



Battery and Time

Leung, Soto, Hankins, Balbuena, Harrison, J. Phys. Chem. C (2016)
Leung & Jungjohann (2017)

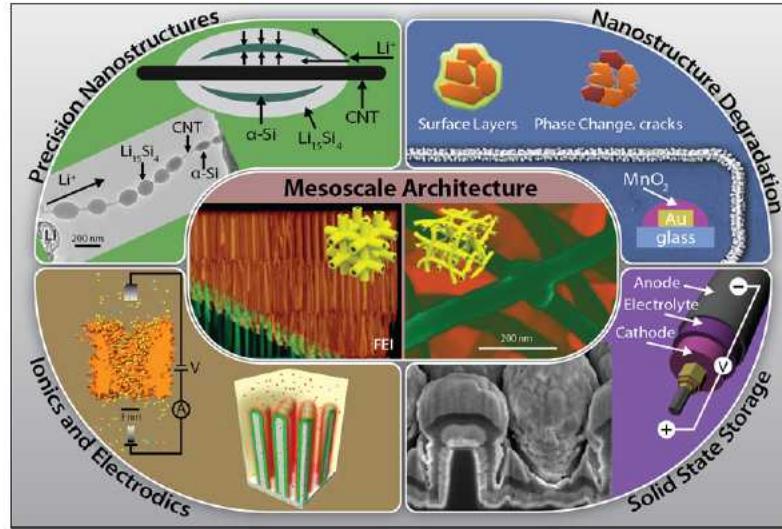
This work was supported by the Assistant Secretary for Energy Efficiency and Renewable Energy, Office of Vehicle Technologies of the U.S. Department of Energy under Contract No. DE-AC02-05CH11231, Subcontract No. 7060634 under the Advanced Batteries Materials Research (BMR) Program.



Nanostructures for Electrical Energy Storage A DOE Energy Frontier Research Center

NEES major research areas

- Nanostructure Interface Science
- Mesoscale Architectures & Ionics
- Nanostructure Degradation Science
- Solid State Energy Storage



This work was supported as part of the Nanostructures for Electrical Energy Storage (NEES), an Energy Frontier Research Center funded by the U.S. Department of Energy, Office of Science.



U.S. DEPARTMENT OF
ENERGY

Office of
Science

NEES III
NANOSTRUCTURES for ELECTRICAL ENERGY STORAGE

Existential Challenges in Energy, Climate Change



Battery UND ZEIT

VON

MARTIN HEIDEGGER



MAX NIEMEYER VERLAG TÜBINGEN

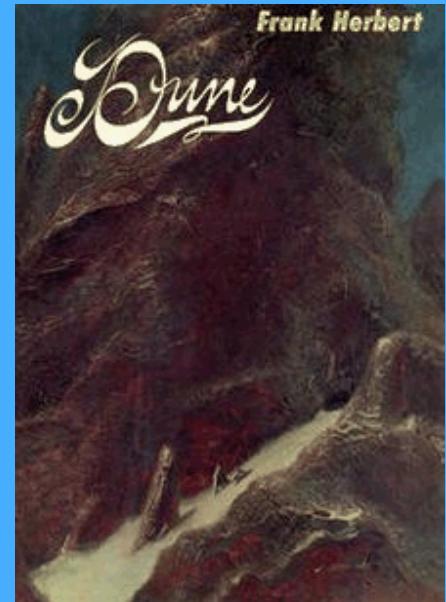
- Battery cycle life, charge transfer rate are *time-dependent*
- So are many elements in battery studies not often acknowledged as such
- Time could be a unifying theme in battery studies

(In this funding climate, hope we are not left with ->



Jean-Paul Sartre
Battery and
Nothingness
The principal text of modern existentialism

Heidegger in popular (& less popular) culture



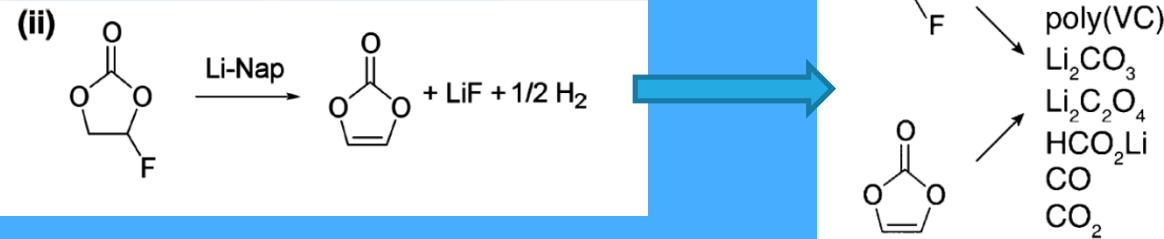
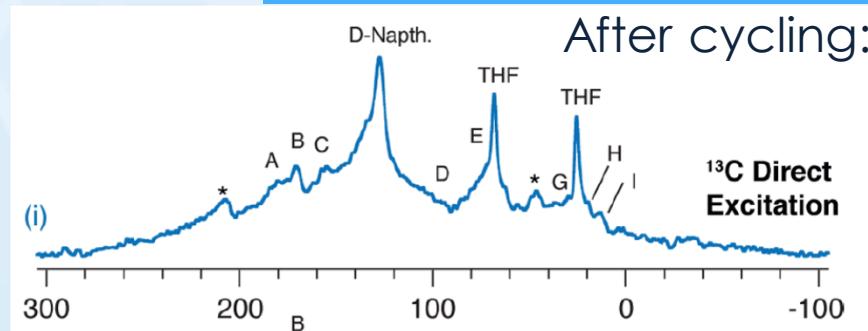
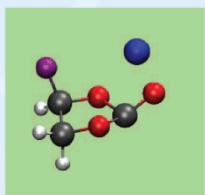
e.g., SEI formation mechanism assigned without regard to time



Fluoroethylene Carbonate and Vinylene Carbonate Reduction: Understanding Lithium-Ion Battery Electrolyte Additives and Solid Electrolyte Interphase Formation

Alison L. Michan,[†] Bharathy. S. Parimalam,[‡] Michal Leskes,[†] Rachel N. Kerber,[†] Taeho Yoon,[‡] Clare P. Grey,[†] and Brett L. Lucht*,[‡]

FEC is a popular electrolyte additive makes better SEI

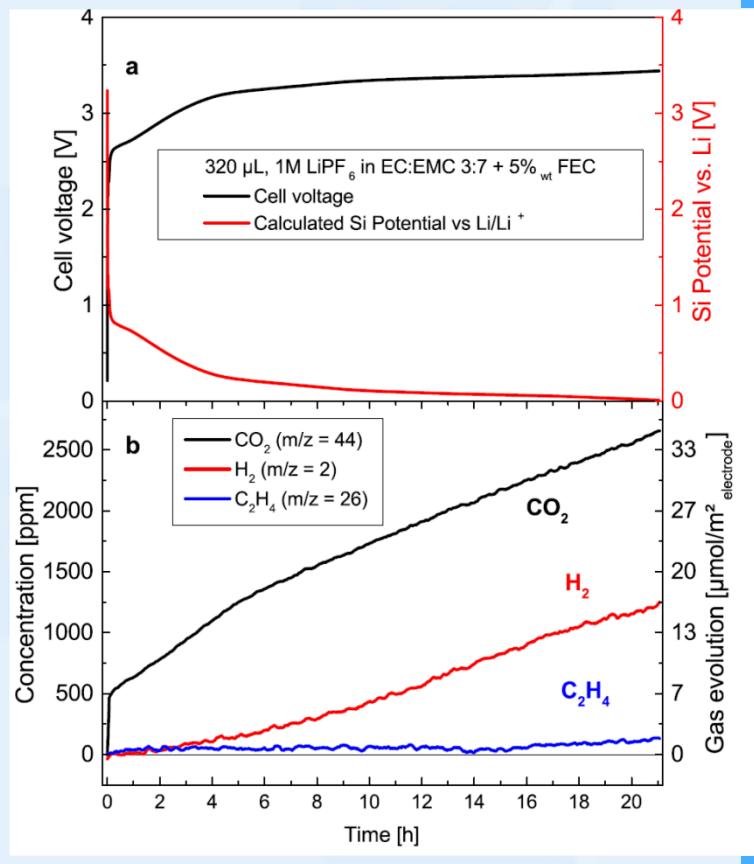


Accounting for time: this mechanism is untenable

Consumption of Fluoroethylene Carbonate (FEC) on Si-C Composite Electrodes for Li-Ion Batteries

Roland Jung,^{a,b,*} Michael Metzger,^{a,*} Dominik Haering,^{a,*} Sophie Solchenbach,^{a,*} Cyril Marino,^{a,c} Nikolaos Tsiovaras,^b Christoph Stinner,^b and Hubert A. Gasteiger^{a,**}

Journal of The Electrochemical Society, 163 (8) A1705-A1716 (2016)



H₂ gas release – 1 hour

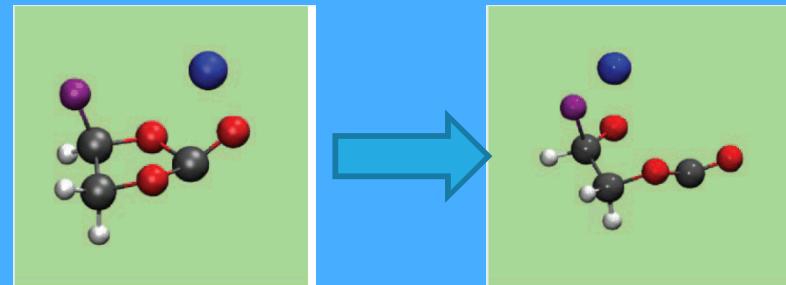
Journal of The Electrochemical Society, 161 (3) A213-A221 (2014)
0013-4651/2014/161(3)/A213/9/\$31.00 © The Electrochemical Society

Modeling Electrochemical Decomposition of Fluoroethylene Carbonate on Silicon Anode Surfaces in Lithium Ion Batteries

Kevin Leung,^{a,*} Susan B. Rempe,^a Michael E. Foster,^a Yuguang Ma,^b Julibeth M. Martinez del la Hoz,^b Na Sai,^c and Perla B. Balbuena^{b,*}

ring opening pre-empts H₂ release

10¹⁰ times faster



ring opening – $\tau \sim 15$ ns

$$1/\tau = \text{rate} = 10^{12} \exp(-\Delta G^*/kT) \text{ (s)}$$

$\Delta G^* \sim \Delta E^* \sim <1 \text{ eV}$
< 1 hour reaction time
“within battery timescale”



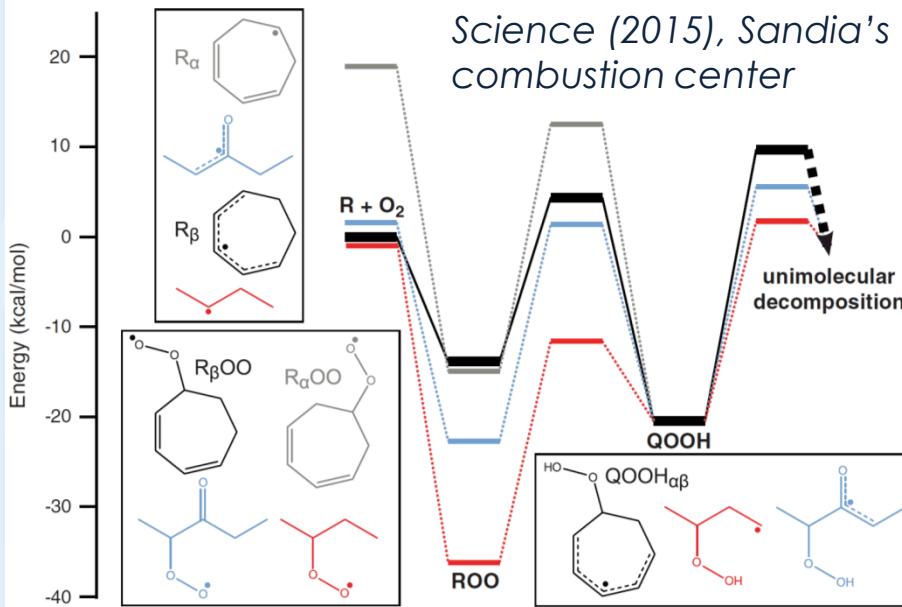
- So, in situ measurement = good
- But experimental platform can seldom span 10^{10} time scales
- Computation really economical at yield reaction time scales



- Screamingly obvious?
- Other scientific communities apply this

Direct observation and kinetics of a hydroperoxyalkyl radical (QOOH)

John D. Savee,* Ewa Papajak,* Brandon Rotavera, Haifeng Huang, Arkke J. Eskola, Oliver Welz,† Leonid Sheps, Craig A. Taatjes, Judit Zádor, David L. Osborn‡



- ... but battery modeling of ΔG^* rare

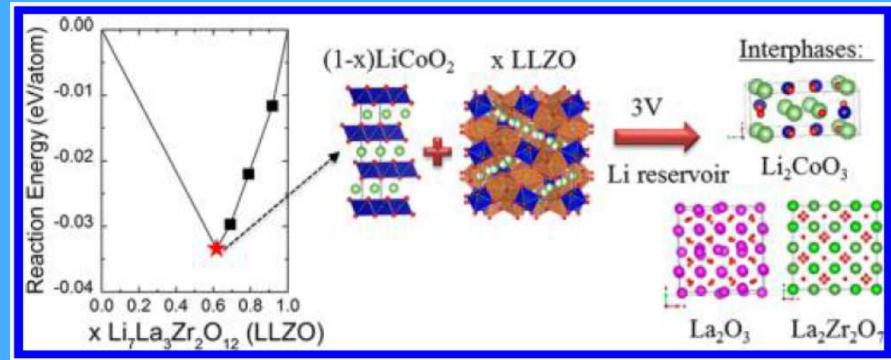
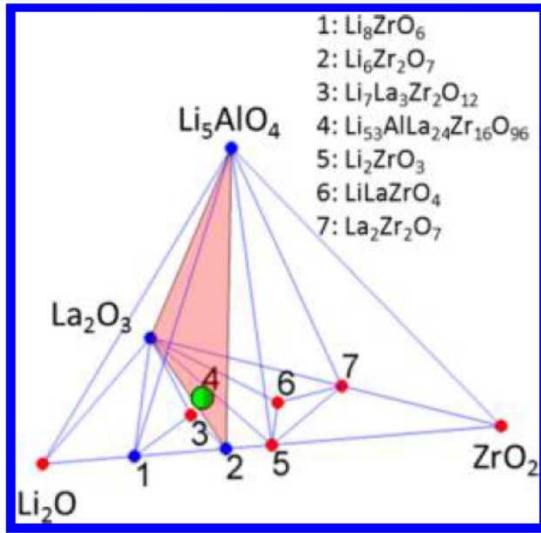


Traditionally battery modeling focuses on materials synthesis

Ceder and coworkers – “materials project, materials genome”

First-Principles Studies on Cation Dopants and Electrolyte/Cathode Interphases for Lithium Garnets *Chem. Mater.* 2015, 27, 4040–4047

Lincoln J. Miara,^{*,†} William Davidson Richards,[‡] Yan E. Wang,[‡] and Gerbrand Ceder[‡]



Focus is on phase diagrams
(exceptions: Li⁺ transport, dumbbell defects)

“When tradition thus becomes master, it does so in such a way that what it transmits is made so inaccessible, ... it blocks our access to those primordial ‘sources’ from which the categories and concepts handed down to us have been in part quite genuinely drawn. Indeed it makes us forget that they have had such an origin, and makes us suppose that the necessity of going back to these sources is something which we need not even understand.”

Heidegger, Being and Time (goodread.com)

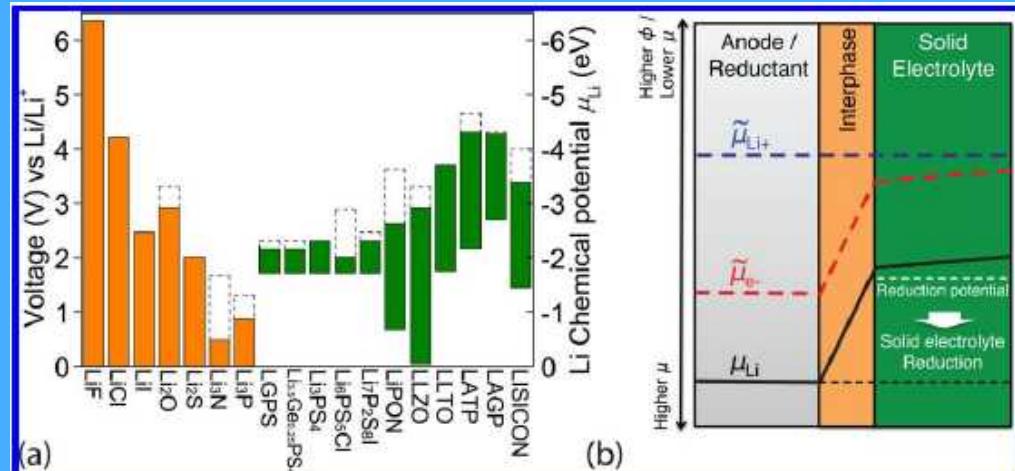
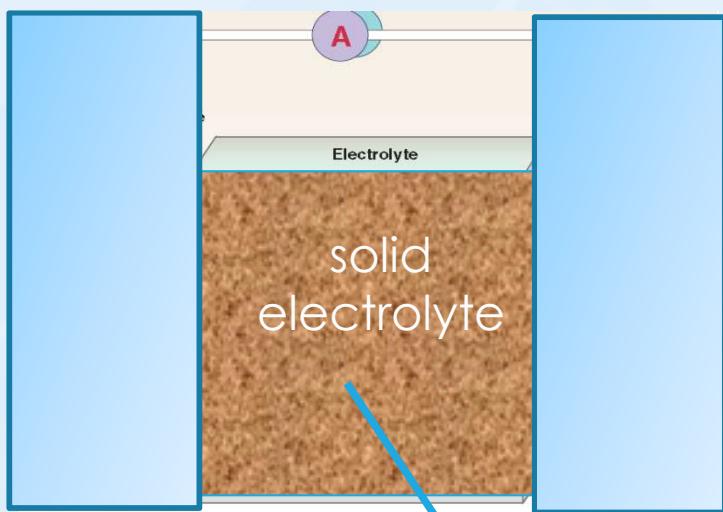


Solid state electrolytes: single phase thermodynamics

Origin of Outstanding Stability in the Lithium Solid Electrolyte Materials: Insights from Thermodynamic Analyses Based on First-Principles Calculations

Yizhou Zhu,[†] Xingfeng He,[†] and Yifei Mo^{*,†,‡}

DOI: 10.1021/acsami.9b07517
ACS Appl. Mater. Interfaces 2019, 11, 23685–23693



decompose into other phase?

