

Oxy-Combustion Modeling for Direct-Fired sCO₂ Power Cycles

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Background and Motivation

Allam Cycle (NetPower)

- Direct-fired (Allam) cycle operates at very high pressures (300 bar) with CO₂ dilution.
- There is a lack of experimental data and modeling experience at these conditions.
- CFD is expected to play a key role in combustor design (flame holding, heat release, CO formation, etc...).
- CO has a significant impact on cycle efficiency.
- Combustion sub-models have not been validated at these conditions.

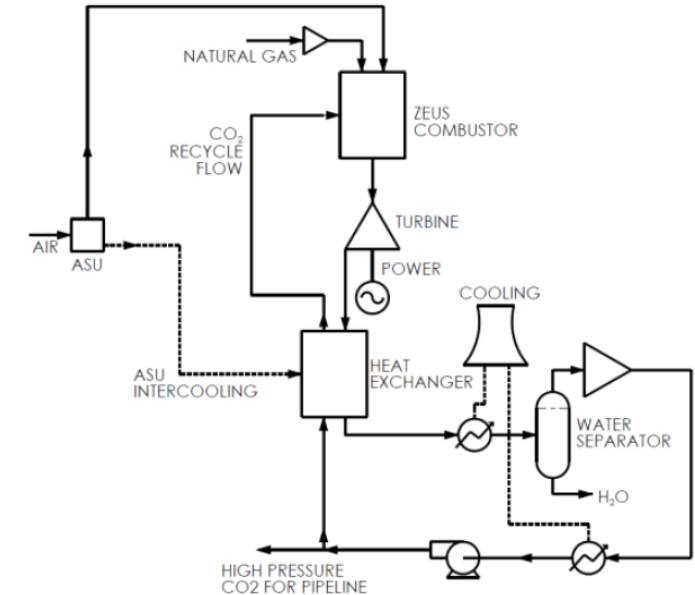


Figure 1. BASIC ALLAM CYCLE NATURAL GAS FLOW DIAGRAM.

Point	Pressure (Bar)	Temperature (°C)
Turbine Inlet (A)	300	1150
Turbine Outlet (B)	30	775
CO2 Compressor Inlet (D)	30	20
CO2 Compressor Outlet (E)	80	65
CO2 Pump Inlet (F)	80	20
CO2 Pump Outlet (G)	300	55
Combustor Inlet (I)	300	750

Three Combustion Modeling Approaches

Three of many...

1) No Turbulence Chemistry Interaction (Laminar).

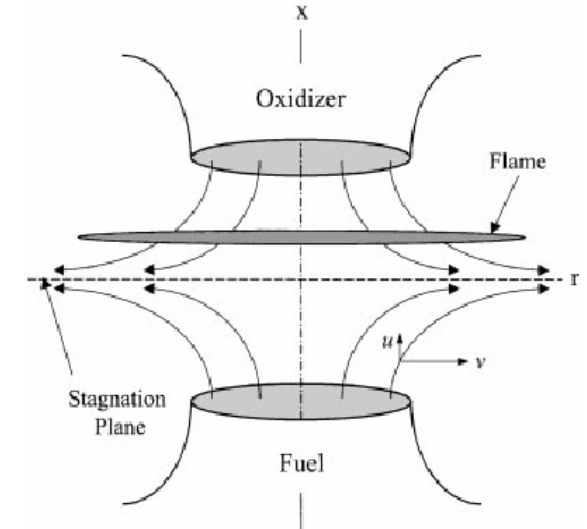
- Ignores sub-grid fluctuations in temperature and concentration.
- Similar to fast mixing at the sub-grid scale.

2) Flamelet Model.

- Assumes turbulent flame is an ensemble of strained laminar flamelets.
- Pre-tabulated table of thermodynamic properties as a function of mixture fraction and local strain rate.

3) Filtered Density Function (composition PDF transport).

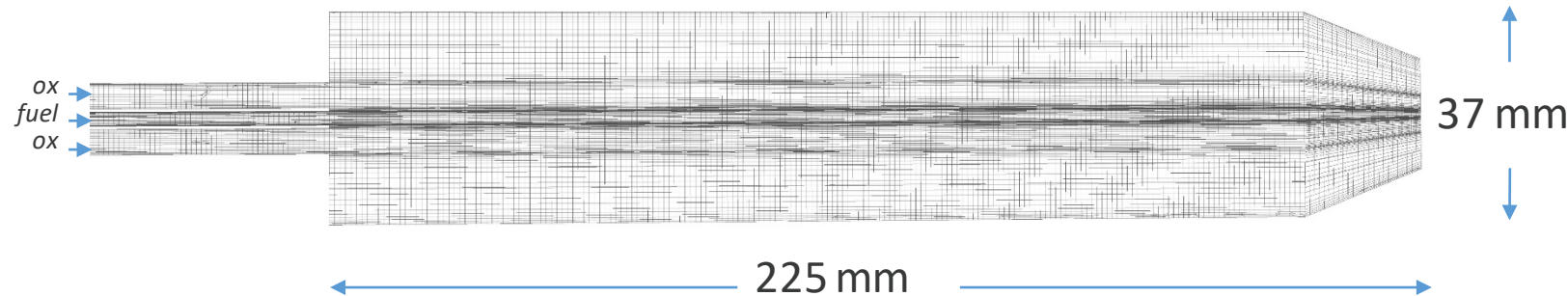
- Transport equation for single-point joint PDF solved (thermochemical state).
- Chemical source term is closed but molecular mixing must be modeled.
- Solved by Monte-Carlo methods (Lagrangian “particle” tracking).
- Coupling with flow solver through density.



$$\begin{aligned} & \frac{\partial F_L}{\partial t} + \frac{\partial [\langle u_i \rangle_L F_L]}{\partial x_i} \\ &= \frac{\partial}{\partial x_i} \left[\left(\gamma + \gamma_t \right) \frac{\partial \left(\frac{F_L}{\langle \rho \rangle_L} \right)}{\partial x_i} \right] \\ &+ \frac{\partial}{\partial \psi_\alpha} [\Omega_m (\psi_\alpha - \langle \varphi_\alpha \rangle_L) F_L] - \frac{\partial (S_\alpha F_L)}{\partial \psi_\alpha} \end{aligned}$$

