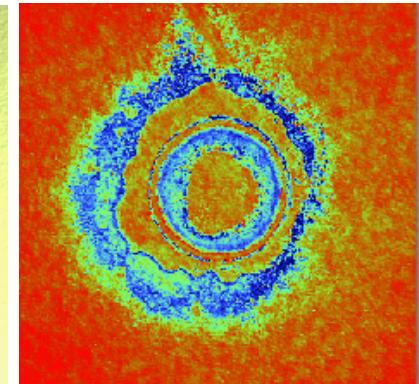
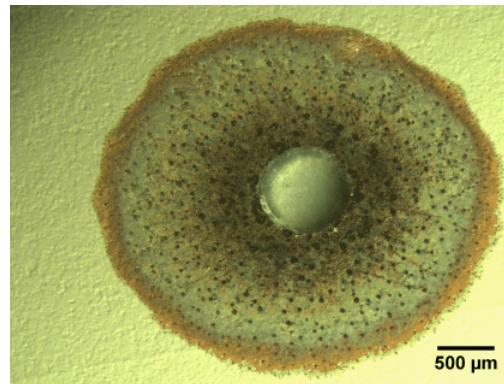
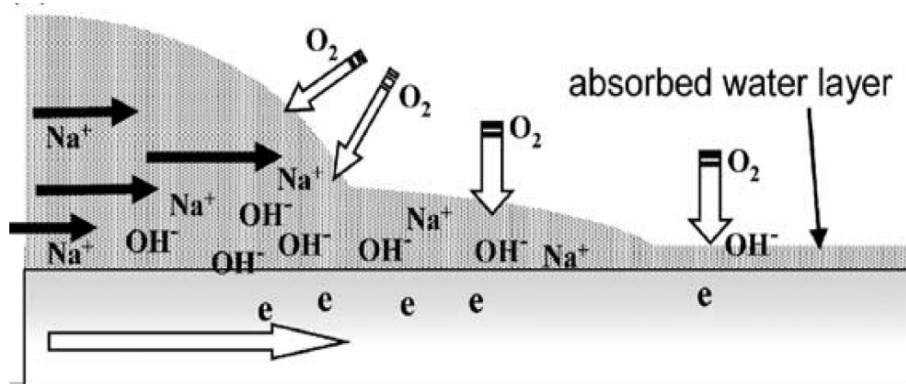


Exceptional service in the national interest



Role of Electrolyte Evolution on Damage Distributions and Rates Under NaCl Drops

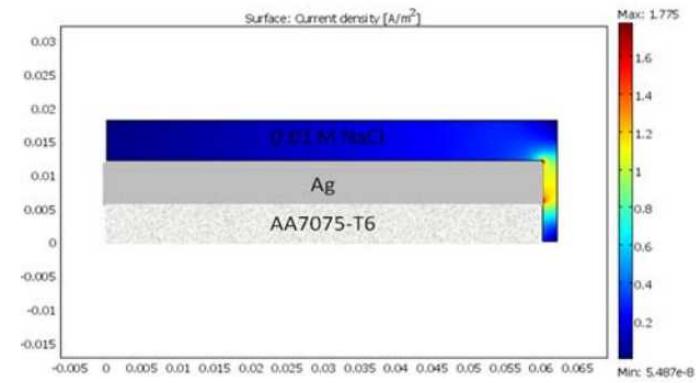
Eric Schindelholz, Harry Moffat, Rob Sorensen



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Electrochemical Modeling of Atmospheric Corrosion

- Electrolyte geometry can govern corrosion damage distributions and kinetics
- Limited experimental options for directly probing corrosion reactions hinders mechanistic insight
- Rich opportunity space for integrated computational and experimental approach



Shi, Kelly, 2013

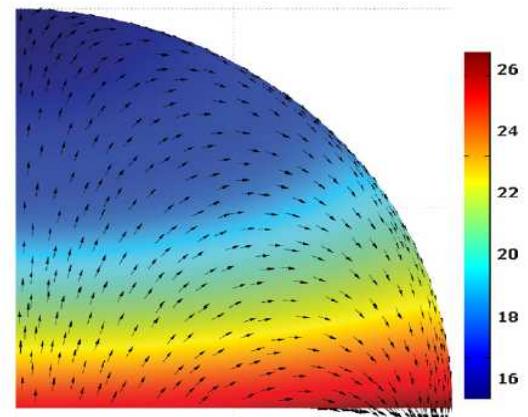


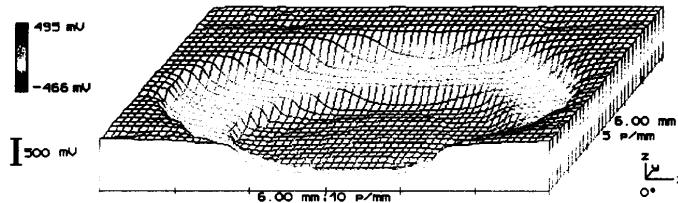
Fig. 10. $(C_{\text{Zn}^{2+}} / C_{\text{Zn}^{2+}}^0)$ of zinc ions and arrow plot of current density vectors showing separation of metal surface into anodic and cathodic regions over time.

Cole et al., 2011

Classic Understanding: Evans Drop

Differential Aeration Cell

Diffusion limited O_2 reduction kinetics control attack rate and damage distribution



