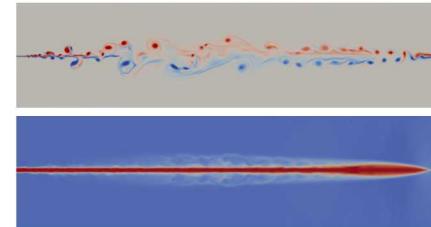
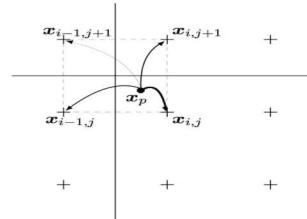
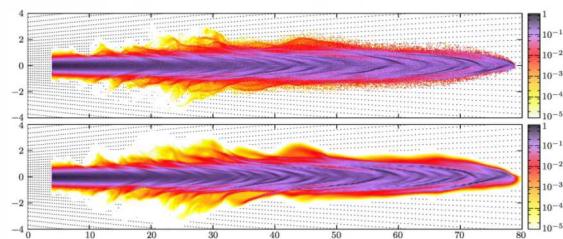


Modeling and simulation of a dense evaporating spray

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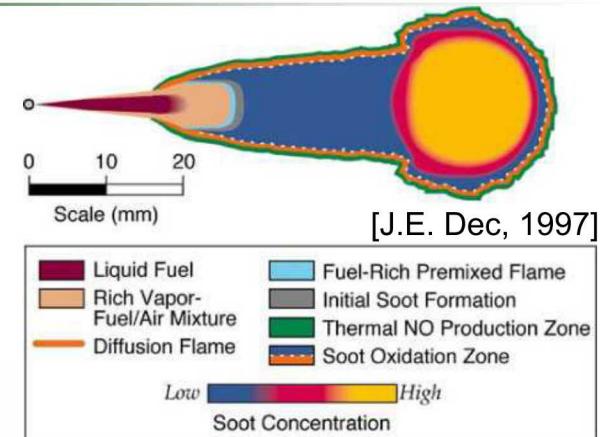


Sandia National Laboratories

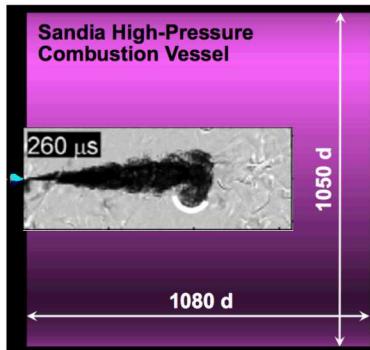
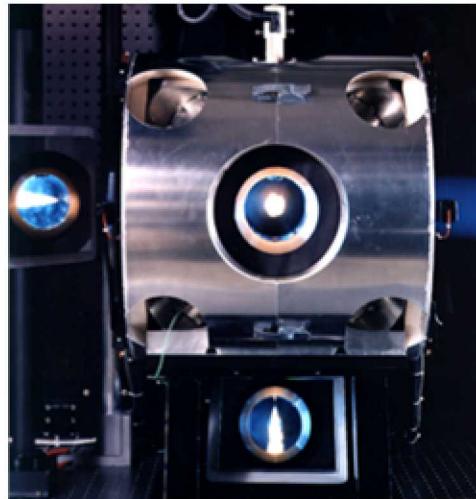
MOTIVATION – Liquid fuel injection

In Diesel and Gasoline engines

- Inlet is turbulent (+ cavitation)
 - $Re \sim 10^5$, $d = 90\mu\text{m}$
- High pressure chamber and sonic flow
 - $p = 60\text{bar}$, $u_i = 600\text{m/s}$
- Atomization process not understood
 - $We \sim 10^4$, $1\mu\text{m} < r_i < 100\mu\text{m}$



→ **MULTI-SCALE&MULTI-PHYSICS** drive **MIXING&COMBUSTION**



Experimental background
High pressure vessels
[Pickett 2010, Skeen 2014]

Need for a
High Fidelity Simulation
that is **affordable**

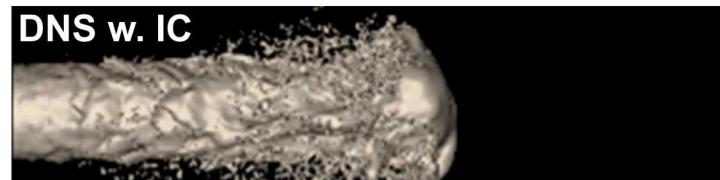
STATE OF THE ART – Injection simulation

No comprehensive simulation approaches

1 DNS with Interface Capturing

[Menard 2007; Desjardins 2010]

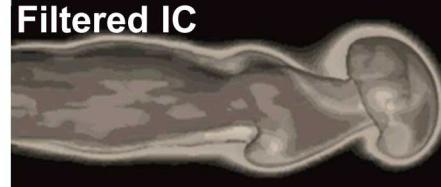
- Accurate and insightful
- Intractably costly



2 Filtered Interface Capturing

[Chesnel 2011]

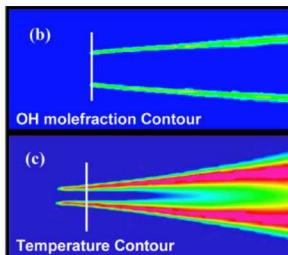
- Promising but empirical



3 Extension of dilute spray with coarse AMR

[Som 2013]

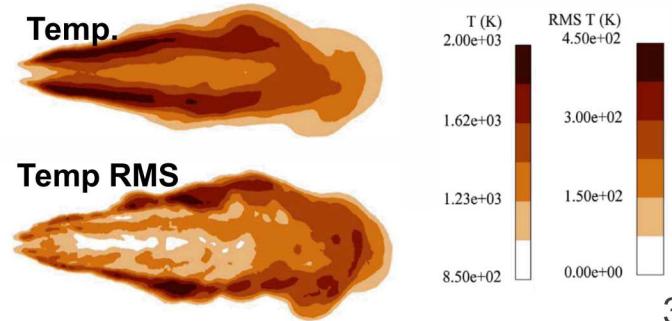
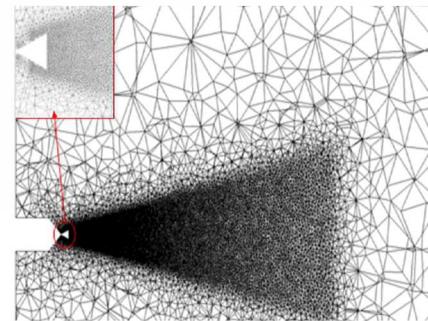
- Essential features missing
- Useful to investigate other physics (e.g. complex chemistry)



1 Prescribed downstream boundary condition

[Tillou 2014]

- Most applicable approach today
- Low predictability



OBJECTIVE – Comprehensive simulation

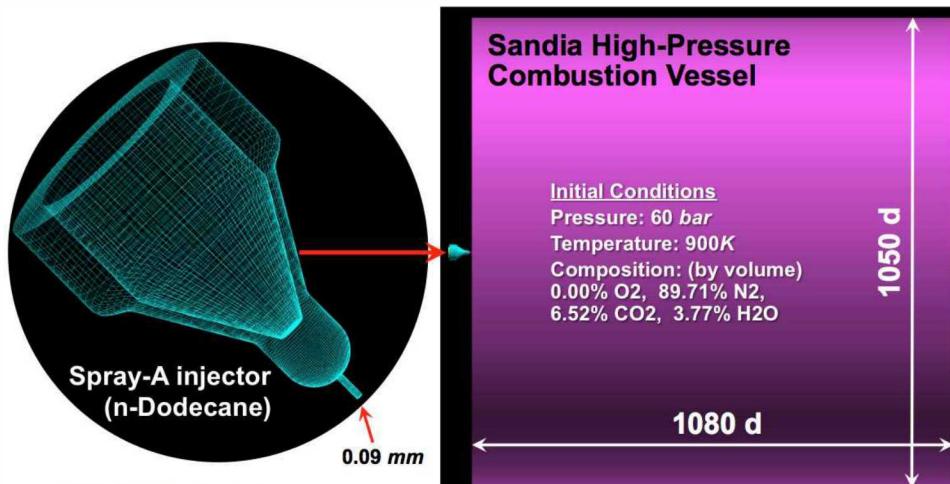
From nozzle outlet to dilute spray

- **Sensitized to nozzle flow** (in an LES sense)
 - $Re \sim 10^5$, $d = 90\mu\text{m}$
- **Robust to high pressures, velocities, and loadings**
 - $p = 60\text{bar}$, $u_i = 600\text{m/s}$
- **Compute the whole chamber** (with combustion)
 - with a billion points

