

Metal Oxides in Solar Thermochemical Cycles: Gaining Breathing Room Through Reactor Design

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Outline

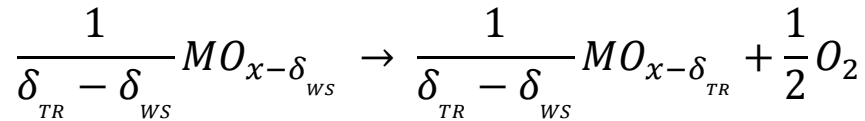
- **Materials role and requirements in two-step cycles**
- **Key efficiency drivers**
- **Achieving low thermal reduction pressure**
- **Electrically forcing reduction and water splitting**
- **Increasing temperature**
- **Fantasy materials**

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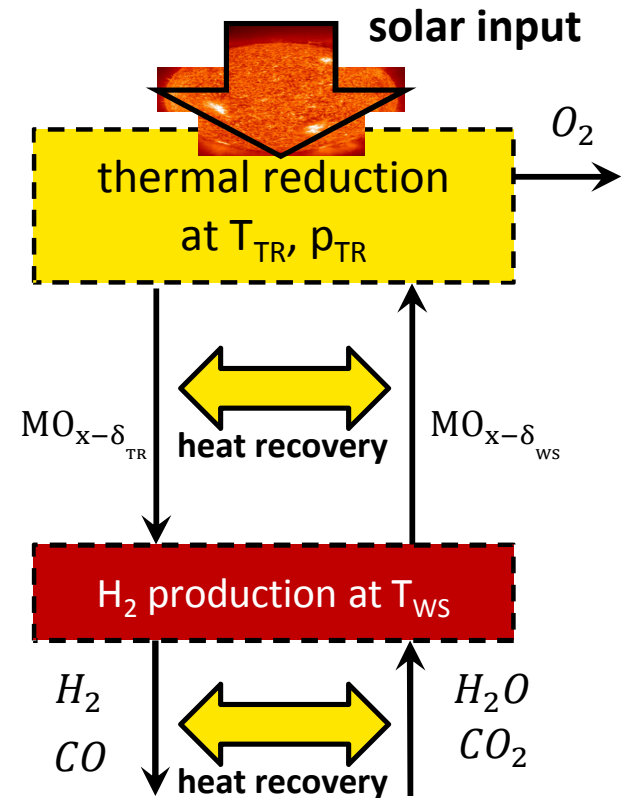
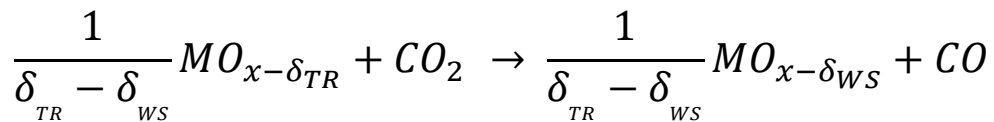
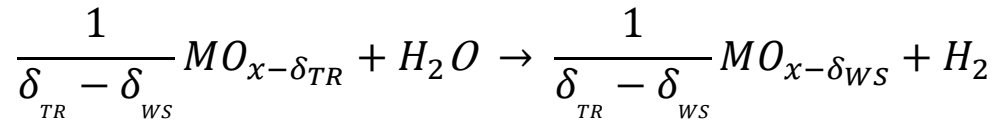
Two-Step Thermochemical Fuel Production

A theoretically simple process

Thermal reduction

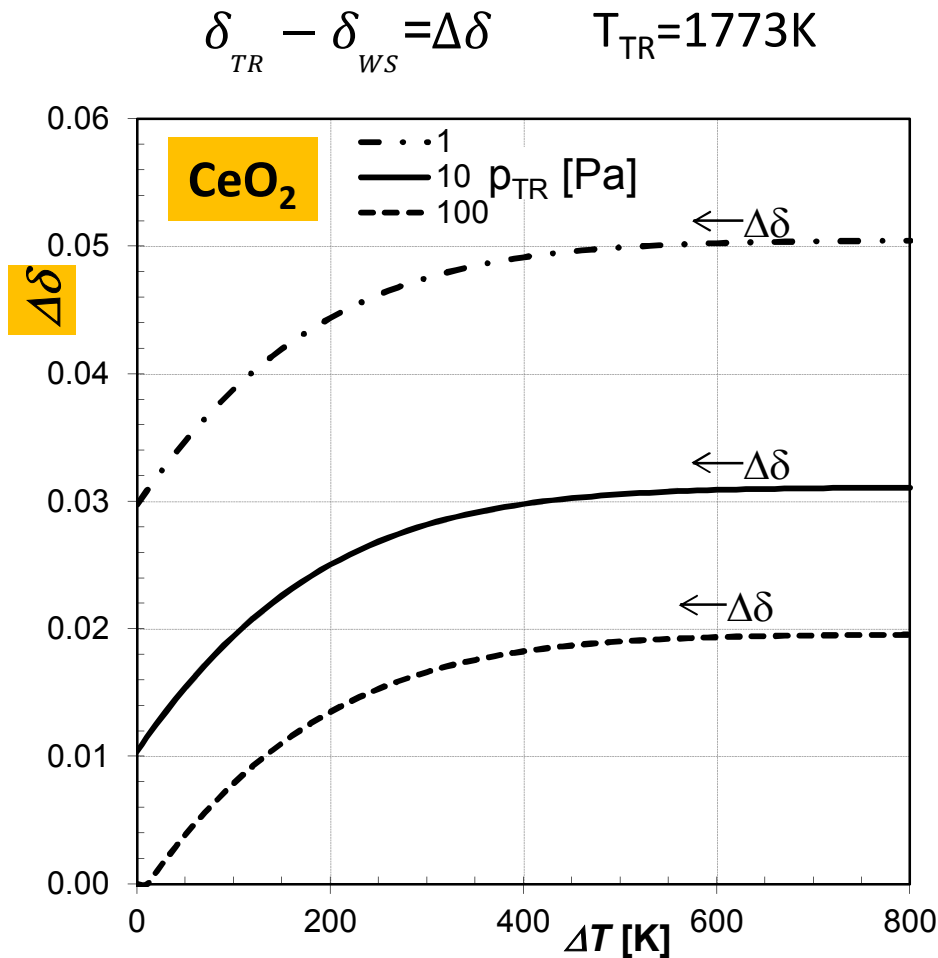


Water/CO₂ splitting

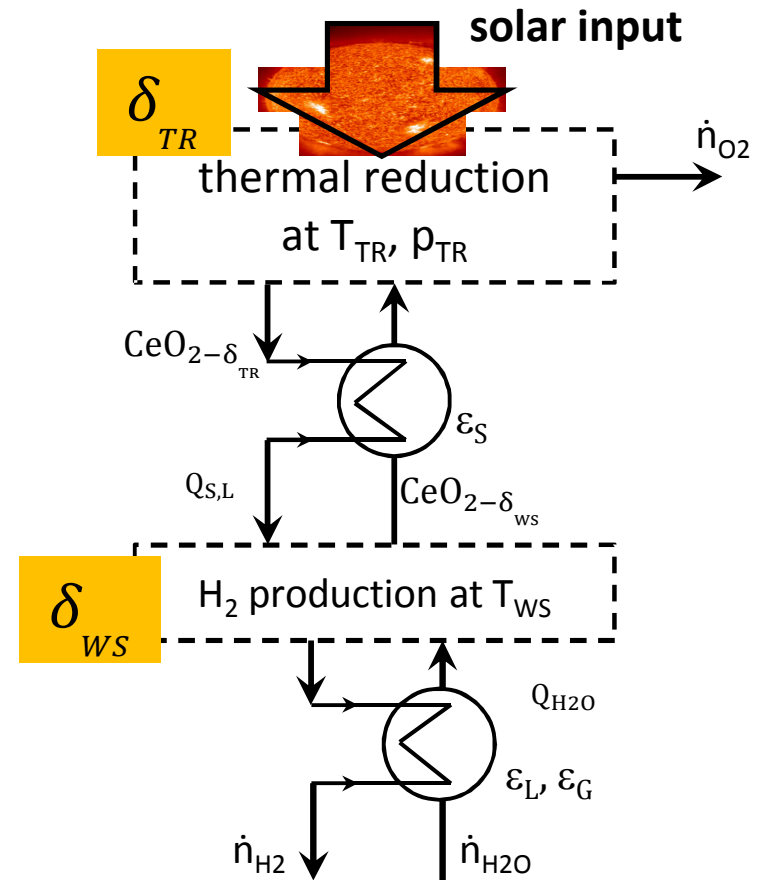


Key Material Requirements: Reactive Oxide

How much CeO_2 per mole H_2 ?

