

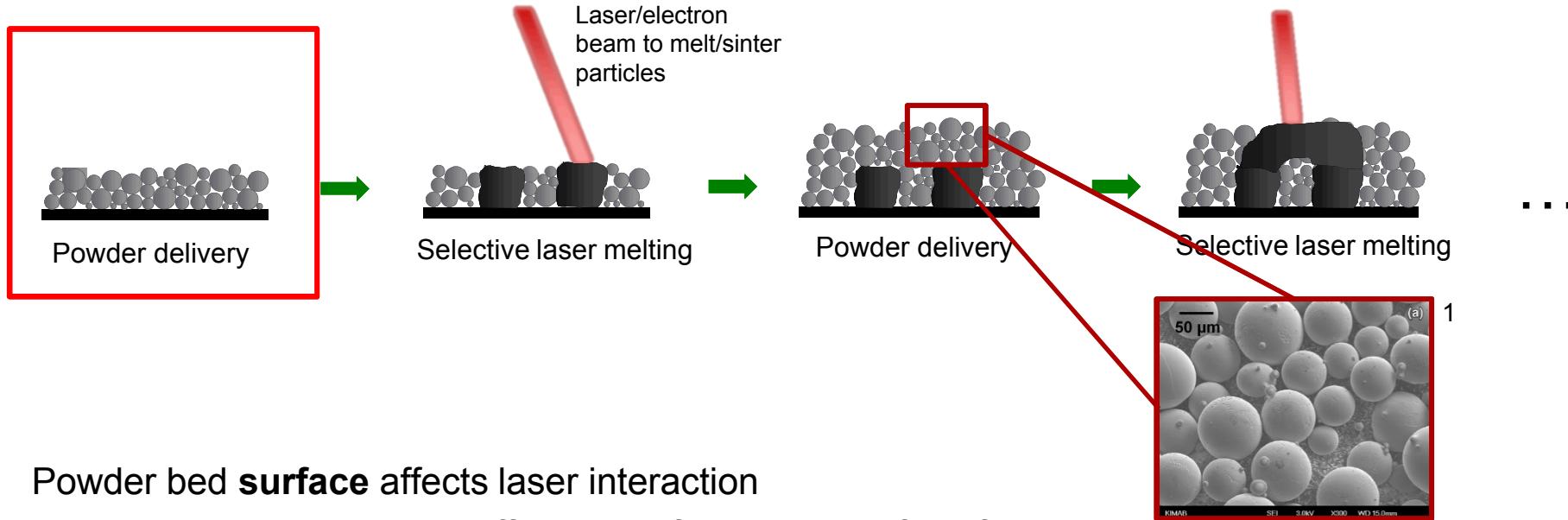
Discrete element modeling of powder spreading and flow for metal additive manufacturing

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Background and Motivation

Layer-by-layer powder bed fusion processes (e.g. SLM/SLS):



- Powder bed **surface** affects laser interaction
- Powder bed **bulk packing** affects void formation, surface finish
- **Variability in powder properties** due to e.g. vendor supply, powder recycling
- Some key length scales:
 - Layer thickness $\sim 30\text{-}100 \mu\text{m}$
 - Laser spot size $\sim 100\text{-}200 \mu\text{m}$
 - Particle diameter $\sim 10\text{-}100 \mu\text{m}$
 - Material defects $\sim 100 \mu\text{m}$



Understanding powder at scale of individual particles is important!

Simulation method: Discrete Element Method (DEM)