$O(1\mu\text{m}, 10\text{ns})$



$O(10^5\mu\text{m}, 10^6\text{ns})$



Injection Conditions

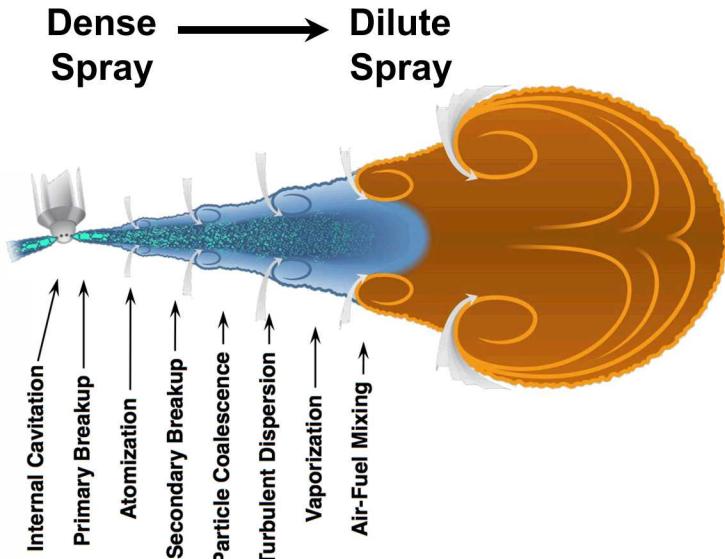
Peak Velocity:	600 m/s
Peak Re_d :	117,000
Density:	650 kg/m ³
Temperature:	363 K

We introduce a
Simplified Approach
 of interface flows
 to describe
 more physical scales

MODEL – Two-phase approach

A simplified but promising approach

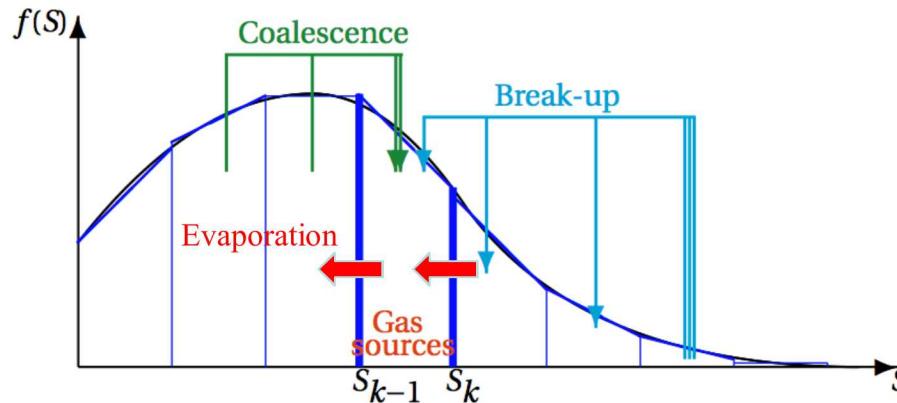
- Coupled Eulerian-Eulerian (gas and liquid moments) can **emulate at once**
 - the inertial behavior of the dense liquid **core**
 - the break-up and dispersion of liquid **blobs** (prescribes size of droplets)
 - the **dilute spray regime** with **droplets**
- Conservation for both **light** and **dense** phases
 - no interface tracking
 - mesoscale-gradients handled more easily
 - as opposed to real gas approaches
 - but no built-in thermodynamics!
- ...provided the transfers = need for **closures!**



MODEL – Sectional method

A cost-efficient way to capture polydispersity

- Various drop sizes are treated as a continuum:
Multi-Fluid [Laurent 2001, Doisneau 2013]



$$\begin{aligned}
 N_{\text{sec}} \text{ systems} \quad \left\{ \begin{array}{lcl}
 \partial_t n_k + \partial_x \cdot (n_k \mathbf{u}_k) & = & {}^2C_k^n + {}^2B_k^n + {}^2E_k^n \\
 \partial_t m_k + \partial_x \cdot (m_k \mathbf{u}_k) & = & {}^2C_k^m + {}^2B_k^m + {}^2E_k^m \\
 \partial_t (m_k \mathbf{u}_k) + \partial_x \cdot (m_k \mathbf{u}_k \otimes \mathbf{u}_k) & = & m_k \mathbf{F}_k + {}^2C_k^u + {}^2B_k^u + {}^2E_k^u \\
 \partial_t (m_k h_k) + \partial_x \cdot (m_k h_k \mathbf{u}_k) & = & m_k \mathbf{H}_k + {}^2C_k^h + {}^2B_k^h + {}^2E_k^h
 \end{array} \right. \quad \rightleftharpoons \text{Navier-Stokes with sources}
 \end{aligned}$$

...many integral source terms to compute

MODEL – Two-phase approach

Pressureless Gas Dynamics (PGD) decouples Lagrangian advection

- The coupled NS-PGD* system

$$\left\{
 \begin{aligned}
 \partial_t \rho_g Y_f + \partial_x \rho_g Y_f \mathbf{u}_g &= \omega_f + \sum_k E_k^{m-g} \\
 \partial_t \rho_g Y_i + \partial_x \rho_g Y_i \mathbf{u}_g &= \omega_i, \quad i \in [1; N_{\text{species}}], i \neq f \\
 \partial_t \rho_g \mathbf{u}_g + \partial_x \rho_g \mathbf{u}_g \otimes \mathbf{u}_g &= -\partial_x p + \sum_k (-\mathbf{F}_k + \mathbf{u}_k E_k^{m-g}) \\
 \partial_t \rho_g e_g + \partial_x \rho_g e_g \mathbf{u}_g &= -p \partial_x \mathbf{u}_g + \sum_k (-H_k + \mathbf{F}_k (\mathbf{u}_g - \mathbf{u}_k) + h_k E_k^{m-g}) \\
 \partial_t m_k + \partial_x m_k \mathbf{u}_k &= E_{k+1}^m + B_k^{m+} + C_k^{m+} - (E_k^m + E_k^{m-g} + B_k^{m-} + C_k^{m-}) \\
 \partial_t m_k \mathbf{u}_k + \partial_x m_k \mathbf{u}_k \otimes \mathbf{u}_k &= \mathbf{F}_k + \mathbf{u}_{k+1} E_{k+1}^m + B_k^{u+} + C_k^{u+} - \mathbf{u}_k (E_k^m + E_k^{m-g} + B_k^{m-} + C_k^{m-}) \\
 \partial_t m_k h_k + \partial_x m_k h_k \mathbf{u}_k &= H_k + \mathbf{u}_{k+1} E_{k+1}^m + B_k^{h+} + C_k^{h+} - h_k (E_k^m + E_k^{m-g} + B_k^{m-} + C_k^{m-})
 \end{aligned}
 \right.$$

pressureless

sections

$k \in [1; N_{\text{sec}}]$

Needs to be closed

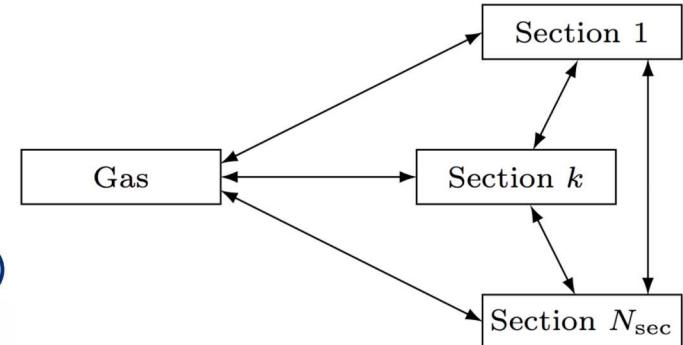
*obtained from kinetic theory or conservation principles

$$\partial_t f + \partial_x \mathbf{c} f + \partial_c \mathbf{F} f + \partial_\theta \mathbf{H} f + \partial_r \mathbf{E} f = \mathbf{B} + \mathbf{C}$$