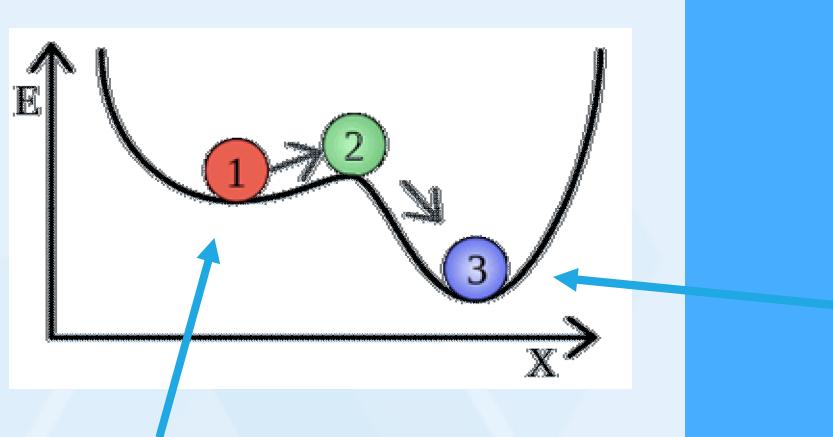
- solid electrolyte stability in all solid state batteries, solid using bulk thermodynamics
- no need to look at explicit interface?
- reasonable because solid interfaces often annealed at high temperature



Reason: materials synthesis occurs at high temperature

(figure by Georg Wiora)

e.g., 900 °C for 10 hours



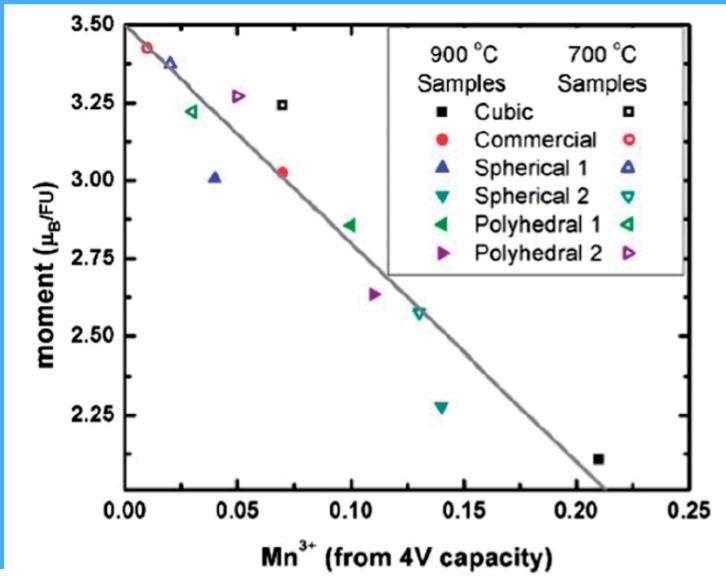
- $1/\tau = \text{rate} = 10^{12} \exp(-\Delta G^*/kT) / \text{s}$
- If $T = 900 \text{ }^\circ\text{C}$, 1 hour $\leftrightarrow \Delta G^* \sim 4 \text{ eV}$
- Most reactions have barriers $\ll 4 \text{ eV}$
- Reaches most stable phase, thermodynamics rules
- Time does not exist

- But even for synthesis, metastability is useful
- Anneal at 700 rather than 900 °C, improves materials

A perspective on the high-voltage $\text{LiMn}_{1.5}\text{Ni}_{0.5}\text{O}_4$ spinel cathode for lithium-ion batteries

Arumugam Manthiram,* Katharine Chemelewski and Eun-Sung Lee

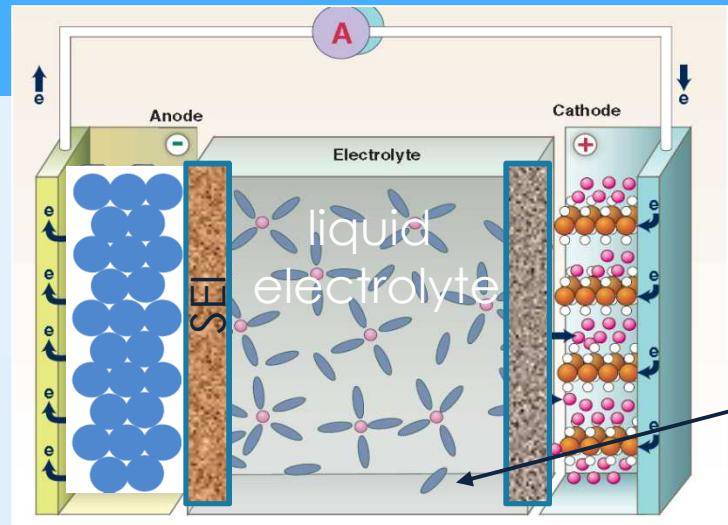
Energy Environ. Sci., 2014, 7, 1339–1350



Interface (SEI passivating films) governed by kinetics

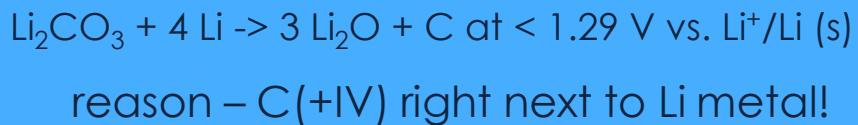
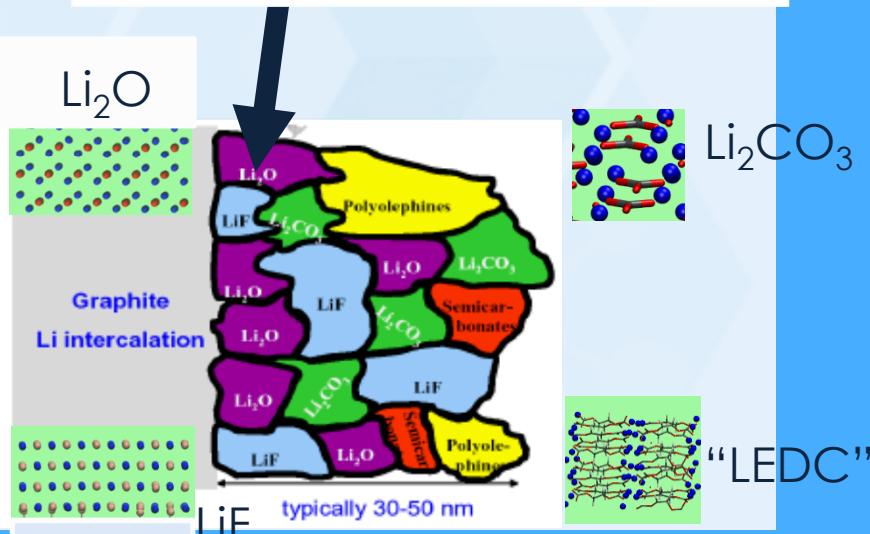


inspired by Ceder et al.'s work, did similar calculations for SEI components



Stability of Solid Electrolyte Interphase Components on Lithium Metal and Reactive Anode Material Surfaces
Kevin Leung,^{*,†} Fernando Soto,[‡] Kie Hankins,[‡] Perla B. Balbuena,[‡] and Katharine L. Harrison[†]

- SEI components thermodynamically unstable, except Li_2O and LiF
- Nevertheless, they are found in expt.
- Thermodynamics fail for SEI films



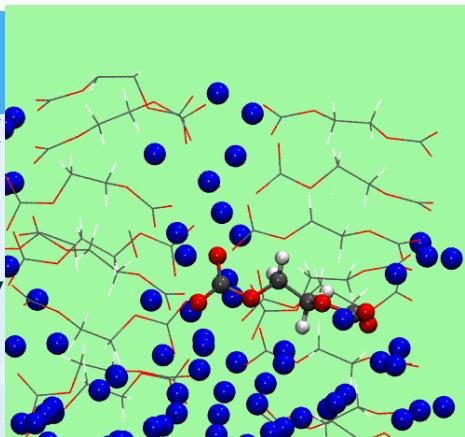
Hypothesis: instability can manifest itself on reactive anode surfaces

LEDC kinetically unstable at Li (100), a-Si interfaces

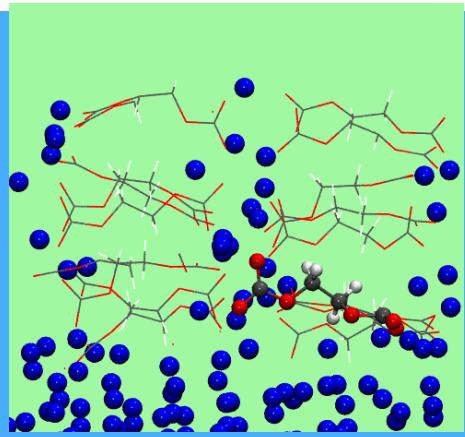


3-layer LEDC
on Li

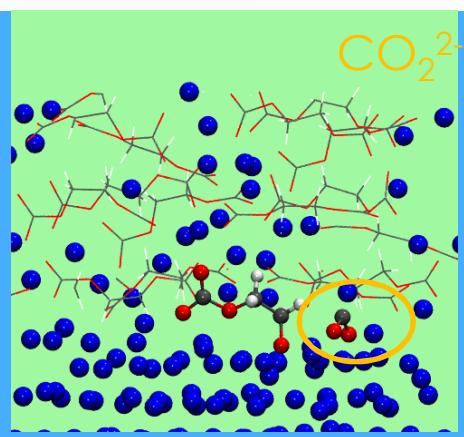
$V_e \sim -0.21$ V
vs. $\text{Li}^+/\text{Li}(s)$



$$\Delta E = 0.00 \text{ eV}$$



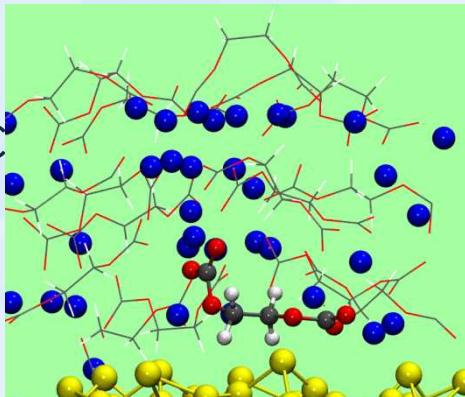
$$\Delta E^* = 0.27 \text{ eV}$$



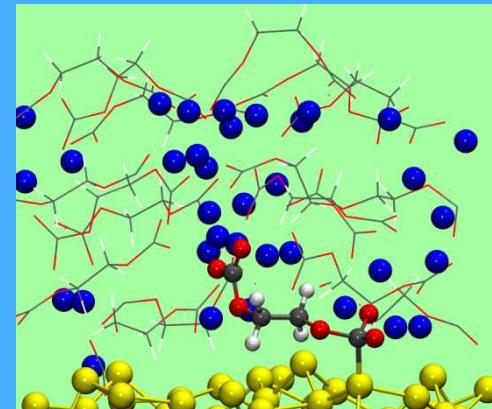
$$\Delta E = -2.10 \text{ eV}$$

3-layer LEDC
on a-Si

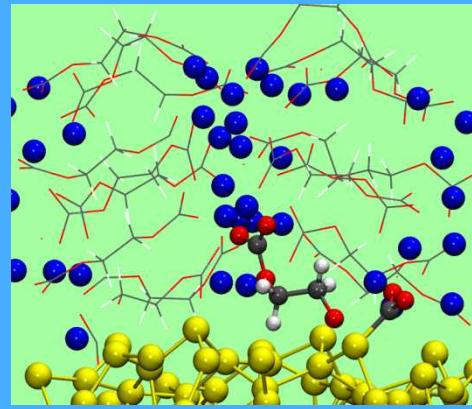
V_e not well
defined



$$\Delta E = 0.00 \text{ eV}$$



$$\Delta E^* = 0.77 \text{ eV}$$



$$\Delta E = -0.18 \text{ eV}$$

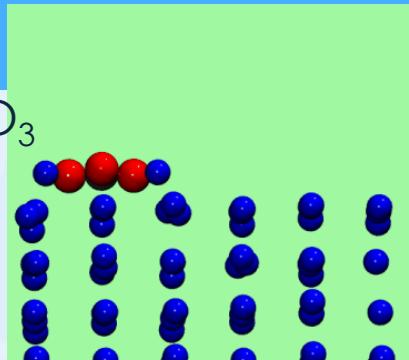
Li_2CO_3 unstable on Li (100) surface, barrier marginal



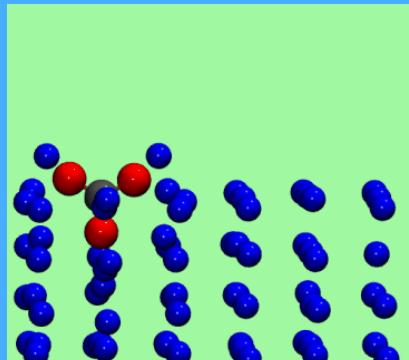
- unstable if reaction exothermic and barrier ≤ 1 eV (< 10 hour reaction time)

single Li_2CO_3

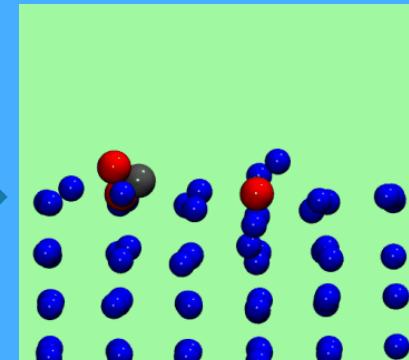
$V_e \sim 1.56$ V
vs. $\text{Li}^+/\text{Li}(s)$



$\Delta E = 0.00$ eV



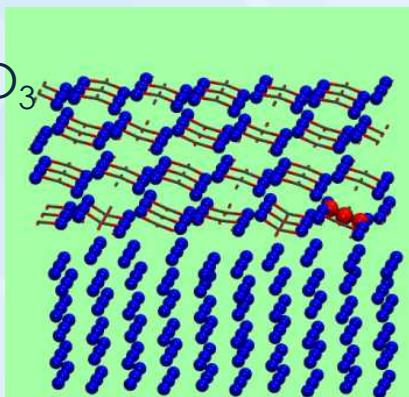
$\Delta E^* = 1.01$ eV



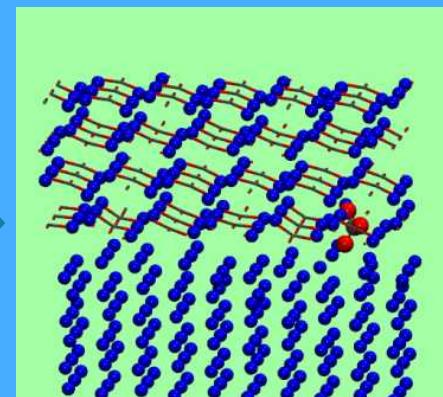
$\Delta E = -0.64$ eV

4-layer Li_2CO_3

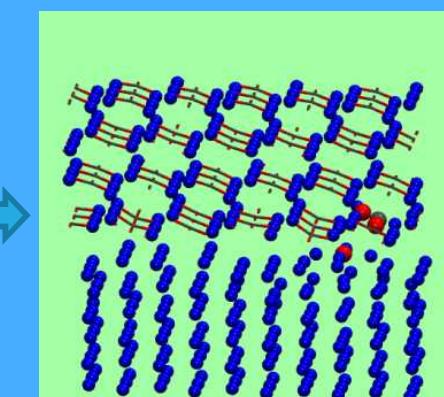
$V_e \sim 0.61$ V
vs. $\text{Li}^+/\text{Li}(s)$



