

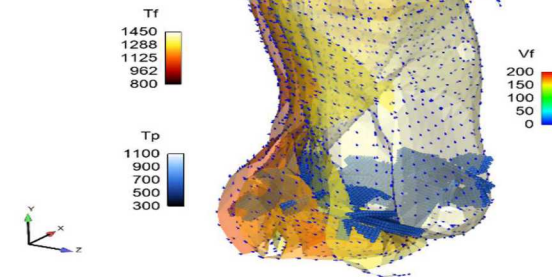


# ASTFE

American Society  
of Thermal and Fluids Engineers



Time = 29.0000



## Composite Material Combustion Modeling Using Thermally Interacting, Chemically Reactive Lagrangian Particles

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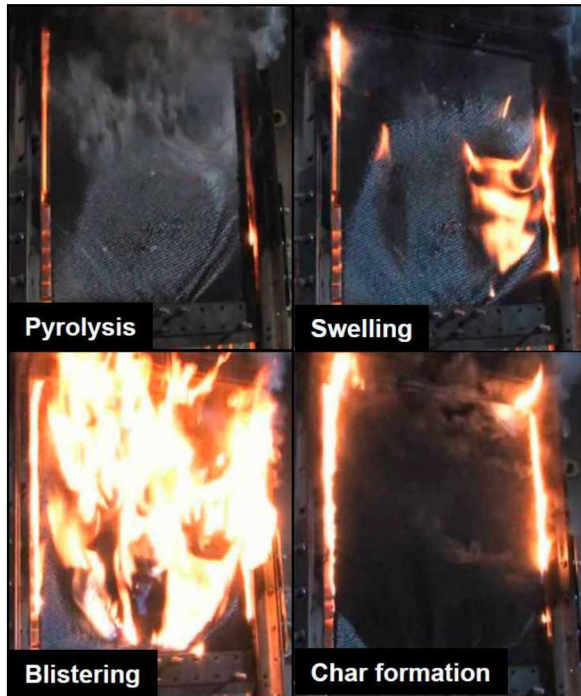


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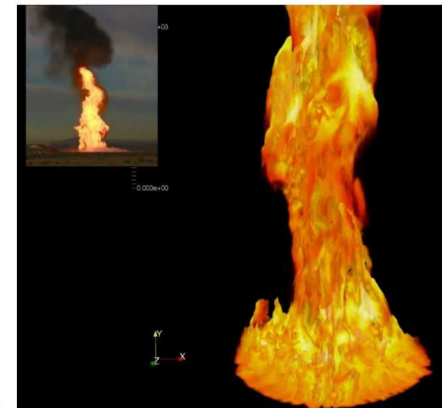


# Carbon Fiber - Reinforced Epoxy Composites

LM F-22 Raptor



- Accidents involving aircraft composed of carbon fiber–reinforced epoxy composites can involve mixed fuel fires
  - Liquid fuel
  - Composite rubble
- Complicated combustion processes
  - Chemical Reactions
    - Solid Phase
    - Gas Phase
  - Thermal transport
    - Convection, conduction, radiation
  - Interaction between solids/liquid/gas





# Modeling Approach - Fluid

- Fluid (CFD) Description
  - Sierra low Mach Fuego
  - CVFEM
  - Variety of turbulence models
  - Gas phase combustion model
    - EDC – Eddy Dissipation Concept
- Particle/Fluid Coupling
  - Momentum (drag)
  - Energy (heat, enthalpy)
  - Mass
  - Species

## SIERRA/Fuego/Syrinx Low Mach Fluids/Radiation Transport Code

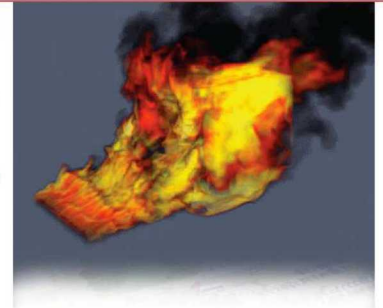
Thermal/Fluids Computational Engineering Sciences Department 1541 at Sandia National Laboratories provides high-fidelity, verified, software-quality assured, massively parallel multi-mechanics coupled analysis codes to the tri-lab community to solve complex problems. SIERRA/Fuego/Syrinx, with coupling to SIERRA/Calore, supports the capability to simulate the abnormal-thermal environment (i.e., transient object heat-up in hydrocarbon pool fire environments that might arise during transportation or storage-accident scenarios).

### SIERRA/Fuego/Syrinx

has been developed under the object-oriented SIERRA Frameworks to easily facilitate multi-mechanics coupling to provide a robust simulation capability for highly sooting, buoyancy-driven turbulent-reacting flow mechanics. The core capability in SIERRA/Fuego is simulation of three-dimensional low-Mach-number turbulent-reacting flows on heterogeneous topological meshes (e.g., a mixture of hexahedral, tetrahedral, pyramid, and wedge elements). An approximate projection algorithm is used with Control Volume Finite Element Method (CVFEM) discretization. SIERRA/Syrinx solves the steady radiation transport equation using Streamwise Upwind Petrov-Galerkin discretization. The combined capability, in addition to coupling of the thermal-analysis code SIERRA/Calore, is required in the qualification effort for weapons in abnormal thermal environments.

