

Steel Corrosion Mechanisms during Pipeline Operation: In-Situ Characterization

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Global problem

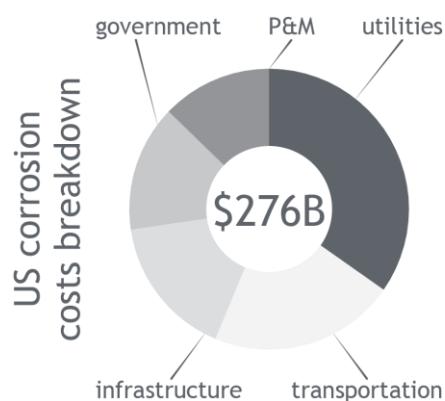
annual US corrosion costs

\$276,000,000,000

\$ 276 B



3.1% US GDP lost to corrosion
investing in controls | dealing with failures



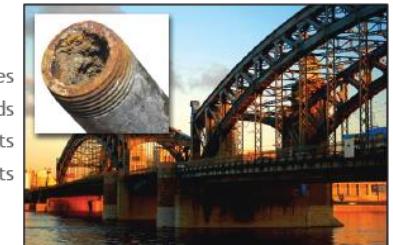
electrical utilities
gas distribution
drinking water
sewers



ships
aircraft
motor vehicles
railroad cars



bridges
railroads
airports
ports



oil & gas pipelines
petroleum refining
mining
chemical/pharma



Pipeline Steel Corrosion: Oil and Gas Extraction

annual US corrosion costs

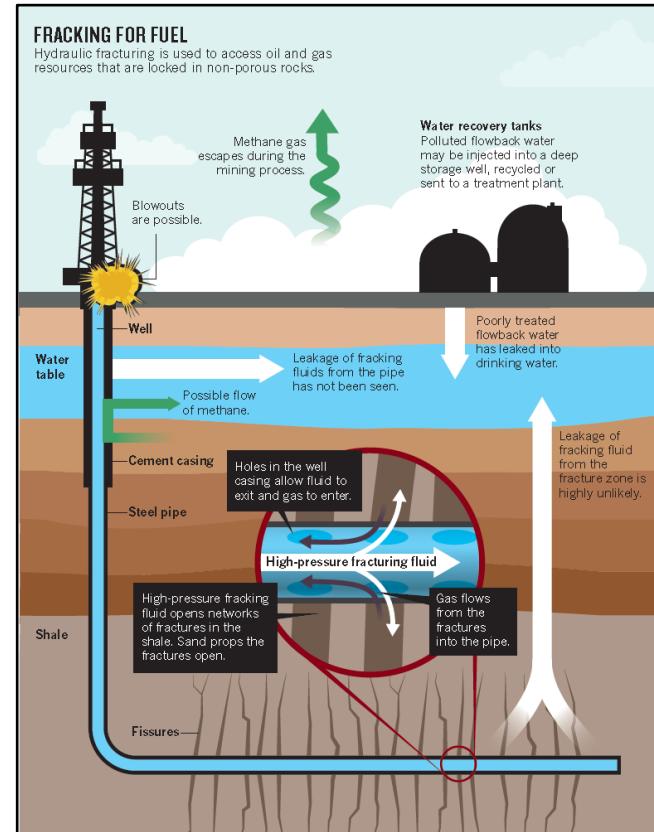
\$276,000,000,000

\$ 276 B



3.1% US GDP lost to corrosion
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Steel failure caused by local corrosion, pitting, and eventual cracking

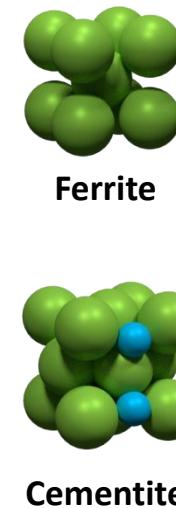
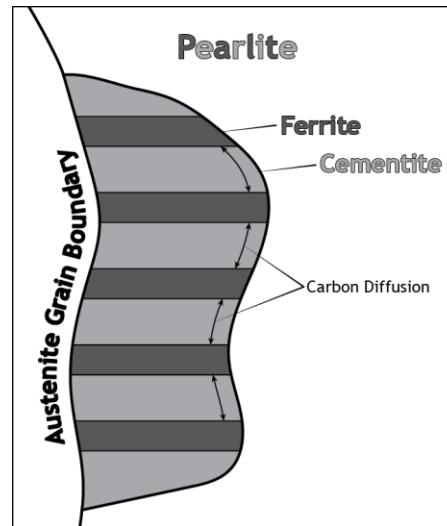
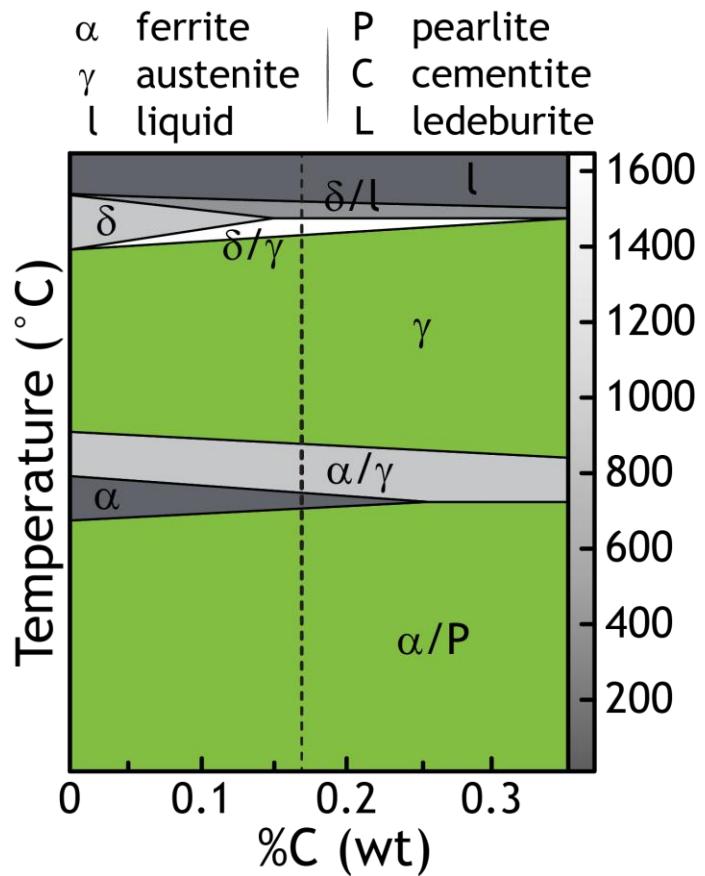


Mechanisms for pipeline corrosion initiation are unclear

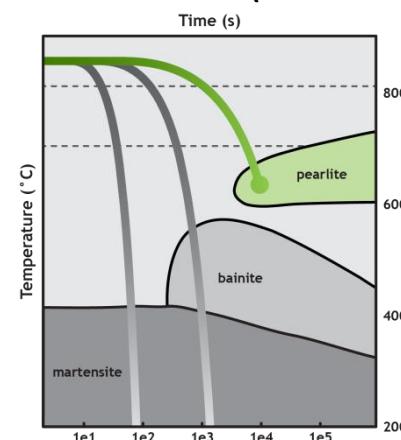
- Grain boundaries are highly susceptible to corrosion in atm environments
- Cementite acts as a cathode, while Fe dissolution occurs in ferrite or pearlite structures, deviation of 10-20 mV between ferrite and cementite (Bai et al, 2015)
- Surface film peeling exposes new surfaces to continue corrosion

Howarth et al., Nature 477, 271 (2011)

Structure & Composition of 1018 Carbon Steel



Pearlite: alternating layers of ferrite (88 wt%) and cementite (12 wt%)



Element	Mass %
Fe	98.305
C	0.160
Mn	0.710
Cu	0.345
Si	0.169
Cr	0.116
Ni	0.107

- 1018 is forged from 1150 – 1280 $^{\circ}\text{C}$ down to a temperature in the area of 600 – 650 $^{\circ}\text{C}$

Pipeline Steel Corrosion: Sweet Corrosion CO₂

Water reacts with dissolved CO₂ to form carbonic acid

Corrosion rate dependent on partial pressure of CO₂ and temperature (affects surface film that is formed)

Protective scale: iron carbonate films form, FeCO₃

Water composition effects the buffering capacity

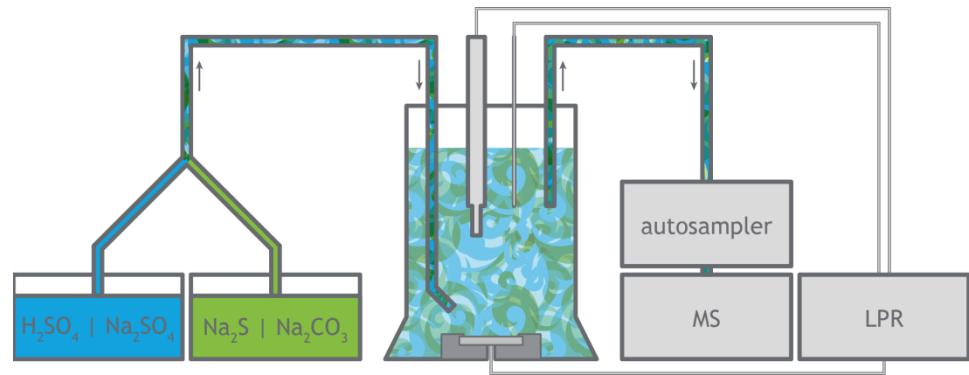
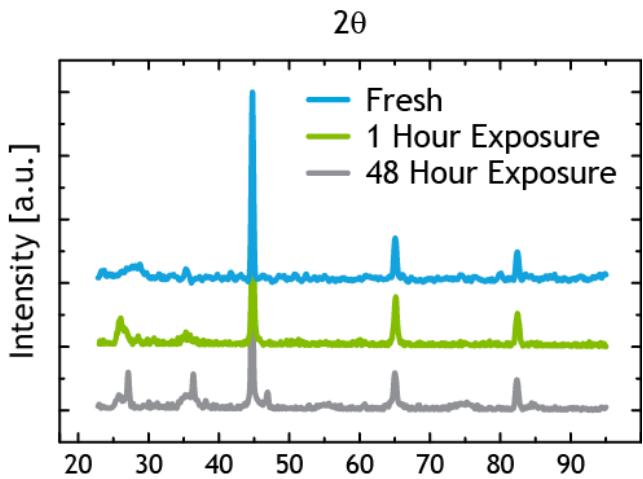
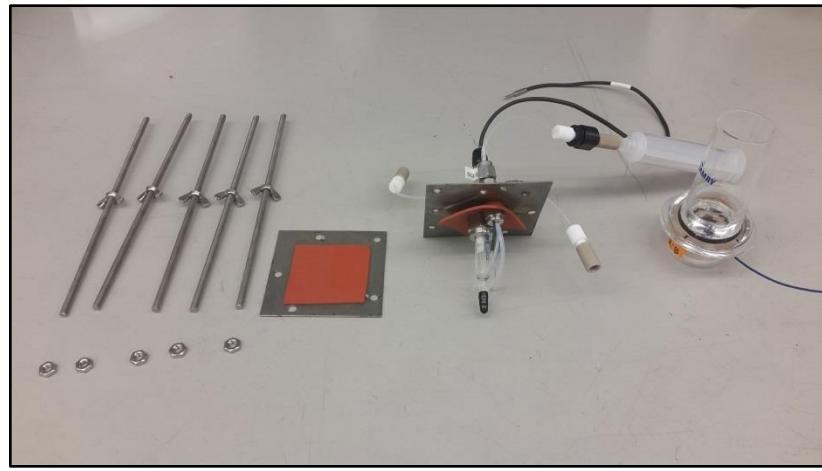
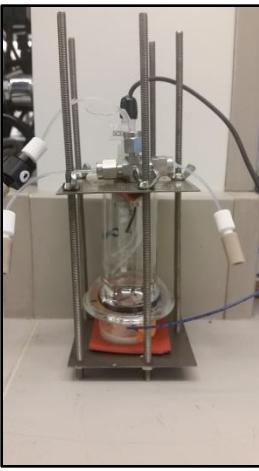
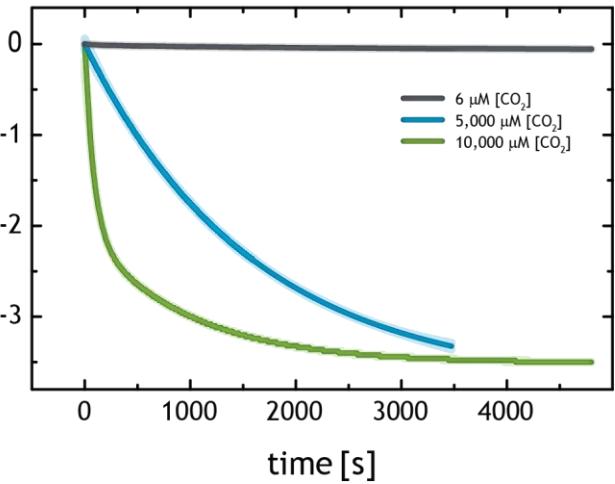
Determinant Parameters:

- Solution composition: pH, wetting, phase ratios
- Salt composition (NaCl, K⁺, Ca²⁺) and concentrations
- CO₂ content
- Temperature & Pressure
- Steel surface: corrosion film, protective molecules
- Fluid dynamics, flow rate (mass transport of CO₂)
- Steel composition



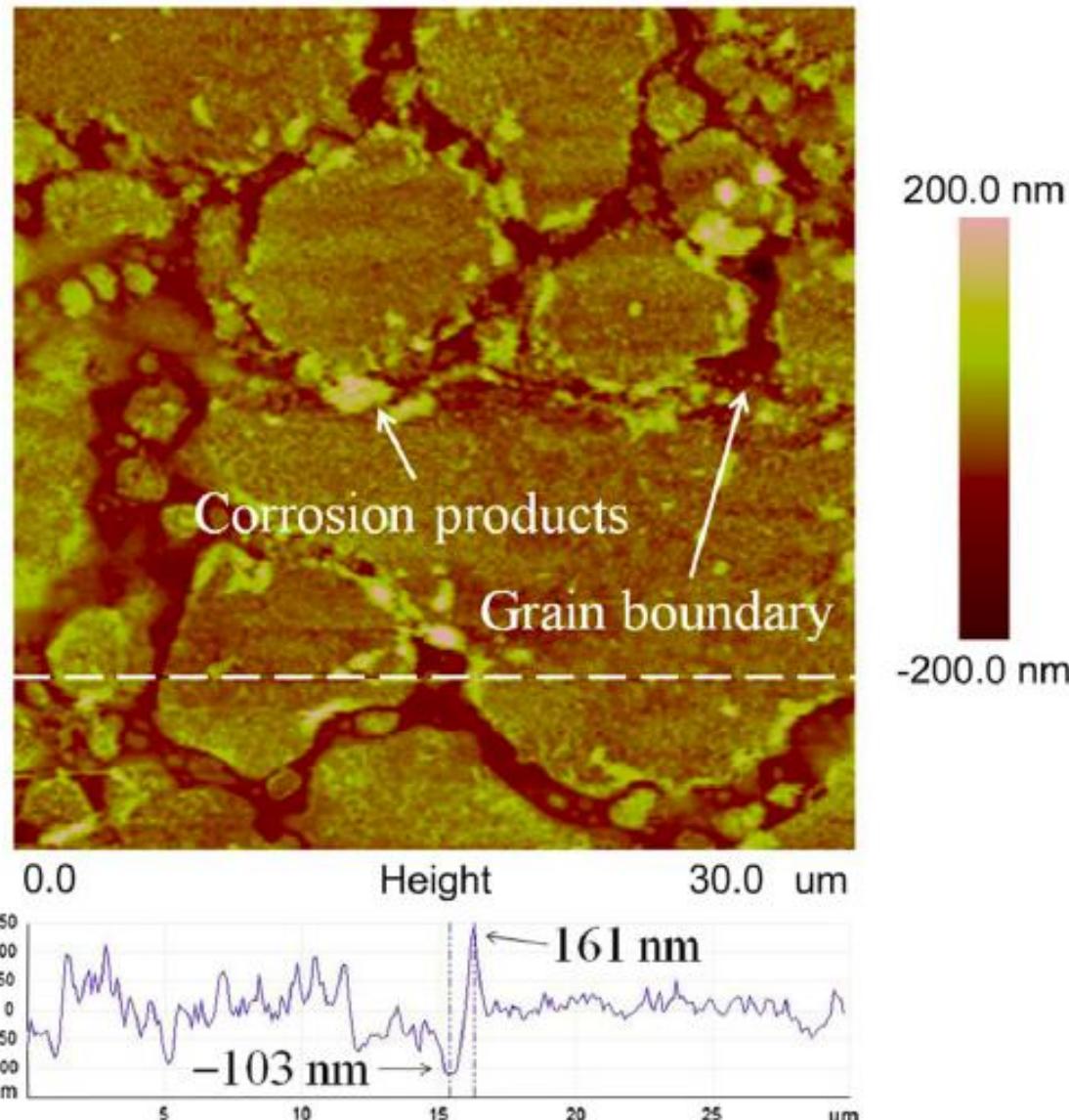
Partnership with ASC to tackle corrosion problem

Δ relative corrosion rate [a.u.]