Computational Setup

Single Injector Domain



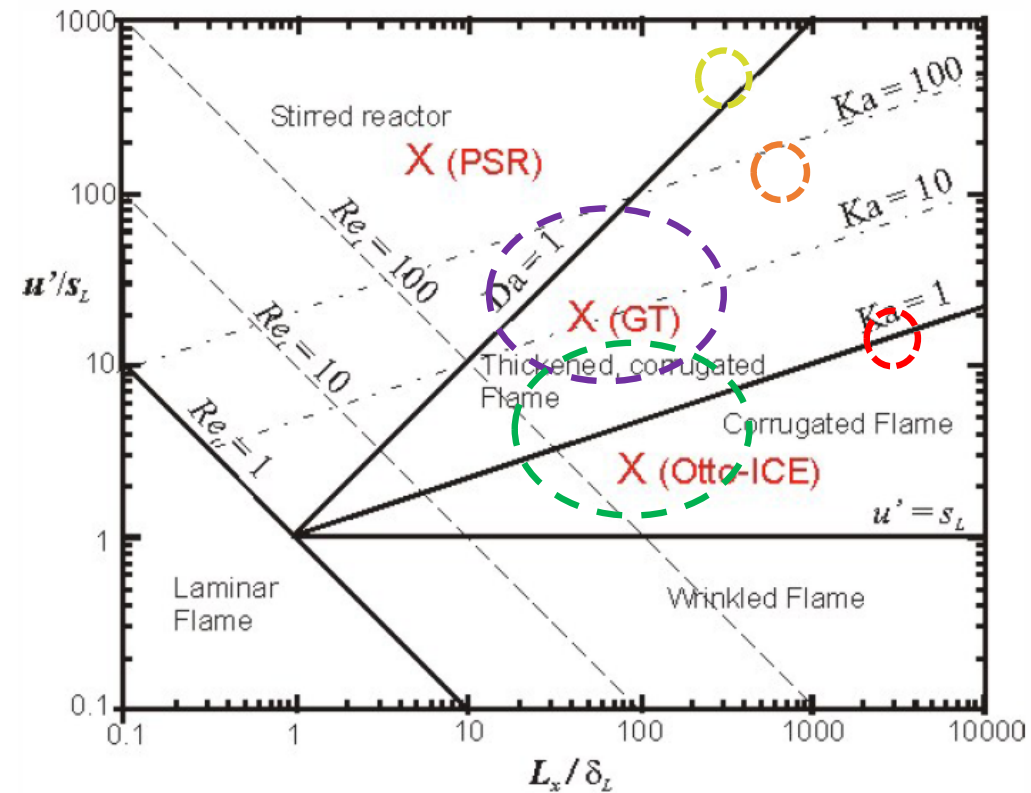
3D 590k hex cells
 $m_F = 0.04762 \text{ kg/s}$
 $\Phi = 0.95$
 $T_F = 476 \text{ K}$
 $T_O = 1014 \text{ K}$
 $P = 300 \text{ bar}$
2.4 MW

- Large Eddy Simulation with transported k -equation.
- 16 Species skeletal mechanism from UCF.*
- Incompressible, pressure-based solver. 2nd order in space and time. Max Courant # ~ 1 .
- CO₂ added to oxidizer stream to change O₂ concentration.
- ANSYS Fluent V18.2

parameter	Case 1	Case 2	Case 3
O ₂ mass fraction	0.250	0.138	0.070
U _{ox} (m/s)	54	94	180
l _T (m)	1.9e-3	2.2e-3	2.0e-3
U' (m/s)	7.5	10.7	23.8
S _L (m/s)	0.58	0.082	0.05
τ_{ign} (s)	1.5e-3	1.6e-3	2.0e-3

Borghi Diagram for Oxy-Combustion

- Three cases shown for 300 bar oxy-combustion define a range of conditions (O_2 from 7-25%) spanning the thickened, corrugated flame regime and stirred reactor.
- Significantly outside the range of gas turbine and IC engine operation.
 - $Re_\#$ and/or $Ka_\#$ significantly larger than gas turbines or IC engines.
- Requires assessment of appropriate turbulent combustion models.

