

# Steel Corrosion Mechanisms during Pipeline Operation: In-Situ Characterization

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# Global problem

annual US corrosion costs

\$276,000,000,000

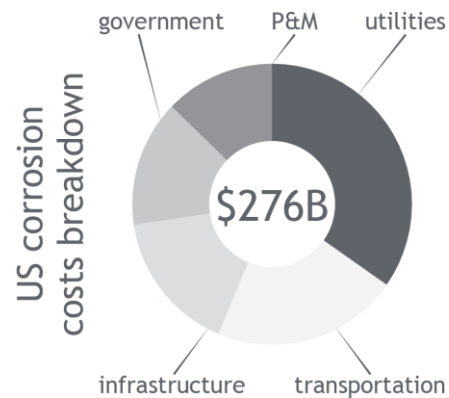
\$ 276 B



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**3.1% US GDP lost to corrosion**  
investing in controls | dealing with failures

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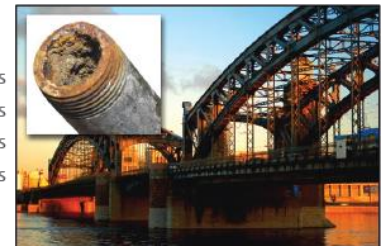
electrical utilities  
gas distribution  
drinking water  
sewers



ships  
aircraft  
motor vehicles  
railroad cars



bridges  
railroads  
airports  
ports



oil & gas pipelines  
petroleum refining  
mining  
chemical/pharma



# Pipeline Steel Corrosion: Oil and Gas Extraction

annual US corrosion costs

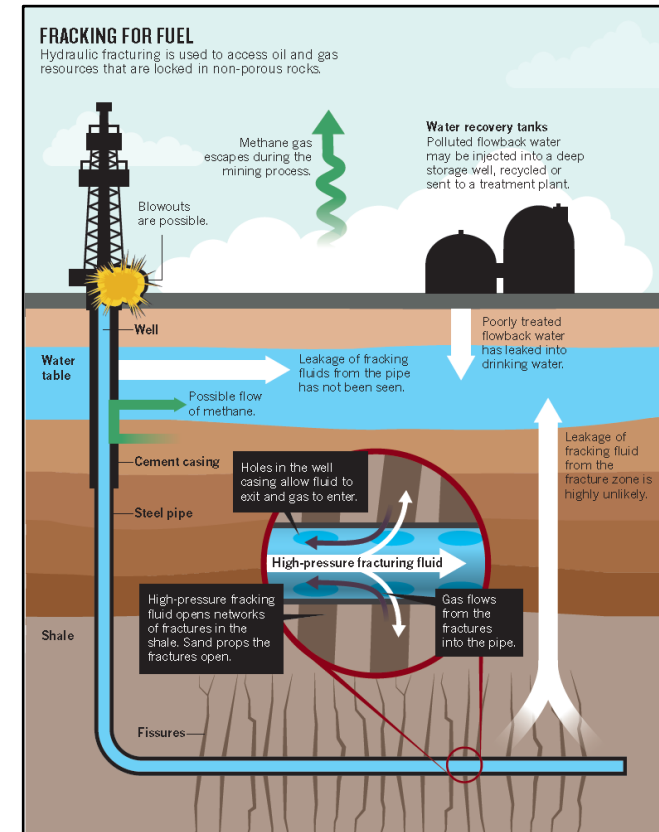
\$276,000,000,000

\$ 276 B



**3.1% US GDP lost to corrosion**  
investing in controls | dealing with failures

Steel failure caused by local corrosion, pitting, and eventual cracking



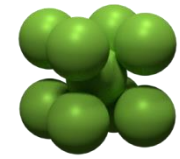
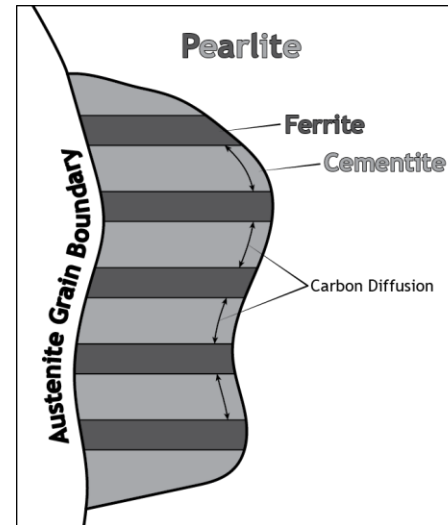
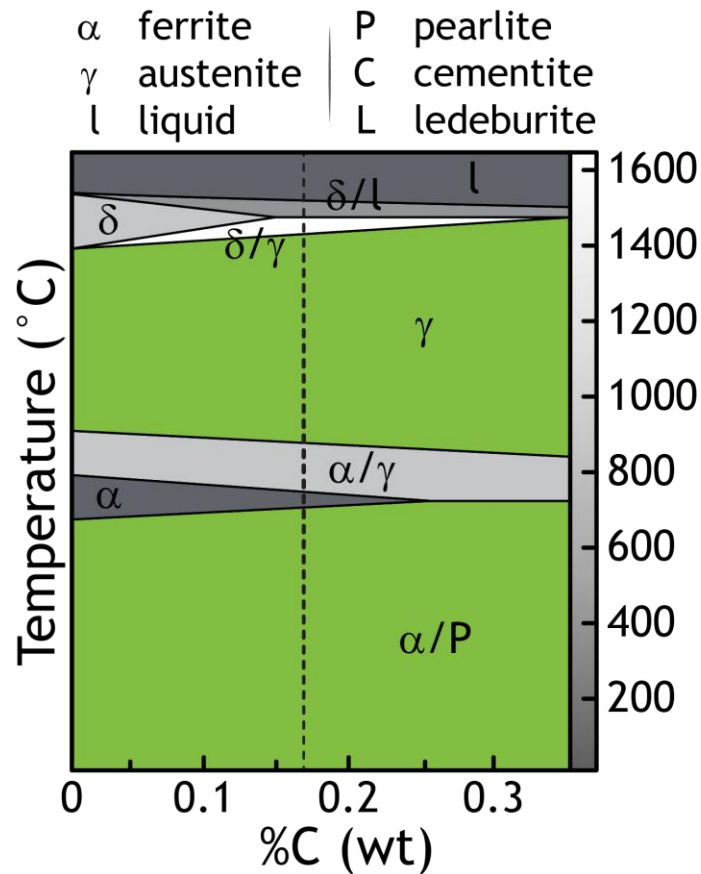
Howarth et al., Nature **477**, 271 (2011)

Mechanisms for pipeline corrosion initiation are unclear

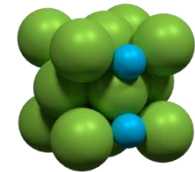
- Grain boundaries are highly susceptible to corrosion in atm environments
- Cementite acts as a cathode, while Fe dissolution occurs in ferrite or pearlite structures, deviation of 10-20 mV between ferrite and cementite (Bai et al, 2015)
- Surface film peeling exposes new surfaces to continue corrosion



# Structure & Composition of 1018 Carbon Steel

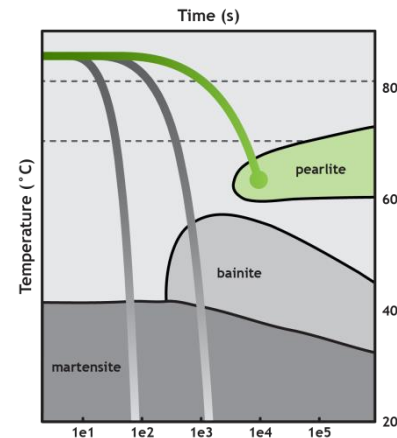


Ferrite



Cementite

**Pearlite:** alternating layers of ferrite (88 wt%) and cementite (12 wt%)



Element	Mass %
Fe	98.305
C	0.160
Mn	0.710
Cu	0.345
Si	0.169
Cr	0.116
Ni	0.107

- 1018 is forged from 1150 – 1280 °C down to a temperature in the area of 600 – 650 °C



# Pipeline Steel Corrosion: Sweet Corrosion CO<sub>2</sub>

Water reacts with dissolved CO<sub>2</sub> to form carbonic acid

Corrosion rate dependent on partial pressure of CO<sub>2</sub> and temperature (affects surface film that is formed)

Protective scale: iron carbonate films form, FeCO<sub>3</sub>

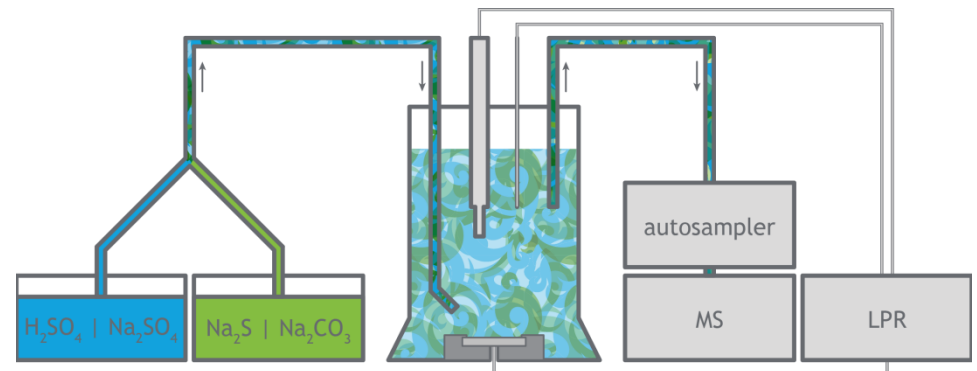
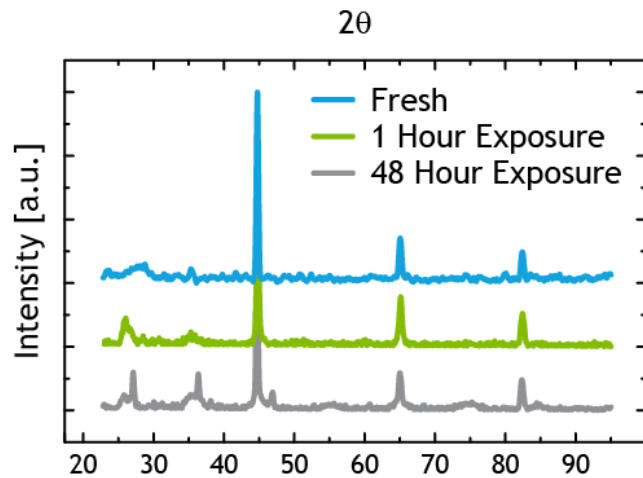
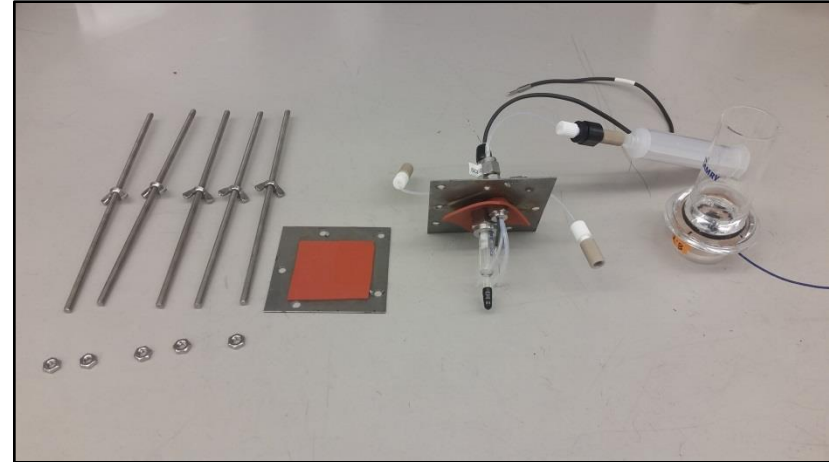
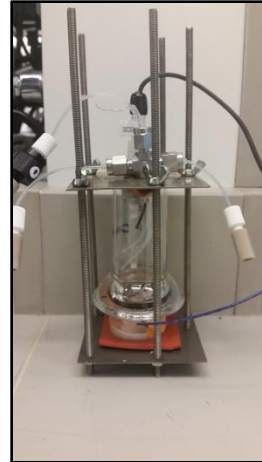
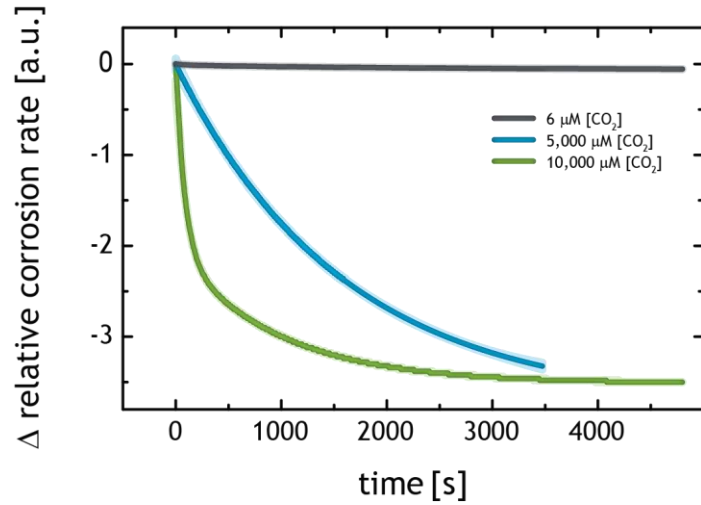
Water composition effects the buffering capacity

## Determinant Parameters:

- Solution composition: pH, wetting, phase ratios
- Salt composition (NaCl, K<sup>+</sup>, Ca<sup>2+</sup>) and concentrations
- CO<sub>2</sub> content
- Temperature & Pressure
- Steel surface: corrosion film, protective molecules
- Fluid dynamics, flow rate (mass transport of CO<sub>2</sub>)
- Steel composition