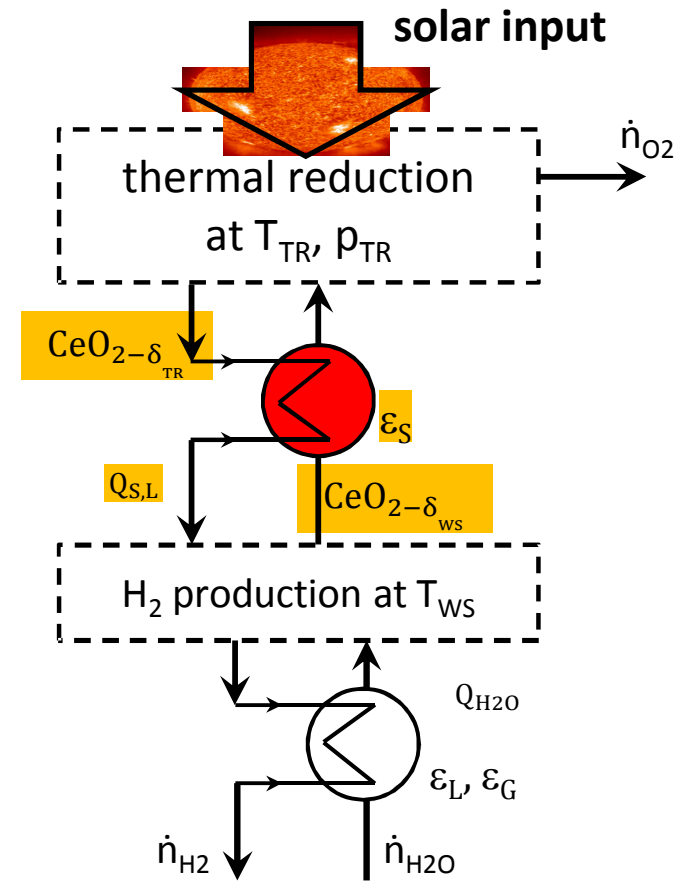
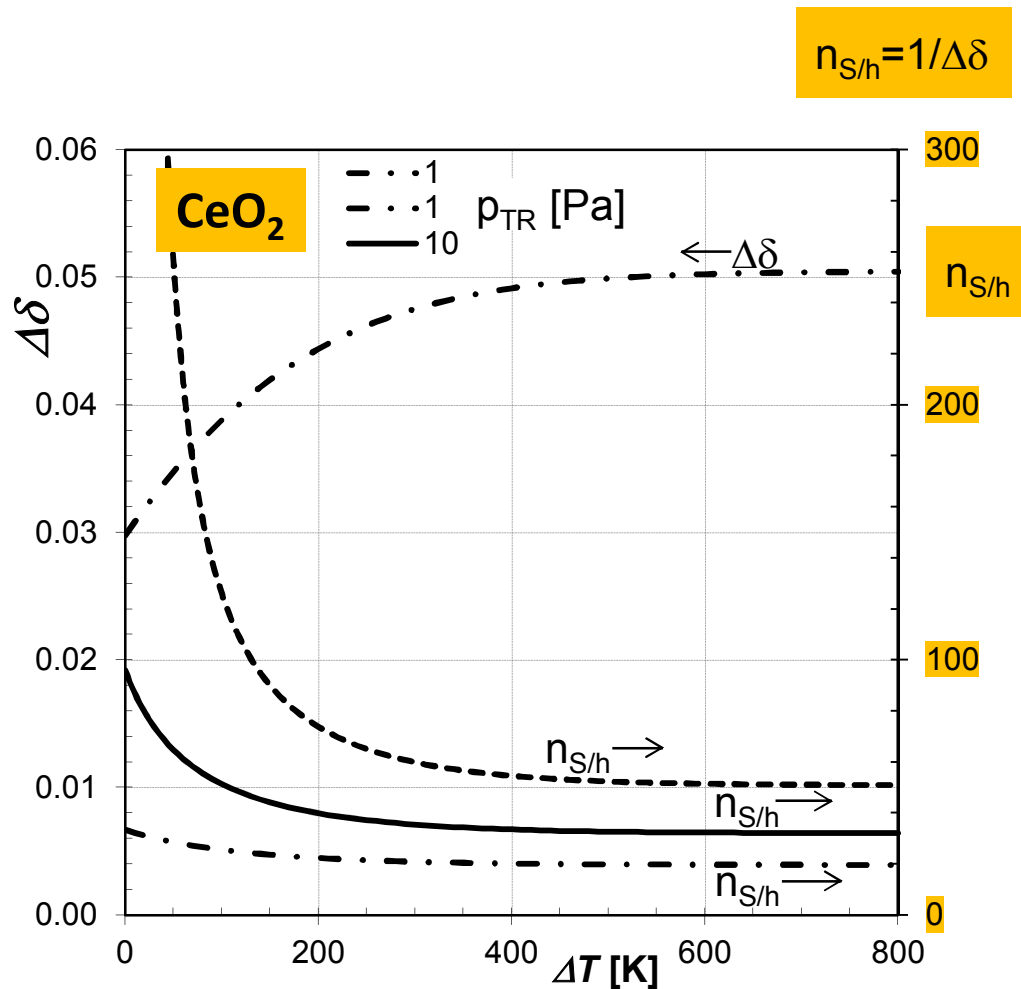


The reversible oxygen capacity can be very low!



Key Material Requirements: Reactive Oxide

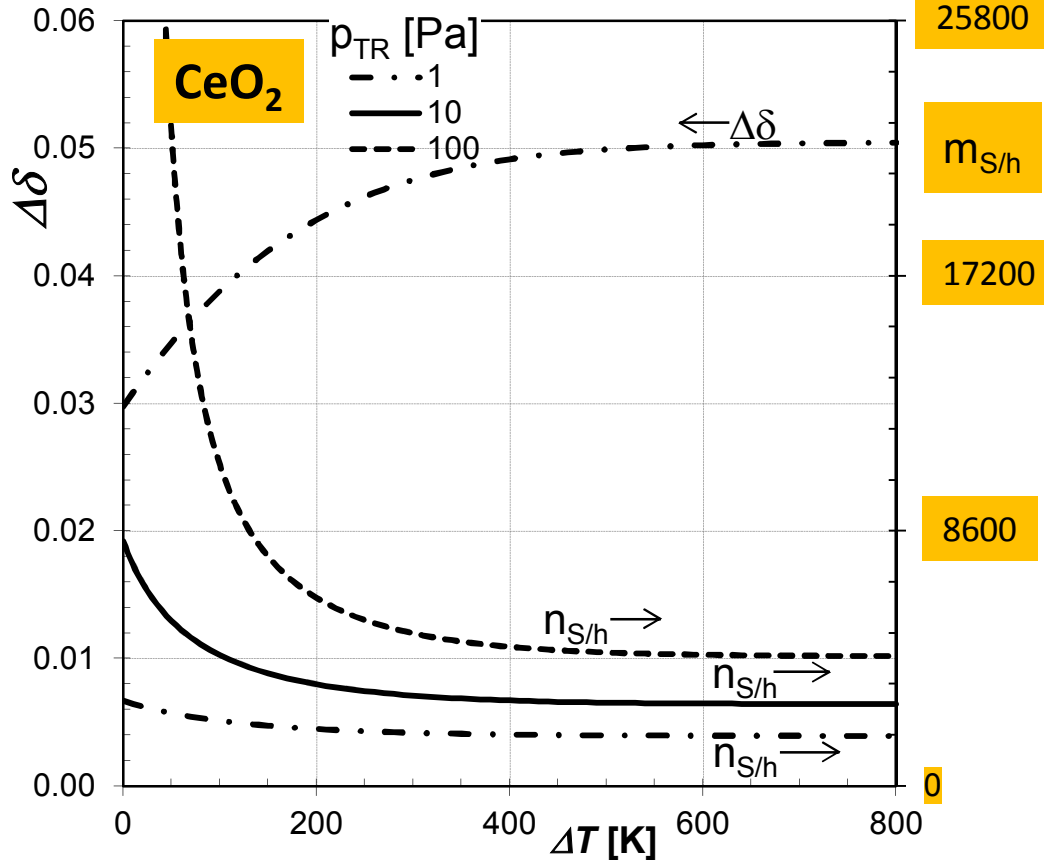
How much CeO_2 per mole H_2 ?



A low reversible oxygen capacity leads to a very high oxide/ H_2 ratio and excessive oxide mass flow and heat recovery requirements

Key Material Requirements: Reactive Oxide

How much CeO_2 per mole H_2 ?



