

Exceptional service in the national interest



State of Art in PCHE Development and Associated Research at Sandia sCO₂ Summit

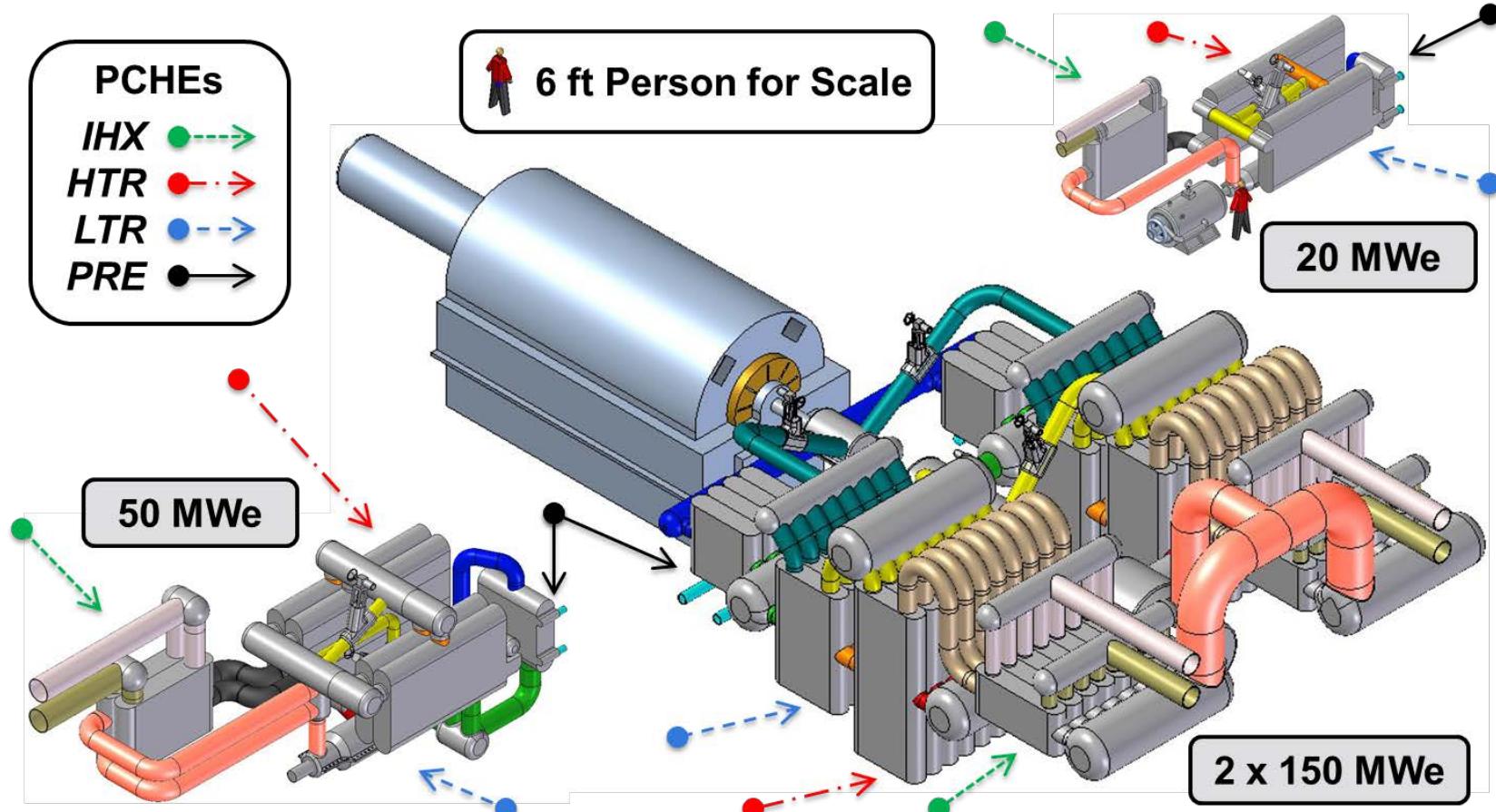
November 14-15, 2017, Albuquerque, NM, USA
Matthew D. Carlson



Sandia National Laboratories is a multimission laboratory managed and operated by National Technology and Engineering Solutions of Sandia, LLC, a wholly owned subsidiary of Honeywell International, Inc., for the U.S. Department of Energy's National Nuclear Security Administration under contract DE-NA0003525. SANDXXXX-XXXX

HEAT EXCHANGER STATE OF THE ART

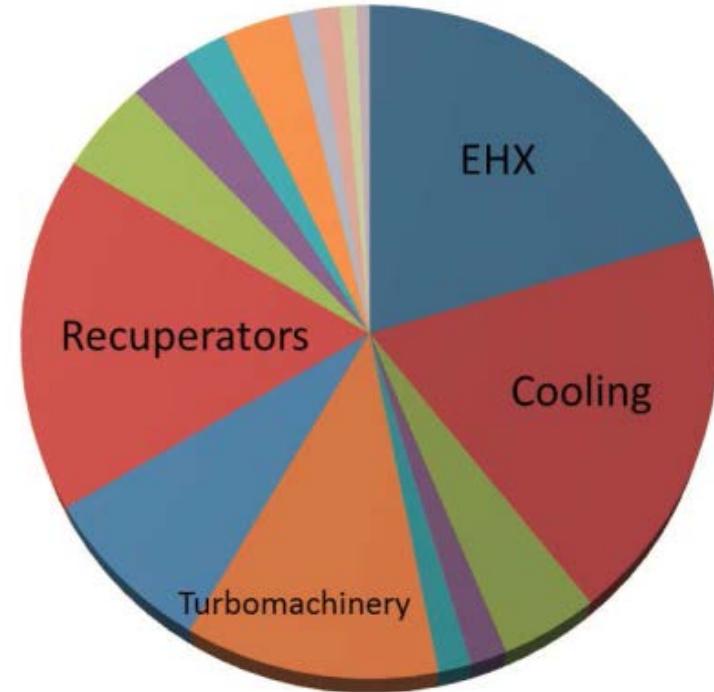
Heat Exchangers are Critical for sCO₂



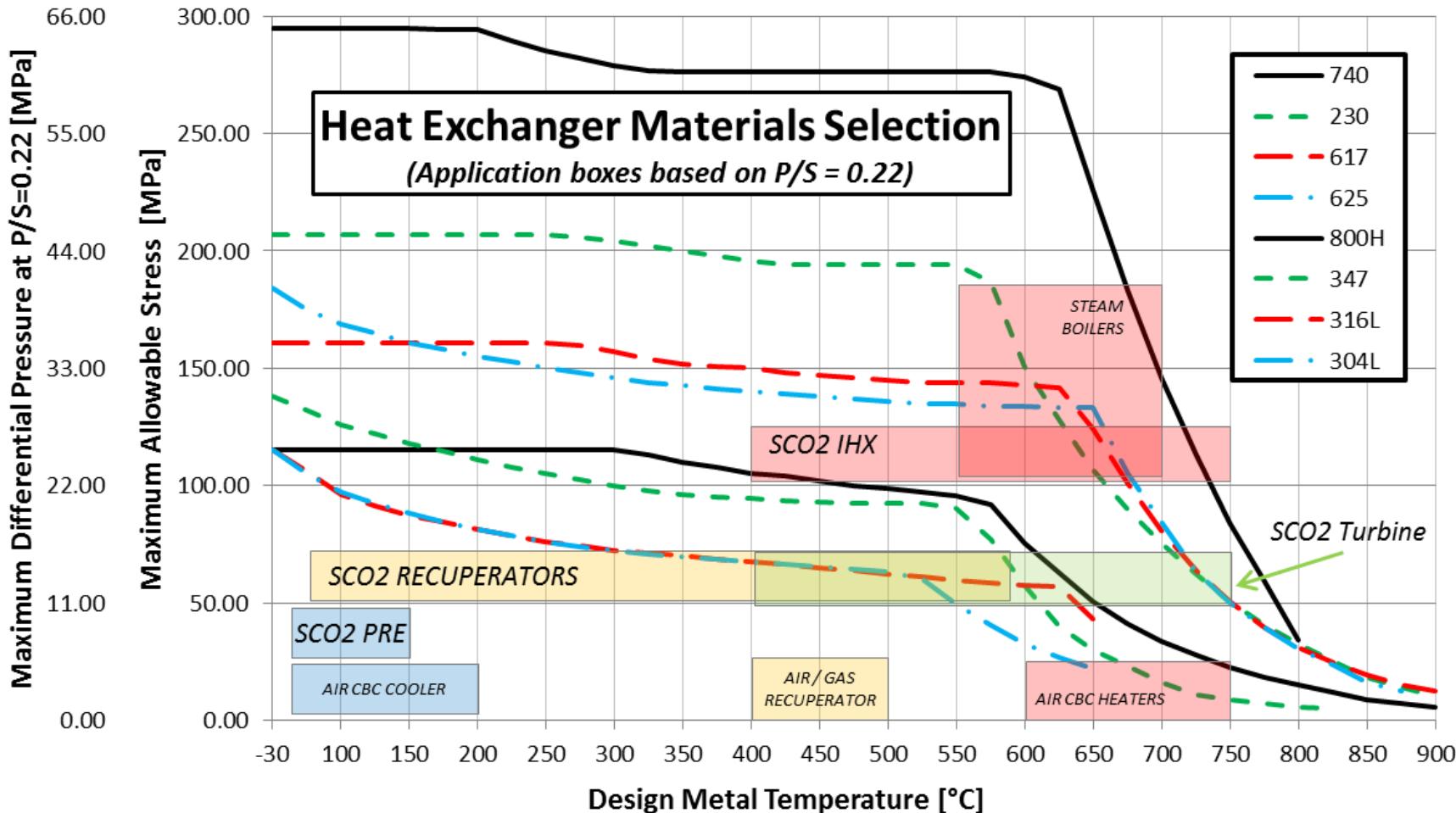
J.P. Gibbs, P. Hejzlar, & M.J. Driscoll. (2006). *Applicability of Supercritical CO₂ Power Conversion Systems to GEN IV Reactors* (Topical Report No. MIT-GFR-037) (p. 97). Cambridge, MA: Center for Advanced Nuclear Energy Systems MIT Department of Nuclear Science and Engineering.