$\Delta E = 0.00$ eV

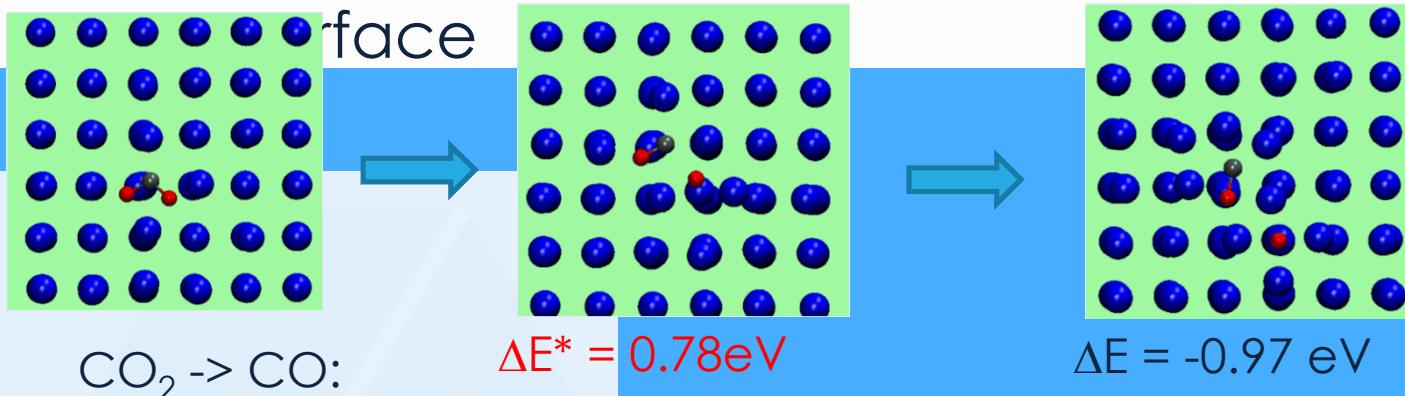


$\Delta E^* = 0.97$ eV



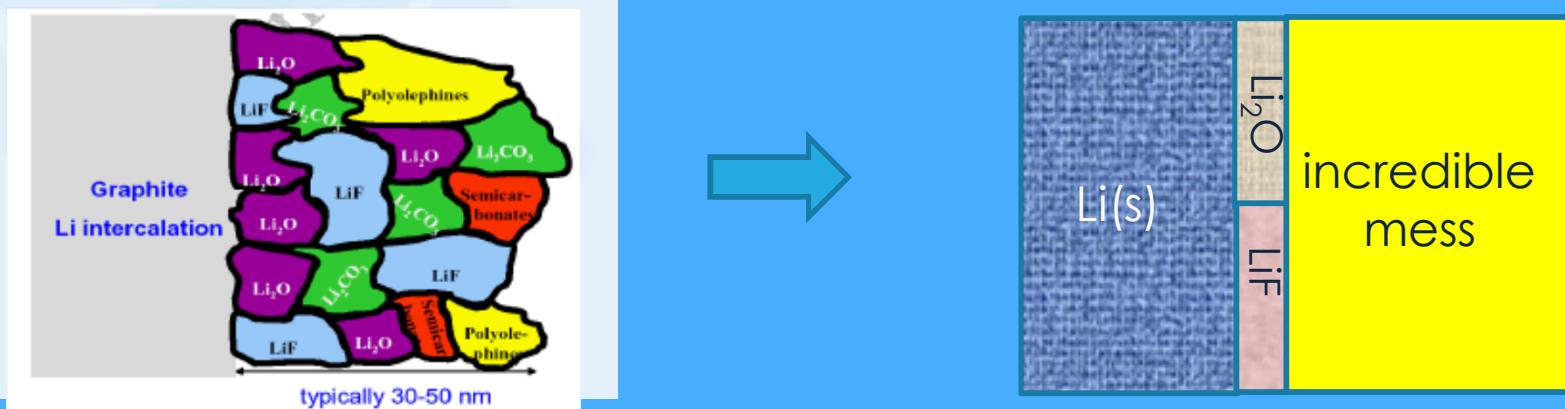
$\Delta E = -0.99$ eV

CO_2 further decomposes on Li (100)



- Previous AIMD simulations of CO on Li(100) reveal decomposition into C and O
- “C” then forms “ Li_xC ”, perhaps ultimately graphite

Destruction of SEI components -> simplification of interface

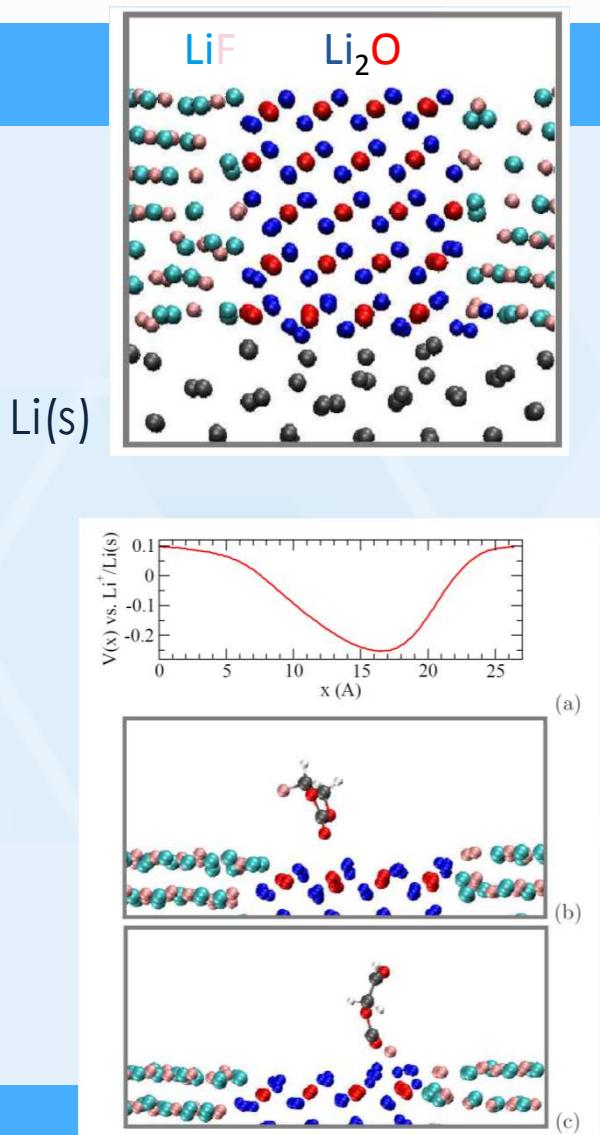


Some clarity in most important interface region

Where this paradigm leads:



hot spots, surface heterogeneities

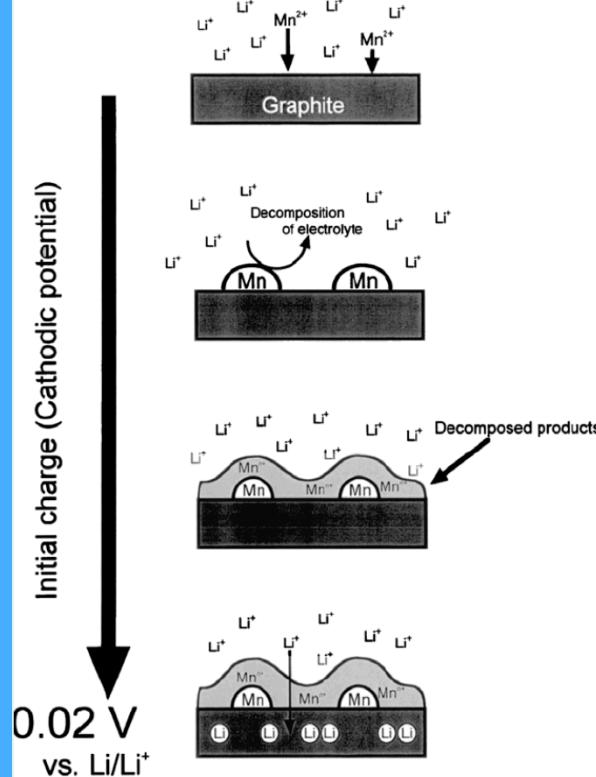


Mn(II) induced SEI disruption

Influence of manganese(II), cobalt(II), and nickel(II) additives in electrolyte on performance of graphite anode for lithium-ion batteries

Electrochimica Acta 47 (2002) 1229–1239

(Thanks to Yue for the reference)



First-Principles Modeling of Mn(II) Migration above and Dissolution from $\text{Li}_x\text{Mn}_2\text{O}_4$ (001) Surfaces

Chem Mater. (2017)

Kevin Leung*^①

the price you pay for metastability

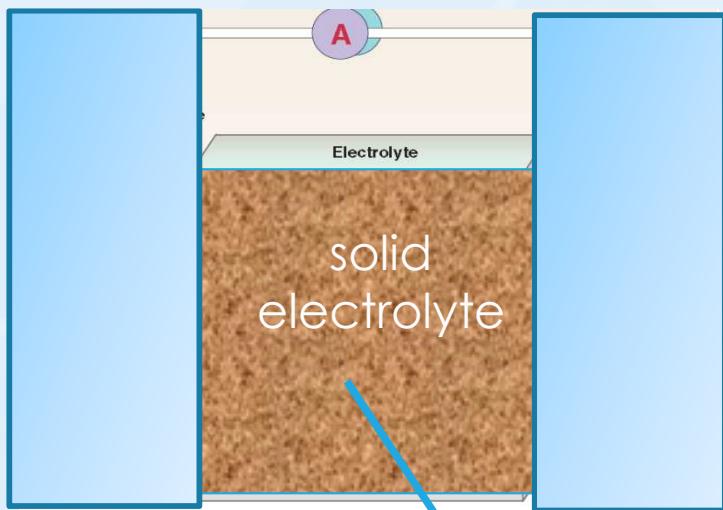


Solid state electrolytes: single phase thermodynamics

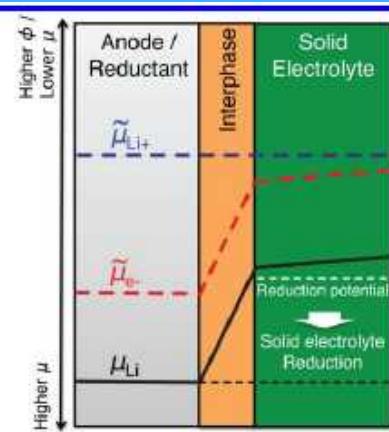
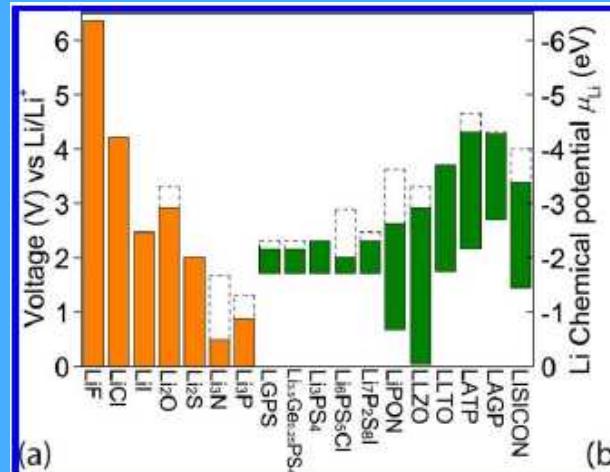
Origin of Outstanding Stability in the Lithium Solid Electrolyte Materials: Insights from Thermodynamic Analyses Based on First-Principles Calculations

Yizhou Zhu,[†] Xingfeng He,[†] and Yifei Mo^{*,†,‡}

DOI: 10.1021/acsami.9b07517
ACS Appl. Mater. Interfaces 2019, 11, 22389–22393



decompose into other phase?

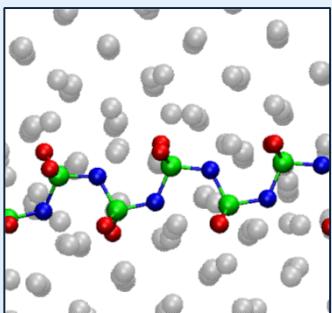


- solid electrolyte stability in all solid state batteries, solid using bulk thermodynamics
- no need to look at explicit interface?
- reasonable because solid interfaces often annealed at high temperature



Going full circle: looking at reaction barriers at solid-solid interfaces

(apply liquid interface techniques to solid electrolyte interfaces)



top view



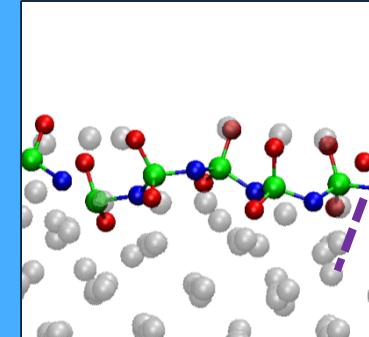
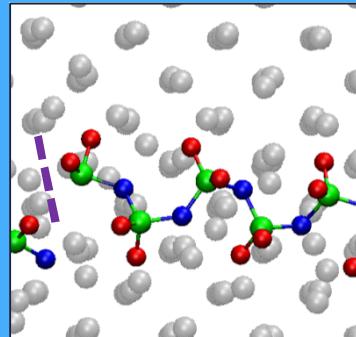
side view

break P-N



$$\Delta E = -1.96 \text{ eV}$$

$$\Delta E^* = 1.37 \text{ eV}$$





Some Notes on Electrostatics

Need extreme care when dealing long-range electrostatics
in periodic boundary conditions (PBC) simulation cells

Monopole, dipole, quadrupole corrections



- charged simulation cell:
monopole (+ quadrupole) correction

Periodic boundary conditions in *ab initio* calculations

G. Makov and M. C. Payne

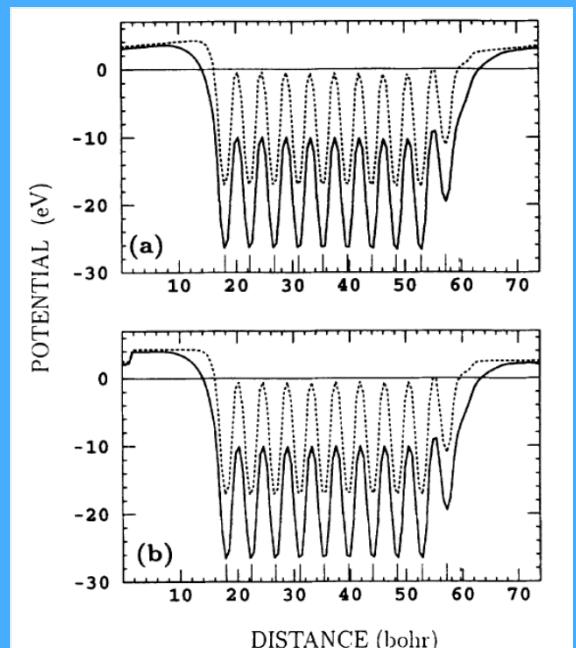
PHYSICAL REVIEW B 51 4014



$$E = E_0 - \frac{q^2 \alpha}{2L} - \frac{2\pi q Q}{3L^3} + O(L^{-5})$$

- In chemistry, see L.R. Pratt et al.
- for homogenous systems

Uncharged cell with vacuum layer:
dipole correction for slab geometries
only charge neutral cells

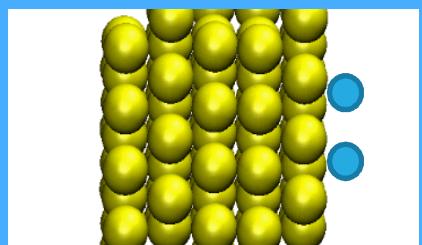


Adsorbate-substrate and adsorbate-adsorbate interactions of Na and K adlayers on Al(111)

Jörg Neugebauer and Matthias Scheffler

PHYSICAL REVIEW B 46 16 067

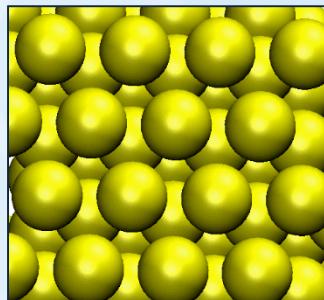
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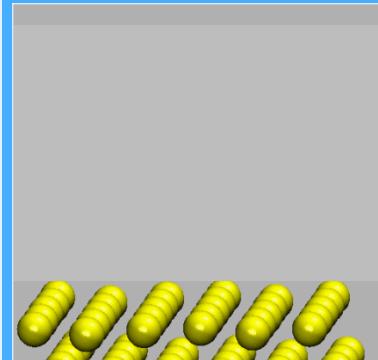
Mean electropotential is undefined



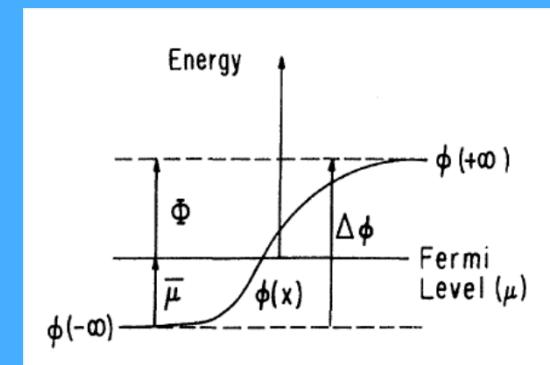
- average electrostatic potential in simulation cell (the $\mathbf{k}=0$ contribution to Ewald summation used in PBC DFT), is always set to zero
- So absolute Fermi level E_F in simulation cell is undefined!
- If we have vacuum region, can assign potential in vacuum to zero
- This allow an absolute reference and yields work function, and voltage



bulk crystal simulation cell: E_F , work function are undefined



defined for metals with interfaces



N.D. Lang & W. Kohn, Theory of Metal Surfaces: Work Function PRB 3, 1215 (1971)