Layer thickness \sim particle diameter

→ continuum models (e.g. $\mu(I)$ rheology)
inherently unsuitable

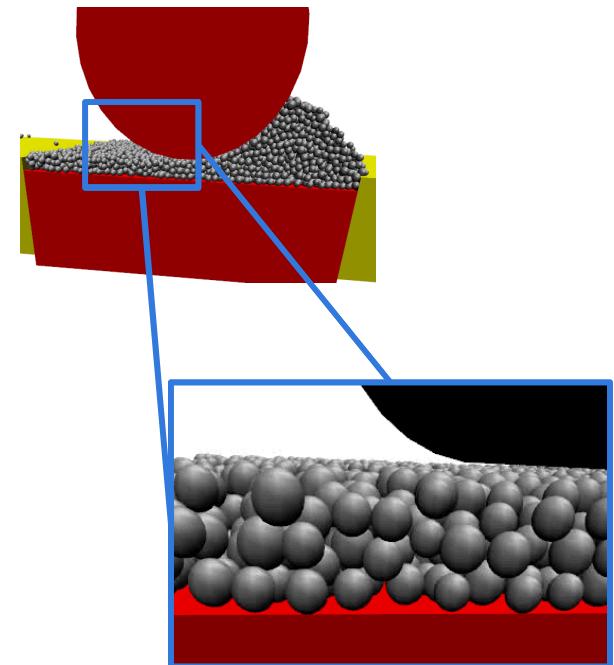
Method of choice: DEM

Advantages:

- Captures individual particle dynamics
- Can handle polydispersity, shape variations, complex geometries
- Material properties captured by contact parameters

Disadvantages:

- Computationally expensive
- **Difficult to parametrize**



Simulation method: Discrete Element Method (DEM)

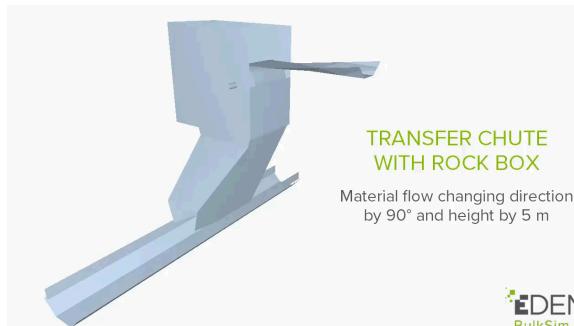
Molecular dynamics-like method:

- Particles modeled explicitly (position, velocity, angular velocity)
- Integrate collective dynamics:

$$\mathbf{F}_i = m_i \frac{d^2 \mathbf{r}_i}{dt^2} \quad \tau_i = I_i \frac{d^2 \mathbf{w}_i}{dt^2} \quad i = 1, \dots, N \quad N \approx 10^5 - 10^6$$

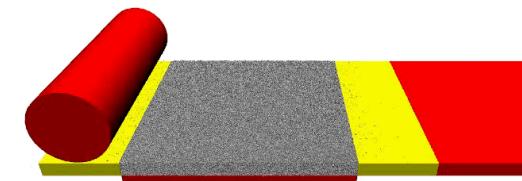
- Forces/torques computed at contact based on reduced order models

Well-established for 'large' particle applications (e.g. mining, pharmaceutical)



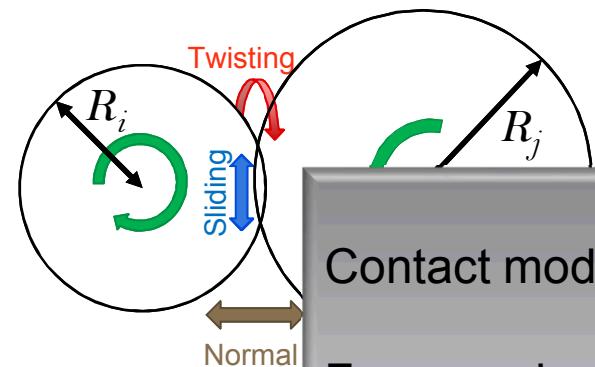
From EDEM youtube channel

Much more challenging for fine/cohesive powders!



<http://lammps.sandia.gov>

Granular contact models



Geometry/kinematics

$\mathbf{r}_i, \mathbf{r}_j$: positions
 $\mathbf{v}_i, \mathbf{v}_j$: translational velocities
 $\boldsymbol{\Omega}_i, \boldsymbol{\Omega}_j$: angular velocities
 a : area of contact*

$$\delta = R_i + R_j - \|\mathbf{r}_i - \mathbf{r}_j\|$$

$$\mathbf{n} = (\mathbf{r}_i - \mathbf{r}_j) / \|\mathbf{r}_i - \mathbf{r}_j\|$$

$$R = \frac{1}{1/R_i + 1/R_j} = \frac{R_i R_j}{R_i + R_j}$$

$$\mathbf{v}_R = \mathbf{v}_i - \mathbf{v}_j$$

$$\mathbf{v}_t = \mathbf{v}_R - (\mathbf{v}_R \cdot \mathbf{n})\mathbf{n}$$

Relative sliding velocity:

$$\mathbf{v}_{tR} = \mathbf{v}_t - (R_i \boldsymbol{\Omega}_i + R_j \boldsymbol{\Omega}_j) \times \mathbf{n}$$

