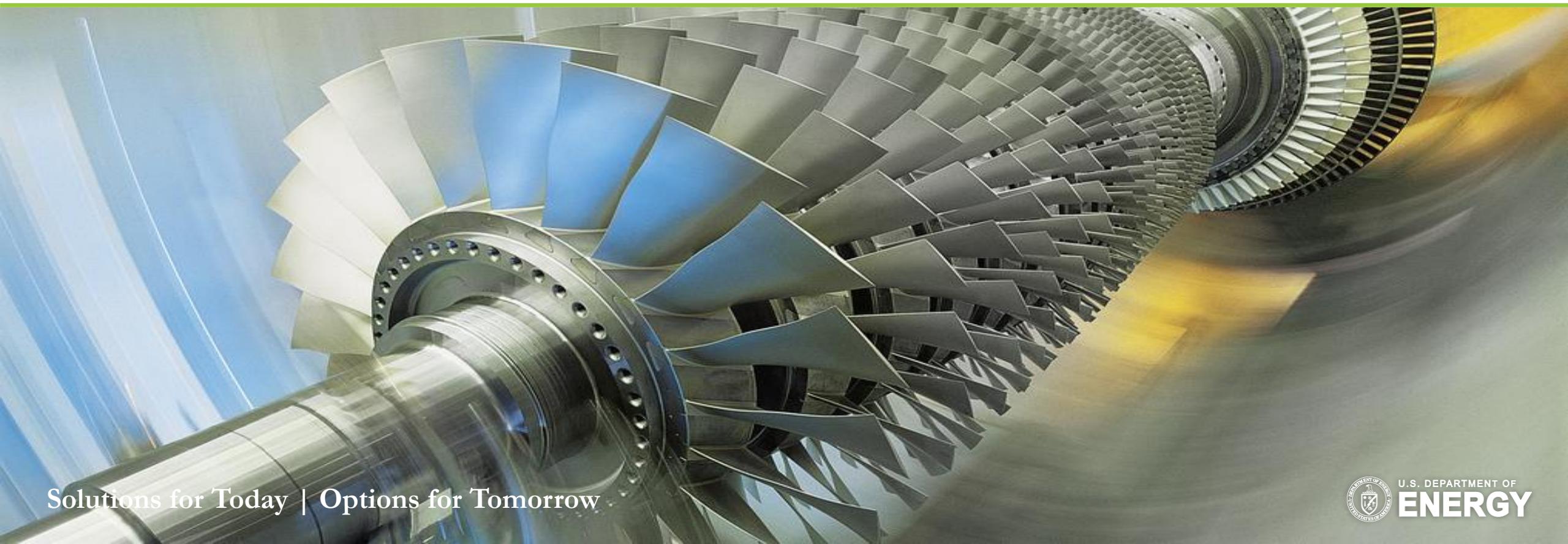


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Dynamic Modeling and Control of a 10 MWe Supercritical CO₂ Recompression Closed Brayton Cycle

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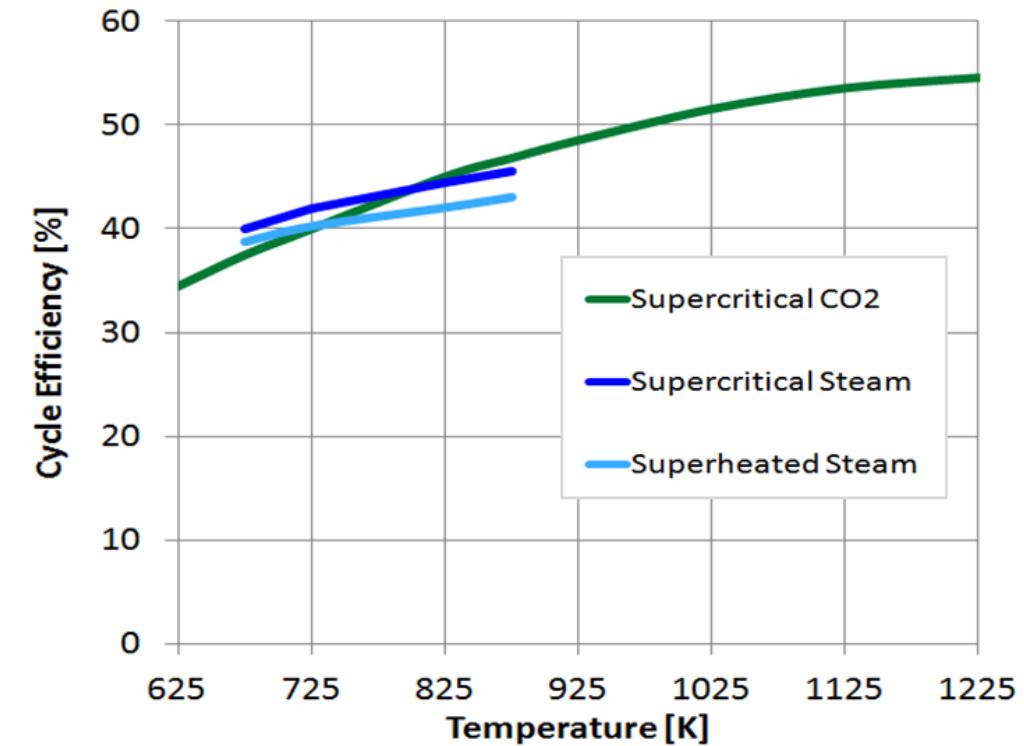
Solutions for Today | Options for Tomorrow



Motivation

Supercritical CO₂ (sCO₂) Brayton Power Cycles

- Potential for higher efficiencies than traditional steam Rankine cycles at equivalent turbine inlet conditions
- Higher density of the sCO₂ working fluid compared to supercritical steam
 - Reduces compressor power requirements
 - Reduces size of turbomachinery by approximately 10X
- Offers potential for flexible operations
 - High efficiency for part-load
 - Low minimum loads
 - Fast ramping