- Not really useful for small polaron systems like transition metal oxide



Computing and Controlling Voltages

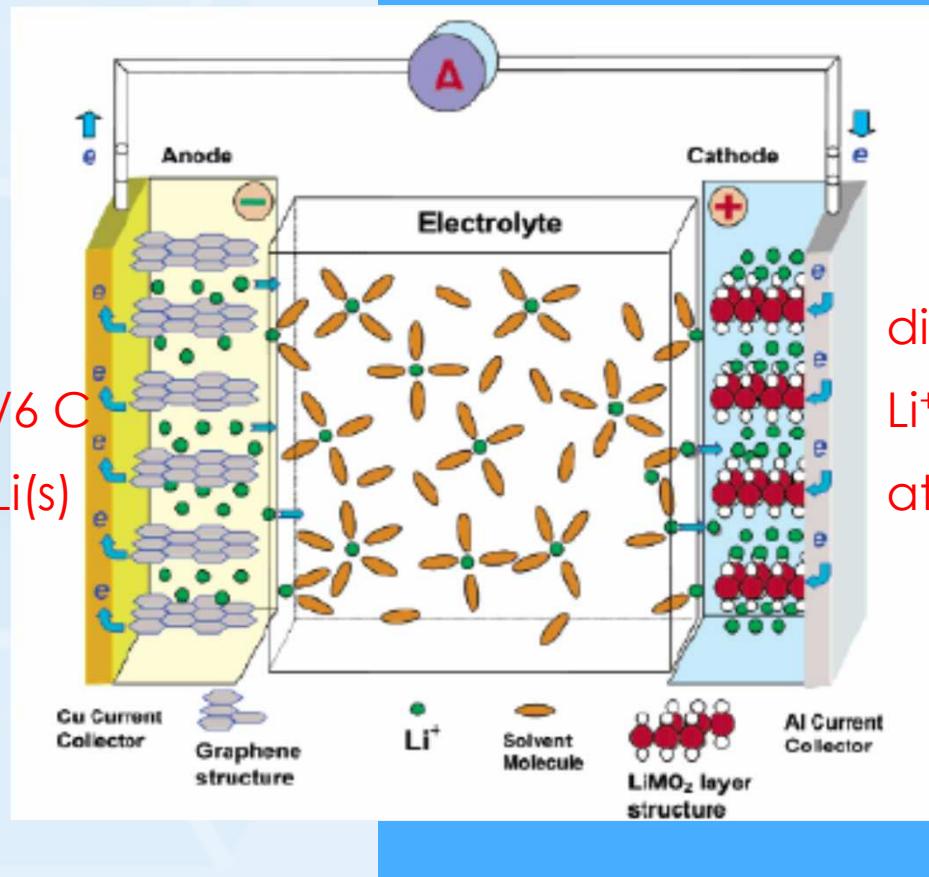
- At battery interfaces, everything depend on voltage
- So far our ability to model voltage dependences are limited

Leung & Tenenby, J. Phys. Chem. C 117:24224 (2013);
Leung, Phys. Chem. Chem. Phys. 17, 1637 (2015)
Leung & Leenheer, J. Phys. Chem. C 119:10234 (2015)



Current lithium current batteries

Anode || electrolyte || cathode



discharge:



at ≥ 0.1 V vs. Li₊/Li(s)

(... also separator membrane, binders, carbon black ...)

discharge:



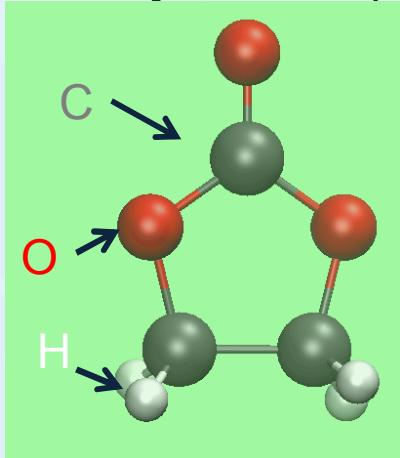
at $\leq 4.0-4.2$ V vs. Li₊/Li(s)

Battery Interfaces



Li into anode: ~ 0.1 V; Li into cathode: > 3.5 V
EC decomposes: > 4.5 V or 6.6 V(?) (cathode)

- At <0.8 V (vs. Li⁺/Li(s)), EC-based electrolyte decomposes on anode

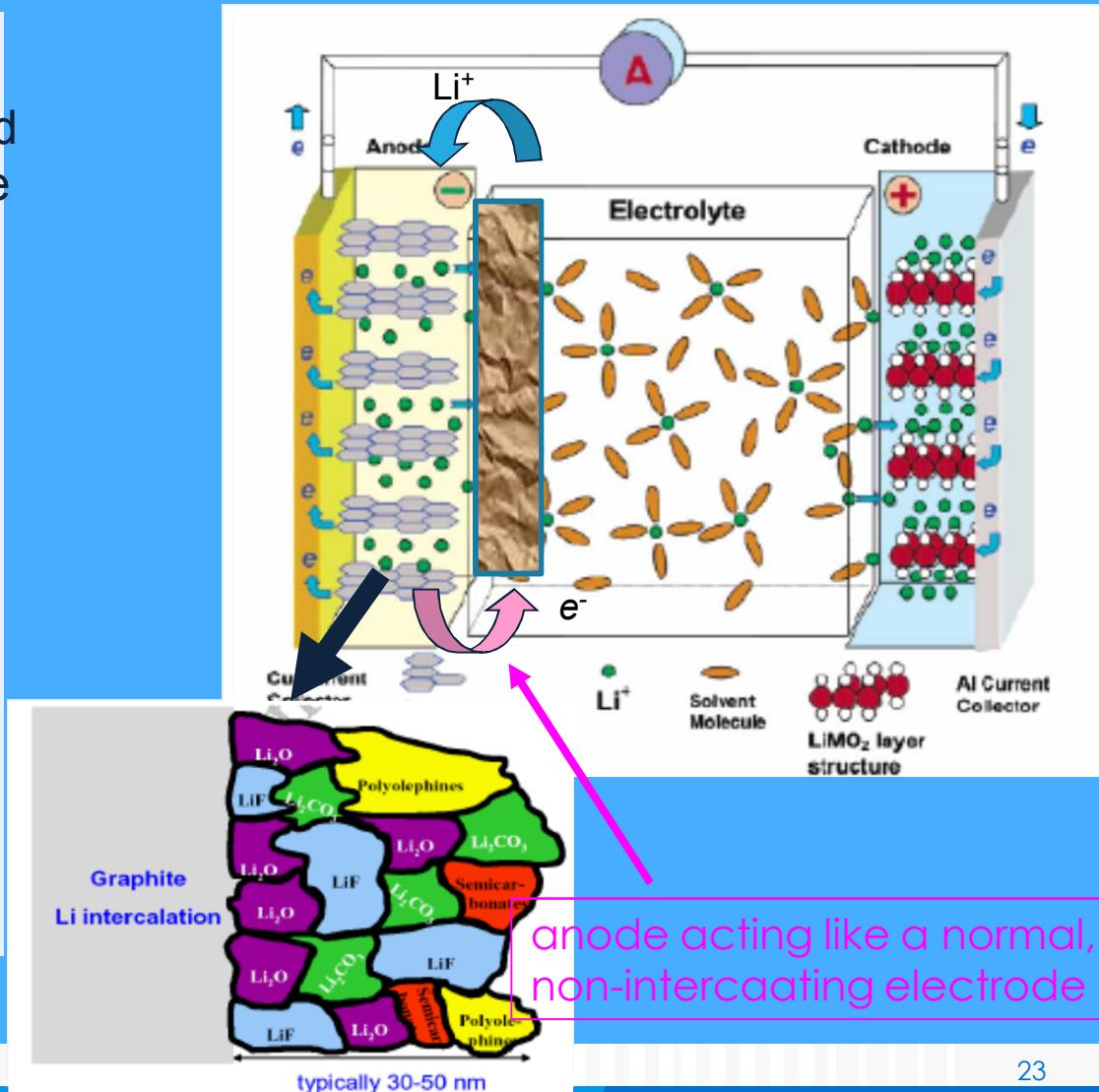


ethylene
carbonate
(EC)

- self-limiting SEI growth stops further electrolyte breakdown

Xu, Chem. Rev. 104:4303 (2004)

- search for alternatives continue



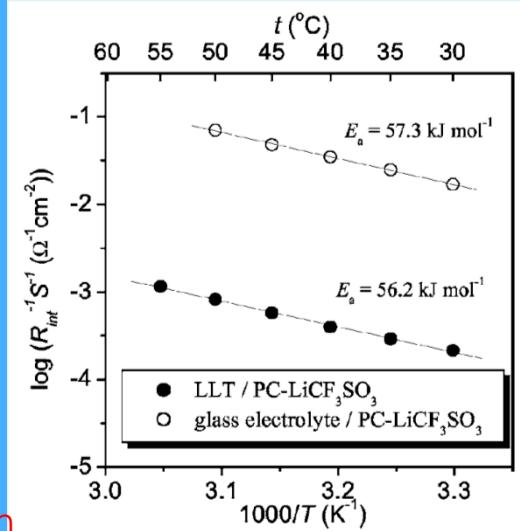
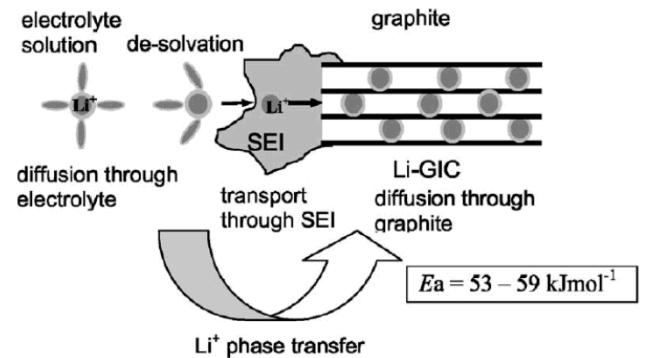


Want to predict Li^+ transfer rate from electrolyte into electrode

Journal of The Electrochemical Society, 152 (11) A2151-A2154 (2005)
0013-4651/2005/152(11)/A2151/4/\$7.00 © The Electrochemical Society, Inc.

Lithium-Ion Transfer at the Interface Between Lithium-Ion Conductive Ceramic Electrolyte and Liquid Electrolyte-A Key to Enhancing the Rate Capability of Lithium-Ion Batteries

Takeshi Abe,^{*z} Fumihiro Sagane, Masahiro Ohtsuka, Yasutoshi Iriyama,^{*} and Zempachi Ogumi^{**}



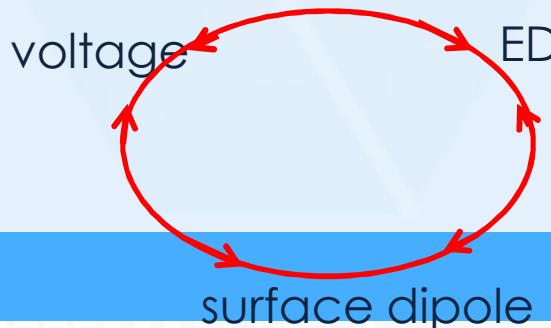
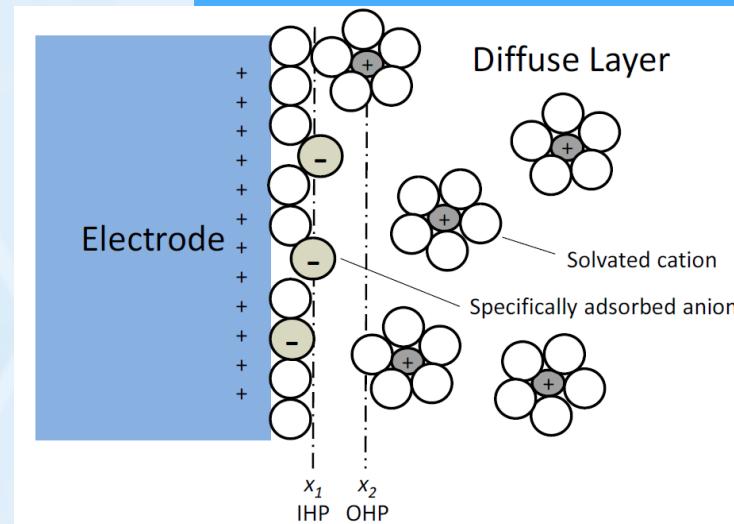
modeling-wise, we are not there yet.

1. electrode surface not pristine; SEI structure not known
2. voltage dependence hard to calibrate



What is “voltage” at atomic lengthscale?

voltage “=” Fermi level + electric double layer



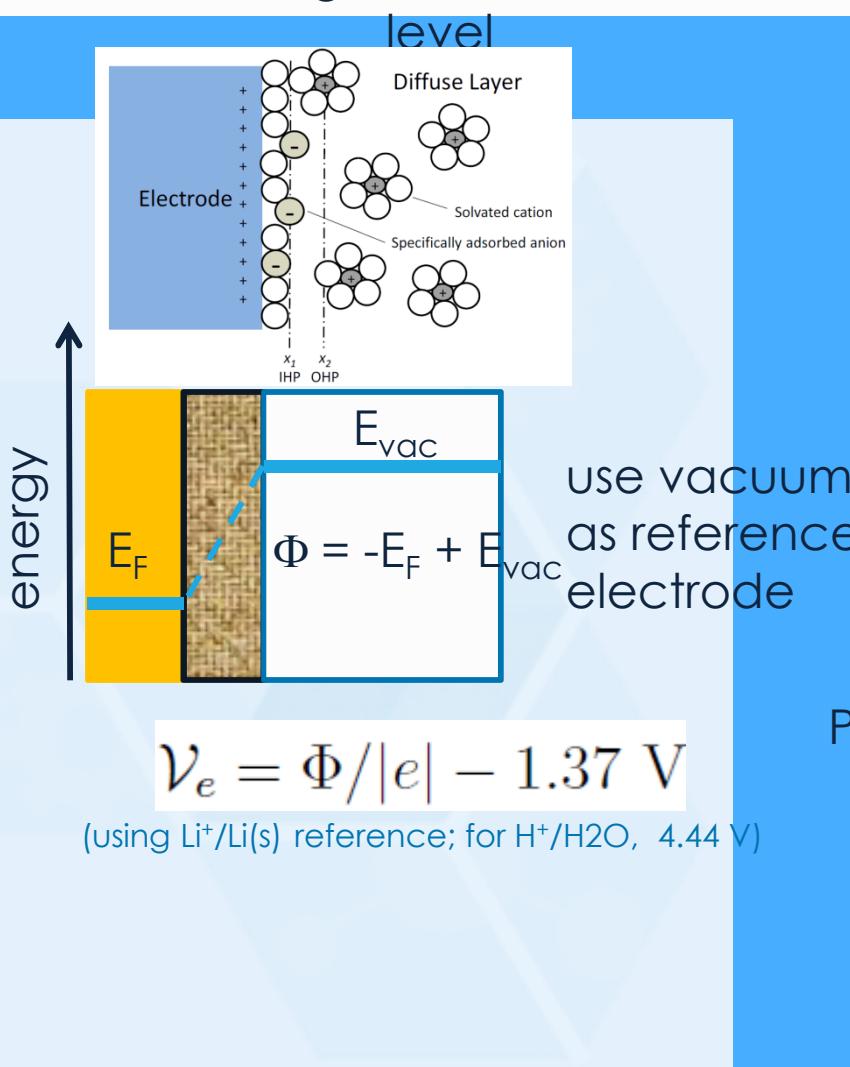
EDL (fancy way of saying there is a dipole layer)

$$\Delta\mathcal{V}_e = -4\pi\delta/(|e|)$$

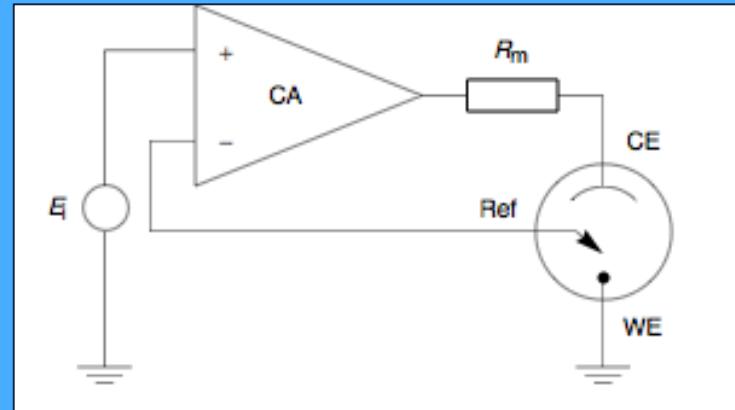
Voltages: DFT calculations vs. expt.