Relative twisting 'velocity':

$$\boldsymbol{\Omega}_T = (\boldsymbol{\Omega}_i(\tau) - \boldsymbol{\Omega}_j(\tau)) \cdot \mathbf{n}$$

Relative rolling velocity:

$$\mathbf{v}_L = -R(\boldsymbol{\Omega}_i - \boldsymbol{\Omega}_j) \times \mathbf{n}$$

* a depends on contact model!

	gran/hertz	dmt/rolling	jkr/rolling
Normal elastic (spring)	$\mathbf{F}_n = k_n \sqrt{R} \delta^{3/2} \mathbf{n}$	$\mathbf{F}_n = \left(\frac{4Ea^3}{3R} - 4\pi\gamma R \right) \mathbf{n}$ $\delta_N = a^2/R$ $F_{\text{pulloff}} = -4\pi\gamma R$	$\mathbf{F}_n = \left(\frac{4Ea^3}{3R} - 2\pi a^2 \sqrt{\frac{4\gamma E}{\pi a}} \right) \mathbf{n}$ $\delta_N = a^2/R - 2\sqrt{\pi\gamma a/E}$ $F_{\text{pulloff}} = -3\pi\gamma R$

Contact models are complicated!

Focus on key physics and associated parameters:

1. Cohesion \rightarrow relates to surface chemistry, morphology
2. Friction \rightarrow relates to surface morphology, micromechanics

Consider both particle/particle and particle/wall interactions

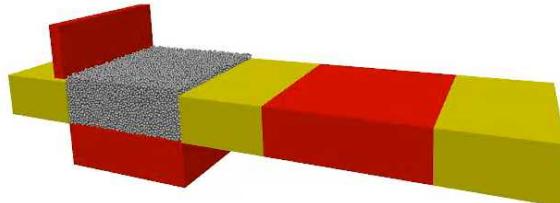
k_N, k_S, k_T, k_R : normal, sliding, twisting, rolling stiffness
 $\eta_N, \eta_S, \eta_T, \eta_R$: normal, sliding, twisting, rolling dissipation
 μ_S, μ_T, μ_R : sliding, twisting, rolling friction coefficients

Rolling frictional		$\ \mathbf{F}_R\ \leq F_{R,\text{crit}}$	$\ \mathbf{F}_R\ \leq F_{R,\text{crit}}$
Twisting elastic ³		$F_{R,\text{crit}} = \mu_R \ \mathbf{F}_n\ $	
Twisting dissipative		$M_t = -k_Q \int_{t_0}^t \Omega_T(\tau) d\tau$	$M_t = -k_Q \int_{t_0}^t \Omega_T(\tau) d\tau$
Twisting frictional		$- \eta_Q \Omega_T$	$- \eta_Q \Omega_T$
		$M_t \leq -M_{t,\text{crit}} \Omega_T / \ \Omega_T\ $ $M_{t,\text{crit}} = \frac{2}{3} a F_{s,\text{crit}}$	$M_t \leq -M_{t,\text{crit}} \Omega_T / \ \Omega_T\ $ $M_{t,\text{crit}} = \frac{2}{3} a F_{s,\text{crit}}$

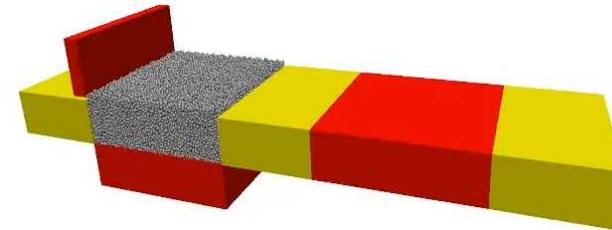
1,2,3: Integrals must be carried out to remove effects of rigid body rotation/twisting of contacting pair