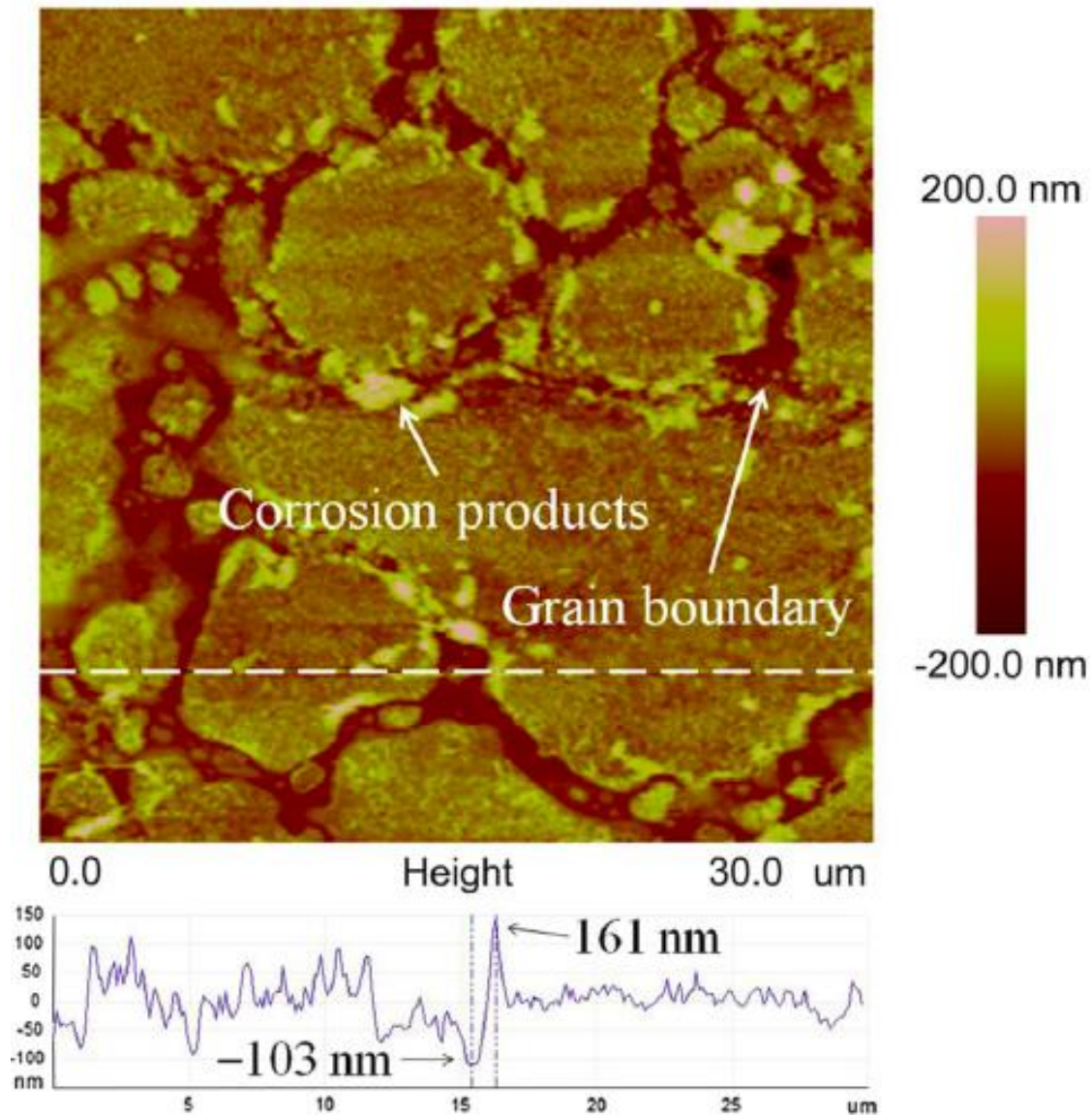


# Partnership with ASC to tackle corrosion problem



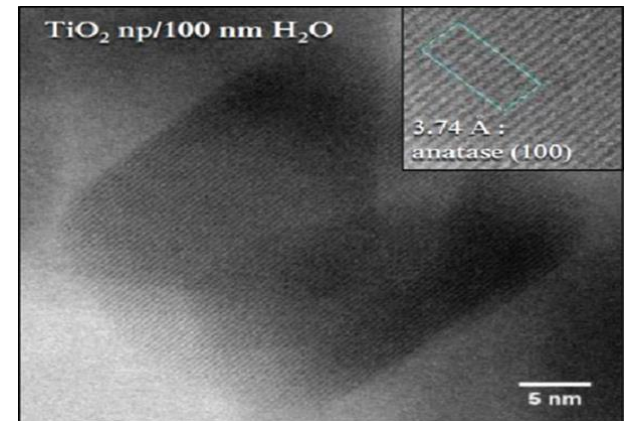
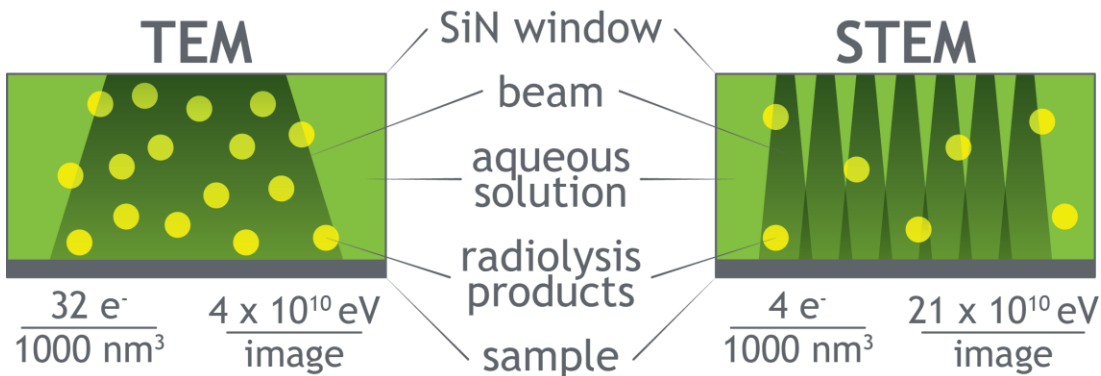
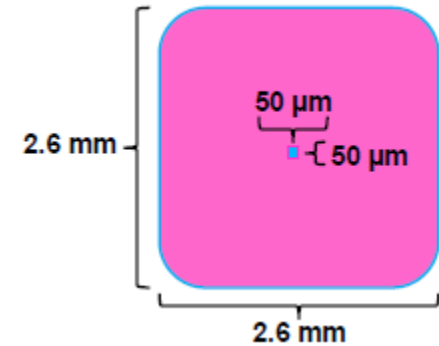
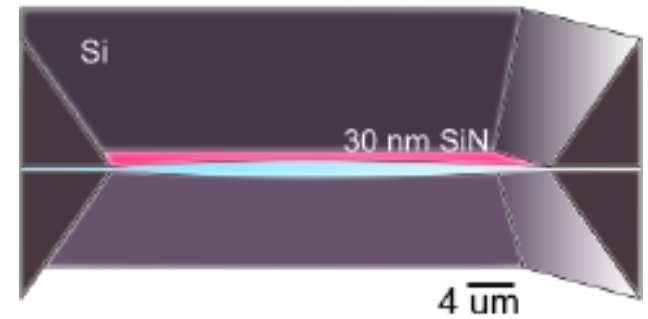
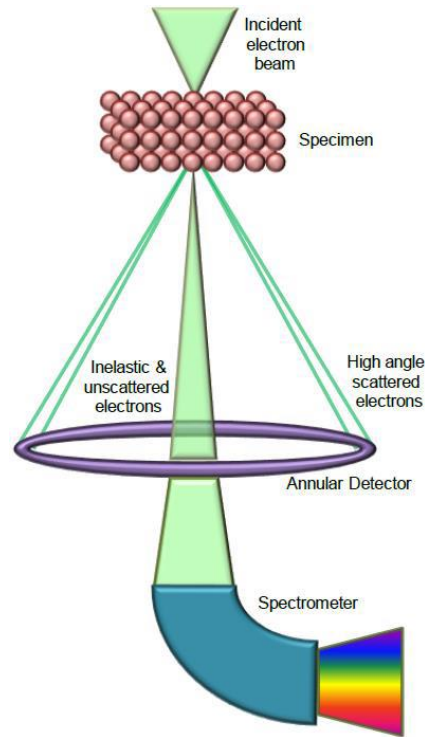
# Corrosion Initiates at Grain Boundaries

Which grain boundaries? Nanoscale sites?

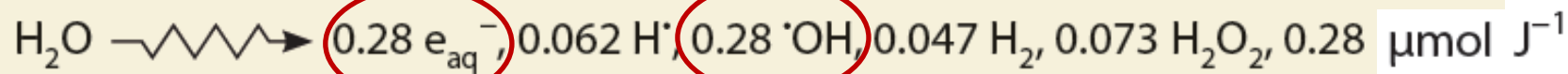




# In-situ TEM Ideally Suited for Nanoscale Corrosion

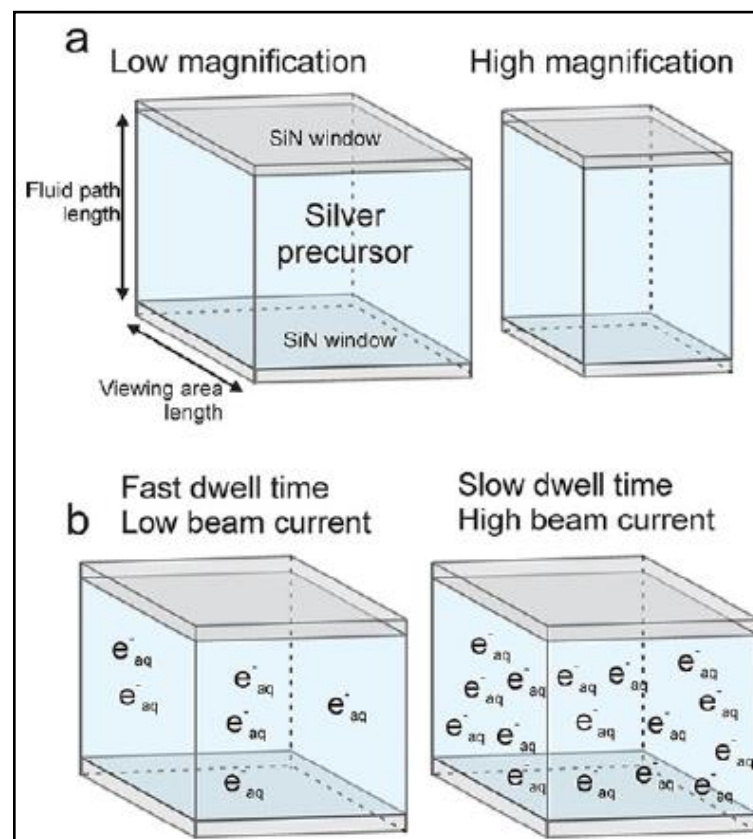
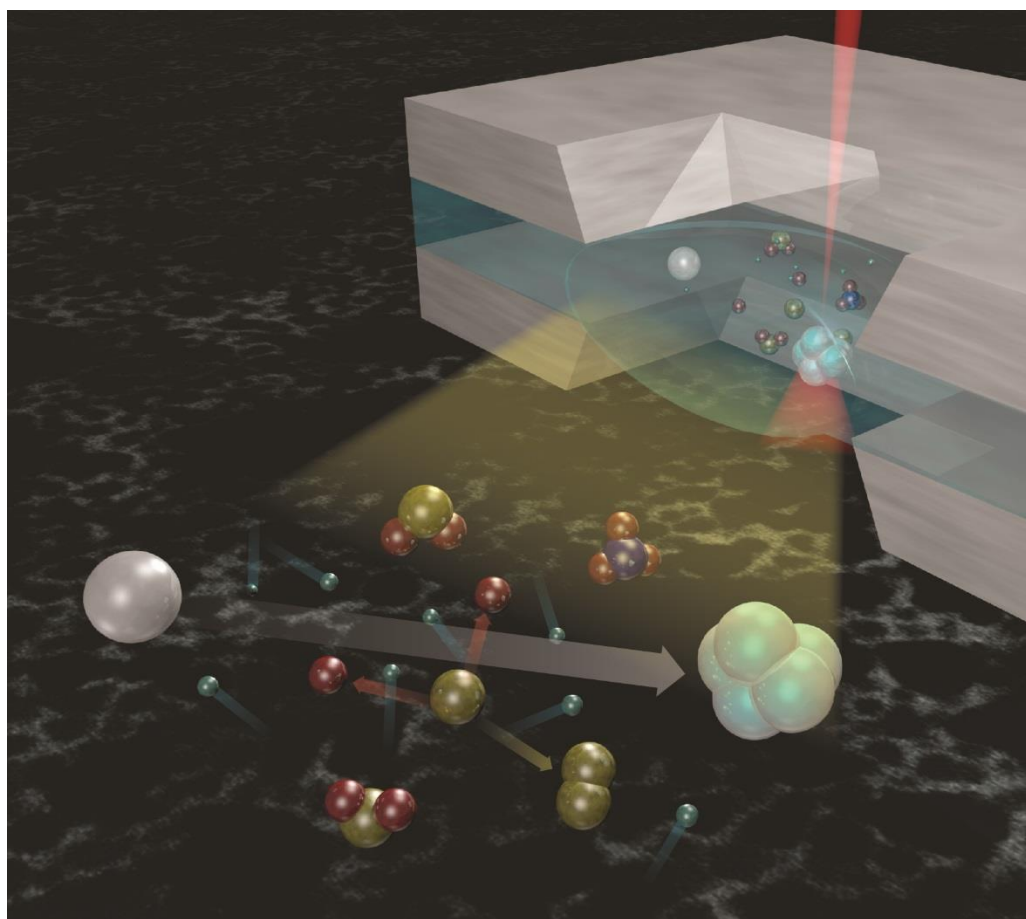


# Electron Beam Radiolysis of Aqueous Media



Buxton, VCH Weinheim (1987)