Heat Exchangers are a Major Cost

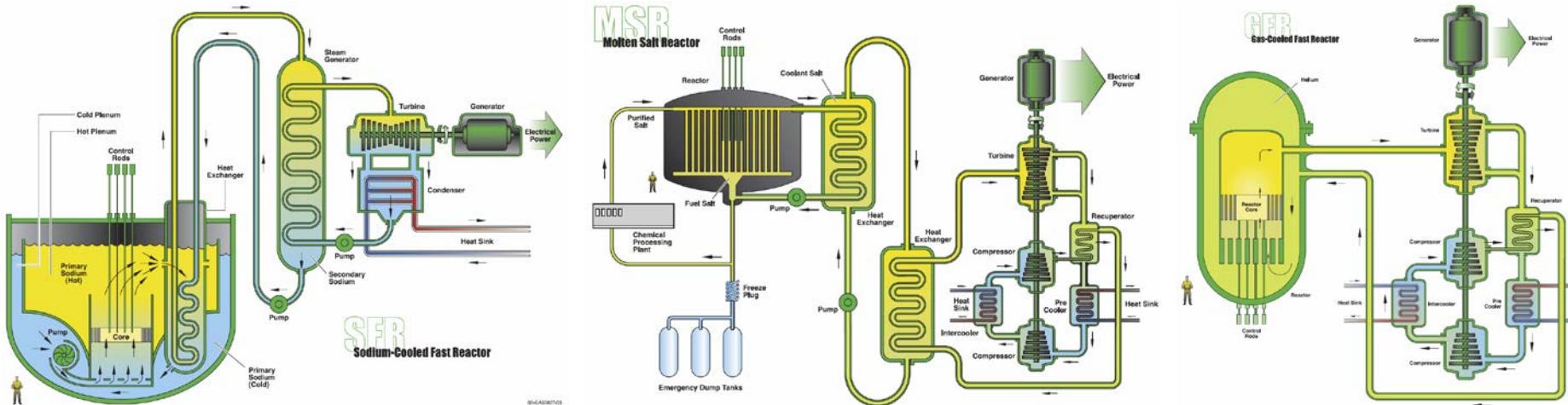
“[A] 30% reduction in HX cost would have [a] meaningful impact on system cost.”



Heat Exchangers push Materials

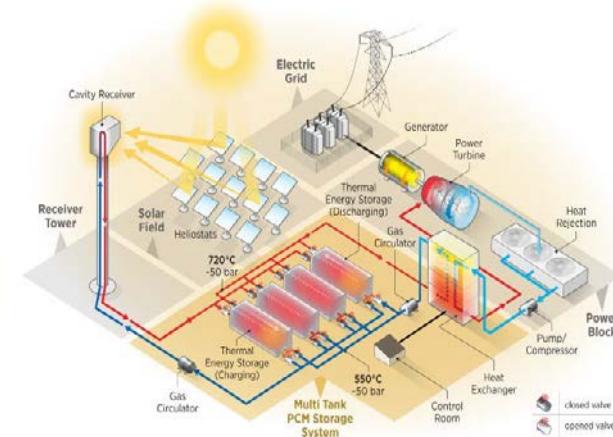
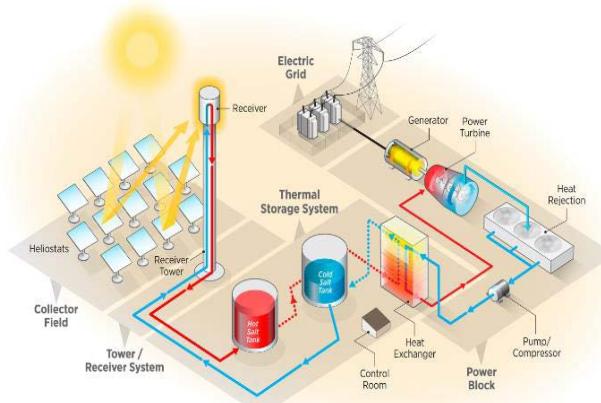
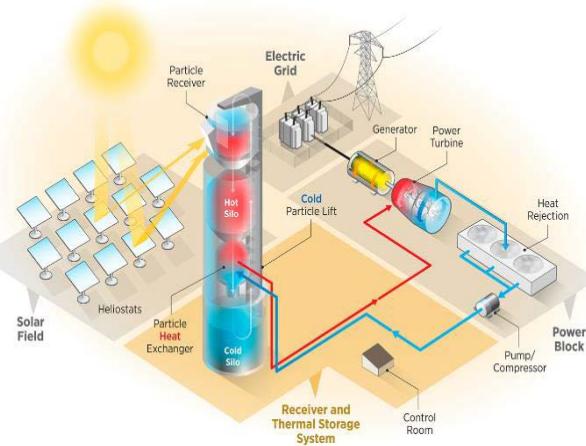


Nuclear Power Pathway Exchangers



Sodium Fast Reactor	Molten Salt Reactor	Gas Fast Reactor
Sodium/Sodium HXer	Salt/Salt HXer	(N/A)
<i>High reliability, tritium</i>	<i>High reliability, tritium</i>	<i>N/A</i>
Sodium/sCO₂ HXer	Salt/sCO₂ HXer	Helium/sCO₂ HXer
<i>Tritium, high pressure</i>	<i>Tritium, high pressure</i>	<i>High pressure</i>
	sCO₂ Recuperator	
	sCO₂ Water Cooler	
		<i>High sCO₂-side temperature and pressure, corrosion, size/cost</i>

Solar Power Pathway Exchangers



Solid (particles)

Particle Receiver

Efficiency

Particle/sCO₂ HXer

Erosion, size/cost, cycling

Liquid (salt)

Molten Salt Receiver

Corrosion, cycling

Molten Salt/sCO₂ HXer

Corrosion, size/cost, cycling

Gas (+ storage)

Gas Receiver

Cycling

*Storage/sCO₂ Hxer

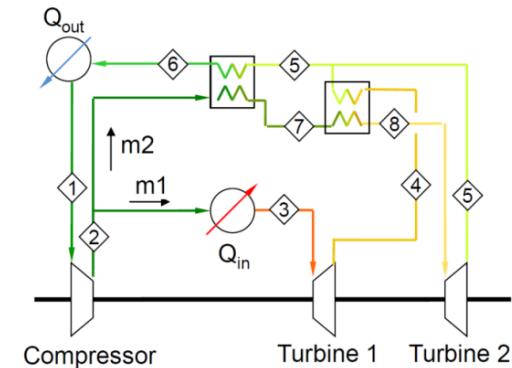
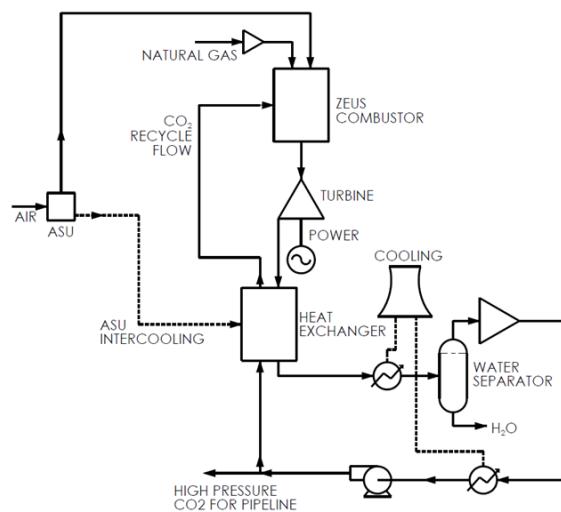
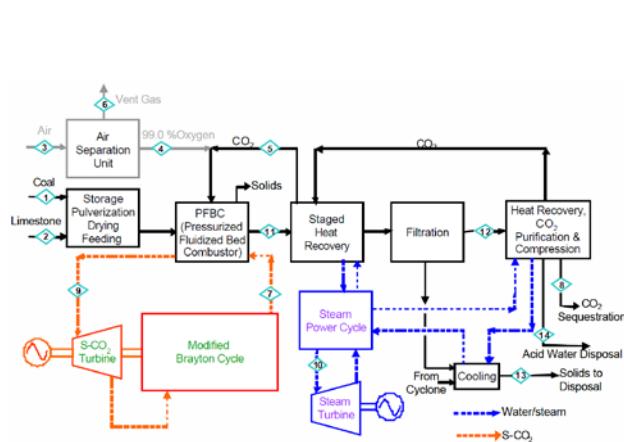
Size/cost, cycling

sCO₂ Recuperator

sCO₂ Air Cooler

High sCO₂-side temperature and pressure, corrosion, size/cost

Fossil Power Pathway Exchangers



Coal (direct)	Natural Gas (direct)	Bottoming Cycle
Combustor	Combustor	Waste Heat Exchanger
<i>High CO₂ combustion</i>	<i>High CO₂ combustion</i>	<i>High temperature/pressure</i>
sCO₂ Recuperator	sCO₂ Recuperator	sCO₂ Recuperator
<i>Combustion products, T/P</i>	<i>Combustion products, T/P</i>	<i>High temperature/pressure</i>
sCO₂ Air Cooler		
<i>High sCO₂-side temperature and pressure, corrosion, size/cost</i>		