2: \mathbf{F}_R is a 'pseudo-force', resulting only in torque $\mathbf{R} \times \mathbf{F}_R$

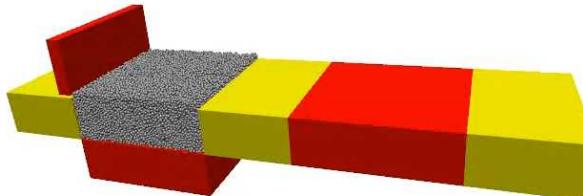
Granular contact models



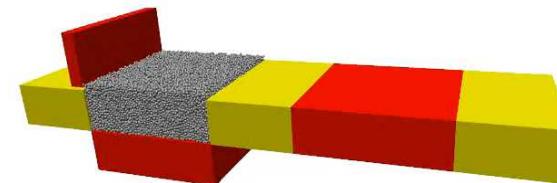
No rolling friction



No sliding friction

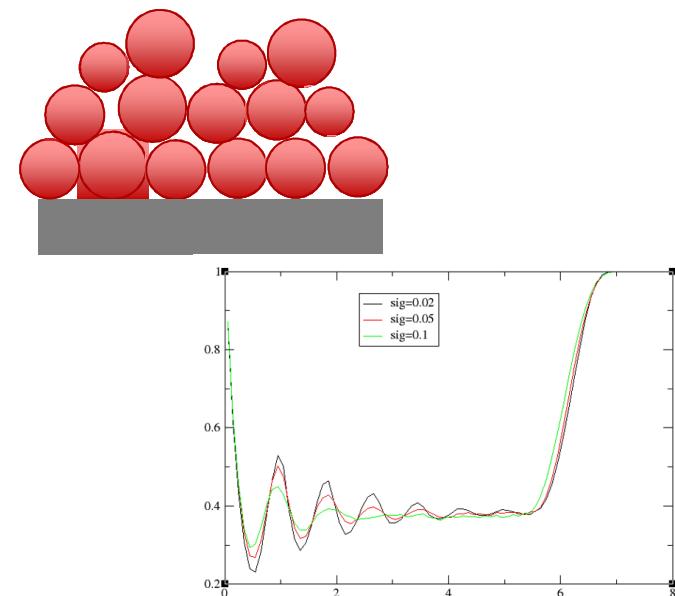
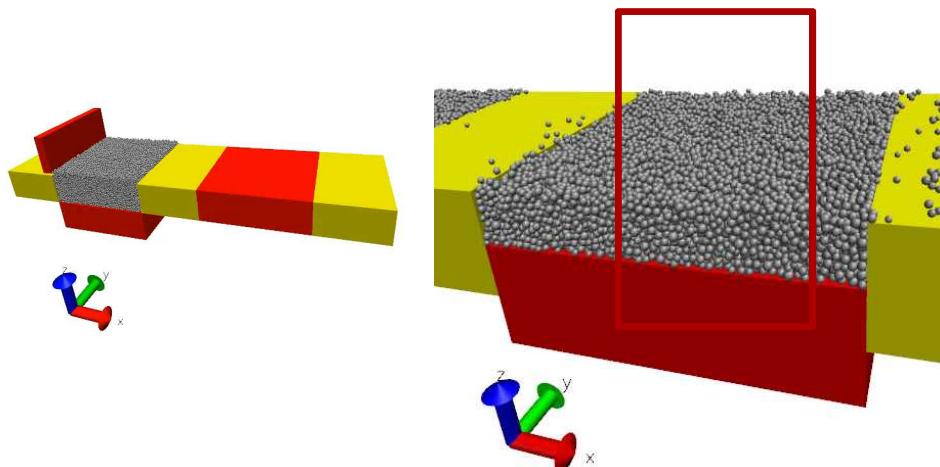