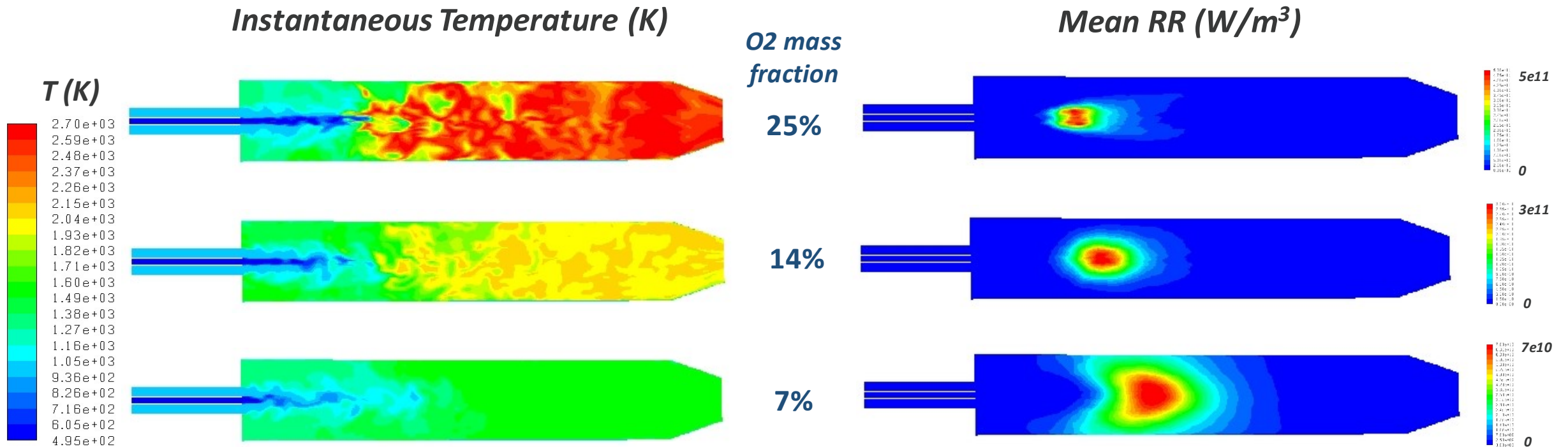


Gas Turbines
IC Engines
sCO₂ 25%O₂
sCO₂ 14%O₂
sCO₂ 7%O₂

Effect of O₂ Concentration

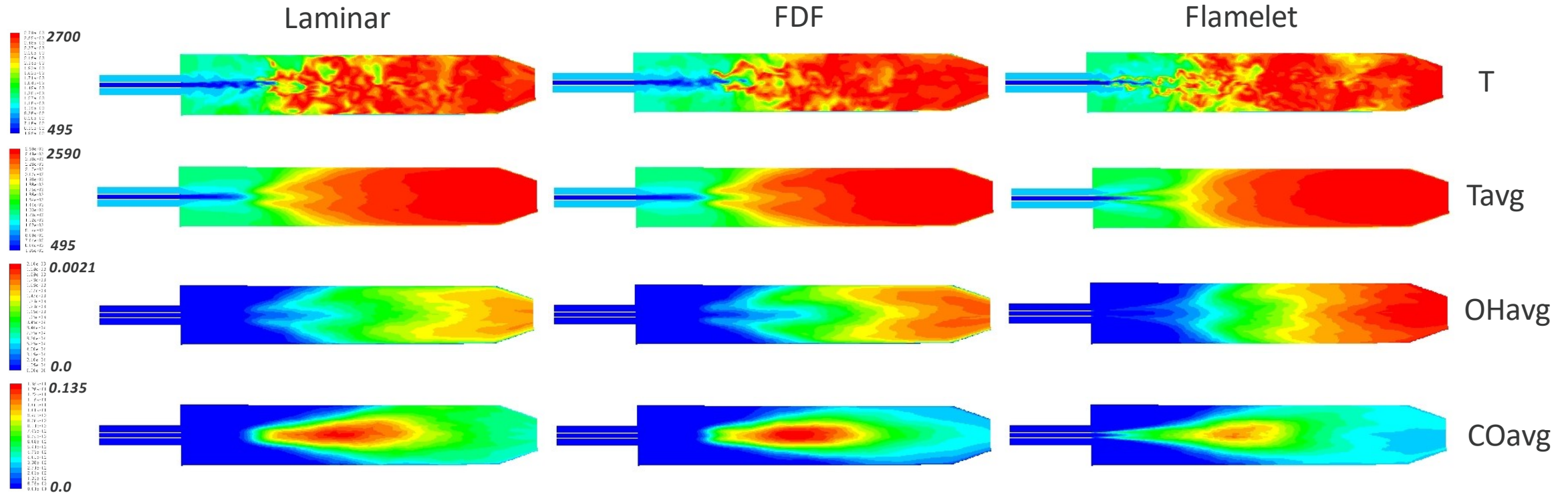
Laminar Model

- Lifted flame at 25% O₂ transitions to autoignition reaction at 7% O₂.
- Similar behavior for both Laminar and FDF models.
- Flamelet model unable to predict autoignition behavior for 7% O₂ case.



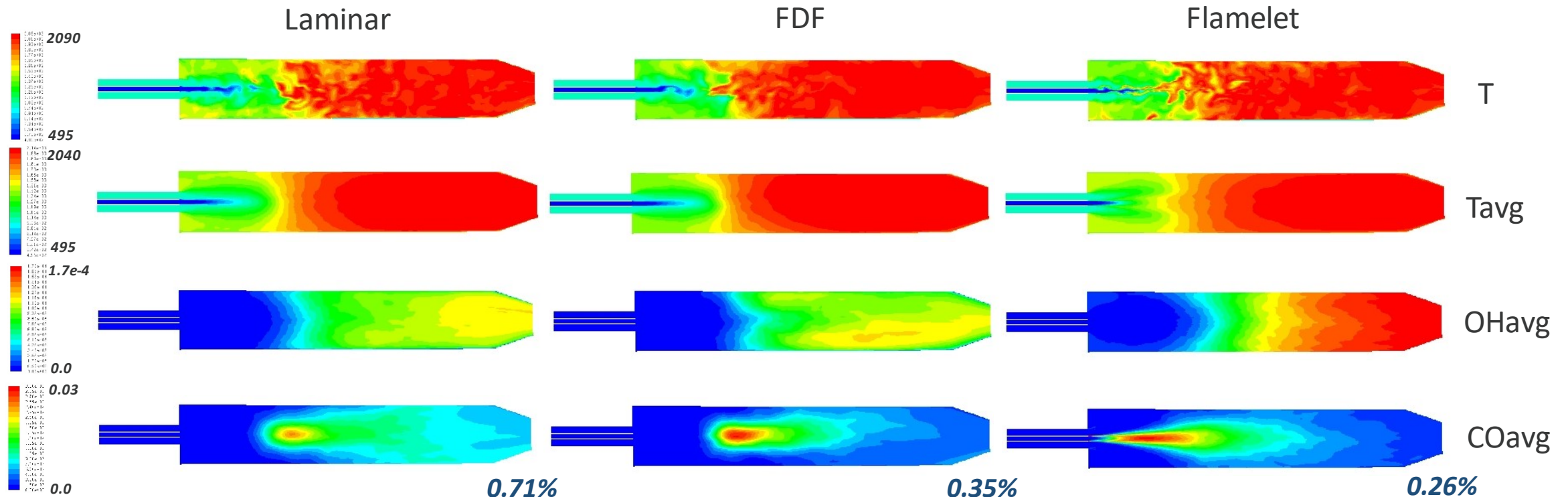
Results for Case 1 (25% O₂)

- Similar flame shape for all three models (lifted flame).
- Peak CO concentration similar for Laminar and FDF models although FDF predicted lower exit CO (3.0% vs 4.4% mass fraction). Maybe better burnout?



Results for Case 2 (14% O₂)

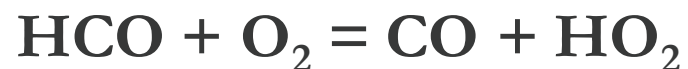
- Similar flame shape for Laminar and FDF models, Flamelet model predicts intermittent flame attachment to injector.
- Similar trend in CO for Laminar and FDF models (similar peak CO and better burnout for FDF model).



