

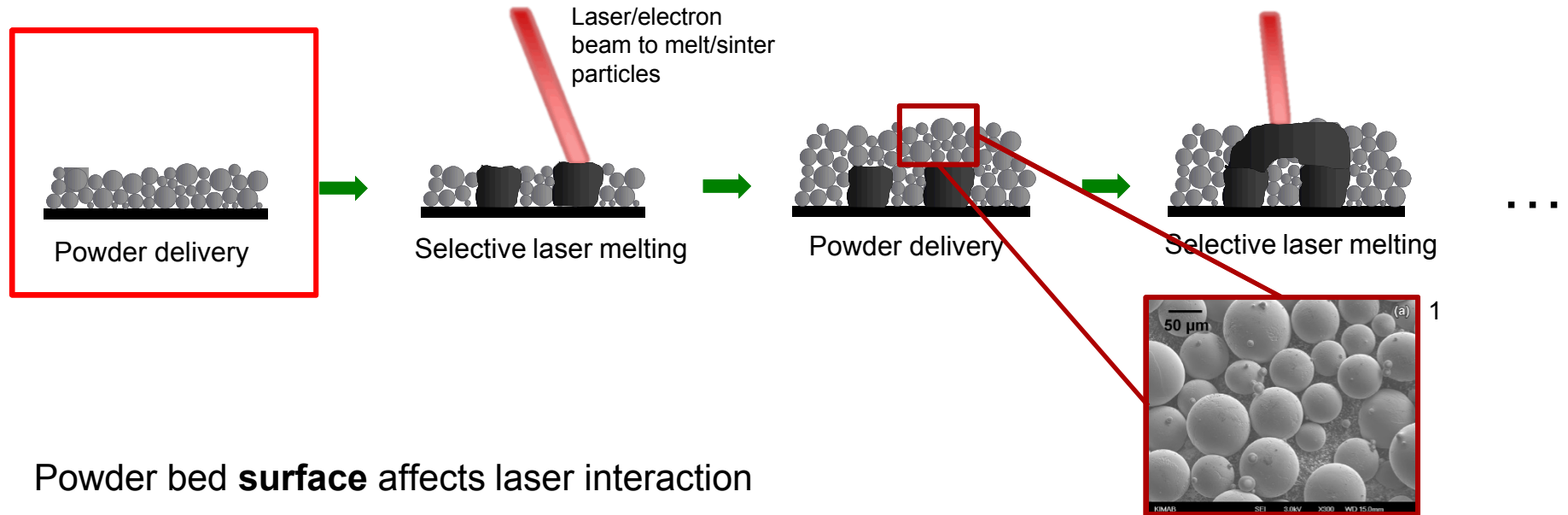
# Discrete element modeling of powder spreading and flow for metal additive manufacturing

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# Background and Motivation

## Layer-by-layer powder bed fusion processes (e.g. SLM/SLS):



- Powder bed **surface** affects laser interaction
- Powder bed **bulk packing** affects void formation, surface finish
- **Variability in powder properties** due to e.g. vendor supply, powder recycling
- Some key length scales:
  - Layer thickness  $\sim 30\text{-}100\ \mu\text{m}$
  - Laser spot size  $\sim 100\text{-}200\ \mu\text{m}$
  - Particle diameter  $\sim 10\text{-}100\ \mu\text{m}$
  - Material defects  $\sim 100\ \mu\text{m}$



Understanding powder at scale of individual particles is important!

# Simulation method:

## Discrete Element Method (DEM)

Layer thickness  $\sim$  particle diameter  
→ continuum models (e.g.  $\mu(I)$  rheology)  
inherently unsuitable