No particle-particle cohesion

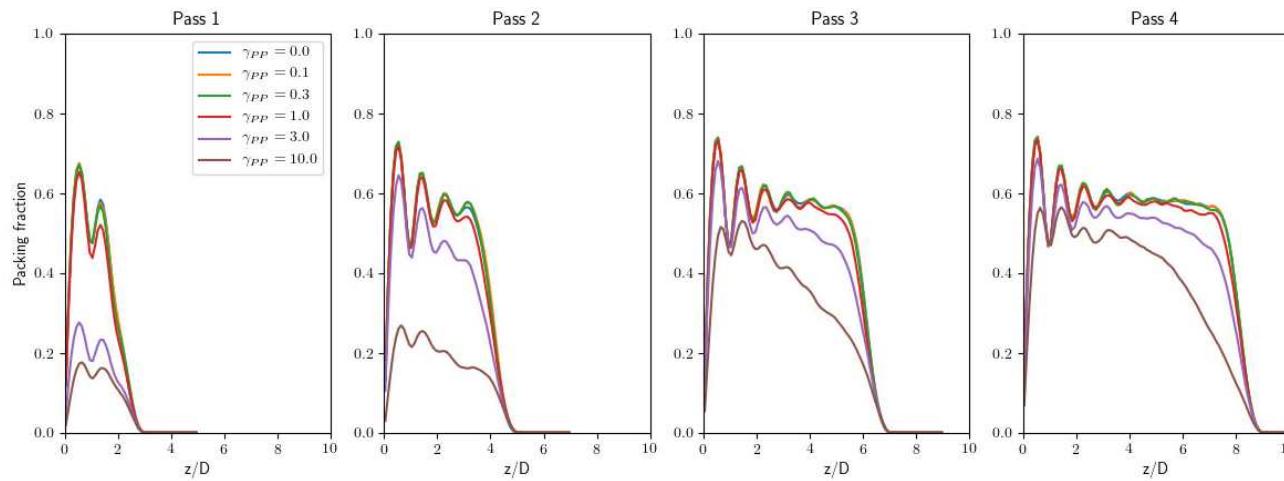


Very high particle-particle cohesion

Analysis of packed beds

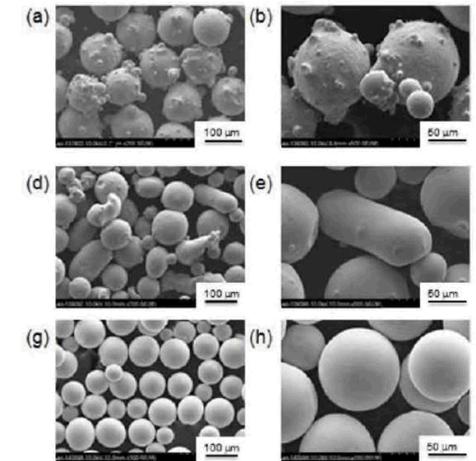
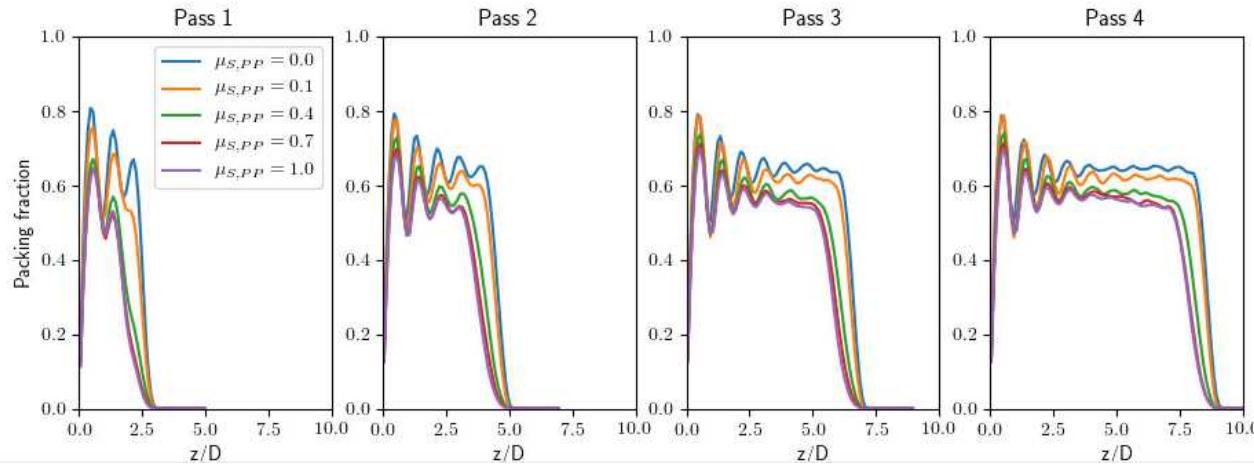