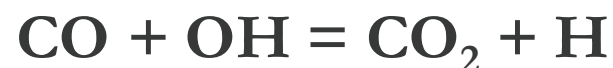
CO Formation and Destruction

16 Species Skeletal Mechanism*

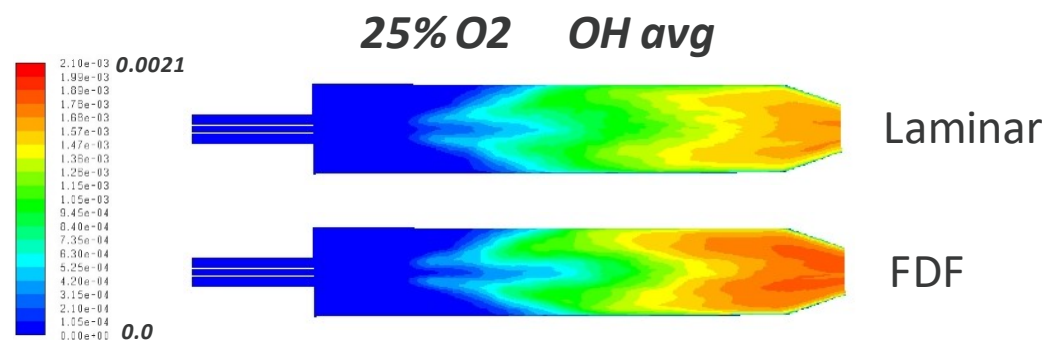
- Main CO formation paths:



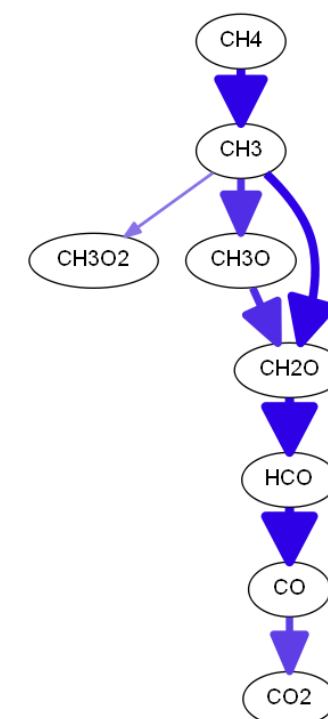
- Main oxidation path:



- Since Laminar and FDF models show similar temperature and OH profiles, “burnout” is not likely the cause of discrepancy in exit CO.



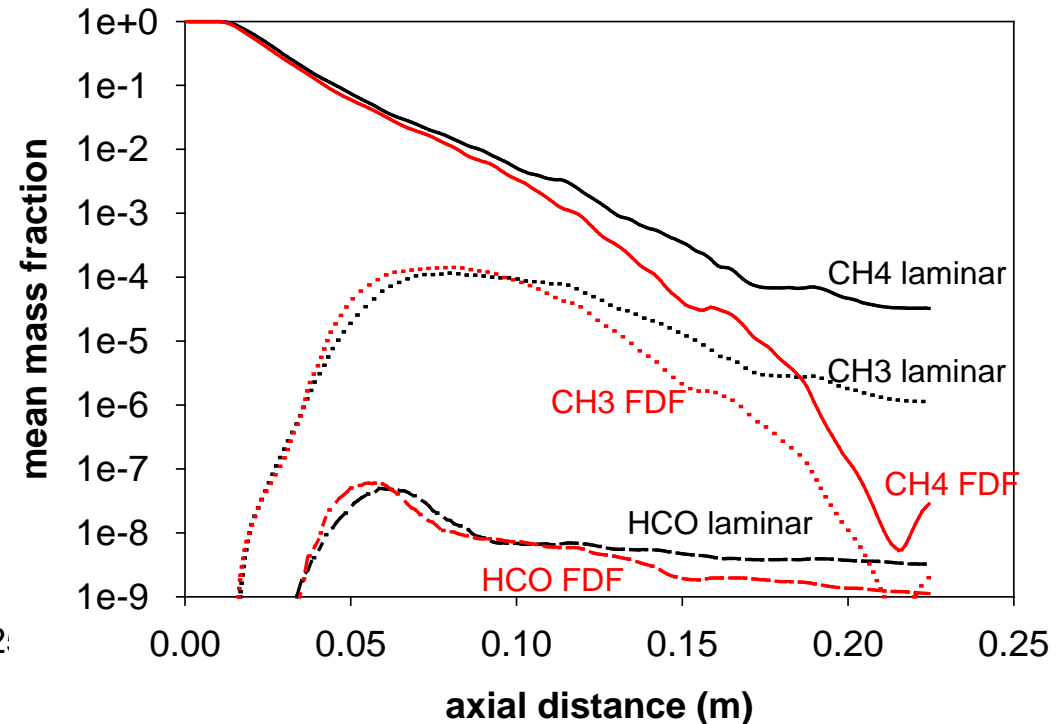
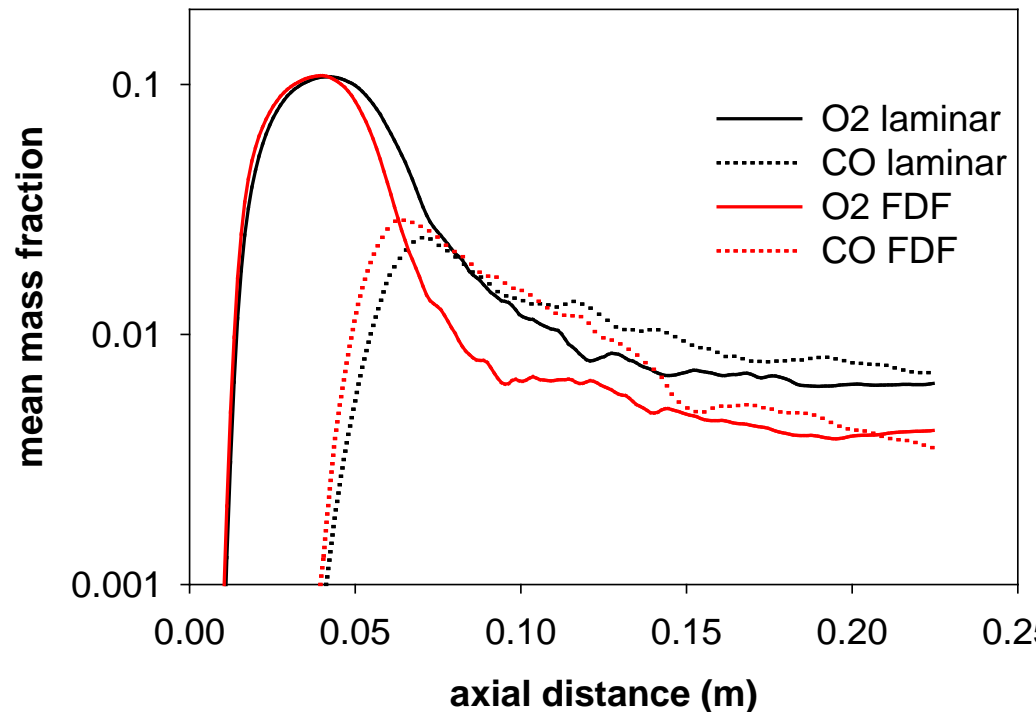
Path Flux Analysis