Configuration Development Gaps

Technology Readiness Levels		sCO ₂ Heating from Various Sources															TIT / °C					
		from Direct Gas Combustion	from Exhaust Gas	from 3 MPa Helium	from Steam	from fluoride molten salts	from nitrate molten salts	from liquid sodium	from liquid lead-bismuth	from Heat Transfer Oil	from Combusting Particles	from Inert Solid Particles	from Geothermal Resources	from sunlight	Yet To Be Identified Materials	Advanced Nickel Alloys	Conventional Nickel Alloys	Austenitic Stainless Steels	to Water	to Humidified Air	to Dry Air	
Molten Salt Reactor	NE				3										4-5	6-8	6-8	2	2-4	700 to 850		
Sodium Fast Reactor (SFR)	NE					3										6-8	6-8	2	2-4	550		
Lead Fast Reactor (LFR)	NE						3								4-5	6-8	6-8	2	2-4	550 to 800		
Helium Gas Reactor (GFR, VHTR)	NE	4-5												2	3	4-5	6-8	6-8	2	2-4	700 to 1000	
Nuclear Shipboard Propulsion	NE															6-8	6-8			200 to 300		
Direct CSP Tower	EE													4-5		4-5	6-8	6-8	2	2-4	500 to 1000	
CSP Tower with Thermal Storage	EE															4-5	6-8	6-8	2	2-4	500 to 1000	
CSP Trough with Thermal Storage	EE					3	2									6-8	6-8	2	2-4	300 to 600		
CSP Dish Generator	EE					3		2							4-5	6-8			2-4	500 to 1000		
Direct Geothermal Plant	GT													2			6-8	6-8	2	2-4	100 to 300	
Indirect Geothermal Plant	GT															6-8	6-8	2	2-4	100 to 300		
Direct Natural Gas Combustion	FE	3-5	4												2	3	4-5	6-8	6-8	2	2-4	1100 to 1500
Integrated Gasification Coal	FE	3-5													2	3	4-5	6-8	6-8	2	2-4	1100 to 1500
Pulverized Coal Fluidized Bed	FE														3	4-5	6-8	6-8	2	2-4	550 to 900	
Waste Heat Recovery	FE		4														6-8	6-8	2	2-4	230 to 650	
Gas Turbine Bottoming	FE		4														6-8	6-8	2	2-4	230 to 650	
Municipal waste to energy	FE		4														6-8	6-8	2	2-4	230 to 650	
10 MWe Pilot	FE		4													4-5	6-8	6-8	2	2-4	550 to 700	
50 MWe Demonstration	FE		4													4-5	6-8	6-8	2	2-4	550 to 700	
		N/A	Gas		Liquid			Solid		>750	750	650	550		sCO ₂ Cooling							
		sCO ₂ Heating from Various Sources															Recuperation MDMT / °C					

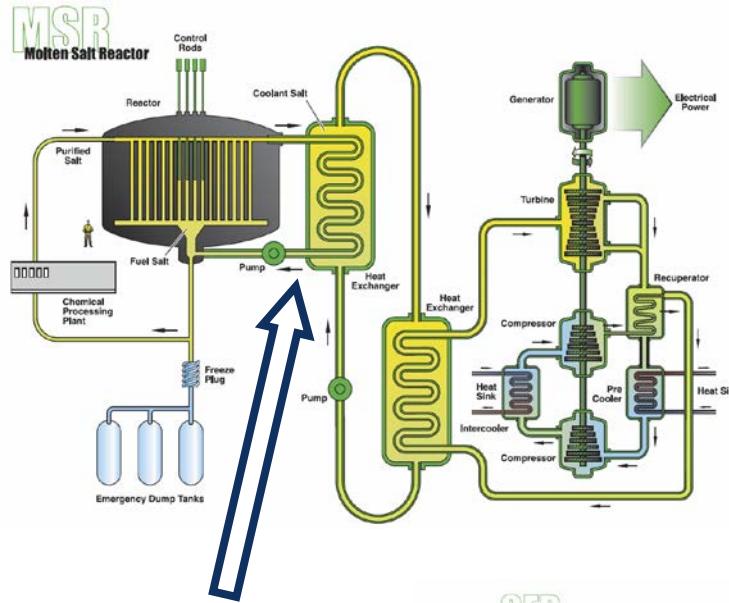
High Temperature
Recuperators

Key Research Areas

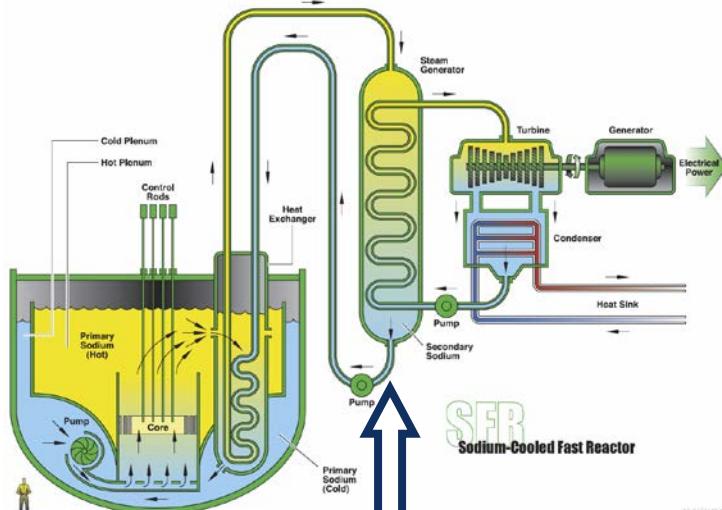
- Lifetime validation of compact heat exchangers
 - Failure modes
 - Pressure/thermal/corrosion-assisted fatigue
 - Creep behavior and lifetime
 - Inspection and monitoring
- Affordable compact heat exchanger configurations
 - Configurations with large (gas/liquid) and small (sCO₂) flow areas
 - Fabrication using advanced corrosion-resistant materials (nickels)
 - Tritium management for nuclear applications
- Methods to leverage low-cost materials at high temperature
 - Corrosion-resistant coatings for stainless steels
 - Coating failure potential and lifetime
 - Modular designs to allow for shorter lifetimes