Effect of particle-particle cohesion γ_{PP} :



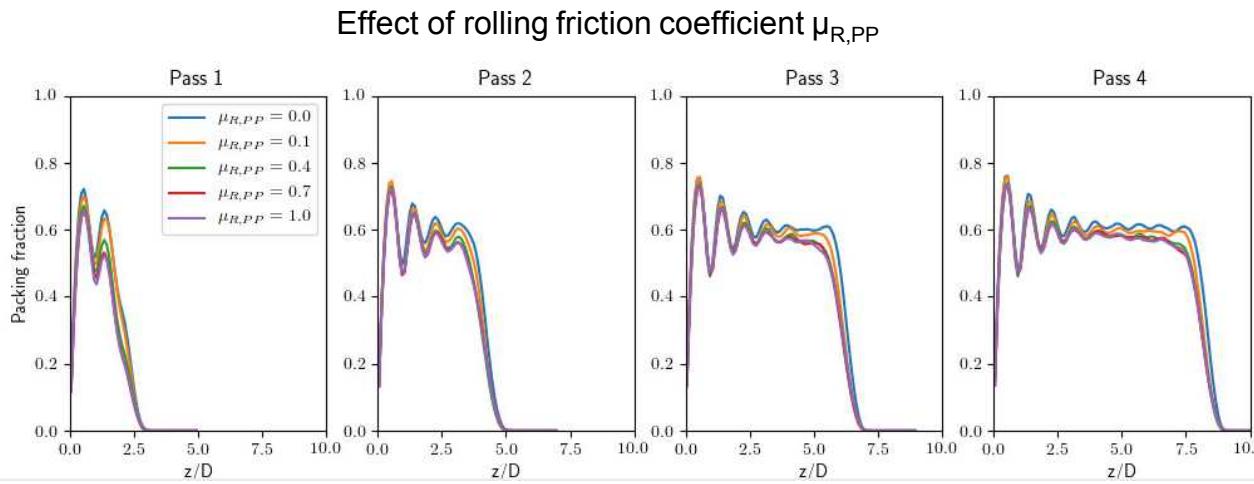
Analysis of packed beds

Effect of sliding friction coefficient $\mu_{S,PP}$

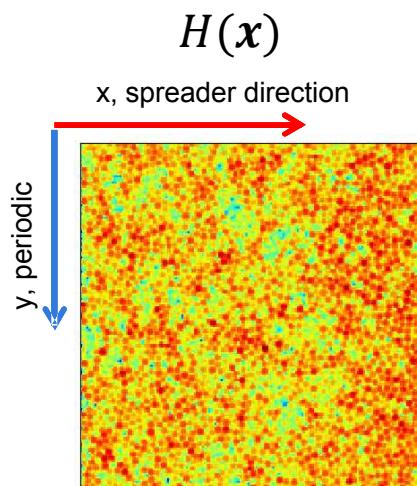
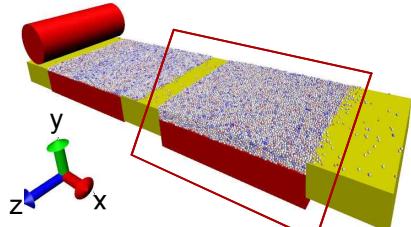


a/b: gas atomisation - d/e: rotary atomisation - g/h: Plasma rotating electrode process [1]

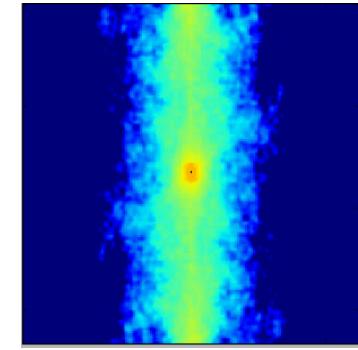
Strondl et al, *JoM* 2015.