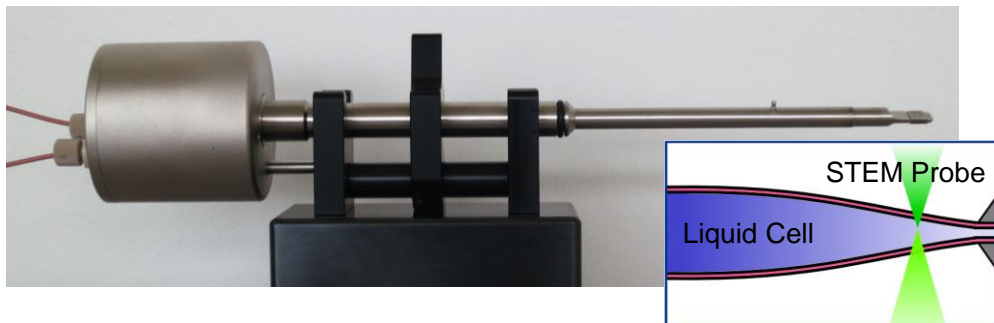
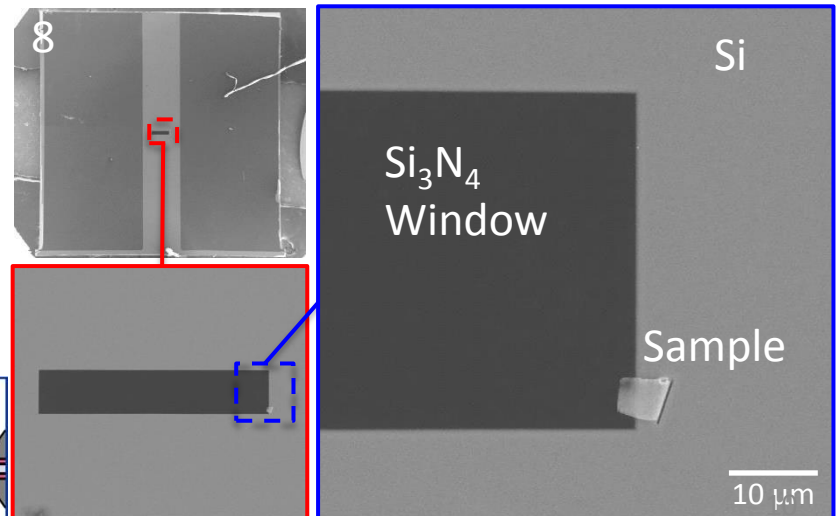
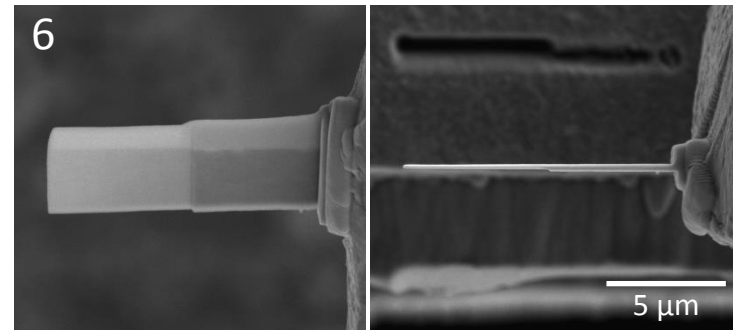
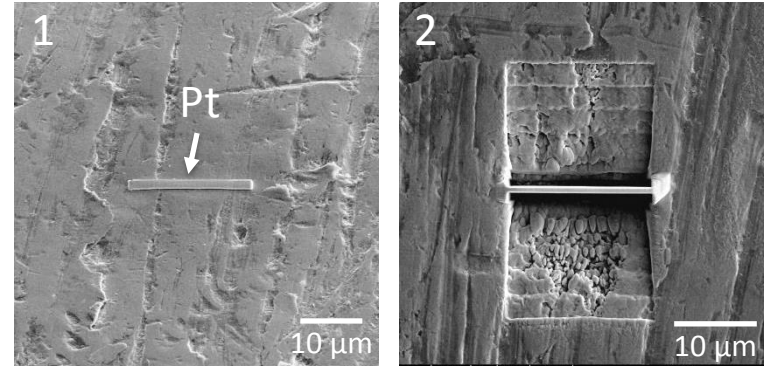
\*Amount of products formed depends on the electron dose



Woehl et al. ACS Nano 6, 8599 (2012).

# Sample Preparation and Screening

1. Deposit protective Pt layer
2. Trench into low-carbon steel
3. U-cut
4. Attach to micromanipulator
5. Transfer to TEM grid
6. 3 step thinning process
7. Precession Electron Diffraction mapping
8. Transfer to SiN membrane chip for corrosion experiment
9. Load sample in Hummingbird Scientific Liquid Cell TEM holder with DI water between top and bottom chip.
10. Prefill intake line with DI water.



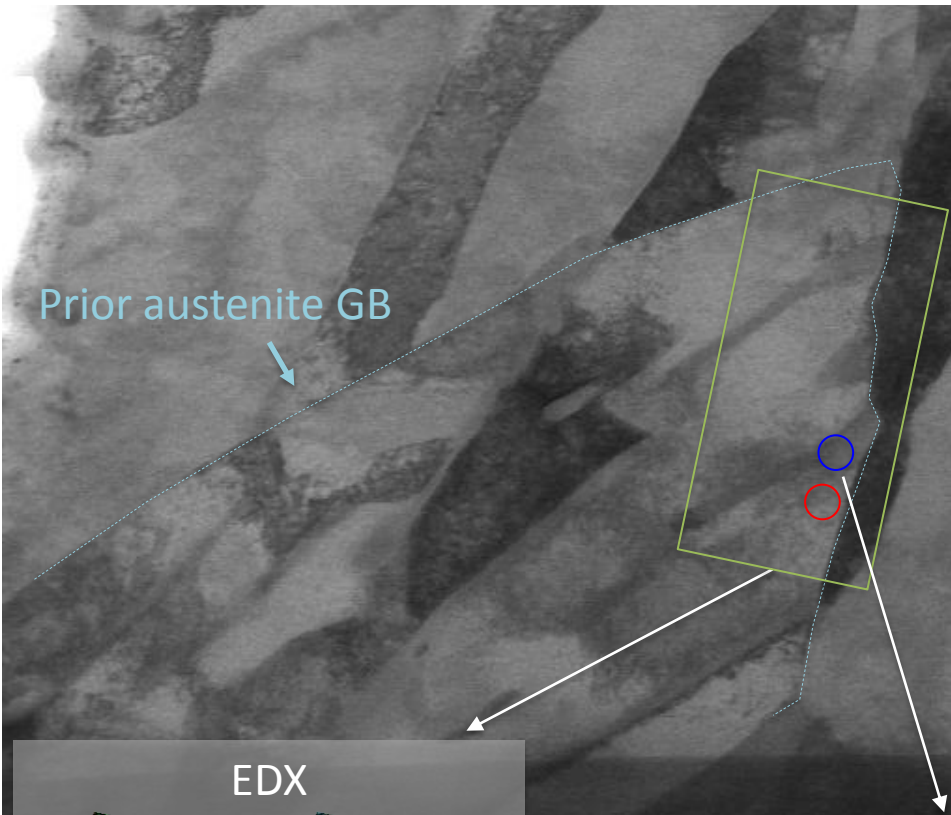


# Focused Ion Beam Sample Preparation

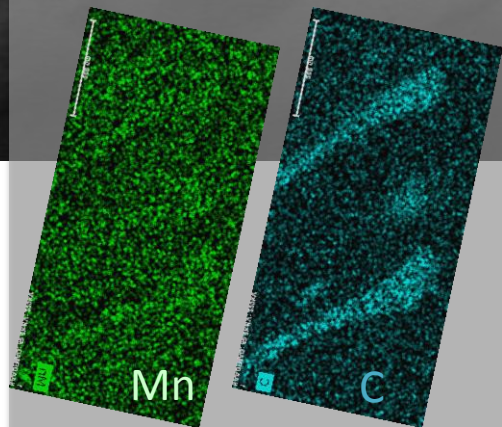


# Low-Carbon Steel Microstructure

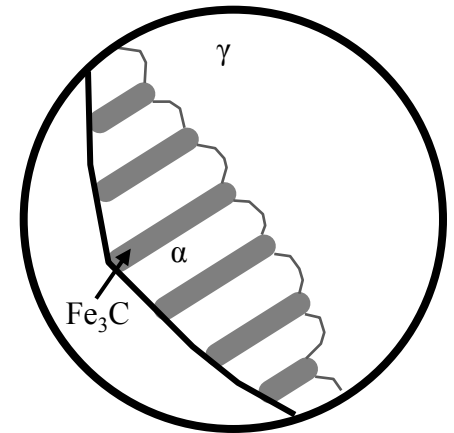
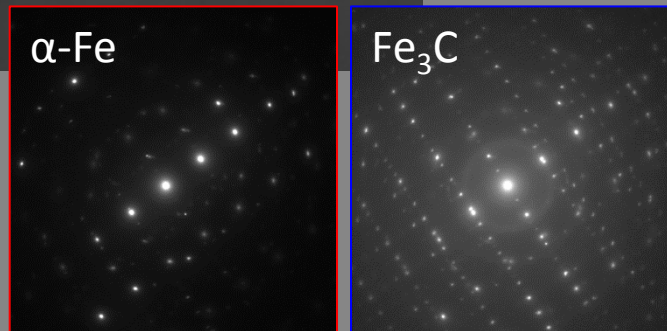
- Primarily BCC  $\alpha$ -Fe
- EDX and nanobeam diffraction show presence of Mn-rich  $\text{Fe}_3\text{C}$  lamellae
- As steel cools past the eutectic temperature from the FCC  $\gamma$ -Fe (austenite) phase, orthorhombic  $\text{Fe}_3\text{C}$  (cementite) and BCC  $\alpha$ -Fe (ferrite) grow, starting at a prior austenite grain boundary



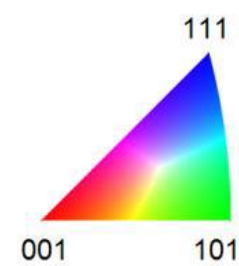
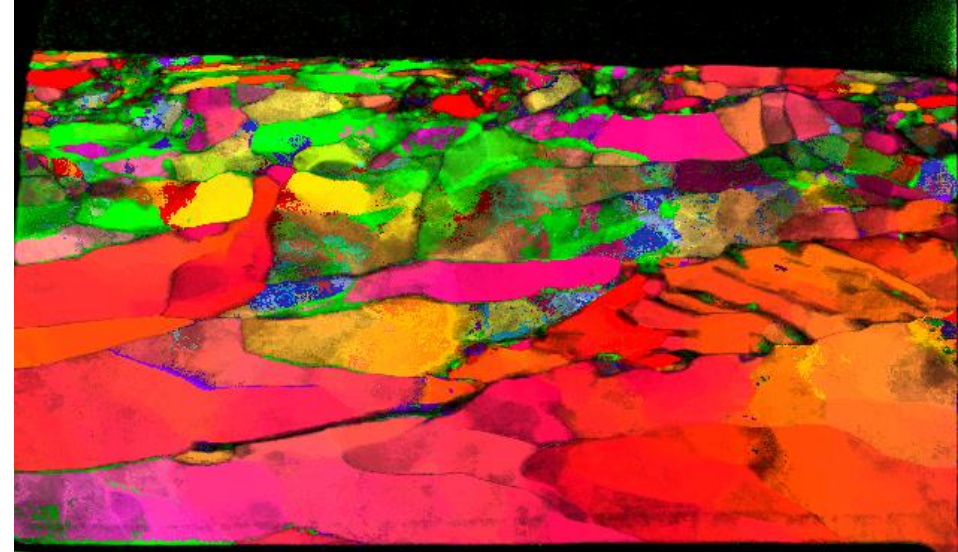
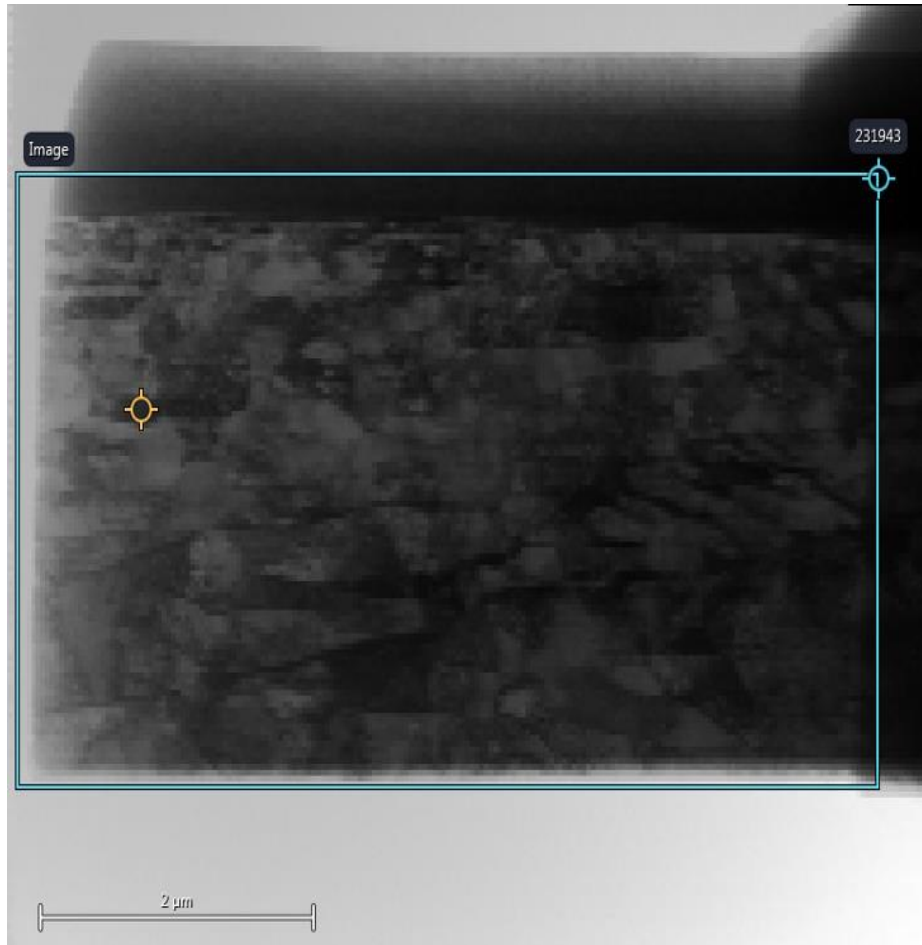
EDX



Nanobeam Diffraction



# Grain Orientation Mapping of BCC Ferrite



10 nm step size across thinned sample region,  
only thin region is placed on SiN membrane window



# Low-Carbon Steel in 0.27 ppm CO<sub>2</sub>: Microstructural Evolution Overview

Dry, 0 min in liquid

10 min in liquid, solution flow start

↑ Flow Direction  
(6 μM CO<sub>2</sub>)

99 min in liquid, 89 min flow time

Dry, after 1047 min in liquid, 900 min flow time

2 μm

- Overall thinning
- Black arrow
  - Edge corrosion
- White arrow
  - Internal grain preferential etching
- White box
  - Preferential  $\alpha$ -Fe etching (over Fe<sub>3</sub>C)