SUMMARY OF SANDIA RESEARCH EFFORTS

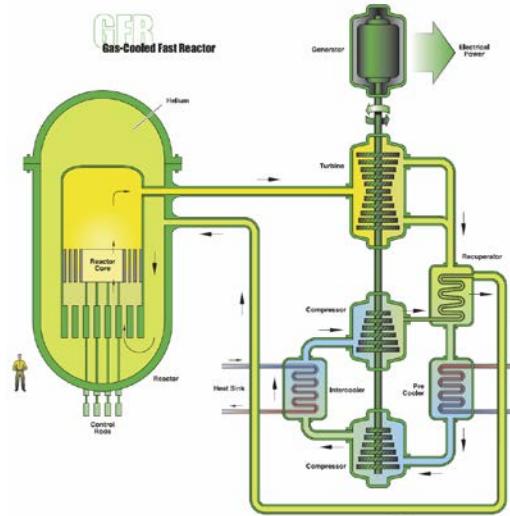
Project Map – Nuclear Applications



UNM NEUP
CFA-15-8667
Double-Walled
Twisted Tube HXers



SFR
Sodium-Cooled Fast Reactor



UW-Madison NEUP
CFA-17-12481
sCO₂-cooled
Space Reactor

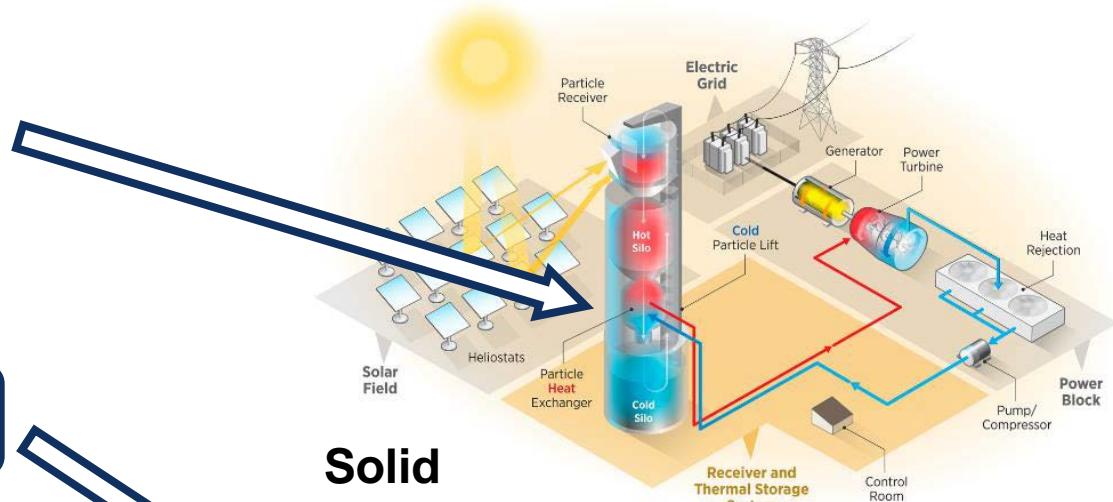
UW-Madison IRP

IRP-17-14227
Compact HXers for
Nuclear Applications

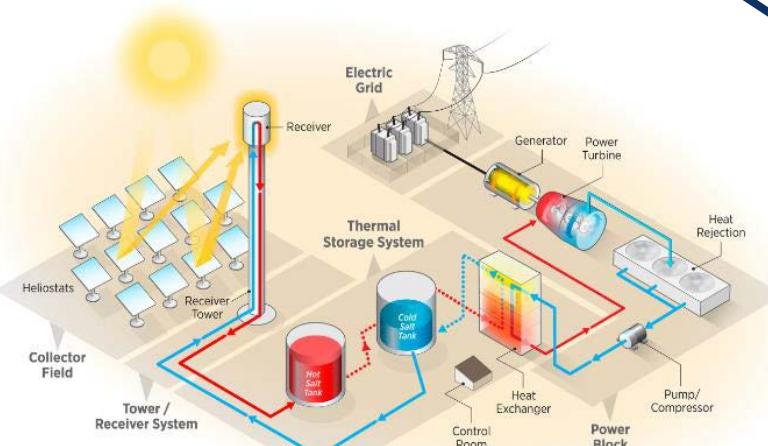
Project Map – Solar Applications

SuNLaMP
1507
Particle-sCO₂ HXer

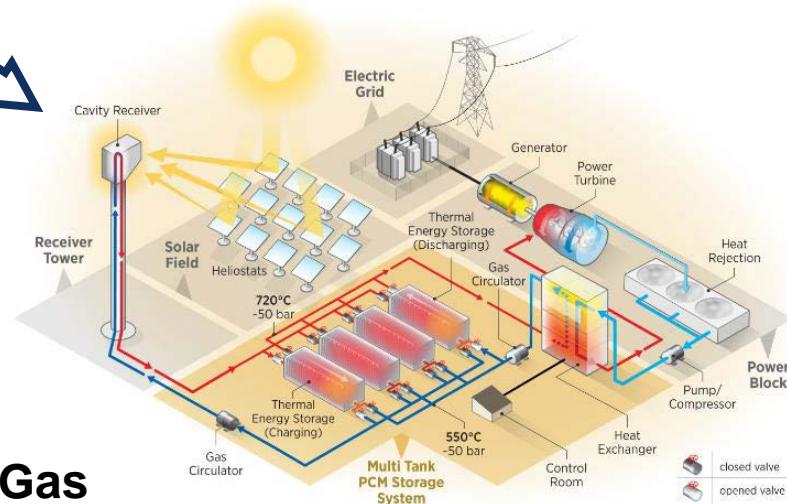
Oregon State University
DE-EE0007108
Direct sCO₂ Gas Receiver