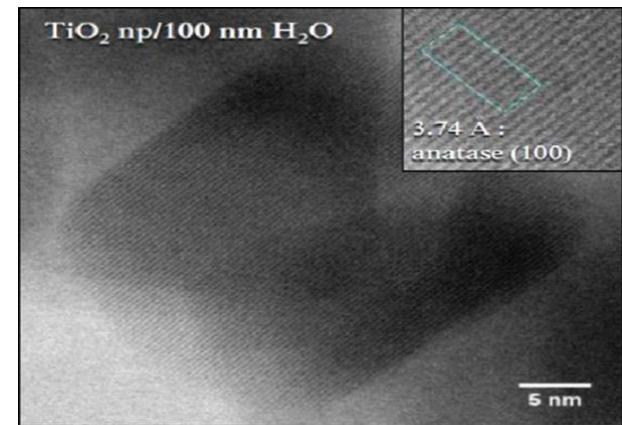
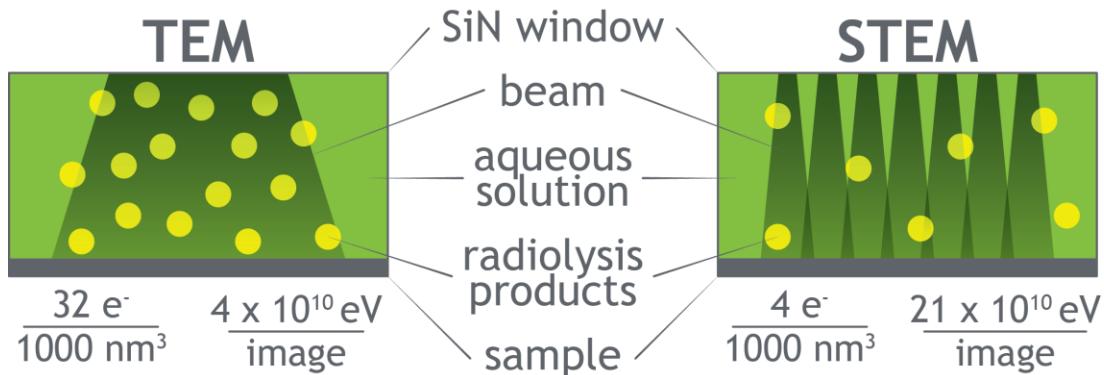
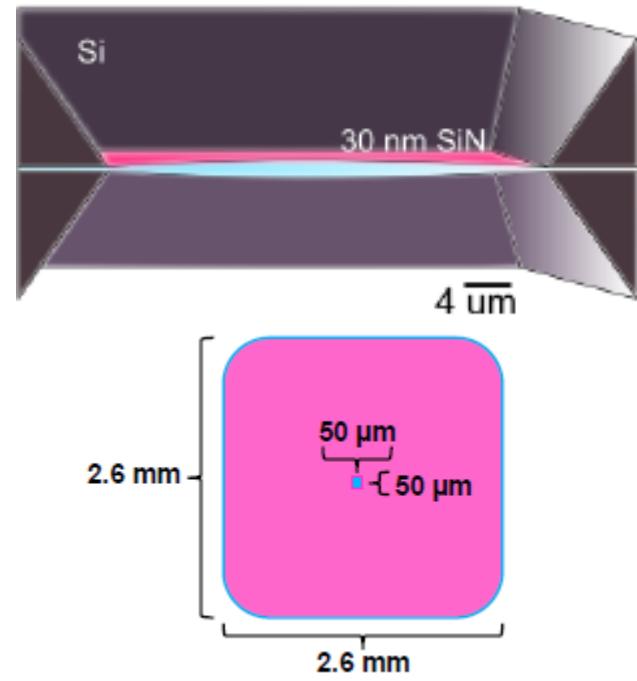
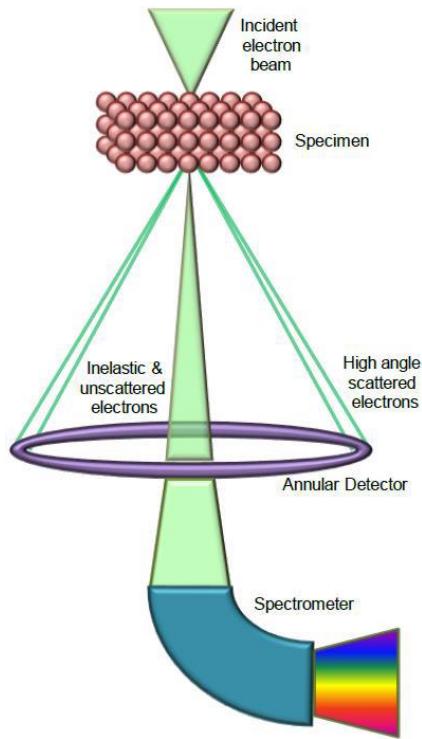


Corrosion Initiates at Grain Boundaries

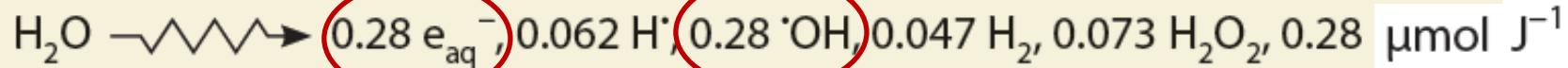
Which grain boundaries? Nanoscale sites?



In-situ TEM Ideally Suited for Nanoscale Corrosion

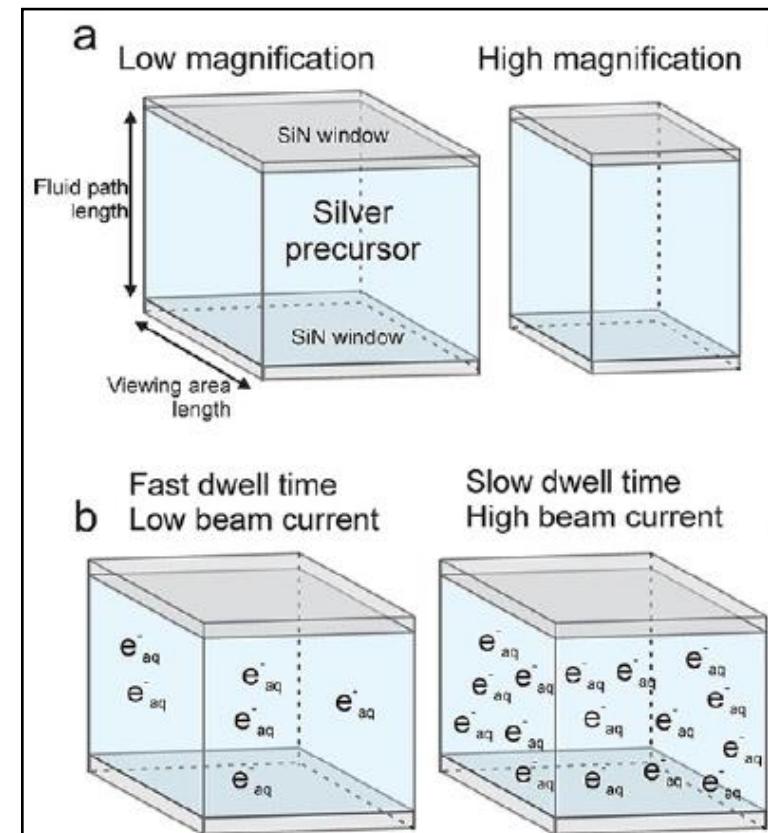
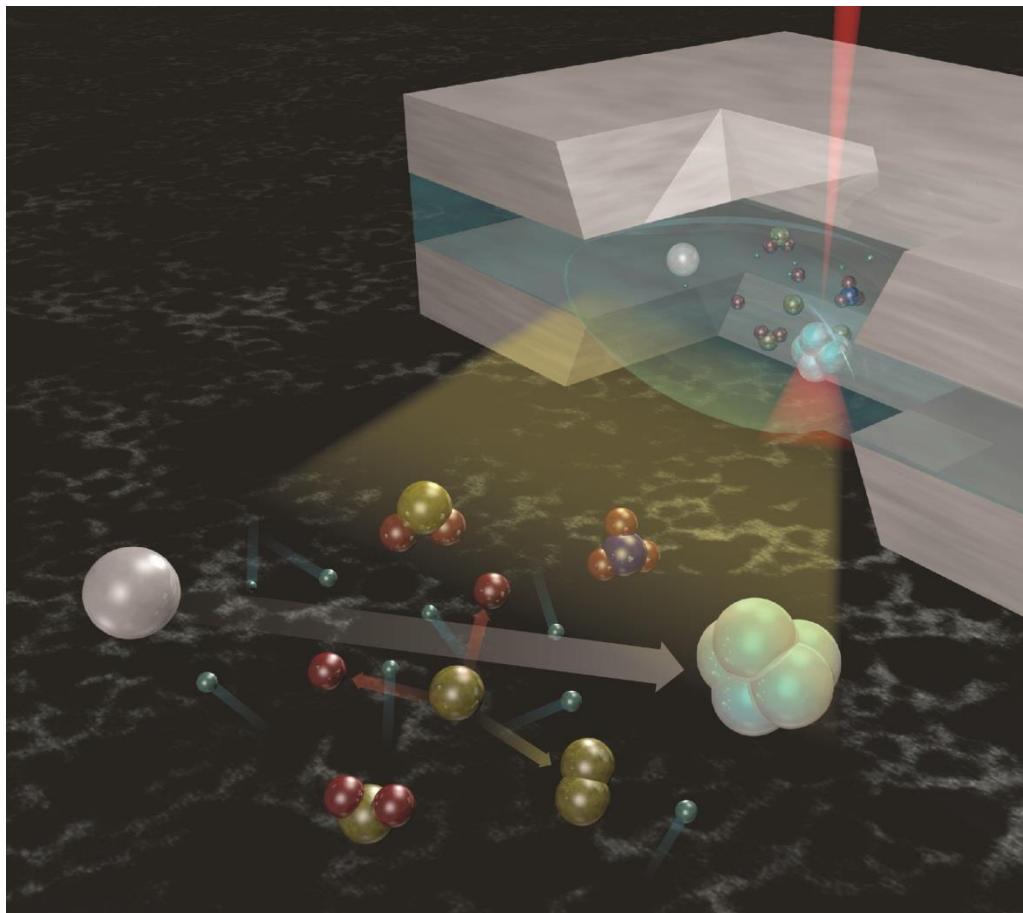


Electron Beam Radiolysis of Aqueous Media



Buxton, VCH Weinheim (1987)

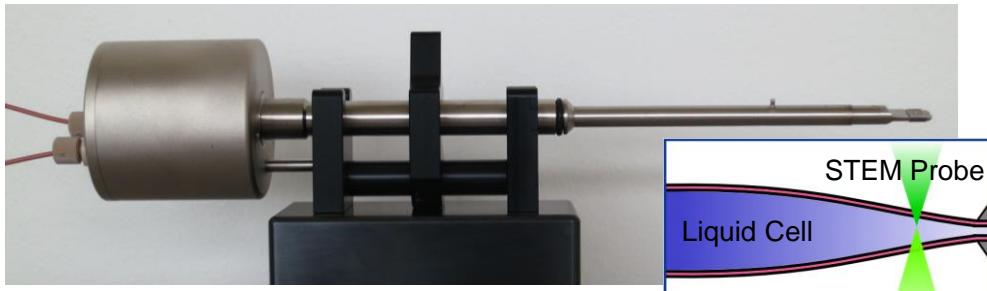
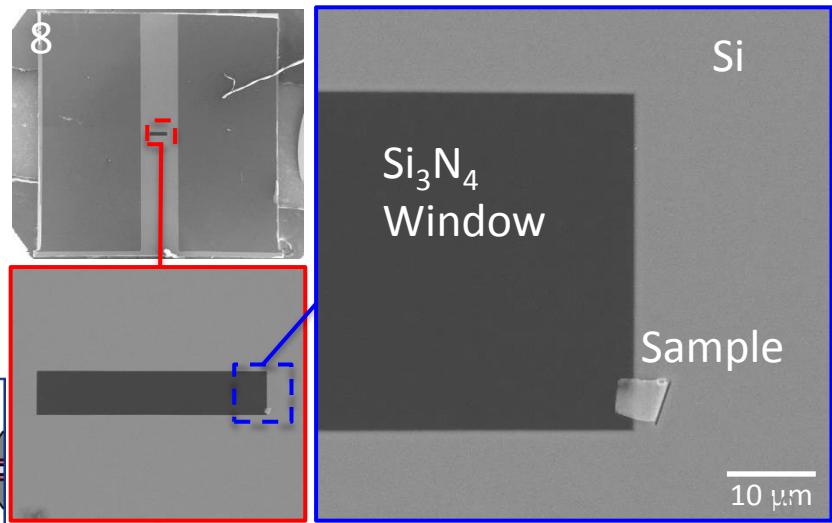
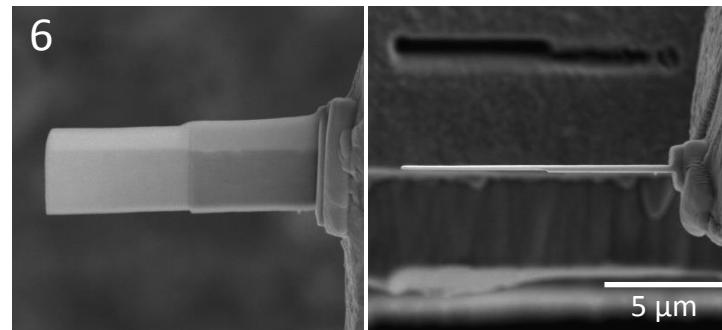
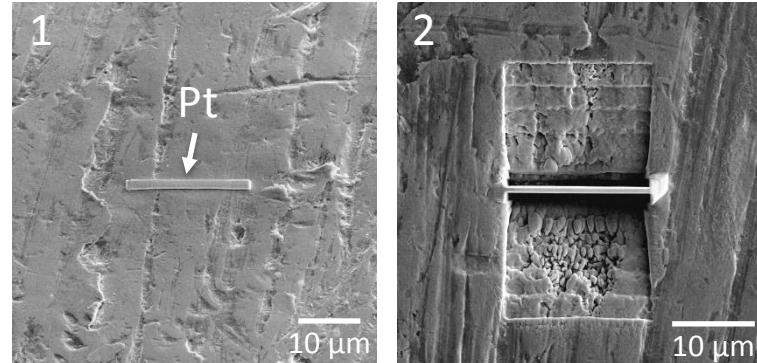
*Amount of products formed depends on the electron dose