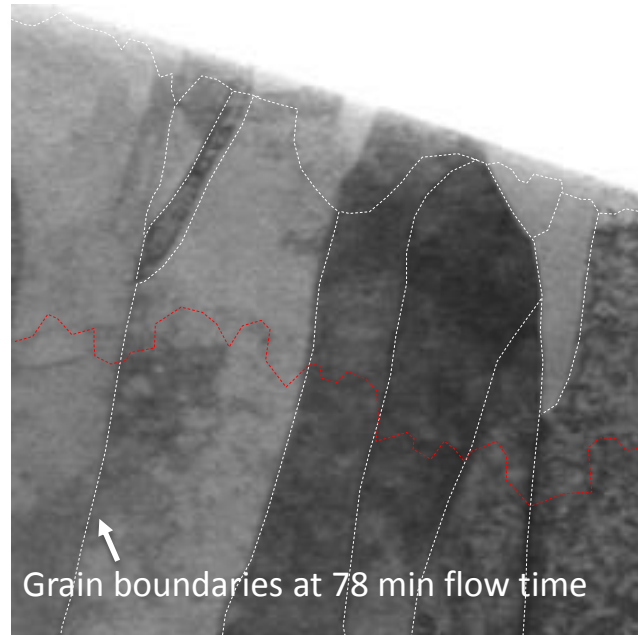


Flow Direction ↑

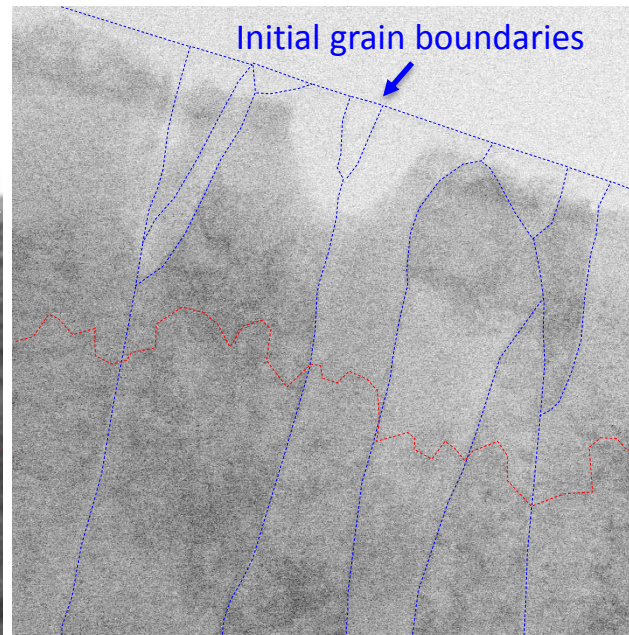


# Edge Corrosion of Steel in 0.27 ppm CO<sub>2</sub>

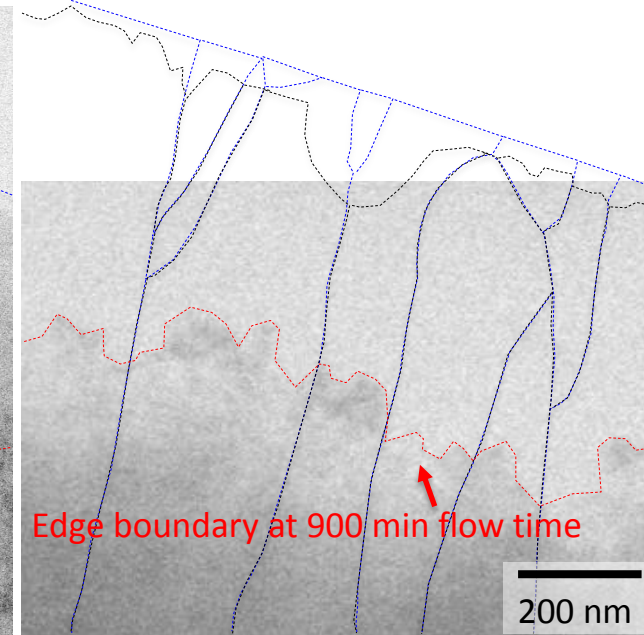
Dry, 0 min in liquid



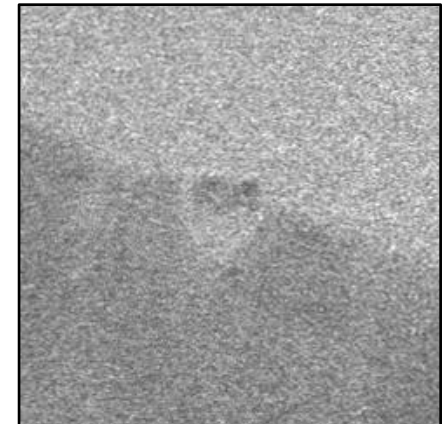
88 min in liquid,  
78 min flow time



Dry, after 1047 min in liquid, 900  
min flow time

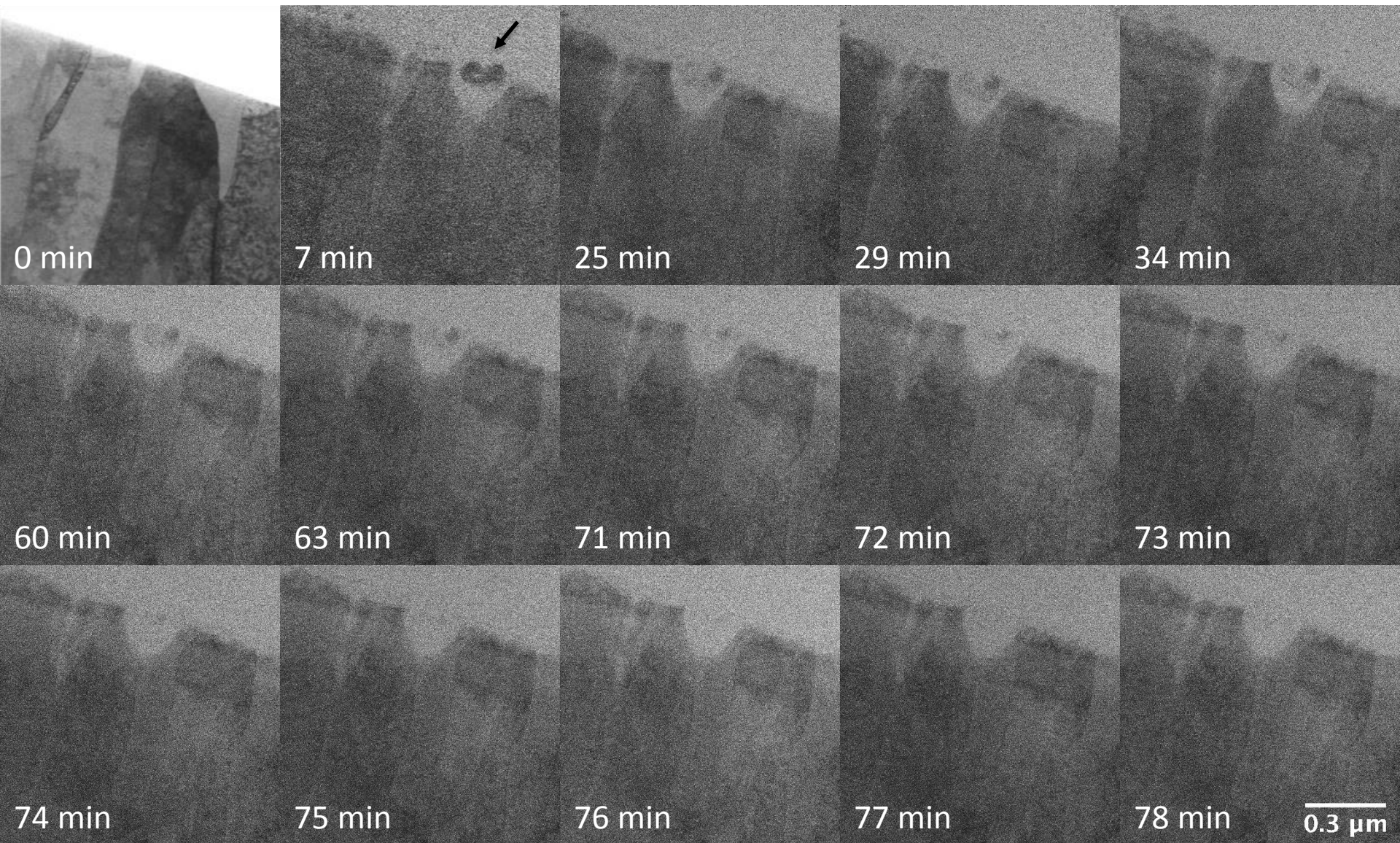


- Initial preferential etching in some areas
- Overall slight etching preference at grain boundaries
- Eventual non-selective etching

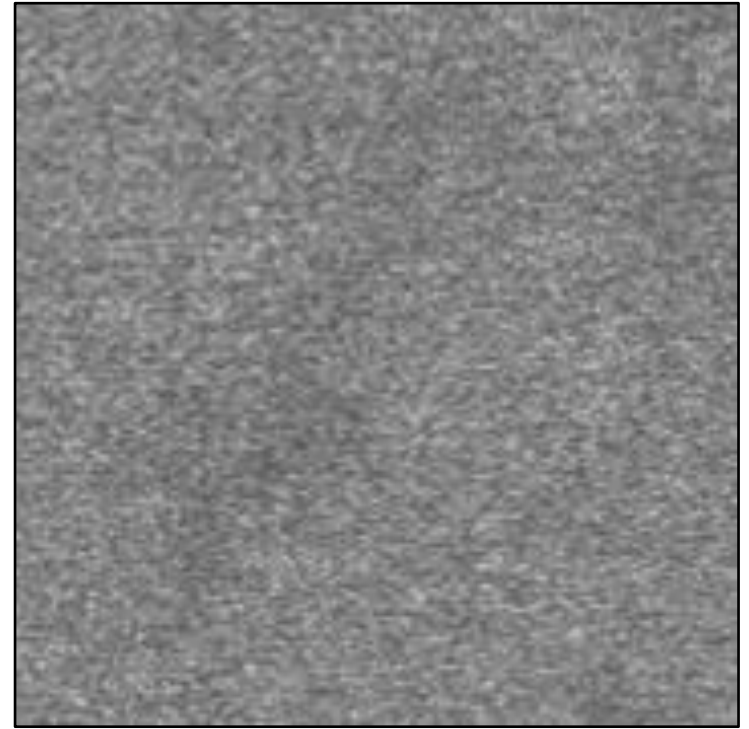
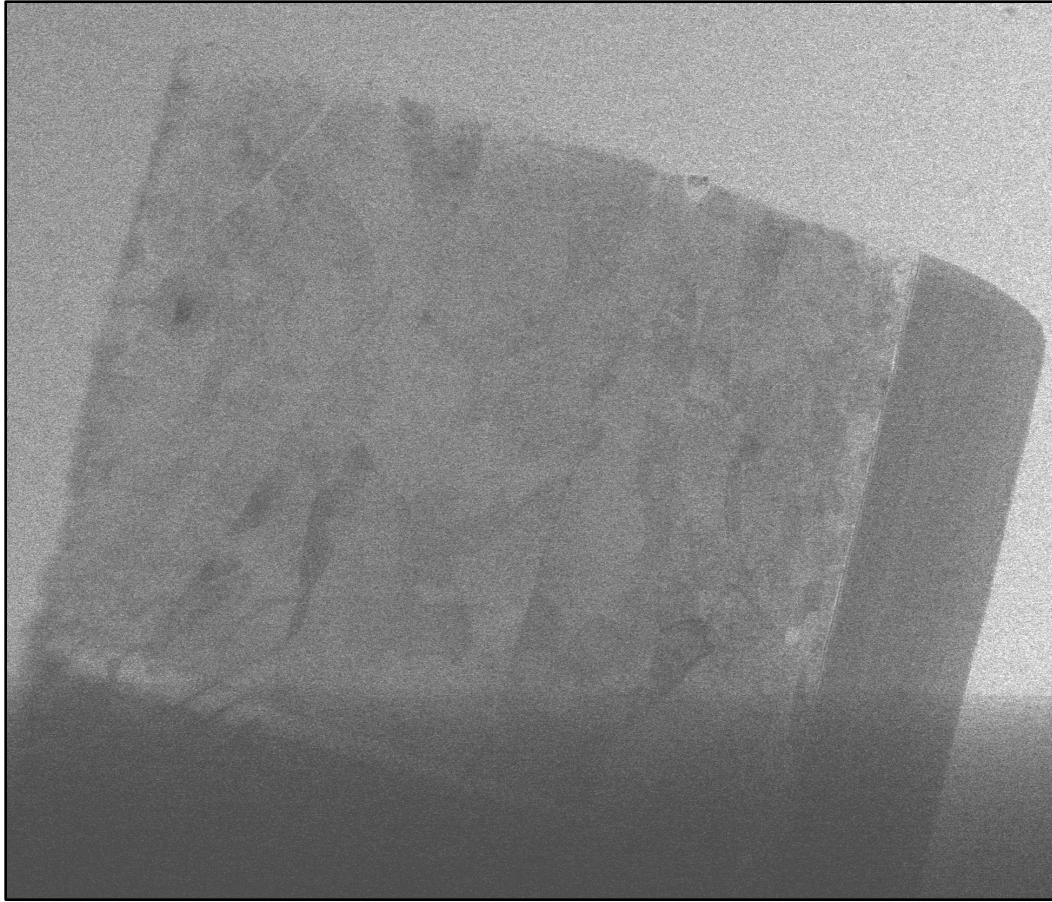