Chen and Mansfeld, 1997

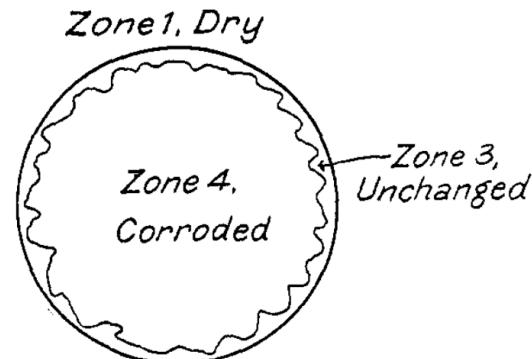
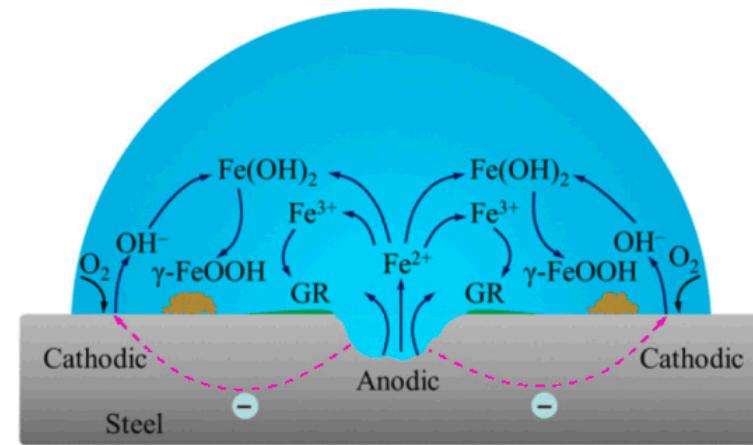


Figure 2—Effect of Drop of Distilled Water on Zinc

Evans, 1926



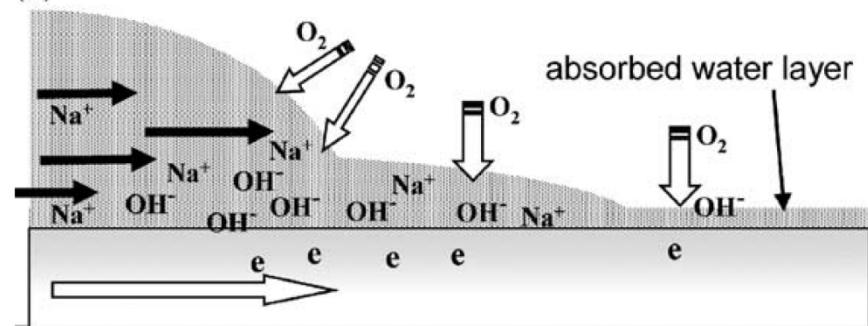
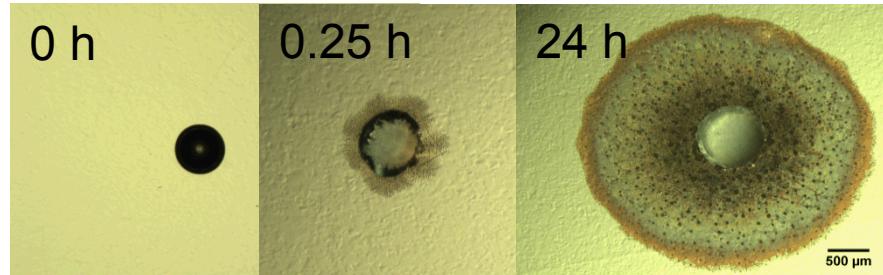
Li and Hihara, 2012

Divergence from Evans Drop

Secondary Spreading

rate and extent

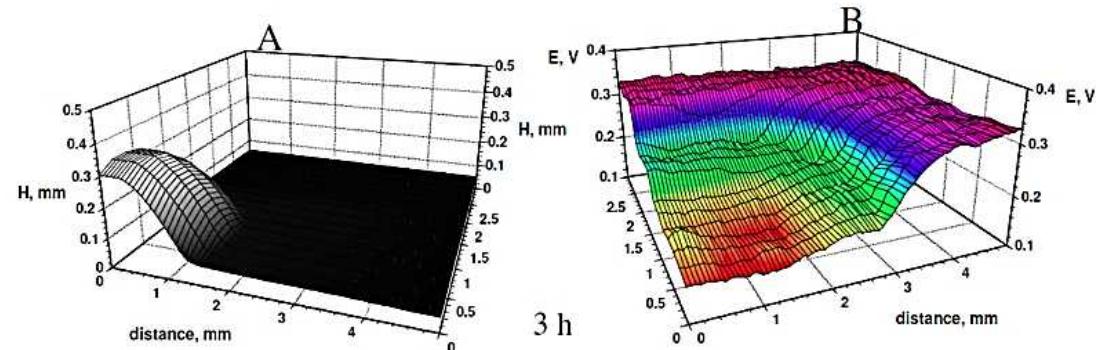
- initial drop size and chemistry
- substrate alloy
- environment (P_{CO_2} , RH)



Tsuru et al, 2004

Impact of Secondary Spreading

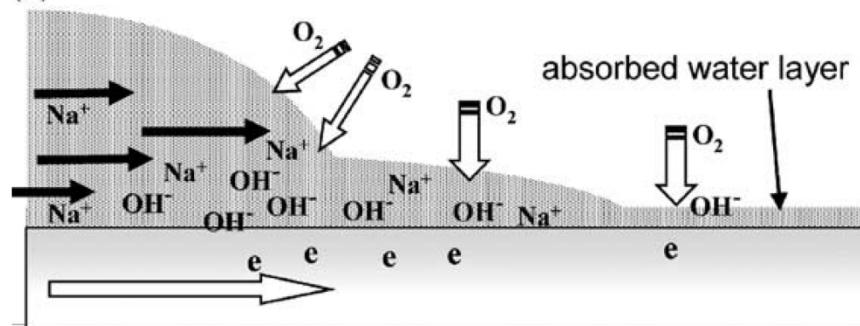
High potential areas in secondary spreading regions



$$I_{m,drop} = I_{O_2,drop} + I_{O_2,film}$$

Chen, 2005

To what extent do films contribute to cathodic current?



Study Framework

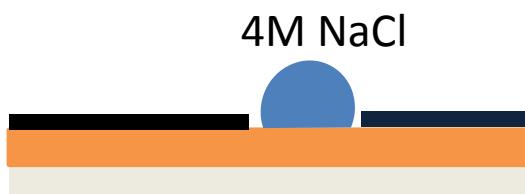
Driving Question

How do secondary films impact corrosion kinetics and damage distributions?