MODEL – The closure problem

LES closures should respect dominant dynamics and equilibrium

- **Need the rate of exchange for**
 - **Momentum** (drag and dynamic subgrid model)
 - **Heat** (heating)
 - **Mass** (vaporization and combustion subgrid model)
- **Derivation from first principles is hard**
 - **All thermophysical properties needed**
 - **Subgrid knowledge needed too** (turbulent & atomizing)
- **Should enforce thermodynamics and equilibria**
 - **Multifluid models** by Saurel's team [D. Furfaro, 2015]



ANALYSIS – Two-way coupling

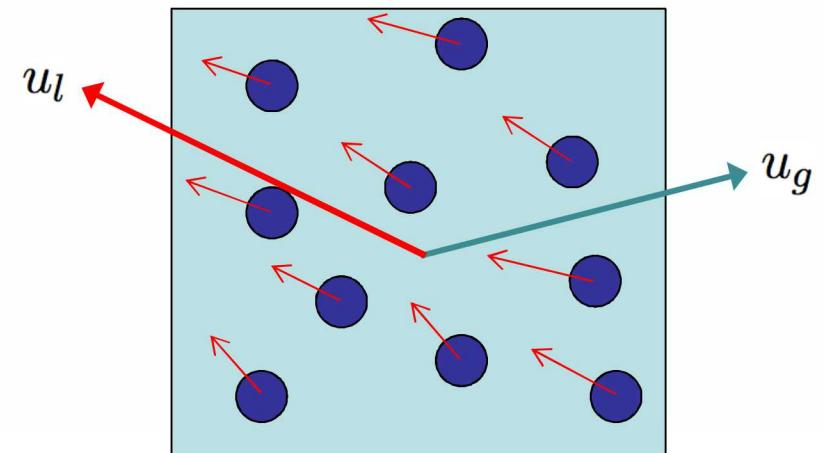
Two-way coupling as the main driver of characteristic times

- **Two-way coupling drives characteristic times**
 - Example for drag (0D): [Doisneau, 2013]

$$\left\{ \begin{array}{l} \partial_t(m_g u_g) = \frac{m_l}{\tau} (u_l - u_g) \\ \partial_t(m_l u_l) = -\frac{m_l}{\tau} (u_l - u_g) \end{array} \right. \Leftrightarrow \left\{ \begin{array}{l} \partial_t(m_g u_g + m_l u_l) = 0 \\ \partial_t(u_l - u_g) = -\frac{1+C}{\tau} (u_l - u_g) \end{array} \right.$$

- Correction factor can be large since C reaches ~ 100

$$\tau_{\text{2-way}} = \frac{\tau}{1+C}$$



ANALYSIS – Two-way coupling

Two-way coupling as the main driver of characteristic times

- **Two-way coupling drives characteristic times**
 - Drag
 - Same argument for heating
 - Vaporization is driven by heating

$$C = \frac{m_l}{m_g}$$

$$\partial_t d^2 = -K$$

$$K = \frac{8\lambda_g}{\rho_l c_{p,g}} \log \left(1 + \frac{c_{p,g}(T_g - T_l)}{h_l} \right)$$

- **Correction factor can be large since C reaches ~ 100**

$$\tau_{\text{2-way}} = \frac{\tau}{1 + C}$$

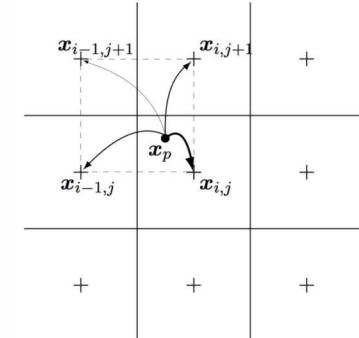
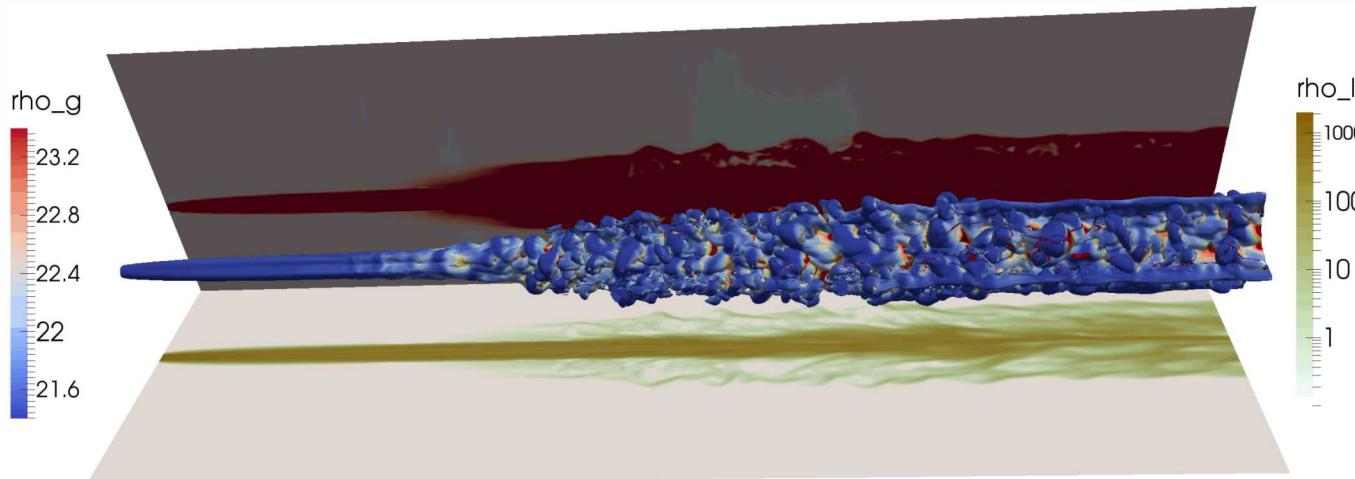
NUMERICS – Two-way coupling needs

Effort on numerical methods for multi-scale coupled flows

- 1) Time integration tailored **splitting**

$$\begin{array}{c}
 \text{Gas transport } \mathcal{T}_g \\
 \hline
 \text{Section transport } \mathcal{T}_k
 \end{array}
 = \begin{array}{c}
 \text{Coupling } \mathcal{R} \\
 \mathcal{F} + \mathcal{H} + \mathcal{E}
 \end{array} + \begin{array}{c}
 \text{Spray sources} \\
 \mathcal{B} + \mathcal{C}
 \end{array}$$