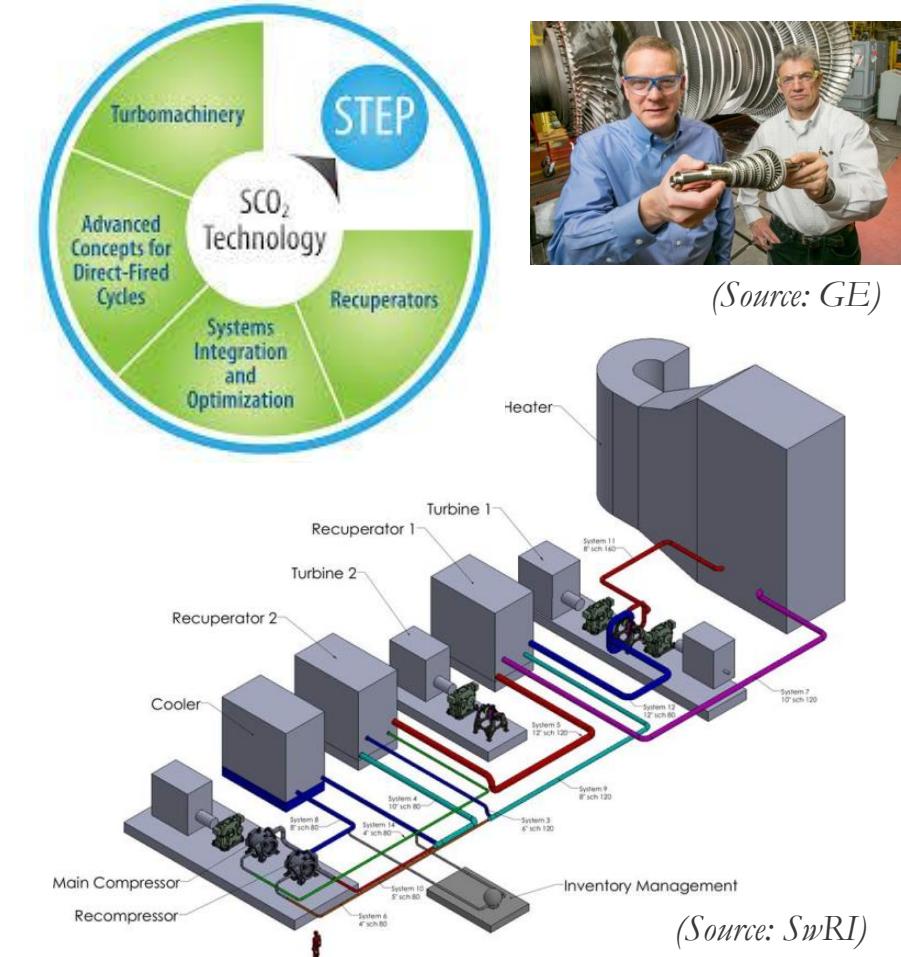


Motivation

U.S. DOE STEP Program: 10 MWe sCO₂ Pilot Plant



- U.S. DOE's Supercritical Transformational Electric Power (STEP) Program
- sCO₂ Pilot Plant Test Facility
 - Awarded to team led by:   
SOUTHWEST RESEARCH INSTITUTE
 - Plan, design, build, and operate an indirect-fired 10 MWe sCO₂ recompression Brayton cycle
 - Turbine inlet temperature: 700-715 °C
 - Verify performance of key components
 - Turbomachinery, heat exchangers, ...
 - Demonstrate cycle design, integration, operability, and controls



(Source: GE)