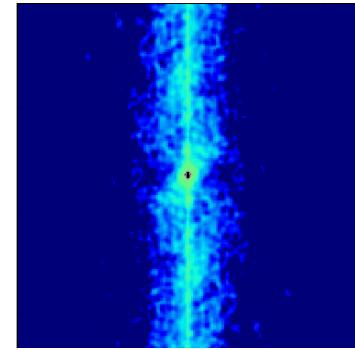
Analysis of powder bed surface



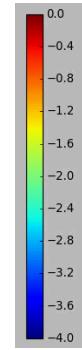
$$ACF(h(x)) = \langle h(x' + x)(h(x') \rangle$$
$$h(x) = (H(x) - \langle H(x) \rangle) / \sigma_{H(x)}$$



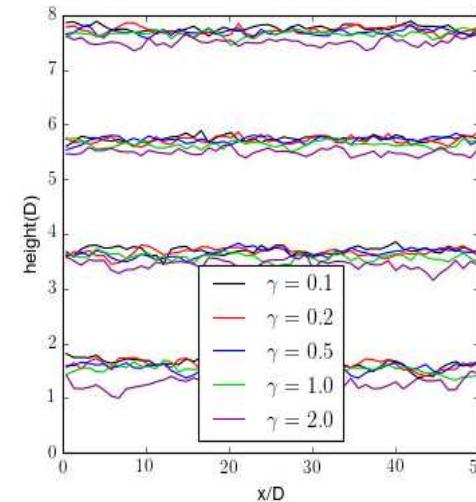
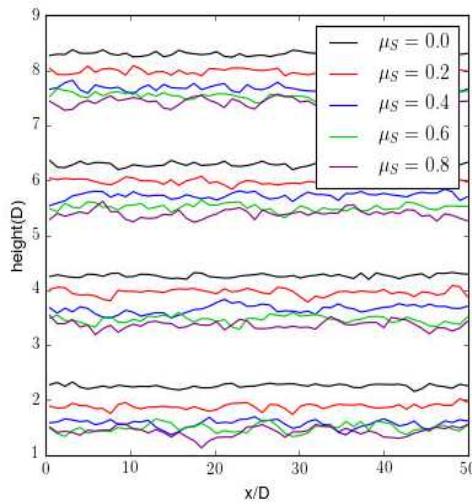
Slider, 4 passes



Roller, 4 passes

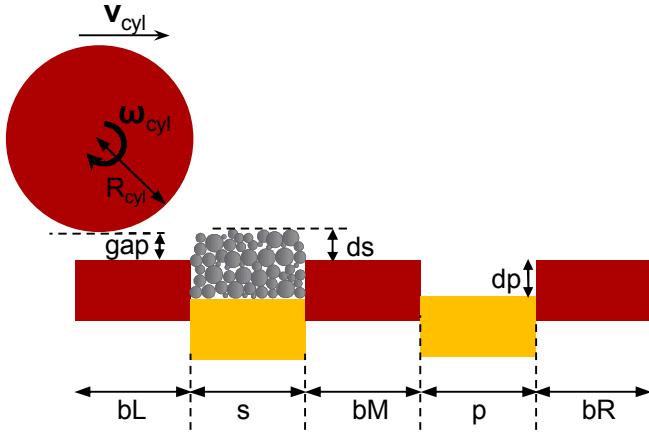


Height as a function of x:

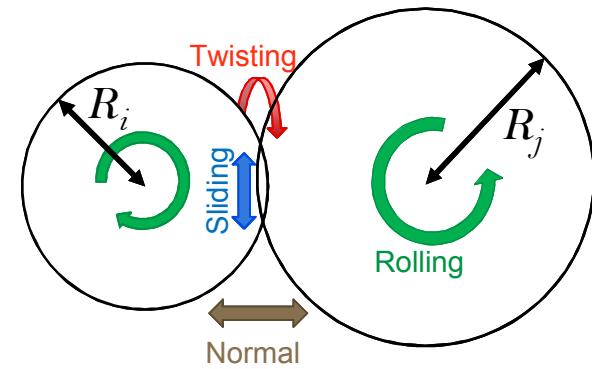


Large parameter space!