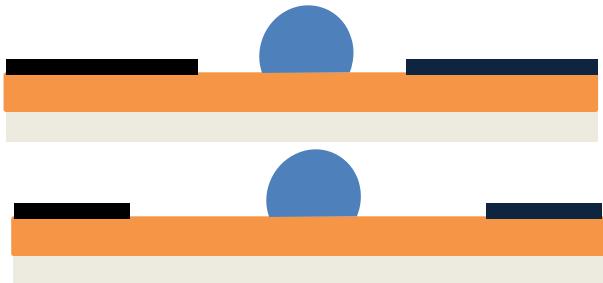
Approach

- Define physiochemical properties of film and realize influence of film and drop size on corrosion rates and damage distributions – Cu, NaCl
- Multiphysics continuum model of droplet-film system- physical-chemical evolution of system for experiment interpretation, predict damage distribution and rates

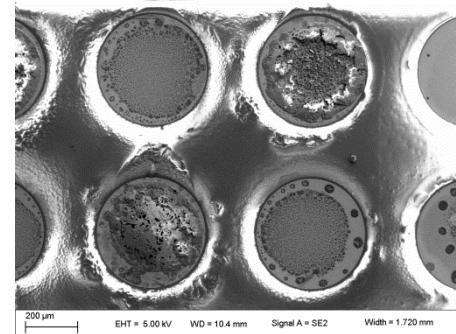
Experimental: NaCl Drops on Cu Pads



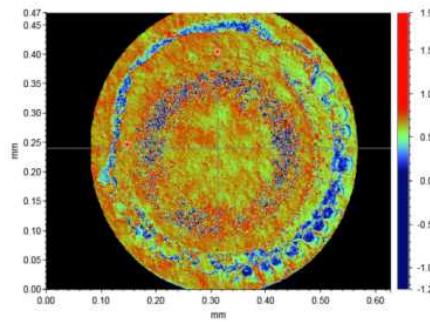
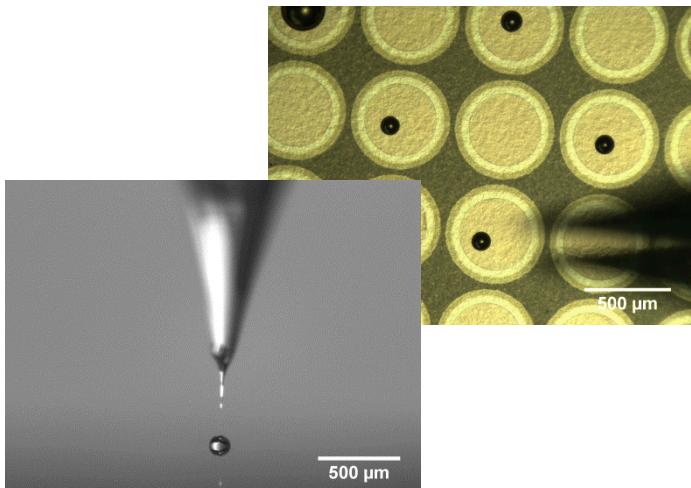
4M NaCl
1 μm Si_3N_4
25 μm Cu



85% RH, 25 °C,
< 1 ppm CO_2



spreading chemistry
and distribution

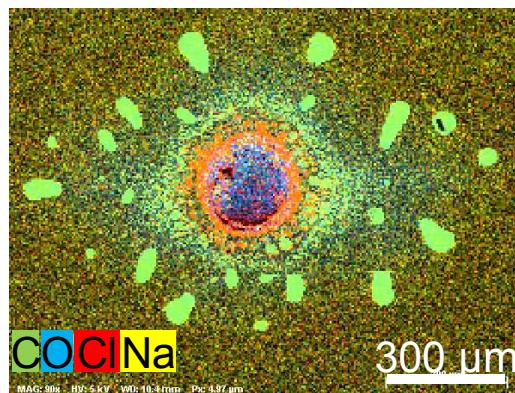
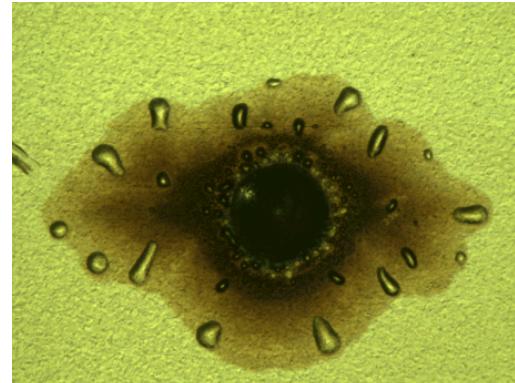
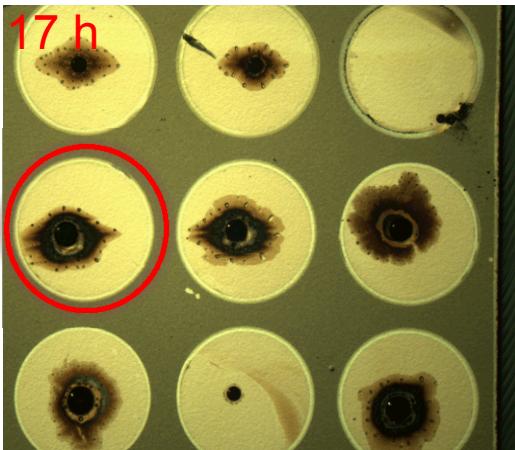
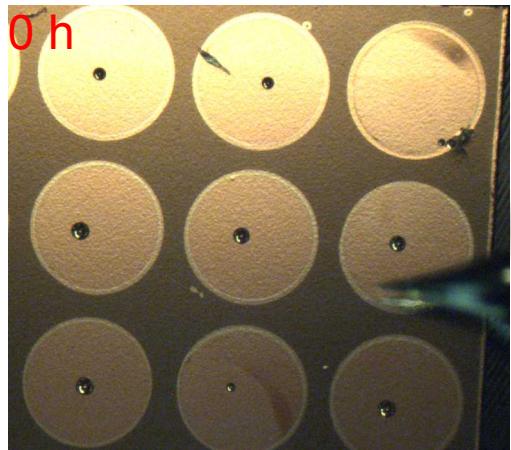