# Edge Corrosion of Steel in 0.27 ppm CO<sub>2</sub>

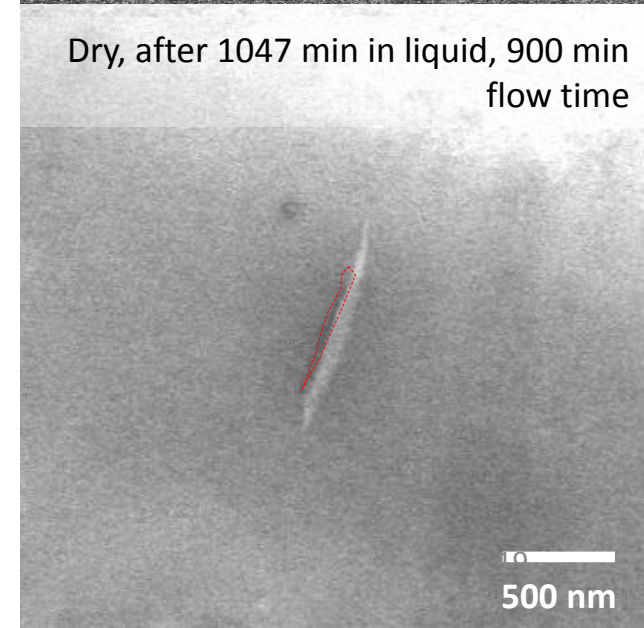
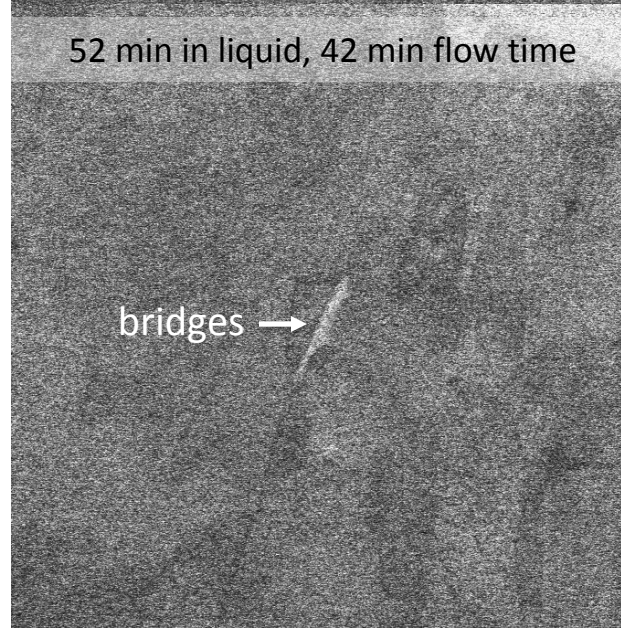
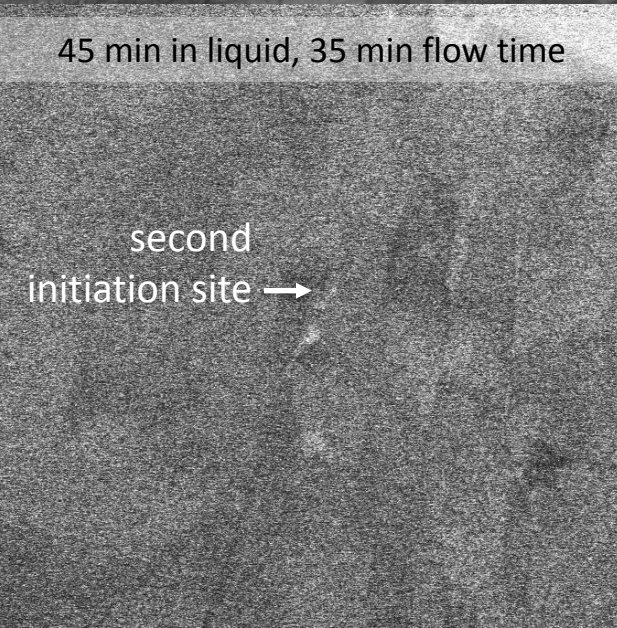
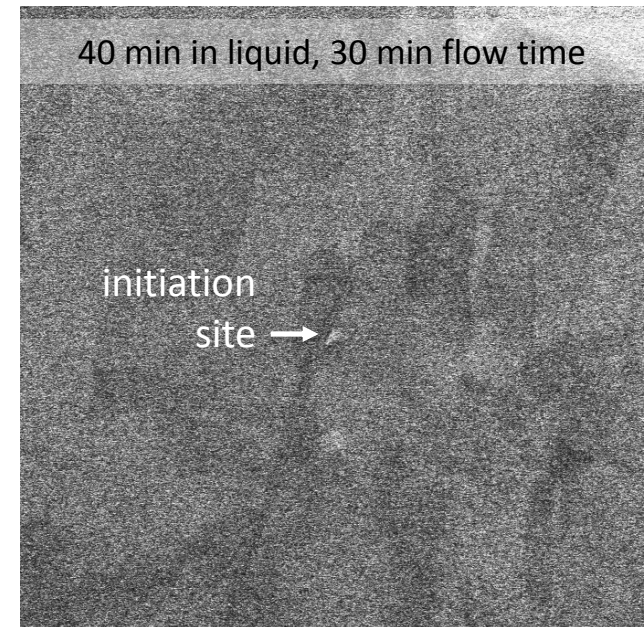
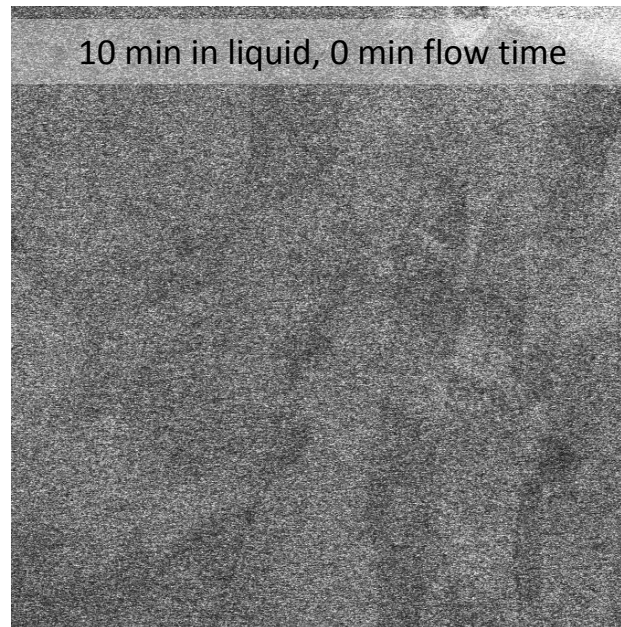
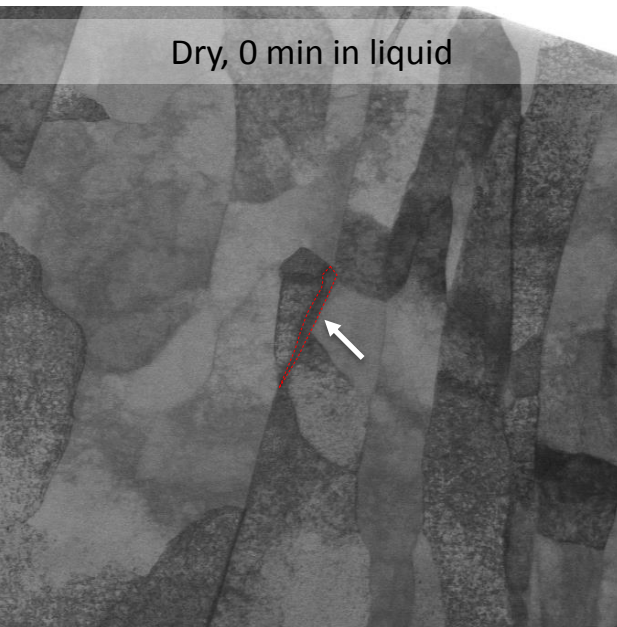


# Internal GB Etching of Steel in 0.27 ppm CO<sub>2</sub>





# Internal GB Etching of Steel in 0.27 ppm CO<sub>2</sub>





# Preferential $\alpha$ -Fe Etching of Steel in 0.27 ppm $\text{CO}_2$

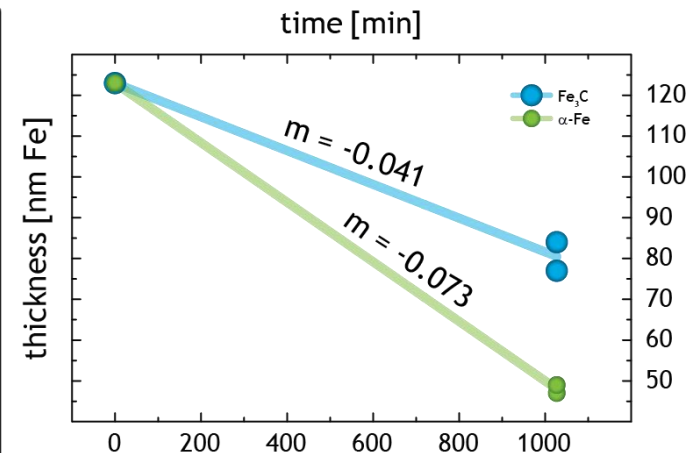
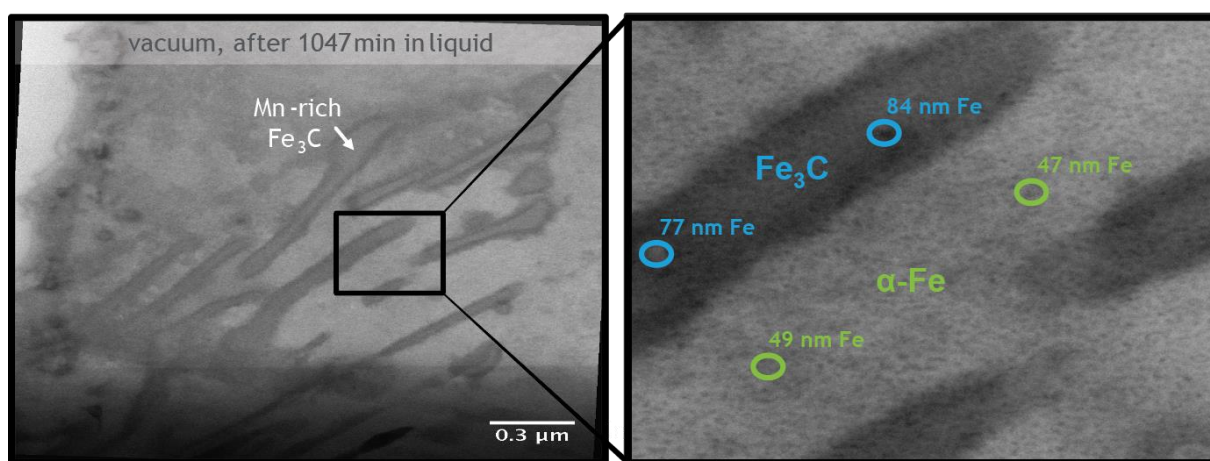
## EELS Thickness Measurements After Experiment

$\text{Si}_3\text{N}_4$  window = 0.38 IMFP ( $\sim 49$  nm)

Initial sample thickness = 1.61 IMFP ( $\sim 123$  nm Fe)

1. 1.16 IMFP ( $\sim 77$  nm Fe)
2. 0.87 IMFP ( $\sim 49$  nm Fe)
3. 1.22 IMFP ( $\sim 84$  nm Fe)
4. 0.86 IMFP ( $\sim 47$  nm Fe)

$\text{Fe}_3\text{C}/\alpha\text{-Fe}$  thickness ratio=1.67





# Galvanic Coupling in Low-Carbon Steel

Ferrite and cementite phases in contact with electrolyte solution will experience charge transfer from the ferrite to the cementite, causing dissolution of the Fe ions in the ferrite grains

- Larger grain size of cementite will result in faster etching of ferrite grain

## **GALVANIC SERIES**

Galvanic Series in Seawater (supplements Farag Table 3.1, page 65), EIT Review Manual, page 38-2  
*Tendency to be protected from corrosion, cathodic, more noble end*

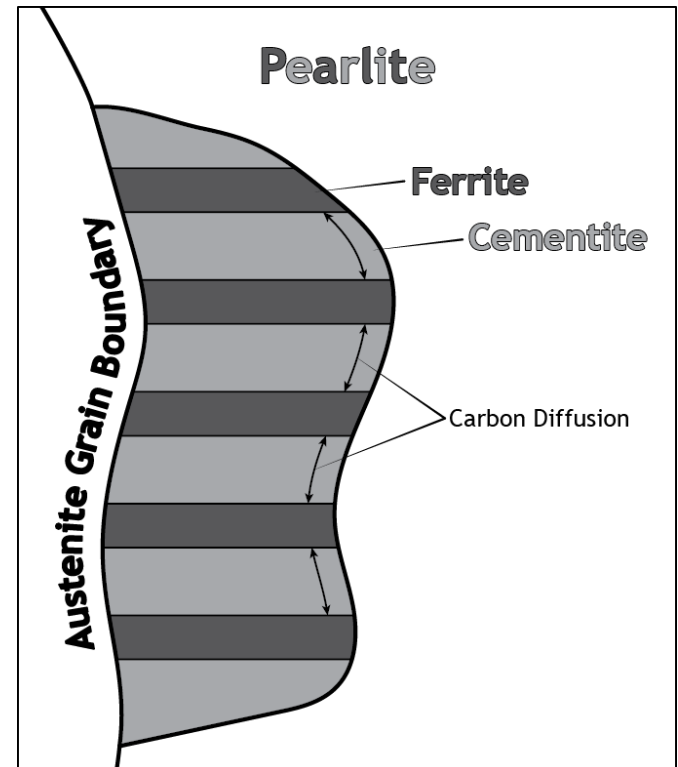
Mercury  
Platinum  
Gold  
Zirconium Graphite  
Titanium  
Hastelloy C Monel  
Stainless Steel (316-passive)  
Stainless Steel (304-passive)  
Stainless Steel (400-passive)  
Nickel (passive oxide)  
Silver  
Hastelloy 62Ni, 17Cr  
Silver solder  
Inconel 61Ni, 17Cr  
Aluminum (passive  $Al_2O_3$ )  
70/30 copper-nickel  
90/10 copper-nickel  
Bronze (copper/tin)  
Copper  
Brass (copper/zinc)  
Alum Bronze Admiralty Brass  
Nickel  
Naval Brass Tin  
Lead-tin  
Lead  
Hastelloy A  
Stainless Steel (active)  
316 404 430 410  
Lead Tin Solder  
Cast iron  
Low-carbon steel (mild steel)  
Manganese Uranium  
Aluminum Alloys  
Cadmium  
Aluminum Zinc  
Beryllium  
Magnesium



**PASSIVE – will not corrode – act as cathode. These elements are least likely to give up electrons!**



**ACTIVE – will corrode – act as anode. These elements most likely to give up electrons!**



10-20 mV between ferrite and cementite

# Pipeline Steel Corrosion: Sour Corrosion H<sub>2</sub>S & CO<sub>2</sub>

Type of corrosion product controls the corrosion rate

Temperature and partial pressure of H<sub>2</sub>S affect the deposition mechanism of film

Polymorphous FeS Corrosion products.

Name	Chemical formula	Crystal structure	Properties
Amorphous	FeS	No specific crystal	Unstable, converts into mackinawite quickly
Mackinawite	Fe <sub>1+x</sub> S (x= 0.02–0.41)	Tetragonal, two- dimensional layer	Metastable, the initial corrosion product
Cubic FeS	FeS	Cubic	Very unstable, can transform into mackinawite, troilite or pyrrhotite
Troilite	FeS	Hexagonal	Stoichiometric end member of the Fe <sub>1-x</sub> S group (x= 0)
Pyrrhotite	Fe <sub>1-x</sub> S (x= 0.05–0.21)	Monoclinic or hexagonal (main)	Thermodynamically stable
Pyrite	FeS <sub>2</sub>	Cubic	Thermodynamically stable

Kermani and Morshed, Cri. Rev. Corr. Sci. Eng. **59**, 659 (2003).