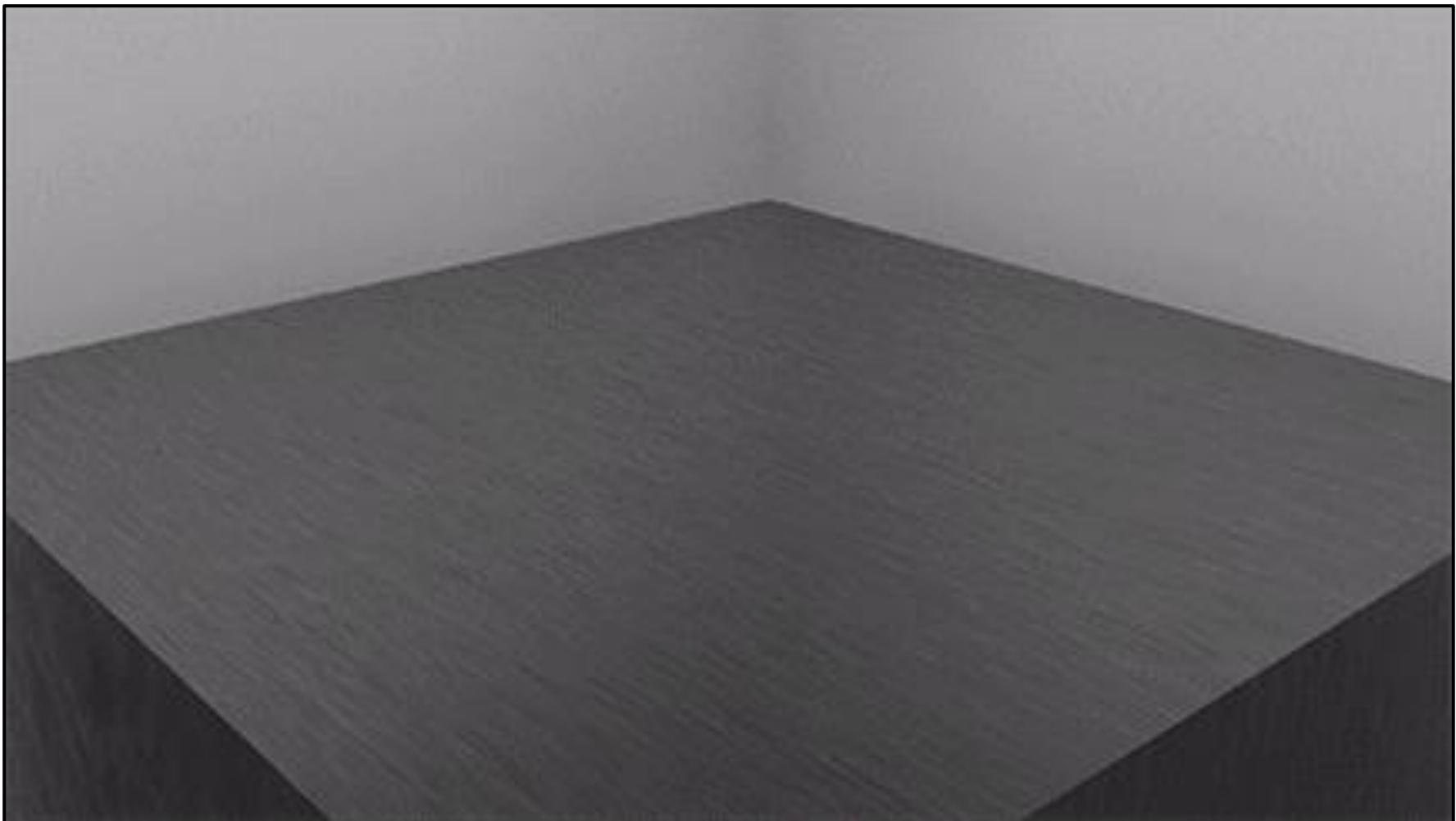
Woehl et al. ACS Nano 6, 8599 (2012).

Sample Preparation and Screening

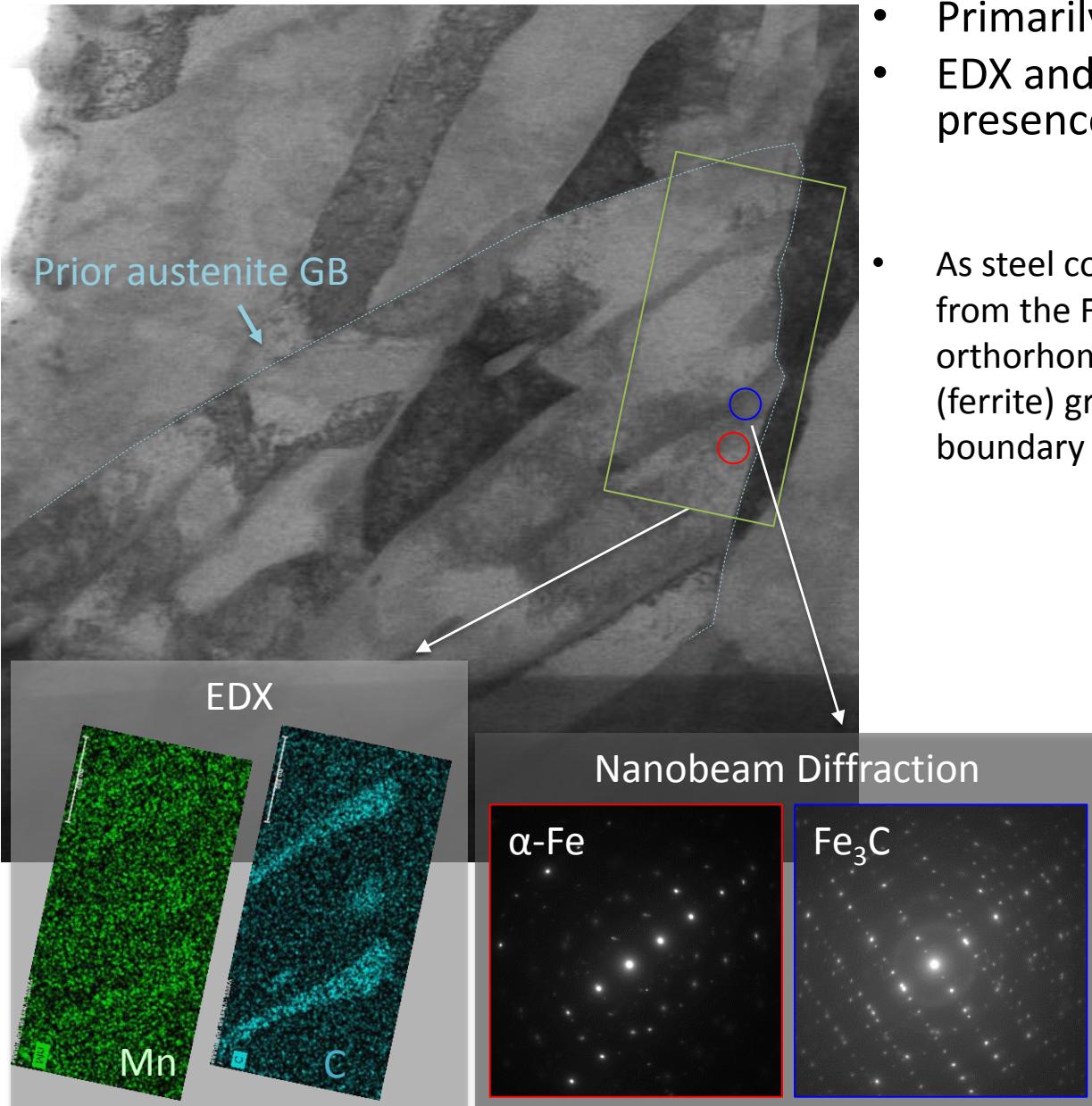
1. Deposit protective Pt layer
2. Trench into low-carbon steel
3. U-cut
4. Attach to micromanipulator
5. Transfer to TEM grid
6. 3 step thinning process
7. Precession Electron Diffraction mapping
8. Transfer to SiN membrane chip for corrosion experiment
9. Load sample in Hummingbird Scientific Liquid Cell TEM holder with DI water between top and bottom chip.
10. Prefill intake line with DI water.



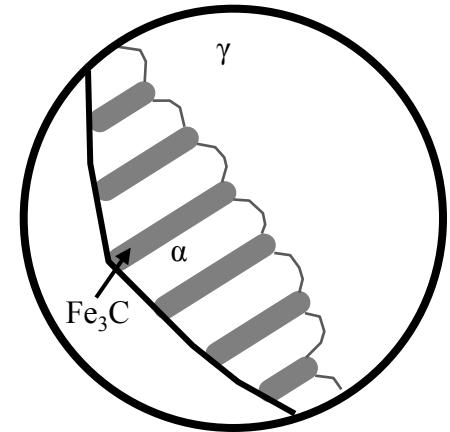
Focused Ion Beam Sample Preparation



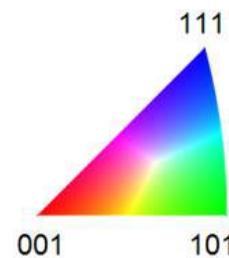
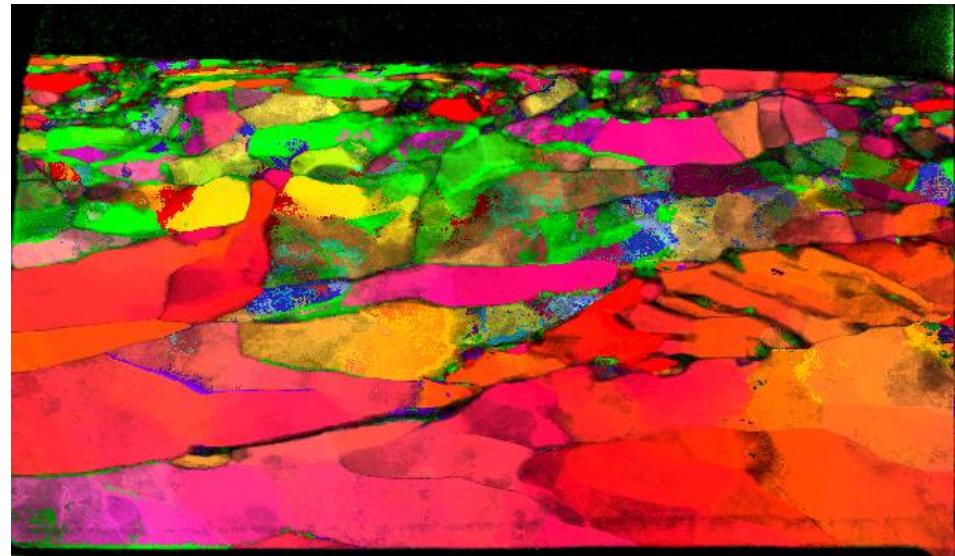
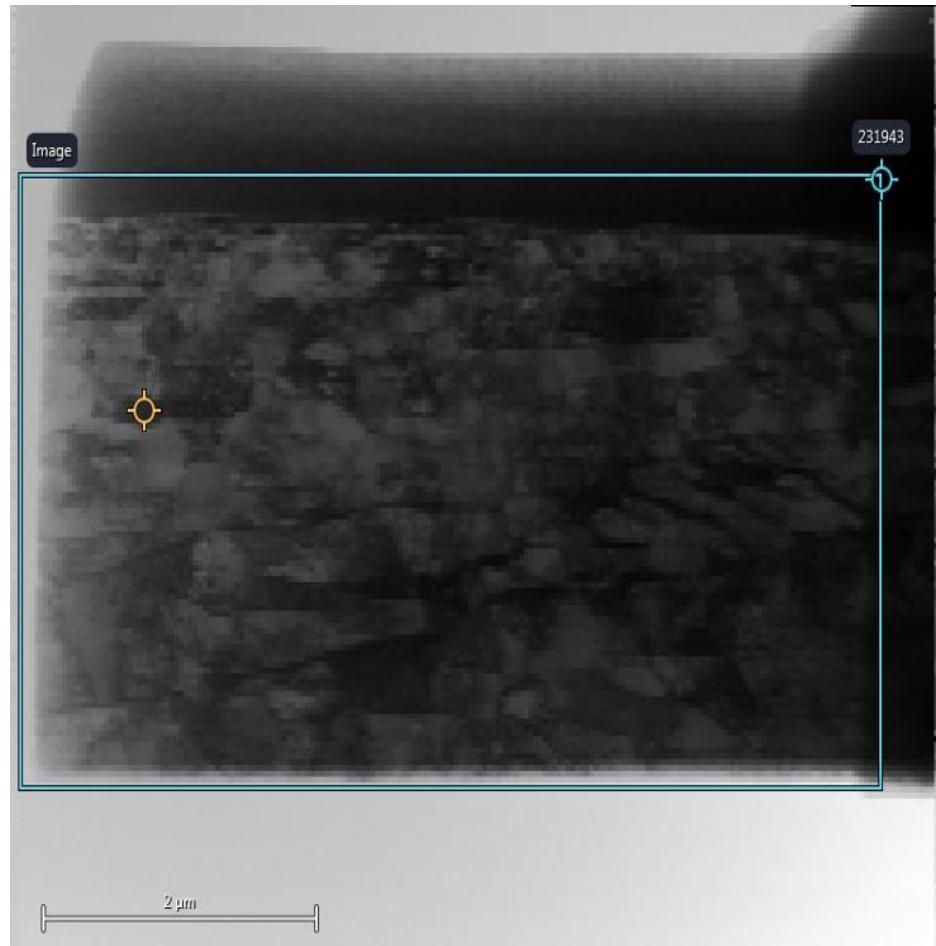
Low-Carbon Steel Microstructure



- Primarily BCC α -Fe
- EDX and nanobeam diffraction show presence of Mn-rich Fe_3C lamellae
- As steel cools past the eutectic temperature from the FCC γ -Fe (austenite) phase, orthorhombic Fe_3C (cementite) and BCC α -Fe (ferrite) grow, starting at a prior austenite grain boundary