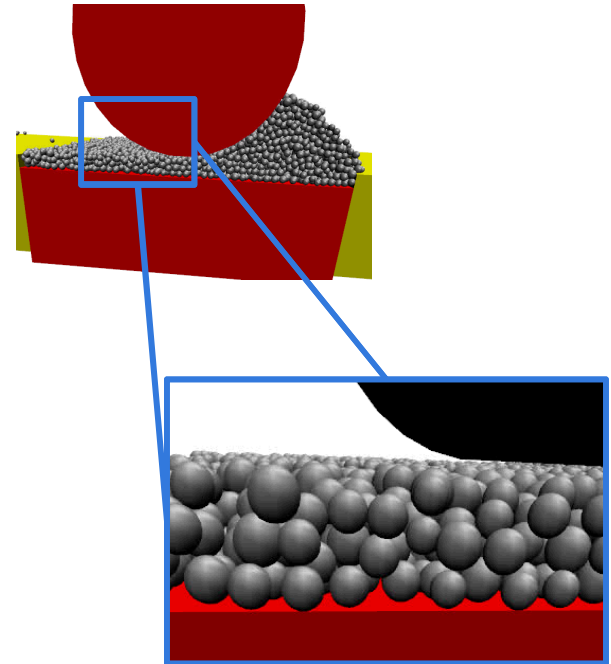
### Method of choice: DEM

#### Advantages:

- Captures individual particle dynamics
- Can handle polydispersity, shape variations, complex geometries
- Material properties captured by contact parameters

#### Disadvantages:

- Computationally expensive
- **Difficult to parametrize**



# Simulation method: Discrete Element Method (DEM)

Molecular dynamics-like method:

- Particles modeled explicitly (position, velocity, angular velocity)
- Integrate collective dynamics:

$$\mathbf{F}_i = m_i \frac{d^2 \mathbf{r}_i}{dt^2} \quad \boldsymbol{\tau}_i = I_i \frac{d^2 \mathbf{w}_i}{dt^2} \quad i = 1, \dots, N \quad N \approx 10^5 - 10^6$$

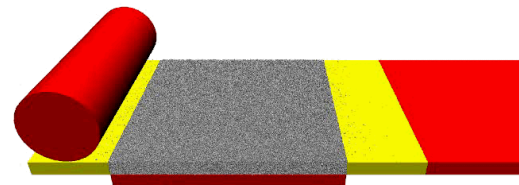
- Forces/torques computed at contact based on reduced order models

Well-established for 'large' particle applications (e.g. mining, pharmaceutical)



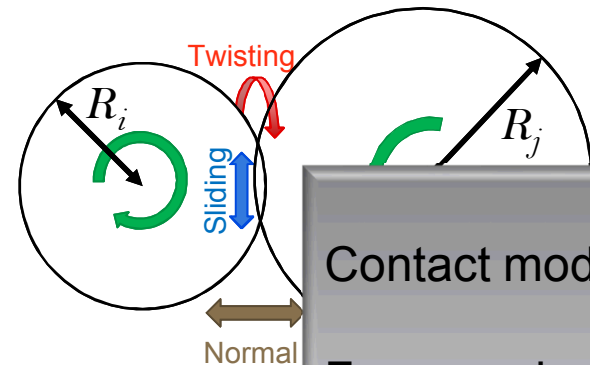
From EDEM youtube channel

Much more challenging for fine/cohesive powders!



<http://lammps.sandia.gov>

# Granular contact models



Geometry/kinematics

$\mathbf{r}_i, \mathbf{r}_j$  : positions  
 $\mathbf{v}_i, \mathbf{v}_j$  : translational velocities  
 $\boldsymbol{\Omega}_i, \boldsymbol{\Omega}_j$  : angular velocities  
 $a$  : area of contact\*

$$\delta = R_i + R_j - \|\mathbf{r}_i - \mathbf{r}_j\|$$

$$\mathbf{n} = (\mathbf{r}_i - \mathbf{r}_j) / \|\mathbf{r}_i - \mathbf{r}_j\|$$

$$R = \frac{1}{1/R_i + 1/R_j} = \frac{R_i R_j}{R_i + R_j}$$

$$\mathbf{v}_R = \mathbf{v}_i - \mathbf{v}_j$$

$$\mathbf{v}_t = \mathbf{v}_R - (\mathbf{v}_R \cdot \mathbf{n})\mathbf{n}$$

Relative sliding velocity:

$$\mathbf{v}_{tR} = \mathbf{v}_t - (R_i \boldsymbol{\Omega}_i + R_j \boldsymbol{\Omega}_j) \times \mathbf{n}$$

Relative twisting 'velocity':

$$\Omega_T = (\boldsymbol{\Omega}_i(\tau) - \boldsymbol{\Omega}_j(\tau)) \cdot \mathbf{n}$$

Relative rolling velocity:

$$\mathbf{v}_L = -R(\boldsymbol{\Omega}_i - \boldsymbol{\Omega}_j) \times \mathbf{n}$$

\* $a$  depends on contact model!