Corrosion doesn't occur on top of the scale film, but below it

Wax protective film: diffusion of CO<sub>2</sub> through wax layer

*Mechanisms of the Anodic Dissolution of Iron in CO<sub>2</sub>-Containing Media<sup>19-20</sup>*

Reaction No.	Reaction or Equilibrium	pH < 4	4<pH<5	pH> 5
1a	HCO <sub>3</sub> <sup>-</sup> ⇌ (HCO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup>	1a	1a	1b
1b	CO <sub>2</sub> + (OH <sup>-</sup> ) <sub>ads</sub> ⇌ (HCO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup>			
2	(HCO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup> ⇌ (HCO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup> + e <sup>-</sup>	⇌	⇌	RDS ⇒
3	(HCO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup> ⇌ (HCO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup> + e <sup>-</sup>	⇌	RDS <sup>(A)</sup> ⇒	⇒
4	(HCO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup> + OH <sup>-</sup> ⇌ (CO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup> + H <sub>2</sub> O	RDS ⇒	⇒	⇒
5	Fe - (CO <sub>3</sub> ) <sub>ads</sub> <sup>-</sup> + H <sub>2</sub> O ⇒ Fe <sup>2+</sup> + HCO <sub>3</sub> <sup>-</sup> + OH <sup>-</sup>	⇒	⇒	⇒
1 → 5	Tafel slope (mV/log)	60/2 = 30	60/1.5=40	60/0.5= 120
1 → 5	H <sup>+</sup> reaction order	-2	-1	0
1 → 5	CO <sub>2</sub> reaction order	1	1	1

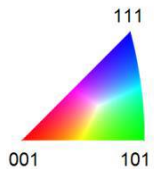
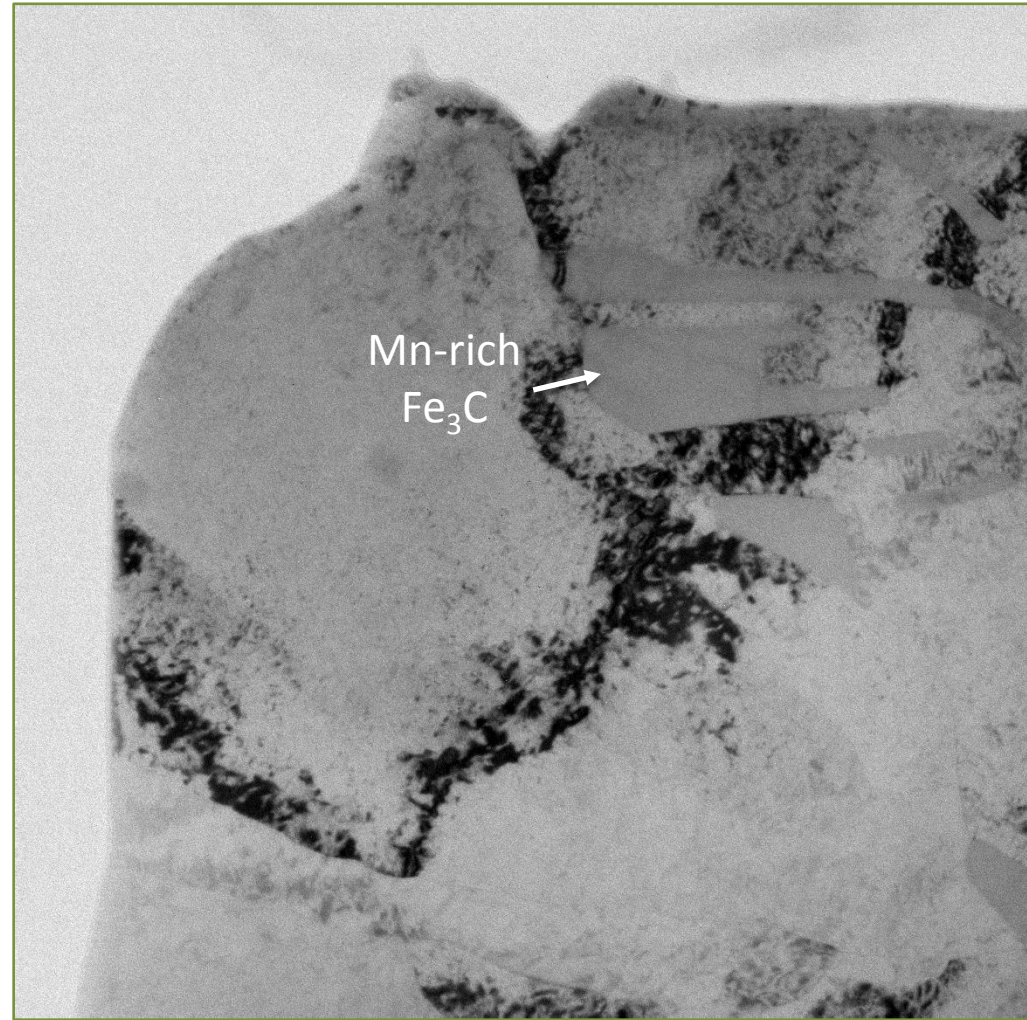
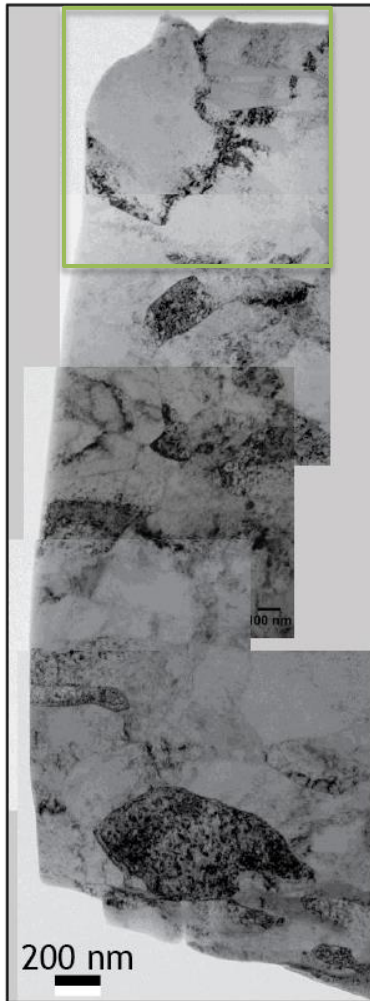
<sup>(A)</sup> RDS = rate-determining step.

Shi et al., Corr. Sci. **102**, 103 (2016).

\* H<sub>2</sub>S can either accelerate corrosion or reduce by providing a protective film on ferrite (small amounts of H<sub>2</sub>S)

\* Iron sulfide is more protective than FeCO<sub>3</sub>

# Grain Orientation Mapping of BCC Ferrite

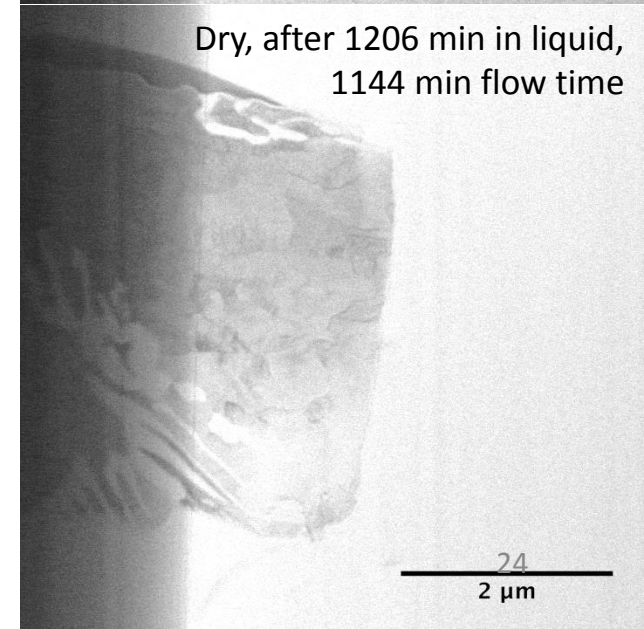
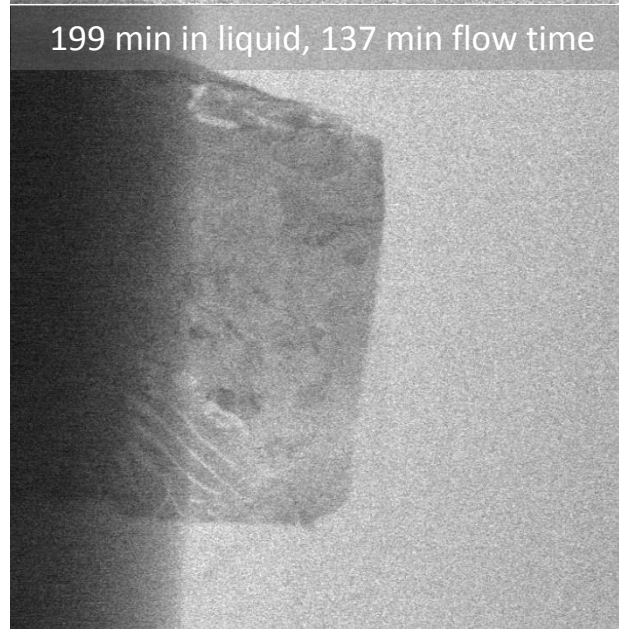
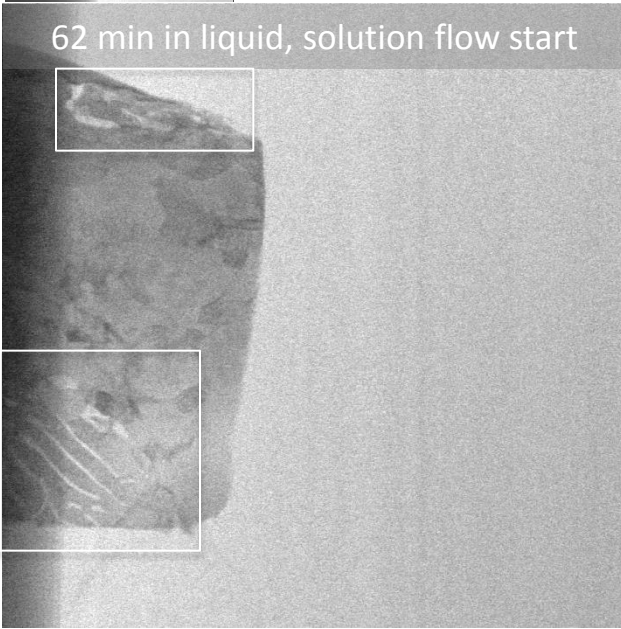
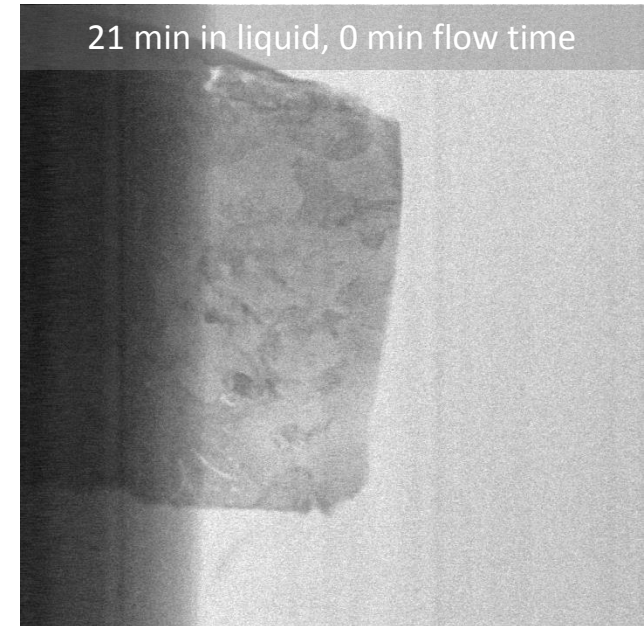
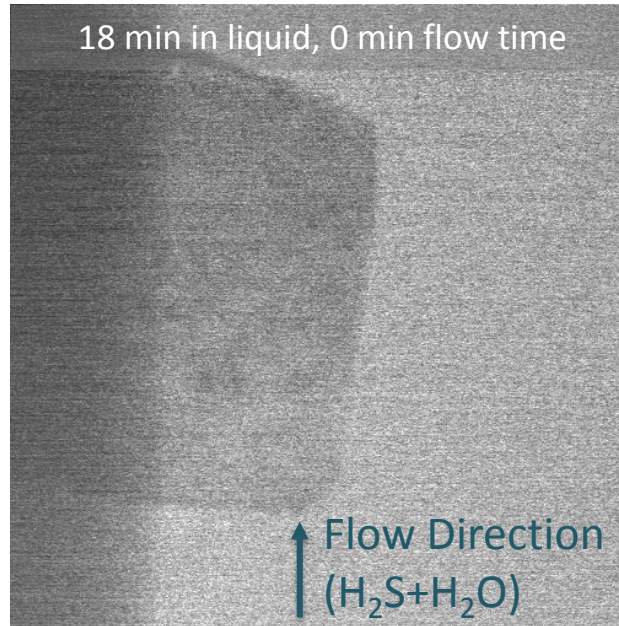
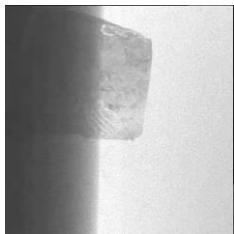


orientation  
map



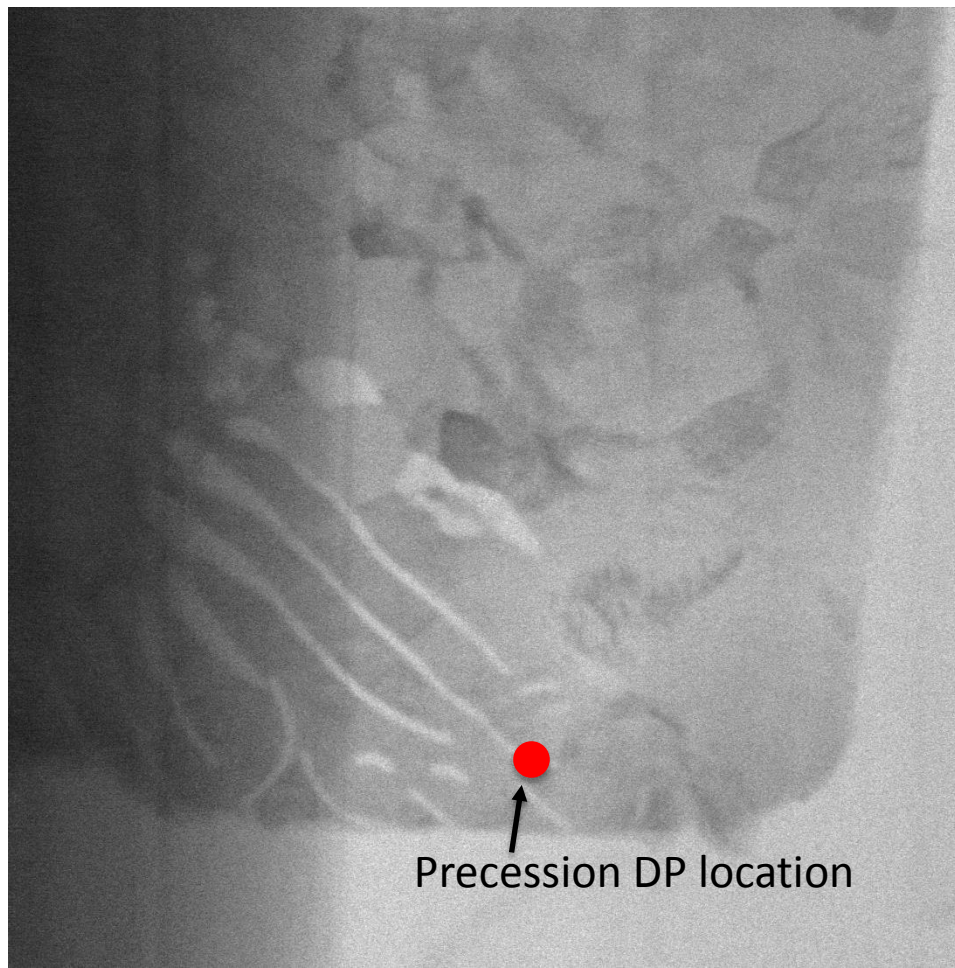
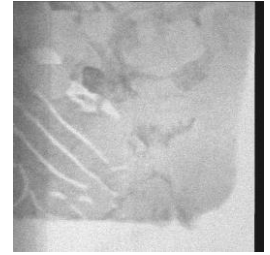
# Steel in 5 ppm $\text{H}_2\text{S}$ + 45 ppm $\text{CO}_2$ : Microstructural Evolution Overview