- 2) Space transport novel **semi-Lagrangian scheme**



NUMERICS – Time integration

A Tailored Operator Splitting

Operator splitting

- Recycle legacy solvers
- Robust time integration
- Local properties enforced
- Adaptable accuracy

$$\begin{array}{c}
 \text{Gas transport } \mathcal{T}_g \\
 \hline
 \text{Section transport } \mathcal{T}_k
 \end{array}
 = \begin{array}{c}
 \text{Coupling } \mathcal{R} \\
 \mathcal{F} + \mathcal{H} + \mathcal{E}
 \end{array} + \begin{array}{c}
 \text{Spray sources} \\
 \mathcal{B} + \mathcal{C}
 \end{array}$$

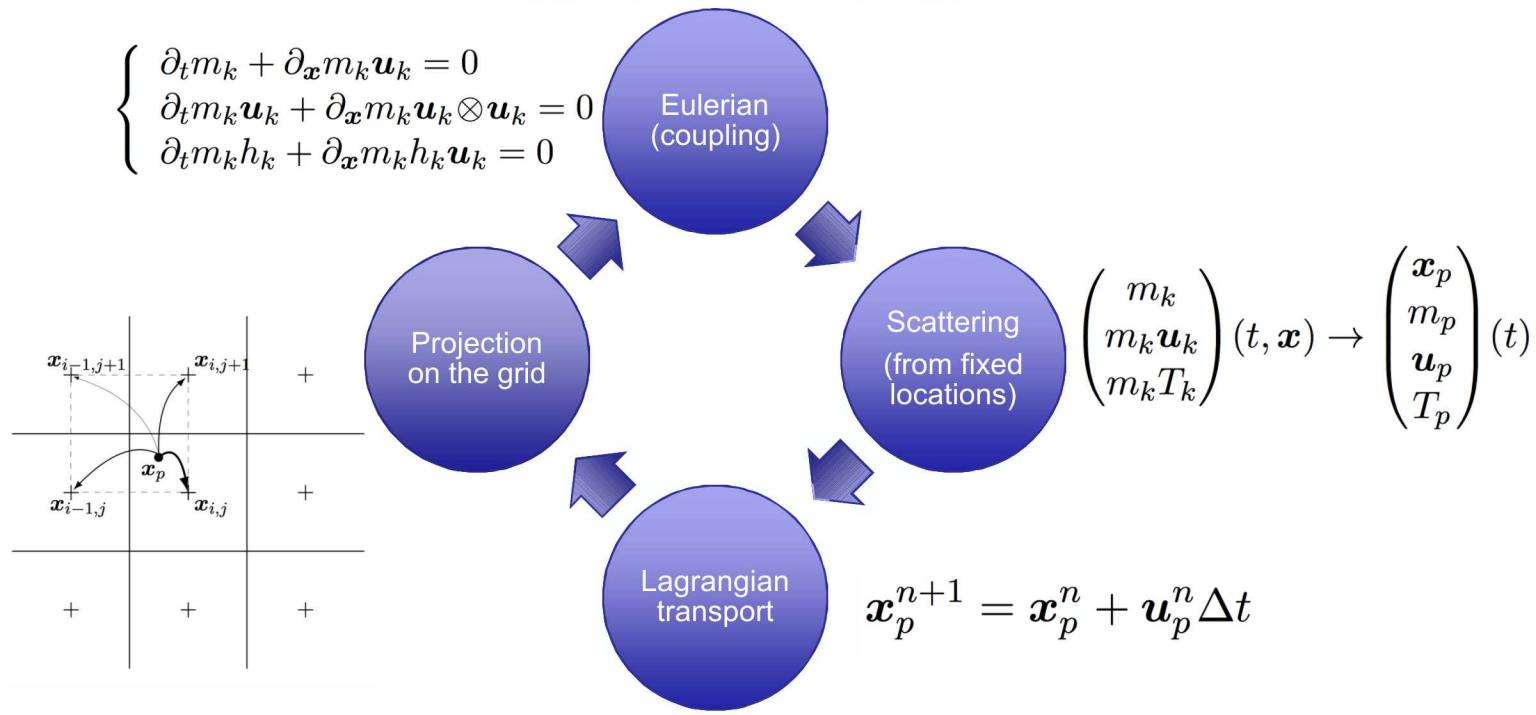
- to integrate all phase exchange terms \mathcal{R} at once (RK4)
 - Realizability, conservativity, equilibrium
 - Strong couplings
- to integrate spray sources $\mathcal{B} + \mathcal{C}$
 - Realizability and convergence
 - Strong particle-particle coupling

$$\mathbf{U}^{n+1} = \mathcal{R} \prod_{k=1}^{N_{\text{sec}}} (\mathcal{T}_k) \mathcal{T}_g \mathbf{U}^n$$

$$\mathbf{U}^n = \begin{pmatrix} \rho_g Y_i \\ \rho_g \mathbf{u}_g \\ \rho_g e_g \\ n_k \\ m_k \\ m_k \mathbf{u}_k \\ m_k h_k \end{pmatrix}^n$$

NUMERICS – PGD transport

A robust and accurate answer to PGD peculiarities

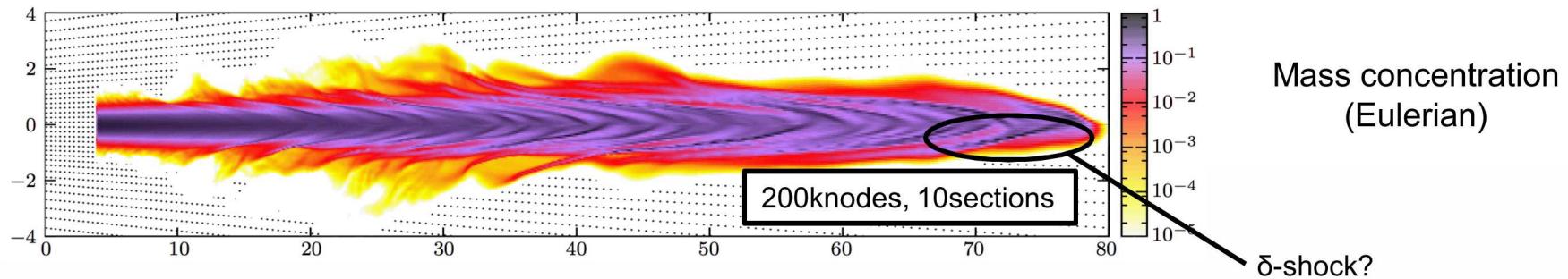


- **Novel semi-Lagrangian PGD transport scheme**
 - **Deterministic: no noise**
 - **Localizes spray info at mesh nodes: good for coupling**
 - **Easier load balancing**
 - **No fluxes to be computed: reduce cost and numerical diffusion**