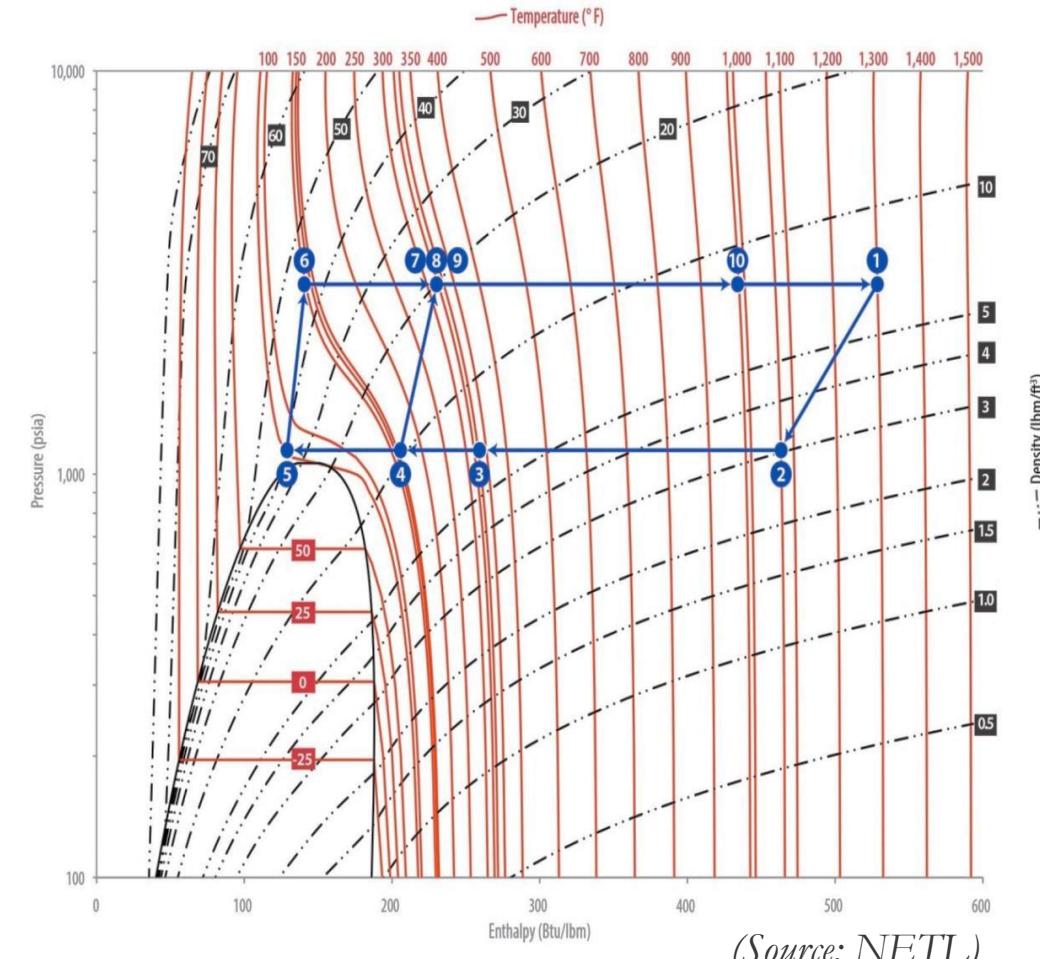
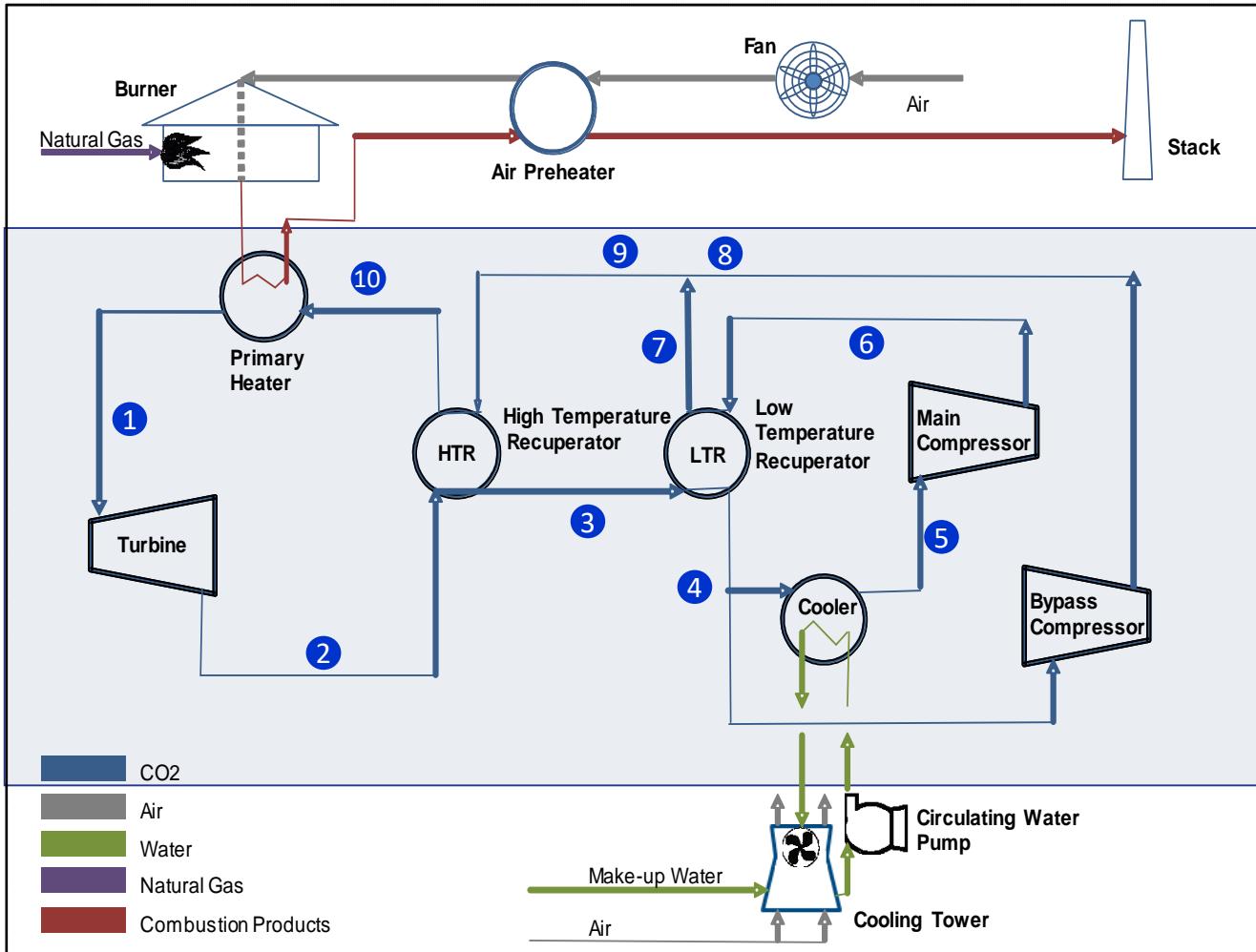


Presentation Overview



- sCO₂ Recompression Brayton Cycle Overview and Dynamic Modeling
- Regulatory Controls for Maximizing Efficiency
- Transient Results for Load-Following Operation
- Concluding Remarks and Ongoing/Future Work

sCO₂ Recompression Brayton Pilot Plant Process Overview



(Source: NETL)