DFT modeling: one electrode/Fermi level



Experiments: >2 electrodes/Fermi levels



Potentiostat controls electronic voltage \mathcal{V}_e

Li content slowly responds to \mathcal{V}_e

\mathcal{V}_e

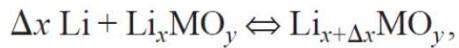


In the battery modeling, voltage means something else

PHYSICAL REVIEW B 70, 235121 (2004)

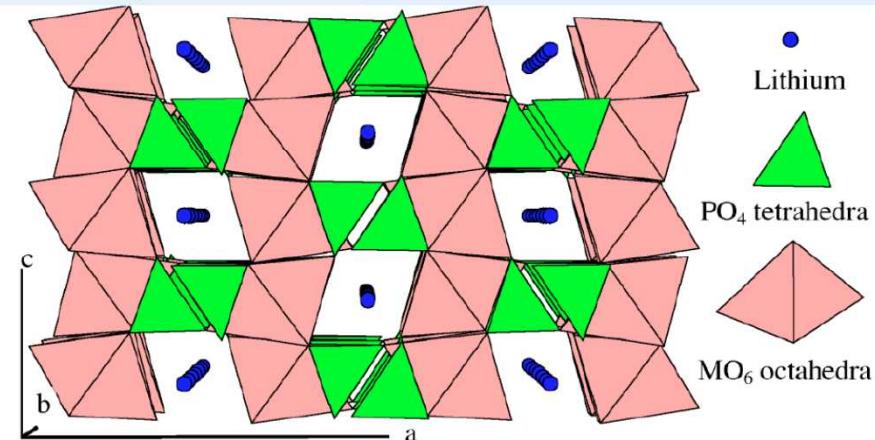
First-principles prediction of redox potentials in transition-metal compounds with LDA+U

F. Zhou | M. Cococcioni, C. A. Marianetti, D. Morgan, and G. Ceder



$$V(x) = - \frac{\mu_{\text{Li}(x)}^{\text{cathode}} - \mu_{\text{Li}}^{\text{anode}}}{F}.$$

$$\langle V \rangle = \frac{-[E(\text{Li}_{x_2} \text{MO}_y) - E(\text{Li}_{x_1} \text{MO}_y) - (x_2 - x_1)E(\text{Li metal})]}{(x_2 - x_1)F}$$



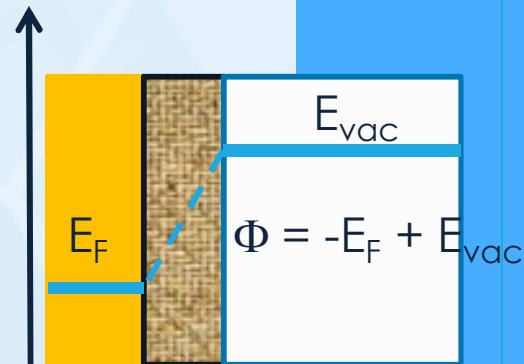
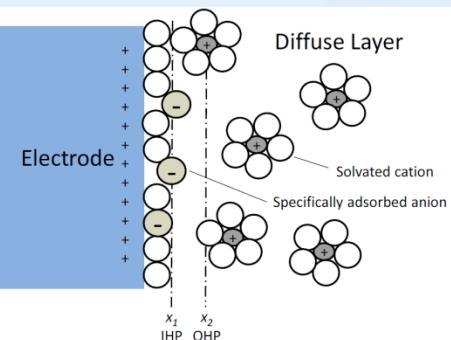
	Mn ²⁺	Mn ³⁺	Mn ⁴⁺	Fe ²⁺	Fe ³⁺	Co ²⁺	Co ³⁺	Co ⁴⁺	Ni ²⁺	Ni ³⁺	Ni ⁴⁺
Olivine	3.92	5.09		3.71	4.90	5.05	6.34		5.26	6.93	
Layered							4.91	5.37		6.70	6.04
Spinel		4.64	5.04				5.62	6.17			
Monoxide (Ref. 40)	3.6			4.6		5.0			5.1		

- Simulation cell has no vacuum level
- Fermi level not defined
- Voltage is here defined via Li chemical potential

LIB: Two voltage definitions: electronic vs. “ionic” voltage (rest of the world vs. battery literature)



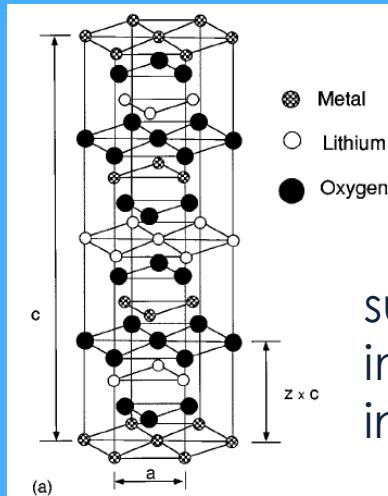
fuel cell, PV supercapacitors: voltage is electronic, interfacial



$$\mathcal{V}_e = \Phi / |e| - 1.37 \text{ V}$$

True instantaneous voltage (“potentiostat”)

Battery modeling: voltage is bulk-like, ionic



$$\mathcal{V}_i = -\frac{\mu_{\text{Li}}^{\text{cathode}}(x) - \mu_{\text{Li}}^{\text{anode}}}{zF}$$

\mathcal{V}_e is undefined!

such calculations implicitly assume an interface supporting

$$\mathcal{V}_i = \mathcal{V}_e$$

Li content slowly responds to \mathcal{V}_e

$$\mathcal{V}_i = \mathcal{V}_e \text{ at equilibrium}$$

$\mathcal{V}_i > \mathcal{V}_e$ more Li enters electrode if possible, lowers \mathcal{V}_i

$\mathcal{V}_i < \mathcal{V}_e$ some Li leaves electrode if possible, raises \mathcal{V}_i

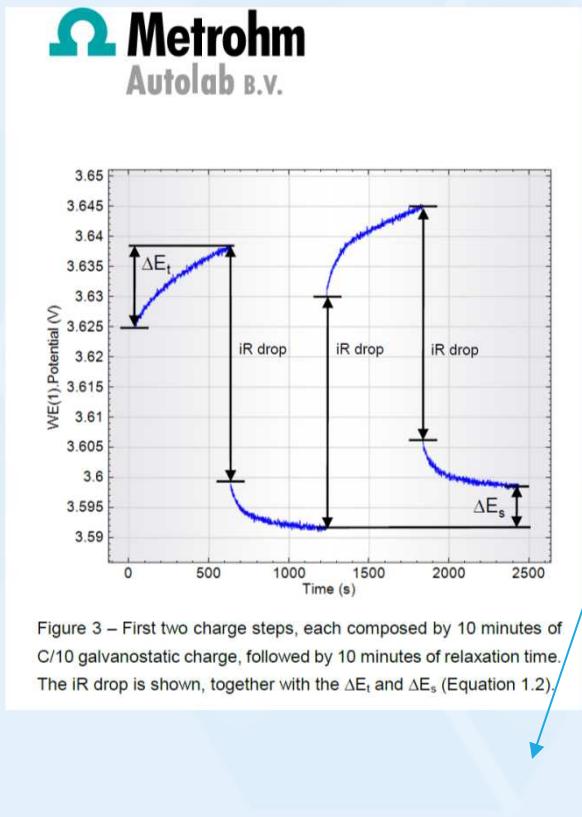
\mathcal{V}_i

\mathcal{V}_i



An arbitrary DFT interface is not at electrochemical equilibrium

Experimental analogy: Galvanostatic Intermittent Titration (GITT)



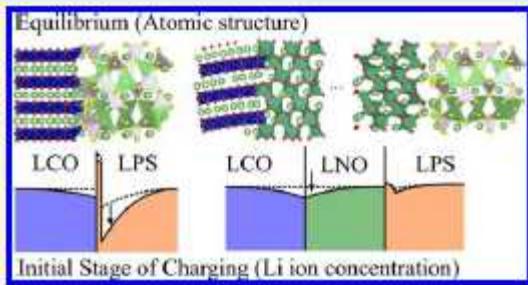
- v_e is the correct instantaneous voltage set by potentiostat
- Li content in solid (or interface) slowly relaxes
- But in DFT calculations, Li hardly move -- little relaxation, system out of equilibrium
- Need to move Li content by hand to make sure we have equilibrium



This confusion about “voltage” occurs in almost all battery interface modeling papers

Space-Charge Layer Effect at Interface between Oxide Cathode and Sulfide Electrolyte in All-Solid-State Lithium-Ion Battery

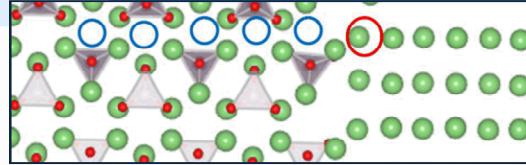
Jun Haruyama,^{†,‡} Keitaro Sodeyama,^{†,§} Liwan Han,^{†,§,||} Kazunori Takagi,^{†,‡} and Yoshitaka Tateyama^{†,‡,§,||}
Chem. Mater. 2014, 26, 4248–4255



Electrode-Electrolyte Interface for Solid State Li-Ion Batteries: Point Defects and Mechanical Strain

Santosh KC,^{a,‡} Roberto C. Longo,^a Ka Xiong,^a and Kyeongjae Cho^{a,b,*,‡}

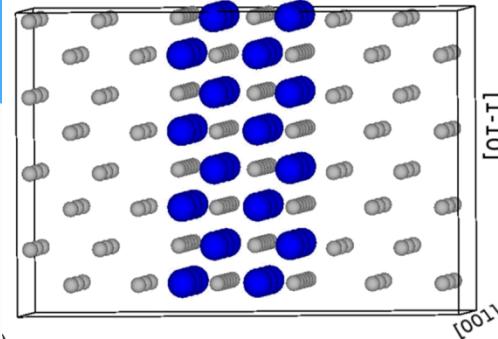
Journal of The Electrochemical Society, 161 (11) F3104-F3110 (2014)



Modeling interfaces between solids: Application to Li battery materials

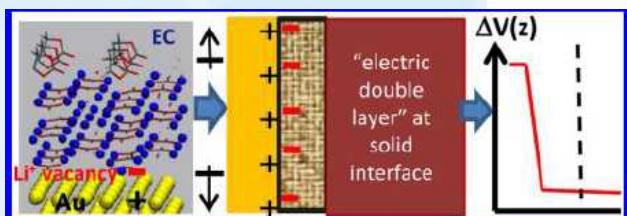
N. D. Lepley and N. A. W. Holzwarth^{*}

PHYSICAL REVIEW B 92, 214201 (2015)



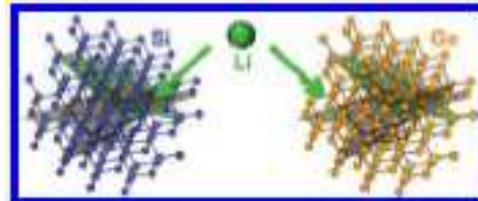
How Voltage Drops Are Manifested by Lithium Ion Configurations at Interfaces and in Thin Films on Battery Electrodes

Kevin Leung* and Andrew Leeheer



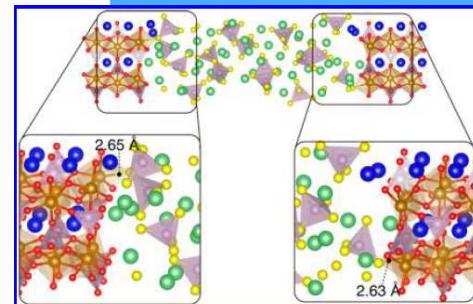
The First-Cycle Electrochemical Lithiation of Crystalline Ge: Dopant and Orientation Dependence and Comparison with Si

Maria K. Y. Chan,[†] Brandon R. Long,[‡] Andrew A. Gewirth,^{*,‡} and Jeffrey P. Greeley^{*,†}



Charged and Discharged States of Cathode/Sulfide Electrolyte Interfaces in All-Solid-State Lithium Ion Batteries

Masato Sumita,^{*,†} Yoshinori Tanaka,[‡] Minoru Ikeda,[†] and Takahisa Ohno^{§,†,‡,§}



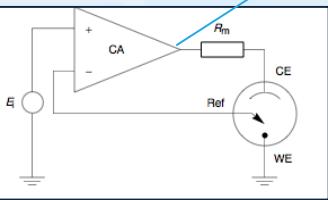
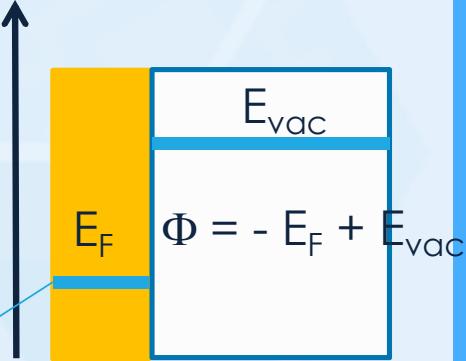
Quiz: what is the “voltage” of Li (100) metal in vacuum?



$$\mathcal{V}_e = \Phi/|e| - 1.37 \text{ V}$$

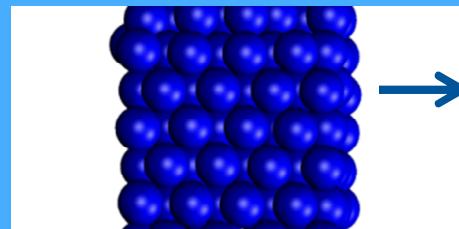
= 1.56 V vs Li⁺/Li(s)

($\Phi = 2.93 \text{ eV}$, CRC handbook)



$$\mathcal{V}_i = (\mu_{\text{Li}} - E_{\text{Li(s)}})/|e|$$

= 0.00 V vs Li⁺/Li(s)
for Li(s) \rightarrow Li⁺ (solv) + e⁻



Li (100)

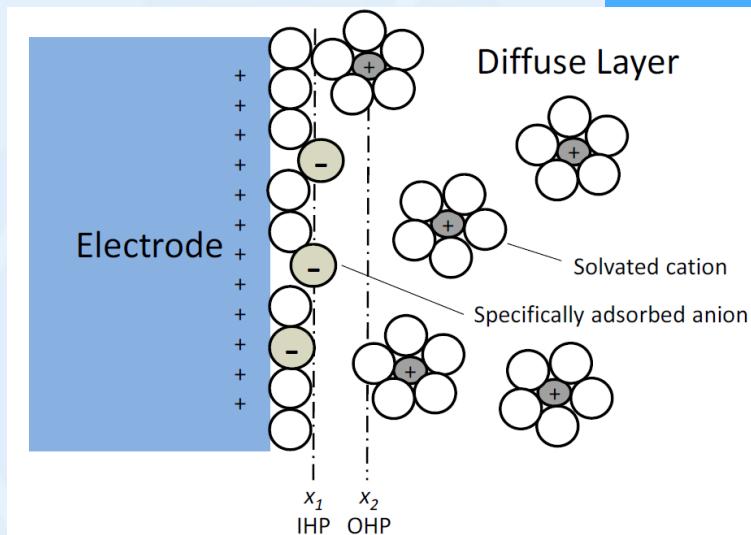
disconnected Li metal is not at electrochemical equilibrium

- Au³⁺ + 3 e⁻ \rightarrow Au(s) is at 1.52 V vs. SHE
- yet we never assume Au slab is at 1.52 V in DFT calculations
- should not assume Li electrode is always in equilibrium either

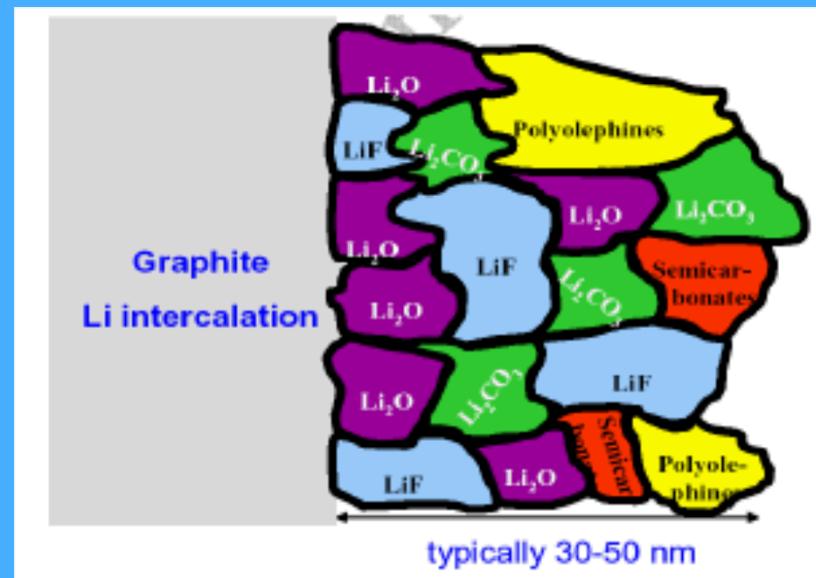


Electric Double Layer (EDL) in lithium ion batteries

pristine electrode
one potential of zero charge (PZC)



LIB electrode
(covered with films)
surface charge? PZC?



Slide 32

E10 Changed title font for consistency.