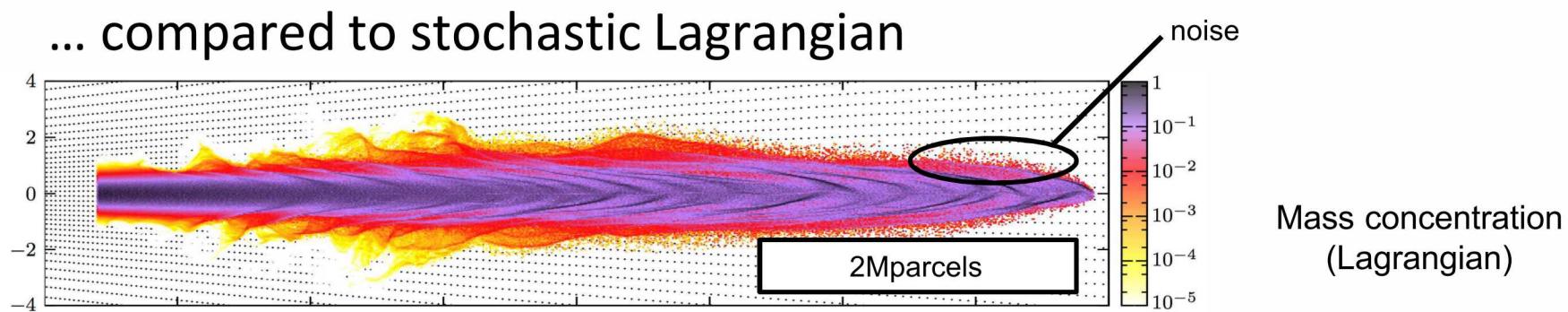
NUMERICS – PGD transport

2D test with prescribed flow field

- Obtained **cost-efficient** and **accurate** results



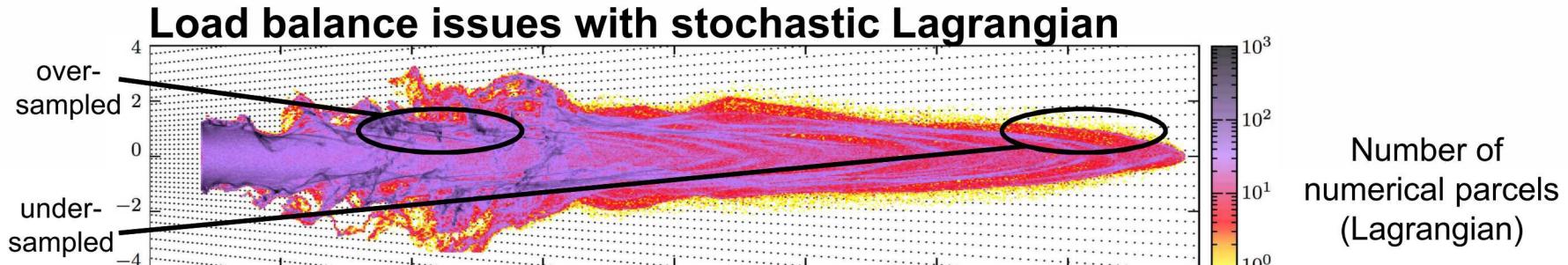
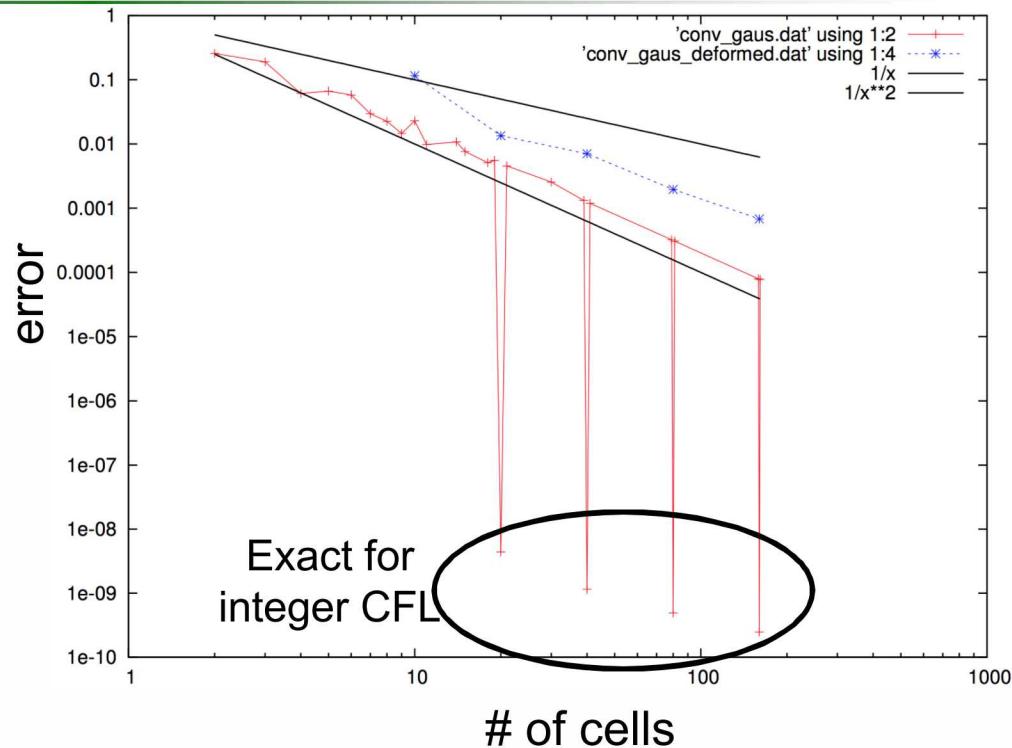
... compared to stochastic Lagrangian



NUMERICS – PGD transport

Transport is 2nd order in space

- **No CFL constraint**
(unconditionally stable)
- **Handles vacuum**
- **Handles δ -shocks**
- **Predictable load**



TEST 1 – Momentum Coupling

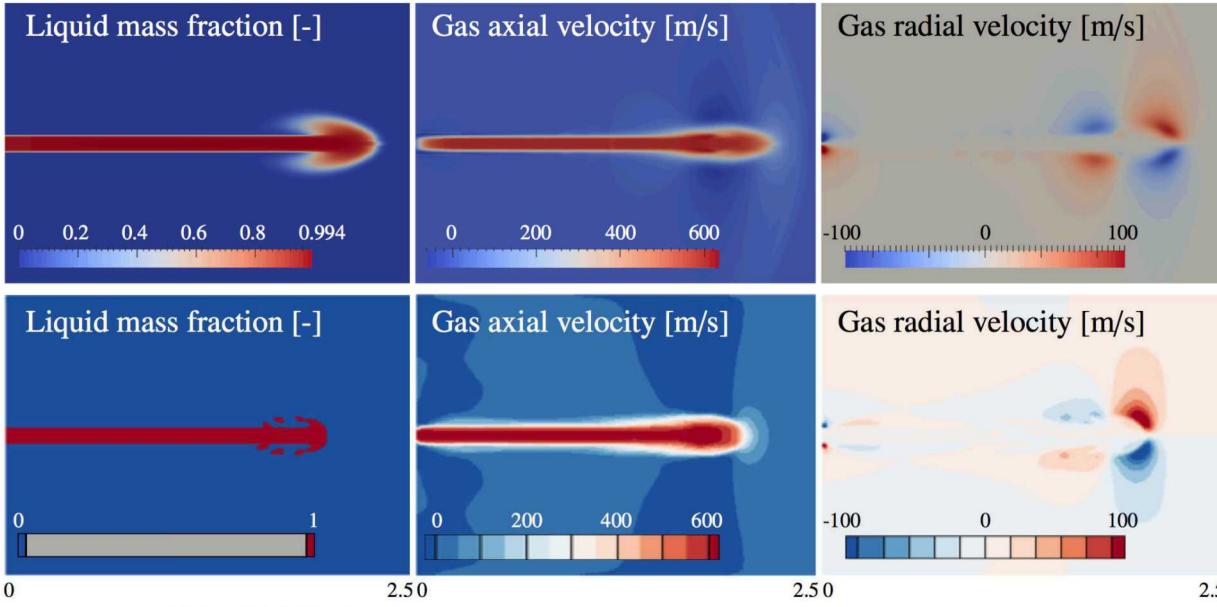
Comparison between E-ES and CLSVOF

✓ Supersonic injection (toy problem)