### Applications

SIERRA/Fuego/Syrinx is widely used to simulate applications as diverse as fire environments and laminar natural convection environments. The code primarily simulates buoyancy-driven turbulent-reacting flow in abnormal thermal environments (fluids, participating media radiation [PMR], and heat conduction). However, the core capability of this simulation tool is laminar/turbulent fluid mechanics and a combination of thermal/isothermal and uniform/nonuniform (with reactions) transport.



SIERRA/Fuego/Syrinx/Calore simulation of the proposed Thermal Test Complex Cross Wind Facility. The simulation includes one fluids and [S4] PMR region with two conduction regions (only outside container seen). 400 million dof; 5000 processor Red Storm run; shown is the volume-rendered temperature field.

### Features

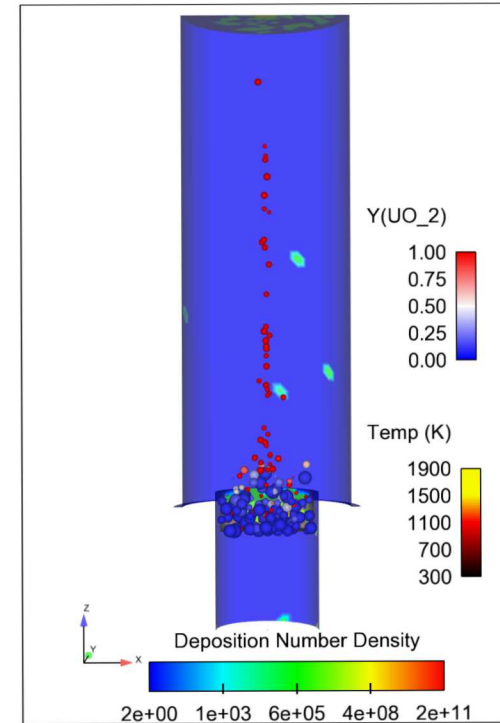
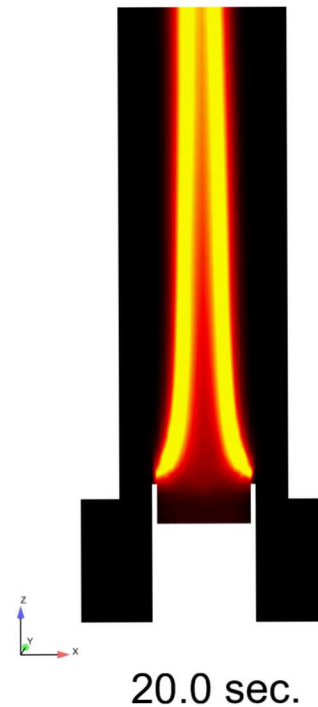
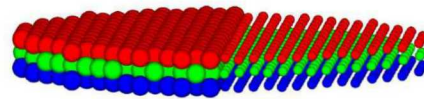
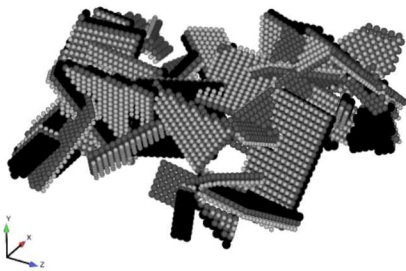
Unique features of SIERRA/Fuego/Syrinx that enable the code to solve complex problems include the following:

- Scalable, parallel solutions (optimal scaling demonstrated up to available resources, i.e., 40 million node mesh, 4096 processors).
- RANS turbulence models including the  $v^2$ -f model of Durbin, standard  $k$ - $\epsilon$  with wall functions, low Reynolds number models, and Large Eddy Simulation (LES) models including  $k$ -sgs, dynamic k-Smagorinsky and TFNS.
- Heterogeneous topology support (e.g., hexahedron, tetrahedral, pyramid, and wedge elements).
- Conjugate heat transfer coupling capability either with simple SIERRA/Fuego conduction region(s) or complex SIERRA/Calore conduction region(s).
- Seamless, state-of-the-art solver/preconditioners (e.g., multi-level methods, through input file declarations of solver libraries such as Trilinos, PetSci, HyPre, Prometheus, etc.).
- Advanced user subroutines