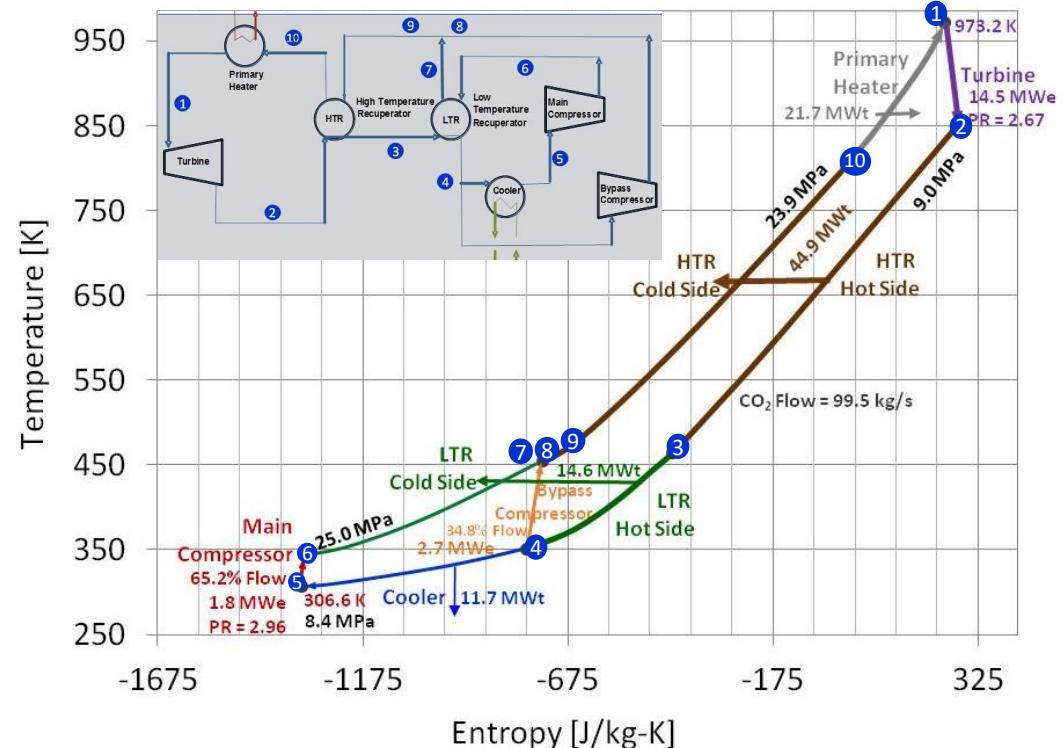
U.S. DEPARTMENT OF
ENERGY

sCO₂ Recompression Brayton Pilot Plant Dynamic Modeling

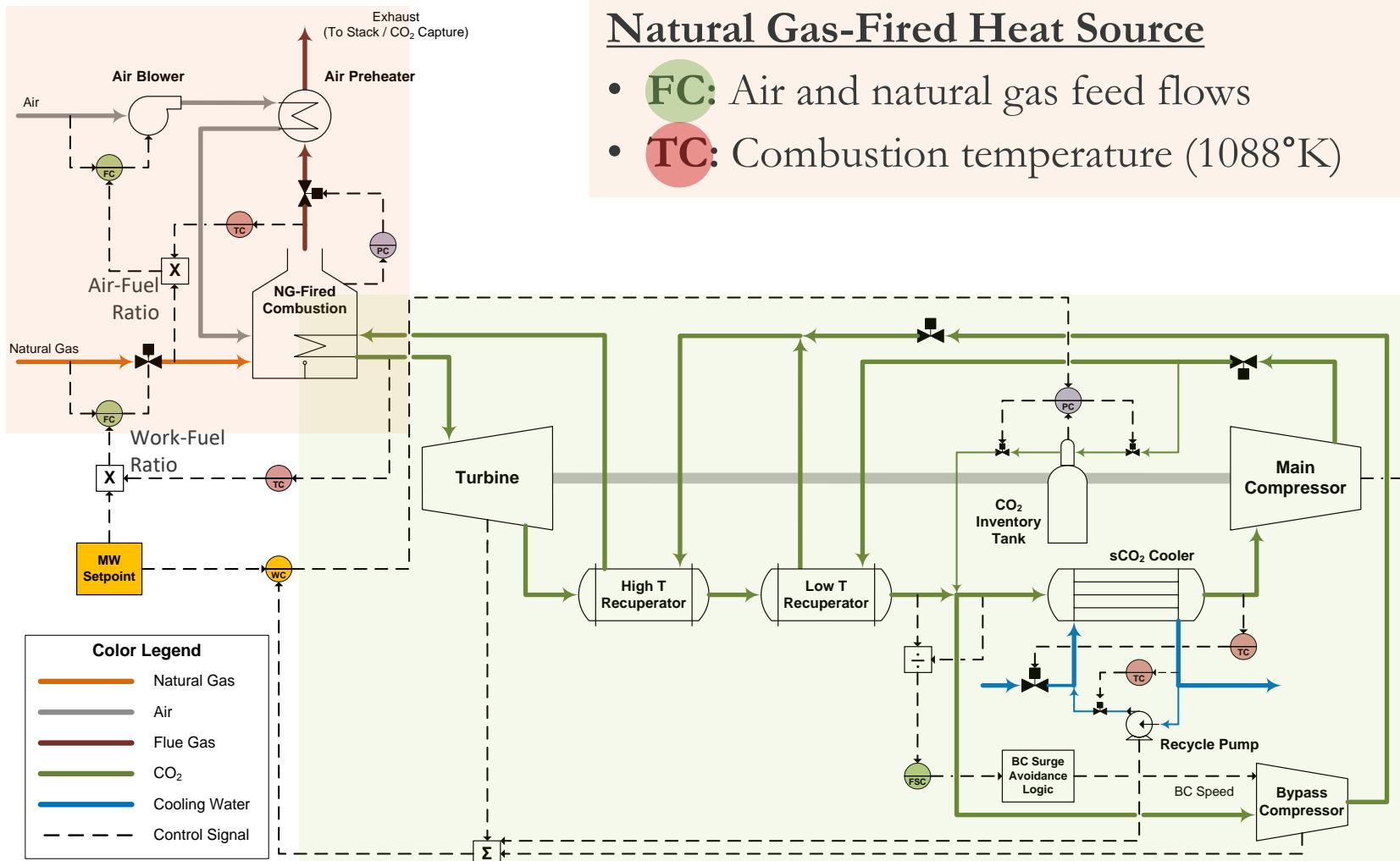


- Software
 - Aspen Plus Dynamics
- Properties
 - NIST REFPROP[†]
- Dynamic Equipment Models
 - Heat Exchangers
 - Shell-and-tube, countercurrent flow
 - Volume, ΔP , metal mass, heat transfer
 - Turbomachinery
 - Isentropic expansion/compression
 - Performance and efficiency curves
 - Piping^{††}
 - Volume, ΔP , and heat transfer