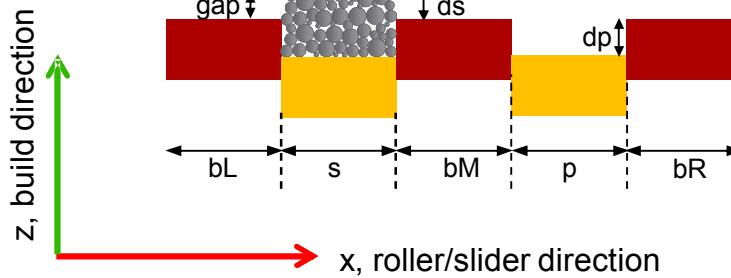
Process-related



Particle-related

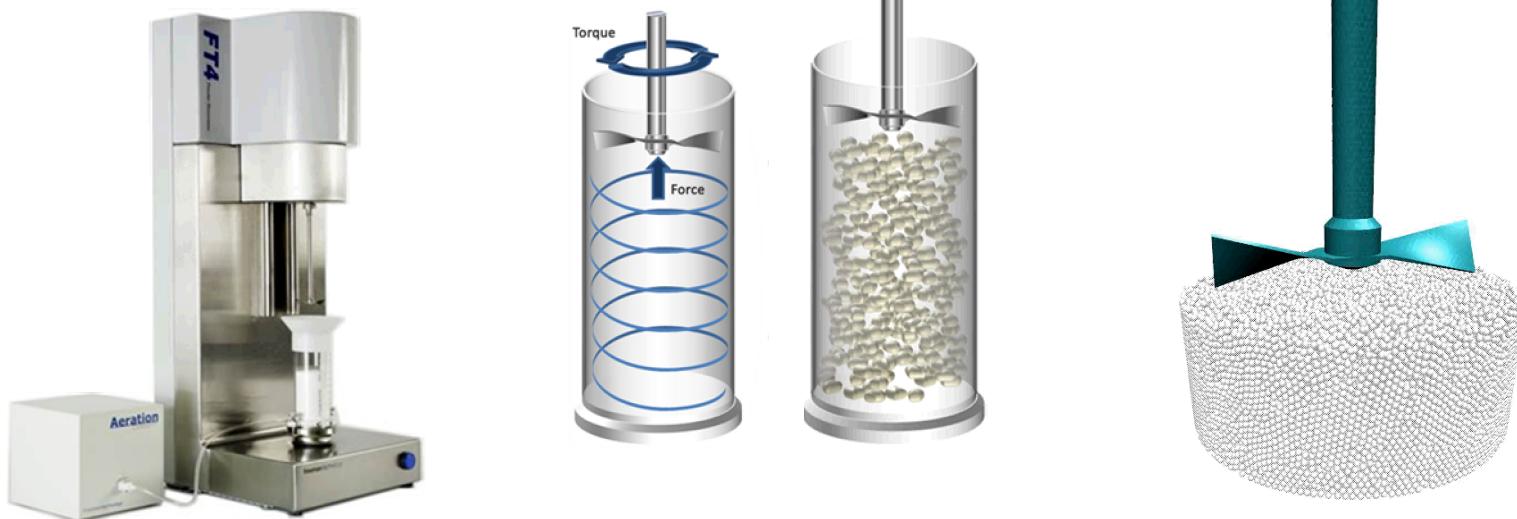


- **Particle size /shape distribution**
- **Contact parameters**
 - **Contact model form**
 - Stiffness, damping → actual values (e.g. $E_y=200$ GPa for steel) lead to prohibitively small time stepping, only need to be sufficiently high so that $\delta \ll R$
 - **Friction** (sliding, rolling, twisting) → relates to particle surface morphology
 - **Cohesion** → particle surface morphology, chemistry
 - Different for particle/particle, particle/wall contact



Toward model calibration

- Direct measurement of particle-scale parameters extremely difficult
- Goal: calibrate DEM parameters based on powder dynamics experiments
- One option: Freeman Technology FT4 rheometer: measure force/torque for various impeller motions



QUESTIONS?