Contact models are complicated!

Focus on key physics and associated parameters:

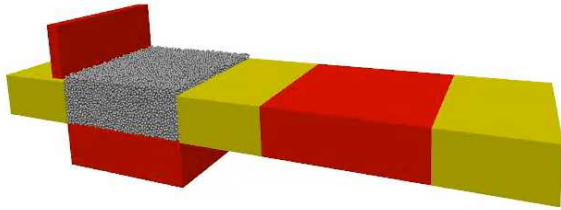
1. Cohesion  $\rightarrow$  relates to surface chemistry, morphology
2. Friction  $\rightarrow$  relates to surface morphology, micromechanics

Consider both particle/particle and particle/wall interactions

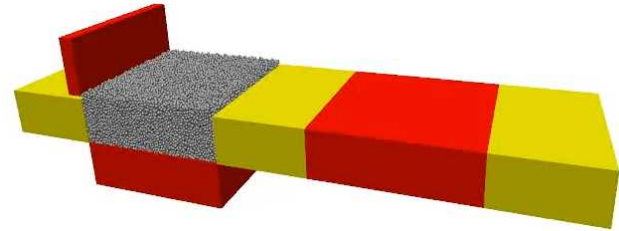
	gran/hertz	dmt/rolling	jkr/rolling
Normal elastic (spring)	$\mathbf{F}_n = k_n \sqrt{R} \delta^{3/2} \mathbf{n}$	$\mathbf{F}_n = \left( \frac{4Ea^3}{3R} - 4\pi\gamma R \right) \mathbf{n}$ $\delta_N = a^2/R$ $F_{\text{pulloff}} = -4\pi\gamma R$	$\mathbf{F}_n = \left( \frac{4Ea^3}{3R} - 2\pi a^2 \sqrt{\frac{4\gamma E}{\pi a}} \right) \mathbf{n}$ $\delta_N = a^2/R - 2\sqrt{\pi\gamma a/E}$ $F_{\text{pulloff}} = -3\pi\gamma R$
Normal dissipative			$\mathbf{v}_R \cdot \mathbf{n}$ or $\eta_N$ based on Tsuji or by
			$-k_S \int_{t_0}^t \mathbf{v}_{tR}(\tau) d\tau$
			$\eta_T \mathbf{v}_{tR}$
			$\ \mathbf{F}_R\  \leq F_{S,\text{crit}}$
			$= \mu_S(\ \mathbf{F}_n\  + F_{\text{pulloff}})$
			$-k_R \int_{t_0}^t \mathbf{v}_L(\tau) d\tau$
			$\mathbf{v}_L$
		$\ \mathbf{F}_R\  \leq F_{R,\text{crit}}$ $F_{R,\text{crit}} = \mu_R \ \mathbf{F}_n\ $	$\ \mathbf{F}_R\  \leq F_{R,\text{crit}}$
Twisting elastic <sup>3</sup>		$M_t = -k_Q \int_{t_0}^t \Omega_T(\tau) d\tau$	$M_t = -k_Q \int_{t_0}^t \Omega_T(\tau) d\tau$
Twisting dissipative		$-\eta_Q \Omega_T$	$-\eta_Q \Omega_T$
Twisting frictional		$M_t \leq -M_{t,\text{crit}} \Omega_T / \ \Omega_T\ $ $M_{t,\text{crit}} = \frac{2}{3} a F_{S,\text{crit}}$	$M_t \leq -M_{t,\text{crit}} \Omega_T / \ \Omega_T\ $ $M_{t,\text{crit}} = \frac{2}{3} a F_{S,\text{crit}}$

1,2,3: Integrals must be carried out to remove effects of rigid body rotation/twisting of contacting pair  
 2:  $\mathbf{F}_R$  is a 'pseudo-force', resulting only in torque  $\mathbf{R} \mathbf{n} \times \mathbf{F}_R$