Solid

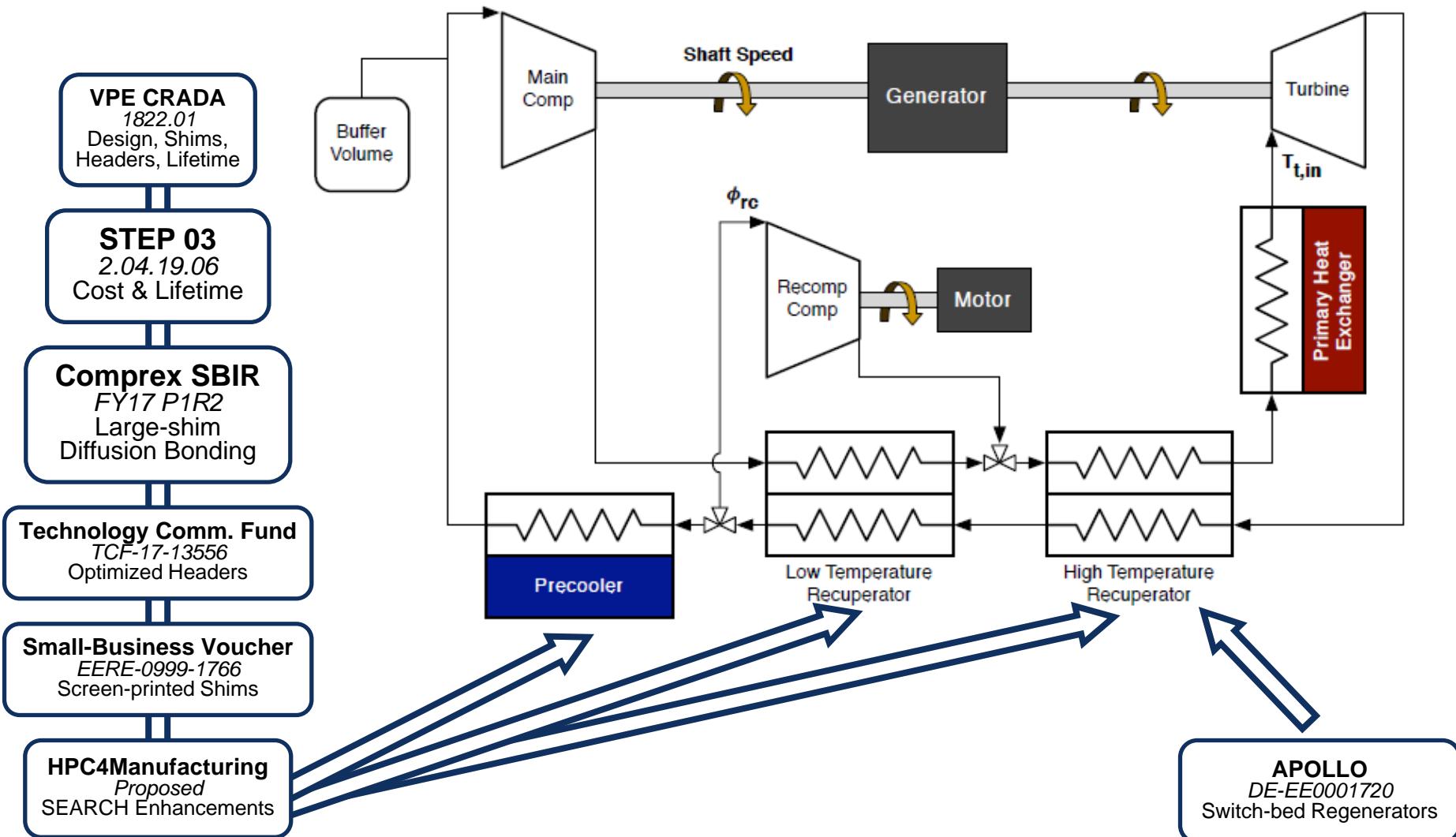


Liquid

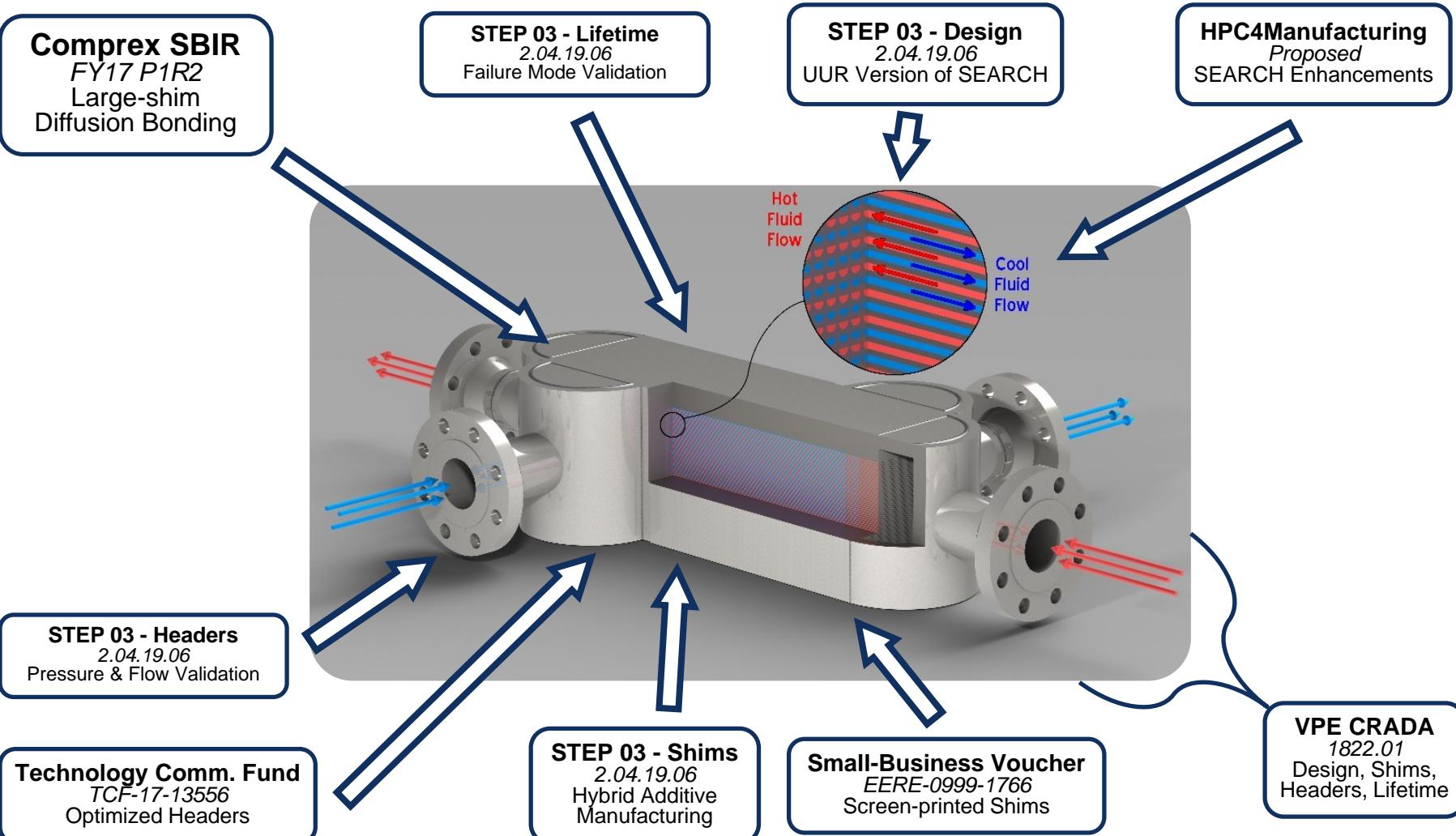


Gas

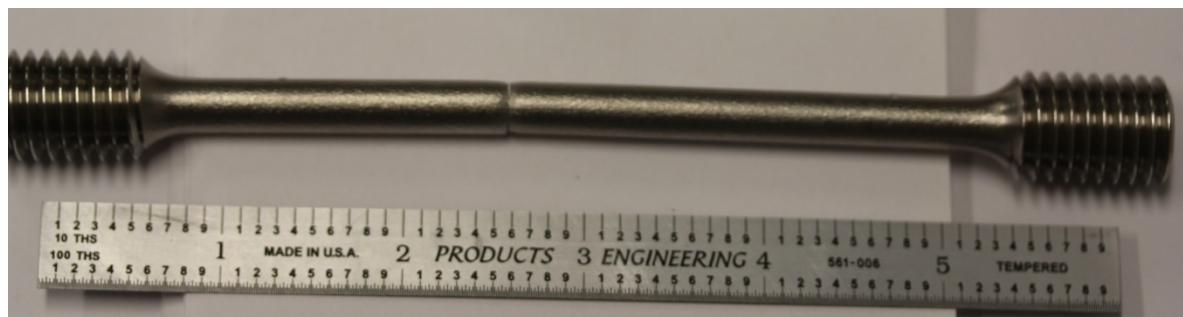
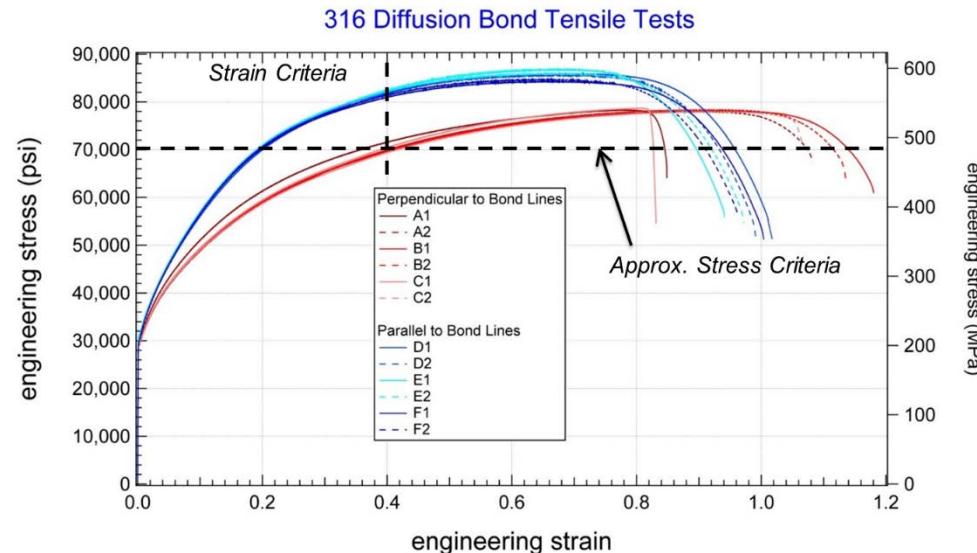
Project Map – sCO₂ Cycle Level



Project Map – Component Level



VPE Bonding Process Certification



SEARCH Heat Exchanger Design Tool

- Sub-hxer model
- ASME BPVC
- Single, two-phase, supercritical flows
- Over 400 fluids

Document Number: **RC1**

Revision Number: **1**

Heat Exchanger Data Sheet

solutionScope\$= All design steps (mech, thermo, TH)

Calculate  Save Inputs  Load Inputs 

Side A (straight)

Side B (Z-side)

Step 1. Side A and B Stream Compositions (by mass %)

Choose the fluid set: **Reprop Fluid(s)**

First 8 fluid components:

100 [%]	WATER.FLD
0 [%]	ACETONE.FLD
0 [%]	Nitrogen.fld
0 [%]	co2.fld
0 [%]	Propane.FLD
0 [%]	BUTANE.FLD
0 [%]	IPENTANE.FLD
0 [%]	HEXANE.FLD

Fouling (val A, val B) **CO2 vapor** **CO2 vapor**

Fouling Factor: $R^*_{f,A} = 0.0001 \text{ [m}^2\text{]}$ $R^*_{f,B} = 0.0001 \text{ [m}^2\text{]}$

Step 2. Specify Fluid Flow Rates

Flow Rate (mass A, mass B) $\dot{m}_A = 80.4 \text{ [kg/s]}$ $\dot{m}_B = 34.9 \text{ [kg/s]}$

$\dot{V}_A = \text{**** [m}^3\text{/s]}$ $\dot{V}_B = \text{**** [m}^3\text{/s]}$

Inlet States (T_A, P_A, T_B, P_B)

Inlet Pressure $P_A = 7.170E+06 \text{ [Pa]}$ $P_B = 2.330E+07 \text{ [Pa]}$

Inlet Temperature $T_{A,in} = 572.8 \text{ [K]}$ $T_{B,in} = 378.1 \text{ [K]}$

Inlet Quality (± 100 = sup or sub) $Q_{A,in} = \text{**}$ $Q_{B,in} = \text{**}$

Outlet Pressure $P_{A,out} = \text{**** [Pa]}$ $P_{B,out} = \text{**** [Pa]}$

Outlet Temperature $T_{A,out} = \text{** [K]}$ $T_{B,out} = 564.2 \text{ [K]}$

Outlet Quality (± 100 = sup or sub) $Q_{A,out} = \text{**}$ $Q_{B,out} = \text{**}$

Step 4. Specify the Allowable Pressure Drop

Pressure Drop $dPsum_A = \text{**** [Pa]}$ $dPsum_B = \text{**** [Pa]}$

Drop / Operating Pressure $dP_{A,\%} = \text{**** [%]}$ $dP_{B,\%} = \text{**** [%]}$