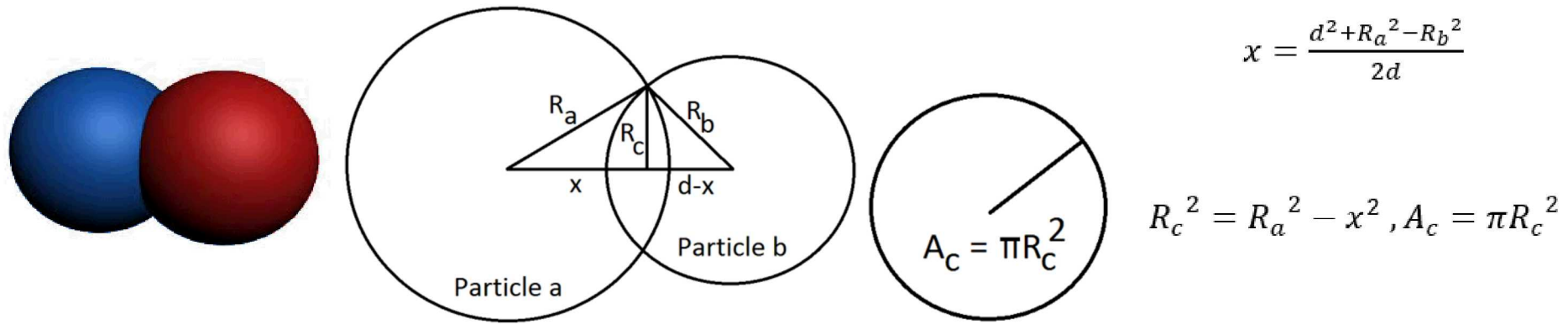
# Modeling Approach - Particles

- Composite Materials Description
  - Bars/Layers of Lagrangian particles
- Particle/Particle thermal Interactions
- Particle Chemical Reactions
  - Fuego General Chemistry model



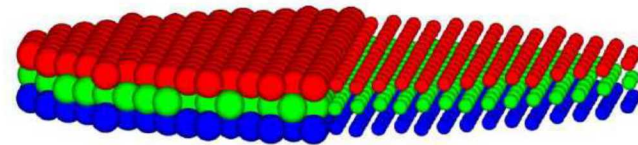


# Particle/Particle Thermal Interactions



## Thermal exchange - pairwise conduction

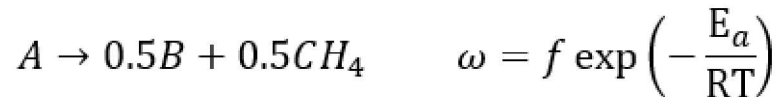
- Circular contact area
- Particle size/conductivities can differ
- Particles exist in composite **Bars** made of **Layers**
  - Same layer/bar - full conduction
  - Same bar/neighboring layers – reduced conduction
  - Different bar|non-neighboring layers – no conduction





# Particle Reactions – General Chemistry Mechanism

## Fuego input section



- Decomposition reaction
  - Arrhenius form
    - $\omega(T)$
    - T changes due to thermal coupling to background fluid/neighboring particles
  - Solid + gas phase products
    - ex:  $B/CH_4$
  - $CH_4$  (gas) combustion – post production
  - More complex forms available

BEGIN PARTICLE DEFINITION solid\_particles

USE PARTICLE SPECIES = A B C D E

PARTICLE TYPE IS GENERALIZED\_PARTICLE

USE SPECIES MATERIAL materialA for A

USE SPECIES MATERIAL materialB for B

USE SPECIES MATERIAL materialC for C

USE SPECIES MATERIAL materialD for D

USE SPECIES MATERIAL materialE for E

ADD PARTICLE INTERFACE parameterSpec

particle is stationary

BEGIN GENERAL CHEMISTRY reactiveMechanism

Begin Reaction R1

Reaction is **A -> 0.5B + 0.5CH4**

Rate Function = Arrhenius **A = 3.33e+15 Ea = 226140000** R = 8314.

Concentration Function = Standard mu = A 1.0

Heat of Reaction = 0

Temperature Phase = LIQUID\_PHASE

Pressure Phase = LIQUID\_PHASE

End Reaction R1



# Demonstration Case 1 : Details

- **Simulation time:** 500s

- **BCs:**

- 1 m/s upward inflow from inlet base (-Y) at  $T = 1000\text{K}$
- Side walls (and lower boundary around inlet) at  $T = 800\text{K}$
- upper open boundary at  $T = 800\text{K}$

- **Particles:**

- 886 particles of size  $d = 0.02\text{m}$  in
- 11 layers, 2 bars
- $T_p(\text{time} = 0) = 300\text{K}$