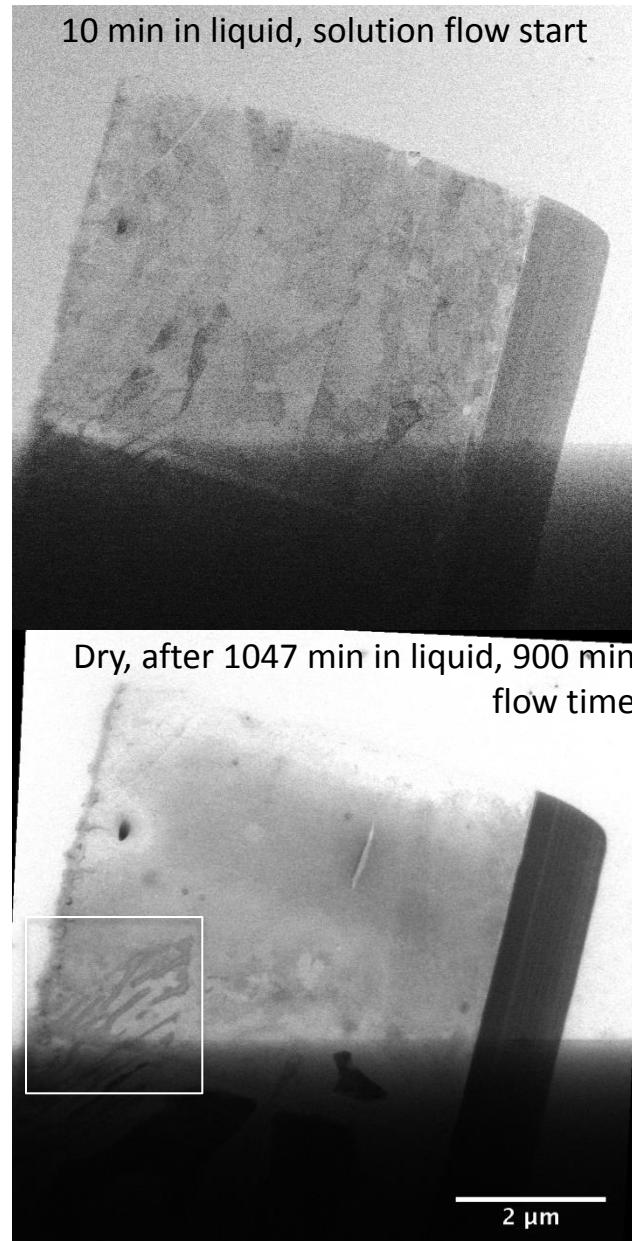
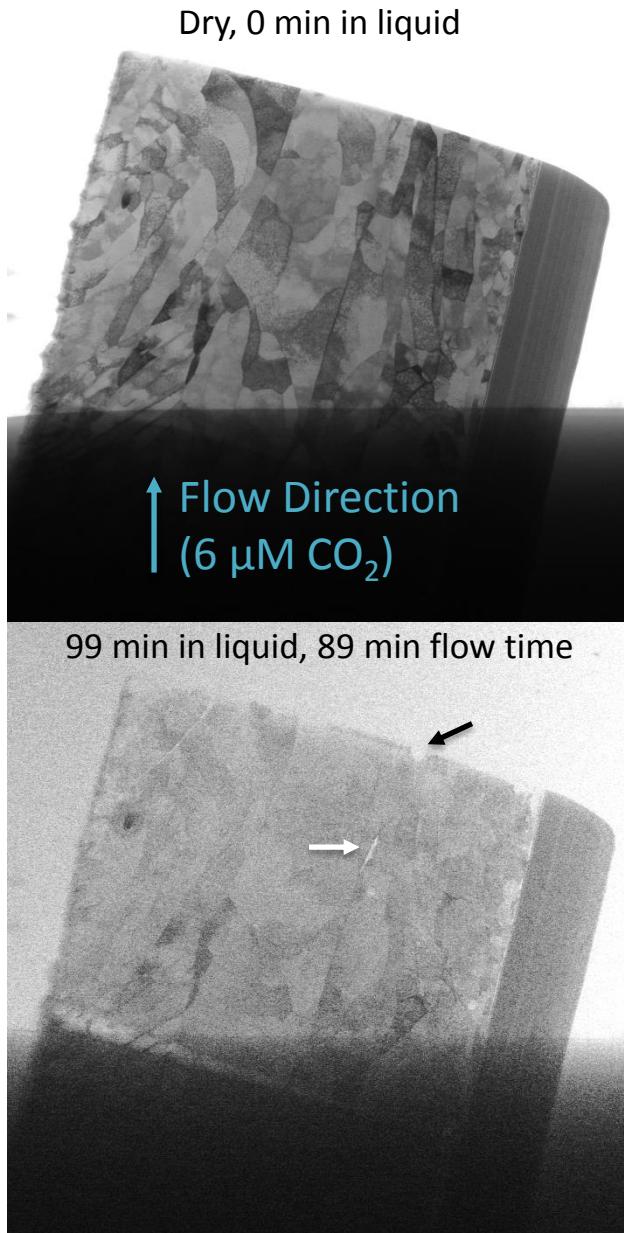
Grain Orientation Mapping of BCC Ferrite

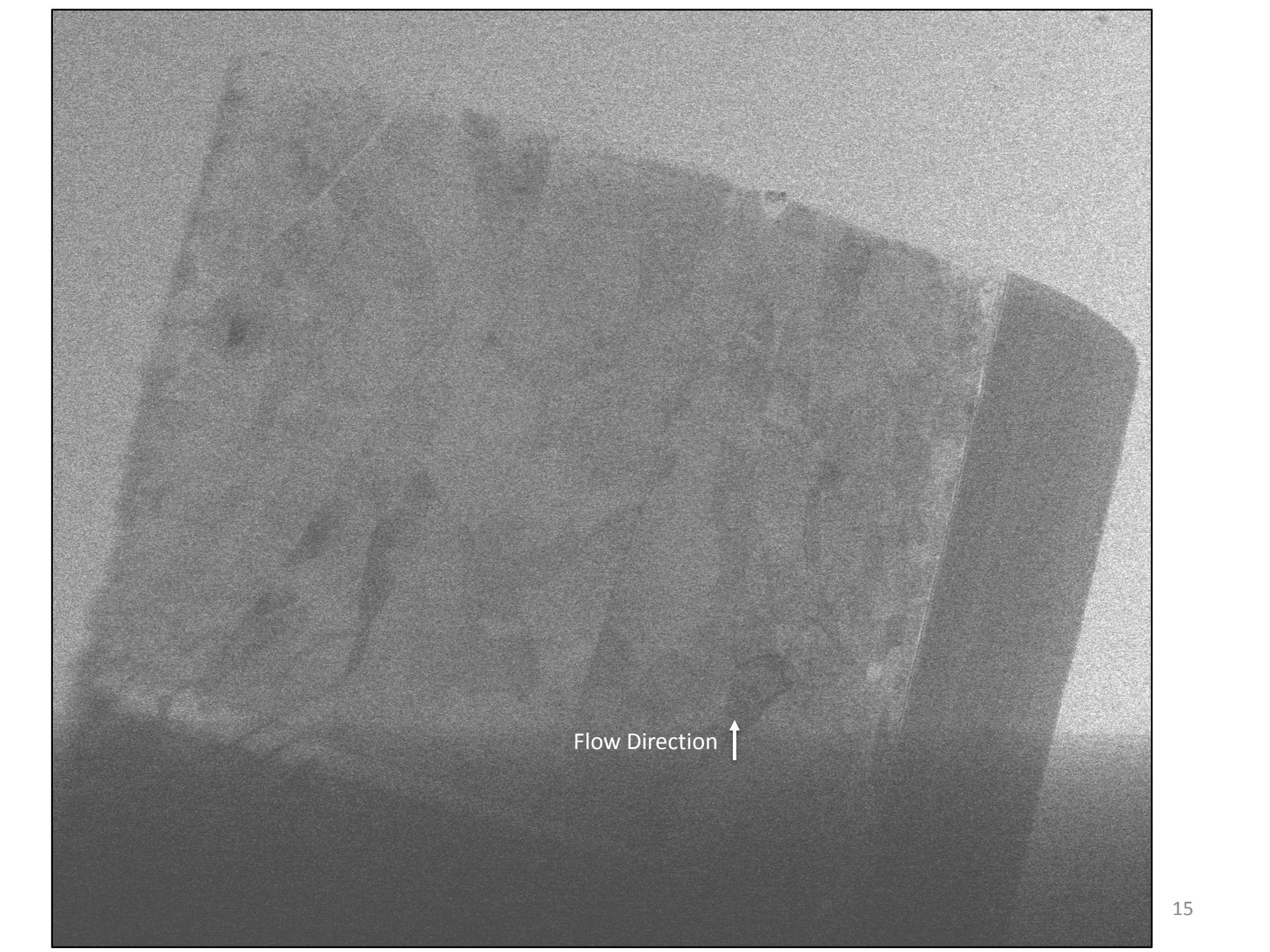


10 nm step size across thinned sample region,
only thin region is placed on SiN membrane window

Low-Carbon Steel in 0.27 ppm CO₂: Microstructural Evolution Overview

- Overall thinning
- Black arrow
 - Edge corrosion
- White arrow
 - Internal grain preferential etching
- White box
 - Preferential α -Fe etching (over Fe₃C)

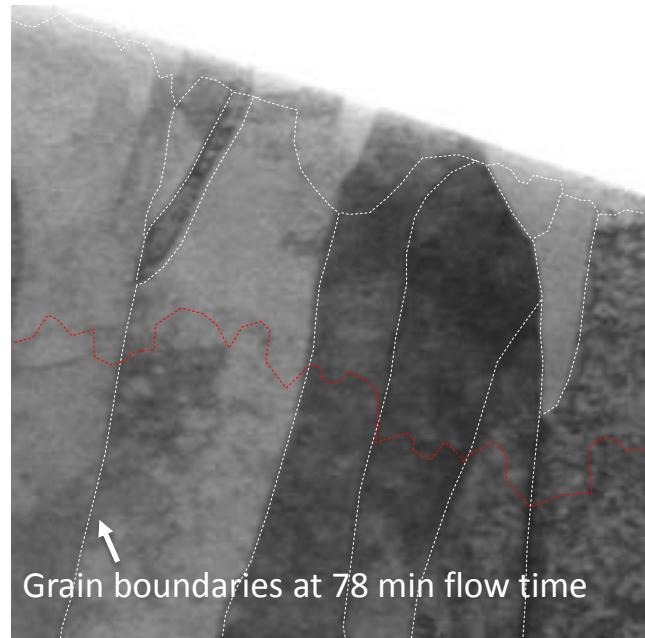




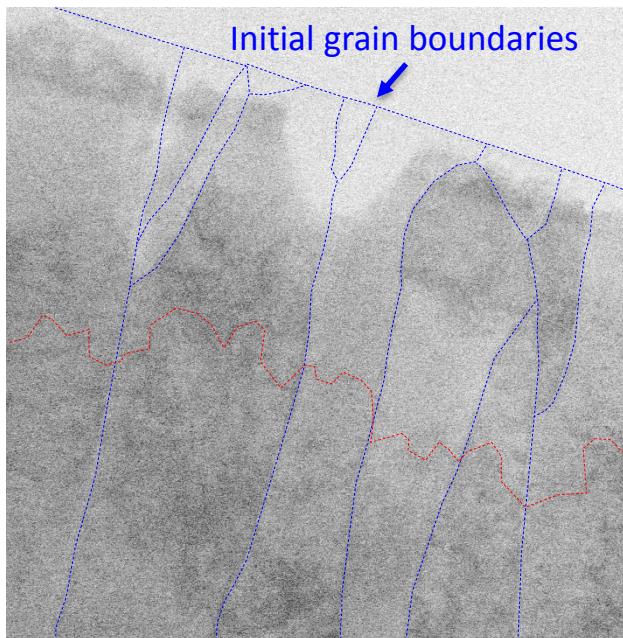
Flow Direction ↑

Edge Corrosion of Steel in 0.27 ppm CO₂

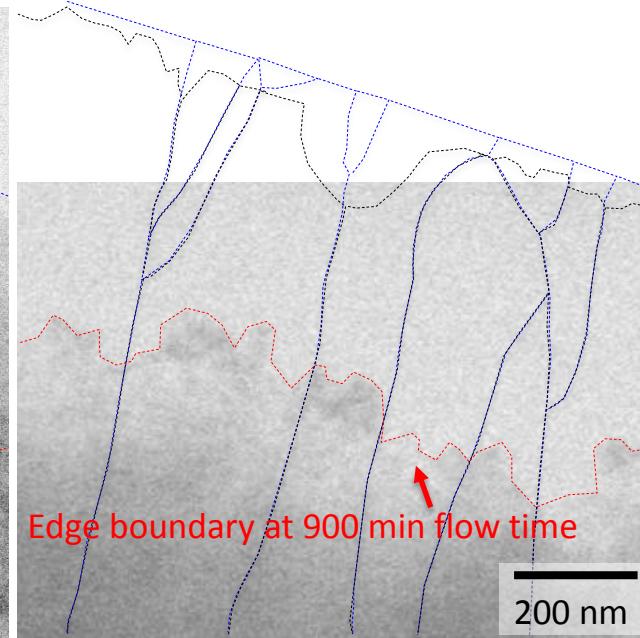
Dry, 0 min in liquid



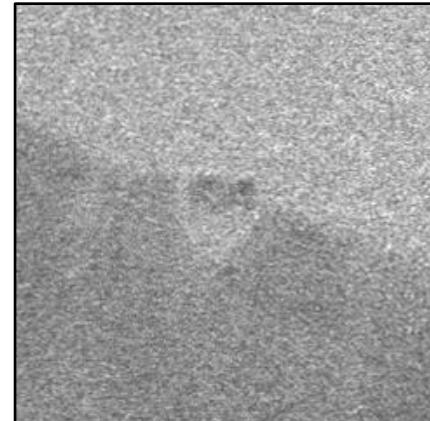
88 min in liquid,
78 min flow time



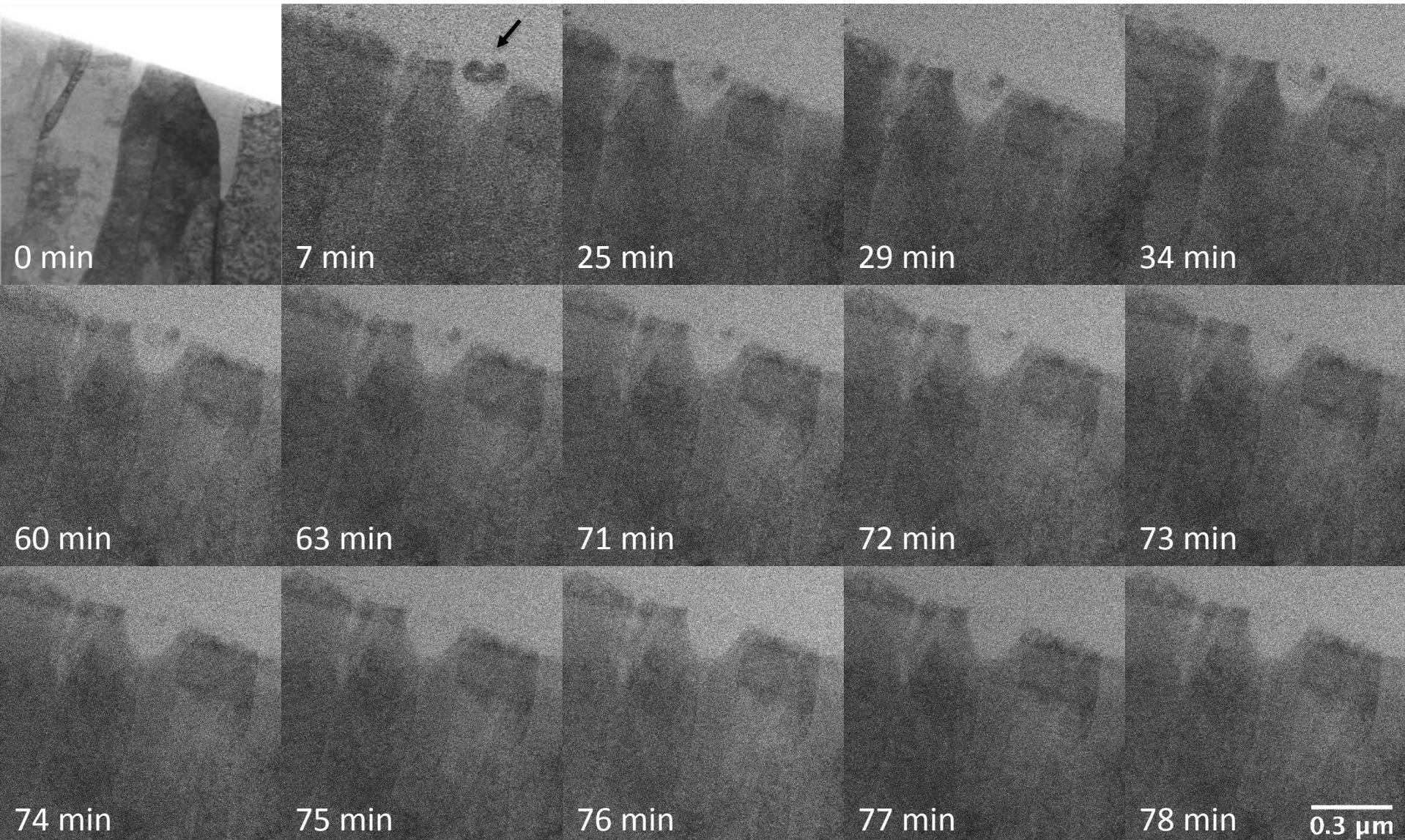
Dry, after 1047 min in liquid, 900
min flow time