Step 5. Specify Header Orientations

Header Axis Orientation **Vertical** **Vertical**

Step 7. Specify Core Channel Geometry

Channel Width $w_A = 0.001289 \text{ [m]}$ $w_B = 0.001289 \text{ [m]}$

Channel Depth $d_A = 0.000763 \text{ [m]}$ $d_B = 0.000763 \text{ [m]}$

Summary of PCHE Design

Job Number **RC1**

Run Date *********

Job Title **Test**

Code Used **ASME Code Section VIII Division 1 - 2013**

Core Length (bet. headers) $L = \text{**** [m]}$

Core Width (bet. headers) $W = \text{**** [m]}$

Core Height $H = \text{**** [m]}$

Core Cross-Section (H x W) $A_c = \text{**** [m}^2\text{]}$

Side A Surface Area $A_{SA} = \text{**** [m}^2\text{]}$

Side B Surface Area $A_{SB} = \text{**** [m}^2\text{]}$

Wetted Volume (core + hdrs) $Vol_{wet} = \text{**** [m}^3\text{]}$

Metal Mass (core + hdrs) $M = \text{*** [kg]}$

Heat Transfer Rate (Duty) $\dot{q} = \text{***** [W]}$

Conductance-Area Product $U_{Asum} = \text{**** [W/K]}$

Side A MAWP $MAWP_A = \text{**** [Pa]}$

Side B MAWP $MAWP_B = \text{**** [Pa]}$

MAWT (same as MDMT) $MAWT = \text{*** [K]}$

Number of Etched Plate Pairs $N_{rows} = \text{** [-]}$

Side A Channels per Plate $N_{chip,A} = \text{* [-]}$

Side B Channels per Plate $N_{chip,B} = \text{* [-]}$

Number of Un-etched Plates $N_{ex} = \text{* [-]}$

Step 9. Other Controls

Max Active core volume width $W_{ACV,max} = 0.1597 \text{ [m]}$

Max Active core volume height $H_{ACV,max} = 2.5 \text{ [m]}$

Extra width provided $W_{extra} = 0 \text{ [m]}$

Extra height provided $H_{extra} = 0 \text{ [m]}$

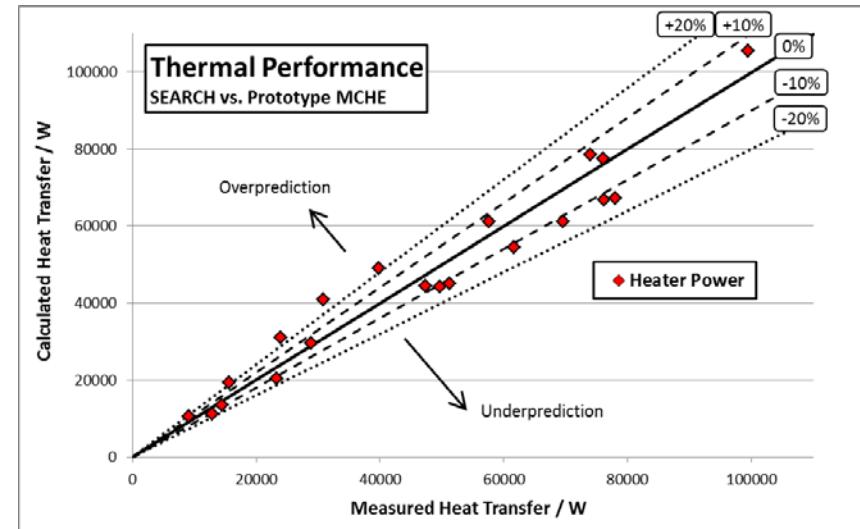
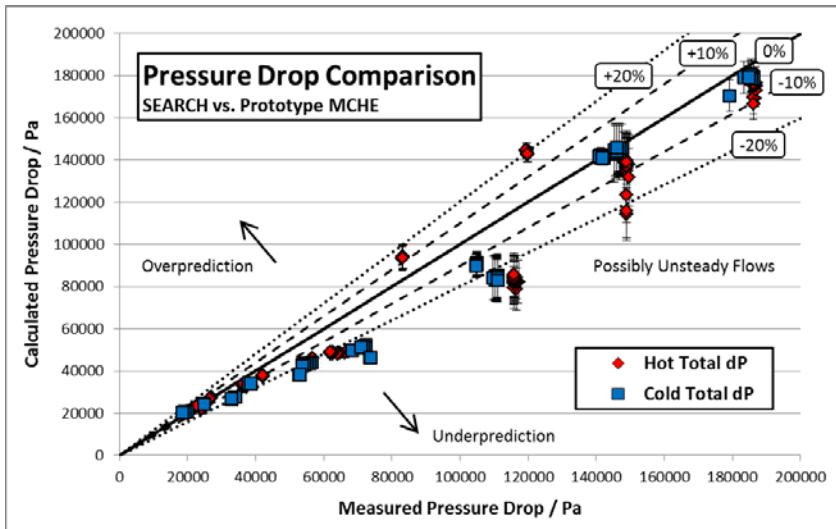
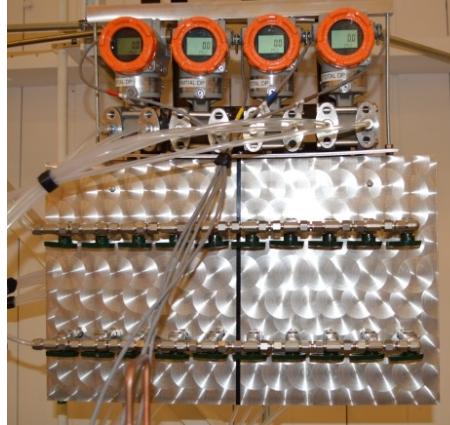
Step 6. Specify the Performance Measure

Choose Measure Type **Side B Outlet Temperature**

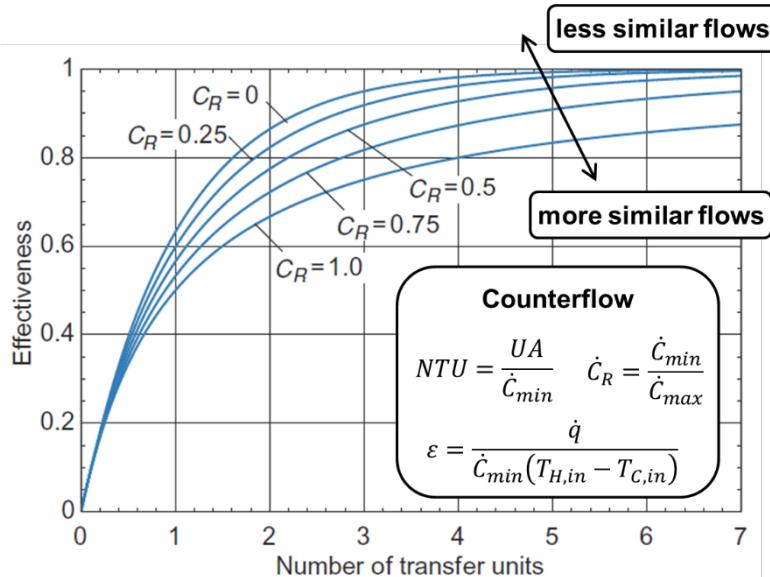
Diffusion Bonding Joint Efficiency $E_{DB} = 0.7 \text{ [-]}$

Header Cylinder Joint Efficiency $E_{cyl} = 0.7 \text{ [-]}$

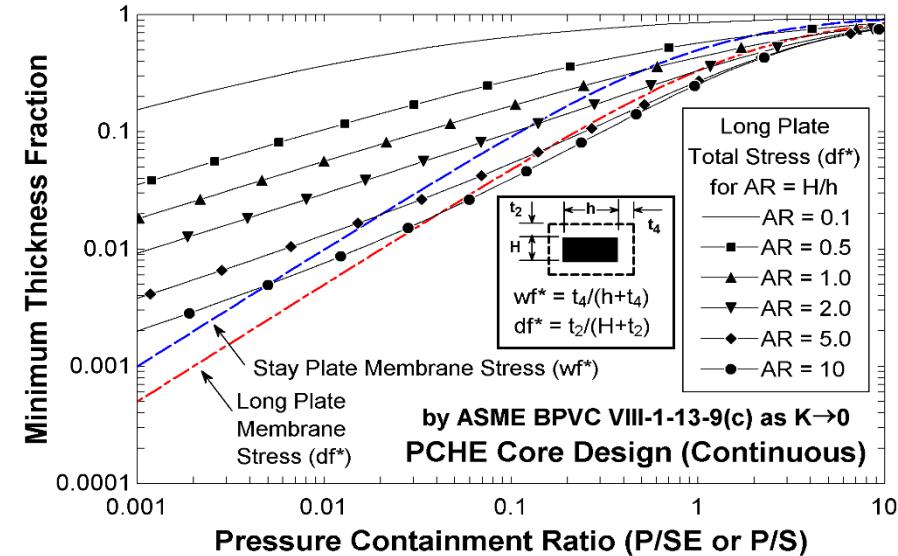
SEARCH Experimental Verification



Design Optimization



Thermodynamics



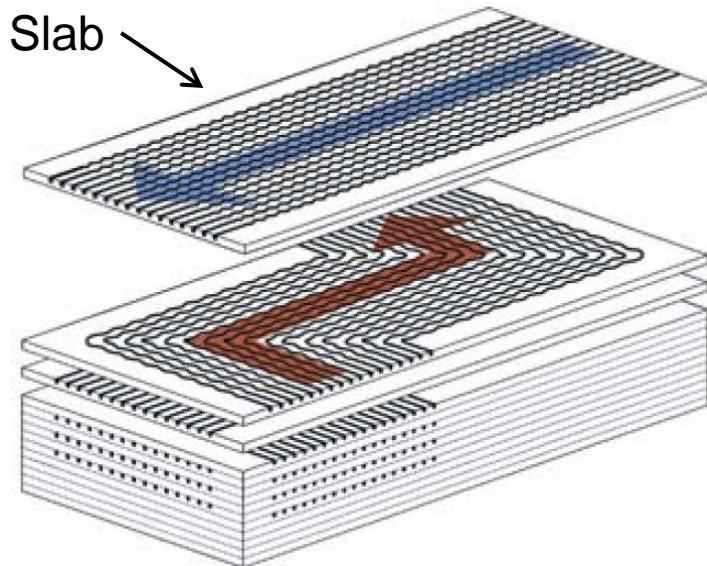
Pressure Containment

Thermal-Hydraulics

$$\Delta x_i = UA_i \left(\frac{1}{h_{A,i} N_{ch,A} p_{ch,A}} + \frac{R''_{f,A,i}}{N_{ch,A} p_{ch,A}} + \frac{t_m}{k_{m,i} W} + \frac{1}{h_{B,i} N_{ch,B} p_{ch,B}} + \frac{R''_{f,B,i}}{N_{ch,B} p_{ch,B}} \right)$$