Scale = 1.2e+06
Reaction path diagram following C

Centerline profiles for Case 2 (14% O₂)

Mean Mass Fractions

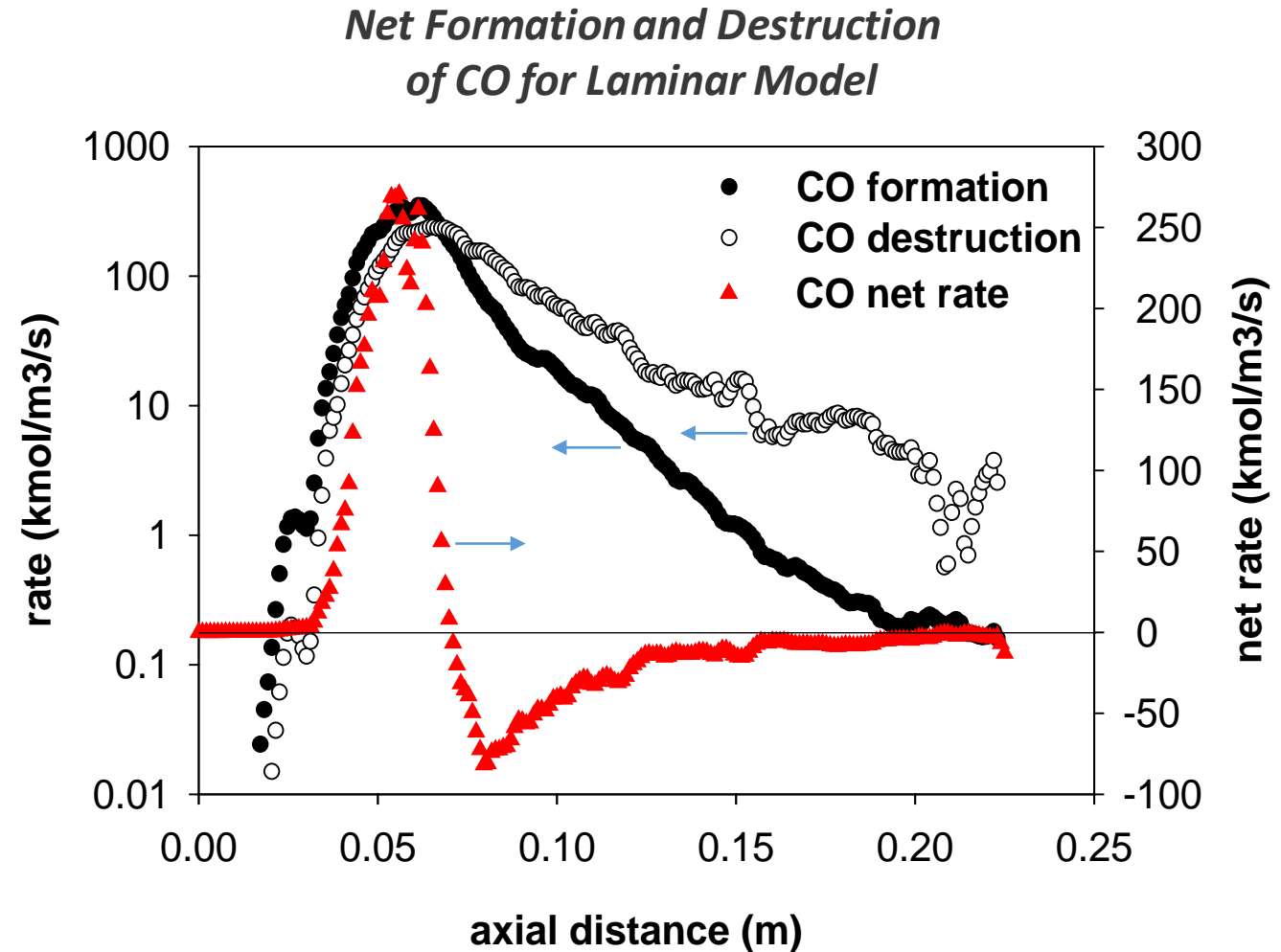


- More rapid decay in CO (and O₂) concentration for FDF model (left plot).
- Right plot shows higher concentrations of unburned fuel for Laminar model (higher CH₄, CH₃, HCO).

Centerline profiles for Case 2 (14% O₂)