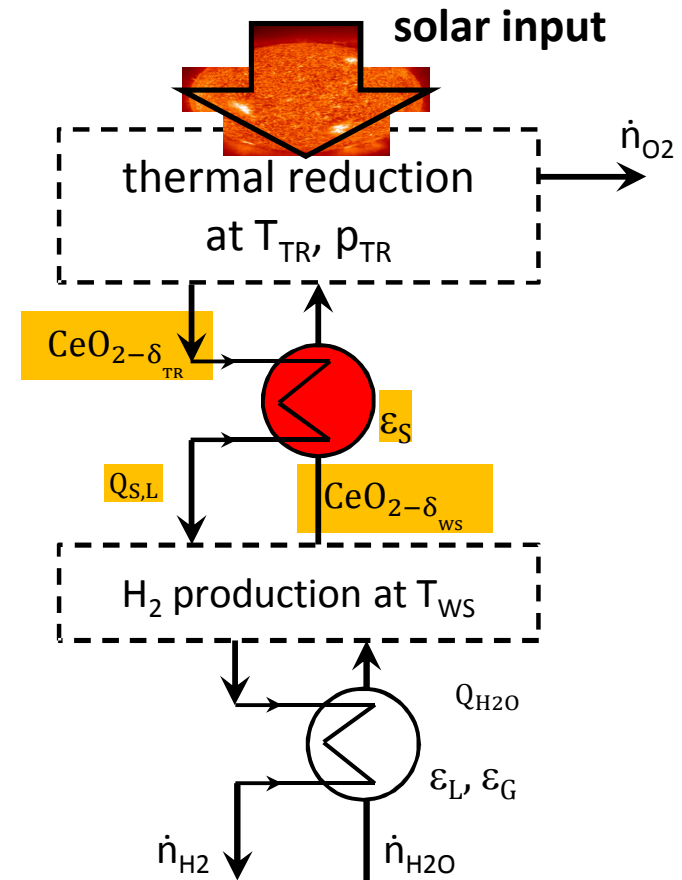
25800

$m_{\text{S/h}}$

17200

8600

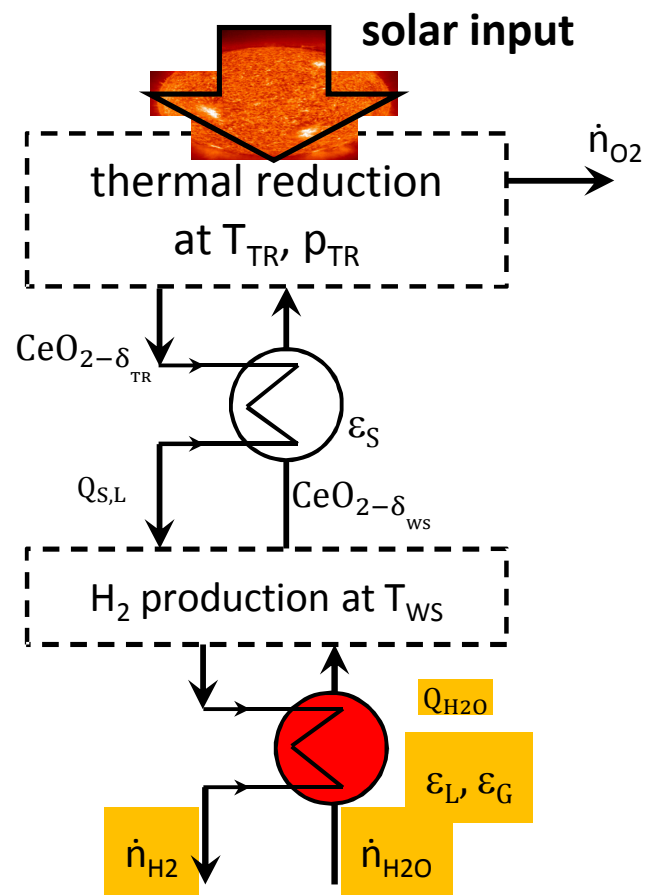
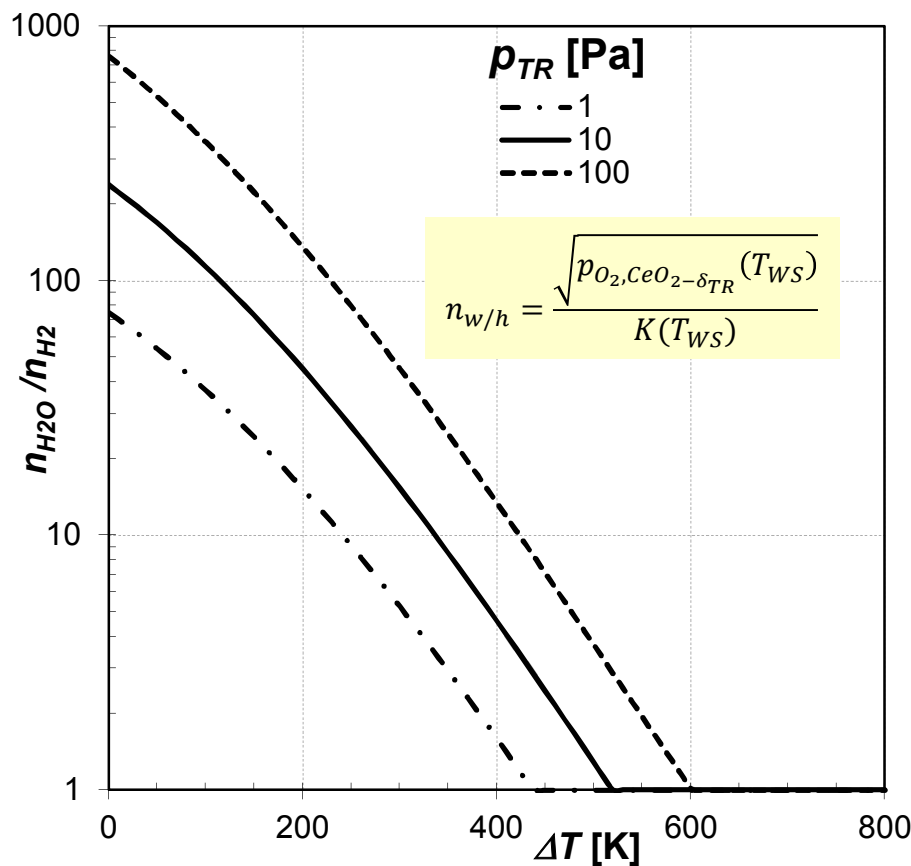
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A low reversible oxygen capacity leads to a very high oxide/ H_2 ratio and excessive oxide mass flow and heat recovery requirements

Key Material Requirements: Steam

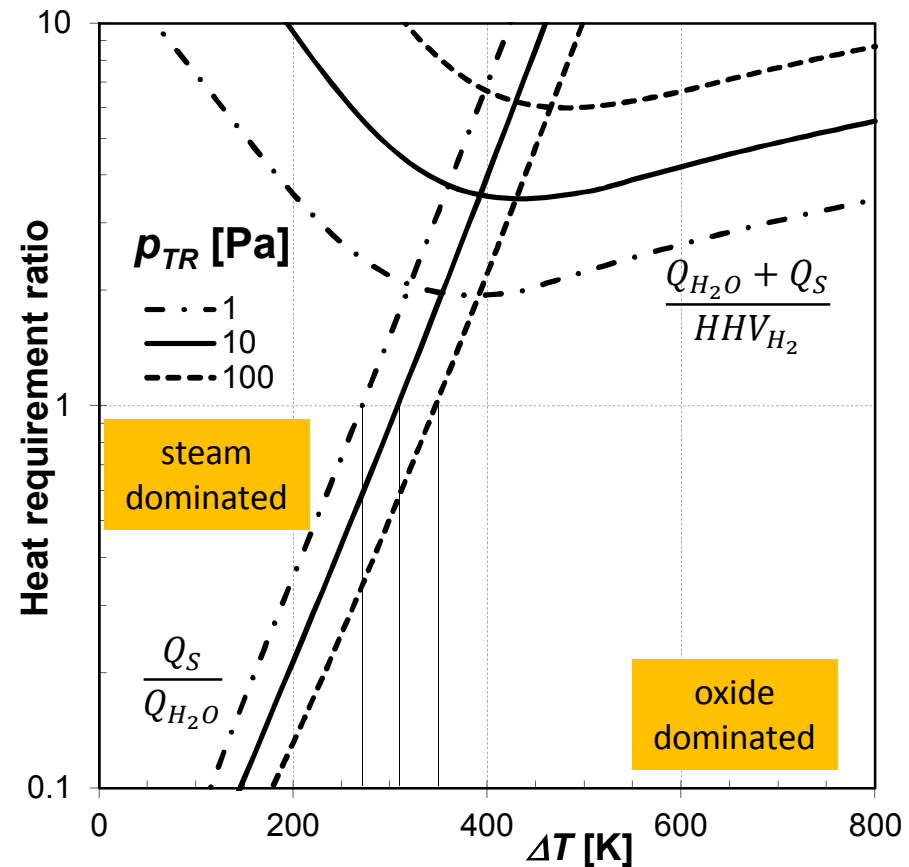
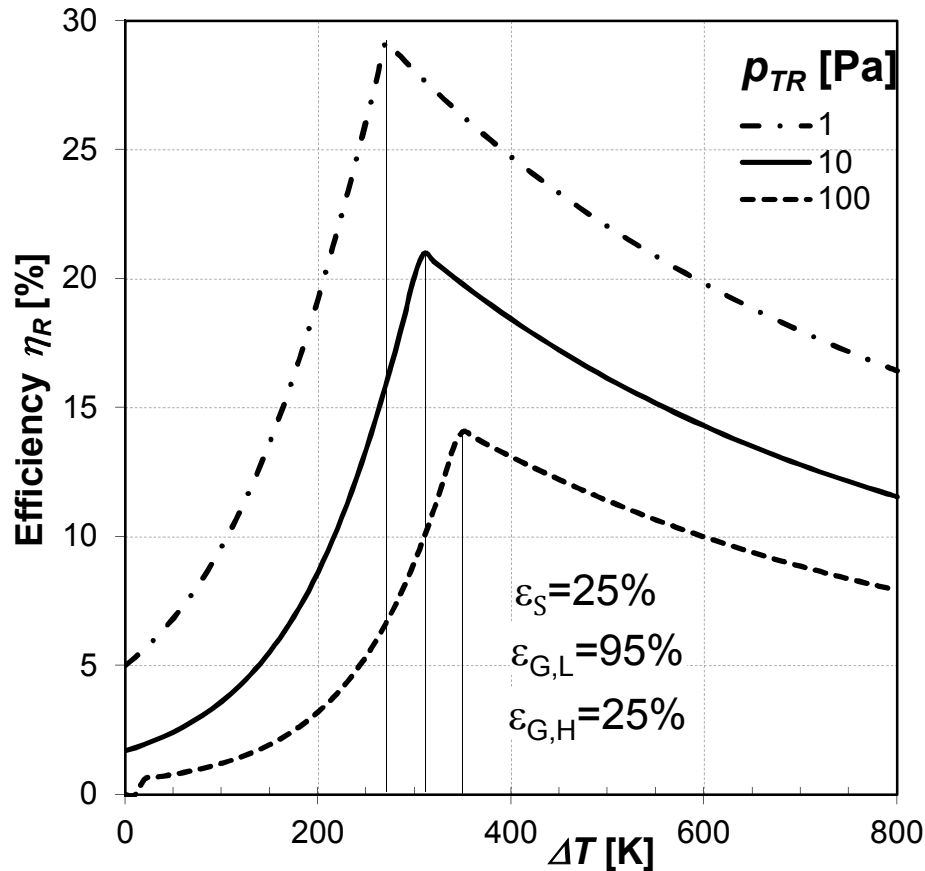
How much steam per mole H_2 ?