- **Particle Materials**

# Material Properties for species A

BEGIN PARTICLE MATERIAL materialA

DENSITY = 1779.0 # kg/m<sup>3</sup>

SPECIFIC\_HEAT = 866.0 # J/Kg-K

ABSORPTIVITY = 1.0 # no units

EMISSION\_MULTIPLIER = 1.0 # no units

VISCOSITY = 100

THERMAL\_CONDUCTIVITY = 50.0 # J/m-s-K

FILM\_PRANDTL\_NUMBER = 1.0 # no units

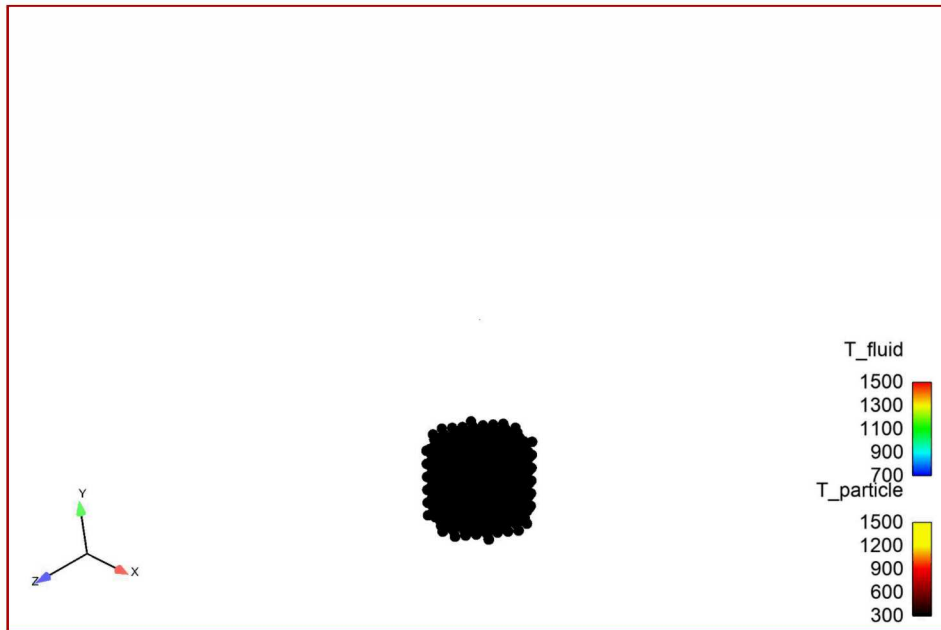
SURFACE\_TENSION = 1.0e3 # J/m<sup>2</sup>

END PARTICLE MATERIAL materialA



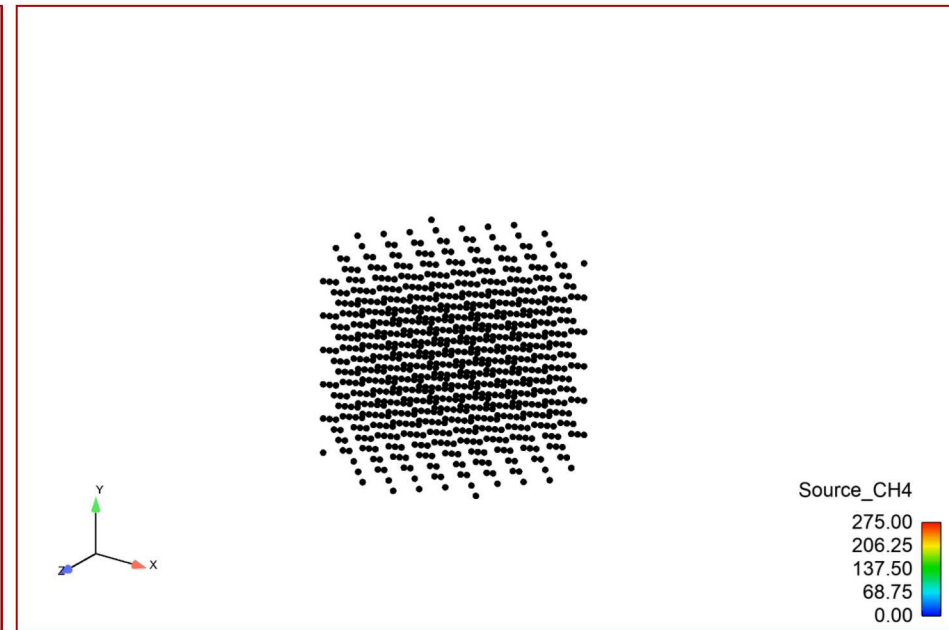
# Demonstration Case 1:

## Temperatures ( $T_f/T_p$ ) and $\text{CH}_4$ Source



Hot inflow on reacting particles.