- Overall thinning
- White boxes
  - Preferential etching of  $\text{Fe}_3\text{C}$  (over  $\alpha\text{-Fe}$ )



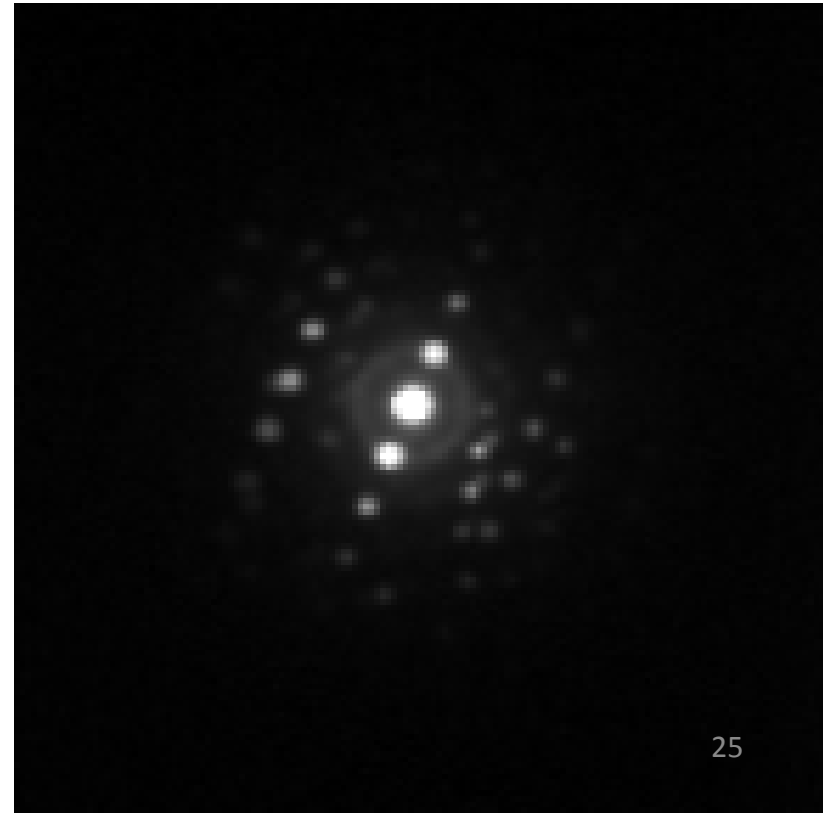
# Fe<sub>3</sub>C Preferential Etching in 5 ppm H<sub>2</sub>S + 45 ppm CO<sub>2</sub>

- Lamellar morphology indicates Fe<sub>3</sub>C
- Pre-experiment precession diffraction pattern acquired at lamella indicates Fe<sub>3</sub>C



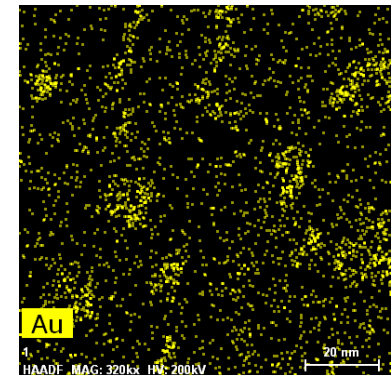
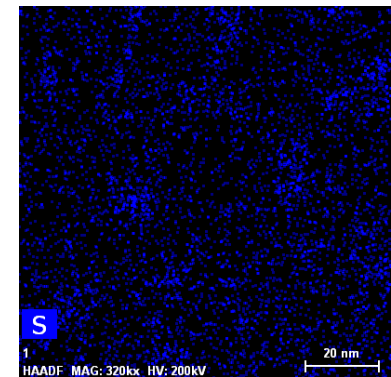
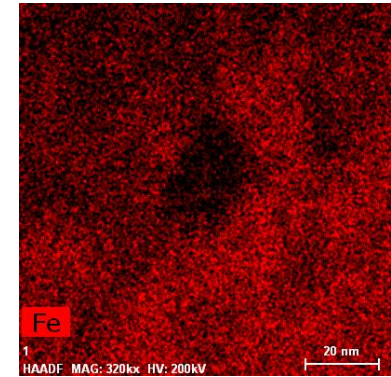
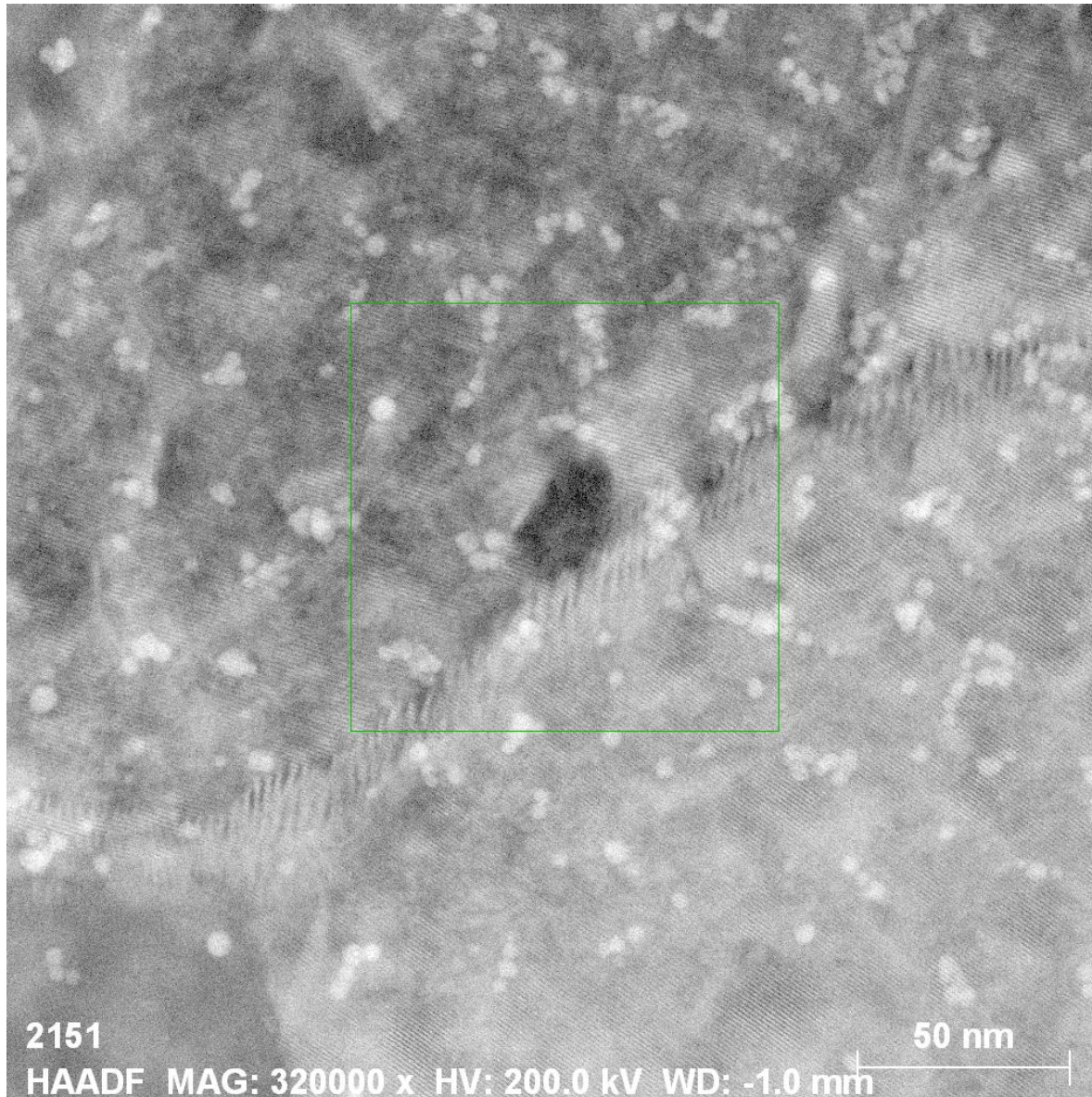
$\alpha$ -Fe [014] ZA