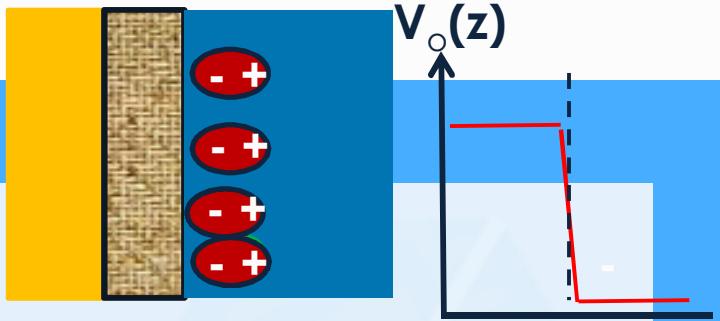
Ernie, 2/10/2012

EDL structures/voltage profiles (liquid outside thin film)

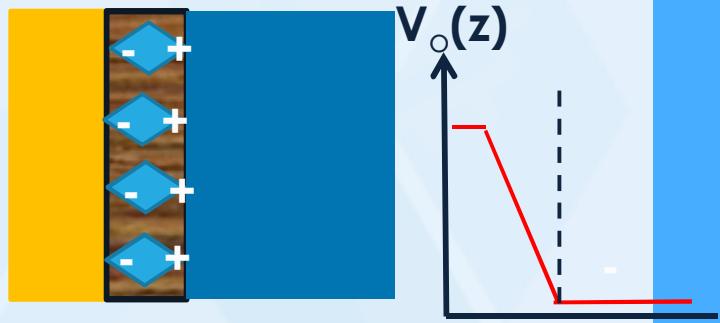


Electrostatic contribution only, ohmic loss not included

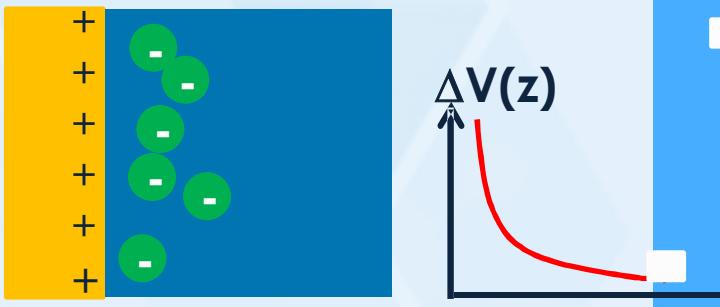
(a)



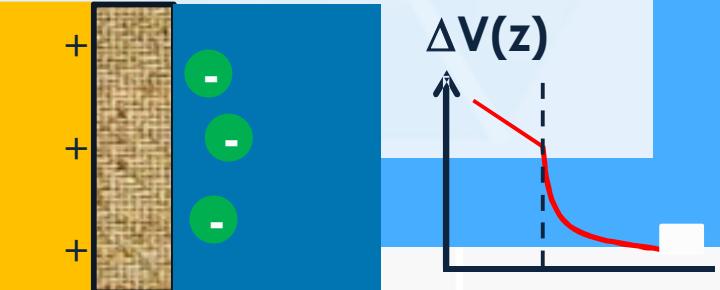
(b)



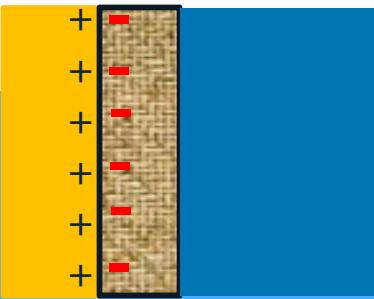
(c)



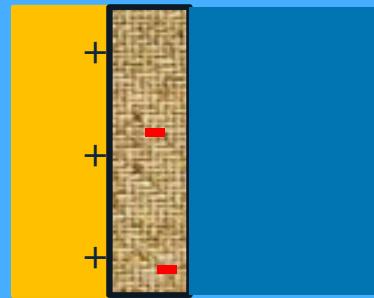
(d)



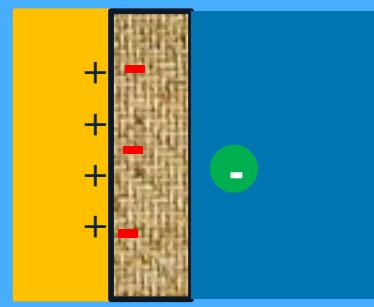
(e)



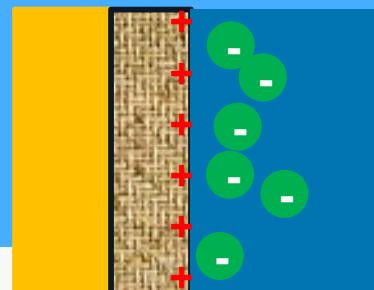
(f)



(g)



(h)



$\Delta V(z)$

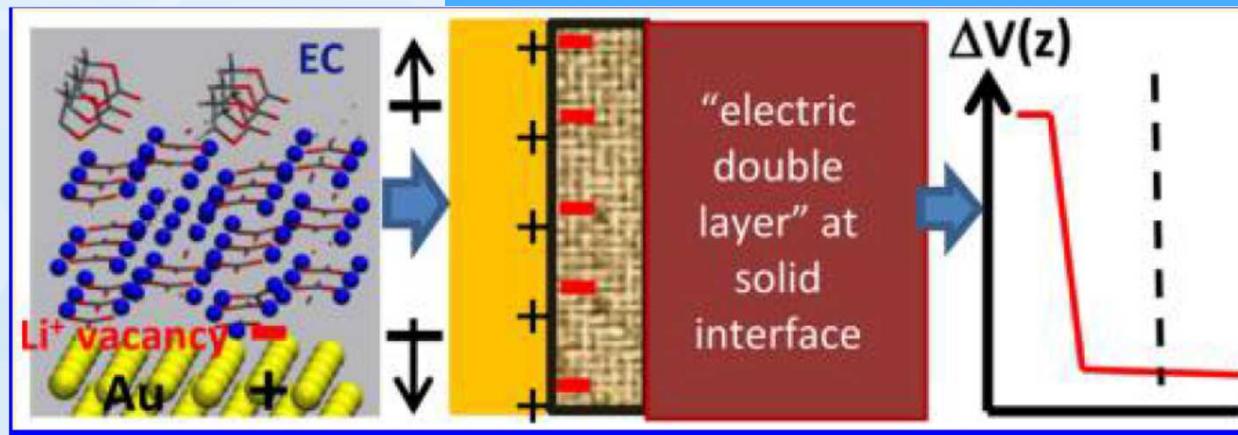
$\Delta V(z)$

$\Delta V(z)$

$\Delta V(z)$



(1) Potential drop at solid-solid interfaces



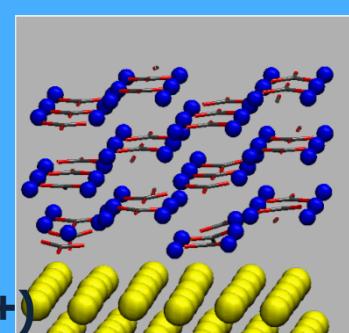
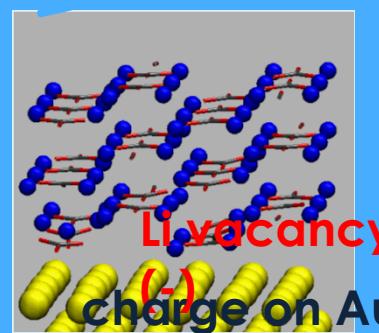
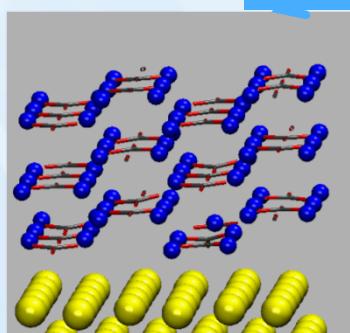
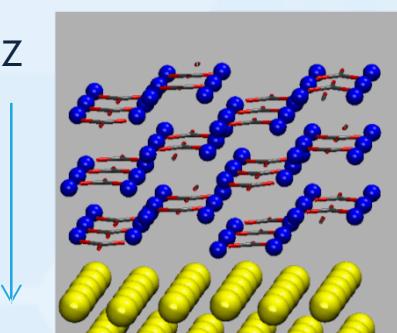
Li_2CO_3 covering Au(111) under UHV conditions



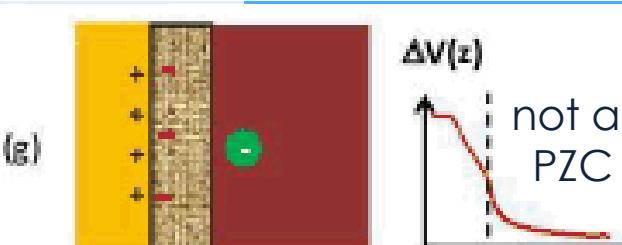
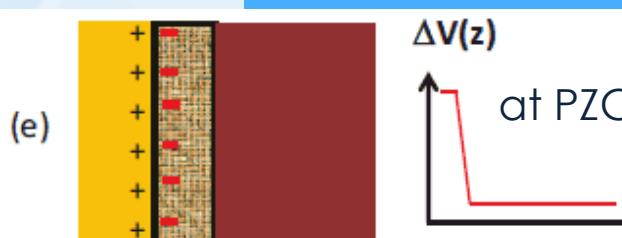
Li_2CO_3 oxidation relevant to Li-air batteries (hysteresis during charging)

Leung & Tenney, JPCC (to appear)

$\Delta N(\text{Li})$	0	-1	-2	-3	-4	-6
ν_e	3.56	3.87	4.03	4.03	4.05	4.41
ν_i	3.53	3.58	3.26	3.55	NA	



- to “oxidize” Li_2CO_3 , remove $(\text{e}^-, \text{Li}^+)$
- $|\text{Au}^+| \text{V}_{\text{Li}^-}|$ surface dipole \rightarrow raise ν_e
- Only one **potential-of-zero-charge** at $\nu_i = \nu_e$

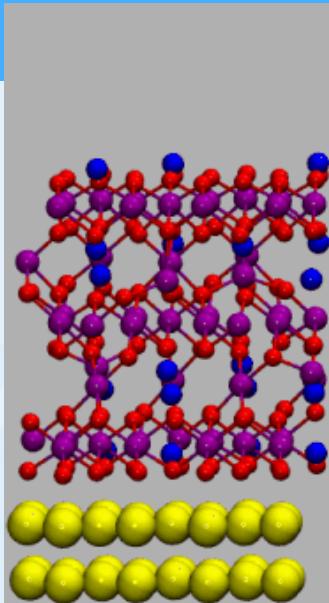


charge separation at interface yields dipole, EDL (c.f. Maier, PRL 2014)

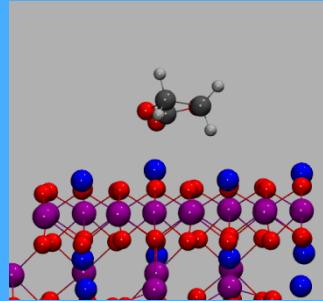
Li vacancies: “space charge” but are mobile (moves to interface) and plentiful



$\text{Li}_x\text{Mn}_2\text{O}_4$ (111) on Au(111) “current collector”

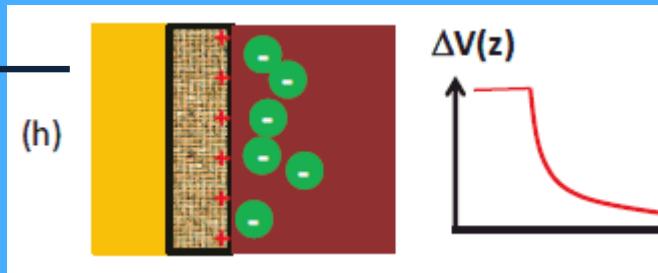
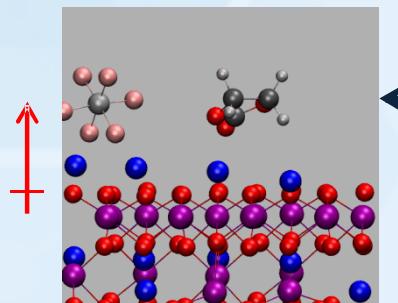


LMO(111)
surface:
Karim et al.,
PRB 87:075322
(2013)



In calculations,
can mimic expt.
with a linear
combination of
surfaces patches
with/without PF_6^- .

$$V_e = a V' + (1-a)V''$$



electronic voltage/Ferm level not so important: LMO is polaronic, not metallic
electronic voltage control surface Li-vacancy/anion concentrations, hotspots

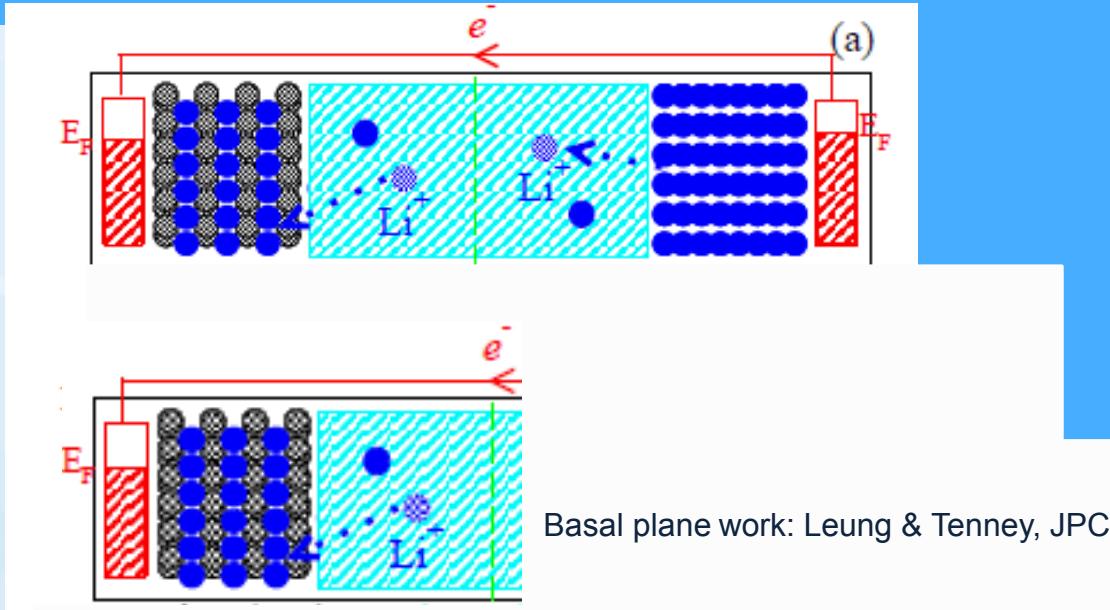


(B) Solid-Liquid Interface

No vacuum! Hard to compute voltage
(pristine electrode, only proof-of-principle)



Our method: Calculating voltage via Li^+ transfer

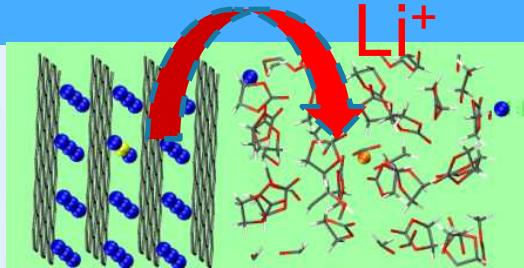


In lithium ion batteries, Li_+ transfer, not just e^- transfer, controls the potential

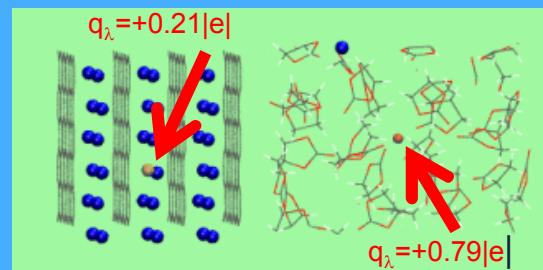
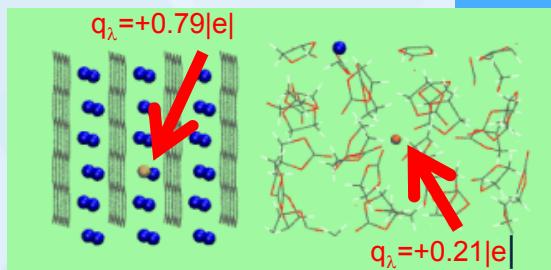
(Our voltage determination method most similar in spirit to Michiel Sprik and coworkers' seminal work for oxide surfaces)



Calculating voltage in lithium ion batteries in charge-neutral cells



$$\Delta G_{\text{hyd}} = \int_0^1 d\lambda \left\langle \frac{dH(\lambda)}{d\lambda} \right\rangle_{\lambda}$$

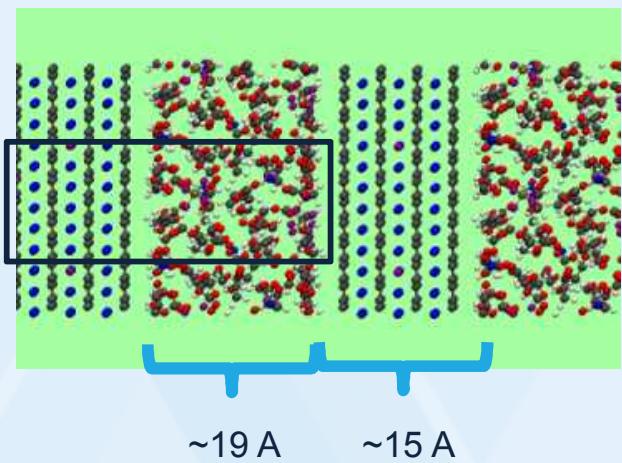


$$\Delta G_t(2 \text{ pts}) \sim 0.5 \langle dH(\lambda) / d\lambda \rangle_{\lambda_1} + 0.5 \langle dH(\lambda) / d\lambda \rangle_{\lambda_2}$$

- moving $\text{Li}^{\lambda+}$ into electrolyte leaves λ electron in electrode
- $\Delta G_t = 0$: Li^+ equally likely to be in LiC_6 or in electrolyte (i.e. at $\sim 0.1 \text{ V}$ vs Li^+/Li)
- make contact with expt. (don't need vacuum gap for absolute voltage)
- 15-34 ps per simulation window



Nanosized simulation cell details



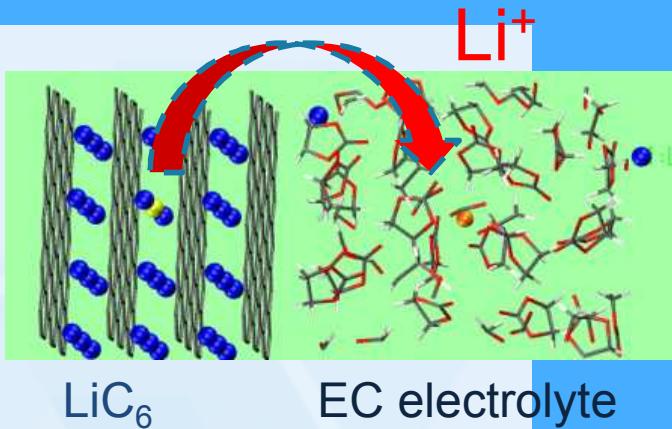
- same simulation cell size to calculate voltage, model electrolyte decomposition
- assume double layer ends at middle of liquid slab (LIB: 1.0 M salt, Debye length ~ 3 Å)
- Method “rigorous” for macroscopic electrochemistry if system size/trajectory length increases

- Put net charge $-n|e|$ on electrode surfaces, calculate voltages
- **n excess Li^+ in liquid EC leaves n excess e^- in electrode**

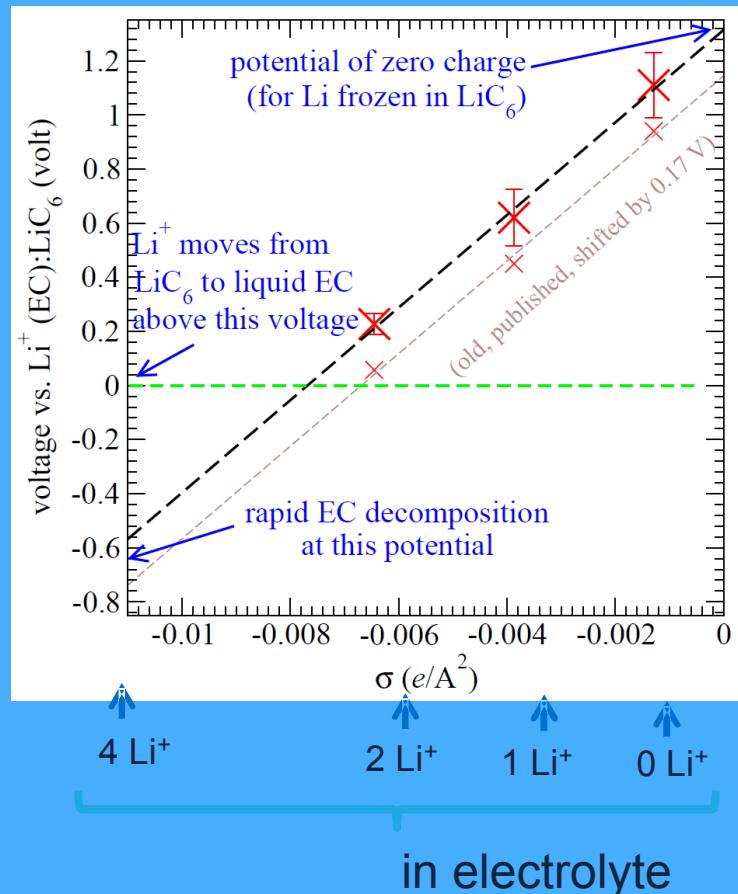
For aqueous systems, there are alternative methods.
See works by Michiel Sprik, Jun Cheng, Giulia Galli, etc.