- Dynamic Results at Full Load (10MWe)
 - Heat Input = 21.7 MWt, Efficiency = 46.1%
 - HTR Duty = 44.9 MWt, LTR Duty = 14.6 MWt
 - Turbine PR = 2.67, BC Flow Split = 34.8%

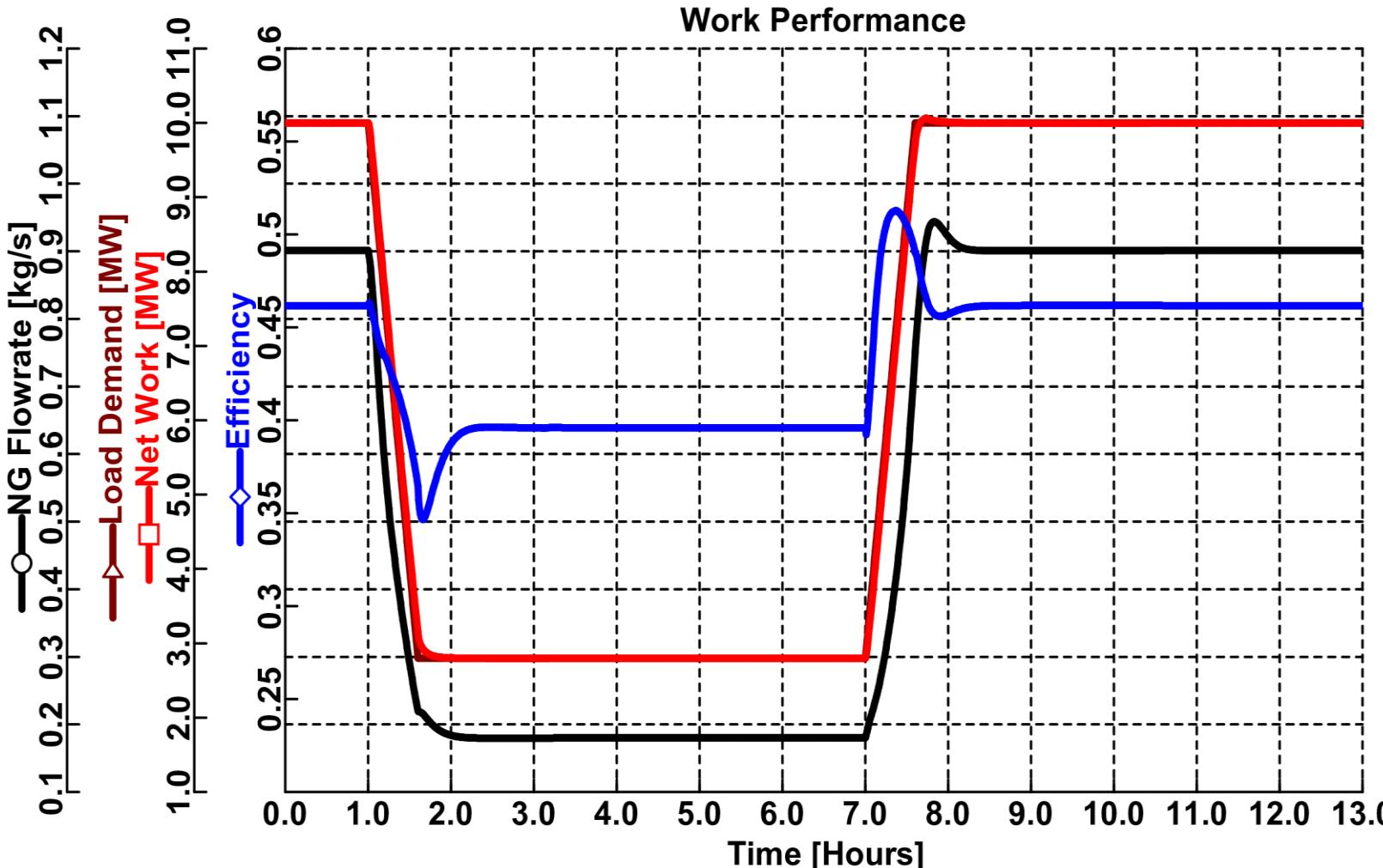


sCO₂ Recompression Brayton Pilot Plant Control Architecture – Maximize Efficiency