Low ΔT or high reduction pressure leads to a high steam/ H_2 ratio

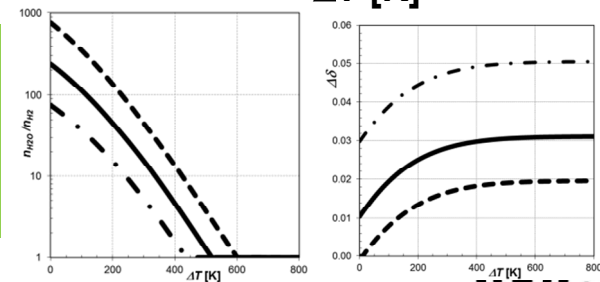
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Maximizing Efficiency: Solid/Steam Heating Balance and a Low Reduction Pressure



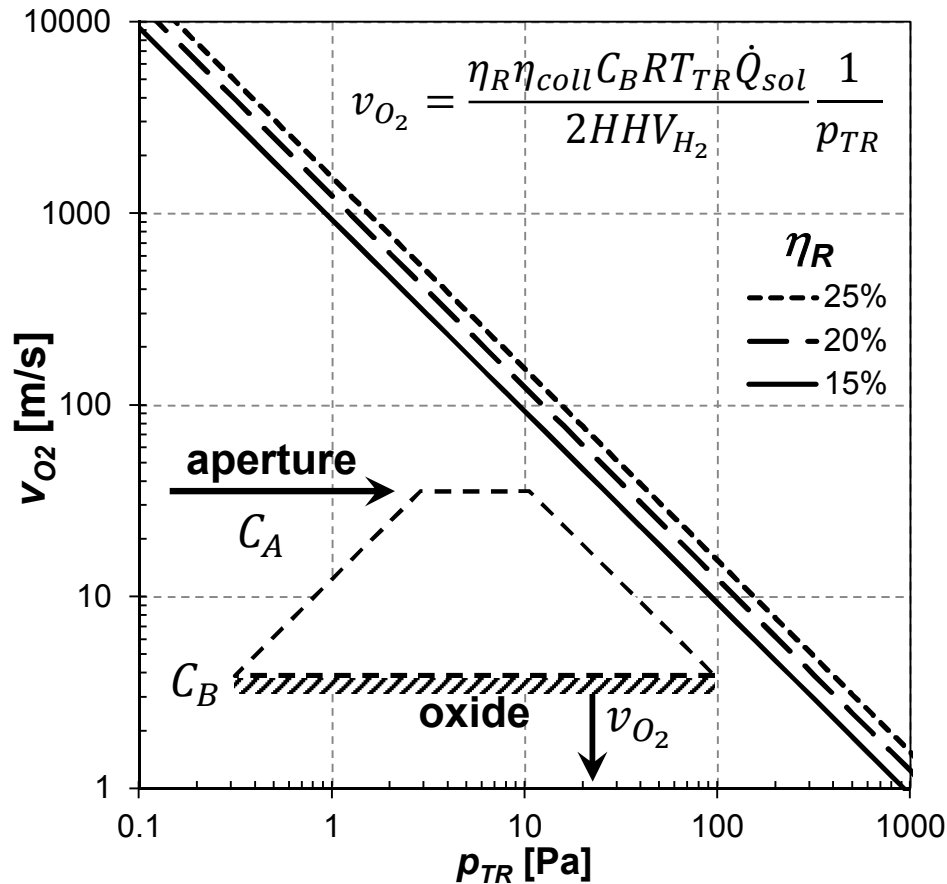
Efficiency is the highest when:

- Oxide and steam heating loads are roughly equal
- Thermal reduction pressure is low

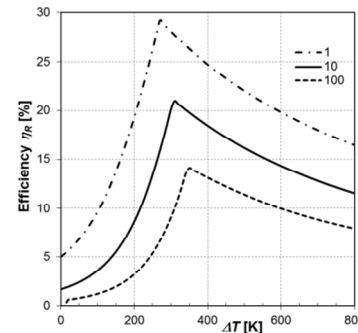
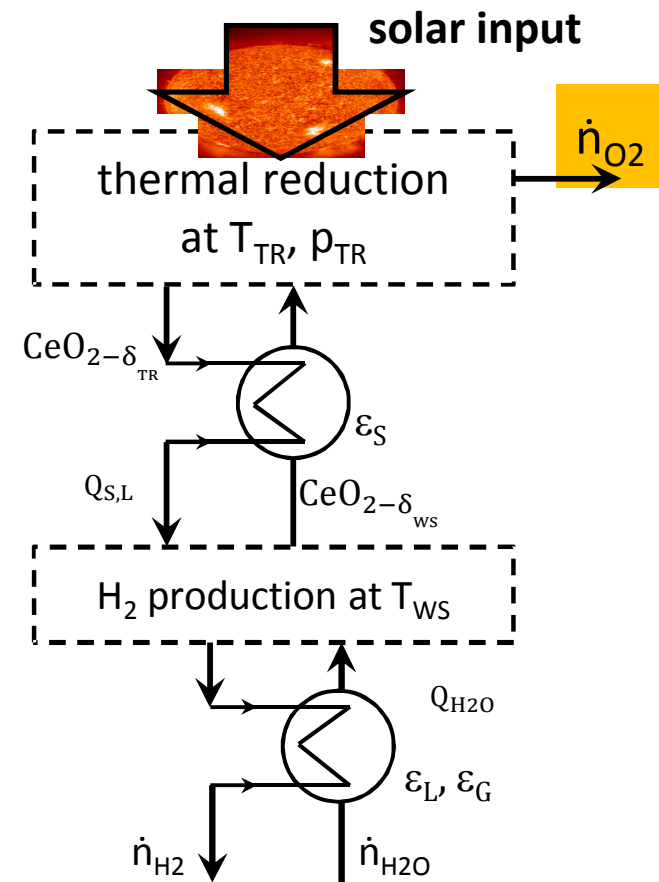


O₂ Pressure Limits: Flow Volume and Speed

Is 1Pa accessible?

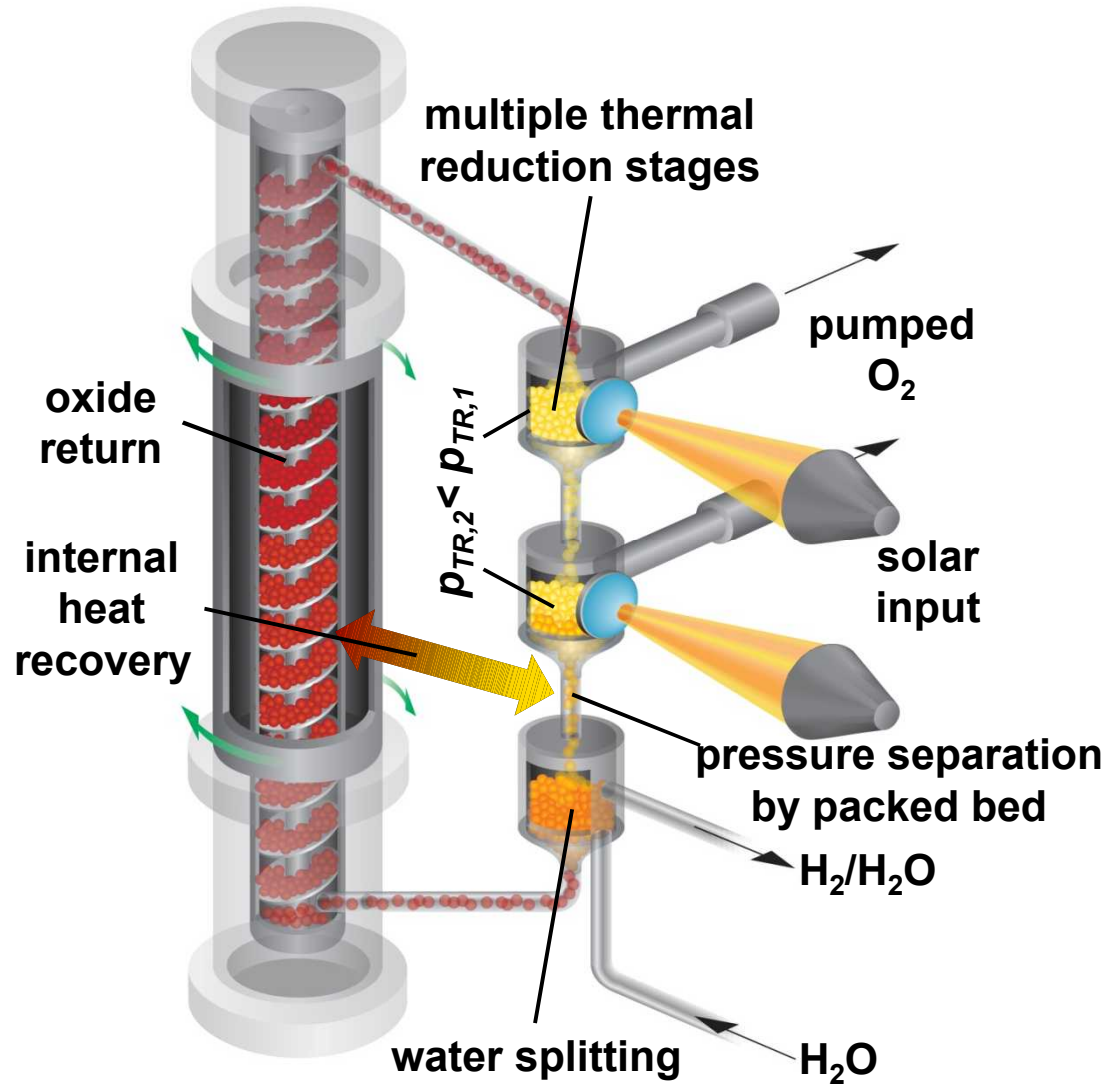


At low pressure required flow volumes and velocities are astronomical!