- When  $T_p \approx 800\text{K}$ , particles release  $\text{CH}_4$
- $\text{CH}_4$  combustion (EDC)  $\rightarrow T_f > 1400\text{K}$  ( $T_f$  isosurfaces shown)
- After particles release  $\text{CH}_4$  they cool to inflow  $T \sim 1000\text{K}$



Source of  $\text{CH}_4$  : where particles heat up and release  $\text{CH}_4$

Last particles to burn out - those at center of particle pack

$\text{CH}_4$  source isosurfaces shown



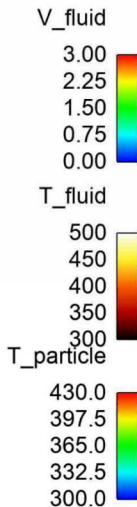
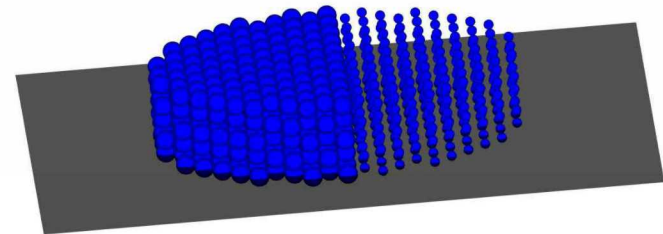
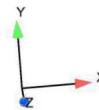
# Demonstration Case 2: Neighboring Bars w/ Layers

## Different Conditions

- BCs:
  - Base:
    - a:  $V_f = 1.0$  m/s (up) - square inlet at @  $T = 1000\text{K}$
    - b:  $V_f = 0.1$  m/s (up) - surrounds inlet @  $T = 300\text{K}$
  - Sides: walls @  $T = 300\text{K}$
  - Top: open boundary at  $T = 300\text{K}$
- 875 particles of size  $d = 0.02\text{m}$  in
  - 5 layers, 2 bars
  - $T_p(t = 0) = 300\text{K}$

Time = 0.0000

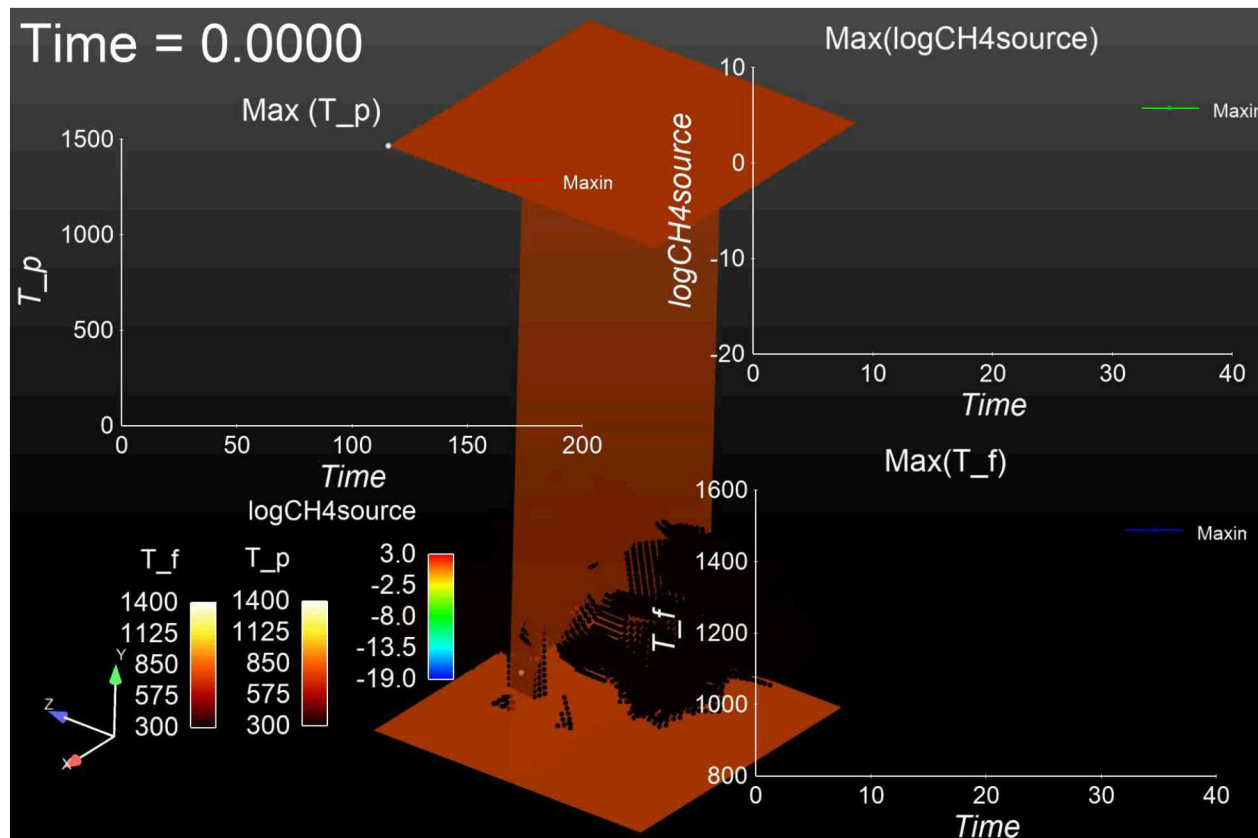
- Isosurface  $T_f = 500\text{K}$  shown
- Particles heated by fluid/conduction
  - Hot particles near hot fluid
- Particles visualized with size scaled by bar#
- $T_p$  not high enough to activate reaction for  $\text{CH}_4$  production (as in previous case)
- $t_{\text{late}}$  : different bars show obvious thermal non-contact