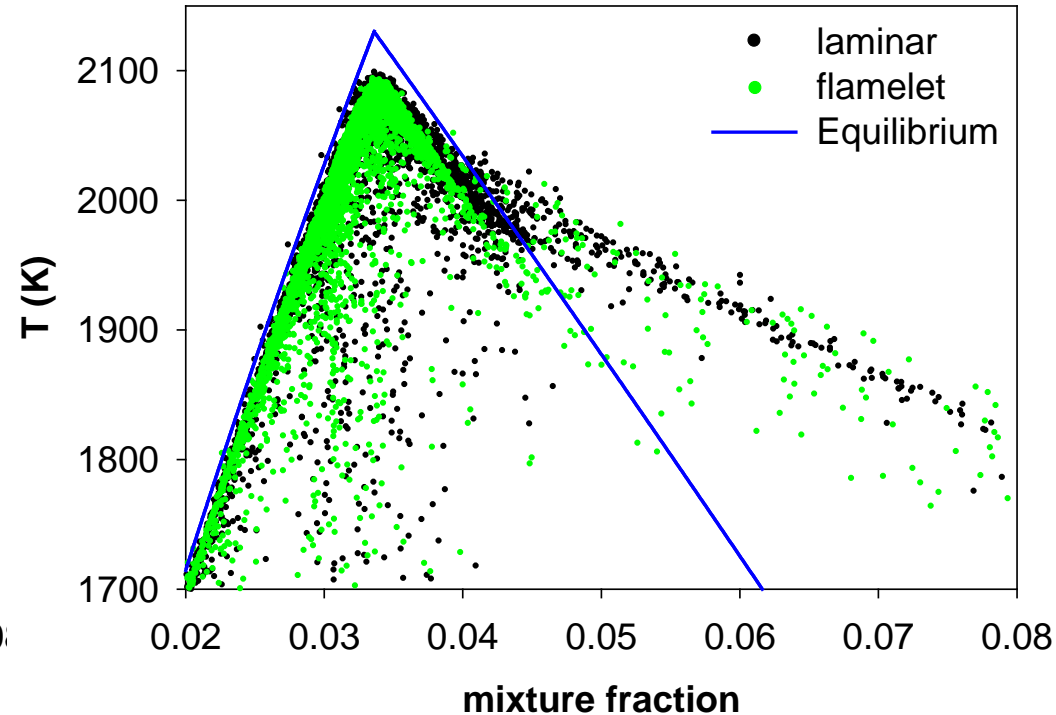
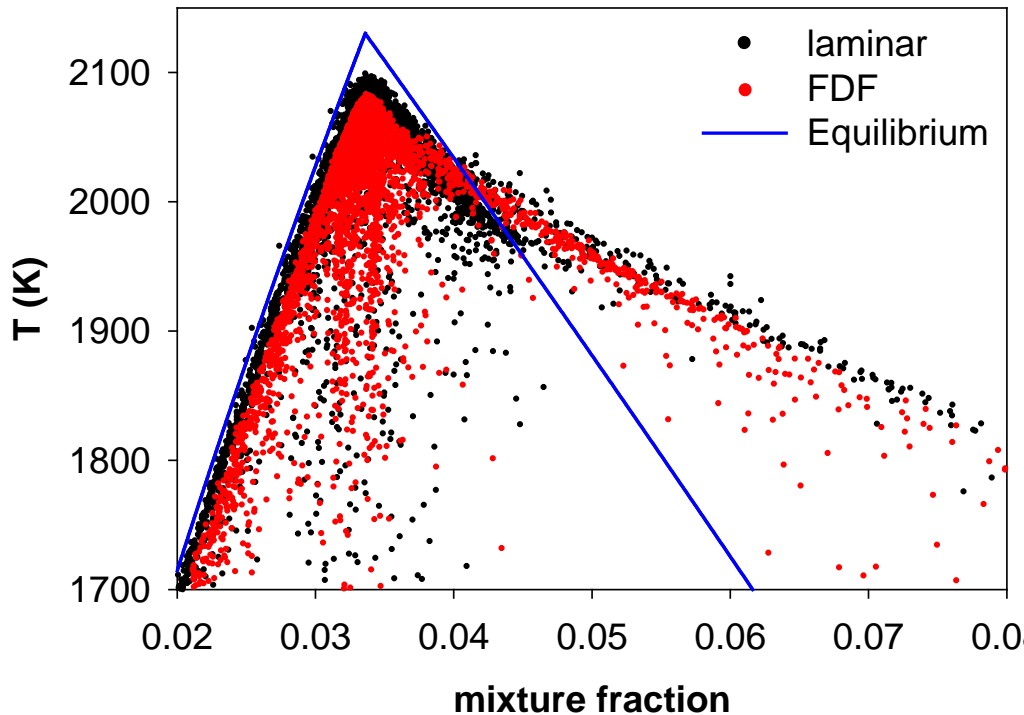
Net Formation and Destruction of CO

- CO destruction dominates in post-flame zone but CO formation is still significant.
- “Pockets” of unburned fuel, CH₃ and HCO apparent with laminar model.
- Somewhat counterintuitive since laminar model assumes fast sub-grid mixing.



Mixture Fraction for Case 2 (14% O₂)

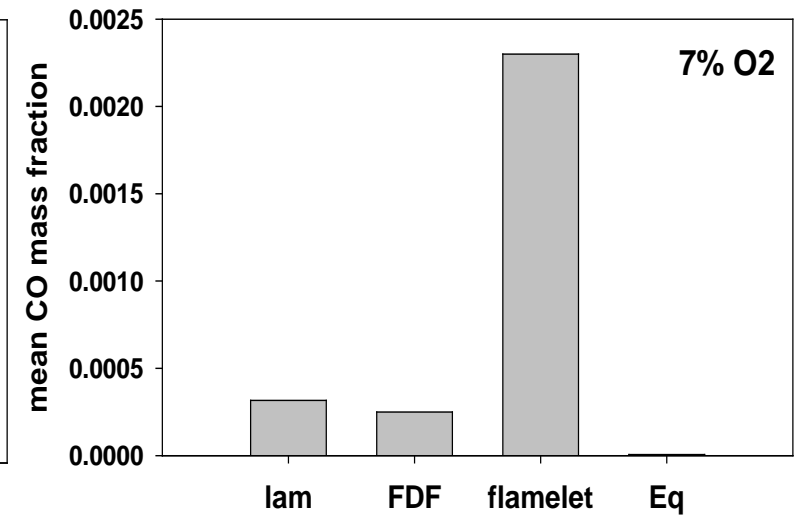
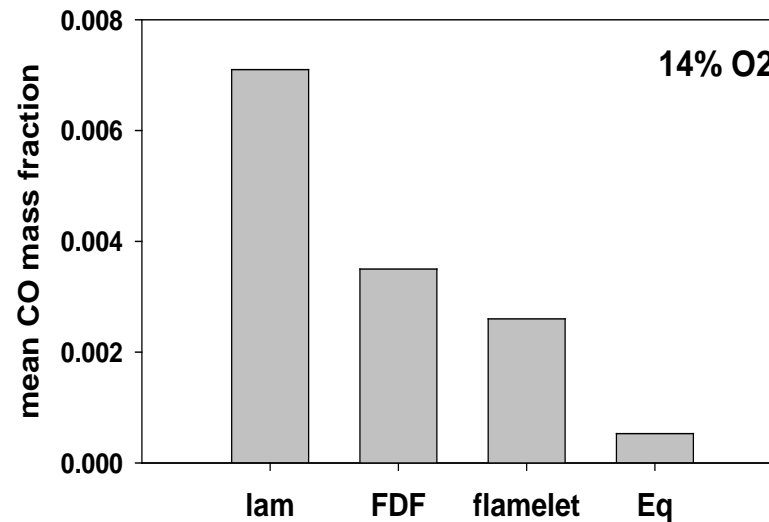
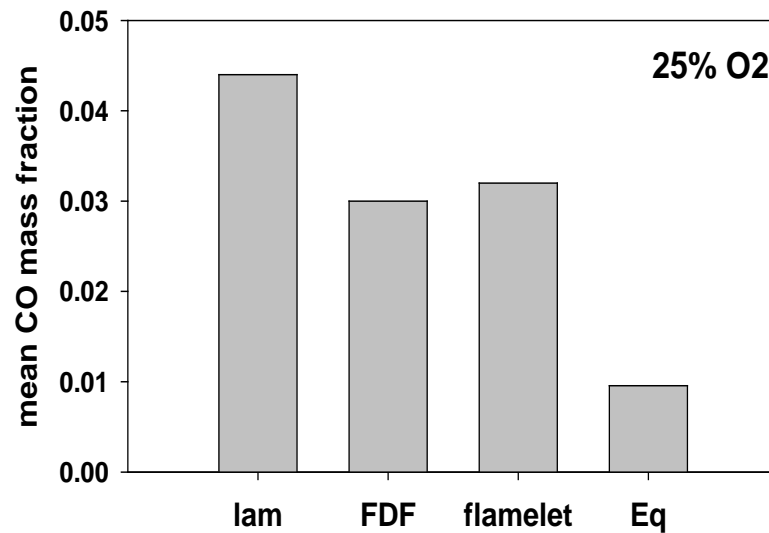
- Instantaneous mixture fraction plots show departure from equilibrium on fuel-rich side.
- Laminar model tends to show higher temperatures (and CO) on fuel-rich side.