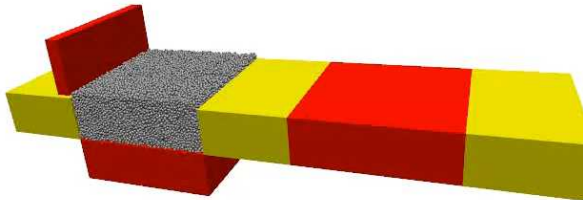
# Granular contact models



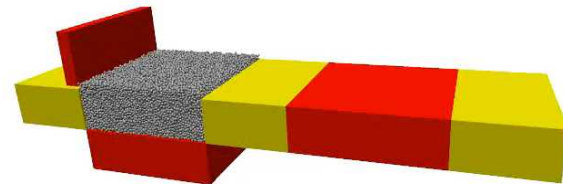
No rolling friction



No sliding friction

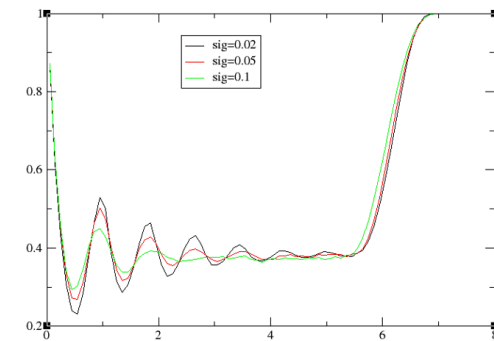
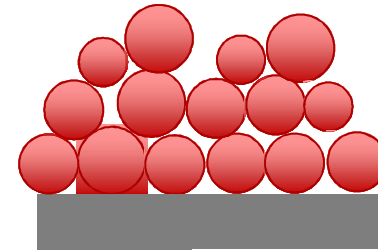
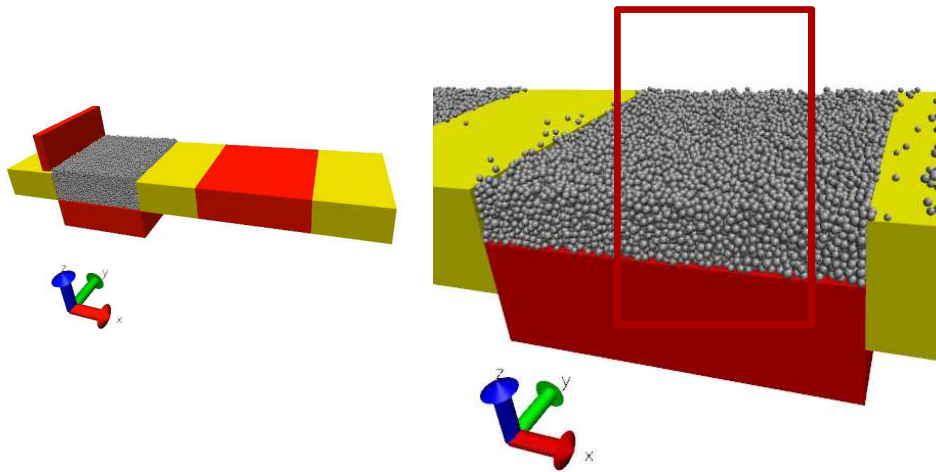