# Demonstration Case 3 – Rubble Pile

- Rubble pile configuration: Randomly placed/oriented bars - multiple layers

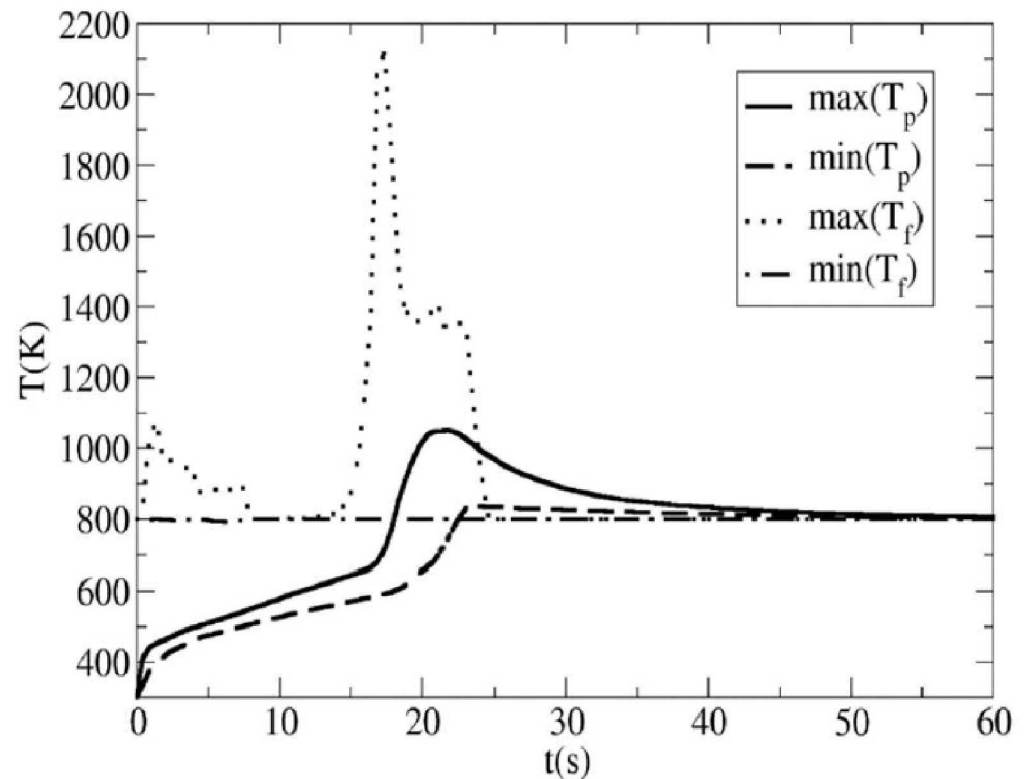


- T<sub>p</sub>, T<sub>f</sub>, CH<sub>4</sub> source shown vs. time
- 200s time interval