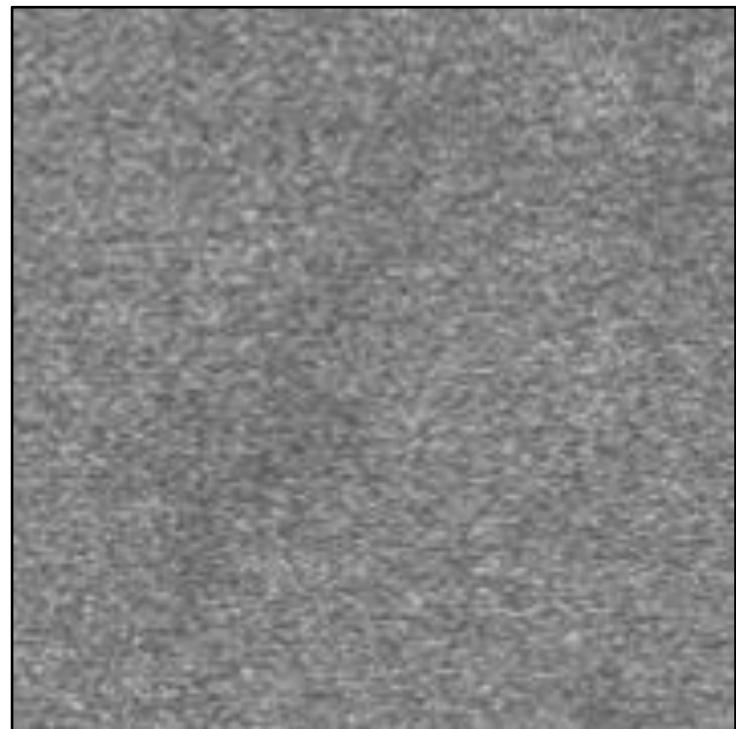
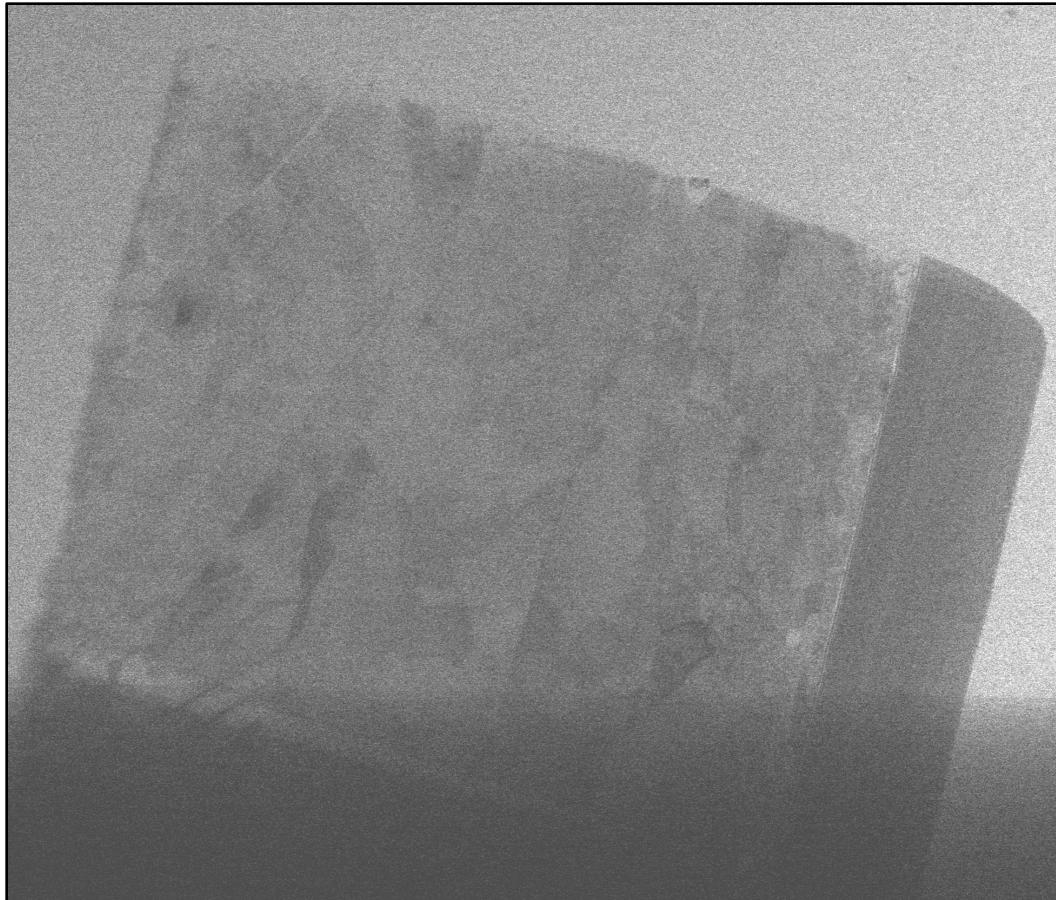
- Initial preferential etching in some areas
- Overall slight etching preference at grain boundaries
- Eventual non-selective etching



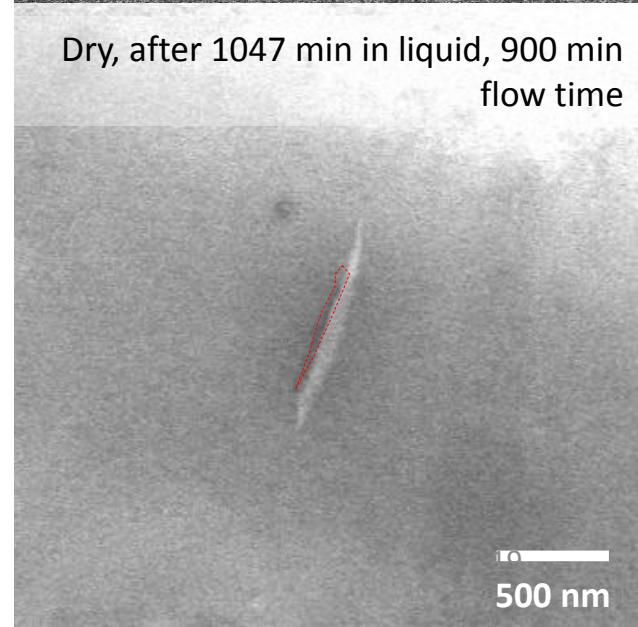
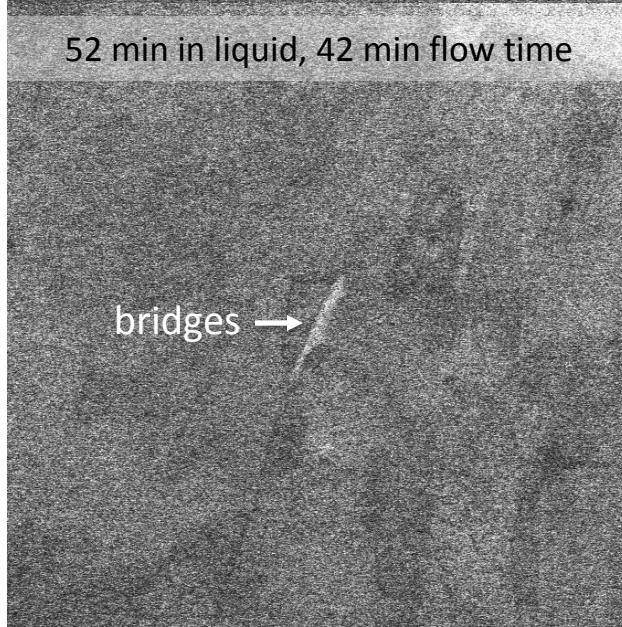
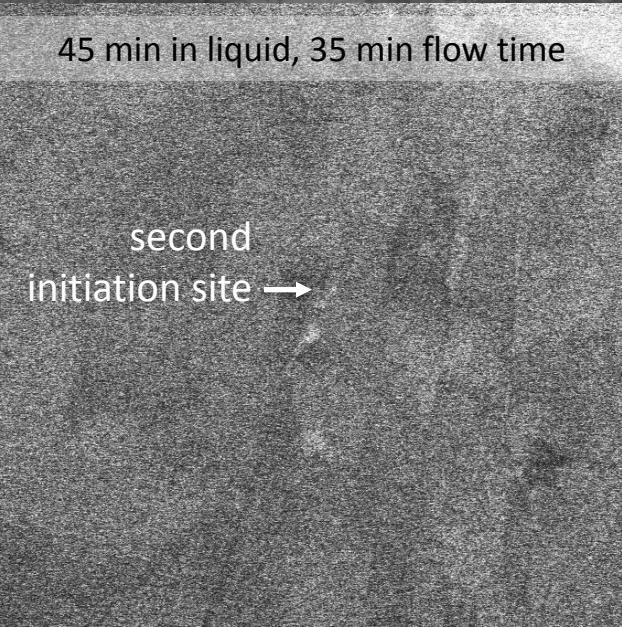
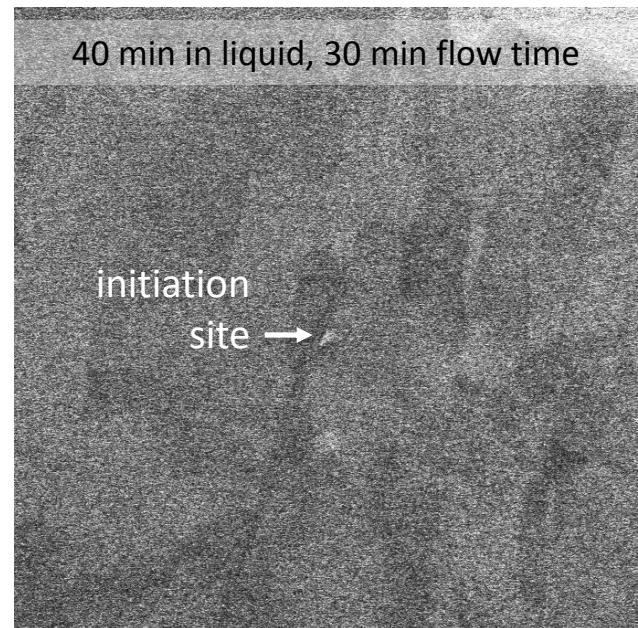
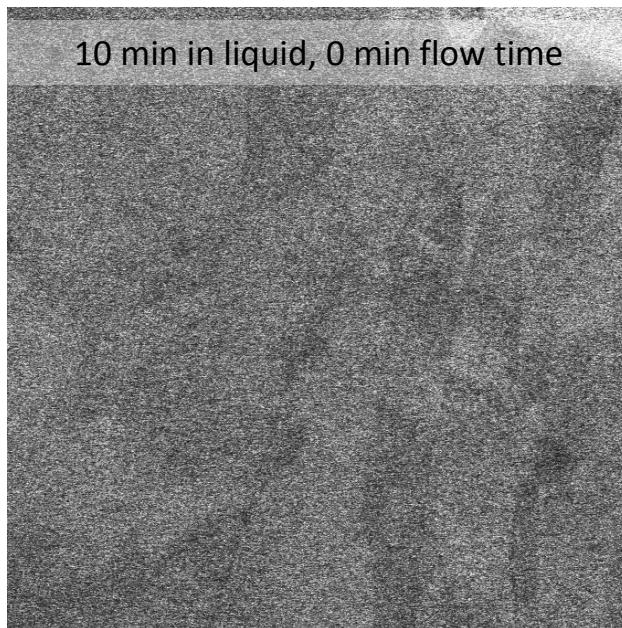
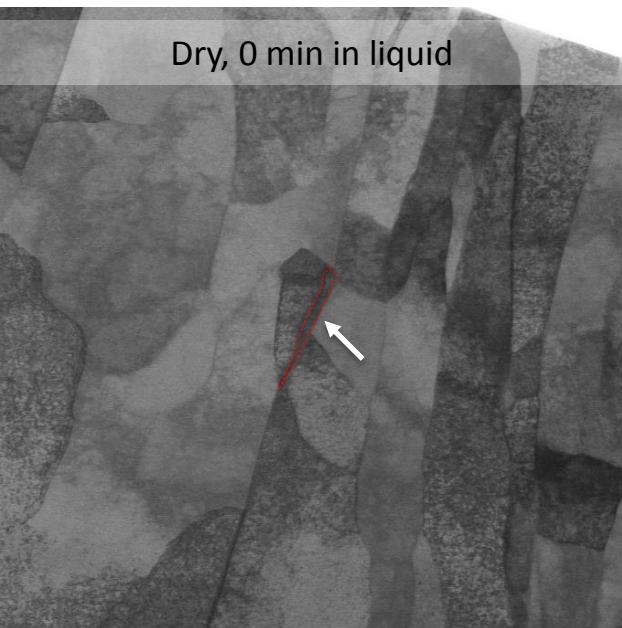
Edge Corrosion of Steel in 0.27 ppm CO₂