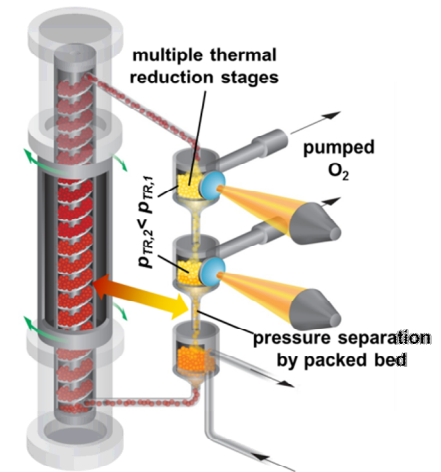
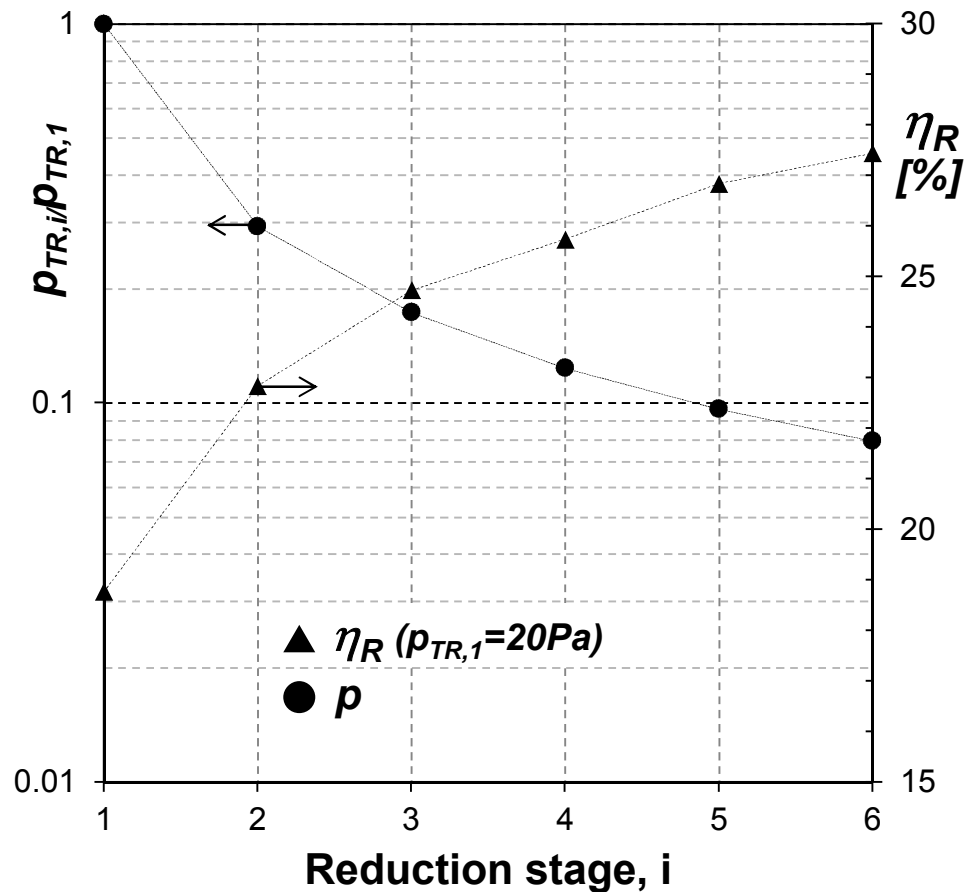
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Staged Reduction Reactor for Low Pressure



Incrementally pumping O_2 reduces the overall flow volume and velocity

Staged Reduction for Low Pressure

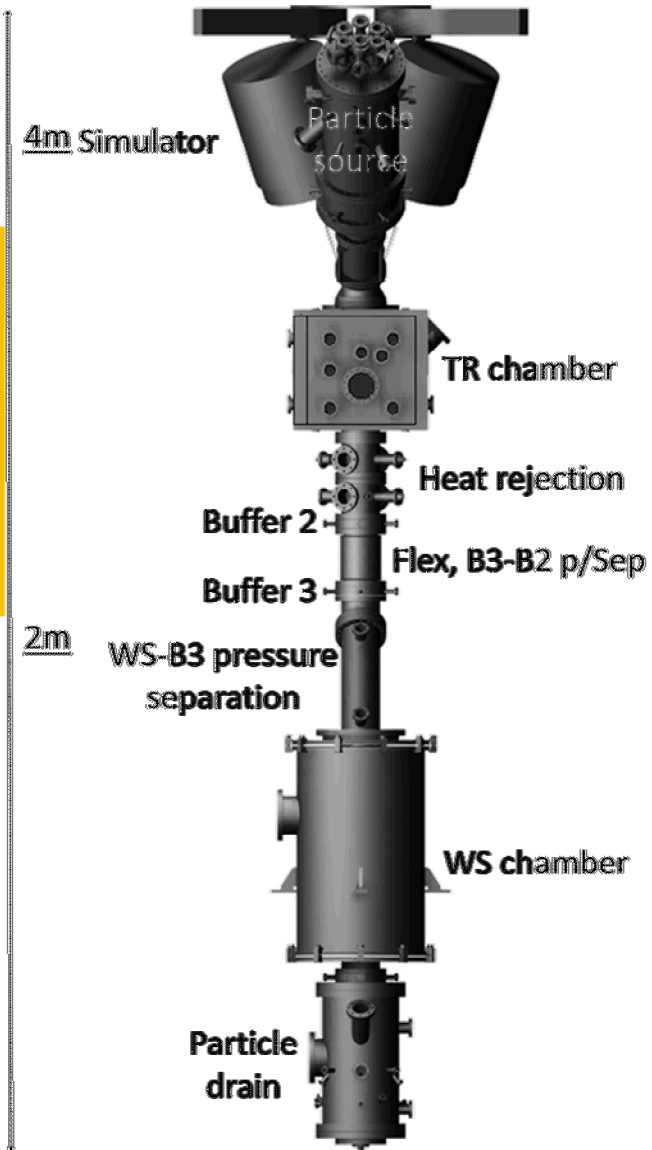
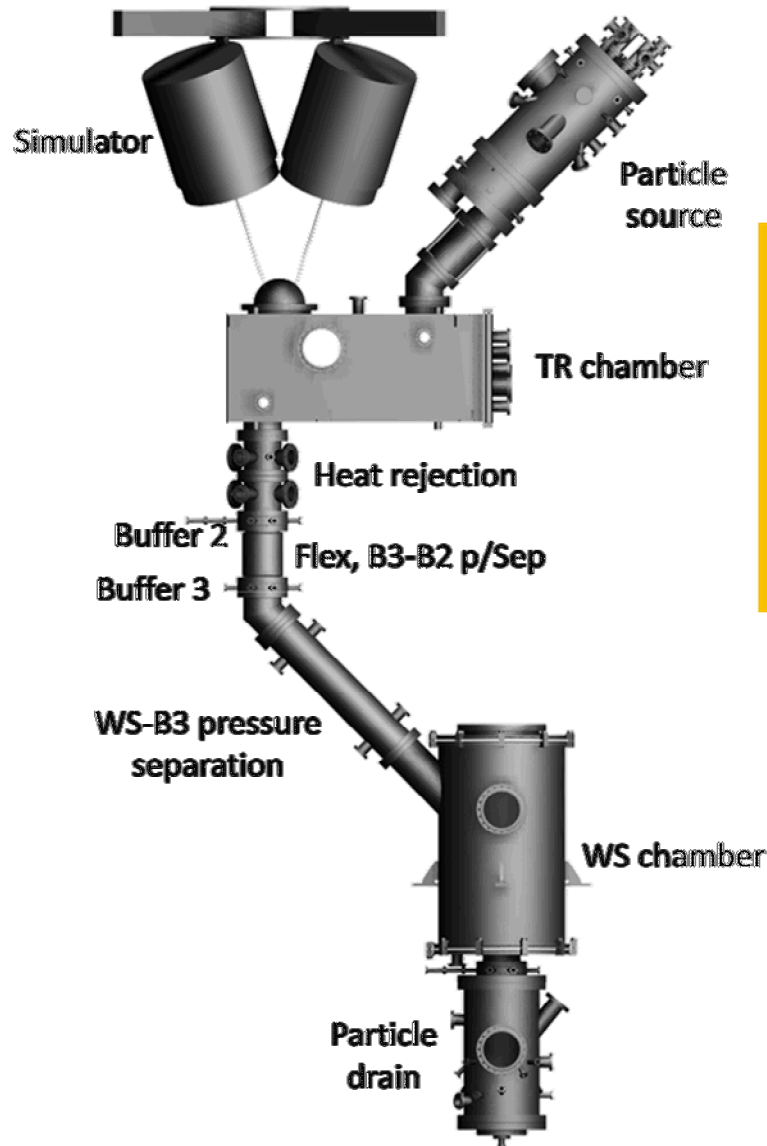


$$p_{TR,i} = \dot{n}_{ox} R T_{TR} \frac{\delta_{TR,i} - \delta_{TR,i-1}}{2 \dot{V}_{O_2}}$$

