf{e}_v$ 

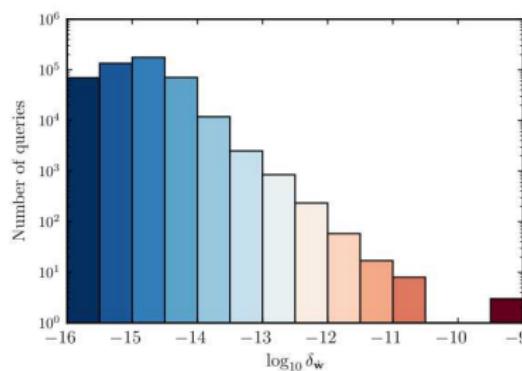
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  - Precision lost when computing difference



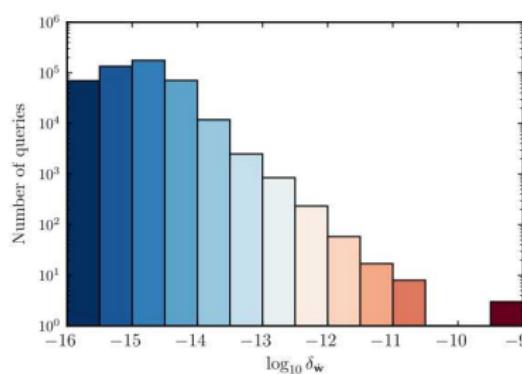
Nonzero Relative Differences in  $\dot{\mathbf{w}}$ 

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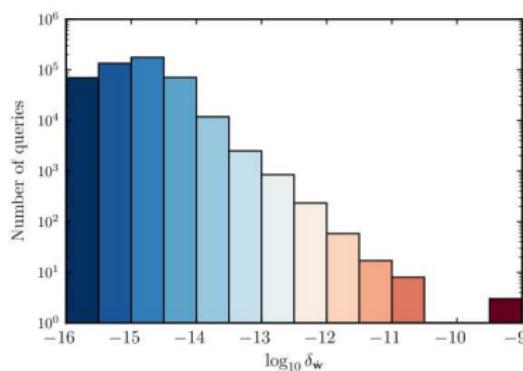
- Relative differences are consistent with our expectations

Nonzero Relative Differences in  $\dot{\mathbf{w}}$ 

- Relative differences are consistent with our expectations
- $\dot{\mathbf{w}} < 10^{-9}$  in all simulations

Nonzero Relative Differences in  $\dot{\mathbf{w}}$ 

- Relative differences are consistent with our expectations
- $\dot{\mathbf{w}} < 10^{-9}$  in all simulations
- $\dot{\mathbf{w}} > 10^{-12}$  for 87/500,000 computed values (5 species, 100,000 simulations)

Nonzero Relative Differences in  $\dot{\mathbf{w}}$ 

- Relative differences are consistent with our expectations
- $\dot{\mathbf{w}} < 10^{-9}$  in all simulations
- $\dot{\mathbf{w}} > 10^{-12}$  for 87/500,000 computed values (5 species, 100,000 simulations)
  - Due to precision loss that can occur from subtraction in
$$\dot{w}_s = M_s \sum_{r=1}^{n_r} (\beta_{s,r} - \alpha_{s,r}) (R_{f_r} - R_{b_r})$$

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- Thermochemical-Source-Term Verification Results
- Summary
  - Code-Verification Techniques

# Code-Verification Techniques

- Manufactured and exact solutions
  - Effective approaches for verifying spatial accuracy – detected multiple issues
  - Rigorous norms improve effectiveness –  $L^\infty$ -norm of error more useful
  - Insufficient for algebraic source terms – both evaluations the same
- Thermochemical-source-term approach
  - Effective approach for verifying implementation – detected multiple issues

## Questions?

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