# Particle/Fluid Temperature Evolution

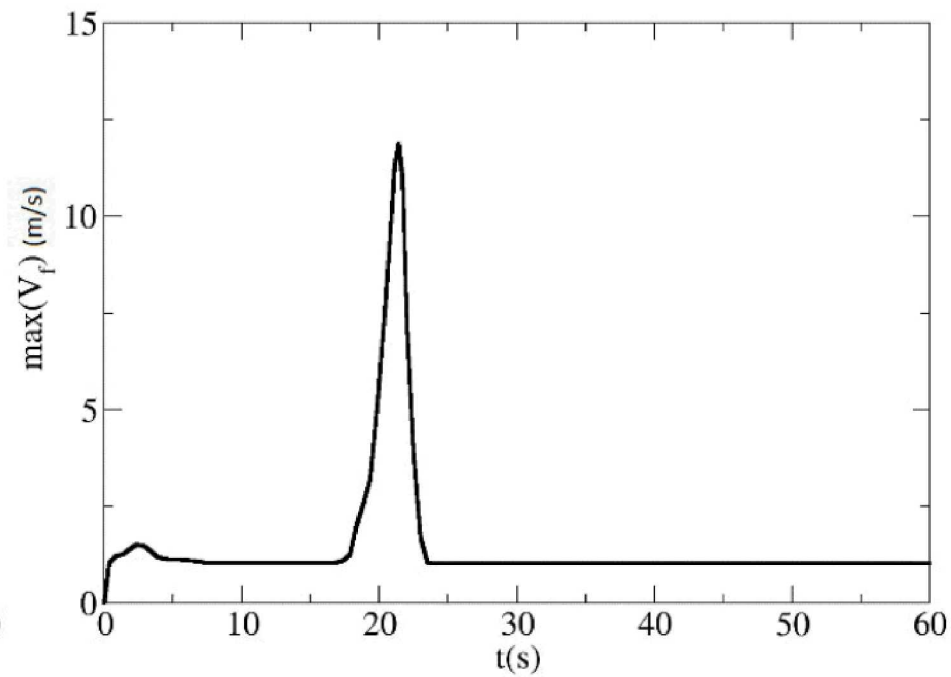
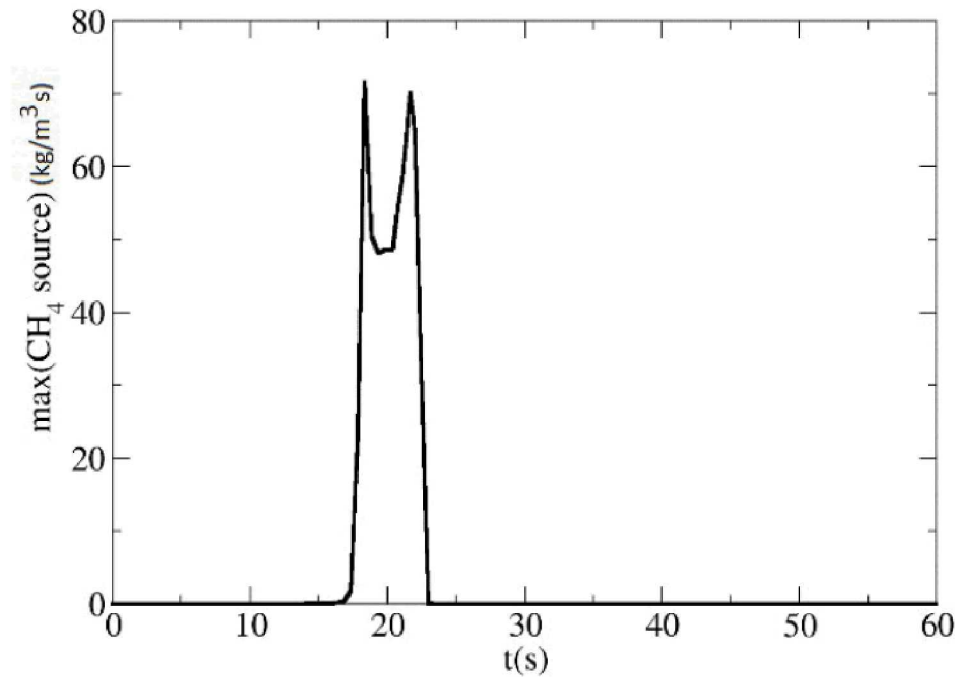
- $T_p \uparrow$  from initial (300K) due to hot inflow (800K)
- Highest  $T_p/T_f$  when  $\text{CH}_4$  combusts
  - Climbing: 15-16s
    - $T_p \sim 650\text{K}$
  - Falling: 22-23s
  - $T_p$  max lags  $T_f$ 
    - Particle thermal mass
- After particle  $\text{CH}_4$  release, particles/fluid cool to ambient
  - $T_p$  again lags  $T_f$  – thermal mass difference