- velocity plug-flow boundary
- no thermal transfer
- $T_{end} = 4\mu\text{s}$

Raptor with E-ES

$\Delta x = 12.5 \mu\text{m}$, $\Delta t = 8 \text{ ns}$



$\Delta x = 13.3 \mu\text{m}$, $\Delta t \sim 6 \text{ ns}$

✓ Agreement on **gas entrainment**

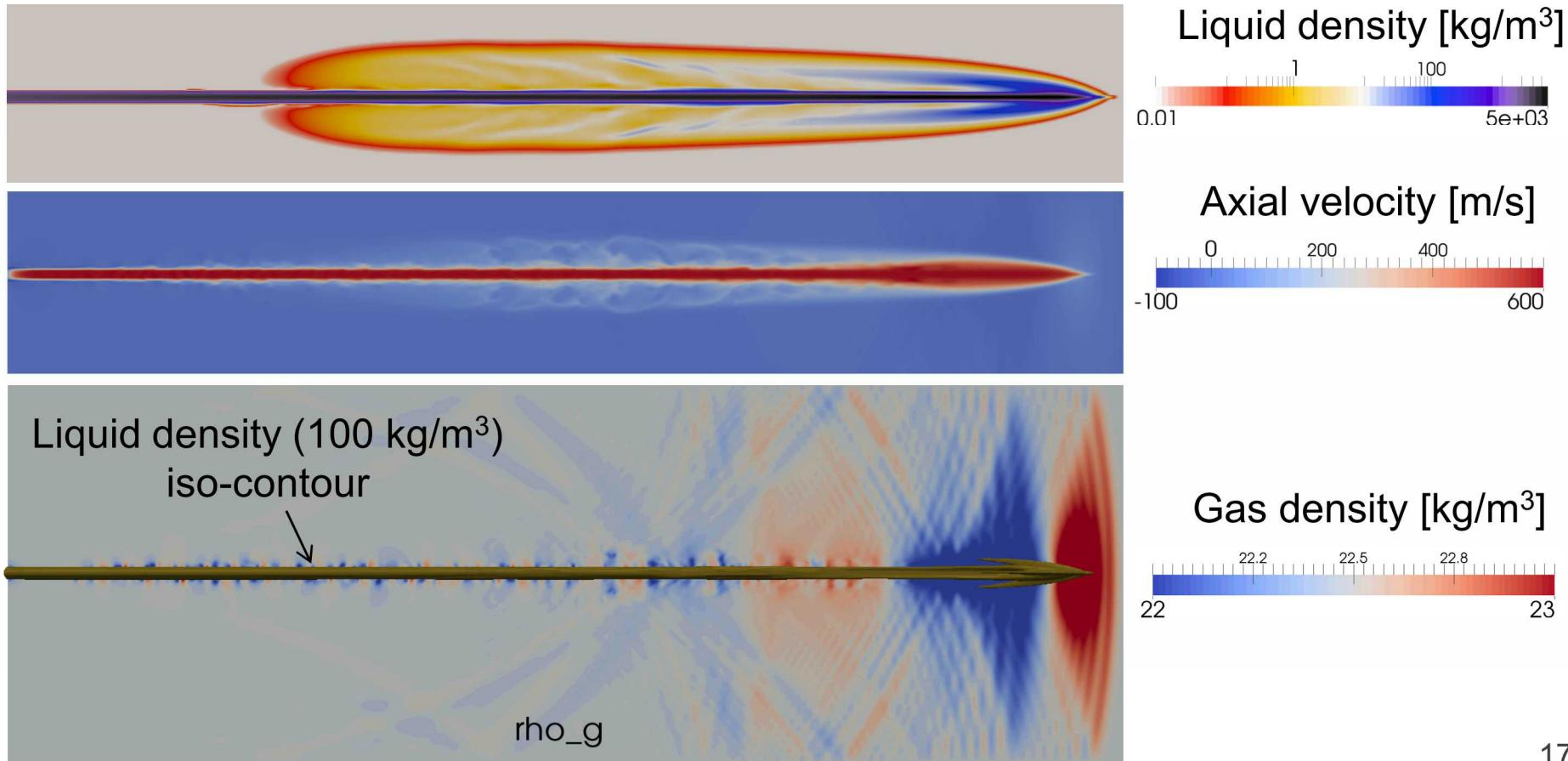
★ Liquid density discrepancy from **pressureless** assumption