Internal GB Etching of Steel in 0.27 ppm CO₂



Internal GB Etching of Steel in 0.27 ppm CO₂



Preferential α -Fe Etching of Steel in 0.27 ppm CO_2

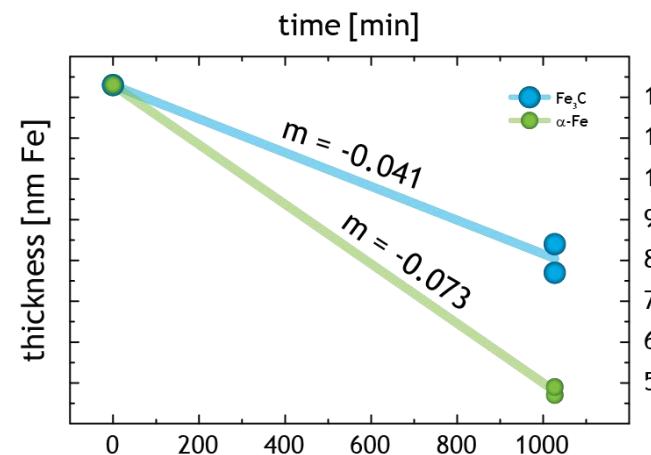
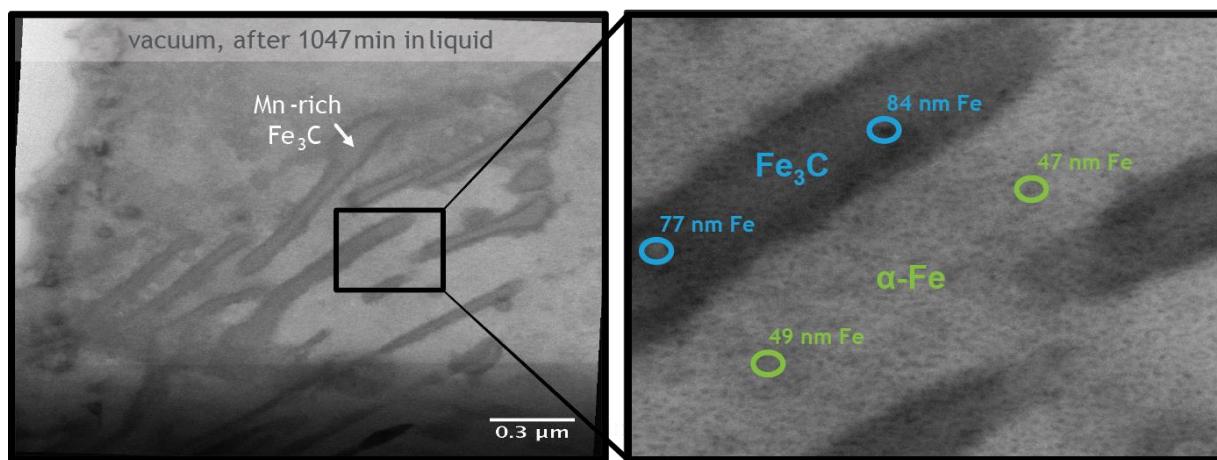
EELS Thickness Measurements After Experiment

Si_3N_4 window = 0.38 IMFP (~ 49 nm)

Initial sample thickness = 1.61 IMFP (~ 123 nm Fe)

1. 1.16 IMFP (~ 77 nm Fe)
2. 0.87 IMFP (~ 49 nm Fe)
3. 1.22 IMFP (~ 84 nm Fe)
4. 0.86 IMFP (~ 47 nm Fe)

$\text{Fe}_3\text{C}/\alpha\text{-Fe}$ thickness ratio = 1.67



Galvanic Coupling in Low-Carbon Steel

Ferrite and cementite phases in contact with electrolyte solution will experience charge transfer from the ferrite to the cementite, causing dissolution of the Fe ions in the ferrite grains

- Larger grain size of cementite will result in faster etching of ferrite grain

GALVANIC SERIES

Galvanic Series in Seawater (supplements Farag Table 3.1, page 65), EIT Review Manual, page 38-2
Tendency to be protected from corrosion, cathodic, more noble end

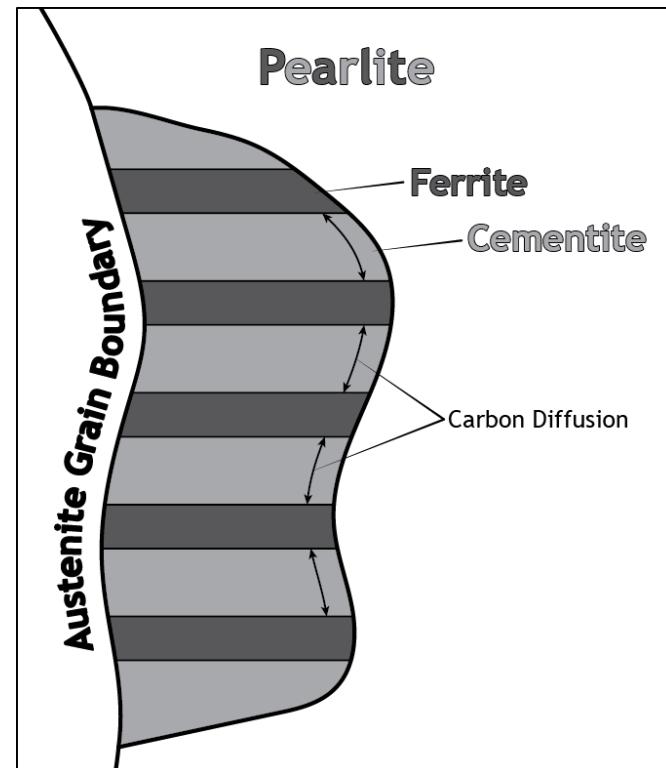
Mercury
Platinum
Gold
Zirconium Graphite
Titanium
Hastelloy C Monel
Stainless Steel (316-passive)
Stainless Steel (304-passive)
Stainless Steel (400-passive)
Nickel (passive oxide)
Silver
Hastelloy 6Ni, 17Cr
Silversolder
Inconel 61Ni, 17Cr
Aluminum (passive Al₂O₃)
70/30 copper-nickel
90/10 copper-nickel
Bronze (copper/tin)
Copper
Brass (copper/zinc)
Alum Bronze Admiralty Brass
Nickel
Naval Brass Tin
Lead-tin
Lead
Hastelloy A
Stainless Steel (active)
316 404 430 410
Lead Tin Solder
Cast iron
Low-carbon steel (mild steel)
Manganese Uranium
Aluminum Alloys
Cadmium
Aluminum Zinc
Beryllium
Magnesium



PASSIVE – will not corrode – act as cathode. These elements are least likely to give up electrons!



ACTIVE – will corrode – act as anode. These elements most likely to give up electrons!



10-20 mV between ferrite and cementite

Pipeline Steel Corrosion: Sour Corrosion H₂S & CO₂

Type of corrosion product controls the corrosion rate

Temperature and partial pressure of H₂S affect the deposition mechanism of film

Polymorphous FeS Corrosion products.

Name	Chemical formula	Crystal structure	Properties
Amorphous	FeS	No specific crystal	Unstable, converts into mackinawite quickly
Mackinawite	Fe _{1+x} S ($x = 0.02-0.41$)	Tetragonal, two-dimensional layer	Metastable, the initial corrosion product
Cubic FeS	FeS	Cubic	Very unstable, can transform into mackinawite, troilite or pyrrhotite
Troilite	FeS	Hexagonal	Stoichiometric end member of the Fe _{1-x} S group ($x = 0$)
Pyrrhotite	Fe _{1-x} S ($x = 0.05-0.21$)	Monoclinic or hexagonal (main)	Thermodynamically stable
Pyrite	FeS ₂	Cubic	Thermodynamically stable

Kermani and Morshed, Cri. Rev. Corr. Sci. Eng. **59**, 659 (2003).

Corrosion doesn't occur on top of the scale film, but below it

Wax protective film: diffusion of CO₂ through wax layer

Mechanisms of the Anodic Dissolution of Iron in CO₂-Containing Media¹⁹⁻²⁰

Reaction No.	Reaction or Equilibrium	pH < 4	4 < pH < 5	pH > 5
1a	$\text{HCO}_3^- \leftrightarrow (\text{HCO}_3^-)_{\text{ads}}$	1a	1a	1b
1b	$\text{CO}_2 + (\text{OH}^-)_{\text{ads}} \leftrightarrow (\text{HCO}_3^-)_{\text{ads}}$			
2	$(\text{HCO}_3^-)_{\text{ads}} \Rightarrow (\text{HCO}_3^+)_\text{ads} + \text{e}^-$	\Rightarrow	\Rightarrow	RDS \Rightarrow
3	$(\text{HCO}_3^+)_\text{ads} \Rightarrow (\text{HCO}_3^+)_\text{ads} + \text{e}^-$	\Rightarrow	RDS $\xrightarrow{(A)}$	\Rightarrow
4	$(\text{HCO}_3^+)_\text{ads} + \text{OH}^- \Rightarrow (\text{CO}_3)_{\text{ads}} + \text{H}_2\text{O}$	RDS \Rightarrow	\Rightarrow	\Rightarrow
5	$\text{Fe} - (\text{CO}_3)_{\text{ads}} + \text{H}_2\text{O} \Rightarrow \text{Fe}^{++} + \text{HCO}_3^- + \text{OH}^-$	\Rightarrow	\Rightarrow	\Rightarrow
1 \rightarrow 5	Tafel slope (mV/log)	$60/2 = 30$	$60/1.5 = 40$	$60/0.5 = 120$
1 \rightarrow 5	H ⁺ reaction order	-2	-1	0
1 \rightarrow 5	CO ₂ reaction order	1	1	1

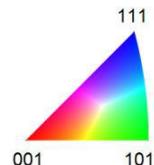
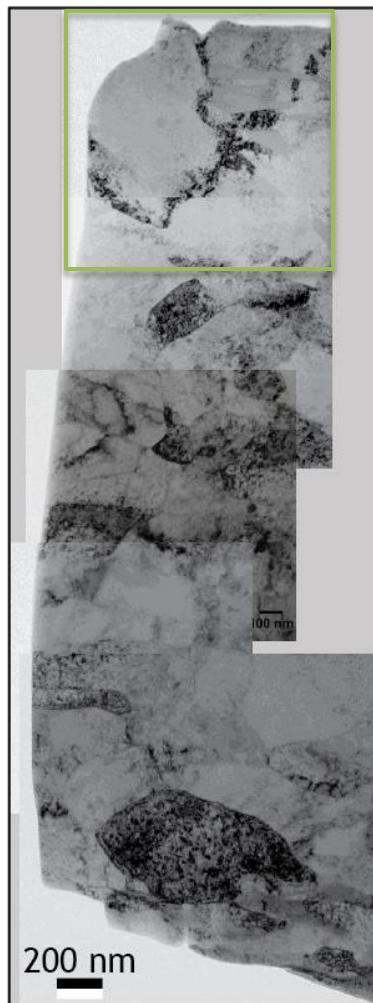
^(A) RDS = rate-determining step.

Shi et al., Corr. Sci. **102**, 103 (2016).

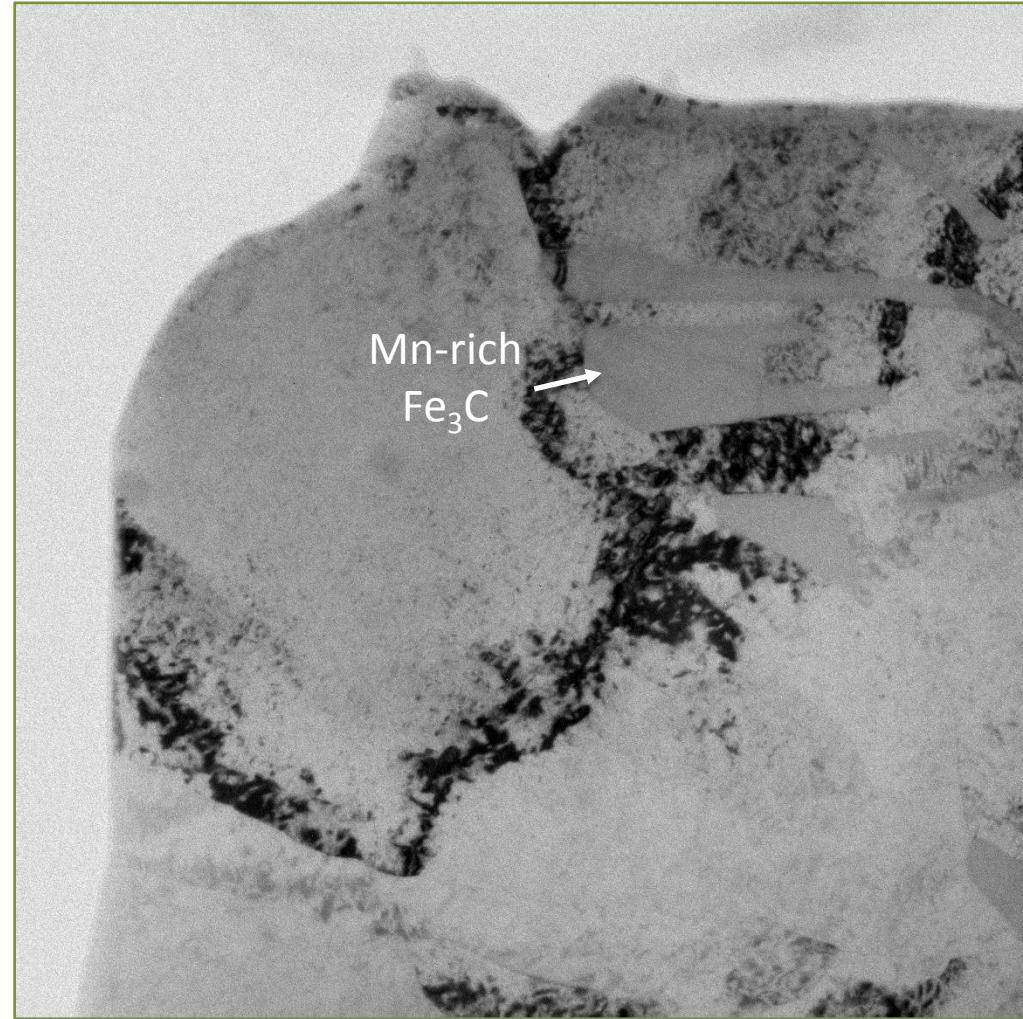
* H₂S can either accelerate corrosion or reduce by providing a protective film on ferrite (small amounts of H₂S)