damage profiles

Unrestricted Spreading: Chemistry

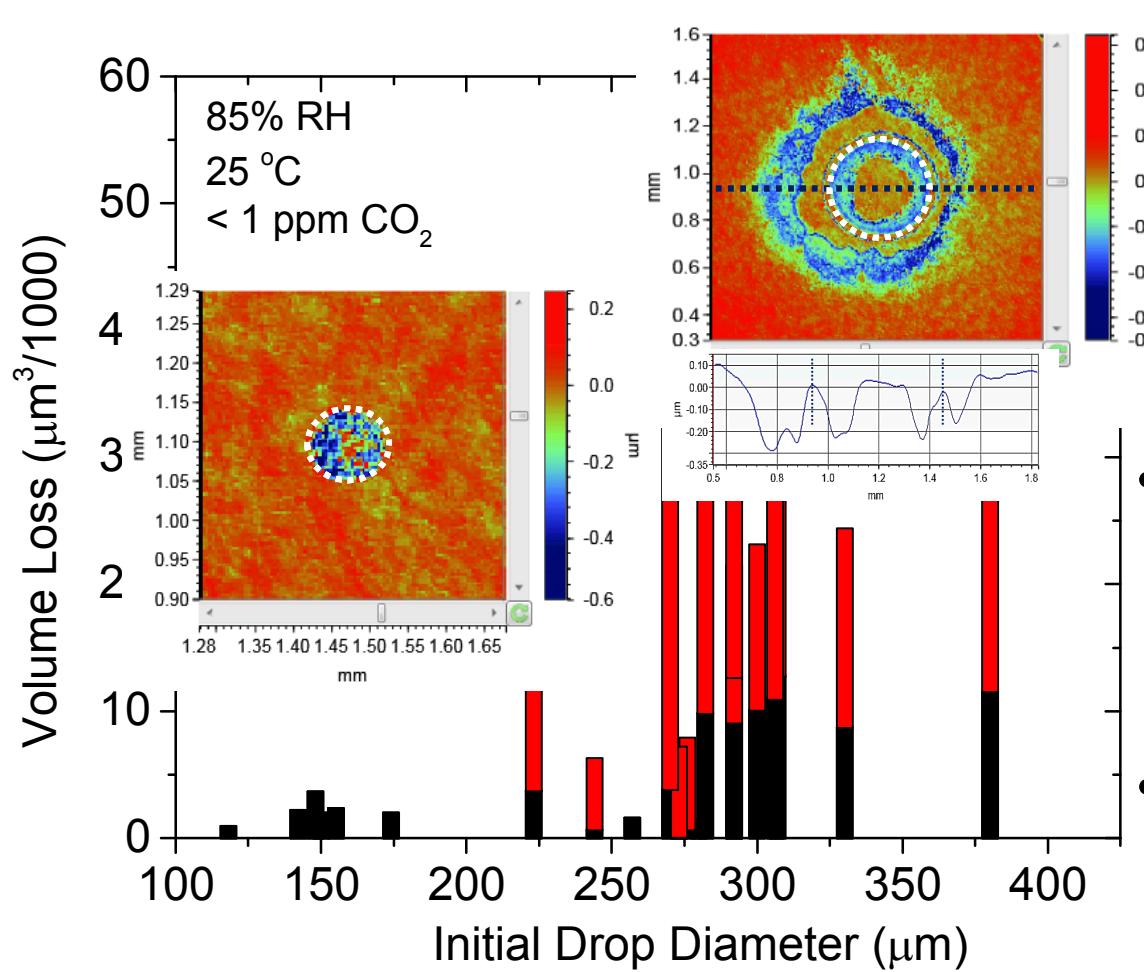
2mm Windows

85% RH, 25 °C,
< 1 ppm CO₂



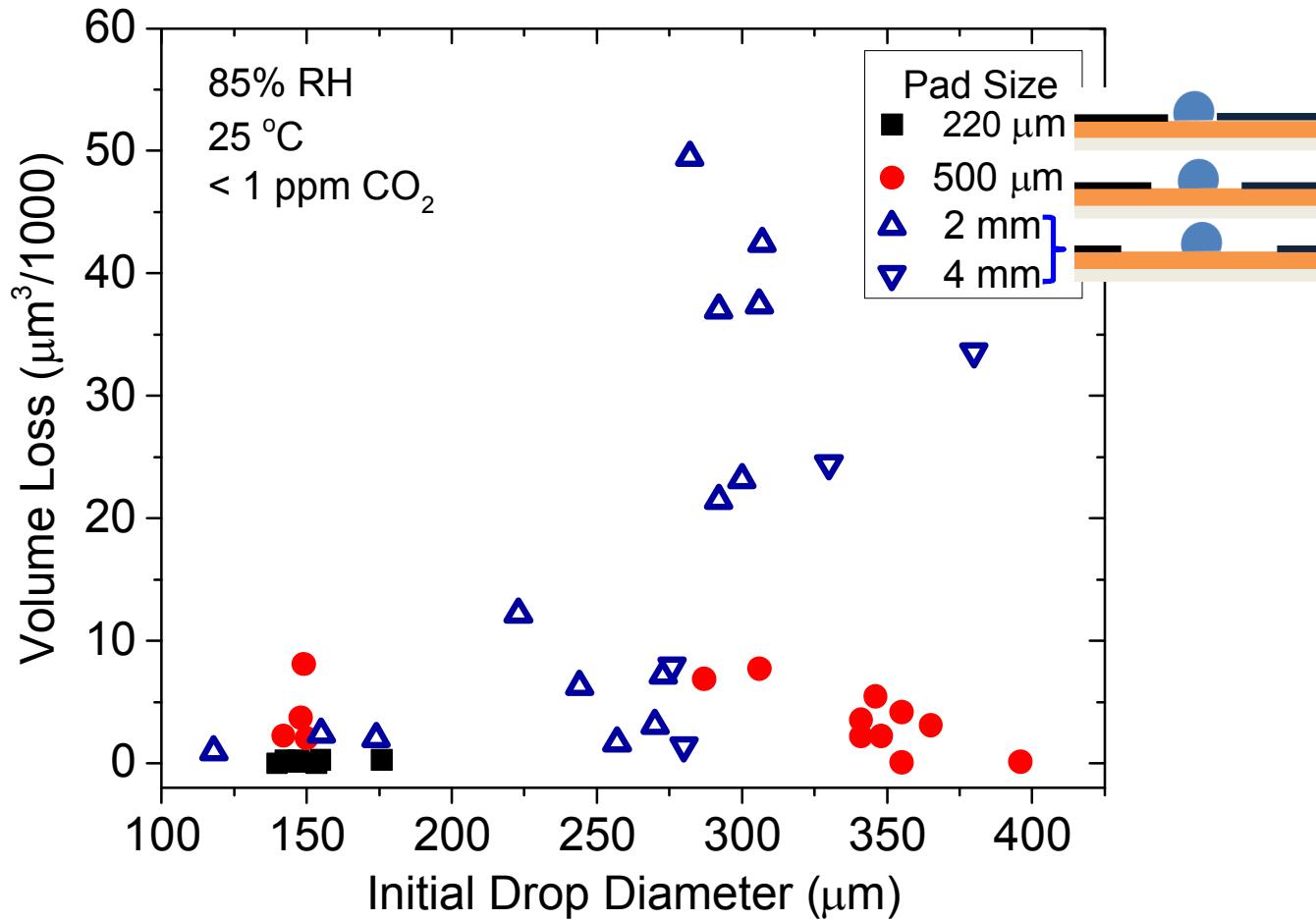
- Spreading chemistry in accordance with previous studies
- After 17 hours, can spread > 2x original drop radius