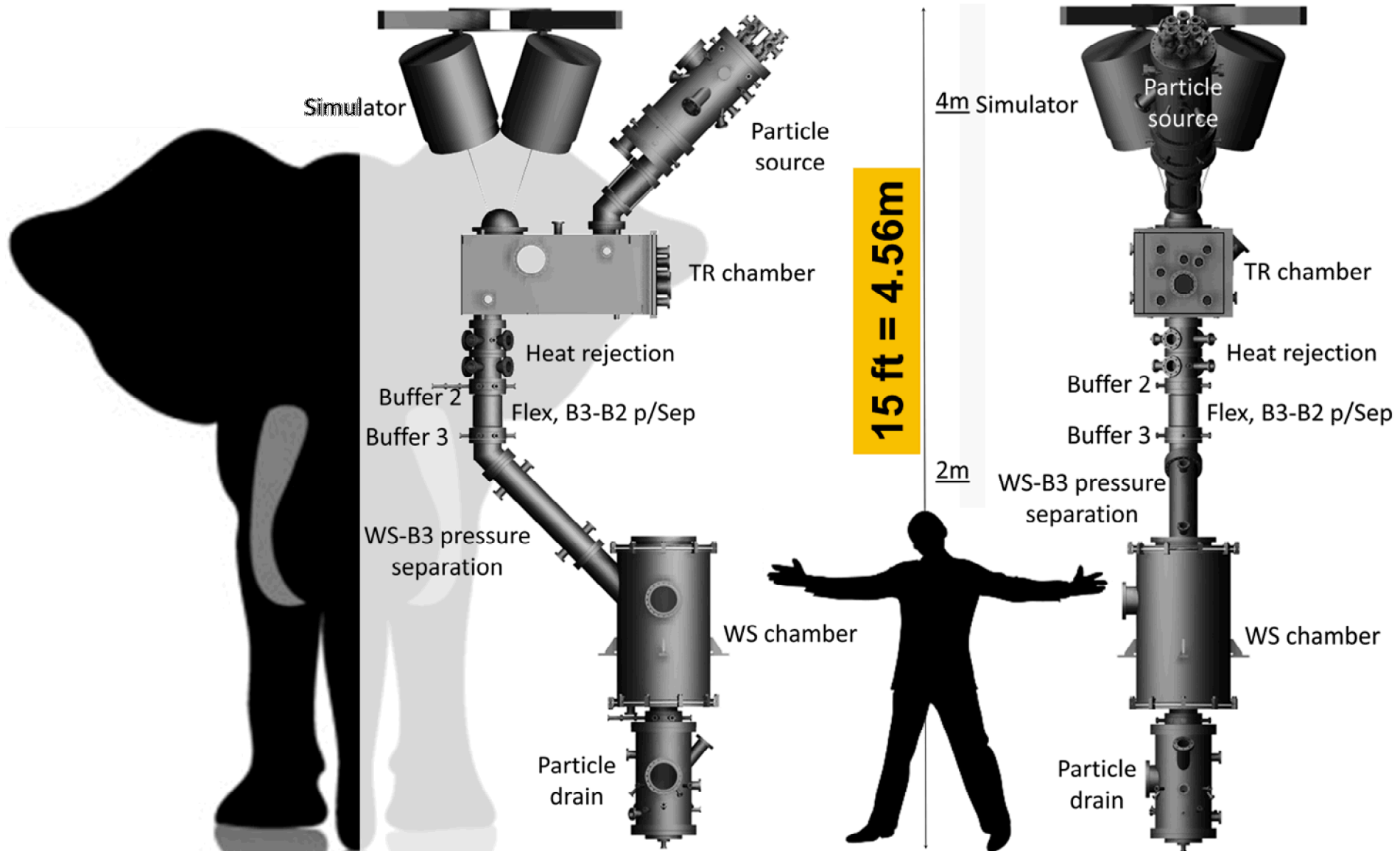
Efficiency is the highest when:

- 10x pressure decrease possible with as few as 5 chambers
- Decreased pump work and size

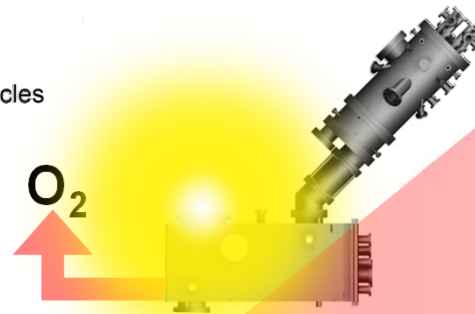
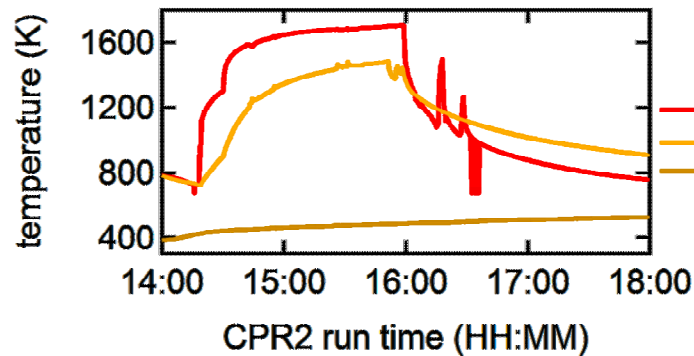
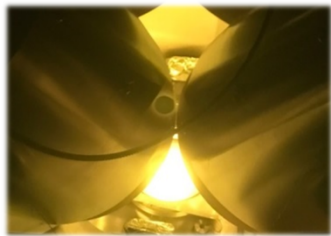
Vacuum and Staged Reduction in Practice