Load-Following Results

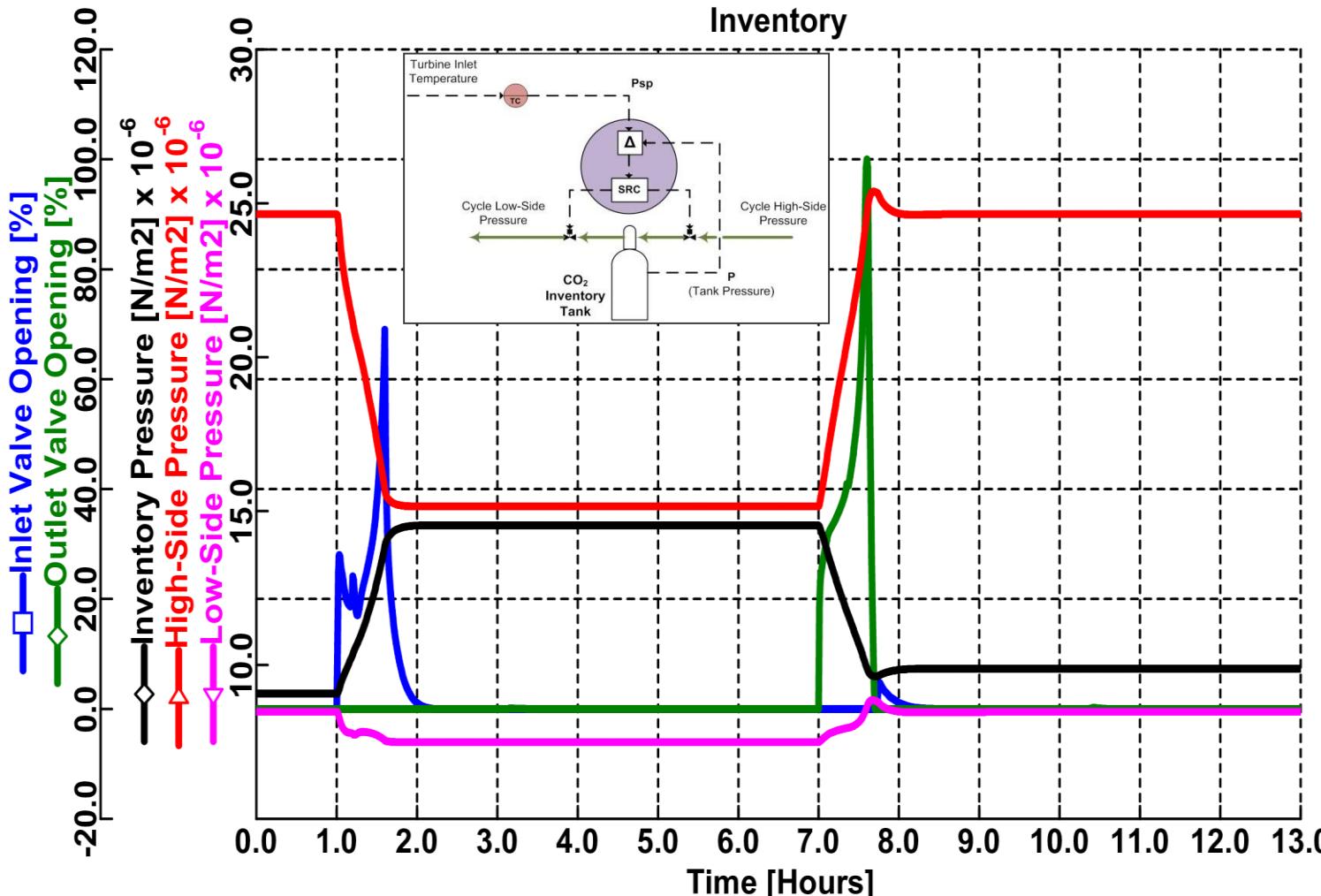
Ramp Down from Full-Load (10 MWe) to 28% Load (2.8 MWe) and Ramp Back Up to Full-Load



- **Load demand** ramped down over a period 0.6 hr (2%/min)
- During ramp-down, **NG flowrate** is reduced and $s\text{CO}_2$ is rapidly removed from the cycle into the inventory tank (Opposite for ramp up)
- 28% load is minimum load at which TIT can be kept at its design value (973°K)
- **Efficiency** drops from 46% to 40%
- Ramp back up to full-load at $t = 7$ hr using same ramp rate
- **Actual net-work** closely follows the **load demand** with no visible lag

Load-Following Results

Inventory Control



Ramp Down

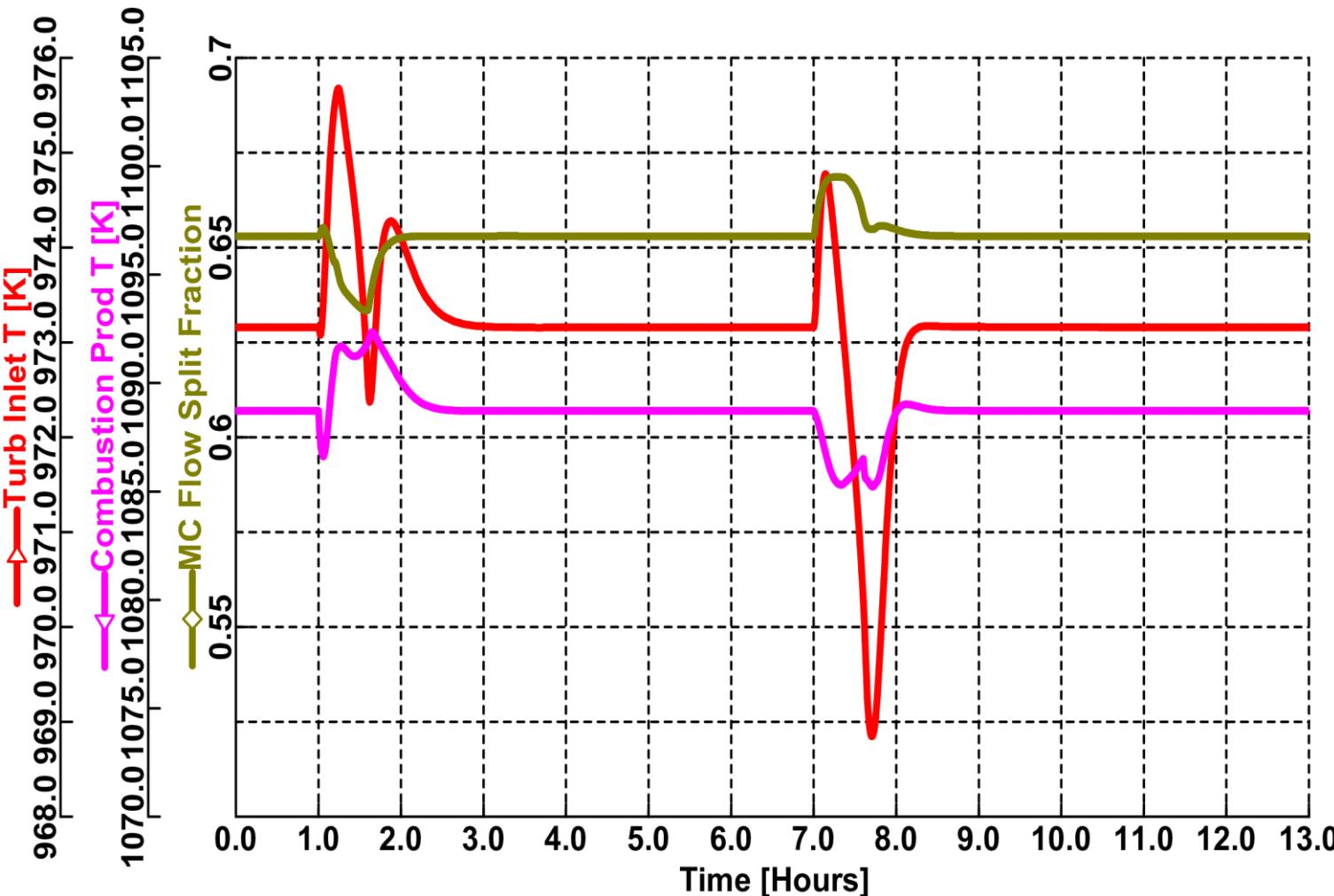
- sCO₂ cycle **high-side pressure** and **low-side pressure** slide down
- sCO₂ is diverted into inventory tank by opening **inlet valve**
- Inventory **tank pressure** increases