$$Z = \frac{Y_C - Y_{C,o}}{Y_{C,F} - Y_{C,o}}$$

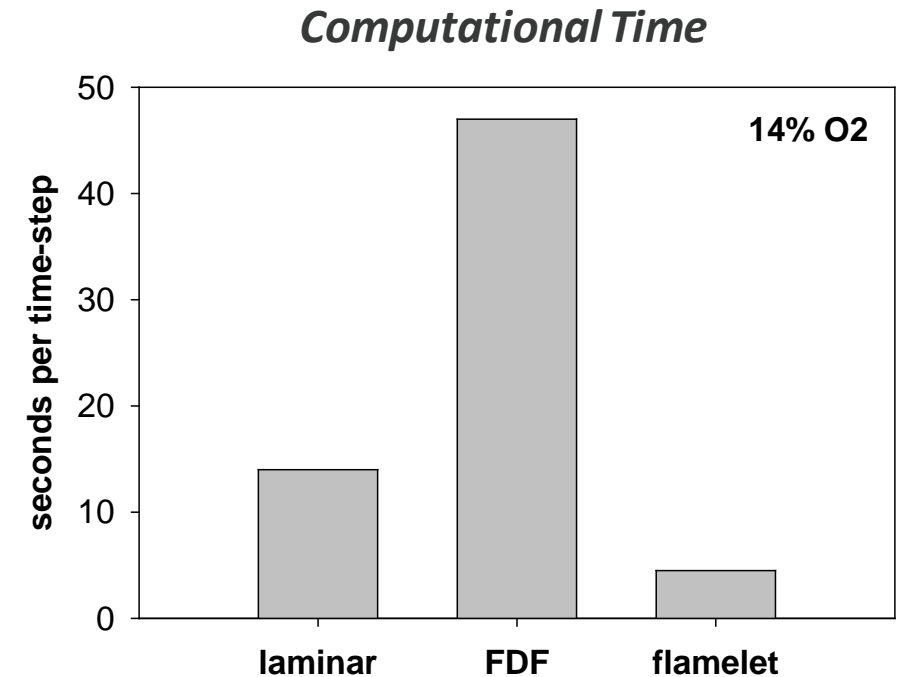
Mean Combustor CO Emissions

- All models predict CO emissions much higher than equilibrium values.
- Laminar model tends to overpredict CO compared to FDF.
- Flamelet model in good agreement with FDF at 25% and 14% O₂ concentration.



Concluding Remarks

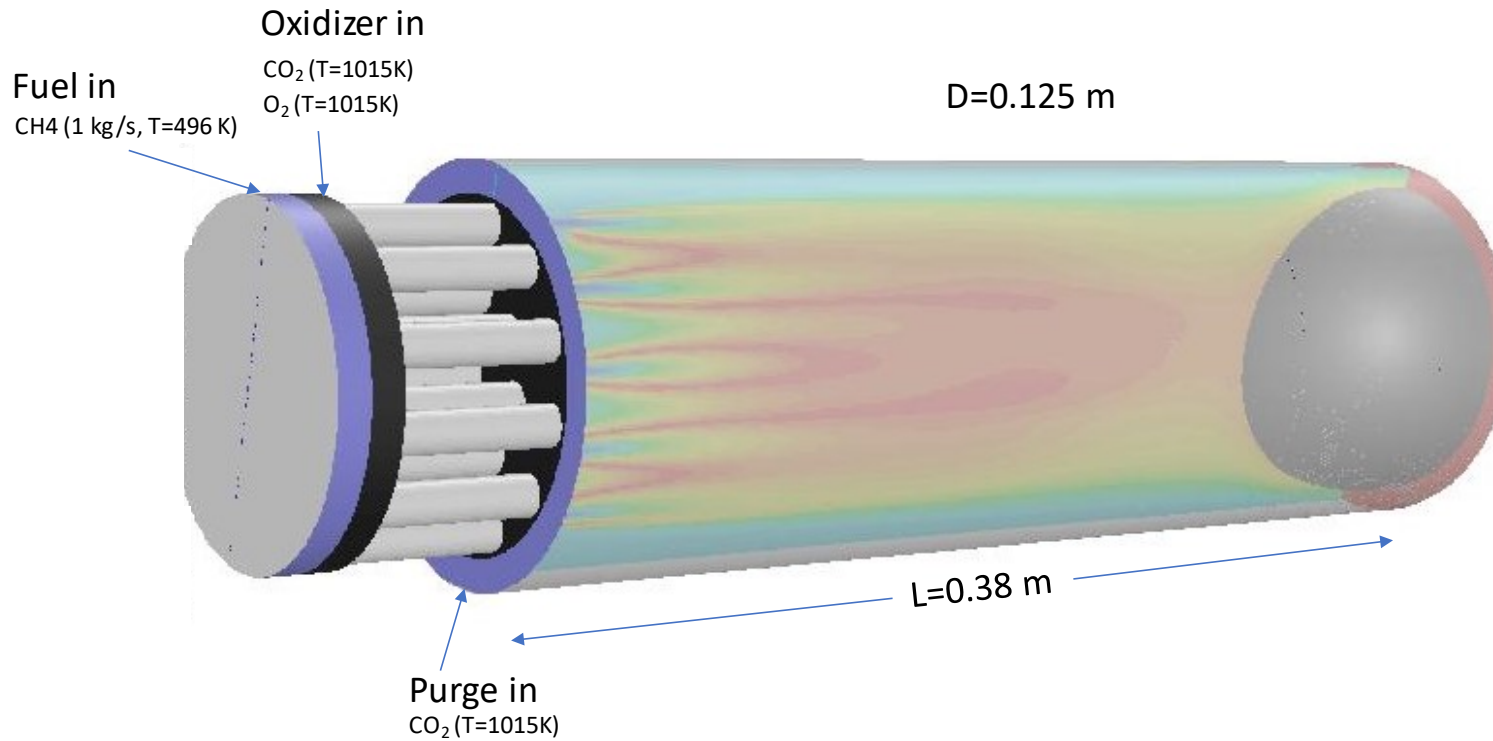
- Decreasing O_2 concentration changes combustion regime from lifted flame to autoignition type of process.
- Combustor CO emissions are a strong function of O_2 concentration (via temperature, OH) and well above equilibrium.
- Flamelet model performed well at 25% and 14% O_2 but can not predict autoignition.
- FDF model provides the most robust treatment of TCI but computationally expensive. Use as a “benchmark case” for comparison.
- Need experimental data for validation!