Hybrid Additive Manufacturing

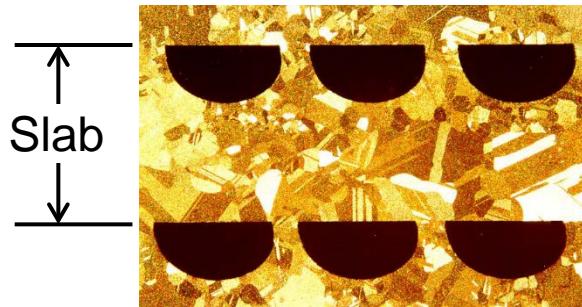
Heat Exchanger Core



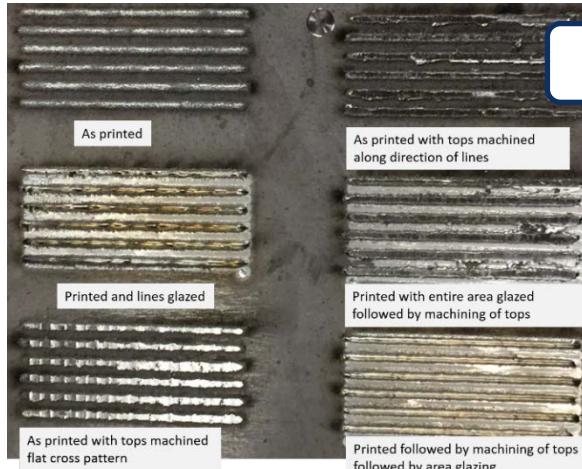
Core and Manifold Assembly



Diffusion Bonding

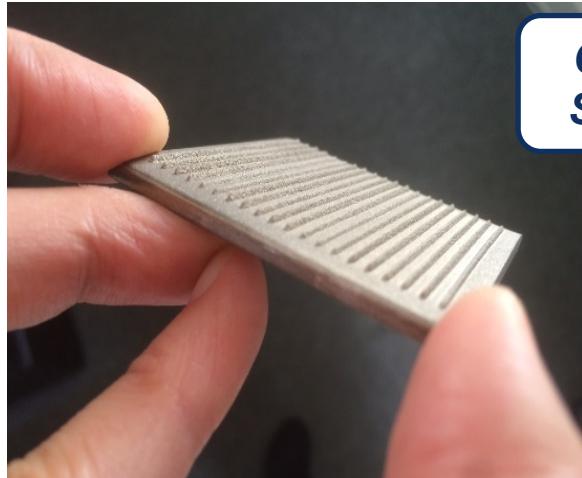
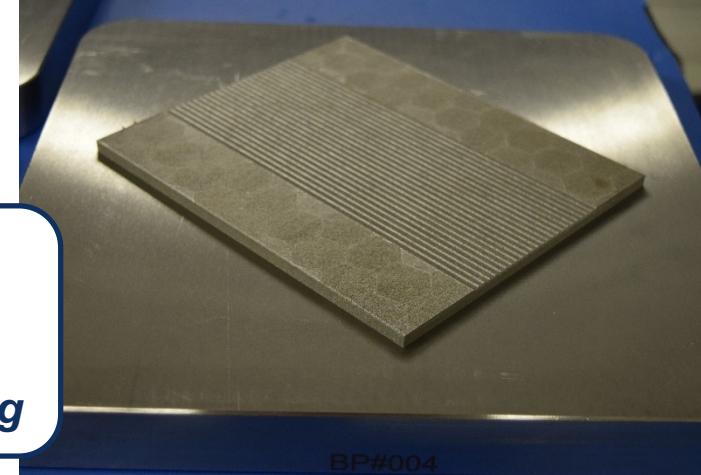


Hybrid Additive Manufacturing



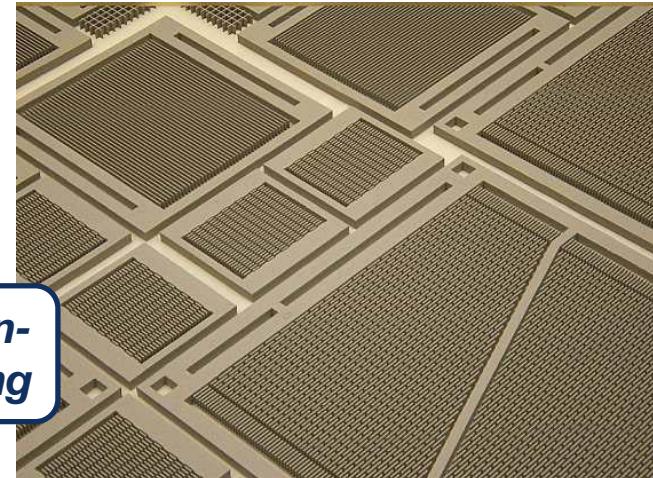
LENS

*Direct
Metal
Laser
Sintering*



**Cold-
Spray**

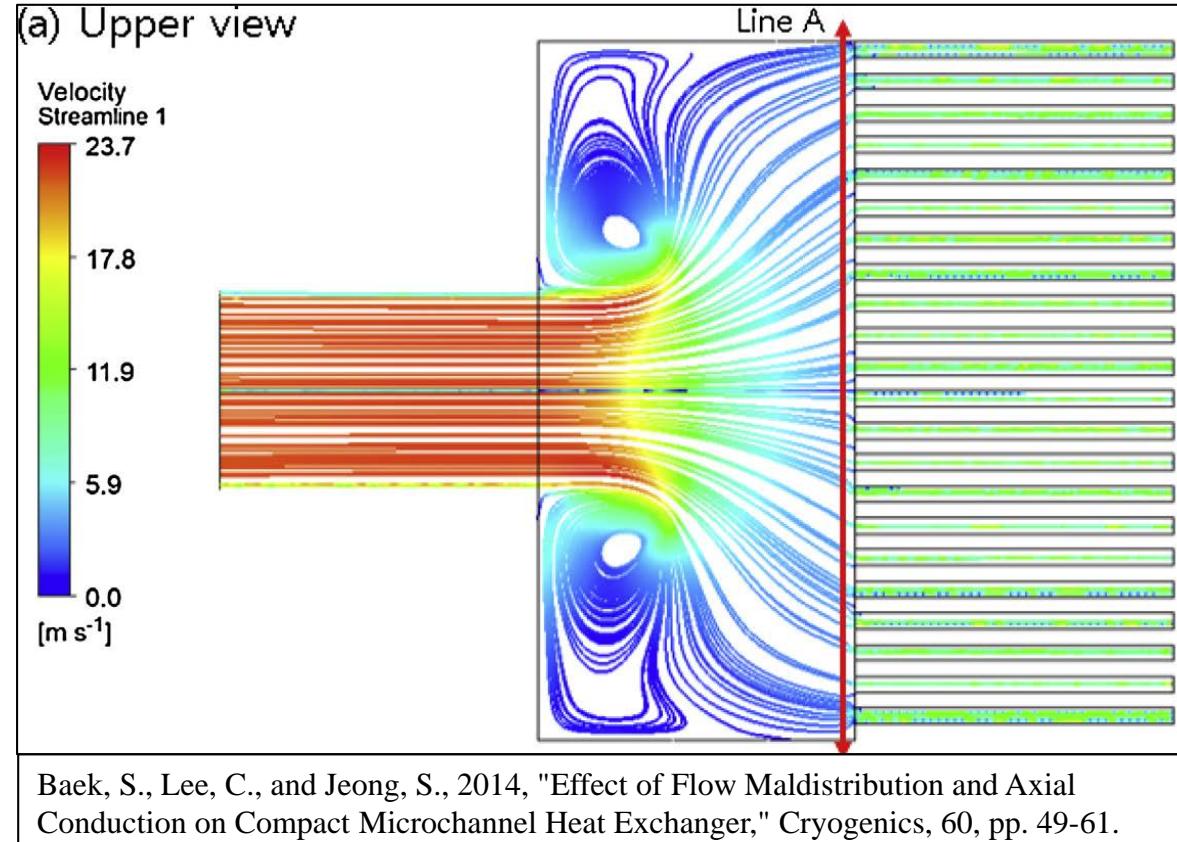
*Screen-
Printing*



Alternative Headers:

Flow maldistribution in PCHEs reduces effectiveness

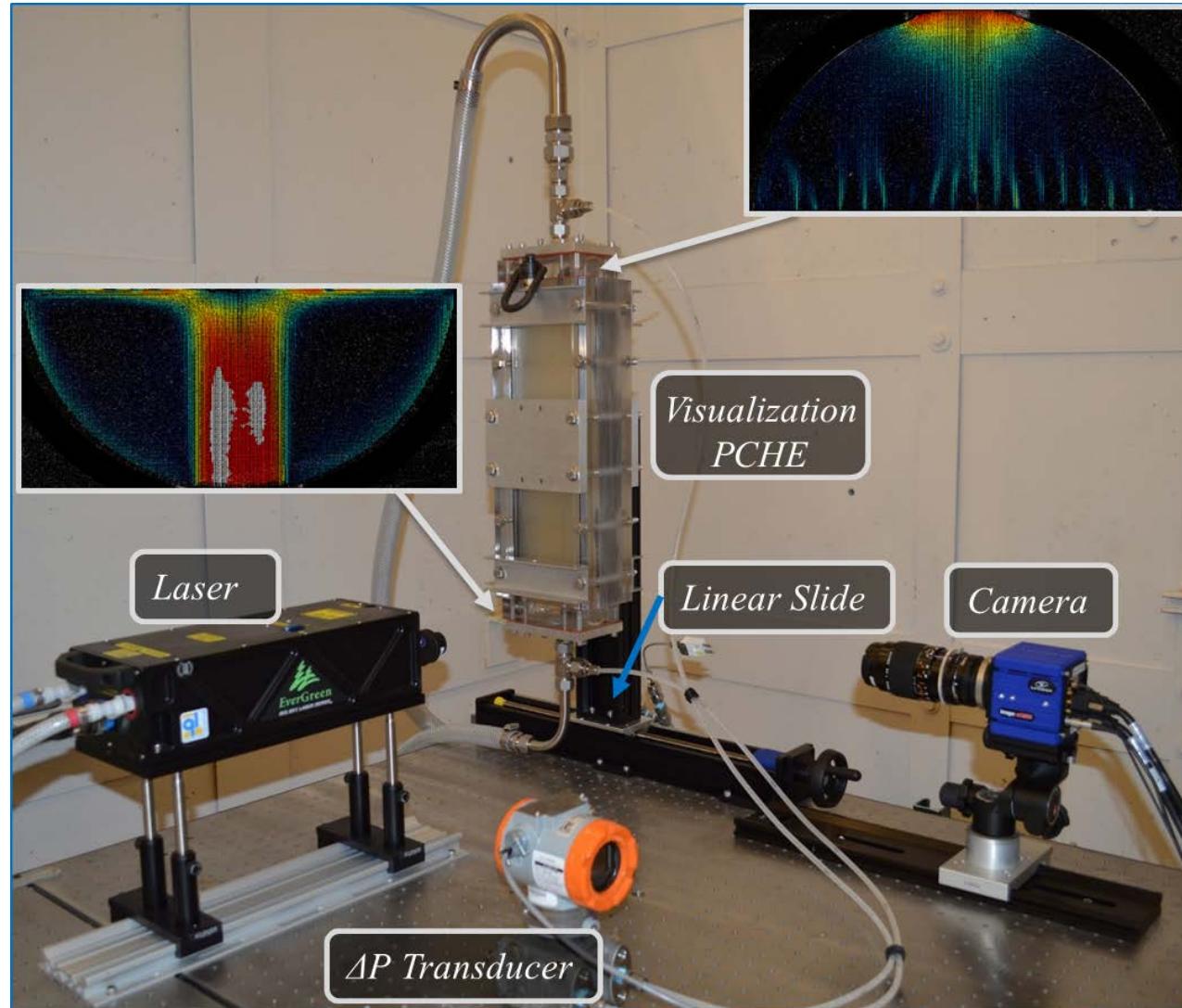
- Flow maldistribution can have a significant impact on compact heat exchanger effectiveness with reductions of 5-15%
- Others have predicted flow maldistribution with computational fluid dynamics (CFD)
- No experimental data are known for this issue



Alternative Headers:

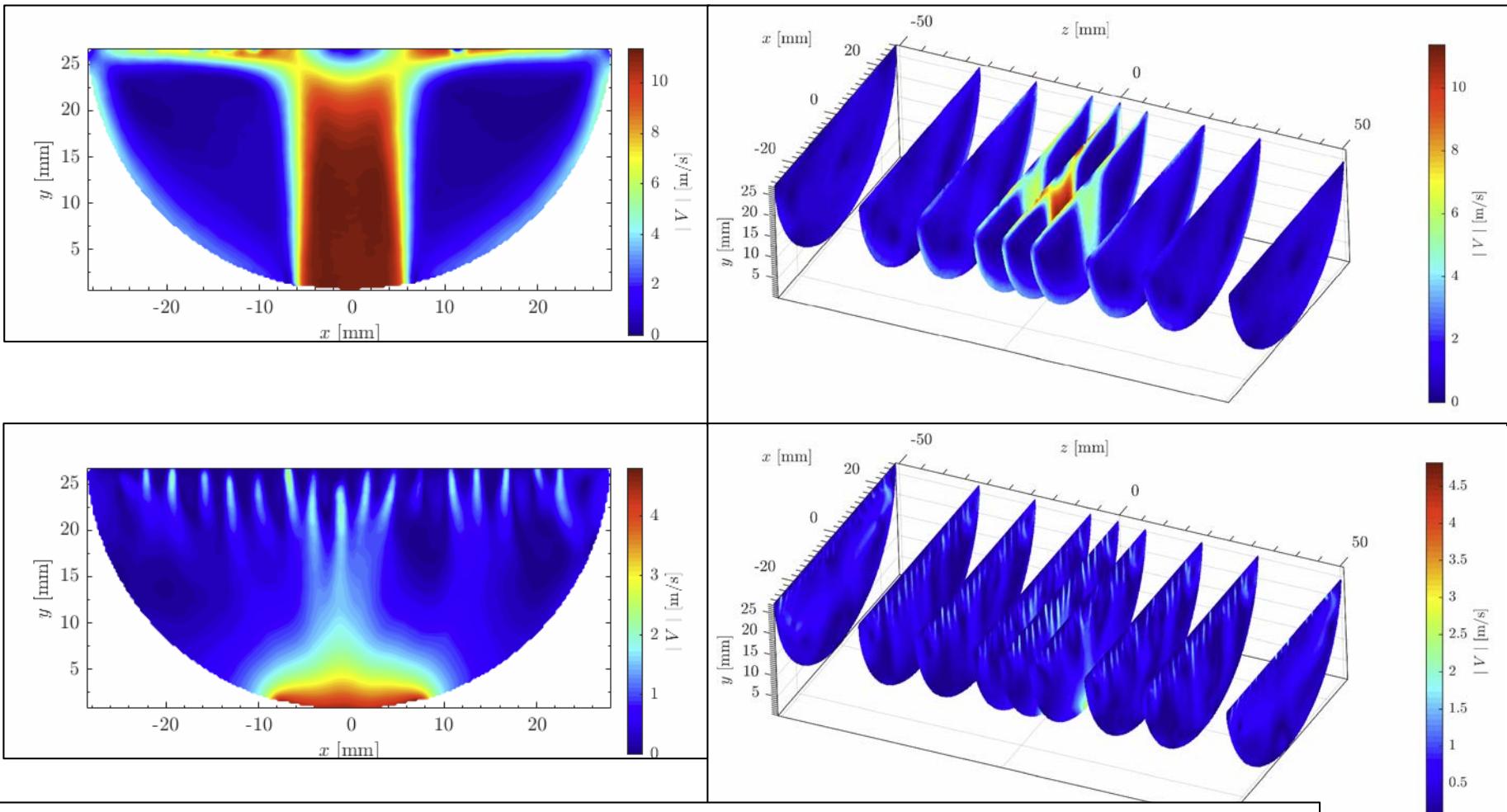
We measured the flow distribution with PIV in a PCHE prototype

- We performed the first known measurements of flow distribution in compact heat exchangers
- An acrylic prototype was made for use with water
- An optical system called Particle Image Velocimetry (PIV) was used to measure flow fields



Alternative Headers:

Velocity magnitude was mapped out in space and reveals variations



Lifetime Validation Testing

- Testing
 - Headers
 - Cores
 - Full Parts
- Flexibility
 - 1 to 10 ksi
 - 10 to 60 ksi
 - Remote operation
- Modes
 - Proof test
 - Burst test
 - Pressure fatigue
 - Thermal fatigue



CONCLUSIONS

Key Research Areas

- Lifetime validation of compact heat exchangers
 - Failure modes
 - Pressure/thermal/corrosion-assisted fatigue
 - Creep behavior and lifetime
 - Inspection and monitoring
- Affordable compact heat exchanger configurations
 - Configurations with large (gas/liquid) and small (sCO₂) flow areas
 - Fabrication using advanced corrosion-resistant materials (nickels)
 - Tritium management for nuclear applications
- Methods to leverage low-cost materials at high temperature
 - Corrosion-resistant coatings for stainless steels
 - Coating failure potential and lifetime
 - Modular designs to allow for shorter lifetimes