No particle-particle cohesion

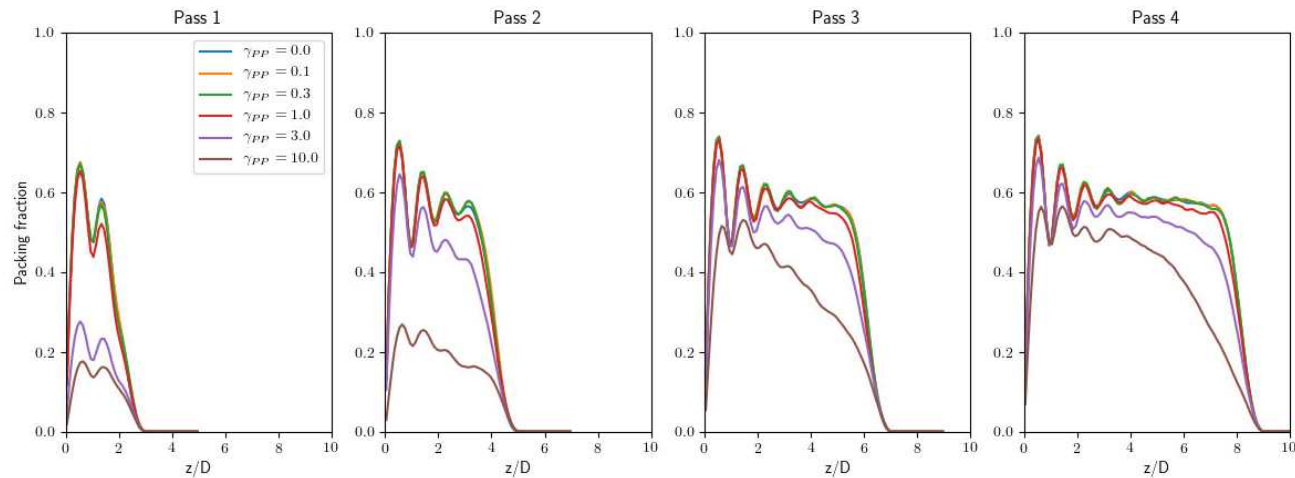


Very high particle-particle cohesion

# Analysis of packed beds

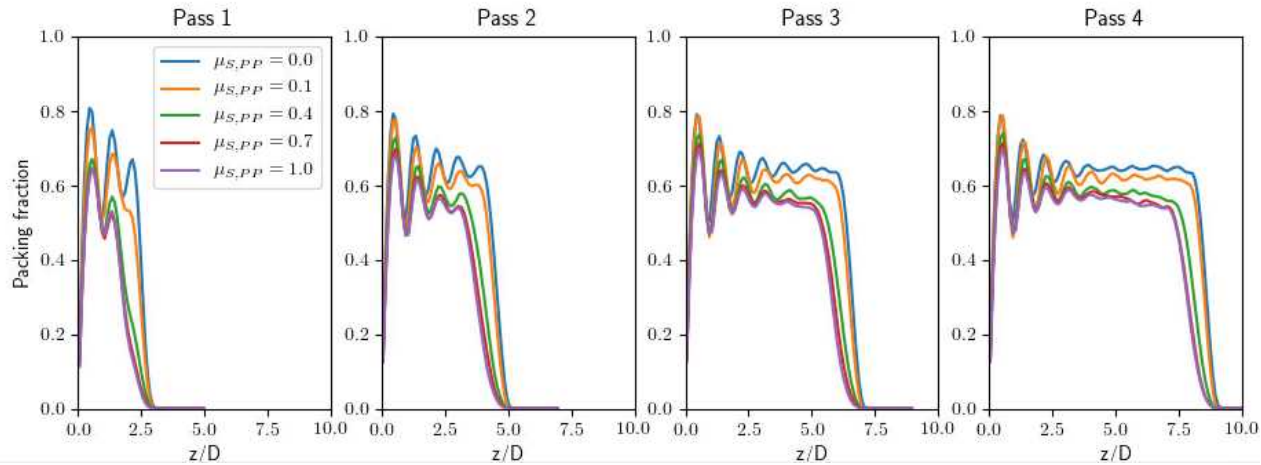


Effect of particle-particle cohesion  $\gamma_{PP}$ :