Unrestricted Spreading: Damage



- Damage and spreading dependent on drop size
- Corrosion under spreading dominates at $\varnothing \geq 225 \mu\text{m}$, inverse Evans

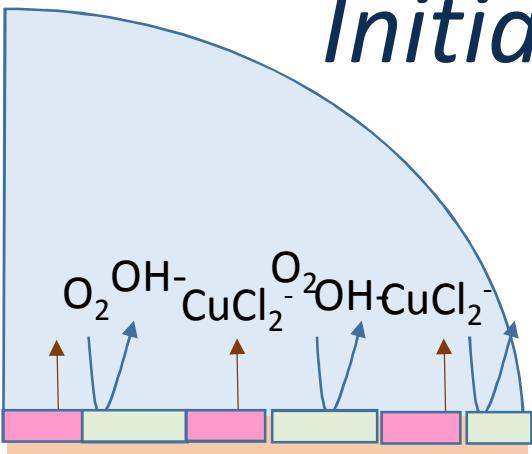
Restricted Substrates: Damage



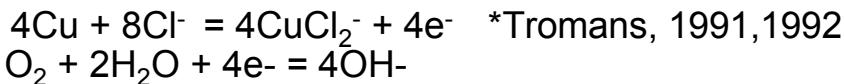
Corrosion loss strongly dependent on spreading S.S. at $\emptyset \geq 225 \mu\text{m}$

Electrolyte and Damage Evolution

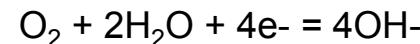
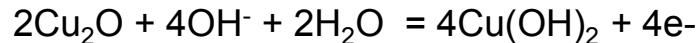
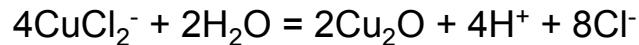
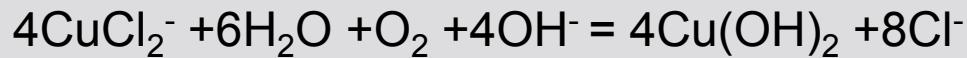
Initiation



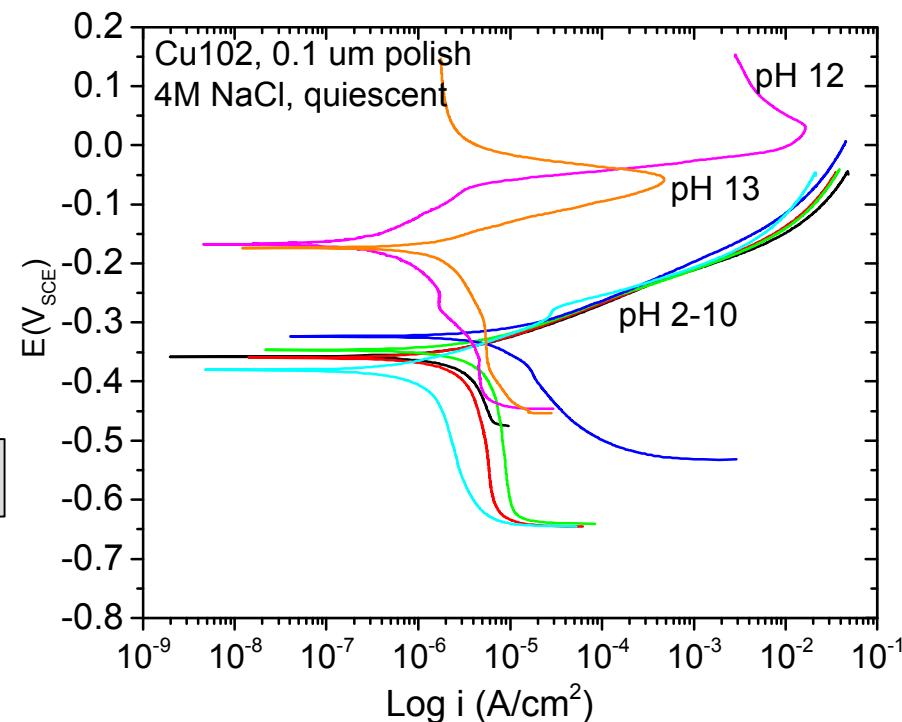
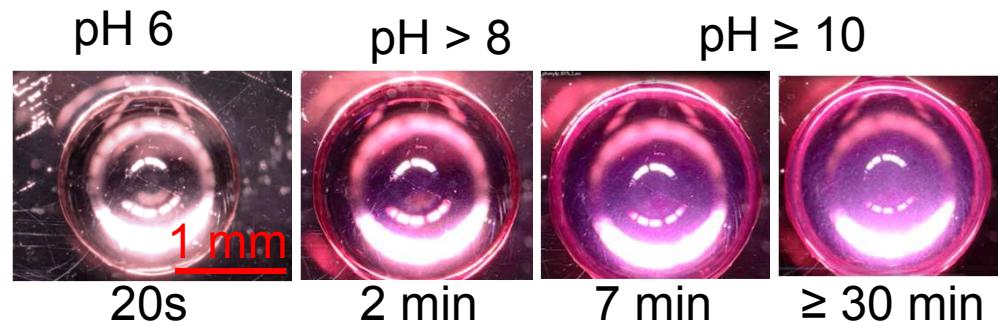
pH 2-10