Fe<sub>3</sub>C [121] ZA

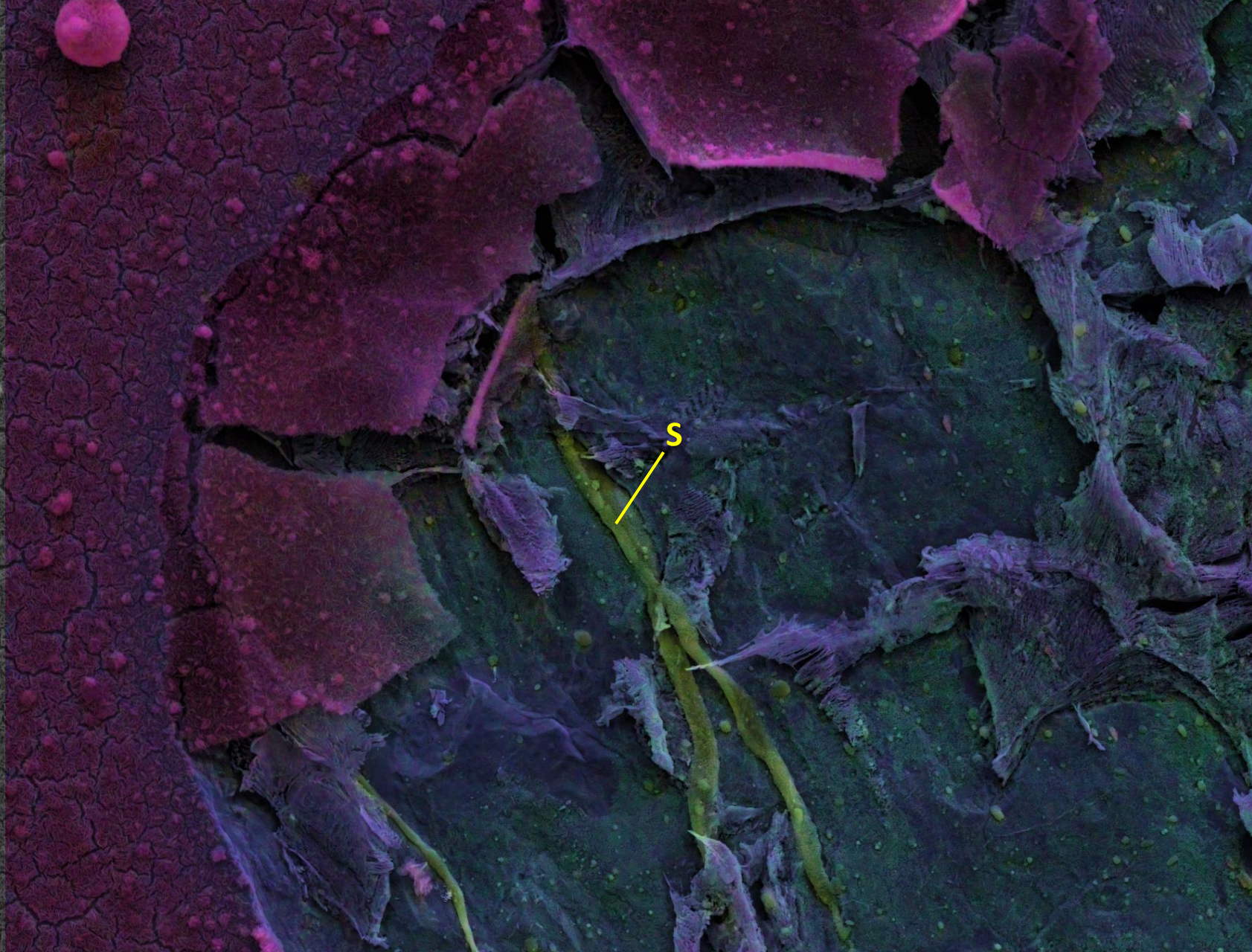




# Determination of Scale Products on Surface

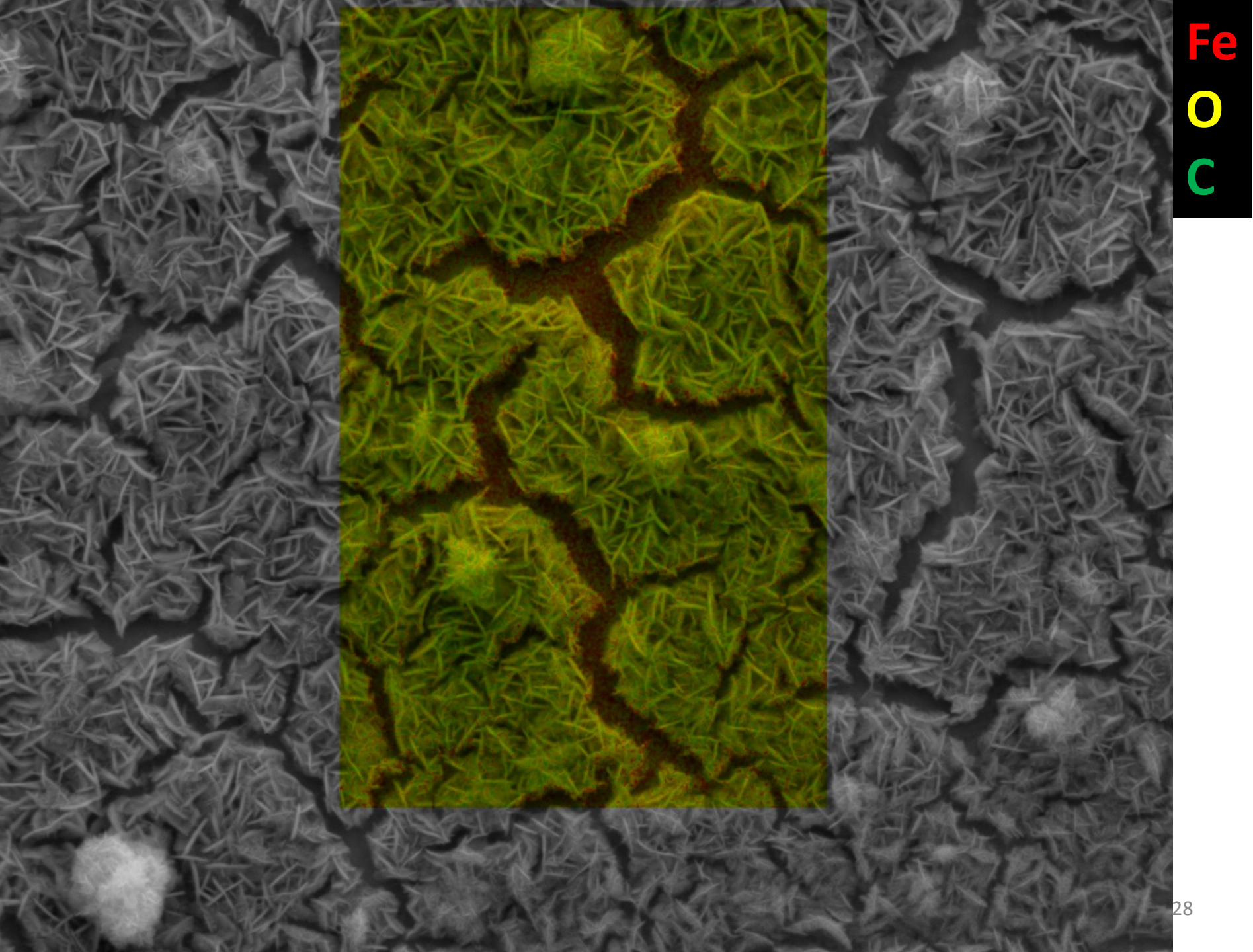






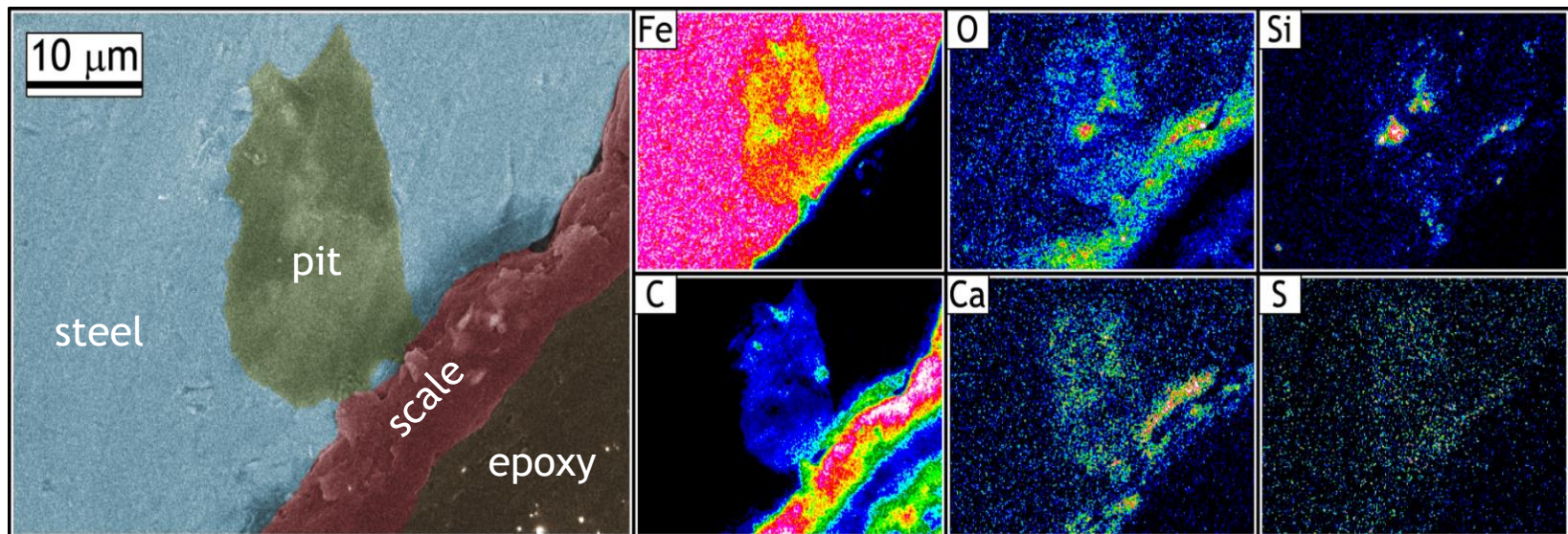
Fe  
O  
C  
S





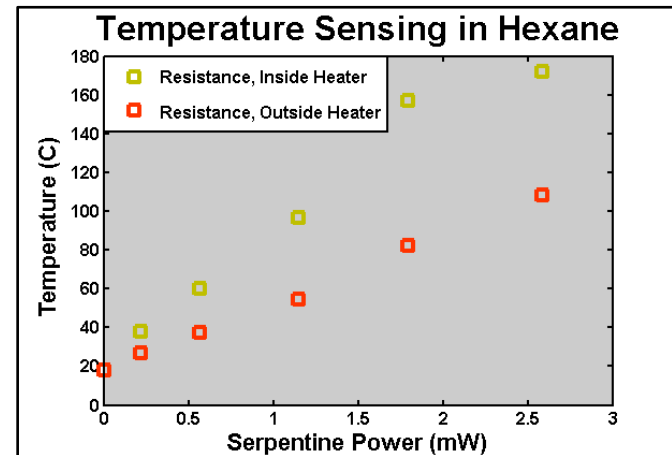
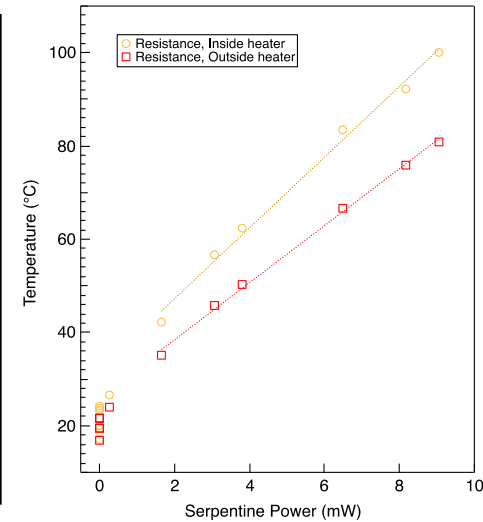
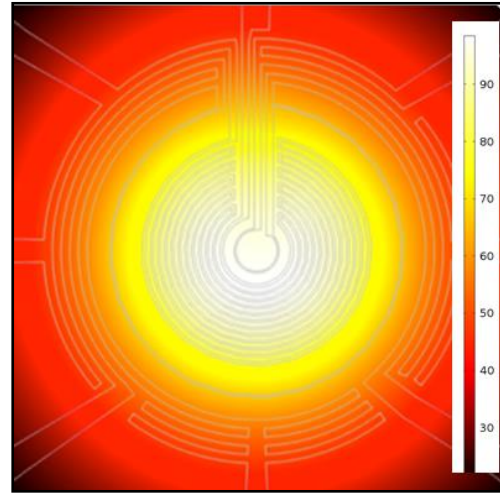
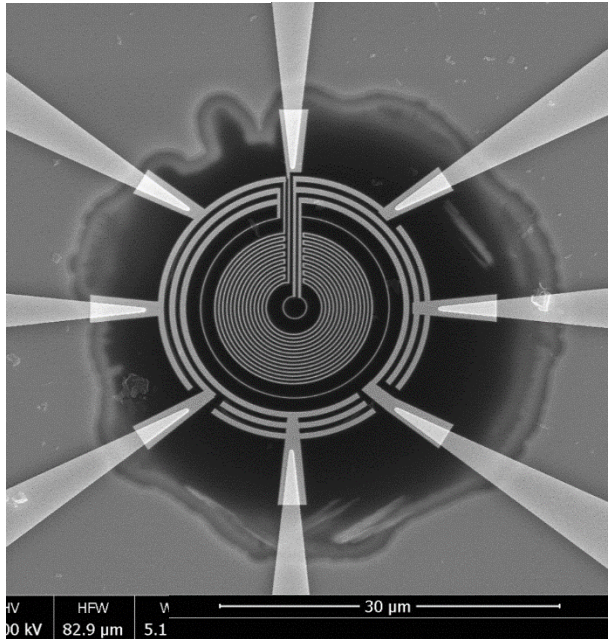
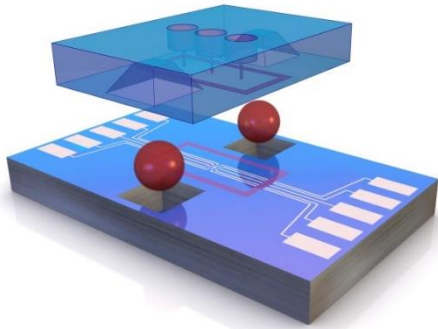
# Summary of Corrosion Initiation in Low-Carbon Steel

- Sweet: 0.27 ppm  $\text{CO}_2$  etches the low-carbon steel
  - Evidence of intergranular corrosion at  $\text{Fe}_3\text{C}/\alpha\text{-Fe}$  interface
  - Preferential etching of  $\alpha\text{-Fe}$  over  $\text{Fe}_3\text{C}$
- Sour: 5 ppm  $\text{H}_2\text{S}$  with 45 ppm  $\text{CO}_2$ 
  - $\text{Fe}_3\text{C}$  preferentially etches over  $\alpha\text{-Fe}$ 
    - Unlike the  $\text{CO}_2$  only solution





# Temperature Dependence of Corrosion



Liquid thickness plays a larger role in heating calibration than the liquid thermal conductivity, therefore measurement of the temperature changes on column is preferable

# Center for Integrated Nanotechnologies

**CINT Core Facility: Albuquerque, NM**



**CINT Gateway Facility: Los Alamos, NM**



***Department of Energy, Basic Energy Sciences national user facility to provide expertise and instrumentation free of charge to support accepted peer-reviewed nanoscience research***



**Sandia  
National  
Laboratories**

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Katie



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Steven



Tanya



Tim



Rachael



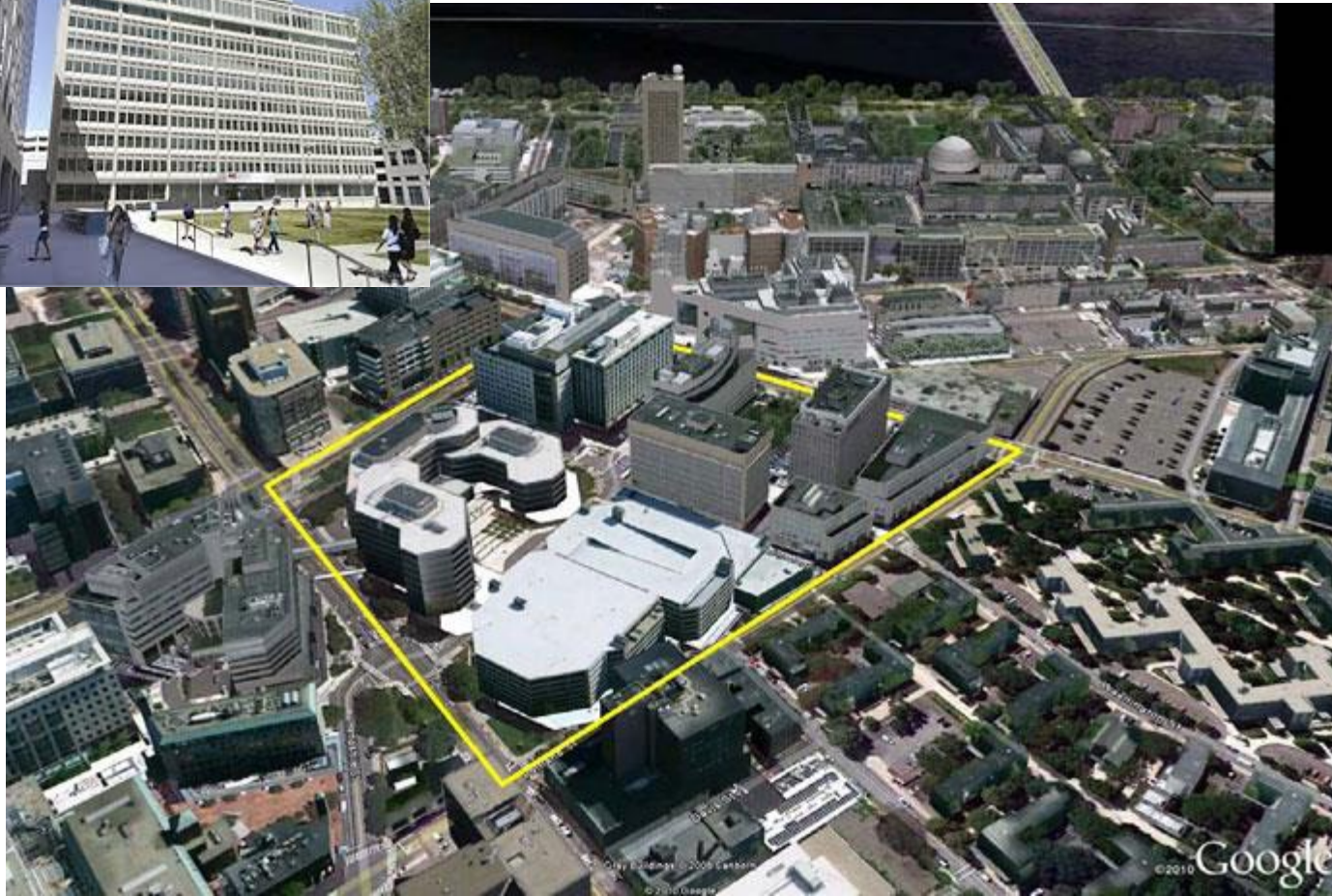
Michele



This work was performed, in part, at the Center for Integrated Nanotechnologies (CINT), a U.S. DOE Office of Basic Energy Sciences user facility. Sandia National Laboratories is a multiprogram laboratory managed and operated by Sandia Corporation, a wholly-owned subsidiary of Lockheed Martin Corporation, for the U.S. Department of Energy's National Nuclear Security Administration under contract DE-AC0494AL85000.



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