* Iron sulfide is more protective than FeCO₃

Grain Orientation Mapping of BCC Ferrite

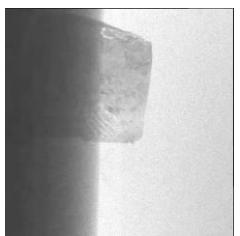


orientation
map

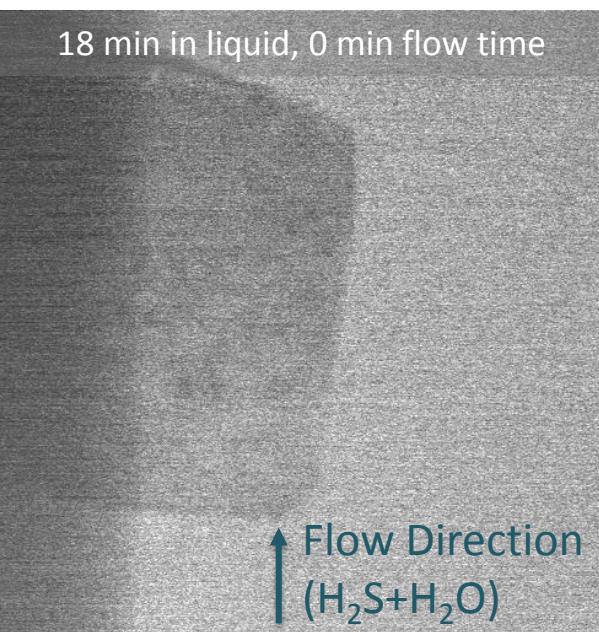


Steel in 5 ppm H₂S + 45 ppm CO₂: Microstructural Evolution Overview

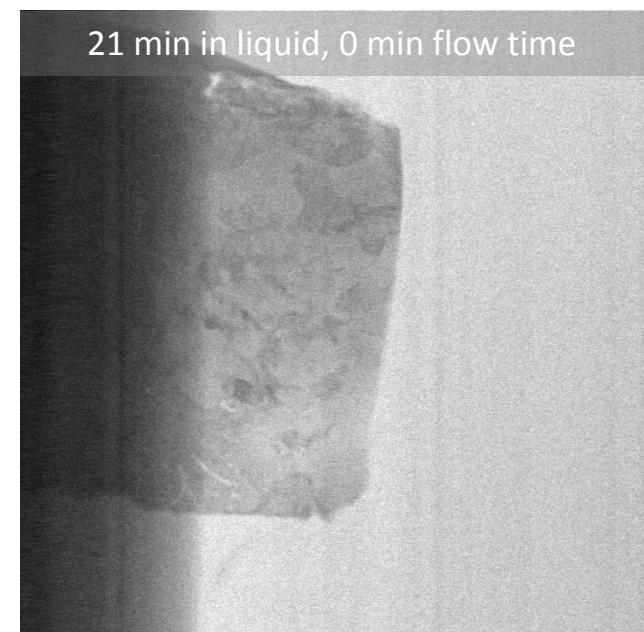
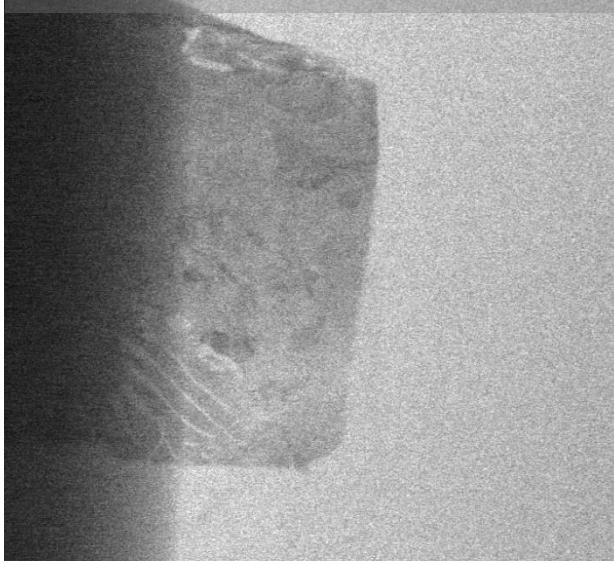
- Overall thinning
- White boxes
 - Preferential etching of Fe₃C (over α -Fe)



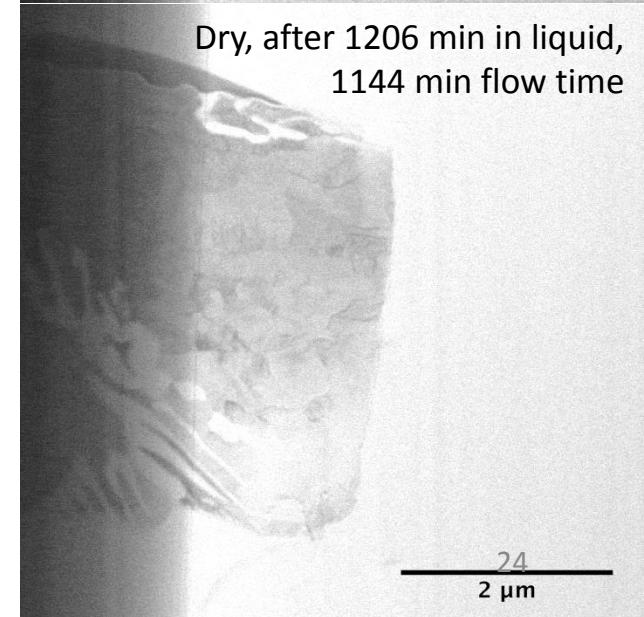
62 min in liquid, solution flow start



199 min in liquid, 137 min flow time

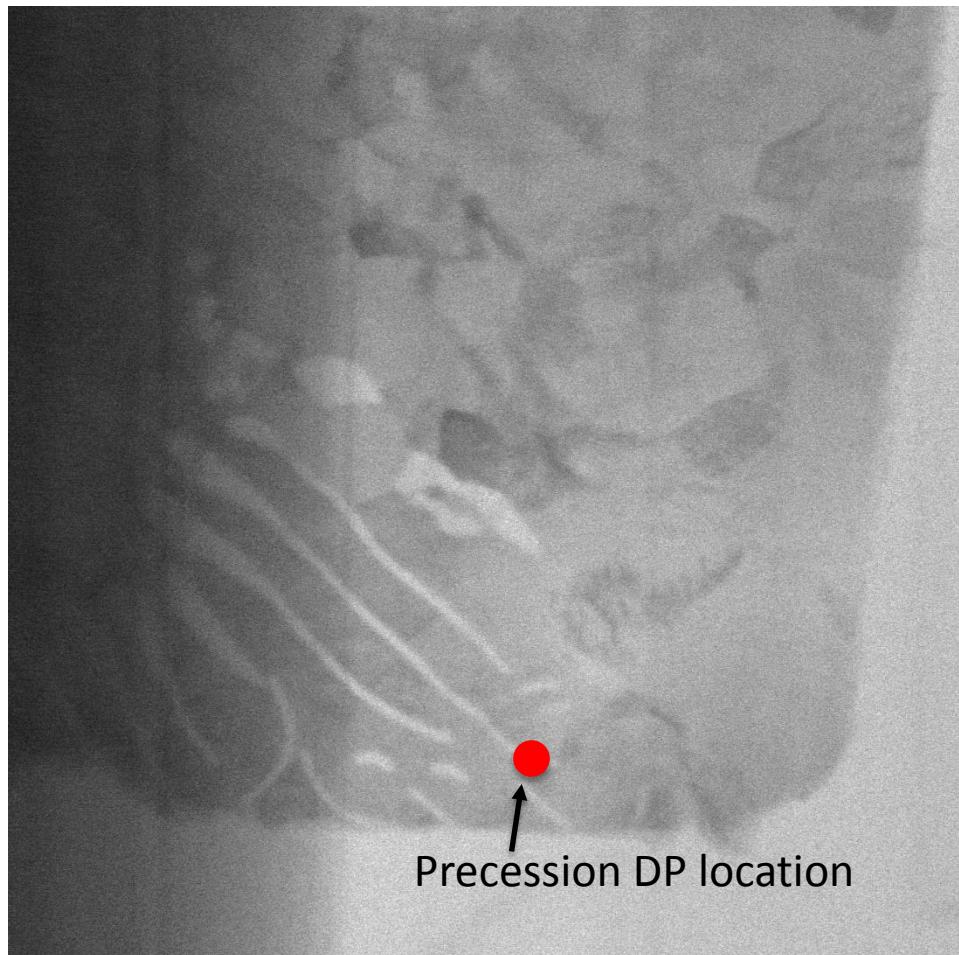


Dry, after 1206 min in liquid,
1144 min flow time

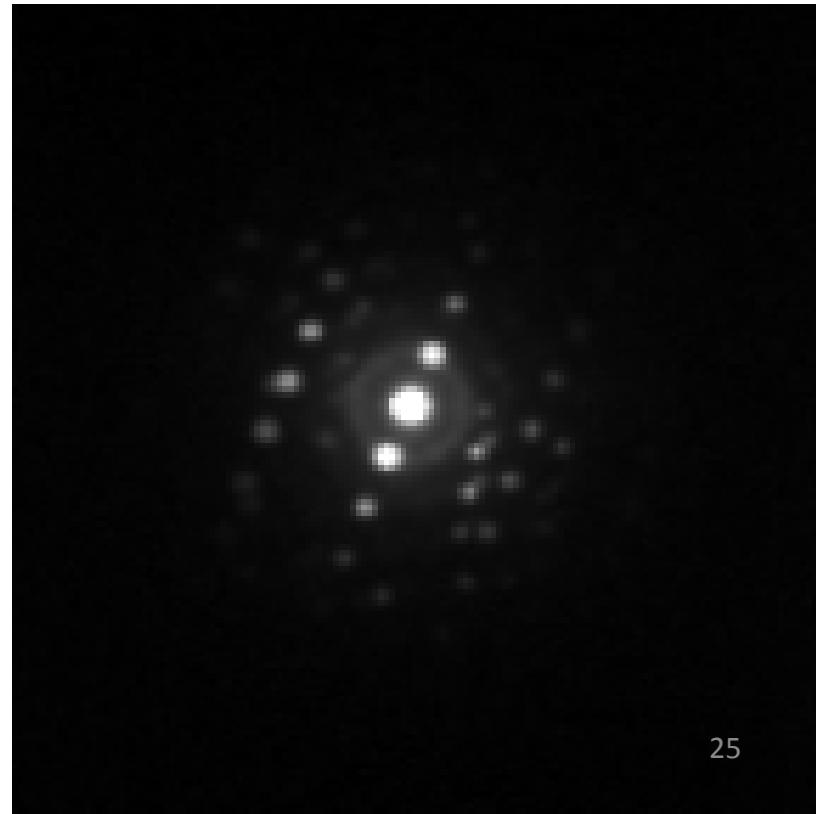


Fe₃C Preferential Etching in 5 ppm H₂S + 45 ppm CO₂

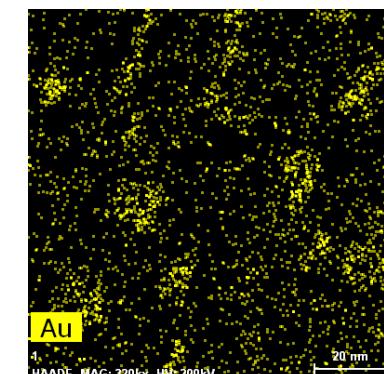
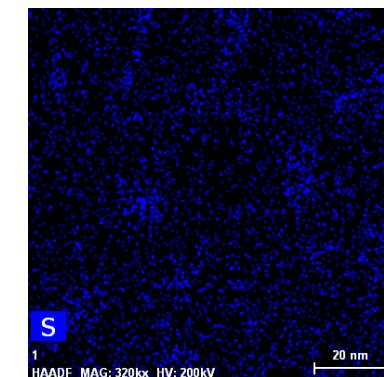
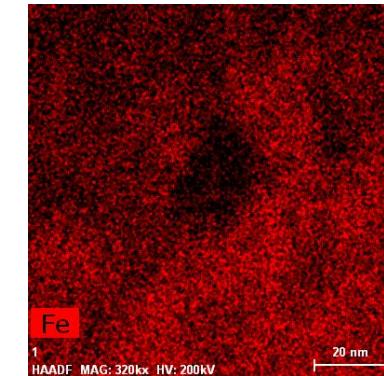
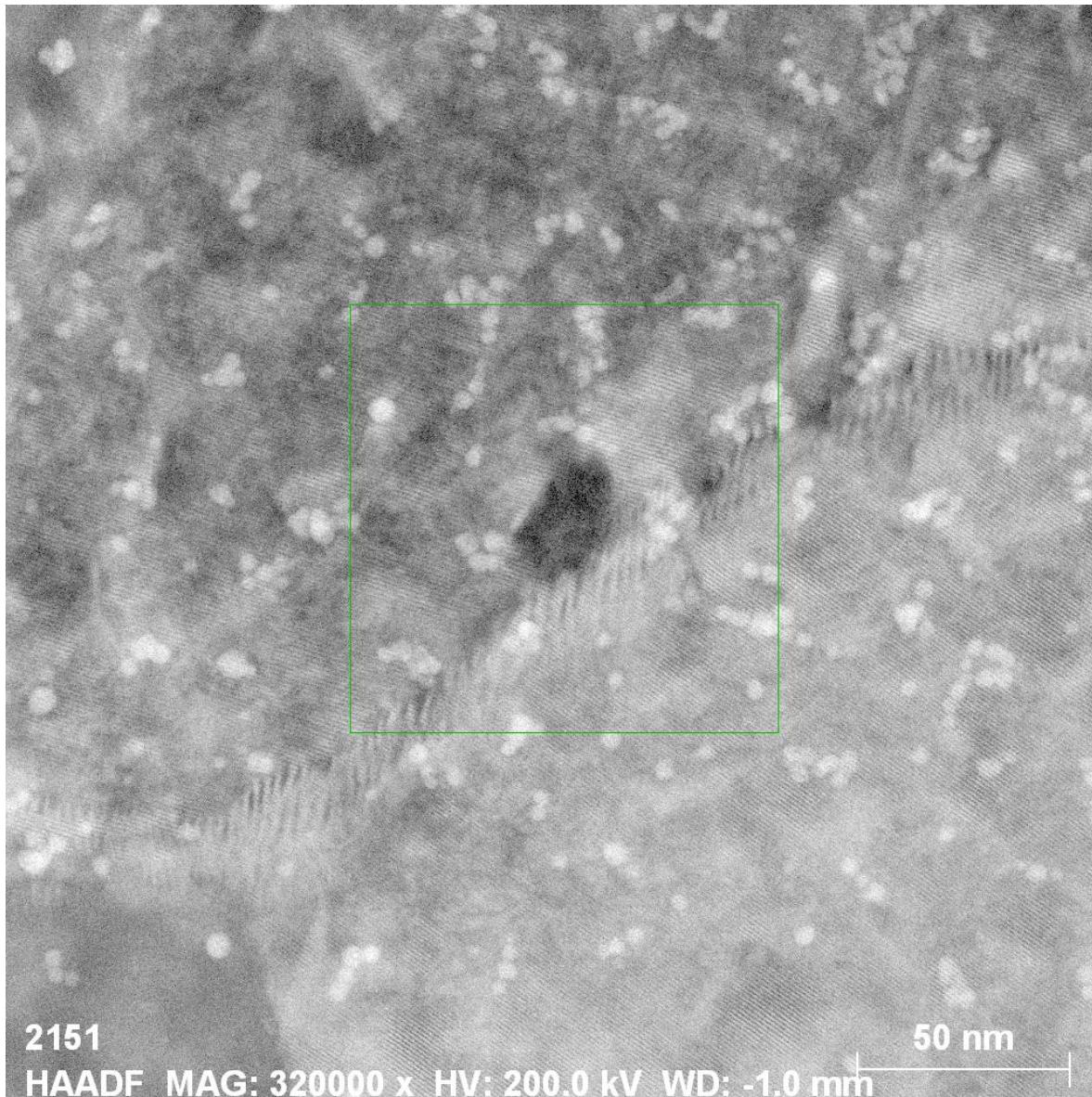
- Lamellar morphology indicates Fe₃C
- Pre-experiment precession diffraction pattern acquired at lamella indicates Fe₃C