pH 12,13

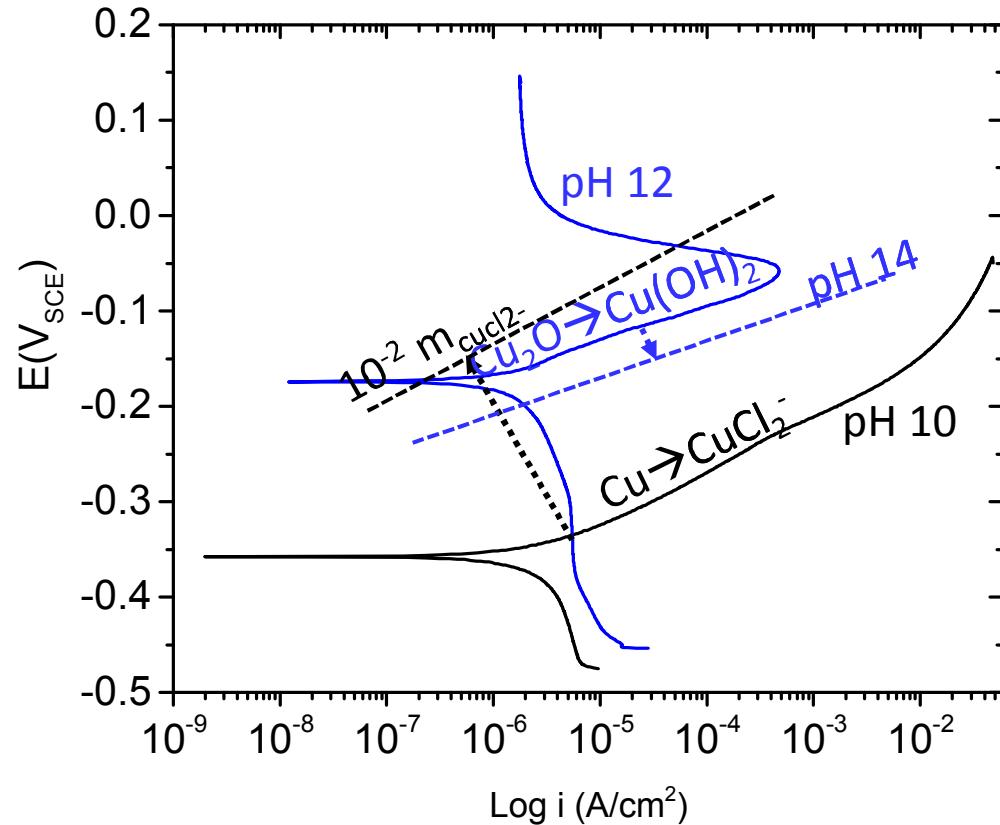
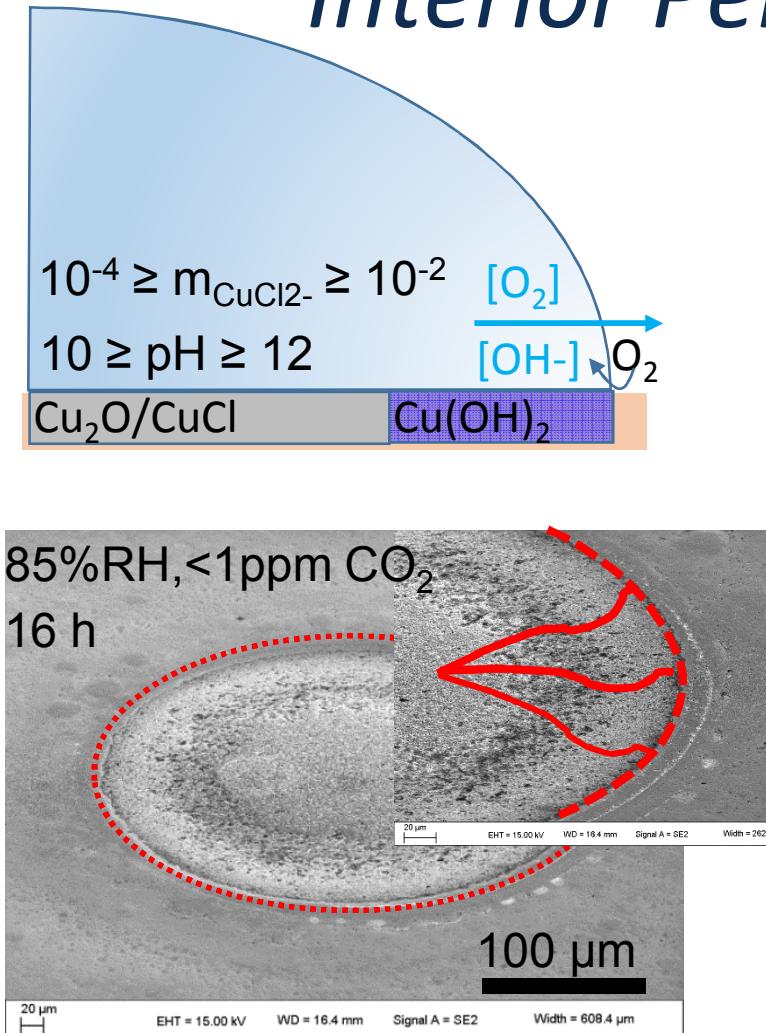