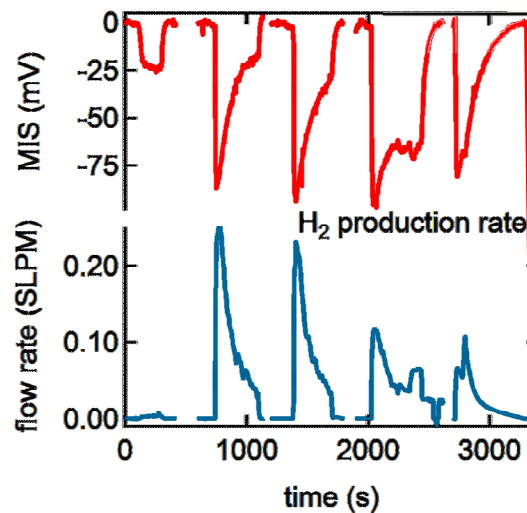
Vacuum and Staged Reduction in Practice



Vacuum and Staged Reduction in Practice

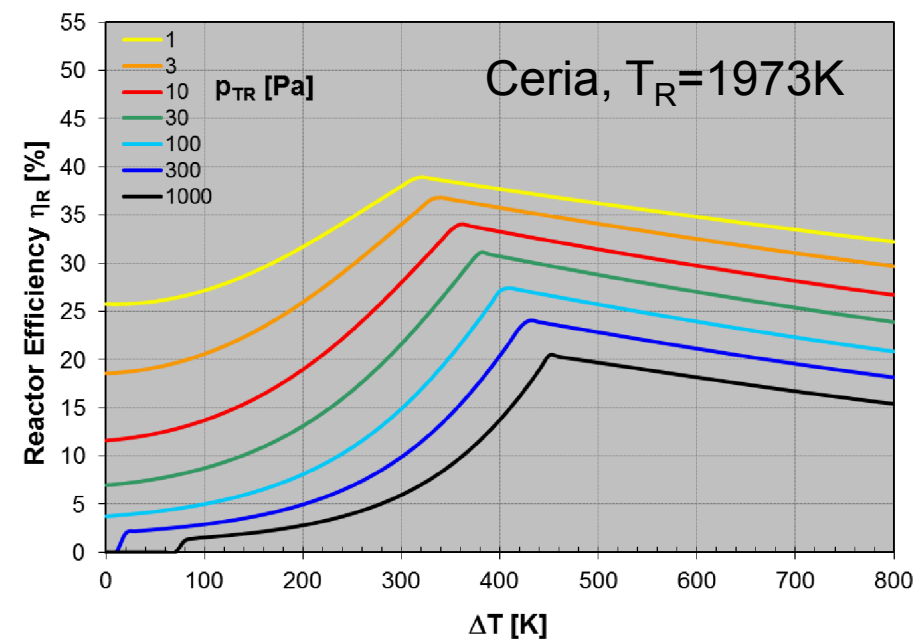
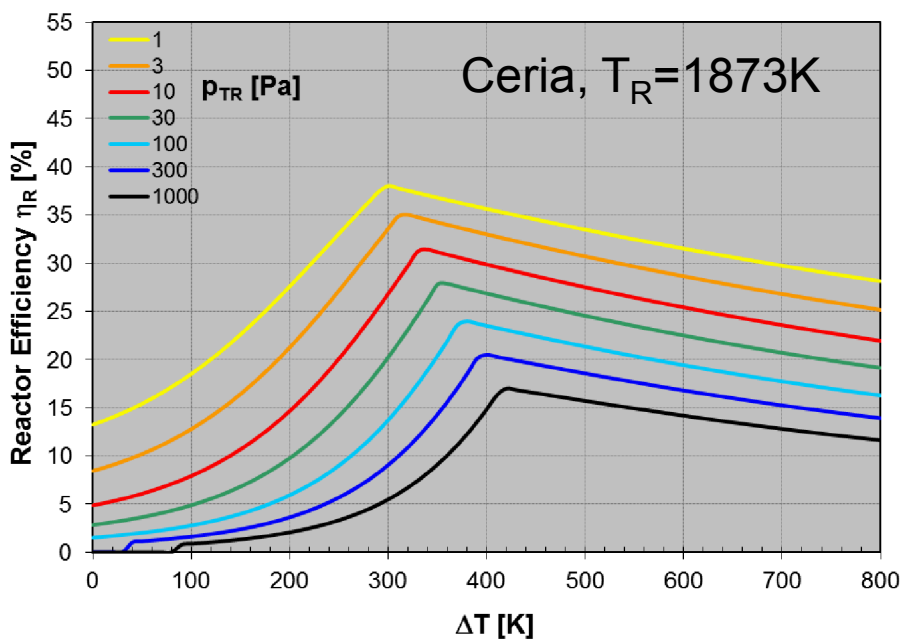
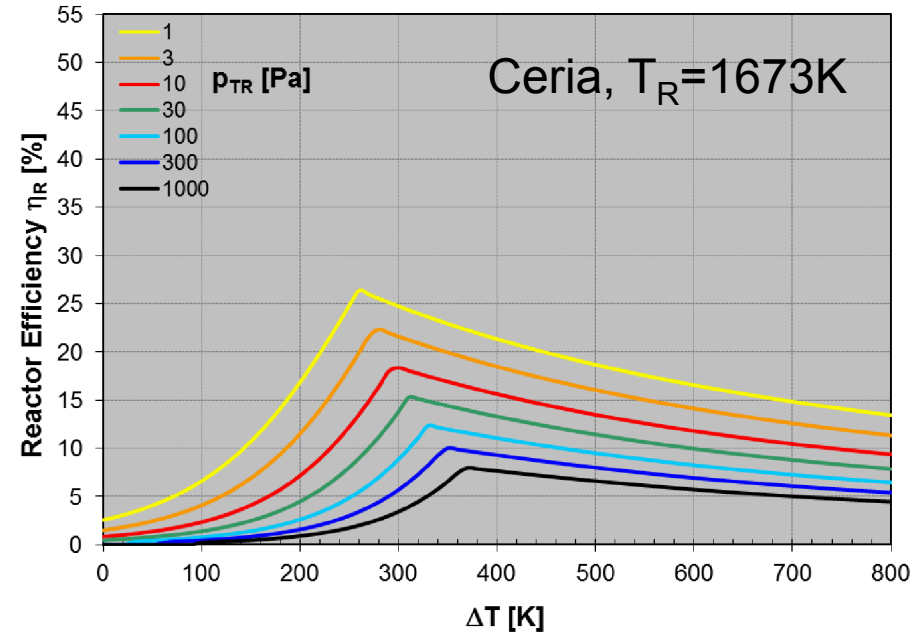
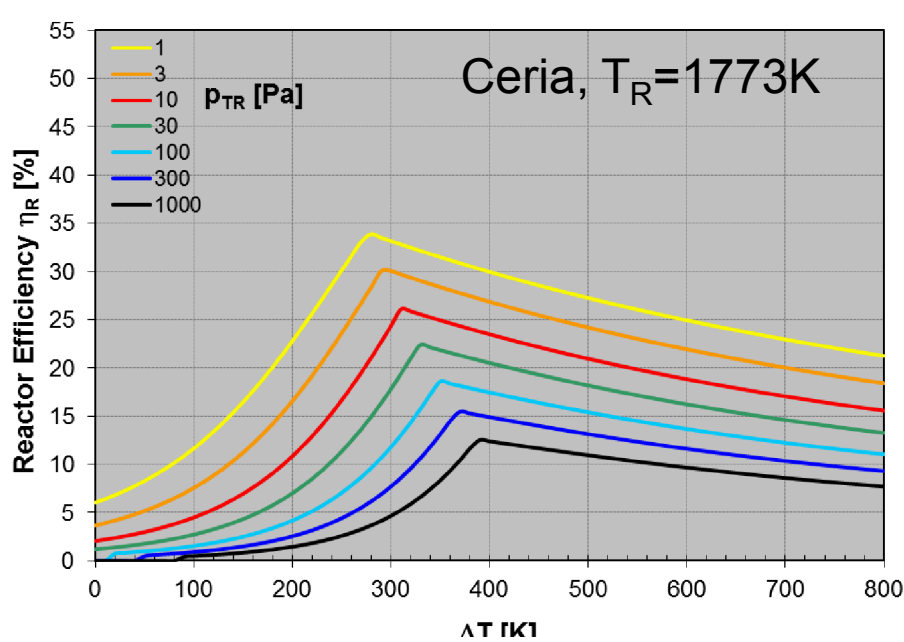


$T_R \sim 1700 \text{ K}$
0.25 SLPM peak H₂ rate



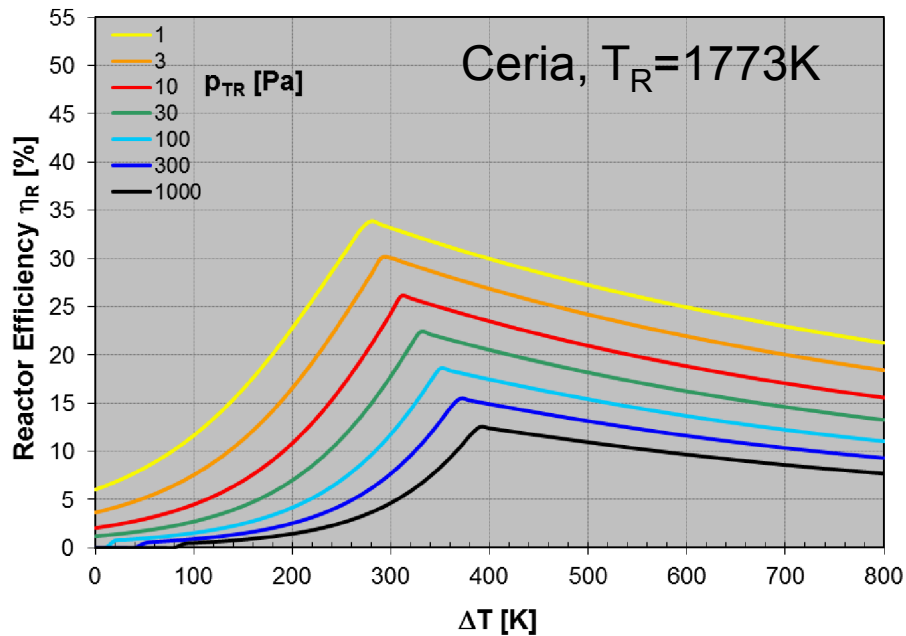
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Playing With Reduction Temperature