★ Jet tip is different because of **lack of surface tension**

TEST 2 – Induced turbulence

Entrainment and induced turbulence by jet injection

- Executed with **RAPTOR + E-ES**

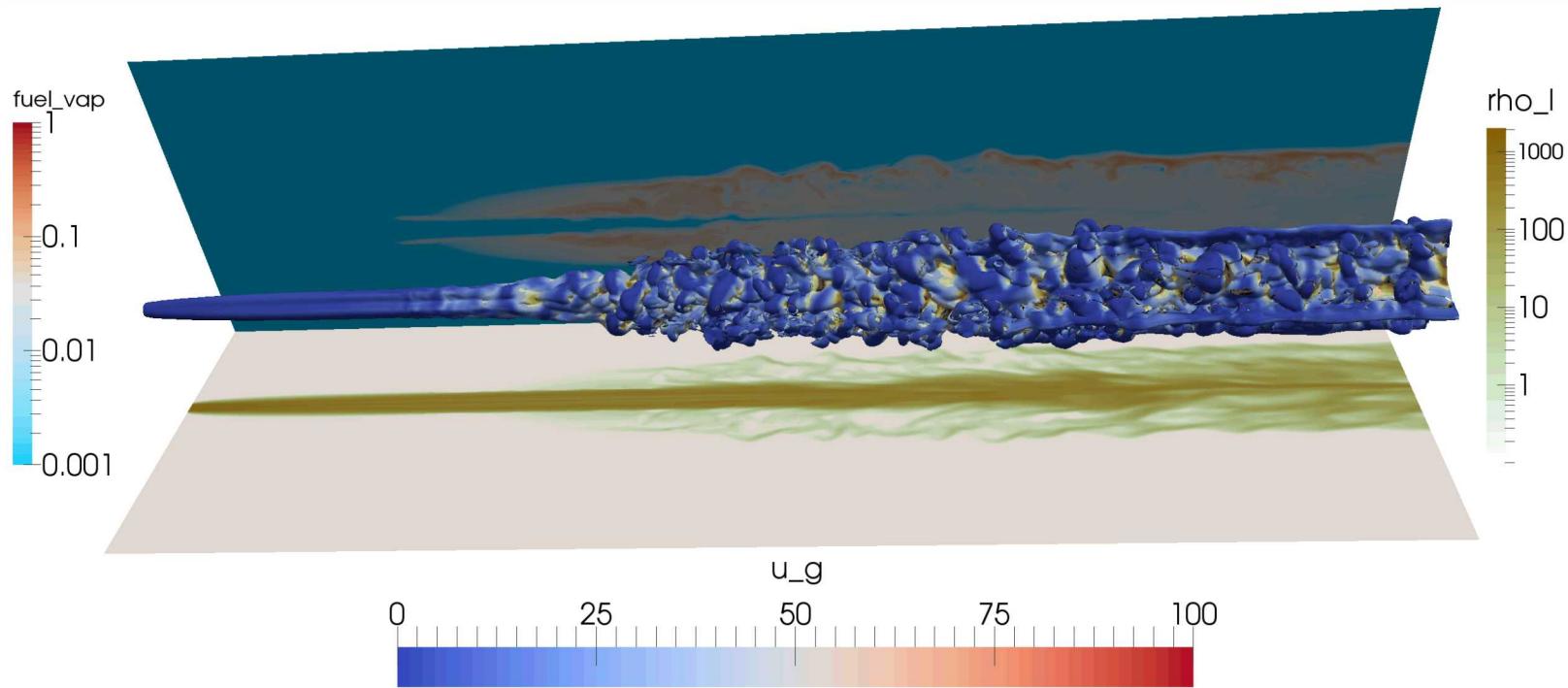


TEST 3 – Fuel vaporization

Fuel vapor footprint

- Executed with **RAPTOR E-ES**

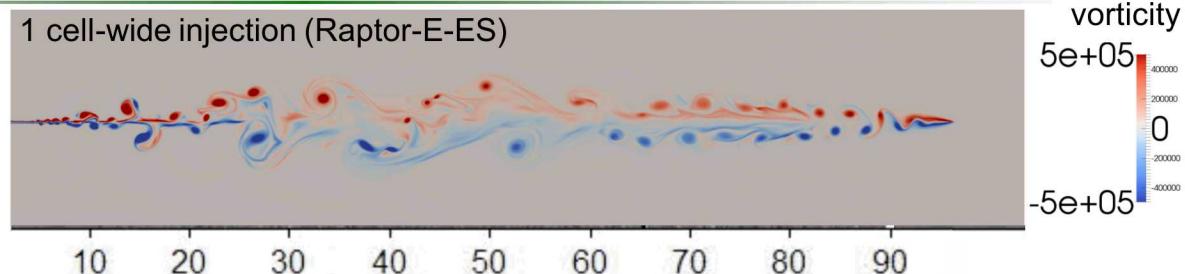
- Box 3x3x10mm
- $d_{inj}=90\mu\text{m}$, $T_{end}=40\mu\text{s}$
- quiescent gas at 60bar, 900K
- n-dodecane at 702kg/m^3 , 600m/s
- 50Mcells (cartesian mesh)
- $\Delta x=12.5\mu\text{m}$, $\Delta t=8\text{ns}$, $T_{end}=40\mu\text{s}$
- 1 section (prescribed initial size)
- PGD transport (δ -shocks)
- d^2 -law



CONCLUSION

Conclusion

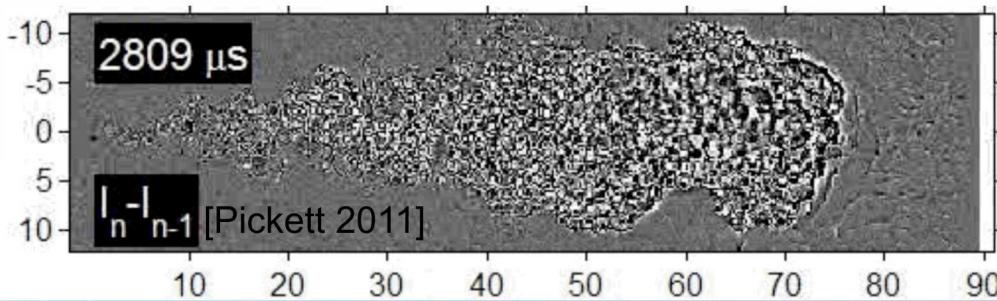
- Kinetic theory
- Two-way coupling
- Dedicated numerics



Spray tools are promising to efficiently handle injection

Perspectives

- Dense core dynamics
 - pressure/crossings
 - turbulence
 - surface tension
- High-pressure mixing
 - atomization
 - “evaporation”
 - LES closure
- Combustion
 - chemistry
 - LES closure
 - numerics
- Verification
 - vs CLSVOF
 - vs stochastic Lagrangian
 - vs Real-Gas solver
- Validation vs ECN results (spray A)
 - $2809 \mu\text{s}$
 - $|I_n - I_{n-1}|$ [Pickett 2011]



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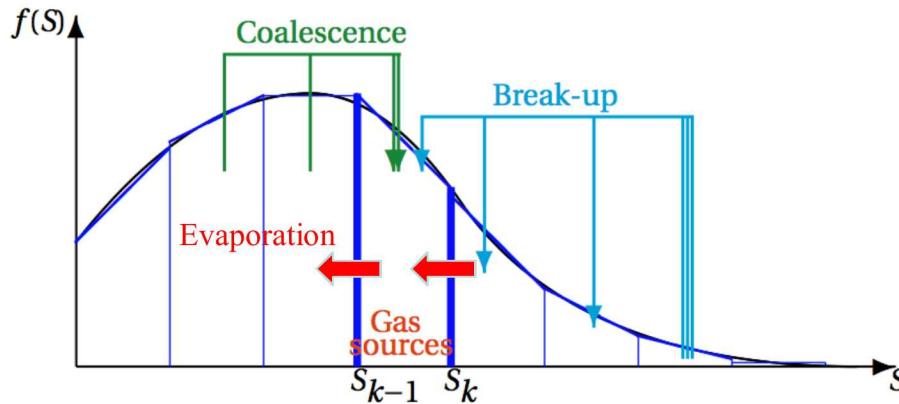
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BACK-UP

MODEL – Sectional method

A cost-efficient way to capture polydispersity

- Various drop sizes are treated as a continuum



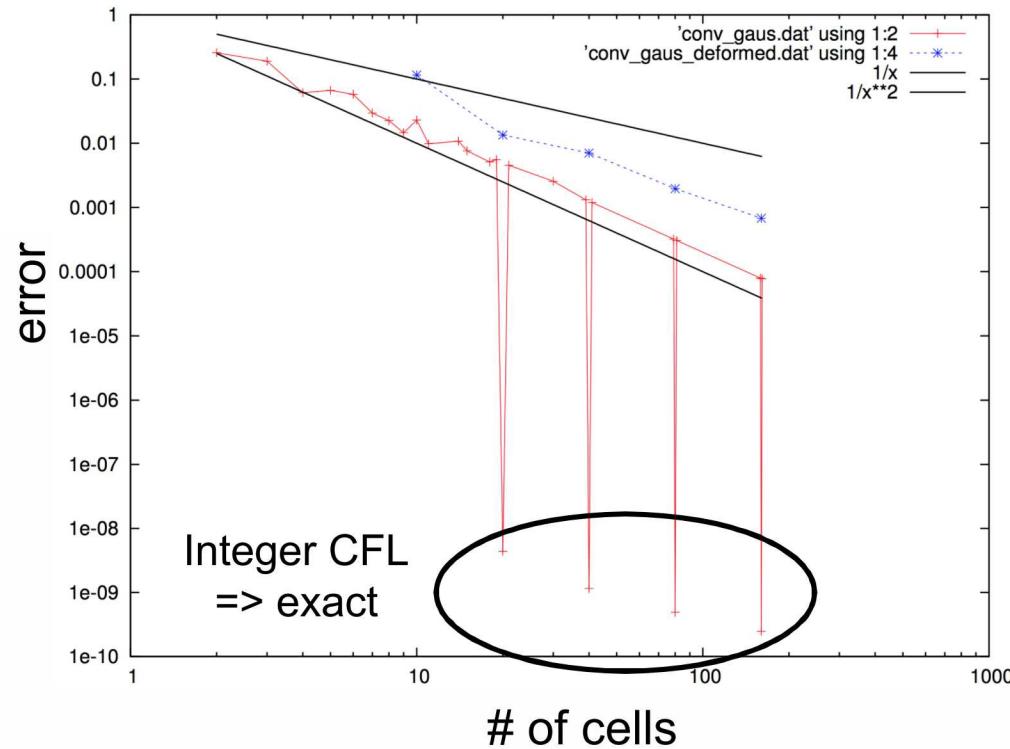
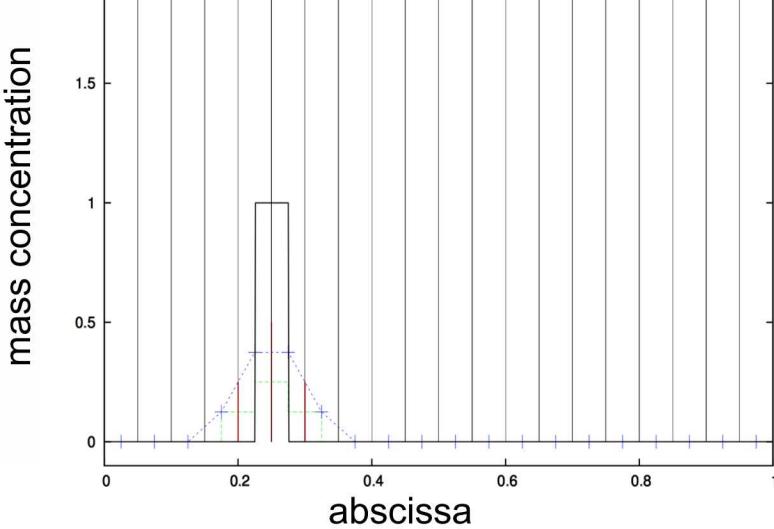
$$\begin{aligned}
 N_{\text{sec}} \text{ systems} \quad \left\{ \begin{aligned}
 \partial_t n_k + \partial_x \cdot (n_k \mathbf{u}_k) &= 2\mathbf{C}_k^n + 2\mathbf{B}_k^n + 2\mathbf{E}_k^n \\
 \partial_t m_k + \partial_x \cdot (m_k \mathbf{u}_k) &= 2\mathbf{C}_k^m + 2\mathbf{B}_k^m + 2\mathbf{E}_k^m \\
 \partial_t (m_k \mathbf{u}_k) + \partial_x \cdot (m_k \mathbf{u}_k \otimes \mathbf{u}_k) &= m_k \mathbf{F}_k + 2\mathbf{C}_k^u + 2\mathbf{B}_k^u + 2\mathbf{E}_k^u \\
 \partial_t (m_k h_k) + \partial_x \cdot (m_k h_k \mathbf{u}_k) &= m_k \mathbf{H}_k + 2\mathbf{C}_k^h + 2\mathbf{B}_k^h + 2\mathbf{E}_k^h
 \end{aligned} \right. \quad \rightleftharpoons \text{Navier-Stokes with sources}
 \end{aligned}$$