pH likely buffered by $CuCl_2^- \leftrightarrow Cu_2O \leftrightarrow Cu(OH)_2$



Electrolyte and Damage Evolution

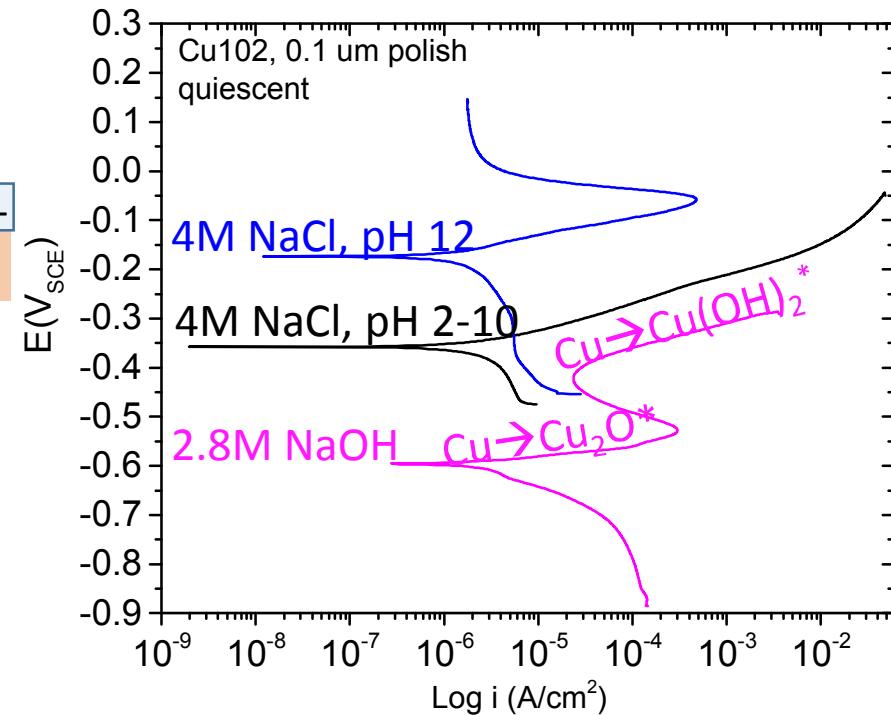
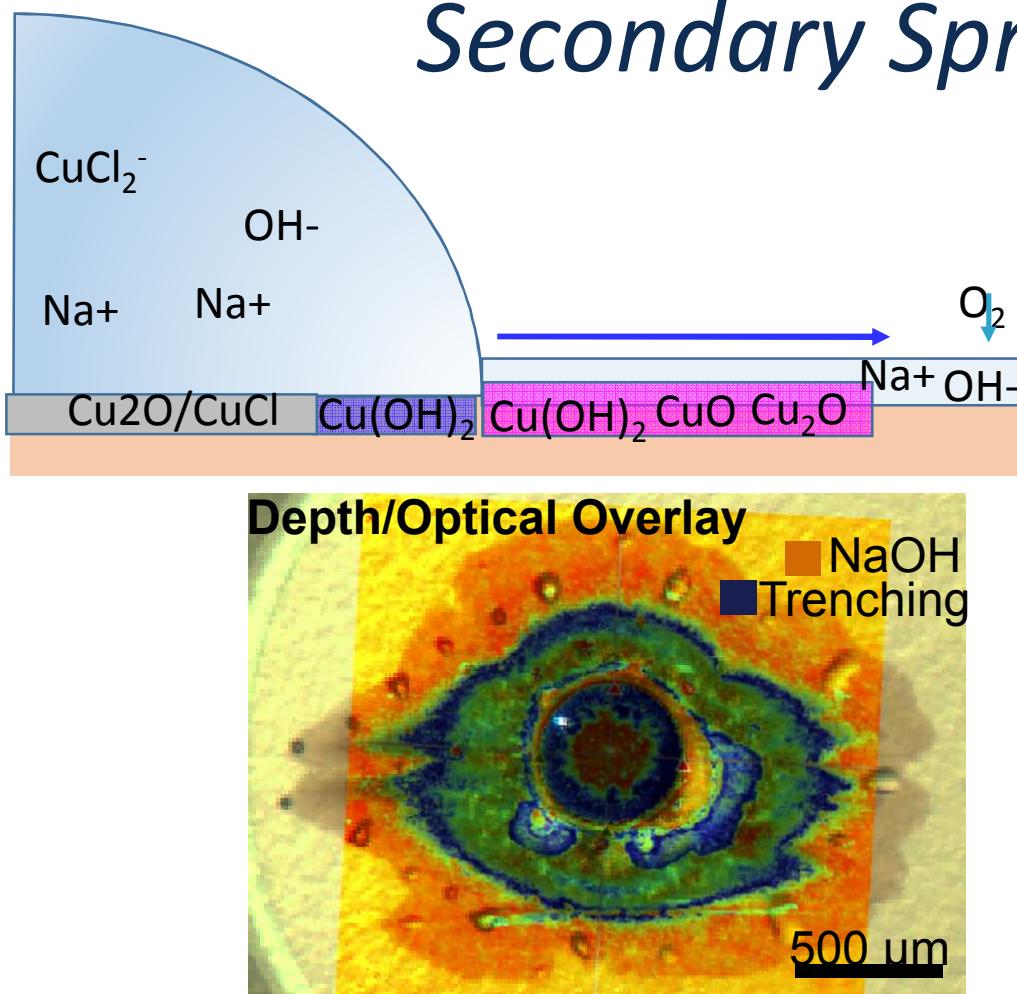
Interior Perimeter Trenching