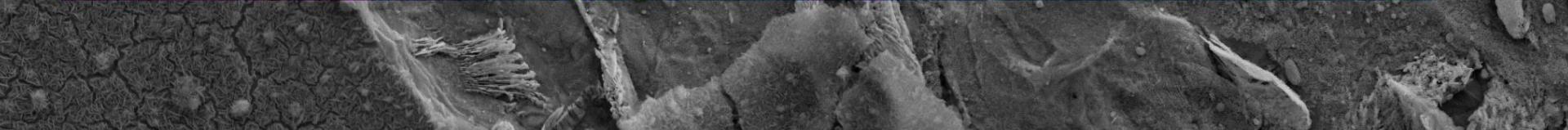
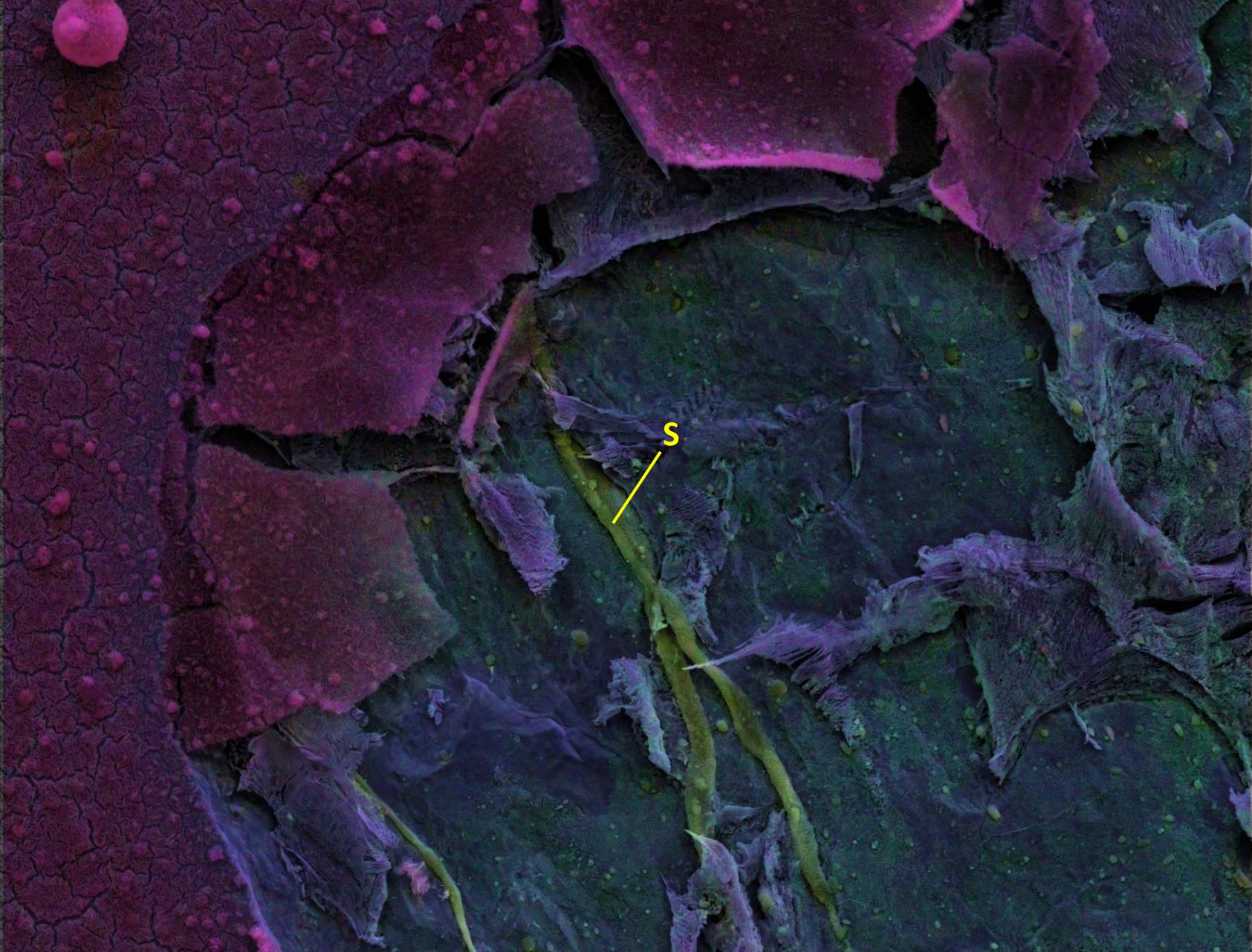
α-Fe [014] ZA
Fe₃C [121] ZA

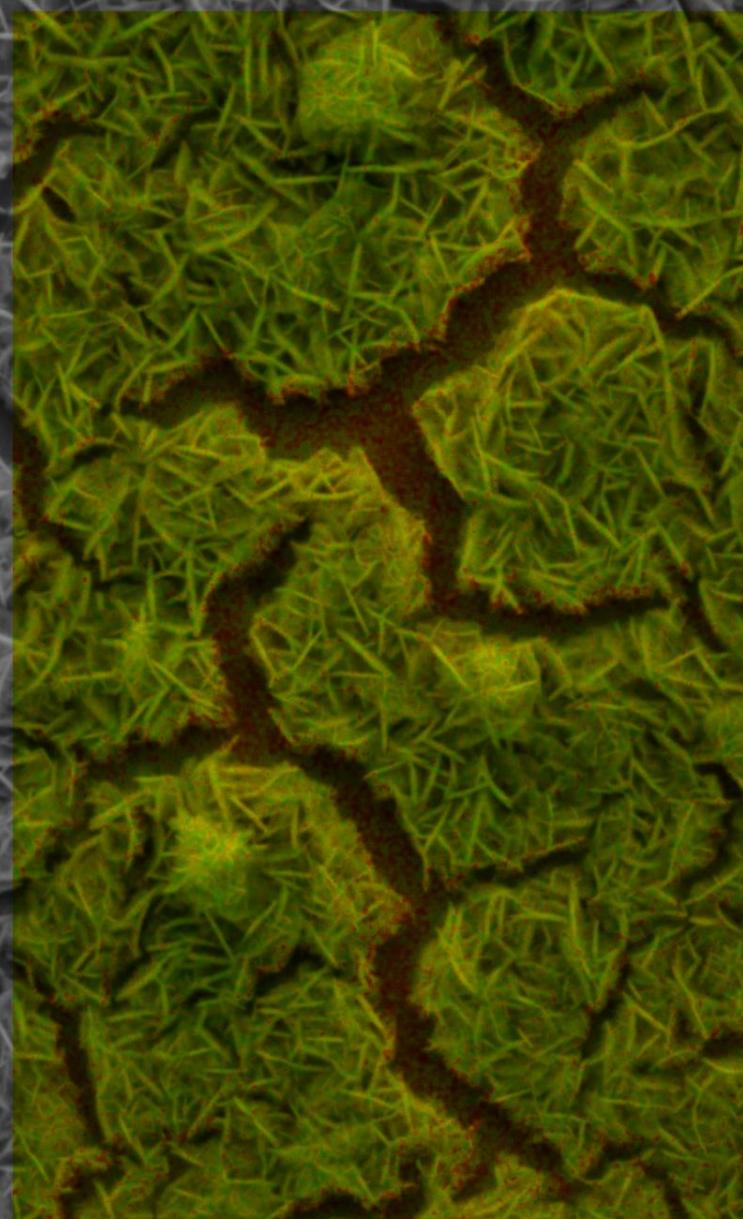


Determination of Scale Products on Surface



Fe
O
C
S

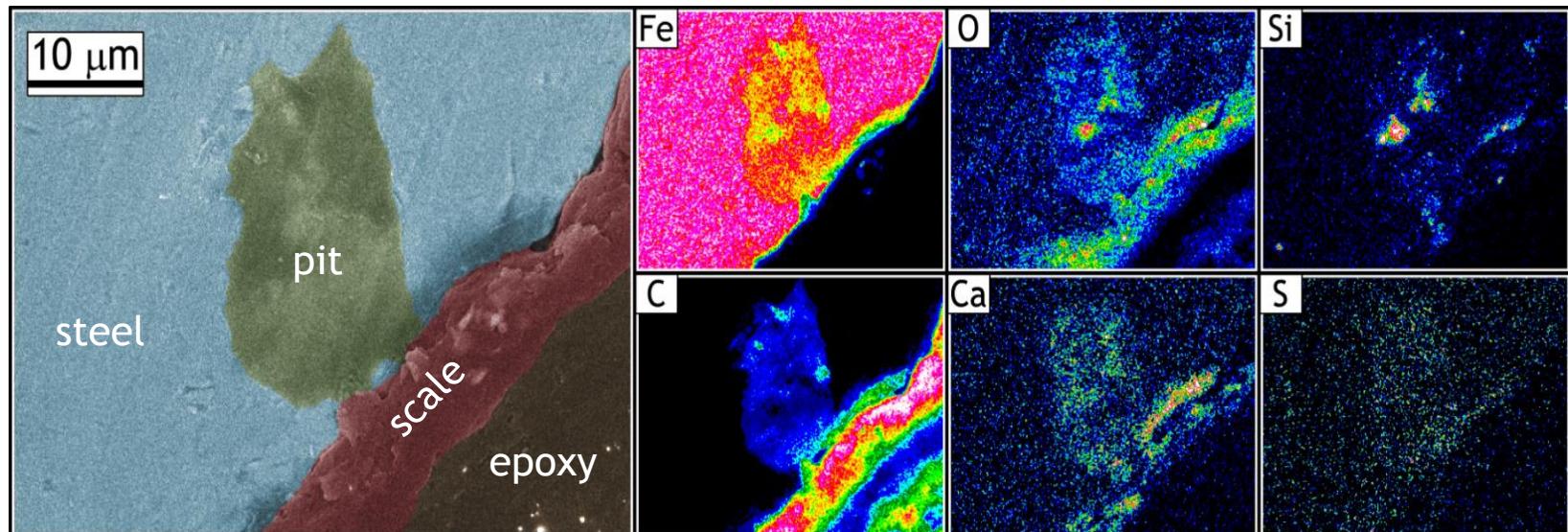




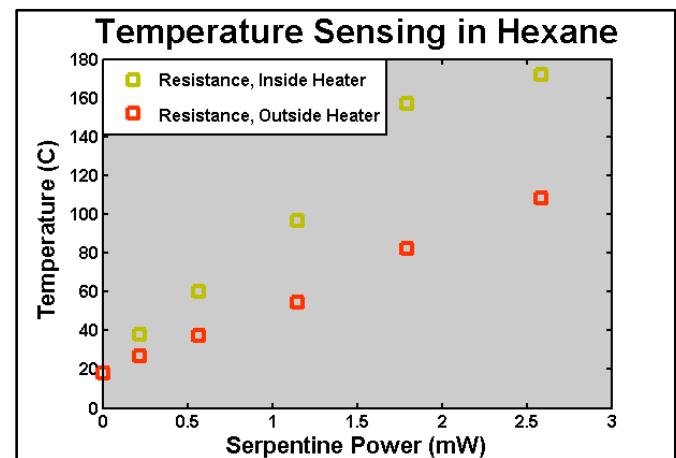
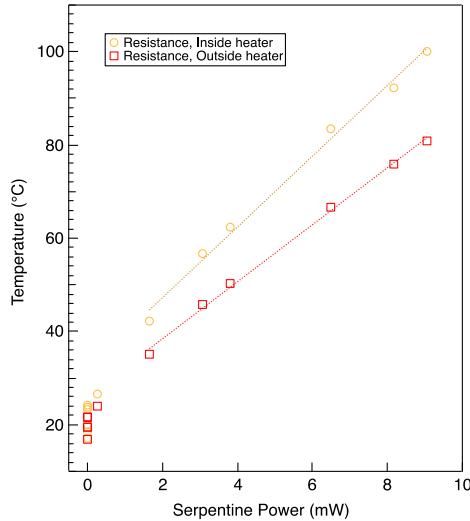
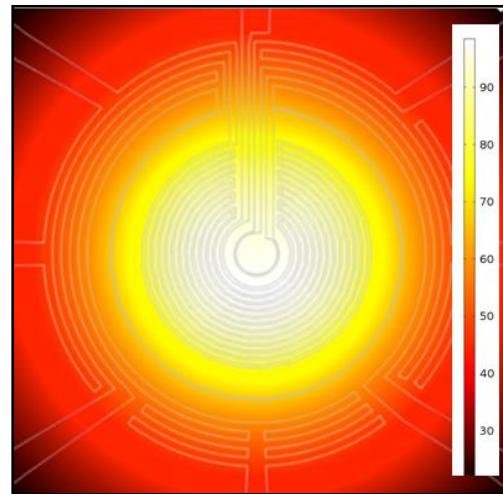
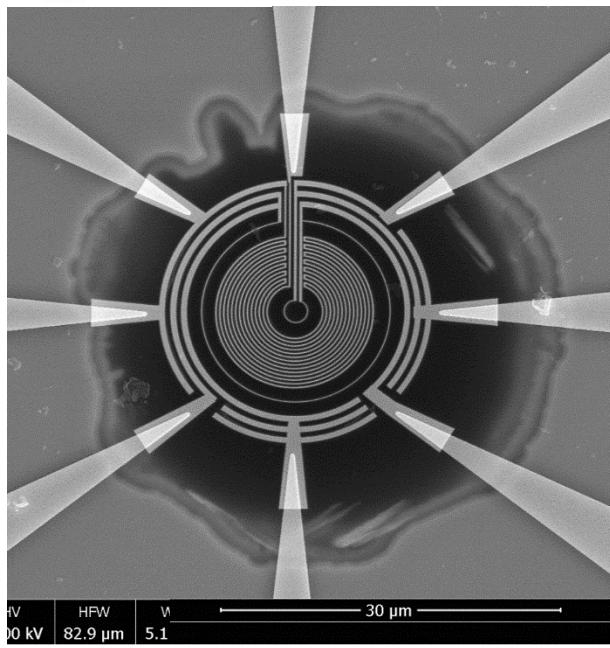
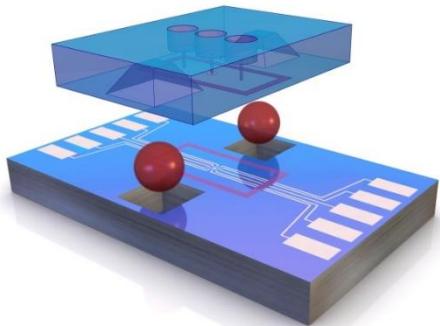
Fe
O
C

Summary of Corrosion Initiation in Low-Carbon Steel

- Sweet: 0.27 ppm CO_2 etches the low-carbon steel
 - Evidence of intergranular corrosion at $\text{Fe}_3\text{C}/\alpha\text{-Fe}$ interface
 - Preferential etching of $\alpha\text{-Fe}$ over Fe_3C
- Sour: 5 ppm H_2S with 45 ppm CO_2
 - Fe_3C preferentially etches over $\alpha\text{-Fe}$
 - Unlike the CO_2 only solution



Temperature Dependence of Corrosion



Liquid thickness plays a larger role in heating calibration than the liquid thermal conductivity, therefore measurement of the temperature changes on column is preferable

Center for Integrated Nanotechnologies

CINT Core Facility: Albuquerque, NM



CINT Gateway Facility: Los Alamos, NM



Department of Energy, Basic Energy Sciences national user facility to provide expertise and instrumentation free of charge to support accepted peer-reviewed nanoscience research



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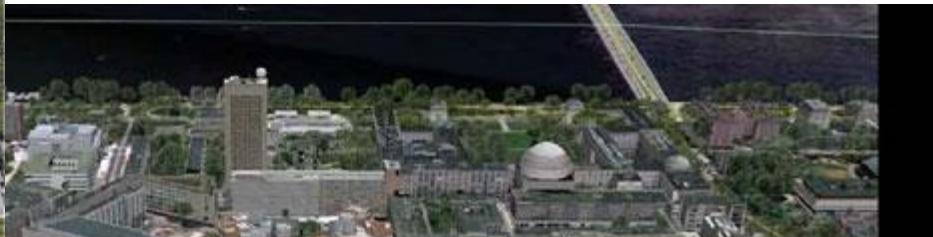


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