...many integral source terms to compute

NUMERICS – PGD transport

Transport is 2nd order in space

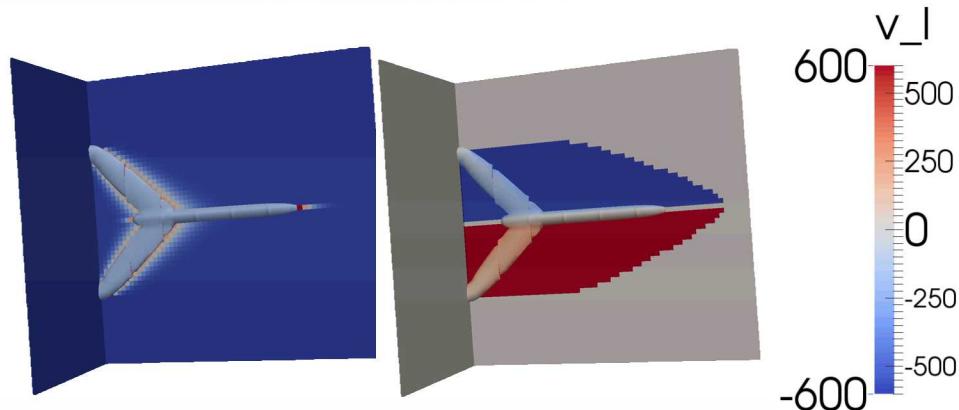
- No CFL constraint (unconditionally stable)
- Handles vacuum
- Handles δ -shocks



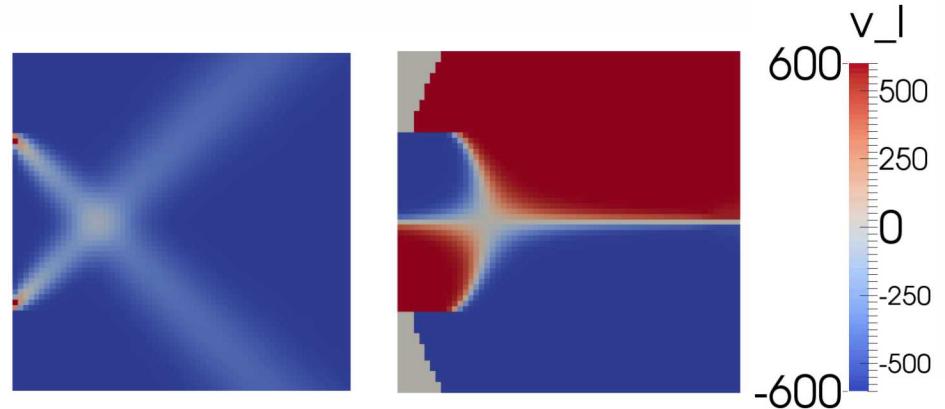
NUMERICS – Beyond PGD transport

Prevention of δ -shocks

- **δ -shocks are an artifact from the PGD assumption**
 - no grid convergence
 - erroneous density and gradients
 - troublesome with two-way coupling



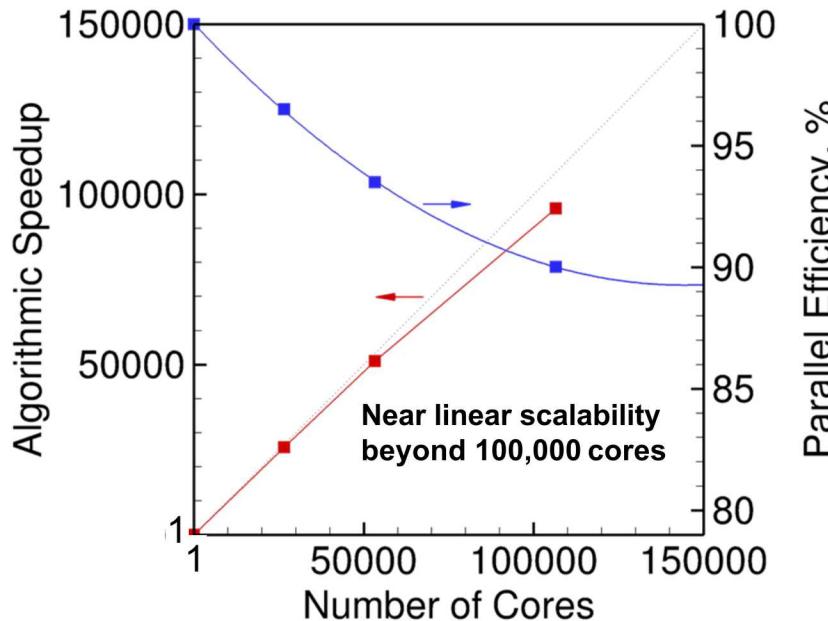
- **Higher order moment methods are developed to solve this**



NUMERICS – Raptor

A general solver optimized for LES

- Theoretical framework
 - Fully-coupled, compressible conservation equations
 - Real-fluid equation of state (high-pressure phenomena)
 - Detailed thermodynamics, transport and chemistry
 - Multiphase flow, spray
 - Dynamic SGS modeling (**No Tuned Constants**)
 - Advanced UQ methods for error/sensitivity analysis
- Numerical framework
 - Staggered finite-volume differencing (non-dissipative, discretely conservative)
 - Dual-time stepping with generalized preconditioning (all-Mach-number formulation)
 - Detailed treatment of geometry, wall phenomena, BC's



- High-performance computing framework (Advanced parallel programming model that makes optimal use of advanced MP-computer architectures)
- Results from strong and weak scaling on Oak Ridge National Laboratory CRAY XK7 (Titan), June 2013
 - Test case – jet-in-cross-flow, 500-million cells
 - **Strong scaling:** 24,000 to 120,000 cores, > 90% efficiency
 - **Weak scaling:** 500-million-cells/24,000-cores to 2-billion-cells/120,000-cores, < 4% increase in CPU time
- Currently being refactored for hybrid multi-core parallelism and GPU acceleration (MPI/OpenMP/OpenACC)