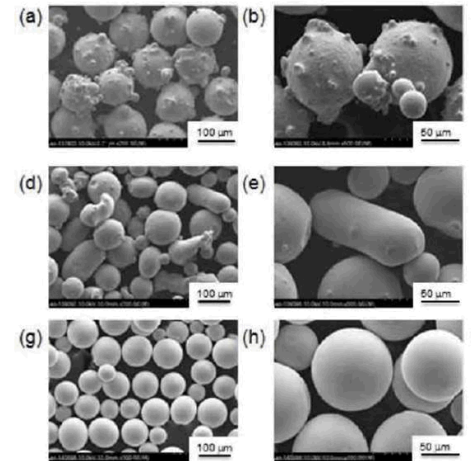
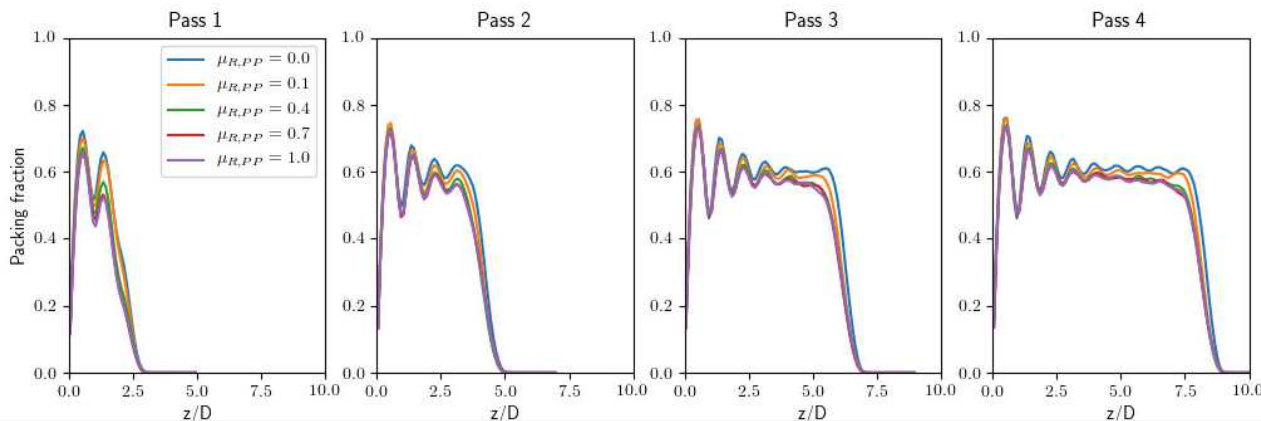


# Analysis of packed beds

Effect of sliding friction coefficient  $\mu_{S,PP}$



Effect of rolling friction coefficient  $\mu_{R,PP}$

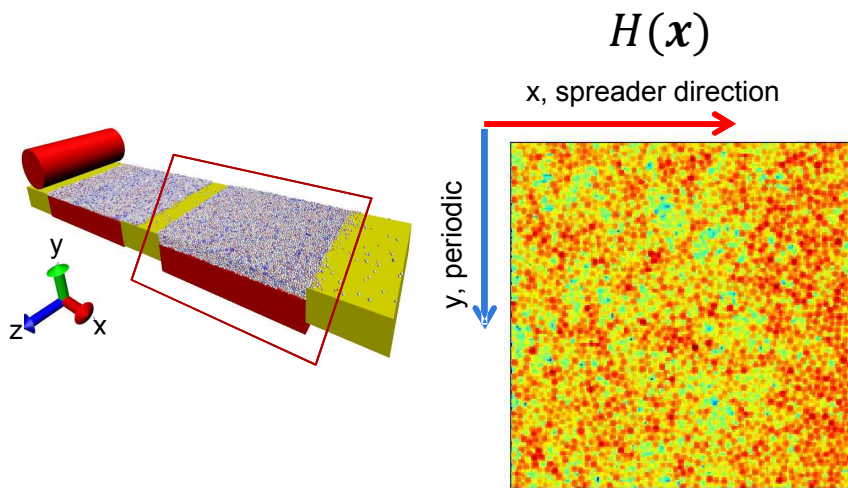


a/b: gas atomisation - d/e: rotary atomisation - g/h: Plasma rotating electrode process [1]

Strondl et al, *JoM* 2015.