$[\text{O}_2]$ gradient may cause trenching near drop edge

Electrolyte and Damage Evolution

Secondary Spreading



*Biton *et al.*, 2006

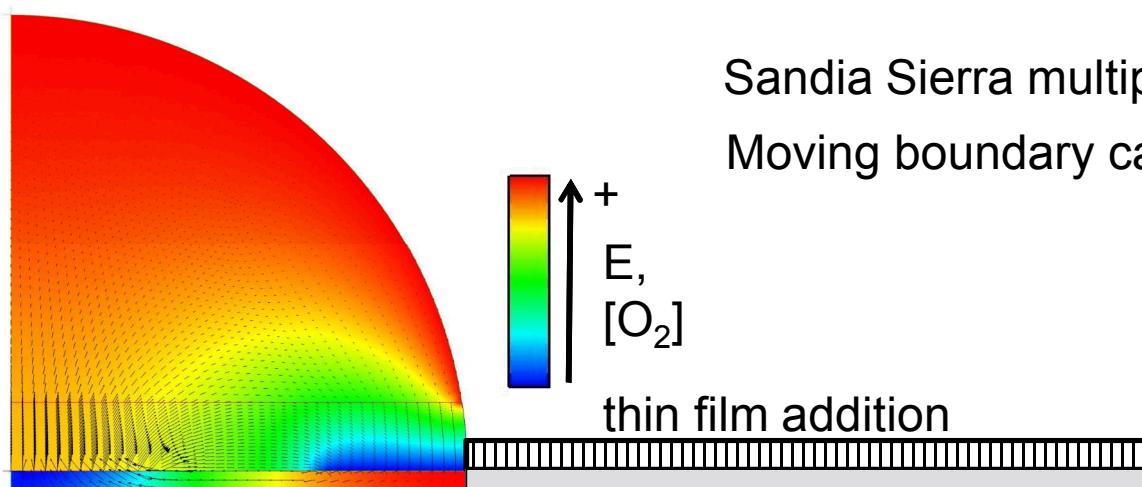
Trenching in spreading film region due to $\text{Cu} \rightarrow \text{Cu}_2\text{O}$, $\text{Cu}(\text{OH})_2$ 13

Conclusions

- Damage distribution and rate highly dependent on drop size/secondary spreading
- Larger drops exhibit damage pattern inverse of classic Evans drop, with greatest corrosion loss in secondary spreading zone- not strictly a cathode
- Damage evolution rationalized via mixed potential theory in analogous bulk electrolyte solution- preferential, high pH anodic dissolution
- Exemplifies need to account for electrolyte evolution in electrochemical atmospheric corrosion models predicting damage distributions and rates

EXTRAS

Droplet-Film Model: Construct



Sandia Sierra multiphysics architecture
Moving boundary capability – electrolyte evolution

Governing Equation- Nernst Planck Boundary Conditions: Butler-Volmer
 $O_2 + 2H_2O + 4e^- \rightarrow 4OH^-$

$$\frac{\partial c_i}{\partial t} = \nabla \left(-D_i \nabla c_i - z_i \frac{D_i F}{RT} \nabla \phi \right)$$

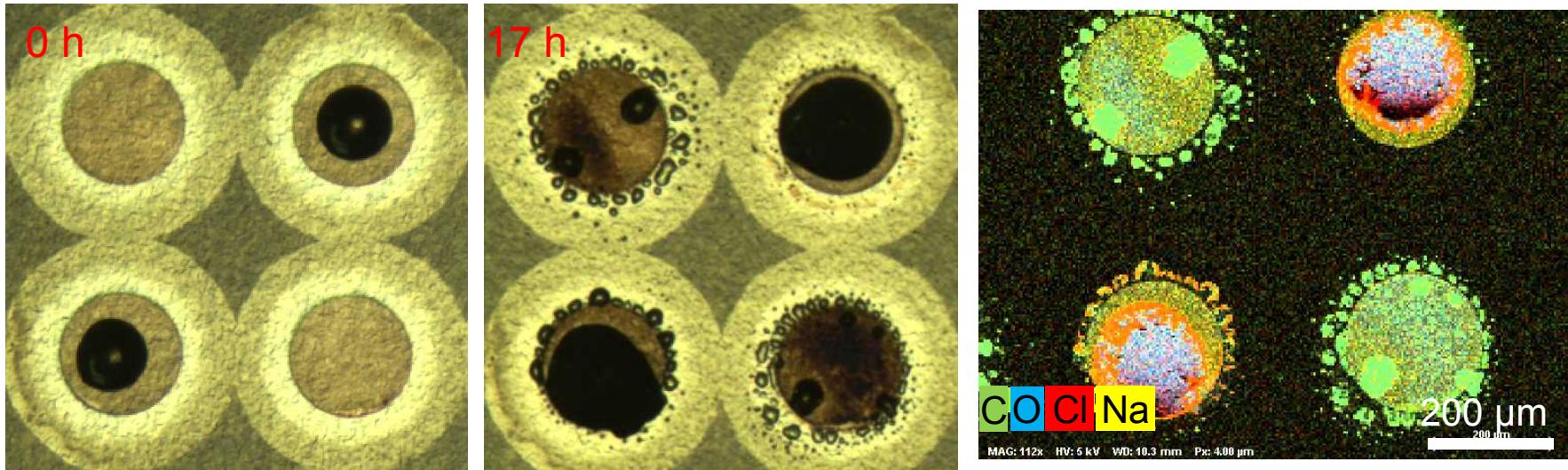
$$i_{O_2/OH} = -i_{o_{O_2/OH}} \exp \left(\frac{-2 \left(1 + \frac{\alpha_{O_2}}{\alpha_{OH}} \right) F}{RT} (\Delta \phi_{O_2/OH}) \right)$$

$$i_{M/M^{x+}} = -i_{o_{M/M^{x+}}} \exp \left(\frac{-x \left(1 + \alpha \frac{M}{M^{x+}} \right) F}{RT} (\Delta \phi_{M/M^{x+}}) \right)$$

Restricted Substrates

220 μm Windows

85% RH, 25 $^{\circ}\text{C}$,
< 1 ppm CO₂



- Development of S.S. chemistry over Si₃N₄ with highest concentrations on non-deposited pads