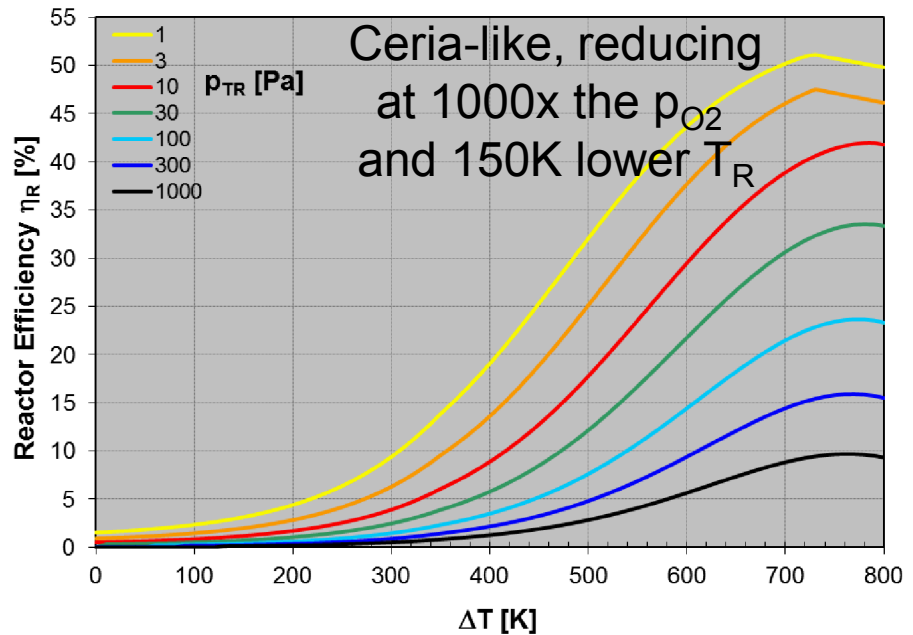
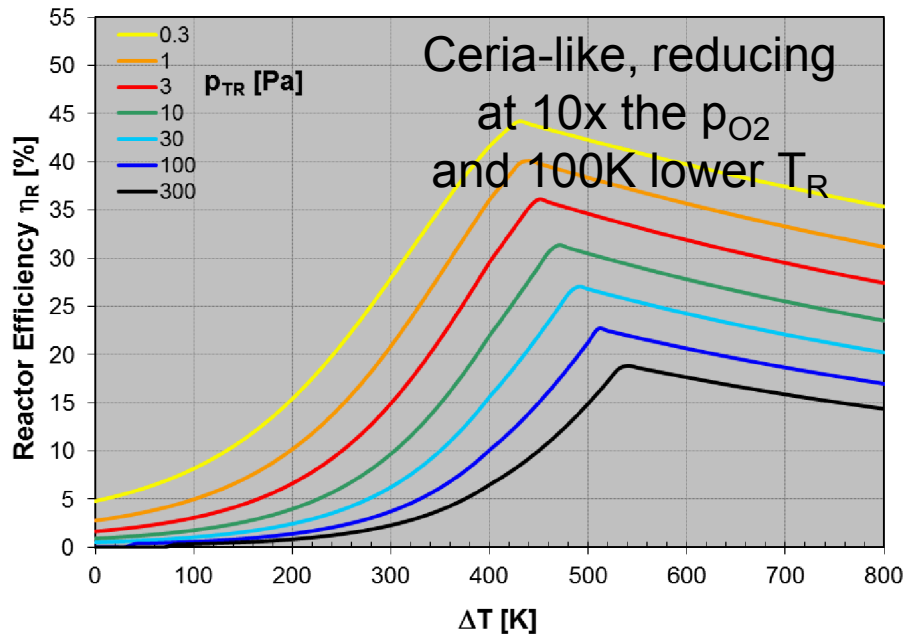
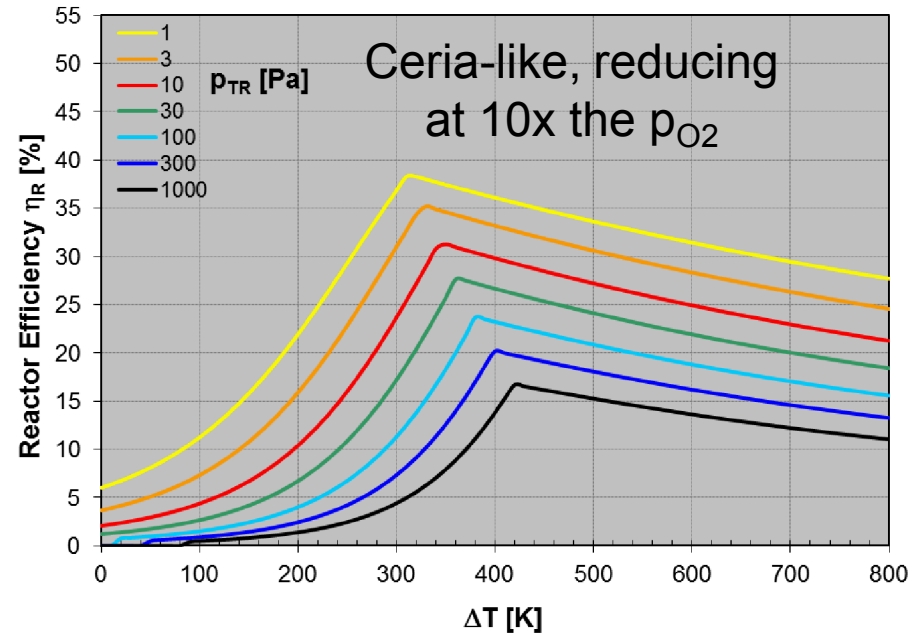
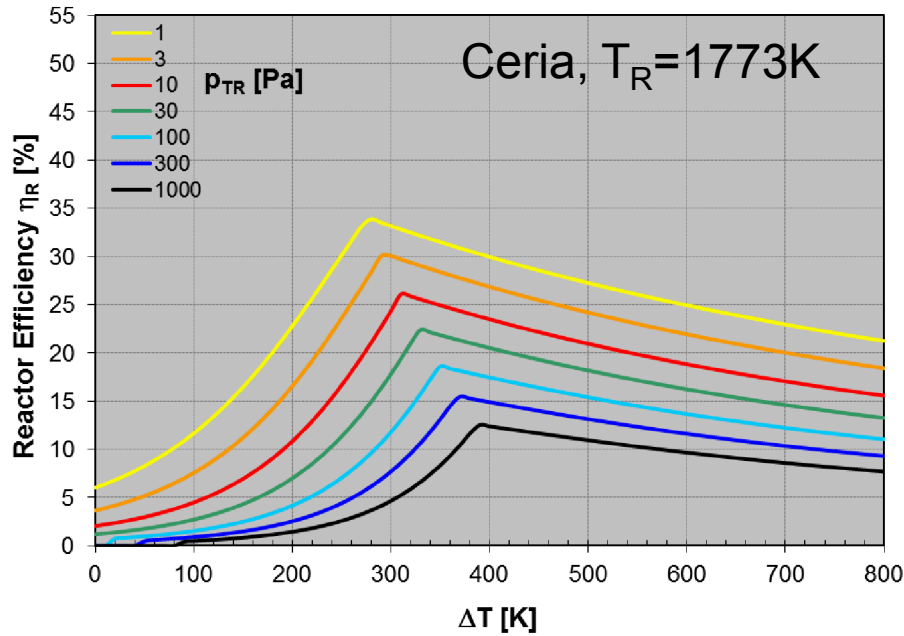
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Playing With Materials Properties

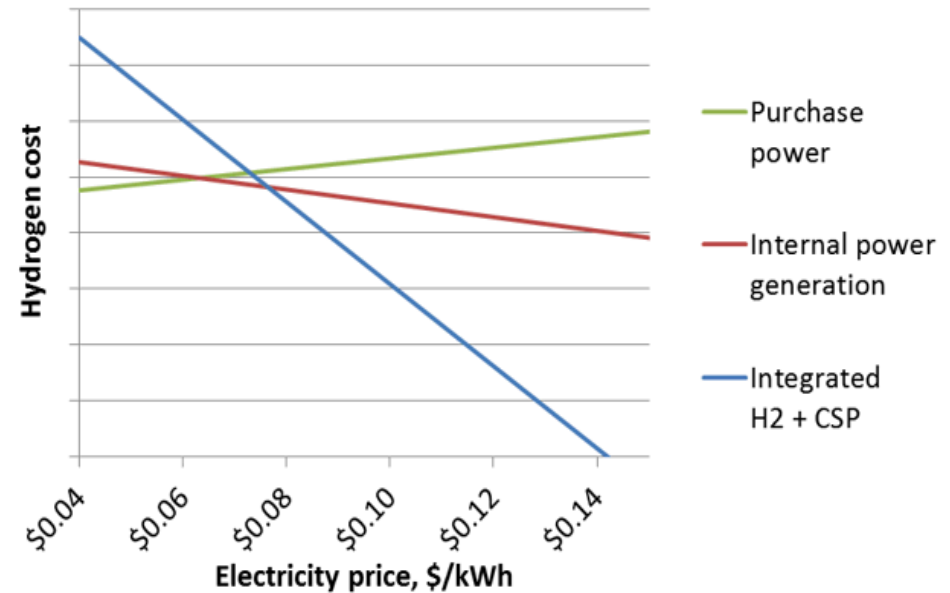
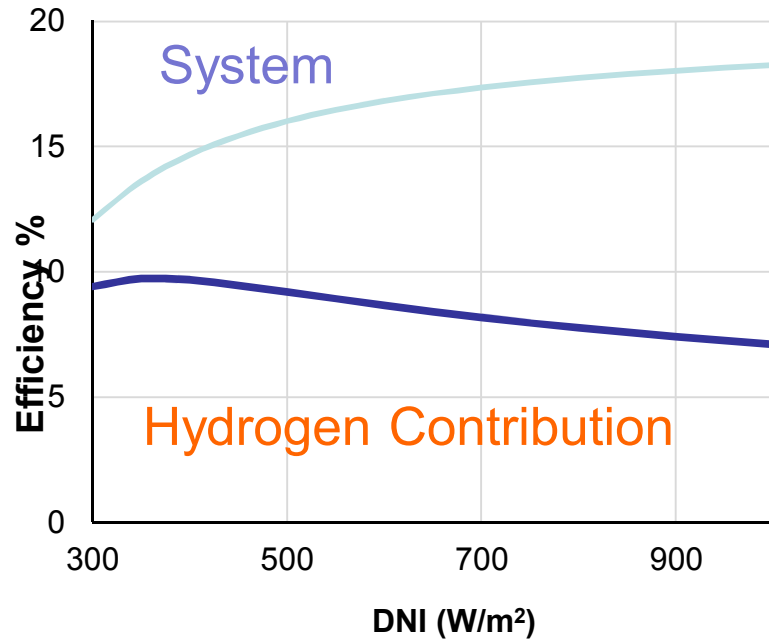


Family of efficiency curves for a CeO_2 reactor.

Playing With Materials Properties



Cogeneration



- Electricity production from waste heat can offset H_2 cost.
 - Ratio of H_2 :Electricity dependent on DNI
 - System efficiency is more complex
 - Impact of high-temperature waste heat amplified by integration with CSP

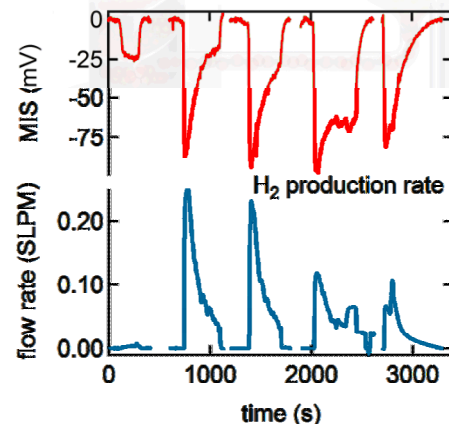
Summary/Interesting questions

- Materials with low $\Delta\delta$ pose a mass flow challenge
- Optimal ΔT can be found to maximize efficiency
- Thermal reduction pressure limited by O_2 flow
- A $>10\times$ pressure decrease feasible in staged reduction
- Best results by combining ΔT_{opt} , staged pumping and advanced reactive oxides
- Future advances in receiver technology for higher T_R ?
- Advanced materials?
- Cogeneration?



Thank You.

Questions?



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