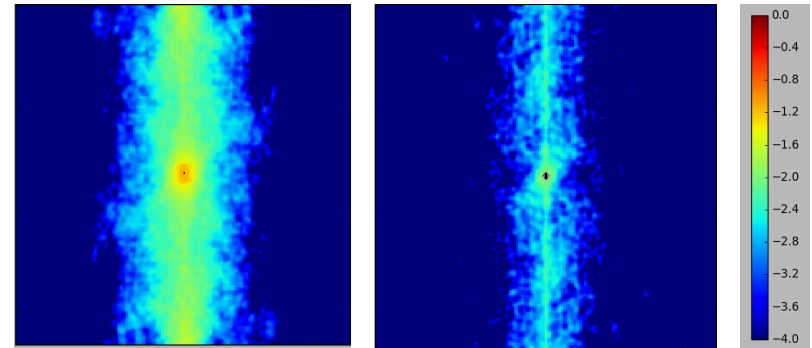


# Analysis of powder bed surface



$$ACF(h(x)) = \langle h(x' + x)(h(x')) \rangle$$

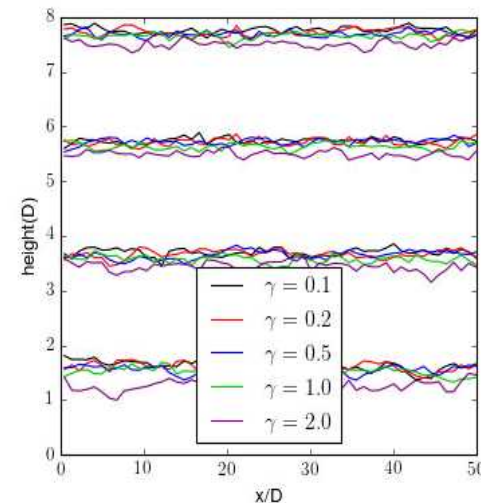
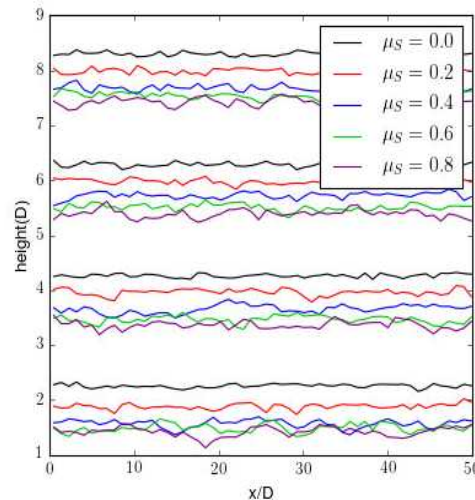
$$h(x) = (H(x) - \langle H(x) \rangle) / \sigma_{H(x)}$$



Slider, 4 passes

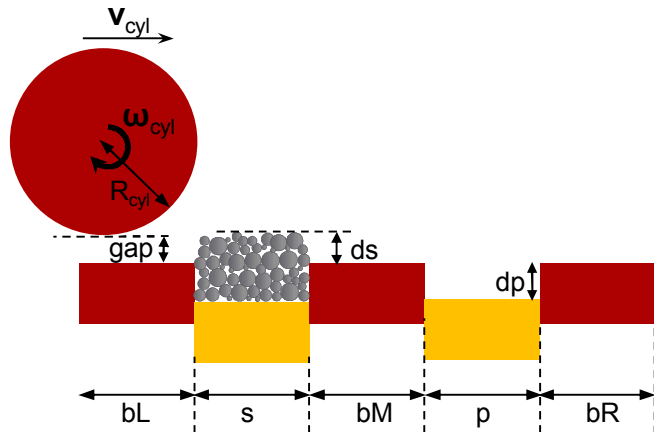
Roller, 4 passes

Height as a function of x:

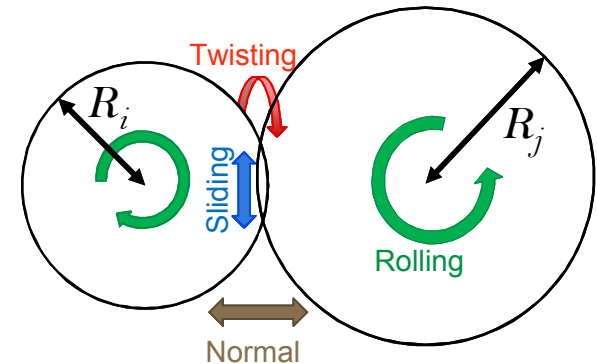


# Large parameter space!

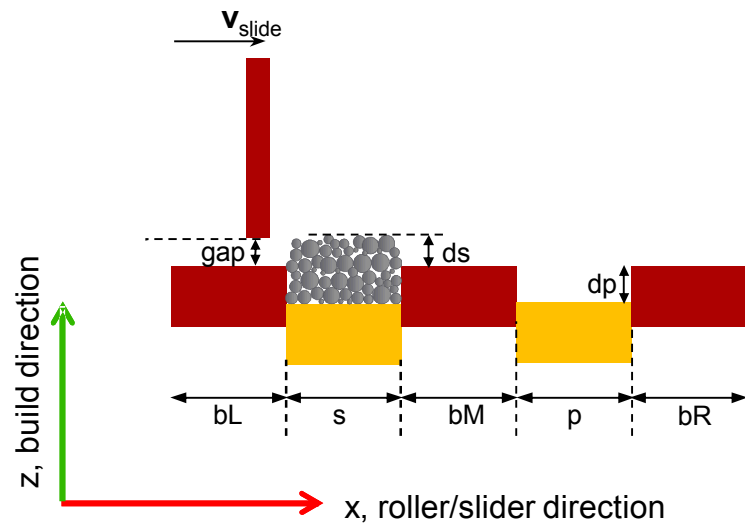
Process-related



Particle-related

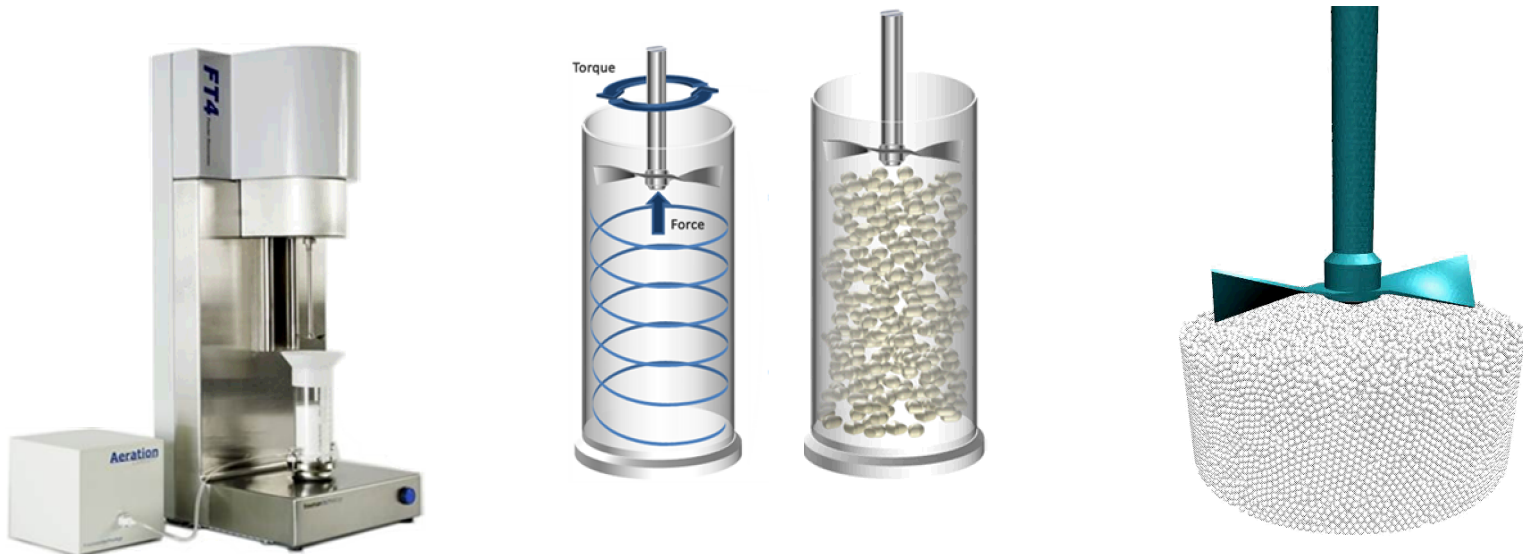


- **Particle size /shape distribution**
- **Contact parameters**
  - **Contact model form**
  - Stiffness, damping  $\rightarrow$  actual values (e.g.  $E_Y=200$  GPa for steel) lead to prohibitively small time stepping, only need to be sufficiently high so that  $\delta \ll R$
  - **Friction** (sliding, rolling, twisting)  $\rightarrow$  relates to particle surface morphology
  - **Cohesion**  $\rightarrow$  particle surface morphology, chemistry
  - Different for particle/particle, particle/wall contact



# Toward model calibration

- Direct measurement of particle-scale parameters extremely difficult
- Goal: calibrate DEM parameters based on powder dynamics experiments
- One option: Freeman Technology FT4 rheometer: measure force/torque for various impeller motions



# QUESTIONS?