Ramp Up

- sCO₂ is put back into cycle by opening **outlet valve**, thereby reducing **tank pressure**
- Split-range controller logic ensures that both valves are never open at the same time, thereby avoiding continuous sCO₂ flow across the tank

Load-Following Results

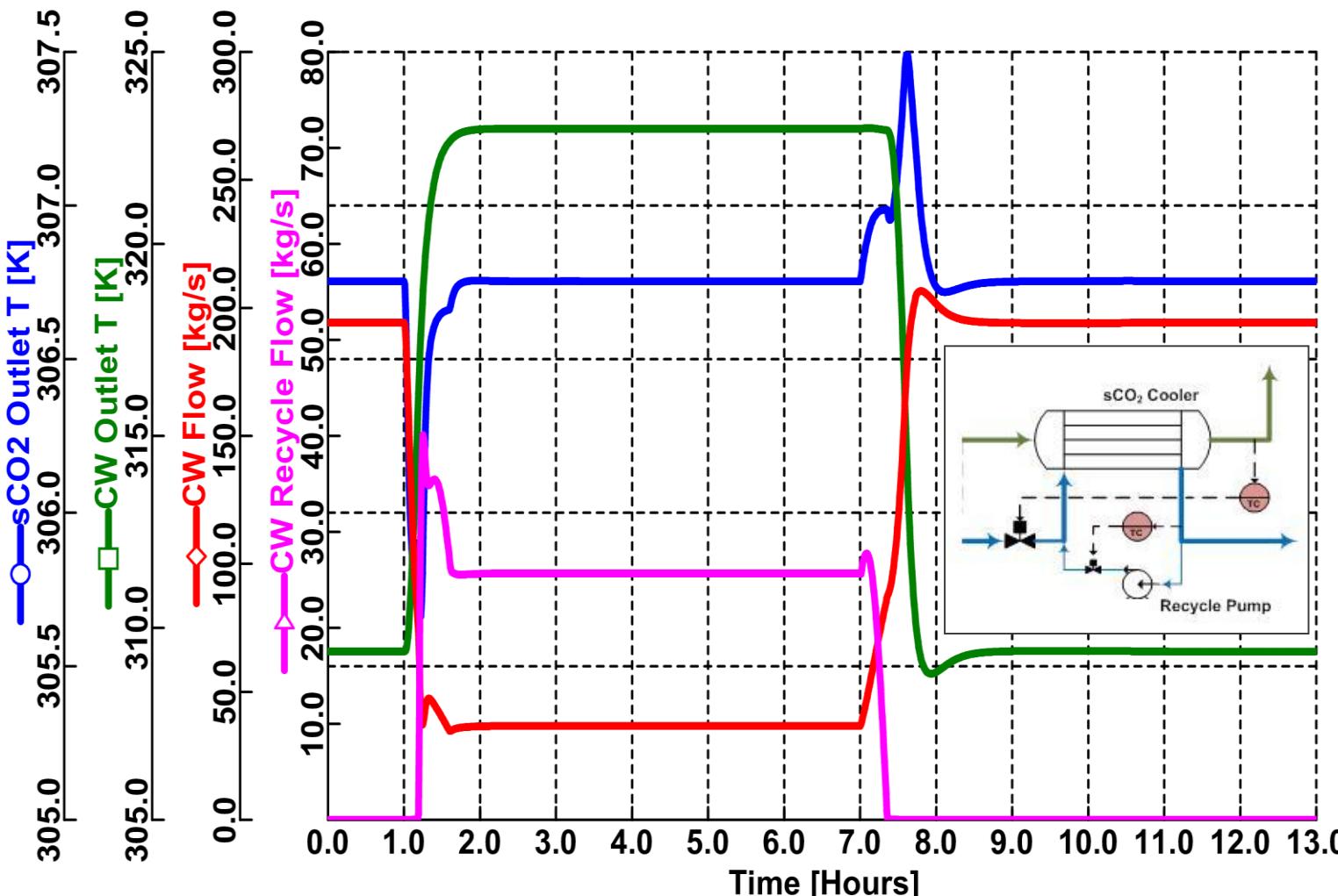
TIT and Combustion Temperature Control



- **TIT** remains within 5°K of design (973°K) and well below UB of 988°K
- **Combustion temperature** is well controlled in the NG furnace which serves as the indirect heat source to the sCO₂ cycle
- **Flow split** between BC and MC is also well controlled