Calculating voltage drop in batteries via ΔG_t of Li^+ transfer



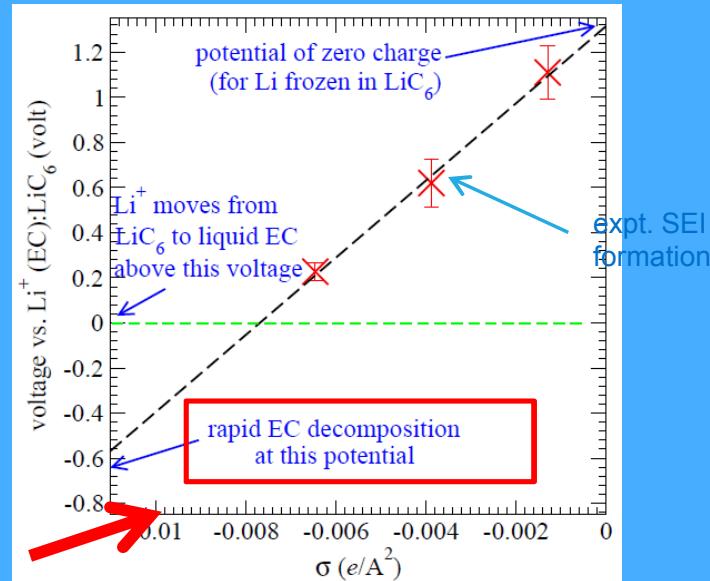
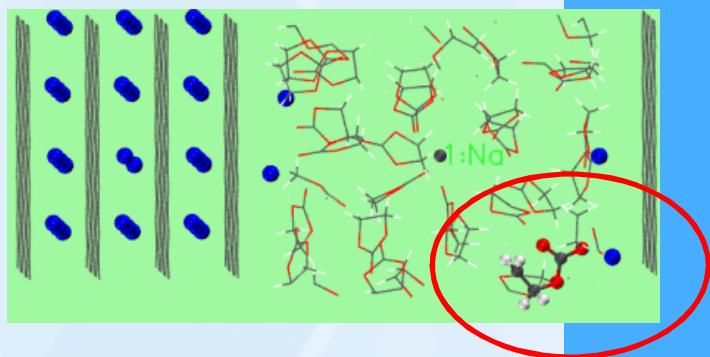
- 0 V vs LiC_6 (y-axis) is ~ 0.1 V vs $\text{Li}^+/\text{Li(s)}$
- Net –ve surface charge (σ) exists on basal plane during Li^+ intercalation
- Small cell size $\rightarrow \sigma$ changes during integration (
$$\Delta G_{\text{hyd}} = \int_0^1 d\lambda \left\langle \frac{dH(\lambda)}{d\lambda} \right\rangle_\lambda$$
). take halfway point for σ value.





EC decomposition seen at very low potentials

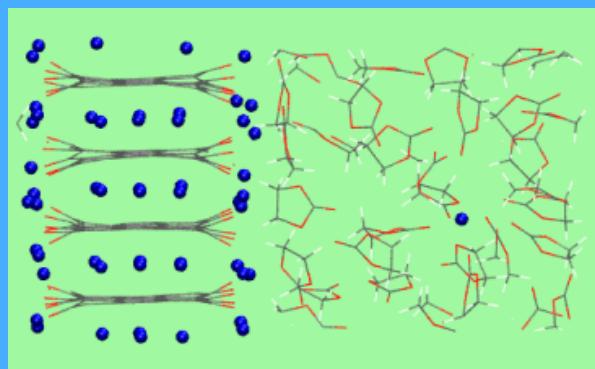
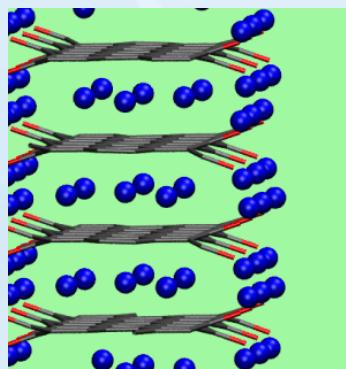
With longer trajectories, should see decomposition at higher voltage



- enough –ve charge (excess e^-) on electrode (compensated by Li^+ in electrolyte for e^- to jump from LiC_6 to EC via a Li^+ bridge at the surface

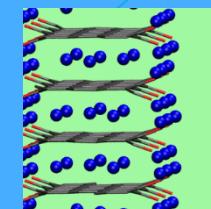
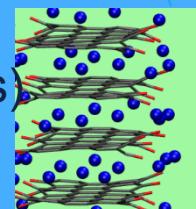
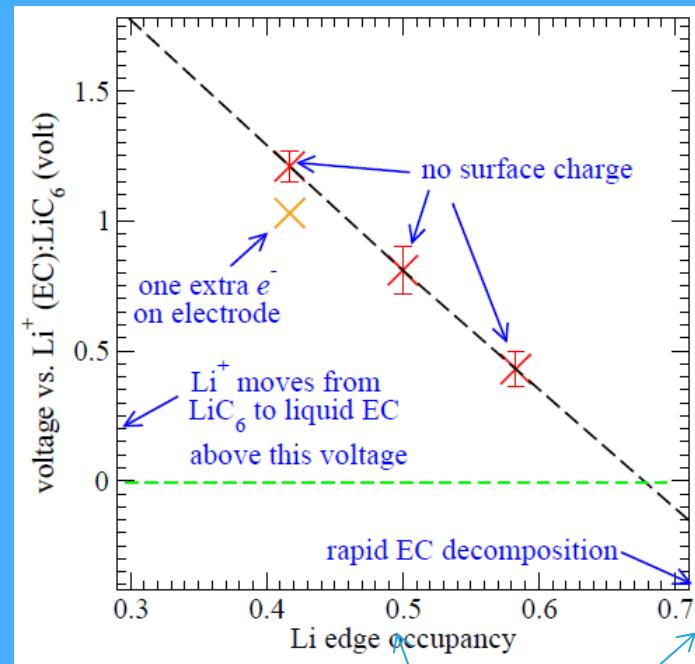
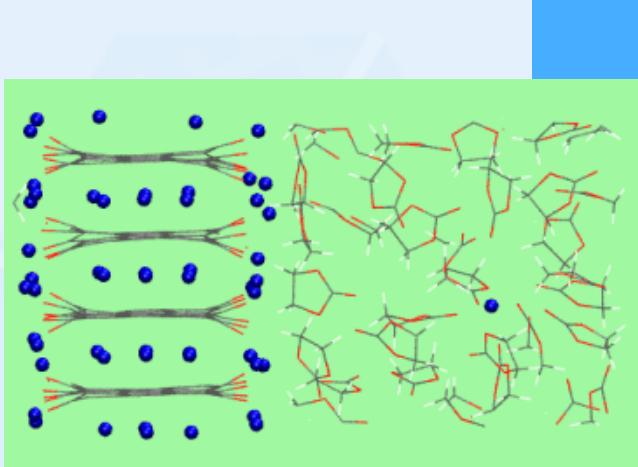


LiC₆ C=O edge planes





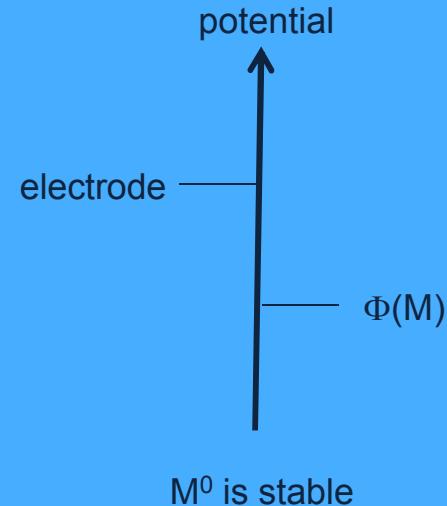
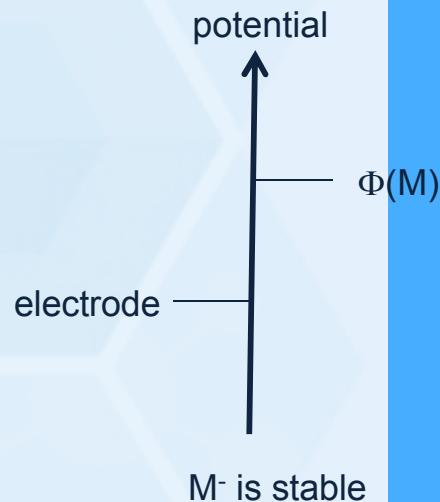
Edge plane: Potential = $V(\sigma, n_{\text{Li}})$, more complicated!



- Focus on $\sigma=0$, vary n_{Li} (Li coverage at C=O edge sites)
- $\Delta G_t = 0$ (Li+ intercalation) when $n_{\text{Li}} = 0.67$
- $n_{\text{Li}} = 1$ used previously too low voltage
- If $n_{\text{Li}} > 0.65$, surface should be positively charged ($\sigma > 0$)



Validation of potential predictions via e^- transfer

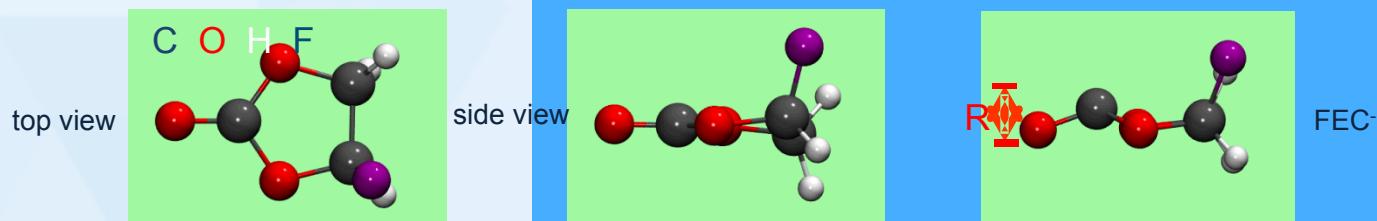




Validation of predicted interfacial potentials via e⁻ transfer to FEC

Similar to ferrocene as marker but FEC reduces at low voltages

Tang, Lu, Newman, [JECS 159:A1775 (2012)]



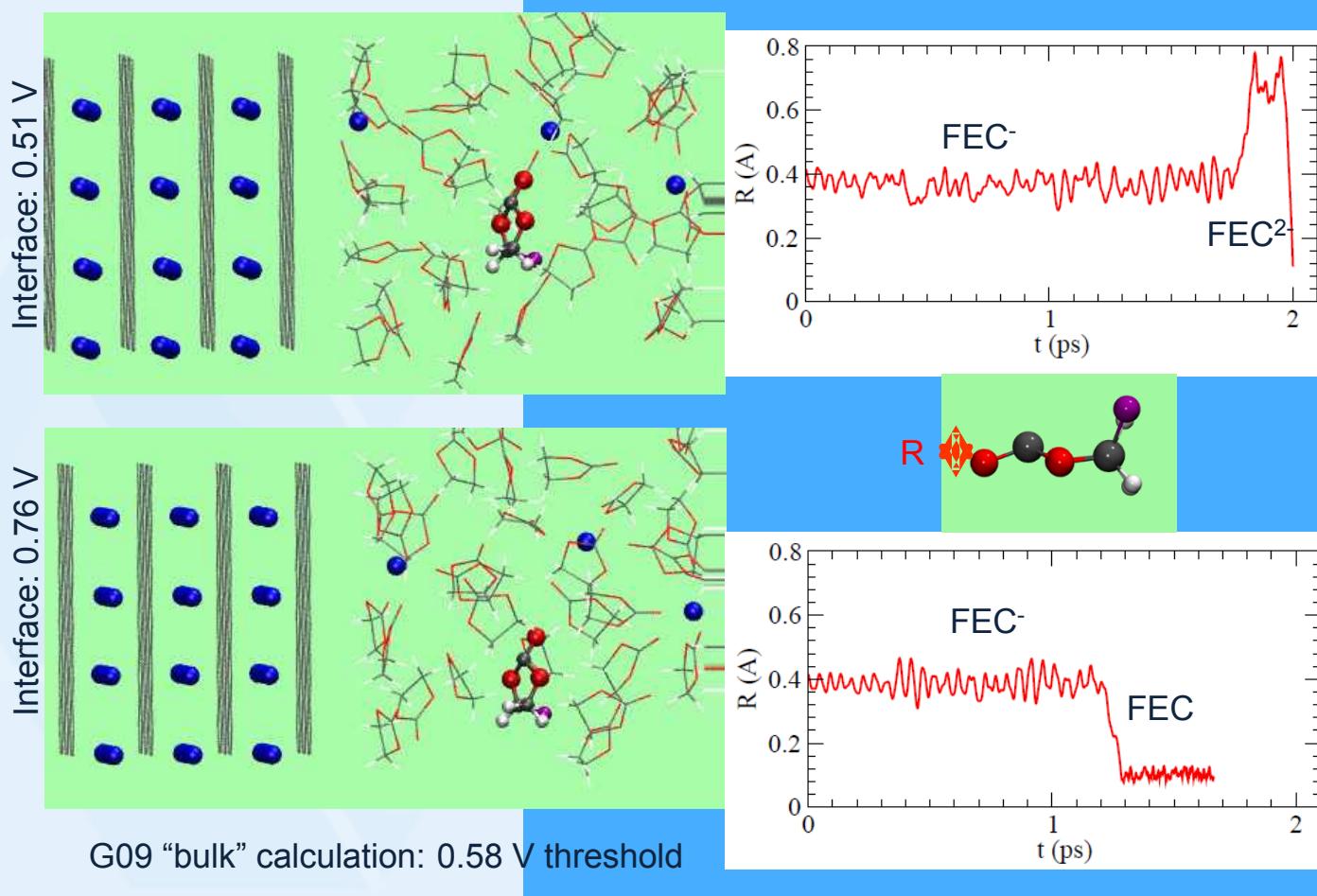
- FEC (fluorethylene carbonate) is a widely used electrolyte additive, gives better SEI
- $R \sim 0$ for FEC, $R \sim 0.4$ A for FEC⁻; thus geometry indicates charge state

$$\Phi = 0.58 \text{ V for FEC not coordinated to Li}^+, \text{DFT/PBE}$$

FEC as additive: , Leung, Rempe, Foster, Ma, Martinez del la Hoz, Sai, and Balbuena, JECS 161:A213 (2014)

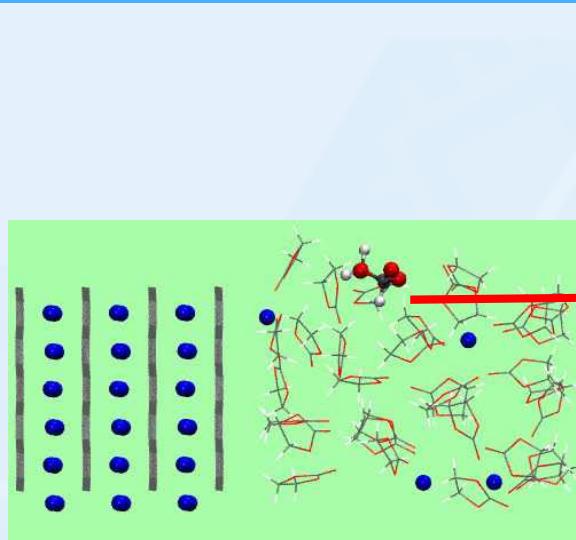


AIMD interfacial potential and g09 bulk liquid" calculations agree to within ~0.15 V in FEC reduction threshold