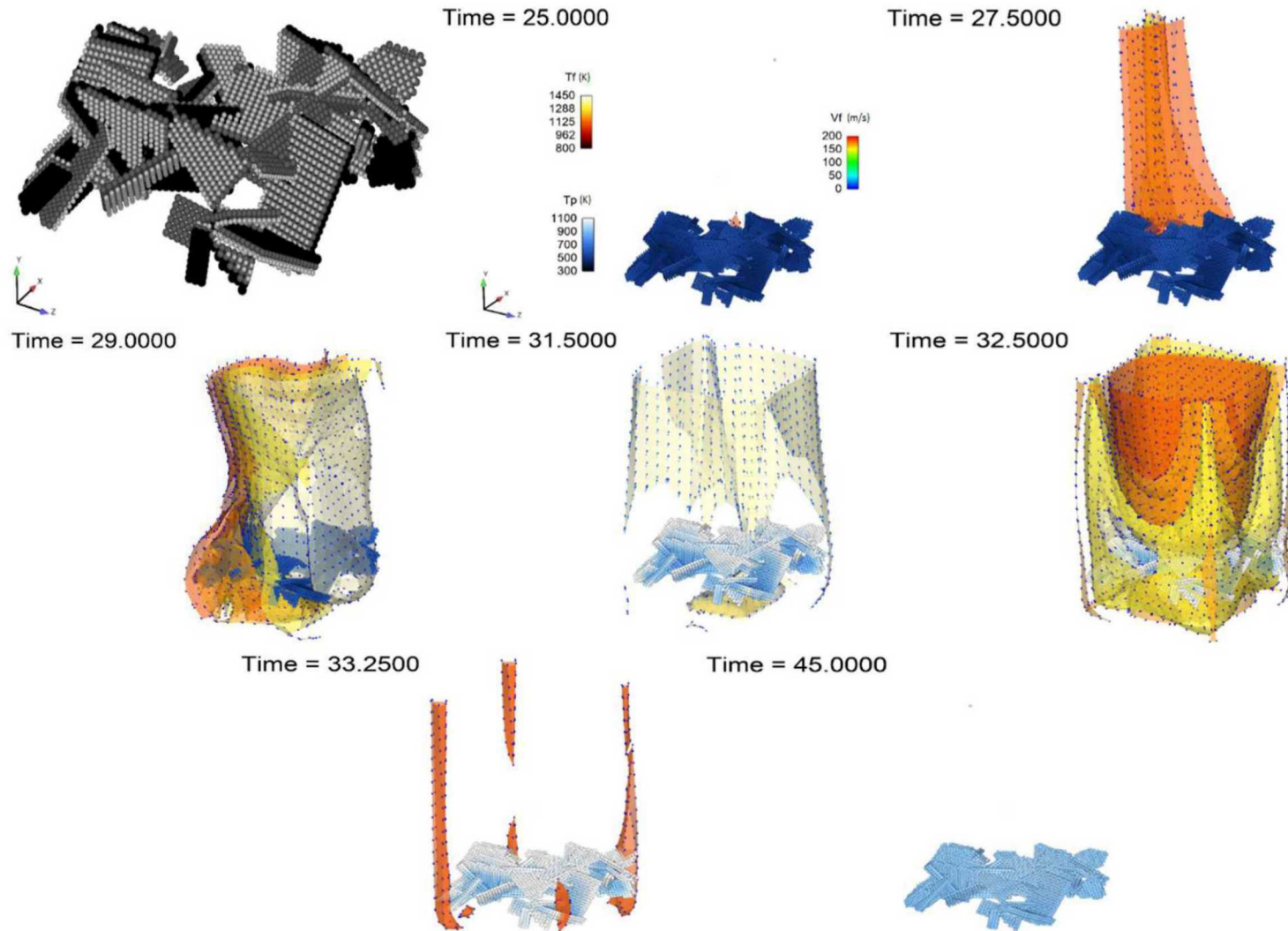
# Evolution of CH<sub>4</sub> release rate / Fluid Velocities

- Particle CH<sub>4</sub> release between 16 – 23 s
- Fluid Velocity during this interval





# Temporal Evolution of System





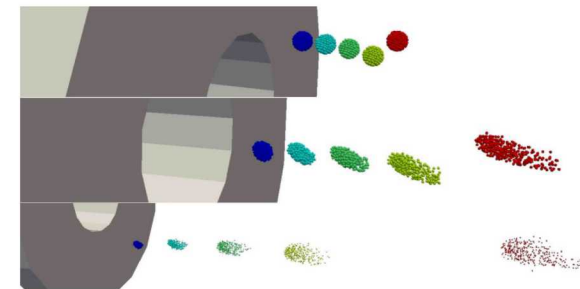
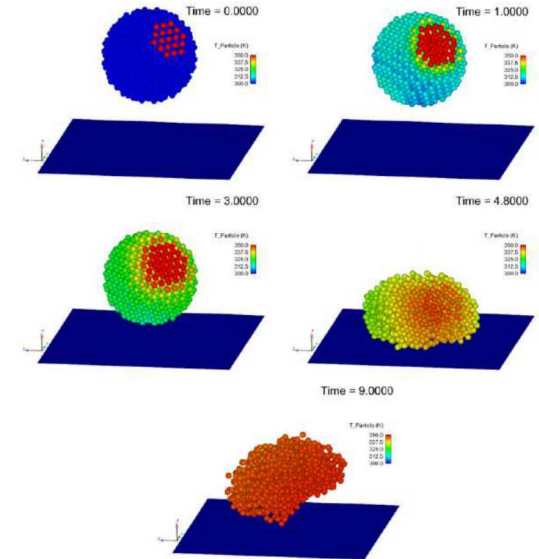
# Conclusions

- Reacting/Thermally interacting particles provide effective description of solid phase combustion as seen in carbon fiber – filled epoxy composites
- Useful in context of mixed fuel fires (liquid + solid)
- Evaporating volume of fluid (VOF) capability
  - in progress
  - Can be coupled to bar/layer reacting description to address full mixed phase fuel problem
- Work remains to be done
  - Rubble geometry currently doesn't change



# For the Future

- Better Chemistry Mechanisms
  - More representative of these materials
- Sophisticated fluid/particle coupling
  - Sandia LDRD - proposal stage of Fuego/LAMMPS coupling
  - Would allow for material motion
    - Layer collapse
    - Ember lofting
    - Interaction with fluid
  - Ongoing progress – significant additions to particle/particle, particle/fluid capabilities to Fuego





# Acknowledgements

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