Load-Following Results

$s\text{CO}_2$ MCIT and Cooling Water Temperature Control



Ramp Down

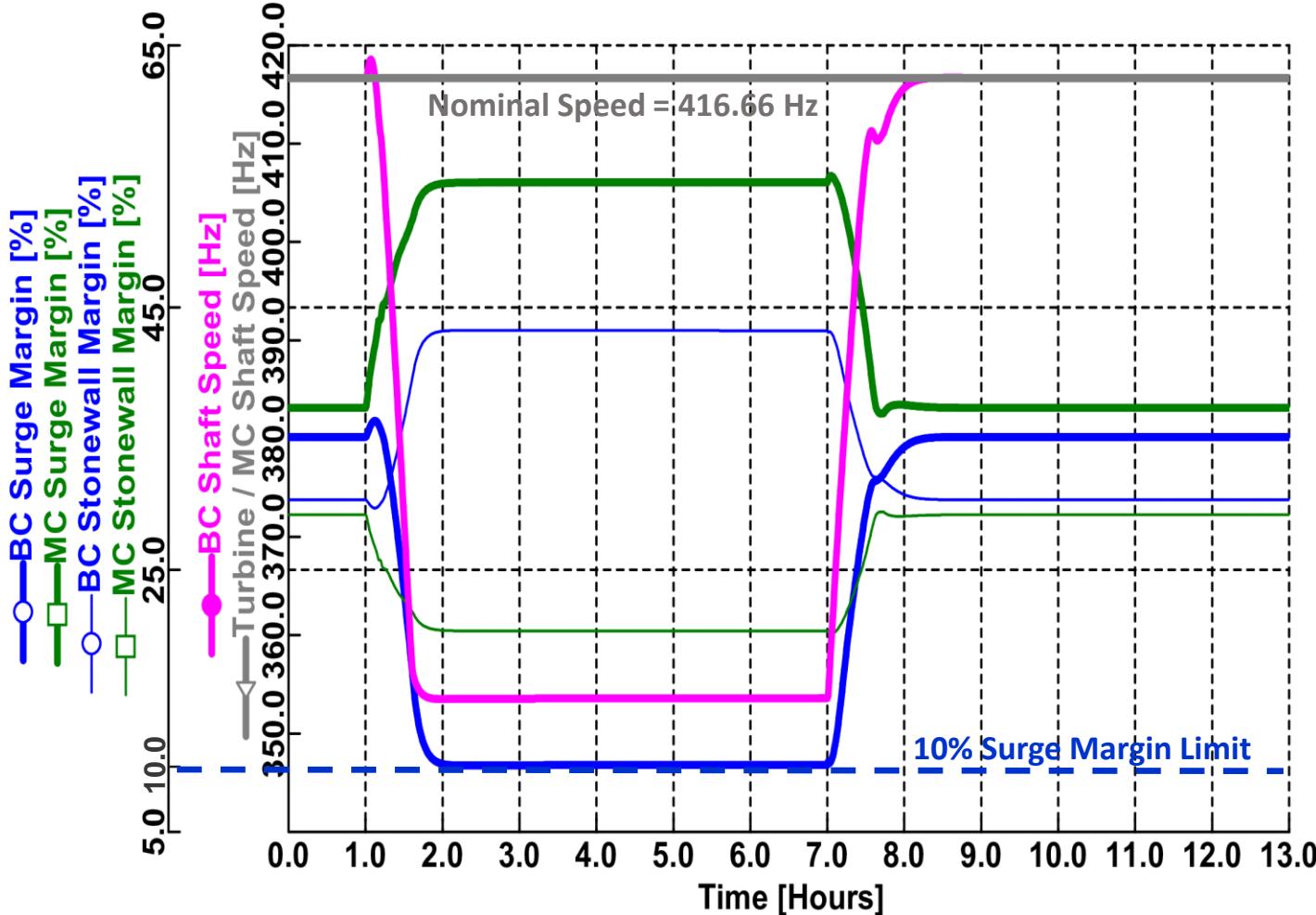
- **CW flow** decreases, keeping $s\text{CO}_2$ MCIT > LB of 304.1°K (T_{Critical})
- **CW outlet temperature** rapidly rises during turndown
- **CW recycle starts** to keep the **CW outlet temperature** at its UB of 323°K

Ramp Down/Up

- **MCIT** is well controlled with a net variation of 1°K

Load-Following Results

Flow-Split Control: Compressor Speeds and Surge Margins



Ramp Down

- In the presence of flow-split-control, (FSC) the **BC shaft-speed** is reduced to maintain the design sCO₂ flow split at its design value
- More flow goes through the MC, increasing the **MC surge margin**
- **BC surge margin** moves very close to constraint of 10%

Comments

- FSC using varying **BC shaft-speed** adds operational complexity
- **BC surge margin** becomes a factor at low loads, requiring the need for surge control

Concluding Remarks

- Developed pressure-driven dynamic model of a 10MWe sCO₂ recompression Brayton pilot plant
- Developed regulatory controls for maximizing efficiency of load-following operations
 - Sliding-pressure operation via inventory control used to maintain TIT
 - CW flow used to maintain sCO₂ MCIT above T_{critical}
 - Flow-split-control used to increase efficiency during load-following operation
- Analyzed cycle performance and control for MW-demand turndown and subsequent ramp-up at a 2%/min ramp rate
 - TIT is maintained at design (973°K) down to 28% load
 - Efficiency over 40% is maintained throughout turndown to 28% load
- Further turndown is achievable using a combination of inventory, flow split, and flow-rate control, while letting the TIT drop below design value[†]

Ongoing and Future Work

10MWe sCO₂ Recompression Brayton Cycle



- **Dynamic Modeling and Control**
 - Compact heat exchanger for cooler and recuperators
 - Turbine controls and compressor surge control
 - Advanced process control, including model predictive control
- **Transient Operations**
 - Startup and shutdown
 - Safety analysis
- **Validation**
 - Exploit real-time data from STEP pilot plant test facility
 - Validate dynamic models and controls

Websites and Contact Information

Office of Fossil Energy: www.energy.gov/fe/office-fossil-energy

NETL: www.netl.doe.gov/

SCO₂ Technology

Program: www.netl.doe.gov/research/coal/energy-systems/sco2-technology

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