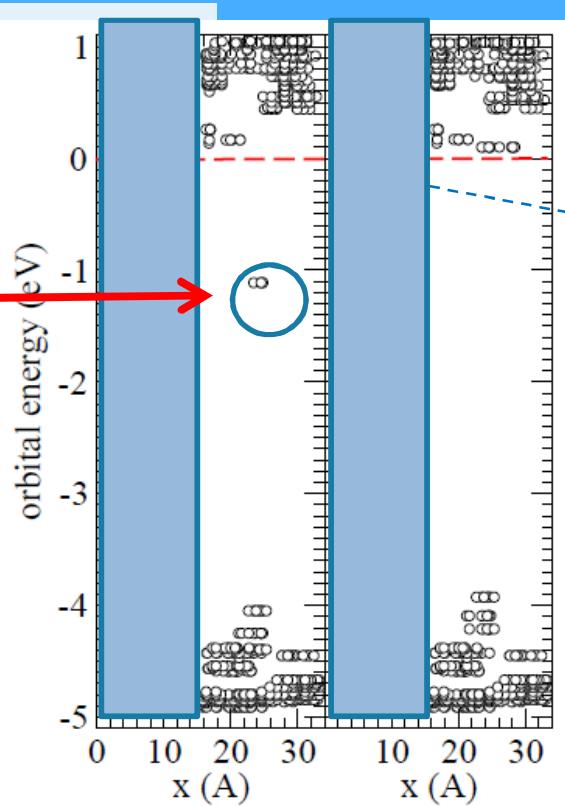




EC⁻ and FEC⁻ form “polaronic” state; e⁻ does not reside in electrolyte LUMO/conduction band



$x < 14 \text{ \AA}$
electrode $x > 14 \text{ \AA}$
electrolyte



In the literature
you often see:

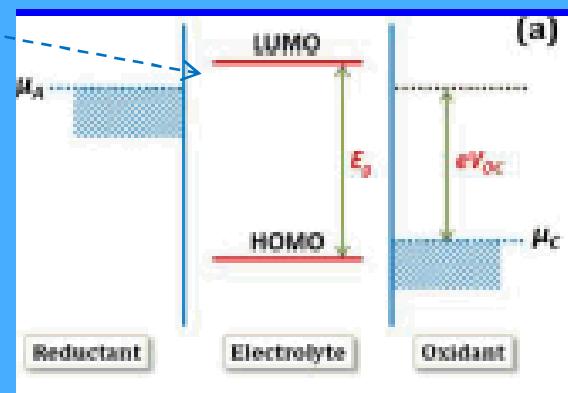


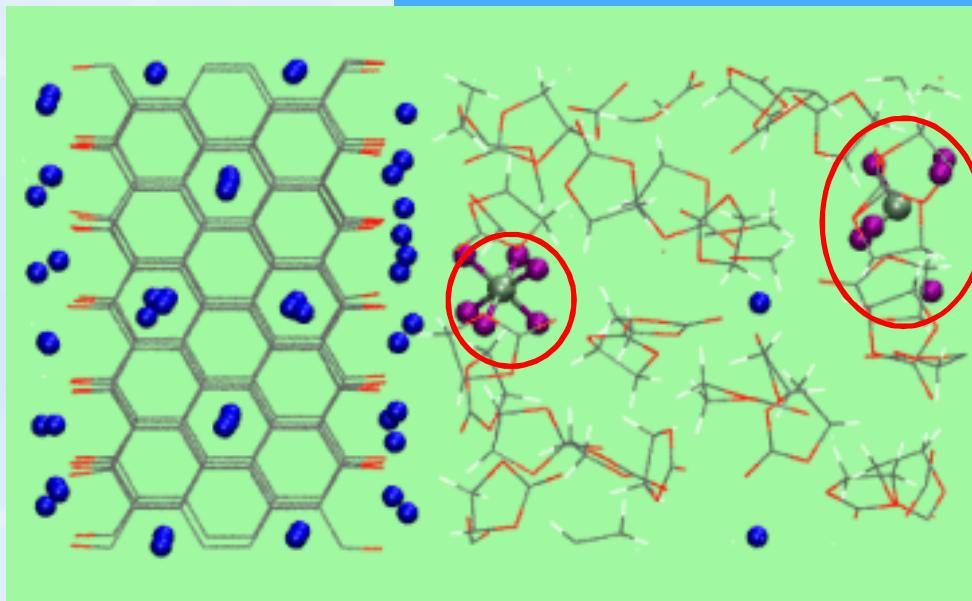
Figure 2. Relative energies of the electrolyte window E_g and the electrode electrochemical potentials μ_A and μ_C with no electrode/electrolyte reaction: (a) liquid electrolyte with solid electrodes; (b) solid

Goodenough & Park,
JACS 135:1167 (2013)

This is wrong!



Application: PF_6^- electrochemical reduction on edge plane?

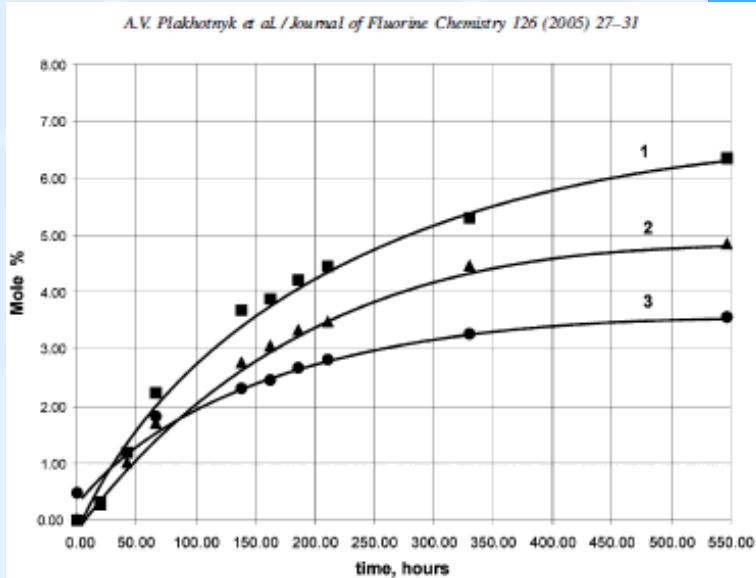




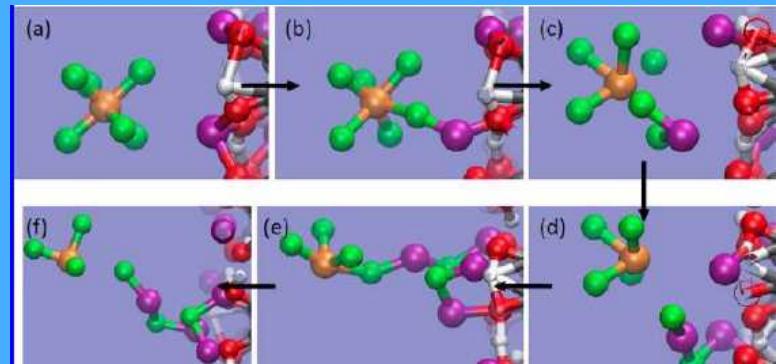
The strange case of PF_6^- degradation

- PF_6^- decomposition, found in SEI, widely accepted to be non-electrochemical
- may be due to thermal/water impurity; indeed, no CV peak for the anion
- But **experiments** with added water outside batteries show slow reaction

Hydrolysis in the system LiPF_6 —propylene carbonate—dimethyl carbonate— H_2O



Modeling PF_6^- degradation in the past



- Previous AIMD study of PF_6^- at mixed C=O, C-OH LiC₆ edge finds *barrierless* electrochemical reduction of anion; but voltage-dependence not known

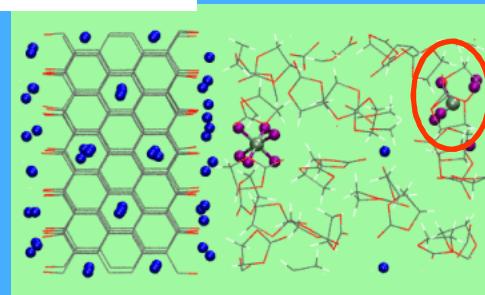
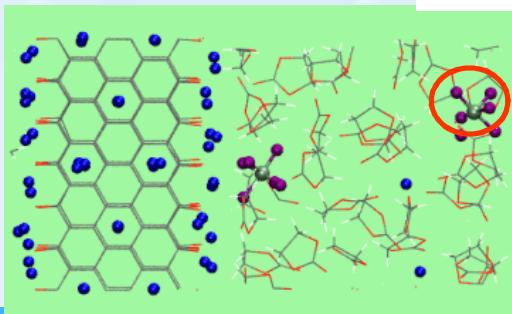
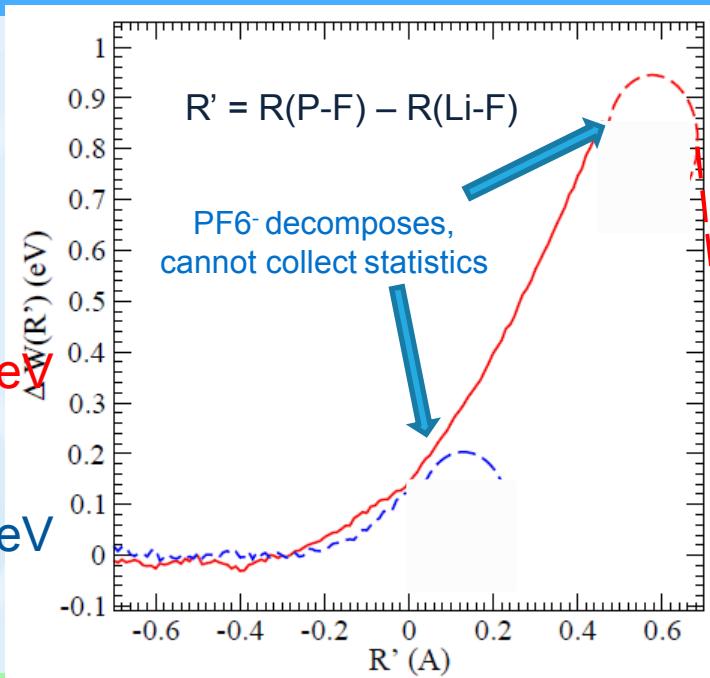
Ganesh, Kent, Jiang, JPCC 116:24476 (2012)



AIMD potential of mean force calculation of P-F bond breaking

interface: 0.53 V
barrier at least 1.0 eV

interface: -0.35 V
barrier at most 0.2 eV

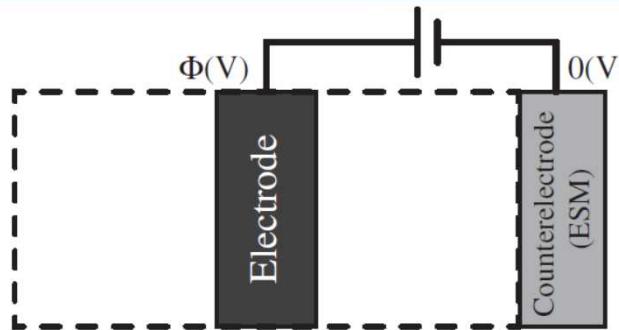




Voltage Calibration: Conclusions

- Devised method for predicting voltage-dependences of liquid/solid interfacial processes
- LiC_6 basal plane negatively charged, edge planes depend on Li content
- PF_6^- reduction on graphite edge incurs high barrier at right potential
- Applications to insulating electrodes, aqueous systems, fuel cells?

Are there easier ways to do this?



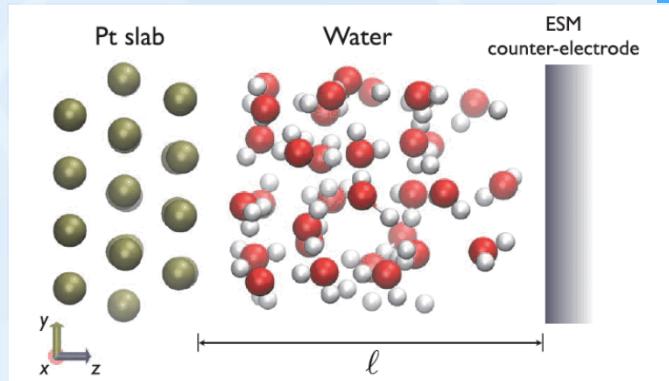
First-Principles Molecular Dynamics at a Constant Electrode Potential

PRL 109, 266101 (2012)

PHYSICAL REVIEW LETTERS

Nicéphore Bonnet,^{1,2} Tetsuya Morishita,¹ Osamu Sugino,² and Minoru Otani¹

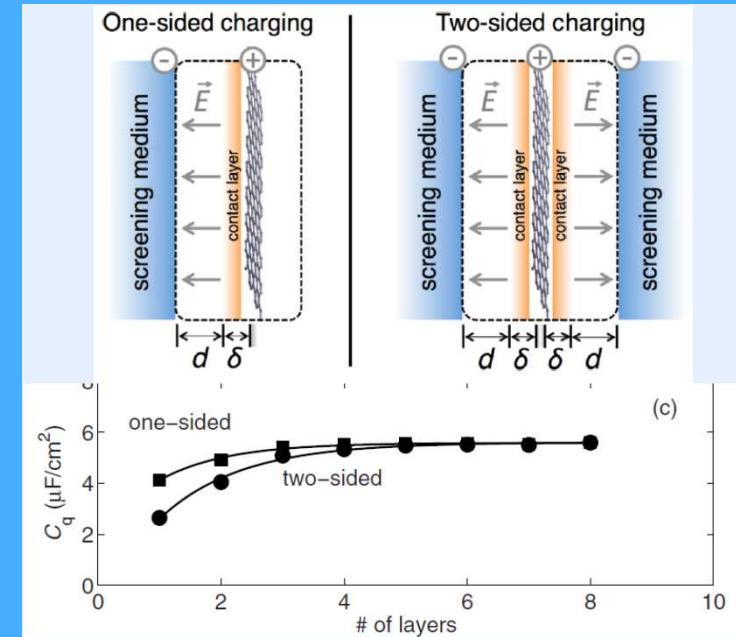
$$\dot{n}_e = \frac{P_{n_e}}{M_{n_e}}, \quad \dot{P}_{n_e} = F_e = \Phi - \Phi_{\text{pot}},$$



Capacitive charge storage at an electrified interface investigated via direct first-principles simulations

Maxwell D. Radin,^{1,*} Tadashi Ogitsu,² Juergen Biener,² Minoru Otani,³ and Brandon C. Wood^{2,†}

PHYSICAL REVIEW B 91, 125415 (2015)



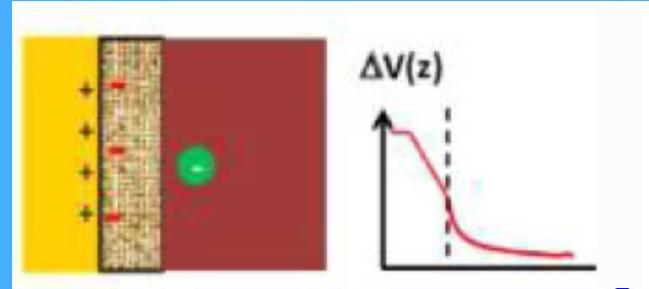
(see also “joint-DFT, which treats the entire liquid as a continuum)

- jDFT not yet calibrated for battery materials/electrolytes
- Li^+ concentration on/near electrode surfaces – major issues
- main issue: they don't yet include EDL contributions inside solids



Solid-solid interface contribution to Electric Double Layer

- In all-solid batteries, this is all there is
- In liquid electrolyte batteries, there are still solid-solid interfaces ("SEI")
- How much of the EDC is from solid-solid and solid-liquid interfaces?
- What are the consequences? (SEI evolution, Li^+ transport ...)



- we don't know the answers
- have barely started asking the right questions



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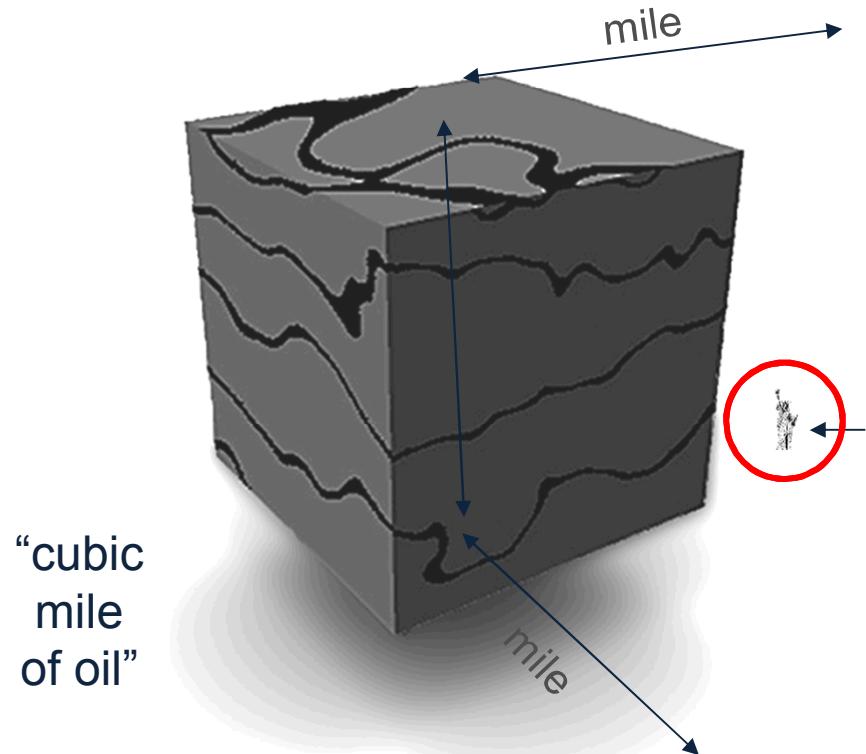
REMINDER: In fairness to all potential authors, late abstracts will not be accepted.

Symposium EN1: Solid-Solid Interfaces in Batteries, Energy Storage and Conversion—Diagnostic and Modeling

Bruce Dunn, Yoshitaka Tateyama, Yue Qi, KL



Energy, climate change, human development





Backup slides