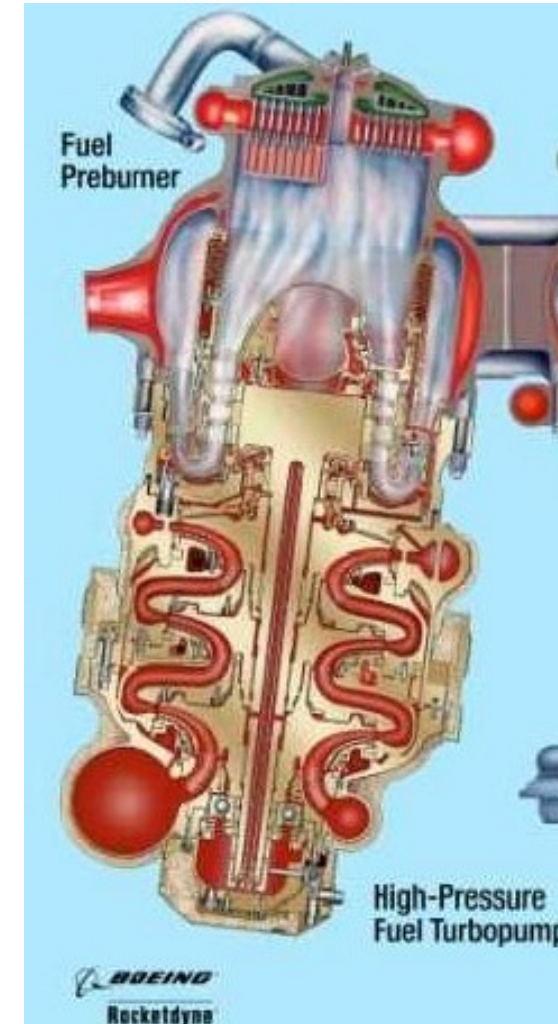
Backup Slides

50 MW Conceptual Combustor

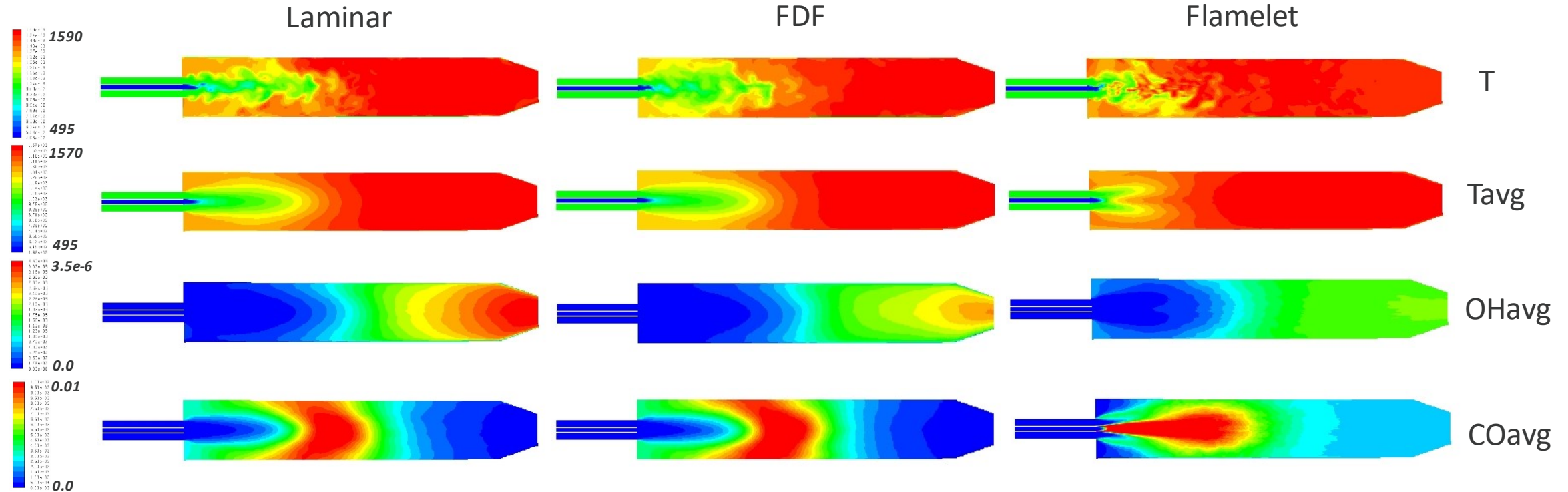
SSME Preburner type combustor – 21 coaxial injectors, 4M Cells



P=300 bar
50 MW Thermal Input



Results for Case 3 (7% O₂)



- FDF and Laminar model show autoignition behavior. Estimated induction time of ~2 msec corresponds to heat release location.
- Flamelet model predicts flame like behavior.